Title: COMPOSITIONS FOR INJECTION MOULDING

Abstract: Use of a filled polymer resin in the manufacture of an article therefrom by injection moulding, a method of manufacturing an article by injection moulding a filled polymer resin, a method for enabling or improving the injection mouldability of a polymer resin comprising recycled polymer, wherein the polymer resin comprises recycled polymer and functional filler, the use of a functional filler in a polymer resin comprising recycled polymer to improve the injection mouldability of the polymer resin, an article of manufacture obtained by injection moulding a filled polymer resin, and a filled polymer resin.
COMPOSITIONS FOR INJECTION MOULDING

TECHNICAL FIELD

The present invention is directed to the use of a filled polymer resin in the manufacture of an article therefrom by injection moulding, to a method of manufacturing an article by injection moulding a filled polymer resin, to a method for enabling or improving the injection mouldability of a polymer resin comprising recycled polymer, wherein the polymer resin comprises recycled polymer and functional filler, to the use of a functional filler in a polymer resin comprising recycled polymer to improve the injection mouldability of the polymer resin, to an article of manufacture obtained by injection moulding a filled polymer resin, and to a filled polymer resin.

BACKGROUND OF THE INVENTION

There is an ever increasing demand to recycle and re-use polymer materials since this provides cost and environmental benefits. However, the reprocessing of recycled polymer waste presents challenges which are not necessarily encountered during processing of polymer compositions derived from virgin polymer. For example, recycled polymers may be unsuitable for injecting moulding.

As the need to recycle polymer waste materials increases, there is a continuing need for the development of new compositions for the economically viable processing of polymer waste materials into high quality articles of manufacture.

SUMMARY OF THE INVENTION

According to a first aspect, the present invention is directed to the use of a filled polymer resin in the manufacture of an article therefrom by injection moulding, wherein the polymer resin comprises recycled polymer and functional filler, wherein the functional filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_m$ of less than about 2.5 $\mu\text{m}$, and wherein the filled polymer resin has:

1. a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or
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(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding; and/or

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, for example, less than about 2.0 g/10 min, and optionally:

(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or

(b) a SFN which is at least 80% of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8.0 g/10 mins @ 2.16 kg/190°C.

According to a second aspect, the present invention is directed to a method of manufacturing an article by injection moulding, the method comprising injection moulding an article from a filled polymer resin, wherein the filled polymer resin comprises recycled polymer and functional filler, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a dso of less than about 2.5 μm, and wherein the filled polymer resin has:

(1) a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or

(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding; and/or

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, for example, less than about 2.0 g/10 min, and optionally:

(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or

(b) a SFN which is at least 80% of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190°C.

According to a third aspect, the present invention is directed to the use of a functional filler in a polymer resin comprising recycled polymer MFI to improve the injection
mouldability of the polymer resin, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_m$ of less than about 2.5 pm.

According to a fourth aspect, the present invention is directed to a method for enabling or improving the injection mouldability of a polymer resin comprising recycled polymer, the method comprising filling the polymer resin with a functional filler, forming a filled polymer resin, and manufacturing an article of manufacture from the filled polymer resin by injection moulding, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_m$ of less than about 2.5 pm, and wherein the filled polymer resin has:

(1) a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or

(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding; and/or

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, for example, less than about 2.0 g/10 mins, and

(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 mins, and/or

(b) a SFN which is at least 80% of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190°C.

According to a fifth aspect, the present invention is directed to an article of manufacture obtained by injection moulding a filled polymer resin as defined in any of the first, second, third or fourth aspects.

According to a sixth aspect, the present invention is directed to a filled polymer resin suitable for use in the manufacture of an article therefrom by injection moulding, wherein the polymer resin comprises recycled polymer and functional filler, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_m$ of less than about 2.5 pm, and wherein the filled polymer resin has:
(1) a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or

(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the MFI of the filled polymer resin during injection moulding; and/or

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, for example, less than about 2.0 g/10 min, and optionally:

(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or

(b) a SFN which is at least 80 % of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190°C.

DETAILED DESCRIPTION OF THE INVENTION

Conventional wisdom is that a polymer resin must have a certain minimum Melt Flow Index (MFI) for it to be suitable for injection moulding. Surprisingly, however, it has been found that a polymer resin comprising recycled polymer and having a relatively low MFI (i.e., relative to the MFI of conventional virgin polymer resin used in injection moulding) can be injected moulded providing functionally and aesthetically acceptable articles of manufacture by filling the polymer resin with a functional filler. The filled polymer resin derived from recycled polymer may perform better even than virgin polymer resin. Without wishing to be bound by theory, it is believed that the polymer resin having a relatively low MFI under testing behaves differently than expected during injection moulding - it injection moulds as if it had a much higher MFI than the MFI measured under testing. It is currently believed that shear thinning effects take place. This surprising finding enables greater utility of recycled polymers previously thought unsuitable for injection moulding, and may provide cost and environmental benefits as injection moulded articles, particularly thin-walled articles of manufacture, can be manufactured from a greater variety of recycled polymers (including mixed polymer), which is normally cheaper than virgin resin, and means reliance on virgin polymers may be reduced and utility of recycled polymers increased, which is environmentally desirable. Further, the inclusion of filler provides additional cost and environmental
benefits as less polymer is used. The filler is functionalised through incorporation of a
surface treatment and/or by controlling particle size.

As such, by "functional filler" is meant a filler material which enhances the
processability by Injection moulding of a polymer resin comprising recycled polymer.
The functional filler comprises inorganic particulate which (i) is surface treated and/or
(ii) has a \(d_{50}\) of no greater than about 2.5 pm. In certain embodiments, functional filler
comprises inorganic particulate having a \(d_{50}\) of no greater than about 2.5 pm which is
surface treated. In certain embodiments, the enhancement in processability may be
assessed by comparison with:

(i) the polymer resin absent the functional filler; and/or
(ii) the polymer resin filled with a filler which is not surface treated and/or has a \(d_{50}\)
greater than 2.5 pm; and/or
(iii) virgin polymer resin having an MFI of at least 2.0 g/10 mins @ 2.16 kg/190° C, or
at least 2.5 g/10 mins @ 2.16 kg/190° C, or from 2.0 g/10 mins to about 30 g/10
mins @ 2.16 kg/190° C, or from 2.5 g/10 mins to about 30 g/10 mins @ 2.16
kg/190° C; and/or
(iv) a virgin polymer resin having an MFI of at least 2.0 g/10 mins @ 2.16 kg/190° C,
or at least 2.5 g/10 mins @ 2.16 kg/190° C, or from 2.0 to about 30 g/10 mins @
2.16 kg/190° C, or from 2.5 g/10 mins to about 30 g/10 mins @ 2.16 kg/190° C,
and which is filled with the functional filler; and/or
(v) a virgin polymer resin having an MFI of at least 2.0 g/10 mins @ 2.16 kg/190° C,
or at least 2.5 g/10 mins @ 2.16 kg/190° C, or from 2.0 g/10 mins to about 30
kg/190° C, or from 2.5 g/10 mins to about 30 g/10 mins @ 2.16
kg/190° C, which is filled with a filler which is not surface treated and/or has a \(d_{50}\)
greater than 2.5 pm; and/or
(vi) a virgin polymer resin having a comparable MFI; and/or
(vii) a virgin polymer resin having a comparable MFI and which is filled with the
functional filler; and/or
(viii) a virgin polymer resin having a comparable MFI and which is filled with a filler
which is not surface treated and/or has a \(d_{50}\) greater than 2.5 pm; and/or
(ix) an unfilled virgin HDPE polymer resin having a MFI of 8.0. g/10 mins @ 2.16
kg/190° C.
Processability metrics include:

(1) the Spiral Flow Number (SFN) of the filled polymer resin (SFN is discussed in greater detail below)

(2) the surface finish of the article formed by injection moulding; and/or

(3) the colour of the article formed by injection moulding; and/or

(4) cycle time; and/or

(5) peak injection pressure (average and/or range, at equivalent MFI); and/or

(6) mould filling (i.e., flowability into and in the mould); and/or

(7) weight range across 32 shots; and/or

(8) de-moulding capability.

The filler polymer resin may be used in the manufacture of an article therefrom by injection moulded, or in a method of manufacturing an article by injection moulding. In certain embodiments, the functional filler is used to enable or improve the injection mouldability of a polymer resin comprising recycled polymer, or is used in a method for enabling or improving the injection mouldability of a polymer resin comprising recycled polymer. The use or method comprises filling the polymer resin with functional filler and manufacturing an article of manufacture therefrom by injection moulding.

In certain embodiments, the article of manufacture is processed from the filled polymer resin at a melt temperature of from about 190 °C to about 250 °C, for example, from about 200 °C to about 240 °C, or from about 205 °C to about 235 °C, or from about 210 °C to about 230 °C, or from about 215 °C to about 230 °C, or from about 220 °C to about 230 °C. Suitable barrel and feed throat temperature settings will be selected depending on the melt temperature.

In certain embodiments, the peak pressure average during injection moulding is from about 500 to 2000 bar, for example, from about 750 to 2000 bar, or from about 750 to about 1500 bar, or from about 750 to about 900 to about 1400 bar, or from about 900 to about 1300 bar, or from about 900 to about 1100 bar, or from about 1100 bar to about 1300 bar. Additionally or alternatively, the peak injection pressure range may be equal to or less than about 7.0 bar, for example, equal to or less than about 6.5 bar, or equal to or less than about 6.0 bar, or equal to or less than about 5.5 bar, or equal to or less than about 5.0 bar, or equal to or less than about 4.5 bar, or equal to or less than
about 4.0 bar, or equal to or less than about 3.5 bar, or equal to or less than about 3.0 bar, or equal to or less than about 2.5 bar.

In certain embodiments, the cycle time (during injection moulding) to produce an article of manufacture is at least about 10 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin under the same processing conditions, for example, at least about 20 % shorter, or at least about 30 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin under the same processing conditions. In certain embodiments, the cycle time is at least 10 % shorter to no more than about 40 % shorter, or at least about 15 % shorter to no more than about 35 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin under the same processing conditions.

In certain embodiments, the cycle time to produce an article of manufacture is equal to or less than about 30 s, for example, equal to or less than about 25 s, or equal to or less than about 20 s, or equal to or less than about 15 s, or equal to or less than about 14 s, or equal to or less than about 13 s, or equal to or less than about 12.8, or equal to or less than about 11 s, or equal to or less than about 10 s. In such embodiments, the said cycle times may be at least about 10 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin under the same processing conditions, for example, at least about 20 % shorter, or at least about 30 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin under the same processing conditions. In certain embodiments, the cycle time is at least 10 % shorter to no more than about 40 % shorter, or at least about 15 % shorter to no more than about 35 % shorter.

In certain embodiments, the weight range across 32 shots (during injection moulding) is less than 0.008 g for an average shot weight of between 3.25 g and 4.0 g, for example, equal to or less than 0.007 g, or equal to or less than 0.006 g, or equal to or less than about 0.005 g for an average shot weight of between 3.25 and 4.0 g.

In certain embodiments:

the melt temperature is from about 190 °C to about 250 °C, for example, from about 200 °C to about 240 °C, or any other melt temperature or range of melt temperature described herein;
the cycle time is (i) is at least about 10% shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin under the same processing conditions, for example, at least about 20% shorter, or at least about 30% shorter, and/or (ii) equal to or less than about 30 s, for example, equal to or less than about 15 s, or any other cycle time or range of cycle time described herein;

the peak pressure average during injection moulding is from about 500 to 2000 bar, for example, from about 750 to 2000 bar, or any other peak pressure average or range of peak pressure average described herein.

The filled polymer resin has a MFI @ 2.16 kg/190° C which is relatively low and which, prior to this invention, would not have been expected to be suitable for injection moulding. MFR may be determined in accordance with ISO 1133, for example, ISO 1133-1:2011 (e.g., by the mass-measurement method).

In certain embodiments, the filled polymer resin has a MFI of less than about 2.5 g/10 mins @ 2.16 kg/190° C, for example less than about 2.0 g/10 min @ 2.16 kg/190° C.

In certain embodiments, the filled polymer resin has a MFI which is equal to or less than about 2.4 g/10 min @ 2.16 kg/190° C, or equal to or less than about 2.25 g/10 min @ 2.16 kg/190° C, or equal to or less than about 2.0 g/10 min @ 2.16 kg/190° C, or equal to or less than about 1.75 g/10 mins @ 2.16 kg/190° C, or equal to or less than about 1.5 g/10 mins, or equal to or less than about 1.0 g/10 mins, or equal to or less than about 0.75 g/10 mins, or equal to or less than about 0.50 g/10 mins, or equal to or less than about 0.35 g/10 mins, or equal to or less than about 0.20 g/10 mins. In certain embodiments, the filled polymer resin has a MFI of at least about 0.05 g/10 mins @ 2.16 kg/190° C, for example, at least about 0.10 g/10 mins @ 2.16 kg/190° C, or at least about 0.15 g/10 mins @ 2.16 kg/190° C, or at least about 0.20 g/10 mins @ 2.16 kg/190° C.

In certain embodiments, the filled polymer resin has a MFI of from about 1.0 g/10 mins @ 2.16 kg/190° C to less than 2.5 g/10 min @ 2.16 kg/190° C, for example, from about 1.25 g/10 mins @ 2.16 kg/190° C to less than 2.5 g/10 mins @ 2.16 kg/190° C, or from about 1.5 g/10 mins @ 2.16 kg/190° C to less than 2.5 g/10 mins @ 2.16 kg/190° C, or from about 1.75 g/10 mins @ 2.16 kg/190° C to less than 2.5 g/10 mins @ 2.16 kg/190° C, or from about 2.0 g/10 mins @ 2.16 kg/190° C to less than g/10 mins @ 2.16 kg/190° C.
In certain embodiments, the filled polymer resin has a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding. In certain embodiments, the MFI during injection moulding is determined under the following conditions (using a Plaque Mould & Demag Ergotec Injection Moulding Machine, for example, a Demag Ergotech 150t System Servo Hydraulic Injection Moulding Machine):

- Melt temperature: 220 °C;
- Back pressure: 90 bar
- Decompression Distance: 8 mm at 30 mm/s
- Screw diameter: 25 mm
- Screw Surface Speed: 700 mm/s
- Injection Speed: 70 mm/s
- Dosing stroke: as required to achieve 100% visual fill with no Holding Stage
- Holding Pressure: as required to achieve a flat continuous surface finish
- Holding Time: 2.0 s
- Cooling Time: 6.0 s
- Clamp Force: 70 t
- Mould temperature: 25 °C
- Hot Tip Temperature: 10 °C above Melt Temperature

Exemplary injection moulding machines include Demag Ergotec Injection Moulding Machine, an E-motion Engel injection moulding machine, for example, an Engel 55t Servo Electric/ injection moulding machine, or a Sumitomo SE180DU System 180t Servo Electric injection moulding machine.

In certain embodiments, the injection moulding process comprises:

- a mould temperature of from about 15 °C to about 40 °C, for example, from about 20 °C to about 30°C, or from about 23 °C to about 27 °C, or about 25 °C; and/or
- a back pressure of from about 50 bar to about 150 bar; and/or
- a screw diameter of from about 20 mm to about 40 mm; and/or
- a screw surface speed of from about 500 mm/s to about 1000 mm/s; and/or
- an injection speed of from about 50 mm/s to about 100 mm/s; and/or
- a holding time of from about 1.0 s to about 5.0 s; and/or
- a cooling time of from about 30-70% of cycle time, for example, from about 2.0 s to about 20 s; and/or
a clamp force of from about 50t to about 150t; and/or
a hot temperature of +/- 20 °C of melt temperature, for example, up to about 20 °C above melt temperature, or up to about 15 °C above melt temperature.

In certain embodiments, the filled polymer resin has a MFI @ 2.16 kg/190°C which is at least 3.0 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding, for example, at least about 3.5 g/10 mins lower, or at least about 4.0 g/10 mins lower, or at least about 4.5 g/10 mins lower, or at least about 5.0 g/10 mins lower, or at least about 5.5 g/10 mins lower, or at least about 6.0 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding. For example, in certain embodiments, the filled polymer has a MFI @ 2.16 kg/190°C of equal to or less than about 1.0 g/10 mins and an apparent MFI during injection moulding of at least about 4 g/10 mins @ 2.16 kg/190°C, for example, an apparent MFI during injection moulding of at least about 5 g/10 mins @ 2.16 kg/190°C. In certain embodiments, the filled polymer has a MFI @ 2.16 kg/190°C of equal to or less than about 0.5 g/10 mins, and an apparent MFI during injection moulding of at least about 4 g/10 mins @ 2.16 kg/190°C, for example, an apparent MFI during injection moulding of at least about 5 g/10 mins @ 2.16 kg/190°C. By "apparent MFI" is meant that the filled polymer resin has a processability by injection moulding which is indicative of a MFI which is higher than the MFI determined @ 2.16 kg/190°C in accordance with ISO 1133 (e.g., ISO 1133-1:2011), e.g., a filled polymer resin having a MFI of 0.5 g/10 mins @ 2.16 kg/190°C processes as if its MFI is at least about 3.5 g/10 mins @ 2.16 kg/190°C, or at least about 4.0 g/10 mins @ 2.16 kg/190°C, or at least about 4.5 g/10 mins @ 2.16 kg/190°C, or at least about 5.0 g/10 mins @ 2.16 kg/190°C, or at least about 5.0 g/10 mins @ 2.16 kg/190°C. In certain embodiments, the apparent MFI is no more than about 8.0 g/10 @ 2.16 kg/190°C higher, for example, no more than about 7.5 g/10 @ 2.16 kg/190°C higher, or no more than about 7.0 g/10 @ 2.16 kg/190°C higher.

In certain embodiments, the filled polymer resin, for example, a filled polymer resin having an MFI of less than about 0.5 g/10 mins @ 2.16 kg/190°C processes (by injection moulding) similarly to an unfilled HDPE virgin resin having an MFI of from about 5-6 g/10 mins @ 2.16 kg/190°C.

Additionally or alternatively, the filled polymer resin may be characterized in terms of Spiral Flow Number (SFN). The spiral flow test provides a measure of the
processability of polymer resin under the more "real life" shear rates seen in the injection moulding process. The SFN is a measure of the length of flow for the tested resin. SFN is determined by injection moulding the polymer resin under the following conditions (using a Spiral Flow Mould and Engel 55t Servo Electric/E-motion injection moulding machine):

| Melt temperature: 220 °C; |
| Back pressure: 90 bar |
| Screw Surface Speed: 550 mm/s |
| Injection time: 1 s or 2 s |
| Injection Speed: 30 mm/s or 15 mm/s |
| Mould temperature: 25 °C |

The spiral flow test is conducted using a spiral mould of appropriate dimensions. Nominal dimensions of the spiral flow mould, sometimes referred to as spiral cavity channel, may be from 500 mm - 1500 mm in length (e.g., from 700 - 1000 mm), from 4 to 8 mm in width (e.g., about 6.35 mm) and from about 0.8 to about 3 mm in depth (e.g., about 1.57 mm).

In certain embodiments, the SFN of the filled polymer resin is at least about 350 mm, for example, at least about 375 mm, or at least about 400 mm, or at least about 410 mm, or at least about 420 mm, or at least about 430 mm, or at least about 440 mm, or at least about 450 mm. In certain embodiments, the SFN is from about 350 mm to about 500 mm, for example, from about 375 mm to about 475 mm, or from about 400 to about 475 mm, or from about 425 mm to about 475 mm, or from about 440 mm to about 460 mm. In such embodiments, the injection time may be 2 s and the injection speed 15 mm/s. In such embodiments, the peak pressure average during injection moulding may be from about 1500 to 2000 bar, for example, from about 1750 to 2000 bar, or from about 1800 to about 1950 bar, or from about 1850 to about 1950 bar, or any other peak pressure average or range of peak pressure average described herein. In such embodiments, the melt temperature may be from about 190 °C to 250 °C, for example, from about 200 °C to about 240 °C, or any other melt temperature or range melt temperatures described herein.
In certain embodiments, the filler polymer resin has a spiral flow number (SFN) which is greater than the SFN of a comparable unfilled virgin HDPE polymer resin having an equivalent MFI @ 2.16 kg/190 °C.

In certain embodiments, the filler polymer resin has a SFN which is at least 80% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, for example, at least about 85% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, or at least about 90% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

In certain embodiments, the filled polymer resin has a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins @ 2.16 kg/190°C, for example, less than about 2.0 g/10 min and (a) a SFN which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or (b) a SFN which is at least 80% of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, for example, at least about 85% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, or at least about 90% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

In certain embodiments, the filled polymer resin has a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins @ 2.16 kg/190°C, for example, less than about 2.0 g/10 min and a SFN which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190 °C of at least about 5.0 g/10 min.

In certain embodiments, the filled polymer resin has a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins @ 2.16 kg/190°C, for example, less than about 2.0 g/10 min and a SFN which is at least 80% of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, for example, at least about 85% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, or at least about 90% of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 min @ 2.16 kg/190 °C.

In certain embodiments, the filled polymer resin has a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins @ 2.16 kg/190°C, for example, less than about 2.0 g/10
a SFN which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and a SFN which is at least 80 % of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 min @ 2.16 kg/190 °C, for example, at least about 85 % of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, or at least about 90 % of the SFN of an unfilled HDPE virgin polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

In certain embodiments, the filled polymer resin is characterised in terms of a ratio of its MFI @ 21/6 kg/190 °C to its MFI @ 2.16 kg/190 °C, referred to herein after as R-MFI. This is indicative of the distribution of molar mass in a given polymer sample. The larger the R-MFI, the broader the molecular weight distribution. For example, a monodisperse polymer where all the chain lengths are equal has a R-MFI of 1. As noted, the R-MFI is calculated as the ratio of the MFI @ 21/6 kg/190 °C to the MFI @ 2.16 kg/190 °C, i.e.,

$$R\text{-MFI} = \frac{\text{MFI @ 21/6 kg/190 °C}}{\text{MFI @ 2.16 kg/190 °C}}$$

Additionally or alternatively, the filled polymer resin may be characterised in terms of the difference between the MFI @ 21/6 kg/190 °C and the MFI @ 2.16 kg/190 °C, i.e.,

$$\Delta\text{MFI} = \text{MFI @ 21/6 kg/190 °C} - \text{MFI @ 2.16 kg/190 °C}$$

In certain embodiments, the filled polymer resin has a R-MFI of at least about 40.0 and/or a AMFI of at least about 4.0. In such embodiments, the filled polymer resin may have a MFI @ 2.16 kg/190 °C of less than about 1.5 g/10 mins, or less than about 1.0 g/10 mins, or less than about 0.75 g/10 mins, or less than about 0.50 g/10 mins, or less than about 0.35 g/10 mins, or less than about 0.20 g/10 mins.

In certain embodiments, the R-MFI is at least about 125, for example, from about 150 to about 500, or from about 150 to about 450, or from about 150 to about 400, or from about 150 to about 350, or from about 200 to about 350, or from about 250 to about 350, or from about 300 to about 350. Additionally or alternatively, AMFI is at least about 41.0, or at least about 42.0, or at least about 43.0, or at least about 44.0, or at least about 45.0, or at least about 46.0, or at least about 47.0, or at least about 48.0, or at least about 49.0, or at least about 50.0, or at least about 51.0, or at least about 52.0,
or at least about 53.0, or at least about 54.0, or at least about 55.0, or at least about 56.0, or at least about 57.0. In certain embodiments, ΔMH is no greater than about 70, for example, no greater than about 65.0, or no greater than about 60.0. In such embodiments, the filled polymer resin may have a MFI @ 2.16 kg/190 °C of less than about 1.5 g/10 mins, or less than about 1.0 g/10 mins, or less than about 0.75 g/10 mins, or less than about 0.50 g/10 mins, or less than about 0.35 g/10 mins, or less than about 0.20 g/10 mins.

In certain embodiments, the filled polymer resin has a broader molecular weight distribution than an unfilled virgin HDPE polymer resin. As such, at a given MFI @ 2.16 kg/190 °C, the filled polymer resin may have a higher R-MFI than an unfilled virgin HDPE polymer resin.

In certain embodiments, the viscosity of the filled polymer resin decreases more rapidly at higher shear rate compared to an unfilled virgin HDPE polymer resin. As such, at a given MFI @ 2.16 kg/190 °C, the viscosity of the filled polymer resin will decrease more rapidly when subjected to an ever increasing shear rate compared to the viscosity decrease of an unfilled virgin HDPE resin subjected to the same increasing shear rate.

In certain embodiments, the filled polymer resin comprises at least about 50 % by weight recycled polymer (based on the total weight of polymer in the filled polymer resin), for example, at least about 60 % by weight, or at least about 70 % by weight, or at about 80 % by weight, or at least about 95 % by weight, or at least about 99 % by weight recycled polymer. In certain embodiments, recycled polymer constitutes substantially all, i.e., about 100 % by weight, of the polymer of the filled polymer resin.

In certain embodiments, the filled polymer resin comprises no more than about 20 % by weight of virgin polymer (based on the total weight of polymer in the filled polymer resin), for example, no more than about 15 % by weight of virgin polymer, or no more than about 10 % by weight of virgin polymer, or no more than 5 % by weight of virgin polymer, or no more than about 2 % by weight of virgin polymer, or no more than about 1 % by weight of virgin polymer, or no more than about 0.5 % by weight of virgin polymer, or no more than about 0.1 % by weight of virgin polymer.

In certain embodiments, the filled polymer resin is free of virgin polymer.
In certain embodiments, the filled polymer resin comprise a mixture of polymer types, for example, a mixture of polyethylene and polypropylene, or a mixture of different types of polyethylene, e.g., HDPE, LDPE and/or LLDPE, or a mixture of different types of polyethylene and polypropylene. In certain embodiments, the filled polymer resin comprises a mixture of polymer types which individually have a MFI of greater than or less than about 2.0 g/10 mins @ 2.16 kg/190 °C) provided the filled polymer resin as a whole has a MFI of less than 2.5 g/10 mins @ 2.16 kg/190 °C, for example, less than 2.0 g/10 mins @ 2.16 kg/190 °C, or less than about 1.5 g/10 mins @ 2.16 kg/190 °C, or less than about 1.0 g/mins @ 2.16 kg/190 °C, or less than about 0.5 g/10 mins @ 2.16 kg/190 °C. In certain embodiments, at least 75 % by weight of the filled polymer resin is a mixture of polyethylene and polypropylene, for example, a mixture of HDPE and polypropylene (based on the total weight of polymer in the filled polymer resin), for example, from 75 % to about 99 % of a mixture of polyethylene and polypropylene, for example, a mixture of HDPE and polypropylene. In such embodiments, HDPE may constitute from about 50 % to about 95 % by weight of the filled polymer resin (based on the total weight of the polymer of the filled polymer resin), for example, from about 60 % to about 90 % by weight, or from about 70 % to about 90 % by weight, of from about 70 % to about 85 % by weight, or from about 70 % to about 80 % by weight, or from about 75 % to about 80 % by weight of the filled polymer resin (based on the total weight of the polymer of the filled polymer resin).

In certain embodiments, the HDPE is mixture of HDPE from different sources, for example, from different types of post-consumer polymer waste, e.g., recycled blow-moulded HDPE and/or recycled injection moulded HDPE.

Generally, HDPE is understood to be a polyethylene polymer mainly of linear, or unbranched, chains with relatively high crystallinity and melting point, and a density of about 0.96 g/cm³ or more. Generally, LDPE (low density polyethylene) is understood to be a highly branched polyethylene with relatively low crystallinity and melting point, and a density of from about 0.91 g/cm³ to about 0.94 g/cm. Generally, LLDPE (linear low density polyethylene) is understood to be a polyethylene with significant numbers of short branches, commonly made by copolymerization of ethylene with longer-chain olefins. LLDPE differs structurally from conventional LDPE because of the absence of long chain branching.
In certain embodiments, the filled polymer resin comprises up to about 20 % by weight of polymers other than HDPE such as, for example, LDPE, LLDPE and polypropylene, any or all of which may be recycled from polymer waste, e.g., post-consumer polymer waste. In certain embodiments, the recycled polymer comprises up to about 20 % by weight polypropylene, based on the total weight of the recycled polymer, for example, from about 1 % to about 20 % by weight, or from about 5 % to about 18 % by weight, or from about 10 % to about 15 % by weight, or from about 12 to about 14 % by weight polypropylene.

In certain embodiments, the polymer component of the filled polymer resin, other than any impact modifier which may be present, is a mixture of polyethylene and polypropylene, for example, a mixture of recycled polyethylene and polypropylene, for example, polyethylene and polypropylene derived from a recycled mixed polyolefin feedstock consisting of polyethylene and polypropylene. In such embodiments, the filled polymer resin may comprise up to about 30 % by weight of recycled polypropylene, based on the total weight of the filled polymer resin, for example, up to about 25 % by weight polypropylene, or up to about 20 % by weight polypropylene, or up to about 15 % by weight polypropylene, or up to about 12.5 % by weight polypropylene, or up to about 10 % by weight polypropylene, or up to about 7.5 % by weight polypropylene, or up to about 5 % by weight polypropylene. In certain embodiments, the filled polymer resin comprises at least about 4 % by weight polypropylene, for example, at least about 6 % by weight polypropylene, or at least about 8 % by weight polypropylene, or at least about 10 % by weight polypropylene, or at least about 12 % by weight polypropylene, based on the total weight of the filled polymer resin. In such embodiments, the polyethylene may be HDPE.

In certain embodiments, filled polymer resin has a density of greater than about 1.00 to equal to or less than about 1.05 g/cm³. Density may be determined in accordance with ISO1183.

In certain embodiments, the functional filler comprises an inorganic particulate having a \( d_{\text{av}} \) of no greater than about 2.5 pm and/or a surface treatment agent on the surface of the inorganic particulate. In certain embodiments, the inorganic particulate has a \( d_{\text{M}} \) of from about 0.1 pm to about 2.0 \( \mu \text{m} \), for example, from about 0.1 pm to about 1.5 pm, or from about 0.1 pm to about 1.0 pm, or from about 0.2 to about 0.9 pm, or from about 0.2 pm to about 0.7 pm, or from about 0.3 pm to about 0.7 pm, or from about 0.4 to...
about 0.6 μm, or from about 0.5 to about 0.6 μm. The particle sizes described herein pertain to the inorganic particulate absent any surface treatment agent.

Unless otherwise stated, particle size properties referred to herein for the inorganic particulate materials are as measured by the well known conventional method employed in the art of laser light scattering, using a CILAS 1064 instrument (or by other methods which give essentially the same result). In the laser light scattering technique, the size of particles in powders, suspensions and emulsions may be measured using the diffraction of a laser beam, based on an application of Mie theory. Such a machine provides measurements and a plot of the cumulative percentage by volume of particles having a size, referred to in the art as the 'equivalent spherical diameter' (e.s.d), less than given e.s.d values. The mean particle size \( d_M \) is the value determined in this way of the particle e.s.d at which there are 50% by volume of the particles which have an equivalent spherical diameter less than that \( d_M \) value.

In certain embodiments, the inorganic particulate does not have a surface treatment on its surface.

In certain embodiments, the inorganic particulate is treated with a surface treatment agent, i.e., a coupling modifier, such that the inorganic particulate has a surface treatment on its surface. In certain embodiments, the inorganic particulate is coated with the surface treatment agent.

The purpose of the surface treatment agent is to improve the compatibility of the inorganic particulate and the polymer matrix with which it is to be combined, and/or improve the compatibility of different polymers in the recycled polymer. In recycled polymer resins the surface treatment may serve to cross-link or graft the different polymers. In certain embodiments, the surface treatment agent serves as a coupling modifier, wherein coupling involves a physical (e.g., steric) and/or chemical (e.g., chemical bonding, such as covalent or van der Waals) interaction between the polymers and/or between the polymers and the surface treatment agent.

In other aspects and embodiments of the present invention, the coating additionally or alternatively comprises a compound selected from the group consisting of one or more fatty acids and one or more salts of fatty acids, for example, stearic acid or calcium stearate.
The inorganic particulate material may, for example, be an alkaline earth metal carbonate or sulphate, such as calcium carbonate, magnesium carbonate, dolomite, gypsum, a hydrous kandite clay such as kaolin, halloysite or ball clay, an anhydrous (calcined) kandite clay such as metakaolin or fully calcined kaolin, talc, mica, perlite or diatomaceous earth, or magnesium hydroxide, or aluminium trihydrate, or combinations thereof.

A preferred inorganic particulate material is calcium carbonate. Hereafter, the invention may tend to be discussed in terms of calcium carbonate, and in relation to aspects where the calcium carbonate is processed and/or treated. The invention should not be construed as being limited to such embodiments.

The particulate calcium carbonate used in the present invention may be obtained from a natural source by grinding. Ground calcium carbonate (GCC) is typically obtained by crushing and then grinding a mineral source such as chalk, marble or limestone, which may be followed by a particle size classification step, in order to obtain a product having the desired degree of fineness. Other techniques such as bleaching, flotation and magnetic separation may also be used to obtain a product having the desired degree of fineness and/or colour. The particulate solid material may be ground autogenously, i.e. by attrition between the particles of the solid material themselves, or, alternatively, in the presence of a particulate grinding medium comprising particles of a different material from the calcium carbonate to be ground. These processes may be carried out with or without the presence of a dispersant and biocides, which may be added at any stage of the process.

Precipitated calcium carbonate (PCC) may be used as the source of particulate calcium carbonate in the present invention, and may be produced by any of the known methods available in the art.

The surface treatment agent, when present, may comprise an O- or N-containing acid functionality, for example, a compound including a hydrocarbyl unsaturation and an O- and/or N-containing acid functionality. In certain embodiments, the hydrocarbyl unsaturation is one or more ethylenic groups, at least one of which may be a terminal group. The acid functionality may comprise a carboxylic acid, carboxy, carbonyl and or ester functionality.
In certain embodiments, the surface treatment agent comprises a compound having a saturated hydrocarbyl group and an O- or N-containing acid functionality, for example, a carboxylic acid, carboxy, carbonyl and or ester functionality.

In certain embodiments, the surface treatment comprises both a compound including a hydrocarbyl unsaturation and an O- and/or N-containing acid functionality, and compound having a saturated hydrocarbyl group and an O- or N-containing acid functionality.

In certain embodiments, the functional filler and, hence, the filled polymer resin does not comprise both of a compound including a hydrocarbyl unsaturation and an O- and/or N-containing acid functionality, and a compound having a saturated hydrocarbyl group and an O- or N-containing acid functionality.

In certain embodiments, the surface treatment agent does not comprise a compound selected from the group consisting of one or more fatty acids and one or more salts of a fatty acid.

In certain embodiments, the compound having a saturated hydrocarbyl group and an O- or N-containing acid functionality is a saturated fatty acid, or a metal salt thereof, or a mixture of such fatty acids and/or salts. In certain embodiments, surface treatment agent comprise stearic acid, optionally in combination with other fatty acids.

In certain embodiments, the compound including a hydrocarbyl unsaturation and an O- and/or N-containing acid functionality is a carboxylic acid or carboxylate, for example, a propanoic group, or an acrylic acid or acrylates, or an imide. Specific examples of coupling modifiers are β-carboxy ethylacrylate, β-carboxyhexylmaleimide, 10-carboxydecylmaleimide and 5-carboxy penty1 maleimide.

In certain embodiments, the compound including a hydrocarbyl unsaturation and an O- and/or N-containing acid functionality is an unsaturated fatty acid, or a metal salt thereof, or a mixture of such fatty acids and/or salts.

In certain embodiments, the surface treatment agent comprises one or more of a C_{18}, C_{2}-C_{18}, and C_{1s} alkylene group. In certain embodiments, said group or groups bridges between a hydrocarbyl unsaturation, for example, a terminal ethylenic group
and an O- and/or N-containing acid functionality. In such embodiments, the O- and/or N-containing acid functionality may be a carboxylic acid or carboxylate, for example, a propanoic group, or an acrylic acid or acrylates, or an imide.

The functional filler may be present in the filled polymer resin in an amount ranging from about 1% up to about 70% by weight, based on the total weight of the filled polymer resin. For example, from about 2% to about 60% by weight, or from about 3% to about 50% by weight, or from about 4% to about 40% by weight, or from about 5% to about 30% by weight, or from about 6% to about 25% by weight, or from about 7%

% to about 20% by weight, or from about 8% to about 15% by weight, or from about 8%

% to about 12% by weight, based on the total weight of the filled polymer resin. The functional filler may be present in amount less than or equal to about 80% by weight of the filled polymer resin, for example, less than or equal to about 70% by weight, or less than or equal to about 60% by weight, or less than or equal to about 50% by weight, or less than or equal to about 40% by weight, or less than or equal to about 30% by weight, or less than or equal to about 20% by weight, or less than or equal to about 50% by weight, based on the total weight of the filled polymer resin.

The surface treatment agent (i.e., coupling modifier) of the functional filler may be present in an amount of from about 0.01% by weight to about 4% by weight, based on the total weight of the filled polymer resin, for example, from about 0.02% by weight to about 3.5% by weight, or from about 0.05% by weight to about 1.4% by weight, or from about 0.1% by weight to about 0.7% by weight, or from about 0.15% by weight to about 0.7% by weight, or from about 0.3% by weight to about 0.7% by weight, or from about 0.5% by weight to about 0.7% by weight, or from about 0.02% by weight to about 0.5%, or from about 0.05% by weight to about 0.5% by weight, or from about 0.1% by weight to about 0.5% by weight, or from about 0.15% by weight to about 0.5% by weight, or from about 0.2% by weight to about 0.5% by weight, or from about 0.3% by weight to about 0.5% by weight, based on the total weight of the filled polymer resin.

Additionally or alternatively, the surface treatment agent may be present in an amount equal to or less than about 5 wt. % based on the total weight of the functional filler, for example equal to or less than about 2 wt. % or, for example equal to or less than about 1.5 wt. %. In an embodiment, the surface treatment agent is present in the functional filler in an amount equal to or less than about 1.2 wt.% based on the total weight of the
functional filler, for example equal to or less than about 1.1 wt. %, for example equal to or less than about 1.0 wt. %, for example, equal to or less than about 0.9 wt. %, for example equal to or less than about 0.8 wt. %, for example equal to or less than about 0.7 wt. %, for example, less than or equal to about 0.6 wt. %, for example equal to or less than about 0.5 wt. %, for example equal to or less than about 0.4 wt. %, for example equal to or less than about 0.3 wt. %, for example equal to or less than about 0.2 wt. % or, for example, less than or about 0.1 wt. %. Typically, the surface treatment agent is present in the functional filler in an amount greater than about 0.05 wt. %. In further embodiments, the surface treatment agent is present in the functional filler in an amount ranging from about 0.1 to 2 wt. % or, for example, from about 0.2 to about 1.8 wt. %, or from about 0.3 to about 1.6 wt. %, or from about 0.4 to about 1.4 wt. %, or from about 0.5 to about 1.3 wt. %, or from about 0.6 to about 1.2 wt. %, or from about 0.7 to about 1.2 wt. %, or from about 0.8 to about 1.2 wt. %, or from about 0.8 to about 1.1 wt. %.

The filled polymer resin may additionally comprise a peroxide-containing additive. In an embodiment, the peroxide-containing additive comprises di-cumyl peroxide or 1,1-Di(tert-butylperoxy)-3,3,5-trimethylcyclohexane. The peroxide-containing additive may not necessarily be included with the surface treatment agent and instead may be added during the compounding of the functional filler and the recycled polymers, as described below. In some polymer systems, e.g., those containing HDPE, the inclusion of a peroxide-containing additive may promote cross-linking of the polymer chains. In other polymer systems, e.g., polypropylene, the inclusion of a peroxide-containing additive may promote polymer chain scission. The peroxide-containing additive may be present in amount effective to achieve the desired result. This will vary between coupling modifiers and may depend upon the precise composition of the inorganic particulate and the polymer. For example, the peroxide-containing additive may be present in an amount equal to or less than about 1 wt. % based on the weight of the filled polymer resin b which the peroxide-containing additive is to be added, for example, equal to or less than about 0.5 wt. %, for example, 0.1 wt %, for example equal to or less than about 0.09 wt. %, or for example equal to or less than about 0.08 wt. % or for example, equal to or less than about 0.06 wt. %. Typically, the peroxide-containing additive, if present, is present in an amount greater than about 0.01 wt. % based on the weight of the filled polymer resin. In certain embodiments, the filled polymer resin comprises from about 0.01 wt. % to about 0.05 wt. % of a peroxide-containing additive, for example, di-cumyl peroxide or 1,1-Di(tert-butylperoxy)-3,3,5-
trimethylcyclohexane, for example, from about 0.01 wt. % to about 0.05 wt. %, or from about 0.01 wt. % to about 0.03 wt. %, or from about 0.0125 wt. % to about 0.0275 wt. %, or from about 0.015 wt. % to about 0.025 wt. %, or from about 0.0175 wt. % to about 0.0225 wt. %, or from about 0.018 wt. % to about 0.022 wt. %, or from about 0.019 wt. % to about 0.021 wt. %, or about 0.02 wt. %. In such embodiments, the filled polymer resin may have a MFI of less than about 2.5 g/10 mins @ 2.16 kg/190°C, for example, from about 1.0 g/10 mins @ 2.16 kg/190°C to about 2.5 g/10 mins @ 2.16 kg/190°C, for example, equal to or less than about 1.5 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 1.0 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 0.5 g/10 mins @ 2.16 kg/190°C

In certain embodiments, the filled polymer resin comprises from about 0.015 wt. % to about 0.025 wt. % of the peroxide-containing additive, for example, di-cumyl peroxide.

In such embodiments, inclusion of a relatively minor amount of peroxide-containing additive may serve to modify, for example, enhance, one or more mechanical properties of injected moulded parts formed from the filled polymer resin, for example, filled polymer resin comprising recycled polyethylene and up to about 20 wt. % of optionally recycled polypropylene, based on the total weight of the filled polymer resin, for example, from about 2-15 wt. % of optionally recycled polypropylene, or from about 3-15 wt. %, or 4-14 wt. %, or 2-10 wt.%, or 3-9 wt.%., or 4-8 wt. %, or 7-15 wt.%., or 8-15 wt.% of optionally recycled polypropylene. In certain embodiments, all of the polypropylene is recycled polypropylene, which may be derived from a recycled mixed polyolfin feedstock comprising polyethylene and polypropylene. Without wishing to be bound by theory, it is believed that a balance of enhanced mechanical properties is obtainable by optimizing the level of peroxide-containing additive in relation to the relative amounts of polyethylene, polypropylene and functional filler. This also demonstrates the ability of the functional filler to decrease the interracial tension between normally immiscible polymer types, e.g., polyethylene and polypropylene, and enhancing mechanical properties.

Mechanical properties include one or more of elongation at break, flexural modulus, ultimate tensile stress (UTS) and Charpy (unnotched) Impact Strength. Tensile properties, e.g., elongation at break and UTS, may be determined in accordance with ISO527-2, at room temperature, using a Tinius Olsen Benchtop tensile tester, and based on average of eight measurements for each test piece. Charpy Impact Strength
may be determined at -20 °C ± 2 °C in accordance with ISO179-2 using an Instron Ceast 9340 falling-weight impact tester. Flexural modulus may be determined in accordance with ISO 178.

In certain embodiments, the injected moulded part has an elongation at break of at least about 15 %, for example, at least about 25 %, or at least about 50 %, or at least about 75 %, or at least about 100 %, or at least about 150 %, or at least about 200 %, or at least about 250 %, or at least about 300 %, or at least about 325 %, or at least about 340 %. In certain embodiments, the elongation at break is no greater than about 500 %, or no greater than about 450 %, or no greater than about 400 %.

In certain embodiments, the injected moulded part has a UTS of from about 15-30 MPa, for example, from about 20-30 MPa, or from about 20-25 MPa, or from about 20-23 MPa, or from about 20-22 MPa, or from about 20-21 MPa.

In certain embodiments, the injected moulded part has a flexural modulus of at least about 750 MPa, for example, at least about 800 MPa, or at least about 850 MPa, or at least about 900 MPa, or from about 900-1250 MPa, or from about 900-1200 MPa, or from about 900-1150 MPa, or from about 900-1 100 MPa, or from about 900-1050 MPa, or from about 900-1000 MPa, or from about 925-975 MPa.

In certain embodiments, an injected moulded part form from the filled polymer resin has one or more of:

(a) an elongation at break of at least about 300 %, for example, when the injected moulded part is formed from a filled polymer resin comprising at least 8 wt. % polypropylene, and optionally no more than about 12 wt. % functional filler;
(b) a UTS of at least about 20 MPa, for example, from about 20-22MPa;
(c) a flexural modulus of at least about 900 MPa; and
(d) a Charpy Impact Strength of at least about 40 kJ/m² (20 °C ± 2 °C), for example, at least about 80 kJ/m² (-20 °C ± 2 °C).

In certain embodiments, for example, embodiments having one or more of (a), (b), (c) and (d) above, the injected moulded part is formed from a filled polymer resin comprising:
from about 0.015 wt. % to about 0.025 wt. % of the peroxide-containing additive, for example, dicumyl peroxide,
a polypropylene content of at least about 8 wt. %, for example, from about 8-15 wt. %,
the balance of the polymer component being polyethylene, optionally wherein the polypropylene and polyethylene are derived from the same recycled mixed polyolefin source,
from about 8-12 wt. % functional filler,
an MFI of less than 2.5 g/10 mins @ 2.16 kg/190°C, for example, from about 2.0 - 2.45 g/10 mins @ 2.16 kg/190°C and optionally up to about 2 wt. % carbon black and up to about 0.5 wt. % antioxidant;
and having:
an elongation at break of at least about 300 %,
and optionally:
a UTS of from about 20-25 MPa, and/or a flexural modulus of at least about 900 MPa, for example, from about 920-1250 MPa, or from about 920-980 MPa, and/or a Charpy Impact Strength of at least about 80 kJ/m² (-20 °C ± 2 °C), for example, from about 80-90 kJ/m² (-20 °C ± 2 °C).

In such embodiments, the functional filler may be ground calcium carbonate having a d50 of from about 0.5-1.5 μm, for example, from about 0.5-1.0 μm, or from about 0.6-1.0 μm, or from about 0.7-0.9 μm, or about 0.8 μm, which is surface treated with a compound according to formula (1).

The functional filler may be prepared by combining the inorganic particulate, surface treatment agent and optional peroxide-containing additive and mixing using conventional methods, for example, using a Steele and Cowlishaw high intensity mixer, preferably at a temperature equal to or less than 80°C. The compound(s) of the surface treatment agent may be applied after grinding the inorganic particulate, but before the inorganic particulate is added to the optionally recycled polymer composition. For example, the surface treatment agent may be added to the inorganic particulate in a step in which the inorganic particulate is mechanically de-aggregated.

The surface treatment agent may be applied during de-aggregation carried out in a milling machine.
The functional filler may additionally comprise an antioxidant. Suitable antioxidants include, but are not limited to, organic molecules consisting of hindered phenol and amine derivatives, organic molecules consisting of phosphates and lower molecular weight hindered phenols, and thioesters. (Exemplary antioxidants include Irganox 1010 and Irganox 215, and blends of Irganox 1010 and Irganox 215. The amount of antioxidant may range from about 0.01 % by weight to about 5 % by weight, based on polymer content, for example, from about 0.05 % by weight to about 2.5 % by weight, or from about 0.05 % by weight to about 1.5 % by weight, or from about 0.05 % by weight to about 1.0 % by weight, or from about 0.05 % by weight to about 0.5 % by weight, or from about 0.05 % by weight to about 0.25 % by weight, or from about 0.05 % by weight to about 0.15 % by weight based on polymer content.

In certain embodiments, the filled polymer resin composition comprises (for example, up to about 5 wt. %, based on the total weight of the filled polymer resin) a secondary filler component other than the functional filler. The secondary filler may be in certain embodiments an uncoated inorganic particulate material, such as for example, the inorganic particulate materials described herein. In certain embodiments, the secondary filler is carbon black, for example, from about 0.1-5.0 wt. % carbon black, or from about 0.5-4.0 wt. %, or from about 0.5-1.5 wt. %, or from about 1.0-3.0 wt. %, or from about 1.5-2.5 wt. %, or about 2.0 wt. %, or about 1.0 wt. %, based on the total weight of the filled polymer resin. The aforementioned amounts may also apply to secondary filler other than carbon black.

In certain embodiments, the filled polymer resin comprises an impact modifier, for example, up to about 20 % by weight of an impact modifier, based on the total weight of the filled polymer resin, for example, from about 0.1 % by weight to about 20 % by weight, or from about 0.5 % by weight to about 15 % by weight, or from about 1 % by weight to about 12.5 % by weight, or from about 2 % by weight to about 12. % % by weight, or from about 1 % by weight to about 10 % by weight, or from about 1 % by weight to about 8 % by weight, or from about 1 % by weight to about 6 % by weight, or from about 1 % by weight to about 4 % by weight of an impact modifier, based on the total weight of the filled polymer resin.

In certain embodiments, the impact modifier is an elastomer, for example, a polyolefin elastomer. In certain embodiments, the polyolefin elastomer is a copolymer of ethylene and another olefin (e.g., an alpha-olefin), for example, octane, and/or or butene and/or
In certain embodiments, the impact modifier is a copolymer of ethylene and octene. In certain embodiments, the impact modifier is a copolymer of ethylene and butene.

In certain embodiments, the impact modifier, for example, polyolefin copolymer as described above, such as an ethylene-octene copolymer, has a density of from about 0.80 to about 0.95 g/cm³ and/or a MFI of from about 0.2 g/10 min (2.16 kg@190 °C) to about 30 g/10 min (2.16 kg@190 °C), for example, from about 0.5 g/10 min (2.16 kg@190 °C) to about 20 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 15 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 10 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 7.5 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 5 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 4 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 3 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 2.5 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 2 g/10 min (2.16 kg@190 °C), or from about 0.5 g/10 min (2.16 kg@190 °C) to about 1.5 g/10 min (2.16 kg@190 °C). In such or certain embodiments, the impact modifier is an ethylene-octene copolymer having a density of from about 0.85 to about 0.86 g/cm³. Exemplary impact modifiers are polyolefin elastomers made by DOW under the Engage(RTM) brand, for example, Engage (RTM) 8842. In such embodiments, the compounded polymer resin may additionally comprise an antioxidant, as described herein.

In certain embodiments, the impact modifier is a copolymer based on styrene and butadiene, for example, a linear block copolymer based on styrene and butadiene. In such embodiments, the impact modifier may have a MFI of from about 1 to about 5 g/10min (200°C @ 5.0kg), for example, from about 2 g/10min (200°C @ 5.0kg) to about 4 g/10min (200°C @ 5.0kg), or from about 3 g/10min (200°C @ 5.0kg) to about 4 g/10min (200°C @ 5.0kg).

In certain embodiments, the impact modifier is a triblock copolymer based on styrene and ethylene/butene. In such embodiments, the impact modifier may have a MFR of from about 15 g/10min (200°C @ 5.0kg) to about 25 g/10min (200°C @ 5.0kg), for example, from about 20 g/10min (200°C @ 5.0kg) to about 25 g/10min (200°C @ 5.0kg).
The articles of manufacture that are obtained by injection moulding a filled polymer resin as described herein are many and various.

In certain embodiments, the article of manufacture is the form of one of the following: panels (e.g., automotive panels), pallets, pipes, doors, shutters, awnings, shades, signs, frames, window casings, mobile phone casings, pails, backboards, wallboards, flooring, tiles, railroad ties, forms, trays, tool handles, stalls, bedding, dispensers, staves, totes, barrels, boxes, packing materials, baskets, racks, casings, binders, dividers, walls, mats, frames, bookcases, sculptures, chairs, tables, desks, art, toys, games, wharves, piers, boats, masts, septic tanks, substrates, computer housings, above- and below-ground electrical casings, PCB covers, furniture, picnic tables, tents, playgrounds, benches, shelters, sporting goods, bedpans, plaques, trays, hangers, servers, pools, insulation, caskets, bookcovers, canes, crutches, luggage buckle and dips, pump parts, and the like.

In certain embodiments, the article of manufacture, or a part thereof, comprises a wall having a thickness of no more than about 5.0 mm, for example, no more than about 4.0 mm, or no more than about 3.0 mm, or no more than about 2.0 mm, or no more than about 1.5 mm, or no more than about 1 mm. In certain embodiments, the article of manufacture, or a part thereof, has a wall thickness of from about 1.0 mm to about 3.0 mm, for example, from about 1.5 mm to about 3.0 mm. It is surprising that such relatively thin-walled parts may be injected moulding from recycled polymer resins.

EXAMPLES

Example 1 - preparation of polymer resins

Filled polymer resins were prepared by compounding. These were as follows:

Sample A - recycled HDPE + 15 wt. % of an uncoated ground calcium carbonate having a $d_M$ of 0.54 pm.

Sample B - a mixture of recycled HDPE and PP + 10 wt. % of a surface treated ground calcium carbonate ($d_M = 0.8 \text{ Mm}$), and having a MFI of 0.29 g/10 mins @ 2.16 kg/190ºc.
Sample C - a mixture of recycled HDPE and PP + 10 wt. % of a surface treated ground calcium carbonate ($d_M = 0.8 \ \mu m$) + 2.5 wt. %% of an ethylene-octene copolymer as impact modifier, and a MFI of 0.15 g/10 mins @ 2.16 kg/190 °C.

Sample D - an unfilled virgin HDPE polymer resin having a MFI of 8.0 g/10 mins @ 2.16 kg/190 °C. This is included for comparative purposes.

Example 2 - injection moulding process

A mobile phone surround was prepared from each sample by injection moulding using a Sumitomo SE180DU System 180t Servo Electric Injection Moulding Machine (Sumitomo SE180DU C360 with a 32 mm standard engineering screw design).

Conditions:

Melt temperature: 220°C.
Feed throat temperature: 70°C
Back Pressure: 90bar
Decompression Distance: 8mm at 30mm/s

Screw Surface Speed: 700mm/s
Injection Speed: 70mm/s
Dosing Stroke: as required to achieve 100% visual fill with no Holding Stage
Holding Pressure: as required to achieve a flat continuous surface finish
Holding Time: 2.0 seconds
Cooling Time: 6.0 seconds
Clamp Force: 100t
Mould Temperature: 25°C

Between each sample blend test the injection unit and hot runner system were purged clean with HDPE.

Results are summarised in Tables 1 and 2,
Example 3 - analysis of Spiral Flow Number (SFN)

The SFN of Samples B, C and D were determined by injection moulding the polymer resin under the following conditions (using a Spiral Flow Mould and Engel 55t Servo Electric/E-motion injection moulding machine):

- MeK temperature: 220 °C;
- Back pressure: 90 bar
- Screw Surface Speed: 550 mm/s
- Injection time: 1 s or 2 s
- Injection Speed: 30 mm/s or 15 mm/s
- Mould temperature: 25 °C

Results are summarized in Tables 3A and 3B.
Example 4

A series of filled polymer resin were prepared as described in Table 4 below. Recycled mixed polyolefin source A had a MFI of 4.01 g/10 mins @ 2.16 kg/190 °C, and recycled polyolefin source B had a MFI of 3.71 g/10 mins @ 2.16 kg/190 °C, i.e., that is before compounding with surface treated ground calcium carbonate (d_{50} = 0.8 pm) functional filler and the other components.

All samples were prepared via melt mixing with a Coperion ZSK twin-screw extruder. The barrel was maintained at 200, 205, 210, 215, 225, 235 and 240 °C from hopper to die. The screw speed was set to 800 rpm, and the feed rate at 8.0 kg/hour. The hot extrudes were immediately quenched in water and pelletized. Test specimens, for mechanics testing, were then produced by injection moulding. Test specimens were prepared using an Arburg Allrounder 320M, and mouldings were conditioned for a minimum of 40 hours at 23 °C and a relative humidity of 50 % prior to the test, in accordance with Procedure A of ASTM D618 (20/23/50).

### Table 3A.

<table>
<thead>
<tr>
<th>Injection Time/Speed</th>
<th>Sample B</th>
<th>Sample C</th>
</tr>
</thead>
<tbody>
<tr>
<td>SFN (mm)</td>
<td>403</td>
<td>416</td>
</tr>
<tr>
<td>Peak Injection Pressure (bar)</td>
<td>1873</td>
<td>1834</td>
</tr>
</tbody>
</table>

### Table 3B.

<table>
<thead>
<tr>
<th>Injection Time/Speed</th>
<th>Sample D</th>
</tr>
</thead>
<tbody>
<tr>
<td>SFN (mm)</td>
<td>470</td>
</tr>
<tr>
<td>Peak Injection Pressure (bar)</td>
<td>1335</td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th>Injection Time/Speed</th>
<th>Sample D</th>
</tr>
</thead>
<tbody>
<tr>
<td>SFN (mm)</td>
<td>495</td>
</tr>
<tr>
<td>Peak Injection Pressure (bar)</td>
<td>1242</td>
</tr>
</tbody>
</table>
Table 4

<table>
<thead>
<tr>
<th>Sample</th>
<th>Recycled mixed polyolefin source A (wt-%)</th>
<th>Recycled mixed polyolefin source B (wt-%)</th>
<th>Functional filler (wt-%)</th>
<th>CB (wt-%)</th>
<th>A/O (wt-%)</th>
<th>DCP (wt-%)</th>
<th>PP Content (wt-%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>88.680</td>
<td>-</td>
<td>10</td>
<td>1.0</td>
<td>0.3</td>
<td>0.02</td>
<td>5.41</td>
</tr>
<tr>
<td>2</td>
<td>88.660</td>
<td>-</td>
<td>10</td>
<td>1.0</td>
<td>0.3</td>
<td>0.04</td>
<td>5.51</td>
</tr>
<tr>
<td>3</td>
<td>83.680</td>
<td>-</td>
<td>15</td>
<td>1.0</td>
<td>0.3</td>
<td>0.02</td>
<td>5.65</td>
</tr>
<tr>
<td>4</td>
<td>83.660</td>
<td>-</td>
<td>15</td>
<td>1.0</td>
<td>0.3</td>
<td>0.04</td>
<td>6.89</td>
</tr>
<tr>
<td>5</td>
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<td>8.79</td>
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<td>1.0</td>
<td>0.3</td>
<td>0.04</td>
<td>8.54</td>
</tr>
<tr>
<td>7</td>
<td>-</td>
<td>83.680</td>
<td>15</td>
<td>1.0</td>
<td>0.3</td>
<td>0.02</td>
<td>9.59</td>
</tr>
<tr>
<td>8</td>
<td>-</td>
<td>83.660</td>
<td>15</td>
<td>1.0</td>
<td>0.3</td>
<td>0.04</td>
<td>13.58</td>
</tr>
</tbody>
</table>

CB = Carbon black; A/O = antioxidant; DCP = di-cumyl peroxide, PP = Polypropylene.

Mechanical testing of each test specimen, and the MFI of the compounded resins prior to injection moulding, is summarized in Table 5.

Elongation at break and UTS were carried out at room temperature using a Tinius Olsen Benchtop tensile tester, with results corresponding to an average of eight measurements for each sample, in accordance with ISO572-2.

Flexural modulus was tested in accordance with ISO 178,

Charpy unnotched impact tests were carried out at -20 °C ±2 °C using a Intron Ceast 9340 falling-weight impact tester, in accordance with ISO179-2. The results provided correspond to an average of complete break measurements for each sample.
Table 5.

<table>
<thead>
<tr>
<th>Sample</th>
<th>1</th>
<th>2</th>
<th>3</th>
<th>4</th>
<th>5</th>
<th>6</th>
<th>7</th>
<th>8</th>
</tr>
</thead>
<tbody>
<tr>
<td>MFI (g/10min, 2.16 kg@190°C)</td>
<td>2.26</td>
<td>2.08</td>
<td>2.38</td>
<td>1.67</td>
<td>2.35</td>
<td>1.39</td>
<td>2.22</td>
<td>1.48</td>
</tr>
<tr>
<td>UTS (MPa)</td>
<td>22.5</td>
<td>23.0</td>
<td>23.0</td>
<td>23.1</td>
<td>21.4</td>
<td>21.7</td>
<td>21.5</td>
<td>21.9</td>
</tr>
<tr>
<td>Break Elongation (%)</td>
<td>28.1</td>
<td>27.6</td>
<td>16.4</td>
<td>19.9</td>
<td>348</td>
<td>304</td>
<td>121</td>
<td>175</td>
</tr>
<tr>
<td>Flexural Modulus (MPa)</td>
<td>1091.1</td>
<td>1087.8</td>
<td>1202.6</td>
<td>994.3</td>
<td>948.1</td>
<td>947.8</td>
<td>1001.8</td>
<td>991.2</td>
</tr>
<tr>
<td>Charpy Impact Strength (KJ/m², -20°C ± 2°C)</td>
<td>48.9</td>
<td>67.1</td>
<td>49.5</td>
<td>71.5</td>
<td>86.2</td>
<td>72.9</td>
<td>54.4</td>
<td>51.4</td>
</tr>
</tbody>
</table>
1. Use of a filled polymer resin in the manufacture of an article therefrom by injection moulding, wherein the polymer resin comprises recycled polymer and functional filler, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_{50}$ of less than about 2.5 µm, and wherein the filled polymer resin has:

   (1) a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or

   (2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding; and/or

   (3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, and optionally:

      (a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or

      (b) a SFN which is at least 80 % of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8.0 g/10 mins @ 2.16 kg/190 °C.

2. A method of manufacturing an article by injection moulding, the method comprising injection moulding an article from a filled polymer resin, wherein the filled polymer resin comprises recycled polymer and functional filler, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_{50}$ of less than about 2.5 µm, and wherein the filled polymer resin has:

   (1) a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or
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(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding; and/or

5

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, and optionally:

(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or

10

(b) a SFN which is at least 80 % of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

3. Use of a functional filler in a polymer resin comprising recycled polymer to improve the injection mouldability of the polymer resin, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a \( d_M \) of less than about 2.5 pm.

4. A method for enabling or improving the injection mouldability of a polymer resin comprising recycled polymer, the method comprising filling the polymer resin with a functional filler, forming a filled polymer resin, and manufacturing an article of manufacture from the filled polymer resin by injection moulding, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a \( d_{so} \) of less than about 2.5 pm, and wherein the filled polymer resin has:

(1) a MFI @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or

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(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the apparent MFI of the filled polymer resin during injection moulding; and/or

35

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins, and
(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 mins, and/or

(b) a SFN which is at least 80% of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

5. Use or method according to any preceding claim, wherein an or the article of manufacture is processed from the filled polymer resin at a melt temperature of from about 200 °C to about 240 °C.

6. Use or method according to any preceding claim, wherein the cycle time to produce an or the article of manufacture is at least about 10 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin, for example, at least about 20 % shorter, or at least about 30 % shorter than the cycle time to produce a like article of manufacture from an unfilled HDPE virgin polymer resin.

7. Use or method according to any preceding claim, wherein: (i) the peak pressure during injection moulding is from about 1000 to 2000 bar, and/or (ii) the peak injection pressure range is equal to or less than about 5.0 bar.

8. Use or method according to any preceding claim, wherein the weight range across 32 shots is less than 0.008 g for an average shot weight of between 3.25 g and 4.0 g.

9. Use or method according to any preceding claim, wherein filled polymer resin has a MFI of less than 2.5 g/10 mins @ 2.16 kg/190°C, for example, equal to or less than about 2.0 g/10 mins @ 2.16 kg/190°C, or equal to or less than about 1.5 g/10 mins @ 2.16 kg/190°C, or equal to or less than about 1.0 g/10 mins @ 2.16 kg/190°C, or equal to or less than about 0.5 g/10 mins @ 2.16 kg/190°C.

10. Use or method according to any preceding claim, wherein the filled polymer resin has a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins and: (a) a SFN which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or (b) a SFN which is at least 80 %
of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, for example, at least about 90 % of SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

11. Use or method according to claim 10, wherein the filled polymer resin has a MFI equal to or less than about 2.0 g/10 mins @ 2.16 kg/190°C, for example, equal to or less than about 1.5 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 1.0 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 0.5 g/10 mins @ 2.16 kg/190°C.

12. Use or method according to any preceding claim, wherein the filled polymer resin has a R-MFI of at least about 100, wherein:

\[ R\text{-MFI} = \frac{\text{MFI} @ 21.6 \text{ kg}}{\text{MFI} @ 2.16 \text{ kg}} \]

and optionally

wherein (MFI @ 21.6 kg) - (MFI @ 2.16 kg) is at least about 40.

13. Use or method according to any preceding claim, wherein the filled polymer resin has a SFN of at least about 350 mm, for example, at least about 400 mm, or at least about 450 mm.

14. Use or method according to any preceding claim, wherein the filled polymer resin comprises at least about 50 % by weight recycled polymer (based on the total weight of polymer in the filled polymer resin).

15. Use or method according to any preceding claim, wherein the filled polymer resin comprises a mixture of polymer types, for example, a mixture of polyethylene and polypropylene, or a mixture of different types of polyethylene, e.g., HDPE, LDPE and/or LLDPE, or a mixture of different types of polyethylene (e.g., HDPE, LDPE and/or LLDPE) and polypropylene

16. Use or method according to any preceding claim, wherein the filled polymer resin is free of virgin polymer.

17. Use or method according to any preceding claim, wherein the function filler is an uncoated inorganic particulate having a \( d_M \) of no greater than about 1.0 \( \mu m \), for example, no greater than about 0.75 \( \mu m \).
18. Use or method according to any one of claims 1-17, wherein the function filler comprises or is a surface-treated inorganic particulate, optionally wherein the inorganic particulate has a $d_{50}$ of from about 0.1 to 2.5 $\mu m$, for example, from about 0.1 to about 1.0 $\mu m$.

19. Use or method according to claim 18, wherein the inorganic particulate is surface-treated with a surface treatment agent is a compound including a hydrocarbyl unsaturation and an O- and/or N-containing acid functionality, and/or a compound having a saturated hydrocarbyl group and an O- or N-containing acid functionality.

20. Use or method according to any preceding claim, wherein the inorganic particulate is calcium carbonate, for example, ground calcium carbonate.

21. Use or method according to any preceding claim, wherein the filled polymer resin comprises an impact modifier and/or a peroxide-containing additive.

22. An article of manufacture obtained by injection moulding a filled polymer resin as defined in any preceding claim.

23. The article of manufacture according to claim 22, wherein the article has a wall having a thickness of no more than about 3 mm, for example, from about 1 mm to about 3 mm.

24. The article according to claim 22 or 23 having one or more of: (a) an elongation at break of at least about 300 %, (b) a UTS of at least about 20 MPa, for example, from about 20-22MPa, (c) a flexural modulus of at least about 900 MPa, and (d) a Charpy Impact Strength of at least about 40 kJ/m$^2$ (20 °C ± 2 °C), for example, at least about 80 kJ/m$^2$ (-20 °C ± 2 °C).

25. A filled polymer resin suitable for use in the manufacture of an article therefrom by injection moulding, wherein the polymer resin comprises recycled polymer and functional filler, wherein the function filler comprises an inorganic particulate which (i) is surface treated and/or (ii) has a $d_M$ of less than about 2.5 $\mu m$, and wherein the filled polymer resin has:
(1) a MR @ 2.16 kg/190°C which is lower than the MFI of the filled polymer resin during injection moulding; and/or

(2) a MFI @ 2.16 kg/190°C which is at least 3 g/10 mins lower than the MFI of the filled polymer resin during injection moulding; and/or

(3) a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 min, and optionally:

(a) a Spiral Flow Number (SFN) which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or

(b) a SFN which is at least 80 % of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

26. Filled polymer resin according to claim 25, wherein filled polymer resin has a MFI of less than 2.5 g/10 mins @ 2.16 kg/190°C, for example, equal to or less than about 2.0 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 1.5 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 1.0 g/10 mins @ 2.16 kg/190°C, or equal to or less than about 0.5 g/10 mins @ 2.16 kg/190°C.

27. Filled polymer resin according to claim 25 or 26, wherein the filled polymer resin has a MFI @ 2.16 kg/190°C of less than about 2.5 g/10 mins, for example, equal to or less than about 2.0 g/10 mins@ 2.16 kg/190°C, and: (a) a SFN which is comparable to an unfilled virgin HDPE resin having a MFI @ 2.16 kg/190°C of at least about 5.0 g/10 min, and/or (b) a SFN which is at least 80 % of the SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C, for example, at least about 90 % of SFN of an unfilled virgin HDPE polymer resin having a MFI of 8 g/10 mins @ 2.16 kg/190 °C.

28. Filled polymer resin according to claim 27, wherein the filled polymer resin has a MFI equal to or less than about 1.0 g/10 mins@ 2.16 kg/190°C, or equal to or less than about 0.5 g/10 mins @ 2.16 kg/190°C.
29. Filled polymer resin according to any one of claims 25-28, wherein the filled polymer resin has a R-MFI of at least about 100, wherein:

\[ R\text{-MFI} = \frac{\text{MFI} @ 21.6 \text{ kg}}{\text{MFI} @ 2.16 \text{ kg}} \]

and optionally wherein (MFI @ 21.6 kg) - (MFI @ 2.16 kg) is at least about 40.

30. Filled polymer resin according to any one of claims 25-29, wherein the filled polymer resin has a SFN of at least about 350 mm, for example, at least about 400 mm, or at least about 450 mm.

31. Filled polymer resin according to any one of claims 25-30, wherein the filled polymer resin comprises at least about 50 % by weight recycled polymer (based on the total weight of polymer in the filled polymer resin).

32. Filled polymer resin according to any one of claims 25-31, wherein the filled polymer resin comprises a mixture of polymer types, for example, a mixture of polyethylene and polypropylene, or a mixture of different types of polyethylene, e.g., HDPE, LDPE and/or LLDPE, or a mixture of different types of polyethylene (e.g., HDPE, LDPE and/or LLDPE) and polypropylene

33. Filled polymer resin according to any one of claims 25-32, wherein the filled polymer resin is free of virgin polymer.

34. Filled polymer resin according to any one of claims 25-33, wherein the function filler is an uncoated inorganic particulate having a \( d_{\text{W}} \) of no greater than about 1.0 \( \mu \text{m} \), for example, no greater than about 0.75 \( \mu \text{m} \).

35. Filled polymer resin according to any one of claims 25-33, wherein the function filler comprises or is a surface-treated inorganic particulate, optionally wherein the inorganic particulate has a \( d_{\text{M}} \) of from about 0.1 to 2.5 pm, for example, from about 0.1 to about 1.0 pm.

36. Filled polymer resin according to any one of claims 25-35, wherein the inorganic particulate is surface-treated with a surface treatment agent selected from a compound including a hydrocarbyl unsaturation and an O- and/or N-containing
acid functionality, and/or a compound having a saturated hydrocarbyl group and an O- or N-containing acid functionality.

37. Filled polymer resin according to any one of claims 25-365, wherein the inorganic particulate is calcium carbonate, for example, ground calcium carbonate.

38. Filled polymer resin according to any one of claims 25-37, wherein the filled polymer resin comprises an impact modifier.

39. Use, method, article or filled polymer resin according to any preceding claim, wherein the filled polymer resin comprises from about 0.01 wt. % to about 0.05 wt. % of a peroxide-containing additive, for example, di-cumyl peroxide or 1,1-Di(tert-butylperoxy)-3,3,5-trimethylcyclohexane, based on the total weight of the filled polymer resin.

40. Use, method, article or filled polymer resin according to claim 39, wherein the filled polymer resin comprises from about 0.015 wt. % to about 0.025 wt. % of the peroxide-containing additive.

41. Use, method article or filled polymer resin according to any preceding claim, further comprising up to about 3 wt. % carbon black, and up to about 0.5 wt. % antioxidant, based on the total weight of the filled polymer resin.

42. Use, method, article or filled polymer resin according to any preceding claim, wherein the polymer component of the filled polymer resin, other than impact modifier when present, consists of polyethylene (e.g., HDPE) and polypropylene derived from a recycled mixed polyolefin feed.
**INTERNATIONAL SEARCH REPORT**

**A. CLASSIFICATION OF SUBJECT MATTER**

IPC(8) - B29B 7/90, 7/116, 15/08; B29C 45/00; C08J 11/04, 11/16; C08K 3/00 (2016.01)
CPC - B29B 7/90, 7/116, 15/08; B29C 45/0013; C08J 11/04, 11/16; C08K 3/0033

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)
IPC(8): B29B 7/90, 7/116, 15/08; B29C 45/00; C08J 11/04, 11/16; C08K 3/00 (2016.01)
CPC: B29B 7/90, 7/116, 15/08; B29C 45/0013; C08J 11/04, 11/16; C08K 3/0033

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)
Patent (US, EP, WO, JP, DE, GB, CN, FR, KR, ES, AU, IN, CA, INPADOC Data); IP.com; Google/Google Scholar; EBSCO; polymer, polypropylene, polyethylene, resin, filler, mineral, inorganic, particle, particulate, injection molding, injection moulding, surface treated, average particle size, median size, d50, melt flow index, melt flow rate, melt index, MFI, MRF, MI, temperature, 2.16 kg, 190 degrees C

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

<table>
<thead>
<tr>
<th>Category*</th>
<th>Citation of document, with indication, where appropriate, of the relevant passages</th>
<th>Relevant to claim No.</th>
</tr>
</thead>
<tbody>
<tr>
<td>X</td>
<td>US 2010/0234513 A1 (MILES, D et al.) 16 September 2010; abstract; paragraphs [0006], [0024], [0029]-[0029], [0044], [0047], [0050]-[0051]</td>
<td>1-3, 25-26</td>
</tr>
<tr>
<td>Y</td>
<td>US 2006/189761 A1 (JIN, YS et al.) 24 August 2006; paragraphs [0021], [0034]; claims 1, 5</td>
<td>4, 5/1-4, 27/25-26, 28/27-25-26</td>
</tr>
<tr>
<td>Y</td>
<td>US 8,067,518 B2 (DAVEY, CR et al.) 29 November 2011; abstract; column 12, lines 49-65; column 13, lines 8-15; tables 1, 3</td>
<td>27/25-26, 28/27-25-26</td>
</tr>
</tbody>
</table>

Further documents are listed in the continuation of Box C.  See patent family annex.

Date of the actual completion of the international search
10 August 2016 (10.08.2016)

Date of mailing of the international search report
02 SEP 2016

Name and mailing address of the ISA/ Mail Stop PCT, Attn: ISA/US, Commissioner for Patents P.O. Box 1450, Alexandria, Virginia 22313-1450 Authentic: No. 1/1-2/1-45000

Authorized officer: Shane Thomas

PCT Helpdesk: 571-272-4300
PCT CSEP: 571-272-7774

Form PCT/ISA/210 (second sheet) (January 2015)
INTERNATIONAL SEARCH REPORT

Box No. II  Observations where certain claims were found unsearchable (Continuation of item 2 of first sheet)

This international search report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
   because they relate to subject matter not required to be searched by this Authority, namely:

2. ☐ Claims Nos.:
   because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:

3. ☒ Claims Nos.: 6-24 and 29-42
   because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box No. III  Observations where unity of invention is lacking (Continuation of item 3 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

1. ☐ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.

2. ☐ As all searchable claims could be searched without effort justifying additional fees, this Authority did not invite payment of additional fees.

3. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:

4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest  ☐ The additional search fees were accompanied by the applicant's protest and, where applicable, the payment of a protest fee.
☐ The additional search fees were accompanied by the applicant's protest but the applicable protest fee was not paid within the time limit specified in the invitation.
☐ No protest accompanied the payment of additional search fees.

Form PCT/ISA/210 (continuation of first sheet (2)) (January 2015)