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(54) **HIGH SHEAR PROCESS FOR THE PRODUCTION OF CHLOROBENZENE**

**Related U.S. Application Data**

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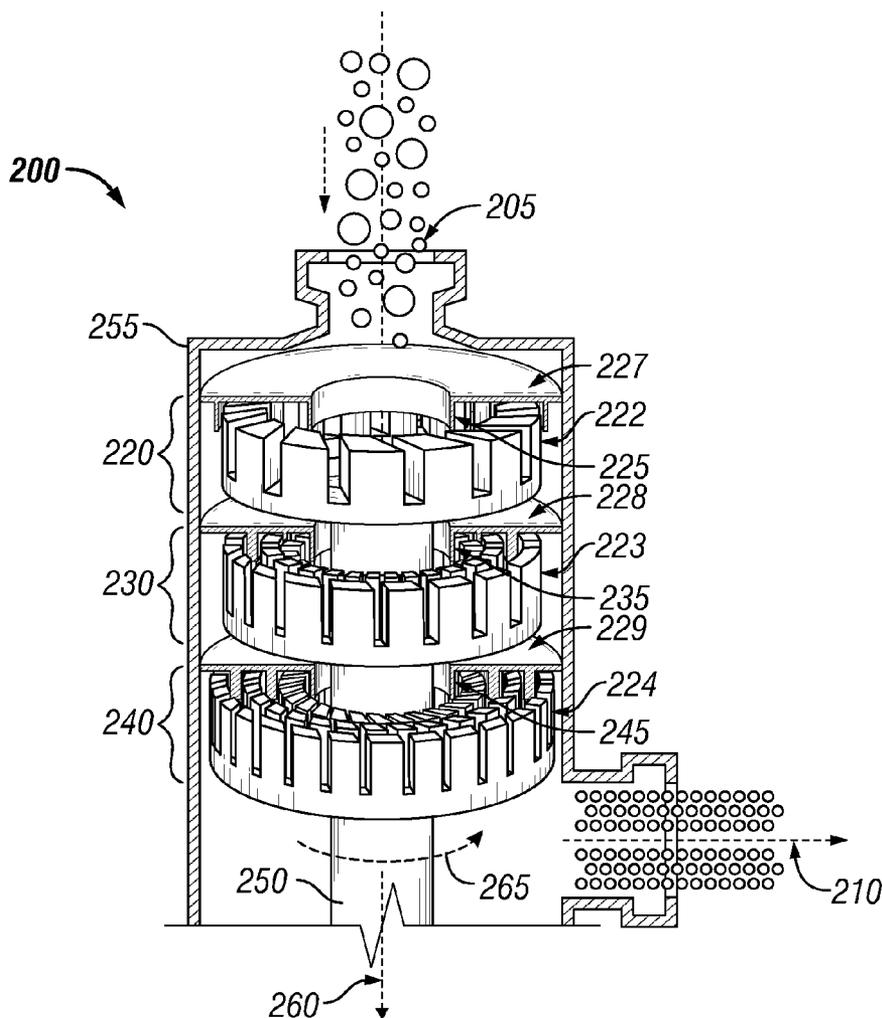
(57) **ABSTRACT**

Use of a high shear mechanical device incorporated into a process for the production of chlorobenzene is capable of decreasing mass transfer limitations, thereby enhancing the chlorobenzene production process. A system for the production of chlorobenzene from benzene and chlorine, the system comprising a reactor and an external high shear device, the outlet of which is fluidly connected to the inlet of the reactor; the high shear device capable of providing a emulsion of chlorine gas bubbles within liquid benzene

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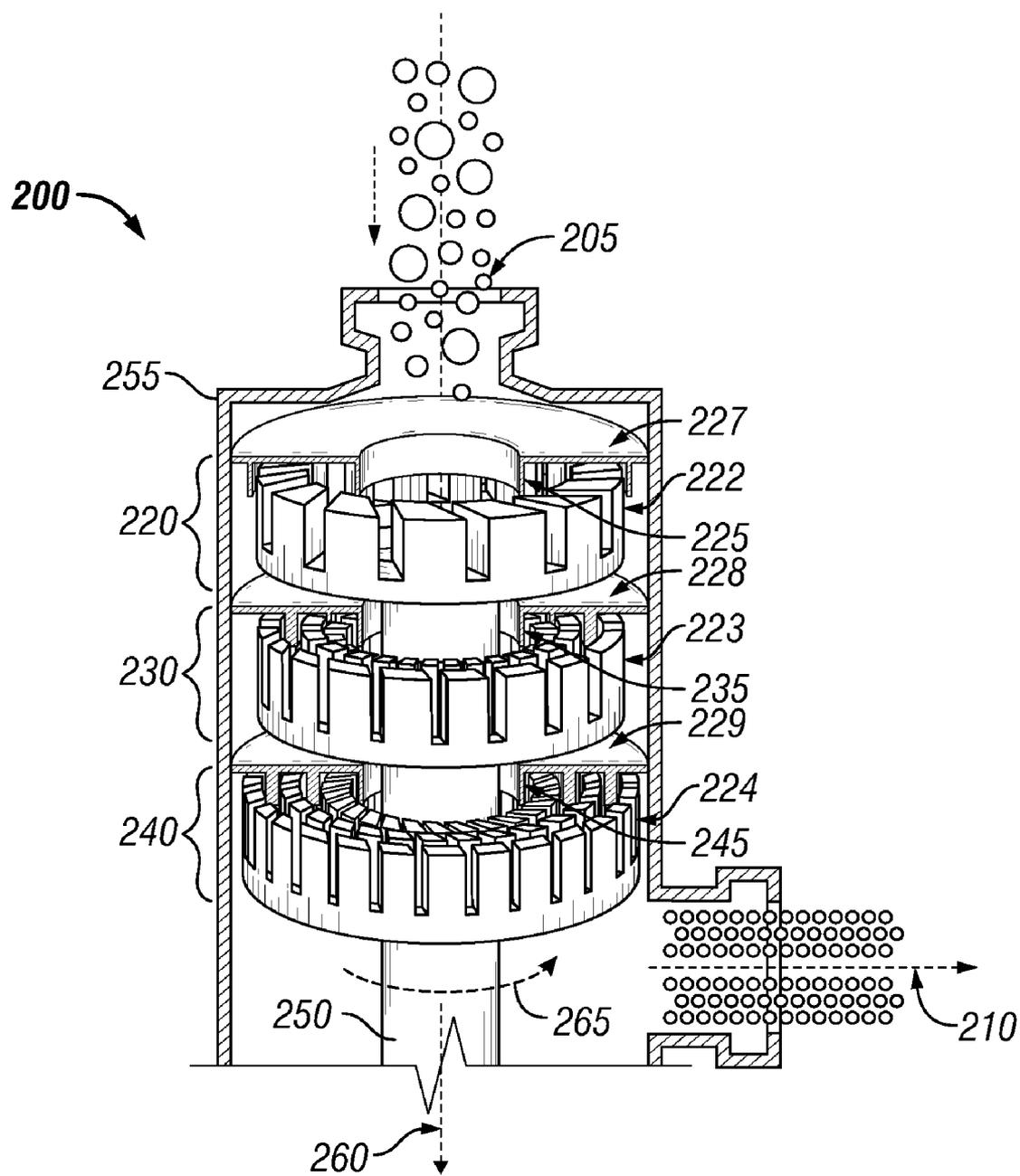


FIG. 1

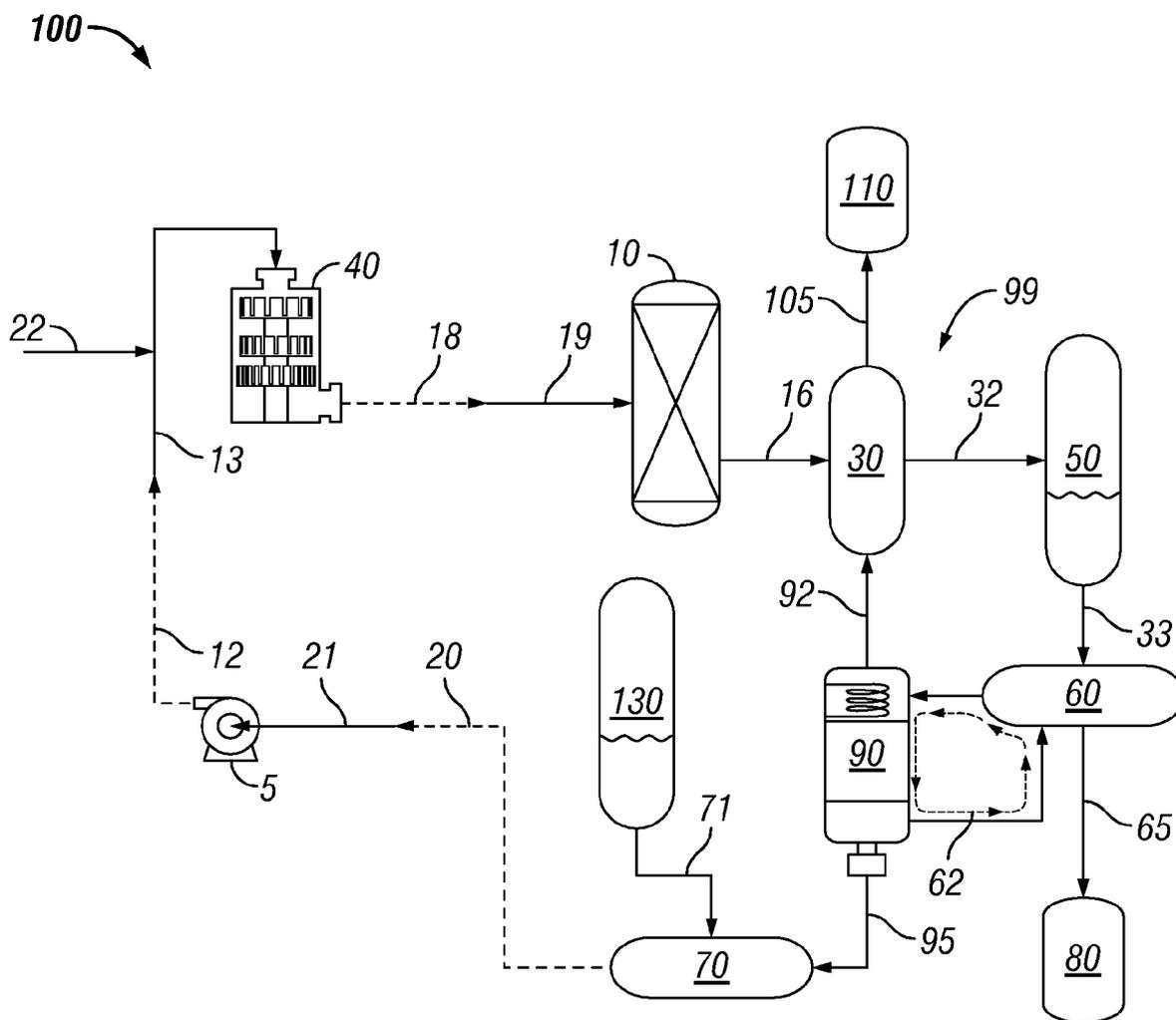


FIG. 2

## HIGH SHEAR PROCESS FOR THE PRODUCTION OF CHLOROBENZENE

### CROSS-REFERENCE TO RELATED APPLICATIONS

**[0001]** This application claims the benefit under 35 U.S.C. § 119(e) of U.S. Provisional Patent Application No. 60/946,524 filed Jun. 27, 2007, the disclosure of which is hereby incorporated herein by reference.

### STATEMENT REGARDING FEDERALLY SPONSORED RESEARCH OR DEVELOPMENT

**[0002]** Not Applicable.

### BACKGROUND OF THE INVENTION

**[0003]** 1. Technical Field

**[0004]** The present disclosure relates generally to the production of chlorobenzene by chlorination of benzene and, more particularly, to apparatus and methods for producing chlorobenzene via chlorination of benzene in a high shear process. More specifically, the disclosure pertains still more particularly to the reduction of mass transfer limitations for converting benzene to chlorobenzene.

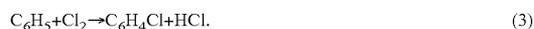
**[0005]** 2. Background of the Invention

**[0006]** Chlorobenzene is used as a solvent with applications in certain pesticide formulations, automotive and industrial degreasers, and as a chemical intermediate to make herbicides, rubber, and dyes. Benzene reacts with chlorine in the presence of a catalyst at room temperature, replacing one of the hydrogen atoms on the benzene ring with a chlorine atom. The catalyst is typically aluminum chloride or iron.

**[0007]** Iron is altered during the reaction such that chlorine forms iron (III) chloride,  $\text{FeCl}_3$ .



**[0008]** This compound acts as the catalyst and behaves like aluminum chloride,  $\text{AlCl}_3$ , in the reaction. The reaction between benzene and chlorine in the presence of either aluminum chloride or iron gives chlorobenzene, or, written more compactly:



As reaction (2) is the desired reaction, certain parameters must be maintained in the reactor. In certain cases, dichlorobenzene can be formed if reaction temperatures are not controlled properly.

**[0009]** There is a need in the industry for improved methods of producing chlorobenzene from benzene and chlorine whereby costs may be reduced via operation at lower temperature and/or pressure, increased product yield, decreased reaction time, and/or reduced capital and/or operating costs.

### SUMMARY OF THE INVENTION

**[0010]** A high shear system and method for accelerating the production of chlorobenzene is disclosed. The disclosed high shear method reduces mass transfer limitations, thereby improving reaction conditions in the reactor such as the reaction rate, temperature, pressure, contact time, and/or product yield. In accordance with certain embodiments of the present

disclosure, a method is provided that enhances the rate of a liquid phase process for the production of chlorobenzene from benzene by providing for more optimal time, temperature, and pressure conditions than are currently used.

**[0011]** The method employs a high shear mechanical device to provide enhanced time, temperature, and pressure conditions resulting in accelerated chemical reactions between multiphase reactants.

**[0012]** In an embodiment, the method comprises the use of a pressurized high shear device to provide for production of chlorobenzene without the need for large volume reactors.

**[0013]** These and other embodiments, features, and advantages will be apparent in the following detailed description and drawings.

### BRIEF DESCRIPTION OF THE DRAWINGS

**[0014]** For a more detailed description of the preferred embodiment of the present invention, reference will now be made to the accompanying drawings, wherein:

**[0015]** FIG. 1 is a cross-sectional diagram of a high shear device for the production of chlorobenzene.

**[0016]** FIG. 2 is a process flow diagram according to an embodiment of the present disclosure including a high shear device for production of chlorobenzene.

### DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

#### Overview

**[0017]** A system and method employs an external high shear mechanical device to provide rapid contact and mixing of chemical ingredients in a controlled environment in the reactor/mixer device. The high shear device reduces the mass transfer limitations on the reaction and thus increases the overall reaction rate.

**[0018]** Chemical reactions involving liquids, gases and solids rely on the laws of kinetics that involve time, temperature, and pressure to define the rate of reactions. In cases where it is desirable to react two or more raw materials of different phases (e.g. solid and liquid; liquid and gas; solid, liquid and gas), one of the limiting factors in controlling the rate of reaction involves the contact time of the reactants. In the case of heterogeneously catalyzed reactions there may be the additional rate limiting factor of having the reaction products removed from the surface of the catalyst to enable the catalyst to catalyze further reactants.

**[0019]** In conventional reactors, contact time for the reactants and/or catalyst is often controlled by mixing which provides contact between two or more reactants involved in a chemical reaction. A reactor assembly that comprises an external high shear mixer makes possible decreased mass transfer limitations and thereby allows the reaction to more closely approach kinetic limitations. When reaction rates are accelerated, residence times may be decreased, thereby increasing obtainable throughput. Alternatively, where the current yield is acceptable, decreasing the required residence time allows for the use of lower temperatures and/or pressures than conventional processes.

#### High Shear Device

**[0020]** High shear devices (HSD) such as a high shear mixer, or high shear mill, are generally divided into classes based upon their ability to mix fluids. Mixing is the process of reducing the size of inhomogeneous species or particles

within the fluid. One metric for the degree or thoroughness of mixing is the energy density per unit volume that the mixing device generates to disrupt the fluid particles. The classes are distinguished based on delivered energy density. There are three classes of industrial mixers having sufficient energy density to consistently produce mixtures or emulsions with particle or bubble sizes in the range of 0 to 50  $\mu\text{m}$ .

[0021] Homogenization valve systems are typically classified as high energy devices. Fluid to be processed is pumped under very high pressure through a narrow-gap valve into a lower pressure environment. The pressure gradients across the valve and the resulting turbulence and cavitations act to break-up any particles in the fluid. These valve systems are most commonly used in milk homogenization and can yield average particle size range from about 0.01  $\mu\text{m}$  to about 1  $\mu\text{m}$ . At the other end of the spectrum are high shear mixer systems classified as low energy devices. These systems usually have paddles or fluid rotors that turn at high speed in a reservoir of fluid to be processed, which in many of the more common applications is a food product. These systems are usually used when average particle, globule or bubble, sizes of greater than 20 microns are acceptable in the processed fluid.

[0022] Between low energy—high shear mixers and homogenization valve systems, in terms of the mixing energy density delivered to the fluid, are colloid mills, which are classified as intermediate energy devices. The typical colloid mill configuration includes a conical or disk rotor that is separated from a complementary, liquid-cooled stator by a closely-controlled rotor-stator gap, which is maybe between 0.025 mm and 10.0 mm. Rotors are usually driven by an electric motor through a direct drive or belt mechanism. Many colloid mills, with proper adjustment, can achieve average particle, or bubble, sizes of about 0.01  $\mu\text{m}$  to about 25  $\mu\text{m}$  in the processed fluid. These capabilities render colloid mills appropriate for a variety of applications including colloid and oil/water-based emulsion processing such as that required for cosmetics, mayonnaise, silicone/silver amalgam formation, or roofing-tar mixing.

[0023] Referring now to FIG. 1, there is presented a schematic diagram of a high shear device 200. High shear device 200 comprises at least one rotor-stator combination. The rotor-stator combinations may also be known as generators 220, 230, 240 or stages without limitation. The high shear device 200 comprises at least two generators, and most preferably, the high shear device comprises at least three generators.

[0024] The first generator 220 comprises rotor 222 and stator 227. The second generator 230 comprises rotor 223, and stator 228; the third generator comprises rotor 224 and stator 229. For each generator 220, 230, 240 the rotor is rotatably driven by input 250. The generators 220, 230, 240 rotate about axis 260 in rotational direction 265. Stator 227 is fixably coupled to the high shear device wall 255.

[0025] The generators include gaps between the rotor and the stator. The first generator 220 comprises a first gap 225; the second generator 230 comprises a second gap 235; and the third generator 240 comprises a third gap 245. The gaps 225, 235, 245 are between about 0.025 mm (0.01 in) and 10.0 mm (0.4 in) wide. Alternatively, the process comprises utilization of a high shear device 200 wherein the gaps 225, 235, 245 are between about 0.5 mm (0.02 in) and about 2.5 mm (0.1 in). In certain instances the gap is maintained at about 1.5 mm (0.06 in). Alternatively, the gaps 225, 235, 245 are different between generators 220, 230, 240. In certain instances, the

gap 225 for the first generator 220 is greater than about the gap 235 for the second generator 230, which is greater than about the gap 245 for the third generator 240.

[0026] Additionally, the width of the gaps 225, 235, 245 may comprise a coarse, medium, fine, and super-fine characterization. Rotors 222, 223, and 224 and stators 227, 228, and 229 may be toothed designs. Each generator may comprise two or more sets of rotor-stator teeth, as known in the art. Rotors 222, 223, and 224 may comprise a number of rotor teeth circumferentially spaced about the circumference of each rotor. Stators 227, 228, and 229 may comprise a number of stator teeth circumferentially spaced about the circumference of each stator. In embodiments, the inner diameter of the rotor is about 11.8 cm. In embodiments, the outer diameter of the stator is about 15.4 cm. In further embodiments, the rotor and stator may have an outer diameter of about 60 mm for the rotor, and about 64 mm for the stator. Alternatively, the rotor and stator may have alternate diameters in order to alter the tip speed and shear pressures. In certain embodiments, each of three stages is operated with a super-fine generator, comprising a gap of between about 0.025 mm and about 3 mm. When a feed stream 205 including solid particles is to be sent through high shear device 200, the appropriate gap width is first selected for an appropriate reduction in particle size and increase in particle surface area. In embodiments, this is beneficial for increasing catalyst surface area by shearing and dispersing the particles.

[0027] High shear device 200 is fed a reaction mixture comprising the feed stream 205. Feed stream 205 comprises an emulsion of the dispersible phase and the continuous phase. Emulsion refers to a liquefied mixture that contains two distinguishable substances (or phases) that will not readily mix and dissolve together. Most emulsions have a continuous phase (or matrix), which holds therein discontinuous droplets, bubbles, and/or particles of the other phase or substance. Emulsions may be highly viscous, such as slurries or pastes, or may be foams, with tiny gas bubbles suspended in a liquid. As used herein, the term “emulsion” encompasses continuous phases comprising gas bubbles, continuous phases comprising particles (e.g., solid catalyst), continuous phases comprising droplets of a fluid that is substantially insoluble in the continuous phase, and combinations thereof.

[0028] Feed stream 205 may include a particulate solid catalyst component. Feed stream 205 is pumped through the generators 220, 230, 240, such that product dispersion 210 is formed. In each generator, the rotors 222, 223, 224 rotate at high speed relative to the fixed stators 227, 228, 229. The rotation of the rotors pumps fluid, such as the feed stream 205, between the outer surface of the rotor 222 and the inner surface of the stator 227 creating a localized high shear condition. The gaps 225, 235, 245 generate high shear forces that process the feed stream 205. The high shear forces between the rotor and stator functions to process the feed stream 205 to create the product dispersion 210. Each generator 220, 230, 240 of the high shear device 200 has interchangeable rotor-stator combinations for producing a narrow distribution of the desired bubble size, if feedstream 205 comprises a gas, or globule size, if feedstream 205 comprises a liquid, in the product dispersion 210.

[0029] The product dispersion 210 of gas particles, or bubbles, in a liquid comprises an emulsion. In embodiments, the product dispersion 210 may comprise a dispersion of a previously immiscible or insoluble gas, liquid or solid into the continuous phase. The product dispersion 210 has an average

gas particle, or bubble, size less than about 1.5  $\mu\text{m}$ ; preferably the bubbles are sub-micron in diameter. In certain instances, the average bubble size is in the range from about 1.0  $\mu\text{m}$  to about 0.1  $\mu\text{m}$ . Alternatively, the average bubble size is less than about 400 nm (0.4  $\mu\text{m}$ ) and most preferably less than about 100 nm (0.1  $\mu\text{m}$ ).

**[0030]** Tip speed is the velocity (m/sec) associated with the end of one or more revolving elements that is transmitting energy to the reactants. Tip speed, for a rotating element, is the circumferential distance traveled by the tip of the rotor per unit of time, and is generally defined by the equation  $V \text{ (m/sec)} = \pi \cdot D \cdot n$ , where  $V$  is the tip speed,  $D$  is the diameter of the rotor, in meters, and  $n$  is the rotational speed of the rotor, in revolutions per second. Tip speed is thus a function of the rotor diameter and the rotation rate.

**[0031]** For colloid mills, typical tip speeds are in excess of 23 m/sec (4500 ft/min) and can exceed 40 m/sec (7900 ft/min). For the purpose of the present disclosure the term 'high shear' refers to mechanical rotor-stator devices, such as mills or mixers, that are capable of tip speeds in excess of 5 m/sec (1000 ft/min) and require an external mechanically driven power device to drive energy into the stream of products to be reacted. A high shear device combines high tip speeds with a very small shear gap to produce significant friction on the material being processed. Accordingly, a local pressure in the range of about 1000 MPa (about 145,000 psi) to about 1050 MPa (152,300 psi) and elevated temperatures at the tip of the shear mixer are produced during operation. In certain embodiments, the local pressure is at least about 1034 MPa (about 150,000 psi). The local pressure further depends on the tip speed, fluid viscosity, and the rotor-stator gap during operation.

**[0032]** An approximation of energy input into the fluid (kW/l/min) can be made by measuring the motor energy (kW) and fluid output (l/min). In embodiments, the energy expenditure of a high shear device is greater than 1000 W/m<sup>3</sup>. In embodiments, the energy expenditure is in the range of from about 3000 W/m<sup>3</sup> to about 7500 W/m<sup>3</sup>. The high shear device **200** combines high tip speeds with a very small shear gap to produce significant shear on the material. The amount of shear is typically dependent on the viscosity of the fluid. The shear rate generated in a high shear device **200** may be greater than 20,000 s<sup>-1</sup>. In embodiments, the shear rate generated is in the range of from 20,000 s<sup>-1</sup> to 100,000 s<sup>-1</sup>.

**[0033]** The high shear device **200** produces a gas emulsion capable of remaining dispersed at atmospheric pressure for at least about 15 minutes. For the purpose of this disclosure, an emulsion of gas particles, or bubbles, in the dispersed phase in product dispersion **210** that are less than 1.5  $\mu\text{m}$  in diameter may comprise a micro-foam. Not to be limited by a specific theory, it is known in emulsion chemistry that sub-micron particles, or bubbles, dispersed in a liquid undergo movement primarily through Brownian motion effects. The bubbles in the emulsion of product dispersion **210** created by the high shear device **200** may have greater mobility through boundary layers of solid catalyst particles, thereby facilitating and accelerating the catalytic reaction through enhanced transport of reactants.

**[0034]** The rotor is set to rotate at a speed commensurate with the diameter of the rotor and the desired tip speed as described hereinabove. Transport resistance is reduced by incorporation of high shear device **200** such that the velocity of the reaction is increased by at least about 5%. Alternatively, the high shear device **200** comprises a high shear colloid mill

that serves as an accelerated rate reactor. The accelerated rate reactor comprises a single stage dispersing chamber. The accelerated rate reactor comprises a multiple stage inline disperser comprising at least 2 stages.

**[0035]** Selection of the high shear device **200** is dependent on throughput requirements and desired particle or bubble size in the outlet dispersion **210**. In certain instances, high shear device **200** comprises a Dispax Reactor® of IKA® Works, Inc. Wilmington, N.C. and APV North America, Inc. Wilmington, Mass. Model DR 2000/4, for example, comprises a belt drive, 4M generator, PTFE sealing ring, inlet flange 1" sanitary clamp, outlet flange ¾" sanitary clamp, 2HP power, output speed of 7900 rpm, flow capacity (water) approximately 300 l/h to approximately 700 l/h (depending on generator), a tip speed of from 9.4 m/s to about 41 m/s (about 1850 ft/min to about 8070 ft/min). Several alternative models are available having various inlet/outlet connections, horsepower, tip speeds, output rpm, and flow rate.

**[0036]** Without wishing to be limited to a particular theory, it is believed that the level or degree of high shear mixing is sufficient to increase rates of mass transfer and may also produce localized non-ideal conditions that enable reactions to occur that would not otherwise be expected to occur based on Gibbs free energy predictions. Localized non ideal conditions are believed to occur within the high shear device resulting in increased temperatures and pressures with the most significant increase believed to be in localized pressures. The increase in pressures and temperatures within the high shear device are instantaneous and localized and quickly revert back to bulk or average system conditions once exiting the high shear device. In some cases, the high shear mixing device induces cavitation of sufficient intensity to dissociate one or more of the reactants into free radicals, which may intensify a chemical reaction or allow a reaction to take place at less stringent conditions than might otherwise be required. Cavitation may also increase rates of transport processes by producing local turbulence and liquid micro-circulation (acoustic streaming). An overview of the application of cavitation phenomenon in chemical/physical processing applications is provided by Gogate et al., "Cavitation: A technology on the horizon," *Current Science* 91 (No. 1): 35-46 (2006). The high shear mixing device of certain embodiments of the present system and methods is operated under what are believed to be cavitation conditions effective to dissociate the benzene into free radicals exposed to chlorination catalysts for the formation of the chlorobenzene product.

#### Description of High Shear Chlorobenzene Production Process and System

**[0037]** The high shear chlorobenzene production process and system of the present disclosure will now be described in relation to FIG. 2 which is a representative process flow diagram of a high shear system (HSS) **100** for the production of chlorobenzene from benzene and chlorine gas. FIG. 2 illustrates the basic components of a representative high shear chlorobenzene production system. These components comprise pump **5**, high shear mixer **40**, and reactor **10**.

**[0038]** Pump **5** is used to provide a controlled flow through-out high shear device (HSD) **40** and high shear system **100** for chlorobenzene production. Pump inlet stream **21** comprises liquid benzene for introduction to pump **5**. In certain embodiments, pump inlet stream **21** comprises dry benzene. Pump **5** increases the pressure of the pump inlet stream **21** to greater than about 203 kPa (about 2 atm); alternatively, the inlet

stream **21** is pressurized to greater than about 304 kPa (about 3 atm). Additionally, pump **5** may build pressure throughout HSS **100**. In this way, HSS **100** combines high shear with pressure to enhance reactant intimate mixing. Preferably, all contact parts of pump **5** are stainless steel, for example, 316 stainless steel. Pump **5** may be any suitable pump, for example, a Dayton Pressure Booster Pump Model 2P372E, Dayton Electric Co (Niles, Ill.).

**[0039]** The pressurized benzene liquid exits pump **5** via pump exit stream **12**. Pump exit stream **12** is in fluid communication with HSD inlet stream **13**. In certain instances, dispersible gas stream **22** comprising chlorine gas is introduced or injected to HSD inlet stream **13**. In some embodiments chlorine gas may continuously be fed into exit stream **12** to form HSD inlet stream **13**. HSD inlet stream **13** comprises a mixture of chlorine gas and catalyst in liquid benzene. Dispersible gas stream **22** and pressurized pump exit stream **12** may be injected separately into HSD inlet stream **13** for processing by high shear device **40**. Furthermore, any suitable chlorination catalyst known to those of skill in the art may be introduced into HSD inlet stream **13** for processing by HSD **40**. In certain instances, the catalyst introduced comprises a Lewis acid catalyst. The catalyst may be chosen from metallic chlorides and iodine. In embodiments, the catalyst is selected from Lewis acids selected from the group consisting of Fe, FeCl<sub>3</sub>, and AlCl<sub>3</sub>. HSD inlet stream **13** is in fluid communication with the high shear device **40**.

**[0040]** HSD **40** serves to intimately mix the liquid benzene solution with dispersible gas stream **22** and the catalyst. As discussed in detail above, high shear device **40** is a mechanical device that utilizes, for example, a stator rotor mixing head with a fixed gap between the stator and rotor. In high shear device **40**, chlorine gas and benzene are mixed to form an emulsion comprising microbubbles and nanobubbles of chlorine gas. In embodiments, the resultant dispersion comprises bubbles in the submicron size. In embodiments, the resultant dispersion has an average bubble size less than about 1.5 μm. In embodiments, the mean bubble size is less than from about 0.1 μm to about 1.5 μm. Not to be limited by a specific method, it is known in emulsion chemistry that submicron particles dispersed in a liquid undergo movement primarily through Brownian motion effects. Thus it is believed that submicron gas particles created by the high shear device **40** have greater mobility through boundary layers of solid catalyst particles thereby facilitating and accelerating the catalytic reaction through greater transport of reactants. In embodiments, the high shear mixing produces gas bubbles capable of remaining dispersed at atmospheric pressure for about 15 minutes or longer depending on the bubble size. In embodiments, the mean bubble size is less than about 400 nm; more preferably, less than about 100 nm. HSD **40** serves to create an emulsion of chlorine bubbles within high shear inlet stream **13** comprising aqueous aldehydes and chlorine gas. The emulsion may further comprise a microfoam.

**[0041]** The emulsion exits HSD **40** by the HSD emulsion stream **18**. The HSD emulsion stream **18** may undergo further processing prior introduction to the reactor **10**. Before introduction to reactor **10**, the moisture content of benzene may be reduced. In certain embodiments, the benzene in HSD emulsion stream **18** comprises dry benzene. HSD emulsion stream **18** is introduced into reactor **10** by reactor inlet stream **19**. Reactor inlet stream **19** is in fluid communication with reactor **10**.

**[0042]** Forming the emulsion in the presence of a catalyst may initiate the reaction process of chlorination. Chlorination reactions will occur whenever suitable time temperature and pressure conditions exist. In instances where a slurry based catalyst is utilized, reaction is more likely to occur at points outside reactor **10**. In this sense chlorination could occur at any point in the flow diagram of FIG. **2** where temperature and pressure conditions are suitable for the reaction. Nonetheless a discrete reactor **10** is often desirable to allow for increased residence time, agitation and heating and/or cooling. In fixed bed catalyst applications, the catalyst increases the rate of the chlorination reaction.

**[0043]** Reactor **10** is configured for chlorobenzene production. Reactor **10** may further comprise temperature control (i.e. heat exchanger), stirring system, and level regulator as known to those of skill in the art. In embodiments, inlet stream **15** is fluidly coupled to the reactor **10**. Inlet stream **15** may comprise additional catalyst for catalyzing the chlorination of benzene to chlorobenzene. As described herein, a Lewis acid may be added to promote the production of chlorobenzene. In certain embodiments, in the reactor **10**, chlorine gas in reacts with dry benzene utilizing a Lewis acid catalyst at a predetermined temperature to yield chlorobenzene mixtures. In embodiments, chlorobenzene production is continuous within the reactor. The reactor **10** is drained by product stream **16**.

**[0044]** A specified reaction temperature may be maintained in the reactor **10**, as known to those of skill in the art. In certain embodiments, the reactor includes internally or externally positioned heat exchangers. Alternatively, heat exchangers may be positioned in any location along the production stream within HSS **100**. Suitable locations for external heat transfer devices include between the pump **5** and the high shear mixer **40**, between the high shear mixer **40** and the reactor **10**, and between the reactor and further processing systems. There are many types of heat transfer devices that may be suitable; such exchangers might include shell and tube, plate, and coil heat exchangers without limitation. Further heat exchangers may be known to one skilled in the art.

**[0045]** The chlorination product stream **16** comprises chlorobenzene, unconverted benzene, and HCl. Product stream **16** may be treated by any means known in the art to recover any unreacted benzene, remove produced HCl, and purify chlorinated benzene. In an embodiment illustrated in FIG. **2**, product stream **16** is fluidly coupled a treatment system **99**. Treatment system **99** comprises treatment vessel **30**; the treatment vessel **30** is fluidly coupled to reactor **10** by product stream **16**. Further, the treatment vessel **30** is drained by catalyst free stream **32** to a holding tank **50**. Holding tank **50** stores the catalyst free chlorobenzene product prior to further treatment. In the illustrated embodiment, holding tank **50** is in fluid communication with a chlorobenzene distillation column(s) **60** via distillation inlet stream **33**. The chlorobenzene distillation column(s) **60** are in fluid connection with further processing streams **80** by the chlorobenzene stream **65**. Chlorobenzene distillation column(s) **60** may be further in communication with a reflux drum **90**, by gas recycle system **62**. Gas recycle system **62** is fluid communication between reflux drum **90** and chlorobenzene distillation column(s) **60**. In certain instances, reflux drum **90** is in fluidly coupled to treatment vessel **30** by water stream **92**. Reflux drum **90** additionally comprises recovered benzene stream **95** in fluid communication with secondary distillation column(s) **70**. Secondary distillation column(s) **70** may drain benzene hold-

ing tank **130** via stream **71** to feed recycle stream **20**. Recycle stream **20** is fluidly coupled to pump inlet stream **21**.

**[0046]** Treatment vessel **30** comprises a tank, vessel, or container configured for acid and catalyst removal. In embodiments, the acid and catalyst from product stream are removed with water before introduction to holding tank **50**. The products comprising chlorobenzene from holding tank **50** are fed into chlorobenzene distillation column(s) **60**. Chlorobenzene stream **65** is removed for further processing into final products such as rubber, dyes, pesticides, and the like, without limitation. Alternatively, Chlorobenzene stream **65** may be sent for further separation, for example to a distillation column wherein monochlorobenzene may be separated from other chlorobenzene isomers, such as paradichlorobenzene, orthodichlorobenzene, and trichlorobenzene.

**[0047]** In certain embodiments, treatment vessel **30** is in fluid communication with solvent recovery system **110**. Water is drained from treatment vessel **30**, with dissolved acids and catalyst, and is sent via stream **105** to the solvent recovery system **110** for further removal of the organics from the water.

**[0048]** Benzene-containing vapor in the gas recycle system **62** is directed from distillation column **60**, condensed, and sent to reflux drum **90**. In embodiments, a portion of benzene from reflux drum **90** is recycled to distillation column(s) **60** by gas recycle system **62**. Water stream **92** may be removed from reflux drum **90** for return to treatment vessel **30** and/or continuing processing by solvent recovery system **110**. A portion of recovered benzene stream **95**, from reflux drum **90**, may be supplemented by wet benzene from holding tank **130**. The stream **71** is sent to secondary distillation column(s) **70** with recovered benzene stream **95** to produce dry benzene. The dry benzene makes up recycle stream **20**, and may be injected into pump inlet stream **21** for recycling through the high shear system, comprising the high shear device **40**.

**[0049]** In embodiments, use of the disclosed process comprising reactant mixing via high shear device **40** allows greater conversion of benzene to chlorobenzene and/or an increase in throughput. In embodiments, there may be several high shear devices **40** used in series. In embodiments, the method comprises incorporating high shear device **40** into an established process thereby enabling the increase in production (greater throughput) from a process operated without high shear device **40**. The superior dissolution provided by the high shear mixing may allow improvements in operating conditions such as temperature, pressure, and contact time while maintaining, or increasing, reaction rate. In embodiments, the method and system of this disclosure enable design of a smaller and/or less capital intensive process than previously possible without the incorporation of external high shear mixer **40**. In embodiments, the disclosed method reduces operating costs/increases production from an existing process. Alternatively, the disclosed method may reduce capital costs for the design of new processes. Potential benefits of this modified system and method for the production of chlorobenzene include, but are not limited to, faster cycle times, increased throughput, reduced operating costs, and/or reduced capital expense due to the possibility of designing smaller reactors and/or operating the chlorobenzene production at lower temperature and/or pressure.

**[0050]** While preferred embodiments of the invention have been shown and described, modifications thereof can be made by one skilled in the art without departing from the spirit and teachings of the invention. The embodiments described

herein are exemplary only, and are not intended to be limiting. Many variations and modifications of the invention disclosed herein are possible and are within the scope of the invention. Where numerical ranges or limitations are expressly stated, such express ranges or limitations should be understood to include iterative ranges or limitations of like magnitude falling within the expressly stated ranges or limitations (e.g., from about 1 to about 10 includes, 2, 3, 4, etc.; greater than 0.10 includes 0.11, 0.12, 0.13, and so forth). Use of the term "optionally" with respect to any element of a claim is intended to mean that the subject element is required, or alternatively, is not required. Both alternatives are intended to be within the scope of the claim. Use of broader terms such as comprises, includes, having, etc. should be understood to provide support for narrower terms such as consisting of, consisting essentially of, comprised substantially of, and the like.

**[0051]** Accordingly, the scope of protection is not limited by the description set out above but is only limited by the claims which follow, that scope including all equivalents of the subject matter of the claims. Each and every claim is incorporated into the specification as an embodiment of the present invention. Thus, the claims are a further description and are an addition to the preferred embodiments of the present invention. The discussion of a reference in the Description of Related Art is not an admission that it is prior art to the present invention, especially any reference that may have a publication date after the priority date of this application. The disclosures of all patents, patent applications, and publications cited herein are hereby incorporated by reference, to the extent they provide exemplary, procedural or other details supplementary to those set forth herein.

We claim:

1. A method for producing chlorobenzene, comprising:  
obtaining a high shear device having at least one rotor/  
stator set configured for producing a tip speed of at least  
5 m/s, wherein the high shear device comprises at least  
one rotor and at least one stator;  
forming an emulsion of benzene and chlorine gas; wherein  
said benzene comprises a pressurized liquid solution,  
and said chlorine gas comprises bubbles in the emulsion  
with a mean diameter of less than about 5  $\mu\text{m}$ ;  
introducing said emulsion into a reactor comprising a cata-  
lyst; and  
reacting said emulsion at a temperature less than about 40°  
C. in said reactor, from which a product comprising  
chlorobenzene is removed.
2. The method of claim 1 said pressurized benzene solution  
is pressurized to least about 203 kPa.
3. The method of claim 1 wherein said chlorine gas bubbles  
have an average diameter of less than about 1.5  $\mu\text{m}$ .
4. The method of claim 1 wherein said high shear device  
has a tip speed of at least about 5 m/s.
5. The method of claim 4 wherein said high shear device  
produces a localized pressure of about 1000 MPa at the tip.
6. The method of claim 1 wherein forming said emulsion  
comprises subjecting said oxidant gas bubbles and pressur-  
ized aqueous solution to a shear rate of greater than about  
20,000  $\text{s}^{-1}$ .
7. The method of claim 1 wherein forming said emulsion  
comprises an energy expenditure of at least 1000  $\text{W}/\text{m}^3$ .
8. The method of claim 1 wherein the emulsion comprises  
a micro-foam.

9. The method of claim 1 wherein the catalyst comprises one chosen from the group consisting of Lewis acids, metallic chlorides, iodine, or combinations thereof.

10. The method of claim 1, further comprising treating the product with hydrochloric acid.

11. The method of claim 10, further comprising distilling the product at least once to remove the chlorobenzene.

12. A method for producing chlorobenzene, the method comprising:

forming an emulsion of chlorine gas bubbles in aqueous solution comprising benzene by introducing liquid benzene and chlorine gas into a high shear device and subjecting the mixture of liquid benzene and chlorine gas to a shear rate of at least  $20,000 \text{ s}^{-1}$ .

13. The method of claim 12 wherein the high shear device comprises at least one rotor and at least one stator.

14. A system for the production of chlorobenzene, the system comprising;

a pump positioned upstream of a dispersible chlorine gas inlet;

a high shear device which produces an emulsion of chlorine gas in an aqueous solution, the dispersion having an average bubble diameter of less than about  $5 \mu\text{m}$ ; and a reactor maintained at a temperature of less than about  $40^\circ \text{C}$ . for the chlorination reaction of benzene to chlorobenzene; the reactor fluidly connected to the outlet of the high shear device.

15. The system of claim 14 wherein the high shear device is configured to produce an emulsion.

16. The system of claim 14 wherein the high shear device comprises a tip speed of at least about  $5 \text{ m/sec}$ .

17. The system of claim 14 wherein said high shear device produces a localized pressure of at least about  $1000 \text{ MPa}$  at the tip.

18. The system of claim 14 wherein said high shear device subjects said oxidant gas bubbles and pressurized aqueous solution to a shear rate of greater than about  $20,000 \text{ s}^{-1}$ .

19. The system of claim 14 wherein said high shear device comprises an energy expenditure of at least  $1000 \text{ W/m}^3$ .

20. The system of claim 14 wherein said high shear feed stream comprises a micro-foam.

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