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# DESCRIPTION

Description

## FIELD OF THE INVENTION

**[0001]** The present invention relates to products made or derived from tobacco, or that otherwise incorporate tobacco, and are intended for human consumption.

## BACKGROUND

**[0002]** Cigarettes, cigars and pipes are popular smoking articles that employ tobacco in various forms. Such smoking articles are used by heating or burning tobacco, and aerosol (e.g., smoke) is inhaled by the smoker. Tobacco may be enjoyed in a so-called "smokeless" form. Particularly popular smokeless tobacco products are employed by inserting some form of processed tobacco or tobacco-containing formulation into the mouth of the user.

**[0003]** Conventional formats for such smokeless tobacco products include moist snuff, snus, and chewing tobacco, which are typically formed almost entirely of particulate, granular, or shredded tobacco, and which are either portioned by the user or presented to the user in individual portions, such as in single-use pouches or sachets. Other traditional forms of smokeless products include compressed or agglomerated forms, such as plugs, tablets, or pellets. Alternative product formats, such as tobacco-containing gums and mixtures of tobacco with other plant materials, are also known. See for example, the types of smokeless tobacco formulations, ingredients, and processing methodologies set forth in US Pat. Nos. 1,376,586 to Schwartz; 4,513,756 to Pittman et al.; 4,528,993 to Sensabaugh, Jr. et al.; 4,624,269 to Story et al.; 4,991,599 to Tibbetts; 4,987,907 to Townsend; 5,092,352 to Sprinkle, III et al.; 5,387,416 to White et al.; 6,668,839 to Williams; 6,834,654 to Williams; 6,953,040 to Atchley et al.; 7,032,601 to Atchley et al.; and 7,694,686 to Atchley et al.; US Pat. Pub. Nos. 2004/0020503 to Williams; 2005/0115580 to Quinter et al.; 2006/0191548 to Strickland et al.; 2007/0062549 to Holton, Jr. et al.; 2007/0186941 to Holton, Jr. et al.; 2007/0186942 to Strickland et al.; 2008/0029110 to Dube et al.; 2008/0029116 to Robinson et al.; 2008/0173317 to Robinson et al.; 2008/0209586 to Neilsen et al.; 2009/0065013 to Essen et al.; and 2010/0282267 to Atchley, as well as WO2004/095959 to Arnarp et al.

**[0004]** Smokeless tobacco product configurations that combine tobacco material with various binders and fillers have been proposed more recently, with example product formats including lozenges, pastilles, gels, extruded forms, and the like. See, for example, the types of products

described in US Patent App. Pub. Nos. 2008/0196730 to Engstrom et al.; 2008/0305216 to Crawford et al.; 2009/0293889 to Kumar et al.; 2010/0291245 to Gao et al.; 2011/0139164 to Mua et al.; 2012/0037175 to Cantrell et al.; 2012/0055494 to Hunt et al.; 2012/0138073 to Cantrell et al.; 2012/0138074 to Cantrell et al.; 2013/0074855 to Holton, Jr.; 2013/0074856 to Holton, Jr.; 2013/0152953 to Mua et al.; 2013/0274296 to Jackson et al.; 2015/0068545 to Moldoveanu et al.; 2015/0101627 to Marshall et al.; and 2015/0230515 to Lampe et al. Additionally, all-white snus portions are growing in popularity, and offer a discrete and aesthetically pleasing alternative to traditional snus. Such modern "white" pouched products may include a bleached tobacco or may be tobacco-free. Through the years, various treatment methods and additives have been proposed for altering the overall character or nature of tobacco materials utilized in tobacco compositions. For example, additives or treatment processes are sometimes utilized in order to alter the chemistry or sensory properties of the tobacco material, or in the case of smokable tobacco materials, to alter the chemistry or sensory properties of mainstream smoke generated by smoking articles including the tobacco material. In some cases, a heat treatment process can be used to impart a desired color or visual character to the tobacco material, desired sensory properties to the tobacco material, or a desired physical nature or texture to the tobacco material. Document US2020/196658 A1 discloses a method of preparing a whitened tobacco material for incorporation within an oral product.

**[0005]** Methods for altering the character and nature of tobacco (and tobacco compositions and formulations) useful in aerosol delivery systems or oral products are provided in the present disclosure.

## **BRIEF SUMMARY**

**[0006]** The present disclosure provides a method of processing a tobacco material to modify the color of the tobacco material, specifically to provide a tobacco material that is lightened in color (i.e., "whitened"). The whitened tobacco material can be used in oral products to give materials adapted for oral use with a whitened appearance.

**[0007]** According to the invention, a method for whitening a tobacco material is provided, the method comprising (i) extracting a tobacco material with a first extraction solution to provide a tobacco solids material and a tobacco extract; (ii) cooking the tobacco solids material in an alkaline cooking liquid comprising sodium sulfide having a pH of greater than 11 to form a tobacco pulp; (iii) treating the tobacco pulp with a first acid to lower the pH of the tobacco pulp and provide a neutralized tobacco pulp; (iv) extracting the neutralized tobacco pulp with a first aqueous solution comprising a first chelating agent to provide an extracted tobacco pulp; and (v) bleaching the extracted tobacco pulp with a bleaching solution to provide a whitened tobacco material. In some embodiments, the method of preparing a whitened tobacco material can further include (vi) treating the bleached tobacco material with a second acid to lower the pH of the bleached tobacco material and provide a neutralized tobacco material; (vii) extracting the neutralized

tobacco material with a second aqueous solution comprising a second chelating agent to provide an extracted tobacco material; and (viii) bleaching the extracted tobacco material with a second bleaching solution comprising a second oxidative agent to provide a whitened tobacco material. In various embodiments, the whitened tobacco material is characterized by an International Organization for Standardization (ISO) brightness of at least about 40%. The whitened tobacco materials provided herein can be used in an oral product, for example. In various embodiments, the bleached tobacco material is dried to a moisture content of less than about 30 percent moisture on a wet basis.

#### **BRIEF DESCRIPTION OF THE DRAWINGS**

**[0008]** Having thus described aspects of the disclosure in the foregoing general terms, reference will now be made to the accompanying drawings, which are not necessarily drawn to scale. The drawings are exemplary only, and should not be construed as limiting the disclosure.

FIG. 1 is a front perspective view illustrating a pouched product according to an embodiment;

FIG. 2 is a flow chart illustrating the general steps for preparing a whitened tobacco material according to an embodiment; and

FIG. 3 is a flow chart illustrating the general steps for an embodiment of the bleaching operation step 120 depicted in FIG. 2.

#### **DETAILED DESCRIPTION**

**[0009]** Aspects of the present disclosure now will be described more fully hereinafter. This invention may, however, be embodied in many different forms and should not be construed as limited to the embodiments set forth herein; rather, these embodiments are provided so that this disclosure will be thorough and complete, and will fully convey the scope of the invention to those skilled in the art. As used in this specification and the claims, the singular forms "a," "an," and "the" include plural referents unless the context clearly dictates otherwise. Reference to "dry weight percent" or "dry weight basis" refers to weight on the basis of dry ingredients (i.e., all ingredients except water).

**[0010]** In various embodiments, the whitening processes described herein include the following steps: hot water extraction, Kraft cook at a pH of 11 or greater, and a bleaching sequence containing an acid stage, a chelating stage, a peroxide stage, a second acid stage, a second chelating stage, and a second peroxide stage. As described in more detail below, the Kraft process breaks the bonds in the tobacco material that link lignin, hemicellulose, and cellulose. Following the Kraft process, the tobacco material is subjected to an acid stage (A), wherein the

tobacco material is treated with an acid to neutralize the tobacco material after the Kraft pulping process to a pH in the range of about 5 to about 11. Following the acid stage, the tobacco material is extracted with water and at least one chelating agent in a chelating stage (Q), which is capable of removing transition metals from the tobacco material. Following the chelating stage, the tobacco material is subjected to an oxidative bleaching stage (P) (e.g., bleaching with a peroxide (e.g., hydrogen peroxide)). In certain embodiments, the acid stage (A), chelating stage (Q), and peroxide stage (P) are then repeated, as described in more detail below.

**[0011]** The whitened tobacco material can be used in combustible aerosol delivery systems, such as cigarettes, cigarillos, cigars, and tobacco for pipes or for roll-your-own or for make-your-own cigarettes, or non-combustible aerosol delivery systems that release compounds from an aerosol-generating material without combusting the aerosol-generating material, such as electronic cigarettes, tobacco heating products, and hybrid systems to generate aerosol using a combination of aerosol-generating materials. Alternatively, the whitened tobacco material can be used as a component of aerosol-free delivery systems that deliver an active ingredient or flavor to a user orally, nasally, transdermally or in another way without forming an aerosol, including but not limited to, lozenges, gums, patches, articles comprising inhalable powders, and oral products such as oral tobacco which includes snus or moist snuff, wherein the active ingredient may or may not comprise nicotine.

**[0012]** The whitened tobacco material can be used, for example, in oral products configured for oral use. The term "configured for oral use" as used herein means that the product is provided in a form such that during use, saliva in the mouth of the user causes one or more of the components of the product (e.g., flavoring agents and/or nicotine) to pass into the mouth of the user. In one embodiment, the product is adapted to deliver components to a user through mucous membranes in the user's mouth and, in addition, said component is an active ingredient (including, but not limited to, for example, nicotine) that can be absorbed through the mucous membranes in the mouth when the product is used. In some embodiments, the product may be adapted to deliver flavor components to a user in addition to the active ingredient.

**[0013]** In one embodiment, the product comprising the composition of the present disclosure is in the form of a composition disposed within a moisture-permeable container (e.g., a water-permeable pouch). Such compositions in the water-permeable pouch format are typically used by placing one pouch containing the composition in the mouth of a human subject/user. Generally, the pouch is placed somewhere in the oral cavity of the user, for example under the lips, in the same way as moist snuff products are generally used. The pouch typically is not chewed or swallowed. Exposure to saliva then causes some of the components of the composition therein (e.g., flavoring agents and/or active ingredients) to pass through e.g., the water-permeable pouch and provide the user with flavor and satisfaction, and the user is not required to spit out any portion of the composition. After about 10 minutes to about 60 minutes, typically about 15 minutes to about 45 minutes, of use/enjoyment, substantial amounts of the composition have been absorbed through oral mucosa of the human subject, and the pouch

may be removed from the mouth of the human subject for disposal.

**[0014]** Certain embodiments will be described with reference to Figure 1 of the accompanying drawings, and these described embodiments involve oral products having an outer pouch and containing a whitened tobacco material. As explained in greater detail below, such embodiments are provided by way of example only, and the oral product can include tobacco compositions in other forms.

**[0015]** Referring to Figure 1, there is shown a first embodiment of an oral product 10. The oral product 10 includes a moisture-permeable container in the form of a pouch 20, which contains a material 15 comprising a whitened tobacco material of a type described herein. The oral product also may optionally comprise, in certain embodiments, a plurality of microcapsules dispersed within the tobacco filler material 15, the microcapsules containing a component (e.g., a flavorant) such as described in greater detail below.

**[0016]** The present disclosure provides a whitened tobacco composition, oral products incorporating such whitened tobacco compositions, and methods for preparing a whitened tobacco composition and for incorporating such compositions within oral products. As used herein, the term "whitened" refers to a composition comprising a tobacco material that has been treated to remove some degree of color therefrom. Thus, a "whitened" tobacco material that is treated according to the methods described herein is visually lighter in hue than an untreated tobacco material. The whitened tobacco composition of the invention can be used as a component of an oral product composition, such as loose moist snuff, loose dry snuff, chewing tobacco, pelletized tobacco pieces, extruded or formed tobacco strips, pieces, rods, or sticks, finely divided ground powders, finely divided or milled agglomerates of powdered pieces and components, flake-like pieces, molded processed tobacco pieces, pieces of tobacco-containing gum, rolls of tape-like films, readily water-dissolvable or water-dispersible films or strips, or capsule-like materials.

**[0017]** As illustrated at operation 90 of Fig. 2, the tobacco whitening process described herein includes providing a tobacco material. Tobaccos used in the tobacco compositions of the invention may vary. In certain embodiments, tobaccos that can be employed include flue-cured or Virginia (e.g., K326), burley, sun-cured (e.g., Indian Kumool and Oriental tobaccos, including Katerini, Prelip, Komotini, Xanthi and Yambol tobaccos), Maryland, dark, dark-fired, dark air cured (e.g., Passanda, Cubano, Jatin and Bezuki tobaccos), light air cured (e.g., North Wisconsin and Galpao tobaccos), Indian air cured, Red Russian and *Rustica* tobaccos, as well as various other rare or specialty tobaccos and various blends of any of the foregoing tobaccos. Descriptions of various types of tobaccos, growing practices and harvesting practices are set forth in Tobacco Production, Chemistry and Technology, Davis et al. (Eds.) (1999), which is incorporated herein by reference. Various representative other types of plants from the *Nicotiana* species are set forth in Goodspeed, The Genus *Nicotiana*, (Chonica Botanica) (1954); US Pat. Nos. 4,660,577 to Sensabaugh, Jr. et al.; 5,387,416 to White et al. and 7,025,066 to Lawson et al.; US Patent Appl. Pub. Nos. 2006/0037623 to Lawrence, Jr. and 2008/0245377 to Marshall et al.

**[0018]** Example *Nicotiana* species include *N. tabacum*, *N. rustic a*, *N. alata*, *N. arentsii*, *N. excelsior*, *N. forgetiana*, *N. glauca*, *N. glutinosa*, *N. gossei*, *N. kawakamii*, *N. knightiana*, *N. langsdorffi*, *N. otophora*, *N. setchelli*, *N. sylvestris*, *N. tomentosa*, *N. tomentosiformis*, *N. undulata*, *N. x sanderae*, *N. africana*, *N. amplexicaulis*, *N. benavidesii*, *N. bonariensis*, *N. debneyi*, *N. longiflora*, *N. maritima*, *N. megalosiphon*, *N. occidentalis*, *N. paniculata*, *N. plumbaginifolia*, *N. raimondii*, *N. rosulata*, *N. simulans*, *N. stocktonii*, *N. suaveolens*, *N. umbratica*, *N. velutina*, *N. wigandioides*, *N. acaulis*, *N. acuminata*, *N. attenuata*, *N. benthamiana*, *N. cavicola*, *N. clevelandii*, *N. cordifolia*, *N. corymbosa*, *N. fragrans*, *N. goodspeedii*, *N. linearis*, *N. miersii*, *N. nudicaulis*, *N. obtusifolia*, *N. occidentalis* subsp. *Hersperis*, *N. pauciflora*, *N. petunioides*, *N. quadrivalvis*, *N. repanda*, *N. rotundifolia*, *N. solanifolia*, and *N. spegazzinii*.

**[0019]** *Nicotiana* species can be derived using genetic-modification or crossbreeding techniques (e.g., tobacco plants can be genetically engineered or crossbred to increase or decrease production of components, characteristics or attributes). See, for example, the types of genetic modifications of plants set forth in US Pat. Nos. 5,539,093 to Fitzmaurice et al.; 5,668,295 to Wahab et al.; 5,705,624 to Fitzmaurice et al.; 5,844,119 to Weigl; 6,730,832 to Dominguez et al.; 7,173,170 to Liu et al.; 7,208,659 to Colliver et al. and 7,230,160 to Benning et al.; US Patent Appl. Pub. No. 2006/0236434 to Conkling et al.; and PCT WO 2008/103935 to Nielsen et al. See, also, the types of tobaccos that are set forth in US Pat. Nos. 4,660,577 to Sensabaugh, Jr. et al.; 5,387,416 to White et al.; and 6,730,832 to Dominguez et al. Most preferably, the tobacco materials are those that have been appropriately cured and aged. Especially preferred techniques and conditions for curing flue-cured tobacco are set forth in Nestor et al., *Beitrag Tabakforsch. Int.*, 20 (2003) 467-475 and US Pat. No. 6,895,974 to Peele. Representative techniques and conditions for air curing tobacco are set forth in Roton et al., *Beitrag Tabakforsch. Int.*, 21 (2005) 305-320 and Staaf et al., *Beitrag Tabakforsch. Int.*, 21 (2005) 321-330. Certain types of unusual or rare tobaccos can be sun cured. Manners and methods for improving the smoking quality of Oriental tobaccos are set forth in US Pat. No. 7,025,066 to Lawson et al.

**[0020]** Representative Oriental tobaccos include katerini, prelip, komotini, xanthi and yambol tobaccos. Tobacco compositions including dark air cured tobacco are set forth in US Patent Appl. Pub. No. 2008/0245377 to Marshall et al. See also, types of tobacco as set forth, for example, in US Patent Appl. Pub. No. 2011/0247640 to Beeson et al.

**[0021]** The *Nicotiana* species can be selected for the content of various compounds that are present therein. For example, plants can be selected on the basis that those plants produce relatively high quantities of one or more of the compounds desired to be isolated therefrom. In certain embodiments, plants of the *Nicotiana* species (e.g., *Galpao commun* tobacco) are specifically grown for their abundance of leaf surface compounds. Tobacco plants can be grown in greenhouses, growth chambers, or outdoors in fields, or grown hydroponically.

**[0022]** Various parts or portions of the plant of the *Nicotiana* species can be employed. For

example, virtually all of the plant (e.g., the whole plant) can be harvested, and employed as such. Alternatively, various parts or pieces of the plant can be harvested or separated for further use after harvest. For example, the flower, leaves, stem, stalk, roots, seeds, and various combinations thereof, can be isolated for further use or treatment. In some embodiments, the tobacco material subjected to the treatments set forth herein is Rustica stems in milled form.

**[0023]** The post-harvest processing of the plant or portion thereof can vary. After harvest, the plant, or portion thereof, can be used in a green form (e.g., the plant or portion thereof can be used without being subjected to any curing process). For example, the plant or portion thereof can be used without being subjected to significant storage, handling or processing conditions. In certain situations, it is advantageous for the plant or portion thereof be used virtually immediately after harvest. Alternatively, for example, a plant or portion thereof in green form can be refrigerated or frozen for later use, freeze dried, subjected to irradiation, yellowed, dried, cured (e.g., using air drying techniques or techniques that employ application of heat), heated or cooked (e.g., roasted, fried or boiled), or otherwise subjected to storage or treatment for later use.

**[0024]** The harvested plant or portion thereof can be physically processed. The plant or portion thereof can be separated into individual parts or pieces (e.g., the leaves can be removed from the stems, and/or the stems and leaves can be removed from the stalk). The harvested plant or individual parts or pieces can be further subdivided into parts or pieces (e.g., the leaves can be shredded, cut, comminuted, pulverized, milled or ground into pieces or parts that can be characterized as filler-type pieces, granules, particulates or fine powders). The plant, or parts thereof, can be subjected to external forces or pressure (e.g., by being pressed or subjected to roll treatment). When carrying out such processing conditions, the plant or portion thereof can have a moisture content that approximates its natural moisture content (e.g., its moisture content immediately upon harvest), a moisture content achieved by adding moisture to the plant or portion thereof, or a moisture content that results from the drying of the plant or portion thereof. For example, powdered, pulverized, ground or milled pieces of plants or portions thereof can have moisture contents of less than about 25 weight percent, often less than about 20 weight percent, and frequently less than about 15 weight percent.

**[0025]** Tobacco compositions intended to be used in an oral form such as that in Figure 1 may incorporate a single type of tobacco (e.g., in a so-called "straight grade" form). For example, the tobacco within a tobacco composition may be composed solely of flue-cured tobacco (e.g., all of the tobacco may be composed, or derived from, either flue-cured tobacco lamina or a mixture of flue-cured tobacco lamina and flue-cured tobacco stem). In one embodiment, the tobacco comprises or is composed solely of sun-cured milled Rustica stems (i.e., *N. rustica* stems). The tobacco within a tobacco composition also may have a so-called "blended" form. For example, the tobacco within a tobacco composition of the present invention may include a mixture of parts or pieces of flue-cured, burley (e.g., Malawi burley tobacco) and Oriental tobaccos (e.g., as tobacco composed of, or derived from, tobacco lamina, or a mixture of

tobacco lamina and tobacco stem).

**[0026]** Portions of the tobaccos within the oral product may have processed forms, such as processed tobacco stems (e.g., cut-rolled stems, cut-rolled-expanded stems or cut-puffed stems), or volume expanded tobacco (e.g., puffed tobacco, such as dry ice expanded tobacco (DIET)). See, for example, the tobacco expansion processes set forth in US Pat. Nos. 4,340,073 to de la Burde et al.; 5,259,403 to Guy et al.; and 5,908,032 to Poindexter, et al.; and 7,556,047 to Poindexter, et al.. In addition, the oral product optionally may incorporate tobacco that has been fermented. See, also, the types of tobacco processing techniques set forth in PCT WO 05/063060 to Atchley et al.

**[0027]** In certain embodiments, the starting tobacco material can include tobacco stems. As used herein, "stem" refers to the long thing part of a tobacco plant from which leaves or flowers grow, and can include the leaves, lamina, and/or flowers. In some embodiments, it can be advantageous to use stalks and/or roots of the tobacco plant. The tobacco stalks and/or roots can be separated into individual pieces (e.g., roots separated from stalks, and/or root parts separated from each other, such as big root, mid root, and small root parts) or the stalks and roots may be combined. By "stalk" is meant the stalk that is left after the leaf (including stem and lamina) has been removed. "Root" and various specific root parts useful according to the present invention may be defined and classified as described, for example, in Mauseth, Botany: An Introduction to Plant Biology: Fourth Edition, Jones and Bartlett Publishers (2009) and Glimn-Lacy et al., Botany Illustrated, Second Edition, Springer (2006). The harvested stalks and/or roots are typically cleaned, ground, and dried to produce a material that can be described as particulate (i.e., shredded, pulverized, ground, granulated, or powdered). As used herein, stalks and/or roots can also refer to stalks and/or roots that have undergone an extraction process to remove water soluble materials. The cellulosic material (i.e., tobacco solids material) remaining after stalks and/or root materials undergo an extraction process can also be useful in the present invention.

**[0028]** Although the tobacco material may comprise material from any part of a plant of the *Nicotiana* species, in certain embodiments, the majority of the material can comprise material obtained from the stems, stalks and/or roots of the plant. For example, in certain embodiments, the tobacco material comprises at least about 90%, at least about 92%, at least about 95%, or at least about 97% by dry weight of at least one of the stem material, the stalk material and the root material of a harvested plant of the *Nicotiana* species.

**[0029]** The tobacco material used in the present invention is typically provided in a shredded, ground, granulated, fine particulate, or powder form. As illustrated at operation 100 of Fig. 2, the tobacco whitening process described herein can include optionally milling a tobacco material. Most preferably, the tobacco is employed in the form of parts or pieces that have an average particle size less than that of the parts or pieces of shredded tobacco used in so-called "fine cut" tobacco products. Typically, the very finely divided tobacco particles or pieces are sized to pass through a screen of about 18 or 16 U.S. sieve size, generally are sized to pass a screen of about 20 U.S. sieve size, often are sized to pass through a screen of about

50 U.S. sieve size, frequently are sized to pass through a screen of about 60 U.S. sieve size, may even be sized to pass through a screen of 100 U.S. sieve size, and further may be sized so as to pass through a screen of 200 U.S. sieve size. It is noted that two scales commonly used to classify particle sizes are the U.S. Sieve Series and Tyler Equivalent. Sometimes these two scales are referred to as Tyler Mesh Size or Tyler Standard Sieve Series. U.S. sieve size is referred to in the present application. If desired, air classification equipment may be used to ensure that small sized tobacco particles of the desired sizes, or range of sizes, may be collected. In one embodiment, the tobacco material is in particulate form sized to pass through an 18 or 16 U.S. sieve size, but not through a 60 U.S. sieve size. If desired, differently sized pieces of granulated tobacco may be mixed together. Typically, the very finely divided tobacco particles or pieces suitable for snus products have a particle size greater than -8 U.S. sieve size, often -8 to +100 U.S. sieve size, frequently -16 to +60 U.S. sieve size. In certain embodiments, the tobacco is provided with an average particle size of about 0.2 to about 2 mm, about 0.5 to about 1.5 mm, about 0.2 to about 1.0 mm, or about 0.75 to about 1.25 mm (e.g., about 1 mm).

**[0030]** The manner by which the tobacco is provided in a finely divided or powder type of form may vary. Preferably, tobacco parts or pieces are comminuted, ground or pulverized into a powder type of form using equipment and techniques for grinding, milling, or the like. Most preferably, the tobacco is relatively dry in form during grinding or milling, using equipment such as hammer mills, cutter heads, air control mills, or the like. For example, tobacco parts or pieces may be ground or milled when the moisture content thereof is less than about 15 weight percent to less than about 5 weight percent. The tobacco material can be processed to provide it in the desired form before and/or after being subjected to the whitening and/or clarification processes described herein.

**[0031]** In some embodiments, the type of tobacco material that is treated (i.e., subjected to the processes described herein) is selected such that it is initially visually lighter in color than other tobacco materials to some degree. Accordingly, one optional step of the method described herein comprises screening various tobacco materials and selecting one or more of the tobacco materials based on their visual appearance (i.e., their "lightness," or "whiteness"). Where conducted, this screening step can, in some embodiments, comprise a visual screening wherein certain tobacco materials (e.g., certain tobacco types) are selected that are visually lighter in hue than other tobacco materials. In some embodiments, the screening can be conducted by means of an automated operation that selects certain tobacco materials based on predetermined characteristics (e.g., having a lightness above a given threshold value). For example, optical instruments (e.g., spectrophotometer/spectroreflectometer) and/or optical sorting equipment can be used for this purpose. Such equipment is available, for example, from Autoelrepho<sup>®</sup> Products, AZ Technology, Hunter Lab, X-Rite, SpecMetrix, and others.

**[0032]** In various embodiments, the tobacco material can be treated to extract one or more soluble components from the tobacco material. As illustrated in Figure 2, this first treatment step can comprise a solvent extraction at operation 105 comprising contacting the tobacco material with a first extraction solution (e.g., water) for a time and at a temperature sufficient to

cause the extraction of one or more components of the tobacco material into the solvent, and separating the extract from the residual tobacco solid material. "Tobacco solid material" as used herein is the solid, residual tobacco material that remains after the liquid component (i.e., tobacco extract) is removed from the material in step 110. "Tobacco extract" as used herein refers to the isolated components of a tobacco material that are extracted from solid tobacco material by a first extraction solution that is brought into contact with the tobacco material in an extraction process in step 105.

**[0033]** Various extraction techniques of tobacco materials can be used to provide a tobacco extract and tobacco solid material. See, for example, the extraction processes described in US Pat. Appl. Pub. No. 2011/0247640 to Beeson et al. Other example techniques for extracting components of tobacco are described in US Pat. Nos. 4,144,895 to Fiore; 4,150,677 to Osborne, Jr. et al.; 4,267,847 to Reid; 4,289,147 to Wildman et al.; 4,351,346 to Brummer et al.; 4,359,059 to Brummer et al.; 4,506,682 to Muller; 4,589,428 to Keritsis; 4,605,016 to Soga et al.; 4,716,911 to Poulouse et al.; 4,727,889 to Niven, Jr. et al.; 4,887,618 to Bernasek et al.; 4,941,484 to Clapp et al.; 4,967,771 to Fagg et al.; 4,986,286 to Roberts et al.; 5,005,593 to Fagg et al.; 5,018,540 to Grubbs et al.; 5,060,669 to White et al.; 5,065,775 to Fagg; 5,074,319 to White et al.; 5,099,862 to White et al.; 5,121,757 to White et al.; 5,131,414 to Fagg; 5,131,415 to Munoz et al.; 5,148,819 to Fagg; 5,197,494 to Kramer; 5,230,354 to Smith et al.; 5,234,008 to Fagg; 5,243,999 to Smith; 5,301,694 to Raymond et al.; 5,318,050 to Gonzalez-Parra et al.; 5,343,879 to Teague; 5,360,022 to Newton; 5,435,325 to Clapp et al.; 5,445,169 to Brinkley et al.; 6,131,584 to Lauterbach; 6,298,859 to Kierulff et al.; 6,772,767 to Mua et al.; and 7,337,782 to Thompson. In certain embodiments, the solvent is added to the tobacco material and the material is soaked for a given period of time (e.g., about 1 h); the extraction product is then filtered to give a tobacco solid material and the solvent and any solubles contained therein are filtered off to give a tobacco extract.

**[0034]** The first extraction solution used for extraction of the tobacco material can vary. For example, in some embodiments, the first extraction solution comprises a first extraction solution having an aqueous character, such as distilled water and/or tap water. In some embodiments, hot water extraction can be used. See, e.g., Li et al, Hot water Extraction of Hemicelluloses from Aspen Wood Chips of Different Sizes, *Bioresources*, 8(4), 2013, pp. 5690-5700. In some embodiments, the first extraction solution can have one or more additives and may contain, for example, organic and/or inorganic acids, bases, or salts, pH buffers, surfactants, or combinations thereof and may comprise minor amounts of one or more organic solvents (e.g., various alcohols, polyols, and/or humectants). The tobacco material extraction step may be carried out under acidic, neutral, or basic conditions. See, e.g., Huang et al, Production of Dissolving Grade Pulp from Tobacco Stalk Through SO<sub>2</sub>-ethanol-water Fractionation, Alkaline Extraction, Bleaching Processes, *Bioresources*, 14(3), 2019, pp. 5544-5558. particularly p5548 which suggests a range of extraction conditions may be effective in removing extractives from tobacco material. In one particular embodiment, the first extraction solution comprises sodium hydroxide (NaOH) (e.g., as a 5% NaOH solution in water). In other embodiments, the first extraction solution can comprise an organic solvent, such as an alcohol (e.g., ethanol, isopropanol, etc.), which can be used alone or in combination with an aqueous

solvent. Hemicellulase, cellulase, or other enzymatic treatment may be employed in the tobacco material extraction step.

**[0035]** Typically, the extraction comprises adding a large excess of one or more solvents to the tobacco material so as to produce a slurry (comprising, for example, 50-90% by weight of the solvent), although the amount of solvent can vary. The solvent(s) can be at room temperature or at an elevated temperature. For example, the solvent can be heated at a temperature of between about room temperature and about 120 °C, preferably about room temperature and about 110 °C (e.g., about 100 °C, about 80 °C, about 60 °C, about 40 °C, or about 20 °C).

**[0036]** In some preferred embodiments, the tobacco material can be combined with water to form a moist aqueous material (e.g., in the form of a suspension or slurry) and the resulting material is typically heated to effectuate extraction of various compounds. The water used to form the moist material can be pure water (e.g., tap water or deionized water) or a mixture of water with suitable co-solvents such as certain alcohols. In certain embodiments, the amount of water added to form the moist material can be at least about 50 weight percent, or at least about 60 weight percent, or at least about 70 weight percent, based on the total weight of the moist material. In some cases, the amount of water can be described as at least about 80 weight percent or at least about 90 weight percent. In some embodiments, the ratio of the amount of water to the amount of tobacco material on a weight basis is in the range of about 5:1 to about 15:1, or about 8:1 to about 12:1. In certain embodiments, the ratio of the amount of water to the amount of tobacco material on a weight basis is about 9:1 (e.g., 1215 lb of water and 135 lb of tobacco material). As described in more detail below, in certain embodiments, the tobacco material can include additional cellulose material such as wood pulp.

**[0037]** In certain embodiments, the tobacco material can be extracted with water and at least one chelating agent which is capable of removing transition metals from the tobacco material. Chelating agents are useful to remove certain metals from the tobacco material that could cause yellowing, and thus interfere with the whitening process. Suitable chelating agents may include, but are not limited to, ethylenediaminetetraacetic acid (EDTA), egtazic acid (EGTA), N-(2-hydroxyethyl)-ethylenediaminetriacetic acid (HEDTA), diethylenetriamine pentaacetic acid (DTPA), nitrilotriacetic acid (NTA), calcium citrate, calcium diacetate, calcium hexametaphosphate, citric acid, gluconic acid, dipotassium phosphate, disodium phosphate, isopropyl citrate, monobasic calcium phosphate, monoisopropyl citrate, potassium citrate, sodium acid phosphate, sodium citrate, sodium gluconate, sodium hexametaphosphate, sodium metaphosphate, sodium phosphate, sodium pyrophosphate, sodium tripolyphosphate, stearyl citrate, tetra sodium pyrophosphate, calcium disodium ethylene diamine tetra-acetate, glucono delta-lactone, potassium gluconate and the like, and their analogs, homologs and derivatives; as described in U.S. Patent No. 9,321,806 to Lo et al. For example, the tobacco material can be extracted with an aqueous solution comprising ethylenediaminetetraacetic acid (EDTA). In some embodiments, the chelating agent can comprise diethylenetriamine pentaacetic acid (DTPA). In various embodiments, the chelating agent(s) can be present in an amount of about 0.01 to about 5.0 dry weight percent, about 0.1 to about 2.0 dry weight

percent, about 0.5 to about 1.5 dry weight percent, about 0.1 to about 0.5 dry weight percent, or about 0.7 to about 1.0 dry weight percent, based on the total dry weight of the tobacco material.

**[0038]** The amount of time for which the tobacco material remains in contact with the first extraction solution can vary. For example, in some embodiments, the tobacco material is in contact with the first extraction solution for about thirty minutes to about six hours (e.g., about 1 hour, about 2 hours, about 3 hours, about 4 hours, about 5 hours, or about 6 hours), although shorter and longer time periods can be used. The amount of time can depend, for example, on the temperature of the first extraction solution. For example, less time may be required to extract the tobacco material using the first extraction solution at a higher temperature than that required to extract the tobacco material with room temperature or a cold solution. The extraction process provides a tobacco solid material and a tobacco extract.

**[0039]** In an example embodiment, the input tobacco material can undergo a water extraction at a temperature of about 75°C to about 100°C (e.g., about 85°C) for an extraction time of about 30 mins to about 120 mins (e.g., about 60 mins). The liquid/material ratio of the aqueous extraction can be about 8:1, for example. In another example embodiment, the input tobacco material can undergo an acidic extraction using e.g., H<sub>2</sub>SO<sub>4</sub>, at a pH of about 3, and a temperature of about 75°C to about 100°C (e.g., about 90°C), for an extraction time of about 30 mins to about 150 mins (e.g., about 120 mins). The liquid/material ratio of the acidic extraction can be about 8:1, for example. In another example embodiment, the input tobacco material can undergo an alkaline extraction using e.g., NaOH 12% solution, at a pH of about 12-14, and a temperature of about 75°C to about 100°C (e.g., about 90°C), for an extraction time of about 30 mins to about 150 mins (e.g., about 120 mins). The liquid/material ratio of the alkaline extraction can be about 5:1, for example. In terms of removing unwanted substances from the tobacco material (e.g., ash, Fe, Ca, K, SiO<sub>2</sub>, Cu, Mg, Mn, etc.), the acidic extraction can be more efficient than the alkaline and aqueous extractions. The aqueous extraction can be more efficient than the alkaline extraction at removing unwanted substances from the tobacco material.

**[0040]** The number of extraction steps can vary. For example, in certain embodiments, the tobacco material is extracted one or more times, two or more times, three or more times, four or more times, or five or more times. In some embodiments, extraction can be performed in a counter-current or washing of the tobacco material. The extraction solution used for each extraction can vary. For example, in one particular embodiment, one or more extractions are conducted using hot water; and in a final extraction, the extraction is conducted using a basic solution (e.g., a 5% NaOH solution). After each extraction step, the tobacco solid material is filtered and the extraction solution and solubles are removed from the tobacco solid material. In certain embodiments, the extracts obtained from each extraction can be combined and clarified, as described in U.S. Pat. No. 9,420,825 to Beeson et al. In other embodiments, some extracts are discarded, such as extracts from later stages. In such embodiments, for example, it may be desirable in some embodiments to use only the tobacco extract obtained from a first extraction of a tobacco material or to combine tobacco extracts obtained from a first and

second extraction of a tobacco material.

**[0041]** Following the extraction process, the tobacco solids material is generally isolated from the tobacco extract, as illustrated at operation 110 of Fig. 2, for example, by filtration or centrifugation, although these methods are not intended to be limiting. Alternatively, in some embodiments, the tobacco solids material can be isolated from the extract by means of distillation (e.g., steam distillation) of the tobacco mixture (e.g., the tobacco slurry). The process of filtration can comprise passing the liquid through one or more filter screens to remove selected sizes of particulate matter. Screens may be, for example, stationary, vibrating, rotary, or any combination thereof. Filters may be, for example, press filters or pressure filters. In some embodiments, the filtration method used can involve microfiltration, ultrafiltration, and/or nanofiltration. A filter aid can be employed to provide effective filtration and can comprise any material typically used for this purpose. For example, some common filter aids include cellulose fibers, perlite, bentonite, diatomaceous earth, and other siliceous materials. To remove solid components, alternative methods can also be used, for example, centrifugation or settling/sedimentation of the components and siphoning off of the liquid. See, for example, the processes and products described in U.S. Pat. App. Pub. Nos. 2012/0152265 to Dube et al. and 2012/0192880 to Dube et al. The extracted solids component can be used as the starting tobacco material in various embodiments of the whitening process described herein.

**[0042]** In some embodiments, a chemical pulping process can be used to pulp and delignify the tobacco biomass at operation 115. A chemical pulping process separates lignin from cellulose fibers by dissolving lignin in a cooking liquor such that the lignin, which binds the cellulose fibers together, can be washed away from the cellulose fibers without seriously degrading the cellulose fibers.

**[0043]** In embodiments of the present disclosure, an alkaline cook (e.g., a Kraft cooking process) is used to produce a tobacco pulp from the tobacco solids material (i.e., the extracted tobacco material). The alkaline cooking liquor can include a strong base such that the pH of the cooking liquor is greater than 10. As used herein, a strong base refers to a basic chemical compound (or combination of such compounds) that is able to deprotonate very weak acids in an acid-base reaction. For example, strong bases that can be useful in the present invention include, but are not limited to one or more of sodium hydroxide, potassium hydroxide, sodium carbonate, sodium bicarbonate, potassium carbonate, potassium bicarbonate, ammonium hydroxide, ammonium bicarbonate, and ammonium carbonate. In some embodiments, the weight of the strong base can be greater than about 5%, greater than about 25%, or greater than about 40% of the weight of the tobacco input. In certain embodiments, the weight of the strong base can be less than about 60% or less than about 50% of the weight of the tobacco input. In still further embodiments, the weight of the strong base can be from about 5% to about 50%, or from about 30% to about 40% of the weight of the tobacco input. Various other chemicals and weight ratios thereof can also be employed to chemically pulp the tobacco input in other embodiments.

**[0044]** In various embodiments, the pulping process is a Kraft cooking process. It is typically understood that the two primary active components of a Kraft cooking liquid are hydroxide ions and hydrosulfide ions. In various embodiments, the Kraft pulping process entails treatment of the tobacco input material with a hot mixture of water, sodium hydroxide (NaOH) or another strong base, and sodium sulfide (Na<sub>2</sub>S), known as white liquor, that breaks the bonds that link lignin, hemicellulose, and cellulose. It is noted that in some embodiments, other chemicals that produce hydroxide ions and/or hydrosulfide ions can be used in the cooking liquor (e.g., NaOH and Na<sub>2</sub>S); however, a conventional Kraft cook or sodium sulfate process comprises NaOH and Na<sub>2</sub>S. The white liquor (also referred to herein as alkaline cooking liquor or alkaline cooking liquid) can be formed by mixing the water, sodium hydroxide, and sodium sulfide until a target pH is achieved. The alkaline cooking liquor can have a pH of greater than 10, a pH of 11 or greater, a pH of 12 or greater, or a pH of 13 or greater. The alkaline cooking liquor can have a pH in the range of about 10 to about 14, about 11 to about 14, or about 12 to about 14, for example. In certain embodiments, the Kraft cook can be done at a pH of about 11, about 12, about 13, or about 14.

**[0045]** It is noted that a Kraft pulping method can produce a higher yield of tobacco pulp materials as compared to other chemical pulping methods known in the art. For example, the yield of tobacco pulp produced from a Kraft cook of tobacco materials can be 28% or greater, 30% or greater, 32% or greater, such as, in the range of about 28-35%, on a weight basis.

**[0046]** In addition to combining a tobacco input with a strong base and sodium sulfide, chemically pulping a tobacco input can include heating the tobacco input and the alkaline cooking liquor. Heating the tobacco input and the strong base can be conducted to increase the efficacy of the chemical pulping. In this regard, an increase in either cooking temperature or time will result in an increased reaction rate (rate of lignin removal).

**[0047]** In some embodiments, the Kraft cook can be conducted at a temperature of about 20°C to about 180°C, or about 120°C to about 160°C. In various embodiments, the maximum temperature of the Kraft cook can be about 180°C, about 170°C, about 165°C, about 160°C, about 155°C, about 150°C, about 140°C, about 120°C, or about 100°C.

**[0048]** In various embodiments, the tobacco material can undergo the Kraft cook for a time period of about 30 to about 480 mins, about 60 to about 240 mins, or about 90 to about 120 mins. In some embodiments, the tobacco material can undergo the Kraft cook for at least about 30 mins, at least about 60 mins, at least about 90 mins, at least about 120 mins, at least about 150 mins, or at least about 240 mins.

**[0049]** In some embodiments, the method of producing a tobacco-derived pulp can include one or more additional operations. See, e.g., U.S. Patent Appl. Pub. No. 2013/0276801 to Byrd Jr. et al. For example, the tobacco input can undergo further processing steps prior to pulping and/or the delignification method can include additional treatment steps (e.g., drying the tobacco input, or depithing the tobacco input). In some embodiments, these additional steps can be conducted to remove pith (which comprises lignin) from the tobacco input and/or

tobacco pulp manually, and thus reduce the amount of chemicals necessary to delignify the tobacco input during a chemical pulping process, for example. Mixing water with the tobacco pulp to form a slurry and filtering the slurry can be conducted, for example, to remove certain materials, such as pith, parenchyma, and tissue from the tobacco pulp. Anthraquinone can be employed in a chemical pulping method in an attempt to provide a higher yield by protecting carbohydrates from the strong base during delignification, for example. Other processing steps known in the pulping and delignification field can be employed in forming tobacco pulp from the raw tobacco input.

**[0050]** In certain embodiments, the tobacco pulp material provided from the pulping process described above can be washed before being subjected to any further operations. For example, water can be used to wash the pulp prior to the bleaching operations described in more detail below. It is further noted that the tobacco materials can be washed following any step in the methods described herein. For example, the tobacco pulp can be washed (*e.g.*, with water) following one or more of the bleaching stages described below.

**[0051]** Tobacco pulp material that has been provided and isolated following the extraction and alkaline pulping steps is bleached (*i.e.*, whitened), as shown in step 120 of Figure 2. As illustrated in FIG. 3, for example, the bleaching step can include several different stages. As illustrated in step 121 (and step 124) of FIG. 3, for example, bleaching the tobacco pulp material can include an acid treatment adapted to, for example, reducing the amount of metals and/or inorganics in the tobacco pulp material, such as SiO<sub>2</sub>, Mn, Mg, and Ca. Without being limited by theory, this acid pre-treatment stage can make a later oxidative bleaching stage more efficient in bleaching the tobacco material. If too many metal ions such as, *e.g.*, Mn, are present in the tobacco material, the peroxide will decompose and oxygen will be formed, thereby resulting in the peroxide losing its bleaching efficiency.

**[0052]** In various embodiments, the tobacco pulp can undergo an acid pre-treatment bleaching process using at least one acid. In various embodiments, the tobacco pulp can be treated with sulfuric acid. In some embodiments, the tobacco pulp can be treated with at least one mineral acid (*e.g.*, hydrochloric acid or another strong acid). During the acid pre-treatment process, the pulp can have, for example, a pulp consistency of about 5% to about 20% (*e.g.*, about 10%). In order to measure pulp consistency, the dryness of the pulp was analyzed before mixing the pulp with any liquids (*e.g.*, an acid plus water) using method ISO 638. The pulp consistency was then determined based on the amount of liquids added. It is noted that pulp consistency can also be measured using TAPPI T240. Pulp consistency describes the measurement of pulp concentration of aqueous (or in this case, acid + water) fiber suspensions. The acid stage of the bleaching can be done at a pH of about 2 to about 6, or about 3 to about 5. In certain embodiments, the acid pre-treatment is done at a pH of about 2.5. In various embodiments, the acid pre-treatment can be done at a temperature of about 40°C to about 100°C, or about 50°C to about 70°C (*e.g.*, about 60°C). In some embodiments, the tobacco solids material can be subjected to the acid pre-treatment for a time of about 30 mins to about 150 mins, or about 60 mins to about 120 mins (*e.g.*, about 90 mins). The liquid/material weight ratio of the acidic extraction can be about 5:1 to about 10:1 (*e.g.*, about 8:1), for example.

**[0053]** In various embodiments, as illustrated at step 122 (and step 125) of FIG. 3, for example, bleaching the tobacco pulp can include a chelating stage where a complexing agent is added to the tobacco pulp material in order to, for example, remove metal content from the pulp material. Without being limited by theory, a chelating pre-treatment can help increase the efficacy of a later oxidative bleaching stage.

**[0054]** The chelating stage can comprise extracting the pulp material with an extraction solution (also referred to herein as "a second extraction solution") comprising at least one chelating agent to provide an extracted tobacco pulp. In various embodiments, the chelating pre-treatment at step 122 can include treatment with at least one chelating agent including, but not limited to EDTA, EGTA, HEDTA, DTPA, NTA, calcium citrate, calcium diacetate, calcium hexametaphosphate, citric acid, gluconic acid, dipotassium phosphate, disodium phosphate, isopropyl citrate, monobasic calcium phosphate, monoisopropyl citrate, potassium citrate, sodium acid phosphate, sodium citrate, sodium gluconate, sodium hexametaphosphate, sodium metaphosphate, sodium phosphate, sodium pyrophosphate, sodium tripolyphosphate, stearyl citrate, tetra sodium pyrophosphate, calcium disodium ethylene diamine tetra-acetate, glucono delta-lactone, potassium gluconate and the like, and their analogs, homologs and derivatives; as described in U.S. Patent No. 9,321,806 to Lo et al. In various embodiments, the chelating pre-treatment includes treating the tobacco pulp with EDTA.

**[0055]** The tobacco pulp can have a pulp consistency of, for example, about 5% to about 20% (e.g., about 5%) during the chelating stage. The chelating stage of the bleaching can be done at a pH of about 4 to about 7, or about 5 to about 6. In certain embodiments, the chelating pre-treatment is done at a pH of about 5.5-6. In various embodiments, the chelating pre-treatment can be done at a temperature of about 50°C to about 120°C, or about 60°C to about 90°C (e.g., about 70°C). In some embodiments, the tobacco pulp material can be subjected to the chelating pre-treatment for a time of about 30 mins to about 150 mins, or about 60 mins to about 120 mins (e.g., about 60 mins). The liquid/material weight ratio of the chelating extraction can be about 5:1 to about 10:1 (e.g., about 5:1), for example.

**[0056]** It is noted that the bleaching operations described herein can include any or all of the acidic pre-treatment and chelating pre-treatment stages. In certain embodiments, the bleaching operation can include none of these pre-treatments. In various embodiments, the tobacco pulp can be washed using any means known in the art between different pre-treatment steps. In certain embodiments of the whitening methods described herein, the tobacco pulp is subjected to an acidic pretreatment and a chelating pre-treatment before an oxidative bleaching stage.

**[0057]** After cooking the tobacco solids material and subjecting the tobacco pulp material to any desired bleaching pre-treatment steps, the tobacco pulp is subjected to an oxidative bleaching stage (e.g., bleaching with a bleaching solution including peroxide (e.g., hydrogen peroxide)), as illustrated at step 123 (and step 126) of FIG. 3. In various embodiments, the oxidative bleaching stage is done at a pH of about 8 to about 14, about 9 to about 12, or about

10 to about 11.5. It is noted that in certain embodiments, a bleaching solution which is too alkaline can adversely affect whitening of the tobacco materials. In particular, in certain embodiments, if the end pH of the pulp materials during/after bleaching is too high, this can cause darkening of the tobacco materials. As such, in various embodiments, the pH of the bleaching solution is below 12, below 11.5, or below 11. In some embodiments, the pH of the bleaching solution is in the range of about 8-12, about 10-12, or about 10-11.5. As described above, the oxidative bleaching operation can be more effective at whitening the tobacco pulp if one or more pre-treatments have been used to lower the amount of metals like Fe, Cu, and especially Mn in the tobacco pulp material.

**[0058]** In various embodiments, Mg can be added as MgSO<sub>4</sub> to the oxidative bleaching stage. Without being limited by theory, the MgSO<sub>4</sub> can help to capture the harmful metals in complexes. In various embodiments, MgSO<sub>4</sub> can be added to the bleaching solution in an amount of about 10-20 kilograms per tonne (kg/t), or about 15-20 kg/t. In certain embodiments, MgSO<sub>4</sub> can be added to the bleaching solution in an amount of about 15 kg/t.

**[0059]** As noted below, in certain embodiments, a combination of tobacco pulp material and wood pulp may undergo a whitening step or any other process step described herein; however, for convenience, the following description refers only to tobacco pulp material. The oxidative bleaching stage can include treatment with various bleaching or oxidizing agents and oxidation catalysts. Example oxidizing agents include peroxides (e.g., hydrogen peroxide), chlorite salts, chlorate salts, perchlorate salts, hypochlorite salts, ozone, ammonia, and combinations thereof. Example oxidation catalysts are titanium dioxide, manganese dioxide, and combinations thereof. Processes for treating tobacco with bleaching agents are discussed, for example, in US Patent Nos. 787,611 to Daniels, Jr.; 1,086,306 to Oelenhein; 1,437,095 to Delling; 1,757,477 to Rosenhoch; 2,122,421 to Hawkinson; 2,148,147 to Baier; 2,170,107 to Baier; 2,274,649 to Baier; 2,770,239 to Prats et al.; 3,612,065 to Rosen; 3,851,653 to Rosen; 3,889,689 to Rosen; 3,943,945 to Rosen; 4,143,666 to Rainer; 4,194,514 to Campbell; 4,366,823, 4,366,824, and 4,388,933 to Rainer et al.; 4,641,667 to Schmekel et al.; and 5,713,376 to Berger; and PCT WO 96/31255 to Giolvas. Other whitening methods using reagents such as ozone and potassium permanganate can also be used. See, for example, US Patent No. 3,943,940 to Minami.

**[0060]** The oxidizing agent (i.e., oxidant or oxidizer) can be any substance that readily transfers oxygen atoms and/or gains electrons in a reduction/oxidation (redox) chemical reaction. Peroxides (e.g., hydrogen peroxide, peracetic acid) are preferred oxidizing agents; however, any oxidizing reagent, including, but not limited to; other oxides (including nitrous oxide, silver oxide, chromium trioxide, chromate, dichromate, pyridinium chlorochromate; and osmium tetroxide); oxygen (O<sub>2</sub>); ozone (O<sub>3</sub>); fluorine (F<sub>2</sub>); chlorine (Cl<sub>2</sub>); and other halogens; hypochlorite, chlorite, chlorate, perchlorite, and other halogen analogues thereof; nitric acid; nitrate compounds; sulfuric acid; persulfuric acids; hydroxyl radicals; manganate and permanganate compounds (e.g., potassium permanganate); sodium perborate; 2,2'-dipyridyldisulfide; and combinations thereof can be used according to the invention. Peroxide activators such as TAED (tetraacetylenediamine) which generates in situ peracetic acid

may be used in the oxidative bleaching stage. See, e.g., URLs: <https://www.tappi.org/content/events/07recycle/presentation/hsieh.pdf>, Zhao et al, *Bioresources*, 5(1), 276-210, 2010, <https://pdfs.semanticscholar.org/8e78/9d93d8cc673e2f13b8daee35e3477c51b3fe.pdf>.

**[0061]** In certain preferred embodiments, the oxidizing reagent used according to the invention is chlorine-free. In certain embodiments, the oxidizing reagent is provided in aqueous solution form. The amount of oxidizing agent used in the methods of the present invention can vary. For example, in certain embodiments, the oxidizing agent is provided in a weight amount of about 0.1 to fifty times the weight of the (dry) tobacco solids material. For example, in some embodiments, the oxidizing agent is provided in a weight amount about equal to the weight of the (dry) tobacco solids material, about 0.25 times the weight of the (dry) tobacco solids material, about 0.5 times the weight of the (dry) tobacco solids material, about 0.7 times the weight of the (dry) tobacco solids material, about 1.0 times the weight of the (dry) tobacco solids material, about 1.25 times the weight of the (dry) tobacco solids material, about 1.5 times the weight of the (dry) tobacco solids material, about 2 times the weight of the (dry) tobacco solids material, or about 5 times the weight of the (dry) tobacco solids material. In some embodiments, the oxidizing agent is provided in a weight amount in the range of about 0.1 to about 5 times the weight of the (dry) tobacco solids material, about 0.2 to about 2.5 times the weight of the (dry) tobacco solids material, about 0.25 to about 1.5 times the weight of the (dry) tobacco solids material, about 0.5 to about 1.0 times the weight of the (dry) tobacco solids material, or about 0.7 to about 0.9 times the weight of the (dry) tobacco solids material. Different oxidizing agents can have different application rates. In certain embodiments wherein the oxidizing agent comprises hydrogen peroxide, the bleaching solution can comprise hydrogen peroxide in a weight of about 0.25-1.5 times the weight of the dry tobacco solids material.

**[0062]** In various embodiments, the bleaching solution comprises hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>). In various embodiments, H<sub>2</sub>O<sub>2</sub> can be added to the bleaching solution in an amount of about 50-250 kilograms per tonne (kg/t), or about 100-200 kg/t, or about 150-200 kg/t. In various embodiments, the bleaching solution comprises H<sub>2</sub>O<sub>2</sub> in an amount of about 100 kg/t or above. In some embodiments, the bleaching solution comprises H<sub>2</sub>O<sub>2</sub> in an amount of about 150 kg/t or above. In various embodiments, the bleaching solution comprises H<sub>2</sub>O<sub>2</sub> in an amount of about 200 kg/t or above. As used herein, tonne refers to a metric ton.

**[0063]** In some embodiments, the tobacco solids material is bleached during the oxidative bleaching stage using both a caustic reagent and an oxidizing agent. In such embodiments, the caustic reagent and oxidizing agent can be provided separately or can be combined. Stepwise addition of a strong base and/or bleaching agent may be used in the bleaching stage. See, e.g., Zhao et al, *Bioresources*, 5(1), 276-210, 2010; URL: <https://pdfs.semanticscholar.org/8e78/9d93d8cc673e2f13b8daee35e3477c51b3fe.pdf>; Sun, Hou, *Journal of Bioresources and Bioproducts*, 3(1),35-39, 2018; URL: <http://www.bioresources-bioproducts.com/index.php/bb/article/view/110/109>. In certain embodiments, multiple oxidative bleaching stages may be applied after the initial extraction

stage.

**[0064]** The caustic reagent can vary and can be, for example, any strong base, including but not limited to, an alkaline metal hydroxide, alkaline earth metal hydroxide, or mixture thereof. In certain example embodiments, the caustic reagent is sodium hydroxide or potassium hydroxide. Alternative reagents that can be used include, but are not limited to, ammonium hydroxide, sodium carbonate, potassium carbonate, ammonia gas, and mixtures thereof. The caustic reagent is generally provided in solution form (e.g., in aqueous solution) and the concentration of the caustic reagent in the solution can vary. Also, the amount of caustic reagent used in the methods of the present invention can vary. For example, in certain embodiments, the caustic reagent is provided in an amount of between about 1% and about 50% dry weight basis (e.g., between about 1% and about 40% or between about 1% and about 30%) by weight of the (dry) tobacco solids material. For example, the caustic reagent can be provided in an amount of about 2%, about 5%, about 7%, about 10%, or about 25% by weight of the (dry) tobacco solids material. It is noted that the quantity of caustic reagent required may, in certain embodiments, vary as a result of the strength of the caustic reagent. For example, more caustic reagent may, in some embodiments, be required where the caustic reagent is a weaker base, whereas less caustic reagent may, in some embodiments, be required where the caustic reagent is a strong base.

**[0065]** In various embodiments, the bleaching solution comprises sodium hydroxide (NaOH). In various embodiments, NaOH can be added to the bleaching solution in an amount of about 20-60 kilograms per tonne (kg/t), or about 35-50 kg/t, or about 35-40 kg/t. In various embodiments, the bleaching solution comprises NaOH in an amount of about 35 kg/t. In some embodiments, the bleaching solution comprises NaOH in an amount of about 40 kg/t. In various embodiments, the bleaching solution comprises NaOH in an amount of about 50 kg/t.

**[0066]** The solids content of the oxidative bleaching stage may be adjusted. Without being limited by theory, higher solids content may be beneficial and result in the need for less oxidative bleaching agent to achieve a target whiteness (or brightness). For example, in certain embodiments, the bleaching solution can include about 0.7-0.9 times more oxidizing agent than dry tobacco material (at about 10% solids), about 1.0 times more oxidizing agent than dry tobacco material (at about 4.5% solids).

In some embodiments, a >25% solids content may be beneficial. See, e.g., <https://www.valmet.com/pulp/mechanical-pulping/bleaching/bleach-tower/>; <https://www.valmet.com/pulp/mechanical-pulping/bleaching/high-consistency-bleaching-phc/>).

**[0067]** As noted above, the percentage of solids during bleaching can vary and can have an impact on the effectiveness of the bleaching operation. The solids percentage is calculated using the following formula:

$$\text{Solids (\%)} = 100 \times (\text{wt dry tobacco}) / (\text{wt dry tobacco} + \text{wt water} + \text{wt oxidizing agent})$$

In various embodiments, the percentage of solids can be in the range of about 1-20%, about 3-15%, or about 3-10%. In some embodiments, the percentage of solids can be in the range of about 2-5%, or about 8-12%. The percentage of solids can be, for example, at least about 2%,

at least about 3%, at least about 4%, at least about 5%, or at least about 10%.

**[0068]** In various embodiments, the bleaching process can further include treatment with one or more stabilizers in addition to an oxidizing agent. For example, the stabilizer can be selected from the group consisting of magnesium sulfate, sodium silicate, and combinations thereof. In various embodiments, the stabilizer(s) can be present in an amount of about 0.01 to about 3.0 dry weight percent, about 0.1 to about 2.5 dry weight percent, or about 0.5 to about 2.0 dry weight percent, based on the total dry weight of the tobacco material solids material.

**[0069]** According to the invention, the tobacco solids material is brought into contact with the caustic reagent and/or oxidizing agent for a period of time. The tobacco material can be brought into contact with the caustic reagent and oxidizing reagent simultaneously, or can be brought into contact with the caustic reagent and oxidizing reagent separately. In one embodiment, the oxidizing reagent is added to the tobacco material and then the caustic reagent is added to the tobacco material such that, after addition, both reagents are in contact with the tobacco material simultaneously. In another embodiment, the caustic reagent is added to the tobacco material and then the oxidizing reagent is added to the tobacco material such that, after addition, both reagents are in contact with the tobacco material simultaneously.

**[0070]** The time for which the tobacco material is contacted with the caustic reagent and/or oxidizing agent can vary. For example, in certain embodiments, the time for which the tobacco material is contacted with the oxidizing agent and any other bleaching agents used is that amount of time sufficient to provide a tobacco solids material with a lightened color as compared to the untreated tobacco material. In certain embodiments, the tobacco material is contacted with the caustic reagent and/or oxidizing agent overnight. Normally, the time period is a period of at least about 10 minutes, typically at least about 30 minutes, or at least about 60 mins, or at least about 90 minutes. In certain embodiments, the time period is a period of no more than about 10 hours, no more than about 8 hours, no more than about 6 hours, no more than about 4 hours, no more than about 2 hours, or no more than about 1 hour.

**[0071]** In certain embodiments, the tobacco material can be heated during treatment with the oxidizing agent and any other bleaching agents used. Generally, heating the tobacco material accelerates the whitening process. Where the tobacco material is heated during treatment, sufficient color lightening is typically achieved in less time than in embodiments wherein the tobacco material is unheated during treatment. The temperature and time of the heat treatment process will vary, and generally, the length of the heat treatment will decrease as the temperature of the heat treatment increases. In certain embodiments, the mixture of tobacco material, caustic reagent, and/or oxidizing agent can be heated at a temperature of between room temperature and about 120 °C (e.g., about 90 °C or about 80 °C). Preferably, the mixture is heated between room temperature and about 90 °C. The heating, where applicable, can be accomplished using any heating method or apparatus known in the art. The heating can be carried out in an enclosed vessel (e.g., one providing for a controlled atmospheric environment, controlled atmospheric components, and a controlled atmospheric pressure), or in a vessel that is essentially open to ambient air. The temperature can be controlled by using

a jacketed vessel, direct steam injection into the tobacco, bubbling hot air through the tobacco, and the like. In certain embodiments, the heating is performed in a vessel also capable of providing mixing of the composition, such as by stirring or agitation. Example mixing vessels include mixers available from Scott Equipment Company, Littleford Day, Inc., Lödige Process Technology, and the Breddo Likwifier Division of American Ingredients Company. Examples of vessels which provide a pressure controlled environment include high pressure autoclaves available from Berghof/America Inc. of Concord, California, and high pressure reactors available from The Parr Instrument Co. (e.g., Parr Reactor Model Nos. 4522 and 4552 described in US Patent No. 4,882,128 to Hukvari et al.). The pressure within the mixing vessel during the process can be atmospheric pressure or elevated pressure (e.g., about 10 psig to about 1,000 psig).

**[0072]** In other embodiments, the heating process is conducted in a microwave oven, a convection oven, or by infrared heating. Atmospheric air, or ambient atmosphere, is the preferred atmosphere for carrying out the optional heating step of the present invention. However, heating can also take place under a controlled atmosphere, such as a generally inert atmosphere. Gases such as nitrogen, argon and carbon dioxide can be used. Alternatively, a hydrocarbon gas (e.g., methane, ethane or butane) or a fluorocarbon gas also can provide at least a portion of a controlled atmosphere in certain embodiments, depending on the choice of treatment conditions and desired reaction products.

**[0073]** In various embodiments, the acid pre-treatment stage (step 121 of FIG. 3), the chelating pre-treatment stage (step 122 of FIG. 3), and the peroxide bleaching stage (step 123 of FIG. 3) can be repeated a second time, as illustrated in steps 124, 125, and 126 of FIG. 3. In certain embodiments, one or more of the acid pre-treatment stage, the chelating pre-treatment stage, and the peroxide bleaching stage can each be repeated two or more times in the overall bleaching process. It is noted that if one or more of the acid pre-treatment stage, the chelating pre-treatment stage, and the peroxide bleaching stage are repeated, the same or different reagents (e.g., acid, chelating agent, bleaching solution, oxidizing agent, caustic reagent, stabilizer, etc.) used in a first iteration of the repeated stage can be used in any subsequent iteration of that stage. For example, a first acid can be used in a first acid pre-treatment stage (step 121 of FIG. 3) and a second acid can be used in a second acid pre-treatment stage (step 124 of FIG. 3). In some embodiments, the first acid and the second acid can be the same. In certain embodiments, the first acid and the second acid can be different from one another.

**[0074]** In certain embodiments, before drying the bleached tobacco material, the bleached tobacco material can be treated with an acid to neutralize the tobacco material after the bleaching process to a pH in the range of about 5 to about 11 (as illustrated at operation 130 of Fig. 2, for example), or such as about 6 to about 10. The bleached tobacco material can be treated with sulfuric acid, hydrochloric acid, citric acid, or any combination thereof. Other acids known in the art can also be used to neutralize the bleached tobacco material. Following treatment with an acid, the pH of the bleached tobacco material can be, for example, approximately 7.

**[0075]** In various embodiments, a wood pulp is added to the solid tobacco materials and/or the tobacco pulp during the overall whitening processes described herein. It is noted that wood pulp can be introduced into the whitening process at any of the steps described herein. For example, in certain embodiments, the methods described herein can further comprise mixing the tobacco solids material with a wood material prior to pulping such that the wood material is also pulped. In certain embodiments, the methods described herein can further comprise mixing the tobacco pulp with a wood pulp after the pulping process. In some embodiments, the wood pulp is a bleached pulp material and can be added after the solid tobacco materials have been pulped and bleached. If unbleached wood pulp is used, an additional caustic extraction step may be required, or the wood pulp can need to be added to the tobacco pulp before the step of bleaching.

**[0076]** In various embodiments, the wood pulp can be market available wood pulp. In certain embodiments, the wood pulp can be a bleached hardwood or softwood pulp. The wood pulp added to the processes described herein can be added in an amount of about 1 to about 20 wt. %, or about 5 to about 15 wt. %, based on the total weight of the pulp used (i.e., the total weight of tobacco pulp and wood pulp used). In some embodiments, the wood pulp can be added in an amount of at least about 1 wt. %, at least about 5 wt. %, or at least about 10 wt. %, based on the total weight of the pulp used. In certain embodiments, the wood pulp can be added in an amount of no more than about 5 wt. %, no more than about 10 wt. %, no more than about 15 wt. %, or no more than about 20 wt. %, based on the total weight of the pulp used.

**[0077]** Following treatment of the tobacco solids material with the oxidizing reagent and any other bleaching agents, the treated tobacco material is generally filtered (i.e., isolated from the caustic reagent and/or oxidizing reagent) and dried (as illustrated at operation 135 of Fig. 2, for example) to give a whitened tobacco material. In certain embodiments, the bleached tobacco material can be dried to a moisture level of about 1-30%, about 5-20%, or about 10-15% moisture on a wet basis. As is known in the art, the term "wet basis" refers to a measurement of the water in a solid, expressed as the weight of water as a percentage of the total wet solid weight.

**[0078]** After drying, the whitened tobacco material can optionally be milled a size in the range of approximately about 5 mm to about 0.1 mm, or about 1 mm to about 0.1 mm. In certain embodiments, the whitened tobacco material can be milled to a size of less than about 10 mm, less than about 5 mm, less than about 2 mm, or less than about 1 mm.

**[0079]** In some embodiments, the whitened tobacco material thus produced can be characterized as lightened in color (e.g., "whitened") in comparison to the untreated tobacco material. Visual and/or instrumental assessments such as those previously described can be used to verify and, if desired, quantify the degree of lightening achieved by way of the presently described method of the invention. Assessment of the whiteness of a material generally requires comparison with another material. The extent of lightening can be

quantified, for example, by spectroscopic comparison with an untreated tobacco sample (e.g., untreated tobacco material). White colors are often defined with reference to the International Commission on Illumination's (CIE's) chromaticity diagram. The whitened tobacco material can, in certain embodiments, be characterized as closer on the chromaticity diagram to pure white than untreated tobacco material. In whitening procedures known in the art, the extracted solids component can be subjected to certain treatments intended to breakdown the fibers of extracted solids material and/or to remove lignin (e.g., a hydrolysis step with at least one acid, a mechanical and/or chemical pulping step, a caustic wash at elevated temperature, etc.). In the whitening processes described herein, the extracted solids component is not subjected to treatment at elevated temperature with sulfur-containing reagents, organic solvents, sodium hydroxide, or an acid between the extracting step and the bleaching step.

**[0080]** After drying, the whitened tobacco material can have an ISO brightness of at least about 30%, at least about 35%, at least about 40%, at least about 45%, at least about 50%, at least about 55%, at least about 60%, at least about 65%, or at least about 70%. In some embodiments, the whitened tobacco material described herein can have an ISO brightness in the range of about 20% to about 90%, about 30% to about 65%, about 35% to about 60%, or about 40% to about 75%. ISO brightness can be measured according to ISO 3688:1999 or ISO 2470-1:2016.

**[0081]** Whiteness of a material can also be characterized based on ASTM E313-73 Whiteness Test. The whiteness of a whitened tobacco material prepared according to the methods disclosed herein can be in the range of about 1-45, 5-40, 10-40, or 10-20, for example. In some embodiments, the whiteness of a whitened tobacco material prepared according to the methods disclosed herein can be at least about 5, at least about 10, at least about 12, at least about 15, at least about 20, or at least about 30.

**[0082]** Whitened tobacco materials as described herein may also be characterized based on TAPPI 227OM-99 Freeness Test. Freeness levels can be indicated as a CSF (Canadian Standard Freeness) value. Freeness level generally is an indicator of the drainage rate of pulp. The higher the value, the easier it is to drain the pulp. Harsher bleaching processes typically used during bleaching of tobacco materials can degrade the individual fibers and undesirably reduce the freeness in bleached tobacco materials. Thus, the whitening methods provided herein can beneficially produce whitened tobacco materials with higher freeness values as compared to other whitening methods which further include a pulping operation. The freeness level of pure tobacco pulp can have a range of about 0 to about 500 CSF. In some embodiments, the freeness of the whitened tobacco materials produced herein can be in the range of about 300 CSF to about 800 CSF, or about 400 CSF to about 700 CSF, or about 500 CSF to about 650 CSF.

**[0083]** The tobacco materials discussed in the present invention can be treated and/or processed in other ways before, after, or during the process steps described above. For example, if desired, the tobacco materials can be irradiated, pasteurized, or otherwise subjected to controlled heat treatment. Such treatment processes are detailed, for example, in

US Pat. Pub. No. 2009/0025738 to Mua et al. In certain embodiments, tobacco materials can be treated with water and an additive capable of inhibiting reaction of asparagine to form acrylamide upon heating of the tobacco material (e.g., an additive selected from the group consisting of lysine, glycine, histidine, alanine, methionine, glutamic acid, aspartic acid, proline, phenylalanine, valine, arginine, compositions incorporating di- and trivalent cations, asparaginase, certain non-reducing saccharides, certain reducing agents, phenolic compounds, certain compounds having at least one free thiol group or functionality, oxidizing agents, oxidation catalysts, natural plant extracts (e.g., rosemary extract), and combinations thereof), and combinations thereof. See, for example, the types of treatment processes described in US Pat. Pub. Nos. 2010/0300463 and 2011/0048434 to Chen et al., and US Pat. 8,991,403 to Chen et al. In certain embodiments, this type of treatment is useful where the original tobacco material is subjected to heat in the extraction and/or distillation process previously described.

**[0084]** The whitened tobacco material can be incorporated within an oral product, such as, for example, a smokeless tobacco product. Depending on the type of oral product being processed, the oral product can include one or more additional components in addition to the whitened tobacco material as described above. For example, the whitened tobacco material can be processed, blended, formulated, combined and/or mixed with other materials or ingredients, such as other tobacco materials or flavorants, active ingredients (e.g., botanical materials, stimulants, amino acids, vitamins, antioxidants, nicotine components, cannabinoids, pharmaceutical agents, or a combination thereof), fillers, binders, pH adjusters, buffering agents, salts, sweeteners, colorants, oral care additives, disintegration aids, antioxidants, humectants, and preservatives. See, for example, those representative components, combination of components, relative amounts of those components and ingredients relative to tobacco, and manners and methods for employing those components, set forth in US Pat. Pub. Nos. 2011/0315154 to Mua et al.; 2007/0062549 to Holton, Jr. et al.; 2012/0067361 to Bjorkholm et al.; 2017/0020183 to Bjorkholm; and 2017/0112183 to Bjorkholm; and US Pat. No. 7,861,728 to Holton, Jr. et al.

**[0085]** The relative amount of whitened tobacco material within the oral product may vary. Preferably, the amount of whitened tobacco material within the oral product is at least about 10%, at least about 25%, at least about 50%, at least about 60%, at least about 70%, at least about 80%, or at least about 90% on a dry weight basis of the formulation. A typical range of tobacco material within the formulation is about 1 to about 99%, more often about 10 to about 50% by weight on a dry basis.

**[0086]** The whitened tobacco material used for the manufacture of the oral products of the invention preferably is provided in a ground, granulated, fine particulate, or powdered form. Although not strictly necessary, the whitened tobacco material may be subjected to processing steps that provide a further grinding for further particle size reduction. The whitening processes of the present invention generally provide a whitened tobacco material with a decreased amount of high molecular weight compounds, leading to more interstitial room and thus higher possible water content in tobacco materials produced therefrom than those from unwhitened

tobacco materials. In certain embodiments, the oral products produced according to the invention provide for faster nicotine release than products produced from unwhitened tobacco materials.

**[0087]** Example flavorants that can be used are components, or suitable combinations of those components, that act to alter the bitterness, sweetness, sourness, or saltiness of the oral product, enhance the perceived dryness or moistness of the formulation, or the degree of tobacco taste exhibited by the formulation. Flavorants may be natural or synthetic, and the character of the flavors imparted thereby may be described, without limitation, as fresh, sweet, herbal, confectionary, floral, fruity, or spicy. Specific types of flavors include, but are not limited to, vanilla, coffee, chocolate/cocoa, cream, mint, spearmint, menthol, peppermint, wintergreen, eucalyptus, lavender, cardamom, nutmeg, cinnamon, clove, cascarilla, sandalwood, honey, jasmine, ginger, anise, sage, licorice, lemon, orange, apple, peach, lime, cherry, strawberry, and any combinations thereof. See also, Leffingwell et al., Tobacco Flavoring for Smoking Products, R. J. Reynolds Tobacco Company (1972). Flavorings also may include components that are considered moistening, cooling or soothing agents, such as eucalyptus. These flavors may be provided neat (i.e., alone) or in a composite (e.g., spearmint and menthol, or orange and cinnamon). Representative types of components also are set forth in US Pat. No. 5,387,416 to White et al.; US Pat. App. Pub. No. 2005/0244521 to Strickland et al.; and PCT Application Pub. No. WO 05/041699 to Quinter et al. Types of flavorants include salts (e.g., sodium chloride, potassium chloride, sodium citrate, potassium citrate, sodium acetate, potassium acetate, and the like), natural sweeteners (e.g., fructose, sucrose, glucose, maltose, mannose, galactose, lactose, and the like), artificial sweeteners (e.g., sucralose, saccharin, aspartame, acesulfame K, neotame, and the like); and mixtures thereof. The amount of flavorants utilized in the tobacco composition can vary, but is typically up to about 10 dry weight percent, and certain embodiments are characterized by a flavorant content of at least about 1 dry weight percent, such as about 1 to about 10 dry weight percent. Combinations of flavorants are often used, such as about 0.1 to about 2 dry weight percent of an artificial sweetener, about 0.5 to about 8 dry weight percent of a salt such as sodium chloride and about 1 to about 5 dry weight percent of an additional flavoring.

**[0088]** Example filler materials include vegetable fiber materials such as sugar beet fiber materials (e.g., FIBREX<sup>®</sup> brand filler available from International Fiber Corporation), oats or other cereal grain (including processed or puffed grains), bran fibers, starch, or other modified or natural cellulosic materials such as microcrystalline cellulose. Additional specific examples include corn starch, maltodextrin, dextrose, calcium carbonate, calcium phosphate, lactose, mannitol, xylitol, and sorbitol. The amount of filler, where utilized in the tobacco composition, can vary, but is typically up to about 60 dry weight percent, and certain embodiments are characterized by a filler content of up to about 50 dry weight percent, up to about 40 dry weight percent or up to about 30 dry weight percent. Combinations of fillers can also be used.

**[0089]** Typical binders can be organic or inorganic, or a combination thereof. Representative binders include povidone, sodium carboxymethylcellulose and other modified cellulosic materials, sodium alginate, xanthan gum, starch-based binders, gum arabic, pectin,

carrageenan, pullulan, zein, and the like. The amount of binder utilized in the tobacco composition can vary, but is typically up to about 30 dry weight percent, and certain embodiments are characterized by a binder content of at least about 5 dry weight percent, such as about 5 to about 30 dry weight percent.

**[0090]** Preferred pH adjusters or buffering agents provide and/or buffer within a pH range of about 6 to about 10, and example agents include metal hydroxides, metal carbonates, metal bicarbonates, and mixtures thereof. Specific example materials include citric acid, sodium hydroxide, potassium hydroxide, potassium carbonate, sodium carbonate, and sodium bicarbonate. The amount of pH adjuster or buffering material utilized in the tobacco composition can vary, but is typically up to about 5 dry weight percent, and certain embodiments can be characterized by a pH adjuster/buffer content of less than about 0.5 dry weight percent, such as about 0.05 to about 0.2 dry weight percent. Particularly in embodiments comprising an extract clarified by distillation, the pH may be lowered by the addition of one or more pH adjusters (e.g., citric acid).

**[0091]** A colorant may be employed in amounts sufficient to provide the desired physical attributes to the tobacco formulation. Example colorants include various dyes and pigments, such as caramel coloring and titanium dioxide. The amount of colorant utilized in the tobacco composition can vary, but is typically up to about 3 dry weight percent, and certain embodiments are characterized by a colorant content of at least about 0.1 dry weight percent, such as about 0.5 to about 3 dry weight percent.

**[0092]** Example humectants include glycerin and propylene glycol. The amount of humectant utilized in the tobacco composition can vary, but is typically up to about 5 dry weight percent, and certain embodiments can be characterized by a humectant content of at least about 1 dry weight percent, such as about 2 to about 5 dry weight percent.

**[0093]** Other ingredients such as preservatives (e.g., potassium sorbate), disintegration aids (e.g., microcrystalline cellulose, croscarmellose sodium, crospovidone, sodium starch glycolate, pregelatinized corn starch, and the like), and/or antioxidants can also be used. Typically, such ingredients, where used, are used in amounts of up to about 10 dry weight percent and usually at least about 0.1 dry weight percent, such as about 0.5 to about 10 dry weight percent. A disintegration aid is generally employed in an amount sufficient to provide control of desired physical attributes of the tobacco formulation such as, for example, by providing loss of physical integrity and dispersion of the various component materials upon contact of the formulation with water (e.g., by undergoing swelling upon contact with water).

**[0094]** In some embodiments, any of the components described above can be added in an encapsulated form (e.g., in the form of microcapsules), the encapsulated form a wall or barrier structure defining an inner region and isolating the inner region permanently or temporarily from the tobacco composition. The inner region includes a payload of an additive either adapted for enhancing one or more sensory characteristics of the oral product, such as taste, mouthfeel, moistness, coolness/heat, and/or fragrance, or adapted for adding an additional

functional quality to the oral product, such as addition of an antioxidant or immune system enhancing function. See, for example, the subject matter of US Pat. Appl. Pub. No. 2009/0025738 to Mua et al.

**[0095]** Representative tobacco formulations may incorporate about 5% to about 95% percent whitened tobacco material, about 5 to about 60% filler, about 0.1% to about 5% artificial sweetener, about 0.5% to about 2% salt, about 1% to about 5% flavoring, about 1% to about 5% humectants (e.g., propylene glycol), and up to about 10% pH adjuster or buffering agent (e.g., sodium bicarbonate or citric acid), based on the total dry weight of the tobacco formulation. The particular percentages and choice of ingredients will vary depending upon the desired flavor, texture, and other characteristics.

**[0096]** Descriptions of various components of snus types of products and components thereof also are set forth in US Pat. App. Pub. No. 2004/0118422 to Lundin et al. See, also, for example, US Pat. Nos. 4,607,479 to Linden; 4,631,899 to Nielsen; 5,346,734 to Wydick et al.; and 6,162,516 to Derr, and US Pat. Pub. No. 2005/0061339 to Hansson et al.

**[0097]** The components of the tobacco composition can be brought together in admixture using any mixing technique or equipment known in the art. The optional components noted above, which may be in liquid or dry solid form, can be admixed with the whitened tobacco material in a pretreatment step prior to mixture with any remaining components of the composition or simply mixed with the whitened tobacco material together with all other liquid or dry ingredients. Any mixing method that brings the tobacco composition ingredients into intimate contact can be used. A mixing apparatus featuring an impeller or other structure capable of agitation is typically used. Example mixing equipment includes casing drums, conditioning cylinders or drums, liquid spray apparatus, conical-type blenders, ribbon blenders, mixers available as FKM130, FKM600, FKM1200, FKM2000 and FKM3000 from Littleford Day, Inc., Plough Share types of mixer cylinders, and the like. As such, the overall mixture of various components with the whitened tobacco material may be relatively uniform in nature. See also, for example, the types of methodologies set forth in US Pat. No. 4,148,325 to Solomon et al.; US Pat. No. 6,510,855 to Korte et al.; and US Pat. No. 6,834,654 to Williams. Manners and methods for formulating snus-type tobacco formulations will be apparent to those skilled in the art of snus tobacco product production.

**[0098]** The moisture content of the oral product prior to use by a consumer of the formulation may vary. Typically, the moisture content of the product, as present within the pouch prior to insertion into the mouth of the user, is less than about 55 weight percent, generally is less than about 50 weight percent, and often is less than about 45 weight percent. For certain oral products, such as those incorporating snus-types of tobacco compositions, the moisture content may exceed 20 weight percent, and often may exceed 30 weight percent. For example, a representative snus-type product may possess a tobacco composition exhibiting a moisture content of about 20 weight percent to about 50 weight percent, preferably about 20 weight percent to about 40 weight percent.

**[0099]** The manner by which the moisture content of the formulation is controlled may vary. For example, the formulation may be subjected to thermal or convection heating. As a specific example, the formulation may be oven-dried, in warmed air at temperatures of about 40°C to about 95°C, with a preferred temperature range of about 60°C to about 80°C for a length of time appropriate to attain the desired moisture content. Alternatively, tobacco formulations may be moistened using casing drums, conditioning cylinders or drums, liquid spray apparatus, ribbon blenders, or mixers. Most preferably, moist tobacco formulations, such as the types of tobacco formulations employed within snus types of products, are subjected to pasteurization or fermentation. Techniques for pasteurizing/heat treating and/or fermenting snus types of tobacco products will be apparent to those skilled in the art of snus product design and manufacture.

**[0100]** The acidity or alkalinity of the tobacco formulation, which is often characterized in terms of pH, can vary. Typically, the pH of that formulation is at least about 6.5, and preferably at least about 7.5. In some embodiments, the pH of that formulation will not exceed about 11, or will not exceed about 9, and often will not exceed about 8.5. A representative tobacco formulation exhibits a pH of about 6.8 to about 8.2 (e.g., about 7.8). A representative technique for determining the pH of a tobacco formulation involves dispersing 5 g of that formulation in 100 ml of high performance liquid chromatography water, and measuring the pH of the resulting suspension/solution (e.g., with a pH meter).

**[0101]** In certain embodiments, the whitened tobacco material and any other components noted above are combined within a moisture-permeable packet or pouch that acts as a container for use of the tobacco. The composition/construction of such packets or pouches, such as the container pouch 20 in the embodiment illustrated in Figure 1, may be varied. Suitable packets, pouches or containers of the type used for the manufacture of smokeless tobacco products are available under the tradenames CatchDry, Ettan, General, Granit, Goteborgs Rape, Grovsnus White, Metropol Kaktus, Mocca Anis, Mocca Mint, Mocca Wintergreen, Kicks, Probe, Prince, Skruf, Epok, and TreAnkrare. The tobacco formulation may be contained in pouches and packaged, in a manner and using the types of components used for the manufacture of conventional snus types of products. The pouch provides a liquid-permeable container of a type that may be considered to be similar in character to the mesh-like type of material that is used for the construction of a tea bag. Components of the loosely arranged, granular tobacco formulation readily diffuse through the pouch and into the mouth of the user.

**[0102]** Non-limiting examples of suitable types of pouches are set forth in, for example, US Pat. Nos. 5,167,244 to Kjerstad and 8,931,493 to Sebastian et al.; as well as US Patent App. Pub. Nos. 2016/0000140 to Sebastian et al.; 2016/0073689 to Sebastian et al.; 2016/0157515 to Chapman et al.; and 2016/0192703 to Sebastian et al. Pouches can be provided as individual pouches, or a plurality of pouches (e.g., 2, 4, 5, 10, 12, 15, 20, 25 or 30 pouches) can be connected or linked together (e.g., in an end-to-end manner) such that a single pouch or individual portion can be readily removed for use from a one-piece strand or matrix of pouches.

**[0103]** A pouch may, for example, be manufactured from materials, and in such a manner, such that during use by the user, the pouch undergoes a controlled dispersion or dissolution. Such pouch materials may have the form of a mesh, screen, perforated paper, permeable fabric, or the like. For example, pouch material manufactured from a mesh-like form of rice paper, or perforated rice paper, may dissolve in the mouth of the user. As a result, the pouch and tobacco formulation each may undergo complete dispersion within the mouth of the user during normal conditions of use, and hence the pouch and tobacco formulation both may be ingested by the user. Other example pouch materials may be manufactured using water dispersible film forming materials (e.g., binding agents such as alginates, carboxymethylcellulose, xanthan gum, pullulan, and the like), as well as those materials in combination with materials such as ground cellulose (e.g., fine particle size wood pulp). Preferred pouch materials, though water dispersible or dissolvable, may be designed and manufactured such that under conditions of normal use, a significant amount of the tobacco formulation contents permeate through the pouch material prior to the time that the pouch undergoes loss of its physical integrity. If desired, flavoring ingredients, disintegration aids, and other desired components, may be incorporated within, or applied to, the pouch material. In various embodiments, a nonwoven web can be used to form an outer water-permeable pouch which can be used to house a composition adapted for oral use.

**[0104]** The amount of material contained within each product unit, for example, a pouch, may vary. In some embodiments, the weight of the material within each pouch is at least about 50 mg, for example, from about 50 mg to about 1 gram, from about 100 to 800 about mg, or from about 200 to about 700 mg. In some smaller embodiments, the weight of the material within each pouch may be from about 100 to about 300 mg. For a larger embodiment, the weight of the material within each pouch may be from about 300 mg to about 700 mg. If desired, other components can be contained within each pouch. For example, at least one flavored strip, piece or sheet of flavored water dispersible or water soluble material (e.g., a breath-freshening edible film type of material) may be disposed within each pouch along with or without at least one capsule. Such strips or sheets may be folded or crumpled in order to be readily incorporated within the pouch. See, for example, the types of materials and technologies set forth in US Pat. Nos. 6,887,307 to Scott et al. and 6,923,981 to Leung et al.; and The EFSA Journal (2004) 85, 1-32.

**[0105]** The oral product can be packaged within any suitable inner packaging material and/or outer container. See also, for example, the various types of containers for smokeless types of products that are set forth in US Pat. Nos. 7,014,039 to Henson et al.; 7,537,110 to Kutsch et al.; 7,584,843 to Kutsch et al.; D592,956 to Thiellier; D594,154 to Patel et al.; and D625,178 to Bailey et al.; US Pat. Pub. Nos. 2008/0173317 to Robinson et al.; 2009/0014343 to Clark et al.; 2009/0014450 to Bjorkholm; 2009/0250360 to Bellamah et al.; 2009/0266837 to Gelardi et al.; 2009/0223989 to Gelardi; 2009/0230003 to Thiellier; 2010/0084424 to Gelardi; and 2010/0133140 to Bailey et al.; 2010/0264157 to Bailey et al.; 2011/0168712 to Bailey et al.; and 2011/0204074 to Gelardi et al.

**[0106]** Products of the present disclosure may be packaged and stored in much the same manner that conventional types of oral products are packaged and stored. For example, a plurality of packets or pouches may be contained in a container used to contain oral products, such as a cylindrical container sometimes referred to as a "puck". The container can be any shape, and is not limited to cylindrical containers. Such containers may be manufactured out of any suitable material, such as metal, molded plastic, fiberboard, combinations thereof, etc. If desired, moist oral products (e.g., products having moisture contents of more than about 20 weight percent) may be refrigerated (e.g., at a temperature of less than about 10° C, often less than about 8 °C, and sometimes less than about 5 °C). Alternatively, relatively dry oral products (e.g., products having moisture contents of less than about 15 weight percent) often may be stored under a relatively wide range of temperatures.

**[0107]** Various oral products disclosed herein are advantageous in that they provide a composition that is non-staining, or is staining to a lesser degree than products comprising only unwhitened tobacco materials. These products thus are desirable in reducing staining of teeth and clothing that may come in contact therewith. It is noted that even the spent (used) product is lighter in color than traditional spent (used) oral tobacco products. Further, the products may have enhanced visual appeal by virtue of their whitened color.

**[0108]** The following examples are provided to further illustrate embodiments of the present disclosure, but should not be construed as limiting the scope thereof. Unless otherwise noted, all parts and percentages are by weight.

## **EXPERIMENTAL**

**[0109]** Embodiments of the present disclosure are more fully illustrated by the following examples, which are set forth to illustrate aspects of the present disclosure and are not to be construed as limiting thereof. In the following examples, g means gram, L means liter, mL means milliliter, and Da means daltons. All weight percentages are expressed on a dry basis, meaning excluding water content, unless otherwise indicated.

**[0110]** It is noted that the raw tobacco material used in each of the examples below, including the comparative examples, was Flue Cured Virginia Stems that was grown in Italy. The stems are a standard tobacco raw material available on the market and commercially used in products as an alternative for the lamina.

**[0111]** It is further noted that each of the kg/t units in the Examples below are referring to kilograms per tonne.

### **Example 1**

[0112] Extracted tobacco materials were subjected to a Kraft cook at a pH of about 14 according to embodiments of the present disclosure.

[0113] The input tobacco materials were subjected to an aqueous extraction process before the cook (i.e., pulping process). The water extraction was done at a temperature of about 85°C for an extraction time of about 60 mins. The liquid/material ratio of the aqueous extraction was about 8:1.

[0114] The extracted tobacco solids material was cooked with a commercially available white liquor comprising water, sodium hydroxide (NaOH), and sodium sulfide (Na<sub>2</sub>S) (pH of cooking liquor was about 14). The weight ratio of liquid to tobacco material was about 10:1. The tobacco solids material was cooked for about 90 mins at a temperature of about 20°C-160°C, and then at a max temperature of about 160°C for 90-180 mins.

[0115] The results from the Kraft cooks are presented in Table 1 below.

**Table 1 - Kraft cooks at pH 14**

Cook Type	Extraction Solvent	Cook Time (h)	Chemical Charge, % as Na <sub>2</sub> O	Yield %	Kappa	Ash % 525°C	ISO Brightness %
Kraft (NaOH and Na <sub>2</sub> S)	Water 90°C, 60 mins	1.5	25	32.8	31.3	24.4	8.3
	Water 90°C, 60 mins	3	25	34.4	33.6	24.1	6.7

[0116] The yield from the Kraft cooks was relatively high as compared to other pulping processes known in the art (>30%). The ISO brightness following the Kraft cook was less than about 10%.

### **Example 2**

[0117] Another cook was done according to the Kraft process as generally described in Example 1 above. For this second Kraft cook, the time at which the tobacco solids material was cooked at max temperature of about 160°C was reduced to about 135 mins. The yield and other properties of the pulp produced from this cook are provided in Table 2 below. These resulting tobacco pulp materials were also bleached, as described in Example 3 below.

**Table 2 - Results for second Kraft cook**

Analyze	Sulfate (Kraft) Cook (Example 1)
Kappa	26.5
ISO Brightness (%)	10.3

Analyze	Sulfate (Kraft) Cook (Example 1)
Ash 525°C (%)	26.5
Yield (%)	34.3
Reject (uncooked material) (%)	0.5

[0118] It is noted that the ISO brightness % for the pulp produced from Kraft cook according to Example 2 was slightly higher than the ISO brightness % for the pulp produced from the Kraft cook according to Example 1 above.

### Example 3

[0119] Tobacco pulp was produced according to the Kraft cook provided in Example 1 above. The tobacco pulp was bleached using one or more of an acid treatment stage (A), a chelating stage (Q), and a peroxide bleaching stage (P).

[0120] For an acid pre-treatment stage (A), the tobacco pulp was treated with sulfuric acid at a pH of about 2.5, at a temperature of about 60°C, for a time of about 90 mins. The pulp consistency was about 10% during the acid treatment.

[0121] For a chelating pre-treatment stage (Q), the tobacco pulp was treated with EDTA at a pH of about 5.5-6.0, at a temperature of about 70°C, for a time of about 60 mins. The pulp consistency was about 5% during the chelating treatment.

[0122] For a peroxide bleaching stage (P), the tobacco pulp was treated with NaOH (40 kg/t), MgSO<sub>4</sub> (15 kg/t), and H<sub>2</sub>O<sub>2</sub> (100-200 kg/t) at a pH of about 10.0-11.5, at a temperature of about 90°C, for a time of about 90 mins. The pulp consistency was about 10% during the peroxide treatment. For bleaching sequences with two peroxide stages for the Kraft pulped material, the H<sub>2</sub>O<sub>2</sub> charge for each peroxide bleaching stage was 100 kg/t.

[0123] Table 3 below shows the results for tobacco pulp prepared according to an embodiment of the present disclosure provided in Example 1 above (Kraft cook) that was then subjected to various bleaching sequences.

**Table 3 - Results from bleaching trials of Kraft cooked tobacco pulp**

Sample (peroxide charge)	ISO Brightness	Whiteness ASTM	Kappa	Ash 525°C (%)
AQ (0 kg/t)	-	-	27.1	9.3
AQP (100 kg/t)	44.9	-5	10.7	10.1
AQP (150kg/t)	44.8	-4	11	10.3
AQP (200 kg/t)	45.3	-4	10.3	10.6

Sample (peroxide charge)	ISO Brightness	Whiteness ASTM	Kappa	Ash 525°C (%)
AQPP (100, 100 kg/t)	34.9	-14	9	10.8
AQPQP (100, 100 kg/t)	39.7	-10	7.5	7.2
AQPAQP (100, 100 kg/t)	45.1	-6	5.3	1.2

[0124] The tobacco pulps bleached with 200 kg/t peroxide in the sequence AQP and with 100 kg/t, 100 kg/t peroxide in the sequence AQPAQP produced the best brightness and whiteness values.

[0125] The ISO brightness values for the pulps bleached with different charges of peroxide in the sequence AQP are about the same level of brightness. Without intending to be limited by theory, one explanation as to why the brightness did not noticeably increase with a higher charge of peroxide can be that the end pH of the pulp for the 150 kg/t and 200 kg/t charges of peroxide was too high. The end pH of these trials was almost 13, which can cause darkening of the bleached material. Similar results were seen in the trials with a second P-stage. The end pH of the pulp was over 12 following the second P-stage in each of those trials.

[0126] The inorganics (e.g., SiO<sub>2</sub>, Mn, Mg, and Ca) in the tobacco pulp after bleaching with the AQP sequence were analyzed. The results are provided in Table 4 below. The inorganic content of the tobacco materials bleached with two peroxide (P) stages showed that an extra A-stage and an extra Q-stage applied to the tobacco materials is effective to lower the metal content in the bleached tobacco materials. A low metal content is beneficial for the bleaching/whitening results of the peroxide stage.

**Table 4 - Inorganic content in the Kraft cooked tobacco pulps bleached with different bleaching sequences**

Sample	Ash 525°C	SiO <sub>2</sub> (mg/kg)	Mn (mg/kg)	Mg (mg/kg)	Fe (mg/kg)	Cu (mg/kg)	Ca (mg/kg)	K (mg/kg)
AQPP (100, 100 kg/t)	10.8	1684	21.6	6330	183	8.4	36600	37.3
AQPQP (100, 100 kg/t)	7.2	1498	10.7	3900	122	3.3	24400	31.8
AQPAQP (100, 100 kg/t)	1.2	1295	1.0	3150	95.1	3.0	851	21.8

#### **Example 4**

[0127] Tobacco pulp was produced according to the Kraft cook provided in Example 2 above. Specifically, the tobacco solids material was cooked for about 90 mins at a temperature of about 20°C-160°C, and then at a max temperature of about 160°C for 135 mins. The pulp was bleached using one or more of an acid treatment stage (A), a chelating stage (Q), and a peroxide bleaching stage (P). The parameters of any acid treatment or chelating stages were the same as those provided in Example 3 above.

[0128] For a first peroxide bleaching stage (P) in these trials, the tobacco pulp was treated with NaOH (35 kg/t), MgSO<sub>4</sub> (15 kg/t), and HzOz (100 kg/t) at a pH of about 10.0-11.5, at a temperature of about 90°C, for a time of about 90 mins. The pulp consistency was about 10% during the peroxide treatment. For a second peroxide bleaching stage (P), the tobacco pulp was treated with NaOH (40 and 50 kg/t), MgSO<sub>4</sub> (15 kg/t), and HzOz (150 and 200 kg/t) at a pH of about 10.0-11.5, at a temperature of about 90°C, for a time of about 90 mins. The pulp consistency was about 10% during the peroxide treatment.

[0129] In one of the bleaching trials, bleached softwood pulp was added to the tobacco pulp (produced from the Kraft cook). The weight ratio of bleached softwood pulp to tobacco pulp was 1:4.

[0130] Table 5 below shows the results for tobacco pulp prepared according to an embodiment of the present disclosure provided in Example 2 above (Kraft cook) that was then subjected to various bleaching sequences.

**Table 5 - Results from bleachins trials of Kraft pulp**

Bleaching Sequence	Bleached Softwood Pulp (%)	Peroxide (kg/t)	ISO Brightness (%)	Whiteness C/2 ASTM	Ash 525°C (%)	Kappa	Yield (%)
AQPAQP	0	100 + 150	49.6	-12.6	1.4	5.4	67.9
AQPAQP	0	100 + 200	59.5	14.7	1.4	5.4	n.a.
AQPAQP	20	100 + 150	71.4	36.4	1.3	5.0	n.a.

[0131] Target whiteness based on ASTM E313-73 Whiteness Test for these bleaching trials was about 10 or greater. Target whiteness was achieved when 200 kg/t of peroxide was charged in the second P-stage and also when 20% dissolving pulp was added to the tobacco solids material. A low ash content and low kappa number was obtained in all samples. The yield was determined to be 67.9% for the entire whitening process (i.e., the hot water extraction, the Kraft cook, and the AQPAQP bleaching sequence).

[0132] The yield for the Kraft bleaching process according to the present example with the AQPAQP bleaching sequence (100 kg/t and 200 kg/t peroxide charges) was measured in each

process step and overall. The results are provided in Table 6 below.

**Table 6 - Yield from Kraft Bleaching Process**

Process Stage	Kraft Bleaching Process	
	Yield in Each Process Step (%)	Total Yield (%)
Water Extraction	62.9	62.9
Cook	34.3	21.6
Bleaching AQP	-	-
Bleaching AQPAQP	67.9	14.6
<b>Total Yield (%)</b>		<b>14.6</b>

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**Patentkrav**

**1.** Fremgangsmåde til fremstilling af et bleget tobaksmateriale, omfattende:

- (i) at ekstrahere et tobaksmateriale med en første ekstraktionsopløsning for at tilvejebringe et tobaksfaststofmateriale og en tobaksekstrakt;
- 5 (ii) at tilberede tobaksfaststofmaterialet i en alkalisk tilberedningsvæske omfattende natriumsulfid og med en pH på mere end 11 for at danne en tobakspulp;
- (iii) at behandle tobakspulpen med en syre for at sænke pH'en af tobakspulpen og tilvejebringe en neutraliseret tobakspulp;
- 10 (iv) at ekstrahere den neutraliserede tobakspulp med en anden ekstraktionsopløsning omfattende mindst et chelateringsmiddel for at tilvejebringe en ekstraheret tobakspulp; og
- (v) at blege den ekstraherede tobakspulp med en blegeopløsning for at tilvejebringe et bleget tobaksmateriale.

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**2.** Fremgangsmåden ifølge krav 1, hvor tilberedningen af tobaksfaststofmaterialet udføres ved en temperatur på ca. 165°C eller derunder.

**3.** Fremgangsmåden ifølge krav 1, yderligere omfattende tørring af det blegede tobaksmateriale til et fugtindhold på mindre end ca. 30 procent fugt på våd basis for at tilvejebringe det blegede tobaksmateriale.

**4.** Fremgangsmåden ifølge krav 1, hvor blegningen af den ekstraherede tobakspulp udføres ved en temperatur i området fra ca. 60°C til ca. 90°C.

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**5.** Fremgangsmåden ifølge krav 1, hvor behandling af tobakspulpen med en syre for at sænke pH'en af tobakspulpen udføres ved en pH på ca. 2 til ca. 6.

**6.** Fremgangsmåden ifølge krav 1, hvor syren er svovlsyre.

30

**7.** Fremgangsmåden ifølge krav 1, hvor ekstraktion af den neutraliserede tobakspulp med en anden ekstraktionsopløsning udføres ved en pH på ca. 4 til ca. 7.

**8.** Fremgangsmåden ifølge krav 1, hvor chelateringsmidlet er EDTA.

**9.** Fremgangsmåden ifølge krav 1, hvor ekstraktionen af tobaksmaterialet udføres ved en temperatur på ca. 100°C eller derunder.

5

**10.** Fremgangsmåden ifølge krav 1, yderligere omfattende formaling af det blegede tobaksmateriale til en størrelse i området fra ca. 5 mm til ca. 0,1 mm.

**11.** Fremgangsmåden ifølge krav 1, yderligere omfattende blanding af mindst et  
10 af tobaksfaststofmaterialet og tobakspulpen med en træpulp før blegning af tobakspulpen.

**12.** Fremgangsmåden ifølge et hvilket som helst af kravene 1-11, yderligere omfattende:

15 (vi) at behandle det blegede tobaksmateriale med en anden syre for at sænke pH'en af det blegede tobaksmateriale og tilvejebringe et neutraliseret tobaksmateriale;

(vii) at ekstrahere det neutraliserede tobaksmateriale med en anden vandig opløsning omfattende et andet chelateringsmiddel for at tilvejebringe et  
20 ekstraheret tobaksmateriale; og

(viii) at blege det ekstraherede tobaksmateriale med en anden blegeopløsning for at tilvejebringe et andet bleget tobaksmateriale.

**13.** Fremgangsmåden ifølge et hvilket som helst af kravene 1-12, yderligere  
25 omfattende inkorporering af det blegede tobaksmateriale i et produkt konfigureret til brændbar aerosollevering, et produkt konfigureret til ikke-brændbar aerosollevering eller et produkt konfigureret til aerosolfri levering.

**14.** Fremgangsmåden ifølge krav 13, omfattende inkorporering af det blegede  
30 tobaksmateriale i et oralt produkt, hvor det orale produkt yderligere omfatter en eller flere yderligere komponenter udvalgt fra gruppen bestående af smagsstoffer, aktive ingredienser, fyldstoffer, bindemidler, pH-justerende midler, buffermidler, farvestoffer, desintegrationshjælpemidler, antioxidanter, fugtighedsbevarende midler og konserveringsmidler.

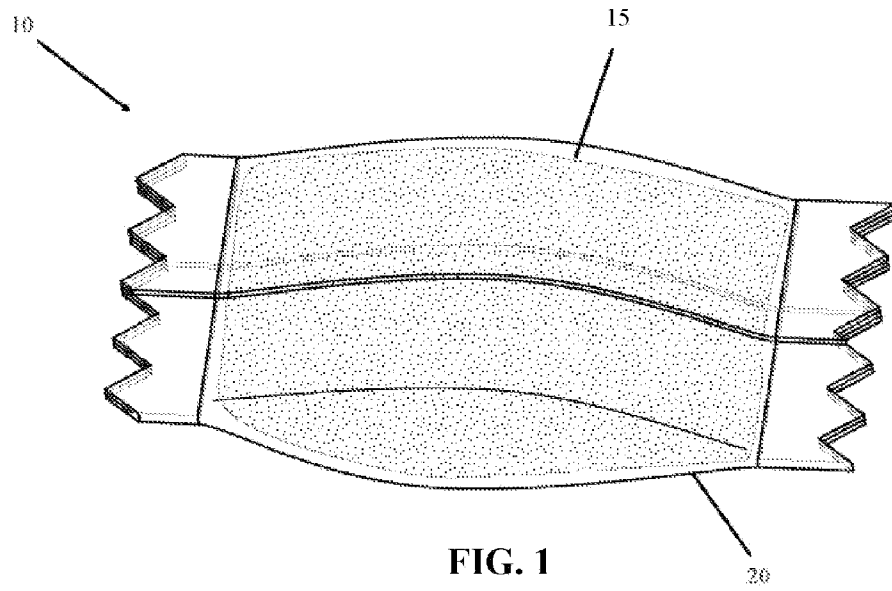
35

**15.** Fremgangsmåden ifølge krav 1, hvor den anden ekstraktionsopløsning er en første vandig opløsning, der omfatter et første chelateringsmiddel; hvor blegeopløsningen er en første blegeopløsning omfattende et første oxidationsmiddel; og yderligere omfattende:

- 5           (vi) at behandle det blegede tobaksmateriale med en anden syre for at sænke pH'en af det blegede tobaksmateriale og tilvejebringe et neutraliseret tobaksmateriale;
- (vii) at ekstrahere det neutraliserede tobaksmateriale med en anden vandig opløsning omfattende et andet chelateringsmiddel for at tilvejebringe et
- 10           ekstraheret tobaksmateriale; og
- (viii) at blege det ekstraherede tobaksmateriale med en anden blegeopløsning omfattende et andet oxidationsmiddel for at tilvejebringe et endeligt bleget tobaksmateriale.

# DRAWINGS

Drawing



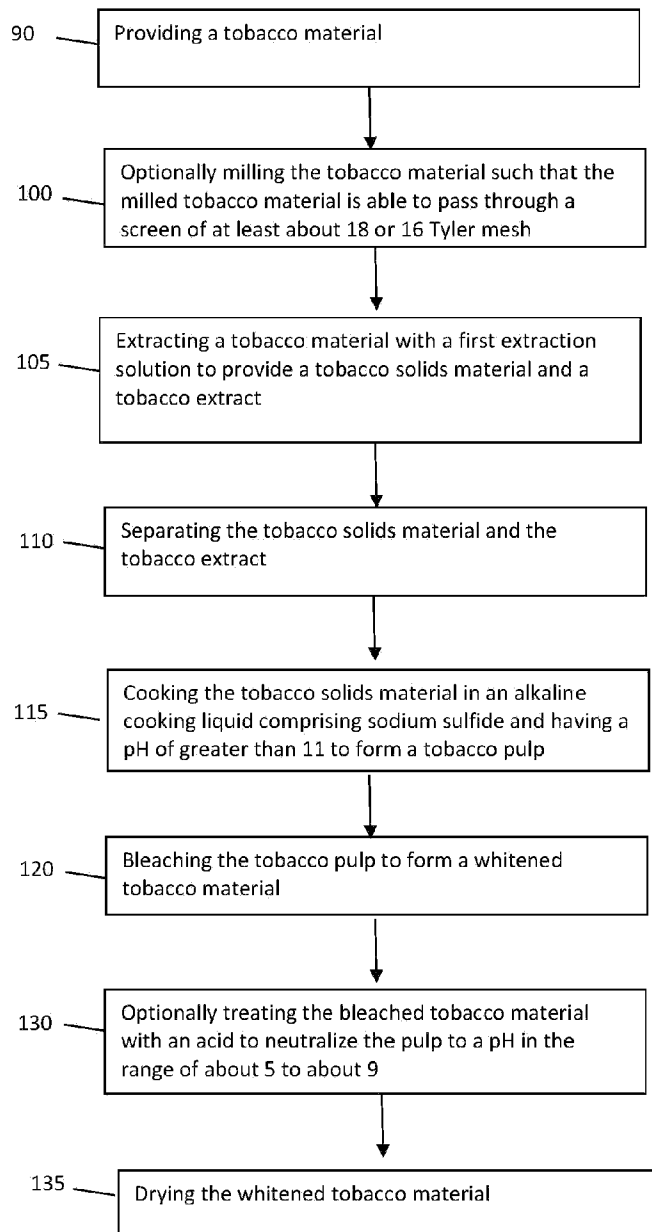


FIG. 2

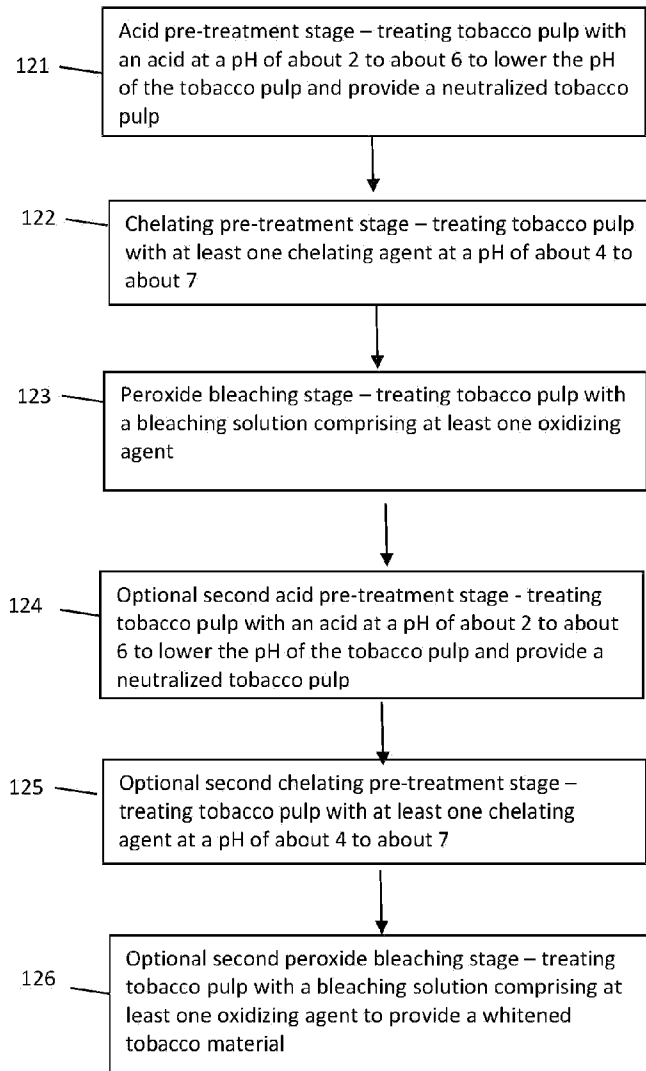


FIG. 3