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(54) **Method and apparatus for spraycasting**

Verfahren und Anlage zum Aufsprühen

Méthode et dispositif de formage par pulvérisation

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Description

[0001] The present invention relates to spraycasting of an atomized molten metal or alloy onto a collector to form a spray deposit with reduced porosity and improved microstructure.

[0002] A spraycast method is described in US Patent 3 826 0301 that involves atomizing a molten metal or alloy and directing the atomized spray onto a collector surface disposed in a spray chamber to form an article. The spray chamber typically is maintained at atmospheric pressure of argon or other non-reactive gas therein while the molten spray is directed onto the collector.

[0003] U.S. Patent 3 826 921, now Reissue 31 767, describes control of the temperature of the spray deposit independent of the temperature of a mold in which an atomized spray is directed to control the structure of the sprayed deposit. To this end, the patent focuses on the conditions of gas atomization of the molten metal or alloy in the atomizing chamber and not the conditions in the spray chamber.

[0004] WO 87/03012 discloses a method as defined by the preamble of claim 1. According to this document, a deposit is formed by directing a spray of gas atomized molten metal or metal alloy onto a substrate being a rotating collector. The spray of metallic particles is oscillated relative to the substrate, preferably along the axis of rotation of the collector, while the deposit is formed; to this end, an atomizer is oscillated by means comprising a cam and a cam follower. The collector surface receiving the deposit may be conical; as an alternative, the axis of rotation of a cylindrical collector may be tilted relative to the mean axis of the oscillating spray. The drawings of WO 87/03012 show deposits with two edge regions each having an outer surface being at an acute angle relative to an axis perpendicular to the mean axis of the oscillating spray; according to the disclosure of this document (see last complete sentence of page 2) the wedge-shaped cross-section of the edge regions of the deposits is a result of the fact that the spray is conical in shape with a high density of particles in the center and a low density at its periphery.

[0005] US-A-4 905 899 discloses details of atomizers useful for gas atomizing a stream of molten metal and for oscillating the spray of atomized metal as required by WO 87/03012. The atomizer is substantially annular in shape having a central opening through which the stream of molten metal is arranged to pass. The annular atomizer comprises an annular gas plenum chamber and a plurality of gas nozzles arranged in a circle circumscribing the stream of molten metal. As in the apparatus of WO 87/03012, the atomizer is tiltable so that, as it is tilted the gas issuing from the nozzles imparts lateral movement to the spray, and for tilting the atomizer in an oscillating manner, a cam and a cam follower are provided. As an alternative to a rotating collector, US-A-4 905 899 discloses an endless belt.

[0006] The known spraycasting methods of making metallic articles continue to suffer from disadvantages that such articles exhibit fissure porosity at an inner region of the deposit on the collector, that the sprayed deposit includes entrapped argon or other gas that increases porosity of the deposit, and that yields of acceptable spraycast articles are unsatisfactorily low from a commercial production standpoint. Moreover, coarse grain banding is evident in the spraycasting of certain nickel base superalloys, such as IN 718.

[0007] The present invention has an object to provide a spraycasting method effective to reduce fissures at an inner region of the deposit on the collector, and this object is achieved by the method defined by claim 1.

[0008] Further improvements of the inventive method are defined by claims 2 to 12.

[0009] By the present invention it is possible to at least reduce some or all of the disadvantages of the prior art methods described above by using, in addition to the method features of claim 1, certain spray parameters, such as collector surface orientation, collector heating, and spray chamber pressure control that provides better thermal control of an atomized spray in flight in the spray chamber and of the sprayed material deposited on the collector in the spray chamber.

[0010] The present invention envisions in an embodiment actively heating the collector in-situ proximate the leading edge of the deposit to improve the quality of the spray deposit by reducing fissure porosity at an inner region of the deposit on the collector. The collector is thermally insulated and capable of accommodating thermal expansion of the collector surface in still a further embodiment of the invention. In addition, the scan rate and distance of a scanning atomizer is slaved to the rotational speed of the collector in an additional embodiment of the invention such that actual atomizer dwell time (spraying time) is lessened as the collector rpm is increased. A tundish having a filter arrangement therein is provided as well to supply quiet, filtered melt to an atomizer for further benefits.

[0011] The present invention preferably includes in a particular embodiment use of a pressure control technique that involves in-situ evacuation of the spray chamber during spray deposition of the atomized metal or alloy on the collector to maintain an inert or non-reactive gas partial pressure no greater than about 533,2 hPas (400 torr) in the spray chamber, preferably a gas partial pressure of from about 13,33 (10) to less than about 533,2 hPas (400 torr). Such low spray chamber gas partial pressure provides a higher temperature of the atomized spray in flight in the spray chamber and of the sprayed material deposited on the collector in the spray chamber. In addition, the amount of entrapped gas in the deposit is reduced as compared to that present in a deposit sprayed at near atmospheric pressure. The atomized spray of molten metal or alloy is generated by supplying a melt to an atomizing device using atomizing gas, such as argon or other gas inert or non-reactive to

the melt, to atomize the melt and direct it as a spray of molten droplets into the spray chamber having an initial (backfilled) inert or non-reactive gas partial pressure of about 533,2 hPas (400 torr) or less therein. Thereafter, the gas partial pressure in the spray chamber is maintained at about 533,2 hPas (400 torr) or less during spray deposition of the atomized spray on the collector by in-situ evacuation of the spray chamber to remove the atomizing gas introduced therein from the atomized spray. For spray cast articles, such as rings and tubes, having rotational symmetry, the collector can be rotated and moved in a single pass relative to the atomizing device to build up a spray deposit.

[0012] The spraycasting method of the present invention provides a higher temperature of the atomized spray and deposited material and reduces entrapped porosity in the deposited material, reduces inner fissure voids proximate the collector surface during spray deposition, and provides a uniform grain size across the thickness of the tubular spray deposit as a result of achievement of improved thermal equilibrium conditions in the deposit during spray deposition. Yields of acceptable spray cast components can be improved as a result.

[0013] These and other objects and advantages of the present invention will become more readily apparent from the following detailed description taken with the following drawings.

DESCRIPTION OF THE DRAWINGS

[0014]

Figure 1 is a schematic perspective view of apparatus in accordance with an embodiment of the invention for practicing the low gas partial pressure control technique of the invention.

Figure 2 and 2A are sectional view of an atomizer and tundish for practicing the invention.

Figure 3 is sectional view of a collector for the sprayed melt.

Figures 4A1 and 4B1 are photographs of as-sprayed IN718 nickel base superalloy material sprayed at 533,2 hPas (400 Torr) and 973,09 hPas (730 Torr), respectively, on an approximately 50,8 cm (20 inch) diameter mandrel. Figures 4A2 and 4B2 are photomicrographs of the as-sprayed IN718 nickel base superalloy material sprayed at 533,2 hPas (400 Torr) and 973,09 hPas (730 Torr), respectively, showing grain size and porosity. The preforms depicted in Figures 4A1 and 4B1 were sprayed at an angle of 0 degrees (see angle AA of Figure 1; i.e. where the longitudinal axis of the collector is horizontal).

Figures 5A and 5B are photomicrographs of electron beam weld heat affected zones of hot isostatically pressed spraycast Waspaloy nickel base superalloy material sprayed at 533,2 hPas (400 Torr) and 973,09 hPas (730 Torr), respectively, showing higher porosity at the weld heat affected zone for the sample sprayed at 973,09 hPas (730 Torr), Fig. 5B.

Figure 6A is a side elevational view of a DC plasma heating torch useful in practicing an embodiment of the invention. Figure 6B is a plan view of the preheat torch of Figure 6A. Figure 6C is an end elevational view of the preheat torch of Figure 6A.

Figure 7A, 7B are photographs of as-sprayed IN718 nickel base superalloy material sprayed at 973,09 hPas (730 Torr) on an approximately 50,8 cm (20 inch) diameter tapered collector surface at an angle of 45 degrees, Figure 7B, (see angle AA of Figure 1) as compared to Figure 7A of 25 degrees, wherein the central regions of the deposits were at 45 and 25 degree angles, respectively, for Figs. 7A and 7B

Figure 8A, 8B are photographs of as-sprayed IN718 nickel base superalloy material sprayed at 533,2 hPas (400 Torr) on an approximately 50,8 cm (20 inch) diameter tapered collector surface at an angle of 25 degrees (see angle AA of Figure 1), wherein the central regions of the deposits were at 25 degree angles for Figs. 8A, 8B. The spray deposits in Figs. 4B, 7 and 8 are shown cut into two pieces after spraying.

Figure 9A illustrates the collector outer surface having a spray cast deposit thereon and the oscillation cycle comprising incremental spray angles of the atomizing nozzle. Figure 9B illustrates the overlapping spray distribution collected on the collector outer surface as a result of the oscillation spray cycle.

DETAILED DESCRIPTION OF THE INVENTION

[0015] Referring to Figure 1, apparatus is schematically illustrated for spraycasting using the pressure control technique in accordance with an embodiment of the present invention. The apparatus comprises a vacuum melting chamber A and a spray chamber B in a walled chamber C. Disposed in the melting chamber A is a refractory crucible 10 in which a metal or alloy charge is melted by induction melting using induction coil 12 disposed about the crucible. The crucible 10 can be tilted about a crucible trunion T as shown to pour the metal or alloy melt at a proper superheat temperature into a refractory tundish 14. As shown in Figures 1-2, the tundish 14 includes a melt holding chamber 14b and a refractory melt discharge nozzle 14c defining a melt discharge orifice 14d (typical diameter of 6,35 - 7,62 mm

(0.250-0.300 inch) such as 7,42 mm (0.292) for IN 718 melt). Melt is discharged from the orifice 14d to an underlying atomizer means 18 disposed beneath the intermediate wall 19 separating the melting chamber A and the spray chamber B. The tundish functions to filter and control flow rate of the metal.

[0016] The melting chamber A is communicated by conduit C1 to a conventional vacuum pump 20 that can evacuate the melting chamber A to very low vacuum levels, such as less than or equal to 0,133 Pas (10 micron Hg), prior to induction melting of the charge in the crucible 10. In this way, oxygen, nitrogen and other gases that could contaminate and/or react with the melt are removed from the chamber A prior to and during melting.

[0017] For purposes of illustrating the invention and not limiting it, spraycasting of a known nickel base superalloy IN 718 begins with charging the crucible 10 with bar stock of the IN 718 superalloy in the appropriate quantity needed. The crucible 10 comprises an alumina lined crucible that is substantially non-reactive with the melted IN 718 superalloy. The solid charge of the IN718 superalloy is induction melted in the crucible 10 by energizing the induction coils 12. The IN 718 melt is heated to an appropriate superheat above the alloy, melting point (e.g. plus 93,3 to 149°C (200 to 300 degrees F) such as for example plus 149°C (300 degrees F) for IN 718 superalloy melt) prior to pouring. The melt temperature is measured by an infrared radiation (IR) pyrometer. Once the melt is stabilized at the superheat temperature, both the melting chamber A and spray chamber B are backfilled with a partial pressure of inert or non-reactive gas to a level less than or equal to about 533,2 hPas (400 torr) via gas discharged from atomizer 18 to be described or from gas sources S1 and/or S2, such as high pressure cylinders or bottles of inert (e.g. argon) or non-reactive gas, and valves V1, V2. Sources S1, S2 can be combined into a single gas source to this end to provide the gas to chambers A, B. Then, the superheated melt is poured into preheated tundish 14.

[0018] The tundish 14 includes an upstanding reticulated ceramic (zirconia) filter 17 having for example 10 to 20 pores per 25,4 mm (inch) that divides the tundish melt holding chamber 14b into a pour chamber 14g that receives the melt from the crucible 10 and a quiescent chamber 14h that is disposed above the melt discharge nozzle 14c to supply quiet melt thereto. The filter 17 acts to filter the alloy melt as it moves from pour chamber 14g to quiescent chamber 14h where the melt enters the melt discharge nozzle 14c and to diffuse turbulence from the pour chamber to the quiescent chamber. A thermocouple array 15 in the tundish records the tundish metal temperature during a spray run.

[0019] The filter 17 is held fixed in lateral position in the tundish as shown by the filter width dimension being received in a cast-in complementary slot in the tundish and is held down vertically by a zirconia brick 17b. The filter 17 has an upper overflow channel 17a and a V-shaped bottom extending in a direction normal to the

plane of the drawing with the apex of the shape cut off to promote drainage of the filter between pours of molten metal in the tundish and to concentrate drainage to this local filter region.

[0020] The melt poured from the crucible 10 into the preheated tundish 14 is discharged from the melt discharge nozzle 14c having nozzle heater 14j disposed therearound. Flow rate of the melt from the discharge orifice 14d is controlled by maintaining an appropriate in-tundish metal head level. A typical flow rate for IN 718 superalloy melt can be in the range of 34 to 43,1 kg (75 to 95 pounds) per minute. The melt discharged from the tundish discharge orifice 14d flows to the atomizer means 18.

[0021] Atomizer means 18 shown in Figures 2 and 2A for atomizing the melt is of the type described in U.S. Patent 4 779 802 and 4 905 899. Atomizer means 18 comprises a static primary gas nozzle 18a disposed about the melt discharge nozzle 14c. The primary, gas nozzle 18a uses a primary gas such as an inert gas (e.g. argon) at a pressure in the range of 2,11 to 4,22 kg/cm² (30 to 60 psig) supplied from manifold 19a to prevent splashback of the melt discharged from orifice 14d, a particular primary gas (argon) pressure for IN 718 melt being 2.46 kg/cm² (35 psig) for splashback prevention. The manifold 19a of the static gas nozzle 18a receives gas from a gas source 22 disposed outside the spray chamber B. The gas source can comprise conventional high pressure cylinders or bottles of inert gas, such as high purity argon, or other gas that is substantially non-reactive with the melt.

[0022] Atomizer means 18 also comprises a scanning gas atomizer 18d that receives the atomized melt from the primary nozzle 18a and uses an atomizing gas such as an inert gas (e.g. argon) at an atomizing gas pressure in the range of 4,92 to 9,84 kg/cm² (70 to 140 psig) supplied from a gas manifold 21 for melt atomization, a particular secondary atomizing gas pressure for IN 718 superalloy melt being 7,73 kg/cm² (110 psig). The scanning atomizer 18d is termed a scanning atomizer because it oscillates in repeated cycles wherein each oscillation cycle includes oscillation through progressively increasing spray angles (relative to its vertical axis) as the collector 30 is axially moved and rotated at controlled rates relative to the atomizer 18d.

[0023] For purposes of illustration only and not limitation, the atomizer 18d can be operated through repeated cycles wherein each cycle includes oscillation through an angle of about 1, 7, and 13 degrees per one revolution of the collector starting from the vertical axis of the atomizer, Figures 9A. That is, the atomizer 18d will oscillate through a 1.06 degree range relative to the vertical axis for one revolution of the collector 30, then oscillate through a 7.41 degree range for one revolution of the collector, and then oscillate through a 13.58 degree range for one revolution of the collector 30. This cycle is repeated as the collector 30 is moved axially from a start deposition position to a finish deposition position

in a single pass to form the desired sprayed deposit as a preform on the collector. The scanning cycle of the atomizer 18d embodying increasing oscillation angles for each revolution of the collector serves to overlap the sprayed deposit as a pattern schematically illustrated in Figure 9B in a uniform distribution over collector lengths limited only by the length of collector 30 in a single pass deposition operation; i.e. where the collector 30 is moved axially from right to the left in Figures 1 and 6 in a single pass relative to atomizer 18d to form the spray deposited preform on the collector surface 104a. In Figure 9B, so-called "sweet spots" of the spray deposit are generally equally spaced by distance R from one another on the collector surface to form a generally uniform spray deposit having the leading edge region shown oriented within 10 to 20 degrees (e.g. 15 degrees shown) to horizontal (or to an axis perpendicular to the spray axis of the atomizing nozzle 18d in the event a non-horizontal nozzle/collector orientation is used).

[0024] The rpm of the collector 30 can be varied as a function of the outer diameter of collector surface 104a to minimize centrifugal stress on the spray cast deposit; e.g. so as not to exceed 1.41 kg/cm² (20 psi). Oscillation of the atomizer 18d is slaved to the rpm of the collector 30 in that the approximate 1, 7, and 13 degree oscillation sequences will still occur over one revolution of the collector, regardless of the collector rpm, and then be repeated until the desired deposit is formed. The dwell time (spraying time) of each oscillation of the cycle thereby is lessened as the collector rotational speed (rpm) is increased.

[0025] The manifold 21 of the scanning atomizer means 18d receives atomizing gas from a gas source 23 disposed outside the spray chamber B. The gas source can comprise conventional high pressure cylinders or bottles of inert gas, such as high purity argon, or other gas that is substantially non-reactive with the melt.

[0026] The static gas nozzle 18a comprises a plurality (12) of gas discharge orifices 18f (diameter of 1,40 mm (0.055 inch)) spaced circumferentially about the melt discharge orifice 14d as shown in Figure 2A. The scanning gas atomizer 18d comprises a plurality (24) of gas discharge orifices 18i (diameter of 3,99 mm (0.1570 inch)) spaced circumferentially about the atomizer spray opening 18j as shown in Figure 2. The opening 18j and gas discharge orifices 18i of atomizer means 18 are relatively located effective to atomize the metal or alloy melt into a spray of fine molten droplets, an atomizer of use being described in U.S. Patent 4 779 802 and 4 905 899. The atomized metal or alloy spray S is directed at underlying mild steel substrate 104 of collector 30 disposed in the spray chamber B in the path of the spray S as shown in Figures 1.

[0027] The collector 30 is mounted on double coaxial shaft mechanism, Figure 3, that rotates the collector and also moves the collector axially from an axial start deposition position to an axial finish deposition position rel-

ative to the atomizer 18d. The inner shaft 31 rotates via the bearing assembly shown between shafts 31, 33 the collector while the outer shaft 33 mounts the collector 30 for axial motion relative to the atomizer 18d. A vacuum seal assembly 31b shown and bearing assembly shown are provided on the chamber double wall to this end. Rotary shaft 31 is driven in rotation by a AC servomotor 34. AC servomotor 34 and AC servomotor 32 are mounted on a common slide or carriage (not shown). AC servomotor 32 through a conventional ball/screw drive arrangement (not shown) drives the common slide or carriage on which motors 32, 34 are disposed for sliding motion together to impart axial motion to shaft 33 while shaft 31 rotates.

[0028] The collector 30 includes external collector substrate surface 104a shaped to impart a desired shape to the spraycast metal or alloy deposited on the collector. Typical standoff distance between the collector outer surface 104a and the atomizer 18d is from 58,4 to 73,7 cm (23 to 29 inches) such as 66 cm (26 inches) for spraying IN 718 superalloy melt.

[0029] The collector 30 can have a cylindrical outer collector surface 104a to form an annular or tubular deposit D having an inner and outer cylindrical collector surface 104a, such as required for a ring or tube. Alternately, the collector surface 104a can be configured as a tapered cone, Figure 6, or any other shape to form the desired spray cast deposit preform thereon.

[0030] In one embodiment of the invention, the collector 30 typically can be preheated prior to initiation of melt spraying by a static induction coil (not shown in Figure 1). The power and time of the collector preheating vary as a function of substrate size and geometry with the final preheat temperature of the substrate typically being in the range of 927 to 982°C (1700 degrees F to 1800 degrees F) for IN 718 nickel base alloy. Alternately, the DC plasma arc torch described below can be used in lieu of such induction preheating. For the spraycasting of IN 718 superalloy, the collector can comprise mild steel, although other materials can be used for the collector depending upon the metal or alloy being spraycast.

[0031] Typical dimensions for a cylindrical collector outer surface 104a employed can include an outer diameter in the range of about 8,9 to 152,4 cm (3.5 inches to 60 inches) and a length of 152,4 cm (60 inches) having a usable spray length of about 142,2 cm (56 inches).

[0032] The collector 30 is shown in more detail in Figure 3 as having a hollow tubular structure that comprises a simple, low-cost construction, supports quick change manufacturing operations, permits insulation of the collector inner diameter, and accommodates thermal expansion of the collector. The collector 30 comprises axial substrate support end plates 100a, 100b and a stainless steel strongback 102 bearing the weight of the other collector components as well as concentrically positioning the end plates 100a, 100b and mild steel collector substrate 104 and its collector surface 104a relative to

collector longitudinal axis. The strongback 102 is welded at its axial end 102a to hub 112. A tension ring 106 and respective ring bolts and nuts 108, 109 engaging the right hand end plate 100b in Figure 3 hold the mild steel collector substrate 104 firmly in 360 degree annular grooves shown between the axial end plates 100a, 100b. The tension ring 106 is fastened to the strongback by a tension ring fastening pin 106a that extends through appropriate diametral holes (not shown) in the tension ring and strongback 102 and by retaining clips 106b that retain the fastening pins in position at their ends. The left hand support end plate 100a is fastened to hub 112 by screws 114. The hub 112 in turn is fastened to an end hub 31a of the rotary shaft by a spline and bolt connection shown for rotation thereby. A vacuum o-ring pack assembly 31b provides a seal at the shaft 33.

[0033] The diameters of the end plates 100a, 100b can be different to provide a tapered collector outer surface profile, Figure 6, in which the outer diameter of the substrate 104 decreases from one end to the other, or vice versa.

[0034] Between the nuts 109 of the tension ring bolt 108 and the adjacent, outwardly facing surface of end plate 100b are positioned respective graphfelt (compressible) washers 110 which function to allow the collector substrate to elongate as it is preheated and while receiving a hot metal spray deposit. This thermal expansion accommodation mechanism preserves the dimensional integrity of the collector.

[0035] Annular space 120 between the outer diameter of the strongback 102 and the inner diameter of the collector substrate 104 is filled with thermal insulation 122 (partially shown), such as Kaowool insulation, which helps to maintain the temperature of the substrate 104 to a sufficient degree to reduce or eliminate inner diameter fissure porosity during the spraying process; e.g. compare upper preform of Figure 8A sans insulation with lower preform of Figure 8B with insulation.

[0036] The collector 30 is rotated relative to the atomizer 18 during deposition of the spray S thereon by the drive motor and shaft 31 connecting the motor and collector 30. The spray S thereby can be deposited around the entire periphery or circumference of the collector outer surface 104a. The speed of rotation of the collector 30 typically is in the range of 100 to 200 rpm for IN 718 melt at a low rate of 34,0 to 43,1 kg (75 to 95 pounds) per minute. The speed of collector rotation is dictated by the allowable centrifugal stress on the deposit; e.g. to maintain the centrifugal stress to not exceed about 1,41 kg/cm² (20 psi). As mentioned hereabove, the atomizer 18d oscillates through repeated cycles each comprising approximate 1, 7 and 13 degree oscillation for each revolution of the collector 30 as it is rotated and moved axially until the deposit is built up along the desired length of the collector.

[0037] The collector preferably includes an angled peripheral "start" surface region 104b typically disposed

proximate collector end plate 100a at which surface region spraying of the atomized metal or alloy is started. The angled surface region 104b helps to catch sprayed material and form a "quick" build up of material at the region 104a (see Figs. 4 and 9A and "start" in Figs. 7 and 8) and conservation of material in the part envelope region. That is, without the collector region 104b, there will be a fall off or tapering off of the deposited material in a manner that is not useful to form the component, thus providing wasted material deposited on the collector. The surface region 104b can be disposed to also shield collector end plate 100a from molten metal spray. A similar angled surface region (not shown) can be provided proximate an opposite end plate 100b or other region of the collector 30 as for example was used to form the end region features of the deposits shown in Figures 7 and 8.

[0038] In the practice of the invention, the spray chamber B is communicated by conduit C2 disposed opposite from the atomizer 18d to a vacuum pumping system that is capable of evacuating the spray chamber B at a high enough rate in order to maintain a selected low gas partial pressure (e.g. argon gas partial pressure when argon is the gas discharged from static atomizer 18a and scanning atomizer 18d) in the spray chamber B during spraycasting of the spray S onto the collector 30. That is, the vacuum system must be capable of exhausting the argon gas from the spray chamber B at a rapid enough rate to maintain the selected low gas partial pressure in the spray chamber while the spray S is directed at and deposited onto the collector 30. Preferably, the gas partial pressure in the spray chamber B is maintained at about 533,2 hPas (400 torr) and below down to about 13,33 hPas (10 torr). The gas partial pressure in chamber B is maintained from about 333,25 hPas (250) to less than 533,2 hPas (400 torr) using the vacuum system described below for spraycasting of superalloy melts, such as IN 718 superalloy melt.

[0039] A suitable vacuum pumping system to achieve such gas partial pressure levels in the spray chamber B comprises first and second stage blowers (pumps) B1, B2 in series with an intercooler B3 disposed between the blowers to lower the heat of compression. The 1st stage blower B1 is a commercially available Stokes HPB 622 blower, while the 2nd stage blower B2 is a commercially available Hibbon SIAV 25 blower. When tied together, the 1st and second stage blowers B1, B2 provide enough vacuum to overcome the atomizing gas flow at 7,73 kg/cm² (110 psi) (i.e. approximately 25,47 m³ (900 cubic feet) per minute) in the spray chamber B during spray deposition and maintain the spray chamber B at a vacuum typically of 266,6 hPas (200 torr) or less than 533,2 hPas (400 torr) during spray deposition. The vacuum level in the spray chamber B is preset into a proportional integrative derivative controller CC (e.g. UDC 3000 controller from Honeywell Inc.) that automatically controls a modulation valve VV between the blowers B1, B2 and the spray chamber B.

[0040] Prior to the atomized spray S being directed into the spray chamber at the collector 30, the spray chamber B is initially evacuated to less than about 0,0133 Pas (1 micron) in concert with evacuation of the melting chamber A by vacuum pump system 20 to remove oxygen, nitrogen and other unwanted gases. After the alloy is melted in crucible 10 under hard vacuum, the chambers A, B are backfilled with inert (e.g. high purity argon) or non-reactive gas in a range less than or equal to about 533,2 hPas (400 torr) gas partial pressure. The backfill gas is provided from the atomizer 18 or gas source S1 and/or S2, such as high pressure cylinders or bottles of high purity inert or non-reactive gas, via valves V1 and/or V2. A single common gas source (not shown) can be provided for the chambers A, B to this same end via a common valve (not shown). After the spray chamber B is backfilled with inert or non-reactive gas partial pressure in the range less than or equal to about 533,2 hPas (400 torr), the melt is teamed or supplied to the atomizer 18 through the tundish 14, and the atomized spray S is directed at the preheated collector 30 for deposition thereon as a spraycast deposit with typical deposit thicknesses being in the range of 1.27 to 10.16 cm (0.5 inch to 4.0 inches). The collector 30 is rotated and moved axially relative to atomizer 18d in a single pass to deposit the sprayed material to form the desired preform shape on the collector surface 104a.

[0041] A typical ratio of atomizing gas-to-metal flow rate ratio used in practicing the invention especially for spray casting nickel base superalloys such as IN 718 is approximately 1.2 to 1, although the invention is not limited in this regard. An advantage of the invention is that the quality of the sprayed deposit does not appear to be as critically tied to gas to metal ratio as it is when the spray pressure in spray chamber B is near atmospheric.

[0042] As mentioned above, the collector 30 is rotated while the spray S is scanned at the collector 30 by scanning atomizer 18d in repeated cycles each including oscillation at approximate 1, 7, and 13 degrees. While the spray S is being directed at and deposited on the collector 30, the vacuum pumps B1, B2 are operable to maintain the gas partial pressure (e.g. argon partial pressure if argon is the atomizing gas) at a low level preferably from about 13.33 hPas (10 torr) to no greater than about 533,2 hPas (400 torr).

[0043] In one embodiment of the invention, the collector 30 is preheated during spraying by a DC plasma torch or gun 130, Figures 6A, 6B, and 6C. In particular, a low pressure DC arc plasma preheat torch or gun is shown to actively heat the collector surface 104 just ahead of the leading edge LE of the deposit as it is formed; i.e. to provide an active in-situ substrate heating during deposition. The torch or gun 130 heats the substrate 104 just ahead of the deposit to 1) increase the bond between the deposit and substrate 104, 2) reduce inner diameter fissure porosity by maintaining a 927 to 982°C (1700 to 1800 degree F) deposit-to-interface

thermal profile, and 3) allow for the focus of thermal energy at the leading edge of the deposit where the thermal energy is needed to these ends. The in-situ preheat of the collector substrate 104 by torch 130 in combination with the collector construction used having thermal insulation 122 yield a consistent inner diameter thermal profile with an attendant elimination of inner diameter fissure porosity in the deposit. The DC plasma arc torch or gun 130 comprises a typical conventional argon plus helium plasma gun typically used in vacuum plasma spray applications. The torch or gun is water cooled via suitable water lines 150 shown connected to the gun 130 and receives suitable plasma gas via suitable gas lines (not shown) connected to the gun.

[0044] Alternately, the aforementioned induction preheating technique can be used to heat the collector; however, induction preheating may only be used to preheat the collector prior to start of spraying whereas the DC plasma source technique can be used prior to and during the spraying.

[0045] The torch or gun 130 is mounted on a slide mechanism shown in Figures 6a, 6B, and 6C residing in the spray chamber B. The slide mechanism carries a boom 142 which is part of the torch assembly. The boom 142 is carried on a slide 144 which is movable by servomotor 145 and ball/screw mechanism 146 in a direction parallel to the diameter of the collector 30 to permit the torch plume P to adjust in radial dimension to the profile of the sprayed deposit to be built up on the substrate surface 104 during spraying; e.g. see Figure 6C.

[0046] The torch 130 and collector 30 initially are positioned at the start deposition position on the collector 30 by axial movement of the double shaft mechanism. The torch 130 can be adjusted such that plasma plume is directed normal to the collector substrate surface 104a or at an angle thereto using a tapered collector surface as described. As the collector 30 is moved axially (from right to left in Figure 6B) during deposition, the plasma plume is directed just ahead of the deposit leading edge LE for the purposes described hereabove.

[0047] In spray casting, the present invention envisions selecting the angle of an outer surface of the leading edge region LE of the spray deposit, Figure 9A, to be at an acute angle to an axis perpendicular to the spray axis of the atomizing nozzle 18d to reduce inner diameter fissure porosity regardless of pressure in the spray chamber. This can be achieved by proper adjustment of the oscillation angles of the atomizing nozzle 18d. Alternately or in addition, the collector outer surface 104a (or alternately angle of the longitudinal axis of collector 30) can be oriented to be off-horizontal to this end. For example, the angle AA, Figure 1, of the collector surface 104a can be selected to be from 10 to 30 degrees such as 25 degrees relative to horizontal (or other acute angle to horizontal) to improve the quality of the spray deposit by reducing inner diameter fissure porosity. When the angle AA of the collector surface 104a is 45 degrees or 0 degrees relative to horizontal, spray cast

IN 718 deposits on the collector 30 may be produced which have less than optimized inner diameter porosity; e.g. compare Figures 4A, 4B (0 degree angle AA) and Figure 7B (45 degree angle AA of tapered collector surface 104a) versus Figure 7A and Figure 8A, 8B (25 degree angle AA of tapered collector surface 104a) in terms of inner diameter fissure porosity present in the deposit.

[0048] Adjustment of the angle AA of the collector surface 104a relative to horizontal can be effected by using a tapered collector substrate 104 as shown in Figure 6. Alternately, the adjustment of the angle AA can be achieved by mounting the aforementioned double shaft mechanism and AC servomotors for the coaxial shafts 31, 33 in a manner to vary the angle of the shafts relative to horizontal to this same end.

[0049] After spraycasting, the deposited ring or tube typically of thickness from 1,27 to 10,16 cm (0.5 to 4.0 inches) is cooled in the spray chamber B under a relative vacuum. The spraycast ring or tube is removed from the collector 30 at ambient temperature and then can be hot isotatically pressed to densify the deposited ring or tube.

[0050] Maintaining of the low gas partial pressure in the spray chamber B in accordance with the invention provides improved control of the temperature of the atomized spray droplets in flight in the spray chamber B and of the atomized metal or alloy deposited on the collector 30 as well as in the reduction of as-sprayed porosity; e.g. see Figures 4B2 having 2.1 volume % porosity at a spray pressure of 973 hPas (730 torr) as compared Figure 4A2 having 0.9 volume % porosity at a spray pressure of 533,2 hPas (400 torr). In effect, the spray chamber pressure control technique provides a higher temperature of the atomized spray droplets in flight in the spray chamber B and as deposited on the collector by reducing droplet thermal convection heat loss that otherwise can occur at higher spray chamber pressures and by allowing thermal equilibrium conditions to be established more quickly in the deposited metal or alloy on the collector 30.

[0051] Figure 4 illustrates the difference in spray-deposited IN 718 ring made at the low pressure (e.g. 533,2 hPas (400 torr)) in spray chamber B pursuant to the invention, Figure 4A1, versus a spray-deposited IN 718 ring made at much higher pressure (e.g. 973 hPas (730 torr)) in spray chamber B, Figure 4B1. In particular, the fissure porosity at the inner diameter (inner diameter of ring proximate the collector 30) and entrapped gas porosity within the ring deposit are both significantly reduced while the same uniform grain size (e.g. ASTM 6-6.5 grain size) is maintained in each ring microstructure without grain banding or layering.

[0052] Figure 4A2 and Figure 4B2 illustrate microstructures of the spray rings of Figure 4A1 and 4B1, respectively. Entrapped argon in the spray deposit pursuant to the invention is significantly reduced (e.g. 0.9 volume % porosity) as compared to entrapped argon in the spray deposit made at the higher 973 hPas (730 torr)

spray atmosphere (e.g. 2.1 volume% porosity). As a further example, entrapped argon in Waspaloy spray cast rings pursuant to the invention exhibit 0.5 ppm by weight Ar as compared to entrapped argon of 1.5 ppm by weight Ar in Waspaloy spray cast rings spray cast near atmospheric pressure in the spray chamber B.

[0053] Moreover, Figure 5 illustrates a lower electron beam weld porosity in a spray-deposited Waspaloy ring made at the low pressure (e.g. 400 torr) in spray chamber B pursuant to the invention, Figure 5A, as compared to electron weld porosity spray-deposited Waspaloy ring made at much higher pressure (e.g. 973 hPas (730 torr)) in spray chamber B, Figure 5B.

[0054] The spray chamber pressure control technique reduces entrapped atomizing gas (as porosity) in the metal or alloy deposited on the collector 30, reduces fissure voids at the inner surface of the deposit immediately adjacent the collector outer surface 30a, and provides a substantially uniform grain size across the thickness of the deposit on the collector 30 as a result of improved thermal equilibrium conditions established in the deposit during spray deposition. Still further, larger diameter ring or tube deposits can be built up on the collector 30; e.g. deposits having a diameter greater than about 30 inches while avoiding grain layering or banding in the deposit can be achieved.

[0055] Spraycasting at 533,2 hPas (400 torr) or less pursuant to the invention versus 730 torr as used heretofore also allows for scalability of the method and apparatus to make larger diameter preforms (deposits) as the convective cooling is lessened with an attendant increase in spray and deposit temperature. Higher spray/deposit temperatures allow for spraying larger diameter preforms at slower rotational speeds (i.e. reduced centrifugal stresses) while maintaining acceptable thermal profiles even at the larger diameters effective to reduce inner diameter fissure porosity and broaden the processing window.

[0056] Spraycasting at 533,2 hPas (400 torr) or less pursuant to the invention reduces inner diameter fissure porosity, reduces entrapped gas in the deposit, and broadens the processing window to produce a variety of component shapes and sizes with uniform deposit microstructure. Further, control of the substrate angle pursuant to an embodiment of the invention also reduces inner diameter fissure porosity and broadens the processing window to produce a variety of component shapes and sizes with uniform deposit microstructure. Use of the scanning atomizer cycle described above, of the thermally insulated collector, and DC plasma arc torch pursuant to other embodiments of the invention also reduce inner diameter fissure porosity and broaden the processing window to produce a variety of component shapes and sizes with uniform deposit microstructure.

[0057] According to another aspect of the present invention a method of making an article is proposed which method comprises the steps of directing an atomized

metal or alloy spray at a collector disposed in a spray chamber, heating the collector proximate a leading edge region of said deposit as said deposit is formed, and collecting the spray on the collector to form a deposit having a leading edge. Preferably, the collector is heated by directing a DC plasma arc torch plume at the collector proximate the leading edge of said deposit.

[0058] As shown above, according to the present invention it is possible to improve the quality of a spraycast article by scanning an atomizer that forms an atomized metal or alloy spray relative to a rotating and axially moving collector disposed in a spray chamber, rotating and axially moving the collector, oscillating the atomizer in a cycle that includes a plurality of successive oscillations which have increasing oscillation angles compared to the preceding oscillation, and repeating the cycle as the collector is rotated and axially moved to collect the spray on the collector to build up a deposit forming the article.

[0059] The present invention also relates to means for producing a spraycast article.

[0060] The present invention thus can produce spray deposited rings and tubes having reduced inner diameter fissures and porosity as compared to spray deposition at the higher (e.g. 973 hPas (730 torr)) pressure while retaining uniform grain size across the thickness of the spray deposit with no grain banding.

[0061] Although certain embodiments of the invention have been shown and described in detail, it should be understood that variations and modifications may be made thereto without departing from the spirit and scope of the invention as set forth in the appended claims.

Claims

1. A method of making an article, comprising directing an atomized metal or alloy spray (S) at a collector (30) disposed in a spray chamber (B) and collecting the spray on the collector to build up a deposit (D) forming an article, said deposit having a leading edge region (LE) with an outer surface being at an acute angle relative to an axis perpendicular to an axis of said spray, wherein said spray is produced by a scanning atomizer (18) oscillating said spray, **characterized in that** said atomizer (18) is oscillated in an oscillation cycle including a plurality of successive oscillations which have increasing oscillation angles compared to the preceding oscillation, and that said oscillation cycle is controlled to provide said leading edge region (LE) with said acute angle being from 10 degrees to 30 degrees.
2. The method of claim 1 wherein a rotating collector (30) is used and a scanning rate of said atomizer (18) is slaved to the rotational speed of said collector such that atomizer dwell time is lessened as the rotational speed of said collector is increased.

3. The method of claim 1 or 2 including disposing said collector (30) in said chamber (B) in a manner to position a collector surface (104) at an acute angle in the range of about 10 to about 30 degrees relative to a reference axis perpendicular to said spray axis.
4. The method of claim 3 wherein the collector is mounted on shaft means which is oriented at about 10 to about 30 degrees relative to a reference axis perpendicular to said spray axis.
5. The method of claim 3 or 4 wherein said reference axis is horizontal.
6. The method of claim 3 wherein the collector surface (104) is a tapered cone.
7. The method of one of claims 1 to 6 wherein a gas partial pressure in said chamber (B) is maintained between 13,33 hPas (10 torr) and less than 533,2 hPas (400 torr) as the spray (S) is directed at the collector (30) to increase temperature of the spray in the spray chamber effective to reduce fissures at an inner region of the deposit on the collector and/or porosity of the deposit on the collector by virtue of reducing entrapped gas.
8. The method of one of claims 1 to 7, further comprising:
 - rotating the collector,
 - moving said atomizer (18) and said collector (30) relative to one another in the direction of the axis of rotation of the collector, and
 - repeating said oscillation cycle as the collector is rotated and the collector and atomizer are axially moved relative to one another to collect the spray on the collector to build up said deposit (D) forming the article.
9. The method of claim 8 wherein the oscillation angles are controlled to have the outer surface of said leading edge region (LE) of the deposited metal or alloy at said acute angle.
10. The method of claim 8 or 9 wherein each oscillation occurs for one revolution of the collector (30) regardless of rotational speed of the collector.
11. The method of one of claims 1 to 10, comprising:
 - heating the collector (30) proximate a leading edge region (LE) of said deposit (D) as said deposit is formed.
12. The method of claim 11 wherein the collector (30)

is heated by directing a DC plasma arc torch plume (P) at the collector proximate the leading edge (LE) of said deposit (D).

Patentansprüche

1. Verfahren zur Herstellung eines Artikels, welches umfasst: Richten eines Sprühstrahls (S) von zerstäubtem Metall oder zerstäubter Legierung auf einen in einer Sprühkammer (B) angeordneten Kollektor (30) und Auffangen des Sprühstrahls auf dem Kollektor zum Aufbauen eines Niederschlags (D), welcher einen Artikel bildet, wobei der Niederschlag einen Vorderkantenbereich (LE) mit einer Außenfläche aufweist, die in einem spitzen Winkel relativ zu einer senkrecht zu einer Achse des Sprühstrahls verlaufenden Achse steht, wobei der Sprühstrahl von einem den Sprühstrahl oszillierenden Abtastzerstäuber (18) erzeugt wird, **dadurch gekennzeichnet, dass** der Zerstäuber (18) in einem Oszillationszyklus oszillieren gelassen wird, welcher eine Mehrzahl von aufeinanderfolgenden Oszillationen umfasst, welche gegenüber der vorausgehenden Oszillation größer werdende Oszillationswinkel aufweisen, und dass der Oszillationszyklus so gesteuert wird, dass der Vorderkantenbereich (LE) mit dem spitzen Winkel in einem Bereich von 10 Grad bis 30 Grad bereitgestellt wird.
2. Verfahren nach Anspruch 1, wobei ein drehbarer Kollektor (30) verwendet wird und eine Abtastrate des Zerstäubers (18) der Drehzahl des Kollektors so untergeordnet ist, dass die Zerstäuberverweilzeit mit wachsender Drehzahl des Kollektors geringer wird.
3. Verfahren nach Anspruch 1 oder 2, umfassend das Anordnen des Kollektors (30) in der Kammer (B) in der Weise, dass eine Kollektoroberfläche (104) in einem spitzen Winkel in dem Bereich von ca. 10 bis ca. 30 Grad relativ zu einer senkrecht zu der Sprühstrahlachse stehenden Bezugsachse positioniert ist.
4. Verfahren nach Anspruch 3, wobei der Kollektor an einem Wellen-Mittel montiert ist, welches unter ca. 10 bis ca. 30 Grad relativ zu einer senkrecht zu der Sprühstrahlachse stehenden Bezugsachse ausgerichtet ist.
5. Verfahren nach Anspruch 3 oder 4, wobei die Bezugsachse horizontal ist.
6. Verfahren nach Anspruch 3, wobei die Kollektoroberfläche (104) ein verjüngter Kegel ist.
7. Verfahren nach einem der Ansprüche 1 bis 6, wobei

ein Gaspartialdruck in der Kammer (B) zwischen 13,33 hPa (10 Torr) und weniger als 533,2 hPa (400 Torr) gehalten wird, während der Sprühstrahl (S) auf den Kollektor (30) gerichtet ist, um die Temperatur des Sprühstrahls in der Sprühkammer zu erhöhen, so dass spaltartige Erscheinungen an einem inneren Bereich des Niederschlags auf dem Kollektor und/oder Porosität des Niederschlags auf dem Kollektor dank Verminderung von Gaseinschlüssen reduziert werden.

8. Verfahren nach einem der Ansprüche 1 bis 7, ferner umfassend:

Drehen des Kollektors,

Bewegen des Zerstäubers (18) und des Kollektors (30) relativ zueinander in Richtung der Drehachse des Kollektors und

Wiederholen des Oszillationszyklus, während der Kollektor gedreht und der Kollektor und Zerstäuber relativ zueinander axial bewegt werden, zum Auffangen des Sprühstrahls auf dem Kollektor zum Aufbau des den Artikel bildenden Niederschlags (D).

9. Verfahren nach Anspruch 8, wobei die Oszillationswinkel so gesteuert werden, dass die Außenfläche des Vorderkantenbereichs (LE) des/der niedergeschlagenen Metalls bzw. Legierung in dem spitzen Winkel steht.

10. Verfahren nach Anspruch 8 oder 9, wobei jede Oszillation über eine Umdrehung des Kollektors (30) auftritt, unabhängig von der Drehzahl des Kollektors.

11. Verfahren nach einem der Ansprüche 1 bis 10, umfassend:

Erwärmen des Kollektors (30) in der Nähe eines Vorderkantenbereichs (LE) des Niederschlags (D) während der Bildung des Niederschlags.

12. Verfahren nach Anspruch 11, wobei der Kollektor (30) durch Richten einer DC-Plasmalichtbogenbrennerfahne (P) auf den Kollektor in der Nähe der Vorderkante (LE) des Niederschlags (D) erwärmt wird.

Revendications

1. Procédé pour fabriquer un article, comprenant une étape consistant à diriger un jet de métal ou d'alliage atomisé (S) vers un collecteur (30) disposé dans une chambre de pulvérisation (B) et recueillir le jet

sur le collecteur pour façonner un dépôt (D) formant un article, ledit dépôt ayant une région de bord avant (LE) avec une surface externe étant à un angle aigu par rapport à un axe perpendiculaire à un axe dudit jet, dans lequel ledit jet est produit par un atomiseur à balayage (18) faisant osciller ledit jet, **caractérisé en ce que** ledit atomiseur (18) est oscillé dans un cycle d'oscillation comprenant une pluralité d'oscillations successives qui ont des angles d'oscillation croissants par rapport à l'oscillation précédente, et **en ce que** ledit cycle d'oscillation est contrôlé pour fournir ladite région de bord avant (LE) avec ledit angle aigu étant compris entre 10 degrés et 30 degrés.

2. Procédé selon la revendication 1, dans lequel un collecteur rotatif (30) est utilisé et une vitesse de balayage dudit atomiseur (18) est asservie à la vitesse de rotation dudit collecteur de sorte que le temps d'arrêt momentané de l'atomiseur est abaissé lorsque la vitesse de rotation dudit collecteur est accrue.

3. Procédé selon la revendication 1 ou la revendication 2, comprenant la disposition dudit collecteur (30) dans ladite chambre (B) de manière à positionner une surface du collecteur (104) à un angle aigu dans la gamme comprise entre environ 10 et environ 30 degrés par rapport à un axe de référence perpendiculaire audit axe du jet.

4. Procédé selon la revendication 3, dans lequel le collecteur est monté sur un moyen d'arbre qui est orienté à un angle compris entre environ 10 et environ 30 degrés par rapport à un axe de référence perpendiculaire audit axe du jet.

5. Procédé selon la revendication 3 ou 4, dans lequel ledit axe de référence est horizontal.

6. Procédé selon la revendication 3, dans lequel la surface du collecteur (104) est un cône effilé.

7. Procédé selon l'une quelconque des revendications 1 à 6, dans lequel une pression partielle de gaz dans ladite chambre (B) est maintenue entre 13,33 hPas (10 torr) et moins de 533,2 hPas (400 torr) lorsque le jet (S) est dirigé vers le collecteur (30) pour augmenter la température du jet dans la chambre de pulvérisation efficace pour réduire les fissures au niveau d'une région interne du dépôt sur le collecteur et/ou la porosité du dépôt sur le collecteur en vertu d'une réduction du gaz piégé.

8. Procédé selon l'une quelconque des revendications 1 à 7, comprenant les étapes consistant à :

faire tourner le collecteur,

faire bouger ledit atomiseur (18) et ledit collecteur (30) l'un par rapport à l'autre dans la direction de l'axe de rotation du collecteur, et répéter ledit cycle d'oscillation lors de la rotation du collecteur et le collecteur et l'atomiseur sont déplacés l'un par rapport à l'autre pour recueillir le jet sur le collecteur pour façonner ledit dépôt (D) formant l'article.

9. Procédé selon la revendication 8, dans lequel les angles d'oscillation sont contrôlés pour avoir la surface externe de ladite région de bord avant (LE) du métal ou alliage déposé audit angle aigu.

10. Procédé selon la revendication 8 ou 9, dans lequel chaque oscillation se produit pendant une rotation du collecteur (30) quelle que soit la vitesse de rotation du collecteur.

11. Procédé selon l'une quelconque des revendications 1 à 10, consistant à :

chauffer le collecteur (30) proche d'une région de bord avant (LE) dudit dépôt (D) lors du formage dudit dépôt.

12. Procédé selon la revendication 11, dans lequel le collecteur (30) est chauffé en dirigeant un panache de chalumeau à arc plasma à courant continu (P) vers le collecteur proche du bord avant (LE) dudit dépôt (D).

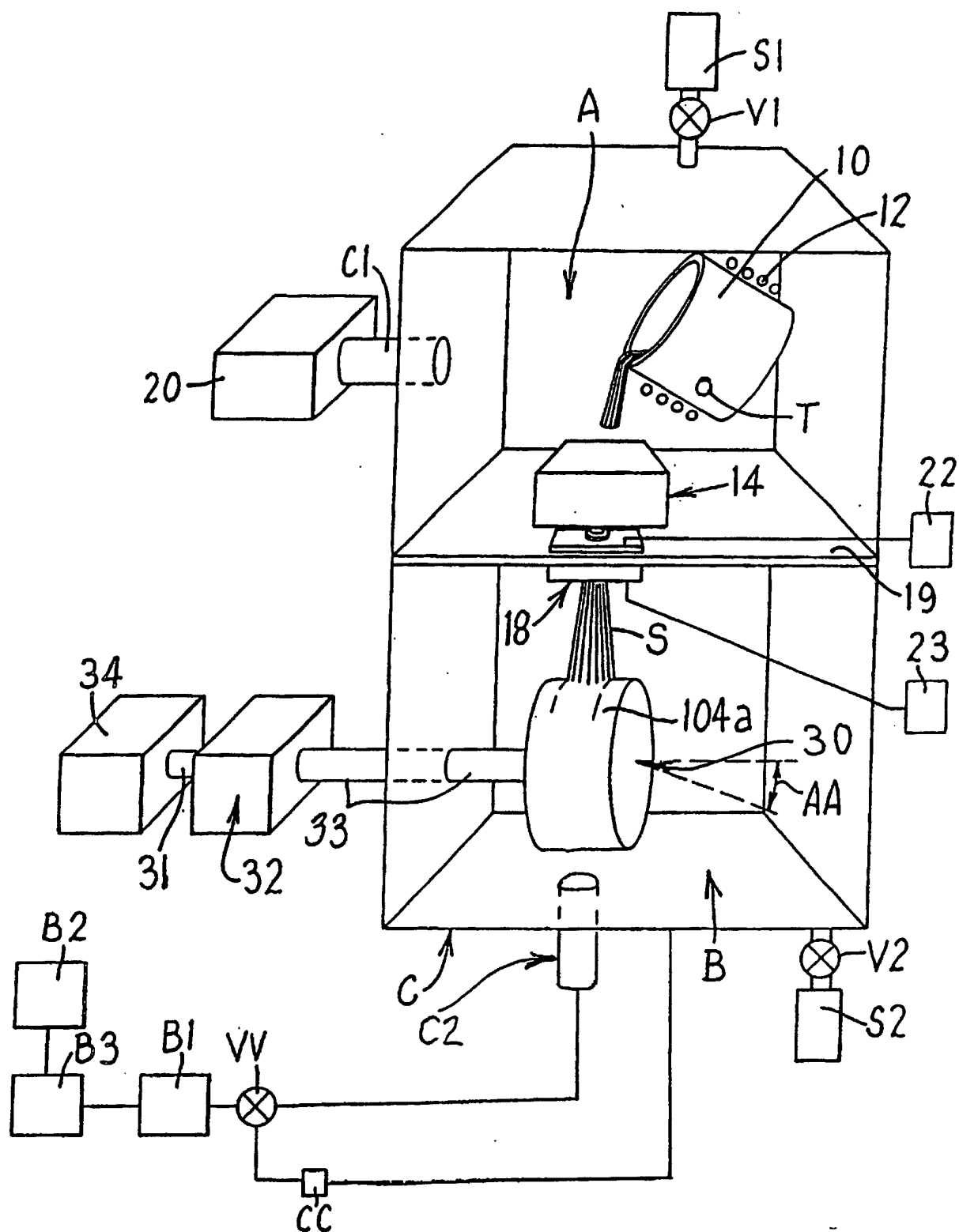


FIG. 1

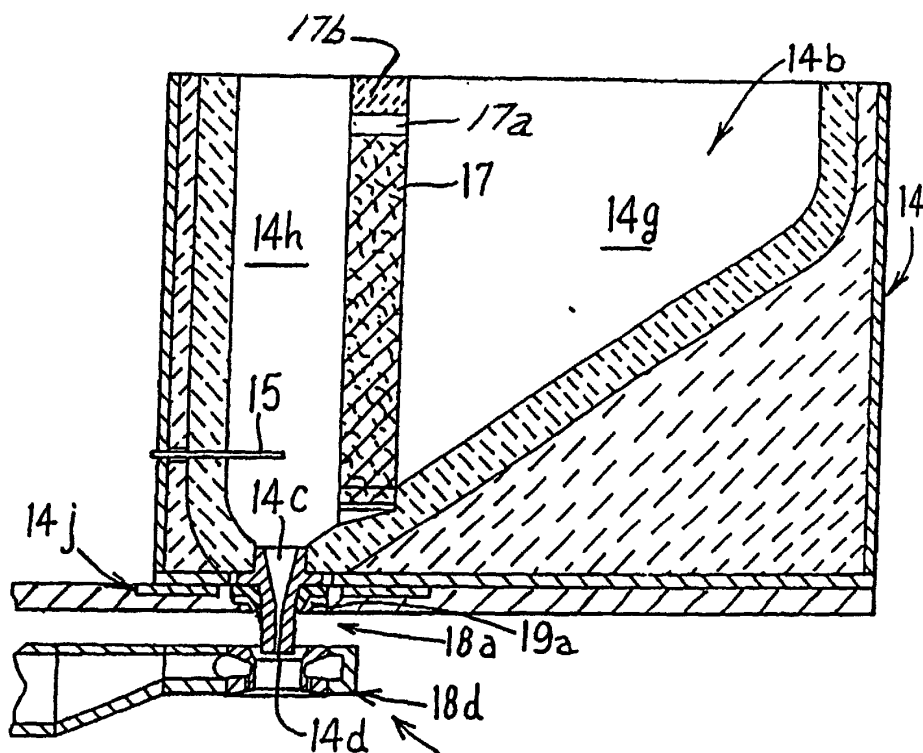


FIG. 2

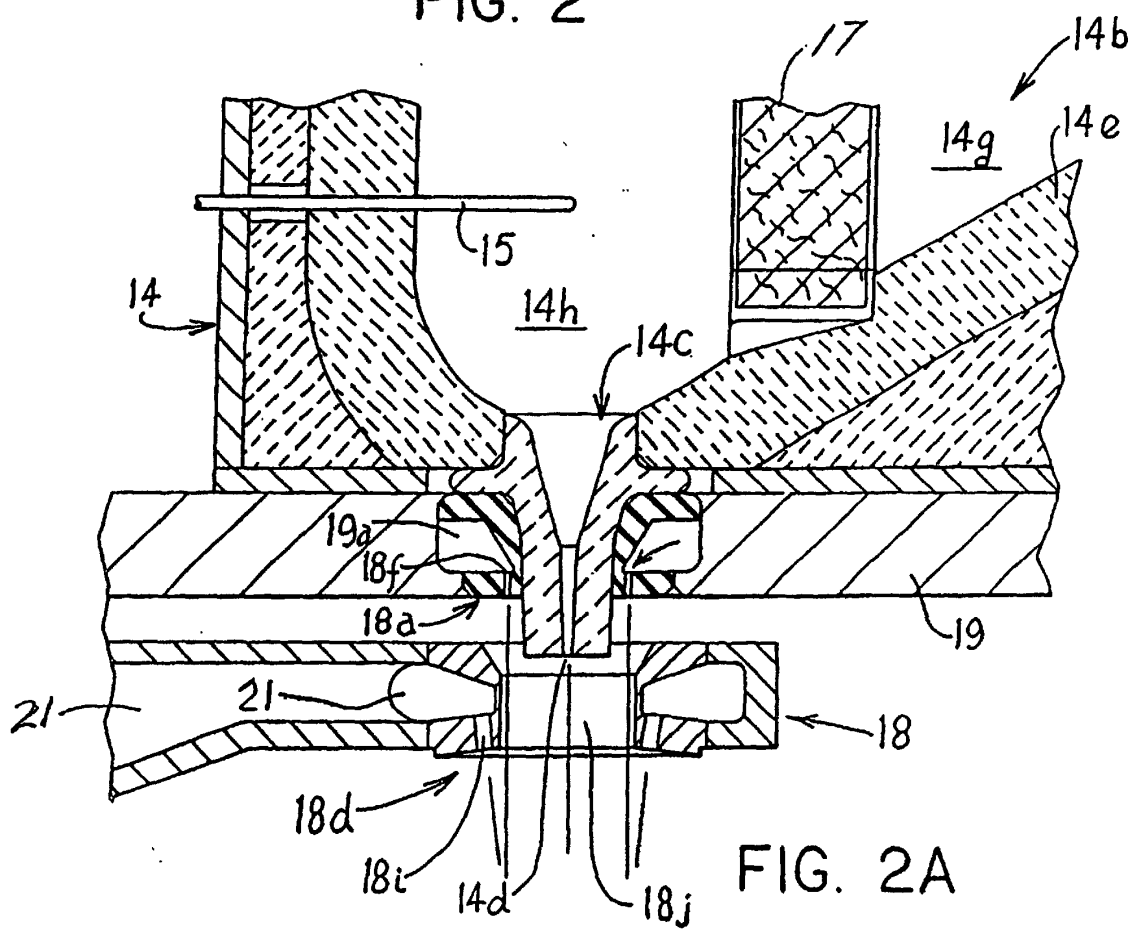


FIG. 2A

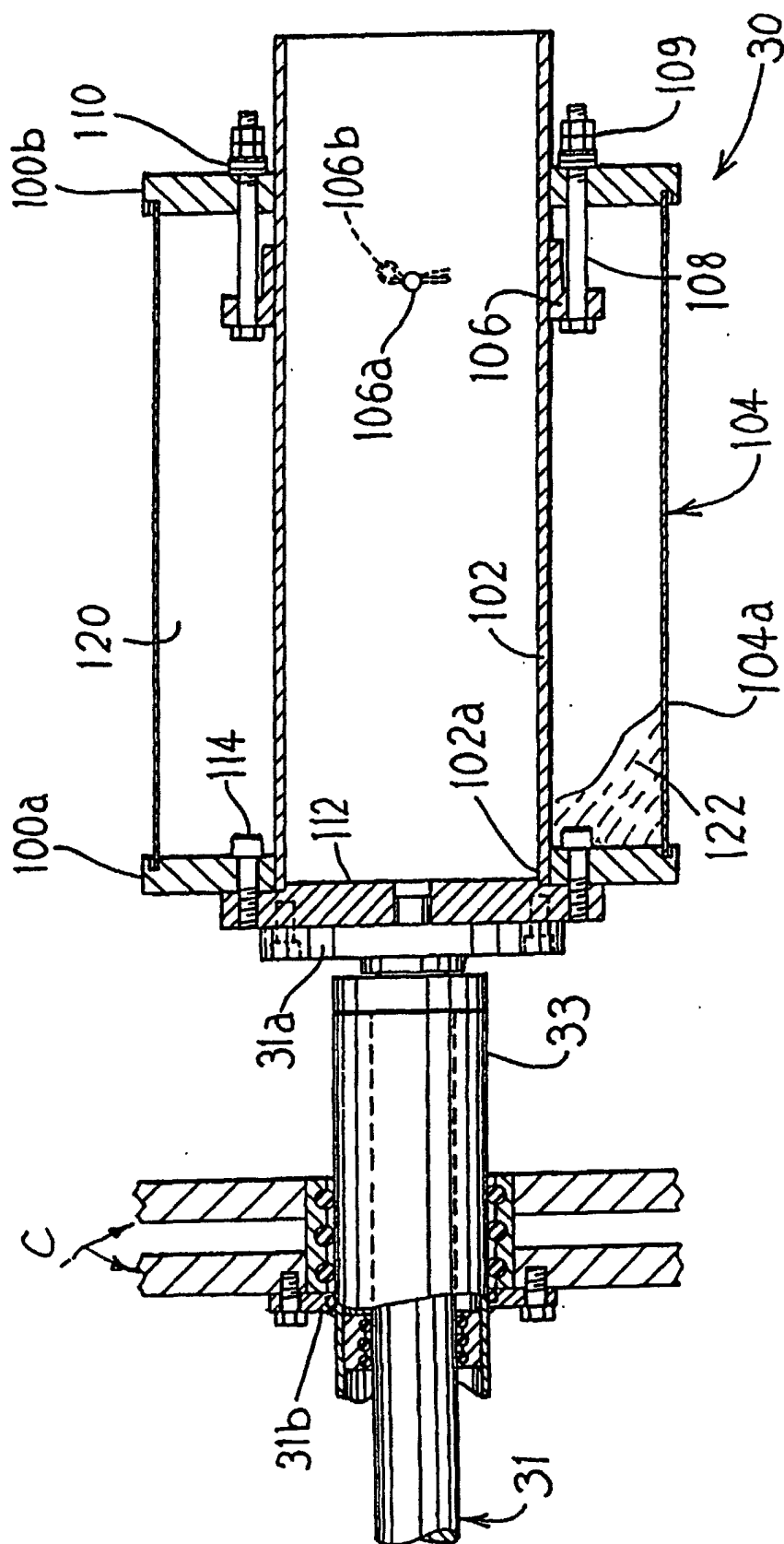
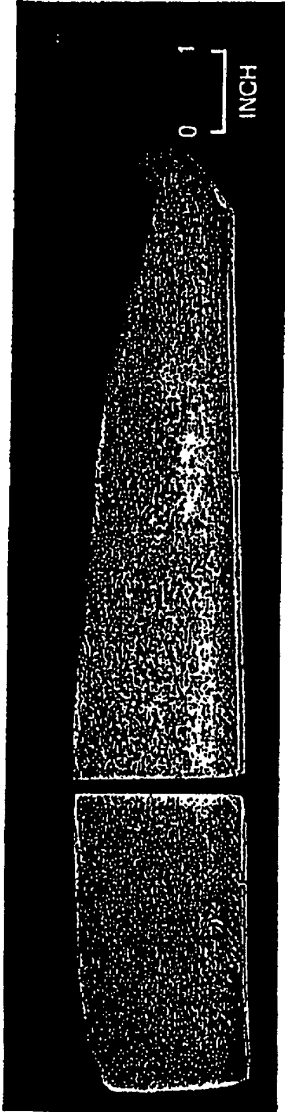
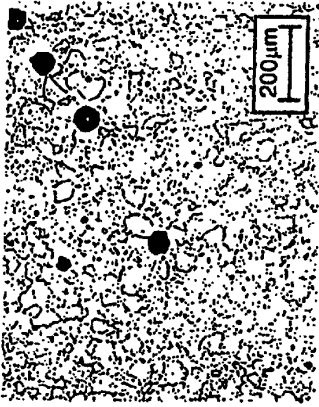


FIG. 3



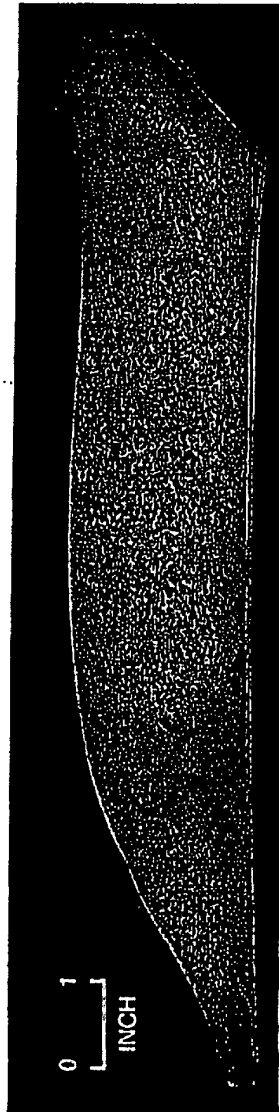
S/N A2-546, 730 Torr Processed

FIG. 4BI



ASTM 6.5 Grain Size / 2.1% Porosity

FIG. 4B2



S/N A2-580, 400 Torr Processed

FIG. 4AI



ASTM 6.5 Grain Size / 0.9% Porosity

FIG. 4A2

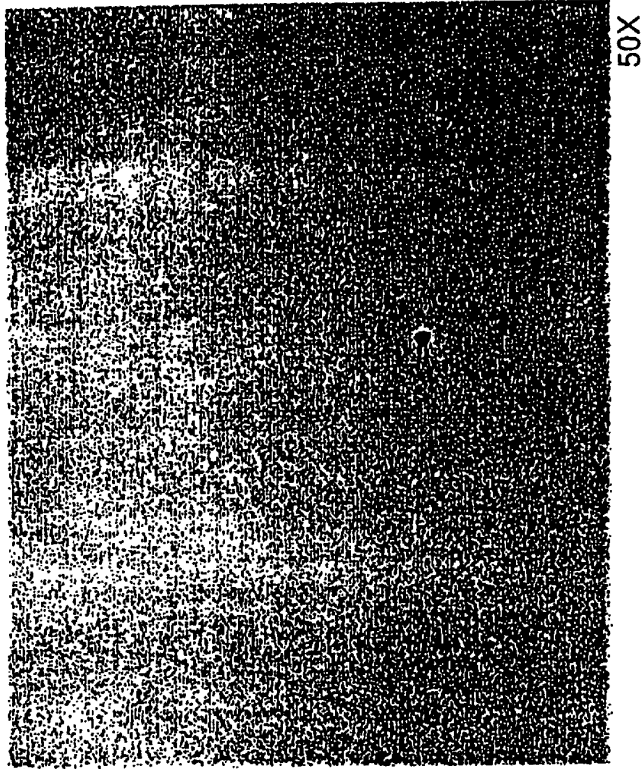


FIG. 5A

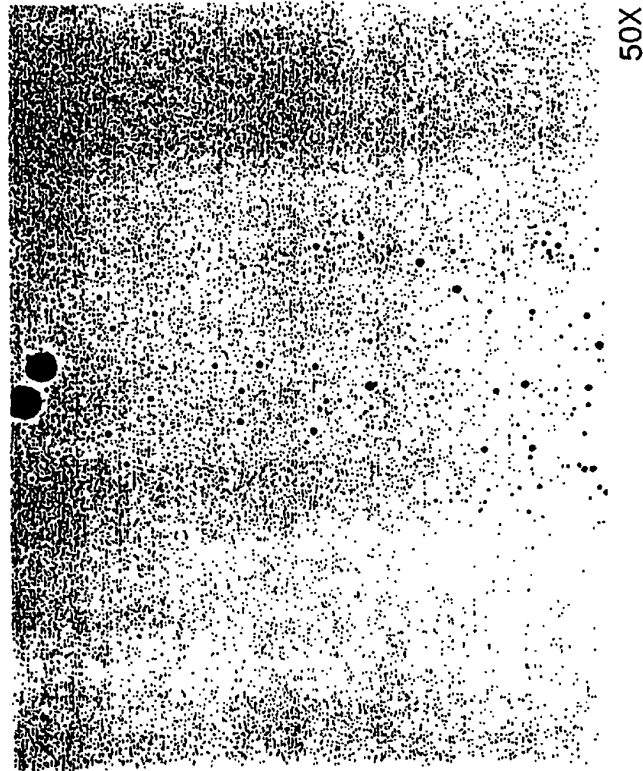


FIG. 5B

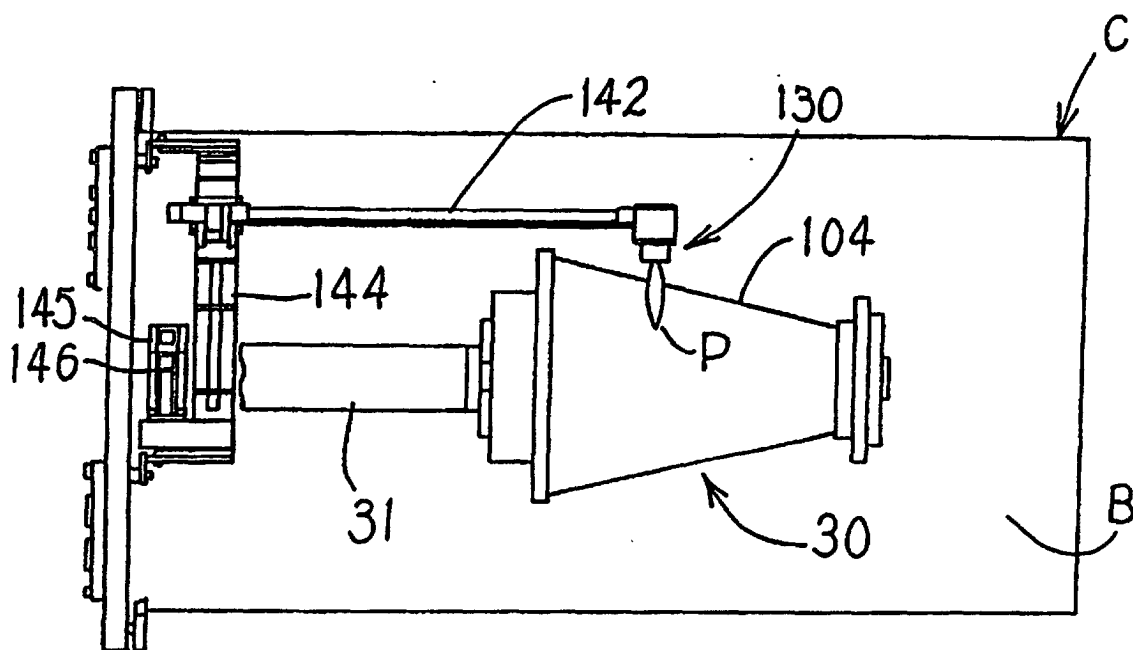


FIG. 6B

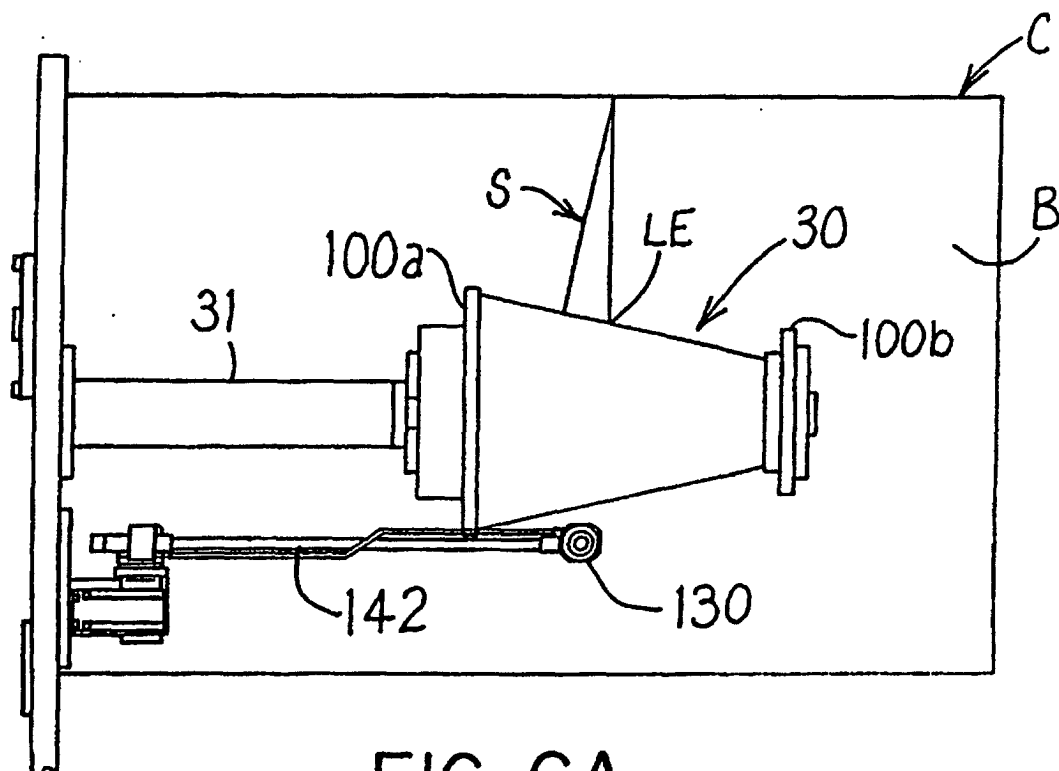


FIG. 6A

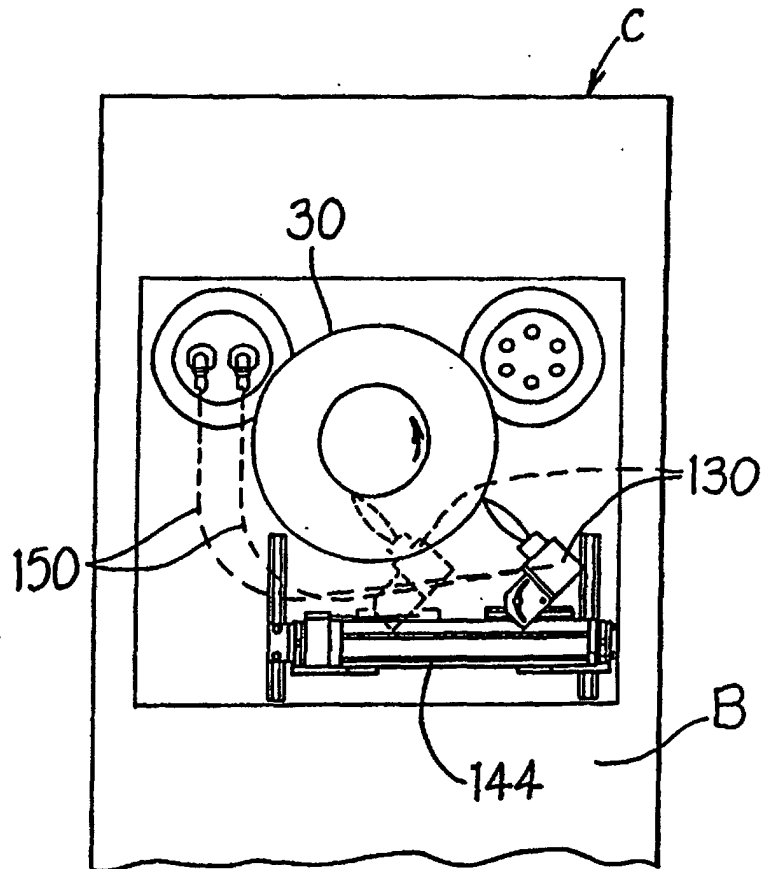


FIG. 6C

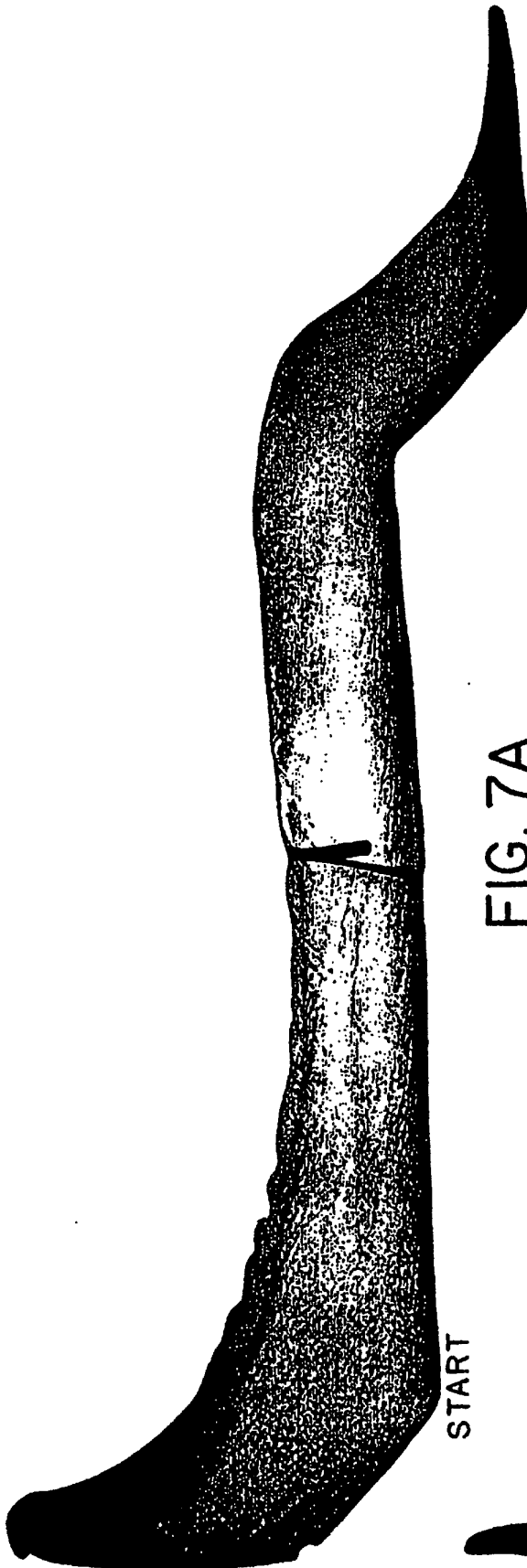


FIG. 7A

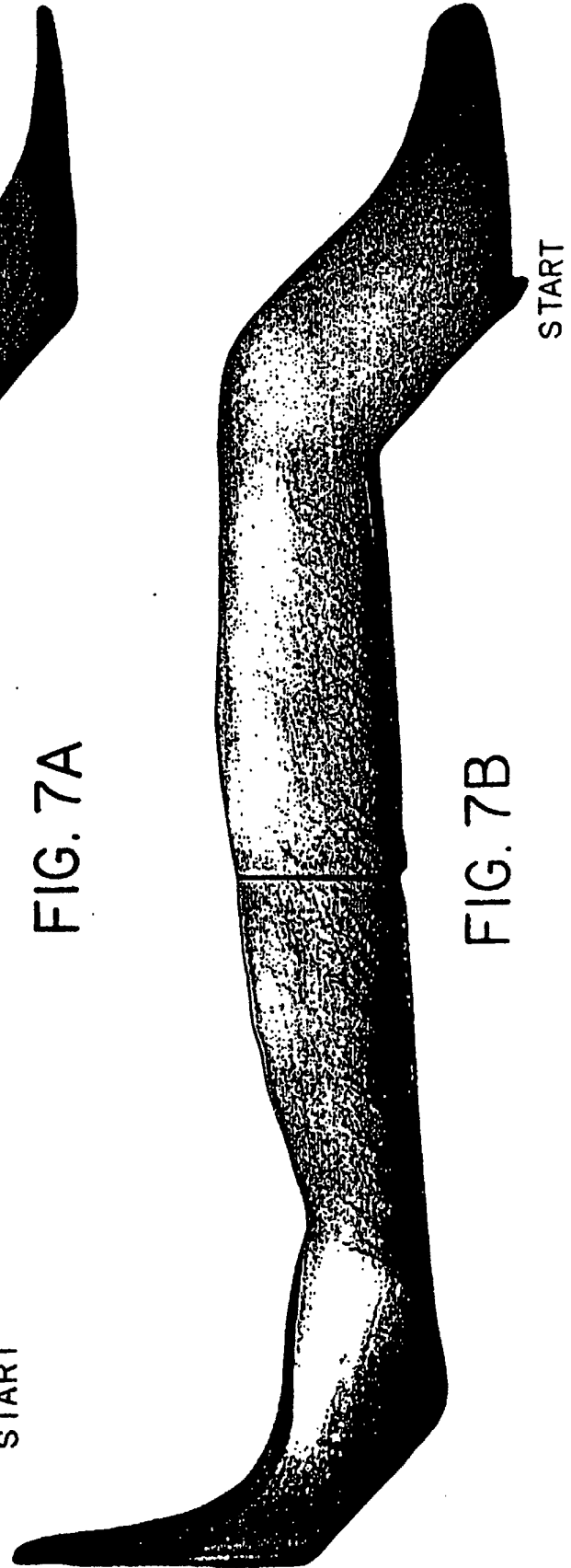


FIG. 7B

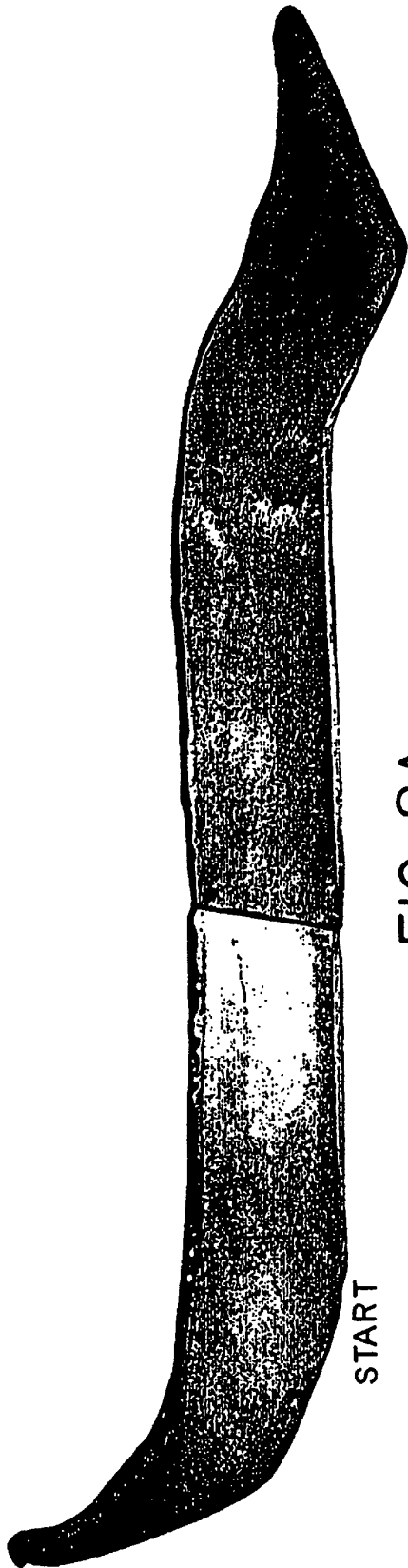


FIG. 8A

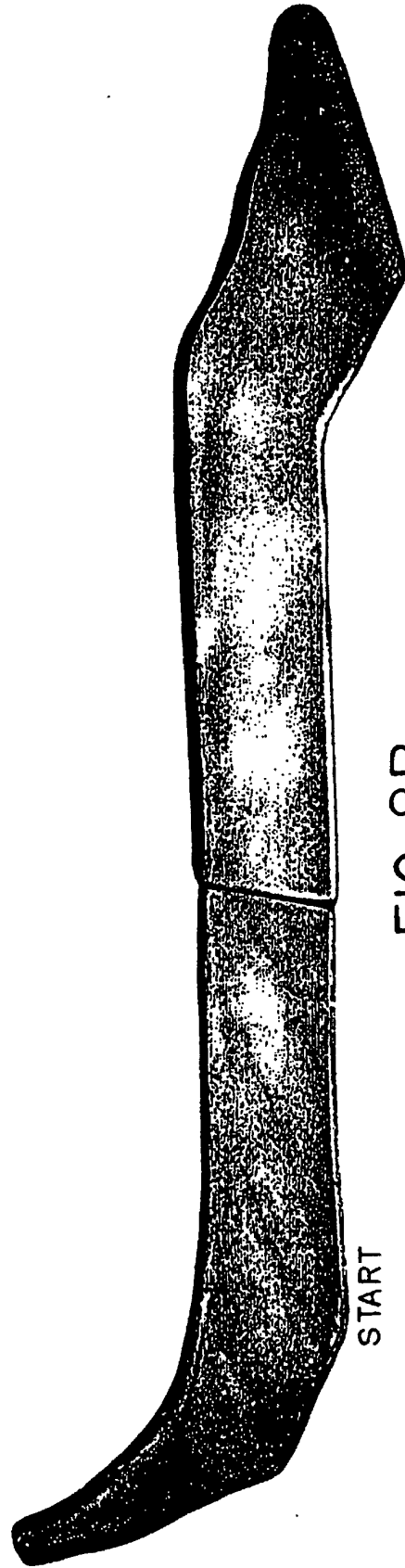
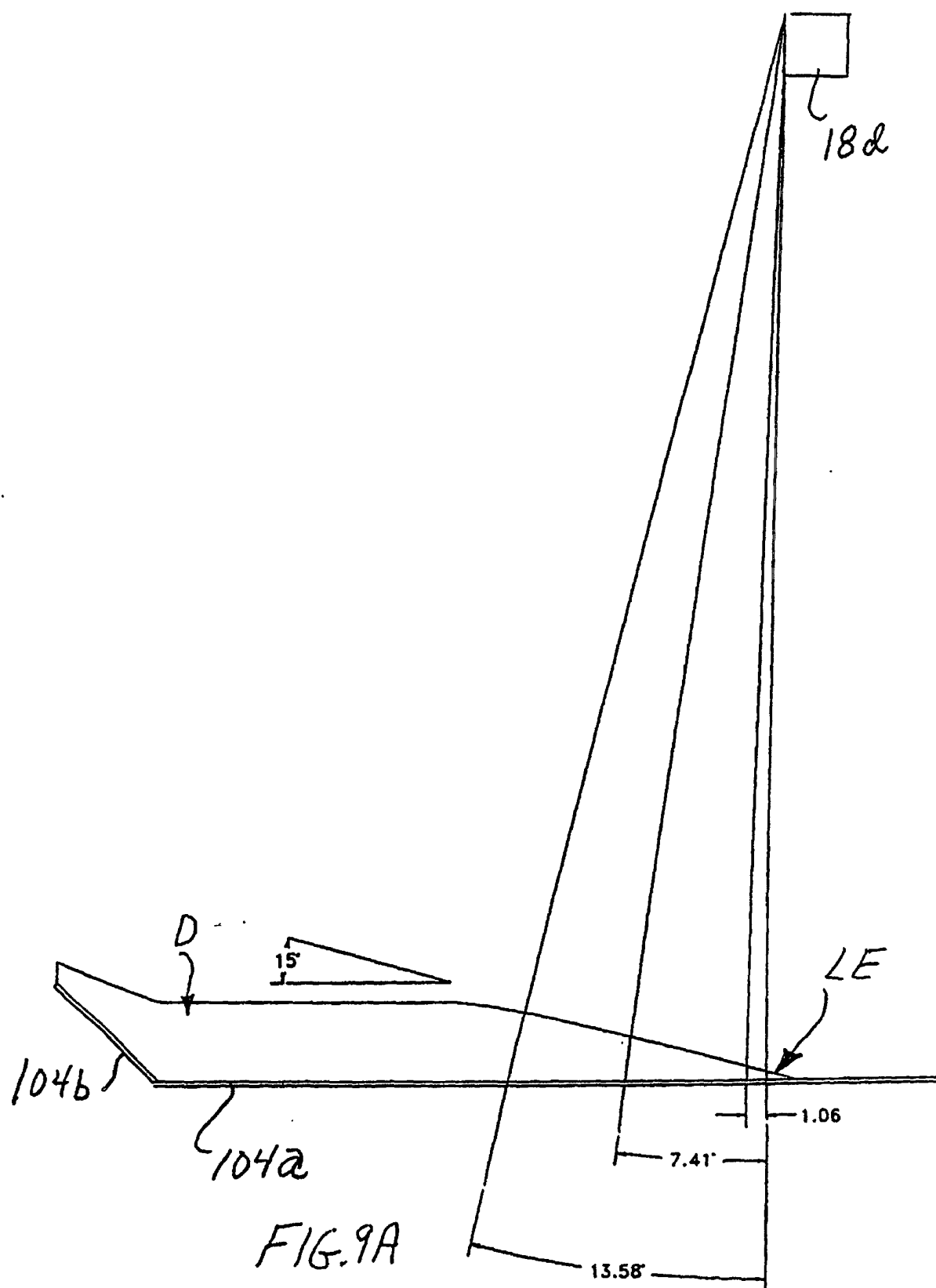


FIG. 8B



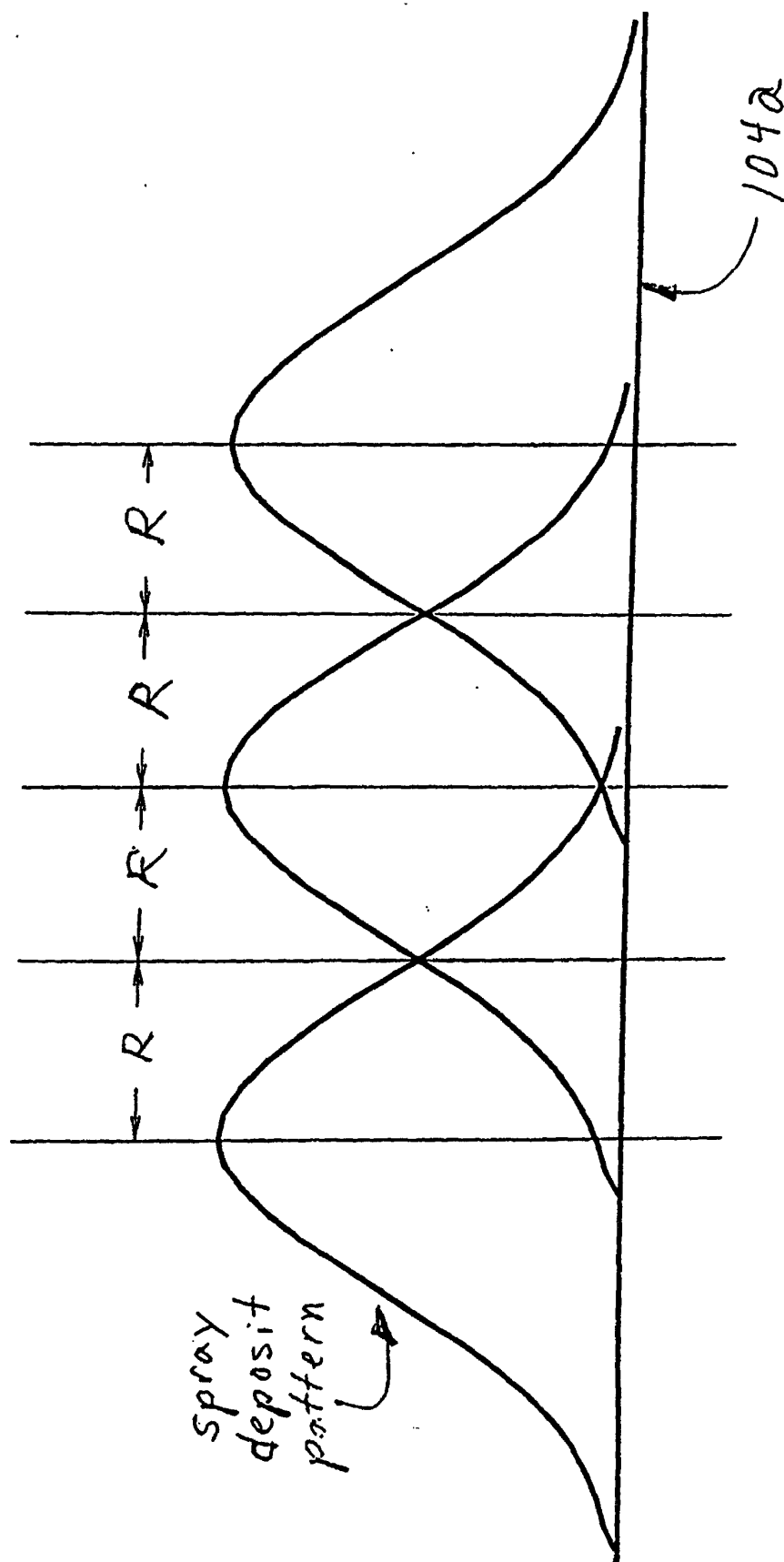


FIG. 9B