

P/00/001
Section 29
P/00/008
Section 29(1)
Regulation 3.1(2)

AUSTRALIA
Patents Act 1990

PATENT REQUEST AND NOTICE OF ENTITLEMENT

We **MONTELL NORTH AMERICA INC.**

of **2801 Centerville Road, New Castle County, DELAWARE, U.S.A.**

being the Applicant and Nominated Person, request the grant of a patent for an invention entitled "COMPOSITIONS OF RANDOM COPOLYMERS OF PROPENE CONTAINING AN ALPHA-OLEFIN AS COMONOMER" which is described in the standard complete specification of patent application no. 35138/93.

Giuliano Cecchin and Floriano Guglielmi are the actual inventors of the invention.

The inventors made the invention for and on behalf of Himont Incorporated in the course of their duties as employees of Himont Incorporated. Subsequently Himont Incorporated changed its name to Montell North America Inc.

Convention priority is claimed from the following basic application(s):

Basic Applicant	Application Number	Application Date	Country	Country Code
Himont Incorporated	MI 92 A 000545	10 March 1992	Italy	IT

The basic application was the first application made in a Convention country in respect of the invention the subject of this request.

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DATED this 31st day of May 1995

MONTELL NORTH AMERICA INC.
By their Patent Attorney

GRIFFITH HACK & CO

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COMPOSITIONS OF RANDOM COPOLYMERS OF PROPENE CONTAINING AN ALPHA-OLEFIN AS
COMONOMER
- International Patent Classification(s)
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- (56) Prior Art Documents
US 4822840
US 4302504
US 4211852
- (57) Claim

1. A semicrystalline polyolefin composition comprising (by weight):

- A) 20-60% of a propene/C₄-C₁₀ α-olefin random copolymer (Fraction A), containing from 1 to 10% of a C₄-C₁₀ α-olefin,
- B) 40-80% of a propene/C₄-C₁₀ α-olefin random copolymer (Fraction B), containing from 15 to 40% of a C₄-C₁₀ α-olefin, same or different from the one present in Fraction A,

wherein the percent by weight of Fraction B (%B), referred to the total composition, and the percent by weight of C₄-C₁₀ α-olefin in Fraction B (C₄^B) satisfy the following relation:

$$\%B \bullet C_4^B \geq 1200;$$

said polyolefin composition having a melting point from 135 to 150°C, a fraction soluble in xylene at 25°C less than 20% by weight, a flexural modulus higher than 700 MPa, and a heat sealing temperature from 90° to 105°C and being a physical blend of A) and B).

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7. A process for the preparation of composition of claim 1, wherein the monomers are polymerized in the presence of stereospecific catalysts supported on active magnesium dihalides in active form, in at least two separate and sequential stages, where Fractions A and B are formed, and each stage is carried out in the presence of the polymer formed and the catalyst used in the immediately preceding stage, said catalyst containing a solid catalyst component comprising a titanium compound having at least one titanium-halogen bond and an internal electron-donor selected from ethers, ketones, lactones, compounds containing N, P and/or S atoms, and esters of mono- and dicarboxylic acids, both supported on magnesium dihalides in active form, said catalyst also containing an Al- alkyl compound, selected from trialkyl-aluminium, AlR_2H and AlR_2OR^1 as a co-catalyst, wherein R is an alkyl radical having 1 to 6 carbon atoms and R^1 represents an aryl radical optionally substituted in one or more positions, and an external electron-donor selected from esters of aromatic carboxylic acids, heterocyclic compounds and silicon compounds containing at least one Si-OR bond, wherein R is a hydrocarbon radical, said catalyst being capable of producing polypropylene having an isotactic index higher than 90.

P/00/011
Regulation 3.2

AUSTRALIA
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664598

ORIGINAL
COMPLETE SPECIFICATION
STANDARD PATENT

Invention Title: COMPOSITIONS OF RANDOM COPOLYMERS OF
PROPENE CONTAINING AN ALPHA-OLEFIN AS
COMONOMER

The following statement is a full description of this invention, including
the best method of performing it known to us:

GH&CO REF: P18765-BB:RPW:RK

The present invention concerns compositions of random copolymers of propene comprising one or more C₄-C₁₀ α -olefins as comonomer, and the process to obtain said compositions.

The copolymer compositions described below are adequate for the production of heat-sealable film that can be used as such thanks to their mechanical and physical properties, or in the preparation of multilayer films obtained, for example, by way of coextrusion with polypropylene. Moreover, said compositions can also be used in the food industry because of their low content of component soluble in xylene at room temperature.

The use of compositions of copolymers of propene with an olefin, mainly ethylene and/or 1-butene, or their blends with other olefin polymers, for the preparation of heat-sealable materials is known in the art.

U.S. patent no. 4,481,336 describes compositions made up of two propene/ethylene and/or butene copolymer fractions, said compositions having heat-sealable, clarity, and nonsticking properties. Said patent teaches that the butene content in the copolymeric fraction present in lower quantities must be greater than 25% by weight with respect to the total monomers, and the quantity of propene must be less than 75% by weight. If said quantities are not adhered to as regards respectively the lower and upper limits, the composition obtained would have poor heat sealability. Moreover, the film obtained by using

said compositions should not be oriented, otherwise the portion of the film subjected to sealing could shrink during the heat-sealing process.

U.S. patent no. 4.822.840 describes copolymer compositions comprising propene/ethylene/ α -olefins random copolymers. The propene is the principal component, and the ethylene is present in quantities ranging from 0.2 to 3.5% by weight.

Italian patent application n. 21601 A/90 concerns a composition comprising a copolymer of propene with an α -olefin, and, preferably, an ethylene/propene copolymer as the second copolymer.

However, the compositions known up to now have characteristics which are not adequate for some of the uses for which said compositions are destined. The disadvantages of said compositions are due to a heat-seal temperature which is not sufficiently low, a solubility in xylene at 25°C which is too high, and a low crystallinity.

It is well known to those of ordinary skill in the art that in order to obtain compositions with a low heat-sealing temperature, they must also have a low melting point.

A new composition has now been found having low solubility in xylene and lower heat-sealing temperature, but a high melting point.

A particular advantage of the copolymer compositions of the present invention is that they are particularly useful for

the production of laminated mono- or bioriented films having a low heat-sealing temperature.

A further advantage of the copolymer compositions of the present invention is their rigidity. Said compositions are much more rigid compared to the compositions known in the art.

The present invention provides semicrystalline compositions comprising (by weight):

- A) 20-60% of a propene/C₄-C₁₀ α -olefin random copolymer (Fraction A), containing from 1 to 10% of a C₄-C₁₀ α -olefin,
- B) 40-80% of a propene/C₄-C₁₀ α -olefin random copolymer (Fraction B), containing from 15 to 40% of a C₄-C₁₀ α -olefin, same or different from the one present in Fraction A,

where the percent by weight of Fraction B (%B), referred to the total composition, and the percent by weight of C₄-C₁₀ α -olefin in Fraction B (C₄^B) satisfy the following relation:

$$\%B \cdot C_4^B \geq 1200.$$

The preferred semicrystalline polyolefin compositions are those where Fraction A constitutes 25-50% by weight and Fraction B 50-75% by weight.

The preferred C₄-C₁₀ α -olefins are 1-butene, 1-pentene, 1-hexene, 1-octene, and 4-methyl-1-pentene. Particularly preferred is 1-butene.

The preferred percent of C₄-C₁₀ α -olefins in Fraction A

is from 3 to 8% by weight, while in Fraction B the preferred percent is from 20 to 30% by weight.

The properties of the compositions of the invention are as follows:

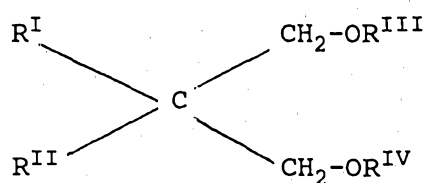
melting point: from 135° to 150°C; fraction soluble in xylene at 25°C: less than 20%, preferably less than 16%; flexural modulus: higher than 700 MPa; heat sealing temperature: from 90° to 105°C.

The compositions of the invention are preferably prepared by way of sequential polymerization of the monomers in the presence of Ziegler-Natta stereospecific catalysts supported on magnesium dihalides in active form. Said catalysts contain, as an essential element, a solid catalyst component comprising a titanium compound having at least one titanium-halogen bond, and an electron-donor compound, both supported on magnesium dihalides in active form. The magnesium dihalide support is present preferably in the form of spheroidal particles having a narrow particle size distribution.

The catalysts used in the process of the invention are characterized by the fact that they are capable of producing polypropylene having an isotactic index higher than 90, preferably higher than 95. Catalysts which have the above mentioned characteristics are well known in patent literature. Particularly useful are the catalysts described in U.S. patent no. 4,339,054, and European patent no. 45,977. Other examples

of suitable catalysts are described in U.S. patents no. 4,472,524 and 4,473,660.

The solid catalyst components used in the preparation of said catalysts contain, as electron-donor, compounds selected from ethers, ketones, lactones, compounds containing N, P, and/or S atoms, and esters of mono- and dicarboxylic acids. Particularly suitable are the esters of phthalic acid, such as diisobutyl, dioctyl, and diphenyl phthalate, and monobutyl monobenzyl phthalate; the esters of malonic acid, such as diisobutyl and diethyl malonate; the aryl and alkyl pivalates; the alkyl, cycloalkyl and aryl maleates; the alkyl and aryl carbonates, such as diisobutyl carbonate, monoethyl monophenyl carbonate, and diphenyl carbonate; the esters of succinic acid, such as mono- and diethyl succinate. Other particularly suitable electron-donors are the 1,3-diethers of formula (I)



where R^{I} and R^{II} , are the same or different, and are $\text{C}_1\text{-C}_{18}$ alkyl, $\text{C}_3\text{-C}_{18}$ cycloalkyl, or $\text{C}_6\text{-C}_{18}$ aryl radicals; R^{III} and R^{IV} , are the same or different, and are alkyl radicals having from 1 to 4 carbon atoms.

The ethers of the type described are illustrated in European patent application no. 361,493.

Examples representative of the ethers of formula (I) are

2-methyl-2-isopropyl-1,3-dimethoxypropane, 2,2-diisobutyl-1,3-dimethoxypropane, and 2-isopropyl-2-cyclopentyl-1,3-dimethoxypropane.

The catalyst components illustrated are prepared according to various methods. One of them consists of milling or co-milling the magnesium dihalide (anhydrous, containing less than 1% of water) with the titanium compound and the electron-donor compound, under conditions which cause the activation of the magnesium dihalide; thereafter, the milled product is treated one or more times with an excess of TiCl_4 at a temperature ranging from 80° to 135°C , and then washed repeatedly with a hydrocarbon (hexane, for example) until no more chlorine ions can be found in the wash water.

According to another method, the anhydrous magnesium dihalide is first preactivated using known methods, then it is reacted with an excess of TiCl_4 containing the electron-donor compound in solution. The operation takes place at a temperature ranging from 80° to 135°C . Optionally the treatment with TiCl_4 can be repeated. The solid is then washed with hexane, or other hydrocarbon solvents, in order to eliminate all traces of nonreacted TiCl_4 .

Another method is based on the reaction between a $\text{MgCl}_2 \cdot n\text{ROH}$ adduct (particularly in spheroidal particle form), where n is generally a number from 1 to 3 and ROH is ethanol, butanol, or isobutanol, and an excess of TiCl_4 containing the

electron-donor compound in solution. The reaction temperature generally ranges from 80 to 120°C. The solid is then separated and caused to react one or more times with TiCl_4 , then washed with a hydrocarbon solvent in order to eliminate all traces of nonreacted TiCl_4 . An alternative method consists of reacting the magnesium alcoholates and chloro-alcoholates (the latter prepared in particular according to the method described in U.S. patent no. 4,220,554), with an excess of TiCl_4 containing the electron-donor compound in solution, operating under the same reaction conditions described above.

Generally, the titanium compound in the solid catalyst component, expressed as Ti content, is present from 0.5 to 10% by weight, and the quantity of electron-donor compound which remains fixed on the solid component (internal donor), generally ranges from 5 to 20% in moles with respect to the magnesium dihalide.

The titanium compounds which can be used for the preparation of the solid catalyst component (a) are the titanium halides and the halo-alcoholates. Titanium tetrachloride is the preferred compound.

Satisfactory results can be obtained also with titanium trihalides, particularly TiCl_3HR , TiCl_3ARA , and titanium halo-alcoholates, such as TiCl_3OR , where R is a phenyl radical.

The reactions indicated above bring to the formation of magnesium dihalide in active form. Besides these reactions,

other reactions are known in the art which cause the formation of activated magnesium halide starting from magnesium compounds different from the magnesium halides, such as carboxylates of magnesium, for example.

The active form of the magnesium dihalides in the solid catalyst components is revealed by the fact that in the X-ray spectrum of the catalyst component the major intensity reflection shows a half-peak breadth at least 30% greater than the one of the major intensity reflection which appears in the unactivated Mg dihalide spectrum, or by the fact that the major intensity reflection, which appears in the spectrum of the unactivated magnesium dihalide (having a surface area smaller than 3 m²/g), is no longer present, but in its place there is a halo with the intensity maximum shifted with respect to the position of the major intensity reflection of the unactivated magnesium dihalide.

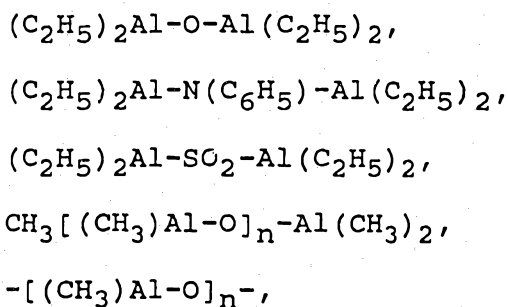
The most active forms are those where the above mentioned halo appears in the X-ray spectrum.

Among the magnesium halides, the chloride is the preferred compound. In the case of the most active forms of magnesium chloride, the X-ray spectrum of the catalyst component shows a halo instead of the reflection which in the spectrum of the unactivated magnesium chloride appears at a distance of 2.56 Å.

The Al-alkyl compounds used as co-catalysts are of the

trialkyl aluminum type, such as Al-triethyl, Al-triisobutyl, Al-tri-n-butyl, and linear or cyclic Al-alkyl compounds containing two or more Al atoms bonded by way of O or N atoms, or SO₂, SO₃ and SO₄ groups.

Some examples of these compounds are:

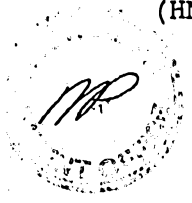


where n is a number from 1 to 20.

One can also use AlR₂H compounds, and AlR₂OR' compounds, where R is an alkyl radical having from 1 to 6 carbon atoms, and R' represents an aryl radical ^{optionally} substituted in one or more positions.

The Al-alkyl compound is generally present in such quantities that the Al/Ti ratio ranges from 1 to 1000.

The electron-donor compounds which can be used as external donors (added together with the Al-alkyl compound) comprise the esters of aromatic acids (such as alkyl benzoates), heterocyclic compounds (such as 2,2,6,6-tetramethylpiperidine, and 2,6-diisopropylpiperidine) and particularly silicon compounds containing at least one Si-OR bond (where R is a hydrocarbon radical). Some examples of silicon compounds are: (t-C₄H₉)₂Si(OCH₃)₂, (C₆H₁₁)₂Si(OCH₃)₂, and (C₆H₅)₂Si(OCH₃)₂.



The 1,3-diethers of formula (I) can also be used advantageously as external donors. In the case where the internal donor is one of the 1,3-diethers of formula (I) the external donor can be omitted.

The polymerization is carried out in at least two stages, during which Fractions A and B of the present invention are prepared. The fractions are formed in separate and in sequential stages. In each stage the operation takes place in the presence of the polymer obtained and the catalyst used in the preceding stage. The order in which Fractions A and B are prepared is not important, however, it is preferred to prepare first Fraction A and then Fraction B.

The polymerization process can be carried out in liquid phase, in the presence or absence of inert solvent, or in gas phase, or using mixed liquid and gas phases. The preferred process is the one which is carried out in gas phase.

The length and temperatures of polymerization during the polymerization stages are not critical; at any rate the preferred temperature range is from 20° to 100°C.

The regulation of the molecular weight is done by using known regulators, preferably hydrogen.

The polymerization process can be preceded by a prepolymerization process where the catalyst is caused to contact with small quantities of olefins.

The following examples illustrate, but do not limit, the

methods of preparation and the characteristics of the composition of the present invention.

Preparation of the solid catalyst component

The solid catalyst component used is prepared from a $\text{MgCl}_2 \cdot 3\text{C}_2\text{H}_5\text{OH}$ adduct produced as follows: in inert atmosphere one introduces in a flask immersed in a bath with the temperature maintained at 120°C , under agitation, 28.4 g of anhydrous MgCl_2 , 49.5 g of pure anhydrous ethanol, 100 ml of ROL OB/30 vaseline oil, 100 ml of silicon oil (viscosity = 350 cs), until the MgCl_2 is dissolved. Thus the MgCl_2 adduct with ethanol in a mixture with the oils is formed. The hot reaction mix is then transferred in an inert atmosphere to a 1500 ml vessel equipped with heating jacket, containing 150 ml of vaseline oil and 150 ml of silicon oil. The mixture is maintained at 120°C while the contents are stirred by way of an Ultra Turrax T-45 N agitator of the Janke & Kunkel K.G. Ika Werke. The stirring continues for 3 minutes at 3000 rpm. The mixture is then discharged into a 2 liter vessel containing 1000 ml of anhydrous n-heptane, kept under agitation and cooled in such a way that the temperature does not exceed 0°C . The microspheres of $\text{MgCl}_2 \cdot 3\text{C}_2\text{H}_5\text{OH}$ thus obtained are recovered by filtration and dried under vacuum at room temperature. The resulting adduct is then dealcoholated by gradually increasing the temperature from 50° to 100°C under nitrogen flow until the alcohol content goes down to 1.5 moles per mole of MgCl_2 . The

partially dealcoholated adduct has a surface area of $9.1 \text{ m}^2/\text{g}$ and an apparent density of 0.564 g/cm^3 .

25 g of said adduct are added to 625 ml of TiCl_4 while under agitation at 0°C . It is then heated to 100°C in one hour. When the temperature reaches 40°C one adds diisobutyl phthalate in a magnesium/diisobutylphthalate molar ratio equal to 8.

The contents of the reactor are heated to 100°C for two hours, then the solids are allowed to settle, and the hot liquid is syphoned off. The solid is washed six times using 200 ml of anhydrous hexane at 60°C , and finally three times at room temperature. The solid, after having been dried under vacuum, has the following characteristics:

- porosity: $0.261 \text{ cm}^3/\text{g}$,
- surface area: $66.5 \text{ m}^2/\text{g}$,
- bulk density: 0.55 g/cm^3 .

Examples 1, 2, 3, 4, and comparative examples 1c and 2c

General operating methods

The polymerization tests have been carried out in a 22 liter stainless steel autoclave equipped with magnetic helical agitator rotating at about 90 rpm.

The gas phase is analyzed in continuous by way of a process gas-chromatograph in order to determine the concentration of 1-butene, propylene and hydrogen. During the polymerization, the 1-butene, propylene, and hydrogen are fed

using flow-meter regulators in order to maintain a constant concentration in the gas phase.

The reaction is carried out at constant temperature and pressure, unless otherwise specified.

The batch operation is conducted in two stages, both in gas phase: during the first stage one carries out the copolymerization of the propylene with the 1-butene to obtain fraction A, during the second stage one carries out the polymerization of the same comonomers to obtain fraction B.

1st stage: at room temperature one introduces in the autoclave in order: a) the proper quantities of propylene, 1-butene, and hydrogen in order to obtain the desired composition of the gas phase and the desired pressure; b) the catalyst system consisting of a solid component (about 1 g), prepared as described above, and of a blend comprising 25 ml of a 25% triethylaluminum (TEAL) solution in hexane and a quantity of dicyclopentyldimethoxysilane (DCPMS) that brings the TEAL/DCPMS molar ratio to 8. The catalyst system is injected into the reactor by way of propylene pressure. The temperature is then brought to operating level (in about 10 minutes) and the reaction continues for the desired time. The residual monomers are eliminated by degassing at 60°C at atmospheric pressure, and a sample of the copolymer is taken from a discharge valve situated at the bottom of the autoclave and sent to be analyzed. The operation lasts about 10 minutes.

2nd stage: one reintroduces in the reactor in order the propylene, 1-butene, and hydrogen in the ratio and quantities needed to obtain the desired composition and pressure of the gas phase, and then the reaction is continued for the proper length of time, which varies according to the reactivity of the catalyst system and the percent of fraction B desired.

At the end of the polymerization test the polymer is discharged from the bottom of the autoclave, stabilized with pentaerythrityl tetrakis[3-(3,5-di-tert-butyl-4-hydroxyphenyl)propanoate] (0.2% by weight), and 2,6-di-tert-butyl-para-cresol (BHT) (0.2% by weight), and dried in an oven under nitrogen flow at 60°C.

The percent by weight of Fractions A and B (%A and %B respectively) with respect to the final composition, the percent by weight of the butene contained in Fraction B (C_4^B), and the intrinsic viscosity of Fraction B (I.V.^B) have been calculated by using the following formulas:

$$\%A = Cl_F / Cl_A,$$

$$C_4^B = [C_4^F - (\%A \cdot C_4^A / 100)] \cdot 100 / \%B,$$

$$I.V.^B = [I.V.^F - (\%A \cdot I.V.^A / 100)] \cdot 100 / \%B,$$

where:

- Cl_F and Cl_A represent, respectively, the chlorine content (from the catalytic residues) of the final composition and of fraction A;
- C_4^F and C_4^A represent, respectively, the percent by

weight of butene contained in the final composition and in fraction A;

- I.V.^F and I.V.^A represent, respectively, the intrinsic viscosity of the final composition and fraction A.

All the tests which have been conducted and relative operating conditions are set forth in Tables 1 and 2, while in Table 3 are shown the data regarding the polymerization yield and characteristics of the final compositions.

The following analytical methods have been used to characterize the compositions of the examples:

- 1-butene content: determined by IR spectroscopy;
- melting point: determined by DSC;
- fraction soluble in xylene: determined by solubilizing a sample of the material in xylene at 125°C, then cooling it to room temperature. The soluble and insoluble fractions are separated by filtration;
- melt index: determined according to method ASTM D 1238, condition L;
- Intrinsic viscosity: determined in tetrahydronaphthalene at 135°C;
- haze: determined according method ASTM D 1003 on 1mm thick specimens;
- seal initiation temperature: determined by preparing 50 µm thick films by extruding the compositions of the examples at about 200°C. Each film thus obtained is laid over a film of

polypropylene having an isotactic index of 97 (in boiling n-heptane), melt index of 4.5 g/10 minutes, said film having thickness of 560 μm . The overlapped films are bonded in a plate-press at 200°C with a load of 9000 Kg. Said load is maintained for 5 minutes. The resulting bonded films are then been stretched to six times their length and width using a TM LONG film stretcher, thus obtaining films of a thickness of about 20 μm . 5x10 cm. specimens are obtained from said films. The sealing values are obtained by applying a 200 g load to heat-sealed samples. For each measurement two of the above specimens are overlapped with the heat-sealable layers, made up of the compositions of the examples, touching each other. Said overlapped specimens are then sealed along the 5 cm. side using a XENTINEL combination laboratory sealer model 12-12 AS. The sealing time is 5 seconds, the pressure 1.2 atm and the width of the seals 2.5 cm. The sealing temperature is increased by 2°C for each sample to be measured. The sealed samples are then cut to obtain 2.5x10 cm strips, whose unsealed ends is attached to a dynamometer, and the minimum seal temperature where the seal does not break when a 200 g load is applied is determined. This overlapped specimens temperature represents the seal initiation temperature (S.I.T.).

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TABLE 1 - FRACTION A

Example n.	1	2	3	4	1c	2c
Temperature °C	60	60	60	60	60	60
Pressure bar	8.8	8.9	8.7	8.8	8.7	8.8
Time min.	120	80	120	60	120	90
1-butene _(gas phase) % moles	8.75	8.63	9.1	9.03	8.9	6.4
H _{2(gas phase)} % moles	1.4	3.0	0.4	1.23	1.8	1.5
Polymer % by weight	50	45	52.1	28.8	61.5	65.1
1-butene % by weight	6.85	6.66	7.68	7.67	7.27	5.06
I.V. dl/g	1.70	1.34	2.33	1.76	1.52	1.66
Sol. xyl. % by weight	1.0	1.7	1.4	1.0	1.3	1.3
Melting point °C	151.0	154.0	149.6	149.5	150.0	154.6

TABLE 2 - FRACTION B						
Example n.	1	2	3	4	1c	2c
Temperature °C	60	60	60	60	60	60
Pressure bar	8.85	8.77	9.0	9.6	9.35	9.20
Time min.	190	180	100	270	120	120
1-butene _(gas phase) % moles	33.2	33.4	32.7	21.8	23.1	26.3
H _{2(gas phase)} % moles	1.4	0.4	3.0	1.0	2.47	1.43
Polymer % by weight	50	55	47.9	71.2	38.5	34.9
1-butene % by weight	30.3	28.49	26.72	21.22	22.37	26.67
I.V. dl/g	1.75	1.94	1.76	1.96	1.84	2.10

TABLE 3 - FINAL COMPOSITION

Example n.	1	2	3	4	1c	2c
Yield kg _{polymer} /g _{cat}	4.1	4.7	4.0	6.0	3.3	4.14
MIL g/10 min.	5.4	7.3	2.9	3.3	2.7	5.6
I.V. dl/g	1.72	1.67	2.06	1.90	2.04	1.81
1-butene % by weight	18.58	18.67	16.80	17.31	13.09	12.60
Sol. Xyl. 25°C	15.3	15.2	13.8	7.2	4.1	6.4
Melting point °C	146.4	148.3	146.2	141.4	145.5	154.7
S.I.T. °C	96	98	102	100	110	110
Flexural Modulus MPa	980	1150	1010	970	1050	1180
Haze %	31.6	39.2	32.3	17.5	35.3	27.9
Appearance	spheres	spheres	spheres	spheres	spheres	spheres
%B · C ₄ ^B	1500	1560	1280	1510	860	930

THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:

1. A semicrystalline polyolefin composition comprising (by weight):

5 A) 20-60% of a propene/C₄-C₁₀ α-olefin random copolymer (Fraction A), containing from 1 to 10% of a C₄-C₁₀ α-olefin,

B) 40-80% of a propene/C₄-C₁₀ α-olefin random copolymer (Fraction B), containing from 15 to 40% of a C₄-C₁₀ α-olefin, same or different from
10 the one present in Fraction A,

wherein the percent by weight of Fraction B (%B), referred to the total composition, and the percent by weight of C₄-C₁₀ α-olefin in Fraction B (C₄^B) satisfy the following relation:

15 %B • C₄^B ≥ 1200;

said polyolefin composition having a melting point from 135 to 150°C, a fraction soluble in xylene at 25°C less than 20% by weight, a flexural modulus higher than 700 MPa, and a heat sealing temperature from 90° to 105°C and
20 being a physical blend of A) and B).

2. The composition of claim 1, wherein the C₄-C₁₀ α-olefins of Fractions A and B are the same.

3. The composition of claim 1, where Fraction A is present in an amount from 25 to 50% by weight and
25 Fraction B from 50 to 75% by weight.

4. The composition of claim 1 wherein the C₄-C₁₀ α-olefin is selected from the group consisting of 1-butene, 1-pentene, 1-hexene, 1-octene, and 4-methyl-1-pentene.

5. The composition of claim 1 wherein the percent
30 of C₄-C₁₀ α-olefin in Fraction A is from 3 to 8% by weight.

6. The composition of claim 1 wherein the percent of C₄-C₁₀ α-olefin in Fraction B is from 20 to 30% by weight.

35 7. A process for the preparation of composition of claim 1, wherein the monomers are polymerized in the presence of stereospecific catalysts supported on active magnesium dihalides in active form, in at least two



separate and sequential stages, where Fractions A and B are formed, and each stage is carried out in the presence of the polymer formed and the catalyst used in the immediately preceding stage, said catalyst containing a solid catalyst component comprising a titanium compound having at least one titanium-halogen bond and an internal electron-donor selected from ethers, ketones, lactones, compounds containing N, P and/or S atoms, and esters of mono- and dicarboxylic acids, both supported on magnesium dihalides in active form, said catalyst also containing an Al- alkyl compound, selected from trialkyl-aluminium, AlR_2H and AlR_2OR^1 as a co-catalyst, wherein R is an alkyl radical having 1 to 6 carbon atoms and R^1 represents an aryl radical optionally substituted in one or more positions, and an external electron-donor selected from esters of aromatic carboxylic acids, heterocyclic compounds and silicon compounds containing at least one Si-OR bond, wherein R is a hydrocarbon radical, said catalyst being capable of producing polypropylene having an isotactic index higher than 90.

8. The process of claim 7, wherein all the polymerization stages are carried out in a gas phase.

9. The process of claim 7 wherein the first stage is carried out in a liquid monomer, and the second in a gas phase.

10. A semicrystalline polyolefin composition substantially as herein described with reference to any one of the Examples excluding comparative examples 1C and 2C.

11. A process for the preparation of a semicrystalline polyolefin composition substantially as herein described with reference to any one of the Examples excluding comparative examples 1C and 2C.

Dated this 25th day of September 1995

MONTELL NORTH AMERICA INC.

By their Patent Attorney
GRIFFITH HACK & CO



"COMPOSITIONS OF RANDOM COPOLYMERS OF PROPENE CONTAINING AN
 α -OLEFIN AS COMONOMER"

ABSTRACT

Semicrystalline polyolefin composition comprising (by weight):

- A) 20-60% of a propene/ C_4 - C_{10} α -olefin random copolymer (Fraction A), containing from 1 to 10% of a C_4 - C_{10} α -olefin,
- B) 40-80% of a propene/ C_4 - C_{10} α -olefin random copolymer (Fraction B), containing from 15 to 40% of a C_4 - C_{10} α -olefin, same or different from the one present in Fraction A,

where the percentage by weight of Fraction B (%B), referred to the total composition, and the percentage by weight of C_4 - C_{10} α -olefin in Fraction B (C_4^B) satisfy the following relation:

$$\%B \cdot C_4^B \geq 1200.$$