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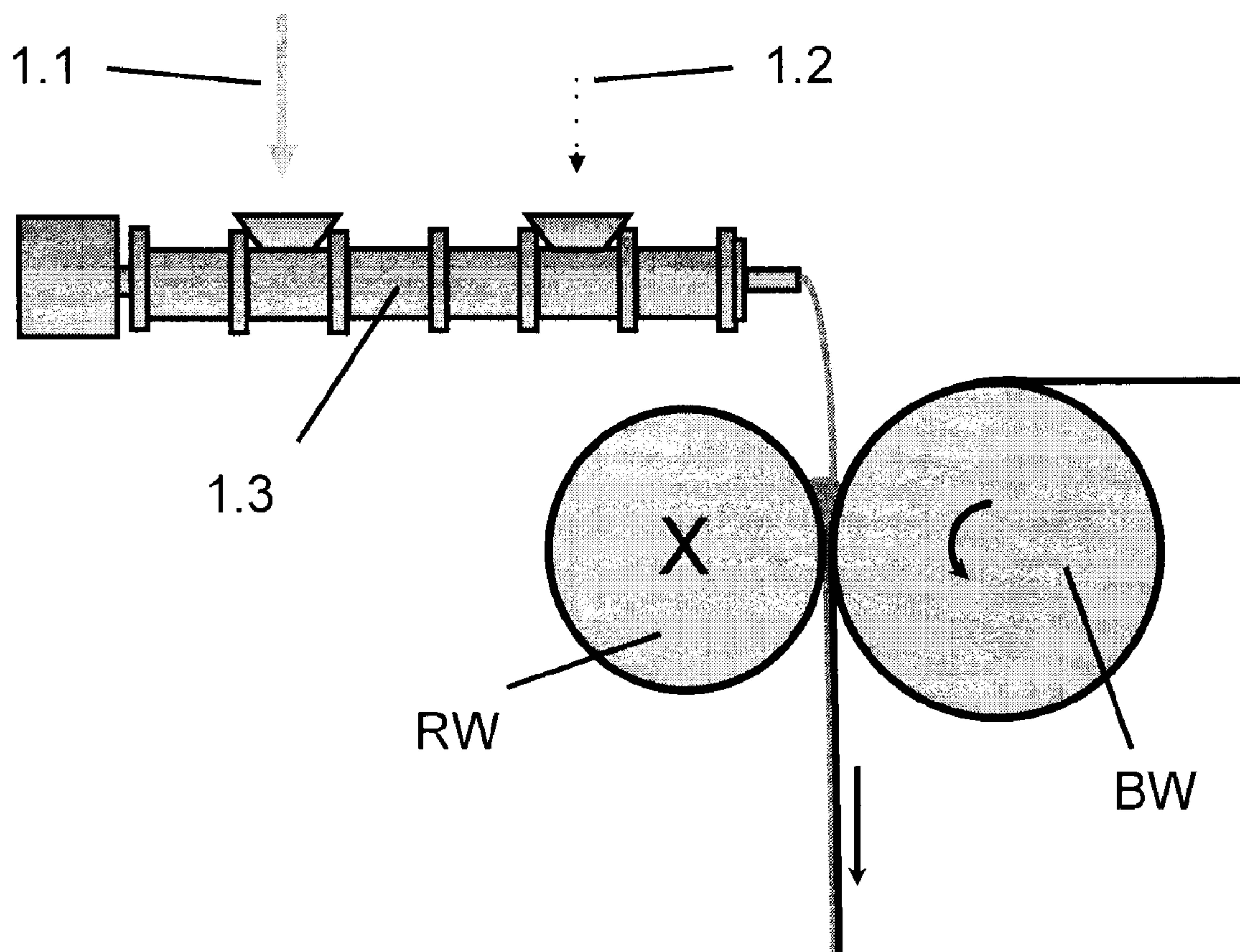
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(54) Titre : POLYACRYLATES A RETICULATION THERMIQUE ET LEUR PROCEDE DE PREPARATION

(54) Title: THERMALLY CROSSLINKING POLYACRYLATES AND PROCESS FOR THEIR PREPARATION



(57) Abrégé/Abstract:

The invention relates to a process for preparing homogeneously crosslinked polymers, in which at least one crosslinker is added to a polymer in the melt, in which the polymer is further processed from the melt, and in which a thermal crosslinking reaction is

(57) **Abrégé(suite)/Abstract(continued):**

brought about by means of the crosslinker, with at least part of the crosslinking reaction taking place after the further processing at a temperature below the melting temperature of the polymer, characterized in that the crosslinker comprises an at least difunctional compound, at least one of the functional groups being an oxazoline group, and the polymer contains functional groups which, at a temperature below the melting temperature of the polymer, are able to react with the oxazolines in a linking reaction in the sense of the thermal crosslinking reaction.

Abstract

The invention relates to a process for preparing homogeneously crosslinked polymers, in which at least one crosslinker is added to a polymer in the melt, in which the polymer is further processed from the melt, and in which a thermal crosslinking reaction is brought about by means of the crosslinker, with at least part of the crosslinking reaction taking place after the further processing at a temperature below the melting temperature of the polymer, characterized in that the crosslinker comprises an at least difunctional compound, at least one of the functional groups being an oxazoline group, and the polymer contains functional groups which, at a temperature below the melting temperature of the polymer, are able to react with the oxazolines in a linking reaction in the sense of the thermal crosslinking reaction.

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Description

Thermally crosslinking polyacrylates and process for their preparation

The invention relates to a process for thermal crosslinking of polymers, in particular of polyacrylates, and to thermally crosslinking and crosslinked polymers thus prepared.

For high-end industrial applications, including more particularly as adhesives, pressure-sensitive adhesives or heat-sealing compositions, the ingredients used include polyacrylates, these polymers having emerged as being highly suitable for the growing requirements in these fields of application.

Thus adhesive compounds are required to have a good tack, but must also meet exacting requirements in the area of shear strength. At the same time, the processing properties must also be good, including in particular a high suitability for the coating of these compositions onto backing materials. This is achieved in particular by polyacrylates with a high molecular weight, high polarity and subsequent efficient crosslinking. Moreover, polyacrylates can be prepared transparently and with weathering stability.

In the coating of polyacrylate compositions from solution or as a dispersion, which can be used, for example, as a pressure-sensitive adhesive, viscoelastic backing or heat-sealing compositions, thermal crosslinking is well-established prior art. In general the thermal crosslinker – for example, a polyfunctional isocyanate, a metal chelate or a polyfunctional epoxide – is added to the solution of a polyacrylate furnished accordingly with functional groups, and this composition is coated in a planar fashion onto a substrate, with the aid of a doctor blade or coating bar, and is subsequently dried. As a result of this process, diluents – that is, organic solvents or water in the case of the dispersions – are evaporated and the polyacrylate, accordingly, is crosslinked. The crosslinking is very important for the coatings, since it gives them sufficient cohesion and thermal shear strength. In the absence of crosslinking, the coatings would be too soft and would flow

away under even a low load. Critical to a good coating outcome is the observance of the pot life (processing life, within which the system is in a processable state), which can vary greatly according to crosslinking system. If this life is too short, the crosslinker has already undergone reaction in the polyacrylate solution; the solution is already incipiently crosslinked (partially gelled or completely gelled) and can no longer be coated out uniformly.

For reasons in particular of environmental protection, the technological operation for the preparation of pressure-sensitive adhesives is in a state of continual development. As a result of the environmental strictures, which have become more restrictive, and as a result of the climbing prices for solvents, there is concern as far as possible to eliminate the solvents from the manufacturing operation for polymers. In the industry, therefore, there is growing importance attached to melt processes (also referred to as hotmelt processes) with solvent-free coating technology for the preparation of polymers, particularly of pressure-sensitive adhesives. In such processes, meltable polymer compositions, in other words polymer compositions which at elevated temperatures undergo a transition to the fluid state without decomposing, are processed. Compositions of this kind can be processed outstandingly out of this melt state. In developments of this operation, the preparation as well can be carried out in a low-solvent or solvent-free procedure.

The introduction of the hotmelt technology is imposing increasing requirements on the adhesives. The aforementioned meltable polyacrylate compositions (other names: "polyacrylate hotmelts", "acrylate hotmelts") in particular are being very intensively investigated for improvements. In the coating of polyacrylate compositions from the melt, thermal crosslinking has to date not been very widespread, despite the potential advantages of this process.

To date acrylate hotmelts have primarily been crosslinked by radiation-chemical methods (UV irradiation, electron irradiation [EBC]). Yet this is a procedure fraught with disadvantages:

- in the case of crosslinking by means of UV rays, only UV-transparent (UV-pervious) layers can be crosslinked;
- in the case of crosslinking with electron beams (electron beam crosslinking or electron beam curing, also EBC), the electron beams possess only a limited depth of

penetration, which is dependent on the density of the irradiated material and on the accelerator voltage;

- in both of the aforementioned processes, the layers after crosslinking have a crosslinking profile, and the pressure-sensitive adhesive layer does not crosslink homogeneously.

The pressure-sensitive adhesive layer must be relatively thin in order for well-crosslinked layers to be obtained. The thickness through which radiation can pass, though indeed varying as a function of density, accelerator voltage (EBC) and active wavelength (UV), is always highly limited; accordingly, it is not possible to effect crosslinking through layers of arbitrary thickness, and certainly not homogeneously.

Also known in the prior art are a number of processes for the thermal crosslinking of acrylate hotmelts. In each of these processes a crosslinker is added to the acrylate melt prior to coating, and then the composition is shaped and wound to form a roll.

Direct thermal crosslinking of acrylate hotmelt compositions containing NCO-reactive groups is described in EP 0 752 435 A1. The isocyanates used, which are free from blocking agents, and are, more particularly, sterically hindered and dimerized isocyanates, require very drastic crosslinking conditions, and so a rational technical reaction presents problems. Under the kind of conditions which prevail on processing from the melt, the procedure described in EP 0 752 435 A1 leads to rapid and relatively extensive crosslinking, and so processing of the composition, particularly with a view to the coating of backing materials, is difficult. In particular it is not possible to obtain any very homogeneous layers of adhesive of the kind that are needed for many technical applications of adhesive tapes.

Also prior art is the use of blocked isocyanates. A disadvantage of this approach is the release of blocking groups or fragments, which have an adverse effect on the adhesive properties. One example is US 4,524,104 A. It describes pressure-sensitive acrylate hotmelt adhesives which can be crosslinked with blocked polyisocyanates together with cycloamidines or salts thereof as catalyst. In this system, the necessary catalyst, but especially the resultant HCN, phenol, caprolactam or the like, may significantly adversely affect the product properties. With this approach, moreover, there is a need for often drastic conditions for the release of the reactive groups. Significant product use is unknown to date and, furthermore, appears unattractive. US 6,340,719 B1 describes

monoisocyanates or polyisocyanates that are likewise blocked and that are incorporated via a double bond into the polyacrylate. Here again the aforementioned problems arise, and a further factor is that the deblocking must in any event not proceed in the course of processing in the melt, since attachment to the polymer backbone may cause a reaction of the liberated isocyanate functionality, with formation of a network, and hence may lead to gelling.

DE 10 2004 044 086 A1 describes a process for thermal crosslinking of acrylate hotmelts wherein a solvent-free functionalized acrylate copolymer which, following addition of a thermally reactive crosslinker, has a processing life which is sufficiently long for compounding, conveying and coating, is coated, preferably by means of a roller method, onto a web-like layer of a further material, more particularly a tapelike backing material or a layer of adhesive, and which, after coating, undergoes subsequent crosslinking under mild conditions until the cohesion achieved is sufficient for pressure-sensitive adhesive tapes.

A disadvantage of this process is that the reactivity of the crosslinker (isocyanate) predetermines the free processing life and the degree of crosslinking. Where isocyanates are used, they react in part during actual addition, as a result of which the gel-free time may be very short, depending on the system. A composition with a relatively high fraction of functional groups such as hydroxyl groups or carboxylic acid can in that case no longer be coated sufficiently well in the coatings. A streaky coat interspersed with gel particles, and therefore not homogeneous, would be the consequence.

A further problem which arises is that the attainable degree of crosslinking is limited. If a higher degree of crosslinking is desired, through addition of a higher quantity of crosslinker, this has drawbacks when polyfunctional isocyanates are used. The composition would react too quickly and would be coatable, if at all, only with a very short processing life and hence at very high coating speeds, which would increase the problems of the non-homogeneous coating appearance.

DE 100 08 841 A1 describes polyacrylates which are obtainable through thermal crosslinking of a polymer mixture which comprises *tert*-butoxycarbonyl (BOC) protecting groups, a cationic photoinitiator and a difunctional isocyanate and/or difunctional epoxide. Also described is a process for preparing crosslinked polyacrylates, in which the polymers to be crosslinked are first protected by introduction of *tert*-butoxycarbonyl groups and the crosslinking takes place only after deprotection by thermal treatment of the polyacrylates

that have then been deprotected. The introduction of the protecting groups in this case is to prevent the crosslinking reaction, which is only desired subsequently, when the operating temperatures prevailing are already high in the course of earlier stages of processing, as is the case, for example, in the hotmelt process. The protection is valid in particular for the crosslinking reaction at this point in time, but also for all other competing reactions which would attack the unprotected functional groups of the polymer to be processed, more particularly its hydroxide groups.

A disadvantage of the process presented therein is that the reactive groups, after coating, must first be released by UV irradiation. Consequently the disadvantages which apply here for thermal crosslinking are the same as those already recited above for radiation-induced crosslinking (UV irradiation). Moreover, combustible isobutene is released.

EP 1 317 499 A describes a process for crosslinking of polyacrylates via UV-initiated epoxide crosslinking, in which the polyacrylates have been functionalized during the polymerization with corresponding groups. The process offers advantages in relation to the shear strength of the crosslinked polyacrylates as compared with conventional crosslinking mechanisms, particularly as compared with electron beam crosslinking. This specification describes the use of difunctional or polyfunctional, oxygen-containing compounds, more particularly of difunctional or polyfunctional epoxides or alcohols, as crosslinking reagents for functionalized polyacrylates, more particularly functionalized pressure-sensitive acrylate hotmelt adhesives.

Since the crosslinking is initiated by UV rays, the resultant disadvantages are the same as those already mentioned.

For the crosslinking of water-based polyacrylates, EP 1 323 802 B1 describes oxazolines, and JP 2006124640 A describes the incorporation of such functionalities into the polymer backbone as reactive groups. Oxazolines are notable for their water solubility, their chemoselectivity - they react, for example, only with carboxylic acids, thiols or amines, even in the presence of hydroxyl groups - and especially high reactivity above 80°C, for which reason they are generally not suitable for a hotmelt operation, since the melting temperature and hence processing temperature is above 80°C and consequently there would be gelling before or during the coating operation.

Transfer to hotmelt systems was therefore not very obvious to a person skilled in the art, owing to the high reactivity at high temperatures.

It is an object of the invention to enable thermal crosslinking of polymers which can be processed from the melt ("polymer hotmelts"), with a sufficiently long processing life ("pot life") being available for the processing from the melt, especially as compared with the pot life of the known thermal crosslinking systems for the corresponding polymer hotmelts. At the same time, it ought to be possible not to use protecting groups which would have to be removed again, possibly, by actinic radiation or other methods, and not to use volatile compounds which afterwards remain in the product and evaporate. Moreover, it ought to be possible to set the degree of crosslinking of the polyacrylate composition to a desired level, without adversely affecting the advantages of the operating regime.

Surprisingly it has been found that a crosslinker comprising a substance having at least one 2-oxazoline, 3-oxazoline or 4-oxazoline group was an outstanding solution to the stated object. Advantageously, the substance itself represents the crosslinker. It is particularly advantageous to use substances whose melting point is at least 10°C above the processing temperature of the polyacrylate melt, and which mix and/or dissolve only slowly with preference, but homogeneously, in the polymer melt.

The invention accordingly provides a process for preparing homogeneously crosslinked polymers,

- in which at least one crosslinker is added to a polymer in the melt,
- in which the polymer is further-processed from the melt,
- and in which a thermal crosslinking reaction is brought about by means of the crosslinker, with at least part of the crosslinking reaction taking place after the further processing at a temperature below the melting temperature of the polymer, where
- the crosslinker comprises an at least difunctional compound, at least one of the functional groups being an oxazoline group, and
- the polymer contains functional groups which, at a temperature below the melting temperature of the polymer, are able to react with the oxazolines in a linking reaction in the sense of the thermal crosslinking reaction.

In a further development of the process of the invention the crosslinking reaction takes place at least partially at room temperature.

The polymers to be crosslinked are preferably polyacrylates. Below, the expression "polyacrylate" is intended in the context of this specification to encompass pure polyacrylates, polymethacrylates, copolymers of acrylate monomers and/or methacrylate monomers and, if desired, further comonomers, and also polymer blends comprising polyacrylates, polymethacrylates and/or copolymers of acrylate monomers and/or methacrylate monomers and, if desired, further comonomers.

The polymers may have been admixed in the melt with further additives, such as tackifying resins, for example (see later on below). The process of the invention is outstandingly suitable for the thermal crosslinking of polymers as a basis for very homogeneous pressure-sensitive adhesives.

In one advantageous embodiment of the process of the invention, the further processing of the polymer from the melt comprises shaping of the polymer composition, more particularly its coating on a backing material, in which case the further processing may also be confined to the shaping or coating operation. Advantageously the crosslinking takes place at least partially after this shaping operation, in particular in the polymer layer.

It has been found that a good crosslinking rate has been achievable, even at a temperature below the melting temperature, more particularly even at room temperature, of the polymer as a result of the addition of one or more functional groups with an accelerating action (referred to below as "accelerator groups").

Crosslinkers used are at least difunctional compounds which contain at least one oxazoline group, the oxazoline group in question being more preferably an oxazoline group with the double bond in position 2 (2-oxazoline group). Use may advantageously be made of difunctional and/or polyfunctional crosslinkers (i.e. those having two or having three or more functional groups), which - in particular for the crosslinking reaction - serve as active centres. Where reference is made below to polyfunctional compounds, the intention, unless specified otherwise, is that difunctional compounds should also be included.

For the inventive teaching it is of advantage if the oxazoline groups are attached via the C atom in position 2 to the framework of the at least difunctional substance, i.e. of the crosslinker. Where the crosslinker substances have two or more oxazoline groups (difunctional or polyfunctional oxazolines), then preferably all of the oxazoline groups are

attached to the crosslinker framework via the C atom in position 2 (cf. in this respect also the reaction scheme of the linking reaction later on below).

In one advantageous embodiment of the invention substances (also referred to as "accelerators") are added to the polymer to be crosslinked that contain the accelerator groups. The accelerator groups may instead or additionally also be functional groups of the polymers themselves, however.

Substance (or group) with an accelerating action means that the substance (or group) supports the crosslinking reaction by ensuring an inventively sufficient reaction rate, while the crosslinking reaction in the absence of the accelerator would not take place at all, or would take place with inadequate speed, at selected reaction parameters, here in particular a temperature situated below the melting temperature of the polyacrylates. The accelerator thus ensures a substantial improvement in the reaction kinetics of the crosslinking reaction. In accordance with the invention this may take place catalytically, or alternatively by incorporation into the reaction events.

The polymers for crosslinking contain functional groups suitable for entering into linking reactions – particularly in the sense of addition reactions or substitution reactions – with oxazoline groups, particularly at temperatures which lie below the melting temperature of the polymers. With very particular preference the polymers contain functional groups which possess the above-described suitability at room temperature.

Suitable functional groups are thiol groups, phenol groups and, with particular advantage, carboxyl groups.

The crosslinking reaction is preferably accompanied by linking of the building blocks bearing the functional groups to the building blocks bearing the oxazoline groups (especially in the sense of crosslinking of the corresponding polymer building blocks bearing the functional groups, via the substances bearing oxazoline groups, as linking bridges).

In the case of the substances containing oxazoline groups, polyfunctional oxazolines are used in particular, i.e. those having at least two oxazoline groups; correspondingly, the overall effect is of indirect linking of the building blocks bearing the functional groups.

On the basis of the high reactivity of the thermal crosslinkers at high temperatures, of the kind that occur in the course of processing (i.e. in particular, at temperatures above the

melting temperature of the polymers), their presence, particularly in the presence of accelerators, would mean that the polymer system could no longer be homogeneously processed, especially compounded and coated, since the compositions would undergo excessive, and excessively rapid, crosslinking or even gelling ("uncontrolled" crosslinking). Through the use of the oxazoline compounds described it has been possible to prevent this behaviour.

A particularly advantageous procedure is to use oxazolines which mix or dissolve only poorly in the polymer melt. In accordance with the invention it is possible to use not only liquid substances containing oxazoline groups but also solid substances containing oxazoline groups as crosslinkers.

Where solid crosslinker substances are used, it is preferred to select those systems whose melting point is at least 10°C, more preferably at least 20°C, above the processing temperature.

In undissolved or solid form, only the oxazoline functionalities that are located at the interfaces are available for reaction with the polymer. The polymer, therefore, would be partially crosslinked, but owing to the small number of nodes there is as yet no gelling, and the polymer continues to be processable. The greater the amount of crosslinker that dissolves in the polymer over time, the greater the extent to which the crosslinking reaction can take place, with a major part proceeding only when the composition has already been applied in a coating operation.

Through the process of the invention it is possible to continue crosslinking of polymers, especially polyacrylates, after processing, especially after coating out as a layer or after application to a backing, with a significantly reduced supply of thermal energy than that for obtaining the melt, i.e. after cooling, without the need for actinic irradiation for this purpose.

In particular, by virtue of the process of the invention, the polymers are capable of undergoing further crosslinking without further thermal energy supplied actively, that is, by process engineering means (heating), more particularly after cooling to room temperature (RT, 20°C) or to a temperature close to room temperature. In particular it is possible in this phase of crosslinking to forego heating, without this causing termination of the crosslinking reaction.

Oxazolines without appropriate accelerators frequently have a sufficient reactivity only under the influence of heat. Accelerator substances such as, for example, Brønsted acids or Lewis acids lead to an improvement in the reactivity in the temperature range of the melt (i.e. at the processing temperature) and also at lower temperatures, more particularly at room temperature. This is particularly important when the polymers processed in hotmelt form are coated within relatively short time periods (a few minutes) and then, in the absence of further supply of heat, cool rapidly down to room temperature or storage temperature. Without the initiation of a further crosslinking reaction it would not be possible to achieve high degrees of crosslinking, and this, especially for many areas of application of polyacrylates, such as their use as pressure-sensitive adhesives in particular, would result in inadequate cohesion of the composition.

As substances having an accelerating action ("accelerators") it is possible more particularly to use Brønsted acids or Lewis acids. The accelerators can either be added as an extra to the reaction mixture or may be present in the form in which they are attached to the polymer; accelerator groups may be, for example, carboxylic or sulphonic acid groups.

Carboxylic acid groups do react with the oxazoline crosslinkers, but the concentration is preferably selected to be higher than that of the oxazoline component, and so they can be regarded both as a reactant and as an accelerator.

Through the inventive combination of the inventive crosslinkers with such accelerators, combined with a poor solubility of the crosslinkers in the polymer with liquid components or a high melting point combined with a poor solubility with solid crosslinkers, it has been possible to offer a particularly advantageous thermal crosslinking process which, in the processing of the polymer hotmelt compositions, in particular in the case of polyacrylate hotmelt compositions, in other words in the melt, does not lead to uncontrolled reactions (gelling of the composition) and allows a sufficiently long time (pot life) for processing, so that, particularly in the case of coating out as a layer or application to a backing, it is possible to create a uniform and bubble-free coat.

In an outstanding and unexpected way, the process of the invention offers the advantage that it is possible to offer a stable crosslinking process for polyacrylates, with outstanding

control possibility in relation to the crosslinking pattern, as a result of substantial decoupling of degree of crosslinking and reactivity (reaction kinetics).

The process of the invention serves outstandingly for the thermal crosslinking of polyacrylates. The starting point is a polymer, a copolymer or a polymer mixture (see above), more particularly a polyacrylate copolymer, based on acrylic esters and/or methacrylic esters, with at least some of the acrylic esters and/or methacrylic esters containing functional groups which are able to react in the manner outlined above, more particularly with formation of a covalent bond, with oxazolines, especially 2-oxazoline groups. The reaction between a 2-oxazoline group and a carboxyl group is illustrated using the following example. Existing protons (particularly from extant carboxyl groups) or added Lewis acids or Brønsted acids cause labilization of the oxazoline ring, by protonation and/or complexation, thereby accelerating the reaction.



R^1 here symbolizes the framework of the polymer to be crosslinked; R^2 symbolizes the framework of the polyfunctional crosslinker. R^2 accordingly comprises at least one functional second group which is able to react with functional groups of the polymer chains to be crosslinked, more particularly one or more further oxazoline groups which are likewise able to react in accordance with the above equation, with the linking of two or more polymer chains to one another being brought about.

The crosslinked polymers, in particular polyacrylates, can be employed for all possible fields of application in which a certain cohesion in the composition is desired. The process is especially advantageous for viscoelastic materials on a polyacrylate basis. One specific area of application of the process of the invention is in the thermal crosslinking of pressure-sensitive adhesives (PSAs), including, in particular, hotmelt PSAs.

With particular advantage the procedure adopted in respect of the process of the invention is one in which the crosslinker is added in the melt of the polymer, in particular polyacrylate, it being already optionally possible to use the crosslinking reaction, and the

polymer is subsequently cooled if the crosslinking reaction has not yet run its course or not until it reaches a very low threshold, to the extent that the polymer retains outstanding processing properties – that is, for example, can be coated homogeneously and/or can be shaped outstandingly. For adhesive tapes in particular a homogeneous, uniform coat pattern is needed, with no lumps, specks or the like to be found in the layer of adhesive. Correspondingly homogeneous polymers are also required for the other forms of application.

Shapability or coatability exists when the polymer has not yet undergone crosslinking or has undergone crosslinking only to a slight degree; advantageously the degree of crosslinking at the start of cooling is not more than 10%, preferably not more than 3%, more preferably not more than 1%. The crosslinking reaction continues to progress after cooling as well, until the ultimate degree of crosslinking is attained.

The term “cooling” here and below also encompasses the passive cooling as a result of removing heating.

The process of the invention can be carried out in particular by initiating the crosslinking in the melt of the polymer in the presence of the crosslinker, more particularly of the crosslinker system (i.e., thermally), preferably at a point in time shortly before further processing, more particularly before shaping or coating. This takes place commonly in a processing reactor (compounder, an extruder for example). The composition is then removed from the compounder and subjected to further processing and/or shaping as desired. In the course of processing or shaping, or afterwards, the polymer is cooled, by deploying active cooling and/or by adjusting the heating, or by heating the polymer to a temperature below the processing temperature (here as well, where appropriate, after active cooling beforehand), if the temperature is not to drop to room temperature.

The further processing or shaping may with particular advantage be the process of coating onto a permanent or temporary backing.

In one very advantageous variant of the invention, the polymer, at or after removal from the processing reactor, is coated onto a permanent or temporary backing and, in the course of or after coating, the polymer is cooled to room temperature (or a temperature in the vicinity of room temperature), more particularly immediately after coating.

Initiation "shortly before" further processing means in particular that the oxazoline component necessary for crosslinking - or at least one of the components necessary for crosslinking in the case of an accelerated reaction (more particularly the substances containing oxazoline groups and/or the accelerator) - is added as late as possible to the hotmelt (i.e. to the melt) (homogeneous processibility on account of degree of crosslinking which is still slight here; see above) but as early as necessary for effective homogenization with the polymer composition. This is of great importance particularly with respect to the preferred poor solubility of preferred liquid oxazoline components, and/or in respect of the slow melting and low solubility of solid oxazoline components, since otherwise the resultant products would not be homogeneous or the after-crosslinking at room temperature would proceed too slowly on account of the slow diffusion of the crosslinker and of the resultant homogenization only as a consequence of said diffusion.

The crosslinker or the crosslinker-accelerator system is selected such that the crosslinking reaction proceeds at a temperature below the melting temperature of the polyacrylate composition, more particularly at room temperature. The possibility of crosslinking at room temperature offers the advantage that there is no need for additional energy to be supplied and therefore that a cost saving can be recorded.

The term "crosslinking at room temperature" in this case refers in particular to the crosslinking at typical storage temperatures of adhesive tapes, viscoelastic non-adhesive materials or the like, and should therefore not be limited to 20°C. In accordance with the invention it is of course also advantageous if the storage temperature differs from 20°C on account of climatic or other temperature fluctuations – or the room temperature differs from 20°C on account of local circumstances – and the crosslinking – in particular without further supply of energy – continues.

Substances used that contain oxazoline groups are, in particular, polyfunctional oxazolines, in other words those which contain at least two oxazoline units per molecule (i.e. are at least difunctional). They may be both aromatic and aliphatic compounds. Particular advantage is given to using difunctional compounds having two oxazoline groups and/or polyfunctional compounds, especially oligomeric or polymeric compounds, as crosslinkers, containing more than two oxazoline groups. With advantage it is possible in the case of the polyfunctional crosslinkers for all of the functional groups that are able

to react in the sense of the thermal crosslinking reaction under the conditions according to the invention to be oxazoline groups.

Outstandingly suitable polyfunctional oxazolines are ortho-, meta- or para-substituted phenylenebisoxazolines, 2,6-bis(2-oxazolin-2-yl)pyridine (and also derivatives with alkyl or aryl substituents on the oxazoline ring), 2,6-bis(8*H*-indeno[1,2-*d*]oxazolin-2-yl)pyridine, 1,2-bis(4,4-dimethyl-2-oxazolin-2-yl)ethane (and also derivatives with alkyl or aryl substituents on the oxazoline ring), 2,2-isopropylidenebis-2-oxazoline (and also derivatives with alkyl or aryl substituents on the oxazoline ring) and also block copolymers consisting of at least two units of α -methylvinyl-2-oxazoline such as, for example, EpocrosTM RPS-1005 from Nippon Shokubai.

As optionally present accelerators it is particularly preferred to use Lewis or Brønsted acids, the latter advantageously being able to be organic or mineral acids. The accelerator may either be added to the reaction mixture or attached in the polymer. This case occurs especially with acrylic acid-containing polymers, since the acrylic acid, which at the same time can also react with the oxazoline, is usually in an excess over the oxazoline and, viewed in this way, the concentration of accelerator can be considered to be constant in spite of the crosslinking reaction.

The polymer to be crosslinked in accordance with the invention preferably comprises at least one polyacrylate. This is an uncrosslinked - or, where appropriate, jointly crosslinked polymer which is obtainable by free-radical addition polymerization of acrylic monomers, a term which includes methylacrylic monomers, and of further, copolymerizable monomers if desired. Where partially crosslinked polymers are used, the melt viscosity must remain at a level which is not a hindrance to the subsequent further processing, more particularly homogeneous shaping, of the composition.

In accordance with the invention, the polyacrylate is preferably a polyacrylate crosslinkable with oxazoline groups. Correspondingly, monomers or comonomers used are preferably functional monomers crosslinkable with oxazoline groups; employed in particular here are monomers with carboxylic acid groups, thiol groups and/or phenol groups; monomers containing carboxylic acid groups are preferred. It is especially advantageous if the polyacrylate contains copolymerized acrylic acid and/or methacrylic acid.

Further advantageous monomers which can be used as comonomers for the polyacrylate are, for example, acrylic and/or methacrylic esters having up to 30 C atoms, vinyl esters of carboxylic acids containing up to 20 C atoms, vinylaromatics having up to 20 C atoms, ethylenically unsaturated nitriles, vinyl halides, vinyl ethers of alcohols containing 1 to 10 C atoms, aliphatic hydrocarbons having 2 to 8 C atoms and one or two double bonds, or mixtures of these monomers.

For the process of the invention it is preferred to use polyacrylate which can be based on the reactant mixture comprising in particular softening monomers, and also monomers with functional groups which are capable of entering into reactions with the oxazoline groups, more particularly addition reactions and/or substitution reactions, and also, optionally, further copolymerizable comonomers, especially hardening monomers. The nature of the polyacrylate to be prepared (pressure-sensitive adhesive; heat-sealing compound, viscoelastic non-adhesive material and the like) can be influenced in particular through variation of the glass transition temperature of the polymer by means of different weight fractions of the individual monomers.

For purely crystalline systems at the melting point T_m there is a thermal equilibrium between crystal and liquid. Amorphous or partially crystalline systems, in contrast, are characterized by the transformation of the more or less hard amorphous or partially crystalline phase into a softer (rubber-like to viscous) phase. At the glass transition point, particularly in the case of polymeric systems, there is a "thawing" (or "freezing" in the case of cooling) of the Brownian molecular motion of relatively long chain segments.

The transition from melting point T_m (also "melting temperature"; actually defined only for purely crystalline systems; "polymer crystals") to the glass transition point T_g (also "glass transition temperature", "glass temperature") can therefore be regarded as a fluid one, depending on the proportion of partial crystallinity in the sample under analysis.

In the context of this specification, in the sense of the remarks above, a statement of the glass transition point encompasses the melting point as well: that is, the glass transition point (or else, synonymously, the glass transition temperature) is also understood as the melting point for the corresponding "melting" systems. The statements of the glass transition temperatures are based on the determination by means of dynamic mechanical analysis (DMA) at low frequencies.

In order to obtain polymers, PSAs or heat-sealing compounds for example, having desired glass transition temperatures, the quantitative composition of the monomer mixture is advantageously selected such that the desired T_g value for the polymer is

produced in accordance with an equation (E1) in analogy to the **Fox** equation (cf. T.G. Fox, Bull. Am. Phys. Soc. 1 (1956) 123).

$$\frac{1}{T_g} = \sum_n \frac{w_n}{T_{g,n}} \quad (E1)$$

In this equation, n represents the serial number of the monomers used, w_n the mass fraction of the respective monomer n (% by weight) and $T_{g,n}$ the respective glass transition temperature of the homopolymer of the respective monomers n in K.

Particular preference is given to using a polyacrylate which can be traced back to the following monomer composition:

- a) acrylic esters and/or methacrylic esters of the following formula $\text{CH}_2 = \text{C}(\text{R}^I)(\text{COOR}^{II})$ where $\text{R}^I = \text{H}$ or CH_3 and R^{II} is an alkyl radical having 4 to 14 C atoms,
- b) olefinically unsaturated monomers with functional groups of the kind already defined for reactivity with oxazoline groups,
- c) optionally further acrylates and/or methacrylates and/or olefinically unsaturated monomers which are copolymerizable with component (a).

For the use of the polyacrylate as a PSA, the fractions of the corresponding components (a), (b) and (c) are selected such that the polymerization product has more particularly a glass transition temperature $\leq 15^\circ\text{C}$ (DMA at low frequencies).

For the preparation of PSAs it is very advantageous to select the monomers of component (a) with a fraction of 45% to 99% by weight, the monomers of component (b) with a fraction of 1% to 15% by weight and the monomers of component (c) with a fraction of 0% to 40% by weight (the figures are based on the monomer mixture for the "base polymer", i.e. without additions of any additives to the completed polymer, such as resins etc).

For the use of a hotmelt adhesive, in other words a material which becomes tacky only as a result of heating, the fractions of the corresponding components (a), (b) and (c) are selected in particular such that the copolymer has a glass transition temperature (T_g) between 15°C and 100°C , preferably between 30°C and 80°C , more preferably between

40°C and 60°C. The fractions of components (a), (b) and (c) are to be selected accordingly.

A viscoelastic material, which, for example, can typically be laminated on both sides with adhesive layers, has in particular a glass transition temperature (T_g) between -50°C to +100°C, preferably between -20°C to +60°C, more preferably 0°C to 40°C. Here again, the fractions of components (a), (b) and (c) are to be selected accordingly.

The monomers of component (a) are more particularly softening and/or apolar monomers.

For the monomers (a) it is preferred to use acrylic monomers which comprise acrylic and methacrylic esters with alkyl groups composed of 4 to 14 C atoms, preferably 4 to 9 C atoms. Examples of monomers of this kind are n-butyl acrylate, n-butyl methacrylate, n-pentyl acrylate, n-pentyl methacrylate, n-amyl acrylate, n-hexyl acrylate, hexyl methacrylate, n-heptyl acrylate, n-octyl acrylate, n-octyl methacrylate, n-nonyl acrylate, isobutyl acrylate, isooctyl acrylate, isooctyl methacrylate, and their branched isomers, such as, for example, 2-ethylhexyl acrylate, 2-ethylhexyl methacrylate.

The monomers of component (b) are, in particular, olefinically unsaturated monomers (b) with functional groups, in particular with functional groups which are able to enter into a reaction with the oxazoline groups.

For component (b) it is preferred to use monomers with functional groups selected from the following recitation: hydroxyl, carboxyl, sulphonic acid or phosphonic acid groups, phenols, thiols or amines.

Particularly preferred examples of monomers of component (b) are acrylic acid, methacrylic acid, itaconic acid, maleic acid, fumaric acid, crotonic acid, aconitic acid, dimethylacrylic acid, β -acryloyloxypropionic acid, trichloroacrylic acid, vinylacetic acid, vinylphosphonic acid, itaconic acid, diethylaminoethyl acrylate, diethylaminoethyl methacrylate, dimethylaminoethyl acrylate, dimethylaminoethyl methacrylate.

For component (c) it is possible in principle to use all vinylically functionalized compounds which are copolymerizable with component (a) and/or with component (b) and are also able to serve for setting the properties of the resultant PSA.

Exemplified monomers for component (c) are as follows:

methyl acrylate, ethyl acrylate, propyl acrylate, methyl methacrylate, ethyl methacrylate, benzyl acrylate, benzyl methacrylate, sec-butyl acrylate, tert-butyl acrylate, phenyl acrylate, phenyl methacrylate, isobornyl acrylate, isobornyl methacrylate, tert-butylphenyl acrylate, tert-butylphenyl methacrylate, dodecyl methacrylate, isodecyl acrylate, lauryl acrylate, n-undecyl acrylate, stearyl acrylate, tridecyl acrylate, behenyl acrylate, cyclohexyl methacrylate, cyclopentyl methacrylate, phenoxyethyl acrylate, phenoxyethyl methacrylate, 2-butoxyethyl methacrylate, 2-butoxyethyl acrylate, 3,3,5-trimethylcyclohexyl acrylate, 3,5-dimethyladamantyl acrylate, 4-cumylphenyl methacrylate, cyanoethyl acrylate, cyanoethyl methacrylate, 4-biphenyl acrylate, 4-biphenyl methacrylate, 2-naphthyl acrylate, 2-naphthyl methacrylate, tetrahydrofurfuryl acrylate, maleic anhydride, hydroxyethyl acrylate, hydroxypropyl acrylate, hydroxyethyl methacrylate, hydroxypropyl methacrylate, 6-hydroxyhexyl methacrylate, allyl alcohol, glycidyl acrylate, glycidyl methacrylate, 2-butoxyethyl acrylate, 2-butoxyethyl methacrylate, methyl 3-methoxyacrylate, 3-methoxybutyl acrylate, phenoxyethyl acrylate, phenoxyethyl methacrylate, 2-phenoxyethyl methacrylate, butyldiglycol methacrylate, ethylene glycol acrylate, ethylene glycol monomethylacrylate, methoxy-polyethylene glycol methacrylate 350, methoxy-polyethylene glycol methacrylate 500, propylene glycol monomethacrylate, butoxydiethylene glycol methacrylate, ethoxytriethylene glycol methacrylate, octafluoropentyl acrylate, octafluoropentyl methacrylate, 2,2,2-trifluoroethyl methacrylate, 1,1,1,3,3,3-hexafluoroisopropyl acrylate, 1,1,1,3,3,3-hexafluoroisopropyl methacrylate, 2,2,3,3,3-pentafluoropropyl methacrylate, 2,2,3,4,4,4-hexafluorobutyl methacrylate, 2,2,3,3,4,4,4-heptafluorobutyl acrylate, 2,2,3,3,4,4,4-heptafluorobutyl methacrylate, 2,2,3,3,4,4,5,5,6,6,7,7,8,8,8-pentadecafluorooctyl methacrylate, dimethylaminopropylacrylamide, dimethylaminopropylmethacrylamide, *N*-(1-methylundecyl)acrylamide, *N*-(n-butoxymethyl)acrylamide, *N*-(butoxymethyl)methacrylamide, *N*-(ethoxymethyl)acrylamide, *N*-(n-octadecyl)acrylamide, and also *N,N*-dialkyl-substituted amides, such as, for example, *N,N*-dimethylacrylamide, *N,N*-dimethylmethacrylamide, *N*-benzylacrylamides, *N*-isopropylacrylamide, *N*-tert-butylacrylamide, *N*-tert-octylacrylamide, *N*-methylolacrylamide, *N*-methylolmethacrylamide, acrylonitrile, methacrylonitrile, vinyl ethers, such as vinyl methyl ether, ethyl vinyl ether, vinyl isobutyl ether, vinyl esters, such as vinyl acetate, vinyl chloride, vinyl halides, vinylidene chloride, vinylidene halide, vinylpyridine, 4-vinylpyridine, *N*-vinylphthalimide, *N*-vinyl lactam, *N*-vinylpyrrolidone, styrene, α - and p-methylstyrene, α -butylstyrene, 4-n-butylstyrene, 4-n-decylstyrene, 3,4-dimethoxystyrene, macromonomers such as

2-polystyrene-ethyl methacrylate (molecular weight M_w of 4000 to 13 000 g/mol), poly(methyl methacrylate)ethyl methacrylate (M_w of 2000 to 8000 g/mol).

Monomers of component (c) can advantageously also be selected such that they contain functional groups which assist subsequent radiation-chemical crosslinking (by means of electron beams, UV, for example). Examples of suitable copolymerizable photoinitiators include benzoin acrylate monomers and acrylate-functionalized benzophenone derivative monomers which assist crosslinking by electron beams, examples being tetrahydrofurfuryl acrylate, *N-tert*-butylacrylamide, and allyl acrylate, this recitation not being conclusive.

Preparation of the polymers

The polyacrylates can be prepared by the methods familiar to a person skilled in the art, with particular advantage by conventional free-radical polymerizations or controlled free-radical addition polymerizations. The polyacrylates can be prepared by copolymerizing the monomeric components using the typical addition-polymerization initiators and also, where appropriate, regulators, with polymerization taking place at the usual temperatures in bulk, in emulsion, for example in water or liquid hydrocarbons, or in solution.

The polyacrylates are preferably prepared by addition polymerization of the monomers in solvents, more particularly in solvents with a boiling range from 50 to 150°C, preferably from 60 to 120°C, using the customary amounts of addition-polymerization initiators, generally 0.01% to 5%, more particularly 0.1% to 2% by weight (based on the total weight of the monomers).

Suitable in principle are all of the customary initiators for acrylates that are familiar to a person skilled in the art. Examples of free-radical sources are peroxides, hydroperoxides and azo compounds, examples being dibenzoyl peroxide, cumene hydroperoxide, cyclohexanone peroxide, di-*tert*-butyl peroxide, cyclohexylsulphonyl acetyl peroxide, diisopropyl percarbonate, *tert*-butyl peroctoate, benzpinacol. In one very preferred procedure the free-radical initiator used is 2,2'-azobis(2-methylbutyronitrile) (Vazo® 67™ from DUPONT) or 2,2'-azobis(2-methylpropionitrile) (2,2'-azobisisobutyronitrile; AIBN; Vazo® 64™ from DUPONT).

Suitable solvents include alcohols, such as methanol, ethanol, *n*- and *iso*-propanol, *n*- and *iso*-butanol, preferably isopropanol and/or isobutanol; and also hydrocarbons such as

toluene and, in particular benzines with a boiling range from 60 to 120°C. In particular it is possible to use ketones, such as acetone, methyl ethyl ketone, methyl isobutyl ketone, and esters, such as ethyl acetate, and also mixtures of solvents of the stated kind, preference being given to mixtures comprising isopropanol, more particularly in amounts from 2% to 15% by weight, preferably 3% to 10% by weight, based on the solvent mixture employed.

The weight-average molecular weights M_w of the polyacrylates are situated preferably in a range from 20 000 to 2 000 000 g/mol; very preferably in a range from 100 000 to 1 000 000 g/mol, most preferably in a range from 150 000 to 500 000 g/mol [the figures for average molecular weight M_w and the polydispersity PD in this specification relate to the determination by gel permeation chromatography (see measurement method A3; experimental section)]. For this purpose it may be advantageous to carry out the addition polymerization in the presence of suitable addition-polymerization regulators such as thiols, halogen compounds and/or alcohols, in order to set the desired average molecular weight.

The polyacrylate preferably has a K value of 30 to 90, more preferably of 40 to 70, as measured in toluene (1% strength solution, 21°C). The K value of Fikentscher is a measure of the molecular weight and viscosity of the uncrosslinked polymer.

Particularly suitable for the process of the invention are polyacrylates which have a narrow molecular weight distribution (polydispersity $PD < 4$). In spite of a relatively low molecular weight, these compositions after crosslinking have a particularly good shear strength. Moreover, the lower molecular weight allows easier processing from the melt, since the flow viscosity is lower than that of a polyacrylate with a broader distribution, with substantially identical service properties. Polyacrylates with a narrow distribution can be prepared advantageously by anionic addition polymerization or by controlled free-radical addition polymerization methods, the latter being particularly suitable. Examples of polyacrylates of this kind which are prepared by the RAFT process are described in US 6,765,078 B2 and US 6,720,399 B2. Via *N*-oxyls as well it is possible to prepare such polyacrylates, as described for example in EP 1 311 555 B1. Atom transfer radical polymerization (ATRP) as well can be used advantageously for the synthesis of polyacrylates with a narrow distribution, the initiator used being preferably monofunctional or difunctional secondary or tertiary halides and, to abstract the halide(s), complexes of Cu, Ni, Fe, Pd, Pt, Ru, Os, Rh, Co, Ir, Ag or Au (cf., for example, EP 0 824 111 A1;

EP 826 698 A1; EP 824 110 A1; EP 841 346 A1; EP 850 957 A1). The various possibilities of ATRP are further described in specifications US 5,945,491 A, US 5,854,364 A and US 5,789,487 A.

The polyacrylates obtainable by the process of the invention can be admixed, prior to thermal crosslinking, with at least one tackifying resin. Tackifying resins for addition are the tackifier resins that are already known and are described in the literature. Reference may be made in particular to all aliphatic, aromatic, alkylaromatic hydrocarbon resins, hydrocarbon resins based on pure monomers, hydrogenated hydrocarbon resins, functional hydrocarbon resins and natural resins. With preference it is possible to use pinene resins, indene resins and rosins, their disproportionated, hydrogenated, polymerized and esterified derivatives and salts, terpene resins and terpene-phenolic resins, and also C5, C9 and other hydrocarbon resins. Combinations of these and further resins may also be used with advantage in order to set the properties of the resultant adhesive in accordance with what is desired. With particular preference it is possible to employ all resins that are compatible (soluble) with the polyacrylate in question. One particularly preferred procedure adds terpene-phenolic resins and/or rosin esters.

Optionally it is also possible for powderous and granular fillers, dyes and pigments, including in particular those which are abrasive and reinforcing, such as, for example, chalks (CaCO_3), titanium dioxides, zinc oxides and carbon blacks, even in high fractions, in other words from 1% to 50% by weight, based on the overall formula, to be metered outstandingly into the polyacrylate melt, incorporated homogeneously and coated on a 2-roll applicator. The conventional methods often fail here, owing to the then very high viscosity of the compounded formulation as a whole.

With great preference it is possible to use different forms of chalk as filler, particular preference being given to the use of Mikrosöhl chalk. With preferred fractions of up to 30% by weight, there is virtually no change in the adhesive properties (shear strength at RT, instantaneous bond strength to steel and PE) as the result of the addition of filler.

It is possible, furthermore, for low-flammability fillers, such as ammonium polyphosphate, for example, and also electrically conductive fillers (such as, for example, conductive carbon black, carbon fibres and/or silver-coated beads), and also thermally conductive materials (such as, for example, boron nitride, aluminium oxide, sodium carbide), and

also ferromagnetic additives (such as, for example, iron(III) oxides), and also additives for increasing volume, especially for producing foamed layers (such as, for example, expandants, solid glass beads, hollow glass beads, microbeads of other materials, expandable microballoons, silica, silicates, organic renewable raw materials, examples being wood flour, organic and/or inorganic nanoparticles, fibres), and also organic and/or inorganic colorants (in the form of pastes, compounded formulations or pigments), ageing inhibitors, light stabilizers, ozone protectants, compounding agents and/or expandants, to be added or compounded in before or after the concentration of the polyacrylate. Ageing inhibitors which can be used are preferably not only primary inhibitors, such as 4-methoxyphenol, but also secondary ageing inhibitors, such as Irgafos[®] TNPP from CIBA GEIGY, both alone and in combination with one another. At this point only the intention here is to refer to further corresponding Irganox[®] products from CIBA GEIGY and Hostano[®] from CLARIANT. Further outstanding agents against ageing that can be used include phenothiazine (C-radical scavenger) and also hydroquinone methyl ether in the presence of oxygen, and also oxygen itself.

Optionally the customary plasticizers (plasticizing agents) can be added, more particularly at concentrations of up to 5% by weight. Plasticizers which can be metered in include, for example, low molecular mass polyacrylates, phthalates, water-soluble plasticizers, plasticizer resins, phosphates, polyphosphates and/or citrates.

In addition, optionally, it is possible for the thermally crosslinkable acrylate hotmelt to be mixed or blended with other polymers. Suitable for this purpose are polymers based on natural rubber, synthetic rubber, EVA, silicone rubber, acrylic rubber, polyvinyl ether. In this context it proves to be advantageous to add these polymers in granulated or otherwise-comminuted form to the acrylate hotmelt prior to the addition of the thermal crosslinker. The polymer blend is produced in an extruder, preferably in a multi-screw extruder or in a planetary roller mixer. To stabilize the thermally crosslinked acrylate hotmelt, and also, in particular, polymer blends of thermally crosslinked acrylate hotmelts and other polymers, it may be useful to irradiate the shaped material with low doses of electron beams. Optionally for this purpose it is possible to admix the polyacrylate with crosslinking promoters such as di-, tri- or polyfunctional acrylate, polyester and/or urethane acrylate.

Further procedure

The uncrosslinked polymer, in particular polyacrylate, can be concentrated in the absence of the crosslinker and accelerator substances. Alternatively it is possible to add one of these classes of compound to the polymer even before concentration, so that the concentration then takes place in the presence of this or these substances.

The polymers are then transferred to a compounder. In particular embodiments of the process of the invention, concentration and compounding may take place in the same reactor.

As a compounder it is possible more particularly to use an extruder. Within the compounder the polymers are present in the melt: either by having been introduced already in the melt state, or by being heated in the compounder until the melt is obtained. In the compounder the polymers are maintained in the melt by heating.

Where neither crosslinkers (oxazolines) nor, if necessary, accelerators are present in the polymer, the possible temperature in the melt is limited by the decomposition temperature of the polymer. The operating temperature in the compounder is typically between 80 to 150°C, more particularly between 100 and 120°C.

The substances containing oxazoline groups are added to the polymer preferably before or with the addition of accelerator, if necessary.

The substances containing oxazoline groups can be added to the monomers even before the polymerization phase or during that phase, provided they are sufficiently stable for it. Advantageously, however, the substances containing oxazoline groups are added to the polymer either prior to addition to the compounder or in the course of addition to the compounder, in other words are introduced into the compounder together with the uncrosslinked polymers.

The time window of the addition prior to coating is guided in particular by the available pot life, in other words the processing life in the melt, without disadvantageous alteration to the properties of the resultant product. With the process of the invention it has been possible to obtain pot lives of several minutes up to several tens of minutes (depending on the choice of experimental parameters), and so the accelerator ought to be added within this timespan prior to coating. Advantageously the accelerator is added to the

hotmelt as late as possible but as early as necessary for there to be effective homogenization with the polymer composition.

Timespans which have emerged as being very advantageous here are those from 2 to 10 minutes, more particularly those of more than 5 minutes, at an operating temperature of 110 to 120°C.

If an accelerator is added, it can be advantageous to add the accelerator substances to the polymers shortly before the further processing of the polymers, in particular a coating or other shaping. The crosslinker (i.e. the oxazoline compound) and the accelerator can also both be added shortly before the further processing of the polymer, in other words advantageously in the phase as set out above for the accelerators. For this purpose it is advantageous to introduce the crosslinker-accelerator system into the operation at one and the same point, including in the form of an oxazoline-accelerator mixture.

In principle it is also possible to switch the times and locations of addition of crosslinker and accelerator in the embodiments set out above, and so the accelerator can be added before the substances containing oxazoline groups.

In the compounding operation the temperature of the polymer on addition of the crosslinkers and/or of the accelerators is between 50 and 150°C, preferably between 70 and 130°C, more preferably between 80 and 120°C.

It has in principle emerged as being very advantageous if the crosslinker, in other words the substance containing oxazoline groups, is added at 0.1-5% by weight, based on the polymer without additives.

It is advantageous to add the accelerator at 0.05-5% by weight, based on the additive-free polymer.

It is particularly advantageous if the crosslinker fraction is selected such as to result in an elastic fraction of at least 20% in the crosslinked polyacrylates. Preferably the elastic fraction is at least 40%, more preferably at least 60% (measured in each case according to measurement method H3; cf. Experimental Section).

In principle the number of functional groups, in other words in particular of the carboxylic acid groups, can be selected such that they are in excess in relation to the oxazoline

groups, and such, therefore, that in the polymer there are only a sufficient number of functional groups – that is, potential crosslinking sites or linking sites in the polymer – in order to obtain the desired crosslinking.

For the action of the crosslinker system of the invention, particularly in the context of the process of the invention, including its variant embodiments, it is particularly advantageous to harmonize the amounts of crosslinker and, if present, accelerator with the amount of functional groups in the polyacrylate that are reactive for the crosslinking reaction, and, where appropriate, with one another, and to optimize these amounts for the desired crosslinking outcome.

To specify the ratios of the constituents of the crosslinker system to one another it is possible more particularly to employ the ratio of the number of oxazoline groups in the crosslinker to the number of reactive functional groups in the polymer. In principle this ratio is freely selectable, and so there is alternatively an excess of functional groups, numerical equivalence of the groups, or an excess of oxazoline groups.

Advantageously this ratio is selected such that the oxazoline groups are in deficit (up to a maximum of numerical equivalence); with very particular preference, the ratio of the total number of oxazoline groups in the crosslinker to the number of functional groups in the polymer is in the range from 0.1 : 1 to 1 : 1.

A further parameter is the ratio of the number of acceleration-active groups in the accelerator to the number of oxazoline groups in the crosslinker, when an accelerator is needed. Acceleration-active groups are regarded in particular as the carboxylic acid functionalities or other acid functionalities in the polymer which react simultaneously with the oxazolines and enter into crosslinking, and also the functionality (corresponding to the number of protons) of separately added organic or inorganic Brønsted acids. Lewis acids, on the other hand, are regarded as monofunctional accelerators. This ratio as well is freely selectable, and so there is alternatively an excess of acceleration-active groups, numerical equivalence of the groups, or an excess of the oxazoline groups.

It is particularly advantageous if the number of acceleration-active groups in the accelerator to the number of oxazoline groups in the crosslinker is from 0.2 : 1 to 4 : 1.

After the composition has been compounded, the polymer is subjected to further processing, more particularly to coating onto a permanent or temporary backing (the permanent backing remains joined to the layer of adhesive in application, whereas the

temporary backing is removed again in the further processing operation, for example in the converting of the adhesive tape, or is removed again from the layer of adhesive at application).

The self-adhesive compositions can be coated using hotmelt coating nozzles that are known to the person skilled in the art, or, preferably, using roll applicators, including coating calenders. The coating calenders may be composed advantageously of two, three, four or more rolls.

Preferably at least one of the rolls is provided with an anti-adhesive roll surface, this applying preferably to all of the rolls that come into contact with the polyacrylate. In an advantageous procedure it is possible for all of the rolls of the calender to have an anti-adhesive finish.

An anti-adhesive roll surface used is with particular preference a steel-ceramic-silicone composite. Roll surfaces of this kind are resistant to thermal and mechanical loads.

Surprisingly for the person skilled in the art it has been found particularly advantageous to use roll surfaces which have a surface structure, more particularly of a kind such that the surface does not produce full contact with the polymer layer to be processed, but instead that the area of contact is lower as compared with a smooth roll. Particularly advantageous are structured rolls such as engraved metal rolls (engraved steel rolls, for example).

Coating may take place with particular advantage in accordance with the coating techniques as set out in WO 2006/027387 A1 from page 12 line 5 to page 20 line 13, and more particularly as in the sections "Variant A" (page 12), "Variant B" (page 13), "Variant C" (page 15), "Method D" (page 17), "Variant E" (page 19), and also Figures Fig. 1 to 6. The stated disclosure passages from WO 2006/027387 A1 are therefore explicitly included in the disclosure content of the present specification.

Particularly good results are achieved with the two- and three-roll calender stacks (cf. in particular variants B – Fig. 3, variant C – Fig. 4 and variant D – Fig. 4 of WO 2006/027387 A1) through the use of calender rolls which are equipped with anti-adhesive surfaces, or with surface-modified rolls – particularly noteworthy here are engraved metal rolls. These engraved metal rolls, preferably engraved steel rolls, have a regularly geometrically interrupted surface structure. This applies with particular advantage to the transfer roll ÜW. These surfaces contribute in a particularly

advantageous way to the success of the coating process, since anti-adhesive and structured surfaces allow the polyacrylate composition to be transferred even to anti-adhesively treated backing surfaces. Various kinds of anti-adhesive surface coatings can be used for the calender rolls. Among those that have proved to be particularly suitable here are, for example, the aforementioned metal-ceramic-silicone composites Pallas SK-B-012/5 from Pallas Oberflächentechnik GmbH, Germany, and also AST 9984-B from Advanced Surface Technologies, Germany.

The transfer rolls (ÜW) in particular may be designed as engraved steel rolls (cf. variants B – Fig. 3, variant C – Fig. 4 and variant D – Fig. 4 of WO 2006/027387 A1). Used with particular preference as transfer roll ÜW are, for example, engraved steel rolls with the designation 140 L/cm and a flight width of 10 µm, examples being those from Saueressig, Germany.

In the course of coating, particularly when using the multi-roll calenders, it is possible to realize coating speeds of up to 300 m/min.

Shown by way of example in Figs. 1 and 2 of the present specification, without any intention that this should impose any restriction, is the compounding and coating operation, on the basis of a continuous process. The polymers are introduced at the first feed point (1.1) into the compounder (1.3), here for example an extruder. Either the introduction takes place already in the melt, or the polymers are heated in the compounder until the melt state is reached. At the first feed point, together with the polymer, the oxazoline-containing compounds are advantageously introduced into the compounder.

Shortly before coating takes place, the accelerators are added, if necessary, at a second feed point (1.2). The outcome of this is that the accelerators are added to the oxazoline-containing polymers not until shortly before coating, and the reaction time in the melt is low.

Coating may take place advantageously, as shown in Figs. 1 and 2, between a coating roll (BW) and a doctor roll (RW) (the doctor roll may be fixed or rotatable, in particular set up to run counter to the coating roll).

The two rolls (BW) and (RW) are arranged in such a way as to form a nip into which the self-adhesive composition (3) is introduced by means, for example, of a distributor die (1). The die is fed in particular by the compounder (cf. Fig. 1; item number 1.3).

The first roll (BW) [coating roll] carries the temporary backing (2) onto which the self-adhesive composition (3) is to be coated. The second roll (RW) [doctor roll] carries an anti-adhesively treated auxiliary backing (5) and presses by means of the auxiliary backing onto the adhesive, thereby depositing the adhesive onto the temporary backing (2) in the form of layer (4). At position (6) the anti-adhesively treated auxiliary backing (5) is taken off again from the layer (4) of self-adhesive composition. The adhesive tape (6), consisting of the layer (4) of adhesive on the temporary backing (2), is guided out of the coating installation.

The reaction regime may also be discontinuous. In corresponding compounders such as reactor tanks, for example, the addition of the polymers, the crosslinkers and the accelerators may take place at different times and not, as shown in Figure 1, at different locations.

Immediately after coating – preferably by means of roller application or by means of an extrusion die – the polymer is only slightly crosslinked, but not yet sufficiently crosslinked. The crosslinking reaction proceeds advantageously on the backing. In the context of this document, such polymers are also included in the term "uncrosslinked polymers".

After the coating operation, the polymer composition cools down relatively rapidly, in fact to the storage temperature, more generally to room temperature. The crosslinker system of the invention is suitable for allowing the crosslinking reaction to continue without the supply of further thermal energy (without heat supply).

The crosslinking reaction between the functional groups of the polyacrylate and the oxazolines by means of the crosslinker system of the invention proceeds even without heat supply under standard conditions (room temperature) completely. Generally speaking, after a storage time of 5 to 14 days, crosslinking is concluded to a sufficient extent for there to be a functional product present (more particularly an adhesive tape or a functional backing layer on the basis of the polyacrylate). The ultimate state and thus the final cohesion of the polymer are attained, depending on the choice of polymer and of crosslinker system, after a storage time of in particular 14 to 100 days, advantageously after 14 to 50 days' storage time at room temperature, and – as expected – earlier at a higher storage temperature.

Crosslinking raises the cohesion of the polymer and hence also the shear strength. The links are very stable. This allows very ageing-stable and heat-resistant products such as adhesive tapes, viscoelastic backing materials or shaped articles.

The physical properties of the end product, especially its viscosity, bond strength and tack, can be influenced through the degree of crosslinking, and so the end product can be optimized through an appropriate choice of the reaction conditions. A variety of factors determine the operational window of this process. The most important influencing variables are the amounts (concentrations and proportions relative to one another) and the chemical natures of the crosslinkers and, if necessary, of the accelerators, the operating temperature and coating temperature, the residence time in compounders (especially extruders) and in the coating assembly, the fraction of functional groups (especially acid groups) in the uncrosslinked polymer, and the average molecular weight of the polyacrylate.

Described below are a number of associations related to the preparation of the inventively crosslinked self-adhesive composition, which more closely characterize the preparation process but are not intended to be restrictive for the concept of the invention.

The process of the invention offers the advantage, in an outstanding and unexpected way, that a stable crosslinking process for polyacrylates can be offered, and one with outstanding control facility in relation to the crosslinking pattern, by virtue of substantial decoupling of degree of crosslinking and reactivity or total reaction kinetics (macrokinetics). The amount of crosslinker added (amount of oxazoline) largely influences the degree of crosslinking of the product, the amount of acid functionalities, in particular of the carboxylic acid functionalities in the polymer that are also capable of crosslinking reaction; and also, if necessary, the additionally added accelerator (Lewis or Brønsted acids) largely controls the reactivity. The solubility of the oxazolines in the polymer melt, and the melting and subsequent dissolution process in the case of solid oxazoline crosslinkers, on the other hand, influences the homogenization and distribution of the crosslinker component in the melt, whereby the overall reaction kinetics (macrokinetics - the interaction of the kinetics of the chemical reactions with the kinetics of the transport processes to the phase boundary and in the phases themselves) is controlled.

It has been observed, surprisingly, that, through the amount of oxazoline-containing substances added, it was possible to preselect the degree of crosslinking, and to do so largely independently of the otherwise selected process parameters of temperature and amount of optionally added accelerator.

Additionally it has been observed that the amount of accelerator added had a direct influence on the crosslinking rate, including thus the time at which the ultimate degree of crosslinking was achieved, but without influencing this absolutely. The reactivity of the crosslinking reaction can be selected such that the crosslinking, during the storage of the completed product as well, under the conditions customary therein (room temperature), leads within a few weeks to the desired degree of crosslinking, in particular without it being necessary additionally to supply thermal energy (actively) or for the product to be treated further.

In addition to the aforementioned parameters, the reactivity of the crosslinking reaction can also be influenced by varying the temperature, if desired, especially in those cases where the advantage of "inherent crosslinking" in the course of storage under standard conditions has no part to play. At constant crosslinker concentration, an increase in the operating temperature leads to a reduced viscosity, which enhances the coatability of the composition but reduces the processing life.

An increase in the processing life is acquired by a reduction in the accelerator concentration or by the removal of an accelerator, reduction in molecular weight, reduction in the concentration of functional groups in the uncrosslinked polymer, reduction of the acid fraction in the uncrosslinked polymer, use of less-reactive crosslinkers (oxazolines) or of less-reactive crosslinker-accelerator systems, and reduction in operating temperature.

An improvement in the cohesion of the composition can be obtained by a variety of pathways. In one, the accelerator concentration is increased, which reduces the processing life. At constant accelerator concentration, it is also possible to raise the molecular weight of the polymer, which is possibly more efficient. In the sense of the invention it is advantageous in any case to raise the concentration of crosslinker (substances containing oxazoline groups). Depending on the desired requirements profile of the composition or of the product it is necessary to adapt the abovementioned parameters in a suitable way.

The invention further provides for the use of at least difunctional compounds, with at least one of the functional groups being an oxazoline group, as thermal crosslinkers for polymers which are processed from the melt; particularly in the context of the above observations for the process of the invention.

Provided by the invention, finally, are homogeneously crosslinked, especially emulsifier-free, polymers obtainable by the process of the invention.

Advantageous applications

The polymers which can be inventively prepared can be used for a broad range of applications. Below, a number of particularly advantageous fields of use are set out by way of example.

The polymer, in particular polyacrylate, prepared by the process of the invention can be used most particularly as a pressure-sensitive adhesive (PSA), preferably as a PSA for an adhesive tape, where the PSA is in the form of a single-sided or double-sided film on a backing sheet. These polymers are especially suitable when a high adhesive coat weight is required, since with this coating technique it is possible to achieve an almost arbitrarily high coat weight, preferably more than 100 g/m², more preferably more than 200 g/m², and to do so in particular at the same time as particularly homogeneous crosslinking through the coat. Examples of favourable applications, without claim to completeness, are technical adhesive tapes, more especially for use in construction, examples being insulating tapes, corrosion control tapes, adhesive aluminium tapes, fabric-reinforced film-backed adhesive tapes (duct tapes), special-purpose adhesive construction tapes, such as vapour barriers, adhesive assembly tapes, cable wrapping tapes, self-adhesive sheets and/or paper labels.

The inventively prepared polymer, in particular polyacrylate, may also very well be made available as a PSA for an unbacked adhesive tape, i.e. in the form of what is called adhesive transfer tape. Here as well, the possibility of setting the coat weight almost arbitrarily high in conjunction with particularly homogeneous crosslinking through the coat is a particular advantage. Preferred weights per unit area are more than 10 g/m² to

5000 g/m², it being possible to obtain layer thicknesses of more than 200 g/m², more than 300 g/m² or higher; more preferably between 100 g/m² and 3000 g/m².

The inventively prepared polymer, in particular polyacrylate, may also be present in the form of a heat-sealing adhesive in adhesive transfer tapes or single-sided or double-sided adhesive tapes. Here as well, for backed pressure-sensitive adhesive tapes, the backing may be an inventively obtained viscoelastic polyacrylate.

One advantageous embodiment of the adhesive tapes obtained accordingly can be used in an advantageous way as a strippable adhesive tape, more particularly a tape which can be detached again without residue by pulling substantially in the plane of the bond.

The process of the invention is also particularly suitable for producing three-dimensional shaped articles, whether they be tacky or not. A particular advantage of this process is that there is no restriction on the layer thickness of the polymer, in particular polyacrylate, to be crosslinked and shaped, in contrast to UV and EBC curing processes. In accordance with the choice of coating assemblies or shaping assemblies, therefore, it is possible to produce structures of any desired shape, which are then able to continue crosslinking to desired strength under mild conditions.

This process is also particularly suitable for the production of particularly thick layers, especially of pressure-sensitive adhesive layers or viscoelastic polymer layers, in particular polyacrylate layers, with a thickness of more than 80 µm. Layers of this kind are difficult to produce with the solvent technology (bubble formation, very slow coating speed, lamination of thin layers one over another is complicated and harbours weak points).

Thick pressure-sensitive adhesive layers may be present, for example, in unfilled form, as straight systems (such as straight acrylates), or in resin-blended form or in a form filled with organic or inorganic fillers. Also possible are layers foamed to a closed-cell or open-cell form in accordance with the known techniques. One possible method of foaming is that of foaming via compressed gases such as nitrogen or CO₂, or else foaming via expandants such as hydrazines or expandable microballoons. Where expandable microballoons are used, the composition or the shaped layer is advantageously activated suitably by means of heat introduction. Foaming may take place in the extruder or after coating. It may be judicious to smooth the foamed layer by means of suitable rollers or

release films. To produce foam-analogous layers it is also possible to add hollow glass beads or pre-expanded polymeric microballoons to the tacky, thermally crosslinked, pressure-sensitive acrylate hotmelt adhesive.

In particular it is possible, using this process, to produce thick layers as well, which can be used as a backing layer for double-sidedly PSA-coated adhesive tapes, with particular preference filled and foamed layers which can be utilized as backing layers for foamlike adhesive tapes. With these layers as well it is sensible to add hollow glass beads, solid glass beads or expanding microballoons to the polymer, in particular polyacrylate, prior to the addition of the crosslinker, of the accelerator or of the crosslinker-accelerator system. Where expanding microballoons are used, the composition or the shaped layer is suitably activated by means of heat introduction. Foaming can take place in the extruder or after the coating operation. It can be judicious to smooth the foamed layer by suitable rolls or release films, or by the lamination of a PSA coated onto a release material. It is possible to laminate a pressure-sensitive adhesive layer onto at least one side of a foamlike viscoelastic layer of this kind. It is preferred to laminate a corona-pretreated polyacrylate layer on both sides. Alternatively it is possible to use differently pretreated adhesive layers, i.e. pressure-sensitive adhesive layers and/or heat-activable layers based on polymers other than on acrylates, onto the viscoelastic layer. Suitable base polymers are adhesives based on natural rubber, synthetic rubbers, acrylate block copolymers, styrene block copolymers, EVA, certain polyolefins, specific polyurethanes, polyvinyl ethers, and silicones. Preferred compositions, however, are those which have no significant fraction of migratable constituents whose compatibility with the polyacrylate is so good that they diffuse in significant quantities into the acrylate layer and alter the properties therein.

Instead of laminating a pressure-sensitive adhesive layer onto both sides, it is also possible on at least one side to use a hotmelt-adhesive layer or thermally activable adhesive layer. Asymmetric adhesive tapes of this kind allow the bonding of critical substrates with a high bonding strength. An adhesive tape of this kind can be used, for example, to affix EPDM rubber profiles to vehicles.

One particular advantage of the thermally crosslinked polymers, in particular polyacrylates, is that these layers, whether utilized as a viscoelastic backing, as a pressure-sensitive adhesive or as a heat-sealing composition, combine an equal surface quality with no crosslinking profile through the layer (or, correspondingly, the shaped

articles produced from polymers) in particular in contrast to UV-crosslinked and EBC-crosslinked layers. As a result it is possible for the balance between adhesive and cohesive properties to be controlled and set ideally for the layer as a whole through the crosslinking. In the case of radiation-chemically crosslinked layers, in contrast, there is always one side or one sublayer which is over- or undercrosslinked.

Experimental Section

The following exemplary experiments are intended to illustrate the invention, but the choice of examples indicated is not intended to subject the invention to any unnecessary restriction.

Measurement methods (general):

Solids content (measurement method A1):

The solids content is a measure of the fraction of non-evaporable constituents in a polymer solution. It is determined gravimetrically, by weighing the solution, then evaporating the evaporable fractions in a drying oven at 120°C for 2 hours and reweighing the residue.

K value (according to Fikentscher) (measurement method A2):

The K value is a measure of the average molecular size of high-polymer materials. It is measured by preparing one per cent strength (1 g/100 ml) toluenic polymer solutions and determining their kinematic viscosities using a Vogel-Ossag viscometer. Standardization to the viscosity of the toluene gives the relative viscosity, from which the K value can be calculated by the method of Fikentscher (Polymer 8/1967, 381 ff.)

Gel permeation chromatography GPC (measurement method A3):

The figures for the weight-average molecular weight M_w and the polydispersity PD in this specification relate to the determination by gel permeation chromatography. Determination is made on a 100 μ l sample subjected to clarifying filtration (sample concentration 4 g/l). The eluent used is tetrahydrofuran with 0.1% by volume of trifluoroacetic acid. Measurement takes place at 25°C. The preliminary column used is a column type PSS-SDV, 5 μ , 10^3 Å, ID 8.0 mm 50 mm. Separation is carried out using the columns of type PSS-SDV, 5 μ , 10^3 Å and also 10^5 Å and 10^6 Å each with ID 8.0 mm x 300 mm (columns from Polymer Standards Service; detection by means of Shodex RI71 differential refractometer). The flow rate is 1.0 ml per minute. Calibration takes place against PMMA standards (polymethyl methacrylate calibration).

Measurement methods (PSAs in particular):180° bond strength test (measurement method H1):

A strip 20 mm wide of an acrylate PSA applied to polyester as a layer was applied to steel plates which beforehand had been washed twice with acetone and once with isopropanol. The pressure-sensitive adhesive strip was pressed onto the substrate twice with an applied pressure corresponding to a weight of 2 kg. The adhesive tape was then removed from the substrate immediately with a speed of 300 mm/min and at an angle of 180°. All measurements were conducted at room temperature.

The results are reported in N/cm and have been averaged from three measurements. The bond strength to polyethylene (PE) was determined analogously.

Holding power (measurement method H2):

A strip of the adhesive tape 13 mm wide and more than 20 mm long (30 mm, for example) was applied to a smooth steel surface which had been cleaned three times with acetone and once with isopropanol. The bond area was 20 mm · 13 mm (length · width), the adhesive tape protruding beyond the test plate at the edge (by 10 mm, for example, corresponding to aforementioned length of 30 mm). Subsequently the adhesive tape was pressed onto the steel support four times, with an applied pressure corresponding to a weight of 2 kg. This sample was suspended vertically, with the protruding end of the adhesive tape pointing downwards.

At room temperature, a weight of 1 kg was affixed to the protruding end of the adhesive tape. Measurement is conducted under standard conditions (23°C, 55% humidity) and at 70°C in a thermal cabinet.

The holding power times measured (times taken for the adhesive tape to detach completely from the substrate; measurement terminated at 10 000 min) are reported in minutes and correspond to the average value from three measurements.

Microshear test (measurement method H3):

This test serves for the accelerated testing of the shear strength of adhesive tapes under temperature load.

Sample preparation for microshear test:

An adhesive tape (length about 50 mm, width 10 mm) cut from the respective sample specimen is adhered to a steel test plate, which has been cleaned with acetone, in such a way that the steel plate protrudes beyond the adhesive tape to the right and the left, and

that the adhesive tape protrudes beyond the test plate by 2 mm at the top edge. The bond area of the sample in terms of height · width = 13 mm · 10 mm. The bond site is subsequently rolled over six times with a 2 kg steel roller at a speed of 10 m/min. The adhesive tape is reinforced flush with a stable adhesive strip which serves as a support for the travel sensor. The sample is suspended vertically by means of the test plate.

Microshear test:

The sample specimen for measurement is loaded at the bottom end with a weight of 100 g. The test temperature is 40°C, the test duration 30 minutes (15 minutes' loading and 15 minutes' unloading). The shear travel after the predetermined test duration at constant temperature is report as the result in μm , as both the maximum value ["max"; maximum shear travel as a result of 15-minute loading]; and the minimum value ["min"; shear travel ("residual deflection") 15 minutes after unloading; on unloading there is a backward movement as a result of relaxation]. Likewise reported is the elastic component in per cent ["elast"; elastic fraction = $(\text{max} - \text{min}) \cdot 100 / \text{max}$].

Measurement methods (three-layer constructions in particular):

90° bond strength to steel – open and lined side (measurement method V1):

The bond strength to steel is determined under test conditions of 23°C +/- 1°C temperature and 50% +/- 5% relative humidity. The specimens were cut to a width of 20 mm and adhered to a steel plate. Prior to the measurement the steel plate is cleaned and conditioned. For this purpose the plate is first wiped down with acetone and then left to stand in the air for 5 minutes to allow the solvent to evaporate. The side of the three-layer assembly facing away from the test substrate was then lined with a 50 μm aluminium foil, thereby preventing the sample from expanding in the course of the measurement. This was followed by the rolling of the test specimen onto the steel substrate. For this purpose the tape was rolled over five times back and forth, with a rolling speed of 10 m/min, using a 2 kg roller. Immediately after the rolling-on operation, the steel plate was inserted into a special mount which allows the specimen to be removed at an angle of 90° vertically upwards. The measurement of bond strength was made using a Zwick tensile testing machine. When the lined side is applied to the steel plate, the open side of the three-layer assembly is first laminated to the 50 μm aluminium foil, the release material is removed, and the system is adhered to the steel plate, and subjected to analogous rolling-on and measurement.

The results measured on both sides, open and lined, are reported in N/cm and are averaged from three measurements.

Holding power – open and lined side (measurement method V2):

Specimen preparation took place under test conditions of $23^{\circ}\text{C} \pm 1^{\circ}\text{C}$ temperature and $50\% \pm 5\%$ relative humidity. The test specimen was cut to 13 mm and adhered to a steel plate. The bond area was 20 mm · 13 mm (length · width). Prior to the measurement, the steel plate was cleaned and conditioned. For this purpose the plate was first wiped down with acetone and then left to stand in the air for 5 minutes to allow the solvent to evaporate. After bonding had taken place, the open side was reinforced with a 50 µm aluminium foil and rolled over back and forth twice using a 2 kg roller. Subsequently a belt loop was attached to the protruding end of the three-layer assembly. The whole system was then suspended from a suitable device and subjected to a load of 10 N. The suspension device is such that the weight loads the sample at an angle of $179^{\circ} \pm 1^{\circ}$. This ensures that the three-layer assembly is unable to peel from the bottom edge of the plate. The measured holding power, the time between suspension and dropping of the sample, is reported in minutes and corresponds to the average value from three measurements. To measure the lined side, the open side is first reinforced with the 50 µm aluminium foil, the release material is removed, and adhesion to the test plate takes place as described. The measurement is conducted under standard conditions (23°C , 55% relative humidity).

Wall hook test (measurement method V3):

Figure 4 shows the arrangement of the test method. A test specimen (3.1) measuring 30 mm · 30 mm and fixed between two polished steel plates (3.2) is subjected to a pressure of 0.9 kN (force P) for 1 minute. Thereafter a lever arm (3.3) 9 cm long is screwed into the uppermost steel plate, and is then loaded with a 1000 g weight (3.4). Care is taken to ensure that the time between application of pressure and loading is not more than two minutes ($t \leq 2 \text{ min}$).

A measurement is made of the holding time, i.e. the time between the suspension and the dropping of the specimen. The result reported is the holding time in minutes as the average from a triplicate determination. The test conditions are $23^{\circ}\text{C} \pm 1^{\circ}\text{C}$ and $50\% \text{ rh} \pm 5\% \text{ rh}$ (rh is relative humidity).

Measurements were made in each case of the open side and of the lined side.

Commercially available chemicals used

<i>Chemical compound</i>	<i>Trade name</i>	<i>Manufacturer</i>	<i>CAS No.</i>
Bis(4- <i>tert</i> -butylcyclohexyl) peroxydicarbonate	Perkadox [®] 16	Akzo Nobel	15520-11-3
2,2'-Azobis(2-methylpropionitrile), AIBN	Vazo [®] 64	DuPont	78-67-1
Terpene-phenolic-based tackifier resin (softening point 110°C, hydroxyl value 45-60)	Dertophene [®] T110	DRT, France	73597-48-5
2,2'-(1,3-Phenylene)bis[4,5-dihydrooxazole]	1,3-PBO	evonik AG	34052-90-9
2,2'-(1,4-Phenylene)bis[4,5-dihydrooxazole]	1,4-PBO	evonik AG	7426-75-7
Styrene-2-isopropenyl-2-oxazoline copolymer	Epocros RPS 1005	Nippon Shokubai Co.	30174-74-4
p-Toluenesulfonic acid monohydrate	-	Sigma-Aldrich	6192-52-5
Isopropylated triaryl phosphate	Reofos [®] 65	Great Lakes, USA	68937-41-7
Hollow glass beads (density 0.28 g/cm ³ ; bulk density 0.16 g/cm ³ , particle diameter 5 – 115 µm [range]; 65 µm [average value])	Q-Cel [®] Hollow Glass Spheres 5028	Potters Industries	
Chalk (density 2.74 g/cm ³ , bulk density 0.56 g/cm ³ , pH value 8.8 – 9.5, solubility [water] 16 mg/l, decomposition point 900°C)	Mikrosöhl [®] 40	Vereinigte Kreidewerke Dammann kg	1317-65-3
Thermoplastic hollow microbeads (particle size 10 – 17 µm; density max. 0.017 g/cm ³ ; expansion temperature 127 - 139°C [start]; 164 – 184°C [max. Exp.])	Expancel [®] 092 DU 40	Akzo Nobel	

all specification figures at 20°C;

Pressure-sensitive adhesive (PSA) examples

Preparation of starting polymers for Examples PSA B1 to B5

Described below is the preparation of the starting polymers. The polymers investigated are prepared conventionally via free radical addition polymerization in solution.

Base polymer P1

A reactor conventional for free-radical polymerizations was charged with 45 kg of 2-ethyl-hexyl acrylate, 45 kg of n-butyl acrylate, 5 kg of methyl acrylate, 5 kg of acrylic acid and 66 kg of acetone/isopropanol (92.5:7.5). After nitrogen gas had been passed through the reactor for 45 minutes with stirring, the reactor was heated to 58°C and 50 g of AIBN were added. Subsequently the external heating bath was heated to 75°C and the reaction was carried out constantly at this external temperature. After 1 h a further 50 g of AIBN were added, and after 4 h the batch was diluted with 20 kg of acetone/isopropanol mixture.

After 5 h and again after 7 h, reinitiation took place with 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case. After a reaction time of 22 h the polymerization was terminated and the batch was cooled to room temperature. The polyacrylate has a conversion of 99.6%, a K value of 59, a solids content of 54%, an average molecular weight of $M_w = 557\,000$ g/mol, polydispersity PD (M_w/M_n) = 7.6.

Base polymer P2

A reactor conventional for free-radical polymerizations was charged with 45 kg of 2-ethyl-hexyl acrylate, 45 kg of n-butyl acrylate, 5 kg of acrylic acid, 150 g of dibenzoyl trithiocarbonate and 66 kg of acetone. After nitrogen gas had been passed through the reactor for 45 minutes with stirring, the reactor was heated to 58°C and 50 g of AIBN were added. Subsequently the external heating bath was heated to 75°C and the reaction was carried out constantly at this external temperature. After 1 h a further 50 g of AIBN were added. After 4 h the batch was diluted with 10 kg of acetone. After 5 h and again after 7 h, reinitiation took place with 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case. After a reaction time of 22 h the polymerization was terminated and the batch was cooled to room temperature.

The polyacrylate has a conversion of 99.5%, a K value of 43.9, a solids content of 56.5%, an average molecular weight of $M_w = 407\,000$ g/mol, polydispersity PD (M_w/M_n) = 2.4.

Base polymer P3

In the same way as in Example P1, 41.5 kg of 2-ethylhexyl acrylate, 41.5 kg of n-butyl acrylate, 15 kg of methyl acrylate, 1 kg of acrylic acid and 1 kg of 2-hydroxyethyl methacrylate (HEMA) were polymerized in 66 kg of acetone/isopropanol (92.5:7.5). Initiation was carried out twice with 50 g of AIBN in each case, twice with 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case, and dilution was carried out with 20 kg of acetone/isopropanol mixture (92.5:7.5). After a reaction time of 22 h the polymerization was terminated and the batch was cooled to room temperature.

The polyacrylate has a conversion of 99.6%, a K value of 69.5, a solids content of 53.3%, an average molecular weight of $M_w = 689\,000$ g/mol, polydispersity PD (M_w/M_n) = 7.8.

Process 1: Concentration/preparation of the hotmelt PSAs:

The acrylate copolymers (base polymers P1 to P3) are very largely freed from the solvent by means of a single-screw extruder (concentrating extruder, Berstorff GmbH, Germany) (residual solvent content $\leq 0.3\%$ by weight; cf. the individual examples). The parameters given here by way of example are those for the concentration of base polymer P1. The screw speed was 150 rpm, the motor current 15 A, and a throughput of 58.0 kg liquid/h was realized. For concentration, a vacuum was applied at three different domes. The reduced pressures were, respectively, between 20 mbar and 300 mbar. The exit temperature of the concentrated hotmelt is approximately 115°C. The solids content after this concentration step was 99.8%.

Process 2: Preparation of the modified hotmelt PSAs and viscoelastic backings

The acrylate hotmelt PSA prepared in accordance with Process 1 as elucidated above were conveyed directly into a downstream Welding twin-screw extruder (Welding Engineers, Orlando, USA; model 30 MM DWD; screw diameter 30 mm, length of screw 1 = 1258 mm; length of screw 2 = 1081 mm; 3 zones). Via a solids metering system, the resin Dertophene® T110 was metered in zone 1 and mixed in homogeneously. In the case of the composition for Examples MT 1 and MT 2, no resin was metered in. In the case of Examples MT 3, MT 4 and MT 5, the corresponding adjuvants were metered in via the solids metering system and were mixed in homogeneously. The parameters given here by way of example are those for resin compounding with base polymer P1. Speed was 451 rpm, the motor current 42 A, and a throughput of 30.1 kg/h was realized. The

temperatures of zones 1 and 2 were each 105°C, the melt temperature in zone 1 was 117°C, and the composition temperature on exit (zone 3) was 100°C.

Process 3: Production of the inventive adhesive tapes, blending with the crosslinker system for thermal crosslinking, and coating

The acrylate hotmelt PSAs prepared by Processes 1–2 were melted in a feeder extruder (single-screw conveying extruder from Troester GmbH & Co. KG, Germany) and using this extruder were conveyed as a polymer melt into a twin-screw extruder (Leistritz, Germany, ref. LSM 30/34). The assembly is heated electrically from the outside and is air-cooled by a number of fans, and is designed such that, with effective distribution of the crosslinker- and/or the crosslinker-accelerator system in the polymer matrix, there is at the same time a short residence time ensured for the adhesive in the extruder. For this purpose the mixing shafts of the twin-screw extruder were arranged in such a way that conveying elements are in alternation with mixing elements. The addition of the respective crosslinkers and accelerators is made with suitable metering equipment, where appropriate at two or more points (Fig. 1: metering points 1.1 and 1.2) and, where appropriate, with the use of metering assistants into the unpressurized conveying zones of the twin-screw extruder.

Following exit of the ready-compounded adhesive, i.e. of the adhesive blended with the crosslinker- and/or the crosslinker-accelerator system, from the twin-screw extruder (exit: circular die, 5 mm diameter), coating takes place in accordance with Fig. 1 onto a backing material in web form. The time between metered addition of the crosslinker-accelerator system and the shaping or coating procedure is termed the processing life. The processing life indicates the period within which the adhesive, blended with the crosslinker- and/or crosslinker-accelerator system, or the viscoelastic backing layer, can be coated with a visually good appearance (gel-free, speck-free). Coating takes place with web speeds between 1 m/min and 20 m/min; the doctor roll of the 2-roll applicator is not driven.

In the examples below and in Tables 1 to 3, the formulations employed, the production parameters and the properties obtained are each described in more detail.

Example B1

The base polymer P1 is polymerized in accordance with the polymerization process described, concentrated in accordance with Process 1 (solids content 99.8%) and then blended with Dertophene® T110 resin in accordance with Process 2. This resin-modified

acrylate hotmelt composition was then compounded in accordance with Process 3 continuously with the crosslinker system consisting of a

- 2,2'-(1,4-phenylene)bis[4,5-dihydrooxazole],

in this case 1,4-BPO from Evonik Industries, Germany (bis-2-oxazoline).

Detailed description: In the twin-screw extruder described in Process 3, a total mass flow consisting of 70 parts of polymer P1 and 30 parts of Dertophene[®] T110 resin of 533.3 g/min (corresponding to 373 grams of the pure polymer per minute) was blended with 1.68 g/min of the bisoxazoline crosslinker 2,2'-(1,4-phenylene)bis[4,5-dihydrooxazole] (corresponding to 0.45% by weight based on polymer). The bisoxazoline was metered via a peristaltic pump at metering point 1.1 (see Fig.1). To improve meterability and the quality of mixing achievable, the crosslinker system used was diluted with the liquid phosphate ester (isopropylated triaryl phosphate; Reofos 65; Great Lakes, USA) (ratio to the crosslinker 0.5:1). The operational parameters are summarized in Table 2.

The processing life of the completed compounded formulation was more than 10 minutes with an average composition temperature of 125°C after departure from the Leistritz twin-screw extruder. Coating takes place on a 2-roll applicator in accordance with Figure 2, at roll surface temperatures of 100°C in each case and with a coat weight of 110 g/m² onto 23 µm PET film. On the adhesive tape thus produced, measurements were made of the bond strength to steel at room temperature and microshear travel at 40°C as a function of the storage time. After 18 days of room-temperature storage, the maximum microshear travel is measured at 220 µm, with an elastic fraction of 79%. Further technical adhesive data of Example B1 are summarized in Table 3. This example shows that very high-performance adhesive tapes can be produced, featuring, among other qualities, high bond strengths to polar and apolar substrates (steel and polyethylene) and good cohesive properties even under the influence of temperature.

Example B2

The base polymer P1, concentrated by Process 1 and blended by Process 2 with Dertophene[®] T110 resin (solids content: 99.8% by weight) was compounded by Process 3 in a twin-screw extruder with the crosslinker-accelerator system, and coated, in the same way as in Example B1.

The crosslinker-accelerator system is composed of

- 2,2'-(1,4-phenylene)bis[4,5-dihydrooxazole],

in this case 1,4-BPO from Evonik Industries, Germany (bis-2-oxazoline)

and

- p-toluenesulfonic acid monohydrate from Sigma-Aldrich (accelerator).

In the same way as in Example B1, 0.45% by weight of the difunctional 2-oxazoline 2,2'-(1,4-phenylene)bis[4,5-dihydrooxazole] and 0.08% by weight of the accelerator p-toluenesulfonic acid monohydrate (in each based on acrylate copolymer) were added by Process 3. The extruder speed of the Leistritz twin-screw extruder was 125 revolutions per minute, the mass throughput 32.0 kg/h. The processing life was 5 minutes for an effective composition temperature of 130°C following departure from the extruder. By means of the roll-applicator in accordance with Figure 2, coating took place with a coat weight of 110 g/m² onto 23 µm PET film.

On the adhesive tape thus produced, measurements were carried out of bond strength, holding power and microshear travel as a function of the storage time of the specimens at room temperature. After 12 days of room-temperature storage, holding powers of more than 10 000 minutes at room temperature were measured. This adhesive tape specimen was crosslinked in a similar manner to Example B1, as evident from the same maximum shear travel of 210 µm and from an elastic fraction of 80% in accordance with "microshear travel" measurement method H3, through which it can be demonstrated that the accelerator controls only the kinetics, and the degree of crosslinking is adjusted via the bisoxazoline. Further technical adhesive data are listed in Table 3 under Example B2.

Example B3

The polymerization of the polymer P2 used, the concentration, resin blending and incorporation of the crosslinker system, and coating, take place essentially as described in Example 1.

The crosslinking system used in this case is composed of a

- 2,2'-(1,3-phenylene)bis[4,5-dihydrooxazole],

in this case 1,3-BPO from Evonik Industries, Germany (bis-2-oxazoline).

In the same way as in Example B1, 0.55% by weight of the difunctional 2-bisoxazoline 2,2'-(1,3-phenylene)bis[4,5-dihydrooxazole] (based on acrylate copolymer) were added. Although this polymer system used, relative to Example B1, has a much narrower molar mass distribution, it has a lower K value of 43.9, and is formulated more moderately in terms of the cohesive properties, the holding powers of 23°C and 70°C. The holding powers at 23°C are 3600 min. Further details of figures specific to the composition are found in Table 1.

Example B4

The polymerization of polymer P2 used, concentration, resin blending and the incorporation of the crosslinker system, and coating, take place essentially as described in Example 1. Contrastingly, in Process 2, the chalk filler Mikrosöhl® 40 was incorporated as well, for which the mixing-screw geometries of the twin-screw extruder used were adapted accordingly. The crosslinker system used here was selected as in Example B3. 0.55% by weight of the difunctional 2-bisoxazoline 2,2'-(1,3-phenylene)bis[4,5-dihydrooxazole] were added (based on acrylate copolymer).

The average composition temperature after exit from the compounding extruder rose from 110°C to 117°C relative to the composition system from Example B3. Not only the measured bond strengths, at 9.4, but also the holding powers, at 5300 min, are improved relative to Example B3.

Further details of figures specific to the composition are found in Table 1, of operational parameters set in Table 2, and of technical adhesive results in Table 3, in each case in row B4.

Example B5

The base polymer P3 concentrated by Process 1 (residual solvent fraction: 0.15% by weight) was compounded by Process 3 in the twin-screw extruder with the crosslinker-accelerator system, and coated, in the same way as in Example B1.

The crosslinker-accelerator system is composed of an

- α -methyl-2-oxazoline styrene copolymer,
in this case Epocros RPS – 1005 from Nippon Shokubai, Japan (oxazoline)

and

p-toluenesulfonic acid monohydrate from Sigma Aldrich (accelerator).

5% by weight of the polyfunctional oxazoline and 0.1% by weight of p-toluenesulfonic acid monohydrate (in each case based on acrylate copolymer) were added by Process 3. The processing life was more than 5 minutes for an effective composition temperature of 114°C after departure from the extruder. By means of the two-roll applicator in accordance with Figure 2, coating took place with a coat weight of 125 g/m² onto 23 μ m PET film.

Where the crosslinker system and/or crosslinker-accelerator system of the invention is used, the crosslinking reaction via the functional groups of the polyacrylate proceeds completely, even without supply of heat, under standard conditions (room temperature).

In general, after a storage time of 5 days to 14 days, the crosslinking reaction has concluded to an extent sufficient to give a functional adhesive tape or functional backing layer. The final crosslinking state and hence the ultimate cohesion of the composition is achieved, depending on the choice of composition/crosslinker system, after storage for 14 to 100 days, in advantageous form after 14 to 50 days of storage time at room temperature; if the storage temperature is higher, these conditions are reached earlier, as expected.

The crosslinking increases the cohesion of the adhesive and hence also the shear strength. These groups are known to be very stable. This permits very ageing-stable and heat-resistant self-adhesive tapes.

Viscoelastic backing and three-layer construction examples

I. Preparation of the pressure-sensitive adhesive

Polyacrylate PSA 1 (PA1):

A 100 l glass reactor conventional for free-radical polymerizations was charged with 2.8 kg of acrylic acid, 8.0 kg of methyl acrylate, 29.2 kg of 2-ethylhexyl acrylate and 20.0 kg of acetone/isopropanol (95:5). After nitrogen gas had been passed through the reactor for 45 minutes with stirring, the reactor was heated to 58°C and 20 g of AIBN were added. Subsequently the external heating bath was heated to 75°C and the reaction was carried out constantly at this external temperature. After a reaction time of 1 h a further 20 g of AIBN were added. After 4 h and again after 8 h, the batch was diluted with 10.0 kg of acetone/isopropanol (95:5) mixture in each case. For reduction of the residual initiators, 60 g portions of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate were added after 8 h and again after 10 h. After a reaction time of 24 h the reaction was terminated and the batch was cooled to room temperature. Subsequently the polyacrylate was blended with 0.4% by weight of aluminium(III) acetylacetonate (3% strength solution in isopropanol), diluted to a solids content of 30% with isopropanol and then coated from solution onto a siliconized release film (50 µm polyester) (coating speed 2.5 m/min, drying tunnel 15 m, temperatures zone 1: 40°C, zone 2: 70°C, zone 3: 95°C, zone 4: 105°C). The coat weight was 50 g/m².

II. Production of the viscoelastic backings

Preparation of the starting polymers for the viscoelastic backings of Examples VT 1 to 5

Described below is the preparation of the starting polymers. The polymers investigated are prepared conventionally via free radical addition polymerization in solution.

Base polymer HPT 1

A reactor conventional for free-radical polymerizations was charged with 40 kg of 2-ethylhexyl acrylate, 40 kg of n-butyl acrylate, 15 kg of methyl acrylate, 5 kg of acrylic acid and 67 kg of acetone/isopropanol (95:5). After nitrogen gas had been passed through the reactor for 45 minutes with stirring, the reactor was heated to 58°C and 40 g of AIBN were added. Subsequently the external heating bath was heated to 75°C and the reaction was carried out constantly at this external temperature. After 1 h a further 60 g of AIBN were added, and after 4 h the batch was diluted with 14 kg of acetone/isopropanol mixture.

After 5 h and again after 7 h, reinitiation took place with 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case. After a reaction time of 22 h polymerization was terminated and the batch was cooled to room temperature. The polyacrylate has a K value of 57, a solids content of 54.6%, an average molecular weight of $M_w = 714\,000$ g/mol, polydispersity PD (M_w/M_n) = 7.6.

Base polymer HPT 2

In the same way as in Example 1, 65 kg of 2-ethylhexyl acrylate, 30 kg of *tert*-butyl acrylate and 5 kg of acrylic acid were polymerized in 67 kg of acetone/isopropanol (95:5). Initiation took place twice with 50 g of AIBN in each case, twice with 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case, and dilution took place with 20 kg of acetone/isopropanol mixture (95:5). After a reaction time of 22 h the polymerization was terminated and the batch was cooled to room temperature.

The polyacrylate has a K value of 61.0, a solids content of 53.2%, an average molecular weight of $M_w = 697\,000$ g/mol, polydispersity PD (M_w/M_n) = 7.1.

Base polymer HPT 3

The procedure adopted was similar to that in Example 1. For the polymerization, 60 kg of 2-ethylhexyl acrylate, 30 kg of styrene, 5 kg of methyl acrylate and 5 kg of acrylic acid were polymerized in 25 kg of ethyl acetate/isopropanol (97:3). Initiation took place twice

with 50 g of AIBN in each case, twice with 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case (after reaction times of 36 h and 44 h), and dilution took place with 20 kg of ethyl acetate/isopropanol mixture (97:3). After a reaction time of 48 h the polymerization was terminated and the batch was cooled to room temperature.

The polyacrylate has a K value of 61, a solids content of 68.4%, an average molecular weight of $M_w = 567\,000$ g/mol, polydispersity PD (M_w/M_n) = 11.8.

Base polymer HPT.4

A reactor conventional for free-radical polymerizations was charged with 65 kg of 2-ethylhexyl acrylate, 30 kg of *tert*-butyl acrylate, 5 kg of acrylic acid, 100 g of benzyl dithiobenzoate and 67 kg of acetone. After nitrogen gas had been passed through the reactor for 45 minutes with stirring, the reactor was heated to 58°C and 50 g of AIBN were added. Subsequently the external heating bath was heated to 75°C and the reaction was carried out constantly at this external temperature. After 1 h a further 50 g of AIBN were added, and after 4 h the batch was diluted with 10 kg of acetone. After 5 h and again after 7 h, an addition was made of 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case. After a reaction time of 22 h polymerization was terminated and the batch was cooled to room temperature.

The polyacrylate has a K value of 49.2, a solids content of 59.2%, an average molecular weight of $M_w = 379\,000$ g/mol, polydispersity PD (M_w/M_n) = 3.1.

Base polymer HPT.5

A reactor conventional for free-radical polymerizations was charged with 68 kg of 2-ethylhexyl acrylate, 25 kg of methyl acrylate, 7 kg of acrylic acid and 66 kg of acetone/isopropanol (95:5). After nitrogen gas had been passed through the reactor for 45 minutes with stirring, the reactor was heated to 58°C and 40 g of AIBN were added. Subsequently the external heating bath was heated to 75°C and the reaction was carried out constantly at this external temperature. After 1 h a further 60 g of AIBN were added, and after 4 h the batch was diluted with 20 kg of acetone/isopropanol (95:5). After 5 h and again after 7 h, an addition was made of 150 g of bis(4-*tert*-butylcyclohexyl) peroxydicarbonate in each case. After a reaction time of 22 h polymerization was terminated and the batch was cooled to room temperature.

The polyacrylate has a K value of 55, a solids content of 55%, an average molecular weight of $M_w = 579\,000$ g/mol, polydispersity PD (M_w/M_n) = 7.9.

Concentration and compounding of base polymers HPT 1–5 for the viscoelastic backings:

The acrylate copolymers HPT 1–5 are freed from the solvents in accordance with Process 1 and where appropriate are subsequently admixed by Process 2 with additives; cf. the individual examples.

Process 4: Production of the 3-layer constructions by means of 2-roll calender

The process was carried out as described in Fig. 3. Using a manifold die (1), the viscoelastic composition (3), already compounded with the crosslinker system and/or crosslinker-accelerator system and, where appropriate, fillers, is supplied to the roll nip. The shaping of the viscoelastic composition to a viscoelastic film takes place between the calender rolls (W1) and (W2) in the roll nip between two self-adhesive compositions (6a, 6b), which in turn are supplied coated onto anti-adhesively treated backing materials (5a, 5b). In this case there is, simultaneously, shaping of the viscoelastic composition to the set layer thickness, and coating with the two supplied self-adhesive compositions. In order to improve the anchoring of the self-adhesive compositions (6a, 6b) on the shaped viscoelastic backing layer (4), the self-adhesive compositions, before being supplied to the roll nip, are corona-treated by means of a corona station (8) (corona unit from Vitaphone, Denmark, 100 W·min/m²). As a result of this treatment, following the production of the three-layer assembly, there is improved chemical attachment to the viscoelastic backing layer.

The web speed on passing through the coating unit is 30 m/min.

Following departure from the roll nip, an anti-adhesive backing (5a) is lined if appropriate, and the completed three-layer product (9) is wound up with the remaining second anti-adhesive backing (5b).

Presented below are specific examples relating to the preparation of the self-adhesive compositions and the coating of the adhesive tapes of the invention, without any intention that the invention should be unnecessarily restricted by the choice of formulations, configurations and operational parameters specified.

Example MT 1

The base polymer HPT1 was concentrated by Process 1 (solids content 99.7%) and then compounded by Process 3 in a twin-screw extruder continuously with the crosslinker system composed of 2,2'-(1,3-phenylene)bis[4,5-dihydrooxazole](1,3-BPO); 0.42% by weight based on the polyacrylate). Coating to produce the viscoelastic backing VT1 from

the base polymer HPT1 between the composition layers PA 1, coated beforehand onto siliconized polyester films, takes place on a 2-roll applicator at roll temperatures of 100°C by Process 4. The layer thickness of the viscoelastic backing VT 1 was 880 μm . The corona power was 100 W·min/m². After seven days of room-temperature storage, the technical adhesive data were measured for both the open and the lined sides. The data of Example MT 1 are summarized in Table 4.

Example MT 2

The base polymer HPT2 was concentrated by Process 1 (solids content 99.8%) and then compounded by Process 3 in a twin-screw extruder continuously with the crosslinker system composed of 2,2'-(1,4-phenylene)bis[4,5-dihydrooxazole](1,4-BPO); 0.36% by weight based on the polyacrylate). Subsequently, in the same way as in Example 1, coating took place between composition layers PA 1, in each case coated beforehand onto siliconized polyester films, on a 2-roll applicator by Process 3. The layer thickness of the viscoelastic backing VT 2 was 850 μm . The corona power was 100 W·min/m². After seven days of room-temperature storage, the technical adhesive data were measured for both the open and lined sides. The data of Example MT 2 are summarized in Table 4.

Example MT 3

The base polymer HPT3 was concentrated by Process 1 (solids content 99.7%) and then compounded by Process 2 with 5.5% by weight of hollow glass beads Q-CEL[®] 5028 (Potters Industries) and compounded by Process 3 in a twin-screw extruder continuously with the crosslinker-accelerator system composed of 2,2'-(1,3-phenylene)bis[4,5-dihydrooxazole] (1,3-BPO; 0.42% by weight based on the polyacrylate) and p-toluenesulfonic acid monohydrate (0.1% by weight based on the polyacrylate). Coating to produce the viscoelastic backing VT3 between the composition layers PA 1, coated beforehand onto siliconized polyester films, takes place on a 2-roll applicator at roll temperatures of 100°C by Process 3. The layer thickness of the viscoelastic backing VT 3 was 800 μm . The corona power was 100 W·min/m². After seven days of room-temperature storage, the technical adhesive data were measured for both the open and the lined sides. The data of Example MT 3 are summarized in Table 4.

Example MT 4

The base polymer HPT4 was concentrated by Process 1 (solids content 99.7%) and then blended by Process 2 with 20% by weight of Mikrosöhl chalk (Mikrosöhl® 40) and compounded by Process 3 in a twin-screw extruder continuously with the crosslinker system composed of 2,2'-(1,4-phenylene)bis[4,5-dihydrooxazole] (1,4-BPO; 0.34% by weight based on the polyacrylate). Coating to produce the viscoelastic backing VT4 between the composition layers PA 1, coated beforehand onto siliconized polyester films, takes place on a 2-roll applicator at roll temperatures of 100°C by Process 3. The layer thickness of the viscoelastic backing VT 4 was 850 µm. The corona power was 100 W·min/m². After seven days of room-temperature storage, the technical adhesive data were measured for both the open and the lined sides. The data of Example MT 4 are summarized in Table 4.

Example MT 5

The base polymer HPT5 was concentrated by Process 1 (solids content 99.8%) and then blended by Process 2 with 3% by weight of unexpanded hollow microbeads Expancel® 092 DU 40 (Akzo Nobel, Germany) and compounded by Process 3 in a twin-screw extruder continuously with the crosslinker-accelerator system composed of an α -methylvinyl-2-oxazoline styrene copolymer (Epocros RPS – 1005; 2.5% by weight based on the polyacrylate) and p-toluenesulfonic acid monohydrate (0.08% by weight based on the polyacrylate). Heat was introduced to expand the mixture in the extruder, and then coating between the composition layers PA 1, coated beforehand onto siliconized polyester films, took place at roll temperatures of 130°C by Process 3. The layer thickness of the expanded viscoelastic backing VT 5 was 800 µm. The corona power for preheating the pressure-sensitive adhesive layers was 100 W·min/m². After seven days of room-temperature storage, the technical adhesive data were measured for both the open and the lined sides. The data of Example MT 5 are summarized in Table 4.

As is apparent from the data in Table 4, the inventively double-sidedly adhesive assembly tapes have very good technical adhesive data. A particularly positive feature is the balanced bonding profile of each of the sides. For a given layer of adhesive on both sides of the adhesive tape, these sides give virtually the same technical adhesive data. This shows the homogeneous crosslinking through the layer. This is surprising for the person skilled in the art. Moreover, these three-layer adhesive tapes do not exhibit delamination. The anchoring of the layers to one another is very good by virtue of the corona treatment

of the pressure-sensitive adhesive layers and the after-crosslinking of the adjacent viscoelastic backing layer.

Table 1: Composition-specific figures

Example	Base polymer	K value	Compounding by Process 2		
			Polymer and adjuvants	Ingredients and amounts	
				Crosslinker	% by weight based on polymer
		[]		Accelerator	
B1	P1	59	70 parts polymer P1 + 30 parts resin DT 110	1,4-BPO	0.45
				-	-
B2	P1	59	70 parts polymer P2 + 30 parts resin DT 110	1,4-BPO	0.45
				p-toluenesulfonic acid	0.08
B3	P2	43.9	70 parts polymer P3 + 30 parts resin DT 110	1,3-BPO	0.55
				-	-
B4	P2	43.9	49 parts polymer P3 + 21 parts resin DT 110 + 30 parts Mikrosöhl® 40 chalk	1,3-BPO	0.55
				-	-
B5	P3	69.5	100 parts polymer P4	Epocros RPS-1005	5
				p-toluenesulfonic acid	0.1

K value = measurement method A2

DT 110 = Dertophene® T110

Table 2: Operational parameters

Ex-ample	Base polymer		Compounding by Process 2	Operational parameters								
	Polymer	K value		Fraction of adjuvants	Total mass throughput TSE [kg/h]	TSE speed [1/min]	Nominal power con- sumption TSE [A]	Pressure at exit of TSE [bar]	Temp. of compo- sition after TSE [°C]	Doctor roll RW	Coating roll BW	Process- ing life [min]
[]	[]	[]										
B1	P1	59	70 parts polymer P1 + 30 parts resin DT 110	32.0	110	15	12	125	100	100	more than 10	
B2	P1	59	70 parts polymer P2 + 30 parts resin DT 110	32.0	110	15	13	130	100	100	5	
B3	P2	43.9	70 parts polymer P3 + 30 parts resin DT 110	12.0	110	8	10	110	100	100	more than 7	
B4	P2	43.9	49 parts polymer P3 + 21 parts resin DT 110 + 30 parts Mikrosöhle® 40 chalk	16.0	120	10	15	117	100	100	more than 7	
B5	P3	69.5	Polymer P4	10.0	100	14	20	114	100	100	more than 5	

TSE = twin-screw extruder; DT 110 = Dertophene® T110

Table 3: Technical adhesive results

Example	Base polymer		Compounding Process 2	Backing film	Technical adhesive properties after storage of specimens for 25 days at room temperature					
	Polymer	K value			Coat weight	Bond strength to steel	Bond strength to PE	Holding power 10N, 23°C	Holding power 10N, 70°C	MST 40°C / elast. fraction
[]	[]	[]	Fraction of adjuvants	[]	[g/m²]	[N/cm]	[N/cm]	[min]	[min]	[µm] / [%]
B1	P1	59	70 parts polymer P1 + 30 parts resin DT 110	23µm PET film	110	11.8	4.6	> 10 000	150	220 / 79
B2	P1	59	70 parts polymer P2 + 30 parts resin DT 110	23µm PET film	110	11.4	4.4	> 10 000	160	210 / 80
B3	P2	43.9	70 parts polymer P3 + 30 parts resin DT 110	23µm PET film	79	8.1	4.4	3 600	15	512 / 67
B4	P2	43.9	49 parts polymer P3 + 21 parts resin DT 110 + 30 parts Mikrosöhl® 40 chalk	23µm PET film	80	9.4	3.1	5 300	28	430 / 73
B5	P3	69.5	only polymer P4	23µm PET film	125	8.6	2.5	7 500	1250	660 / 81

Bond strength steel / PE = measurement method H1
Holding power = measurement method H2

MST = Microshear travel = measurement method H3
DT 110 = Dertophene® T110

Table 4: Product construction and technical adhesive data of the three-layer constructions

Ex- ample	Three-layer product			Backing thick- ness [µm]	Bond strength for steel [N/cm]		Holding power 10 N 23°C [min]		Wall hook test [min]		MST 40°C / elast. fraction [µm] / [%]
	PSA 1	Visco- elastic backing layer	PSA 2		open side	lined side	open side	lined side	open side	lined side	
MT 1	50 g/m ² PA 1	VT 1	50 g/m ² PA 1	880	22.9	23.2	> 10000	> 10000	2580	2795	284 / 91
MT 2	50 g/m ² PA 1	VT 2	50 g/m ² PA 1	850	17.8	17.6	8850	8970	2876	2256	617 / 78
MT 3	50 g/m ² PA 1	VT 3	50 g/m ² PA 1	800	20.7	20.2	> 10000	> 10000	9320	9360	346 / 79
MT 4	50 g/m ² PA 1	VT 4	50 g/m ² PA 1	850	13.7	13.6	7540	7468	2880	2568	738 / 75
MT 5	50 g/m ² PA 1	VT 5	50 g/m ² PA 1	800	13.5	13.6	> 10000	> 10000	> 10000	> 10000	967 / 76

Bond strength steel = measurement method V1

Holding power = measurement method V2

Wall hook test = measurement method V3

Claims

1. Process for preparing homogeneously crosslinked polymers,
 - in which at least one crosslinker is added to a polymer in the melt,
 - in which the polymer is further-processed from the melt,
 - and in which a thermal crosslinking reaction is brought about by means of the crosslinker, with at least part of the crosslinking reaction taking place after the further processing at a temperature below the melting temperature of the polymer,characterized in that
 - the crosslinker comprises an at least difunctional compound, at least one of the functional groups being an oxazoline group, and
 - the polymer contains functional groups which, at a temperature below the melting temperature of the polymer, are able to react with the oxazolines in a linking reaction in the sense of the thermal crosslinking reaction.
2. Process according to Claim 1, characterized in that the further processing of the polymer from the melt comprises shaping of the polymer composition, more particularly coating onto a backing material.
3. Process according to either of the preceding claims, characterized in that the homogeneously crosslinked polymer serves as a basis for a pressure-sensitive adhesive.
4. Process according to any of the preceding claims, characterized in that the polymer is a polyacrylate.
5. Process according to any of the preceding claims, characterized in that additionally, during the crosslinking reaction, functional groups (accelerators) which have an accelerating action for the crosslinking reaction at a temperature below the melting temperature of the polymer are present.
6. Process according to any of the preceding claims, characterized in that the crosslinker is a liquid oxazoline derivative.

7. Process according to any of the preceding claims, characterized in that the crosslinker is a solid which melts only above the melting temperature of the polymer and can be incorporated homogeneously into the polymer melt.
8. Process according to any of the preceding claims, characterized in that a difunctional or polyfunctional oxazoline is used as crosslinker.
9. Process according to Claim 7, characterized in that a difunctional or polyfunctional 2-oxazoline is used as crosslinker.
10. Process according to any of the preceding claims, characterized in that the functional groups of the polymer which, at a temperature below the melting temperature of the polymer, are able to react with the oxazolines in a linking reaction in the sense of the thermal crosslinking reaction are wholly or partly carboxyl groups.
11. Process according to any of Claims 5 to 9, characterized in that a Brønsted acid, preferably an organic acid or a mineral acid, is used as accelerator.
12. Process according to any of Claims 5 to 9, characterized in that a Lewis acid is used as accelerator.
13. Process according to any of the preceding claims, characterized in that the crosslinking reaction takes place at least partially at room temperature.
14. Homogeneously crosslinked, especially emulsifier-free, polymers obtainable by a process according to any of Claims 1 to 12.
15. Use of at least difunctional compounds, at least one of the functional groups being an oxazoline group, as thermal crosslinkers for polymers which are processed from the melt, especially polyacrylates.

1/4

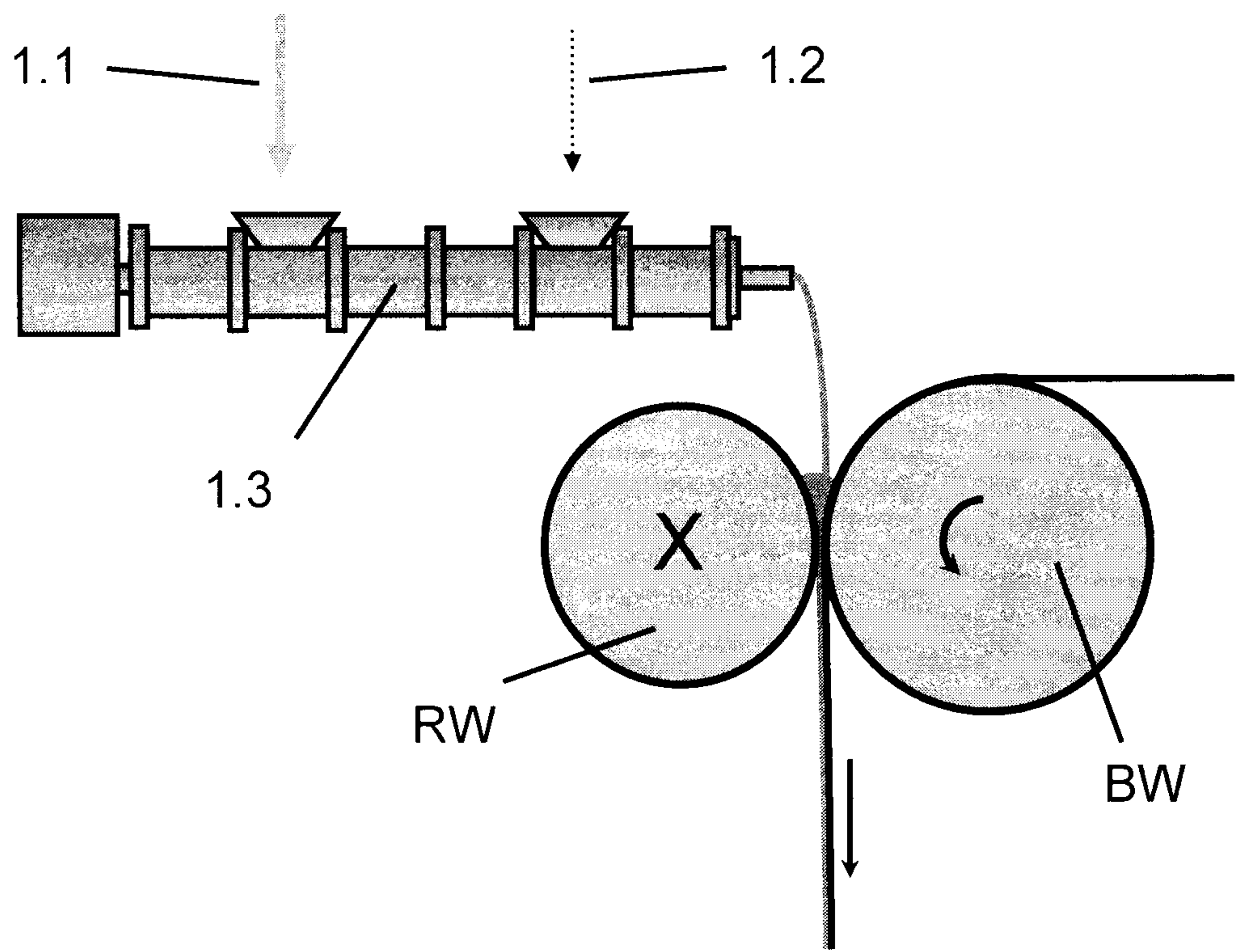


Fig. 1

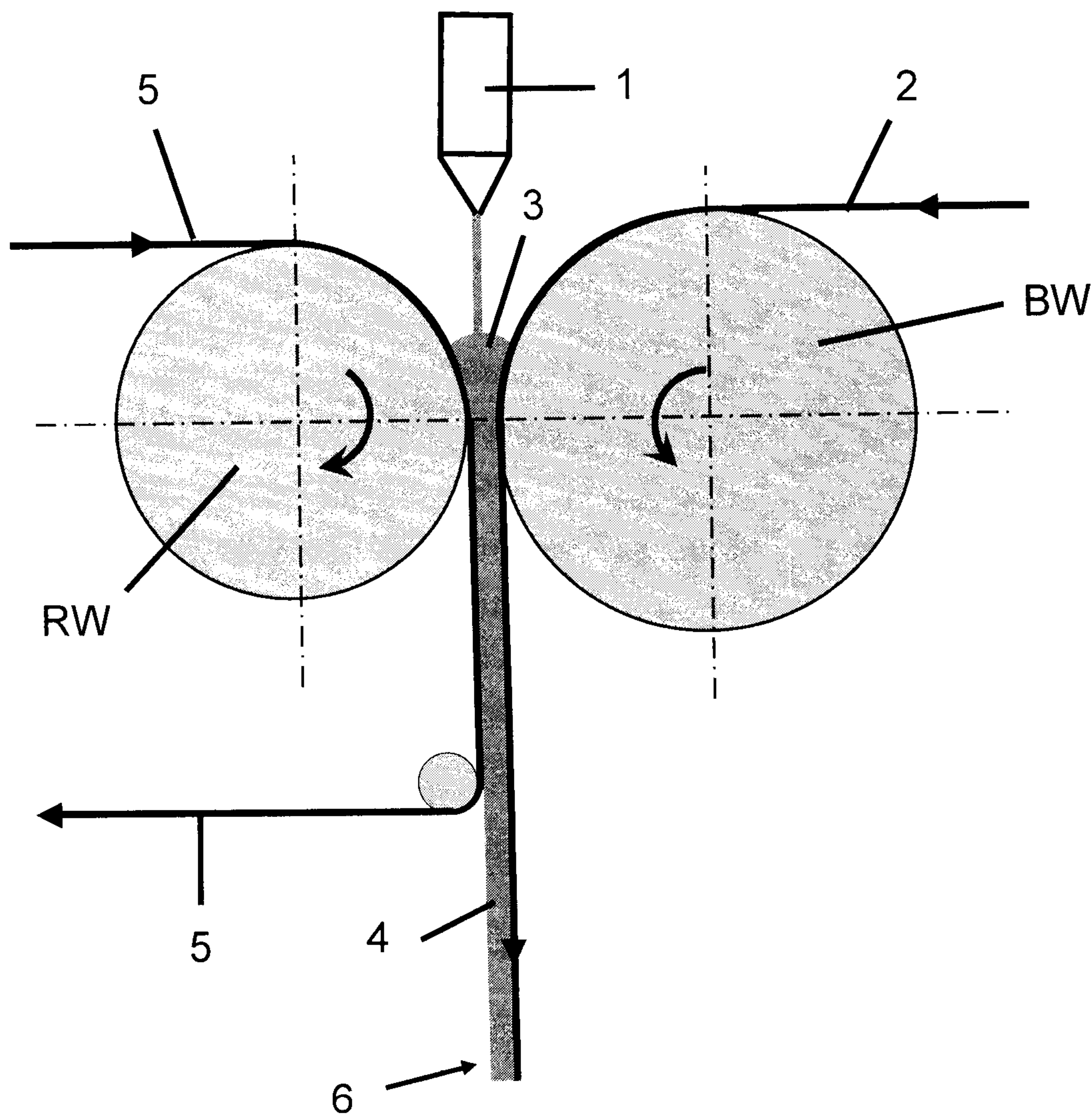


Fig. 2

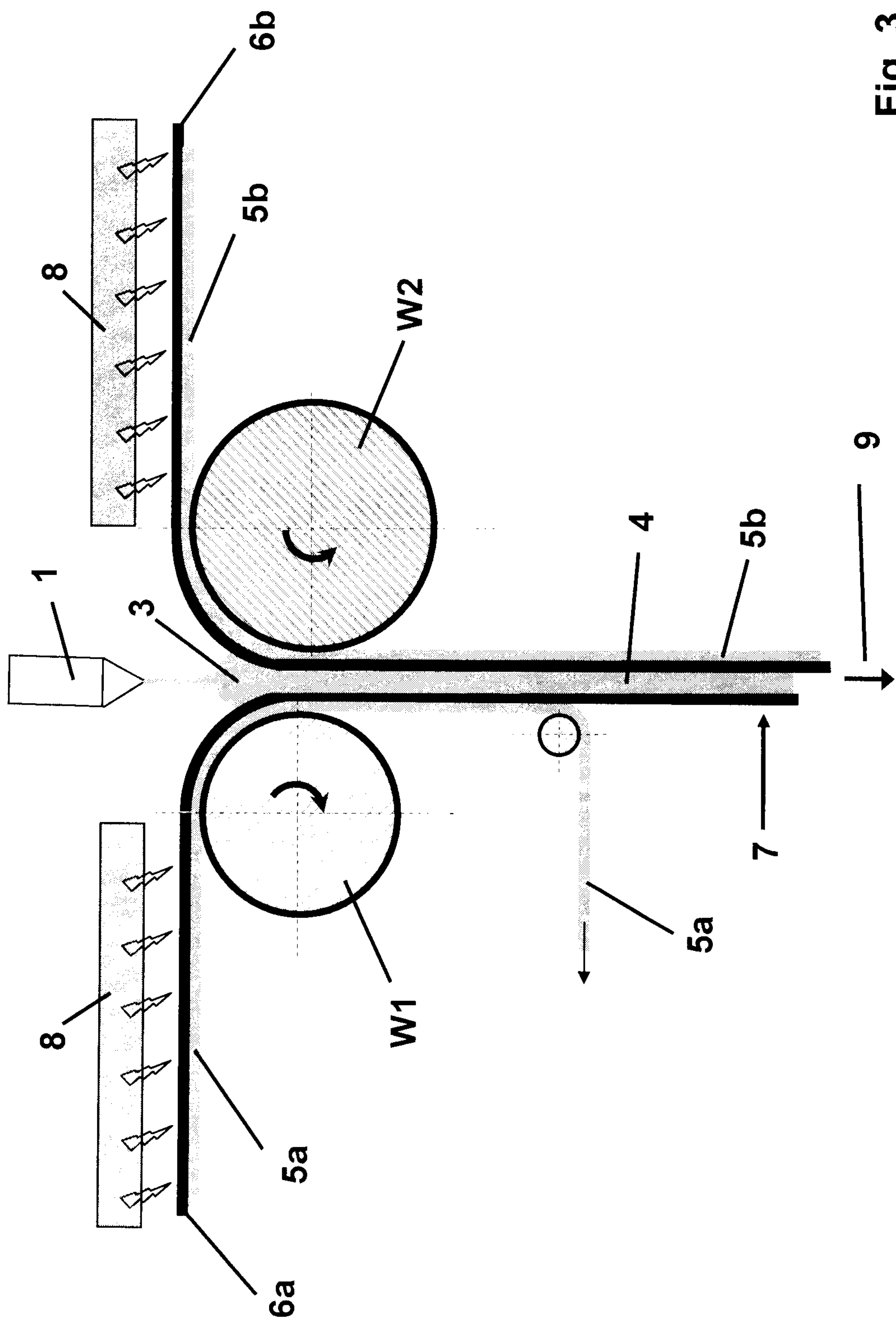


Fig. 3

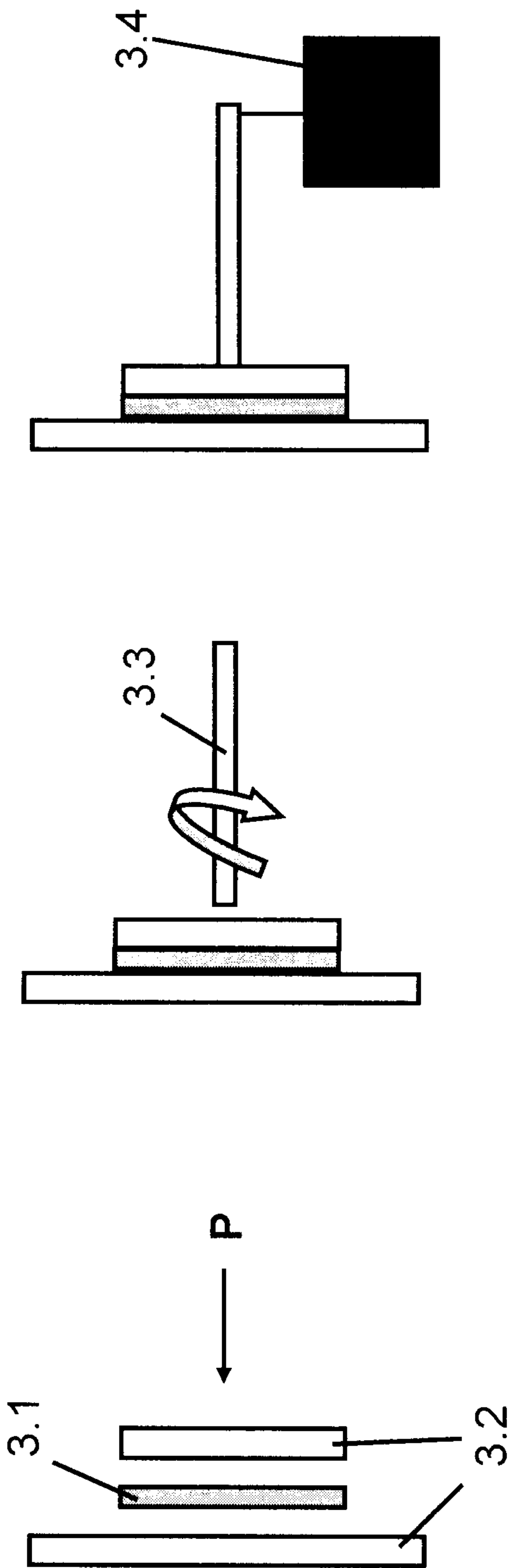


Fig. 4

