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(54) ELECTROPROCESSED PHENOLIC MATERIALS AND METHODS

ELEKTROVERARBEITETE PHENOLISCHE MATERIALIEN UND VERFAHREN

MATIÈRES PHÉNOLIQUES SOUMISES À UN TRAITEMENT ÉLECTRIQUE ET PROCÉDÉS

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Description**BACKGROUND**

5 **[0001]** Engineered materials with controlled or unique structural attributes have found application in biomedical, military, filtration, catalyst, optics, and electronic fields. Researchers have, therefore, devoted their efforts into developing new fabrication technologies throughout the last decade. Specifically, the fundamental understanding and development of nano-sized materials have become an area of increasing popularity.

10 **[0002]** A nanometer is a billionth of a meter, or 10^{-9} m. Nanotechnology is the study and use of materials, devices, and systems of the scale of about one nanometer up to about 100 nanometers. One reason for the interest in materials of this size is the discovery that some essential properties of materials, such as strength and fatigue, are nonlinearly and individually based on the microstructure of materials. Another major driving force behind the interest in nanotechnology is the desire to build smaller, lighter, stronger, and faster devices. If researchers can learn to manipulate individual atoms on the nanometer scale, some experts believe that the results could lead to a revolution in computing, electronics, energy, materials design, manufacturing, medicine, and numerous other fields.

15 **[0003]** Electrospinning is a non-conventional fiber fabrication technique that can be used to produce fibers with diameters on the nanometer scale. It is also useful for the production of microfibers, which have larger diameters than nanofibers (from about 0.1 microns to several tens of microns). The vast majority of research and development of electrospinning has viewed the technique as a terminal process in the fabrication of fibers. By way of example, investigators have studied various polymer systems for "spinnability", characterized the fiber surfaces and dimensions, examined the topology, and performed systematic studies of processing variables to improve fundamental understanding of the process and the fibers produced. However, extremely little has been done in the area of using electroprocessing as a precursor to subsequent processing steps.

20 **[0004]** Despite the developments to date, there remains a need for electroprocessing techniques that provide an attractive avenue for fabrication of novel materials with enhanced or "tunable" characteristics not obtainable by other means. Preferably, such techniques would use electroprocessing to produce fibers and materials of nano- or micro-scale dimensions, which are subjected to further processing to create materials tailored to specific applications of interest. More preferably, it would be desirable to develop material fabrication techniques in which electroprocessing is used as a precursor step to subsequent processing steps.

30

SUMMARY

35 **[0005]** Electropocessed phenolic materials, including nanofibers, microfibers, beads, films and materials comprising these electropocessed phenolic materials are provided. In addition, processes for synthesizing these electropocessed phenolic materials are provided.

40 **[0006]** In one embodiment a process for making electropocessed phenolic materials is provided. The process comprises providing a phenolic polymeric system and electropocessing the phenolic polymeric system to create electropocessed phenolic materials. The process preferably further comprises curing the phenolic materials, and carbonizing the cured materials to provide carbonized phenolic materials. The electropocessing may be performed by electrospinning or electrospraying the phenolic polymeric system.

45 **[0007]** In another embodiment a process for making activated electropocessed materials is provided. The process comprises activating an electropocessed material under activating conditions. Preferably the electropocessed material is an electropocessed phenolic material.

50 **[0008]** In yet another embodiment a process for making phenolic fibers is provided. The process comprises providing a phenolic polymeric system and electrostatically spinning the phenolic polymeric system to create phenolic fibers. The process preferably further comprises curing the phenolic fibers, and carbonizing the cured fibers to provide carbonized phenolic fibers.

55 **[0009]** A further embodiment relates to a process for making phenolic beads. The process comprises providing a phenolic polymeric system, and electrostatically spraying the phenolic polymeric system to create phenolic beads, the beads having a diameter of 100 nanometers to 10 microns.

60 **[0010]** In another embodiment, a process for making phenolic beads comprises providing a phenolic polymeric system, electrostatically spraying the phenolic polymeric system to create beads, the beads having a diameter of 100 nanometers to 10 microns. The process further comprises curing the phenolic beads; and carbonizing the cured phenolic beads to provide carbonized phenolic beads.

65 **[0011]** A fibrous material can be produced comprising a non-woven network of carbonized phenolic fibers wherein the carbonized phenolic fibers have a diameter of 10 microns to 50 nanometers. Preferably, the fibers have a relatively large BET surface area and a uniform pore size distribution.

70 **[0012]** Phenolic beads can be produced by an electrospraying process. Phenolic beads may be electrosprayed to

form a film or may be electrosprayed and collected as individual beads.

[0013] A smoking article can be provided which comprises a filter comprising electrospun carbonized fibers. In exemplary embodiments, the electrospun carbonized fibers are activated carbonized fibers.

[0014] A cigarette filter comprising electrospun carbonized fibers is also provided. In exemplary embodiments, the electrospun carbonized fibers are activated carbonized fibers.

[0015] A cut filler composition comprising electrospun carbonized fibers is also provided. In exemplary embodiments, the electrospun carbonized fibers are activated carbonized fibers.

[0016] An exemplary method of making a cigarette filter comprises incorporating electrospun carbonized fibers into a cavity and/or a component of a cigarette filter.

[0017] An exemplary method of making a cigarette comprises (i) providing a cut filler to a cigarette making machine to form a tobacco column; (ii) placing a paper wrapper around the tobacco column to form a tobacco rod; and (iii) attaching a cigarette filter including electrospun carbonized fibers to the tobacco rod to form the cigarette.

[0018] Another exemplary method of making a cigarette comprises (i) adding electrospun carbonized fibers to tobacco cut filler; (ii) providing the cut filler to a cigarette making machine to form a tobacco column; and (iii) placing a paper wrapper around the tobacco column to form a tobacco rod of the cigarette.

[0019] An exemplary method of smoking a smoking article comprises electrospun carbonized fibers, said method comprising lighting the article to form smoke and drawing the smoke through the article, wherein during the smoking of the article, the electrospun carbonized fibers preferentially remove one or more selected components from mainstream smoke.

[0020] In an exemplary embodiment a smoking article wrapper is provided, which comprises electrospun carbonized fibers. In exemplary embodiments, the electrospun carbonized fibers are activated carbonized fibers.

[0021] A smoking article can be provided which comprises a filter comprising electrosprayed carbonized beads. In exemplary embodiments, the electrosprayed carbonized beads are activated carbonized beads.

[0022] A cigarette filter comprising electrosprayed carbonized beads is also provided. In exemplary embodiments, the electrosprayed carbonized beads are activated carbonized beads.

[0023] A cut filler composition comprising electrosprayed carbonized beads is also provided. In exemplary embodiments, the electrosprayed carbonized beads are activated carbonized beads.

[0024] An exemplary method of making a cigarette filter comprises incorporating electrosprayed carbonized beads into a cavity and/or a component of a cigarette filter.

[0025] In an exemplary embodiment a smoking article wrapper is provided, which comprises electrosprayed carbonized beads. In exemplary embodiments, the electrosprayed carbonized beads are activated carbonized beads.

[0026] An exemplary method of making a cigarette comprises (i) providing a cut filler to a cigarette making machine to form a tobacco column; (ii) placing a paper wrapper around the tobacco column to form a tobacco rod; and (iii) attaching a cigarette filter including electrosprayed carbonized beads to the tobacco rod to form the cigarette.

[0027] Another exemplary method of making a cigarette comprises (i) adding electrosprayed carbonized beads to tobacco cut filler; (ii) providing the cut filler to a cigarette making machine to form a tobacco column; and (iii) placing a paper wrapper around the tobacco column to form a tobacco rod of the cigarette.

[0028] An exemplary method of smoking a smoking article comprises electrosprayed carbonized beads, said method comprising lighting the article to form smoke and drawing the smoke through the article, wherein during the smoking of the article, the electrosprayed carbonized beads preferentially remove one or more selected components from mainstream smoke.

BRIEF DESCRIPTION OF THE DRAWINGS

[0029]

FIG. 1 illustrates a setup for electrostatic processing.

FIG. 2A illustrates a cigarette design.

FIG. 2B illustrates another cigarette design.

FIG. 2C illustrates another cigarette design.

FIG. 2D illustrates another cigarette design.

FIG. 3A illustrates a SEM of electrospun polymer solution of a 1:1 ratio of 50 wt% novolak with 6.5% hexamethylene tetramine in ethanol and 40 wt% resole in ethanol (Example 1) spun at conditions of 15 kilovolts ($\pm 2\text{kV}$), 10 ml/hr ($\pm 4 \text{ ml/hr}$) and deposition distance of 17 cm ($\pm 2.5 \text{ cm}$).

FIG. 3B illustrates a SEM of cured (cross-linked) electrospun fibers (Example 1), from a polymer solution as described above in FIG. 3A. Curing conditions were a ramp rate of 0.1°C/min to 160°C, where the sample remained at the final temperature for 6 hours.

FIG. 3C illustrates a SEM of carbonized fibers (Example 1) from a polymer solution as described above in FIG.

3A. Conditions of carbonization were a ramp rate of 10°C/min to 800°C and remained at final temperature for 2 hours. FIG. 4 illustrates an adsorption isotherm of the carbonized fibers (Example 1) from a polymer solution as described above in FIG. 3A.

5 FIG. 5 illustrates results of BET surface area, micropore volume, and total pore volume for electrospun phenolic nanofibers, cured electrospun phenolic nanofibers, and carbonized electrospun phenolic nanofibers (Example 1) and for a non-electrospun phenolic polymer, a non-electrospun cured phenolic polymer, and a non-electrospun carbonized phenolic polymer (Example 2).

FIG. 6 illustrates the pore volume distribution from carbonized electrospun phenolic fibers (Example 1).

10 FIG. 7 depicts HRTEM images of carbonized electrospun phenolic resin fibers at (a) 1000°C, (b and c) 1600°C showing partial alignment; (d) graphite at 1600°C; and (e and f) 1800°C.

FIG. 8A depicts XRD for carbonized electrospun phenolic resin fibers at (a) 1000°C, (b) 1200°C, (c) 1400°C, (d) 1600°C, (e) 1800°C, and (f) 2000°C.

FIG. 8B depicts XRD for the sample holder.

15 FIG. 9 illustrates an SEM of phenolic beads produced by electrospraying (Example 5).

FIG. 10A illustrates a phenolic resin carbonized electrospun fibers (1:1 ratio of 50 wt% novolak and 50 wt% resole, both in EtOH).

FIG. 10B illustrates PAN carbonized electrospun fibers (10 wt% PAN in DMF).

10 FIG. 11 illustrates adsorption isotherms for carbonized electrospun PAN (10 wt % in DMF), Argon at 87.29K at carbonization temperatures of (a) 800°C, (b) 1000°C, (c) 1200°C, (d) 1400°C, and (e) 1600°C.

20 FIG. 12 depicts SEM micrographs of (a) 50 w/w% resole (in ethanol) electrospun fibers and (b) 50 w/w% novolak (in ethanol) electrospun fibers.

FIG. 13 depicts adsorption isotherms of argon at 87.29 K for carbonized electrospun phenolic resin fibers at (a) 600°C, (b) 800°C, (c) 1000°C, (d) 1200°C, (e) 1400°C, (f) 1500°C, (g) 1600°C, (h) 1800°C, and (i) 2000°C.

25 FIG. 14 depicts adsorption isotherms of argon at 87.29 K for (a) electrospun phenolic resin fibers and (b) cured electrospun phenolic resin fibers.

FIGS. 15A and 15B depict BET specific surface area for carbon electrospun fibers as a function of thermal treatment.

FIG. 16 depicts the pore size distribution using DFT for carbonized electrospun phenolic resin fibers. Curve (a) represents 800°C, curve (b) represents 1000°C, curve (c) represents 1200°C.

30 FIG. 17A depicts a HRTEM of carbonized "as-is" (no electrospinning) phenolic resin blend at 1800°C. Graphitization was not found to occur in the phenolic resins that had not been electrospun. This figure is a graph showing a comparison of reduction in formaldehyde delivery in a control cigarette versus a test cigarette including activated carbonized electrospun fibers.

FIG. 17B depicts a Fast Fourier transform of FIG. 17A showing a spacing between the sheets of about 3.7 Å.

35 FIG. 18 depicts a SEM of electrospun material produced when iron oxide nanoparticles were added to PAN fibers and carbonized at 1200°C.

FIG. 19 Adsorption Isotherms (Argon @87.29K) for green and activated phenolic resin carbonized electrospun fibers.

FIG. 20 Adsorption Isotherms (Argon @87.29K) for activated PAN conventionally-processed carbonized fibers.

FIG. 21 Adsorption Isotherms (Argon @87.29K) for green and activated PAN carbonized electrospun fibers.

40 FIG. 22 is a graph showing a comparison of reduction in formaldehyde delivery in a control cigarette versus a test cigarette including activated carbonized electrospun fibers.

DETAILED DESCRIPTION

[0030] Electroprocessed phenolic materials, including fibers, films and beads are provided. Fibers, fibrous mats, beads and films produced by electrostatic processing are attractive materials because they provide a high surface to volume ratio that is unattainable by conventional processing techniques, such as extrusion, dry spinning, wet spinning, melt spinning, and the like.

[0031] The properties of the electroprocessed phenolic materials may be tuned by post-electroprocessing treatments to provide the materials with properties suited for the intended use. These post-electroprocessing treatments include curing, carbonization, and activation.

Definitions

[0032] Unless otherwise stated, the following terms used in the specification and claims have the meanings given below:

55 "Halo" means fluoro, chloro, bromo, or iodo.

"Nitro" means the group -NO₂.

"Hydroxy" means the group-OH.

"Alkyl" means a linear saturated monovalent hydrocarbon group of one to twenty carbon atoms, preferably one to twelve atoms, or a branched saturated monovalent hydrocarbon group of three to twenty carbon atoms, preferably three to twelve atoms. Examples of alkyl groups include, but are not limited to, groups such as methyl, ethyl, n-propyl, isopropyl, n-butyl, isobutyl, sec-butyl, t-butyl, n-pentyl, and the like.

5 "Alkylene" means a linear divalent hydrocarbon group of one to twenty carbon atoms, preferably one to twelve atoms, or a branched divalent hydrocarbon group of three to twenty carbon atoms, preferably three to twelve atoms.

Examples of alkylene groups include, but are not limited to, methylene, ethylene, 2-methylpropylene, and the like.

10 "Alkenyl" means a linear unsaturated monovalent hydrocarbon group of two to twenty carbon atoms, preferably two to twelve, or a branched monovalent hydrocarbon group of three to twenty carbon atoms, preferably three to twelve atoms, containing at least one double bond, (-C=C-). Examples of alkenyl groups include, but are not limited to, allyl, vinyl, 2-but enyl, and the like.

15 "Alkynyl" means a linear monovalent hydrocarbon group of two to twenty carbon atoms, preferably two to twelve, or a branched monovalent hydrocarbon group of three to twenty carbon atoms, preferably three to twelve atoms, containing at least one triple bond, (C=C). Examples of alkynyl groups include, but are not limited to, ethynyl, propynyl, 2-butynyl, and the like.

"Haloalkyl" means an alkyl substituted with one or more, preferably one to 6, of the same or different halo atoms. Examples of haloalkyl groups include, for example, trifluoromethyl; 3-fluoropropyl, 2,2-dichloroethyl, and the like.

20 "Hydroxyalkyl" refers to an alkyl substituted with one or more -OH groups provided that if two hydroxy groups are present they are not both on the same carbon atom. Examples of hydroxyalkyl groups include, for example, hydroxymethyl, 2-hydroxyethyl, 2-hydroxypropyl, and the like.

"Alkylthio" refers to the group "alkyl-S-" which includes, by way of example, methylthio, butylthio, and the like.

"Cyanoalkyl" refers to an alkyl substituted with one or more -CN groups.

25 "Alkoxy" refers to the group "alkyl-O-" which includes, by way of example, methoxy, ethoxy, n-propoxy, iso-propoxy, n-butoxy, tert-butoxy, sec-butoxy, n-pent oxy, n-hexoxy, 1,2-dimethylbutoxy, and the like.

"Alkoxyalkyl" refers to the group "-alkylene-O-alkyl" which includes, by way of example, 2-propoxyethylene, 3-methoxybutylene, and the like.

30 "Alkenoxy" refers to the group "alkenyl-O-" which includes, by way of example, allyloxy, vinyloxy, 2-butenyloxy, and the like.

"Alkenoxyalkyl" refers to the group "alkenyl-O-alkylene-" which includes, by way of example, 3-allyloxy-propylene, 2-(2-propenoxy)ethylene, and the like.

35 "Haloalkoxy" refers to the group "haloalkyl-O-" which includes, by way of example, trifluoromethoxy, 2,2-dichloroethoxy, and the like.

"Haloalkylthio" refers to the group "haloalkyl-S-" which includes, by way of example, trifluoromethylthio, 2,2-difluoropropylthio, 3-chloropropylthio, and the like.

40 "Amino" refers to the group "-NR_aR_b" wherein R_a and R_b are independently H, alkyl, haloalkyl, alkenyl, cycloalkyl, aryl, substituted aryl, heteroaryl, or substituted heteroaryl.

"Carboxy" means the group "C(O)." "

45 "Acyloxy" means the group -C(O)R' wherein R' is alkyl, alkenyl, alkynyl, aryl, substituted aryl, heteroaryl, or substituted heteroaryl.

"Cycloalkyl" means a cyclic saturated hydrocarbon group of 3 to 8 ring atoms, where one or two of C atoms are optionally replaced by a carbonyl group. The cycloalkyl group may be optionally substituted with one, two, or three substituents, preferably alkyl, alkenyl, halo, hydroxyl, cyano, nitro, alkoxy, haloalkyl, alkenyl, and alkenoxy. Representative examples include, but are not limited to, cyclopropyl, cyclohexyl, cyclopentyl, and the like.

50 "Aryl" means a monovalent monocyclic or bicyclic aromatic carbocyclic group of 6 to 14 ring atoms. Examples include, but are not limited to, phenyl, naphthyl, and anthryl. The aryl ring may be optionally fused to a 5-, 6-, or 7-membered monocyclic non-aromatic ring optionally containing 1 or 2 heteroatoms independently selected from oxygen, nitrogen, or sulfur, the remaining ring atoms being C where one or two C atoms are optionally replaced by a carbonyl. Representative aryl groups with fused rings include, but are not limited to, 2,5-dihydro-benzo[b]oxepine, 2,3-dihydrobenzo[1,4]dioxane, chroman, isochroman, 2,3-dihydrobenzofuran, 1,3-dihydroisobenzofuran, benzo[1,3]dioxole, 1,2,3,4-tetrahydroisoquinoline, 1,2,3,4-tetrahydroquinoline, 2,3-dihydro-1H-indole, 2,3-dihydro1H-isoindole, benzimidazole-2-one, 2-H-benzoxazol-2-one, and the like.

55 "Substituted aryl" means an aryl ring substituted with one or more substituents, preferably one to three substituents selected from the group consisting of alkyl, alkenyl, alkynyl, halo, alkoxy, acyloxy, amino, hydroxyl, carboxy, cyano, nitro, and thioalkyl. The aryl ring may be optionally fused to a 5-, 6-, or 7-membered monocyclic non-aromatic ring optionally containing 1 or 2 heteroatoms independently selected from oxygen, nitrogen, or sulfur, the remaining ring atoms being C where one or two C atoms are optionally replaced by a carbonyl.

"Heteroaryl" means a monovalent monocyclic or bicyclic aromatic radical of 5 to 10 ring atoms containing one, two, or three ring heteroatoms selected from N, O, or S, the remaining ring atoms being C. Representative examples

include, but are not limited to, thienyl, benzothienyl, pyridyl, pyrazinyl, pyrimidinyl, pyridazinyl, quinolinyl, quinoxalinyl, imidazolyl, furanyl, benzofuranyl, thiazolyl, isoxazolyl, benzisoxazolyl, benzimidazolyl, triazolyl, pyrazolyl, pyrrolyl, indolyl, 2-pyridonyl, 4-pyridonyl, N-alkyl-2-pyridonyl, pyrazinonyl, pyridazinonyl, pyrimidinonyl, oxazolonyl, and the like.

5 "Substituted heteroaryl" means a heteroaryl ring substituted with one or more substituents, preferably one to three substituents selected from the group consisting of alkyl, alkenyl, alkynyl, halo, alkoxy, acyloxy, amino, hydroxyl, carboxy, cyano, nitro, and thioalkyl.

"Aryloxy" means a group "-O-Ar" where Ar is an aryl group or substituted aryl group. Examples include, but are not limited to, benzyloxy, 4-trifluoromethyl-benzyloxy, and the like.

10 "Arylalkoxy" means a group "-O-alkylene-Ar" where Ar is an aryl group or substituted aryl group. Examples include, but are not limited to, 2-(phenyl)ethoxy, 3-(phenyl)propoxy, and the like.

"Arylalkoxyalkyl" means a group "-alkylene-O-alkylene-Ar" where Ar is an aryl group or substituted aryl group. Examples include, but are not limited to, benzyloxy-propylene, benzyloxy-ethylene, and the like.

15 "Alkylcarboxyalkyl" means a group "-R'(O)R" where R' is an alkylene group and R is an alkyl group as defined above.

"Carboxylic" means a group -C(O)-OH.

"Alkyloxycarboxy" means a group -C(O)-OR where R is an alkyl group as defined above.

"Sulfonic acid" means a -SO₃H group.

20 "Electroprocessing or electrostatic processing" refers to techniques for forming materials from polymeric systems by subjecting the polymeric system to an electric field. Electroprocessing includes the techniques of electrospinning and electrospraying, as described herein. The techniques of electroprocessing may be used to create nanofibers, microfibers, beads, thin films, or combinations thereof.

25 "Electroprocessed materials" refer to materials created by electroprocessing polymeric systems. Electroprocessed materials include nanofibers, microfibers, wet particles which coalesce into beads, beads or fibers precipitated out of non-compatible solvents, thin films, dry porous films, fibrous mats or webs, and the like, and combinations thereof.

25 [0033] Electroprocessed materials as described herein are created by electrospinning and/or electrospraying a precursor polymer system. Preferably, the precursor polymer system is a phenolic polymer system. Accordingly, the electroprocessed materials as described herein are made by electrostatically processing a phenolic polymeric system. This phenolic polymeric system may be a phenolic polymer solution or a phenolic polymer melt.

30 **Phenolic Polymer System**

[0034] The phenolic polymers of the solution or melt may be any phenolic polymers, including commercially available phenolic resins and phenolic polymers synthesized by techniques known to those of skill in the art, phenolic copolymers, 35 blends of phenolic polymers with other polymers, and phenolic polymers, phenolic copolymers, and blends containing additives, and mixtures thereof.

[0035] In the phenolic polymer, the phenyl ring is substituted with one or more hydroxy groups, preferably one or two. The phenyl rings of the phenolic polymers may also be substituted with one or more functional groups such as halo; 40 nitro; alkyl; alkenyl; alkynyl; haloalkyl; hydroxyalkyl; cyanoalkyl; alkylthio; alkoxy; alkoxyalkyl; alkenoxy; alkenoxyalkyl; haloalkoxy; haloalkylthio; amino; carboxylic; acyloxy; cycloalkyl; aryl; substituted aryl; heteroaryl; substituted heteroaryl; aryloxy; arylalkoxy; arylalkoxyalkyl; alkylcarboxylalkyl; alkyloxycarboxy, sulfonic acid, and combinations thereof.

[0036] The hydroxy group or the other functional groups may be reacted to provide additional types of functionalization in the phenolic polymers. For example, a hydroxy group of the phenolic polymer may be reacted with aminopropylsilane to graft an amino functional group onto the phenolic polymer. These functional groups will be retained after electrostatically 45 processing the phenolic polymers.

[0037] The molecular weight of the phenolic polymers may vary as long as the phenolic polymers can be electrostatically processed, as desired. In fact, the desired molecular weight of the phenolic polymers may vary depending on whether a phenolic solution or phenolic polymeric melt is to be electrostatically processed. In addition, if a phenolic solution is to be electrostatically processed, the molecular weight may vary as the concentration of the solution varies. Furthermore, 50 the molecular weight of the phenolic polymers may vary according to the technique to be used to electroprocess the polymeric system (i.e., whether the polymeric systems are to be electrospun or electrosprayed). In addition, the molecular weight of the phenolic polymers may vary according to which phenolic polymer is being used. In general, it is desirable to use a phenolic polymer which is as linear as possible with as high of a molecular weight as is possible while maintaining the desired linearity.

55 [0038] In general, in electroprocessing the molecular weight of the phenolic polymer may be between about 900 and 50,000. If the phenolic polymer is to be electrospun, for example, the molecular weight is preferably between about 9,000 and 30,000. The higher molecular weight linear phenolic polymers, in particular novolak, may spin at similar weight percent conditions in solvent as lower molecular weight branched phenolic polymers. Using a higher molecular weight

solution with a similar concentration may afford additional strength to the resulting nanofibers.

[0039] Commercially available phenolic polymers are available as phenolic resins. Phenolic resins are the condensation product of phenol and formaldehyde and can be differentiated into primarily two types, novolak and resole, depending on the reactant ratio and the catalyst used. Novolaks are made with an acid catalyst and with a formaldehyde/phenol ("F/P") ratio of less than one, so they have a linear structure and are cured with a cross-linking agent. Resoles are made with an alkaline catalyst and with a phenol/formaldehyde ("F/P") ratio of \geq one, so they have multifunctionality structure that can be cured by itself with no need for a curing agent. The phenolic polymers may be commercially available novolaks, commercially available resoles, and mixtures thereof. Novolak phenolic resins are commercially available in a variety of molecular weights, all of which may be herein suitable, and are commercially available from Durez Corporation (Addison, TX). Resole phenolic resins are also commercially available in a variety of molecular weights, all of which may be herein suitable, and are also commercially available from Durez (Addison TX).

[0040] Carbon materials derived from novolak phenolic resins are also available as Novocarb™ from Mast Carbon Ltd. (United Kingdom) and Novoloid™ from American Kynol, Inc. (Pleasantville, NY). Phenolic resins are also available as Bakelite AG™ from Georgia Pacific (Atlanta, GA). Additionally, phenolic resins are commercially available from a variety of manufacturers, including, for example, Amoco Electronic Materials (Alpharetta GA), Cytec Fiberite, Inc. (Tempe, AZ), Occidental Chemical Corp (Dallas, TX), Plaslok Corp. (Buffalo, NY), Plastics Engineering, Inc. (Auburn Hills, MI), Resinoid Engineering Corp. (Hebron, OH), Rogers Corp. (Rogers, CT), Ametek/Westchester Plastics (Nesquehoning, PA), Schenectady International, Inc. (Schenectady, NY), Solutia, Inc. (St. Louis, MO), and Union Carbide Corp. (Danbury, CT).

[0041] Commercially available phenolic resins are relatively inexpensive polymers, thus providing relatively inexpensive electroprocessed materials, including nanofibers, microfibers, films, and the like and combinations thereof, and end-use products in which the electroprocessed materials are used. Since the phenolic resins are relatively inexpensive, they have advantages in large-scale production of electroprocessed materials and products containing these electro-processed materials. Other advantages of electroprocessed materials from phenolic resins include a high chemical yield, high chemical purity, good biocompatibility, low toxicity characteristics, high thermal resistance, resistance to corrosion, and easy activation for use as adsorbents.

[0042] In addition to commercially available phenolic polymers, the phenolic polymers may be synthesized by any technique to synthesize phenolic polymers. These techniques include, for example, condensing any reactive phenol or substituted phenol with a reactive aldehyde. In addition, techniques to synthesize phenolic polymers include polymerization of phenols or substituted phenols using enzymes, as described in Akkara, et al., "Synthesis and Characterization of Polymers Produced by Horseradish Peroxidase in Dioxane," *Journal of Polymer Science: Part A: Polymer Chemistry*, vol. 29, (1991) 1561-1574. Phenols, which can be used to synthesize the phenolic polymers, include, for example, phenol [C₆H₅OH], cresoles (including meta-, ortho-, para-, and mixtures thereof) [CH₃C₆H₄OH], xylenols [(CH₃)₂C₆H₃OH], p-phenylphenol [C₆H₅C₆H₄OH], bisphenols [(C₆H₄OH)₂], resorcinol [C₆H₄(OH)₂], p-tertiarybutylphenol, alkyl substituted phenol, diphenylolpropane, and the like, and mixtures thereof. Reactive aldehydes, which can be used to synthesize the phenolic polymers, include, for example, formaldehyde and furfural.

[0043] Resole and novolak can be synthesized from the reaction of formaldehyde with phenol. Whether resole or novolak is formed is dependent upon the mode of catalyst and molar ratio of formaldehyde, to phenol. See, e.g., Gardziella, A.; Pilato, L.A.; Knop, A *Phenolic Resins: Chemistry, Applications, Standardization, Safety and Ecology*, 2nd Ed., Springer-Verlag: Berlin, 2000. Different curing conditions are generally used to crosslink resole and novolak resins. Resoles can be cured by thermal treatment, acids or bases or possibly by other special curing systems, such as carboxylic acid esters, anhydrides, amides and carbonates, which have been reported to accelerate the curing process. See, e.g., Peng, W; Riedl, B.; Barry A.O. *J. Appl. Poly Sci.* 1993, 48, 1757. Curing novolak requires a source of formaldehyde or the commonly utilized curing agent, hexamethylenetetramine; additionally, other methods have been reported which consist of solid resole, bismethyol cresol, bisoxazolines, and bisbenzoxazines. See, e.g., Sergeev, V.A. et al, *Poly Sci. Ser B*, 1995, 37: 5/6, 273; Cuthbertson, B.M.; Tilsa, O.; Devinney, M.L.; Tufts TA, *SAMPE* 1989, 34: 2483; and Pilato, L.A.; Michno, M.J. *Advanced Composite Materials*, Springer-Verlag: Berlin, 1994.

[0044] The phenolic polymers may also be copolymers of a phenolic polymer and a copolymerizable monomer. These copolymerizable monomers include, for example, cresols (including meta-, ortho-, para-, and mixture thereof), xylenols, p-phenylphenol, bisphenols, resorcinol, p-tertiarybutylphenol, alkyl substituted phenol, diphenylolpropane, phenols with additional polymerizable functionality, such as p-vinyl phenol or methacrylates such as 2-(4-hydroxyphenyl)ethyl methacrylate, and the like, and mixtures thereof. The copolymerizable monomers may also include polyesters, unsaturated polyesters, epoxies, melamine-formaldehyde, polyimides, urea-fonnaldehydes, and the like, and mixtures thereof. The copolymerizable monomers may further include styrene, diallyl phthalate, diacetone acrylamide, vinyl toluene, and the like, and mixtures thereof.

[0045] For instance, the phenolic polymer(s) and co-polymerizable monomer(s) can be copolymerized in an organic solvent polymerization medium in the presence of a polymerization initiator to produce a phenolic copolymer. The sequence of addition of the phenolic polymer(s) and monomer(s) to be copolymerized and initiation of polymerization

may be varied so long as a phenolic co-polymer is formed. For instance, all monomers to be copolymerized may be added to a reaction vessel and then polymerization may be initiated. In the alternative, a portion of the phenolic polymer(s) and monomers may be added to the reaction vessel, and polymerization may be initiated. Within an appropriate amount of time, the remaining phenolic polymer(s) and/or monomers may be added, wherein the remaining phenolic polymers and monomers may be added all at once or in stages so long as a phenolic co-polymer is formed. Preferably, all phenolic polymer(s) and monomers to be copolymerized are initially added to the reaction vessel and then polymerization is initiated. After co-polymerization, the reaction mixture may be cooled and dried, if desired, to provide a friable resin. The friable resin may be pulverized to provide a powdered phenolic co-polymer.

[0046] The phenolic polymers may also be a blend of a phenolic polymer with any other polymer system that is miscible with the phenolic polymeric solution or melt. Phenolic polymers may be miscible with any polymer system that is a hydrogen bond acceptor. The polymers that may be blended with the phenolic polymers include, for example, poly(acrylic acid), poly(vinyl acetate), cellulose acetate, poly(ethyleneimine), poly(ethylene-co-vinylacetate), poly(lactic acid), mixtures thereof, and the like. The phenolic polymer may be blended with an additional polymer system to provide, enhance, or alter specific properties of the ultimate phenolic electroprocessed material. Accordingly, a miscible polymer system may be selected based on the property to be provided, enhanced, or altered. For example, to improve mechanical properties of phenolic fibers, the phenolic polymers may be blended with poly(acrylic acid). The miscible polymer system, which is selected, is blended into the phenolic polymeric solution or melt prior to electrostatically processing.

[0047] The phenolic polymers may also be blended or doped with additives to provide, enhance, or alter specific properties of the electrostatic processing of the phenolic polymeric solutions. In addition, additives may be added to provide, enhance or alter specific properties the phenolic electroprocessed material obtained or to aid in the subsequent processing of the phenolic material. Examples of additives suitable for use in the phenolic polymers include, for example, dispersed metals of various dimensions and geometries, metal oxides, metal salts, surfactants, curing/cross-linking agents, stabilizers, porosity enhancers, non-volatile and non-compatible solvents, various salts, and mixtures thereof. The additives may act during carbonization to stabilize or to facilitate carbonization. Particular examples of additives include copper nanoparticles, iron oxide nanoparticles, hexamethylenetetramine, PtCl_2 , and the like.

[0048] In addition, after processing the resulting electroprocessed material may be infused with an additive. As such, the cured phenolic materials may be impregnated with metal salts or metal particles by dipping the cured phenolic materials in a metal salt solution or impregnating the phenolic materials with metals. In addition, the cured phenolic materials may be dipped in base to create a phenoxide material. This phenoxide material may be dipped in a metal salt solution to create phenoxide salts. In addition, the cured phenolic materials may be sulfonated.

[0049] The phenolic polymers may be provided for electrostatic processing as a solution, dispersion, or melt. A phenolic polymer solution is a solution of phenolic polymers in an appropriate solvent. A phenolic polymeric dispersion of phenolic polymers in an appropriate solvent may also be used in the process. The solvent of the solution may be any volatile solvent in which the phenolic polymers (including phenolic polymers, copolymers, blends, and phenolic polymers, copolymers, and blends containing additives) are soluble. The solvent should not deleteriously impact the electrostatic processing. Namely, the solvent should sufficiently evaporate from the fiber without leaving a residue that will deleteriously impact the physical properties of the resulting phenolic electrostatically processed material.

[0050] Advantageously the phenolic polymers are relatively readily dissolved and as such are soluble in solvents that are relatively friendly. Therefore, solvents in which the polymers are soluble have relatively low toxicity (i.e., have LD_{50} values) and are generally considered safe to use. Solvents that may be used include alcohols, ketones, chlorinated hydrocarbons, and mixtures thereof. In addition, solvents that may be used include aqueous mixtures of one or more alcohols, fluorinated alcohols, ketones, and bases (organic bases or inorganic bases). In particular, the solvents include, for example, acetone, ethanol, isopropyl alcohol, hexafluoropropanol, ethyl acetate, dichloromethane, and mixtures thereof and aqueous mixtures of one or more of ethanol, acetone, isopropyl alcohol, and a base such as ammonium hydroxide, and the like.

[0051] As described above, solvents, which may be suitable for use in the present process, may be preferred to many solvents typically used in electrostatic processing, as the solvents typically used tend to be considerably more toxic and are typically not considered safe for general use. Other polymeric systems, such as poly(acrylonitrile) (PAN), are not as readily soluble as the phenolic polymers and thus require solvents that are not considered as friendly. These typical solvents include N,N-dimethylacetamide, dimethylformamide, and dimethylsulfoxide. The solvents, which can be used in the present process, are easily handled on both a small scale and a large scale, thus providing additional advantages for large-scale production.

[0052] The concentration of the phenolic polymeric solutions may vary as long as the phenolic polymeric solution can be electrostatically processed, as desired. In fact, the desired concentration of the phenolic polymeric solution may vary depending on whether a phenolic solution is to be electrospun or electrosprayed. In addition, the concentration of the phenolic solution may vary as the molecular weight of the phenolic polymer used varies. In addition, the concentration of the phenolic polymers may vary according to which phenolic polymer is being used.

[0053] In electroprocessing the concentration of the phenolic polymeric solution may be between about 5 to greater

than 90 weight percent phenolic polymeric system. If the phenolic polymer is to be electrospun, for example, the concentration is preferably between about 40 to 60 weight percent phenolic polymeric system. The weight percent is based on the total phenolic polymeric system including any co-polymerizable monomers, other miscible polymer systems, additives, as well as the phenolic polymer. By way of example, a higher molecular weight phenolic polymer may be electroprocessed at a lower concentration and a lower molecular weight phenolic polymer may be electroprocessed at a higher concentration.

Preparing the Phenolic Polymer System

10 [0054] The phenolic polymeric solutions are made by selecting the proper amounts of the components of the phenolic polymeric solution, including phenolic polymers, co-polymerizable monomers, other polymers to be blended, and additives, and thoroughly mixing the components in an appropriate solvent by techniques known to those of skill in the art. For example, the phenolic polymer components may be added to a solvent with stirring. In addition, the phenolic polymer components may be added to a solvent and agitated with shaking on a platform shaker.

15 [0055] The sequence of addition of the components of the phenolic polymeric solution to the solvent and mixing until dissolved may be varied so long as a phenolic polymeric solution is prepared. For example, all components of the polymeric solution including any additives may be added to a solvent at once and then mixed until dissolved together. In the alternative each component may be added sequentially with mixing until each is dissolved before adding the next component. By way of example, one phenolic polymer may be added and mixed until dissolved. After the first is dissolved, 20 a second phenolic polymer may be added to the solution and mixed until dissolved. Then an additive may be added to the solution of the two phenolic polymers and mixed until dissolved, and so on. Or if the polymeric solution is a mixture of two phenolic polymeric solutions (for example, resole and novolak), two separate phenolic polymeric solutions may be prepared by adding each phenolic polymer individually to a solvent and mixing until dissolved and then the individual 25 solutions may be mixed together. If any additives are desired in this mixture of phenolic polymeric solutions, the additives may be added to the individual phenolic polymer solutions before mixing them together or the combined mixture of the polymeric solutions.

[0056] If the phenolic polymer is to be a co-polymer of a phenolic polymer and a co-polymerizable monomer, then the phenolic polymer and co-polymerizable monomer are mixed under conditions to be co-polymerized prior to forming the phenolic solution. The co-polymer obtained is then mixed with an appropriate solvent.

30 [0057] In the alternative, the phenolic solution may comprise 100 weight % phenolic polymers and thus may be a polymer melt. Polymer melts comprising phenolic polymers may be prepared by techniques known to those of skill in the art. To melt blend the components of the phenolic solution, the powdered phenolic polymers may be premixed. Premixing may be achieved by any suitable means. An illustrative small-scale mixer is a Vitamixer of the Vitamix Corporation in Cleveland, Ohio. The premixed components are then placed in a heated extruder where the mixture is melt 35 mixed. The phenolic polymer melt can be electrostatically processed in the same manner as a phenolic polymeric solution. The phenolic polymer melt may be electrostatically processed by techniques as described in Larrondo, L. and St. John Manley, J. "Electrostatic Fiber Spinning from Polymer Melts, I. Experimental Observations on Fiber Formation and Properties," Journal of Polymer Science, Polymer Physics Ed., vol. 19, (1981) 909-920, the contents of which are herein incorporated by reference in their entirety.

Electrostatic Processing

40 [0058] After a phenolic polymeric system comprising phenolic polymers, and optionally additives is prepared, the phenolic system is electrostatically processed to create phenolic nanofibers, microfibers, and films or materials comprising these electrospun phenolic materials. For example, the phenolic polymeric system can be electrostatically spun to create phenolic fibers and mats or webs comprising these fibers. Also, the phenolic polymeric systems can be electrostatically sprayed to create films. The phenolic polymeric system can be electrostatically processed (i.e., spun or sprayed) using equipment for electrostatically processing of polymers, such as described in, Kenawy, et al., "Electrospinning of Poly(ethylene-co-vinyl alcohol) Fibers," Biomaterials, vol. 24 (2003) 907-913, the contents of which are herein incorporated by reference in their entirety. In contrast to conventional fiber forming techniques, such as melt or dry spinning, which 45 generally produce fibers which are on the order of 10 μm in diameter, electroprocessing generates fibers of nano-sized dimensions. The electroprocessing technique involves applying a high voltage to a capillary and pumping a polymer solution or melt through it. Nano-fibers of polymer collect as a non-woven mat on a grounded target some distance from the source. The mechanism is simple in the absence of an electric field; the fluid forms a droplet at the exit of the capillary 50 and its size is determined by surface tension. When an electric field is present, it induces charges into the fluid, which quickly relax to the surface. The coupling of the surface charges and the external electric field creates a tangential stress, resulting in the deformation of the droplet into a conical shape (Taylor cone). See, e.g., Taylor, Sir G., Proc. Roy. Soc. London A 1969, 313, 453. Once the electric field exceeds a critical value needed to overcome the surface tension, a

fluid jet ejects from the apex of the cone. Both electrostatic and fluid dynamic instabilities can contribute to the basic operation of the process. Properties of the polymer and fluid combined with the process variables dictate whether the operating regime is one of electrospraying or electrospinning.

[0059] Electrospraying is typically observed in low molecular weight and/or low concentration polymeric solutions where molecular chain entanglements are not sufficient enough to support a developing fiber filament. Instead, the ejected jet breaks up into small droplets as the applied electric field overcomes the surface tension of the solution. Electrospinning is the preferred mechanism for fiber formation. At sufficiently high concentration, with the advantage of chain entanglements, fluid instability forms a continuous, small-diameter whipping filament that thins as it bends and accelerates over a large path length before reaching the target. See, e.g., Reneker, D.H.; Yarin, A. L.; Fong, H. and Koombhongse, S. J. Applied Physics 2000, 87 (9), 4531. Electric field strength and solution concentration are two key variables influencing the resulting fiber characteristics.

[0060] In general, electrospraying utilizes experimental apparatuses that are similar to those used for electrospinning. As used herein, the terms electrostatically processing and/or electroprocessing includes the technique of electrospinning and electrospraying.

[0061] In a preferred embodiment, the technique of electroprocessing uses a delivery means, an electric field, and a capture point; which may include a capture or collection means. The delivery point is simply a place where at least one droplet of the phenolic polymeric system can be introduced or exposed to an electric field. This delivery point can be oriented anywhere in space adjacent to the electric field, for example, below the electric field or horizontally adjacent to the electric field. The capture point is simply a place where the stream or jet of polymeric fibers or droplets can be collected. It is preferred that the delivery point and capture point be conductive so as to be useful in creating the electric field. But it should be understood that the apparatus is not limited to this type of configuration or setup inasmuch as the delivery point and capture point can be non-conductive points that are simply located within or adjacent to an electric field.

[0062] The electric field should be strong enough to overcome gravitational forces on the polymeric solution, overcome surface tension forces of the polymeric system, provide enough force to form a stream or jet of solution in space, and accelerate that stream or jet across the electric field. As the skilled artisan will recognize, surface tension is a function of many variables. These variables include the type of polymer, the type of solvent, the solution concentration, and the temperature. It may be useful to electroprocess within a vacuum environment because greater electrical forces can be used within the vacuum.

[0063] In electrospinning, the concentration of the phenolic polymeric system should be high enough so that randomly coiled polymeric molecules within the solution can come together and form an oriented array of fibers. As described above, in electrospinning preferably a phenolic polymeric solution is utilized and the phenolic polymeric solution is 40 to 60 weight percent phenolic polymers.

[0064] In a preferred embodiment, the electroprocessing apparatus is configured as illustrated in FIG. 1, so that the stream of phenolic system is pulled horizontally through space. As illustrated in FIG. 1, a delivery means 10, which is a syringe, a grounded collecting means 20, a power supply 30 for generating an electric field are present. As noted above, the technique employed in electroprocessing the phenolic polymeric systems need not employ a delivery means that horizontally delivers the phenolic polymeric system to the electric field. It has, however, been found to be particularly useful to employ this configuration because the horizontal delivery configuration can be used in conjunction with a pumping means that allows the system to be pumped to the tip of the delivery means at a constant volume rate so that skins that are sometimes found on the surface of the system are continuously broken as the system is delivered to the electric field. It should be appreciated that the dripping of the system from the delivery means should be avoided. To do so, the pressure at the orifice of the delivery means should be less than that associated with the surface tension of the system. The skilled artisan will appreciate that there are other ways by which one could control the delivery of the phenolic polymeric system to the electric field. Other techniques include manipulating the size of the orifice of the delivery means, or manipulating the air pressure above the system within the delivery means.

[0065] Accordingly, the phenolic polymeric system is introduced to the electrified field via a charged delivery device or charged means for delivering the phenolic polymeric system. These devices or means should include an orifice that is capable of delivering a controlled amount of phenolic polymeric system. The preferred orifice has a diameter from about 0.5 to about 1.0 mm. As noted above, it is preferred that the phenolic polymeric system be delivered to the electrified field horizontally so that gravitational forces do not introduce an excess amount of phenolic polymer into the electrified field. In one example (as shown in FIG 1), a phenolic polymeric system is delivered to an electrified field via a horizontally mounted syringe (10). In another example, a pipet containing a conductive portion, such as a wire, can be used. The skilled artisan will be able to readily select other devices or means that can deliver a controlled amount of phenolic polymeric system to the electrified field. A delivery means is not necessary for carrying out the electrostatic processing inasmuch as phenolic fibers can be produced from a simple droplet of solution. Also, electroprocessing can be carried out from a beaker of solution, from a watch glass of solution, or any device for holding an amount of phenolic polymeric system.

[0066] Preferably, the stream of fiber from the phenolic polymeric system is delivered to a collecting or capturing device

(20), or means for capturing the stream of fibers or the film. Examples of a capturing device or means for capturing include, but are not limited to, a wire mesh, a polymeric mesh, a rotating cylinder, a metal grid, metal foil, paper, a syringe needle, a decomposable substrate such as a decomposable polymer fiber, an electrospun substrate, and the like. The skilled artisan will be able to readily select other devices or means that can be employed to capture the fibers as they travel through the electric field. The collecting or capturing device is preferably grounded to attract the charged phenolic fibers. The capturing device can be selected based on the intended use of the phenolic material. By spinning onto an electrospun substrate, a laminate of electrospun materials can be created.

5 [0067] The collecting or capturing device can be of different morphologies and geometries and the electrostatically produced fibers or film can acquire these different geometries when dried. An example of a specific geometry may be a web of a single layer, multiple layer, interlaced fibers of different sources, hollow tubes, and the like.

10 [0068] As the skilled artisan will recognize, the electrified field necessary to create a stream of fibers through space can be achieved by charging the delivery means or the capture means. Where the delivery means is charged, the capture means will be grounded (as illustrated in FIG. 1); and where the capture means is charged, the delivery means will be grounded.

15 [0069] In one embodiment, electrospinning a solution of from about 40 to about 60 weight percent of phenolic polymeric solution in ethanol at room temperature and atmospheric pressure, is carried out using an electric field of about 0.5 to about 5 kV/cm. In another embodiment, a 50/50 solution of from about 40 to about 60 weight percent of resole and about 40 to 60 weight percent of novolak in ethanol, at room temperature and pressure, is electrospun using an electric field of from about 1 to about 2 kV/cm. The spinning rate can be controlled by adjusting both the flow of the phenolic solution 20 and the electric field.

[0070] In contrast to electrostatic spinning, electrostatic spraying occurs when the phenolic system does not flow smoothly from the delivery means through the electric field to the collection means and instead forms droplets or clusters of solution that are sprayed onto the collection means in distinct units. While an electrospun fiber continuously collects on the collection means, the electrosprayed beads collect in individual, distinct droplets.

25 [0071] Whether phenolic materials are formed by electrostatic spraying or spinning can be controlled by manipulating components of the polymeric system and/or changing process parameters such as applied voltage, distance to target, volumetric flow rate, and the like. In addition, whether a solution electrospins or electrosprays can be controlled by changing physical characteristics of the phenolic polymeric system such as changes in concentration, solvent selection, polymer molecular weight, polymer branching, and the like.

30 [0072] Once the materials have been electroprocessed, they can be collected as fibrous mats or films. Once they are collected, it has been found to be particularly useful for the electroprocessed materials to be cured and then carbonized. After carbonization, the electroprocessed phenolic materials may be activated if desired.

35 [0073] The properties of the electroprocessed phenolic materials may be tuned by post-electroprocessing treatments to provide the materials with properties suited for the intended use. These post-electroprocessing treatments include curing, carbonization, and activation.

Electroprocessed Phenolic Beads

40 [0074] Relatively inexpensive electroprocessed beads can also be provided using commercially available phenolic resins. For example, after a phenolic polymeric system comprising phenolic polymers, and optionally additives is prepared, the phenolic system can be electrostatically processed to create phenolic beads. In exemplary embodiments, phenolic polymeric system can electrostatically sprayed to create beads. The phenolic polymeric system can be electrostatically processed (i.e., sprayed) using equipment for electrostatically processing polymers such as described in Kenawy et al., *Electrospinning of Poly(ethylene-co-vinyl alcohol) Fibers*, *Biomaterials*, Vol. 24 (2003) 907-913, the contents of which is hereby incorporated by reference in its entirety.

45 [0075] When electrostatically processing, a delivery means is not necessary inasmuch as phenolic beads can be produced from a single droplet of solution.

50 [0076] Preferably, the stream of beads from the phenolic polymeric system, produced by electroprocessing, is delivered to a collecting or capturing device (20), or means for capturing the stream of beads, such as, for example, containers of varied geometries and constructions. Examples of a capturing device or means for capturing include, but are not limited to, a wire mesh, a polymeric mesh, a rotating cylinder, a metal grid, metal foil, paper, a syringe needle, a decomposable substrate such as a decomposable polymer fiber, an electrospun substrate, and the like. The skilled artisan will be able to readily select other devices or means that can be used to capture the beads as they travel through the electrical field. The collecting or capturing device is preferably grounded to attract the charged phenolic beads. The capturing device can be selected based on the intended use of the phenolic material.

55 [0077] As the skilled artisan will recognize, the electrified field necessary to create a stream of beads through space can be achieved by charging the delivery means or the capture means. Where the delivery means is charged, the capture means will be grounded (as illustrated in FIG. 1); and where the capture means is charged, the delivery means will be

grounded.

[0078] Preferably in an electrospraying process the collecting or capturing device is a liquid collection bath or substrate. When using a liquid collection bath, beads that can be subsequently solidified as individual particles are formed. When spraying on a substrate, the beads can be sprayed onto the substrate in such a way as to create a film. In the alternative, the beads can be sprayed onto the substrate such that they retain their individual and distinct shape. These beads on the substrate may be subsequently solidified (i.e., residual solvent evaporated) to create individual particles. Typically, when spraying onto a substrate to create a film, the beads retain residual solvent to aid in creating the film.

[0079] When using a liquid collection bath, the liquid should be a liquid that is a non-compatible solvent, including, for example water, mixtures of water and alcohol (such as 90 proof ethanol), oils, such as, for example, vegetable oil, peanut oil, and silicon oil and the like, and mixtures thereof. The liquid collection bath can be made using any device suitable for holding the non-compatible solvent into which the phenolic beads can be electrosprayed. For example, the bath can be formed in a tray, pan, beaker, and the like. Electrospraying produces uniform polymer beads or droplets when sprayed into a nonsolvent liquid. The beads are separated and collected from the liquid collection bath by suitable means, including, for example filtration. The electrosprayed phenolic beads have a diameter of a few nanometers to several hundreds of microns, and preferably from 100 nm to 10 microns, and even more preferably 50 nm to 5 microns.

[0080] Once the beads have been electroprocessed, they can be collected. Once they are collected, it has been found to be particularly useful for the electroprocessed beads to be cured and then carbonized. After carbonization, the electroprocessed phenolic beads can be activated if desired.

[0081] The properties of the electroprocessed phenolic beads can be tuned by post-electroprocessing treatments to provide the beads with properties suited for the intended use. These post-electroprocessing treatments include curing, carbonization, and activation.

Curing Process

[0082] Accordingly, the electroprocessed materials are collected and then can be subject to a curing process. The curing process is preferably accomplished by heating the electroprocessed phenolic materials to a temperature of 20 to 180°C at a ramp rate of 0.1 to 5°C/min. In the curing process the electroprocessed phenolic materials are preferably held at the curing temperature for 2 to 8 hours. The curing should be performed slowly enough that the electroprocessed phenolic material cures and does not melt. Alternatively, the phenolic resin, when in the form of beads, may be cured rapidly by spinning directly in a container containing oil of a temperature ranging between 120 to 180°C. It has been discovered that curing the phenolic material prior to a carbonization process advantageously prevents the material from melting and forming a congealed mass during carbonization.

[0083] The cured phenolic materials may be impregnated with metal salts or metal particles by dipping the cured phenolic materials in a metal salt solution or impregnating the phenolic materials with metals. In addition, the cured phenolic materials may be dipped in base to create a phenoxide material. This phenoxide material may be dipped in a metal salt solution to create phenoxide salts. The cured phenolic materials may further be sulfonated.

Carbonization of Electroprocessed Phenolic Fibers

[0084] Once the electroprocessed phenolic fibers have been cured, they can be carbonized. Accordingly, the cured electroprocessed phenolic fibers can be subject to a carbonization process.

[0085] The carbonization process is preferably accomplished by heating the phenolic electroprocessed fibers to a temperature of 700 to 2000°C at a ramp rate of 1 to 25°C/min under an inert atmosphere and holding at the curing temperature for 2 to 8 hours. The inert atmosphere may be under nitrogen, argon, and the like. Low temperature carbonization may be carried out to about 1100°C in an inert atmosphere. Carbonization from about 1200°C to about 2000°C may be carried out in an inert/vacuum furnace.

[0086] Carbon fibers derived from phenolic precursors are typically referred to as "non-graphitizing" carbons, a description that has been given by Franklin which refers to a "random layer structure" whereby at sufficiently high temperatures, up to 3000 °C, ordered crystallite regions form within the "non-ordered" structure. See, e.g., Franklin, R. *Acta Cryst.* 1951, 4, 253. Kawamura and Jenkins reported similar findings on the surface of the phenolic resin fibers at temperatures of 2500°C. See, e.g., Kawamura, K. and Jenkins, G.M. *J. Mat. Sci.*, 1970, 5, 262. Masters and McEnaney studied cellulosic carbon and found that the dominant feature was an intertwined network of carbon layers ("ribbons"). See, e.g., Masters, K.J. and McEnaney, B., "The development of the structure of microporous carbons" in *Characterization of Porous Solids*, eds. Gregg, S.J., Sing, K.S.W. and Stoeckli, H.F., Society of Chemical Industry: London, 1979. Kawamura and Jenkins described these carbons as containing mainly sp^2 carbon atoms in a hexagonal array and determined that increasing temperature resulted in a decrease in the interplanar spacing from 3.85 Å at 900°C to 3.66 Å at 1600°C. They reported these materials to be non-graphitizing carbons and found micropores to be present even at the highest temperatures studied. Transmission electron microscopy and X-ray diffraction were key characterization tools used for

studying the microstructure of the materials.

[0087] In contrast, according to processes as described herein, the heat treatment (i.e., the carbonization) of the electroprocessed phenolic fibers results in a change in its structure, and may lead to the formation of a highly-ordered, crystalline graphite where the C-C bond length of an aromatic layer is 1.42 Å and the spacing between the planes is 3.35 Å. See, e.g., Oberlin, A. and Bonnami, S., Carbonization and Graphitization in Graphite and Precursors, World of Carbon, Vol.1, Delhaès, P., ed., Gordon and Breach Science Publishers: France, 2001. Accordingly, the carbonization treatment may result in a microstructural rearrangement of the electroprocessed phenolic fibers. As the temperature of the carbonization process is increased, a greater microstructural rearrangement to provide highly graphitic sheets may be obtained.

[0088] By way of example, phenolic polymeric systems consisting of a 1:1 blend of resole and novolak were electrospun into sub-micron sized fibers that were subsequently cured and carbonized at temperatures ranging from 800°C to 2000°C to form nano-sized-carbon fibers. Argon adsorption data revealed that the carbonized electrospun fibers, formed at 800°C to 1400°C, were predominantly microporous compared to the electrospun fibers pyrolyzed at 1600°C to 2000°C, which were non-porous. Thermal treatment resulted in structural rearrangement within the fiber leading to increased order as temperature was increased. This structural rearrangement was evidenced by transmission electron microscopy which showed randomly oriented "ribbons" of graphene sheets at the lower temperatures. These ribbons grew in thickness as temperatures were increased by increasing the number of graphene sheets contributing to the ribbons. X-ray diffraction showed a corresponding decrease in the interlayer spacing with increased temperatures. Along the edges of the fibers HRTEM showed that the graphene sheets began to show partial alignment parallel to the longitudinal dimension of the fibers. Some of the grains also showed the growth of crystalline graphite, which may have nucleated on these aligned sheets. Lower temperatures of thermal treatment, corresponded with microporosity and randomness of the graphene sheets. Elevated temperatures, on the other hand, showed increased alignment of the sheets and a corresponding loss of porosity in the adsorption data. The curved nature of the packets of graphene sheets, the alignment of sheets mantling the fibers with an impervious layer, and the appearance of graphite on the surfaces, and in some cases, a large proportion of the carbon fiber.

[0089] High resolution transmission electron microscopy and X-ray diffraction are key characterization tools for use in studying the microstructure of materials.

[0090] During carbonization, the cured phenolic electroprocessed fibers are thermally degraded to form products that undergo either condensation reactions or volatilization, the competition between these processes determining the carbon yield. The carbon residue is formed by condensation of polynuclear aromatic compounds and expulsion of side chain groups. However, many carbonaceous materials retain a significant concentration of heteroatoms, especially nitrogen and oxygen, and mineral matter such as iron, ceramics, and the like (B. McEnaney, Carbon, vol. 26, No. 3 (1988), pp. 267-274). The carbonization process can provide a carbon yield of at least 40 to 75 percent, (i.e., this carbon yield is the percent yield of the carbonization process, assuming the product is approximately 100 percent carbon). Scanning electron microscopy (SEM) confirmed that the fiber morphology generated during the electrospinning process is retained throughout curing and carbonization.

[0091] Iron oxide nanoparticles can be added to the polymeric system to be electroprocessed so that graphite forms in the electroprocessed fibers at much lower temperatures than what is typically found or expected. For instance, an experiment was conducted where 3w/w% iron oxide (30nn) particles were dispersed into 10w/w% PAN/DMF solution and electrospun at 18.5 kV with a deposition distance of 15cm. The fibers were first carbonized to 800°C in a Thermolyne 2110 tube furnace with 0.2 L/min continuous nitrogen flow. The carbonized fibers were then transferred to a R.D.25 Red Devil high temperature inert/vacuum furnace and carbonized to 1000°C and 1200°C (two different runs). Graphite was observed in both of the carbonized fibers as well as iron carbide. **FIG. 18** depicts a SEM of electrospun material produced when iron oxide nanoparticles were added to PAN fibers and carbonized at 1200°C.

Carbonization of Electroprocessed Phenolic Beads

[0092] Once the electroprocessed phenolic beads have been cured, they can be carbonized. Accordingly, the cured electroprocessed phenolic beads can be subject to a carbonization process.

[0093] The carbonization process is preferably accomplished by heating the phenolic electroprocessed beads to a temperature of 700 to 2000°C at a ramp rate of 1 to 25°C/min under an inert atmosphere and holding at the curing temperature for 2 to 8 hours. The inert atmosphere may be under nitrogen, argon, and the like. Low temperature carbonization may be carried out to about 1100°C. Carbonization from about 1200°C to about 2000°C may be carried out in an inert/vacuum furnace.

[0094] Carbon beads derived from phenolic precursors are typically referred to as "non-graphitizing" carbons, a description that has been given by Franklin which refers to a "random layer structure" whereby at sufficiently high temperatures, up to 3000°C, ordered crystallite regions form within the "non-ordered" structure. See, e.g., Franklin, R. *Acta Cryst.* 1951, 4, 253. Kawamura and Jenkins reported similar findings on the surface of the phenolic resin fibers at

temperatures of 2500°C. See, e.g., Kawamura, K. and Jenkins, G.M. J. Mat. Sci., 1970, 5, 262. Masters and McEnaney studied cellulosic carbon and found that the dominant feature was an intertwined network of carbon layers ("ribbons"). See, e.g., Masters, K.J. and McEnaney, B., "The development of the structure of microporous carbons" in Characterization of Porous Solids, eds. Gregg, S.J., Sing, K.S.W. and Stoeckli, H.F., Society of Chemical Industry: London, 1979. Kawamura and Jenkins described these carbons as containing mainly sp^2 carbon atoms in a hexagonal array and determined that increasing temperature resulted in a decrease in the interplanar spacing from 3.85 Å at 900°C to 3.66 Å at 1600°C. They reported these materials to be non-graphitizing carbons and found micropores to be present even at the highest temperatures studied. Transmission electron microscopy and X-ray diffraction were key characterization tools used for studying the microstructure of the materials.

[0095] In contrast, according to processes as described herein, the heat treatment (i.e., the carbonization) of the electroprocessed phenolic beads results in a change in its structure, and may lead to the formation of a highly-ordered, crystalline graphite where the C-C bond length of an aromatic layer is 1.42 Å and the spacing between the planes is 3.35 Å. See, e.g., Oberlin, A. and Bonnami, S., Carbonization and Graphitization in Graphite and Precursors, World of Carbon, Vol.1, Delhaès, P., ed., Gordon and Breach Science Publishers: France, 2001. Accordingly, the carbonization treatment may result in a microstructural rearrangement of the electroprocessed phenolic beads. As the temperature of the carbonization process is increased, a greater microstructural rearrangement to provide highly graphitic sheets may be obtained.

[0096] High resolution transmission electron microscopy and X-ray diffraction are key characterization tools for use in studying the microstructure of materials.

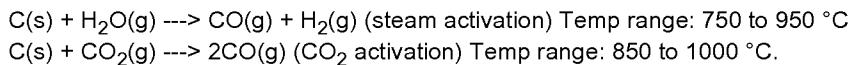
[0097] During carbonization, the cured phenolic electroprocessed beads are thermally degraded to form products that undergo either condensation reactions or volatilization, the competition between these processes determining the carbon yield. The carbon residue is formed by condensation of polynuclear aromatic compounds and expulsion of side chain groups. However, many carbonaceous materials retain a significant concentration of heteroatoms, especially nitrogen and oxygen, and mineral matter such as iron, ceramics, and the like (B. McEnaney, Carbon, vol. 26, No. 3 (1988), pp. 267-274). The carbonization process can provide a carbon yield of at least 40 to 75 percent, (i.e., this carbon yield is the percent yield of the carbonization process, assuming the product is approximately 100 percent carbon). Scanning electron microscopy (SEM) confirmed that the fiber morphology generated during the electrospraying process is retained throughout curing and carbonization.

[0098] Iron oxide nanoparticles can be added to the polymeric system to be electroprocessed so that graphite forms in the electroprocessed beads at much lower temperatures than what is typically found or expected.

Activation Process

[0099] The adsorptive capacity of the carbonized phenolic materials may be lower than desired for some applications, or the pore size of the carbonized phenolic materials may not be optimized for a particular application. Accordingly, additional porosity in the carbonized phenolic electroprocessed materials can be developed by an activation process (i.e. by reaction of the carbon with oxidizing gases (e.g. H_2O or CO_2). The activation process etches the carbon structure to generate new pores (from non-porous portions), more large pores (larger than those present in the material before activation), or enlarge existing pores. Activation is an optional process and may be used to create additional porosity as the carbonized phenolic materials contain significant pore volume without activation.

[0100] Typical activation reactions are performed using either steam or CO_2 . The reaction equations for typical activation reactions are as follows:



[0101] The activation process is preferably accomplished by heating the carbonized phenolic materials to a temperature of 700 to 1000°C under a mixture of oxidizing gas and inert atmosphere. In the activation process the carbonized phenolic materials are preferably held at the activation temperature for 20 minutes to 5 hours, depending on the extent of activation desired. The mixture of oxidizing gas and inert atmosphere may be under a carbon dioxide and nitrogen or argon mixture, a steam and nitrogen or argon mixture, and the like. The activation times may be varied to create various pore size distributions and increased surface area. Since the carbonized phenolic materials comprise micropores, activation may be used to create additional micropores. Activation may also be used to create larger pores or mesopores (pores ranging from 20 to 500 angstroms). Mesopores may be desired for certain applications to make materials comprising the activated phenolic materials more selective or suitable for particular applications.

Properties of the Electroprocessed Materials

[0102] The electroprocessed phenolic materials, including fibers and films, and materials made from the electroprocessed materials, have been found to have particularly advantageous properties. The electroprocessed phenolic materials, comprising fibers and films, can be characterized using all or some of the following techniques: scanning electron microscopy (SEM), transmission electron microscopy (TEM), high resolution transmission electron microscopy (HRTEM), atomic force microscopy (AFM), Fourier transform infrared spectroscopy (FTIR), x-ray diffraction (XRD), Raman spectroscopy, and the like.

[0103] The properties of the electroprocessed phenolic materials may be tuned by post-electroprocessing treatments to provide the materials with properties suited for the intended use. These post-electroprocessing treatments include curing, carbonization, and activation.

[0104] Adsorption isotherms can provide a great deal of information about the porous structure of solids, as it is the equilibrium relationship between the quantity of the adsorbed material and the pressure or concentration in the bulk fluid phase at constant temperature. When a solid (adsorbent) is exposed to a gas or vapor (adsorbate), the solid begins to adsorb the gas onto its surface and into its pores. Adsorption occurs because of forces acting between the solid and the gas molecules. The theory developed by Brunauer, Emmett and Teller (BET), despite its restrictions, was the first attempt to create a universal theory of physical adsorption. See, e.g., Brunauer, S.; Emmett, P.H. and Teller, E., *J. Amer. Chem. Soc.* 1938, 60, 309.

[0105] The classification of Brunauer, Emmett, Deming, Deming and Teller (BDDT or BET classification) led to the IUPAC classification for the five types of isotherms. See, e.g., Brunauer, S., Deming, L.S., Deming, W.S. and Teller, E., *J. Amer. Chem. Soc.* 1940, 62, 1723; Brunauer, S., Emmett, P.H. and Teller, E., *J. Amer. Chem. Soc.* 1938, 60, 309; Sing, K.S.W.; Everett, D.H.; Haul, R.A.W.; and Moscow, L.; Pierotti, R.A.; Rouquerol, T.; Siemieniewska, T. *Pure Appl. Chem.* 1985, 57, 603. Type I is observed by the physical adsorption of gases onto microporous solids. The most commonly used characterization of the internal structure of microporous carbons is the pore size distribution. However, gas adsorption on solid surfaces and in pore spaces is a complex phenomenon involving mass and energy interactions and phase changes where the pores are rarely of uniform size and geometry. Furthermore, the individual effects due to structural and energetic heterogeneity cannot be separated. See, e.g. Jaroniec, M. and Madey, R., *In Physical Adsorption on Heterogeneous Solids, Studies in Physical and Theoretical Chemistry*, 59, Elsevier Science: New York, 1988. Various models have been developed over the years to mathematically describe the phenomena of physical adsorption of gas or liquid in these cracks and pores. They are based on experimental evidence, thermodynamic and statistical mechanical principles, such as density functional theory. See, e.g., Valladares, D.L., Reinoso, F.R., and Zgrablich, G., *Carbon* 1998, 36(10), 1491; Webb, P.A., Orr, C., with contributions from Camp, R.W., Olivier, J.P. and Yunes, Y.S., *Analytical Methods in Fine Particle Technology*, Micromeritics Instrument Corporation, Norcross, GA, 1997; Tarazona, P., *Phys. Rev.* 1985, 31, 2672; Tarazona, P.; Marconi, U.M.B.; and Evans, R. *Mol. Phys.* 1987, 60, 543; Tarazona, P. *Mol. Phys.* 1984, 52, 847; Seaton, N.A.; Walton, J.P.R.B.; and Quirke, N. *Carbon* 1989, 27, 853; and Peterson, B.K., Walton, J.P.R.B. and Gubbins, K.E., *J. Chem. Soc* 1896, 82, 1789.

[0106] The various methods rely on different assumptions in order to obtain relationships allowing the calculation of the main characteristics of the heterogeneity. Density functional theory (DFT) is a molecular-based, statistical thermodynamic theory that relates the adsorption isotherm to the microscopic properties of the system, including, the fluid-fluid and fluid-solid interaction energy parameters, the pore size, the pore geometry, and the temperature which has been utilized.

[0107] DFT can be used to calculate pore size distributions from argon adsorption isotherms at 87.29 K. The results suggest that carbonization temperature affects pore size distribution of the carbon fibers. For carbonization temperatures up to 1400°C, the electrospun carbonized phenolic fibers exhibit type I isotherms in the IUPAC classification and have narrow pore size distributions with average pore widths of less than 6 Å. For carbonization temperatures equal to or greater than 1600 °C the carbon fibers are non-porous. As the carbonization temperature is increased, the total pore volume decreases and the average pore widths also decrease. X-ray diffraction and high resolution transmission electron microscopy (HRTEM) is utilized to gain further insight into the microstructure. As the temperature is increased, the incremental pore size distribution (calculated by DFT) shifts from a maximum, narrow distribution at 5 Å at 800°C, to non-detectable micropores at temperatures greater than 1400°C. This pore size distribution shift coincides with increased ordering within the carbon structure as evidenced by a decrease in the d-interplanar spacing at $2\theta \approx 26^\circ$ from X-ray diffraction data and an increase in the stacking height of the graphene sheets observed by high resolution transmission electron microscopy (HRTEM).

[0108] In particular, phenolic fibers, including nanofibers and microfibers, have been found to be particularly advantageous because of the small fiber diameter that can be achieved. Preferably, the electrospun phenolic fibers have diameters of 10 microns to 50 nanometers, and more preferably the electrospun phenolic fibers have diameters of 5 microns to 50 nanometers. The variation in the fiber diameters can be due to the variation in flow rate, voltage, and deposition distance during the electrospinning process. Because of this diameter, the phenolic fibers can be used to

form nano materials to be used in many applications. The diameter of the phenolic fibers may be measured using a SEM.

[0109] Preferably, the electroprocessed phenolic materials, including nanofibers, microfibers and films, are cured and then carbonized as described above. The carbonized phenolic materials have been found to have particularly advantageous properties. As described above, preferably the carbonization process has a yield of 40 to 70 percent. In addition, the carbonized phenolic materials may comprise highly ordered graphitic sheets. Carbonizing the phenolic materials at higher temperatures, for example from 1200 to 3000°C, may increase the graphitic proportion of the carbonized materials. These highly ordered graphitic sheets provide desirable properties to the carbonized phenolic materials including, for example, increased conductivity. There is a relationship between the conductivity, C-H content, and graphitic content. In addition, as the proportion of the ordered graphitic structure is increased, an even smaller pore size distribution may be achieved. Accordingly, the carbonization temperature may be optimized to provide the desired properties. By way of example, if a highly ordered graphitic structure is desired, the carbonization temperature can be increased and if a less ordered structure is desired, the carbonization temperature can be decreased. Accordingly, the resulting material can be tuned for the application of interest.

[0110] Carbonized phenolic nanofibers and microfibers have diameters of 10 micron to 50 nanometers, preferably 3 microns to 100 nanometers. In addition, the carbonized phenolic materials have desirable Brunauer, Emmett and Teller (BET) surface area, pore volume, and pore size distribution. Surface area and pore size distribution of the electroprocessed phenolic materials can be measured using adsorption of argon, and thermal property measurements of the materials can be done with thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC). To measure adsorption characteristics, inverse gas chromatography and gas chromatography coupled with mass spectrometry can be utilized.

[0111] In comparison to electroprocessed phenolic materials, cured electroprocessed phenolic materials, and non-electrospun carbonized phenolic materials, the carbonized electroprocessed phenolic materials have a relatively large BET surface area with a narrow pore size distribution of micropores.

[0112] The high external surface area to volume ratio and the uniform porosity properties provide the carbonized electroprocessed phenolic materials with desirable properties. As is readily understood in the art, external surface area is inversely proportional to the particle size. Since the carbonized phenolic materials have nano or micro-sized dimensions, the carbonized phenolic materials have a large external surface areas.

[0113] The carbonized phenolic materials produced by electroprocessing have a relatively large BET surface area. By way of example, the carbonized phenolic materials have a BET surface area of at least 400 to 800 m²/g. The BET surface area may be measured using a Micromeritics ASAP 2010 instrument.

[0114] Although the electroprocessed and cured phenolic materials exhibit minimal internal surface area, the carbonized electroprocessed phenolic materials have a relatively high internal surface area. The carbonized phenolic materials can be provided with a micropore volume of 0.2 to 0.4 cm³/g. The carbonized phenolic materials can be provided with a surprising uniform pore volume distribution. The carbonized phenolic materials are comprised of greater than 70% micropores, preferably greater than 90%, even more preferably greater than 98%, and even more preferably approximately 100%. Micropores are smaller than 20 angstroms. The pore volume and pore volume distribution may be measured by using a Micromeritics ASAP 2010 instrument and are calculated using a molecular-based statistical thermodynamic theory that relates the adsorption isotherm to the microscopic properties of the system, including the pore size. This calculation is well known in the art and is as described in Webb, Paul A and Clyde Orr, "Section 3.3.7 Density functional theory," Analytical Methods in Fine Particle Technology (1997) 81-87. The carbonized phenolic materials have a total volume of at least approximately 0.2 to 0.5 cm³/g.

[0115] Accordingly, the carbonized phenolic materials possess a significant degree of porosity, or pore volume, even without the optional processing step of activation as required by many materials to create acceptable porosity. However, activation may be performed on the carbonized phenolic materials to create even more pores, and to create pores that are larger than those present in the material before activation. Activated phenolic materials may comprise micropores or a mixture of micropores and mesopores. Mesopores are those ranging from 20 to 500 angstroms. Accordingly, activated phenolic materials may have a broader pore size distribution than the carbonized phenolic materials. The activated phenolic materials may comprise 100% micropores or approximately 99 to 100% micropores. Mesopores may be desired for certain applications to make materials comprising the activated phenolic materials more selective or suitable for particular applications.

[0116] Activated phenolic nanofibers and microfibers have diameters of 5 microns to 100 nanometers, preferably 1 micron to 50 nanometers. In addition, the activated phenolic materials have desirable Brunauer, Emmett and Teller (BET) surface area, pore volume, and pore size distribution. Surface area and pore size distribution of the electroprocessed phenolic materials can be measured using adsorption of argon, and thermal property measurements of the materials can be done with thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC). To measure adsorption characteristics, inverse gas chromatography and gas chromatography coupled with mass spectrometry can be utilized.

[0117] The high external surface area to volume ratio and the uniform porosity properties provide the activated elec-

trprocessed phenolic materials with desirable properties, and thus these activated electroprocessed phenolic materials may be useful as adsorbents. As is readily understood in the art, external surface area is inversely proportional to the particle size. Since the activated phenolic materials have nano or micro-sized dimensions, the activated phenolic materials have a large external surface areas.

5 [0118] The activated phenolic materials produced by electroprocessing have a relatively large BET surface area. By way of example, the activated phenolic nanofibers have a BET surface area of 1000 m²/g and higher. The BET surface area may be measured using a Micromeritics ASAP 2010 instrument.

10 [0119] In exemplary embodiments, phenolic materials activated at a temperature between about 800°C and about 1250°C will have a BET surface area of at least about 800 m²/g and will have at least about 60% and preferably at least about 65% micropores having a pore width of less than about 7Å. Additionally, in other exemplary embodiments, phenolic materials activated at a temperature of at least about 1400°C will have a BET surface area of at least about 800 m²/g, and at least about 40%, preferably at least about 45% micropores having a pore width of less than about 7Å.

15 [0120] Although the electroprocessed and cured phenolic materials exhibit minimal internal surface area, the activated electroprocessed phenolic materials have a relatively high internal surface area. The activated phenolic materials can be provided with a micropore volume of 0.2 to 0.6 cm³/g. The activated phenolic materials can be provided with a surprising uniform pore volume distribution. The activated phenolic materials, are comprised of greater than 70% micropores, preferably greater than 80%, more preferably greater than 90%, even more preferably greater than 98%, and even more preferably approximately 100%. Micropores are smaller than 20 angstroms. The pore volume and pore volume distribution may be measured by using a Micromeritics ASAP 2010 instrument and are calculated using a 20 molecular-based statistical thermodynamic theory that relates the adsorption isotherm to the microscopic properties of the system, including the pore size. This calculation is well known in the art and is as described in Webb, Paul A and Clyde Orr, "3.37 Density functional theory," Analytical Methods in Fine Particle Technology (1997) 81-87. The activated phenolic materials have a total volume of at least approximately 0.2 to 0.6 cm³/g.

25 **Properties of the Electroprocessed Beads**

[0121] Electroporessed phenolic beads made from the electroprocessed materials, have been found to have particularly advantageous properties. The electroporessed phenolic beads can be characterized using all or some of the 30 following techniques: scanning electron microscopy (SEM), transmission electron microscopy (TEM), high resolution transmission electron microscopy (HRTEM), atomic force microscopy (AFM), Fourier transform infrared spectroscopy (FTIR), x-ray diffraction (XRD), Raman spectroscopy, and the like.

[0122] The properties of the electroporessed phenolic beads may be tuned by post-electroprocessing treatments to provide the materials with properties suited for the intended use. These post-electroprocessing treatments include curing, carbonization, and activation.

35 [0123] Adsorption isotherms can provide a great deal of information about the porous structure of solids, as it is the equilibrium relationship between the quantity of the adsorbed material and the pressure or concentration in the bulk fluid phase at constant temperature. When a solid (adsorbent) is exposed to a gas or vapor (adsorbate), the solid begins to adsorb the gas onto its surface and into its pores. Adsorption occurs because of forces acting between the solid and the gas molecules. The theory developed by Brunauer, Emmett and Teller (BET), despite its restrictions, was the first 40 attempt to create a universal theory of physical adsorption. See, e.g., Brunauer, S.; Emmett, P.H. and Teller, E., J. Amer. Chem. Soc. 1938, 60, 309.

[0124] The classification of Brunauer, Emmett, Deming, Deming and Teller (BDDT or BET classification) led to the IUPAC classification for the five types of isotherms. See, e.g., Brunauer, S., Deming, L.S., Deming, W.S. and Teller, E., J. Amer. Chem. Soc. 1940, 62, 1723; Brunauer, S., Emmett, P.H. and Teller, E., J. Amer. Chem. Soc. 1938, 60, 309; Sing, K.S.W.; Everett, D.H.; Haul, R.A.W.; and Moscov, L.; Pierotti, R.A.; Rouquerol, T.; Siemieniewska, T. Pure Appl. Chem. 1985, 57, 603. Type I is observed by the physical adsorption of gases onto microporous solids. The most commonly 45 used characterization of the internal structure of microporous carbons is the pore size distribution. However, gas adsorption on solid surfaces and in pore spaces is a complex phenomenon involving mass and energy interactions and phase changes where the pores are rarely of uniform size and geometry. Furthermore, the individual effects due to structural and energetic heterogeneity cannot be separated. See, e.g. Jaroniec, M. and Madey, R., In Physical Adsorption on Heterogeneous Solids, Studies in Physical and Theoretical Chemistry, 59, Elsevier Science: New York, 1988. Various 50 models have been developed over the years to mathematically describe the phenomena of physical adsorption of gas or liquid in these cracks and pores. They are based on experimental evidence, thermodynamic and statistical mechanical principles, such as density functional theory. See, e.g., Valladares, D.L., Reinoso, F.R., and Zgrablich, G., Carbon 1998, 36(10), 1491; Webb, P.A., Orr, C., with contributions from Camp, R.W., Olivier, J.P. and Yunes, Y.S., Analytical Methods in Fine Particle Technology, Micromeritics Instrument Corporation, Norcross, GA, 1997; Tarazona, P., Phys. Rev. 1985, 31, 2672; Tarazona, P.; Marconi, U.M.B.; and Evans, R. Mol. Phys. 1987, 60, 543; Tarazona, P. Mol. Phys. 1984, 52, 847; Seaton, N.A.; Walton, J.P.R.B.; and Quirke, N. Carbon 1989, 27, 853; and Peterson, B.K., Walton, J.P.R.B. and 55

Gubbins, K.E., J. Chem. Soc 1896, 82, 1789.

[0125] The various methods rely on different assumptions in order to obtain relationships allowing the calculation of the main characteristics of the heterogeneity. Density functional theory (DFT) is a molecular-based, statistical thermodynamic theory that relates the adsorption isotherm to the microscopic properties of the system, including the fluid-fluid and fluid-solid interaction energy parameters, the pore size, the pore geometry, and the temperature which has been utilized.

[0126] DFT can be used to calculate pore size distributions from argon adsorption isotherms at 87.29 K. The results suggest that carbonization temperature affects pore size distribution of the carbon beads.

[0127] Preferably, the electroprocessed phenolic beads are cured and then carbonized as described above. The carbonized phenolic beads have been found to have particularly advantageous properties. As described above, preferably the carbonization process has a yield of 40 to 70 percent. In addition, the carbonized phenolic beads may comprise highly ordered graphitic sheets. Carbonizing the phenolic materials at higher temperatures, for example from 1200 to 3000°C, may increase the graphitic proportion of the carbonized materials. These highly ordered graphitic sheets provide desirable properties to the carbonized phenolic materials including, for example, increased conductivity. There is a relationship between the conductivity, C-H content, and graphitic content. In addition, as the proportion of the ordered graphitic structure is increased, an even smaller pore size distribution may be achieved. Accordingly, the carbonization temperature may be optimized to provide the desired properties. By way of example, if a highly ordered graphitic structure is desired, the carbonization temperature can be increased and if a less ordered structure is desired, the carbonization temperature can be decreased. Accordingly, the resulting material can be tuned for the application of interest.

[0128] In comparison to electroprocessed phenolic materials, cured electroprocessed phenolic materials, and non-electrosprayed carbonized phenolic materials, the carbonized electroprocessed phenolic beads have a relatively large BET surface area with a narrow pore size distribution of micropores.

[0129] The high external surface area to volume ratio and the uniform porosity properties provide the carbonized electroprocessed phenolic beads materials with desirable properties. As is readily understood in the art, external surface area is inversely proportional to the particle size. Since the carbonized phenolic materials have nano or micro-sized dimensions, the carbonized phenolic materials have a large external surface areas.

[0130] The carbonized phenolic beads produced by electroprocessing have a relatively large BET surface area. By way of example, the carbonized phenolic materials have a BET surface area of at least 400 to 800 m²/g. The BET surface area may be measured using a Micromeritics ASAP 2010 instrument.

[0131] Although the electroprocessed and cured phenolic beads exhibit minimal internal surface area, the carbonized electroprocessed phenolic beads have a relatively high internal surface area. The carbonized phenolic beads can be provided with a micropore volume of 0.2 to 0.4 cm³/g. The carbonized phenolic beads can be provided with a surprising uniform pore volume distribution. The carbonized phenolic beads are comprised of greater than 70% micropores, preferably greater than 90%, even more preferably greater than 98%, and even more preferably approximately 100%. Micropores are smaller than 20 angstroms. The pore volume and pore volume distribution may be measured by using a Micromeritics ASAP 2010 instrument and are calculated using a molecular-based statistical thermodynamic theory that relates the adsorption isotherm to the microscopic properties of the system, including the pore size. This calculation is well known in the art and is as described in Webb, Paul A and Clyde Orr, "Section 3.3.7 Density functional theory," Analytical Methods in Fine Particle Technology (1997) 81-87. The carbonized phenolic materials have a total volume of at least approximately 0.2 to 0.5 cm³/g.

[0132] Accordingly, the carbonized phenolic beads possess a significant degree of porosity, or pore volume, even without the optional processing step of activation as required by many materials to create acceptable porosity. However, activation may be performed on the carbonized phenolic beads to create even more pores, and to create pores that are larger than those present in the material before activation. Activated phenolic beads may comprise micropores or a mixture of micropores and mesopores. Mesopores are those ranging from 20 to 500 angstroms. Accordingly, activated phenolic materials may have a broader pore size distribution than the carbonized phenolic materials. The activated phenolic materials may comprise 100% micropores or approximately 99 to 100% micropores. Mesopores may be desired for certain applications to make materials comprising the activated phenolic materials more selective or suitable for particular applications.

[0133] The high external surface area to volume ratio and the uniform porosity properties provide the activated electroprocessed phenolic beads with desirable properties, and thus these activated electroprocessed phenolic beads may be useful as adsorbents. As is readily understood in the art, external surface area is inversely proportional to the particle size. Since the activated phenolic beads have nano or micro-sized dimensions, the activated phenolic beads have a large external surface areas.

[0134] The activated phenolic beads produced by electroprocessing have a relatively large BET surface area. By way of example, the activated phenolic beads have a BET surface area of 800 m²/g and higher. The BET surface area may be measured using a Micromeritics ASAP 2010 instrument.

[0135] In exemplary embodiments, electrosprayed phenolic beads activated at a temperature between about 800°C

and about 1250°C will have a BET surface area of at least about 800 m²/g and higher, and will have at least about 60% and preferably at least about 65% micropores having a pore width of less than about 7 Å. Additionally, in other exemplary embodiments, electrosprayed phenolic beads have a BET surface area of at least about 1400 m²/g, and at least about 40%, preferably at least about 45% micropores having a pore width of less than about 7 Å.

5 [0136] Although the electroprocessed and cured phenolic beads exhibit minimal internal surface area, the activated electroprocessed phenolic beads have a relatively high internal surface area. The activated phenolic beads can be provided with a micropore volume of 0.2 to 0.6 cm³/g. The activated phenolic beads can be provided with a surprising uniform pore volume distribution. The activated phenolic materials are comprised of greater than 70% micropores, preferably greater than 80%, more preferably greater than 90%, even more preferably greater than 98%, and even more 10 preferably approximately 100%. Micropores are smaller than 20 angstroms. The pore volume and pore volume distribution may be measured by using a Micromeritics ASAP 2010 instrument and are calculated using a molecular-based statistical 15 thermodynamic theory that relates the adsorption isotherm to the microscopic properties of the system, including the pore size. This calculation is well known in the art and is as described in Webb, Paul A and Clyde Orr, "Section 3.3.7 Density functional theory," *Analytical Methods in Fine Particle Technology* (1997) 81-87. The activated phenolic materials have a total volume of at least approximately 0.2 to 0.6 cm³/g.

Uses of the Electroprocessed Materials

20 [0137] The carbonized electroprocessed phenolic materials, and the activated materials, possess particularly advantageous properties that allow the materials to be used for a variety of useful purposes. The high external surface to volume ratio of the carbonized phenolic materials provide the materials with properties which make them appropriate for catalyst supports in catalysis or fuel cell applications, high surface area composites, including carbon fiber/polymer composites and carbon fiber/carbon composites, and high surface area filtration applications. The uniform porosity of the carbonized phenolic materials provides the materials with properties which make them appropriate for selective 25 filtration applications and fuel cell applications. Both the carbonized and the activated phenolic materials may exhibit improved bonding, strength, and conductivity.

30 [0138] The potential applications of these electroprocessed phenolic materials, including fibers, fibrous mats, beads and films are numerous and diverse. Materials produced by electrospinning phenolic polymers have shown promising results in a variety of applications, including, for example, tissue scaffolding, protective clothing, drug release, membranes, 35 nano-machines, sensors, nano-composite reinforcement, laboratory and chemical engineering equipment, electrodes for electrochemical processes, medical and dental inserts, adsorbents for filtration, catalyst supports, flame resistant safety products, composites, various biomedical applications, reinforcement materials, electrically conducting fillers, artificial muscles, field emitters, gas and electrochemical energy storage matrices such as batteries and fuel cells, and the like. Furthermore, electroprocessed phenolic materials have properties that make them suitable for applications in the areas of nanoelectronics, nanomechanics, and composites. Another advantage of producing nanofibers having a diameter of less than about 1 micrometer is the ability to analyze the fiber for many of its physical and chemical characteristics.

40 [0139] An additional advantage of the phenolic materials is that the properties of the materials readily can be tuned according to the intended end use. One skilled in the art can readily tune the properties in a variety of ways. By way of example, the composition of the phenolic polymeric system may be adjusted to achieve desired properties. In addition, the conditions under which the phenolic polymeric solution is electroprocessed can be adjusted to provide certain properties. The conditions of post-electroprocessing treatments, including curing, carbonization, and optionally activation, can be adjusted to provide desired properties.

45 [0140] Preferably, "tunable" porosity can be created within the fibers with activation, such that selective adsorbents can be created. (Unfunctionalized carbon typically exhibits broad-based adsorptions.) These selective adsorbents may be used in any applications in which adsorbents are needed for filtration.

50 [0141] By using electrospinning to provide orientation to the fibers, preferably graphitic-like materials can be produced in "non-graphitizing" precursors, which would extend the material options and reduce energy costs associated with temperatures in excess of about 2500°C. High proportions of graphite, in typically non-graphitizing carbons, could provide enhanced electrical properties, thus extending their functionality in fuel cells, batteries and as supercapacitors. Enhanced property characteristics found in nano-sized carbon fibers from electrospun precursors could be an alternative to nanotubes for selected applications.

Use in Smoking Articles

55 [0142] In one embodiment, the electroprocessed materials may be used in a smoking article. A preferred smoking article is a cigarette. In exemplary embodiments, the electroprocessed material can be an activated electroprocessed material. The electroprocessed activated materials can be located in a filter. In exemplary embodiment the smoking

article comprises from about 10 mg to about 200 mg of the electroprocessed activated fibers and/or beads, more preferably about 25 mg to about 100 mg.

[0143] In a particular embodiment, the activated electroprocessed fibers and/or beads may be used in a cigarette filter. Preferably, the cigarette filter comprises from about 10 mg to about 200 mg of the electroprocessed activated fibers and/or beads, more preferably about 25 mg to about 100 mg. In yet another embodiment, a cut filler composition comprising the electroprocessed activated fibers and/or beads described above is provided.

[0144] The activated electroprocessed fibers and/or beads can be used as a filtration agent. In particular, the activated electroprocessed fibers and/or beads can be used as filters for a smoking article to remove light gases from mainstream smoke. The light gases are selected from the group consisting of methane, carbon monoxide, nitrogen oxide, formaldehyde, acid aldehyde and the like, and combinations thereof. The term "mainstream" smoke includes the mixture of gases passing down the tobacco rod and issuing through the filter end, i.e. the amount of smoke issuing or draw from the mouth end of a smoking article during smoking of the smoking article. The mainstream smoke contains smoke that is drawn in through the lit region of the smoking article, possibly diluted by air that is drawn in through the paper wrapper.

[0145] The activated electroprocessed fibers and/or beads are made by the above-described process in which a phenolic polymer system is electroprocessed to provide phenolic fibers and/or beads, the phenolic fibers and/or beads are cured, the cured phenolic fibers and/or beads are carbonized, and the carbonized fibers and/or beads are activated to provide activated electroprocessed fibers.

[0146] The activated electroprocessed fibers and/or beads are good adsorbents for light gases and thus are good adsorbents for use in smoking articles. Typical adsorbents include any material that has the ability to condense or hold molecules of other substances on its surface. While not wishing to be bound by theory, adsorption is mainly caused by London Dispersion Forces, a type of Van der Waals force, which exists between molecules. The forces act within extremely short ranges, and are additive. In gas phase adsorption, molecules are condensed from the bulk phase within the pores of the activated carbon. The driving force for adsorption is the ratio of the partial pressure and the vapor pressure of the compound. In liquid or solid phase adsorption the molecules go from the bulk phase to being adsorbed in the pores in a semi-liquid or solid state.

[0147] While typical adsorbents including charcoal and graphite have some ability to adsorb molecules, the activated electroprocessed fibers and/or beads as described herein are preferred adsorbents for smoking articles because the activated electroprocessed fibers and/or beads have stronger physical adsorption forces, and higher volumes of adsorbing porosity for light gases. It has been surprisingly discovered that these activated electroprocessed fibers and/or beads have strong physical adsorption forces, and high volumes of adsorbing porosity for light gases over activated carbon that has not been formed by an electroprocessing technique.

[0148] The activated electroprocessed materials may be included in the smoking articles in the form of granules, beads, monoliths, fragments, powder or fibers. In exemplary embodiments activated electroprocessed fibers and/or beads may be used in the smoking articles in the place of typical adsorbents. Alternatively, the activated electroprocessed fibers and/or beads may be used in the smoking articles in combination with an additional absorbent, such as other carbon, silica gel, activated carbon particles, alumina, polyester resins, zeolite and zeolite-like materials, and mixtures thereof. In exemplary embodiments, the activated carbon particles can have an average particle size of about 6 mesh to 300 mesh. In exemplary embodiments, a flavorant can also be provided downstream of the electrospun carbonized fibers and/or beads. This combination may compliment removal of the desired constituents from the mainstream smoke.

[0149] In a preferred embodiment, the pores of the activated carbon comprise at least 80% micropores and more preferably greater than 90% micropores. The ratio of micropores to total pores may be varied by adjusting the conditions of the post-electroprocessing treatments, including curing, carbonization, and activation. The ratio of micropores to total pores may be varied depending upon the selected light gases from mainstream tobacco smoke that are to be targeted and removed. Thus, as described herein the pore sizes and pore distribution can be adjusted accordingly as needed for the intended application.

[0150] The activated electroprocessed fibers and/or beads have a sufficient surface area to preferentially adsorb light gases from cigarette smoke.

[0151] The activated electroprocessed fibers and/or beads may be used in a variety of applications, including smoking articles, cut filler compositions and cigarette filters. Thus, in one embodiment, a smoking article comprising the activated electroprocessed fibers and/or beads is provided. The smoking article may be any article containing smokeable material, such as a cigarette, a pipe, a cigar and a non-traditional cigarette. Non-traditional cigarettes include, for example, cigarettes for electrical smoking systems as described in commonly-assigned U.S. Pat. Nos. 6,026,820; 5,988,176; 5,915,387; 5,692,526; 5,692,525; 5,666,976; and 5,499,636. The activated electroprocessed fibers and/or beads may be located in a filter. The activated electroprocessed fibers and/or beads may be used in the smoking articles in the place of typical adsorbents. Alternatively, the activated electroprocessed fibers and/or beads may be used in the smoking articles in combination with an additional absorbent, such as other carbon, silica gel, and the like. This combination may compliment removal of the desired constituents from the mainstream smoke.

[0152] An effective amount of activated electroprocessed fibers and/or beads to remove or lower the amount of one

or more selected light gases in mainstream smoke is used. Typical smoking articles will include from about 10 mg to about 200 mg of the activated electroprocessed fibers and/or beads, more preferably about 25 mg to about 100 mg, although the amount needed can also be determined easily by routine experimentation and/or adjusted accordingly.

[0153] Cigarette filters comprising the activated electroprocessed fibers and/or beads are provided. Any conventional or modified filter may incorporate the activated electroprocessed fibers and/or beads. In one embodiment, the activated electroprocessed fibers and/or beads are incorporated into or onto a support such as paper (e.g., tipping paper) that is located along a filter portion of a cigarette. As will be recognized by persons skilled in the art, such paper can be used, for example, as a wrapper or a liner in the filter portion of the cigarette. The activated electroprocessed fibers and/or beads can also be loaded onto a support such as lightly or tightly folded paper inserted into a hollow portion of the cigarette filter. The support is preferably in the form of a sheet material such as crepe paper, filter paper, or tipping paper. However, other suitable support materials such as organic or inorganic cigarette compatible materials can also be used.

[0154] FIG. 2A illustrates a cigarette 30 having a tobacco rod 31, a filter portion 32, and a mouthpiece filter plug 33. As shown, a surface-modified adsorbent can be loaded onto folded paper 34 inserted into a hollow cavity such as the interior of a free-flow sleeve 35 forming part of the filter portion 32.

[0155] FIG. 2B shows a cigarette 30 having a tobacco rod 31 and a filter portion 32, wherein the folded paper 34 is located in the hollow cavity of a first free-flow sleeve 36 located between the mouthpiece filter 33 and a second free-flow sleeve 37. The paper 34 can be used in forms other than as a folded sheet. For instance, the paper 34 can be deployed as one or more individual strips, a wound roll, etc. In whichever form, a desired amount of surface-modified adsorbent can be provided in the cigarette filter portion by adjusting the amount of surface-modified adsorbent coated per unit area of the paper and/or the total area of coated paper employed in the filter (e.g., higher amounts of surface-modified adsorbent can be provided simply by using larger pieces of coated paper). In the cigarettes shown in FIGS. 2A and 2B, the tobacco rod 31 and the filter portion 32 are joined together with tipping paper 38. In both cigarettes, the filter portion 32 may be held together by filter overwrap 39.

[0156] The activated electroprocessed fibers and/or beads can be incorporated into the filter paper in a number of ways. For example, the activated electroprocessed fibers and/or beads can be mixed with water to form a slurry. The slurry can then be coated onto pre-formed filter paper and allowed to dry. The filter paper can then be incorporated into the filter portion of a cigarette in the manner shown in FIGS. 2A and 2B. Alternatively, the dried paper can be wrapped into a plug shape and inserted into a filter portion of the cigarette. For example, the paper can be wrapped into a plug shape and inserted as a plug into the interior of a free-flow filter element such as a polypropylene or cellulose acetate sleeve. In another arrangement, the paper can comprise an inner liner of such a free-flow filter element.

[0157] Alternatively, the activated electroprocessed fibers and/or beads can be added to the filter paper during the paper-making process. For example, the activated electroprocessed fibers and/or beads can be mixed with bulk cellulose to form a cellulose pulp mixture. The mixture can be then formed into filter paper according to methods known in the art.

[0158] In another embodiment, the activated electroprocessed fibers and/or beads are incorporated into the fibrous material of the cigarette filter portion itself. Such filter materials include, but are not limited to, fibrous filter materials including paper, cellulose acetate fibers, and polypropylene fibers. This embodiment is illustrated in FIG. 2C, which shows a cigarette 30 comprised of a tobacco rod 31 and a filter portion 32 in the form of a plug-space-plug filter having a mouthpiece filter 33, a plug 40, and a space 41. The plug 40 can comprise a tube or solid piece of material such as polypropylene or cellulose acetate fibers. The tobacco rod 31 and the filter portion 32 are joined together with tipping paper 38. The filter portion 32 may include a filter overwrap 39. The filter overwrap 39 containing traditional fibrous filter material and surface-modified adsorbent can be incorporated in or on the filter overwrap 39 such as by being coated thereon. Alternatively, the activated electroprocessed fibers can be incorporated in the mouthpiece filter 33, in the plug 40, and/or in the space 41. Moreover, the activated electroprocessed fibers and/or beads can be incorporated in any element of the filter portion of a cigarette. For example, the filter portion may consist only of the mouthpiece filter 33 and the activated electroprocessed fibers and/or beads can be incorporated in the mouthpiece filter 33 and/or in the tipping paper 38.

[0159] Various techniques can be used to apply the activated electroprocessed fibers and/or beads to filter fibers or other substrate supports. For example, the activated electroprocessed fibers and/or beads can be added to the filter fibers before they are formed into a filter cartridge, e.g., a tip for a cigarette. The activated electroprocessed fibers and/or beads can be added to the filter fibers, for example, in the form of a dry powder or a slurry by methods known in the art. If the activated electroprocessed fibers and/or beads are applied in the form of a slurry (e.g., using a solvent that allows the organic impregnate to remain on the adsorbate), the fibers are allowed to dry before they are formed into a filter cartridge.

[0160] In another preferred embodiment, the activated electroprocessed fibers and/or beads are employed in a hollow portion of a cigarette filter. For example, some cigarette filters have a plug/space/plug configuration in which the plugs comprise a fibrous filter material and the space is simply a void between the two filter plugs. That void can be filled with the activated electroprocessed fibers and/or beads as described herein. An example of this embodiment is shown in FIG. 2C. The activated electroprocessed fibers and/or beads can be in granular form or can be loaded onto a suitable

support.

[0161] In another embodiment, the activated electroprocessed fibers and/or beads are employed in a filter portion of a cigarette for use with a smoking device as described in U.S. Pat. No. 5,692,525, the entire content of which is hereby incorporated by reference. FIG. 2D illustrates one type of construction of a cigarette 100 which can be used with an electrical smoking device. As shown, the cigarette 100 includes a tobacco rod 60 and a filter portion 62 joined by tipping paper 64. The filter portion 62 preferably contains a tubular free-flow filter element 102 and a mouthpiece filter plug 104. The free-flow filter element 102 and mouthpiece filter plug 104 may be joined together as a combined plug 110 with plug wrap 112. The tobacco rod 60 can have various forms incorporating one or more of the following items: an overwrap 71, another tubular free-flow filter element 74, a cylindrical tobacco plug 80 preferably wrapped in a plug wrap 84, a tobacco web 66 comprising a base web 68 and tobacco flavor material 70, and a void space 91. The free-flow filter element 74 provides structural definition and support at the tipped end 72 of the tobacco rod 60. At the free end 78 of the tobacco rod 60, the tobacco web 66 together with overwrap 71 are wrapped about cylindrical tobacco plug 80. Various modifications can be made to a filter arrangement for such a cigarette incorporating activated electroprocessed fibers and/or beads.

[0162] In such a cigarette, the activated electroprocessed fibers and/or beads can be incorporated in various ways such as by being loaded onto paper or other substrate material which is fitted into the passageway of the tubular free-flow filter element 102 therein. It may also be deployed as a liner or a plug in the interior of the tubular free-flow filter element 102. Alternatively, the activated electroprocessed fibers and/or beads can be incorporated into the fibrous wall portions of the tubular free-flow filter element 102 itself. For instance, the tubular free-flow filter element or sleeve 102 can be made of suitable materials such as polypropylene or cellulose acetate fibers and the activated electroprocessed fibers and/or beads can be mixed with such fibers prior to or as part of the sleeve forming process.

[0163] In another embodiment, the activated electroprocessed fibers and/or beads can be incorporated into the mouthpiece filter plug 104 instead of in the element 102. However, as in the previously described embodiments, activated electroprocessed fibers and/or beads may be incorporated into more than one component of a filter portion such as by being incorporated into the mouthpiece filter plug 104 and into the tubular free-flow filter element 102.

[0164] The filter portion 62 of FIG. 2D can also be modified to create a void space into which the surface-modified adsorbent can be inserted.

[0165] As explained above, activated electroprocessed fibers and/or beads can be incorporated in various support materials. When the activated electroprocessed fibers are used in filter paper, the fibers may have an average fiber diameter of 5 μm to 100 nm, preferably 1 μm to 500 nm. In exemplary embodiments, activated electroprocessed fibers can have an average length of about 1/10 mm to about 12 mm, more preferably about 1/2 mm to about 6 mm, when used, for example, in a plug section of a smoking article.

[0166] The amount of activated electroprocessed fibers and/or beads employed in the cigarette filter by way of incorporation on a suitable support such as filter paper and/or filter fibers depends on the amount of light gases in the tobacco smoke and the amount of light gases desired to be removed. As an example, the filter paper and the filter fibers may contain from 10% to 50% by weight of the activated electroprocessed fibers and/or beads.

[0167] An embodiment relates to a method of making a cigarette filter, said method comprising: (i) providing activated electroprocessed fibers as described above, and (ii) incorporating the activated electroprocessed fibers and/or beads into a cigarette filter. Any conventional or modified methods for making a filter may be used to incorporate the activated electroprocessed fibers and/or beads.

[0168] Another embodiment relates to a method of making a cigarette, said method comprising: (i) providing a cut filler to a cigarette making machine to form a tobacco rod; (ii) placing a paper wrapper around the tobacco rod; (iii) providing a cigarette filter comprising activated electroprocessed fibers and/or beads as described above; and (iv) attaching the cigarette filter to the tobacco rod to form the cigarette. In yet another embodiment, a method of making a cigarette is provided. The method comprises: (i) adding activated electroprocessed fibers and/or beads as described above to a cut filler; (ii) providing the cut filler comprising the activated electroprocessed fibers and/or beads to a cigarette making machine to form a tobacco rod; and (iii) placing a paper wrapper around the tobacco rod to form the cigarette.

[0169] In another embodiment, a smoking article wrapper is provided, which comprises electrospun carbonized fibers. In exemplary embodiments, the electrospun carbonized fibers are activated carbonized fibers.

[0170] In another embodiment a smoking article wrapper is provided, which comprises electrosprayed carbonized beads. In exemplary embodiments, the electrosprayed carbonized beads are activated carbonized beads.

[0171] Examples of suitable types of tobacco materials which may be used include flue-cured, Burley, Maryland or Oriental tobaccos, the rare or specialty tobaccos, and blends thereof. The tobacco material can be provided in the form of tobacco lamina; processed tobacco materials such as volume expanded or puffed tobacco, processed tobacco stems such as cut-rolled or cut-puffed stems, reconstituted tobacco materials; or blends thereof. The invention may also be practiced with tobacco substitutes.

[0172] In cigarette manufacture, the tobacco is normally employed in the form of cut filler, i.e. in the form of shreds or strands cut into widths ranging from about {fraction (1/10)} inch to about {fraction (1/20)} inch or even {fraction (1/40)}

inch. The lengths of the strands range from between about 0.25 inches to about 3.0 inches. The cigarettes may further comprise one or more flavorants or other additives (e.g. burn additives, humectants, combustion modifying agents, coloring agents, binders, etc.) known in the art.

[0173] Techniques for cigarette manufacture are known in the art, and may be used to incorporate the surface-modified adsorbent. The resulting cigarettes can be manufactured to any desired specification using standard or modified cigarette making techniques and equipment. The cigarettes of the invention may range from about 50 mm to about 120 mm in length. Generally, a regular cigarette is about 70 mm long, a "King Size" is about 85 mm long, a "Super King Size" is about 100 mm long, and a "Long" is usually about 120 mm in length. The circumference is from about 15 mm to about 30 mm in circumference, and preferably around 25 mm. The packing density is typically between the range of about 100 mg/cm³ to about 300 mg/cm³, and preferably 150 mg/cm³ to about 275 mg/cm³.

[0174] In yet another embodiment is provided a method of smoking a smoking article comprising activated electro-processed fibers and/or beads as described above. The method comprises lighting the smoking article to form smoke and inhaling the smoke, wherein during the smoking of the cigarette, the activated electroprocessed fibers and/or beads preferentially removes light gases selected from the group consisting of methane, carbon monoxide, nitrogen oxide, formaldehyde, acid aldehyde, and the like, and combinations thereof from mainstream smoke.

[0175] "Smoking" of a cigarette means the heating or combustion of the cigarette to form smoke, which can be inhaled. Generally, smoking of a cigarette involves lighting one end of the cigarette and inhaling the cigarette smoke through the mouth end of the cigarette, while the tobacco contained therein undergoes a combustion reaction. However, the cigarette may also be smoked by other means. For example, the cigarette may be smoked by heating the cigarette and/or heating using electrical heater means, as described in commonly-assigned U.S. Pat. Nos. 6,053,176; 5,934,289; 5,934,289, 5,591,368 or 5,322,075, for example.

EXAMPLES

[0176] The following examples are illustrative examples that are intended to be non-limiting.

[0177] *Materials.* Commercially available phenolic resins, resole and novolak with 6.5wt% hexamethylene-tetramine were generously provided by Durez Corporation. Poly(acrylonitrile), (PAN) and N,N-dimethyl formamide, (DMF) 99%, [D15855-0] were purchased from Aldrich Chemical Co., Inc. Ethyl alcohol (200 proof, Acros Organics) and DMF were utilized as the solvents for the phenolic resins and PAN, respectively. Commercially available phenolic resins, resole (average molecular weight of 9,700 g/mol) and novolak (average molecular weight of 13,200 g/mol) with 6.5wt% hexamethylene-tetramine were generously provided by Durez Corporation. Ethyl alcohol (200 proof, Acros Organics) was utilized as the solvent.

[0178] *Electrospinning Set-up.* Due to the low production volume of final product and the need for sufficient quantity of material for subsequent processing and characterization, multiple runs of the electrospinning processes, for both the PAN and phenolic resins, were executed using the same lots of raw materials.

Example 1

Synthesis of Phenolic Nanofibers from a Resole/Novolak Polymeric Solution

[0179] A 40%wt solution of Resole (Average MW=9300) in ethanol was prepared by mixing the dry powder with the ethanol in a 125ml Nalgene bottle. The solution was agitated on a platform shaker for at least 24 hours in order to ensure complete dissolution. A second solution of 50%wt Novolak (Average MW=13000) with 6.5%wt Hexamethylenetetramine in ethanol was prepared by mixing the dry powder with the ethanol in a 125ml Nalgene bottle. The solution was agitated on a platform shaker for at least 24 hours in order to ensure complete dissolution. Once each solution had completely dissolved, a 1:1 mixture of the 40% wt Resole and 50%wt Novolak was prepared.

[0180] The composite solution was then transferred to a 10ml Becton & Dickinson (B&D) polypropylene syringe fitted with a 2"(inch) 18- gauge stainless steel blunt tip pipetting needle. The solution was delivered at a flow rate of 8-13 ml/hr using a KD Scientific model 100 syringe pump, but could be lower if desired (5-6 ml/hr) or higher (up to 20 ml/hr) with this specific arrangement. However, if the flow rate was too high, then dripping at the needle tip occurred. The voltage of 15 to 17 kilovolts (kV) was applied to the needle in order to achieve electrospinning conditions and was set at 15 kV for the majority of the experiment. The voltage was applied to the needle via an alligator clip that was connected to a Spellman High Voltage Electronics Corporation model SL10 high voltage power supply (output 0-60 kilovolts/166 micro-amperes). A minimal current of less than one microampere was drawn once voltage was applied. The collection target for the electrospun fibers was located 15-20 cm from the syringe needle tip (source) and consisted of a rotating cylindrical aluminum drum that was of the following dimensions: 3 inches in length and diameter, respectively.

[0181] During the electrospinning process, almost complete evaporation of the ethanol occurred to yield a dry nonwoven electrospun fibrous mat. In order to ensure the ethanol was essentially eliminated, the electrospun fibers were allowed

to remain on the rotating drum for about 5 to 10 minutes before removing the mat from the drum. After the electrospinning process was complete, the non-woven electrospun fibrous mat was then removed from the drum, weighed, and transferred to a quartz boat and the quartz boat with the electrospun fibers were then placed in a Thermolyne 21100 tube furnace. The total mass of the electrospun fibrous mat before curing was 11.1680 g.

[0182] The tube furnace was used to cure the electrospun mat by heating to 160°C at a ramp rate of 0.1°C/min, with a nitrogen flow rate of 0.20 L/min. The curing process was continued for 2-8 hours once the furnace temperature reached 160°C to ensure crosslinking. It is expected that the cured fibers may be left in the furnace for 48 hours, under the stated conditions of 160°C and a nitrogen flow rate of 0.2 L/min with minimal impact on the fibers. No subjective differences were observed when allowing the cured fibers to be exposed to the curing conditions for an extended period of time.

10 While a ramp rate of 0.1 °C/min was effective in the curing process, however, the ramp rate up to 1-2°C/min. The curing temperature is above the melting temperature and thus, the only way to retain the fiber morphology is to expose the material to a very gradual increase in temperature to ensure crosslinking begins before the glass transition temperature of the polymer is attained.

[0183] After the curing, the sample mass was recorded to be 11.1575 g. The cured fibrous material was placed on a quartz boat and into the Thermolyne 21100 tube furnace and the temperature was increased to 800°C at a ramp rate of 10°C/min and a nitrogen flow rate of 0.5 L/min. Once a temperature 800°C was achieved, the furnace remained isothermal for 2 hours. After the sample was carbonized, it was cooled to room temperature and the mass of the carbonized fibers was recorded to be 6.2998 g. In this particular example, the carbon yield was 56.46%.

[0184] The electrospun, cured and carbonized fibers produced from the 1:1 ratio of 50wt% novolak in ethanol to 40wt% resole in ethanol were characterized utilizing a JMS-840 (JEOL) scanning electron microscope (SEM) to determine if the fiber structure remained intact throughout post-electrospinning processing. The SEM images for a 1:1 blend of 40 wt% resole and 50 wt% novolak (with 6.5% hexamethylenetetramine) dissolved in ethanol are shown in FIGs. 3A, 3B and 3C, for the electrospun, cured, and carbonized fibers, respectively. The carbonized fibers showed diameters as small as 50 nanometers, with the largest being about 3.5 microns. The variation in the fiber diameter was due to the variation in the flow rate, voltage and deposition distance during the electrospinning processing. (See FIGs. 3A, 3B and 3C).

[0185] In order to determine the surface area and total pore volume of the fibrous material, a Micromeritics ASAP 2010 instrument was utilized. To those familiar with the relationship between particle size and external surface area, it is understood that there is an inverse relationship. Electrospun fibers afford a large external surface area due to the nano-sized and micro-sized fiber diameter. The internal surface area of the fibers was also measured.

[0186] The electrospun fibers, cured fibers and carbonized fibers were individually prepared for the surface area and total pore volume (total pore volume and pore volume distribution are calculated from density functional theory). Each sample was placed in a glass tube and evacuated of moisture and atmospheric vapors. The cured fibers and carbonized fibers were exposed to temperatures of 150°C during the evacuation step, but the electrospun fibers were not exposed to this temperature during evacuation in order to avoid melting and altering the fiber morphology. Each sample was evacuated for 2 hours. The glass tube and the tube with the sample were weighed to determine the sample mass.

[0187] The glass tube with each sample was placed in the holder for the surface area measurement after the mass of the material for each run was determined. Argon was used for the measurements. The results of the measurements showed minimal internal surface area for the electrospun and cured fibers, 2-3 m²/g, whereby the carbonized fibers showed a relatively high surface area of about 600 m²/g for duplicate samples. The carbon fibers exhibit a Type I isotherm as illustrated in FIG. 4. The results of the BET Surface Area, micropore volume, and total pore volume for the electrospun phenolic fibers, the cured phenolic fibers, and the carbonized phenolic fibers are summarized in Table I in FIG. 5.

[0188] Of the total pore volume of the carbonized electrospun fibers, the pore size distribution consisted of micropores, which were predominately 5 Å. The pore size distribution of the carbonized electrospun fibers of Example 1 is illustrated in FIG. 6.

Example 2

Comparative Example - Synthesis of Non-electrospun Phenolic Materials

[0189] To determine if the same internal surface area could be generated from the aforementioned novolak/resole blend, without the precursor electrospinning step, a portion of the same polymeric solution that was used for electrospinning was placed into the quartz tube and cured at the stated conditions (without electrospinning to create a fibrous mat). After evaporation of the solvent and curing was accomplished, the sample was weighed and a portion of the sample was saved for the surface area measurement.

[0190] The cured, non-electrospun material was placed in the tube furnace and subjected to the carbonization conditions previously described. The sample was cooled and weighed. The cured non-electrospun and carbonized non-electrospun samples of 1:1 ratio of 50wt% novolak with 6.5% hexamethylenetetramine and 40wt% resole were prepared

for the surface area measurements as stated above. The results of the cured and carbonized non-electrospun samples showed similar results as the electrospun and cured fibers as described above (i.e. negligible internal surface area). Therefore, carbonizing the non-electrospun samples did not create high internal surface area as it did in the carbonized electrospun fibers. Accordingly, the electrospinning process is effective in producing the carbon fibers with a high internal surface area.

[0191] The results of the BET Surface Area, micropore volume, and total pore volume for the non-electrospun sample, the cured non-electrospun sample, and the carbonized non-electrospun sample are summarized in Table II in FIG. 5.

Examples 3

Measurement of Graphitic Content of Phenolic Fibers

[0192] A portion of the cured fibers of Example 1 were exposed to carbonization temperatures of 1000°C, with a ramp rate of 10°C /min and a nitrogen flow rate of 0.5 to 0.6 L/min. The carbon yield was 54.65%. The carbonized fibers were characterized using Transmission Electron Microscopy to determine if the fibers exhibited ordering with the disordered carbon structure or indications of graphite. A Philips Tecnai instrument (TEM) was utilized to study the sample at high magnification. The carbonized sample (1000°C) showed an increase in order in a proportion of the fiber as evidenced by systematic alignment at the microscopic level. Although the proportion of the structure that was ordered relative to the non-ordered was not quantified, the ordered proportion may be able to be progressively increased by increasing the temperature during pyrolysis (up to 2000°C). This increase in temperature may shift the proportions of ordered to non-ordered, and thus alter the material properties. Samples of the cured fibers of Example 1 are exposed to temperatures of 1200°C, 1500°C, 1600°C, 1800°C and 2000°C using a high temperature furnace, Web 25 Red Devil, in an inert atmosphere of argon.

[0193] The carbonized fibers carbonized at 800°C was also characterized using Transmission Electron Microscopy to determine if the fibers exhibited ordering with the disordered carbon structure or indications of graphite. A Philips Tecnai instrument (TEM) was utilized to study the sample at high magnification. The carbonized sample (800°C) showed no significant degree of observable crystallinity.

[0194] FIG. 7 depicts HRTEM images of carbonized electrospun phenolic resin fibers at (a) 1000°C, (b and c) 1600°C showing partial alignment; (d) graphite at 1600°C; and (e and f) 1800°C. FIG. 8A depicts XRD for carbonized electrospun phenolic resin fibers at (a) 1000°C, (b) 1200°C, (c) 1400°C, (d) 1600°C, (e) 1800°C, and (f) 2000°C. FIG. 8B depicts XRD for the sample holder.

Example 4

Doping with Copper Nanoparticles

[0195] In a variation of Example 1, copper nanoparticles of 20-30 nanometers were dispersed into the solution of 40wt% resole in ethanol. The resole solution was combined with a novolak solution, prepared as described in Example 1. The combined solution is electrospun as described in Example 1. The resulting phenolic fibers are then cured and carbonized, also as described.

[0196] The copper nanoparticles increase the conductivity of the solution, thus improving the spinnability. The copper nanoparticles also provide the final carbonized phenolic fibers with improved electrical properties, thus making them suitable for a broader range of applications.

Example 5

Electrospraying

[0197] Phenolic solutions of 20 to 35 wt% resole (Average MW=9700) in ethanol, phenolic solutions of 20 to 35 wt% novolak (Average MW=13,000) in ethanol, and phenolic solutions of 15 to 35 wt% novolak (Average MW=29,295) in ethanol were prepared as described above for Example 1. These phenolic solutions were individually subjected to electrospraying instead of electrospinning. The electrospraying process uses a non-solvent liquid in a beaker as the target.

[0198] When a non-solvent liquid was used as the target, the electrospraying process produced uniform polymer spheres (beads). The beads are separated and collected from the beaker of non-solvent liquid. The beads are processed (i.e., cured and carbonized) as described above for Example 1.

[0199] The beads, obtained from a phenolic solutions of 15 wt% novolak (Average MW=29,295) in ethanol, were analyzed by SEM and FIG. 9 illustrates a SEM of the beads prior to any subsequent processing. The bead diameters were measured as 100 nanometers to 5 microns.

Example 6**Phenolic Polymer Blends**

5 **[0200]** Phenolic polymer blends with poly(acrylic acid) and cellulose acetate were prepared and then electrospun. Blends of 12 to 1 and 9 to 1 phenolic polymer to poly(acrylic acid) (Average MW = 1.5 million) were prepared using a 40 wt% novolak (Average MW=13000) prepared as described in Example 1. In addition, blends of 12 to 1 and 9 to 1 phenolic polymer to poly(acrylic acid) were prepared using a 50/50 mixture of resole and novolak prepared as described in Example 1.

10 **[0201]** The resulting solutions were electrospun as described above for Example 1. The resulting phenolic nanofibers are cured and carbonized, also as described above for Example 1. The mechanical properties of these carbonized phenolic nanofibers are tested for tensile strength and elasticity.

15 **[0202]** Polymer blends with cellulose acetate were also prepared. A 50/50 blend of cellulose acetate solution and novolak solution was prepared. The cellulose acetate solution was a 15 wt% solution of cellulose acetate (Average MW=30,000) in a 2:1 mixture of acetone and dimethylamide. The novolak solution was a 50 wt% solution of novolak (Average MW=13,000) in ethanol, prepared as described in Example 1. In addition, a 3/1 blend of phenolic polymeric solution and cellulose acetate solution was prepared. The phenolic polymeric solution was a 50/50 mixture of resole and novolak in ethanol, prepared as described in Example 1. The cellulose acetate solution was a 12 wt% solution of cellulose acetate (Average MW=50,000) in acetone.

20 **[0203]** The resulting solutions were electrospun as described above for Example 1. The resulting phenolic nanofibers are cured and carbonized, also as described above for Example 1. The mechanical properties of these carbonized phenolic nanofibers are tested for tensile strength and elasticity.

Example 7**Preparation of Phenolic Electrospun Fibers**

25 **[0204]** *Electrospinning of phenolic resins.* A homogeneous blend of 1:1 resole and novolak was prepared using a 50 w/w% solution of resole in ethyl alcohol (EtOH) and a 50 w/w% solution of novolak, with 6.5wt% of hexamethylenetetramine, in EtOH. The resulting polymeric solution was drawn into a 10-ml polypropylene syringe fitted with a two inch, 18-gauge stainless steel blunt tip needle. The syringe and attached stainless steel needle filled with the polymer solution were placed on a KD Scientific (model 100) syringe pump and set to deliver 10 ml/hr of solution to a grounded aluminum target when charged via a high voltage supply (Spellman High Voltage Electronics Corporation, model SL10). The applied voltage was 16-17 kilovolts (kV) and the distance from the tip of the needle to the grounded collection device was 15 cm. The grounded collection device consisted of a 3-inch diameter rotating aluminum cylinder layered with removable aluminum foil. A schematic of the electrospinning experimental set-up used for this study is depicted in FIG. 1. Additionally, 50 w/w% novolak in EtOH and 50 w/w% resole in EtOH were electrospun using the aforementioned conditions.

30 **[0205]** *Curing of Phenolic resins.* The phenolic resin electrospun fibrous mats and "non-electrospun" polymeric solution were cured to form infusible, crosslinked materials before carbonizing. For the electrospun materials, the curing process was crucial in order to retain the fiber morphology generated during the electrospinning process. A portion of the resole/novolak polymer solution was cured as-is for comparison to the electrospun fibers. The pre-weighted materials for curing were placed in a quartz boat and in the center of a quartz tube in a Thermolyne 21100 tube furnace. The temperature ramped to 160°C and held isothermally for at least two hours with 0.2 L/min continuous nitrogen purge.

35 **[0206]** *Carbonization of phenolic resins.* The cured electrospun fibers and cured bulk phenolic resin materials were carbonized at temperatures of 800°C and 1000°C using the Thermolyne 21100 tube furnace. For each carbonization run, the pre-weighed material was placed in a quartz boat, which was slid into the same center location in the tube furnace. For the carbonization cycle, the temperature was ramped to the set-point at 10°C /min and held isothermally for two hours with 0.5 L/min continuous nitrogen flow.

40 **[0207]** For carbonization at temperatures greater than 1000°C, a R.D. Webb 25 Red Devil high temperature vacuum/inert gas furnace was utilized. The electrospun samples were first carbonized in the Thermolyne 21100 tube furnace using the aforementioned cycle. After the process was completed at 800°C or 1000°C, the sample was weighed and placed into a graphite cup and into the Red Devil underneath several layers of graphite and ceramic insulation. The pressure was reduced to less than 50 torr using a vacuum pump and purged with argon until positive pressure was obtained. The purge cycle was repeated three times prior to starting each higher temperature carbonization cycle to ensure removal of oxygen and moisture from the system. For the carbonization, the temperature was ramped to the predetermined set-point at a rate of 10°C/min and held isothermally for two hours with 0.5 L/min continuous argon flow. The primary difference between the lower temperature carbonization and the higher temperature carbonization was that

argon was utilized instead of nitrogen for the inert environment.

Example 8

5 Comparison of Phenolic Electrospun Fibers and PAN Electrospun Fibers

[0208] *Phenolic Electrospun Fibers.* Phenolic electrospun fibers were prepared as described above for Example 7.

[0209] *Electrospinning of PAN.* 8wt% and 10wt% solutions of PAN in DMF were prepared. A flask filled with PAN in DMF, at the predetermined concentration, was placed in a mineral oil bath and on a heating plate, whereby the temperature of the solution was maintained below 70°C to form a homogeneous solution. The aforementioned procedure described for the electrospinning of phenolic resins was utilized for PAN. Various processing conditions were investigated to determine the most suitable for fabricating fibers for subsequent carbonization. Process variables investigated were applied voltage, volumetric flow rate and deposition distance. The electrospinning conditions selected for PAN were 18.5kV, 10ml/hr and 15cm, for applied voltage, volumetric flow rate and deposition distance, respectively. The target was also layered with aluminum foil for easy removal of the fibrous mat. The fibrous mat was removed from the foil and stored, similar to the procedure described for electrospun phenolic resins.

[0210] *Stabilization of PAN.* The electrospun PAN fibers were stabilized in a Fisher Scientific Isotemp programmable furnace (Model 495A). The fibrous mat was placed on aluminum foil and into the furnace with a constant air flow and the following program for the heating cycle: ramp heating rates 1, 2 and 3 of 1°C/min, temperature 1, 2 and 3 of 200°C, 250°C and 300°C, respectively; and dwell times 1, 2 and 3 of 120 min. The furnace was ramped down to room temperature at faster rate and shorter dwell times for each three steps. Upon completion of the stabilization cycle, the fibrous material was weighed. The solution consisting of 10wt% PAN in DMF was utilized for the carbonization study.

[0211] *Pyrolysis/Carbonization.* The PAN materials were carbonized at temperatures of 800°C to 1000°C using the Thermolyne 21100 tube furnace. For each carbonization run, the preweighed material was placed into a quartz boat, which was slid into the same center location in the tube furnace. For the carbonization temperatures of 800°C to 1000°C, a heating ramp rate of 10°C /min with a continuous nitrogen volumetric flow rate of 0.5 L/min was utilized. After the temperature set point was obtained, the material was held isothermally for two hours. The cooling process was similar to that described for the curing process for the phenolic resins. The carbonization yield for the phenolic resins at 800°C was approximately 50% compared to 40% for the PAN. No significant weight loss occurs at the temperatures above 800°C.

[0212] For carbonization at temperatures greater than 1000°C, a R.D. Webb 25 Red Devil high temperature vacuum/inert gas furnace was utilized. The electrospun samples were first carbonized in the Thermolyne 21100 tube furnace using the aforementioned cycle. After the process was completed at 800°C or 1000°C, the sample was weighed and placed into a graphite cup and into the Red Devil underneath several layers of graphite and ceramic insulation. The pressure was reduced to less than 50 torr using a vacuum pump and purged with Argon until positive pressure was obtained. The purge cycle was repeated three times prior to starting each higher temperature carbonization cycle to ensure all oxygen and moisture were removed from the system. A similar cycle to that of the 800°C and 1000°C was utilized for the higher temperature carbonization, using a heating ramp rate of 10°C/min with a continuous argon volumetric flow rate of 0.5 L/min and an isothermal dwell time of 2 hours. When the isothermal cycle was completed, the temperature was ramped down to that of room temperature conditions. The primary difference between the lower temperature carbonization and the higher temperature carbonization was that argon was utilized instead of nitrogen for the inert environment. At the completion of each cycle, the sample was weighed.

[0213] *Scanning Electron Microscopy.* The electrospun, intermediate cross-linked or stabilized, and carbonized fibrous materials of phenolic resins in EtOH and PAN in DMF were characterized using scanning electron microscopy, JEOL JMS-840, to obtain a qualitative measure of fiber diameter distribution, morphology, and impact of multiple processing steps. Of specific interest was to ensure that fiber morphology was retained after the fibrous materials were subjected to the elevated temperatures of the curing and carbonization. Prior to the analysis, the samples were placed on aluminum sample plugs and sputter coated with a thin layer of palladium/gold alloy to ensure the samples were electrically conductive.

[0214] *Adsorption.* Adsorption isotherms and surface area of the materials were determined using a Micromeritics ASAP 2010 instrument (Norcross, GA.) and the incremental and pore size distribution calculated by density function theory (DFT) using software provided with the instrument and are summarized in Table 1. Prior to the measurements, each cured and carbonized sample was placed into a 1.27cm outside diameter sample tube closed with a SealFrit, and degassed for 2 hours at a temperature of 150°C and a vacuum pressure less than 20torr on the degas port of the analyzer. After the degassing process was completed, the sample tube assembly was transferred to the analysis port. Argon was selected as the probe molecule because it is spherical, monatomic and non-polar and is preferred over nitrogen for studies of microporosity. For relative pressure less than 0.01, a fixed volumetric dosing of 10cm³/g of liquid argon was applied, and for relative pressures greater than or equal to relative pressures of 0.01, the volumetric argon dosing amount was calculated based on satisfying predetermined relative pressures up to and including relative pressures

of approximately 0.9.

[0215] Scanning electrospun microscopy was utilized to ascertain information regarding fiber diameter and morphology. The electrospun fibers retained their morphology throughout curing/stabilization and carbonization processing. Although a significant weight loss occurred during the processing, it was difficult to determine a percent reduction in fiber diameter from the SEM micrographs due to the overall variability in fiber diameter. FIGS. 10A and 10B show SEM micrographs of the carbonized phenolic resin and PAN electrospun fibers produced at 1000°C, respectively; whereby the specific electrospinning were described in the experimental section. The diameters of the carbonized phenolic fibers (FIG. 10A) ranged from about 250 nm to 2-3 μ m, compared to the diameters of the carbonized PAN fibers (FIG. 10B) that ranged from about 150 nm to 500 nm. PAN carbon fibers with diameters as small as 75-100 nm were produced from lower concentration PAN/DMF solutions, specifically 8wt%. Electrospun, carbonized PAN fibers have been reported as low as 50nm and smaller. Commercial available PAN carbon fibers were also carbonized for comparison to the electrospun fibers. The commercially PAN fiber diameters were approximately 10 μ m, and thus, significantly larger than both the carbonized electrospun phenolic resin and PAN fibers.

[0216] Although mechanical properties were not measured in this study, the carbonized PAN fibers were strong enough to withstand multiple handling steps without breaking, whereas the phenolic fibers required gentle handling during the processing stages to minimize breakage. The mechanical properties of electrospun, carbonized phenolics, may be improved by using additives, co-polymers, blends of other polymer systems and the like.

[0217] The results of the BET specific surface area, micropore volume and total pore volumes calculated using DFT are shown below in Table 1. The BET results indicated that as carbonization temperature was increased, the specific surface area decreased. The BET specific surface area of the carbonized phenolic fibers at 1600°C was significantly lower than that of the lower carbonization temperatures and was more representative of the PAN carbonized fibers. The carbonized electrospun PAN showed a significantly lower BET specific surface area than all of the carbonized electrospun phenolic resins, with the exception of the phenolic resin carbonized at 1600°C. Due to the limited quantity of the sample (approximately 50mg), differentiation between samples with BET specific surface areas of around 100 m²/g or less should be considered essentially the same, as the experimental error was higher with the non-porous samples.

[0218] According to IUPAC nomenclature, micropores have widths less than 20 angstroms (or 2 nm), mesopores have widths between 20 angstroms and 500 angstroms (2 nm to 50 nm), and macropores have widths greater than 500 angstroms (50nm). The electrospun phenolic resins carbonized at temperatures of 800°C to 1400°C showed a total pore volume that was essentially all micropore volume. The electrospun phenolic resin carbonized at 1600°C showed no measurable micropore volume. The carbonized electropun PAN showed a significantly lower total pore volume, and thus, micropore volume, when compared to that of the carbonized electrospun phenolic resins.

Table 1. BET surface area and pore volume (DFT) for carbonized electrospun phenolic resins and PAN.

35 Sample	Description	BET Surface Area (m ² /g)	DFT Pore Volume	
			Micropore Volume (cm ³ /g)	Total Volume (cm ³ /g)
36 PHC800	Phenolic Blend @800°C	571	0.226	0.232
40 PHC1000	Phenolic Blend @1000°C	506	0.200	0.208
45 PHC1200	Phenolic Blend @1200°C	525	0.211	0.211
50 PHC1400	Phenolic Blend @1100°C	413	0.165	0.165
55 PHC1600	Phenolic Blend @1600°C	21	0.001	0.031
PANC800	PAN @800°C	141	0.025	0.056
PANC1000	PAN @1000°C	108	0.011	0.033
PANC1200	PAN @1200°C	32	0.002	0.014
PANC1400	PAN @1400°C	28	0.003	0.009
PANC1600	PAN @1600°C	60	0.000	0.000

[0219] When electrospun, stabilized/cured and carbonized, PAN/DMF and phenolic resin/EtOH polymeric solutions create fibrous materials with distinctly different adsorption properties. The carbonized phenolic fibers showed relatively high microporosity, with no additional activation or etching of the fibers, when compared to the carbonized PAN fibers which showed negligible porosity. The pore volume can be reduced by exposing the material to increasingly higher temperatures, thus allowing the capability of potentially tuning the pore size distribution for a specific application of interest. The phenolic fibers can be produced using an environmentally benign solvent, which makes them more attractive from a safety perspective compared to the PAN, which utilizes DMF as the solvent.

Characterization

[0220] *Scanning Electron Microscopy (SEM).* The electrospun, intermediate cross-linked, and carbonized fibrous materials of phenolic resin were characterized using scanning electron microscopy (JEOL JSM-840) to obtain a qualitative measure of fiber diameter distribution, morphology, and impact of multiple processing steps. Of specific interest was to ensure that fiber morphology was retained after the fibrous materials were subjected to the elevated temperatures of curing and carbonization. Prior to the analysis, the samples were placed on aluminum sample plugs and sputter coated with a thin layer of palladium/gold alloy to ensure that the samples were electrically conductive.

[0221] **FIG. 10A** illustrates a phenolic resin carbonized electrospun fibers (1:1 ratio of 50wt% novolak and 50wt% resole, both in EtOH). The results from the SEM micrographs indicate the fiber morphology generated during electrospinning has been retained throughout the curing and carbonization processes. Although fiber diameters of approximately 200 nm were observed for the electrospun fibers, the majority of the diameters ranged from approximately 500 nm to several microns. After the electrospun fibers were cured and pyrolyzed, the resulting fibers appeared to range from about 100 nm to approximately 1 μm or less. **FIGs. 12A** and **12B** show SEM micrographs of electrospun fibers generated from a 50 w/w% solution of resole in EtOH and a 50 w/w% solution of novolak in EtOH. However, the fibers either did not adequately crosslink or have the mechanically integrity desired for subsequent carbonization. Alternative electrospinning conditions and curing conditions are currently being investigated with the individual resole and novolak fibers in addition to different ratios of resole to novolak.

[0222] *Adsorption.* Argon adsorption isotherms were measured at 87.29 K using a Micromeritics ASAP 2010 analyzer (accelerated surface area and porosimeter, Norcross, GA). Prior to the experiments, cured and carbonized samples were degassed for 2 hours at 150°C under a vacuum pressure less than 20 torr. The specific surface area, A_{BET} , was determined from the linear part of the BET equation ($P/P_0 = 0.06 \sim 0.30$). The pore size distribution for the samples was calculated by employing the regularization method according to Density Functional Theory (DFT) using DFT Plus. See, e.g., Micromeritics Instrument Corporation, DFT plus, Norcross, GA, 1997. For relative pressure less than 0.01, a fixed volumetric dosing of 10 cm^3/g of liquid argon was applied. For relative pressures greater than or equal to 0.01, the volumetric argon dosing amount was calculated based on satisfying predetermined relative pressures up to and including approximately 0.9.

[0223] The amount of gas adsorbed is a function of partial pressure (concentration) of the adsorbate, temperature of the system, the adsorbate and the adsorbent. Measuring the amount of a compound adsorbed on an adsorbent versus concentration or pressure at a constant temperature results in an adsorption isotherm. **FIG. 13** shows Ar adsorption isotherms from pyrolyzed electrospun phenolic fibers at temperatures ranging from 600°C to 2000°C. The carbon fibers generated at temperatures of 800°C to 1400°C exhibit typical type I adsorption isotherms as defined by the IUPAC classification. The isotherms are characterized by a sharp vertical rise indicative of micropore filling at relative pressures of around 10^{-6} to 10^{-5} followed by a gradual increase in adsorbed volume as relative pressure increases. After a relative pressure of about 0.1 is reached, the further increase in adsorption is relatively low as indicated by the almost horizontal line as relative pressure approaches 0.9. The total volume of argon adsorbed was over 200 cm^3/g for carbon fibers pyrolyzed at 800°C, 190 cm^3/g for the 1000°C and 1200°C carbon fiber samples and approximately 150 cm^3/g for the fibers produced at 1400°C. In contrast, the argon adsorption isotherms for the carbon fibers pyrolyzed at temperatures of 1600°C to 2000°C indicate the material is non-porous. The total volume adsorbed over the relative pressure range of 10-6 to 0.9 was approximately 25 cm^3/g , 6 cm^3/g and 1 cm^3/g for the 1600°C, 1800°C and 2000°C samples, respectively. Similarly, the adsorption behavior of the electrospun and cured electrospun fibers indicate these materials are also non-porous, shown in **FIG. 14**, where the total adsorbed volume was 13 cm^3/g and 5 cm^3/g , respectively. A portion of the polymeric solution consisting of a 1:1 blend of novolak and resole in ethanol was cured and subsequently pyrolyzed without being processed into fibers via electrospinning. The argon adsorption isotherms indicated these materials are non-porous.

[0224] *BET specific surface areas.* The BET specific surface areas for the electrospun, cured and carbonized fibers are provided in Table 1. The electrospun and cured electrospun fibers showed essentially no internal surface area. The electrospun fibers pyrolyzed at temperatures of 800°C to 1400°C revealed specific BET surface areas ranging from almost 600 m^2/g to about 400 m^2/g , with the lowest carbonization temperature yielding the highest surface area. At carbonization temperatures exceeding 1400°C, the materials showed BET specific surface areas less than 25 m^2/g and

thus indicating the material to be essentially non-porous. **FIG. 15** shows BET surface areas for carbonized electrospun fibers as a function of thermal treatment. The curve indicates that a transformation took place within the material, such as a densification of the material and elimination of defects within the ribbon-like planes. The surface areas for the carbon fibers pyrolyzed at the higher temperatures are more indicative of that found for typical glassy carbons for the entire temperature range studied. The non-electrospun phenolic resin blend cured and pyrolyzed at temperatures of 800°C, 1200°C and 1800°C yielded BET specific surface areas of less than 25 m²/g. The reasons for the relatively high specific surface for the pyrolyzed electrospun fibers at temperatures of 800°C to 1400°C with no activation is hypothesized to be, in part, a function of processing technique, the nano-sized fiber dimension and an interlayer spacing of greater than 4 Å between the disorganized ribbons of single or double-layered graphene sheets that form a measurable gap for adsorption to occur. It has been reported that theoretical calculations and gas adsorption have indicated that microporosity in non-graphitized carbons consists mainly of slit pores of 6-8 Å in width. The carbon fibers pyrolyzed at the higher temperatures will be discussed in subsequent sections.

[0225] *X-ray diffraction.* XRD patterns were collected after carbonization of the electrospun and non-electrospun phenolic resins using a Philips Analytical (currently PANalytical) X'PERT PRO X-ray diffraction system using Cu K α radiation at 45kV and 40 mA and X'celerator detector. The samples were ground to powder and prepared as thin layers on aluminum slides. The data was collected using a step size of 0.00836° and a scan rate of 0.008848°/20/s between 2°20 and 75°20.

[0226] XRD was performed on the carbonized electrospun fibers (1000°C to 2000°C) to provide additional insight into the structural changes occurring as a function of thermal treatment. As shown in **FIGs. 8A** and **8B** show the reflections from the sample holder) a broad band is observed corresponding to reflections from (00.2) planes at $2\theta \approx 26^\circ$ which is low in intensity at 1200°C and increases as the temperature is incrementally increased 2000°C. Small crystal sizes and various crystal imperfections, such as strains and faulting can affect the diffraction pattern, producing peak broadening. A shift in the (00.2) peak with thermal treatment results from a decrease in the interlayer spacing, $d(002)$, as shown in Table 2.

Table 2. X-ray diffraction: crystallite size in c-direction interplanar spacing $d(00.2)$ of carbonized electrospun phenolic fibers at temperatures of 1000°C to 2000°C

Temp °C	2 θ °	Interplanar d-spacing Å	Stack Height L_c nm
1000	24.92	3.57	11
1200	24.97	3.56	42
1400	25.02	3.56	32
1600	26.46	3.37	210
1800	26.38	3.38	171
2000	26.49	3.36	280

[0227] At temperatures of 1600°C, 1800°C, and 2000°C, the interlayer spacings of $d(00.2)$ are 3.37 Å, 3.38 Å and 3.36 Å, respectively, indicating the presence of graphite. The non-electrospun phenolic resin blend pyrolyzed at temperatures of 1000°C, 1200°C and 1800°C indicated interlayer spacings $d(00.2)$ of 3.58 Å, 3.48 Å and 3.46 Å, respectively, indicating the materials to have a low degree of order, but increased order with increasing temperature. The Scherrer equation was utilized to calculate the mean crystallite size, in the c-direction, L_c , where $L_c = K\lambda / B_{(2\theta)} \cos \theta$.

[0228] In the Scherrer equation, K is the shape factor and a value of 0.9 was utilized, $B_{(2\theta)}$ is the breadth of diffraction peak (full width half maximum, FWHM minus the instrument breadth) in radians for the (002) peak, λ is the X-ray wavelength (1.541874 Å) and θ is the diffraction angle. The results, shown in Table 2, indicate a trend of increasing crystallite size, or stack height of the graphene sheets, as a function of temperature. The results should be used only for trending purposes as the equation was derived for cubic crystals, and although it is often applied to peak breadths of noncubic materials, it is more appropriate in this case as an approximation.

[0229] *Pore Size Distribution.* The pore size distributions (PSD), calculated by density function theory (DFT), indicate the pore widths for the carbon electrospun fibers pyrolyzed at temperatures of 800°C to 1400°C to be predominantly microporous. **FIG. 16**, curves (a), (b), (c) and (d) show the pore size distribution curves for pore widths ranging from 4 Å (low-end capability of measurement) to 10 Å which is the region of the measured porosity for these samples. For the 800°C sample a relatively narrow Gaussian-type distribution is observed that is centered at approximately 5 Å. As the pyrolysis temperature is increased to 1000°C, the pore size distribution shifts into two smaller Gaussian-type peaks of essentially the same breadth and height, thus indicating a portion of the pores sizes have been reduced. As the temperature is increased to 1200°C and then 1400°C, a Gaussian-type distribution is still present and centered around 5 Å, but with a tail to the right. This is evidence of further structure rearrangement of the ribbon-like network. Additionally, it appears there may also be a shift to even smaller sized pores that are less than 4 Å, however other analytical

techniques are required to validate this hypothesis. The micropore, mesopore and total volume and for the electrospun fibers pyrolyzed at temperatures ranging from 800°C to 1400°C are summarized in Table 3 and show the total volume to consist of predominantly micropores with volumes ranging from 0.226 cm³/g to 0.165 cm³/g, respectively.

5 **Table 3. BET surface area and pore size distribution (DFT) for carbonized electrospun phenolic resins**

Sample	Temp (°C)	S _{BET} (m ² g ⁻¹)	V _{micro} (cm ³ g ⁻¹)	V _{meso} (cm ³ g ⁻¹)	V _{total} (cm ³ g ⁻¹)
e-spun	25	3	0.000	0.006	0.006
cured e-spun	160	36	0.000	0.030	0.030
e-spun and carbonized	800	575	0.226	0.007	0.233
e-spun and carbonized	1000	506	0.200	0.008	0.208
e-spun and carbonized	1200	525	0.211	0.000	0.211
e-spun and carbonized	1400	413	0.165	0.000	0.165
e-spun and carbonized	1600	21	0.001	0.003	0.004
e-spun and carbonized	1800	4	0.000	0.007	0.007
e-spun and carbonized	2000	10	0.001	0.003	0.004

20 [0230] There appears to be a formation of micropore volume in electrospun phenolic fibers pyrolyzed at temperatures ranging from 800°C to 1400°C, with the most uniform distribution observed for the 800°C that is centered around 5 Å. As the temperature is incrementally increased to 2000°C, a decrease in open micropore volume is observed. The micropore volume observed for the carbonized electrospun fibers was not present in the non-electrospun materials produced from the same phenolic resin blend for the temperature range of 800°C to 1800°C. It has been reported that "non-graphitizing" carbons and synthetic polycrystalline graphite possess considerable porosity that is intimately associated with the structure of the carbon, as well as the manufacturing techniques and the precursor materials. Although it is not well understood, it appears that electrospinning provides a mechanism for creating carbon precursors, that when pyrolyzed at temperatures 800°C to 1400°C, results in the formation of microporous phenolic resin-derived carbon nanofibers.

25 [0231] *High Resolution Transmission Electron Microscopy (HRTEM).* HRTEM images were obtained to ascertain the effect of thermal treatments on the microstructures of the fibrous carbon materials. The instrument used was a Philips/FEI Tecnai F20 field emission transmission electron microscope operating at a 200 KV accelerating potential. Energy dispersive spectra were collected with an EDAX thin window detector with an EDAX pulse height analyzer and the data was analyzed with Emispec's Tecnai image analysis (TIA) software. HRTEM images were collected with a Gatan imaging filter (GIF) as were electron energy loss spectra (EELS). Fast Fourier transforms of the lattice images, analyses of the 30 transforms, and analyses of the EELS spectra were performed with Gatan's Digital micrograph software.

35 [0232] Phenolic resin blend that had not been electrospun was pyrolyzed and examined by HRTEM for comparison of the carbon structures with those that are formed from electrospinning. Macroscopically, this produced a mass of glassy material with conchoidal fracture. FIG. 17 depict HRTEM images of crushed aliquots of the glass revealing that it consisted of a tangle of interwoven linear features. These linear features are the edges of the aromatic graphene sheets mentioned earlier with a thickness of one carbon atom. The sheets are bundled into packets of parallel sheets and contorted into accurate to nearly circular orientations. Thicknesses of these bundles are variable, as seen in the image, but typically range from two to as many as seven sheets per bundle. The contorted or nearly circular geometry of the graphene sheet packets would likely preclude permeability to gases (in this case Ar) used for BET determinations. Thicknesses between the sheets define the (00.2) d-spacing detected by X-ray diffraction. These can be measured directly in the image 40 directly or "averaged" across the image with a fast Fourier transform. The frequency denoting the (00.2) spacings appears as a diffuse ring about the origin. The center of this ring, the "average" spacing, indicated that the interplanar spacing between the graphene sheets within this image is about 3.79 Å. An additional ring lying outside of this frequency corresponds to the {10.0} spacings of 2-H graphite at 2.15 Å. Although the interplanar spacings have been related to graphite, it should be noted that there are no large regions within this glassy material that would be termed crystalline graphite. 45 The diffuse nature of the (00.2) ring indicated that this spacing is variable and its ring geometry indicates random orientations of the c axis, and therefore the graphene sheets. By contrast, the {10.0} intensity is sharp, indicating much less variability of the C-C distances within each graphene sheet. Electron diffraction patterns, which sample a larger area than that shown in the HRTEM image, look similar with an average interlayer (00.2) spacing of about 3.47 Å. This is almost identical to that determined above by X-ray diffraction of 3.46 Å.

50 [0233] HRTEM images of carbonized electrospun fibers look very similar superficially, in that they consisted of graphene sheets. As the carbonization temperature was increased from 1000°C to 1600°C, the number of sheets per bundle also increased, from one to 6 or more layers. This condition seems to remain essentially constant up to 2000°C. Above 55

1600°C the pyrolyzed samples displayed another interesting phenomenon. The sheets closest to the sides of each fiber tended to be partially aligned with that edge. This is apparent in some of the images and their Fourier transforms, as well as in some of the electron diffraction patterns. The sides of the fibers would have experienced greater surface tension than the interior of the fibers during the spinning process. As the fiber diameter decreases, this surface, and presumably the graphene sheet alignment, would increase. With increased alignment of the graphene sheets, a structure more closely approaching that of classical graphite would be formed. Graphitic grains were indeed found sporadically in many of the fibers of electrospun phenolic resin heated to 1600°C or higher (FIG. 7). They were commonly found at the edges of the fibers where they could have nucleated on the aligned graphene sheets in that region. A mechanism called stress graphitization has been reported whereby a sudden transformation to graphite occurs. See, e.g., Ihagaki, M. and Meyer, R.A., in *Chemistry and Physics of Carbon*, Thrower, P.A. and Radovic, L.R., ed., Dekker: NY, vol. 26, 1999. Shear stresses introduce strain into porous carbons by flattening pores. See, e.g., Oberlin, A. and Terrière, G. *Carbon*, 1975, 13, 367 and Bustin, R.M.; Rouzaud, J.N. and Ross, J.V. *Carbon*, 1995, 33(5), 679. This phenomena has been observed in thin polyimide films (Kapton, Upilex, Novax and PPT) that were carbonized and graphitized up to 3000°C. They were found to graphitize suddenly above 2100°C when the pore walls break. See, e.g., Bourgerette, C.; Oberlin, A.; and Inagak, M. *J. Mater. Res.*, 1995, 10(4), 1024.

[0234] The structure of these crystals is interesting in that an intensity appears at about 2.08 Å at an angle of about 80° from the c axis. This suggested that the intensity represented the (10.1) reflection of rhombohedral (3-R) graphite (space group R3) rather than 2-H graphite which was assumed for most of the carbon. Nevertheless, variation in stacking and orientation of the c axis renders highly streaked intensities when large portions of any crystal are analyzed.

Example 9

Activated Carbon Fibers from Electrospun Phenolic resins

[0235] *Phenolic Electrospun Fibers.* Phenolic electrospun fibers were prepared as described above for Example 7. The samples carbonized at 1000°C were selected for subsequent activation.

[0236] *Activation.* Carbonized electrospun phenolic fibers were subjected to an activation process. To activate the carbonized phenolic fibers, a sample was placed in a quartz tube and the quartz tube was placed into a tube furnace (Thermolyne). The furnace was purged with a N₂/CO₂ mixture (N₂/CO₂ mixture can be varied from 100 % CO₂ to 10% CO₂). The temperature of the furnace was increased to between 900 and 1000°C. The activation process was continued for 20 min to 5 hours once the temperature reached 900 to 1000° C. After activating, the argon adsorption isotherms were measured at 87.29K for the activated carbonized electrospun Phenolic fibers and the volume of argon adsorbed, and the total pore volume, the micropore volume, and BET surface area were calculated.

[0237] *Adsorption.* Adsorption isotherms and surface area of the materials were determined using a Micromeritics ASAP 2010 instrument (Norcross, GA.) and the incremental and pore size distribution calculated by density function theory (DFT) using software provided with the instrument and are summarized in Table 4. Prior to the measurements, each cured and carbonized sample was placed into a 1.27cm outside diameter sample tube closed with a SealFrit, and degassed for 2 hours at a temperature of 150°C and a vacuum pressure less than 20torr on the degas port of the analyzer. After the degassing process was completed, the sample tube assembly was transferred to the analysis port. Argon was selected as the probe molecule because it is spherical, monatomic and non-polar and is preferred over nitrogen for studies of microporosity. For relative pressure less than 0.01, a fixed volumetric dosing of 10cm³/g of liquid argon was applied, and for relative pressures greater than or equal to relative pressures of 0.01, the volumetric argon dosing amount was calculated based on satisfying predetermined relative pressures up to and including relative pressures of approximately 0.9.

[0238] The results of the BET specific surface area, micropore volume and total pore volumes calculated using DFT are shown below in Table 4 for the activated, carbonized electrospun phenolic fibers. According to IUPAC nomenclature, micropores have widths less than 20 angstroms (or 2 nm), mesopores have widths between 20 angstroms and 500 angstroms (2 nm to 50 nm), and macropores have widths greater than 500 angstroms (50nm).

Table 4. BET surface area and pore volume (DFT) for activated, carbonized electrospun Phenolic resins.

Phenolic Resins		DFT				
Burn-off (%)	SA _{BET} (m ² /g)	V _{ultra-micro} (cm ³ /g)	V _{super-micro} (cm ³ /g)	V _{tot-micro} (cm ³ /g)	V _{meso} (cm ³ /g)	V _{total} (cm ³ /g)
0	506	0.152	0.048	0.200	0.008	0.208
15	872	0.234	0.115	0.350	0.002	0.352
26	1033	0.283	0.131	0.414	0.000	0.414

(continued)

Phenolic Resins		DFT				
Burn-off (%)	SA _{BET} (m ² /g)	V _{ultra-micro} (cm ³ /g)	V _{super-micro} (cm ³ /g)	V _{tot-micro} (cm ³ /g)	V _{meso} (cm ³ /g)	V _{total} (cm ³ /g)
40	1239	0.308	0.189	0.496	0.000	0.496
62	1404	0.235	0.326	0.561	0.000	0.561
72	1548	0.280	0.344	0.624	0.000	0.624

[0239] In Example 9, the varying percentages of burn-off shown in Table 4 were obtained by exposing the original carbonized, electrospun phenolic fibers (processed at the same conditions) to different activation times, or dwell times. Alternatively, concentration of the oxidizing gas, temperature, or different oxidizing gas, such as steam, could be used to manipulate the resulting properties of activated fibers. As the % burn-off increased, the specific BET surface area increased. **FIG. 19** shows the argon adsorption isotherms for the activated, carbonized electrospun phenolic fibers. The total pore volume and the supermicropore volume increased as a function of increasing percent burn-off (supermicropores are defined with pores having widths between 7Å and 20Å, M.M. Dubinin, Carbon, 1989, 27(3):457-467). Under the activation utilized to generate this series of activated samples, the mesopore volume did not develop.

Example 10

Activated Carbon Fibers from Electrospun PAN

[0240] *Electrospun1 PAN.* Electrospun PAN was prepared as described above for Example 8. The samples carbonized at 1000°C were selected for subsequent activation.

[0241] *Activation.* Carbonized electrospun PAN were then subjected to an activation process. To activate the carbonized, electrospun PAN fibers, a sample was placed in a quartz tube and the quartz tube was placed into a tube furnace (Thermolyne). The furnace was purged with a N₂/CO₂ mixture (N₂/CO₂ mixture can be varied from 100 % CO₂ to 10% CO₂). The temperature of the furnace was increased to between 900 and 1000°C. The activation process was continued for 20 min to 5 hours once the temperature reached 900 to 1000°C. After activating, the argon adsorption isotherms were measured at 87.29K for the activated carbonized PAN fibers and the volume of argon adsorbed, and the total pore volume, the micropore volume, and BET surface area were calculated. **FIG. 20.**

[0242] *Adsorption.* Adsorption isotherms and surface area of the materials were determined using a Micromeritics ASAP 2010 instrument (Norcross, GA.) and the incremental and pore size distribution calculated by density function theory (DFT) using software provided with the instrument and are summarized in Table 5. Prior to the measurements, each cured and carbonized sample was placed into a 1.27cm outside diameter sample tube closed with a SealFrit, and degassed for 2 hours at a temperature of 150°C and a vacuum pressure less than 20torr on the degas port of the analyzer. After the degassing process was completed, the sample tube assembly was transferred to the analysis port. Argon was selected as the probe molecule because it is spherical, monatomic and non-polar and is preferred over nitrogen for studies of microporosity. For relative pressure less than 0.01, a fixed volumetric dosing of 10cm³/g of liquid argon was applied, and for relative pressures greater than or equal to relative pressures of 0.01, the volumetric argon dosing amount was calculated based on satisfying predetermined relative pressures up to and including relative pressures of approximately 0.9.

Table 5. BET surface area and pore volume (DFT) for activated, carbonized electrospun PAN.

PAN		DFT				
Burn-off (%)	SA _{BET} (m ² /g)	V _{ultra-micro} (cm ³ /g)	V _{super-micro} (cm ³ /g)	V _{tot-micro} (cm ³ /g)	V _{meso} (cm ³ /g)	V _{total} (cm ³ /g)
0	108	0.000	0.011	0.011	0.022	0.033
12	416	0.089	0.072	0.161	0.009	0.170
22	888	0.120	0.196	0.316	0.044	0.360
31	1128	0.144	0.233	0.376	0.094	0.470
47	1362	0.108	0.295	0.403	0.161	0.561
60	1462	0.195	0.517	0.712	0.078	0.790

[0243] In Example 10, the varying percentages of burn-off shown in Table 5 were obtained by exposing the original carbonized, electrospun PAN fibers (processed at the same conditions) to different activation times, or dwell times. Alternatively, concentration of the oxidizing gas, temperature, or different oxidizing gas, such as steam, could be used to manipulate the resulting properties of activated fibers. As the % burn-off increased, the specific BET surface area increased. FIG. 21 shows the argon adsorption isotherms for the activated, carbonized electrospun phenolic fibers. The total pore volume and the supermicropore volume increased as a function of increasing percent burn-off. Under the activation utilized to generate this series of activated samples, the mesopore volume developed.

Example 11

Activated Commercially-Available Carbon Fibers from Phenolic resins (Novoloid Fibers)

[0244] Cured novoloid fibers were purchased from American Kynol, Inc. (NY). The purchased cured fibers were carbonized using the experimental set-up and conditions as described in Examples 9 and 10. The carbonized novoloid fibers were then activated following the same procedures described in Example 9. The carbonized and activated commercially-processed novoloid fibers at 17% burn-off showed a specific BET surface area of 873 m²/g, which was similar to the activated carbonized electrospun phenolic fibers at comparable burn-off. Inverse Gas Chromatography (IGC) manufactured by Surface Measurement Systems, Allentown, PA was used to investigate the adsorption characteristics for light gases. In each measurement, approximately 25 mg of activated carbon fiber sample (activated carbonized electrospun phenolic fibers and activated, carbonized novoloid fibers) was packed into a 30 cm long, 3-mm inner diameter glass column. Glass wool was placed both end of the glass column to hold the sample in the center. Helium was used as the carrier gas and methane was selected as the model gas. In the measurement, 20 mL/min helium-methane mixture with a volumetric ratio of 20:1 was continuously purged through the column and the concentration of methane at the outlet was monitored with a Flame Ionization Detector. The breakthrough curves were measured; the volume of methane adsorbed and heat of adsorption were calculated. Comparison of the results was shown in Table 6.

Table 6. Comparison of Methane Adsorption for activated carbon fibers: electrospun versus commercially-processed

Activated Carbon fiber type	BET SA (m ² /g)	% Burn-off	Total micropore vol (cm ³ /g)	Total pore vol (cm ³ /g)	Amount Adsorbed (mMol/g)	Heat of Absorption E (kJ/mol)
Phenolic Resin E-spun fibers	872	15.0%	0.35	0.352	0.69	-11.42
Commercial novoloid fibers	873	16.9%	0.32	0.393	0.35	-6.06

[0245] Table 6 shows both samples possess similar specific BET surface areas, % burn-off, total micropore volume, however, the activated carbonized electrospun phenolic resins fibers showed a higher amount of methane adsorbed and exothermic heat of adsorption (negative refers to "exothermic" and indicates thermodynamically favorable in this case) when compared to the activated carbonized novoloid fibers. Although methane was used as a model gas in this case, it is anticipated that carbon monoxide, nitrogen oxide, acetaldehyde, ammonia, ethane, hydrogen, oxygen, formaldehyde, butane, etc. will show similar results.

Example 12

Activated Commercially-Available PAN Fibers

[0246] Stabilized PAN fibers were obtained from Zoltek, St. Louis, MO. The purchased stabilized fibers were carbonized using the experimental set-up and conditions as described in Examples 9 and 10. The carbonized fibers were then activated and the adsorption properties were measured following the same procedures described in Examples 9 and 10. Table 7 shows the specific BET surface areas, and calculated pore size distribution (using DFT) for the activated carbon conventionally-spun fibers.

Table 7. BET surface area and pore volume (DFT) for activated, carbonized conventionally-processed PAN.

		DFT				
Burn-off (%)	SA _{BET} (m ² /g)	V _{ultra-micro} (cm ³ /g)	V _{super-micro} (cm ³ /g)	V _{tot-micro} (cm ³ /g)	V _{meso} (cm ³ /g)	V _{total} (cm ³ /g)
0	ND	ND	ND	ND	ND	ND
7	70	0.000	0.022	0.022	0.020	0.042
17	123	0.000	0.022	0.022	0.020	0.042
41	77	0.000	0.012	0.012	0.017	0.029
53	103	0.000	0.018	0.018	0.024	0.042

[0247] The activated carbon fibers that were conventionally spun showed significantly different properties than the activated electrospun PAN counterparts, shown in Example 10. The specific BET surface area, micropore volume and total pore volume were significantly less than that for the activated carbonized electrospun PAN fibers. The specific BET surface area for the activated carbonized conventionally processed PAN at 53% burn-off was 103 m²/g compared to specific BET surface areas of 1362 and 1462 m²/g at 47% and 60% burn-off, respectively, for the activated carbonized electrospun PAN fibers. Thus, it is expected that the activated, electrospun PAN fibers will show enhanced adsorption characteristics, similar to that described in Example 11, for a range of light gases.

Example 13

Example of Metal Salt Added to Phenolic Resin Electrospinning Mixture

[0248] The metal salt, dihydrogen hexachloroplatinate (IV) (Aldrich) was dry blended to a dry mixture of novolak and resole powder (blended at a ratio of 1:1). The dry blend mixture contained 2.12 g platinum salt and 33.78 g phenolic resin powder (or 16.89 grams of each resin). The dry blend was then dissolved in ethanol to yield a 50 wt% polymer solution. The polymer solution was electrospun using the conditions disclosed in Example 1. The resulting electrospun fiber was cured in a Thermolyne tube furnace at 160°C with a ramp rate of 0.1°C/min and held isothermally for 2 hours. The cured sample was then carbonized in the same furnace at 800°C with 0.5 L/min of continuous nitrogen purge. The sample was removed from the Thermolyne furnace and placed in a graphite cup and into the Red Devil high temperature furnace (R.D. Webb). Before carbonizing the sample at 1200°C, a purge cycle was completed three times to remove oxygen and moisture from the system. A ramp rate of 10°C/min was utilized to reach the carbonization temperature of 1200°C with 0.5 L/min of continuous argon purge. After the carbonization temperature of 1200°C was obtained, the sample was held at the temperature for 2 hours before cooling to room temperature. FIG. 1 shows a HRTEM image of the carbonized fibers with platinum. The metal salt was reduced to platinum metal and provided nucleation sites for graphitic formation. The HRTEM shows crystalline graphite.

Claims

1. A process for making phenolic materials comprising:
 - 45 a) providing a phenolic polymeric system;
 - b) electrostatically processing the phenolic polymeric system,
 - c) curing the phenolic materials; and
 - d) carbonizing the cured materials to provide carbonized phenolic materials.
2. A process according to claim 1, wherein the carbonized phenolic materials are fibers, beads, nanofibers, microfibers, films or combinations thereof.
3. A process according to claim 1 or 2 for making phenolic fibers or beads further comprising curing the phenolic fibers or beads where
 - 55 a) the curing is performed by heating the phenolic fibers or beads to a temperature of 20 °C to 180 °C at a ramp rate of 0.1 degC/min to 5 degC/min and holding at the temperature for 2 hours to 8 hours;
 - b) the carbonizing is performed by heating the cured fibers or beads to a temperature of 700 °C to 2000 °C at

a ramp rate of 1 degC/min to 25 degC/min under inert atmosphere and holding at the temperature for 2 hours to 8 hours;

c) the carbonizing has a carbon yield of at least 40 percent;

d) the phenolic polymeric system is a phenolic polymeric solution or a phenolic polymer melt.

5

4. A process according to claim 1, 2 or 3 for making phenolic fibers or beads comprising:

- a) providing a phenolic polymeric system;
- b) electrostatically spinning the phenolic polymeric system to create phenolic fibers or electrostatically spraying the phenolic polymeric system to create phenolic beads, the beads having a diameter of 100 nanometers to 10 microns;
- c) curing the phenolic fibers or beads;
- d) carbonizing the cured fibers or beads to provide carbonized phenolic fibers or beads; and
- e) activating the carbonized phenolic fibers or beads to provide activated phenolic fibers or beads.

15

5. A process according to claim 4 wherein

- a) the activating step is performed by heating the carbonized phenolic fibers or beads to a temperature of 700 °C to 1000 °C under oxidizing environment and holding at the temperature for 20 minutes to 5 hours;
- b) the carbonizing is performed by heating the cured fibers or beads to a temperature of 700 °C to 2000 °C at a ramp rate of 1 degC/min to 25 degC/min under inert atmosphere and holding at the temperature for 2 to 8 hours;
- c) the carbonizing has a carbon yield of at least 40 percent; or
- d) the phenolic polymeric system is a phenolic polymeric solution or a phenolic polymer melt.

25 6. A process according to any preceding claim wherein the phenolic polymeric system comprises

- a) polymers selected from the group consisting of novolak, resole and mixtures thereof, or
- b) a solution comprising a solvent selected from the group consisting of ethanol, isopropanol, acetone, ethyl acetate, dichloromethane, hexafluoropropanol, and mixtures thereof.

30

7. A process according to claim 1 wherein the phenolic polymeric system is a solution of 40 to 60 weight percent phenolic polymer in a solvent selected from the group consisting of ethanol, isopropanol, acetone, ethyl acetate, dichloromethane, hexafluoropropanol, and mixtures thereof.

35 8. A process according to any preceding claim wherein the phenolic polymeric system is a solution comprising a mixture of (i) a solution of 40 to 60 weight percent resole in a solvent selected from the group consisting of ethanol, isopropanol, acetone, ethyl acetate, dichloromethane, hexafluoropropanol, and mixtures thereof and (ii) a solution of 40 to 60 weight percent novolak in a solvent selected from the group consisting of ethanol, isopropanol, acetone, ethyl acetate, dichloromethane, hexafluoropropanol, and mixtures thereof.

40

9. A process according to claim 8 wherein the phenolic polymeric system is a solution comprising 30 to 70 weight percent resole solution and 70 to 30 weight percent novolak solution.

45 10. A process according to any preceding claim further comprising adding an additive to the phenolic polymeric system prior to electrostatically spinning or spraying the system.

11. A process according to claim 10 wherein the additive is

50 a) selected from the group consisting of dispersed metals, metal oxides, metal salts, surfactants, curing agents, cross-linking agents, stabilizers, porosity enhancers, nonvolatile and non-compatible solvents, and mixtures thereof, or

b) selected from the group consisting of copper nanofibers, hexamethylenetetramine, PtCl_2 , and mixtures thereof.

55 12. A process according to any preceding claim, further comprising the step of adding a polymer blend to the phenolic polymeric system prior to electrostatically spinning or spraying the system.

13. A process according to claim 12, wherein the polymer blend is selected from the group consisting of poly(acrylic

acid), cellulose acetate, poly(vinyl acetate), poly(ethyleneimine), poly(ethylene-co-vinylacetate), poly(lactic acid), and mixtures thereof.

5 14. Phenolic beads or a film produced by the process according to any preceding claim.

10 15. A process according to any of claims 1 to 13 for making phenolic beads wherein the beads are electrostatically sprayed onto a substrate to create a film.

15 16. A process according to any of claims 1 to 13 wherein the phenolic materials are phenolic fibers and wherein the carbonized phenolic fibers have a diameter of about 10 microns to 50 nanometers.

20 17. A fibrous material comprising a non-woven network of carbonized phenolic fibers made by a process according to claim 16.

25 18. A fibrous material according to claim 17 wherein

a) the carbonized phenolic fibers comprise greater than 70% micropores or greater than 90% microphores;

b) the carbonized phenolic fibers have a BET surface area of 400 m²/g to 800 m²/g;

c) the carbonized phenolic fibers have a micropore volume of 0,2 cm³/g to 0,4 cm³/g; or

20 d) the fibrous material further comprises an additive and/or a polymer blend selected from the group consisting of poly(acrylic acid), cellulose acetate, poly(vinyl acetate), poly(ethyleneimine), poly(ethylene-co-vinylacetate), poly(lactic acid), and mixtures thereof.

25 19. A fibrous material according to claim 17 or 18 wherein

a) the non-woven network of carbonized phenolic fibers is in the form of a mat of non-woven fibers or

b) the non-woven network further comprises phenolic beads.

30 20. An activated phenolic fiber or bead produced by a process according to any of claims 1 to 13 wherein

a) when the fiber or bead is activated at a temperature of between about 800 °C and about 1250 °C, the activated fiber has a BET surface area of at least about 800 m²/g and has at least about 60% micropores having a pore width of less than about 7 Å or

35 b) when the fiber or bead is activated at a temperature of between about 800 °C and about 1260 °C, the activated bead has a BET surface area of at least about 1400 m²/g and has at least about 40% micropores having a pore width of less than about 7 Å.

40 21. A component of a smoking article comprising a filter comprising electrospun carbonized fibers and/or electrosprayed carbonized beads made by a process according to any of claims 1 to 13.

45 22. A method of making the component of claim 21 comprising incorporating electrospun carbonized fibers and/or electrosprayed carbonized beads therein in a cavity and/or in a component of a cigarette filter.

23. A smoking article including a component comprising electrospun carbonized fibers and/or a filter comprising electrosprayed carbonized beads made by a process according to any of claims 1 to 13.

Patentansprüche

50 1. Prozess zum Herstellen von Phenolmaterialien, aufweisend:

a) Bereitstellen eines Phenol-Polymer systems;

b) elektrostatisches Verarbeiten des Phenol-Polymer systems;

c) Aushärten der Phenolmaterialien; und

55 d) Karbonisieren der ausgehärteten Materialien, um karbonisierte Phenolmaterialien bereitzustellen.

2. Prozess nach Anspruch 1, wobei die karbonisierten Phenolmaterialien Fasern, Perlen, Nanofasern, Mikrofasern, Folien oder Kombinationen davon sind.

3. Prozess nach Anspruch 1 oder 2 zum Herstellen von Phenolfasern oder -perlen, weiter aufweisend das Aushärten der Phenolfasern oder -perlen, wobei

5 a) das Aushärten mittels Erwärmen der Phenolfasern oder -perlen auf eine Temperatur von 20 °C bis 180 °C bei einer Anstiegsrate von 0,1 °C/Min bis 5 °C/Min und Halten auf der Temperatur für 2 Stunden bis 8 Stunden ausgeführt wird;

10 b) das Karbonisieren mittels Erwärmen der ausgehärteten Fasern oder Perlen auf eine Temperatur von 700 °C bis 2000 °C bei einer Anstiegsrate von 1 °C/Min bis 25 °C/Min unter inerter Atmosphäre und Halten auf der Temperatur für 2 Stunden bis 8 Stunden ausgeführt wird;

15 c) das Karbonisieren eine Kohlenstoffausbeute von mindestens 40 Prozent aufweist;

20 d) das Phenol-Polymersystem eine Phenol-Polymerlösung oder eine Phenol-Polymerschmelze ist.

4. Prozess nach Anspruch 1, 2 oder 3 zum Herstellen von Phenolfasern oder -perlen, aufweisend:

25 a) Bereitstellen eines Phenol-Polymersystems

15 b) elektrostatisches Spinnen des Phenol-Polymersystems, um Phenolfasern zu erzeugen, oder elektrostatisches Sprühen des Phenol-Polymersystems, um Phenolperlen zu erzeugen, wobei die Perlen einen Durchmesser von 100 Nanometer bis 10 Mikrometer aufweisen;

20 c) Aushärten der Phenolfasern oder -perlen

20 d) Karbonisieren der ausgehärteten Fasern oder Perlen, um karbonisierte Phenolfasern oder -perlen bereitzustellen; und

25 e) Aktivieren der karbonisierten Phenolfasern oder -perlen, um aktivierte Phenolfasern oder -perlen bereitzustellen.

25 5. Prozess nach Anspruch 4, wobei

30 a) der Aktivierungsschritt mittels Erwärmen der karbonisierten Phenolfasern oder -perlen auf eine Temperatur von 700 °C bis 1000 °C unter oxidierendem Milieu und Halten auf der Temperatur für 20 Minuten bis 5 Stunden ausgeführt wird;

35 b) das Karbonisieren mittels Erwärmen der ausgehärteten Fasern oder Perlen auf eine Temperatur von 700 °C bis 2000 °C bei einer Anstiegsrate von 1 °C/Min bis 25 °C/Min unter inerter Atmosphäre und Halten auf der Temperatur für 2 bis 8 Stunden ausgeführt wird;

40 c) das Karbonisieren eine Kohlenstoffausbeute von mindestens 40 Prozent aufweist; oder

35 d) das Phenol-Polymersystem eine Phenol-Polymerlösung oder eine Phenol-Polymerschmelze ist.

6. Prozess nach einem der vorstehenden Ansprüche, wobei das Phenol-Polymersystem aufweist

45 a) Polymere, die ausgewählt sind aus der Gruppe bestehend aus Novolak, Resol und Mischungen davon oder

40 b) eine Lösung, die ein Lösungsmittel aufweist, das ausgewählt ist aus der Gruppe bestehend aus Ethanol, Isopropanol, Aceton, Essigester, Dichlormethan, Hexafluorpropanol und Mischungen davon.

7. Prozess nach Anspruch 1, wobei das Phenol-Polymersystem eine Lösung von 40 bis 60 Gewichtsprozent Phenolpolymer in einem Lösungsmittel ausgewählt aus der Gruppe bestehend aus Ethanol, Isopropanol, Aceton, Essigester, Dichlormethan, Hexafluorpropanol und Mischungen davon ist.

45 8. Prozess nach einem der vorstehenden Ansprüche, wobei das Phenol-Polymersystem eine Lösung ist, die eine Mischung aus (i) einer Lösung von 40 bis 60 Gewichtsprozent Resol in einem Lösungsmittel ausgewählt aus der Gruppe bestehend aus Ethanol, Isopropanol, Aceton, Essigester, Dichlormethan, Hexafluorpropanol und Mischungen davon und (ii) einer Lösung von 40 bis 60 Gewichtsprozent Novolak in einem Lösungsmittel ausgewählt aus der Gruppe bestehend aus Ethanol, Isopropanol, Aceton, Essigester, Dichlormethan, Hexafluorpropanol und Mischungen davon aufweist.

50 9. Prozess nach Anspruch 8, wobei das Phenol-Polymersystem eine Lösung ist, die 30 bis 70 Gewichtsprozent Resollösung und 70 bis 30 Gewichtsprozent Novolaklösung aufweist.

55 10. Prozess nach einem der vorstehenden Ansprüche, weiter aufweisend das Hinzufügen eines Zusatzstoffs zum Phenol-Polymersystem vor dem elektrostatischen Spinnen oder Sprühen des Systems.

11. Prozess nach Anspruch 10, wobei der Zusatzstoff

5 a) ausgewählt ist aus der Gruppe bestehend aus dispergierten Metallen, Metalloxiden, Metallsalzen, Tensiden, Härtungsmitteln, Vernetzern, Stabilisatoren, Porositätsverstärkern, nicht flüchtigen und nicht kompatiblen Lösungsmitteln und Mischungen davon oder
b) ausgewählt ist aus der Gruppe bestehend aus Kupfernanofasern, Hexamethylentetramin, PtCl_2 und Mischungen davon.

10 12. Prozess nach einem der vorstehenden Ansprüche, weiter aufweisend den Schritt des Hinzufügens eines Polymergemischs zum Phenol-Polymer system vor dem elektrostatischen Spinnen oder Sprühen des Systems.

15 13. Prozess nach Anspruch 12, wobei das Polymergemisch ausgewählt ist aus der Gruppe bestehend aus Poly(acrylsäure), Zelluloseacetat, Poly(vinylacetat), Poly(ethylenimin), Poly(ethylen-co-vinylacetat), Poly(milchsäure) und Mischungen davon.

14. Phenolperlen oder Phenolfolie, die durch den Prozess nach einem der vorstehenden Ansprüche hergestellt ist.

15 15. Prozess nach einem der Ansprüche 1 bis 13 zum Herstellen von Phenolperlen, wobei die Perlen elektrostatisch auf ein Substrat gesprührt werden, um eine Folie zu erzeugen.

20 16. Prozess nach einem der Ansprüche 1 bis 13, wobei die Phenolmaterialien Phenolfasern sind, und wobei die karbonisierten Phenolfasern einen Durchmesser von ungefähr 10 Mikrometer bis 50 Nanometer aufweisen.

25 17. Fasermaterial, das ein Vliesstoffnetzwerk aus karbonisierten Phenolfasern aufweist, die durch einen Prozess nach Anspruch 16 hergestellt sind.

18. Fasermaterial nach Anspruch 17, wobei

30 a) die karbonisierten Phenolfasern größer als 70 % Mikroporen oder größer als 90 % Mikroporen aufweisen;
b) die karbonisierten Phenolfasern eine BET-Oberfläche von 400 m^2/g bis 800 m^2/g aufweisen;
c) die karbonisierten Phenolfasern ein Mikroporenvolumen von 0,2 cm^3/g bis 0,4 cm^3/g aufweisen; oder
d) das Fasermaterial weiter einen Zusatzstoff und/oder eine Polymermischung ausgewählt aus der Gruppe bestehend aus Poly(acrylsäure), Zelluloseacetat, Poly(vinylacetat), Poly(ethylenimin), Poly(ethylen-co-vinylacetat), Poly(milchsäure) und Mischungen davon aufweist.

35 19. Fasermaterial nach Anspruch 17 oder 18, wobei

40 a) das Vliesstoffnetzwerk aus karbonisierten Phenolfasern die Form einer Matte aus Vliesstofffasern aufweist oder
b) das Vliesstoffnetzwerk weiter Phenolperlen aufweist.

20. Aktivierte Phenolfaser oder -perle, die durch einen Prozess nach einem der Ansprüche 1 bis 13 hergestellt ist, wobei

45 a) wenn die Faser oder Perle bei einer Temperatur zwischen ungefähr 800 °C und ungefähr 1250 °C aktiviert wird, die aktivierte Faser eine BET-Oberfläche von mindestens ungefähr 800 m^2/g aufweist und mindestens ungefähr 60 % Mikroporen mit einer Porenweite von kleiner als ungefähr 7 Å aufweist oder
b) wenn die Faser oder Perle bei einer Temperatur zwischen ungefähr 800 °C und ungefähr 1250 °C aktiviert wird, die aktivierte Perle eine BET-Oberfläche von mindestens 1400 m^2/g aufweist und mindestens ungefähr 40 % Mikroporen mit einer Porenweite von kleiner als ungefähr 7 Å aufweist.

50 21. Komponente eines Raucherartikels, der einen Filter aufweist, der elektrogespinnene karbonisierte Fasern und/oder elektrogesprühte karbonisierte Perlen aufweist, die durch einen Prozess nach einem der Ansprüche 1 bis 13 hergestellt sind.

55 22. Verfahren zum Herstellen der Komponente nach Anspruch 21, aufweisend das Aufnehmen elektrogespinnener karbonisierter Fasern und/oder elektrogesprühter karbonisierter Perlen darin in einem Hohlraum und/oder in einer Komponente eines Zigarettenfilters.

23. Raucherartikel, der eine Komponente beinhaltet, die elektrogespinnene karbonisierte Fasern aufweist und/oder einen Filter, der elektrogesprühnte karbonisierte Perlen aufweist, die durch einen Prozess nach einem der Ansprüche 1 bis 13 hergestellt sind.

5

Revendications

1. Procédé pour fabriquer des matières phénoliques comprenant :

- 10 a) la fourniture d'un système de polymères phénoliques ;
- b) le traitement électrostatique du système de polymères phénoliques ;
- c) le durcissement des matières phénoliques ; et
- d) la carbonisation des matières durcies pour fournir des matières phénoliques carbonisées.

15 2. Procédé selon la revendication 1, dans lequel les matières phénoliques carbonisées sont des fibres, des billes, des nanofibres, des microfibres, des films ou des combinaisons de ceux-ci.

3. Procédé selon la revendication 1 ou 2 pour fabriquer des fibres ou des billes phénoliques comprenant en outre le durcissement des fibres ou des billes phénoliques, où

20 a) le durcissement est effectué en chauffant les fibres ou les billes phénoliques à une température allant de 20 °C à 180 °C à une vitesse de montée de 0,1 degré C/min à 5 degrés C/min et en maintenant la température pendant 2 heures à 8 heures ;

25 b) la carbonisation est effectuée en chauffant les fibres ou billes durcies à une température de 700 °C à 2000 °C à une vitesse de montée de 1 degré C/min à 25 degrés C/min sous une atmosphère inerte et en maintenant la température pendant 2 heures à 8 heures ;

 c) la carbonisation a un rendement en carbone d'au moins 40 pour-cent ;

 d) le système de polymères phénoliques est une solution de polymères phénoliques ou des polymères phénoliques fondus.

30 4. Procédé selon les revendications 1, 2 ou 3 pour fabriquer des fibres ou des billes phénoliques comprenant :

- a) la fourniture d'un système de polymères phénoliques ;
- 35 b) le filage électrostatique du système de polymères phénoliques pour créer des fibres phénoliques ou la pulvérisation électrostatique du système de polymères phénoliques pour créer des billes phénoliques, les billes ayant un diamètre de 100 nanomètres à 10 microns ;
- c) le durcissement des fibres ou des billes phénoliques ;
- d) la carbonisation des fibres ou billes durcies pour fournir des fibres ou des billes phénoliques carbonisées ; et
- 40 e) l'activation des fibres ou des billes phénoliques carbonisées pour fournir des fibres ou billes phénoliques activées.

5. Procédé selon la revendication 4, dans lequel

- a) l'étape d'activation est effectuée en chauffant les fibres ou les billes phénoliques carbonisées à une température de 700 °C à 1000 °C dans un environnement oxydant et en maintenant la température pendant 20 minutes à 5 heures ;
- 45 b) la carbonisation est effectuée en chauffant les fibres ou les billes durcies à une température de 700 °C à 2000 °C à une vitesse de montée de 1 degré C/min à 25 degrés C/min sous atmosphère inerte et en maintenant la température pendant 2 à 8 heures ;
- c) la carbonisation a un rendement en carbone d'au moins 40 pour-cent ; ou
- 50 d) le système de polymères phénoliques est une solution de polymères phénoliques ou des polymères phénoliques fondus.

55 6. Procédé selon une quelconque revendication précédente, dans lequel le système de polymères phénoliques comprend

- a) des polymères choisis dans le groupe constitué de novolaque, de résol et de mélanges de celles-ci, ou
- b) une solution comprenant un solvant choisi dans le groupe constitué d'éthanol, d'isopropanol, d'acétone,

d'acétate d'éthyle, de dichlorométhane, d'hexafluoropropanol, et de mélanges de ceux-ci.

7. Procédé selon la revendication 1, dans lequel le système de polymères phénoliques est une solution de 40 à 60 pour-cent en poids d'un polymère phénolique dans un solvant choisi dans le groupe constitué d'éthanol, d'isopropanol, d'acétone, d'acétate d'éthyle, de dichlorométhane, d'hexafluoropropanol, et de mélanges de ceux-ci.

8. Procédé selon une quelconque revendication précédente, dans lequel le système de polymères phénoliques est une solution comprenant un mélange de (i) une solution de 40 à 60 pour-cent en poids de résol dans un solvant choisi dans le groupe constitué d'éthanol, d'isopropanol, d'acétone, d'acétate d'éthyle, de dichlorométhane, d'hexafluoropropanol, et de mélanges de ceux-ci et (ii) une solution de 40 à 60 pour-cent en poids de novolaque dans un solvant choisi dans le groupe constitué d'éthanol, d'isopropanol, d'acétone, d'acétate d'éthyle, de dichlorométhane, d'hexafluoropropanol, et de mélanges de ceux-ci.

9. Procédé selon la revendication 8, dans lequel le système de polymères phénoliques est une solution comprenant de 30 à 70 pour-cent en poids d'une solution de résol et de 70 à 30 pour-cent en poids d'une solution de novolaque.

10. Procédé selon une quelconque revendication précédente, comprenant en outre l'ajout d'un additif au système de polymères phénoliques avant le filage électrostatique ou la pulvérisation du système.

11. Procédé selon la revendication 10, dans lequel l'additif est

20 a) choisi dans le groupe constitué de métaux dispersés, d'oxydes métalliques, de sels métalliques, de tensioactifs, d'agents de durcissement, d'agents de réticulation, d'agents stabilisants, d'agents améliorant la porosité, de solvants non volatils et incompatibles, et de mélanges de ceux-ci, ou

25 b) choisi dans le groupe constitué de nanofibres de cuivre, d'hexaméthylène tétramine, de PtCl_2 , et de mélanges de ceux-ci.

12. Procédé selon une quelconque revendication précédente, comprenant en outre l'étape d'ajout d'un mélange de polymères au système de polymères phénoliques avant le filage électrostatique ou la pulvérisation du système.

30 13. Procédé selon la revendication 12, dans lequel le mélange de polymères est choisi dans le groupe constitué d'acide polyacrylique, d'acétate de cellulose, d'acétate de polyvinyle, de polyéthylèneimine, de poly(acétate de vinyle-co-éthylène), d'acide polylactique, et de mélanges de ceux-ci.

35 14. Billes ou film phénoliques produits par le procédé selon une quelconque revendication précédente.

15. Procédé selon l'une quelconque des revendications 1 à 13, pour fabriquer des billes phénoliques, dans lequel les billes sont pulvérisées électrostatiquement sur un substrat pour créer un film.

40 16. Procédé selon l'une quelconque des revendications 1 à 13, dans lequel les matières phénoliques sont des fibres phénoliques, et dans lequel les fibres phénoliques carbonisées ont un diamètre d'environ 10 microns à 50 nanomètres.

45 17. Matière fibreuse comprenant un réseau non-tissé de fibres phénoliques carbonisées fabriqué par un procédé selon la revendication 16.

18. Matière fibreuse selon la revendication 17, dans laquelle

50 a) les fibres phénoliques carbonisées comprennent plus de 70 % de micropores ou plus de 90 % de micropores ;

b) les fibres phénoliques carbonisées ont une aire de surface BET de 400 m^2/g à 800 m^2/g ;

c) les fibres phénoliques carbonisées ont un volume de micropores de 0,2 cm^3/g à 0,4 cm^3/g ; ou

d) la matière fibreuse comprend en outre un additif et/ou un mélange de polymères choisis dans le groupe constitué d'acide polyacrylique, d'acétate de cellulose, d'acétate de polyvinyle, de polyéthylèneimine, de poly(éthylène-co-vinylacétate), d'acide polylactique, et de mélanges de ceux-ci.

55 19. Matière fibreuse selon la revendication 17 ou 18, dans laquelle

a) le réseau non-tissé de fibres phénoliques carbonisées se présente sous la forme d'un tapis de fibres non-

tissées ou

b) le réseau non-tissé comprend en outre des billes phénoliques.

20. Fibre ou bille phénolique activée produite par un procédé selon l'une quelconque des revendications 1 à 13, où,

5 a) lors de l'activation de la fibre ou de la bille à une température comprise entre environ 800 °C et environ 1250 °C, la fibre activée a une aire de surface BET d'au moins environ 800 m²/g et a au moins environ 60 % de micropores ayant une largeur de pore inférieure à environ 7 Å ou
10 b) lors de l'activation de la fibre ou de la bille à une température comprise entre environ 800 °C et environ 1250 °C, la bille activée a une aire de surface BET d'au moins environ 1400 m²/g et a au moins environ 40 % de micropores ayant une largeur de pore inférieure à environ 7 Å.

21. Composant d'un article à fumer comprenant un filtre comprenant des fibres carbonisées électro-filées et/ou billes carbonisées électro-pulvérisées fabriquées par un procédé selon l'une quelconque des revendications 1 à 13.

15 22. Procédé pour fabriquer le composant selon la revendication 21, comprenant l'incorporation de fibres carbonisées électro-filées et/ou de billes carbonisées électro-pulvérisées contenues dans une cavité et/ou dans un composant d'un filtre de cigarette.

20 23. Article à fumer incluant un composant comprenant des fibres carbonisées électro-filées et/ou un filtre comprenant des billes carbonisées électro-pulvérisées fabriquées par un procédé selon l'une quelconque des revendications 1 à 13.

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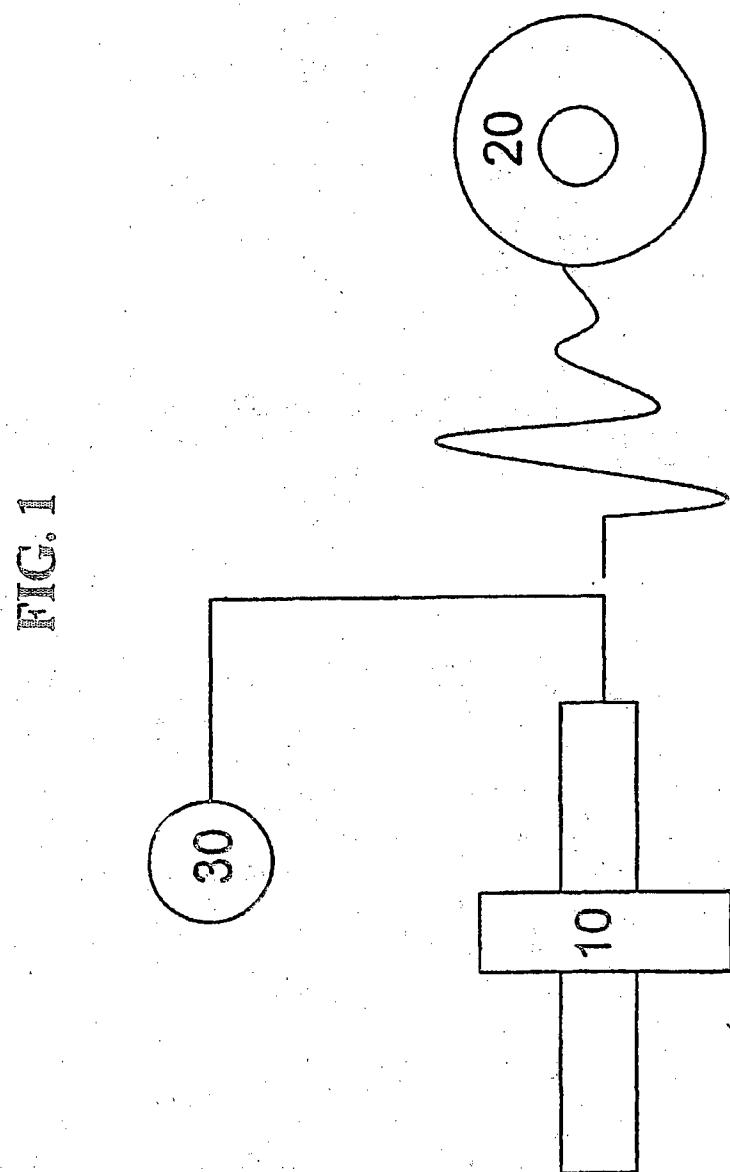
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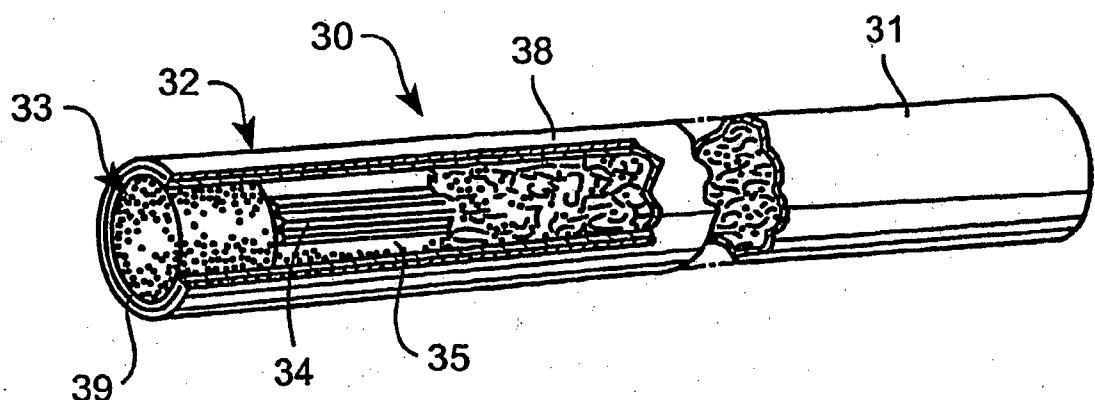


FIG. 2A

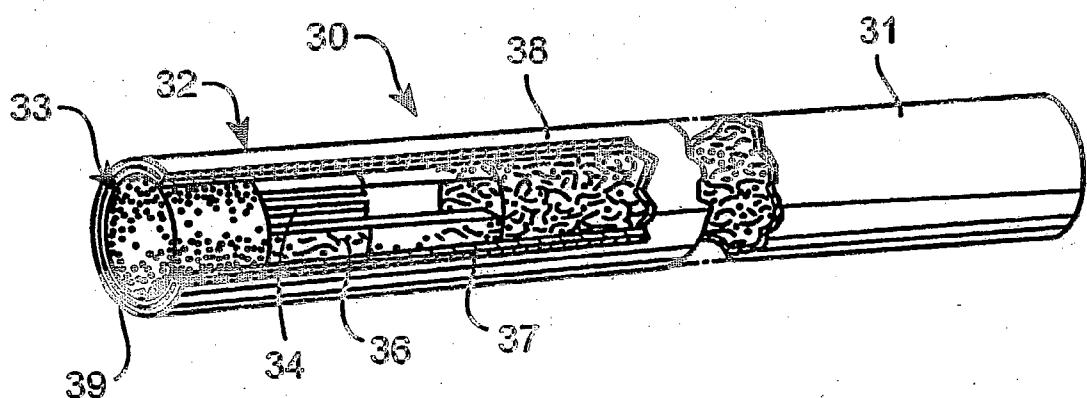


FIG. 2B

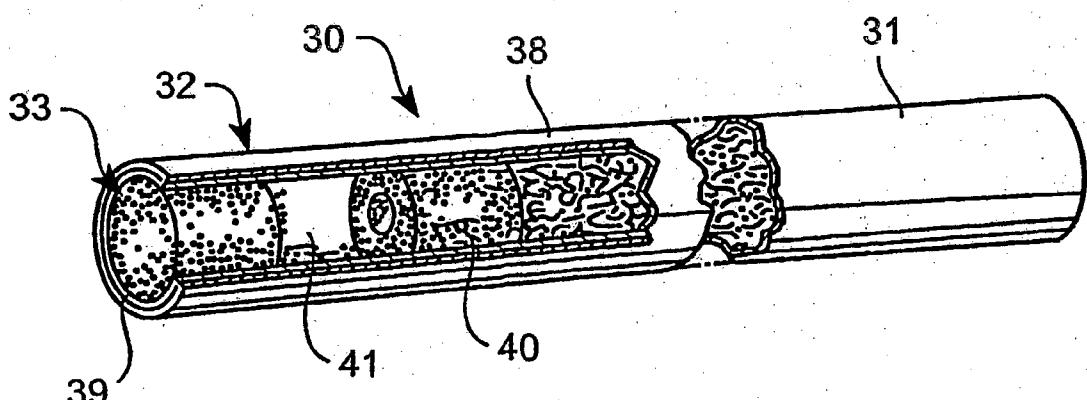


FIG. 2C

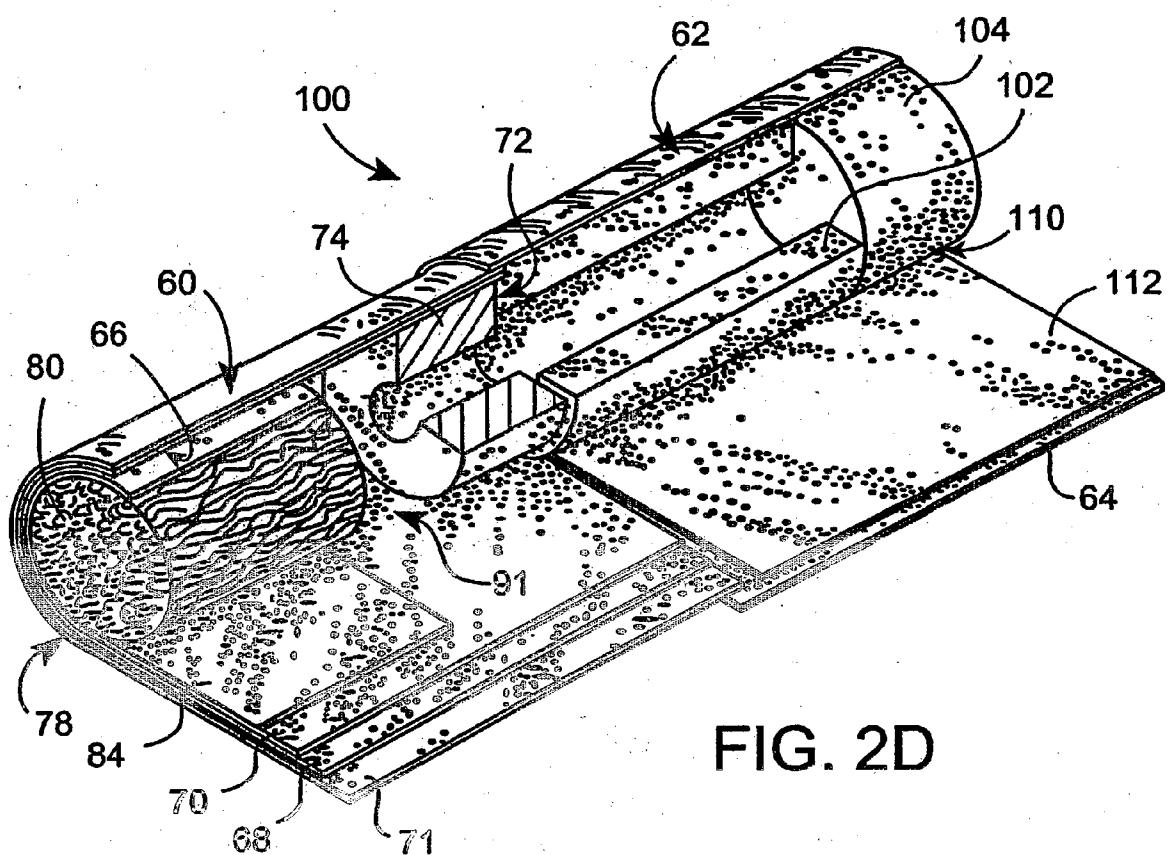


Fig 3A illustrates a SEM of electrospun polymer solution of a 1:1 ratio of 50 wt% novolak with 6.5% hexamethylenetetramine in ethanol and 40 wt% resole in ethanol (Example 1) spun at conditions of 15 kilovolts (± 2 kV), 10 ml/hr (± 4 ml/hr) and deposition distance of 17 cm (± 2.5 cm).

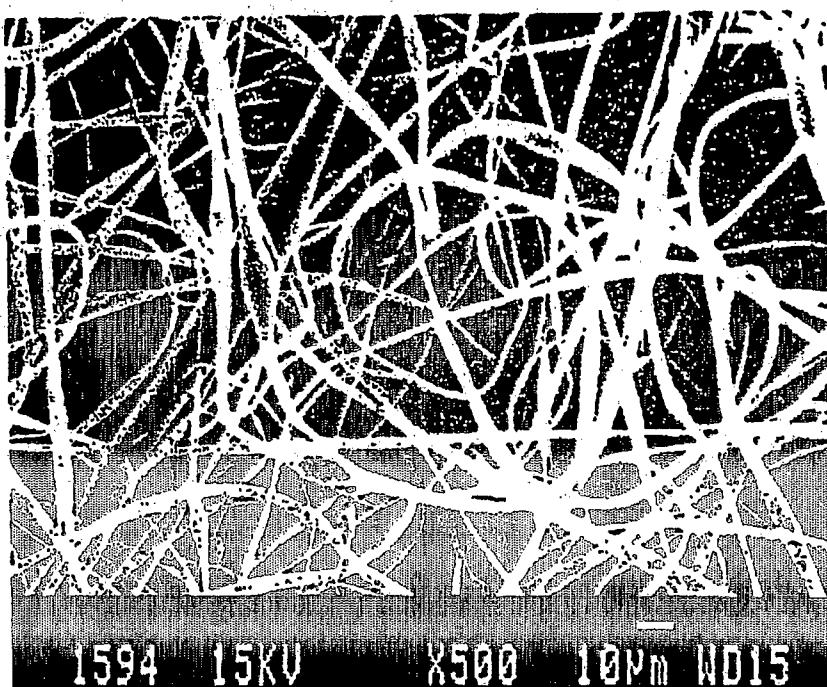


FIG. 3B illustrates a SEM of cured (cross-linked) electrospun fibers (Example 1), from a polymer solution as described above in **FIG. 3A**. Curing conditions were a ramp rate of 0.1°C/min to 160°C, where the sample remained at the final temperature for 6 hours.

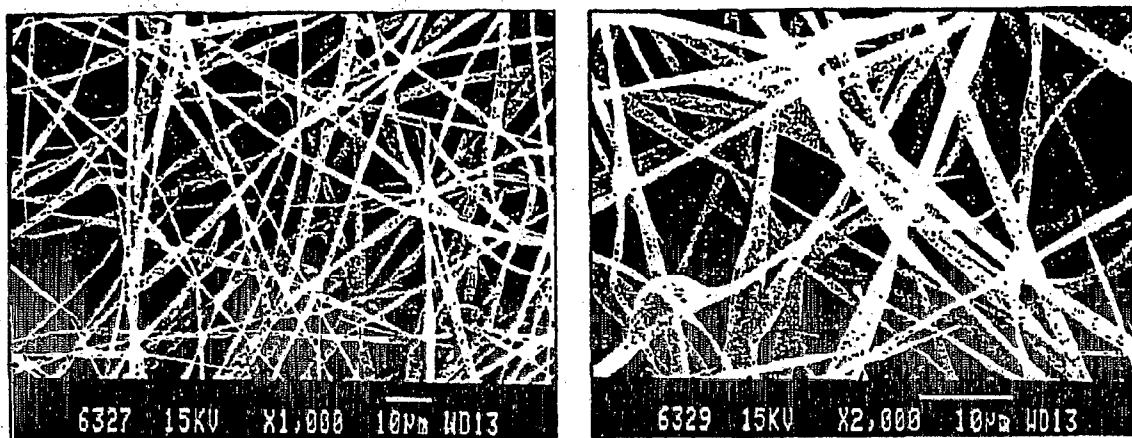


FIG. 3C illustrates a SEM of carbonized fibers (Example 1) from a polymer solution as described above in **FIG. 3A**. Conditions of carbonization were a ramp rate of 10°C/min to 800°C and remained at final temperature for 2 hours.

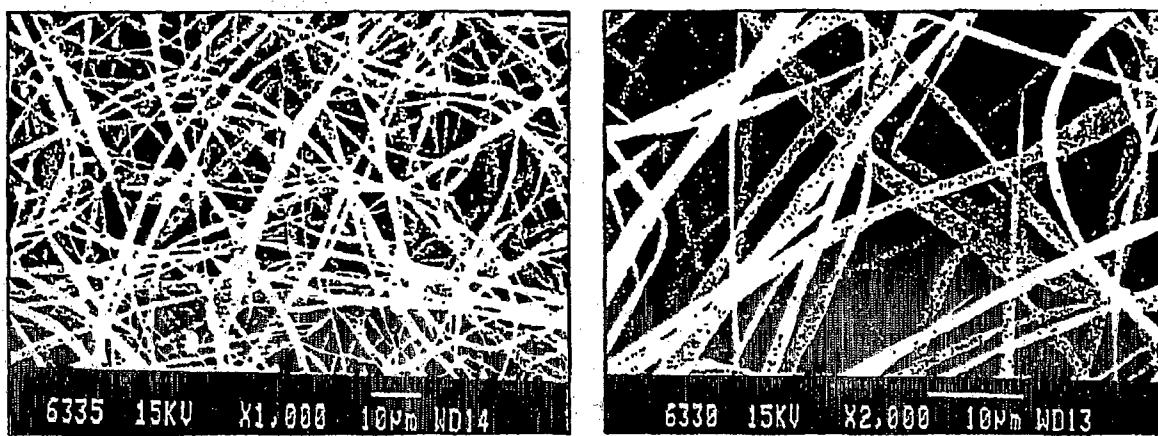


FIG. 4 illustrates an adsorption isotherm of the carbonized fibers (Example 1) from a polymer solution as described above in **FIG. 3A**. (a) electrospun fibers carbonized at 800°C compared to (b) the electrospun and cured fibers (pre-carbonized)

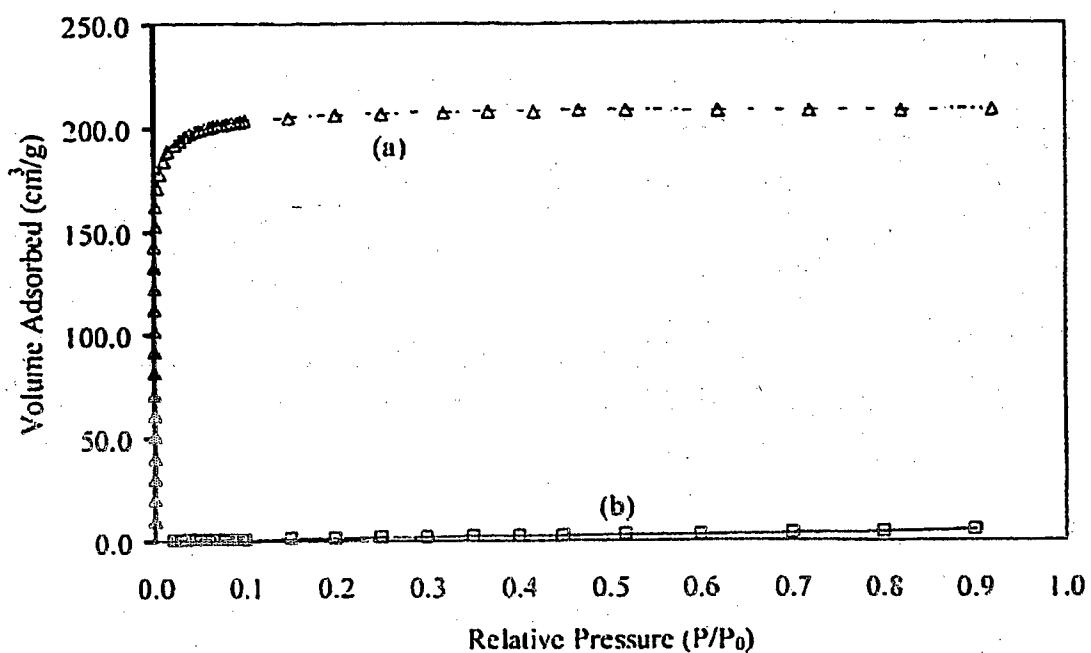


FIG. 5

Table I

#	Electrospun and Processed Fibers	BET Surface Area (m ² /g)		DFT Pore Volumes	
				Micropore Volume (cm ³ /g)	Total Volume (cm ³ /g)
1	Electrospun Fibers	< 5		ND	ND
2	Cured Electrospun Fibers	< 5		ND	ND
3	Carbonized Electrospun Fibers	575 ± 25		0.235 ± 0.005	0.235 ± 0.005

Table II

#	Non-Electrospun and Processed Polymer Solution	BET Surface Area (m ² /g)		DFT Pore Volumes	
				Micropore Volume (cm ³ /g)	Total Volume (cm ³ /g)
4	Non-electrospun (Phenolic resin 1:1 ratio of novotak and resole in ethanol)	< 5		ND	ND
5	Cured non-electrospun phenolic resin blend	< 5		ND	ND
6	Carbonized non-electrospun phenolic resin blend	< 5		ND	ND

FIG. 6 illustrates the pore volume distribution from carbonized electrospun phenolic fibers (Example 1).

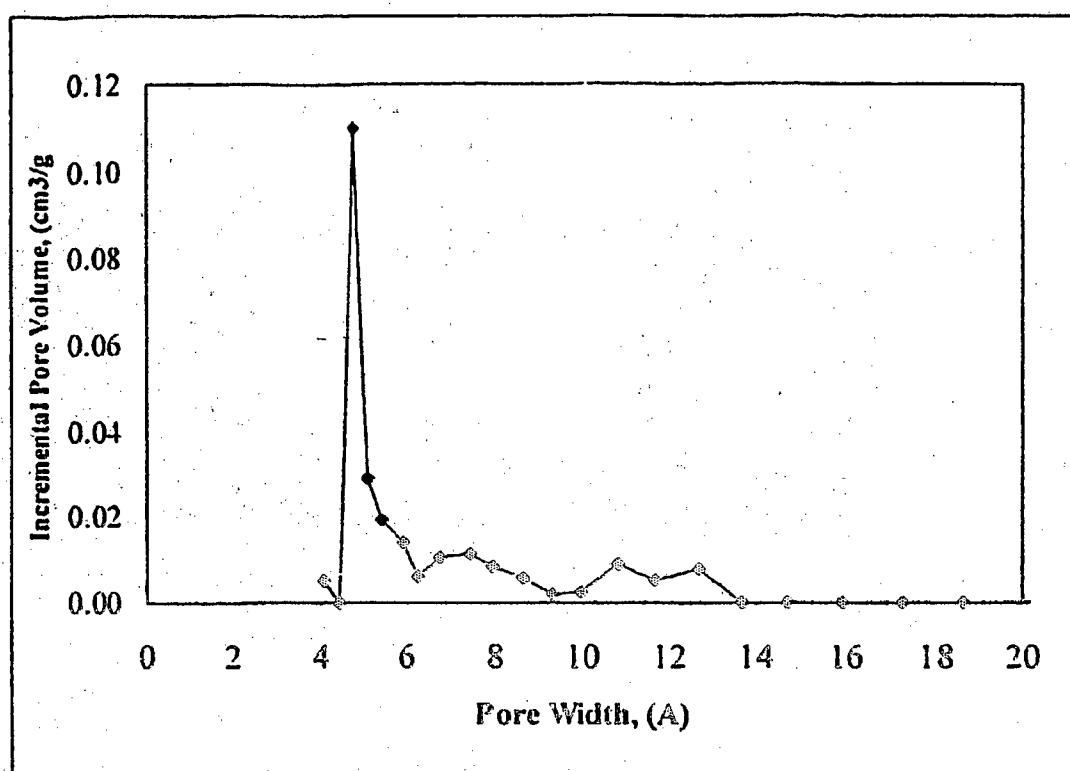


FIG. 7 depicts HRTEM images of carbonized electrospun phenolic resin fibers at (a) 1000°C, (b and c) 1600°C showing partial alignment; (d) graphite at 1600°C; and (e and f) 1800°C.

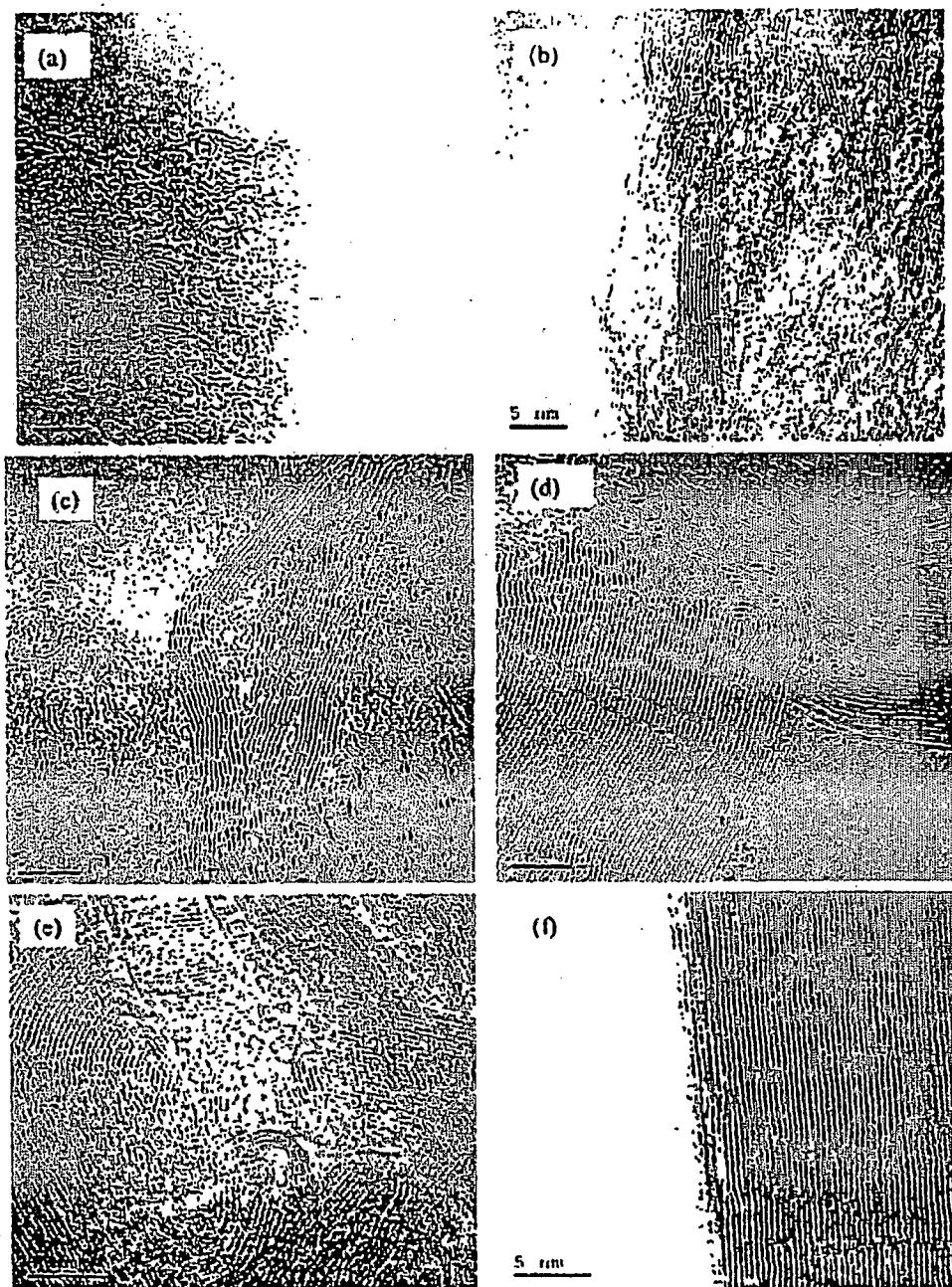


FIG. 8A depicts XRD for carbonized electrospun phenolic resin fibers at (a) 1000°C, (b) 1200°C, (c) 1400°C, (d) 1600°C, (e) 1800°C, and (f) 2000°C.

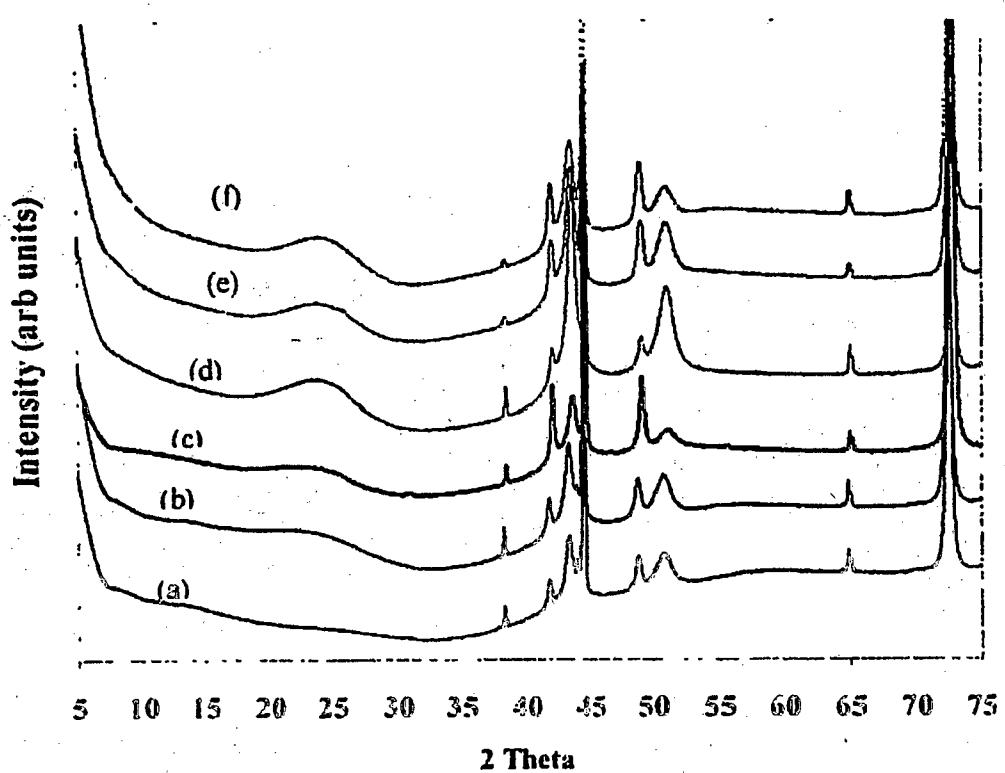


FIG. 8B depicts XRD for the sample holder.

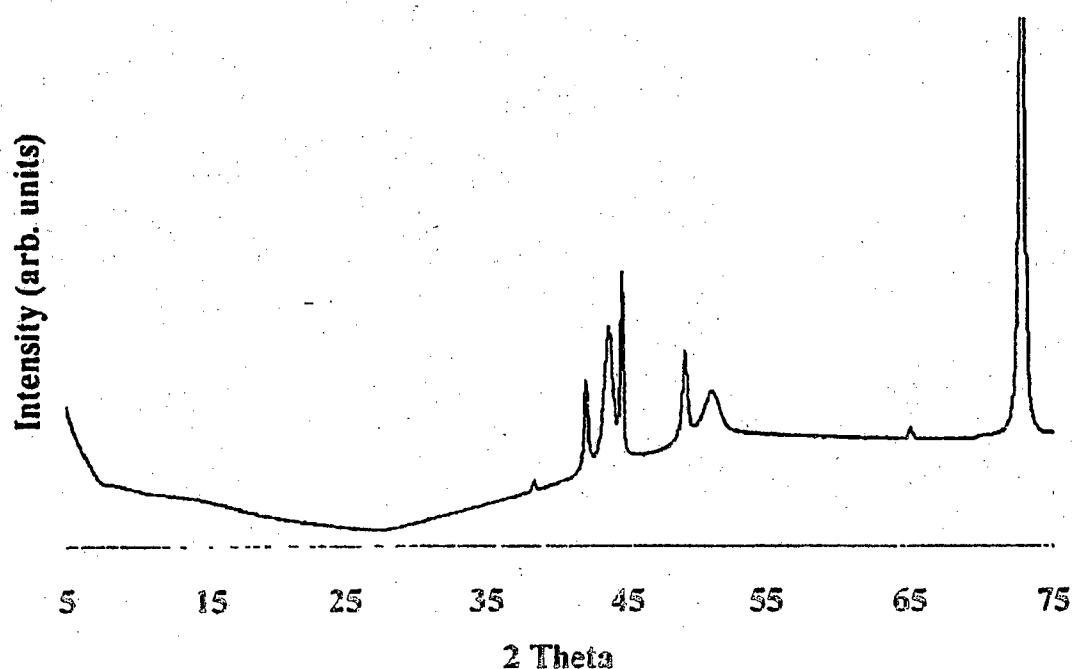


FIG. 9 illustrates an SEM of phenolic beads produced by electrospraying (Example 5).

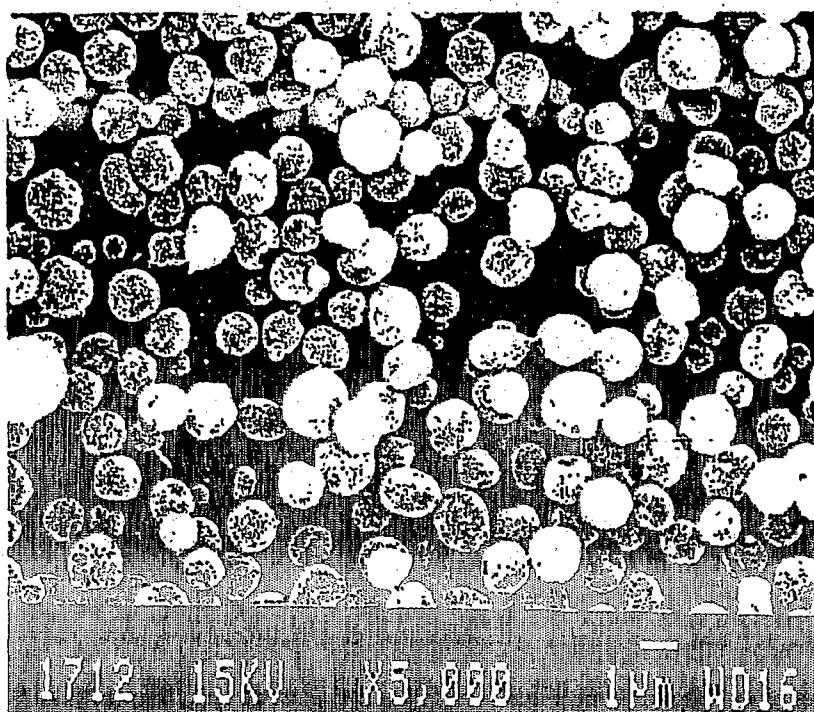


FIG. 10A illustrates phenolic resin fibers (1:1 blend of novolak and resole, 50 wt% concentration of polymer in ethanol) carbonized at temperatures of (a) 1000°C, (b) 1400°C, and (c) 1800°C.

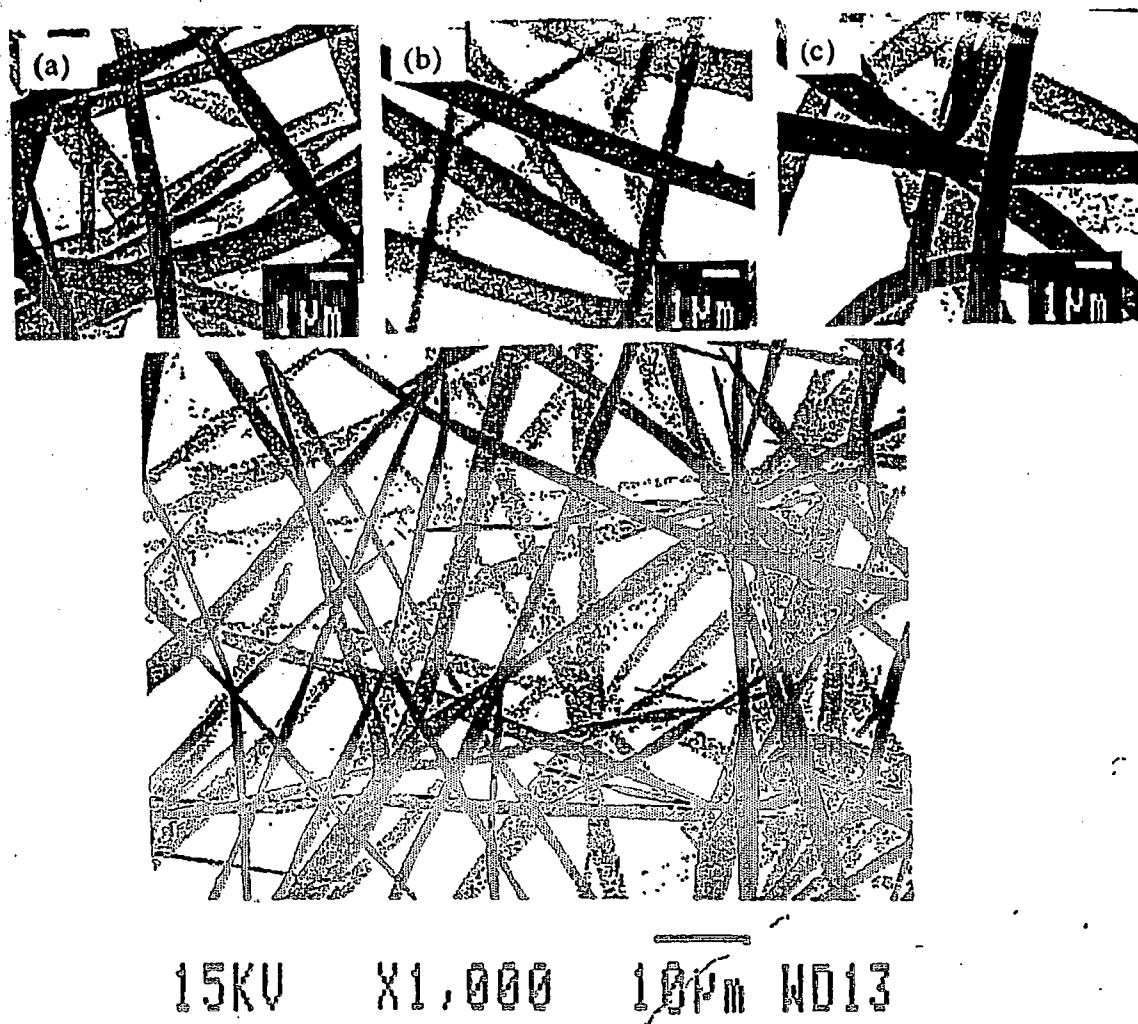
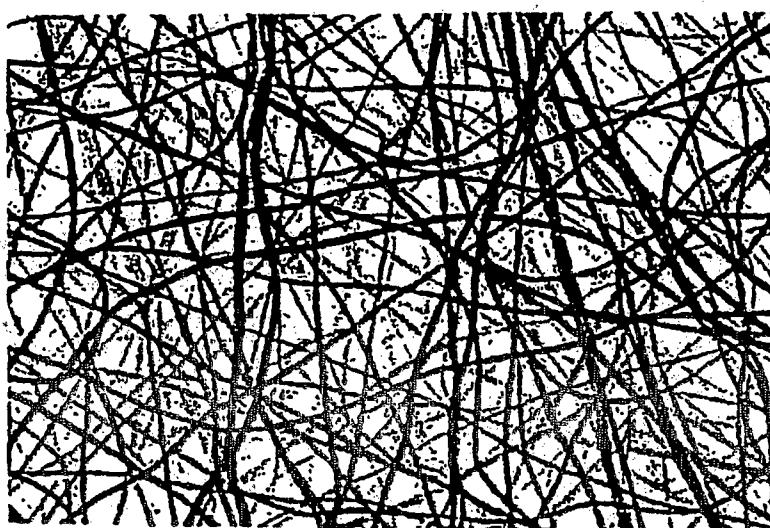


FIG. 10B illustrates PAN carbonized electrospun fibers (10wt% PAN in DMF).



15KV X2,000 10nm WD15

FIG. 11 illustrates adsorption isotherms for carbonized electrospun PAN (10wt% in DMF), Argon at 87.29K at carbonization temperatures of (a) 800°C, (b) 1000°C, (c) 1200°C, (d) 1400°C, and (e) 1600°C.

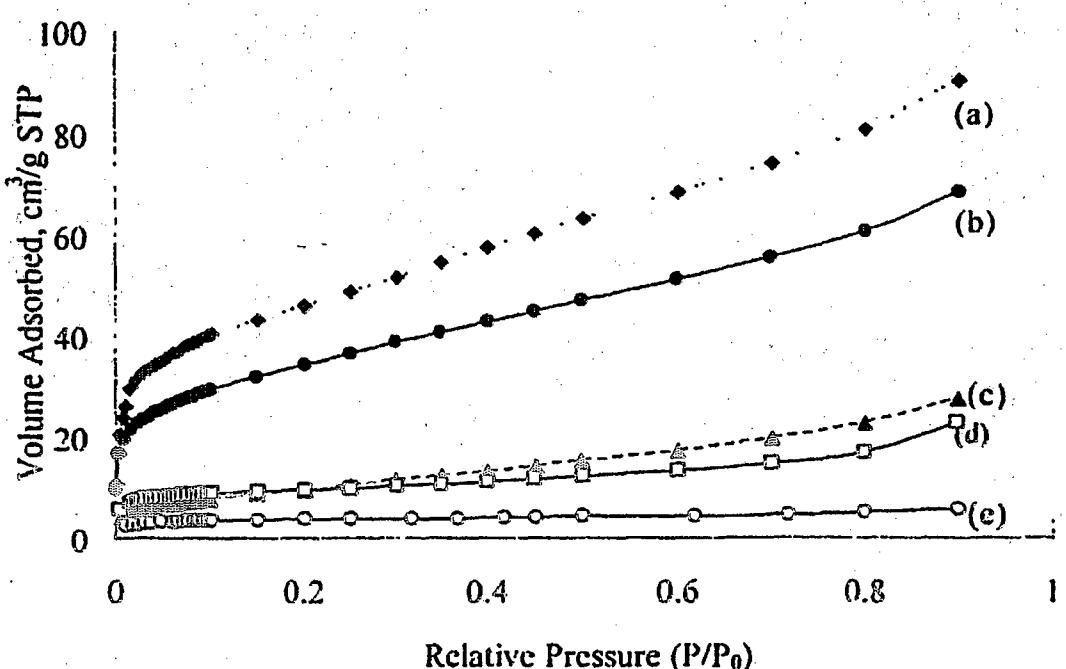


FIG. 12 SEM of electrospun (a) novolak with an average MW~29,000 g/mol, 50 wt% polymer in ethanol) and (b) resolc with an average MW~9700 g/mol (40 wt% polymer in ethanol)

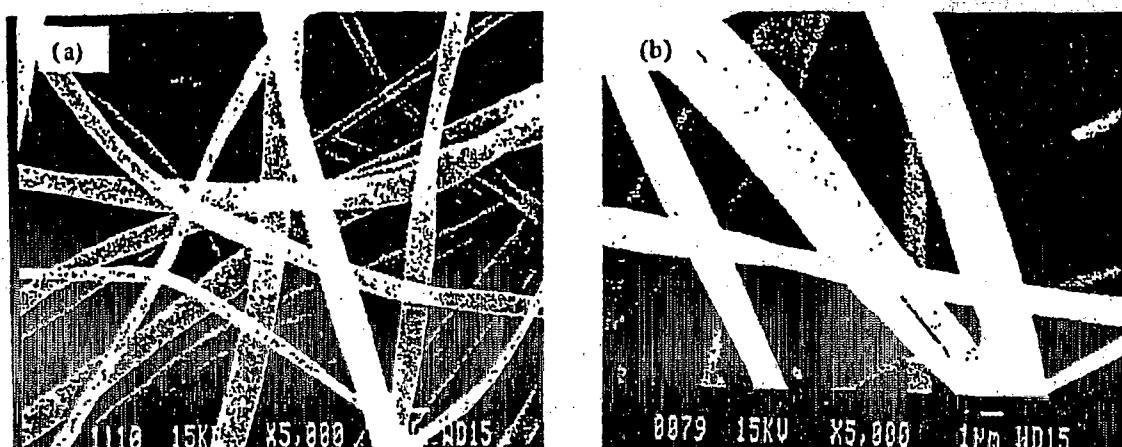


Figure 13 depicts argon adsorption isotherms at 87.29K for carbonized electrospun phenolic resin fibers at (a) 600°C, (b) 800°C, (c) 1000°C, (d) 1200°C, (e) 1400°C, (f) 1500°C, (g) 1600°C, (h) 1800°C, and (i) 2000°C.

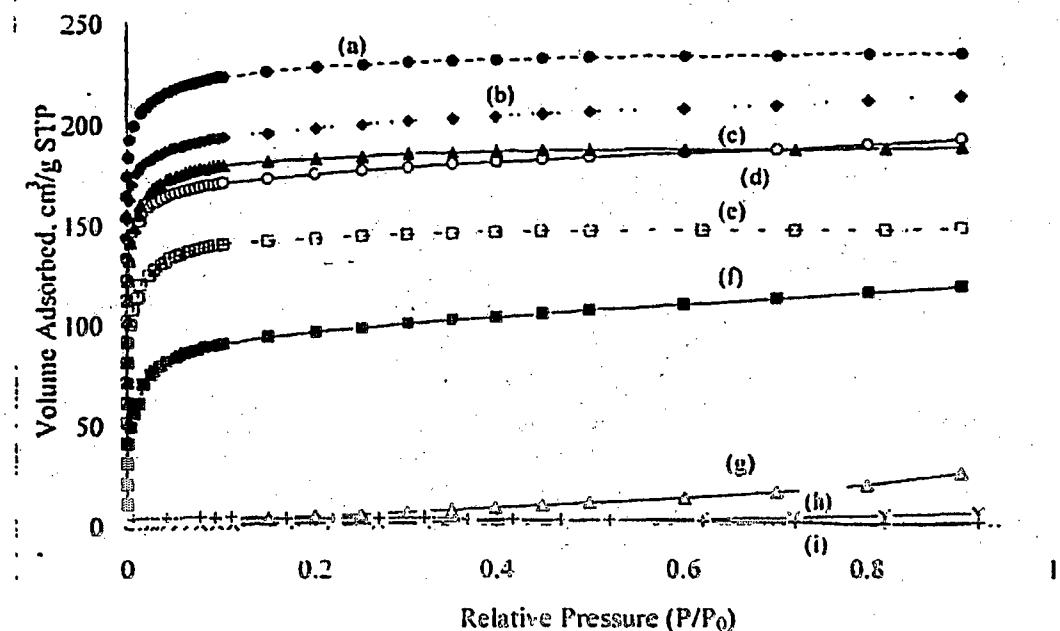
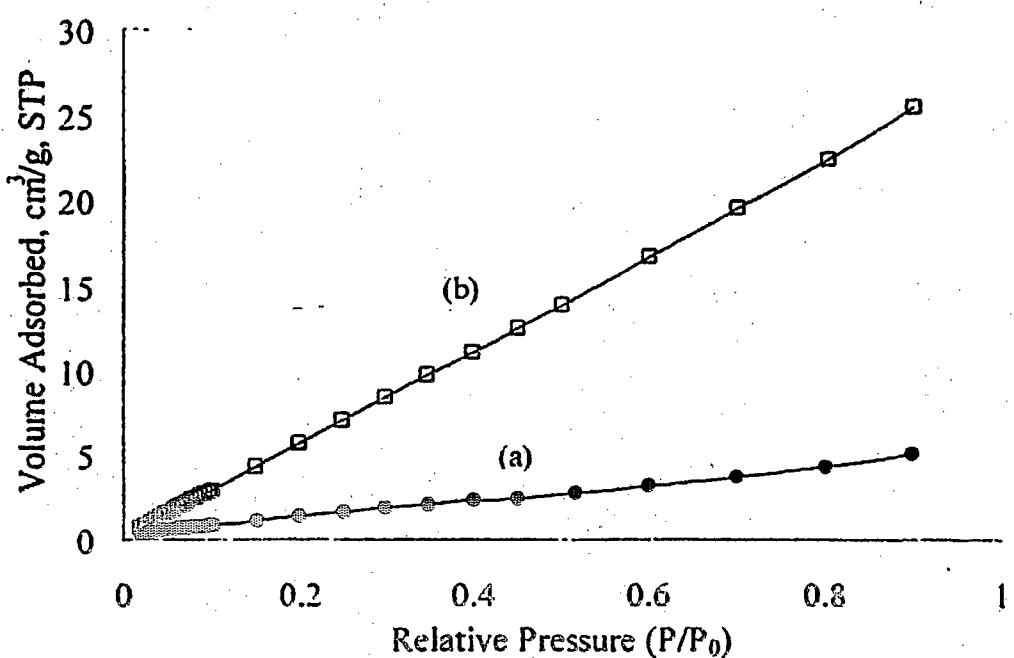


FIG. 14 depicts adsorption isotherms of argon at 87.29 K for (a) electrospun phenolic resin fibers and (b) cured electrospun phenolic resin fibers.



FIGs. 15A and 15B depicts BET specific surface area for carbon electrospun fibers as function of thermal treatment.

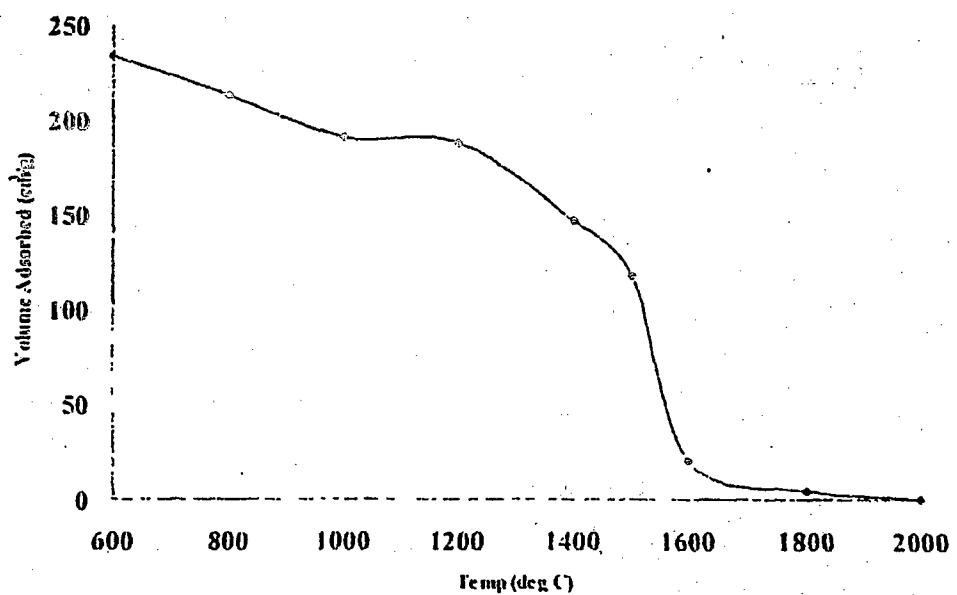
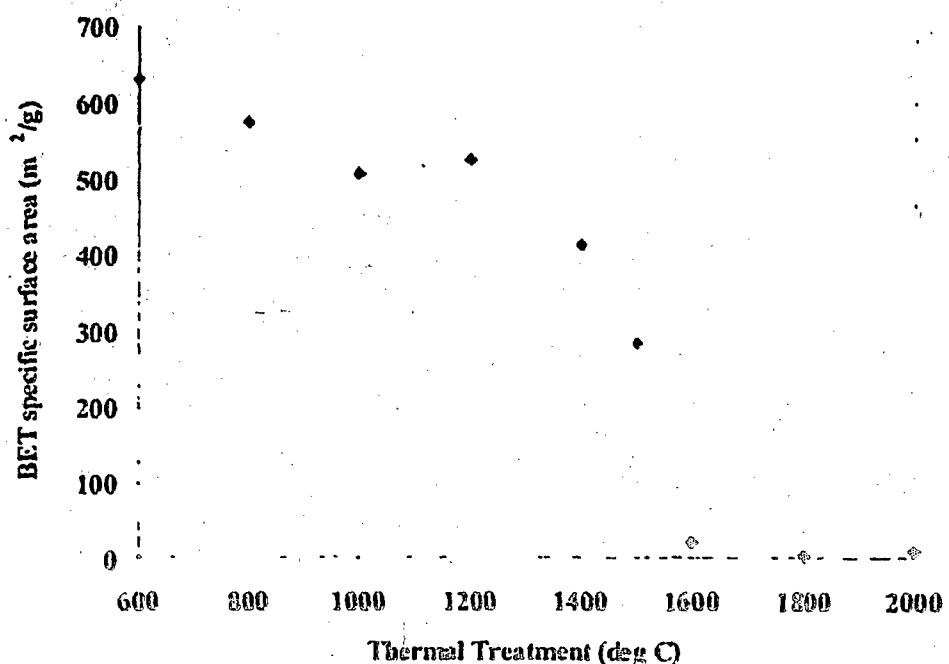


FIG. 16 depicts the pore size distribution using DFT for carbonized electrospun phenolic resin fibers. Curve (a) represents 800°C, curve (b) represents 1000°C, curve (c) represents 1200°C.

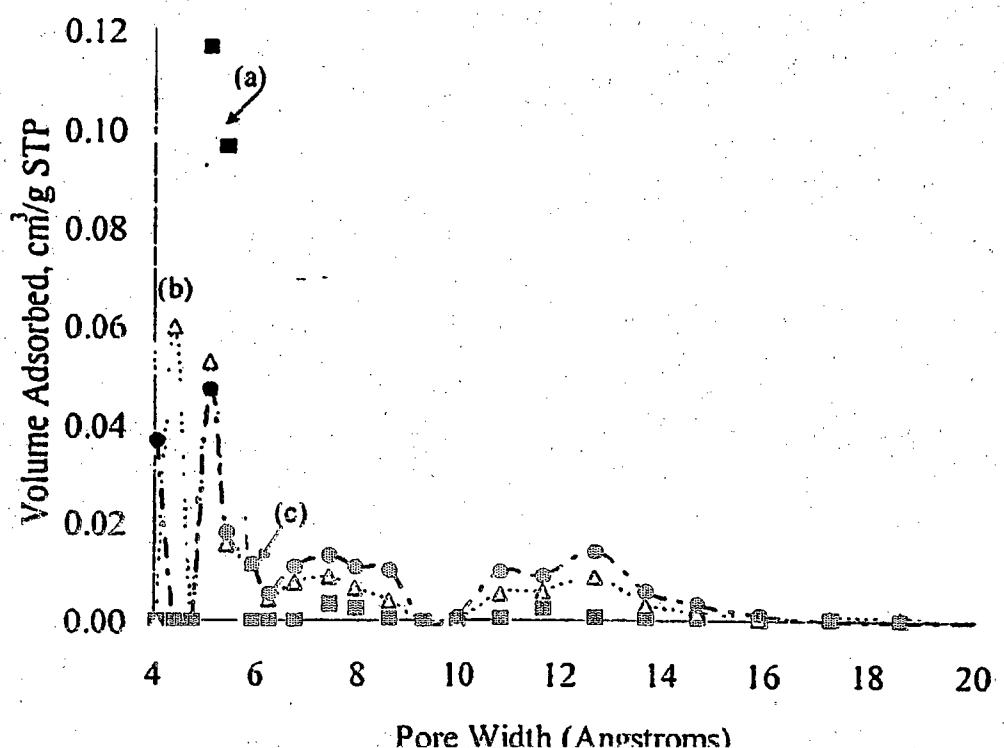


FIG. 17A High Resolution TEM of non-electrospun phenolic resin carbonized at 1800 °C and FIG. 17B Fast Fourier Transform of 17A showing ribbon-like, non-crystalline graphite structure

FIG. 17A

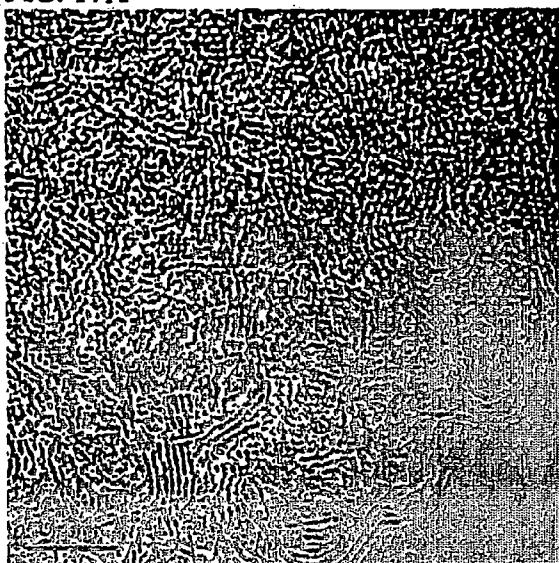
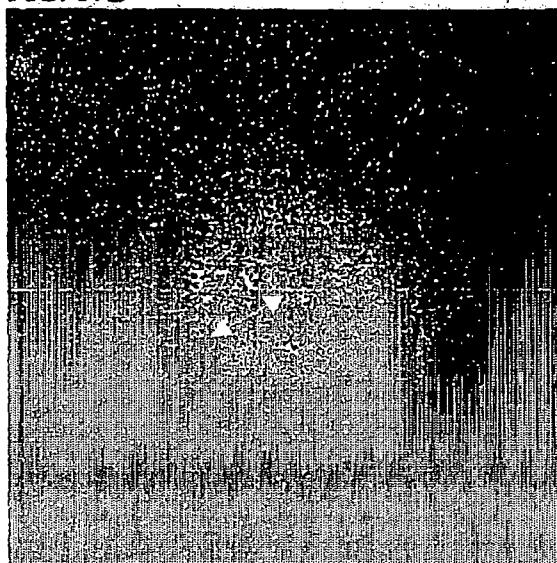


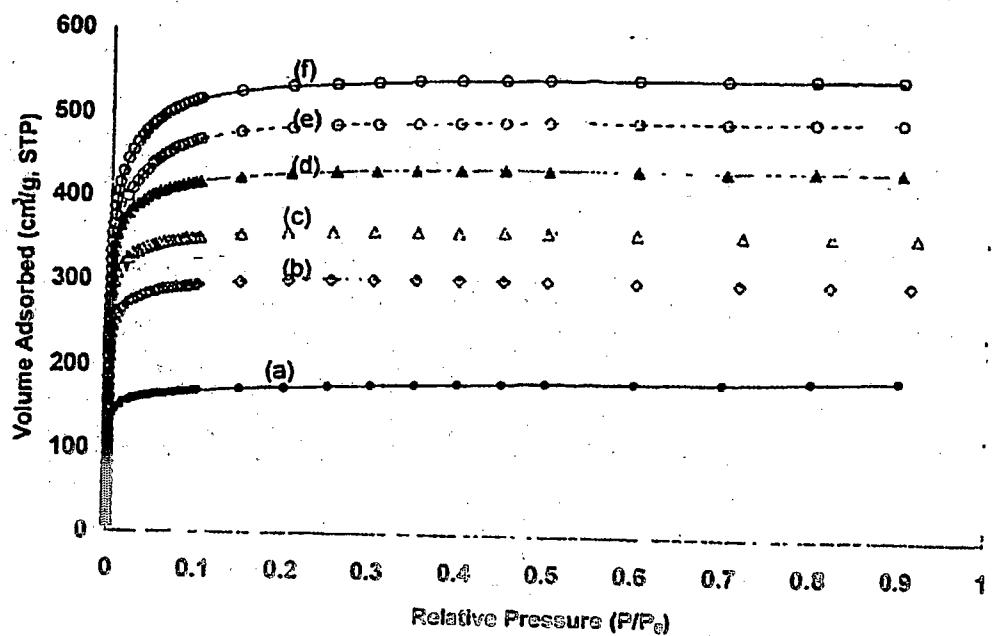
FIG. 17B



FIGs. 18a and 18b depicts a TEM of electrospun material produced when iron oxide nanoparticles were added to PAN fibers and carbonized at 1200°C.

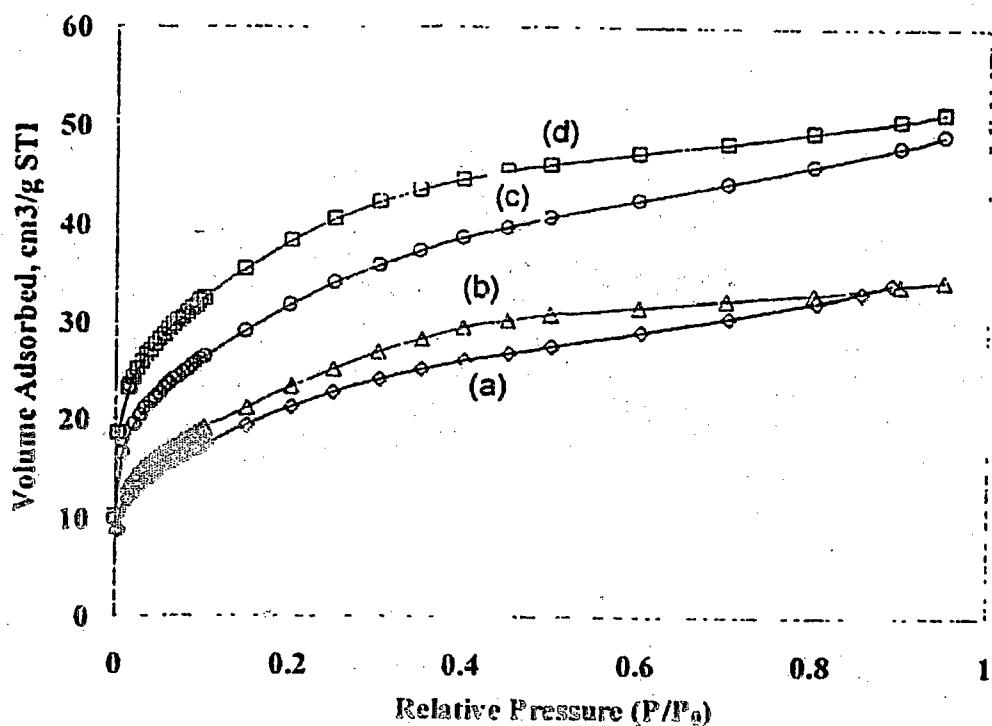


FIG. 19 Adsorption Isotherms (Argon @87.29K) for green and activated phenolic resin carbonized electrospun fibers



- (a) 0% burn-off, BET SA = $508\text{ m}^2/\text{g}$.
- (b) 15% burn-off, BET SA = $872\text{ m}^2/\text{g}$.
- (c) 26% burn-off, BET SA = $1033\text{ m}^2/\text{g}$.
- (d) 40% burn-off, BET SA = $1239\text{ m}^2/\text{g}$.
- (e) 62% burn-off, BET SA = $1404\text{ m}^2/\text{g}$.
- (f) 72% burn-off, BET SA = $1548\text{ m}^2/\text{g}$.

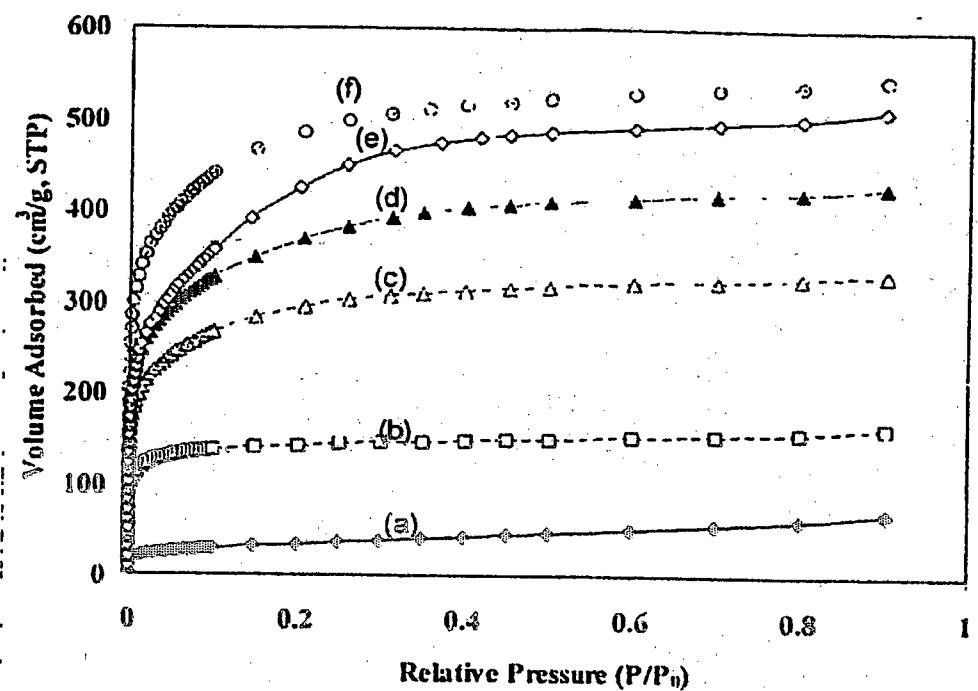
FIG. 20 Adsorption Isotherms (Argon @87.29K) for activated PAN conventionally-processed carbonized electrospun fibers



(non-activated carbon fibers showed no measurable adsorption volume of argon)

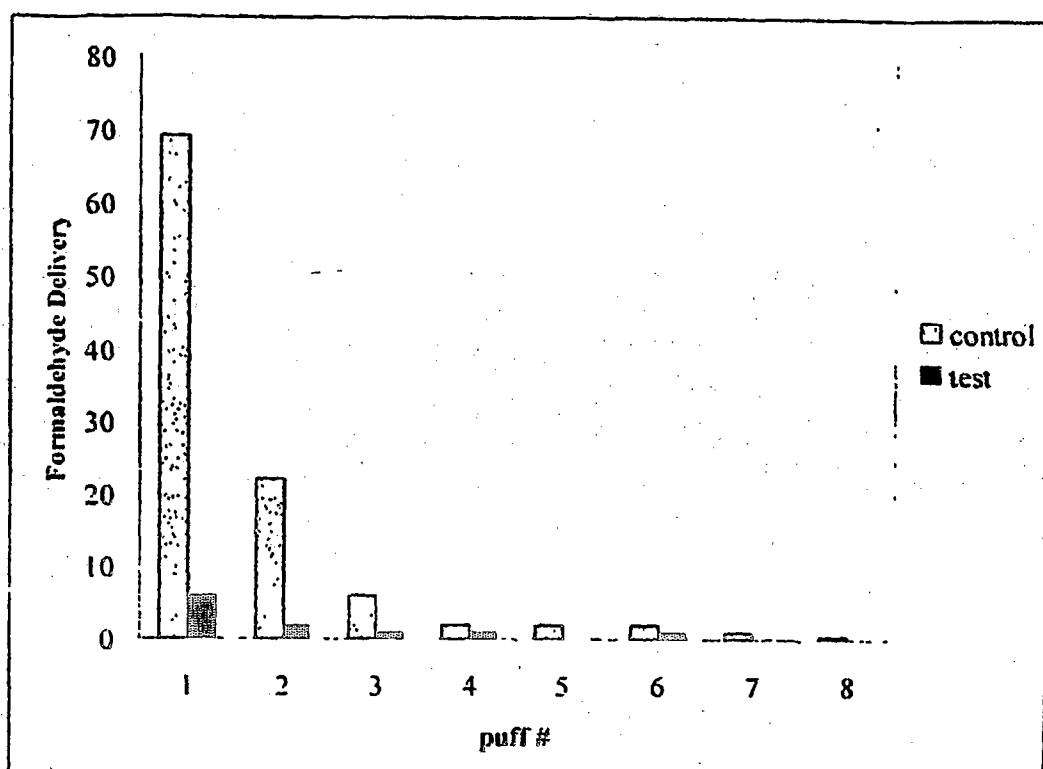
- (a) 7% burn-off, BET SA = $70 \text{ m}^2/\text{g}$.
- (b) 17% burn-off, BET SA = $123 \text{ m}^2/\text{g}$.
- (c) 41% burn-off, BET SA = $77 \text{ m}^2/\text{g}$.
- (d) 53% burn-off, BET SA = $103 \text{ m}^2/\text{g}$.

FIG. 21 Adsorption Isotherms (Argon @87.29K) for green and activated PAN carbonized electrospun fibers



- (a) 0% burn-off, BET SA = 108 m²/g.
- (b) 12% burn-off, BET SA = 416 m²/g.
- (c) 22% burn-off, BET SA = 888 m²/g.
- (d) 31% burn-off, BET SA = 1128 m²/g.
- (e) 47% burn-off, BET SA = 1362 m²/g.
- (f) 60% burn-off, BET SA = 1462 m²/g.

FIG. 22 Control (Reference 2R4F) versus Test (2R4F with 50 mg activated carbonized electrospun fibers) shows reduction of formaldehyde delivery. Formaldehyde deliveries are typically highest in lighting puff. Test cigarette with activated carbonized electrospun phenolic resin fibers shows significant reduction.



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SZABADALMI IGÉNYPONTOK

1. Eljárás fenol tartalmú anyagok előállítására, amelynek során:
 - a) fenol tartalmú polímer rendszert hozunk létre;
 - b) a fenol tartalmú polímer rendszert elektrosztatikus úton fejdeleggük;
 - c) a fenol tartalmú anyagokat kikeményítjük; és
 - d) karbonizált fenol tartalmú anyagok létrehozásához a kikeményített anyagokat karbonizáljuk
2. Az 1. igénypont szerinti eljárás, ahol a karbonizált fenol tartalmú anyagok szálak, szemcsék, nanoszálak, mikroszálak, filmek vagy ezek kombinációi.
3. Az 1. vagy a 2. igénypont szerinti eljárás fenol tartalmú szálak vagy szemcsék előállítására, amelynek során a fenol tartalmú szálakat vagy szemcséket kikeményítjük, ahol:
 - a) a kikeményítést a fenol tartalmú szálakat vagy szemcséket 0,1°C/perc és 5°C/perc közötti hőmérsékletfelfutási ütemmel 20°C és 180°C közötti hőmérsékletre hevítve és 2-8 órán át a tekintett hőmérsékleten tartva hajljuk végre;
 - b) a karbonizálást a kikeményített szálakat vagy szemcséket inert atmoszférában 1°C/perc és 25 °C/perc közötti hőmérsékletfelfutási ütemmel 700°C és 2000°C közötti hőmérsékletre hevítve és 2-8 órán át a tekintett hőmérsékleten tartva hajljuk végre;
 - c) a karbonizálás szénhozama legalább 40%;
 - d) a fenol tartalmú polímer rendszer fenol tartalmú polímeroidat vagy fenol tartalmú polímer ömledék.
4. Az 1., a 2., vagy a 3. igénypont szerinti eljárás fenol tartalmú szálak vagy szemcsék előállítására, amelynek során:
 - a) fenol tartalmú polímer rendszert hozunk létre;
 - b) a fenol tartalmú polímer rendszert fenol tartalmú szálak létrehozásához elektrosztatikus szálhúzásnak vagy fenol tartalmú szemcsék létrehozásához elektrosztatikus porlasztásnak vetjük alá, a szemcsék átmérője 100 nanométer és 10 mikrométer között van;
 - c) a fenol tartalmú szálakat vagy szemcséket kikeményítjük;
 - d) a karbonizált fenol tartalmú szálak vagy szemcsék előállításához a kikeményített szálakat vagy szemcséket karbonizáljuk; és
 - e) aktivált fenol tartalmú szálak vagy szemcsék előállításához a karbonizált fenol tartalmú szálakat vagy szemcséket aktiváljuk.
5. A 4. igénypont szerinti eljárás, ahol:
 - a) az aktiválást a karbonizált fenol tartalmú szálakat vagy szemcséket oxidáló környezetben 700°C és 1000°C közötti hőmérsékletre hevítve, valamint 20 perc és 6 óra közötti időtartamon át a tekintett hőmérsékleten tartva hajljuk végre;
 - b) a karbonizálást a kikeményített szálakat vagy szemcséket inert atmoszférában 1°C/perc és 25 °C/perc közötti hőmérsékletfelfutási ütemmel 700°C és 2000°C közötti hőmérsékletre hevítve és 2-8 órán át a tekintett hőmérsékleten tartva hajljuk végre;
 - c) a karbonizálás szénhozama legalább 40%, vagy
 - d) a fenol tartalmú polímer rendszer fenol tartalmú polímeroidat vagy fenol tartalmú polímer



Örmiedék.

6. Az előző igénypontok bármelyike szerinti eljárás, ahol a fenol tartalmú polimer rendszer a
 - a) novolak, rezol és ezek keverékei alkotta csoportból választott polimereket, vagy az
 - b) etanol, izopropanol, aceton, etil-acetát, díklór-metán, hexafluoro-propanol és ezek keverékei alkotta csoportból választott oldószeret tartalmazó oldatot tartalmaz.
7. Az 1. igénypont szerinti eljárás, ahol a fenol tartalmú polimer rendszert 40-60 tömeg% fenol tartalmú polimérnek az etanol, izopropanol, aceton, etil-acetát, díklór-metán, hexafluoro-propanol és ezek keverékei alkotta csoportból választott oldószerbeli oldatot képezi.
8. Az előző igénypontok bármelyike szerinti eljárás, ahol a fenol tartalmú polimer rendszert (i) 40-60 tömeg% rezolinak az etanol, izopropanol, aceton, etil-acetát, díklór-metán, hexafluoro-propanol és ezek keverékei alkotta csoportból választott oldószerbeli oldatának, valamint (ii) 40-60 tömeg% novolaknak az etanol, izopropanol, aceton, etil-acetát, díklór-metán, hexafluoro-propanol és ezek keverékei alkotta csoportból választott oldószerbeli oldatának a keverékből álló oldat képezi.
9. A 8. igénypont szerinti eljárás, ahol a fenol tartalmú polimer rendszert 30-70 tömeg% rezol oldatot és 70-30 tömeg% novolak oldatból álló oldat képezi.
10. Az előző igénypontok bármelyike szerinti eljárás, amelynek során a fenol tartalmú polimer rendszer elektrosztatikus szálhúzását vagy porlasztását megelőzően a rendszerhez adalékanyagot adunk hozzá.
11. A 10. igénypont szerinti eljárás, ahol az adalékanyagot a
 - a) diszpergált fémek, fémoxidok, fémosok, felületaktív anyagok, kikeményítő anyagok, térhálósító szerek, stabilizálószerek, porozitásfokozók, nemillékony és nemkompatibilis oldószerek, valamint ezek keverékei alkotta csoportból, vagy a
 - b) réz nanoszállak, hexametilen-tetramin, PtCl_2 , és ezek keverékei alkotta csoportból választjuk ki.
12. Az előző igénypontok bármelyike szerinti eljárás, amelynek során a fenol tartalmú polimer rendszer elektrosztatikus szálhúzását vagy porlasztását megelőzően a rendszerhez polimerelegyet adunk hozzá.
13. A 12. igénypont szerinti eljárás, ahol a polimerelegyet a poliakrilsav, cellulóz-acetát, poli(vinil-acetát), polietilénimin, poli(etilén-vinil-acetát), politejsav és ezek keverékei alkotta csoportból választjuk ki.
14. Fenol tartalmú szemcsék vagy film, melyek az előző igénypontok bármelyike szerinti eljárással vannak előállítva.
15. Az 1-13. igénypontok bármelyike szerinti eljárás fenol tartalmú szemcsék előállítására, ahol film előállításához a szemcséket elektrosztatikusan hordozóra porlasztjuk.
16. Az 1-13. igénypontok bármelyike szerinti eljárás, ahol a fenol tartalmú anyagokat fenol tartalmú szálak képezik, továbbá a karbonizált fenol tartalmú szálak átmérője mintegy 10 mikron és 50 nanométer között van.
17. Szálasanyag, amely a 16. igénypont szerinti eljárással előállított karbonizált fenol tartalmú szálak nemszöft térhálóját tartalmazza.

18. A 17. igénypontról szerinti szálasanyag, ahol

- a karbonizált fenol tartalmú szálak 70%-nál nagyobb mennyiségű mikropórust vagy 90%-nál nagyobb mennyiségű mikropórust tartalmaznak;
- a karbonizált fenol tartalmú szálak BET felületi területe $400 \text{ m}^2/\text{g}$ és $800 \text{ m}^2/\text{g}$ között van;
- a karbonizált fenol tartalmú szálak mikropórus-térfogata $0,2 \text{ cm}^3/\text{g}$ és $0,4 \text{ cm}^3/\text{g}$ között van;
- vagy
- a szálasanyag adalékanyagot és/vagy a poliakrilsav, cellulóz-acetát, poli(vinil-acetát), polietilenimin, poli(etylén-vinil-acetát), politejsav és ezek keverékei alkotta csoportból választott polimereleget tartalmaz.

19. A 17. vagy a 18. igénypontról szerinti szálasanyag, ahol

- a karbonizált fenol tartalmú szálak nemszöjt térháját nemszöjt szálak lapja képezi, vagy
- a nemszöjt térhájot fenol tartalmú szemcséket is tartalmaz.

20. Aktivált fenol tartalmú azál vagy szemcse, ami az 1-13. igénypontok bármelyike szerinti eljárásával van előállítva, ahol

- a szál vagy szemcse mintegy 800°C és mintegy 1250°C közötti höméréséleten történő aktiválásakor az aktivált szál BET felületi területe legalább mintegy $800 \text{ m}^2/\text{g}$ továbbá mikropórusai legalább mintegy 60%-ának a pörusszélessége mintegy 7 \AA -nél kisebb, vagy
- a szál vagy szemcse mintegy 800°C és mintegy 1250°C közötti höméréséleten történő aktiválásakor az aktivált szemcse BET felületi területe legalább mintegy $1400 \text{ m}^2/\text{g}$, továbbá mikropórusai legalább mintegy 40%-ának a pörusszélessége mintegy 7 \AA -nél kisebb.

21. Dohányzási cikk összetevő, amelynek az 1-13. igénypontok bármelyike szerinti eljárásával előállított elektromosan fonott karbonizált szálakat és/vagy elektromosan porlasztott karbonizált szemcséket tartalmazó szűrője van.

22. Eljárás a 21. igénypontról szerinti összetevő előállítására, amelynek során üregben és/vagy cigarettafüzében az összetevőbe elektromosan fonott karbonizált szálakat és/vagy elektromosan porlasztott karbonizált szemcséket foglalunk bele.

23. Dohányzási cikk, amelynek egy az 1-13. igénypontok bármelyike szerinti eljárásával előállított elektromosan fonott karbonizált szálakat és/vagy elektromosan porlasztott karbonizált szemcséket magában foglaló szűrőt tartalmazó összetevője van.