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CA 2193607 C 2005/05/03

(11)(21) **2 193 607**

(12) **BREVET CANADIEN  
CANADIAN PATENT**

(13) **C**

(22) Date de dépôt/Filing Date: 1996/12/20

(41) Mise à la disp. pub./Open to Public Insp.: 1997/06/21

(45) Date de délivrance/Issue Date: 2005/05/03

(30) Priorité/Priority: 1995/12/21 (195 47 907.6) DE

(51) Cl.Int.<sup>6</sup>/Int.Cl.<sup>6</sup> C08J 3/12, B29B 13/10, B29C 67/04

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(54) Titre : POUDRES A MOULER DE POLYTETRAFLUOROETHYLENES MODIFIES QUI NE S'ECOULENT PAS  
LIBREMENT

(54) Title: NON-FREE FLOWABLE MOLDING POWDERS OF MODIFIED POLYTETRAFLUOROETHYLENES

(57) Abrégé/Abstract:

Non-free flowable, non-dusting molding powders with a bulk density of more than 450 g/l are obtained when a suspension polymer of tetrafluoroethylene with a content of 0.01 to 1 % by weight of units of at least one perfluoro(alkyl-vinyl) ether is ground to a particle diameter of 10 to 50 µm and agglomerated in water.



**Abstract**

**Non-free flowable molding powders of modified polytetrafluoroethylenes**

Non-free flowable, non-dusting molding powders with a bulk density of more than 450 g/l are obtained when a suspension polymer of tetrafluoroethylene with a content of 0.01 to 1 % by weight of units of at least one perfluoro(alkyl-vinyl) ether is ground to a particle diameter of 10 to 50  $\mu\text{m}$  and agglomerated in water.

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## Non-free flowable molding powders of modified polytetrafluoroethylenes

### Description

5 The invention relates to non-free flowable (non-pourable) molding powders of a suspension polymer with units of tetrafluoroethylene and 0.01 to 1 % by weight, preferably 0.02 to 0.5 % by weight, of units of at least one  
10 perfluoro(alkyl-vinyl) ether with an alkyl group of 1 to 4 carbon atoms, preferably n-perfluoropropyl, having a bulk density of at least 450 g/l, obtainable by grinding the primary particles to an average particle diameter  $d_{50}$  of 10 to 50  $\mu\text{m}$ , preferably 15 to 25  $\mu\text{m}$ , in particular about 20  $\mu\text{m}$ , and reagglomerating these particles in water  
15 to give a non-dusting agglomerate having a particle diameter  $d_{50}$  of about 30 to about 100  $\mu\text{m}$ , preferably about 40 to about 90  $\mu\text{m}$ .

The invention furthermore relates to a process for the preparation of a non-free flowable, non-dusting molding  
20 powder having a bulk density of at least 450 g/l and an agglomerate diameter  $d_{50}$  of about 30 to about 100  $\mu\text{m}$ , preferably about 40 to about 90  $\mu\text{m}$ , which comprises grinding a suspension polymer with units of tetrafluoroethylene and 0.01 to 1 % by weight of units of at least  
25 one perfluoro(alkyl-vinyl) ether with an alkyl group of 1 to 4 carbon atoms to a particle diameter  $d_{50}$  of 10 to 50  $\mu\text{m}$  and agglomerating the particles in water.

The invention furthermore relates to the use of the molding powders according to the invention in compression  
30 molding or compaction sintering.

As is known, polytetrafluoroethylene (PTFE) can be prepared by aqueous free radical polymerization by two

different processes, that is to say suspension and emulsion polymerization. These two processes naturally lead to polymers which differ fundamentally in morphological terms. As a consequence, the two processes also  
5 require fundamentally different working up and processing methods.

The emulsion polymers comprise largely regular, spherical latex particles having a diameter of about 100 to 300 nm, which are agglomerated by a precipitation process to give  
10 a so-called paste powder having an average particle diameter of 400 to 700  $\mu\text{m}$ . The specific surface area of such paste powders is 10 to 25  $\text{m}^2/\text{g}$ . These paste powders are further processed by the so-called paste extrusion process to give liners, tubes, hoses and tapes. The  
15 characteristic of paste extrusion is that shaping is carried out by forming a paste of the paste powder with gasoline (benzine) or other liquids which are water-immiscible but wet PTFE, using a paste extruder at far below the melting point of the PTFE. This shaping  
20 extrusion is usually followed by sintering at temperatures significantly above the melting point of the PTFE. PTFE emulsion polymers therefore cannot be processed as thermoplastics because of their exceptionally high melt viscosity of up to a few 100 GPas.

25 PTFE suspension polymers also cannot be processed as thermoplastics because of their high melt viscosity. Special processing techniques based on the method of metallurgical compaction sintering have therefore been developed. For this compaction sintering, the suspension  
30 polymer must be converted into a molding powder which can be employed.

For this purpose, the suspension polymer, which is obtained in coarse, irregularly shaped grains having a diameter of up to 1500  $\mu\text{m}$ , is first finely ground to a  
35 particle diameter of about 10 to 50  $\mu\text{m}$ , preferably by dry grinding, in particular in an air mill. The ground



material is also irregularly shaped. The molding powder thus produced is therefore not free-flowable and cannot be metered adequately for automatic processing by compaction. The bulk density is about 300 to 400 g/l.

5 This non-free flowable molding powder is chiefly compacted to cylinders or hollow cylinders under pressures of up to about 500 bar. These unsintered preforms (green compacts) are then sintered and commodity articles such as skived films or sealing rings are then  
10 produced by mechanical processing. To achieve high-grade final properties, the molding powder must have an adequate deformability during the production of the green compact, so that the primary particles can be packed densely against one another without inclusions of air and  
15 the green compact thus has an adequate so-called green strength for further processing.

In addition to being unusable for automatic processing by compaction and the difficulties in reliable filling of molds, the non-free flowable molding powder has the  
20 further disadvantage of a low bulk density. This means that larger shaping units are necessary. Another disadvantage is to be seen in the dusting during the production of the green compact. Dusting necessitates greater expenditure on keeping the processing unit clean,  
25 since PTFE dust is regarded as toxic, especially in connection with smoking.

There has therefore been no lack of attempts to eliminate the disadvantages mentioned. Thus, processes which render the molding powder free-flowing (pourable) and easier to  
30 meter by agglomeration processes have been developed. The known agglomeration processes essentially comprise agglomerating the non-free flowable molding powder to more or less regularly shaped granule grains, the average particle diameter of which is between 100 and 600  $\mu\text{m}$ , by  
35 a suitable mechanical treatment in a usually two-phase liquid system (comprising water and a solvent of limited

water-miscibility which wets the PTFE, such as gasolines and fluorochlorohydrocarbons). These granule grains are distinguished by a smooth surface and a certain grain stability for their handling and transportation. The free-flowing molding powders thus produced have a high bulk density, usually above 800 g/l, do not dust and accordingly offer considerable advantages over the non-free flowable molding powder.

However, these advantages are at the expense of a significant deterioration in the profile of properties. Thus, the tear strength and dielectric strength are significantly reduced, and the sintered articles have a higher content of voids, that is to say more pores up to so-called "pinholes". The cause of the deterioration in properties is the necessarily poorer compactibility and deformability of the free-flowing powder due to the agglomeration. Thus, for example, the contour lines of the granule grain can be clearly detected in 100  $\mu\text{m}$  thick skived films under a microscope at 20-fold magnification in phase contrast.

The change in properties by granulation of a PTFE molding powder is shown in the following Table 1, the abbreviations here and in the following having the meanings given below:

25	BD:	Bulk density according to DIN 53466 or ISO 12086 in g/l
	$d_{50}$ :	Average particle diameter in $\mu\text{m}$ , measured with a laser particle measuring instrument from Sympatec (Clausthal-Zellerfeld, Germany)
30	TS:	Tear strength in $\text{N/mm}^2$ , according to DIN 53457 or ISO 12086, test specimens: strips 15 mm wide
	EB:	Elongation at break in %, determined according to DIN 53457 or ISO 12086
35	DS:	Dielectric strength in $\text{kV/mm}$ , according to DIN 53481, measurement arrangement ball (diameter 20 mm)/plate (diameter 50 mm)

Table 1

		Powder properties		Properties of 100 $\mu$ m skived films		
		BD	d <sub>50</sub>	TS	EB	DS
	Molding powder, crude	380	18	42	480	110
5	Molding powder, agglomerated	830	450	32	360	80

The deterioration in properties seems inherent to the system, since the particle stability required impedes dense packing of the primary particles and of the granule grains during compaction. This deterioration in properties is also observed during granulation of a molding powder of "modified" PTFE, although to a lesser extent. "Modified" PTFE is understood as meaning a polymer which comprises low contents of comonomers, but in which the main property of the PTFE of not being processable as a thermoplastic is retained. The suspension polymers of tetrafluoroethylene employed according to the invention, with 0.01 to 1 % by weight of units of at least one perfluoro(alkyl-vinyl) ether are such "modified" poly-tetrafluoroethylenes. One characteristic of the modified suspension polymers is their lower melt viscosity by about one to two orders of magnitude, which enables them to be welded, for example, without auxiliaries. Although the lowered melt viscosity leads to a better coalescence of the primary particles during sintering, the disadvantages of agglomeration inherent to the system cannot yet be overcome, as the following Table 2 shows for a suspension polymer with 0.09 % by weight of perfluoro(n-propyl-vinyl) ether.

Table 2

		Powder properties		Properties of 100 $\mu$ m skived films		
		BD	d <sub>50</sub>	TS	EB	DS
	Molding powder, crude	400	18	42	660	110
5	Molding powder, agglomerated	820	450	35	560	85

As can be seen from the skived films, the free-flowable molding powder does not lead to the high profile of properties of the non-free flowable molding powder.

There was therefore the object of developing a molding powder which, although it is non-free flowable, offers processing advantages over the known molding powders, in particular a higher bulk density and dust-free handling during production of the green compacts.

This object is achieved according to the invention by subjecting molding powders of modified suspension PTFE which are known per se to mechanical treatment in the presence of water. Granulating auxiliaries such as organic solvents can be omitted here. Volatile emulsifiers, such as the ammonium salt of perfluorooctanoic acid (perfluorocaproic acid), can be added as auxiliaries, but are not necessary. Regular shaping of the granule grain is consciously omitted here.

Granulation in water as a medium is known for non-modified PTFE from US-A-3 366 615, a free-flowable product being produced.

US-A-3 855 191 relates to a non-free flowable molding powder of modified PTFE which has been produced with relatively large amounts of fluorinated dispersing agent and then ground under wet conditions to a relatively wide



particle size distribution. Such products show an onerous dust development during processing. The possibility of agglomeration in water, organic solvents or a mixture thereof is indeed mentioned, but for the purpose of  
5 improving the free-flowing.

An increase in the bulk density can indeed also be achieved by grinding the polymers to an average particle diameter of  $>50 \mu\text{m}$  and omitting agglomeration. However, these products also show an onerous dust development. If  
10 a product ground to an average particle diameter of  $> 50 \mu\text{m}$  is agglomerated in the context of the invention, skived films which are visually inhomogeneous are obtained from these. The mechanical properties are also significantly poorer than in the case of products  
15 obtained from molding powders according to the invention.

A non-dusting, non-free flowable molding powder of modified suspension PTFE having a high bulk density thus cannot be prepared by the processes known to date, and neither by modifications of the process according to the  
20 invention defined above.

The invention is illustrated in more detail in the following examples.

#### Examples 1 to 4

##### General experimental procedure:

25 A finely ground, modified suspension PTFE (as defined below) is introduced, while stirring, into a cylindrical 15 l glass vessel (160 x 300 mm), fitted with a blade baffle and a 3-blade propeller stirrer and containing 4 l of water, and stirring is continued for 70 minutes. The  
30 agglomerated molding powder thus obtained is separated off from the water by sieving and dried at  $180^{\circ}\text{C}$  in a drying cabinet for 8 hours.

Dusting of the molding powder is evaluated visually by observing the formation of dust from a 500 ml glass bottle half-filled with molding powder when it is turned upside down.

- 5 The final properties are measured on skived films. These originated from a cylindrical block weighing 13 kg which was compacted and sintered in a known manner. The granular material is compacted in layers with the starting material in this block. Changes in the final properties  
10 during agglomeration can therefore be evaluated better.

The properties of starting molding powders are shown in the following Table 3. For comparison, non-modified PTFE is compared here, as "molding powder A" with a PTFE, as  
15 "molding powder B", modified with 0.05 % by weight of perfluoro(n-propyl-vinyl) ether. "Molding powder B" is the starting material for the molding powder according to the invention.

Table 3

	Powder properties		Properties of 100 $\mu$ m skived films		
	BD	d <sub>50</sub>	TS	EB	DS
20 Molding powder A	355	24	40	460	85
Molding powder B	400	24	42.5	525	103

#### Comparison Examples 1 to 4

- 2.5 kg of molding powder A were stirred in 4 l of water  
25 at 1000 rpm. Comparison Examples 3 and 4 were carried out in the presence of 4 g of ammonium perfluorocaprylate. Table 4 shows the results.

Table 4

Comparison example	Tempera- ture [°C]	Powder properties		Properties of 100 $\mu$ m skived films		
		BD	d <sub>50</sub>	TS	EB	DS
1	45	670	62	40	410	70
2	25	490	74	41	490	107
3	45	530	85	39	400	70
4	25	490	86	39	410	75

The molding powders thus obtained do not dust and are not free-flowable. As shown in comparison with Table 1, the final properties are largely retained, but the skived films are visually inhomogeneous, that is to say they show specks of different transparency. Such films are unacceptable for use.

#### Examples 5 to 10

2.5 kg of molding powder of suspension PTFE modified with 0.05 % by weight of perfluoro(n-propyl-vinyl) ether are stirred with 4 l of water at the stirrer speed stated (in rpm). Examples 9 and 10 were carried out in the presence of 4 g of ammonium perfluorocaprylate. Table 5 shows the results.

Table 5

Ex-ample	Tempera- ture [°C]	rpm	Powder properties		Properties of 100 $\mu$ m skived films		
			BD	d <sub>50</sub>	TS	EB	DS
5	23	800	530	41	38.5	550	106
6	45	1200	530	65	40	550	96
7	45	800	585	64	36	500	85
8	25	1000	500	83	42	555	112
9	25	1000	450	43	40	540	108
10	45	1000	560	70	43	565	99

10 All the agglomerated molding powders mentioned do not  
dust and have a significantly increased bulk density. The  
final properties of the skived films are retained com-  
pared with the starting material. The films are visually  
homogeneous and free from pores and therefore of high  
15 quality.

#### Examples 11 and 12

A molding powder which has been modified with 0.1 % by  
weight of perfluoro(n-propyl-vinyl) ether was employed  
here. Stirring was carried out at 1000 rpm. Table 6 shows  
20 the results.

Table 6

Example	Tempera- ture [°C]	Powder properties		Properties of 100 μm skived films		
		BD	d <sub>50</sub>	TS	EB	DS
Starting material		420	24	42	660	110
11	25	555	48	38.5	590	101
12	45	650	67	38	585	99

25 These powders also show the same good properties as the  
products according to Examples 5 to 10.



CLAIMS:

1. A non-free flowable, non-dusting molding powder having a bulk density of at least 450 g/l of a suspension polymer with units of tetrafluoroethylene and 0.01 to 1 % by weight of units of at least one perfluoro(alkyl-vinyl) ether with an alkyl group of 1 to 4 carbon atoms, obtained by grinding the primary particles to an average particle diameter  $d_{50}$  of 10 to 50  $\mu\text{m}$  and reagglomerating these particles in water to give an average agglomerate diameter  $d_{50}$  of about 30 to about 100  $\mu\text{m}$ .
2. A molding powder as claimed in claim 1, wherein the content of perfluoro(alkyl-vinyl) ether is 0.02 to 0.5 % by weight.
3. A molding powder as claimed in claim 1 or 2, which has an average agglomerate diameter  $d_{50}$  of about 40 to about 90  $\mu\text{m}$ .
4. A process for the preparation of a non-free flowable, non-dusting molding powder having a bulk density of at least 450 g/l, which comprises grinding a suspension polymer with units of tetrafluoroethylene and 0.01 to 1 % by weight of units of at least one perfluoro(alkyl-vinyl) ether with an alkyl group of 1 to 4 carbon atoms to a particle diameter  $d_{50}$  of 10 to 50  $\mu\text{m}$  and agglomerating the particles in water to give an average agglomerate diameter  $d_{50}$  of about 30 to about 100  $\mu\text{m}$ .
5. The process as claimed in claim 4, wherein a polymer which has a content of 0.02 to 0.5 % by weight of the ether is employed.

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6. The process as claimed in claim 4 or 5, wherein the polymer is ground to a particle diameter  $d_{50}$  of 15 to 25  $\mu\text{m}$ .
- 5 7. The process as claimed in claims 4 to 6, wherein an agglomerate diameter of about 40 to about 90  $\mu\text{m}$  is established.
8. The use of a molding powder according to any one of claims 1 to 3, in compacton sintering.

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