



(51) International Patent Classification:

D21C 1/00 (2006.01) *D21C 7/00* (2006.01)
D21C 3/00 (2006.01)

(21) International Application Number:

PCT/EP2017/081930

(22) International Filing Date:

07 December 2017 (07.12.2017)

(25) Filing Language:

English

(26) Publication Language:

English

(30) Priority Data:

16202942.5 08 December 2016 (08.12.2016) EP

(71) Applicant: VALMET AB [SE/SE]; 851 94 Sundsvall (SE).

(72) Inventor: LAMBERT, Francois; Ljungbacken 8, 85460 Sundsvall (SE).

(74) Agent: MAIWALD PATENTANWALTS- UND RECHTSANWALTSGESELLSCHAFT MBH; Angela Zumstein, Elisenstr. 3 / Elisenhof, 80335 Munich (DE).

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AO, AT, AU, AZ, BA, BB, BG, BH, BN, BR, BW, BY, BZ, CA, CH, CL, CN, CO, CR, CU, CZ, DE, DJ, DK, DM, DO, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT, HN, HR, HU, ID, IL, IN, IR, IS, JO, JP, KE, KG, KH, KN, KP, KR, KW, KZ, LA, LC, LK, LR, LS, LU, LY, MA, MD, ME, MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM, PA, PE, PG, PH, PL, PT, QA, RO, RS, RU, RW, SA, SC, SD, SE, SG, SK, SL, SM, ST, SV, SY, TH, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW.

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LR, LS, MW, MZ, NA, RW, SD, SL, ST, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, RU, TJ,

(54) Title: METHOD AND SYSTEM FOR TREATING BIOMASS

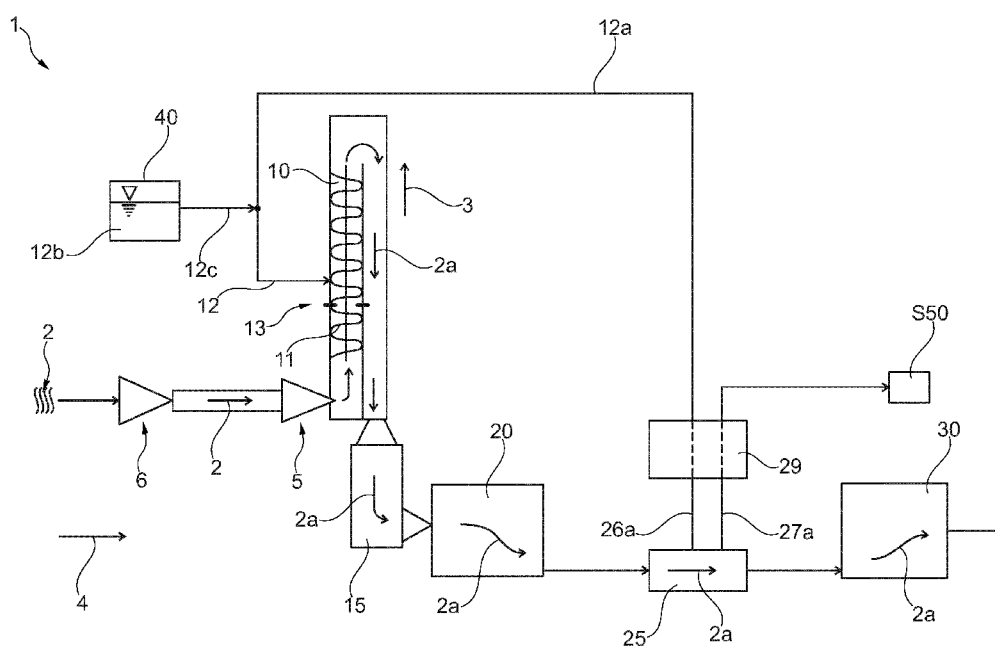


Fig. 1

(57) Abstract: The invention relates to a method for treating biomass (2). In a step (S10), biomass (2) and an impregnation liquid are fed into a first reactor unit (10) such that the biomass (2) is impregnated with the impregnation liquid while the biomass (2) is transferred through the first reactor unit (10) by a conveyor means (11). In another step (S20), the impregnated biomass (2a) is transferred from the first reactor unit (10) to a separation unit (25), wherein at least a part of the impregnation liquid is separated from the impregnated biomass (2a) within the separation unit. In a step (S30), the separated impregnation liquid is discharged from the separation unit (25), such that a first part (26a) of the impregnation liquid is recirculated back to the first reactor unit (10). The invention further relates to a system for treating biomass (2).

TM), European (AL, AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HR, HU, IE, IS, IT, LT, LU, LV, MC, MK, MT, NL, NO, PL, PT, RO, RS, SE, SI, SK, SM, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, KM, ML, MR, NE, SN, TD, TG).

Published:

— *with international search report (Art. 21(3))*

Method and system for treating biomass

Field of the invention

5

The invention generally relates to impregnation systems. In particular, the invention relates to a method for treating biomass as well as to a system for treating biomass.

Background of the invention

10

Treating biomass becomes relevant in many different fields. For example, an impregnation of biomass is a treatment process in the paper and pulp industry in which the biomass is impregnated with an impregnation liquid such that a reaction between the biomass and the impregnation liquid takes place. After the reaction

15 between the biomass and the impregnation liquid, excess or residual impregnation liquid which was not used during the impregnation may be discharged such that a transfer of residual impregnation liquid to subsequent steps after the impregnation step is prevented. It is further required to provide a homogeneous impregnation during the impregnation step. Therefore, it is important to adjust the amount of
20 impregnation liquid required for a certain amount of biomass.

Summary of the invention

It is an object of the present invention to provide an improved impregnation process
25 for biomass.

This object is achieved by the subject-matter of the independent claims. Further exemplary embodiments are evident from the dependent claims and the following description.

30

According to an aspect of the present invention, a method for treating biomass is given. In a step of the method, the biomass and an impregnation liquid are fed into a first reactor unit such that the biomass is impregnated with the impregnation liquid

- 2 -

while the biomass is transferred through the first reactor unit by a conveyor means. In another step, the impregnated biomass is transferred from the first reactor unit to a separation unit wherein at least a part of the impregnated liquid is separated from the impregnated biomass within the separation unit. In another step, the separated
5 impregnation liquid is discharged from the separation unit such that only a first part of the separated impregnation liquid is recirculated back to the first reactor unit.

Using such a method for treating biomass advantageously provides a better utilization of the impregnation liquid since impregnation liquid which was already
10 used for the impregnation of the biomass can be recirculated back to the first reactor in which the impregnation of the biomass takes place. In other words, the impregnation liquid can be reused or recycled. This leads to a better utilization of the filtrate and better impregnation of raw material, e. g. biomass, with the impregnation liquid resulting in a more homogeneous impregnation or hydrolysis of the biomass.

15 The conveyor means with which the biomass is transferred through the first reactor may be a screw conveyor. For example, the first reactor unit is a longitudinal vessel arranged vertically with respect to an earth's surface. In this manner, it is possible to fill the first reactor unit with impregnation liquid up to a predetermined fill level such
20 that the entire biomass is transferred through the impregnation liquid. This means that the biomass is transferred in an upward direction within the first reactor unit and through the impregnation liquid such that a homogeneous impregnation of the biomass with the impregnation liquid is achieved. After the biomass has been impregnated with the impregnation liquid it is conveyed or transferred to the
25 separation unit such that excess impregnation liquid which was not used during the impregnation of the biomass can be discharged at the separation unit and recirculated back to the first reactor unit. Between the impregnation within the first reactor unit and the separation of the impregnation liquid within the separation unit, further steps such as for example a hydrolysis in a second reactor unit may be provided. In
30 particular, a hydrolysis of the biomass may be carried out in the second reactor unit

- 3 -

in the presence of impregnation liquid. The material may then be diluted at a downstream part of the second reactor unit, e.g. between the second reactor unit and the separation unit. The dilution may be carried out with impregnation liquid or a part of the impregnation liquid which is not recirculated back to the first reactor unit
5 but also with a part of the impregnation liquid which is recirculated back to the first reactor unit.

However, the separated impregnation liquid is divided into different parts such that only one part, e. g. the first part of the impregnation liquid is recirculated back to the
10 first reactor unit. This means that the first part of the impregnation liquid may be recirculated back to the first reactor unit whereas a second part of the impregnation liquid which was separated from the impregnated biomass in the separation unit is transferred to another step of the process, for example to a treatment step downstream of the separation unit. This aspect will be explained in more detail
15 hereinafter.

The separation unit may comprise a plurality of different separation devices such that a stepwise separation of the impregnation liquid from the impregnated biomass is provided. Preferably, the separation of the impregnation liquid from the impregnated
20 biomass is carried out in two different steps. The separation unit may comprise a screw conveyor by means of which the impregnated biomass is transferred through the separation unit during the separation of the impregnation liquid from the impregnated biomass.

25 Further conveyor means, like for instance screw conveyors, may be integrated into the system in order to enable the conveyance or transfer of the impregnated biomass from the first reactor unit to the separation unit.

According to an embodiment of the invention, the separation of the impregnation
30 liquid within the separation unit comprises a compression stage in which the

- 4 -

impregnation liquid is released from the impregnated biomass by compressing the impregnated biomass preferably with a screw press.

- In this manner, it is possible to effectively extract the impregnation liquid from the impregnated biomass, in particular the impregnation liquid which was not used during the foregoing steps like the impregnation itself or a hydrolysis step. The unused impregnation liquid may be defined as the part of the impregnation liquid which did not react with the biomass in the impregnation step or hydrolysis step. The extracted impregnation liquid may contain organic acid such as acetic acid created during the hydrolysis of the raw material, e.g. the biomass. The concentration of organic acid may vary depending on the fraction of the extracted liquid. The impregnation liquid may also contain sugar as monomer or oligomer as well as solid material such fiber.
- 5
- 10
- 15
- 20
- The screw press which may have the shape of a plug screw provides the required pressure within the material such that the impregnation liquid can be released from the pores or cavities within the material, e. g. within the impregnated biomass. It is possible to set a predetermined pressure within the separation unit such that a compression of impregnated biomass is enabled in order to release the impregnation liquid from the impregnated biomass. However, the present invention is not limited to a screw press in order to provide the required pressure for releasing the impregnation liquid from the impregnated biomass.

- According to another embodiment of the invention, the first part of the impregnation liquid released from the impregnated biomass in the compression stage is recirculated back to the first reactor unit whereas another part, e. g. the second part of the impregnation liquid released from the impregnated biomass in the compression stage is transferred to a treatment step downstream the separation unit.
- 25

- 5 -

The part of the impregnation liquid released from the impregnated biomass in the compression stage which is recirculated back to the first reactor unit may also be referred to as the first part of the impregnation liquid released from the impregnated biomass. In particular, the part of the impregnation liquid that contains much acid,
5 e.g. more than a predetermined content of acid, and/or less sugar, e.g. less than a predetermined content of sugar, is recirculated back to the first reactor unit.

The other part of the impregnation liquid released from the impregnated biomass in the compression stage which is transferred to the treatment step downstream the
10 separation unit may also be referred to as the second part of the impregnation liquid released from the impregnated biomass.

It is also possible that the other part, e. g. the second part of impregnation liquid released from the impregnated biomass is not transferred to a treatment step
15 downstream the separation unit, but is instead used for other purposes or simply disposed. Recirculating the first part of impregnation liquid back to the first reactor unit may be carried out simultaneously or alternatively to transferring the second part of the impregnation liquid to the treatment step downstream the separation unit. The ratio between the first part of impregnation liquid and the second part of
20 impregnation liquid may be between 0.5 and 5 if gravity draining is used in a first stage, e.g. a drainage stage, and compression is used in a second stage, e.g. a compression stage. The different stages will be described in the description of the figures in more detail. The ratio between the first part of impregnation liquid and the second part of impregnation liquid may be between 0.5 and 3 if the biomass is
25 diluted at the downstream part of the second reactor unit. If no dilution occurs downstream of the second reactor unit, the ratio between the first part of impregnation liquid and the second part of impregnation liquid may be between 1.5 and 3.

It is possible that the ratio between the first part of impregnation liquid and the
30 second part of impregnation liquid may be up to about 20 to 25 if a compression

- 6 -

screw is used for the separation. Additionally, the separated impregnation liquid, e.g. the filtrate, may be collected in a different zone apart from the compression screw, in particular when no separate draining stage or draining screw is provided.

- 5 However, the separation unit may comprise two stages in which the impregnation liquid is released from the impregnated biomass. For example, in the first stage, the first part of impregnation liquid is released from the impregnated biomass and in the second stage, the second part of impregnation liquid is released from the impregnated biomass. The stage or location at which the impregnation liquid is released from the
- 10 impregnated biomass may determine the target location to which the different parts of impregnation liquid are supplied.

According to another embodiment of the invention, the separation of the impregnation liquid within the separation unit comprises a drainage stage in which

15 free impregnation liquid is drained from the impregnated biomass preferably by gravity draining.

In this case, the free impregnation liquid may be drained from the impregnated biomass without compression. It should be understood that free impregnation liquid

20 in the sense of the present invention means that this kind of liquid may be released from the impregnated biomass without compression or other activities on the impregnated biomass. In other words, free impregnation liquid may be obtained by gravity effects since this type of impregnation liquid is not chemically bound within the biomass. In particular, the free impregnation liquid is released from the

25 impregnated biomass by the influence of the earth's gravity such that the impregnation liquid simply flows out or is drained off the impregnated biomass. Therefore, the free impregnation liquid may also be referred to as gravity drained impregnation liquid. Afterwards, the drained free impregnation liquid may be received within a drain tray.

- 7 -

The free impregnation liquid which is drained from the impregnated biomass is to be distinguished from the part of the impregnation liquid which is released from the impregnated biomass in the compression stage. In other words, there exist two stages in the separation unit wherein in a first stage, a drainage of free impregnation liquid
5 is provided and in a second stage, a compression of the impregnated biomass is provided such that the impregnation liquid is squeezed out of the impregnated biomass.

According to another embodiment of the invention, the free, e. g. gravity drained
10 impregnation liquid drained from the impregnated biomass in the drainage stage is transferred to a treatment step downstream the separation unit.

Therefore, it is possible that the second part of the impregnation liquid is the free impregnation liquid that is released from the impregnated biomass and transferred to
15 the treatment step downstream the separation unit. Furthermore, it is possible that the first part of the impregnation liquid is the part of the impregnation liquid that is released from the impregnated biomass in the compression stage and which is recirculated back to the first reactor unit. This aspect will be described in more detail in the description of the figures.

20 According to another embodiment of the invention, a fractionation of the separated first part of impregnation liquid is carried out in a fractionation unit until a predetermined purity degree of the recirculated impregnation liquid is reached.

25 According to yet another embodiment of the invention, a fractionation of the separated second part of impregnation liquid is carried out in the fractionation unit, for example simultaneously to the fractionation of the first part of the separated impregnation liquid, until a predetermined purity degree of the second part of the separated impregnation liquid is reached.

30

According to another embodiment of the invention, a filtration of the separated first part of impregnation liquid is carried out in a filtration unit until a predetermined purity degree of the recirculated impregnation liquid is reached.

- 5 According to yet another embodiment of the invention, a filtration of the separated second part of impregnation liquid is carried out in the filtration unit, for example simultaneously to the filtration of the first part of the separated impregnation liquid, until a predetermined purity degree of the second part of the separated impregnation liquid is reached.

10

For example, the filtration may be carried out to separate a solid phase present in the liquid, e.g. fibers, from a dissolved substance. Therefore, a screening equipment for observing the predetermined purity degree of the impregnation liquid and a filter or other separation equipment may be provided for achieving the preferred purity
15 degree of impregnation liquid after separation. The filtered impregnation liquid may be called filtrate or filtered impregnation liquid. However, using the expression recirculated first or second part of impregnation liquid does not exclude that this recirculated impregnation liquid is filtered after separation.

- 20 In some cases, only a combined liquid stream, e. g. a stream of impregnation liquid comprising solid fractions is separated from the impregnated biomass. The liquid stream, e. g. the impregnation liquid separated from the impregnated biomass, can then either be sent directly to the first reactor unit or it can first be filtrated. For example, a separation of sugar from furfural is possible in the filtration unit. A
25 membrane filtration and/or a nano-filtration may be applied in order to filter the separated impregnation liquid after it has been separated from the impregnated biomass in the separation unit. For example, solids and particles can be filtered out of the separated impregnation liquid in this way. It can be important to remove solid material such as fiber from the filtrate as to provide a proper recirculation without a
30 clogging of the liquid lines between the separation unit and the first reactor unit. For

example, filtration is applied before membrane nano-filtration such that coarse solid fractions can be filtered out of the separated impregnation liquid. During the nano-filtration, certain molecules can be separated from the impregnation liquid.

Furthermore, it is advantageous to remove the furfural from the filtrate in order to
5 avoid an undesired enrichment of furfural at certain locations. The filtration may for instance be carried out using a so-called optifilter.

The separation may also be considered as a dewatering or washing of the impregnated biomass. Consequently, the separation stage in which the impregnation
10 liquid is separated from the impregnated biomass may also be called dewatering stage or washing stage.

The separation may be carried out under pressurized conditions. In this case it may also be possible that the impregnation of the biomass in the first reactor unit is also
15 carried out under pressurized conditions. However, it may also be possible that a pressure within the first reactor unit may be adjusted independently of a pressurization of the separation unit. According to the present invention, it is possible to obtain several liquid streams, e. g. impregnation liquid streams which are fed to different steps within the treatment system of the biomass. Each of the liquid streams
20 may be treated differently, for example by applying different filtration methods. The filtration is generally carried out in order to remove solids and dissolved material but also to separate dissolved substances in several fraction.

According to another aspect of the invention, the recirculated first part of
25 impregnation liquid from the separation unit is mixed with impregnation liquid from a reservoir before injecting the mixed impregnation liquid to the first reactor unit.

In particular, the mixing of the recirculated first part of impregnation liquid and the impregnation liquid from the reservoir may be carried out in a pipe between the
30 reservoir and the first reactor unit.

In this manner, it is possible to combine the recirculated impregnation liquid with fresh impregnation liquid from the reservoir. This also provides the possibility to adjust certain chemical characteristics of the impregnation liquid fed into the first reactor unit. For example, the amount of the impregnation liquid fed from the
5 reservoir and/or the amount of impregnation liquid recirculated from the separation unit may be adjusted. However, it is possible to apply a separation of higher gravity particles by sedimentation in a separate tank before or after mixing the recirculated first part of impregnation liquid and the impregnation liquid from the reservoir. The recirculated first part of impregnation liquid may also be fed into the reservoir first in
10 order to mix the fresh impregnation liquid with the recirculated impregnation liquid in the reservoir. In this case the reservoir may be used for the sedimentation of the higher gravity particles in the impregnation liquid. Using a separate tank or the reservoir provides the possibility to control the composition of the impregnation liquid in the system and therefore also the composition of the impregnation liquid to
15 be fed into the first reactor unit.

It is also possible that only water is added or fed into the reservoir and that the impregnation liquid is recirculated in order to recirculate organic acid such as acetic acid that may be formed in a hydrolysis reaction in the second reactor unit.

20

According to another embodiment of the invention, the recirculated first part of impregnation liquid from the separation unit is injected into the first reactor unit such that the recirculated first part of impregnation liquid is reused for impregnating the fed biomass with the first reactor unit.

25

Reusing the impregnation liquid which was separated in the separation unit advantageously reduces the costs since the amount of fresh impregnation liquid provided, for example, by the reservoir can be reduced. Furthermore, organic acid which is generated during the hydrolysis in the second reactor unit may be used as
30 chemicals, in particular as chemicals for the impregnation liquid. In other words, the

- 11 -

separated impregnation liquid which is recirculated back to the first reactor unit is used for the impregnation of the biomass for a second time. The amount of recirculated impregnation liquid and/or the amount of fresh impregnation liquid from the reservoir may be adjusted such that a predetermined fill level within the reactor
5 unit can be adjusted. The chemical characteristics of the impregnation liquid fed into the first reactor unit can be adjusted by controlling the amount of fresh impregnation liquid and the amount of recirculated impregnation liquid.

According to another embodiment of the invention, the impregnated biomass is fed
10 from the first reactor unit into a second reactor unit before transferring the impregnated biomass to the separation unit wherein a hydrolysis of the impregnated biomass takes place within the second reactor unit.

In other words, the impregnation and the hydrolysis may take place in separate
15 reactor units with different environmental conditions. The transfer of the impregnated biomass from the first reactor unit to the hydrolysis stage, e. g. the second reactor unit, may be provided by a conveyor means, for example by a screw conveyor. However, the second reactor unit in which the hydrolysis takes place may be arranged between the first reactor unit in which the biomass is impregnated and
20 the separation unit in which a part of the impregnation liquid is separated from the impregnated biomass in order to be recirculated back to the first reactor unit.

During the impregnation and hydrolysis of the impregnated biomass, a reaction between the biomass and the impregnation liquid may take place. Therein, most part
25 of the impregnation liquid does not react with the biomass during impregnation or hydrolysis and may therefore be separated from the impregnated biomass in the separation unit.

According to another embodiment of the invention, a transfer of the impregnated
30 biomass from the separation unit to a third reactor unit is carried out wherein a steam

- 12 -

impact, in particular a steam explosion on the impregnated biomass takes place within the third reactor unit.

5 A steam explosion is a violent boiling or flashing of water into a steam due to a rapid pressure drop. In particular, a steam explosion leads to a rapid decrease in pressure resulting in a flashing and a destruction of the structure of the material, e.g. the hydrolyzed or impregnated biomass.

10 According to an embodiment of the invention, the impregnation liquid comprises chemicals selected from the group consisting of an acid, a catalyst or mixtures thereof. The impregnation liquid may also be pure water.

15 The chemicals may be added to the impregnation liquid before it is fed into the first reactor unit. Therefore, the chemicals may be fresh chemicals added into the system or reused chemicals from the recirculated impregnation liquid.

For example, the impregnation liquid is an aqueous solution, EtOH or mixtures thereof. The chemicals are selected from the group consisting of a catalyst, an acid, a mineral acid preferably H_2SO_4 , organic acid preferably acetic acid or mixtures thereof. H_2SO_4 is the preferred chemical. Liquid containing acetic acid, for example from the recirculated stream, is also a preferred chemical.

25 In the context of the present invention, the term “impregnation liquid” is to be understood as a liquid reactant comprising chemicals, wherein the liquid reactant may be an aqueous solution, EtOH or a similar mixture and the chemicals may comprise a catalyst, an acid like H_2SO_4 or acetic acid or similar mixtures. The liquid reactant may comprise water or another solvent. Alternatively, a mixture of water and solvent is possible. The liquid reactant may be derived from a recirculation of filtrates, liquids or pressates which are obtained at different positions in the process, especially in the separation unit. However, the liquid reactant may also be a

condensate or partial condensate of a steam explosion flash vapor, a byproduct from evaporation, a distillation of fermented slurry, or a filtrate from a further dewatering stage.

- 5 According to another embodiment of the invention, the impregnation liquid is fed into the first reactor unit up to a predetermined fill level such that at least a part of the biomass which is fed into the first reactor unit is in permanent contact with the impregnation liquid for a predetermined time span.
- 10 Preferably, the entire biomass is in contact with the impregnation liquid for the predetermined time span. In this manner, it is possible that the whole biomass is transferred or conveyed through the impregnation liquid such that a homogeneous impregnation of the biomass with the impregnation liquid takes place. For example, the first reactor unit is vertically arranged with respect to the earth's surface wherein
- 15 the impregnation liquid is filled into the first reactor unit up to the predetermined fill level. The biomass is fed into the first reactor unit at a bottom part of the first reactor unit and the impregnated biomass is discharged from the first reactor unit at a top part of the first reactor unit. Therefore, the biomass is conveyed in an upward direction within the first reactor unit such that the biomass passes or is conveyed
- 20 through the impregnation liquid before the impregnated biomass can be discharged from the first reactor unit at the top part.

- According to another embodiment of the invention, the conveyor means of the first reactor unit is a screw conveyor arranged with a vertical component, in particular
- 25 vertically within the first reactor unit such that the biomass is conveyed in an upward direction during the impregnation.

The conveyor means may comprise at least two screw conveyors. In a preferred embodiment of the invention, exclusively two screw conveyors are vertically

- 14 -

arranged within the first reactor unit. It is possible that the two screw conveyors are arranged in parallel within the first reactor unit.

5 The screw conveyor provides a continuous movement of the biomass in the upward direction during the impregnation and ensures that a minimum contact time between the biomass and the impregnation liquid can be provided. The time during which the biomass has to be impregnated by the impregnation liquid is determined by the type of material, e. g. the biomass, or the type of impregnation liquid used for
10 impregnation or by the fill level of the impregnation liquid within the first reactor unit.

However, an adjustment of these influencing parameters may either be carried out manually or automatically within the system.

15 According to another embodiment of the invention, the biomass is compressed in a compression unit before feeding the biomass into the first reactor unit wherein the compression unit in particular comprises a plug screw for compressing the biomass.

By means of the plug screw, a plug of biomass can be provided before it is fed into
20 the first reactor unit. Thus, the biomass can be fed into the first reactor unit in a compacted form.

In yet another embodiment of the invention, the biomass is pre-compressed in a pre-compression unit before compressing the biomass within the compression unit
25 wherein the pre-compression unit in particular comprises a force feed screw for pre-compressing the biomass.

In this manner, it is possible to compress bulky material like for example straw grass, etc. However, it can be distinguished between wood material or non-wood material

- 15 -

which is fed into the first reactor unit as biomass. A pre-compression is preferably used if non-wood material is used as biomass.

5 According to another embodiment of the invention, the biomass is compressed in a second compression unit before feeding the biomass into the second reactor unit wherein the second compression unit in particular comprises a plug screw for compressing the impregnated biomass. Therein the second compression unit may be arranged between the first reactor unit and the second reactor unit.

10 In yet another embodiment of the invention, the biomass is pre-compressed in a second pre-compression unit before compressing the biomass within the second compression unit wherein the second pre-compression unit in particular comprises a force feed screw for pre-compressing the impregnated biomass. Therein the second pre-compression unit may be arranged between the first reactor unit and the second
15 reactor unit, in particular between the first reactor unit and the second compression unit.

According to another embodiment of the invention, the biomass is compressed in a third compression unit before feeding the biomass into the third reactor unit wherein
20 the third compression unit in particular comprises a plug screw for compressing the impregnated biomass. Therein the third compression unit may be arranged between the second reactor unit and the third reactor unit.

In yet another embodiment of the invention, the biomass is pre-compressed in a third
25 pre-compression unit before compressing the biomass within the third compression unit wherein the third pre-compression unit in particular comprises a force feed screw for pre-compressing the impregnated biomass. Therein the third pre-compression unit may be arranged between the second reactor unit and the third reactor unit, in particular between the second reactor unit and the third
30 compression unit.

- 16 -

Therefore, at least one compression unit and/or pre-compression unit is arranged upstream of each reactor unit.

5 According to another embodiment of the invention, at least a part of the recirculated first part of impregnation liquid is recirculated back to a downstream part of the second reactor unit such that a dilution of the impregnated biomass from the second reactor unit takes place. This recirculated first part of impregnation liquid may be fed into a conveyor line between the second reactor unit and the separation unit, wherein the impregnated biomass is transferred through the conveyor line.

10

According to another embodiment of the invention, at least a part of the recirculated second part of impregnation liquid is recirculated back to a downstream part of the second reactor unit such that a dilution of the impregnated biomass from the second reactor unit takes place. This recirculated second part of impregnation liquid may be fed into a conveyor line between the second reactor unit and the separation unit, wherein the impregnated biomass is transferred through the conveyor line.

15

According to another aspect of the present invention, a system for treating biomass is given. The system comprises a first reactor unit for impregnating biomass with an impregnation liquid while the biomass is transferred through the first reactor unit by a conveyor means. The system for treating biomass further comprises a separation unit for separating at least a part of the impregnation liquid from the impregnated biomass. The separated impregnation liquid is discharged from the separation unit such that only a first part of the separated impregnation liquid is recirculated back to the first reactor unit.

20

25

The discharge of the separated impregnation liquid from the separation unit may be carried out by means of a screw which compresses the impregnated biomass such that the impregnation liquid is released from the impregnated biomass. A pump may

be integrated in a line for conveying the separated impregnation liquid between the separation unit and the first reactor unit.

5 The inventive method and the inventive system for treating biomass may be used in a process for recovering sugars from biomass. The method and the system comprise the impregnation, the hydrolysis and the separation, e. g. a dewatering or washing of the impregnated biomass in the separation unit such that the impregnation liquid is recycled to the impregnation step arranged upstream the hydrolysis step. The impregnation liquid may for instance be an acidic liquid. Residual acidic liquid can
10 be recovered in the process and at the same time a more rapid and/or a more selective hydrolysis can be achieved since the acidic liquid functions as a catalyst in the hydrolysis process.

In general, the method or the process comprises the following steps:

15

In a first step, an impregnation of the biomass is carried out using the recycled liquid containing acid from the dewatering step, e. g. the separation step. In a second step, the hydrolysis of the material, e. g. the biomass, is carried out. In a third step, the hydrolyzed material is dewatered to remove the liquids in the separation unit. In a
20 fourth step, the removed liquids, e. g. the impregnation liquid is recycled by recirculating the liquid back to the impregnation step in which the biomass is impregnated using the recycled liquid.

Brief description of the drawings

25

Fig. 1 schematically shows a system for treating biomass according to an embodiment of the invention.

Fig. 2A shows a separation unit according to an embodiment of the invention.

30

Fig. 2B shows a separation unit according to another embodiment of the invention.

Fig. 3 shows a flow diagram for a method for treating biomass according to an embodiment of the invention.

Detailed description of the drawings

Fig. 1 shows a system 1 for treating biomass 2. The system 1 comprises a first reactor unit 10 for impregnating biomass 2 with an impregnation liquid while the biomass 2 is transferred through the first reactor unit 10 by a conveyor means 11 which for instance is a screw conveyor. The biomass 2 is impregnated with impregnation liquid in the first reactor unit 10 such that impregnated biomass 2a is obtained. The separation unit 25 is adapted for separating at least a part of the impregnation liquid from the impregnated biomass 2a. The separated impregnation liquid 26a, 27a is discharged from the separation unit 25 such that only a part of the impregnation liquid 26a is recirculated back to the first reactor unit 10.

The biomass 2 is fed by means of a compression unit 5 into the first reactor unit 10. A pre-compression unit 6 may be arranged before the compression unit 5 such that the biomass 2 is pre-compressed in the pre-compression unit 6 before it is further compressed in the compression unit 5. After compressing the biomass 2, it is introduced into the first reactor unit 10. The reactor unit 10 is filled with impregnation liquid up to a predetermined fill level 13. The reactor unit 10 may be a longitudinal vessel vertically arranged with respect to the earth's surface. The vertical direction is indicated by arrow 3 and the horizontal direction which is substantially parallel to the earth's surface is indicated by arrow 4. The biomass 2 is introduced into the reactor unit 10 and is conveyed by the conveyor means 11 in the vertical direction 3 wherein during the conveyance of the biomass 2 through the first reactor unit 10, the biomass 2 is impregnated by the impregnation liquid filled into

- 19 -

the first reactor unit 10. The impregnation liquid may be provided by a reservoir 40 and/or by a recirculation circuit which is connected to the separation unit 25.

5 The impregnated biomass 2a is then fed into a buffer tank 15 which is arranged between the first reactor unit 10 and a second reactor unit 20 in which a hydrolysis of the impregnated biomass 2a takes place.

10 The impregnated biomass 2a is then transferred to the separation unit 25 after the hydrolysis of the impregnated biomass 2a within the second reactor unit 20. In the separation unit 25, the impregnated biomass 2a and the impregnation liquid solved in the impregnated biomass 2a are at least partly separated. In particular, the impregnation liquid is separated from the impregnated biomass 2a within the separation unit 25. The impregnation liquid separated from the impregnated biomass 2a is then discharged wherein only a part of the impregnation liquid 26a is
15 recirculated back to the first reactor unit 10, for example via recirculation line 12a. Another part 27a of the separated impregnation liquid may be discharged and fed to a further treatment step S50 downstream the separation unit 25. Before the first part of the separated impregnation liquid 26a is fed back into the reactor unit 10, a filtration of this impregnation liquid 26a may be carried out in a filtration unit 29. For
20 example, before the first part of the separated impregnation liquid 26a is fed back into the reactor unit 10, a fractionation of this impregnation liquid 26a may be carried out in a fractionation unit 29. The second part of the impregnation liquid 27a which is fed to a further treatment step S50 downstream the separation unit 25 may also be filtered in the fractionation unit 29. Within the fractionation unit or filtration unit 29,
25 a separation of solid particles within the impregnation liquid may be carried out such that a predetermined purity degree of the recirculated impregnation liquid 26a as well as for the second part of the impregnation liquid 27a which is fed to the treatment step S50 may be adjusted. Evaporation and concentration of compounds present in the separated impregnation liquid 26a may also be carried out in the fractionation
30 unit 29.

- 20 -

The impregnated biomass 2a is transferred to a third reactor unit 30 after the separation of the excess impregnation liquid within the separation unit 25. In the third reactor unit 30, a steam explosion reaction of the impregnated biomass 2a is carried out.

5

Before feeding the impregnation liquid into the first reactor unit 10 via the recirculation line 12a, a mixing of fresh impregnation liquid 12b from the reservoir 40 and the recirculated impregnation liquid 26a from the separation unit 25 may be carried out. In this manner, it is possible to adjust chemical characteristics of the
10 impregnation liquid fed into the first reactor unit 10. Therefore, the line 12a for feeding the recirculated impregnation liquid 26a from the separation unit 25 as well as a line 12c from the reservoir 40 are connected in order to feed the mixed impregnation liquid via line 12 into the first reactor unit 10.

15 Fig. 2A shows an embodiment of the separation unit 25 in detail. In particular, Fig. 2A shows a two-staged separation unit 25 in which a drainage stage 27 and a compression stage 26 are provided. The impregnated biomass 2a is fed into the drainage stage 27 in which free impregnation liquid 27a is drained from the impregnated biomass 2a. This free impregnation liquid 27a which may also be called
20 the second part of the impregnation liquid 27a is then transferred to a treatment step S50 downstream the separation unit 25. However, it is also possible that this drained, second part of the impregnation liquid 27a is recirculated back to the first reactor unit 10.

25 The impregnated biomass 2a is then fed into the compression stage 26 in which the first part of the impregnation liquid 26a is released from the impregnated biomass 2a by compression. The compression may be provided by a screw press 28 in the compression stage 26. The first part of the impregnation liquid 26a released from the impregnated biomass 2a in the compression stage 26 is also recirculated back to the
30 first reactor unit 10. The separation unit 25 may comprise other stages in which

impregnation liquid can be released from the impregnated biomass 2a. The characteristics, e. g. the composition of the impregnation liquid separated in the drainage stage 27 and in the compression stage 26 of the separation unit 25 may be different. In particular, the characteristics of the separated impregnation liquid 26a, 27a may determine the target location of the separated parts of impregnation liquid 26a, 27a, for example whether these parts of impregnation liquid 26a, 27a are transferred to the first reactor unit 10 or to the treatment step S50 downstream the separation unit 25.

10 As shown in Fig. 2A the compression stage 26 is arranged before the drainage stage 27 within the separation unit 25. However, it is also possible that the drainage stage 27 is arranged before the compression stage 26.

Fig. 2B shows an embodiment of the separation unit 25 with only one stage, in particular with a compression stage 26. It is possible that, in the compression stage 26, a part of impregnation liquid 27a is drained from the impregnated biomass 2a and that another part of the impregnation liquid 26a is released from the impregnated biomass 2a by the compression. The compression stage 26 may thus result in a first part of impregnation liquid 26a released from the impregnated biomass 2a by compression and a second part of impregnation liquid 27a drained from the impregnated biomass 2a wherein the first part of impregnation liquid 26a and the second part of impregnation liquid 27a are fed or transferred to different target locations.

25 The separation unit 25 may also be referred to as a dewatering or washing stage. The separation unit 25 comprises a drainage stage integrated into the compression stage 26. The drainage stage may comprise a drain screw for conveying the impregnated biomass 2a during the drainage in which free water is released from the impregnated biomass 2a. The compression stage 26 may comprise one of a screw press, a plug

screw, twin rolls or simply a press such that the first part of the impregnation liquid 26a can be released from the impregnated biomass 2a.

In case the separation unit 25 comprises a one-stage configuration, e. g. the
5 separation unit 25 only comprises the compression stage 26, then the compression stage 26 may comprise one of a screw press, a plug screw, twin rolls or simply a press. Furthermore, several areas within the compression unit 26 may be provided in which different parts of the liquid are released from the impregnated biomass 2a. In this manner, it is possible that the first part of impregnation liquid 26a is released
10 separately from the second part of impregnation liquid 27a.

Fig. 3 shows a flow diagram for a method for treating biomass 2. In step S1 of the method, a pre-compression of the biomass 2 in a pre-compression unit 6 is carried out before compressing the biomass 2 within a compression unit 5. The pre-
15 compression unit 6 may comprise a force feed screw for pre-compressing the biomass 2. In a step S2 of the method, a compression of the biomass 2 in a compression unit 5 is carried out before feeding the biomass 2 to a first reactor unit 10, wherein the compression unit 5 comprises a plug screw for compressing the biomass 2. In a step S10 of the method, the biomass 2 and an impregnation liquid are
20 fed into the first reactor unit 10 such that the biomass 2 is impregnated with the impregnation liquid while the biomass 2 is transferred through the first reactor unit 10 by a conveyor means 11. In a step S11, impregnated biomass 2a is fed from the first reactor unit 10 into a second reactor unit 20 before transferring the impregnated biomass 2a to the separation unit 25, wherein a hydrolysis of the impregnated
25 biomass 2a takes place within the second reactor unit 20. In a step 20 of the method, the impregnated biomass 2a is transferred from the first reactor unit 10 to the separation unit 25 wherein at least a part of the impregnation liquid 26a, 27a is separated from the impregnated biomass 2a within the separation unit 25. In a further step S30 of the method, the separated impregnation liquid 26a, 27a is discharged
30 from the separation unit 25 such that only a part of the impregnation liquid 26a is

- 23 -

recirculated back to the first reactor unit 10. In another step S31, a fractionation or a filtration of the separated impregnation liquid 26a, 27a is carried out in a fractionation unit 29 or filtration unit 29 such that a predetermined purity degree of the recirculated impregnation liquid 26a can be adjusted. In another step S32, a
5 mixing of the recirculated impregnation liquid 26a from the separation unit 25 with fresh impregnation liquid 12b from the reservoir 40 is carried out before injecting the mixed impregnation liquid into the first reactor unit 10. In another step S33, an injection of the recirculated impregnation liquid 26a from the separation unit 25 into the first reactor unit 10 is carried out such that the recirculated impregnation liquid
10 26a is reused for impregnating the fed biomass 2 within the first reactor unit 10. In another step S40, the impregnated biomass 2a is transferred from the separation unit 25 to a third reactor unit 30 wherein a steam explosion on the impregnated biomass 2a takes place within the third reactor unit 30. In yet another step S50 of the method, a second part of the impregnation liquid 27a separated in the separation unit 25, e. g.
15 the part of the separated impregnation liquid which is not recirculated back to the first reactor unit 10 is transferred to a treatment step downstream the separation unit 25.

While the invention has been illustrated and described in detail in the drawings and
20 the foregoing description, such illustration and description are to be considered illustrative and exemplary and not restrictive; the invention is not limited to the disclosed embodiments. Other variations to the disclosed embodiments can be understood and effected by those skilled in the art and practicing the claimed invention, from a study of the drawings, the disclosure, and the appended claims. In
25 the claims the term “comprising” does not exclude other elements, and the indefinite article “a” or “an” does not exclude a plurality. The mere fact that certain measures are recited in mutually different dependent claims does not indicate that a combination of these measures cannot be used to advantage. Any reference signs in the claims should not be construed as limiting the scope of protection.

Claims

1. A method for treating biomass, comprising:

5 Feeding biomass (2) and an impregnation liquid into a first reactor unit (10) such that the biomass (2) is impregnated with the impregnation liquid while the biomass (2) is transferred through the first reactor unit (10) by a conveyor means (11, S10);

10 Transferring the impregnated biomass (2a) from the first reactor unit (10) to a separation unit (25), wherein at least a part of the impregnation liquid is separated from the impregnated biomass (2a) within the separation unit (25, S20);

Discharging the separated impregnation liquid from the separation unit (25), such that a first part (26a) of the separated impregnation liquid is recirculated back to the first reactor unit (10, S30)

15

2. The method according to claim 1,

wherein the separation of the impregnation liquid within the separation unit (25) comprises a compression stage (26) in which the impregnation liquid is released from the impregnated biomass (2a) by
20 compressing the impregnated biomass (2a) preferably with a screw press (28).

3. The method according to claim 2,

wherein a second part (27a) of the impregnation liquid released from the impregnated biomass (2a) in the compression stage (26) is transferred to a
25 treatment step (S50) downstream the separation unit (25).

- 25 -

4. The method according to any one of the preceding claims,
wherein the separation of the impregnation liquid within the
separation unit (25) comprises a drainage stage (27) in which free
impregnation liquid (27a) is drained from the impregnated biomass (2a)
5 without compression, preferably by gravity draining.
5. The method according to claim 4,
wherein the free impregnation liquid (27a) drained from the
impregnated biomass (2a) in the drainage stage (27) is transferred to a
10 treatment step (S50) downstream the separation unit (25).
6. The method according to any one of the preceding claims, comprising:
Fractionating the separated first part of impregnation liquid (26a) in a
fractionation unit (29) until a predetermined purity degree of the recirculated
15 impregnation liquid is reached (S31).
7. The method according to any one of the preceding claims, comprising:
Mixing the recirculated first part of impregnation liquid (26a) from the
separation unit (25) with impregnation liquid (12b) from a reservoir (40)
20 before injecting the mixed impregnation liquid to the first reactor unit (10,
S32).
8. The method according to any one of the preceding claims, comprising:
Injecting the recirculated first part of impregnation liquid (26a) from
25 the separation unit (25) into the first reactor unit (10) such that the
recirculated first part of impregnation liquid (26a) is used for impregnating
the fed biomass (2) within the first reactor unit (10, S33).

- 26 -

9. The method according to any one of the preceding claims, comprising:
Feeding the impregnated biomass (2a) from the first reactor (10) unit
into a second reactor unit (20) before transferring the impregnated biomass
(2a) to the separation unit (25), wherein a hydrolysis of the impregnated
5 biomass (2a) takes place within the second reactor unit (20, S11).
10. The method according to any one of the preceding claims, comprising:
Transferring the impregnated biomass (2a) from the separation unit
(25) to a third reactor unit (30), wherein a steam impact, in particular a steam
10 explosion of the impregnated biomass (2a) takes place within the third reactor
unit (30, S40).
11. The method according to any one of the preceding claims,
wherein the impregnation liquid is fed into the first reactor unit (10)
15 up to a predetermined fill level (13) such that at least a part of the biomass (2)
which is fed into the first reactor unit (10) is in permanent contact with the
impregnation liquid.
12. The method according to any one of the preceding claims,
20 wherein the conveyor means (11) of the first reactor unit (10) is a
screw conveyor arranged with a vertical component, in particular vertically
within the first reactor unit (10) such that the biomass (2) is conveyed in an
upward direction (3) during the impregnation.
- 25 13. The method according to any one of the preceding claims, comprising:
Compressing the biomass (2) in a compression unit (5) before feeding
the biomass (2) into the first reactor unit (10), wherein the compression unit
(5) comprises a plug screw for compressing the biomass (2, S2).
- 30 14. The method according to any one of the preceding claims, comprising:

- 27 -

Pre-compressing the biomass (2) in a pre-compression unit (6) before compressing the biomass (2) within the compression unit (5), wherein the pre-compression unit (6) in particular comprises a force feed screw for pre-compressing the biomass (2, S1).

5

15. A system for treating biomass, comprising:

a first reactor unit (10) for impregnating biomass (2) with an impregnation liquid while the biomass (2) is transferred through the first reactor unit (10) by a conveyor means (11);

10

a separation unit (25) for separating at least a part of the impregnation liquid from the impregnated biomass (2a);

wherein the separated impregnation liquid is discharged from the separation unit (25), such that a first part (26a) of the separated impregnation liquid is recirculated back to the first reactor unit (10).

15

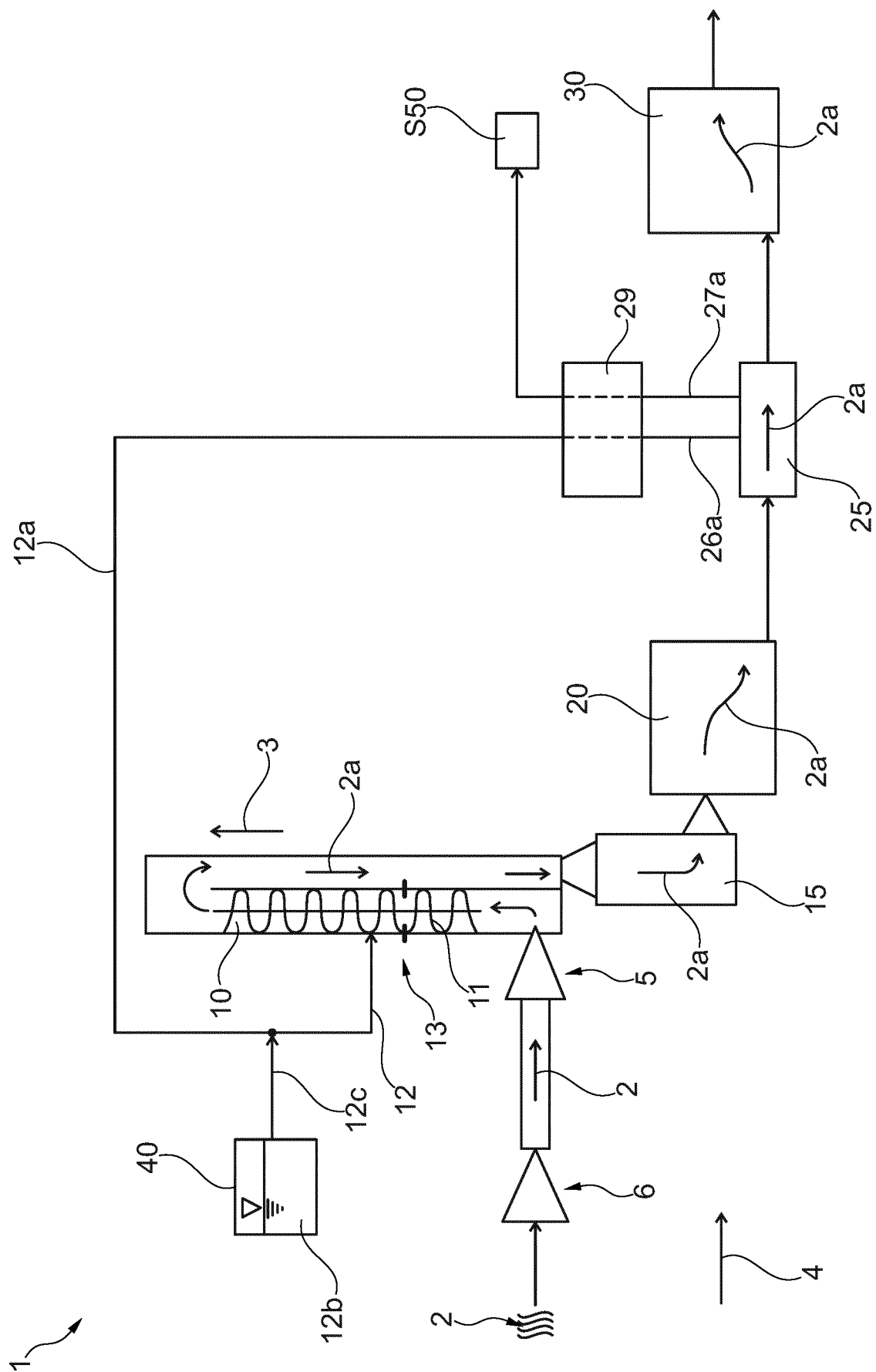


Fig. 1

2/2

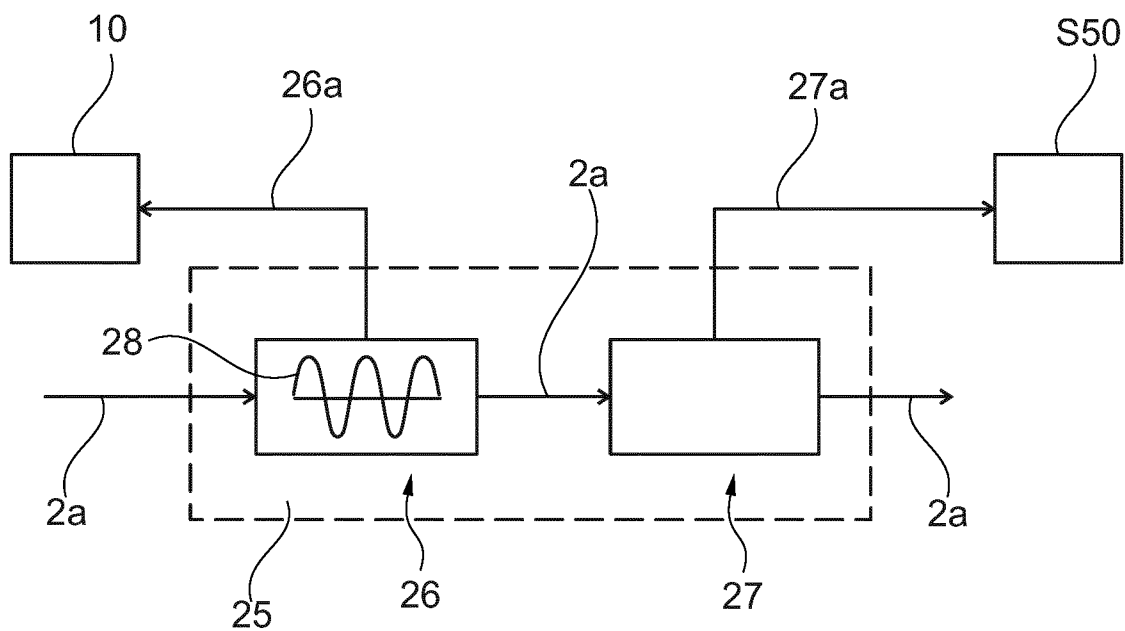


Fig. 2A

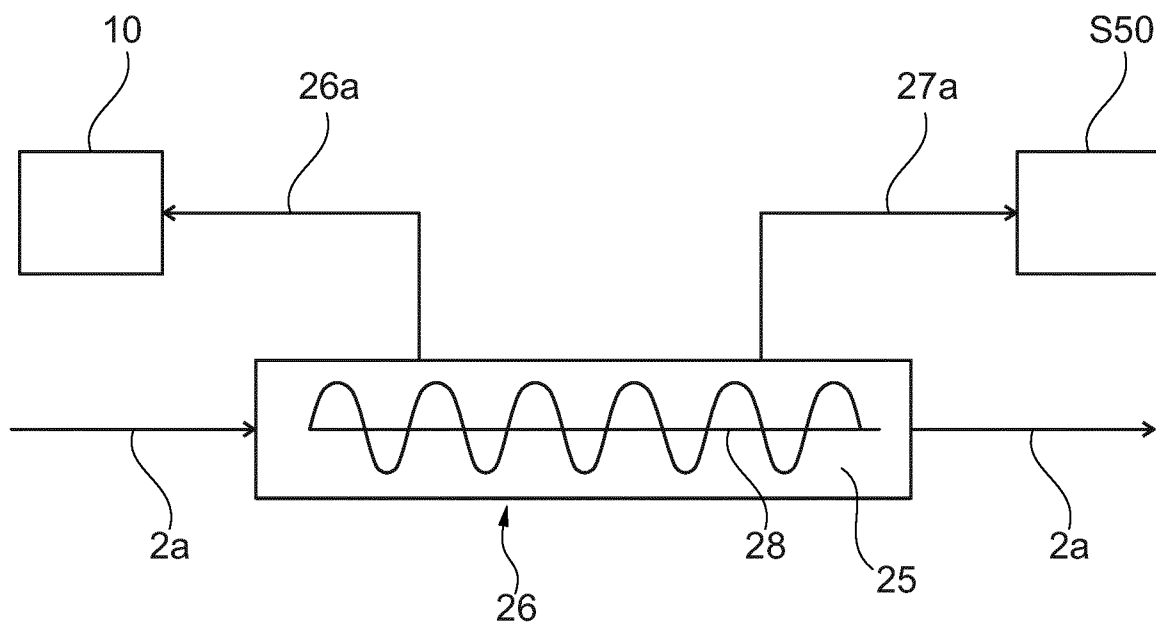


Fig. 2B

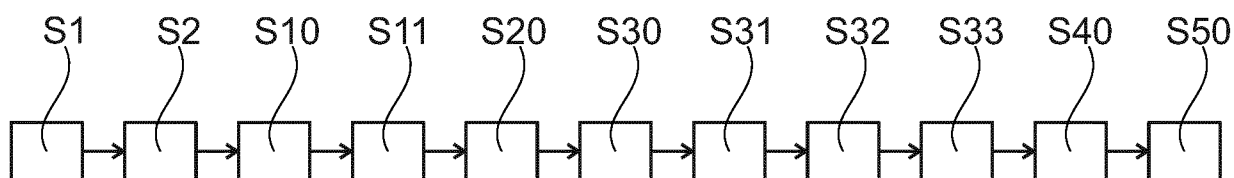


Fig. 3

INTERNATIONAL SEARCH REPORT

International application No
PCT/EP2017/081930

A. CLASSIFICATION OF SUBJECT MATTER

INV. D21C1/00 D21C3/00 D21C7/00
ADD.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
D21C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPO-Internal, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 2009/012779 A2 (ATLAS STORD DENMARK [DK]; FOSBOL PEDER [DK]; HANSEN PALLE [DK]) 29 January 2009 (2009-01-29)	1-15
Y	claims 1,2,7	1,15
Y	WO 2007/009463 A2 (HOLM CHRISTENSEN BIOSYSTEMER A [DK]; HOLM CHRISTENSEN BOERGE [DK]; HOL) 25 January 2007 (2007-01-25) page 27, line 20 - line 22	1,15
Y	WO 2011/039635 A2 (NOVA PANGAEA TECHNOLOGIES LTD [GB]; NORTH PETER HERBERT [IE]) 7 April 2011 (2011-04-07) figures 1, 2	1,15



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier application or patent but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

29 January 2018

Date of mailing of the international search report

06/02/2018

Name and mailing address of the ISA/

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040,
Fax: (+31-70) 340-3016

Authorized officer

Ponsaud, Philippe

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No

PCT/EP2017/081930

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 2009012779	A2	29-01-2009	AT 503027 T 15-04-2011
		BR PI0814664 A2 18-02-2015	
		CA 2694245 A1 29-01-2009	
		DK 2185734 T3 18-07-2011	
		EP 2185734 A2 19-05-2010	
		US 2010216202 A1 26-08-2010	
		WO 2009012779 A2 29-01-2009	

WO 2007009463	A2	25-01-2007	AU 2006272198 A1 25-01-2007
		BR PI0613681 A2 13-07-2010	
		BR PI0622271 A2 09-08-2011	
		CA 2615844 A1 25-01-2007	
		CA 2831082 A1 25-01-2007	
		CA 2959268 A1 25-01-2007	
		CN 101268121 A 17-09-2008	
		CN 101798584 A 11-08-2010	
		DK 1910448 T3 02-01-2017	
		EP 1910448 A2 16-04-2008	
		EP 2172568 A1 07-04-2010	
		EP 2520608 A1 07-11-2012	
		EP 2520609 A1 07-11-2012	
		EP 2657275 A1 30-10-2013	
		ES 2606281 T3 23-03-2017	
		HR P20161565 T1 10-03-2017	
		MX 343301 B 01-11-2016	
		NZ 565629 A 30-06-2011	
		NZ 592233 A 31-08-2012	
		NZ 601075 A 31-01-2014	
		UA 100662 C2 25-01-2013	
		UA 114465 C2 26-06-2017	
		US 2010041119 A1 18-02-2010	
		US 2012138246 A1 07-06-2012	
		US 2013143263 A1 06-06-2013	
		US 2015232579 A1 20-08-2015	
		US 2016153010 A1 02-06-2016	
		WO 2007009463 A2 25-01-2007	
		ZA 200801439 B 26-11-2008	

WO 2011039635	A2	07-04-2011	AP 3563 A 27-01-2016
		BR 112012007026 A2 01-03-2017	
		CA 2775656 A1 07-04-2011	
		DK 2483331 T3 28-08-2017	
		EP 2483331 A2 08-08-2012	
		ES 2630053 T3 17-08-2017	
		LT 2483331 T 25-07-2017	
		US 2011100359 A1 05-05-2011	
		US 2014123973 A1 08-05-2014	
		US 2016068920 A1 10-03-2016	
		WO 2011039635 A2 07-04-2011	
		ZA 201202754 B 26-06-2013	
