Title: COP2 LOADED RED PHOSPHORUS, PREPARATION AND USE OF THE SAME

Abstract: Disclosed are a photocatalyst of CoP₂ loaded red phosphorus, a preparation method thereof, and a method for photocatalytic hydrogen production from water under visible light irradiation over the photocatalyst of CoP₂ loaded red phosphorus.
CoP₂ loaded red phosphorus, preparation and use of the same

CROSS-REFERENCE TO RELATED APPLICATIONS

[0000] This application claims the benefits of U.S. Provisional Patent Application No. 61/700,751 as filed on September 13, 2012. The disclosure of the provisional application is incorporated herein by reference in its entirety.

TECHNICAL FIELD

[0001] The present application relates to a photocatalyst, a preparation method and a use thereof.

TECHNICAL BACKGROUND

[0002] Hydrogen is an important industrial raw material and a special gas having reducibility in petrochemical and fine organic synthesis industries. It is also used in aerospace and viewed as the energy source of the future, due to its high combustion enthalpy (-286 kJ/mol). Currently, the technologies for hydrogen production are mainly steam reforming from hydrocarbons, electrolysis and thermolysis. Hydrogen-gas as a fuel to drive vehicles such as buses, cars and the like is not used very often because the technique necessary to generate energy out of hydrogen is very expensive.

[0003] Solar-induced photocatalytic hydrogen production from water is a clean and renewable source of energy, and has been considered as a promising way to alleviate this problem. Under irradiation, photogenerated electrons from a photocatalyst could reduce water to hydrogen. This technology is an environmentally friendly process and promising to produce hydrogen in a low cost. Besides, hydrogen can be produced in situ and does not need to be transported.

[0004] However, the efficiency and the application of photocatalytic hydrogen production are limited by the narrow absorption of semiconductor and the need of expensive co-catalyst, such as Pt. Even though great efforts have been made to develop new photocatalysts and co-catalysts, these problems still could not be solved.
Accordingly, a novel and desirable photocatalyst with a suitable conduction band energy for transferring photogenerated electrons to water is needed.

SUMMARY

[0005] In one aspect, the present application provides a photocatalyst of CoP₂ loaded red phosphorus.

[0006] In another aspect, the present application provides a method for preparing a photocatalyst of CoP₂ loaded red phosphorus, comprising:

a) growing CoP₂ from a red phosphorus in water; and

b) treating the CoP₂ loaded red phosphorus at a temperature ranging from 450°C to 650 °C.

[0007] In another aspect, the present application provides a method for photocatalytically producing hydrogen from water in the presence of a sacrificial agent over a photocatalyst of CoP₂ loaded red phosphorus.

[0008] In another aspect, the present application provides a use of CoP₂ as a co-catalyst for a red phosphorus.

[0009] CoP₂ loaded red phosphorus as provided in the present application is a photocatalyst with broad visible light absorption and high photocatalytic efficiency for hydrogen production from water. The absorption band edge of red phosphorus can be up to 700 nm, which can be driven by visible light. When used for hydrogen production from water, the performance of CoP₂ can be up to 6 times higher compared with the common co-catalyst of Pt under the same conditions. Moreover, as a non-noble metal co-catalyst, the price of CoP₂ is about 200 times lower than that of Pt.

BRIEF DESCRIPTION OF THE DRAWINGS

[0010] FIG. 1a shows TEM image of CoP₂ loaded red phosphorus prepared in Example 1.

[0011] FIG. 1b shows another TEM image of CoP₂ loaded red phosphorus prepared in Example 1.
DETAILED DESCRIPTION

[0012] In the following description, certain specific details are included to provide a thorough understanding of various disclosed embodiments. One skilled in the relevant art, however, will recognize that embodiments may be practiced without one or more of these specific details, or with other methods, components, materials, etc.

[0013] Unless the context requires otherwise, throughout the specification and claims which follow, the word "comprise" and variations thereof, such as, "comprises" and "comprising" are to be construed in an open, inclusive sense, which is as "including, but not limited to".

[0014] Reference throughout this specification to "one embodiment", or "an embodiment", or "in another embodiment", or "some embodiments", or "in some embodiments" means that a particular referent feature, structure, or characteristic described in connection with the embodiment is included in at least one embodiment. Thus, the appearance of the phrases "in one embodiment", or "in an embodiment", or "in another embodiment", or "in some embodiments" in various places throughout this specification are not necessarily all referring to the same embodiment. Furthermore, the particular features, structures, or characteristics may be combined in any suitable manner in one or more embodiments.

[0015] It should be noted that, as used in this specification and the appended claims, the singular forms "a", "an", and "the" include plural referents unless the content clearly dictates otherwise. In this application, the use of "or" means "and/or" unless stated otherwise.

[0016] In one aspect, the present application provides a photocatalyst of CoP$_2$ loaded red phosphorus.

[0017] In some embodiments of the present application, CoP$_2$ is loaded at about 0.5 % to about 7.0 % by weight, preferably about 1.0 % to about 4.0 % by weight, more preferably about 2.0 % to about 4.0 % by weight, most preferably about 2.0 % by weight.

[0018] In some embodiments of the present application, the red phosphorus contained in the photocatalyst preferably is a crystalline red phosphorus.
[0019] In some embodiments of the present application, the CoP₂ loaded red phosphorus has photocatalytic activity and can be used for hydrogen production from water.

[0020] In another aspect, the present application provides a method for preparing a photocatalyst of CoP₂ loaded red phosphorus, comprising:

a) growing CoP₂ from a red phosphorus in water; and

b) treating the CoP₂ loaded red phosphorus at a temperature ranging from about 450 °C to about 650 °C, preferably about 450 °C to about 500 °C, more preferably about 450 °C.

[0021] In some embodiments of the present application, the step of growing CoP₂ from a red phosphorus is carried out by the hydrothermal reaction of a cobalt compound with a red phosphorus.

[0022] In some embodiments of the present application, the hydrothermal reaction of the cobalt compound with the red phosphorus can be carried out at a temperature ranging from 150 °C to 200 °C for 12-24 hours, preferably about 200 °C for about 12-20 hours, more preferably about 200 °C for about 12 hours.

[0023] In some embodiments of the present application, the cobalt compound that can be used includes but is not limited to cobalt acetate, cobalt chloride, potassium cobalt cyanide, and a combination thereof.

[0024] In some embodiments of the present application, the red phosphorus used in step a) is an amorphous red phosphorus.

[0025] In some embodiments of the present application, the molar ratio of the red phosphorus to the cobalt compound used in step a) can be 50-2000:1, preferably 100-600:1, more preferably 400-600:1.

[0026] In some embodiments of the present application, a molar concentration of the red phosphorus in water in step a) can be 0.1-1 M, preferably 0.2-0.4 M.

[0027] In some embodiments of the present application, CoP₂ loaded red phosphorus in step b) can be thermally treated at a temperature ranging from about 450 °C to about 650 °C for about 2 hours - about 15 hours, preferably at about 450 °C to about 500 °C for about 2 hours - about 15 hours, more preferably at a temperature of
about 450 °C for about 5 hours - about 12 hours.

[0028] In some embodiments of the present application, CoP₂ loaded red phosphorus in step b) can be thermally treated under vacuum.

[0029] In some embodiments of the present application, the method for preparing the photocatalyst of CoP₂ loaded red phosphorus further comprises a step of purifying the red phosphorus before growing CoP₂ from the red phosphorus in water.

[0030] In some embodiments of the present application, the red phosphorus is purified in water by the hydrothermal method at a temperature of about 200 °C. Specifically, the step of purifying the red phosphorus comprises dispersing a commercially available red phosphorus in water to obtain a suspension, heating the resulting suspension to about 200 °C and maintaining at the same temperature for about 12 hours to remove surface oxidation.

[0031] In another aspect, the present application provides a method for photocatalytically producing hydrogen from water in the presence of a sacrificial agent over a photocatalyst of CoP₂ loaded red phosphorus.

[0032] The photo-induced hydrogen production from water over the photocatalyst of CoP₂ loaded red phosphorus is evaluated below. In order to increase the efficiency of photo-generated electrons and hydrogen formation, it is preferable to add a hole sacrificial agent during the formation of hydrogen to aid the separation of photo-generated electrons and holes.

[0033] Accordingly, in some embodiments of the present application, the sacrificial agent that can be used includes but is not limited to methanol, citric acid, ascorbic acid, lactic acid and a mixture thereof, preferably methanol, ascorbic acid and lactic acid, more preferably ascorbic acid and lactic acid, most preferably lactic acid.

[0034] In some embodiments of the present application, the sacrificial agent can be used at such amount that the concentration of the sacrificial agent in water is about 1 % to about 15 %, preferably about 3 % to about 10 %, more preferably about 5 %. Where the used sacrificial agent is solid, such as citric acid, ascorbic acid and the like, the above concentration unit is weight percentage. Where the used sacrificial agent is liquid, such as methanol, lactic acid and the like, the above concentration unit is
volume percentage.

[0035] In some embodiments of the present application, the photocatalyst of CoP$_2$ loaded red phosphorus can be used at a catalytic amount, which can be determined by a person skilled in the art through conventional techniques in the art.

[0036] In some embodiments of the present application, the hydrogen production from water can be carried out under visible light irradiation. The visible light is in the range of from 400 nm to 750 nm.

[0037] Briefly, the present application provides the method for photocatalytically producing hydrogen from water comprising

a) mixing the photocatalyst of CoP$_2$ loaded red phosphorus, the sacrificial agent and water; and

b) irradiating a mixture obtained from step a) with a visible light.

[0038] In some embodiments of the present application, the above-mentioned mixing step can be carried out by adding the photocatalyst of CoP$_2$ loaded red phosphorus and the sacrificial agent to water or adding the photocatalyst of CoP$_2$ loaded red phosphorus to a solution of the sacrificial agent in water or adding the sacrificial agent to a suspension of the photocatalyst of CoP$_2$ loaded red phosphorus in water.

[0039] In another aspect, the present application provides a use of CoP$_2$ as a co-catalyst for red phosphorus. When used for hydrogen production from water, the optimal performance of CoP$_2$ as the co-catalyst is 6 times higher than that of the common co-catalyst, Pt.

[0040] The CoP$_2$ loaded red phosphorus is also characterized by X-ray diffraction (XRD), transmission electron microscopy (TEM) and UV-Vis spectrophotometer, respectively, in which XRD is performed with a Rigaku SmartLab X-ray diffractometer using Cu Ka irradiation ($\lambda = 1.5406$ Å); transmission electron microscopy images were recorded using a CM-120 microscope (Philips, 120kV) coupled with an energy-dispersive X-ray (EDX) spectrometer (Oxford Instrument); the electron microscopy samples were prepared by dispersing the powder in ethanol with ultrasonication for 20s; and UV-vis diffuse reflectance spectra were achieved using a
UV-vis spectrophotometers (Cary 100 scan spectrophotometers, Varian). Figures 1a and 1b show TEM images of CoP$_2$ loaded red P prepared according to the present application.

EXAMPLES

[0041] Embodiments of the present application are disclosed in further detail in the following examples, which are not in any way intended to limit the scope of the present invention.

EXAMPLE 1
Preparation of CoP$_2$ loaded red phosphorus

[0042] 100 mg of commercially available red phosphorus was dispersed in 15 ml of de-ionized water to form a suspension. The resulted suspension was put into a Teflon-lined stainless autoclave, heated to 200 °C and maintained at 200 °C for 12 h to remove surface oxidation. 1 mg of Cobalt (II) acetate tetrahydrate (purity > 99.999 %, available from Sigma-Aldrich without further purification) was added into 15 mL of de-ionized water together with 100 mg of purified red phosphorus. After ultrasonic treatment for 5 min, the resulted mixture was transferred into a preheated oven at 200 °C and maintained at the same temperature for 20 h. After the hydrothermal reaction, the reaction mixture is filtrated and the resulted powders were washed with 8 ml of de-ionized water and 8 ml of ethanol for three times, separately. The washed powders were dried at 60 °C. The dried powders were crystallized in a vacuum tube furnace at 450 °C for 12 h. The crystallized products were washed with 8 ml of water and 8 ml of ethanol, and then dried at 60 °C to obtain the photocatalyst of CoP$_2$ loaded crystalline red phosphorus.

EXAMPLE 2
Photocatalytic hydrogen production from water over CoP$_2$ loaded red phosphorus

[0043] The photocatalytic H$_2$ evolution experiment was carried out in a Pyrex reaction cell connected to a closed gas circulation and evacuation system. 50 mg of the
CoP$_2$ loaded red phosphorus as prepared in Example 1 was dispersed in 100 mL of 5 vol% of aqueous solution of lactic acid as a hole sacrificial agent. The resulted suspension was purged with argon to remove dissolved air before irradiation. The resulted suspension was irradiated by a 300 W xenon lamp with an appropriate cut-off filter and a water filter. The amount of hydrogen generated from photocatalytic water splitting was measured by Techcomp GC7900 gas chromatography with a TCD detector and a capillary column (Molecular Sieve 5 Å). High purity nitrogen gas was used as a carrier gas.

EXAMPLE 3
Effect of loading amount of CoP$_2$ on hydrogen production

[0044] CoP$_2$ loaded red phosphorus was prepared in the same manner as in Example 1 with the exception of different amounts of cobalt (II) acetate tetrahydrate. 1 mg, 2 mg, 4 mg, 6 mg, and 8 mg of cobalt (II) acetate tetrahydrate were used to prepare the CoP$_2$ loaded red phosphorus having different weight percentage of CoP$_2$, respectively. The photocatalytic H$_2$ evolution experiments were carried out under the same conditions as in Example 2 with the exception of CoP$_2$ loaded red phosphorus having different weight percentage of CoP$_2$. The rates of hydrogen production in the presence of different percentages of CoP$_2$ with 5 vol% of aqueous solution of lactic acid as the sacrificial agent were shown in Table 1.

<table>
<thead>
<tr>
<th>Sample</th>
<th>Red</th>
<th>Co(acac)$_2$·4H$_2$O (mg)</th>
<th>H$_2$O (mL)</th>
<th>Temperature (°C)</th>
<th>Percentages of CoP$_2$ (wt %)</th>
<th>The rate of H$_2$ production (µmol h$^{-1}$ g$^{-1}$)</th>
</tr>
</thead>
<tbody>
<tr>
<td>50</td>
<td>100</td>
<td>0</td>
<td>15</td>
<td>200</td>
<td>0</td>
<td>2.7</td>
</tr>
<tr>
<td>51</td>
<td>100</td>
<td>1</td>
<td>15</td>
<td>200</td>
<td>0.5</td>
<td>54.1</td>
</tr>
</tbody>
</table>
The above results show that the photocatalytic activity of 0.5 wt% CoP₂ loaded red P is 20 times as much as that of red P, and the photocatalytic activity of 2.0 wt% CoP₂ loaded red P is 75 times as much as that of red P.

EXAMPLE 4
Effect of amount of sacrificial agent on hydrogen production

2 wt% CoP₂ loaded red phosphorus was prepared in the same manner as in Example 1. The photocatalytic H₂ evolution experiments were carried out under the same conditions as in Example 2 with the exception of different volume percentages of lactic acid. The rates of hydrogen production in the presence of different volume percentages of lactic acid were shown in Table 2.

<table>
<thead>
<tr>
<th>Lactic acid (vol%)</th>
<th>0</th>
<th>1</th>
<th>3</th>
<th>5</th>
<th>8</th>
<th>10</th>
</tr>
</thead>
<tbody>
<tr>
<td>The rate of H₂ production (µmol h⁻¹ g⁻¹)</td>
<td>29.1</td>
<td>67.3</td>
<td>133.7</td>
<td>203.0</td>
<td>210.7</td>
<td>215.2</td>
</tr>
</tbody>
</table>

EXAMPLE 5
Effect of different sacrificial agent on hydrogen production

2 wt% CoP₂ loaded red phosphorus was prepared in the same manner as in Example 1. The photocatalytic H₂ evolution experiments were carried out under the same conditions as in Example 2 with the exception of different sacrificial agents. The rates of hydrogen production in the presence of different sacrificial agents were shown in Table 3.
TABLE 3

Comparison of the rate of hydrogen production from water with different sacrificial agents over 2 wt% CoP₂ loaded red phosphorus

<table>
<thead>
<tr>
<th>Sacrificial agents (5 %)ᵃ</th>
<th>Methanol</th>
<th>Ascorbic acid</th>
<th>Lactic acid</th>
<th>Citric acid</th>
</tr>
</thead>
<tbody>
<tr>
<td>The rate of H₂ production (µmol h⁻¹ g⁻¹)</td>
<td>120.3</td>
<td>181.1</td>
<td>203.0</td>
<td>100.5</td>
</tr>
</tbody>
</table>

ᵃ: For methanol and lactic acid, the unit is volume percentage, for ascorbic acid and citric acid, the unit is weight percentage.

EXAMPLE 6

Comparison between CoP₂ and Pt as co-catalysts

[0048] CoP₂ loaded red phosphorus was prepared in the same manner as in Example 1. The photocatalytic H₂ evolution experiments were carried out under the same conditions as in Example 2 with the exception of CoP₂ loaded red phosphorus having different percentages of CoP₂ and Pt loaded red phosphorus having different percentages of Pt. The rates of hydrogen production in the presence of CoP₂ or Pt as a co-catalyst with different percentages were shown in Table 4.

TABLE 4

Comparison of the rate of hydrogen production between CoP₂ and Pt as the co-catalyst with different percentages in the presence of 5 vol% of aqueous solution of lactic acid as the sacrificial agent.

<table>
<thead>
<tr>
<th>wt %</th>
<th>0.5</th>
<th>1</th>
<th>2</th>
<th>3</th>
<th>4</th>
</tr>
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<tbody>
<tr>
<td>H₂ᵃ</td>
<td>CoP₂</td>
<td>Pt</td>
<td>CoP₂</td>
<td>Pt</td>
<td>CoP₂</td>
</tr>
<tr>
<td>0.5</td>
<td>54.0</td>
<td>17.6</td>
<td>88.0</td>
<td>33.2</td>
<td>203.0</td>
</tr>
</tbody>
</table>

ᵃ: The rate of H₂ production (µmol h⁻¹ g⁻¹)

[0049] The above results show that the optimal performance of CoP₂ as a co-catalyst is even higher than that of Pt by a factor of 6. Without bound by any theory, this enhanced photocatalytic activity may be attributed to the coordination effect
between Co atoms of CoP₂ with water. This interaction would decrease the bond strength of O-H, and thus H₂O would be more easily decomposed after accepting the photogenerated electrons.

[0050] All of the above U.S. patents, U.S. patent application publications, U.S. patent applications, foreign patents, foreign patent applications and non-patent publications referred to in this specification and/or listed in the Application Data Sheet, are incorporated herein by reference, in their entirety.

[0051] From the foregoing it will be appreciated that, although specific embodiments of the invention have been described herein for purposes of illustration, various modifications may be made without deviating from the spirit and scope of the invention. Accordingly, the invention is not limited except as by the appended claims.
What is claimed is:

1. A photocatalyst of CoP₂ loaded red phosphorus.

2. The photocatalyst of claim 1, wherein CoP₂ is loaded onto the red phosphorus at about 0.5 % to about 7.0 % by weight, preferably about 1.0 % to about 4.0 % by weight, more preferably about 2.0 % to about 4.0 % by weight, most preferably about 2.0 % by weight.

3. The photocatalyst of claim 1 or 2, wherein the red phosphorus contained therein is a crystalline red phosphorus.

4. The photocatalyst of any one of claims 1 to 3, wherein the photocatalyst has photocatalytic activity and can be used for hydrogen production from water.

5. A method for photocatalytically producing hydrogen from water comprising:
   a) mixing the photocatalyst of CoP₂ loaded red phosphorus of claim 1, a sacrificial agent and water; and
   b) irradiating a mixture obtained from step a) with a visible light.

6. The method of claim 5, wherein the sacrificial agent is selected from the group consisting of methanol, citric acid, ascorbic acid, lactic acid and a mixture thereof, preferably methanol, ascorbic acid and lactic acid, more preferably ascorbic acid and lactic acid, most preferably lactic acid.

7. The method of claim 5 or 6, wherein the sacrificial agent is used at such amount that the concentration of the sacrificial agent in water is about 1 % to about 15 % by volume, preferably about 3 % to about 10 % by volume, more preferably about 5 % by volume when the sacrificial agent is a liquid; or the sacrificial agent is used at such amount that the concentration of the sacrificial agent in water is about 1 % to
about 15 % by weight, preferably about 3 % to about 10 % by weight, more preferably about 5 % by weight when the sacrificial agent is a solid.

8. The method of any one of claims 5-7, wherein the CoP$_2$ loaded onto the red phosphorus has about 0.5 wt% to about 7.0 wt%, preferably about 1.0 wt% to about 4.0 wt%, more preferably about 2.0 wt% to about 4.0 wt%, most preferably about 2.0 wt% of CoP$_2$.

9. The method of any one of claims 5-8, wherein the visible light is in the range of from 400 nm to 750 nm.

10. A method for preparing the photocatalyst of CoP$_2$ loaded red phosphorus of claim 1, comprising:
   a) growing CoP$_2$ from a red phosphorus in water; and
   b) treating the CoP$_2$ loaded red phosphorus obtained from step a) at a temperature ranging from about 450 °C to about 650 °C, preferably about 450 °C to about 500 °C, more preferably about 450 °C.

11. The process of claim 10, wherein the step a) of growing CoP$_2$ from the red phosphorus is carried out by a hydrothermal reaction of a cobalt compound with the red phosphorus.

12. The process of claim 11, wherein the hydrothermal reaction of the cobalt compound with the red phosphorus is carried out at a temperature ranging from 150 °C to 200 °C for 12-24 hours, preferably about 200 °C for 12 hours-20 hours, more preferably about 200 °C for about 12 hours.

13. The process of claim 11 or 12, wherein the cobalt compound is selected from the group consisting of cobalt acetate, cobalt chloride, potassium cobalt cyanide and a combination thereof.
14. The process of any one of claims 10-13, wherein the red phosphorus used in step a) is an amorphous red phosphorus.

15. The process of any one of claims 11-14, wherein a molar ratio of the red phosphorus to the cobalt compound used in step a) is 50-2000:1, preferably 100-600:1, more preferably 400-600:1.

16. The process of any one of claims 10-15, wherein a molar concentration of the red phosphorus in water in step a) is 0.1-1M, preferably 0.2-0.4M.

17. The process of any one of claims 10-16, wherein the CoP$_2$ loaded red P in step b) is thermally treated at a temperature ranging from about 450 °C to about 650 °C for about 2 hours - about 15 hours, preferably at about 450 °C to about 500 °C for about 2 hours - about 15 hours, more preferably at a temperature of about 450 °C for about 5 hours - about 12 hours.

18. The process of claim 10 or 17, wherein the CoP$_2$ loaded red P in step b) is thermally treated under vacuum.

19. The process of claim 10, wherein the method further comprises a step of purifying the red phosphorus before growing CoP$_2$ from the red phosphorus in water.

20. The process of claim 19, the red phosphorus is purified in water by a hydrothermal method at a temperature of about 200 °C.

21. A use of CoP$_2$ as a co-catalyst for a red phosphorus.

22. The use of claim 21, wherein CoP$_2$ is loaded onto the red phosphorus at about 0.5 % to about 7.0 % by weight, preferably about 1.0 % to about 4.0 % by
weight, more preferably about 2.0 % to about 4.0 % by weight, most preferably about 2.0 % by weight.

23. The use of claim 21 or 22, wherein the red phosphorus is a crystalline red phosphorus.
Fig. 1
INTERNATIONAL SEARCH REPORT

International application No. PCT/CN2013/001055

A. CLASSIFICATION OF SUBJECT MATTER

See the extra sheet
According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC: B01J, C01B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

CNPAT, CNKI, WPI, EPDOC, GOOGLE SCHOLAR: cobalt phosphide?, red phosphorus, CoP₂, photocataly+, co-catalyst, cobalt, Co, P, phosphorus, hydrothermal synthesis, hydrothermal reaction, carrier, hydrogen, water

C. DOCUMENTS CONSIDERED TO BE RELEVANT

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<td>A</td>
<td>CN 102029169 A (DALIAN INSTITUTE OF CHEMICAL PHYSICS, CHINESE ACADEMY OF SCIENCES) 27 April 2011 (27.04.2011) the whole document</td>
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* Special categories of cited documents:
  'A' document defining the general state of the art which is not considered to be of particular relevance
  'E' earlier application or patent but published on or after the international filing date
  'L' document which may throw doubts on priority claim (S) or which is cited to establish the publication date of another citation or other special reason (as specified)
  'O' document referring to an oral disclosure, use, exhibition or other means
  'P' document published prior to the international filing date but later than the priority date claimed

'B' later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

'C' document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

'D' document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

Note: The table above shows the relevant claims and documents cited in the international search report.

Date of the actual completion of the international search: 18 November 2013 (18.11.2013)


Name and mailing address of the ISA/CN
The State Intellectual Property Office, the P.R.China
6 Xitucheng Rd., Jimen Bridge, Haidian District, Beijing, China 100088
facsimile No. 86-10-62019451

Authorized officer: PAN, Hui
Telephone No. (86-10) 4769

Form PCT/ISA/210 (second sheet) (July 2009)
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### INTERNATIONAL SEARCH REPORT

**Information on patent family members**

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B01J27/18(2006.01)i
B01J23/75(2006.01)i
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C01B25/08(2006.01)i