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EP 0 246 105 B1

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Description

This invention concerns recovering coal from aqueous slurries of coal fines also containing associated impurities as suspended fine solids and compositions of use in the recovery process.

Coal as mined (run-of-mine coal) contains a proportion of impurities (hereinafter called 'shale') and, in the case of the fine particles present, separation of the coal from the shale presents considerable problems. In the case of mines where modern, mechanical extraction techniques are used, typically a proportion as high as about 20% of the run-of-mine coal consists of particles smaller than 0.5 mm. This fine 'coal' typically has a substantial coal content but also a substantial shale content so it is important to make use of the coal content but also to remove shale from it. Modern coal preparation processes result in the fines (separated from coarser material) being in the form of aqueous slurries.

In the United Kingdom the usual way of separating coal fines from shale fines in aqueous slurries is by means of froth flotation followed by filtration. However, the efficiency of this process is seriously affected by the presence of ultra-fine (of less than about 50 microns) matter (both coal and shale), often present in significant proportions in the material requiring treatment.

When froth flotation is not used, the usual separation technique applied to the aqueous slurry of fines is to pass the slurry through a hydrocyclone and then feed the hydrocyclone underflow to a screen having apertures of about 0.25 mm. The "product" i.e. coal fines with a reduced proportion of shale fines is the matter retained by the screen whilst the hydrocyclone overflow and the matter passing through the screen are discarded. A consequent disadvantage is that the significant proportion of the coal having particle sizes below 0.25 mm is lost.

Another technique that has been proposed for separating coal fines from shale fines in aqueous slurries is oil agglomeration. In this process coal fines are selectively agglomerated, with respect to shale fines, by use of an oil "binder" and the coal agglomerates are then separated from the shale fines by a screening or classification process. However, the process has the disadvantage of requiring a substantial proportion of oil in relation to the solids in the slurry being treated.

EP-A-0166897 describes a process for beneficiating oxidised coal by froth flotation in which modified coal, produced by a subjecting coal having oxidised surfaces to high shear agitation in water and desliming the resulting aqueous coal mixture, is introduced to a surface treating mixture comprised of a polymerisable monomer having the formula $XHC = CHX'$, a catalyst and a liquid organic carrier. An aqueous coal slurry is admixed with a surface treating mixture under polymerisation conditions and the resultant surface treated coal is rendered hydrophobic.

According to the present invention there is provided a method of recovering coal fines from an aqueous slurry also containing shale as suspended fine solids in which the coal fines are rendered hydrophobic, the resulting mixture is agitated, gas is introduced into the slurry to form bubbles whereby flocs of coal fines formed are caused to float, and the underlying slurry containing shale is discarded characterised in that the coal fines are rendered hydrophobic by the addition to the slurry of a hydrophobic polyvinylether in a liquid organic carrier.

It has been found in accordance with the invention that coal fines can be flocculated efficiently by use of hydrophobic polyvinylethers and that the flocculation is highly selective for coal fines in preference to shale fines. Thus in the above method flocs of coal fines are formed selectively in preference to flocs of shale fines and a high degree of selectivity can be achieved. The agglomeration of the coal fines into flocs reduces the exposed surface area of the coal and thereby reduces entrainment of shale fines with the coal. Moreover, the coal fines can be formed into flocs of sufficient strength to survive vigorous agitation of the slurry and by agitation of the slurry the flocs of coal fines can be caused to 'extrude' shale fines and water that may initially have been entrained within the flocs.

It has been found that if gas is not introduced into the mixture and bubbles formed causing flocs of coal fines formed to float, little separation of coal and shale is achieved and the sediment contains coal and shale fines in proportion not greatly different from the original ones and there is little distinction between different levels of the sediment. It is thought that the reason for this is that as the flocs of coal fines descend in the slurry they entrain shale fines and thus the benefit of selective flocculation of the coal fines is lost to a greater or lesser extent. The introduction of the gas e.g. air and formation of the bubbles may be effected by sufficiently vigorous agitation of the mixture or a specific device may be used to introduce gas into the mixture and form the bubbles.

It is much preferred that the method of the invention should be performed as a froth flotation in a froth flotation cell, using, in addition to polyvinylether and carrier, a frother, as used in conventional froth flotation processes. When the method is performed in this manner the organic liquid not only acts as a carrier for the polyvinylether but it also acts as a so-called collector in the conventional froth flotation sense. When the

method is conducted in this manner high selectivity is easily retained but with the advantage that greatly reduced dosage rates of polyvinylether are effective. In the froth flotation form of the method, the polyvinylether dosage may be as low as say 0.5 kg/tonne of slurry solids. Moreover as with the method in general, high yields are obtainable i.e. not only is the method highly selective as between coal fines and shale fines but also a high proportion of the coal fines, particularly those of very low particle sizes (less than about 50 microns) can be recovered.

Polyvinylethers have been found to be particularly satisfactory in the case of the more aliphatic coals e.g. steam coals.

Gas oil has been found to be a particularly satisfactory carrier for the polyvinylether. Examples of other carriers that may be used include diesel oil, and kerosene and other petroleum and coal-based distillates. To aid solution of the polyvinylether in the liquid a co-solvent compatible with the carrier may be used. Examples of co-solvents that may be used include toluene, xylenes and other aromatic solvents and hexane and other paraffinic solvents. Co-solvents may be particularly useful if the polyvinylether is of high molecular weight.

The efficiency of the method is dependent on the dosage rate of the polyvinylether in relation to the solids in the slurry. In a simple form of the method (not involving froth flotation) some recovery of the coal fines may be achieved with a dosage rate as low as for example, 2.45 kg. polyvinylether/tonne of slurry solids but under the same conditions an almost double dosage rate of 4.71 gave far superior results. The optimum dosage rate in any particular case is that just sufficient to cause effective flocculation of substantially all the coal fines. Whilst high selectivity may be retained with lesser rates, only partial recovery of the coal fines is then achievable. Rates higher than the optimum are simply wasteful of the polyvinylether.

It has been found that it is not the liquid, organic carrier e.g. gas oil alone that yields the good results in the method of the invention. In general, if e.g. gas oil is used without a hydrophobic polyvinylether, the selectivity is largely lost and in the case of a froth flotation method, use of gas oil and a conventional frother but no hydrophobic polyvinylether results in a low yield i.e. the coal fines are not efficiently flocculated.

According to a further aspect of the invention, an additive composition for use in the froth flotation method of the invention comprises 5 - 25% of hydrophobic polyvinylether, 5 - 25% of frother and 50 - 90% of liquid organic carrier, all by weight. The frother may be as in the known froth flotation process, and may be for example methyl isobutyl carbinol or a mixture of polypropylene glycol ethers available under the tradename TEEFROTH G. The composition is preferably used in an amount not greater than 10 kg per tonne of slurry solids, especially 0.5 - 5 kg per tonne.

The method of the invention gives rise to a secondary advantage in that the coal flocs formed are more readily filtered than coal fines which have not been flocculated. Moreover, not only can the filtration be carried out more quickly but also it gives rise to a coal residue having the advantage of a lower water content. These effects are thought to result from the formation of relatively large coal flocs having fully hydrophobic surfaces and low shale content.

The method of the invention is applicable to coal/shale slurries of the types that in the past have been subjected to conventional froth flotation processes. In such slurries the size of the coal and shale particles is usually less than 500 microns and commonly up to 50% by weight of the particles can have sizes less than 50 microns.

The presence of substantial proportions of ultra-fine particles e.g. less than 50 microns seriously impairs the efficiency of the conventional froth flotation process. By use of a hydrocyclone a typical feed for a conventional froth flotation process can be split into two fractions, one containing particles of predominantly 50 microns and upwards and the other particlespredominantly less than 50 microns. The fraction containing the larger particles may then be treated by a conventional froth flotation process with increased efficiency whilst the method of the invention is especially well suited to the treatment of the fraction containing the smaller particles.

The invention is illustrated by the following examples, in which some of the processes described are not according to the invention and are included for comparison purposes.

EXAMPLE 1

Experiments were carried out on a synthetic aqueous coal/shale slurry containing equal weights of coal and shale fines and having a solids content of 5% by weight. The ash content of the solids was 46% by weight. Of the solids, 80% by weight were of particle sizes less than 63 microns.

Three different treatment processes were applied to the slurry. In Process I the chosen additive was added to a sample of the slurry in a separating funnel and the mixture stirred at a low speed such that

thorough mixing occurred but there was substantially no creation of air bubbles in the slurry. The stirring was then discontinued, solids allowed to sediment out, the sediment separated from the slurry above and both the sediment and the overlying slurry collected, the sediment returned to the funnel, water added and the resultant mixture again stirred slowly, the stirring again discontinued and solids again allowed to sediment out and the sediment separated from the overlying slurry and both collected. The sediment was filtered, dried and weighed (to determine the product yield of the process) and then burnt and reweighed (to determine the ash content of the product). The two portions of collected separated slurry were separately filtered and the residues dried, weighed and burnt (to determine their ash contents).

In Process II the above process was generally repeated but using high speed stirring such that numerous air bubbles were created in the slurry and caused solids to float rather than sediment out. Accordingly in this process on each of the two occasions the underlying slurry was separated from the floated-out solids rather than the sediment being separated from the overlying slurry.

In Process I and II sodium hexametaphosphate was included in the initial slurry as shale dispersant at a concentration of 2.5% by weight.

In Process III the chosen additive was added to a sample of the slurry and the mixture then subjected to froth flotation using froth flotation apparatus of the Leeds cell design. The floated-out matter was separated from the underlying slurry and the latter collected and the former returned with added water to the Leeds cell which was then operated again. The floated-out matter was again separated from the underlying slurry and both collected. The floated-out matter was filtered, dried and weighed (to determine the product yield) and burnt and re-weighed (to determine the ash content of the product). The two portions of collected separated slurry were separately filtered and the residues dried, weighed and burnt.

The experimental data is given in Table 1.

TABLE 1

Example	Additive (kg./tonne slurry solids)			Process	Product		1st Tailings ash (%)	2nd Tailings ash (%)
	polyvinyl ether Polymers	Gas Oil	Frother		Yield(%)	Ash(%)		
1.1	4.84(A25)	10.62	-	I	37.9	23.47	63.3	47.6
1.2	4.15(130)	21.63	-	I	30.9	23.6	56.1	53.4
1.3	2.45(A25)	5.39	-	II	13.3	5.45	52.2	69.9
1.4	4.71(A25)	10.34	-	II	30.6	6.52	62.9	84.2
1.5	4.04(130)	20.98	-	II	51.0	7.56	85.9	86.2
1.6	-	25	-	II	55.6	24.4	74.1	59.8
1.7	0.53(A25)	1.17	0.2	III	52.8	9.01	90.7	84.8
1.8	0.54(130)	2.80	0.2	III	48.6	6.24	89.8	63.8
1.9	-	3.33	0.2	III	34.2	7.78	79.3	34.3

In the Table 'A25' and '130' signify a polyvinyl ethyl ether and a polyvinyl isobutyl ether available under the tradenames Lutonal A25 and Lutonal 130 respectively from BASF United Kingdom Limited. These are hydrophobic polymers. In the Table 'frother' signifies the known frother methyl isobutyl carbinol. First and second 'tailings' in the Table refer to the solids respectively in the initially and subsequently separated slurries. In connection with the figures for 'yield', it should be noted that the theoretical maximum for the

yield of coal is 50%, as half the weight of the initial slurry solids is coal and the other half shale.

Example 1.6 in the Table is shown as being conducted according to Process II. However, although high speed stirring was used such that numerous air bubbles were created in the slurry, the solids sedimented out rather than floated and thus the separation steps were conducted in accordance with Process I rather than Process II.

Examples 1.1 and 1.2, which use Process I, are included only for comparison purposes. The product ash contents are high, signifying a substantial proportion of shale in the product. Example 1.3, which uses Process II, gives a much lower ash content but the yield is low. Example 1.4, where the additive application rate is approximately doubled, gives a much higher yield but the ash content is still low. Examples 1.5, again using Process II, gives a good yield of low ash content and the high ash contents of the tailings signify that little coal is lost in the tailings. The contrast with Example 1.2 using Process I but otherwise generally similar is very marked.

Example 1.6 is included only for comparison purposes and shows that Process II is not effective in the absence of the polyvinylether: whilst the product yield is high, the product has a high ash i.e. shale content.

Examples 1.7 and 1.8, using Process III, give good yields with low ash contents and in comparison with Examples 1.4 and 1.5, using Process II and also using the same polyvinylethers and gas oil, the application rates of the polyvinylether and gas oil are very much lower.

Example 1.9, included only for comparison purposes, shows that if gas oil and frother are used in Process III without the polyvinylether a greatly reduced yield results.

EXAMPLE 2

Process IV, which was the same as Process III described in Example 1 except that froth flotation was done once instead of twice, was carried out on an aqueous coal/shale slurry from a coal preparation plant using in one series of experiments an additive composition according to the invention and in another series of experiments the froth flotation oil in current use on the plant at the time.

The ash content of the solids in the slurry was 36.5% by weight, and of the solids 69% by weight were of particle size less than 53 microns.

The composition of the additive was, by weight:-

- 60% gas oil
- 20% mixture of polypropylene glycol ethers (TEEFROTH G)
- 20% polyvinyl ethyl ether (LUTONAL A25)

A range of dosages comparable to normal practice was used for both the additive composition and the froth flotation oil, and in each experiment the flotation time was 180 seconds.

The results obtained are tabulated in Table 2 in which Combustible Recovery is defined as

$$\frac{(100 - \text{Wt.}\% \text{ Product Ash}) \times \text{Product Weight}}{(100 - \text{Wt.}\% \text{ Feed Ash}) \times \text{Feed Weight}} \times 100$$

TABLE 2

	Dosage (kg/tonne)	Product Ash wt %	Yield wt %	Combustible Recovery wt %	Tails Ash wt %
Additive Composition	0.82	14.3	16.4	21.9	40.1
	0.84	14.6	23.4	31.7	43.6
	1.16	15.4	43.5	58.5	54.6
	1.21	13.0	42.4	55.1	47.8
	1.43	15.3	52.8	69.1	57.6
	2.09	16.7	60.8	80.0	67.6
Froth Flotation Oil	0.67	17.6	21.9	27.9	40.5
	0.90	20.1	34.7	44.1	46.2
	1.04	20.6	39.5	49.3	46.7
	1.21	18.6	39.6	50.5	47.8
	1.49	20.3	46.8	57.9	48.9
	1.96	19.9	53.9	67.8	55.5

The results obtained using the additive composition are, over the range of dosages investigated, superior to those obtained using the conventional froth flotation oil, and particularly at high dosages are characterised by higher weight yields and lower product ash contents. For example at a dosage of 1.21 kg ash is reduced by 5.6% by weight and the yield increased by 2.8% by weight.

EXAMPLE 3

Process IV as described in Example 2 was carried out on a sample of particle size less than 105 microns screened from a run-of-mine coal/shale slurry in which the particle size of the solids was less than 500 microns. The ash content of the solids in the sample was 45% by weight. 86% by weight of the solids

EP 0 246 105 B1

in the sample had a particle size of less than 20 microns and an ash content of 46.4% by weight, and the remaining 14% by weight contained 30% by weight ash.

The additive composition described in Example 2 was compared with a proprietary froth flotation oil used in a conventional froth flotation process.

The results obtained are tabulated in Table 3.

TABLE 3

	Additive Composition	Froth Flotation Oil	Froth Flotation Oil
Dosage kg/tonne	0.25	0.25	0.65
Flotation Time (secs)	120	360	120
Product Ash (% wt)	17.0	19.6	20.6
Yield (% wt)	54.0	34.0	45.2
Tails Ash (% wt)	80.9	60.2	68.9
Combustible Recovery (% wt)	83.6	51.0	67.0

Columns 2 and 3 of Table 3 represent optimum results for the additive composition and for the froth flotation oil respectively at a dosage level of 0.25 kg/tonne. The flotation time using the additive composition is lower but the additive composition also produces lower product ash and an appreciably higher yield. Column 4 shows that flotation time using the proprietary froth flotation oil can be reduced by increasing the amount of oil used. However, this results in an increase in the product ash, and the high yield value achieved using the additive composition is still not reached.

EXAMPLE 4

A bulk feed sample of a coal/shale slurry was screened at 500 microns. Part of the sample was retained for normal froth flotation for comparison purposes and the remainder was classified in a 5 cm hydrocyclone.

One part of the overflow from the cyclone was subjected to froth flotation using Process IV described in Example 2 and the additive composition described in Example 2, and another part of the overflow was similarly treated using the froth flotation oil normally used to treat the slurry in the mine.

The underflow was diluted with water to approximately 6% solids by weight and similar froth flotation treatments were carried out on portions of the diluted material to those carried out on the overflow material.

Froth flotation was also carried out on the retained screened feed sample using the froth flotation oil normally used to treat the particular coal/shale slurry in practice.

The results obtained are tabulated in Tables 4.1, 4.2 and 4.3. In the Tables AC signifies that the additive composition was used and FFO indicates that the froth flotation oil was used.

TABLE 4.1

UNDERFLOW - AFTER 45 SECS FLOTATION				
	DOSAGE (kg/tonne)	PRODUCT ASH (wt %)	YIELD (wt %)	COMBUSTIBLE RECOVERY (wt %)
FFO	0.210	7.58	18.85	33.25
AC	0.356	12.02	48.27	76.76
FFO	0.360	9.47	47.78	74.88
AC	0.551	13.66	54.76	86.39
FFO	0.700	13.69	56.67	86.96
AC	0.724	14.25	55.78	87.33
FFO	0.860	18.30	56.77	88.78
AC	1.047	14.21	60.90	91.09

EP 0 246 105 B1

TABLE 4.2

OVERFLOW - AFTER 45 SECS FLOTATION					
5		DOSAGE (kg/tonne)	PRODUCT ASH (wt %)	YIELD (wt %)	COMBUSTIBLE RECOVERY (wt %)
	AC	1.080	25.82	21.54	53.02
10	FFO	1.210	29.86	21.16	49.56
	AC	1.560	27.67	24.28	58.84
	FFO	1.600	30.92	23.15	53.56
	AC	1.890	28.51	23.42	56.14
15	FFO	2.210	33.27	25.00	54.75
	AC	2.480	29.34	26.44	62.63
	FFO	2.750	32.58	25.81	57.95
	AC	3.560	32.91	31.53	67.51

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COMPARISON OF SCREENED FEED AND UNDERFLOW USING FROTH FLotation OIL

	DOSAGE (kg/tonne)	FLotation TIME (s)	PRODUCT ASH (wt %)	YIELD (wt %)	COMBUSTIBLE RECOVERY (wt %)
UNDERFLOW	0.210	45	7.58	18.85	33.25
FEED	0.300	90	17.18	32.99	66.58
UNDERFLOW	0.360	45	9.47	47.78	74.88
FEED	0.500	90	21.71	43.39	82.07
UNDERFLOW	0.700	45	13.69	56.67	86.96
FEED	0.730	90	25.07	47.42	84.97
UNDERFLOW	0.860	45	18.30	56.77	88.78

TABLE 4.3

The results demonstrate the benefits to be obtained by using a hydrocyclone to split the feed for a conventional froth flotation into one fraction containing fine particles of a size predominantly less than 50 microns (overflow) and another fraction containing relatively coarse particles of a size predominantly in the range of 50 - 500 microns (underflow) and then treating the fraction containing the fines by the method of the invention and the other fraction by a conventional froth flotation process.

For the underflow froth flotation using the additive composition of the invention gave similar results to the conventional froth flotation using the froth flotation oil except at a high dosage level (greater than about 0.8 kg/tonne) at which level the additive composition produced a lower ash product. For the overflow while product ash levels remained relatively high using either the additive composition or the froth flotation oil, the

ash contents were up to 4% lower using the additive composition and weight yields were in general improved. The results in Table 4.3 show that the conventional froth flotation applied to the cyclone underflow i.e. feed slurry from which fine particles have been removed is more efficient at lower dosages of froth flotation oil than froth flotation applied to unclassified feed slurry.

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Claims

1. A method of recovering coal fines from an aqueous slurry also containing shale as suspended fine solids in which the coal fines are rendered hydrophobic, the resulting mixture is agitated, gas is introduced into the slurry to form bubbles whereby flocs of coal fines formed are caused to float, and the underlying slurry containing shale is discarded characterised in that the coal fines are rendered hydrophobic by the addition to the slurry of a hydrophobic polyvinylether in a liquid organic carrier.
2. A method according to Claim 1 characterised in that the hydrophobic polyvinylether is polyvinyl ether or polyvinyl isobutyl ether.
3. A method according to Claim 1 or Claim 2 characterised in that the liquid organic carrier is gas oil, diesel oil or kerosene.
4. A method according to any one of Claims 1 to 3 characterised in that a co-solvent compatible with the carrier is used to aid solution of polyvinyl ether.
5. A method according to Claim 4 characterised in that the co-solvent is an aromatic solvent.
6. A method according to Claim 5 characterised in that the aromatic solvent is toluene or xylene.
7. A method according to Claim 4 characterised in that the co-solvent is a paraffinic solvent.
8. A method according to Claim 7 characterised in that the paraffinic solvent is hexane.
9. A method according to any one of Claims 1 to 8 characterised in that a frother is used and the method is performed as a froth flotation in a froth flotation cell.
10. A method according to Claim 9 characterised in that the frother is methyl isobutyl carbinol or a mixture of polypropylene glycol ethers.
11. A method according to Claim 9 characterised in that an additive composition comprising 5 - 25% by weight of hydrophobic polyvinyl ether, 5 - 25% by weight of frother and 50 - 90% by weight of liquid organic carrier is used at up to 10 kg per tonne of slurry solids.
12. A method according to Claim 11 characterised in that the additive composition is used at 0.5 - 5 kg per tonne of slurry solids.
13. An additive composition for use in a method of recovering coal fines according to Claim 9 characterised in that the composition comprises 5 - 25% by weight of hydrophobic polyvinyl ether, 5 - 25% by weight of frother and 50 - 90% by weight of liquid organic carrier.

Revendications

1. Procédé pour récupérer les fines de charbon d'une dispersion aqueuse contenant aussi du schiste à l'état de solides fins en suspension, dans lequel les fines de charbon sont rendues hydrophobes, le mélange résultant est agité, du gaz est introduit dans la dispersion pour former des bulles de façon que les flocons de fines de charbon formés soient amenés à flotter et la dispersion sous-jacente contenant le schiste est rejetée, caractérisé en ce que les fines de charbon sont rendues hydrophobes par addition à la dispersion d'un éther polyvinylique hydrophobe dans un véhicule organique liquide.
2. Procédé suivant la revendication 1, caractérisé en ce que l'éther polyvinylique hydrophobe est l'éther polyvinyléthylique ou l'éther polyvinylisobutylique.

3. Procédé suivant la revendication 1 ou 2, caractérisé en ce que le véhicule organique liquide est le gazole, le combustible diesel ou le kérosène.
- 5 4. Procédé suivant l'une quelconque des revendications 1 à 3, caractérisé en ce qu'un cosolvant compatible avec le véhicule est utilisé pour favoriser la dissolution de l'éther polyvinylique.
5. Procédé suivant la revendication 4, caractérisé en ce que le cosolvant est un solvant aromatique.
- 10 6. Procédé suivant la revendication 5, caractérisé en ce que le solvant aromatique est le toluène ou le xylène.
7. Procédé suivant la revendication 4, caractérisé en ce que le cosolvant est un solvant paraffinique.
8. Procédé suivant la revendication 7, caractérisé en ce que le solvant paraffinique est l'hexane.
- 15 9. Procédé suivant l'une quelconque des revendications 1 à 8, caractérisé en ce qu'un moussant est utilisé et le procédé est exécuté comme flottation par mousse dans une cellule de flottation par mousse.
- 20 10. Procédé suivant la revendication 9, caractérisé en ce que le moussant est le méthylisobutylcarbinol ou un mélange d'éther polypropylèneglycolique.
11. Procédé suivant la revendication 9, caractérisé en ce qu'une composition d'additif comprenant 5 à 25% en poids d'éther polyvinylique hydrophobe, 5 à 25% en poids de moussant et 50 à 90% en poids de véhicule organique liquide est utilisée jusqu'à raison de 10 kg par tonne de solides de la dispersion.
- 25 12. Procédé suivant la revendication 11, caractérisé en ce que la composition d'additif est utilisée à raison de 0,5 à 5 kg par tonne de solides de la dispersion.
- 30 13. Composition d'additif à utiliser dans un procédé de récupération de fines de charbon suivant la revendication 9, caractérisée en ce que la composition comprend 5 à 25% en poids d'éther polyvinylique hydrophobe, 5 à 25% en poids de moussant et 50 à 90% en poids de véhicule organique liquide.

Patentansprüche

- 35 1. Verfahren zur Rückgewinnung von Feinkohle aus einer wäßrigen Trübe, die auch als feiner Feststoff verteilte Berge enthält, bei dem man Feinkohle hydrophobiert, das entstandene Gemisch rührt, zur Blasenbildung Gas in die Trübe einleitet, wodurch die gebildeten Feinkohleflocken zum Aufschwimmen gebracht werden, und die darunterliegende, Berge enthaltende Trübe verwirft, dadurch gekennzeichnet, daß die Feinkohle durch Zusatz eines hydrophoben Polyvinylethers in einem flüssigen organischen Träger zur Trübe hydrophobiert wird.
- 40 2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß der hydrophobe Polyvinylether Polyvinylether oder Polyvinylisobutylether ist.
- 45 3. Verfahren nach Anspruch 1 oder 2, dadurch gekennzeichnet, daß der flüssige organische Träger Gasöl, Dieselöl oder Kerosin ist.
- 50 4. Verfahren nach einem der Ansprüche 1 bis 3, dadurch gekennzeichnet, daß man zur Unterstützung der Auflösung des Polyvinylethers ein mit dem Träger verträgliches Hilfslösungsmittel verwendet.
5. Verfahren nach Anspruch 4, dadurch gekennzeichnet, daß das Hilfslösungsmittel ein aromatisches Lösungsmittel ist.
- 55 6. Verfahren nach Anspruch 5, dadurch gekennzeichnet, daß das aromatische Lösungsmittel Toluol oder Xylol ist.
7. Verfahren nach Anspruch 4, dadurch gekennzeichnet, daß das Hilfslösungsmittel ein paraffinisches

Lösungsmittel ist.

8. Verfahren nach Anspruch 7, dadurch gekennzeichnet, daß das paraffinische Lösungsmittel Hexan ist.

5 9. Verfahren nach einem der Ansprüche 1 bis 8, dadurch gekennzeichnet, daß ein Schäumer verwendet und das Verfahren als Schaumaufbereitung in einer Schaumflotationszelle durchgeführt wird.

10. Verfahren nach Anspruch 9, dadurch gekennzeichnet, daß der Schäumer Methylisobutylcarbinol oder ein Gemisch von Polypropylenglykolethern ist.

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11. Verfahren nach Anspruch 9, dadurch gekennzeichnet, daß man eine aus 5 - 25 Gew.-% hydrophobem Polyvinylether, 5 - 25 Gew.-% Schäumer und 50 - 90 Gew.-% flüssigem organischen Träger bestehende Zusatzzusammensetzung in einer Menge von bis zu 10 kg pro Tonne Trübefeststoffe einsetzt.

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12. Verfahren nach Anspruch 11, dadurch gekennzeichnet, daß man die Zusatzzusammensetzung in einer Menge von 0,5 - 5 kg pro Tonne Trübefeststoffe einsetzt.

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13. Zusatzzusammensetzung zur Verwendung bei einem Verfahren zur Rückgewinnung von Feinkohle nach Anspruch 9, dadurch gekennzeichnet, daß die Zusammensetzung aus 5 - 25 Gew.-% hydrophobem Polyvinylether, 5 - 25 Gew.-% Schäumer und 50 - 90 Gew.-% flüssigem organischen Träger besteht.

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