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Description

- [0001]** The invention relates to an integrated process for co-producing methanol and ammonia from syngas, more specifically to a process of co-producing methanol and ammonia from a hydrocarbon feedstock and air. The invention further relates to an integrated process for co-producing methanol and urea, more specifically to a process of co-producing methanol and urea from a hydrocarbon feedstock and air.
- 10 **[0002]** Such a process is known from patent publication US 7521483 B2. This document describes a process for co-producing methanol and ammonia from natural gas and air, comprising the steps of
- 15 i. feeding air to an air separation section to make an oxygen (O_2) and a nitrogen (N_2) stream;
 - ii. reforming desulphurised natural gas with the O_2 stream and steam in a combined reforming section to make a syngas mixture comprising carbon monoxide (CO), carbon dioxide (CO_2), steam (H_2O) and hydrogen (H_2);
 - iii. Dividing the syngas mixture into a first and a second syngas stream;
 - 20 iv. Feeding the first syngas stream to a syngas purification section to make a CO_2 and a H_2 stream;
 - v. Dividing the H_2 stream into a first and a second stream;
 - vi. Purifying the first H_2 stream with the N_2 stream to make a pure H_2/N_2 stream;
 - 25 vii. Feeding the H_2/N_2 stream to an ammonia synthesis section to make an ammonia stream;
 - viii. Feeding the second H_2 stream and the second syngas stream to a methanol loop reactor to make a methanol-containing mixture;
 - ix. Separating crude methanol from the methanol-containing mixture and recycling the remaining gas to the methanol loop reactor;
 - 30 x. Feeding the crude methanol to a methanol purification section to result in a methanol stream.

[0003] It is indicated that this process enables production of up to 5000 mtpd (metric ton per day) of methanol combined with up to 4000 mtpd of ammonia. The process may further comprise reacting the CO₂ and NH₃ formed into up to 6800 mtpd of urea.

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[0004] Methanol is one of the most important chemical raw materials; most of the methanol produced is used as a starting material or solvent for synthesis, whereas its use in the fuel and energy sector is expected to increase significantly. Since the 1960's, methanol synthesis from sulphur-free synthesis gas (syn-
10 gas) with Cu-based catalysts has become the major route, as it can be operated at fairly mild reaction conditions. An overview of methanol processes can be found for example in the chapter "Methanol" in "Kirk-Othmer Encyclopedia of Chemical Technology" (Wiley InterScience; posted on-line 2005/02/18, available via DOI: 10.1002/0471238961.1305200805140712.a01.pub2).

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[0005] Ammonia is another major chemical raw material, which is used for making urea and other fertilizers, and various chemicals like caprolactam and melamine. It is produced world-wide from nitrogen and hydrogen, typically the hydrogen is obtained via steam reforming of natural gas (or other hydrocarbon
20 feedstock). An overview of ammonia processes can be found for example in the chapter "Ammonia" in "Kirk-Othmer Encyclopedia of Chemical Technology" (Wiley InterScience; posted on-line 2001/10/18, available via DOI: 10.1002/0471238961.0113131503262116.a01.pub2).

25 **[0006]** For both methanol and ammonia production, it is advantageous -from an economical viewpoint- to develop single line plants with capacity as high as possible. Manufacturing capacity of a single line plant, incorporating only one operating unit or device for each relevant reaction or separation step, is typically limited for technological and economical reasons by a maximum capacity of one
30 or more of its units. Reliability of all units is paramount, as minimizing down-time is a prerequisite for economical operation. For example, a single state-of-the-art air separation unit (abbreviated as ASU) is considered to produce at most about 4000 mtpd (or 5200 kmol/h) of oxygen. Such ASU subsequently limits produc-

tion capacity of reactors using oxygen as reactant; for example of an auto-thermal reforming (ATR) unit producing syngas from natural gas, steam and oxygen (an ATR is basically a combination of a steam methane reformer (SMR) and a partial oxidation (POX) reactor). Limitations in the maximum size of a SMR unit, on the other hand, lay in the number of reactor tubes. About 1000 tubes is considered to be the maximum for a single unit operation, otherwise it will not be possible to control uniform distribution of gasses and thus heat transfer to all tubes. Further capacity limitation results from a certain maximum amount of energy that can be transferred to the tubes. It is thus estimated that a technically and economically feasible SMR reactor of maximum capacity is currently characterized by a maximum reforming heat load of about 1150 GJ/h. Methanol is typically produced on large scale in a so-called loop reactor, because conversion of syngas into methanol is relatively low. This means that an enormous volume of gas needs to be handled and recycled. For this reason, methanol loop reactors have currently a maximum capacity of 5000-6000 mtpd of methanol.

[0007] Integration of methanol and ammonia plants offers further options to reduce costs and boost capacity, by sharing unit operations, internally recycling material streams and re-use of energy (heat). In older processes, a syngas containing carbon oxides (CO and CO₂), hydrogen and nitrogen is made, and converted partially to methanol in a methanol loop reactor, methanol is separated from the effluent, and unreacted gas is purified and then fed to an ammonia reactor downstream. An example hereof is given in US 4367206, proposing an improvement of such sequential methanol and ammonia co-production using syngas containing carbon oxides, hydrogen and nitrogen as feed, by carrying out the methanol synthesis in two stages, with and without water being present. In DE 3336649 A1 sequential co-production of methanol and ammonia from methane and air is described, wherein the hydrogen/nitrogen ammonia synthesis gas stream is made by reacting excess hydrogen, separated from effluent of the methanol loop reactor, with air.

[0008] An integrated process for co-producing methanol and ammonia is also disclosed in US 6333014 B1, which process contains the steps of

- i. Reforming desulphurised hydrocarbon with steam and air in primary and secondary reformer to make a syngas mixture;
- ii. Dividing the syngas mixture into a first and a second syngas stream;
- iii. Cooling the first syngas stream to remove a water stream, and feeding remaining syngas to a methanol once-through reactor to make a methanol-containing mixture;
- iv. Separating the methanol-containing mixture into crude methanol and methanol-free gas;
- v. Feeding the second syngas stream to a high-temperature CO convertor;
- vi. Feeding effluent of the high-temperature CO convertor, the methanol-free gas and the water stream to a low-temperature CO convertor;
- vii. Feeding effluent of the low-temperature CO convertor to an ammonia synthesis section to make ammonia.

[0009] US 5180570 also describes an integrated process for co-producing methanol and ammonia from a hydrocarbon feedstock and air, which comprises the steps of

- i. separating air into substantially pure O₂ and N₂ streams;
- ii. reforming desulphurised hydrocarbon with steam and O₂ in a combined reforming section to make a methanol syngas stream;
- iii. Feeding the methanol syngas stream to a methanol loop reactor to make a methanol-containing mixture;
- iv. Separating crude methanol from the methanol-containing mixture, and recycling a first part of the remaining gas to the methanol loop reactor;
- v. Purifying a second part of the remaining gas and mixing it with N₂ to make a ammonia syngas stream;
- vi. Feeding the ammonia syngas stream to an ammonia synthesis section to make ammonia.

[0010] Considering the increasing demand for fuel and energy, there is a need in industry for ever larger and more efficient methanol and ammonia plants. Presently operated integrated production processes for making methanol and ammonia from hydrocarbon feedstock typically use methanol loop reactors, which have maximum capacity on the order of 5000 mtpd, and need to handle gas volumes about 5 times as much for recycling effluent gas.

[0011] There is a continuous need in the industry for a single-line process for making methanol and ammonia in an efficient and economical way, applying unit operations not exceeding current practical capacity limitations (as described above).

[0012] This object is achieved according to the present invention as defined in the description and claims, more specifically with a process for co-producing methanol and ammonia, wherein a syngas mixture consisting essentially of carbon monoxide (CO), carbon dioxide (CO₂) and hydrogen (H₂) is first partially reacted in a methanol once-through reactor, unreacted syngas is divided into a first and a second stream, the first stream is purified and fed to an ammonia synthesis section, and the second stream is fed to a methanol synthesis and purification section comprising a methanol loop reactor.

[0013] With the process according to the invention it is possible to produce methanol and ammonia at very high capacities in an integrated single process. For example, the process allows production of 8000 mtpd of methanol and 2000 mtpd of ammonia starting from natural gas and air, and applying a methanol loop reactor well below current maximum capacity limits. The process further shows a balanced production of ammonia and carbon dioxide, thus allowing co-production of urea also to be integrated.

[0014] In the process according to the invention for co-producing methanol and ammonia, a syngas mixture consisting essentially of carbon monoxide (CO), carbon dioxide (CO₂) and hydrogen (H₂) is first partially reacted into methanol. Syngas is generally defined as a gaseous mixture made by reforming a hydro-

carbon feedstock, and contains hydrogen (H₂) and carbon monoxide (CO), and optionally other gas components like carbon dioxide (CO₂), water (H₂O), methane (CH₄), and nitrogen (N₂). Within the context of the present invention, a syngas mixture consisting essentially of carbon monoxide (CO), carbon dioxide (CO₂) and hydrogen (H₂) is understood to contain only minor amounts of other components; i.e. at such levels that the methanol synthesis reaction is not negatively affected. For example, the water content is below the maximum amounts generally accepted in a feed for methanol production. Typically, syngas as obtained from a reforming section is cooled and condensed to essentially remove the water present. Nitrogen content of the syngas is also low, as preferably no air is added during the preceding reforming process, but rather only steam and oxygen.

[0015] The composition of synthesis gas, and thus its suitability for use for e.g. methanol production, is characterized mainly by its hydrogen and carbon monoxide content; generally presented by the so-called stoichiometric number (SN), which is defined as

$$SN = ([H_2] - [CO_2]) / ([CO] + [CO_2])$$

wherein the concentrations of components are expressed in vol% or mol%.

[0016] The value of SN is dependent on the feedstock and the reforming process used to make syngas. An overview of different suitable reforming technologies and their advantages and limitations is for example given by P. F. van den Oosterkamp in chapter "Synthesis Gas Generation: Industrial" of the "Encyclopedia of Catalysis" (John Wiley & Sons; posted on-line 2002/12/13, available via DOI: 10.1002/0471227617.eoc196).

[0017] For methanol synthesis a syngas mixture is used that preferably has a SN of 1.9-2.5, more preferably SN is 1.9-2.3, 2.0-2.2, or 2.0-2.1. For co-producing methanol and ammonia the SN of the syngas may be somewhat higher

than for methanol only, excess of hydrogen will be used in the ammonia synthesis section; but preferably composition is optimised for methanol conversion.

[0018] In the process according to the invention the syngas mixture can have
5 been made or can be made with any known process that results in the desired composition and quantities of syngas. Preferably, the syngas is made with a combined reforming process, i.e. with a process wherein a combination of different reforming reactors is used. Generally, reforming reactors are classified as being one of the following types. Conventionally, reforming of methane-rich
10 feedstock is done in a steam methane reformer (hereinafter abbreviated as SMR) by first mixing feedstock with steam and then feeding to a combustion-type (also called fired) reactor. A second type is a heat-exchange type steam reforming reactor that is heated with hot gasses produced elsewhere in the process (also called gas heated reformer, hereinafter abbreviated as GHR). An
15 auto-thermal reformer (abbreviated as ATR) is a reforming unit wherein the gasses undergo a (catalytic) partial oxidation reaction with oxygen under essentially adiabatic conditions in addition to further reaction with steam, the excess heat generated by the exothermic oxidation reactions being used to supply heat for the endothermic steam reforming reaction. In a partial oxidation reactor
20 (POX) feedstock is mainly reformed by thermal partial oxidation and steam reforming. If a feedstock is used that is rich in higher hydrocarbons, like naphtha, the feedstock is typically first treated in a so-called pre-reforming step, in order to convert the heavy hydrocarbons in the feed into methane, hydrogen and carbon oxides. Such a pre-reformer is typically operated adiabatically, and is generally
25 referred to as an adiabatic pre-reformer (APR).

[0019] Suitable examples of reforming processes are known from for example the above reference, from WO 2008/122399 A1, and from the documents cited therein.

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[0020] Preferably, the process according to the invention further comprises a combined reforming section, wherein a desulphurised hydrocarbon feedstock is reformed with oxygen and steam. The inventive process is distinguished from

prior art processes a.o. in that all syngas produced with specified composition is first fed to a methanol reactor.

[0021] In a preferred way of operating the process according to the invention
5 syngas is made with a combined reforming process as described in WO 2008/-
122399 A1, wherein a desulphurised methane-rich feedstock is mixed with
steam and passed through an adiabatic pre-reformer (APR), and wherein pre-
reformed gas from the APR is divided into three streams that are fed to a steam
methane reformer (SMR), a gas heated reformer (GHR) and -together with oxy-
10 gen- to an auto-thermal reformer (ATR), which 3 reforming reactors are opera-
ted in parallel.

[0022] In a further preferred way of operating the process according to the in-
vention, syngas is made with a combined reforming process from a desulphu-
15 rised gaseous hydrocarbon feedstock, wherein the feedstock is divided into a
first and a second feedstock stream, the first feedstock stream is mixed with
steam and fed to a gas heated reformer (GHR) and a steam methane reformer
(SMR) operated in series, and the second feedstock stream is mixed with refor-
med gas coming from the SMR and then fed with oxygen to a partial oxidation
20 reformer (POX).

[0023] Because the syngas used as feed for partially reacting into methanol
contains only low levels of nitrogen, preferably oxygen is used for partial oxida-
tion during the reforming process. For this reason, the process according to the
25 invention preferably further comprises an air separation section, wherein pure
oxygen and nitrogen streams are made by separating from air, which oxygen
and nitrogen are applied for making syngas and ammonia in the process, re-
spectively. Any conventional air separation unit (ASU) able to deliver the nee-
ded quantities can be applied in the process according to the invention.

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[0024] In the process of the present invention any hydrocarbon feedstock that is
gaseous at reforming conditions can be used, like a hydrocarbon mixture having
H/C ratio of about 2 to 4. Suitable examples include hydrocarbons like methane,

ethane, methane-rich mixtures, or light naphtha (mixture of mainly C5-C9 paraffin compounds).

[0025] A suitable example of a methane-rich feedstock is natural gas, as obtained from gas or oil fields. The primary component of natural gas is methane, which is generally present in amounts of from 80 to 97 mol%. Natural gas also contains other gaseous hydrocarbons such as ethane, typically from about 3 to 15 mol%, propane, butane and small amounts of higher hydrocarbons (generally less than 5 mol% in total), as well as sulphur-containing gases, like hydrogen sulphide, in varying amounts. Further minor (or even trace) amounts of nitrogen, helium, carbon dioxide, water, odorants, and metals like mercury can also be present. The exact composition of natural gas varies with its source.

[0026] Organo-sulphur compounds and hydrogen sulphide (H_2S) are common contaminants of hydrocarbons from natural sources, which should be removed prior to use of hydrocarbon gas as a feedstock in the present process, to avoid poisoning of reforming catalysts. Desulphurisation can be done with conventional techniques. In a suitable process, organo-sulphur compounds in the feedstock are converted to H_2S with a hydrogen-rich stream (for example a purge stream from a methanol synthesis loop), which is subsequently removed by passing over a suitable absorbent, to result in a sulphur content of the desulphurised gaseous feed of typically below 1 ppm.

[0027] Preferably, the desulphurised hydrocarbon feedstock in the process according to the invention is a methane-rich feedstock that contains as least 75 mol% of methane (based on total hydrocarbon content of the feedstock), more preferably at least 80, 85, 90, 92, 94 even at least 96 mol% of methane.

[0028] In the process according to the invention for co-producing methanol and ammonia, a syngas mixture is first partially reacted in a methanol once-through reactor. Within the context of this invention, a 'methanol once-through reactor' is understood to mean a reaction section wherein syngas is partly reacted into methanol, and unreacted effluents (syngas) are not recycled to the reactor.

Such reactor is thus different from a 'methanol loop reactor', which is a reaction section wherein feed gas is partly reacted into methanol, and unreacted effluents are continuously separated and recycled to the reactor. In a loop reactor section significantly higher volumes of gas thus need to be handled, e.g. gas flow rates about 4-6 times higher compared to a once-through reactor, and accordingly larger reactor and associated equipment (heat-exchangers, separator, compressor, etc) are needed. Investment and operating costs for a once-through methanol reactor system are thus markedly lower than for a methanol loop reactor handling the same amount of feed gas. The process according to the invention also applies a methanol loop reactor section downstream, but of relatively small size.

[0029] A further advantage of the process according to the invention is that the concentration of carbon oxides is relatively high in the syngas feed, resulting in relatively high conversion to methanol. Syngas conversion to methanol in the once-through methanol reactor may be as high as 15, 20, 25, 30, 35, 40, 45 or even 50 % in the process according to the invention.

[0030] In the process according to the invention syngas is first partially reacted in a methanol once-through reactor, whereafter unreacted syngas is divided into a first and a second stream, the first stream is then purified and fed to an ammonia synthesis section, and the second stream is fed to a methanol synthesis and purification section. The ammonia synthesis section, and the methanol synthesis and purification section can be any conventional system typically applying loop reactors and ammonia respectively methanol separators, and operated at conditions as known to a skilled person, for example from the general references given above. Such systems will therefore not be further described in detail.

[0031] The volume ratio of the first to the second stream of unreacted syngas is dependent on conversion to methanol, initial composition of the syngas and desired amounts of methanol and ammonia to be made, and can vary from about 50/50 to about 80/20. Preferably, the first and the second stream are divided in

a ratio of from about 55/45 to 77/23 or from about 60/40 to 75/25, more preferably from 65/35 to 73/27. In a preferred embodiment the ratio is about 70/30.

[0032] The invention more specifically relates to a process for co-producing methanol and ammonia, comprising the steps of

- a) Feeding a syngas mixture consisting essentially of CO, CO₂ and H₂ to a methanol once-through reactor to make a methanol/syngas mixture;
- b) Separating the mixture of step a) into crude methanol and unreacted syngas;
- c) Dividing the unreacted syngas of step b) into a first and a second stream;
- d) Feeding the first stream of step c) to a syngas purification section to make a CO, a CO₂ and a H₂ stream;
- e) Feeding the H₂ stream of step d) together with a N₂ stream to an ammonia synthesis section to make an ammonia stream;
- f) Feeding the second stream of step c) and the CO stream of step d) to a methanol loop reactor to make a methanol-containing mixture;
- g) Separating crude methanol from the methanol-containing mixture and recycling the remaining gas to step f);
- h) Feeding the crude methanol from step b) and from step g) to a methanol purification section to result in a methanol stream.

[0033] Preferably, the process according to the invention co-produces methanol and ammonia from a methane-rich feedstock and air, and comprises the steps of

- a") Feeding air to an air separation section to make an O₂ and a N₂ stream;
- a') Reforming a desulphurised hydrocarbon feedstock with O₂ from step a") and steam in a combined reforming section to make a syngas mixture consisting essentially of CO, CO₂ and H₂;
- a) Feeding the syngas mixture of step a') to a methanol once-through reactor to make a methanol/syngas mixture;
- b) Separating the mixture of step a) into crude methanol and unreacted syngas;
- c) Dividing the unreacted syngas of step b) into a first and a second stream;

- d) Feeding the first stream of step c) to a syngas purification section to make a CO, a CO₂ and a H₂ stream;
- e) Feeding the H₂ stream of step d) together with the N₂ stream of step a") to an ammonia synthesis section to make an ammonia stream;
- 5 f) Feeding the second stream of step c) and the CO stream of step d) to a methanol loop reactor to make a methanol-containing mixture;
- g) Separating crude methanol from the methanol-containing mixture and recycling the remaining gas to step f);
- h) Feeding the crude methanol from step b) and from step g) to a methanol purification section to result in a methanol stream.
- 10

[0034] The invention further relates to an integrated process for co-producing methanol and urea according to the process as described, further comprising a subsequent step of making urea in a urea synthesis section from the CO₂ and NH₃ formed in the process. As urea synthesis section any urea production technology, equipment and process conditions as known in the art can be used.

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[0035] In these processes according to the invention, preferred steps and options are those as already described in the above. The process of the invention will be discussed in more detail using an embodiment represented by the simplified block scheme as depicted in Figure 1. In this figure and in the following the symbols within the blocks have following meaning:

20

- ASU Air separation unit
- SG Syngas generation section
- 25 M1 Methanol once-through reactor section
- CS Carbon dioxide separation unit
- DR Dryer unit
- HS Hydrogen separation unit
- ME Methanator unit
- 30 AL Ammonia synthesis section
- ML Methanol loop reactor section
- DS Methanol distillation unit
- UR Urea synthesis section

C1-C5 Compressor units 1 - 5.

[0036] The numbers used for the various process streams are further elucidated in the text below. The indicated pressures and temperatures are estimates
5 for this embodiment; and are not limiting as alternative schemes and conditions may be applied as well.

[0037] In this scheme the ambient air feed stream **3** is separated in the ASU into essentially pure oxygen stream **4** (of at least 99.8% purity; typically compressed to e.g. 3 - 5 MPa), essentially pure nitrogen stream **5** (less than 5 ppm of
10 impurities like O₂ and Ar; atmospheric), and a purge stream **6** containing a.o. nitrogen and argon. Nitrogen stream **5** is compressed in C2 to stream **27** (about 4 - 6 MPa; 140 - 170 °C) for use in the ammonia section.

[0038] Hydrocarbon feed **1** is reformed in the combined reforming section SG with oxygen stream **4** and steam (not shown) into a syngas mixture, which is cooled and condensed water is removed. Resulting stream **2** (about 3 - 4 MPa; 35 - 45 °C) is compressed in C1 to stream **7** (about 7 - 9 MPa; 90 - 120 °C). The entire amount of synthesis gas stream **7** is then fed to M1, operated at 7 - 8
15 MPa and at temperature of about 220 - 250 °C. After passing the reactor crude methanol is removed, and fed as stream **9** (about 3 - 4 MPa; 40 - 50 °C) for purification in unit DS. With this arrangement about 3000 - 5000 mtpd of methanol is produced in section M1.
20

[0039] The remaining unreacted gas stream **8** (volume about 40 - 45 % reduced vs **7**) is then split at a ratio of about 70/30, but depending on desired ammonia/methanol product distribution, into stream **10** and stream **11** (both at about 6 - 8 MPa; 45-55 °C) for further methanol and ammonia production.
25

[0040] Stream **11** is mixed with CO-enriched stream **30** (about 6 - 7 MPa; 20 - 30 °C) from cryogenic hydrogen separation unit HS to make combined stream **21** (about 6 - 7 MPa; 40 - 45 °C) and further compressed in C4 to stream **22** (about 9 - 11 MPa; 80 - 100 °C), which is fed to conventional size methanol loop
30

reactor ML, operated at about 8 - 10 MPa and 220 - 250 °C. Condensed crude methanol stream **24** from ML (about 3 - 4 MPa; 40 - 45 °C) is then sent for purification in methanol distillation unit DS, together with stream **9**. A small purge gas stream from unit DS, originating from flashing of high pressure crude methanol streams 9 and 24 is not shown in the scheme. Unreacted gas is recompressed and recycled to the loop reactor ML (not shown); a purge stream **23** (about 0.3 - 0.5 MPa; 40 - 50 °C) is used as fuel within the process. Methanol product is obtained as stream **26**; stream **25** represents waste water.

10 **[0041]** In order to simplify the scheme, scrubbing water streams used for removing unreacted gasses from methanol with water in units M1 and ML are not shown.

[0042] The other divided stream **10** is further processed for ammonia synthesis. First carbon dioxide content is reduced in a conventional CO₂ separation section CS, which can be e.g. a MDEA, MEA, Benfield, Catacarb or Rectisol unit; resulting in substantially CO₂-free stream **12** (about 7 - 8 MPa; 40 - 45 °C) and CO₂ stream **13** (atmospheric). Stream **12** is subsequently passed through molecular sieve drying unit DR at about 6.5 - 7.5 MPa to result in substantially CO₂- and H₂O-free stream 14 (about 6.5 - 7.5 MPa; 40 - 50 °C) before it enters hydrogen separation unit HS, which is cryogenically operated at about -205 to -210 °C by expanding to a pressure of about 4 - 5 MPa. The resulting hydrogen stream **15** (about 4 - 5 MPa; 20 - 30 °C) contains still about 1 vol% CO, and is then passed through methanator unit ME, operated at about 2.5 - 5.0 MPa and 275 - 375 °C, to give stream **16** (about 4 - 4.5 MPa; 90 - 100 °C) containing less than 10 ppm of carbon oxides. CO separated as stream **30** is preferably used to increase amount of methanol by mixing with stream **11**.

[0043] Stream **16** is mixed with the required amount of nitrogen of stream **27** to give mixed stream **17** (about 4 - 5 MPa; 105 - 115 °C) containing hydrogen and nitrogen at 3/1 ratio; which is compressed in C3 to give stream **18** (about 15 - 16 MPa; 110 - 130 °C). Stream **18** is then fed as make-up gas to a loop in ammonia synthesis section AL, which reactor is operated at about 15 - 20 MPa and

350-450 °C. A small purge stream **19** (about 0.3 - 0.5 MPa; 20 - 30 °C) is used as fuel within the process. Ammonia product is obtained as stream **20**, typically at 2 - 3 MPa and 40 - 50 °C.

- 5 **[0044]** In a further preferred embodiment, CO₂ stream **13** is sent to urea synthesis section UR, after compression to about 16 - 20 MPa and 100 - 150 °C in unit C5, with the desired amount of ammonia via stream **20**, to result in urea product **29** (in prilled or granular form).
- 10 **[0045]** The invention therefore also relates to an integrated production plant that is suitable for making methanol and ammonia from syngas with the process of the invention, comprising a methanol once-through reactor, a methanol loop reactor, a methanol purification section, a syngas purification section, and an ammonia synthesis section.

15

- [0046]** The invention further relates to an integrated production plant suitable for making methanol and ammonia from a methane-rich feedstock and air with the process according to the invention, comprising a combined reforming section, an air-separation section, a methanol once-through reactor, a methanol loop
- 20 reactor, a methanol purification section, a syngas purification section, and an ammonia synthesis section.

- [0047]** The invention further relates to an integrated production plant suited for making methanol and urea from syngas applying the process of the invention,
- 25 comprising a methanol once-through reactor, a methanol loop reactor, a methanol purification section, a syngas purification section, an ammonia synthesis section, and a urea synthesis section; as well as to an integrated production plant for making methanol and urea from a methane-rich feedstock and air applying the process of the invention, comprising a combined reforming section,
- 30 an air-separation section, a methanol once-through reactor, a methanol loop reactor, a methanol purification section, a syngas purification section, an ammonia synthesis section, and a urea synthesis section.

Example

[0048] Production of methanol, ammonia, and urea from a syngas mixture with the process according to the invention as embodied in the flow scheme of Figure 1 and described above, is now further elucidated using the standard simulation package Pro-II, taking as boundary condition a maximum input of 5208 kmol/h of oxygen from an ASU to a combined reforming process as described in WO 2008/122399 A1.

[0049] In Table 1 the conditions (temperature and pressure) are given for each process step or stream, following the numbering of Figure 1, as well as the calculated mass balance expressed in kgmol/h (or mtpd).

[0050] It can be concluded from this simulation that with the process according to the invention it is feasible to co-produce for example about 8000 mtpd of methanol and about 2000 mtpd of ammonia. The ammonia may be converted into about 3500 mtpd of urea, using the carbon dioxide available within the process.

Table 1

Stream	Composition									Conditions	
	H ₂	CO	CO ₂	CH ₄	N ₂	CH ₃ OH	NH ₃	H ₂ O	Total	T	P
	(kgmol/h)									(°C)	MPa
1	Natural Gas Feed: 13999 kgmol/h										
2	34107.0	9603.1	4113.5	393.2	771.6			157.3	49145.7	45	3
3	Air to ASU										
4	O ₂ from ASU: 5208 kgmol/h (4000 mtpd)										
5					2535.8				2535.8	45	0.1
6	Excess N ₂ and Ar vent from ASU										
7	34107.0	9603.1	4113.5	393.2	771.6			94.5	49082.9	96.3	7.8
8	20715.1	3303.9	3569.9	387.4	769.1	47.2		57.4	28850.0	51	7.2
9	20.7	24.0	269.9	5.8	2.5	6501.7		510.8	7335.4	45	7.2
10	14717.0	2347.2	2536.2	275.2	546.4	33.6		40.8	20496.4	50	7.2

Stream	Composition									Conditions	
	H ₂	CO	CO ₂	CH ₄	N ₂	CH ₃ OH	NH ₃	H ₂ O	Total	T	P
	(kgmol/h)									(°C)	MPa
11	5998.1	956.7	1033.7	112.2	222.7	13.7		16.6	8353.6		
12	14682.7	2347.2	17.9	275.2	541.1			23.7	17887.8	45	7.2
13	34.2		2518.4		5.3			273.0	2830.9	45	0.1
14	14682.7	2347.2		275.2	541.1				17846.2	45	7.2
15	7856.0	79.4							7935.4	25	4.5
16	7617.9			79.4				79.4	7776.6	97	4.4
17	7617.9			79.4	2535.8			79.4	10312.5	113	4.4
18	7617.9			79.4	2535.8			79.4	10312.5	122	15.9
19	261.5			65.0	83.7		6.1		416.3		
20	Ammonia: 4893 kgmol/h (2000 mtpd)										
21	12824.9	3224.5	1033.7	387.4	763.8	13.7		16.6	18264.6	43	6.8
22	12824.9	3224.5	1033.7	387.4	763.8	13.7		16.6	18264.6	86	10
23	4169.0	153.5	153.7	368.8	754.9	4.9		8.2	5613.0	49	9.5
24	16.4	4.1	44.8	18.6	8.8	3911.2		893.9	4897.8	45	9.5
25								1519.0	1519.0		4.6
26	Methanol: 10403 kgmol/h (8000 mtpd)										
27					2535.8				2535.8	165	4.6
28	34.2		2518.4		5.3			15.4	2573.3		
29	Urea: 2430 kgmol/h (3500 mtpd)										
30	6826.7	2267.9		275.2	541.1				9910.9	25	6.8

Patentkrav

1. Fremgangsmåde til samtidig fremstilling af methanol og ammoniak, hvori en syntesegasblanding bestående af i al væsentlighed af carbonmonoxid (CO),
5 carbondioxid (CO₂) og hydrogen (H₂) først delvis omsættes i en methanolgennemløbsreaktor, og ureageret syntesegas opdeles i en første og en anden strøm, hvor den første strøm oprenses og fødes til en ammoniaksyntesesektion, og den anden strøm fødes til en methanolsyntese- og oprensningssektion omfattende en methanolsløjfareaktor.
10
2. Fremgangsmåde til samtidig fremstilling af methanol og ammoniak ifølge krav 1 omfattende trinnene:
 - a) fødnings af en syntegasblanding bestående i al væsentlighed af CO, CO₂
15 og H₂ til en methanolgennemløbsreaktor for at fremstille en methanol/syntesegasblanding,
 - b) separering af blandingen fra trin a) i råmethanol og uomsat syntesegas,
 - c) opdeling af den ureagerede syntesegas fra trin b) i en første og en anden strøm,
 - 20 d) fødnings af den første strøm fra trin c) til en syntesegasoprensningssfunktion for at fremstille en CO-, en CO₂- og en H₂-strøm,
 - e) fødnings af H₂-strømmen fra trin d) sammen med en N₂-strøm til en ammoniaksyntesesektion for at fremstille en ammoniakstrøm,
 - f) fødnings af den anden strøm fra trin c) og CO-strømmen fra trin d) til en
25 methanolsløjfareaktor for at fremstille en methanolholdig blanding,
 - g) adskillelse af råmethanol fra den methanolholdige blanding og tilbageførsel af den resterende gas til trin f),
 - h) fødnings af den rå methanol fra trin b) og fra trin g) til en methanoloprensningsssektion for at resultere i en methanol-strøm.
30
3. Fremgangsmåde til samtidig fremstilling af methanol og ammoniak ifølge krav 1 eller 2 omfattende trinnene:

- a'') føddning af luft til en luftadskillelsessektion for at fremstille en O_2 - og en N_2 -strøm,
- a') reforming af en afsvovlet carbonhydridråvare med O_2 fra trin a'') og damp i en kombineret reformningssektion for at fremstille en syntesegasblanding bestående i al væsentlighed CO , CO_2 og H_2 ,
- 5 a) føddning af syntesegasblandingen fra trin a') til en methanolgennemløbsreaktor for at fremstille en methanol/syntesegas-blanding,
- b) separering af blandingen fra trin a) i rå methanol og uomsat syntesegas,
- c) opdeling af den ureagerede syntesegas fra trin b) i en første og en anden strøm,
- 10 d) føddning af den første strøm fra trin c) til en syntesegasoprensningssktion for at fremstille en CO -, CO_2 - og en H_2 -strøm,
- e) føddning af H_2 -strømmen fra trin d) sammen med N_2 -strømmen fra trin a'') til en ammoniaksyntesesektion for at fremstille en ammoniakstrøm,
- 15 f) føddning af den anden strøm fra trin c) og CO -strømmen fra trin b) til en methanolsløjfereaktor for at fremstille en methanolholdig blanding,
- g) adskillelse af råmethanol fra den methanolholdige blanding og tilbageføring af den resterende gas til trin f),
- h) føddning af råmethanolen fra trin b) og fra trin g) til en methanoloprensningssktion, hvilket resulterer i en methanolstrøm.
- 20
4. Fremgangsmåde ifølge et vilkårligt af kravene 1 - 3, hvor syntesegasblandingen har et støkiometrisk tal SN fra 1,9 til 2,3.
- 25 5. Fremgangsmåde ifølge krav 3, hvor en methanrigråvare blandes med damp og ledes gennem en adiabatisk præreformer (APR), og hvor præreformet gas fra APR deles i tre strømme, som fødes til en dampmethanreformer (SMR), en gasopvarmet reformer (GHR) og sammen med oxygenet til en autotermisk reformer (ATR), hvilke 3 reformingsreaktorer betjenes parallelt.
- 30 6. Fremgangsmåde ifølge et vilkårligt af kravene 1 - 5, hvor carbonhydridråvaren er en methanrig råvare, som indeholder mindst 75 mol% methan.

7. Fremgangsmåde ifølge et vilkårligt af kravene 1 - 6, hvor den første og anden strøm af uomsat syntesegas deles i et forhold fra 50/50 til 80/20.
8. Fremgangsmåde ifølge krav 7, hvor forholdet af den første til den anden
5 strøm er 70/30.
9. Fremgangsmåde til samtidig fremstilling af methanol og urinstof omfattende fremgangsmåden ifølge et vilkårligt af kravene 1 - 8, og et efterfølgende trin med fremstilling af urinstof i en urinstofsyntesesektion, fra CO_2 og H_2 dannet i
10 fremgangsmåden.
10. Fremstillingsanlæg til at fremstille methanol og ammoniak fra syntesegas ifølge fremgangsmåden ifølge et vilkårligt af kravene 1 - 9 omfattende en methanolgennemløbsreaktor, en methanolsløjferektor, en methanoloprensnings-
15 sektion, en syntesegasoprensningssektion og en ammoniaksyntesesektion.

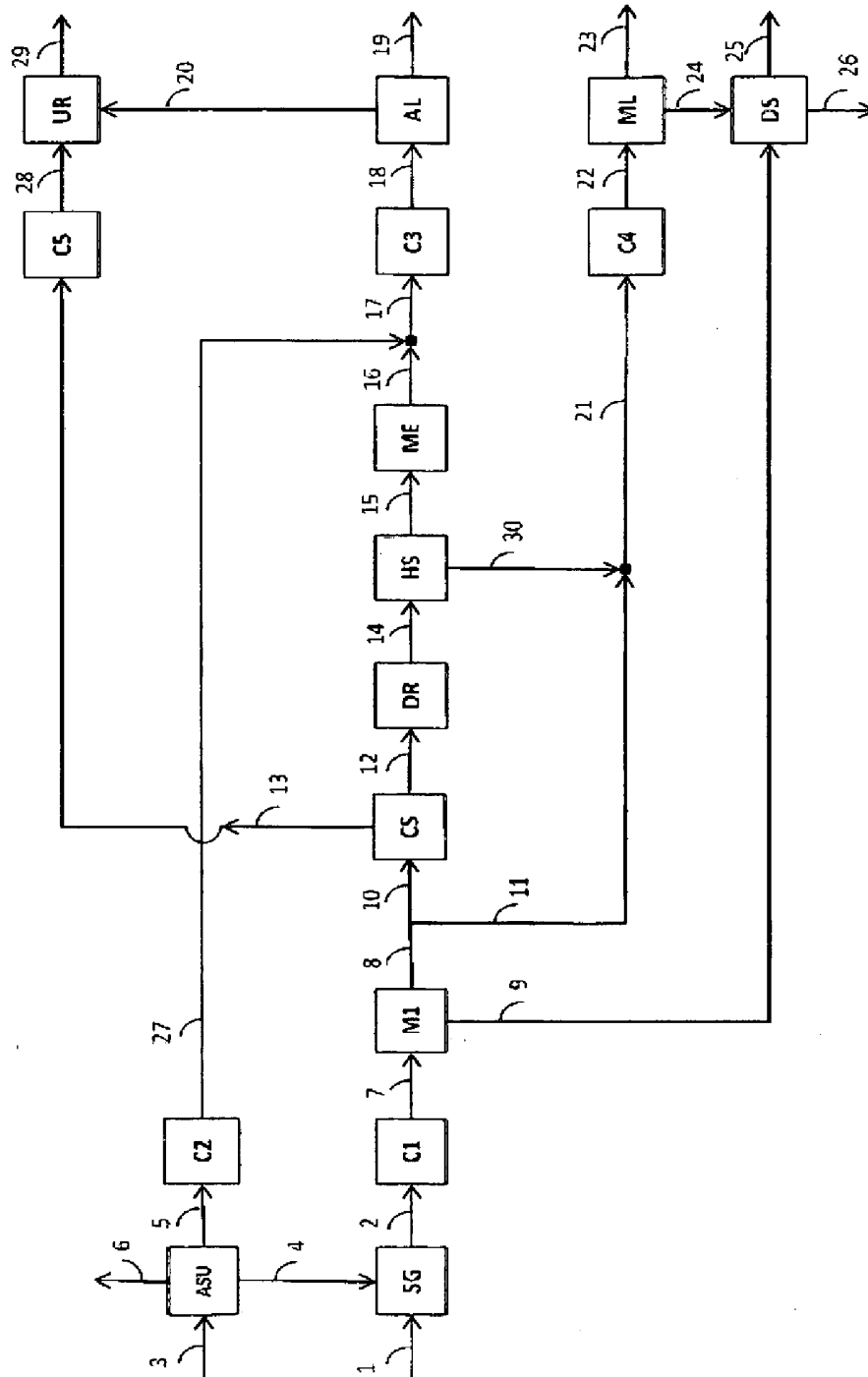


Fig-1