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(54) **Title:** PREPARATION OF SULFONATED POLYOXADIAZOLE POLYMERS

(57) **Abstract:** Described is the preparation of sulfonated polyoxadiazole polymers with a high degree of sulfonation and good flammability properties. The polymers are useful in articles such as fibers.

TITLE

PREPARATION OF SULFONATED POLYOXADIAZOLE POLYMERS

CROSS-REFERENCE TO RELATED APPLICATION

5 This application claims the benefit of priority of U.S. Provisional Application Nos. 61/423620, filed on Dec 16, 2010, the entirety of which is herein incorporated by reference.

FIELD OF THE INVENTION

10 The invention is directed to methods of preparing sulfonated polyoxadiazole polymers.

BACKGROUND

15 Workers that can be exposed to flames, high temperatures, and/or electrical arcs and the like, need protective clothing and articles made from thermally resistant fabrics. Any increase in the effectiveness of these protective articles, or any increase in the comfort, durability, and dyeability of these articles while maintaining protection performance, is welcomed.

20 Polyoxadiazole polymers have unique properties and are useful in many fields, for example high performance fibers, such as flame retardant fibers. One method to improve flammability is to prepare sulfonated polyoxadiazole polymers. These methods have included the use of sulfonated monomers and post-sulfonation. Gomes et al. (US 2009/0318109, US2008/01 93652, US2009/0203870) reacted hydrazine sulfate and aromatic dicarboxylic acids in phosphoric acid to form mono-sulfonated polyoxadiazole copolymers, and subsequently post-sulfonated the polymer. Another method is the use of oleum during polymerization to sulfonate the polymer as it is prepared. Lee et al. (US 7,528,216 and US 7,582,721) prepared random polyoxadiazole copolymers by reacting
25 aromatic dicarboxylic acids with hydrazine sulfate in a limited amount of
30 oleum, and prepared sulfonated random polyoxadiazole copolymers using sulfonated monomers (US 7,528,217).

There is a need for an easy method to prepare polyoxadiazole polymers with a high degree of sulfonation that produce polymers with improved properties, such as flame retardancy and dyeability.

5

SUMMARY

One aspect of the invention is a process for preparing a polymer, comprising the steps of:

- a) combining hydrazine, oleum, 4,4'-oxybis(benzoic acid), and one or both of terephthalic acid and isophthalic acid, to form a reaction mixture, wherein the oleum is added in an amount of at least about 5 molar equivalents of SO_3 based on the number of moles of hydrazine; and
- b) heating the reaction mixture to a temperature of about 100°C to about 180°C until a polymer is prepared.

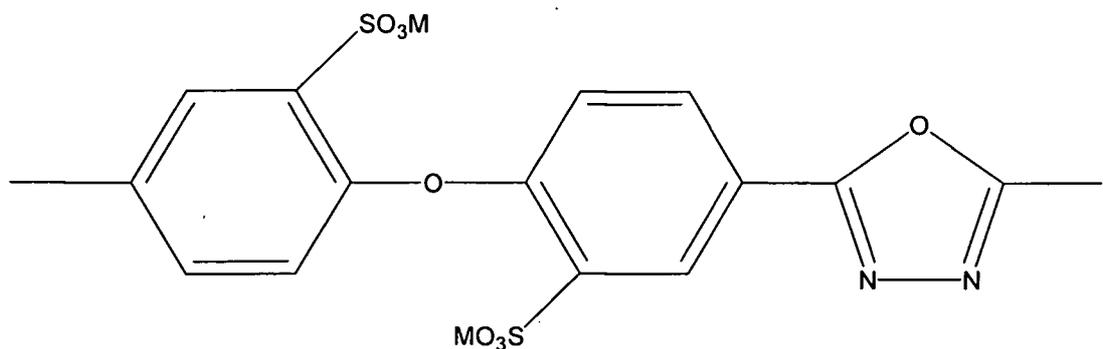
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The polymer can be a sulfonated copolyoxadiazole polymer.

DETAILED DESCRIPTION

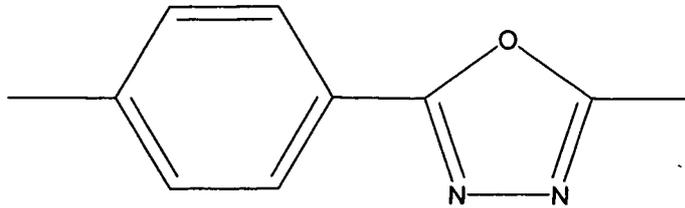
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Disclosed is a polymer comprising repeat units of Formula (I) and one or both of Formula (II) and (Ha):



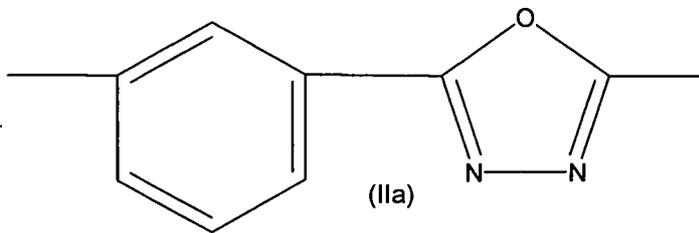
(I)

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(II)

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(IIa)

wherein M is a cation.

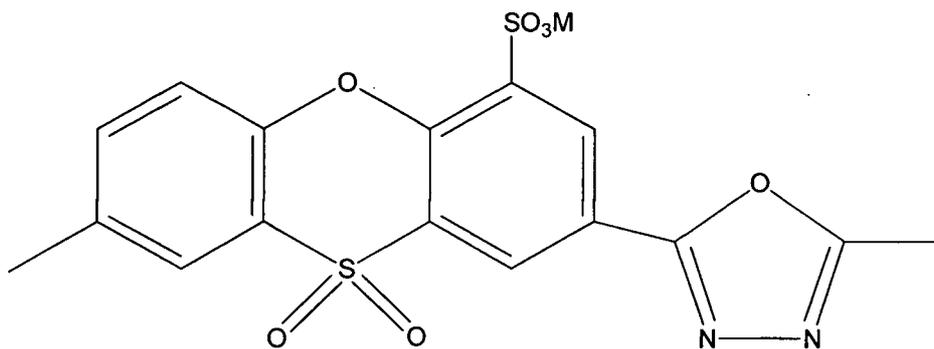
10 M is typically a monovalent cation such as H, Li, Na, K, or NH_4 . In one embodiment Formula (I) is present at about 5 molar % to about 50 molar %, or about 5 molar % to about 40 molar %, or about 10 molar % to about 30 molar %, and one or both of Formula (II) and (IIa) is present at about 50 molar % to about 95 molar %, or about 60 molar % to about 95
15 molar %, or about 70 molar % to about 90 molar %. In another embodiment Formula (II) is used in about 60 to about 95 molar %, or about 70 to about 90 molar %; and Formula (IIa) is used in about 0 to about 30 molar %, or about 0 to about 20 molar %. In another embodiment, Formula (II) is not present or Formula (IIa) is not present.

20 M can be converted to another M at any time, either before or after spinning or formation into a shaped article. When M is H, the polymer can be neutralized by contact with a salt, such as but not limited to sodium bicarbonate, sodium hydroxide, cesium hydroxide, lithium hydroxide,

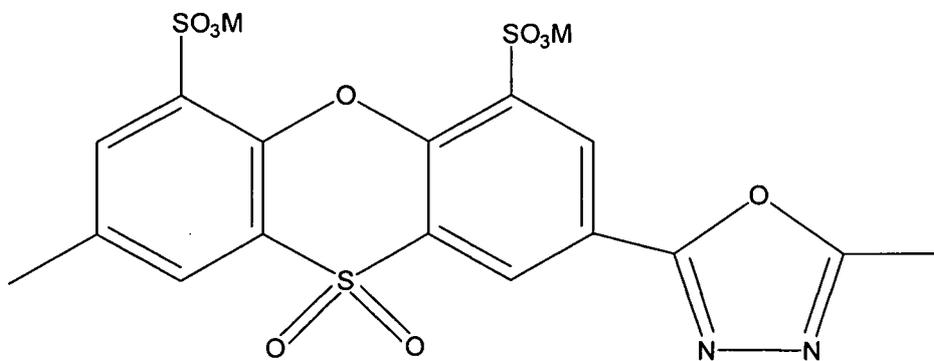
potassium hydroxide, or potassium carbonate. The ion exchange and/or neutralization can be performed by any method known in the art.

The polymer can further comprise repeat units of other moieties in the polymer chain. These repeat units can comprise one or both of

5 Formula (III) and Formula (IIa):



(III)



(IIa)

10

This embodiment is characterized by its ring-closed structure. In one embodiment, Formula (I) is present at about 5 molar % to about 50 molar %, or about 5 molar % to about 40 molar %, or about 10 molar % to about 30 molar %, and one or both of Formula (II) and (IIa) is present at

15 about 50 molar % to about 95 molar %, or about 60 molar % to about 95 molar %, or about 70 molar % to about 90 molar %, and one or both of

Formula (III) and Formula (IIa) is present at about 1 molar % to about 50 molar % or about 5 molar % to about 30 molar %, or about 5 molar % to about 20 molar %. In another embodiment, Formula (IIa) is present at less than about 5 %. In another embodiment, Formula (II) is not present or
5 Formula (IIa) is not present.

The polymers disclosed can have at least about 2 weight %, 4 weight %, or 6 weight % sulfur content. The amount of sulfur can be increased by sulfonation of the monomers before polymerization, or sulfonation of the polymer.

10 The polymers disclosed herein can be made by any method or process known in the art. One suitable method comprises the steps of:
a. combining hydrazine, oleum, 4,4'-oxybis(benzoic acid), and one or both of terephthalic acid and isophthalic acid, to form a reaction mixture, wherein the oleum is added in an amount of at
15 least about 5 molar equivalents of SO_3 based on the number of moles of hydrazine; and
b. heating the reaction mixture to a temperature of about 100°C to about 180°C until a sulfonated copolyoxadiazole polymer is prepared.

20 Other monomers may also be present in the reaction mixture.

The process described herein can prepare sulfonated polyoxadiazole copolymers that comprise at least about 2 weight %, 4 weight %, or 6 weight % sulfur content. The amount of sulfur can be increased by additional process steps in which the 4,4'-oxybis(benzoic
25 acid), or one or both of terephthalic acid and isophthalic acid are further sulfonated before polymerization, and/or process steps in which the polyoxadiazole copolymer product is sulfonated. This sulfonation can be performed by any method known in the art that is not detrimental to the final product, such as contact with oleum, sulfuric acid, or other sulfonation
30 agent.

Hydrazine can be used directly, or used in the form of a solid hydrazine salt. One suitable solid salt is hydrazine sulfate, $[\text{N}_2\text{H}_5]\text{HSO}_4$, also called hydrazinium sulfate.

Oleum, also known as fuming sulfuric acid, disulfuric acid or pyrosulfuric acid, refers to a solution of various compositions of sulfur trioxide (**SO₃**) in sulfuric acid. Typically 20-30% oleum is used, more typically 30%, which refers to the weight % of **SO₃** in the sulfuric acid. The
5 oleum is added in an amount of at least about 5 molar equivalents of **SO₃**, or more typically at least about 6 molar equivalents, based on the number of moles of hydrazine.

The amounts of the reagents used is dependent on the desired percentage of the repeat units in the final polymer. Based on the total
10 amount of dicarboxylic acids used, 4,4'-oxybis(benzoic acid) (OBBA) is used in amounts of at about 1 molar % to about 50 molar %, or about 5 molar % to about 50 molar %, or about 10 molar % to about 30 molar %, and one or both of terephthalic acid and isophthalic acid is used in amounts about 50 molar % to about 99 molar %, or about 50 molar % to
15 about 95 molar %, or about 70 molar % to about 90 molar %. In another embodiment terephthalic acid is used in about 50 to about 90 molar %, or about 70 to about 80 molar %; and isophthalic acid is used in about 0 to about 30 molar %, or about 0 to about 20 molar %. In another embodiment, terephthalic acid is not present or isophthalic acid is not
20 present. Various ratios of hydrazine can be could be used, but is typically used at about a 1:1 molar ratio of dicarboxylic acids : hydrazine.

The ingredients can be combined in any order, but typically the solid ingredients are first thoroughly mixed together and then combined with the oleum. In one embodiment, the oleum is added in a single step;
25 that is, added in one aliquot. In another embodiment, the oleum and OBBA can be mixed together prior to the addition of the other dicarboxylic acids and hydrazine. The mixture is then thoroughly mixed by stirring or other agitation means until sufficiently dissolved, typically at least five minutes. This dissolution can be performed at room temperature up to about 100
30 °C.

In one embodiment, the process comprises the steps of:

a1) combining hydrazine or salt thereof, 4,4'-oxybis(benzoic acid), and one or both of terephthalic acid and isophthalic acid to form a pre-mixture;

a2) stirring the pre-mixture for at least 5 minutes; and

5 a3) adding oleum to the pre-mixture in an amount of at least about 5 molar equivalents of SO₃ based on the number of moles of hydrazine to form a reaction mixture.

After dissolution, the mixture is allowed to react until sufficient polymer has formed. Typically the polymerization reaction is performed at
10 a temperature of about 100 °C to about 180 °C, or about 120 °C to about 140 °C, for at least about 0.5 hours. The temperature can be maintained or increased or ramped up during the reaction. The temperature can be used to control the amounts of sulfonation and type of sulfonated
repeating units in the final polymer. For instance, if more sulfonation
15 and/or ring-closed repeating units are desired then the temperature should be increased, typically to greater than about 120 °C. If less sulfonation and/or ring-closed repeating units are desired then the temperature should be lower, typically less than about 100 °C.

Also disclosed is a sulfonated copolyoxadiazole polymer prepared
20 by the process described herein, and shaped articles and fibers made therefrom.

The polymers described herein can be formed into a shaped article, such as films, fibrils, fibers for floe, and fibers for textile uses. It can be spun into fibers via solution spinning, using a solution of the polymer in
25 either the polymerization solvent or another solvent for the polymer. Fiber spinning can be accomplished through a multi-hole spinneret by dry spinning, wet spinning, or dry-jet wet spinning (also known as air-gap spinning) to create a multi-filament yarn or tow as is known in the art.

Shaped articles as described herein include extruded or blown
30 shapes or films, molded articles, and the like. Films can be made by any known technique such as casting the dope onto a flat surface, extruding the dope through an extruder to form a film or extruding and blowing the dope film to form an extruded blown film. Typical techniques for dope film

extrusion include processes similar to those used for fibers, where the solution passes through a spinneret or die into an air gap and subsequently into a coagulant bath. More details describing the extrusion and orientation of a dope film can be found in Pierini et al. (U. S. Pat. No. 5,367,042); Chenevey, (4,898,924); Harvey et al., (4,939, 235); and Harvey et al., (4,963,428). Typically the dope film prepared is preferably no more than about 250 mils (6.35 mm) thick and more preferably it is at most about 100 mils (2.54 mm) thick.

"Fiber" is defined as a relatively flexible, unit of matter having a high ratio of length to width across its cross-sectional area perpendicular to its length. Herein, the term "fiber" is used interchangeably with the term "filament" or "end" or "continuous filament". The cross section of the filaments described herein can be any shape, such as circular or bean shaped, but is typically generally round, and is typically substantially solid and not hollow. Fiber spun onto a bobbin in a package is referred to as continuous fiber. Fiber can be cut into short lengths called staple fiber. Fiber can be cut into even smaller lengths called floe. Yarns, multifilament yarns or tows comprise a plurality of fibers. Yarn can be intertwined and/or twisted.

"Floe" is defined as fibers having a length of 2 to 25 millimeters, preferably 3 to 7 millimeters and a diameter of 3 to 20 micrometers, preferably 5 to 14 micrometers. If the floe length is less than 3 millimeters, paper strength made from the floe is severely reduced, and if the floe length is more than 25 millimeters, it is difficult to form a uniform paper web by a typical wet-laid method. If the floe diameter is less than 5 micrometers, it can be difficult to commercially produce with adequate uniformity and reproducibility, and if the floe diameter is more than 20 micrometers, it is difficult to form uniform paper of light to medium basis weights. Floe is generally made by cutting continuous spun filaments into specific-length pieces.

The term "fibrids" as used herein, means a very finely-divided polymer product of small, filmy, essentially two-dimensional, particles known having a length and width on the order of 100 to 1000 micrometers

and a thickness only on the order of 0.1 to 1 micrometer. Fibrids are made by streaming a polymer solution into a coagulating bath of liquid that is immiscible with the solvent of the solution. The stream of polymer solution is subjected to strenuous shearing forces and turbulence as the polymer is
5 coagulated.

Fibrids and floe prepared from the polymers described herein can be used to form a paper, especially a thermally stable paper or paper that can accept ink or color more readily than other high performance papers. As employed herein the term paper is employed in its normal meaning and
10 it can be prepared using conventional paper-making processes and equipment and processes. The fibrous material, i.e. fibrids and floe can be slurried together to form a mix which is converted to paper such as on a Fourdrinier machine or by hand on a handsheet mold containing a forming screen. Reference may be made to Gross USP 3,756,908 and Hesler et
15 al. USP 5,026, 456 for processes of forming fibers into papers. If desired, once the paper is formed it is calendered between two heated calendering rolls with the high temperature and pressure from the rolls increasing the bond strength of the paper. Calendering also provides the paper with a smooth surface for printing. Several plies with the same or different
20 compositions can be combined together into the final paper structure during forming and/or calendering. In one embodiment, the paper has a weight ratio of fibrids to floe in the paper composition of from 95:5 to 10:90. In one preferred embodiment, the paper has a weight ratio of fibrids to floe in the paper composition of from 60:40 to 10:90.

25 The paper is useful as printable material for high temperature tags, labels, and security papers. The paper can also be used as a component in materials such as printed wiring boards; or where dielectric properties are useful, such as electrical insulating material for use in motors, transformers and other power equipment. In these applications, the paper
30 can be used by itself or in laminate structures either with or without impregnating resins, as desired. In another embodiment, the paper is used as an electrical insulative wrapping for wires and conductors. The wire or conductor can be totally wrapped, such a spiral overlapping wrapping of

the wire or conductor, or can wrap only a part or one or more sides of the conductor as in the case of square conductors. The amount of wrapping is dictated by the application and if desired multiple layers of the paper can be used in the wrapping. In another embodiment, the paper can also be used as a component in structural materials such as core structures or honeycombs. For example, one or more layers of the paper may be used as the primarily material for forming the cells of a honeycomb structure. Alternatively, one or more layers of the paper may be used in the sheets for covering or facing the honeycomb cells or other core materials.

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10 Preferably, these papers and/or structures are impregnated with a resin such as a phenolic, epoxy, polyimide or other resin. However, in some instances the paper may be useful without any resin impregnation.

Fibers may be spun from solution using any number of processes, however, wet spinning and air-gap spinning are the best known. In wet spinning, the spinneret extrudes the fiber directly into the liquid of a coagulation bath and typically the spinneret is immersed or positioned beneath the surface of the coagulation bath. In air-gap spinning (also sometimes known as "dry-jet" wet spinning) the spinneret extrudes the fiber first into a gas, such as air, for a very short duration and then the fiber is immediately introduced into a liquid coagulation bath. Typically the spinneret is positioned above the surface of the coagulation bath, creating an "air-gap" between the spinneret face and the surface of the coagulation bath. The general arrangement of the spinnerets and baths is well known in the art, with the figures in U.S. Patent Nos. 3,227,793; 3,414,645; 3,767,756; and 5,667,743 being illustrative of such spinning processes for high strength polymers.

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"Dry spinning" means a process for making a filament by extruding a solution into a heated chamber having a gaseous atmosphere to remove the solvent, leaving a solid filament. The solution comprises a fiber-forming polymer in a solvent which is extruded in a continuous stream through one or more spinneret holes to orient the polymer molecules. This is distinct from "wet spinning" or "air-gap spinning" wherein the polymer solution is extruded into a liquid precipitating or coagulating medium to

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regenerate the polymer filaments. In other words, in dry spinning a gas is the primary solvent extraction medium, and in wet spinning a liquid is the primary solvent extraction medium. In dry spinning, after formation of solid filaments, the filaments can then be treated with a liquid to either cool the
5 filaments or wash the filaments to further extract remaining solvent.

The fibers in the multi-filament yarn, or tow, after spinning can then be treated to neutralize, wash, dry, or heat treat the fibers as needed using conventional technique to make stable and useful fibers. The fibers formed from the polymers described herein are useful in a variety of applications.
10 They are colorless, or colorless to white in color, although impurities can impart discoloration, and are particularly useful as flame retardant fibers as the polymers have a limiting oxygen index of about 24 or greater, or about 26 or greater, or about 28 or greater, or about 30 or greater.

In one embodiment, the fibers can be spun from sulfuric acid
15 solutions ranging in concentration from 5 to 25 wt % polymer using a spinneret with 5-50 holes having diameter of 0.003" or 0.008". The volumetric flow rate of spinning solution is typically 0.3-2 mL/min. The fiber is then extruded directly into a coagulation bath filled with a room temperature or elevated temperature or sub-ambient temperature solution
20 containing 0-70 wt. % sulfuric acid, saturated salt solutions, or basic aqueous solutions.

The number, size, shape, and configuration of the orifices can be varied to achieve the desired fiber product. The extruded dope is fed into a coagulation bath with or without prior passage through a noncoagulating
25 fluid layer. The noncoagulating fluid layer is generally air but can be any other inert gas or liquid which is a noncoagulant for the dope.

The fibers and/or film can contain common additives such as dyes, pigments, antioxidants, delusterants, antistatic agents, and U.V. stabilizers, added either to the spin solution, dope or to the coagulation
30 bath, or coated on the fiber during or after the spinning process.

The sulfonated polyoxadiazole copolymers prepared by the process disclosed above can be neutralized either before or after formation into a shaped article, so that the H cation is replaced by another cation, typically

a monovalent cation such as Li, Na, K, or NH₄. This is performed by contacting the sulfonated polyoxadiazole copolymer with a neutralization agent, typically a basic salt such as sodium bicarbonate or other ion exchange agent.

5 As used herein, the term "staple fibers" refers to fibers that are cut to a desired length or are stretch broken, or fibers that occur naturally with or are made having a low ratio of length to the width of the cross-sectional area perpendicular to that length when compared with filaments. Man
made staple fibers are cut or made to a length suitable for processing on
10 cotton, woolen, or worsted yarn spinning equipment. The staple fibers can have (a) substantially uniform length, (b) variable or random length, or (c) subsets of the staple fibers have substantially uniform length and the staple fibers in the other subsets have different lengths, with the staple fibers in the subsets mixed together forming a substantially uniform
15 distribution.

In some embodiments, suitable staple fibers have a length of about 0.25 centimeters (0.1 inches) to about 30 centimeters (12 inches). In some
embodiments, the length of a staple fiber is from about 1 cm (0.39 in) to about 20 cm (8 in). In some preferred embodiments the staple fibers made
20 by short staple processes have a staple fiber length of about 1 cm (0.39 in) to about 6 cm (2.4 in).

The staple fibers can be made by any process. For example, the staple fibers can be cut from continuous straight fibers using a rotary
cutter or a guillotine cutter resulting in straight (i.e., non crimped) staple
25 fiber, or additionally cut from crimped continuous fibers having a saw tooth shaped crimp along the length of the staple fiber, with a crimp (or repeating bend) frequency of preferably no more than 8 crimps per
centimeter.

The staple fibers can also be formed by stretch breaking continuous
30 fibers resulting in staple fibers with deformed sections that act as crimps. Stretch broken staple fibers can be made by breaking a tow or a bundle of continuous filaments during a stretch break operation having one or more break zones that are a prescribed distance creating a random variable

mass of fibers having an average cut length controlled by break zone adjustment.

Spun staple yarn can be made from staple fibers using traditional long and short staple ring spinning processes that are well known in the art. For short staple, cotton system spinning fiber lengths from about 1.9 to 5.7 cm (0.75 in to 2.25 in) are typically used. For long staple, worsted or woolen system spinning, fibers up to about 16.5 cm (6.5 in) are typically used. However, this is not intended to be limiting to ring spinning because the yarns may also be spun using air jet spinning, open end spinning, and many other types of spinning which converts staple fiber into useable yarns.

Spun staple yarns can also be made directly by stretch breaking using stretch-broken tow to top staple processes. The staple fibers in the yarns formed by traditional stretch break processes typically have length of up to about 18 cm (7 in) long. However spun staple yarns made by stretch breaking can also have staple fibers having maximum lengths of up to around 50 cm (20 in.) through processes as described for example in PCT Patent Application No. WO 0077283. Stretch broken staple fibers normally do not require crimp because the stretch-breaking process imparts a degree of crimp into the fiber.

The staple fibers can also be formed by stretch breaking continuous fibers resulting in staple fibers with deformed sections that act as crimps. Stretch broken staple fibers can be made by breaking a tow or a bundle of continuous filaments during a stretch break operation having one or more break zones that are a prescribed distance creating a random variable mass of fibers having an average cut length controlled by break zone adjustment.

The term continuous filament refers to a flexible fiber having relatively small-diameter and whose length is longer than those indicated for staple fibers. Continuous filament fibers and multifilament yarns of continuous filaments can be made by processes well known to those skilled in the art.

Many different fibers can be used as the textile staple fiber. In some embodiments aramid fiber can be used in the blend as the textile staple fiber. In some preferred embodiments meta-aramid fibers are used in the blend as the textile staple fiber. By aramid is meant a polyamide wherein at least 85% of the amide (-CONH-) linkages are attached directly to two aromatic rings. A meta-aramid is such a polyamide that contains a meta configuration or meta-oriented linkages in the polymer chain. Meta-aramid fibers are currently available under the trademarks Nomex® from E. I. du Pont de Nemours of Wilmington, Delaware. Additives can be used with the aramid and, in fact it has been found that up to as much as 10 percent, by weight, of other polymeric material can be blended with the aramid or that copolymers can be used having as much as 10 percent of other diamine substituted for the diamine of the aramid or as much as 10 percent of other diacid chloride substituted for the diacid chloride of the aramid. In some embodiments, the preferred meta-aramid fiber is poly(meta-phenylene isophthalamide (MPD-I). This fiber may be spun by dry or wet spinning using any number of processes; United States Patent Nos. 3,063,966 and 5,667,743 are illustrative of useful processes.

In some embodiments para-aramid fibers can be used as the textile staple fiber in the blend for increased flame strength and reduced thermal shrinkage. Para-aramid fibers are currently available under the trademarks Kevlar® from E. I. du Pont de Nemours of Wilmington, Delaware and Twaron® from Teijin Ltd. of Tokyo, Japan. For the purposes herein, Technora® fiber, which is available from Teijin Ltd. of Tokyo, Japan, and is made from copoly(p-phenylene/3,4'diphenyl ester terephthalamide), is considered a para-aramid fiber.

In some embodiments polyazole fibers can be used as the textile fiber in the blend. For example, suitable polyazoles include polybenzazoles, polypyridazoles, and the like, and can be homopolymers or copolymers. Additives can be used with the polyazoles and up to as much as 10 percent, by weight, of other polymeric material can be blended with the polyazoles. Also copolymers can be used having as much as 10 percent or more of other monomer substituted for a monomer of the

polyazoles. Suitable polyazole homopolymers and copolymers can be made by known procedures, such as those described in U.S. Patents 4,533,693 (to Wolfe, et al., on Aug. 6, 1985), 4,703,103 (to Wolfe, et al., on Oct. 27, 1987), 5,089,591 (to Gregory, et al., on Feb. 18, 1992),
5 4,772,678 (Sybert, et al., on Sept. 20, 1988), 4,847,350 (to Harris, et al., on Aug. 11, 1992), and 5,276,128 (to Rosenberg, et al., on Jan. 4, 1994).

In some embodiments the preferred polybenzazoles are polybenzimidazoles, polybenzothiazoles, and polybenzoxazoles. If the polybenzazole is a polybenzimidazole, preferably it is poly[5,5'-bi-1H-
10 benzimidazole]-2,2'-diyl-1,3-phenylene which is called PBI. If the polybenzazole is a polybenzothiazole, preferably it is a polybenzobisthiazole and more preferably it is poly(benzo[1,2-d:4,5-d']bisthiazole-2,6-diyl-1,4-phenylene which is called PBT. If the polybenzazole is a polybenzoxazole, preferably it is a polybenzobisoxazole and more
15 preferably it is poly(benzo[1,2-d:4,5-d']bisoxazole-2,6-diyl-1,4-phenylene which is called PBO. In some embodiments the preferred polypyridazoles are rigid rod polypyridobisazoles including poly(pyridobisimidazole), poly(pyridobisthiazole), and poly(pyridobisoxazole). The preferred poly(pyridobisoxazole) is poly(1,4-(2,5-dihydroxy)phenylene-2,6-
20 pyrido[2,3-d:5,6-d']bisimidazole which is called PB. Suitable polypyridobisazoles can be made by known procedures, such as those described in U.S. Patent 5,674,969.

In some embodiments modacrylic fibers can be used. The preferred modacrylic fibers used in this invention are copolymers of acrylonitrile
25 combined with vinylidene chloride. The copolymer can have, in addition, an antimony oxide or antimony oxides for improved fire retardancy. Such useful modacrylic fibers include, but are not limited to, fibers disclosed in United States Patent No. 3,193,602 having 2 weight percent antimony trioxide, fibers disclosed in United States Patent No. 3,748,302 made with
30 various antimony oxides that are present in an amount of at least 2 weight percent and preferably not greater than 8 weight percent, and fibers disclosed in United States Patent Nos. 5,208,105 & 5,506,042 having 8 to 40 weight percent of an antimony compound. The preferred modacrylic

fiber is commercially available from Kaneka Corporation, Japan, in various forms, some containing no antimony oxides while others such as Protex C are said to contain 10 to 15 weight percent of those compounds.

In some preferred embodiments the various types of staple fibers are present as a staple fiber blend. By fiber blend it is meant the combination of two or more staple fiber types in any manner. Preferably the staple fiber blend is an "intimate blend", meaning the various staple fibers in the blend form a relatively uniform mixture of the fibers. In some embodiments the two or more staple fiber types are blended prior to or while the yarn is being spun so that the various staple fibers are distributed homogeneously in the staple yarn bundle.

Fabrics can be made from the spun staple yarns and can include, but is not limited to, woven or knitted fabrics. General fabric designs and constructions are well known to those skilled in the art. By "woven" fabric is meant a fabric usually formed on a loom by interlacing warp or lengthwise yarns and filling or crosswise yarns with each other to generate any fabric weave, such as plain weave, crowfoot weave, basket weave, satin weave, twill weave, and the like. Plain and twill weaves are believed to be the most common weaves used in the trade and are preferred in many embodiments.

By "knitted" fabric is meant a fabric usually formed by interlooping yarn loops by the use of needles. In many instances, to make a knitted fabric spun staple yarn is fed to a knitting machine which converts the yarn to fabric. If desired, multiple ends or yarns can be supplied to the knitting machine either plied or unplied; that is, a bundle of yarns or a bundle of plied yarns can be co-fed to the knitting machine and knitted into a fabric, or directly into a article of apparel such as a glove, using conventional techniques. In some embodiments it is desirable to add functionality to the knitted fabric by co-feeding one or more other staple or continuous filament yarns with one or more spun staple yarns having the intimate blend of fibers. The tightness of the knit can be adjusted to meet any specific need. A very effective combination of properties for protective

apparel has been found in for example, single jersey knit and terry knit patterns.

In some particularly useful embodiments, the spun staple yarns can be used to make flame-resistant garments. In some embodiments the garments can have essentially one layer of the protective fabric made from the spun staple yarn. Exemplary garments of this type include jumpsuits and coveralls for fire fighters or for military personnel. Such suits are typically used over the firefighters clothing and can be used to parachute into an area to fight a forest fire. Other garments can include pants, shirts, gloves, sleeves and the like that can be worn in situations such as chemical processing industries or industrial electrical/utility where an extreme thermal event might occur. In some preferred embodiments the fabrics have an arc resistance of at least 0.8 calories per square centimeter per ounce per square yard.

In one embodiment the fiber mixture of the polymeric staple fiber and the textile staple fiber is formed by making an intimate blend of the fibers. If desired, other staple fibers can be combined in this relatively uniform mixture of staple fibers. The blending can be achieved by any number of ways known in the art, including processes that creel a number of bobbins of continuous filaments and concurrently cut the two or more types of filaments to form a blend of cut staple fibers; or processes that involve opening bales of different staple fibers and then opening and blending the various fibers in openers, blenders, and cards; or processes that form slivers of various staple fibers which are then further processed to form a mixture, such as in a card to form a sliver of a mixture of fibers. Other processes of making an intimate fiber blend are possible as long as the various types of different fibers are relatively uniformly distributed throughout the blend. If yarns are formed from the blend, the yarns have a relatively uniform mixture of the staple fibers also. Generally, in most preferred embodiments the individual staple fibers are opened or separated to a degree that is normal in fiber processing to make a useful fabric, such that fiber knots or slubs and other major defects due to poor

opening of the staple fibers are not present in an amount that detract from the final fabric quality.

In a preferred process, the intimate staple fiber blend is made by first mixing together staple fibers obtained from opened bales, along with
5 any other staple fibers, if desired for additional functionality. The fiber blend is then formed into a sliver using a carding machine. A carding machine is commonly used in the fiber industry to separate, align, and deliver fibers into a continuous strand of loosely assembled fibers without substantial twist, commonly known as carded sliver. The carded sliver is
10 processed into drawn sliver, typically by, but not limited to, a two-step drawing process.

Spun staple yarns are then formed from the drawn sliver using techniques including conventional cotton system or short-staple spinning processes such as open-end spinning and ring-spinning; or higher speed
15 air spinning techniques such as Murata air-jet spinning where air is used to twist the staple fibers into a yarn. The formation of spun yarns can also be achieved by use of conventional woolen system or long-staple processes such as worsted or semi-worsted ring-spinning or stretch-break spinning. Regardless of the processing system, ring-spinning is the
20 generally preferred method for making the spun staple yarns.

EXAMPLES

Unless otherwise stated, the examples were all prepared using the following procedures. Ratios of reagents are given as mole ratios. Oleum,
25 was obtained from E. I. du Pont de Nemours and Company, Wilmington, DE. Terephthalic acid (TA), isophthalic acid (IA), 4,4'-oxybis(benzoic acid) (OBBA), methane sulfonic acid, polyphosphoric acid, and dimethylsulfoxide were obtained from Sigma-Aldrich®. Hydrazine sulfate was obtained from Acros Organics. Sulfuric acid and sodium bicarbonate
30 were obtained from EMD Chemicals, Inc.

General polymerization procedure

Unless otherwise specified, the following general polymerization

procedure was used in each example while varying the ratio of the monomers, as specified. To a dried 100 mL glass reactor equipped with a glass mechanical stirrer, nitrogen inlet, and reagent addition ports were added via powder funnel hydrazine sulfate (0.015 mol, 1 molar equivalent) and the dicarboxylic acid(s) in amounts that total 1 molar equivalent. The molar ratios of dicarboxylic acids : hydrazine sulfate were 1:1, unless otherwise specified. The specific molar ratios of each dicarboxylic acid are specified in the examples. The solid ingredients were blended together thoroughly for 15 minutes under nitrogen. To this blended mixture of solids was added 19.028 g (0.0712 mol SO_3) of 30% oleum (fuming sulfuric acid, 30% by weight free SO_3 content) at room temperature while stirring. The reaction kettle was completely sealed and leak-free (including stirrer shaft) to prevent vapor phase ingredients from escaping the kettle. The mixture was mechanically stirred at room temperature for several minutes. The reactor was then immersed into an oil bath, and heated to 130 °C. The polymerization was allowed to proceed for 4 hours at 130°C. During the polymerization, the stir rate was often reduced or stopped if the viscosity of the polymerization solution became too high.

In some examples, pre-reacted 4,4'-oxybis(benzoic acid (OBBA) was used. OBBA was dissolved in 30% oleum, and the reaction was allowed to proceed for 6.5 hours at 130 °C. The reactor was charged with hydrazine sulfate and the other dicarboxylic acids, in the same ratios as above. The solution of 4,4'-oxybis(benzoic acid) was then added. The mixture contained a lot of solid chunks which did not incorporate into the reaction mixture well until approximately 200 minutes had passed at 130 °C . The polymerization was allowed to proceed for 4 hours at 130 °C.

General fiber formation procedure

Three methods were used to prepare fibers. Fibers in Examples 1-19 were prepared by the following. The polymer reaction mixture was diluted with sulfuric acid (95-98%). Sufficient sulfuric acid was added so that the solution viscosity was high enough such that a thin continuous stream could be dropped into a blender containing water while rotating at

a rate, to ensure that the coagulated fiber not be pulled apart. Optimization of this process was determined for each polymerization. In order to coagulate fiber, a rubber septum was added to the top of the blender blade, which allowed for the fiber to be wound around and collected. The fiber was then rewound onto a glass vial, typically by hand, washed with water, and then soaked in dilute sodium bicarbonate until fully neutralized. The fiber was then washed and soaked with water to remove any residual sodium bicarbonate. The fibers were allowed to dry at ambient conditions. In some examples, a sample of the fiber was dried under high vacuum at room temperature for molecular weight determination by size exclusion chromatography (SEC) in methane sulfonic acid.

Fibers in Examples 20 and 21 were prepared by the following procedure. The fibers were spun from sulfuric acid solutions that ranged in concentration from 6-9 wt % polymer. The solution was delivered by a gear pump through a spinneret with 10 holes having diameter of 0.005" or 0.008". The volumetric flow rate of spinning solution was 0.3-2 mL/min. The fiber was extruded directly into a coagulation bath filled with a room temperature solution that was 0-20 wt. % sulfuric acid. Fiber residence time in the coagulation bath was between 15 and 60 seconds. The fiber emerged from the coagulation bath through a ceramic guide into a wash bath of room temperature water. In the wash bath the fiber was wrapped around two speed-controlled driven rolls and then drawn 50-100%. Three wraps were usually made around each of these rolls. The fiber was wound onto a phenolic core. The wound fiber bobbins were then neutralized in 0.5 wt % sodium bicarbonate solution, washed in de-ionized water and air dried at room temperature in a series of batch steps.

Fibers were also prepared by the following procedure. The fibers were spun from sulfuric acid solutions that ranged in concentration from 4-14 wt % polymer. The solution was delivered by a gear pump through a spinneret with 10-20 holes having diameter of 0.003" or 0.008". The volumetric flow rate of spinning solution was 0.3-2 mL/min. The fiber was extruded directly above a coagulation bath filled with a room temperature, elevated temperature, or sub-ambient temperature solution that was 0-70

wt. % sulfuric acid. The fiber was 1/8" to 6 inches from the coagulation bath. Fiber residence time in the coagulation bath was between 15 and 60 seconds. The fiber emerged from the coagulation bath through a ceramic guide into a wash bath of room temperature, elevated temperature, or sub-ambient temperature water, acid aqueous, or basic aqueous solution. In the wash bath the fiber was wrapped around two speed-controlled driven rolls and then drawn 0-500%. Three wraps were usually made around each of these rolls. The fiber was wound onto a phenolic core. The wound fiber bobbins were then neutralized in slightly basic solution, washed in de-ionized water and air dried at room temperature or elevated temperature or dried in a vacuum oven at room temperature or elevated temperature in a series of batch steps.

General cast film preparation procedure

The polymerization solution was diluted with sulfuric acid (95-98%) until the viscosity achieved would allow pouring onto a glass plate to give a uniform film. This viscosity was typically less than the viscosity required to coagulate fiber. The polymer and glass plate were immersed into a water bath in order to coagulate the film. The coagulated film was washed with water and then soaked in dilute sodium bicarbonate until fully neutralized. The film was then washed and soaked with water to remove any residual sodium bicarbonate. The film was pressed under varying amounts of pressure between paper towels, repeatedly, until mostly dry by touch. The film was then placed between aluminum foil sheets and pressed at 10,000 lb for 5 minutes. The resulting film was dried under high vacuum at room temperature for 24 hours.

General pulp film preparation procedure

A cast film as prepared above was pulped into small particles in a blender with water. The solids were filtered through a glass fritted filter and washed with water repeatedly. The solid was pulped in the blender again with dilute sodium bicarbonate solution until neutralized, filtered through a glass fritted filter and washed with water repeatedly. The solid was pulped

in the blender again with water, filtered through a glass fritted filter and washed with water repeatedly. The pulping process was then repeated. The solid film was dried on the glass fritted filter until it could be gently removed in one piece. The film was pressed under varying amounts of pressure between paper towels, repeatedly, until mostly dry by touch. The film was then placed between aluminum foil and pressed at 10,000 lb for 30 minutes. The film was dried under high vacuum at room temperature.

LOI measurement

10 Limiting Oxygen Index (LOI) is the minimum concentration of oxygen, expressed as a volume percent, in a mixture of oxygen and nitrogen that will just support the flaming combustion of a material initially at room temperature under the conditions of ASTM G125 / D2863. LOI was measured using a modified ASTM method (ASTM D 2863) to allow
15 for rapid screening of the samples. Films were mounted in sample holder which was inserted in the LOI apparatus and covered with a glass chimney. The oxygen content within the glass chimney was controlled digitally. The film was exposed to a flame, and the oxygen level in the chimney was increased until the sample burns. The LOI of any given
20 sample was measured at the point at which candle-like burning can be sustained. Sample data and results are summarized in Table 1.

TABLE 1

Ex.	IA mol%	TA mol%	OBBA mol%	M _n (g/mol)	M _w (g/mol)	M _w /M _n	LOI	
1	10	80	10	6000	17800	2.96	27	Off-white, fairly strong, T _{d onset} was ~503°C
2	5	75	20	31000	69100	2.23	30.5 ± 0.5	White, strong
3	0	80	20	36600	67300	1.84	30.2 ± 0.9	Colorless to white, strong, high degree of elongation
4	0	50	50	30500	49700	1.63	23.0 ± 0.0	White, weak, high degree of elongation
5	0	60	40	30200	57800	1.92	29.0 ± 1.0	Colorless to white, fairly strong
6	0	70	30	28900	56600	1.96	31.3 ± 1.1	White to colorless, very strong, high degree of elongation
7	0	95	5	32700	90500	2.77	26.0 ± 0.0	Yellow, strong, high degree of elongation
8	0	90	10	31100	77900	2.50	26.7 ± 0.5	Yellow, strong, high degree of elongation
9	0	75	25	58100	77300	1.33	31.0 ± 1.0	Colorless to white, strong, high degree of elongation
10 (1)	0	75	25	16100	54800	3.40	25	Films prepared. No sulfonation
11	0	75	25	24100	47000	1.95	35	Films prepared
12	0	75	25	26100	59700	2.29	34	Colorless to white, strong, high degree of elongation
13 (2)	0	75	25	30500	71300	2.34	>33	Films prepared
14 (2)	0	75	25	15500	42000	2.71	34	Films prepared
15	0	82	18	29800	85500	2.87	29	Colorless to white, fairly strong, high degree of elongation
16 (2)	0	75	25	13000	38200	2.95	32.2 ± 0.3	White fiber was fairly weak
17 (2)	0	75	25	12000	34900	2.92	32	White fiber was fairly weak
18	0	75	25	25600	64200	2.51	31.5 ± 0.5	Colorless to white, strong, high degree of elongation
19 (3)	0	0	100	10900	33800	3.10	--	Polymer was water soluble
20 (4)	20	80	0	19300	45200	2.34	--	Colorless to white, strong, high degree of elongation
21 (5)	0	75	25	19300	41100	2.12	35.3 ± 0.6	Colorless to white, strong, high degree of elongation

- (1) Comparative example. Oleum was replaced by polyphosphoric acid and sulfuric acid was replaced by phosphoric acid
- (2) Pre-reacted OBBA was used
- 5 (3) Comparative example
- (4) Comparative example performed on larger scale. Polymer was prepared by mixing 86.885 grams (0.6677 moles hydrazine) of solid hydrazine sulfate, 105.12 grams (0.6327 moles) of solid terephthalic acid, and 9.000 grams (0.0333 moles) of solid isophthalic acid were mixed and blended together in a mixer for 30 min. A first
- 10 addition of 30% oleum, 534 grams oleum (2.001 moles of SO_3) was added at 25 °C, mechanically stirred at 25 °C for 15 minutes, then heated to 120 °C with mechanical stirring until a constant torque was observed on the mixer (60 minutes). A second addition of 30% oleum, 611 grams oleum (2.290 moles of SO_3) was then added at 130 °C. The temperature was maintained at 130 °C for 2 hours until the viscosity of the solution reached a plateau, then cooled to room temperature.
- 15 (5) Example performed on larger scale (2L) using hydrazine sulfate (1.005 molar equivalents), terephthalic acid, 4,4'-oxybis(benzoic acid), and 20 % oleum. The resulting extremely viscous amber mixture was quenched and diluted to 9.42 wt% by the addition of water.
- 20

EXAMPLE 22

Proof of Sulfonation of 4,4'-oxybis(benzoic acid)

4,4'-Oxybis(benzoic acid) (87 mg, Aldrich 99%) were added to 0.9 mL of 30 % oleum. The material was stirred for < 1 minutes at ambient

25 temperature and transferred immediately to a 5 mm outer diameter (o.d) tube suitable for nuclear magnetic resonance (NMR) spectroscopic studies. Into the NMR tube had previously been inserted a sealed capillary containing dimethyl sulfoxide[^] for deuterium lock and chemical shift referencing. The tube was immediately inserted into a NMR probe held at

30 30 °C. After a brief period to homogenize ("shim") the magnetic field, an automated series of ^1H NMR spectra were acquired on the sample.

Resonances at 8.11 and 6.98 ppm were assigned to ^1H nuclei of unsulfonated rings, and resonances at 8.47, 8.18, and 7.06 ppm were assigned to those of sulfonated rings substituted at the position *ortho* to the ether linkage. During the course of the kinetic spectral acquisition, the

35 resonances assigned to unsulfonated rings diminished in intensity, and

those assigned to sulfonated rings increased, indicating sulfonation of the rings. The half-life of this process at 30 °C was 52 min.

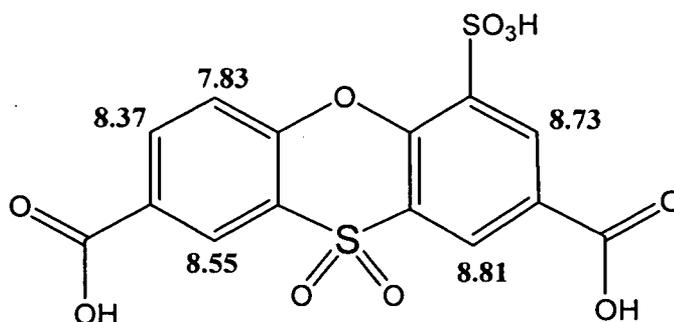
EXAMPLE 23

5 Proof of structure of sulfonylated 4,4'-oxybis(benzoic acid)

A 40 mL vial containing a magnetic stir bar was charged with 4,4'-oxybis(benzoic acid) (6.0 g) and 30% oleum (39.6 g). The mixture was heated in a 130 °C hot block for 3 days. Samples (1 mL) of the resulting clear brown solution were then quenched with water and vortexed to mix.
10 The precipitated solids were filtered and sparingly washed with ice water. The remaining solid was predominately the monosulfonated sulfone product and the aqueous filtrate predominately contained the disulfonated sulfone. ¹H NMR spectrum and LC/MS were performed and indicate that the desired sulfonated and sulfonylated products were formed.

15 A saturated solution of the monosulfonated sulfone product was prepared in water-d₂ containing a trace of sodium 3-trimethylsilylpropionate-d₄ as a chemical shift referent. The solution was inserted in a NMR probe and heated to 60 °C to ensure dissolution. A series of NMR two dimensional correlation experiments were performed to
20 elucidate the structure of the material. These experiments permitted assignment of the ¹H resonances of the primary product, 4-sulfophenoxathiine-2,8-dicarboxylic acid 10,10-dioxide. The ¹H assignments (in ppm relative to chemical shift referent at 0.00 ppm) are shown in the following below.

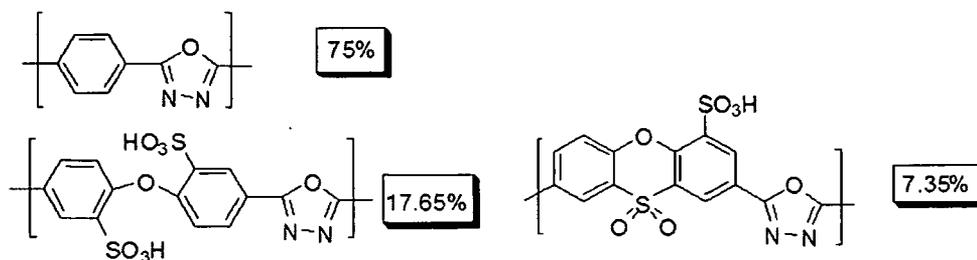
25



EXAMPLE 24Proof of sulfonylation and sulfonation of polymers

Poly(phenylene-co-4,4'-oxybis(benzoic acid) disulfonate oxadiazole) (34.4 mg), in which the terephthalic acid and 4,4'-
 5 oxybis(benzoic acid) monomer units were present in a 70:30 molar ratio, were dissolved in 30% oleum (1.384 g) at 50 °C. This material was transferred into a cylindrical tube with 3 mm o.d., suitable for use in NMR spectroscopy. This tube was then frozen in liquid nitrogen, evacuated, and flame-sealed. The sealed tube was inserted in a 5 mm o.d. NMR tube,
 10 with the interstitial space between the tubes filled with dimethylsulfoxide- d_6 . The tubes were then inserted in a NMR probe and heated to 130 °C. Upon reaching temperature, an automated series of ^1H NMR spectral acquisitions was initiated, using quantitative acquisition conditions so as to study the kinetics of reaction. Sulfonylation of the 4,4'-oxybis(benzoic acid)
 15 rings was observed, as discussed in previous examples.

The material formed in Example 9 was analyzed via NMR, and using the spectral assignments from above, it was found that 17.65 % of the OBBA monomer was in the disulfonated form, 7.35% was in the monosulfonated sulfone form, and a trace amount was in the disulfonated sulfone, which is 5.34 weight % of S:
 20



* Note: the SO_3H could be in the salt form- Na^+ , etc

Elemental analysis was performed on the material from Example 6
 25 and found 43.26% C, 3.07% H, 30.06 %O, 10.18% N and 6.50% S.

EXAMPLE 25

Synthesis of poly(oxadiazole) (POD) containing 80:10:10
 terephthalic acid : 4,4'-oxybis(benzoic acid) : 5-sulfoisophthalic acid

To a dried 100 ml_ glass reactor equipped with a glass mechanical stirrer, nitrogen inlet, and reagent addition ports were added via powder funnel hydrazine sulfate (0.015 mol, 1.007 molar equivalents) and the dicarboxylic acids (terephthalic acid (1.994 g, 0.8 molar equivalents), 4,4'-oxybis(benzoic acid) (0.387 g, 0.1 molar equivalents), and 5-sulfoisophthalic acid (0.402 g, 0.1 molar equivalents)) in amounts that total 1 molar equivalent. The solid ingredients were blended together thoroughly for 15 minutes under nitrogen. To this blended mixture of solids was added 28.5 g of 20% oleum (fuming sulfuric acid, 20% by weight free SO₃ content) at room temperature while stirring. The reaction kettle was completely sealed and leak-free (including stirrer shaft) to prevent vapor phase ingredients from escaping the kettle. The mixture was mechanically stirred at room temperature for several minutes. The reactor was then immersed into an oil bath, and heated to 130 °C. The polymerization was allowed to proceed for 4 hours at 130°C. During the polymerization, the stir rate was often reduced or stopped if the viscosity of the polymerization solution became too high.

20

EXAMPLE 2625% OBBA-POD fiber dyed in Red Dye #29 with benzyl alcohol carrier

To a round bottom flask containing a magnetic stir bar and fiber (0.037 g) was added a solution (82 g) consisting of 10 wt% MERPOL HCS (Aldrich, 1.25 g), TSPP (Aldrich, sodium pyrophosphate tetrabasic, 0.25 g) and DI water (248.50 g). The mixture was placed into a 29 °C oil bath and heated at approximately 3 °C/ min to 85 °C then held at that temperature for 20 min. The fiber was washed with hot water and with room temperature water. The wet fiber was returned to a round bottom flask containing a magnetic stir bar. To the flask was added a solution 0.1 wt% MERPOL HCS (0.005 g) and a solution (55.00 g) containing benzyl alcohol (Aldrich, 3.75 g) and DI water (121.25 g). The mixture was heated in a 46 °C bath for 15 min. Next, Red Dye #29 (Aldrich, 0.0032 g, 7.96 wt% dye to fiber) was dissolved into 10.00 g of a solution containing

benzyl alcohol (3.75 g) and DI water (121.25 g) and added to the reaction mixture. The mixture was heated in the 46 °C for an additional 10 min, the red solution had become slightly pink and the fiber was deep red. The mixture was removed from the heated bath and the pH was 6.3. The pH
5 was adjusted to 3.9 by the addition of acetic acid (1 drop of 0.85 wt%). The mixture was then heated in a 74 °C bath for 15 min and the dye solution had become colorless. The mixture was heated at reflux in a 130 °C bath for an additional 60 min. The fiber was washed with hot water and again with room temperature water. The wet fiber was returned to a round
10 bottom flask containing a magnetic stir bar. To the flask was added 0.1 wt% MERPOL HCS (0.04 g) and DI water (50.00 g). The mixture was heated at 85 °C for an 20 min. The fiber was washed with hot water and again with room temperature water. It was blotted dry in a paper towel then placed into an 82 °C oven for 3 h. Cross-sectional optical microscopy
15 was utilized to ensure complete dye uptake.

CLAIMS

What is claimed is:

- 5 1. A process for preparing a polymer, comprising the steps of:
a) combining hydrazine, oleum, 4,4'-oxybis(benzoic acid), and
one or both of terephthalic acid and isophthalic acid, to form a
reaction mixture, wherein the oleum is added in an amount of at
least about 5 molar equivalents of SO₃ based on the number of
10 moles of hydrazine; and
b) heating the reaction mixture to a temperature of about 100°C
to about 180°C until a polymer is prepared.
2. The process of Claim 1 wherein the oleum is added in an amount of
15 at least about 6 molar equivalents of SO₃ based on the number of moles
of hydrazine.
3. The process of Claim 1 wherein the oleum is added in one step.
- 20 4. The process of Claim 1 wherein the heating is performed at about
120 °C to about 140 °C for at least about 0.5 hours.
5. The process of Claim 1 wherein step a) comprises the steps of:
1) combining hydrazine or salt thereof, 4,4'-oxybis(benzoic
25 acid), and one or both of terephthalic acid and isophthalic acid to form a
pre-mixture;
2) stirring the pre-mixture for at least 5 minutes; and
3) adding oleum to the pre-mixture in an amount of at least
about 5 molar equivalents of SO₃ based on the number of moles of
30 hydrazine to form a reaction mixture.
6. The process of Claim 1 wherein the reaction mixture comprises
about 1 molar % to about 50 molar % of 4,4'-oxybis(benzoic acid) and
about 50 molar % to about 99 molar % of one or both of terephthalic acid

and isophthalic acid, based on the total amount of 4,4'-oxybis(benzoic acid), terephthalic acid and isophthalic acid present.

7. The process of Claim 1 wherein the reaction mixture comprises
5 about 10 molar % to about 30 molar % of 4,4'-oxybis(benzoic acid) and
about 70 molar % to about 90 molar % of one or both of terephthalic acid
and isophthalic acid, based on the total amount of 4,4'-oxybis(benzoic
acid), terephthalic acid and isophthalic acid present.
- 10 8. The process of Claim 1 further comprising the step
c) contacting the sulfonated copolyoxadiazole polymer with a
neutralization agent.
9. The process of Claim 1 wherein the polymer is a sulfonated
15 copolyoxadiazole polymer.

INTERNATIONAL SEARCH REPORT

International application No PCT/US2011/063271

A. CLASSIFICATION OF SUBJECT MATTER INV. C08G73/08 ADD.		
According to International Patent Classification (IPC) or to both national classification and IPC		
B. FIELDS SEARCHED		
Minimum documentation searched (classification system followed by classification symbols) C08G		
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched		
Electronic data base consulted during the international search (name of data base and, where practical, search terms used) EPO-Internal , WPI Data, COMPENDEX, INSPEC		
C. DOCUMENTS CONSIDERED TO BE RELEVANT		
Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 2007/255037 AI (LEE KIU-SEUNG [US] ET AL) 1 November 2007 (2007-11-01) cited in the application claims 1, 10; example 1 -----	1-9
X	DD 292 919 A5 (AKAD WISSENSCHAFTEN DDR [DE]) 14 August 1991 (1991-08-14) claims 1, 6; examples 1, 3 -----	1-9
A	W0 2008/042115 AI (DU PONT [US]; LEE KIU-SEUNG [US]; HAPJZLER JON DAVID [US]) 10 April 2008 (2008-04-10) cited in the application the whole document -----	1-9
<input type="checkbox"/> Further documents are listed in the continuation of Box C. <input checked="" type="checkbox"/> See patent family annex.		
* Special categories of cited documents :		
"A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art. "&" document member of the same patent family	
Date of the actual completion of the international search	Date of mailing of the international search report	
14 February 2012	21/02/2012	
Name and mailing address of the ISA/ European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016	Authorized officer Lux, Rudolf	

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No PCT/US2011/063271

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