



(86) Date de dépôt PCT/PCT Filing Date: 2004/04/20
(87) Date publication PCT/PCT Publication Date: 2005/12/01
(45) Date de délivrance/Issue Date: 2012/01/03
(85) Entrée phase nationale/National Entry: 2006/10/11
(86) N° demande PCT/PCT Application No.: US 2004/012039
(87) N° publication PCT/PCT Publication No.: 2005/113141

(51) Cl.Int./Int.Cl. *B01J 29/85* (2006.01),
C07C 5/22 (2006.01), *C10G 45/00* (2006.01),
C10G 71/00 (2006.01)

(72) Inventeurs/Inventors:
GALPERIN, LEONID B. (DECEASED), US;
MCCALL, MICHAEL J., US;
KOCAL, JOSEPH A., US;
JAN, DENG-YANG, US

(73) Propriétaire/Owner:
UOP LLC, US

(74) Agent: MACRAE & CO.

(54) Titre : CATALYSEUR POUR L'OUVERTURE SELECTIVE DE PARAFFINES CYCLIQUES ET PROCEDE
D'UTILISATION DU CATALYSEUR

(54) Title: CATALYST FOR SELECTIVE OPENING OF CYCLIC PARAFFINS AND PROCESS FOR USING THE
CATALYST

(57) **Abrégé/Abstract:**

A catalyst and process using the catalyst for opening cyclic paraffins are described. The catalyst comprises a Group VIII metal component, a molecular sieve, a refractory inorganic oxide component and optionally a modifier component. Examples of the molecular sieve are MAPSOs, SAPOs, UZM-8 and UZM-15. Preferred Group VIII metals include platinum, palladium and rhodium while alumina is a preferred inorganic oxide. Finally, examples of the optional modifier are niobium, titanium and rare earth elements such as ytterbium.



(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property
Organization
International Bureau



(43) International Publication Date
1 December 2005 (01.12.2005)

PCT

(10) International Publication Number
WO 2005/113141 A1

(51) International Patent Classification⁷: **B01J 29/85**,
C10G 71/00, C07C 5/22, C10G 45/00

(21) International Application Number:
PCT/US2004/012039

(22) International Filing Date: 20 April 2004 (20.04.2004)

(25) Filing Language: English

(26) Publication Language: English

(71) Applicant (for all designated States except US): **UOP LLC** [US/US]; 25 EAST ALGONQUIN ROAD, DES PLAINES, Illinois 60016-6101 (US).

(72) Inventors; and

(75) Inventors/Applicants (for US only): **GALPERIN, Leonid, B.** [US/US]; UOP LLC, 25 E. ALGONQUIN ROAD, DES PLAINES, IL 60016-6101 (US). **MCCALL, Michael, J.** [US/US]; UOP LLC, 25 E. ALGONQUIN ROAD, DES PLAINES, IL 60016-6101 (US). **KOCAL, Joseph, A.** [US/US]; UOP LLC, 25 E. ALGONQUIN ROAD, DES PLAINES, IL 60016-6101 (US). **JAN, Deng-Yang** [US/US]; UOP LLC, 25 E. ALGONQUIN ROAD, DES PLAINES, IL 60016-6101 (US).

(74) Common Representative: **UOP LLC**; John G. Tolomei, Assistant Secretary-Patent Matters, 25 EAST ALGONQUIN ROAD, DES PLAINES, Illinois 60016-6101 (US).

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NA, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM, ZW.

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IT, LU, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Published:

— with international search report

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: CATALYST FOR SELECTIVE OPENING OF CYCLIC PARAFFINS AND PROCESS FOR USING THE CATALYST

(57) Abstract: A catalyst and process using the catalyst for opening cyclic paraffins are described. The catalyst comprises a Group VIII metal component, a molecular sieve, a refractory inorganic oxide component and optionally a modifier component. Examples of the molecular sieve are MAPSOs, SAPOs, UZM-8 and UZM-15. Preferred Group VIII metals include platinum, palladium and rhodium while alumina is a preferred inorganic oxide. Finally, examples of the optional modifier are niobium, titanium and rare earth elements such as ytterbium.

WO 2005/113141 A1

CATALYST FOR SELECTIVE OPENING OF CYCLIC PARAFFINS AND PROCESS FOR USING THE CATALYST

BACKGROUND OF THE INVENTION

[0001] This invention relates to a catalyst for the selective opening of cyclic
5 paraffins which comprises a Group VIII metal component, a molecular sieve, a
refractory oxide and optionally a modifier. This invention also relates to a process for
selective ring opening using the catalyst.

[0002] Olefins are used in various reactions to produce important chemical
compounds. Accordingly, demand for olefins is ever increasing and therefore new
10 processes or increased efficiencies in existing processes are required. One of the main
processes used in preparing light olefins is naphtha steam cracking. It is known that
the efficiency of steam cracking depends on the specific composition of the naphtha
feed. Specifically it has been demonstrated that converting naphthenes to acyclic
paraffins, e.g. n-paraffins significantly improves olefin yield from the steam cracker.
15 There is, therefore, a need for an improved ring opening catalyst.

[0003] Improved ring opening catalysts are also necessary because of increasing
demand for environmentally friendly products and clean burning high performance
fuels. In this case naphthene rings are opened to give acyclic paraffins which in turn
can be isomerized. These isomerized paraffins have improved characteristics than the
20 corresponding naphthenes.

[0004] An increased amount of paraffins is also required in providing
reformulated gasoline. Reformulated gasoline differs from the traditional product in
having a lower vapor pressure, lower final boiling point, increased content of
oxygenates, and lower content of olefins, benzene and aromatics.

25 [0005] Reduction in gasoline benzene content often has been addressed by
changing the cut point between light and heavy naphtha, directing more of the
potential benzene formers to isomerization instead of to reforming. No benzene is
formed in isomerization, wherein benzene is converted to C₆ naphthenes and C₆

naphthenes are isomerized toward an equilibrium mixture of cyclohexane and methylcyclopentane or converted to paraffins through ring opening. It is believed that such C₆ cyclics are preferentially adsorbed on catalyst sites relative to paraffins, and the cyclics thus have a significant effect on catalyst activity for isomerization of paraffins. Refiners thus face the problem of maintaining the performance of light-naphtha isomerization units which process an increased concentration of feedstock cyclics.

[0006] Catalysts which are useful for ring opening are known and include a high chloride platinum component dispersed on a refractory inorganic oxide which is described in US-A-5,463,155. US-A-5,811,624 describes a catalyst for the selective opening of 5 and 6 membered rings which consists of a transition metal catalyst selected from the group consisting of carbides, nitrides, oxycarbides, oxynitrides, and oxycarbonitrides. The transition metal is selected from the group consisting of metals from Group IVA, VA, VIA of the Periodic Table of the Elements. US-A-6, 235,962 B1 discloses a catalyst for ring opening which comprises a carrier consisting of alumina, a metal modifier selected from the group consisting of scandium, yttrium and lanthanum, and at least one catalytically active metal selected from the group consisting of platinum, palladium, rhodium, rhenium, iridium, ruthenium, and cobalt. US-A-5,382,730 discloses a process for ring opening and isomerization of hydrocarbons where the catalyst comprises an aluminosilicate zeolite such as Zeolite Y or Zeolite Beta and a hydrogenation component. US-A-5,345,026 discloses a process for conversion of cyclic hydrocarbons to non-cyclic paraffin hydrocarbons where the catalyst comprises a hydrogenation-dehydrogenation component and an acidic solid component comprising a group IVB metal oxide modified with an oxyanion of a group VIB metal. US-A-3,617,511 discloses a catalyst for conversion of cyclic hydrocarbons to paraffins where the catalyst comprises rhodium or ruthenium on a halogen promoted refractory oxide. US-A-6,241,876 discloses a ring opening catalyst which comprises a large pore crystalline molecular sieve component with a faujasite structure and an alpha acidity of less than one and a Group VIII noble metal. U.S. Publication No. 2002/43481 A1 discloses a catalyst for naphthalene ring opening which comprises at least one Group VIII metal selected from iridium,

platinum, rhodium and ruthenium on a refractory inorganic oxide substrate containing at least one of an alkali metal and alkaline earth metal. Finally U.S. Publication No. 2002/40175 A1 discloses a naphthene ring opening catalyst comprising a Group VIII metal selected from iridium, platinum, palladium, rhodium, ruthenium and combinations thereof. With the metal being supported on the substrate comprising at least one of a Group IB, IIB, and IVA metal.

DETAILED DESCRIPTION OF THE INVENTION

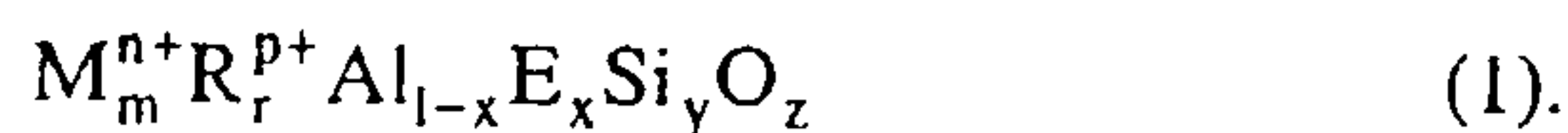
[0007] One aspect of the present invention is a catalyst which is useful for opening or cleaving naphthenic rings. The catalyst of the present invention comprises a Group VIII metal component an optional modifier component, a molecular sieve and a refractory inorganic oxide. The molecular sieves which can be used in the present invention are any of those which have 8, 10 or 12 ring pores and which have weak to medium acidity. Acidity of the molecular sieves can be determined by one of several techniques. One method involves measuring the ability of the molecular sieves to crack heptane, i.e. heptane cracking test. The cracking test involves placing a sample (250 mg) of the molecular sieve to be tested into a microreactor and drying the catalyst for 30 minutes at 200°C using flowing hydrogen. The sample is then reduced by heating for one hour at 500°C in flowing hydrogen. After cooling to 450°C a feedstream comprising hydrogen gas saturated with heptane at 0°C is flowed over the sample. Online analysis of the effluent gas is carried out using gas chromatography after holding for 20 minutes at a temperature from 450-550°C. A weakly acidic molecular sieve will have a heptane conversion of no more than 20% and preferably no more than 10%, while a moderately acidic molecular sieve will have a cracking conversion of no more than 40% and preferably no more than 30%. Another test method is ammonia temperature programmed desorption or NH₃-TPD. This test basically involves contacting a molecular sieve sample with ammonia and then measuring the amount of ammonia desorbed over a temperature range of 200°C to 500°C. Details of this test procedure are provided in US-A-4,894,142. Molecular sieves with moderate acidity will desorb less than 0.4mmol of NH₃/g total over the 200°C to 500°C range, while a weakly

acidic molecular sieve will desorb a total of less than 0.2mmol of NH₃/g over the 200°C to 500°C temperature range. Finally, acidity can be measured by pyridine infrared (IR). Specific examples of molecular sieves with weak to moderate acidity, include but are not limited to MAPSOs, SAPOs, UZM-4, UZM-4M, UZM-5, UZM-5P, UZM-5HS, UZM-6, UZM-8, UZM-8HS, UZM-15, UZM-15HS, UZM-16, UZM-16HS and mixtures thereof. MAPSO molecular sieves are disclosed in US-A-4,758,419. A preferred MAPSO is MAPSO-31. SAPO molecular sieves are disclosed in US-A-4,440,871. Preferred SAPOs are SAPO-11, SAPO-34 and SM-3 (US-A-4,943,424). UZM-4 is described in US-A-6,419,895 B1 while UZM-5, UZM-5P and UZM-6 are described in US-A-6,388,157 B1. The other UZM molecular sieves are described in the following U.S. Patent Applications.

<u>Zeolite</u>	<u>U.S. Application No.</u>
UZM-4M	6,776,975
UZM-5HS	6,982,074
UZM-8	6,756,030
UZM-8HS	7,713,513
UZM-15 and UZM-15HS	6,890,511
UZM-16 and UZM-16HS	6,752,980

[0008] Further, all the molecular sieves identified by a UZM designation will collectively be referred to as UZM zeolites. For completeness, the following brief description of the UZM zeolites described in the patent applications above will be provided below.

[0009] All of the UZM zeolites have a microporous crystalline structure of at least AlO₂ and SiO₂ tetrahedral units. UZM-8, UZM-15 and UZM-16 have a composition on an as-synthesized and anhydrous basis expressed by an empirical formula of:



M is at least one exchangeable cation selected from the group consisting of alkali and alkaline earth metals, "m" is the mole ratio of M to (Al + E) and, "n" is the weighted average valence of M. R is defined as follows:

- 1) UZM-8: R is at least one organoammonium cation selected from the group consisting of quaternary ammonium cations, diquaternary ammonium cations, protonated amines, protonated diamines, protonated alkanolamines and quaternized alkanolammonium cations, "r" is the mole ratio of R to (Al + E).
- 5 2) UZM-15: R is at least one first quaternary organoammonium cation comprising at least one organic group having at least two carbon atoms, and optionally a second organoammonium cation selected from the group consisting of quaternary ammonium cations, protonated amines, protonated diamines, protonated alkanolamines, diquaternaryammonium cations, quaternized alkanolamines and mixtures thereof, "r" is the mole ratio of R to (Al + E); and
- 10 3) UZM-16: R is benzyltrimethylammonium (BzTMA) cation or a combination of BzTMA and at least one organoammonium cation selected from the group consisting of quaternary ammonium cations, protonated amines, protonated diamines, protonated alkanolamines, diquaternaryammonium cations, quaternized alkanolamines and mixtures thereof, "r" is the mole ratio of R to (Al + E).
- 15

[0010] E is an element selected from the group consisting of Ga, Fe, In, Cr, B, and mixtures thereof. The other variables are defined as "p" is the weighted average valence of R; "x" is the mole fraction of E, "y" is the mole ratio of Si to (Al + E) and "z" is the mole ratio of O to (Al + E). The values of "m", "n", "r", "p", "x", "y" and "z" are presented in Table A.

20

Table A

Variable	UZM-8	UZM-15	UZM-16
m	0 to 2.0	0 to 2.0	0 to 0.75
n	1 to 2	1 to 2	1 to 2
r	0.05 to 5.0	0.25 to 5.0	0.25 to 5.0
p	1 to 2	1 to 2	1 to 2
x	0 to 1.0	0 to 1.0	0 to 1.0
y	6.5 to 35	7 to 50	3 to 2.5
z	$(m \cdot n + r \cdot p + 3 + 4 \cdot y)/2$	$(m \cdot n + r \cdot p + 3 + 4 \cdot y)/2$	$(m \cdot n + r \cdot p + 3 + 4 \cdot y)/2$

[0011] These zeolites are also characterized by x-ray diffraction patterns having at least the *d*-spacings and relative intensities set forth in Table B (UZM-8), Table C (UZM-15) and Table D (UZM-16).

Table B (UZM-8)

2- θ	<i>d</i> (Å)	<i>I</i> / <i>I</i> ₀ %
6.40 - 6.90	13.80 - 12.80	w - s
6.95 - 7.42	12.70 - 11.90	m - s
8.33 - 9.11	10.60 - 9.70	w - vs
19.62 - 20.49	4.52 - 4.33	m - vs
21.93 - 22.84	4.05 - 3.89	m - vs
24.71 - 25.35	3.60 - 3.51	w - m
25.73 - 26.35	3.46 - 3.38	m - vs

5

Table C (UZM-15)

2- θ	<i>d</i> (Å)	<i>I</i> / <i>I</i> ₀ %
8.35 - 9.30	10.58 - 9.50	w-m
12.30 - 13.30	7.19 - 6.65	w-m
16.60 - 17.20	5.34 - 5.15	w-m
19.00 - 19.80	4.67 - 4.48	w-m
20.80 - 22.30	4.27 - 3.98	w
23.55 - 23.95	3.77 - 3.71	w-m
24.03 - 24.47	3.70 - 3.63	w-m
25.50 - 26.25	3.49 - 3.39	vs
48.30 - 49.10	1.88 - 1.85	w

Table D (UZM-16)

2- θ	d(Å)	I/I ₀ %
3.86-4.22	22.87 - 20.92	w-m
7.60-7.84	11.62 - 11.27	s-vs
11.58-11.86	7.64 - 7.46	w-m
13.29-13.54	6.65 - 6.53	m
13.90-14.20	6.36 - 6.23	w
15.34-15.68	5.77 - 5.65	m
19.30-19.65	4.60 - 4.51	m
20.37-20.73	4.35 - 4.28	m-s
23.18-23.54	3.83 - 3.78	m-s
23.57-23.89	3.77 - 3.72	s-vs
24.68-25.03	3.60 - 3.55	m-s
26.84-27.23	3.32 - 3.27	m
28.15-28.58	3.17 - 3.12	m
31.25-31.71	2.86 - 2.82	vs
33.37-33.76	2.68 - 2.65	w
35.89-36.36	2.50 - 2.47	m
48.05-48.52	1.89 - 1.87	w-m
51.38-51.90	1.78 - 1.76	w-m
55.35-56.04	1.66 - 1.64	w-m
58.08-58.64	1.59 - 1.57	w

[0012] The UZM-8, UZM-15 and UZM-16 zeolites are prepared by a hydrothermal crystallization of a reaction mixture prepared by combining reactive sources of R, aluminum, silicon and optionally M and E. The sources of aluminum include but are not limited to aluminum alkoxides, precipitated aluminas, aluminum metal, sodium aluminate, organoammonium aluminates, aluminum salts and alumina sols. Specific examples of aluminum alkoxides include, but are not limited to aluminum ortho sec-butoxide and aluminum ortho isopropoxide. Sources of silica include but are not limited to tetraethylorthosilicate, colloidal silica, precipitated silica, alkali silicates and organoammonium silicates. A special reagent consisting of an organoammonium aluminosilicate solution can also serve as the simultaneous source of Al, Si, and R. Sources of the E elements include but are not limited to alkali borates, boric acid, precipitated gallium oxyhydroxide, gallium sulfate, ferric sulfate, ferric chloride,

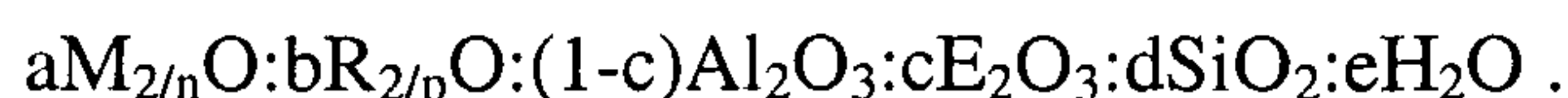
chromium nitrate and indium chloride. Sources of the M metals include the halide salts, nitrate salts, acetate salts, and hydroxides of the respective alkali or alkaline earth metals. R can be introduced as an organoammonium cation or an amine. When R is a quaternary ammonium cation or a quaternized alkanolammonium cation, the sources
5 include but are not limited to the hydroxide, chloride, bromide, iodide and fluoride compounds. Specific examples include without limitation DEDMA hydroxide, ETMA hydroxide, tetramethylammonium hydroxide, tetraethylammonium hydroxide, hexamethonium bromide, tetrapropylammonium hydroxide, methyltriethylammonium hydroxide, tetramethylammonium chloride, propylethyldimethylammonium hydroxide
10 (PEDMAOH), trimethylpropylammonium hydroxide, trimethylbutylammonium hydroxide (TMBAOH), N,N,N,N',N',N'-hexamethyl 1,4 butanedi ammonium hydroxide (DQ4), and choline chloride. The source of R may also be neutral amines, diamines, and alkanolamines that subsequently hydrolyzes to form an organoammonium cation. Specific examples are triethanolamine, triethylamine, and N,N,N',N' tetramethyl-1,6-
15 hexanedi amine. Preferred sources of R without limitation are ETMAOH, DEDMAOH, and HM(OH)₂.

[0013] In a special case, a reagent in the form of an aluminosilicate stock solution may be used. These solutions consist of one or more organoammonium hydroxides and sources of silicon and aluminum that are processed to form a clear homogenous solution
20 that is generally stored and used as a reagent. The reagent contains aluminosilicate species that typically don't show up in zeolite reaction mixtures derived directly from separate sources of silicon and aluminum. The reagent is generally alkali-free or contains alkali at impurity levels from the silicon, aluminum, and organoammonium hydroxide sources. One or more of these solutions may be used in a zeolite synthesis. In
25 the case of substitution of Al by E, the corresponding metallosilicate solution may also be employed in a synthesis.

[0014] As shown above, not all the R cations can produce all of the three UZM structures. Thus the preparation of UZM-15 requires at least one first organoammonium cation having at least one organic group with at least two carbon atoms, e.g. DEDMA,
30 ETMA, TMBA, DQ4 and PEDMA and optionally (in addition to the first

organoammonium cation) a second organoammonium compound. The preparation of UZM-16 requires benzyltrimethylammonium (BzTMA) or a combination of BzTMA and at least one organoammonium cation as described above.

[0015] The reaction mixture containing reactive sources of the desired components
5 can be described in terms of molar ratios of the oxides by the formula:



[0016] The values of the variables for the UZM-8, 15 and 16 are presented in Table E along with general and preferred reaction conditions. The reaction mixtures are reacted at the stated conditions in a sealed reaction vessel under autogenous pressure.

10

Table E

Reaction Mixture Compositions and Reaction Conditions for UZM Zeolites

Variable	UZM-8	UZM-15	UZM-16
a	0 to 25	0 to 5	0 to 5
b	1 to 80	1.5 to 80	1 to 120
c	0 to 1.0	0 to 1.0	0 to 1.0
d	10 to 100	10 to 100	5 to 100
e	100 to 1500	100 to 1500	50 to 1500
Temp(°C)- broad range	85°C to 225°C	85°C to 225°C	80°C to 160°C
Temp(°C)-preferred range	125°C to 150°C	140°C to 175°C	95°C to 125°C
Time- broad range	1 day to 28 days	12 hrs. to 20 days	2 days to 30 days
Time- preferred range	5 days to 14 days	2 days to 10 days	5 days to 15 days

[0017] After crystallization is complete, the solid product is isolated from the heterogeneous mixture by means such as filtration or centrifugation, and then washed with de-ionized water and dried in air at ambient temperature up to 100°C.

15 [0018] As-synthesized, the zeolites will contain some of the exchangeable or charge balancing cations in its pores. These exchangeable cations can be exchanged for other cations, or in the case of organic cations, they can be removed by heating under controlled conditions. Ion exchange involves contacting the zeolites with a solution

containing the desired cation (at molar excess) at exchange conditions. Exchange conditions include a temperature of 15°C to 100°C and a time of 20 minutes to 50 hours. Calcination conditions include a temperature of 300°C to 600°C for a time of 2 to 24 hours.

5 [0019] A special treatment for removing organic cations which provides the ammonium form of the zeolite is ammonia calcination. Calcination in an ammonia atmosphere can decompose organic cations, presumably to a proton form that can be neutralized by ammonia to form the ammonium cation. The resulting ammonium form of the zeolite can be further ion-exchanged to any other desired form. Ammonia
10 calcination conditions include treatment in the ammonia atmosphere at temperatures between 250°C and 600°C and more preferably between 250°C and 450°C for times of 10 minutes to 5 hours. Optionally, the treatments can be carried out in multiple steps within this temperature range such that the total time in the ammonia atmosphere does not exceed 5 hours. Above 500°C, the treatments should be brief, less than a half hour
15 and more preferably on the order of 5-10 minutes. Extended calcination times above 500°C can lead to unintended dealumination along with the desired ammonium ion-exchange and are unnecessarily harsh as most organoammonium templates easily decompose at lower temperatures.

[0020] The UZM-4M, UZM-5HS, UZM-8HS, UZM-15HS and UZM-16HS
20 zeolites are prepared from their respective parent zeolite by a number of various techniques and are represented by the empirical formula:



[0021] In formula (2), E and "x" are as defined above except for UZM-4M and UZM-5HS where "x" varies from 0 to 0.5. M1 is at least one exchangeable cation
25 selected from the group consisting of alkali metals, alkaline earth metals, rare earth metals, ammonium ion, hydrogen ion and mixtures thereof, a is the mole ratio of M1 to (Al + E), n is the weighted average valence of M1, y' is the mole ratio of Si to (Al + E) and z'' is the mole ratio of O to (Al + E). The values of the variables for the zeolites are presented below in Table F.

Table F

Variable	UZM-4M	UZM-5HS	UZM-8HS	UZM-15HS	UZM-16HS
a	0.15 to 1.5	0.15 to 50	0.05 to 50	0.01 to 50	0.01 to 50
n	1 to 3	1 to 3	1 to 3	1 to 3	1 to 3
y'	1.75 to 500	greater than 5	greater than 6.5	greater than 7	greater than 3
z''	$(a \cdot n + 3 + 4 \cdot y')/2$	$(a \cdot n + 3 + 4 \cdot y')/2$	$(a \cdot n + 3 + 4 \cdot y')/2$	$(a \cdot n + 3 + 4 \cdot y')/2$	$(a \cdot n + 3 + 4 \cdot y')/2$

[0022] The value of y' is greater than the specific value set forth in Table F to virtually pure silica. By virtually pure silica is meant that virtually all the aluminum and/or the E metals have been removed from the framework. It is well known that it is virtually impossible to remove all the aluminum and/or E metal. Numerically, a zeolite is virtually pure silica when y' has a value of at least 3,000, preferably 10,000 and most preferably 20,000. Thus, ranges for y' are from 3, 5, 6.5 or 7 to 3,000 preferably greater than 10 to 3,000; 3, 5, 6.5 or 7 to 10,000 preferably greater than 10 to 10,000 and 3, 5, 6.5 or 7 to 20,000 preferably greater than 10 to 20,000.

10 [0023] The zeolites UZM-4M, UZM-5HS, UZM-8HS, UZM-15HS and UZM-16HS are further characterized by an x-ray diffraction pattern having at least the d-spacings and relative intensities set forth in Tables G, H, I, J and K respectively.

Table G
UZM-4M

2θ	$d(\text{\AA})$	$I/I_0\%$
6.55 – 6.83	13.49 – 12.93	m
7.63 – 7.91	11.58 – 11.17	vs
13.27 – 13.65	6.67 – 6.48	m-s
14.87 – 15.25	5.95 – 5.81	m-vs
15.35 – 15.74	5.77 – 5.63	m
18.89 – 19.31	4.69 – 4.59	m
20.17 – 20.50	4.40 – 4.33	w-m
20.43 – 20.85	4.34 – 4.26	m
21.51 – 21.97	4.13 – 4.04	m-vs
24.14 – 24.67	3.68 – 3.60	m-s
24.47 – 24.98	3.63 – 3.56	m-s
27.73 – 28.27	3.21 – 3.15	w-m
30.11 – 30.73	2.97 – 2.90	m-s
31.13 – 31.75	2.87 – 2.81	w-m

Table H
UZM-5HS

2θ	$d(\text{\AA})$	$I/I_0\%$
< 6.79	> 13.0	w-m
8.26 - 7.52	10.70 - 11.75	m-vs
10.65 - 10.04	8.30 - 8.80	m-vs
12.32 - 11.79	7.18 - 7.50	s-vs
16.56 - 15.53	5.35 - 5.70	m-vs
19.71 - 18.78	4.50 - 4.72	w-m
23.58 - 22.72	3.77 - 3.91	w-m
24.37 - 23.64	3.65 - 3.76	m-vs

Table I
UZM-8HS

2θ	$d(\text{\AA})$	$I/I_0\%$
6.90 - 7.40	12.8 - 11.94	w-vs
8.15 - 8.85	10.84 - 9.98	m-vs
14.10 - 14.70	6.28 - 6.02	w-vs
19.40 - 20.10	4.57 - 4.41	w-s
22.00 - 22.85	4.04 - 3.89	m-vs
24.65 - 25.40	3.61 - 3.50	w-m
25.70 - 26.50	3.46 - 3.36	w-vs

Table J
UZM-15HS

2θ	$d(\text{\AA})$	$I/I_0\%$
8.75 - 10.30	10.12 - 8.60	w-vs
12.70 - 13.40	6.98 - 6.62	m-s
19.00 - 20.30	4.68 - 4.38	w
25.50 - 26.50	3.50 - 3.37	m-vs

5

Table K
UZM-16HS

2θ	$d(\text{\AA})$	$I/I_0\%$
7.70 - 8.40	11.47 - 10.52	m - vs
11.70 - 12.10	7.56 - 7.31	w
13.35 - 14.56	6.63 - 6.08	s - vs
20.60 - 21.70	4.31 - 4.09	w
24.60 - 25.65	3.62 - 3.47	m - s

[0024] The UZM-4M, UZM-5HS, UZM-8HS, 15HS and 16HS are prepared by removing aluminum and optionally inserting silicon into the structure thereby increasing the Si/Al ratio and thus modifying the acidity and ion exchange properties of the zeolites. These treatments include: a) contacting with a fluorosilicate solution or slurry; b) calcining or steaming followed by acid extraction or ion-exchange; c) acid extraction or d) any combination of these treatments in any order.

10

[0025] Fluorosilicate treatment is known in the art and is described in US-A-6,200,463 B1, which cites US-A-4,711,770 as describing a process for treating a zeolite with a fluorosilicate salt. General conditions for this treatment are contacting the zeolite with a solution containing a fluorosilicate salt such as ammonium
5 fluorosilicate (AFS) at a temperature of 20°C to 90°C.

[0026] The acids which can be used in carrying out acid extraction include without limitation mineral acids, carboxylic acids and mixtures thereof. Examples of these include sulfuric acid, nitric acid, ethylenediaminetetraacetic acid (EDTA), citric
10 acid, oxalic acid, etc. The concentration of acid which can be used is not critical but is conveniently between 1 wt-% to 80 wt-% acid and preferably between 5 wt-% and 40 wt-% acid. Acid extraction conditions include a temperature of 10°C to 100°C for a time of 10 minutes to 24 hours. Once treated with the acid, the treated UZM zeolite is isolated by means such as filtration, washed with deionized water and dried at
15 ambient temperature up to 100°C.

[0027] The extent of dealumination obtained from acid extraction depends on the cation form of the starting UZM as well as the acid concentration and the time and temperature over which the extraction is conducted. For example, if organic cations are present in the starting UZM zeolite, the extent of dealumination will be slight
20 compared to a UZM zeolite in which the organic cations have been removed. This may be preferred if it is desired to have dealumination just at the surface of the UZM zeolite. As stated above, convenient ways of removing the organic cations include calcination, ammonia calcination, steaming and ion exchange. Calcination, ammonia calcination and ion exchange conditions are as set forth above. Steaming conditions
25 include a temperature of 400°C to 850°C with from 1% to 100% steam for a time of 10 minutes to 48 hours and preferably a temperature of 500°C to 600°C, steam concentration of 5 to 50% and a time of 1 to 2 hours.

[0028] It should be pointed out that both calcination and steaming treatments not only remove organic cations, but can also dealuminate the zeolite. Thus, alternate
30 embodiments for dealumination include: a calcination treatment followed by acid

extraction and steaming followed by acid extraction. A further embodiment for dealumination comprises calcining or steaming the starting UZM zeolite followed by an ion-exchange treatment. Of course an acid extraction can be carried out concurrently with, before or after the ion exchange.

5 [0029] The ion exchange conditions are the same as set forth above, namely a temperature of 15°C to 100°C and a time of 20 minutes to 50 hours. Ion exchange can be carried out with a solution comprising a cation (M1') selected from the group consisting of alkali metals, alkaline earth metals, rare earth metals, hydrogen ion, ammonium ion, and mixtures thereof. By carrying out this ion exchange, the M1
10 cation is exchanged for a secondary or different M1' cation. In a preferred embodiment, the UZM composition after the steaming or calcining steps is contacted with an ion exchange solution comprising an ammonium salt. Examples of ammonium salts include but are not limited to ammonium nitrate, ammonium chloride, ammonium bromide, and ammonium acetate. The ammonium ion containing
15 solution can optionally contain a mineral acid such as but not limited to nitric, hydrochloric, sulfuric and mixtures thereof. The concentration of the mineral acid is that amount necessary to give a ratio of H^+ to NH_4^+ of 0 to 1. This ammonium ion exchange aids in removing any debris present in the pores after the steaming and/or calcination treatments.

20 [0030] It is apparent from the foregoing that, with respect to effective process conditions, it is desirable that the integrity of the zeolite crystal structure be substantially maintained throughout the dealumination process, and that the zeolite retains at least 50%, preferably at least 70% and more preferably at least 90% of its original crystallinity. A convenient technique for assessing the crystallinity of the
25 products relative to the crystallinity of the starting material is the comparison of the relative intensities of the *d*-spacing of their respective X-ray powder diffraction patterns. The sum of the peak intensities, in arbitrary units above the background, of the starting material is used as the standard and is compared with the corresponding peak intensities of the products. When, for example, the numerical sum of the peak
30 heights of the molecular sieve product is 85 percent of the value of the sum of the

peak intensities of the starting zeolite, then 85 percent of the crystallinity has been retained. In practice it is common to utilize only a portion of the peaks for this purpose, as for example, five or six of the strongest peaks. Other indications of the retention of crystallinity are surface area and adsorption capacity. These tests may be preferred when the substituted metal significantly changes, e.g., increases, the absorption of x-rays by the sample or when peaks experience substantial shifts such as in the dealumination process.

[0031] After having undergone any of the dealumination treatments as described above, the UZM zeolite is usually dried and can be used as discussed below. The properties of the modified UZM zeolite can be further modified by one or more additional treatment. These treatments include steaming, calcining or ion exchanging and can be carried out individually or in any combination. Some of these combinations include but are not limited to:

	steam	→	calcine	→	ion exchange;
15	calcine	→	steam	→	ion exchange;
	ion exchange	→	calcine	→	steam
	ion exchange	→	steam	→	calcine;
		steam	→	calcine;	

[0032] The dealumination treatment described above can be combined in any order to provide the zeolites of the invention although not necessarily with equivalent result. It should be pointed out that the particular sequence of treatments, e.g., AFS, acid extraction, steaming, calcining, etc can be repeated as many times as necessary to obtain the desired properties. Of course one treatment can be repeated while not repeating other treatments, e.g., repeating the AFS two or more times before carrying out steaming or calcining, etc. Finally, the sequence and/or repetition of treatments will determine the properties of the final UZM-4M, UZM-5HS, UZM-8HS, 15HS or 16HS composition.

[0033] In specifying the proportions of the zeolite starting material or adsorption properties of the zeolite product and the like herein, the "anhydrous state" of the zeolite will be intended unless otherwise stated. The term "anhydrous state" is employed herein to refer to a zeolite substantially devoid of both physically adsorbed and chemically adsorbed water.

[0034] A second component of the catalyst of the invention is a catalytic metal component which is selected from the metals of Group VIII (Groups 8, 9 and 10 of the IUPAC designation) of the Periodic Table of the Elements and preferably from the noble metals. The group of noble metals are ruthenium, rhodium, palladium, platinum, iridium and osmium. Preferred catalytic metals are platinum, palladium, rhodium, ruthenium, iridium and mixtures thereof.

[0035] The catalytic metal component can be deposited either on the molecular sieve or on a refractory inorganic oxide component. Inorganic oxides which can be used are any of those well known in the art and include but are not limited to aluminas, silica/alumina, silica, titania, calcium oxide, magnesium oxide, clays and zirconia. In order to avoid confusion it is pointed out that the term silica/alumina does not mean a physical mixture of silica and alumina but means an acidic and amorphous material that has been cogelled or coprecipitated. The term is well known in the art, see e.g. US-A-3,909,450; US-A-3,274,124 and US-A-4,988,659. The aluminas which can be used include gamma alumina, theta alumina, delta and alpha alumina.

[0036] The catalytic metal component is deposited onto either the zeolite or inorganic oxide by means well known in the art such as spray impregnation or evaporative impregnation. Both spray or evaporative impregnation use a solution containing a decomposable compound of the desired metal. By decomposable is meant that upon heating the compound decomposes to provide the catalytic metal or catalytic metal oxide. Non-limiting examples of decomposable compounds which can be used include chloroplatinic acid, palladic acid, chloroiridic acid, rhodium trichloride, ruthenium tetrachloride, osmium trichloride, iron chloride, cobalt chloride, nickel chloride, iron nitrate, cobalt nitrate, nickel nitrate, rhodium nitrate, ammonium chloroplatinate, platinum tetrachloride hydrate, palladium chloride, palladium nitrate,

tetraamine platinum chloride and tetraamminepalladium (II) chloride. The solvent which is used to prepare the solution is usually water although organic solvents such as alcohols, dimethyl formamide (DMF), dimethylsulfoxide (DMSO), tetrahydrofuran (THF) and amines, e.g., pyridine can be used.

5 [0037] Spray impregnation involves taking a small volume of the solution and spraying it over the support (zeolite or oxide) while the support is moving. When the spraying is over, the wetted support can be transferred to other apparatus for drying or finishing steps.

[0038] One particular method of evaporative impregnation involves the use of a
10 steam-jacketed rotary dryer. In this method the support is immersed in the impregnating solution which has been placed in the dryer and the support is tumbled by the rotating motion of the dryer. Evaporation of the solution in contact with the tumbling support is expedited by applying steam to the dryer jacket. The impregnated support is then dried at a temperature of 60°C to 300°C and then calcined at a temperature of 300°C to 850°C
15 for a time of 30 minutes to 8 hours to give the calcined catalyst.

[0039] When the molecular sieve is the support, the catalytic metal component can also be deposited thereon by ion-exchange. Ion-exchange is carried out by contacting the molecular sieve with a solution containing a compound of the desired metal at ion-exchange conditions which include a temperature of 20°C to 100°C for a
20 time from 5 minutes to 6 hours.

[0040] When the catalytic metal component is deposited on the refractory inorganic oxide component, the catalyst comprises separate particles. One configuration is a loose mixture of the two particles (refractory oxide and zeolite particles) or the particles are mixed and then formed into shaped articles such as
25 cylinders, pellets, pills, spheres, irregularly shaped particles, etc. Methods of preparing such shaped articles are well known in the art. In the case where the catalytic metal is deposited on the molecular sieve, then the inorganic oxide acts as a binder so that the resultant mixture can be formed into any of the shapes described above.

[0041] In another embodiment, the molecular sieve and inorganic oxide are first mixed and formed into a shaped article and then the catalytic metal is deposited onto the composite article by any of the means described above. In this case, the catalytic metal is believed to be deposited on both the inorganic oxide and zeolite supports.

5 Regardless of how and where the catalytic metal is deposited, it is present in the final catalyst in an amount from 0.01 to 10 weight percent of the catalyst expressed as the metal. It should also be pointed out that the metal component can be present on the catalyst in its elemental (zero valent) state or as the oxide.

[0042] The catalyst can also contains a modifier which modifies the activity of the
10 catalytic metal. The modifier is selected from the group consisting of titanium, niobium, rare earth elements, tin, rhenium, zinc, germanium and mixtures thereof. Preferred rare earth elements are cerium, ytterbium, lanthanum, dysprosium and mixtures thereof. The modifier component is deposited by the same techniques as described above for the catalytic metals. Further, the modifier can be deposited on the
15 support before, after or simultaneously with the catalytic metal, although not necessarily with equivalent results. It is preferred to deposit the modifier with the catalytic metal. The amount of modifier can vary substantially but is usually in the range of 0.1 to 50 wt.-%, preferably 1 to 10 wt.-% of the catalyst as the element.

[0043] The catalyst described above is used in a process where cyclic paraffins are
20 opened or cleaved to acyclic paraffins. The feeds which can be used in the ring opening process are any of those which comprises C₅ - C₆ aliphatic rings, i.e. naphthenic rings. Naphtha feeds can vary considerably in the amount of aromatic, naphthene and paraffin components which they contain. Depending on the source, feeds can contain from 15% to 55% naphthenes. One example of naphtha feed was
25 found to contain 17 wt.-% aromatics, 44 wt.-% naphthenes and 39 wt.-% aromatics.

[0044] The feedstream is contacted with the catalyst at ring opening conditions which include a temperature of 200°C to 600°C, a pressure of atmospheric to 20,684 kPag, and preferably from 1379 kPag to 13790 kPag, a liquid hourly space velocity of 0.1 to 30 hr⁻¹ and preferably 2 to 10 hr⁻¹ and H₂/HC (hydrocarbon) ratio from 0.1 to
30 30 and preferably from 1 to 10.

[0045] The following examples are presented in illustration of this invention and are not intended as undue limitations on the generally broad scope of the invention as set out in the appended claims.

EXAMPLE 1

5 [0046] An aluminum sol was prepared by dissolving aluminum metal in HCl. In a container 822.4g of the Al-sol, containing 105.32g Al (as Al_2O_3) and 94g Cl were blended with 2.91g of NbCl_5 at 60°C for 12 hours. To this there were added 302.1g of hexamethylene tetraamine (HMT) and 15.4g of water. Droplets of the resulting mixture were formed and dropped into a hot oil tower which formed gelled spheres.
10 The spheres were then aged at 140°C for 1.5 hours, washed with 20 liters of 0.25% NH_3 solution for 2 hours at 95°C, dried at 100°C for 16 hours and then calcined at 550°C for 2 hours in air with 3% steam.

[0047] In a rotary impregnator, 50 cc of the above spheres were impregnated with a 50 cc aqueous solution containing 8.89 cc of chloroplatinic acid (CPA) (Pt
15 concentration was 28.08 mg Pt/cc) and 2g of HCl (37%). The excess solution was evaporated at 100°C and the catalyst was then calcined at 525°C in flowing air (3600 cc/min.) and 45 cc/min. of 1.0M HCl for 30 minutes. Finally, the calcined catalyst was reduced at 500°C with 3000 cc/min. of H_2 for one hour. Analysis of the catalyst showed it contained 0.93 wt-% Pt and 0.49 wt-% Nb. This catalyst was identified as
20 catalyst A.

EXAMPLE 2

[0048] In a container 766.2g of alumina was mixed with 27g HNO_3 (70%) followed by the addition of 71.4g TiO_2 and 563.9g of water and mixed for 30 minutes to form a dough. The dough was extruded through a 0.073" dieplate and the
25 extrudates calcined in air at 550°C for two hours.

[0049] In a rotary evaporator, 72.26g of the above extrudates were combined with 100 ml of an aqueous solution containing 4.92 ml of HCl (37%) and 12.8 ml of CPA. The solution was evaporated and the catalyst was calcined and then reduced as

described in Example 1. Analysis of the catalyst showed it contained 0.49 wt-% Pt. This catalyst was identified as catalyst B.

EXAMPLE 3

5 [0050] In a rotary evaporator 148.24g of gamma alumina extrudates were impregnated with 200 ml of an aqueous solution containing 26.03 mL of CPA, 1.60 g $\text{La}(\text{NO}_3)_3$ and 9.99mL HCl (44%). The wet powder was dried, calcined and reduced as described in Example 1. Analysis of the catalyst showed it contained 0.5wt-% Pt and 0.32wt-% La. This catalyst was identified as catalyst C.

EXAMPLE 4

10 [0051] In a rotary evaporator 148.24g of gamma alumina extrudates were impregnated with 200 mL of an aqueous solution containing 26.68 mL of CPA, 1.11 g of NbCl_5 and 9.99mL HCl (44%). The wet extrudates were dried, calcined and reduced as described in Example 1. Analysis of the catalyst showed it contained 0.48 wt-% Pt and 0.16 wt-% Nb. This catalyst was identified as catalyst D.

15

EXAMPLE 5

[0052] In a rotary evaporator 63.63g of theta alumina oil dropped spheres were impregnated with 100 mL of an aqueous solution containing 11.45mL of CPA, 0.62 g of $\text{YbCl}_3 \cdot 6\text{H}_2\text{O}$ and 4.29mL HCl (44%). The wet spheres were dried, calcined and reduced as described in Example 1. Analysis of the catalyst showed it contained 0.49
20 wt-% Pt and 0.46 wt-% Yb. This catalyst was identified as catalyst E.

EXAMPLE 6

[0053] In a rotary evaporator 148.24g of gamma alumina extrudates were impregnated with 200mL of an aqueous solution containing 26.68 mL of CPA, and 9.99mL HCl (44%). The wet extrudates were dried, calcined and reduced as
25 described in Example 1. Analysis of the catalyst showed it contained 0.52 wt-% Pt. This catalyst was identified as catalyst F.

EXAMPLE 7

[0054] In a rotary evaporator 148.28g of gamma alumina extrudates were impregnated with 200 mL of an aqueous solution containing 26.68 mL of CPA, 1.45 g YbCl₃·6H₂O and 9.99 mL HCl (44%). The wet extrudates were dried, calcined and
5 reduced as described in Example 1. Analysis of the catalyst showed it contained 0.51 wt-% Pt and 0.40 wt-% Yb. This catalyst was identified as catalyst G.

EXAMPLE 8

[0055] In a rotary evaporator 95.73g of theta alumina oil dropped spheres were impregnated with 150 mL of an aqueous solution containing 17.41 mL of CPA and
10 6.52mL HCl (44%). The wet spheres were dried, calcined and reduced as described in Example 1. Analysis of the catalyst showed it contained 0.50 wt-% Pt . This catalyst was identified as catalyst H.

EXAMPLE 9

[0056] In a rotary evaporator 148.24g of alumina extrudates were impregnated
15 with an aqueous solution containing 200 mL of CPA, 1.62 g Dy(NO₃)₃ and 9.99mL HCl (44%). The wet extrudates were dried, calcined and reduced as described in Example 1. Analysis of the catalyst showed it contained 0.50 wt-% Pt and 0.39 wt-% Dy. This catalyst was identified as catalyst I.

EXAMPLE 10

20 [0057] Catalysts B to I were tested for methylcyclopentane ring opening activity and selectivity as follows. The catalysts were tested by placing 35mg of 250-450 um meshed particles into a microreactor and pretreated at 450°C for 4 hours using dry hydrogen floured at 45 cm³/min. The samples were then tested using a feed of 2.7% methylcyclopentane in hydrogen as a carrier gas at temperatures of 200°C to 350°C at
25 weight hourly space velocities (w 2/sv) of 0.5 to 6hr⁻¹. The results of the testing at 350°C and WHSV of 0.5hr⁻¹ are presented in Table 1.

Table 1
Effect of Modifiers on Ring Opening Activity

Catalyst I.D.	MCP Conv. %	RO Yield %
B	80	72
C	74	71
D	82	75
E	73	70
F	68	60
G	65	60
H	62	57
I	59	55

[0058] The results provided in Example 10 show that modifiers such as Nb, Ti, and Yb improve both the activity and selectivity of platinum for ring opening.

5

EXAMPLE 11

[0059] Samples of catalysts A, B and H were mixed with a sample of UZM-16 (70% UZM-16/30% catalyst) and tested for methylcyclohexane ring opening activity and selectivity as follows. In an Incollog 800 HTM tube reactor there were placed 2.0 g of 40-60 mesh crushed extrudates of A,B or H and 1.0 g of UZM-16. The reactor was heated using an infrared furnace. Inert spacers were placed before the catalyst bed to minimize dead volume and pre-heat the feed. The feed consisted of methylcyclohexane (>98% purity) which was mixed with hydrogen carrier gas (>99% pure) in a heated mixing chamber and then downflowed through the catalyst bed at a weight hourly space velocity of 1.5 hr⁻¹. Measurements were taken at temperatures of 260-400°C and a pressure of 5516 kPag (800 psig). The reactor effluent was analyzed by an on-line gas chromatograph and the results are presented in Table 2.

15

Table 2

Effect of Molecular Sieves on Ring Opening Activity

Catalyst ID	Temperatures	MCH Conversion (wt-%)	C ₇ Paraffin Select. (wt-%)	C ₇ Paraffin Yield %
UZM-16 + Cat H	383	86	52	45
UZM-16 + Cat A	391	93	59	55
UZM-16 + Cat B	401	96	54	52

EXAMPLE 12

[0060] Aluminum tri-sec-butoxide (95%), 46.32g, was added to 626.31g
 5 diethyldimethylammonium hydroxide (20%) and dissolved with vigorous stirring. To
 this mixture, 142.5g precipitated silica, Ultrasil™ VN3P3 (85% SiO₂), was added
 with continuous stirring. In a separate beaker, 21.47g TMACl (97%) and 5.22g NaCl
 were dissolved in 58.18g de-ionized H₂O. This solution was then added to the
 previous reaction mixture. The resulting mixture was homogenized for 20 min and
 10 the final reaction mixture was then distributed among several autoclaves including
 one 0.6L stainless steel stirred autoclave. The 0.6L autoclave was heated to and held
 at 150°C for 120 hr. after which the solids were collected by centrifugation, washed
 with de-ionized water and dried at 95°C.

[0061] The products isolated from the 0.6L reaction exhibited an x-ray diffraction
 15 pattern consistent with the characteristic lines for the zeolite designated UZM-15. A
 sample of the UZM-15 (60 g) was then mixed with 120 ml of 1.57 M HCl solution
 and heated to 95°C for 1 hour to remove a good portion of organic templates. The
 slurry was then filtered while still hot and washed with 500 ml of de-ionized H₂O.

The filter cake was air dried overnight, treated with HCl as described above, washed using two 500 ml portions of de-ionized H₂O and dried at 95°C.

[0062] Extrudates of 70 wt-% zeolite (UZM-15) and 30% alumina were prepared by first mulling 19.1 grams of Condea SBTM alumina with 29.0 grams of 20% HNO₃.

5 The HCl extracted UZM-15 (37.0 grams), Solka Floc (1.5 grams) extrusion aid and additional de-ionized H₂O were then added to the peptized alumina and mulled for additional time until a consistent dough texture was obtained. The dough was then pushed through a die plate with 0.16 cm die holes to form green extrudate, which was then activated first in N₂ and then air at 500°C for 2 hours. This catalyst was
10 identified as sample J.

EXAMPLE 13

[0063] An aluminosilicate reaction mixture was prepared by adding 35.2 grams of Al (Osec-Bu)₃ (95+%) to 927.5 grams BzTMAOH (40%), and then stirring for 20 minutes, followed by the slow addition of 416.5 grams of colloidal silica (LUDOXTM
15 AS-40, 40% SiO₂). The resulting mixture was then reacted in an autoclave at 125°C for 120 hours. The solid product was recovered and washed, and showed an x-ray pattern consistent with that of UZM-16. The powder was then calcined at 500°C and then NH₄NO₃ exchanged, filtered, washed with de-ionized H₂O and dried at 90°C. The catalyst comprising 70 wt-% UZM-16 and 30 wt-% Al₂O₃ was prepared using a
20 procedure similar to that described in Example 12. This catalyst was identified as sample K.

EXAMPLE 14

[0064] An aluminosilicate reaction mixture was prepared in the following manner. Al(Osec-Bu)₃ (97%), 804.4g, was added to 7330g of DEDMAOH, (20% aq) with
25 vigorous stirring. To this mixture, 2530g precipitated silica, (UltrasilTM VN SP3, 89% SiO₂) was added with continuous mixing. A solution of 127g NaOH in 3115g deionized H₂O was prepared and added to the previous mixture and homogenized for 30 min. The resulting mixture was reacted in an autoclave at 150°C for 185 hours. The solid product was collected by filtration, washed with de-ionized water, and dried at 95°C. The
30 product was identified as UZM-8 by powder x-ray diffraction analysis. The zeolite was

first NH_4NO_3 exchanged to remove sodium, then prepared into a catalyst of 70 wt-% UZM-8 and 30 wt-% Al_2O_3 using a procedure similar to that described in Example 12. This catalyst was identified as sample L.

EXAMPLE 15

5 [0065] An aluminosilicate reaction mixture was prepared in the following manner. $\text{Al}(\text{Osec-Bu})_3$ (97%), 66.51g, was added to 918.29g of DEDMAOH, (20% aq) with vigorous stirring. To this mixture, 208.95g precipitated silica, (Ultrasil™ VN SP3, 89% SiO_2) was added with continuous mixing. A solution of 37.2g Na_2SO_4 in 169.05g deionized H_2O was prepared and added to the previous mixture and
10 homogenized for 10 min. A 1.7g portion of UZM-8 seed was added to the mixture, followed by an additional 20 min of mixing. A 1077.3g portion of this final reaction mixture was transferred to a 2-L Teflon-lined autoclave. The autoclave was placed in an oven set at 150°C and the mixture was reacted quiescently for 10 days. The solid product was collected by filtration, washed with de-ionized water, and dried at 95°C .
15 The product was identified as UZM-8 by powder x-ray diffraction analysis. The zeolite was first NH_4NO_3 exchanged to remove sodium, then prepared into a catalyst of 70 wt-% UZM-8 and 30 wt-% Al_2O_3 using a procedure similar to that described in Example 12. This catalyst was identified as sample M.

EXAMPLE 16

20 [0066] In a container 219.3g of alumina were mixed with 12.9g of HNO_3 (70%) and to this peptized mixture there were added 109.6g of alumina, 84.3g of SM-3 molecular sieve (prepared according to US-A-4,943,424), 1.5g of methacel A4M and 197.4g water. The resulting dough was mixed for 35 minutes and then extruded through a 0.16 cm die. The extrudates were dried at 300°C for 1 hour and then 550°C
25 for 2 hours in flowing air. This catalyst was identified as sample N.

EXAMPLE 17

[0067] A catalyst containing SAPO-11 and alumina was prepared per Example 5. The SAPO-11 was prepared according to US-A-4,440,871. This catalyst was identified as sample O.

EXAMPLE 18

[0068] Platinum was dispersed on samples J to O by taking 8.35g of each sample and contacting it with 15ml of a solution containing 2.97cc chloroplatinic acid (28.08mg Pt/ml) and 0.569ml HCl (37%) in a rotary evaporator. The solution was
5 impregnated at 100°C and the impregnated base was calcined at 525°C in flowing air (3600cc/min) and 45cc/min HCl for 30 minutes. The calcined catalyst was reduced in flowing hydrogen 3000cc/min H₂ at 500°C for 1 hour. The amount of platinum on the finished catalyst was found to be 1 wt-%. The catalysts were labeled catalysts J to O respectively.

10

EXAMPLE 19

[0069] Catalysts J to O were tested for methylcyclohexane ring opening activity and selectivity as follows. In on Incolloy™ tube reactor there were placed 3g of 40-60 mesh crushed extrudates of each sample. The reactor was heated using an infrared furnace. Inert spacers were placed before the catalyst bed to minimize dead volume
15 and pre-heat the feed. The feed consisted of methylcyclohexane (>98% purity) which was mixed with hydrogen carrier gas (>99% pure) in a heated mixing chamber and then flowed through the catalyst bed at a weight hourly space velocity of 5 hr⁻¹. Measurements were taken at various temperatures and a pressure of 5516 kPa (800 psi). The reactor effluent was analyzed by an on-line gas chromatograph and the
20 results are presented in Table 3 below.

Table 3

Methylcyclohexane Activity for Several Catalysts

Catalyst ID	Temperature (°C):	MCH Conversion	C ₇ Paraffin Selectivity	C ₇ Paraffin Yield	C ₇ Naphthene Yield	C ₆ - Yield (no methane)
Catalyst J	384	88	46%	41.0	26.2	17.9
Catalyst K	412	89	46%	40.6	16.1	23.0
Catalyst L	369	91	28%	25.5	29.9	15.4
Catalyst M	393	95	4%	4.3	10.7	77.7
Catalyst N	386	89	61%	54.3	13.9	18.7
Catalyst O	410	92	62%	56.7	6.6	23.4

CLAIMS:

1. A catalyst for opening cyclic paraffins comprising a Group VIII (IUPAC Groups 8-10) metal component, a modifier component, a molecular sieve and a refractory inorganic oxide, wherein the molecular sieve is selected from the group consisting of UZM-4, UZM-4M, UZM-5, UZM-5HS, UZM-5P, UZM-6, UZM-8, UZM-8HS, UZM-15, UZM-15HS, UZM-16, UZM-16HS and mixtures thereof; and wherein the modifier component is selected from the group consisting of titanium, niobium, rare earth elements, tin, rhenium, zinc, germanium and mixtures thereof.

2. The catalyst of claim 1 where the Group VIII metal is selected from the group consisting of platinum, palladium, rhodium, ruthenium, iridium and mixtures thereof.

3. The catalyst of claim 1 or 2 where the refractory inorganic oxide is selected from the group consisting of alumina, silica, silica/alumina, calcium oxide, magnesium oxide, clays, zirconia and mixtures thereof.

4. The catalyst of claim 1 where the rare earth element is selected from the group consisting of cerium, ytterbium, lanthanum, dysprosium and mixtures thereof.

5. A process for producing acyclic paraffins from cyclic paraffins comprising contacting a feed stream comprising cyclic paraffins with a catalyst at ring opening conditions to convert at least a portion of the cyclic paraffins to acyclic paraffins, the catalyst comprising the catalyst of any one of claims 1-4.

6. The process of claim 5 where the ring opening conditions include a temperature of 200°C to 600°C, a pressure of atmospheric to 20,684 kPag and a liquid hourly space velocity of 0.1 to 30 hr⁻¹.