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Harmon et al.

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(54) **MIXING SYSTEM FOR AFTERTREATMENT SYSTEM**

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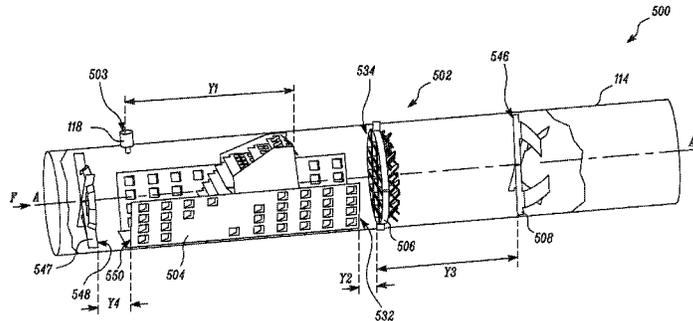
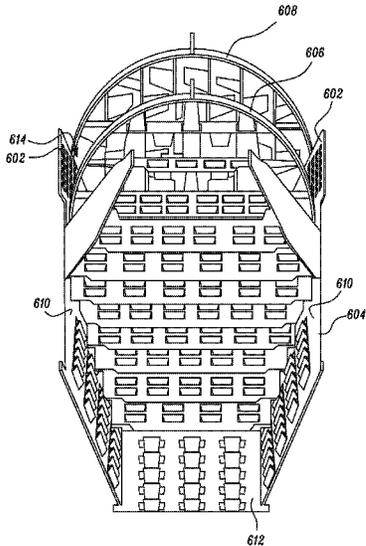
(57) **ABSTRACT**

A mixing system for an aftertreatment system is disclosed. The mixing system includes a mixing tube. The mixing tube is provided in fluid communication with an exhaust conduit. The mixing system also includes a reductant injector positioned at an injection location on the mixing tube. The mixing system further includes a mixer assembly positioned downstream of the injection location. The mixer assembly includes a plurality of mixing elements provided in a series arrangement, such that each of the plurality of mixing elements is provided downstream of one another.

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12 Claims, 10 Drawing Sheets



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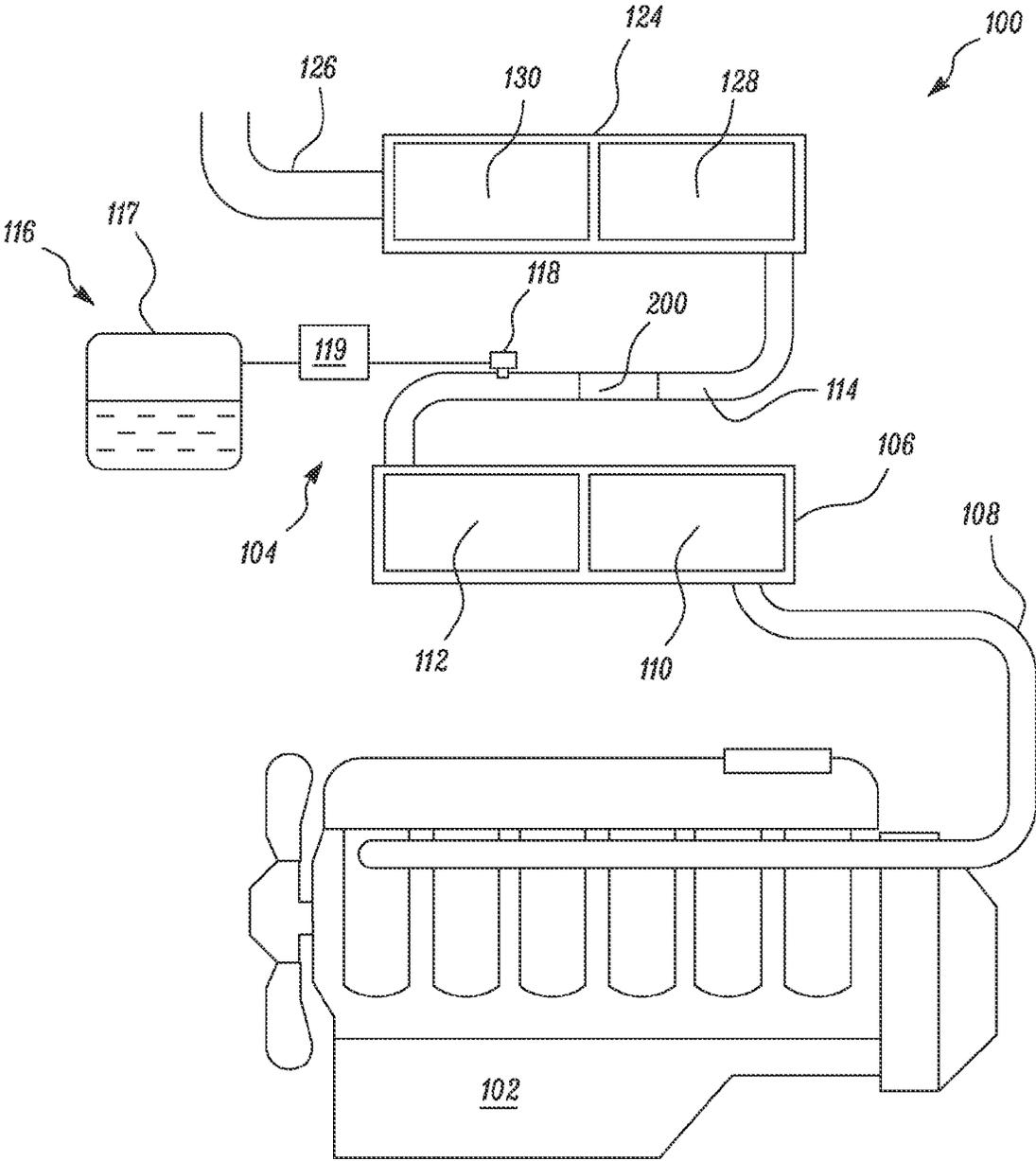


FIG. 1

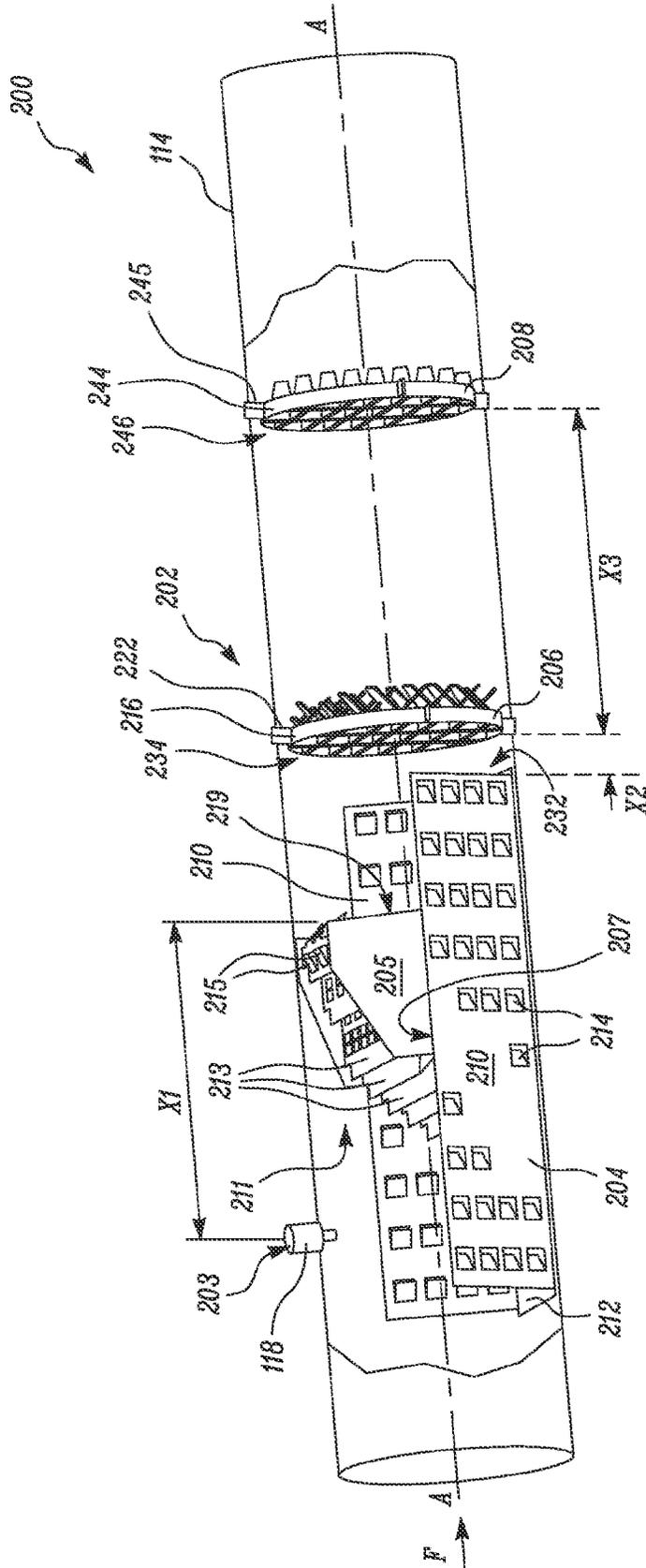


FIG. 2

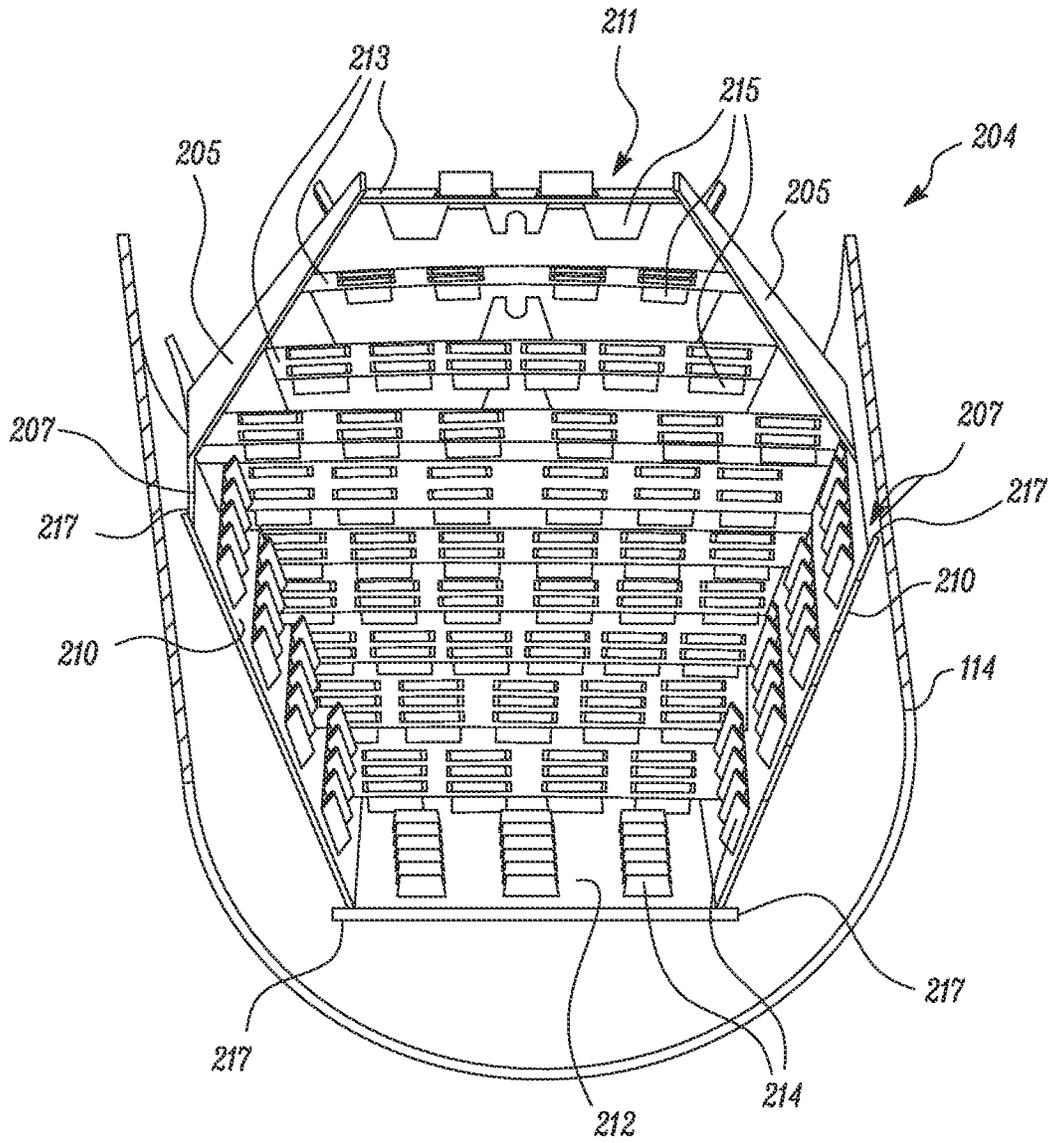


FIG. 3

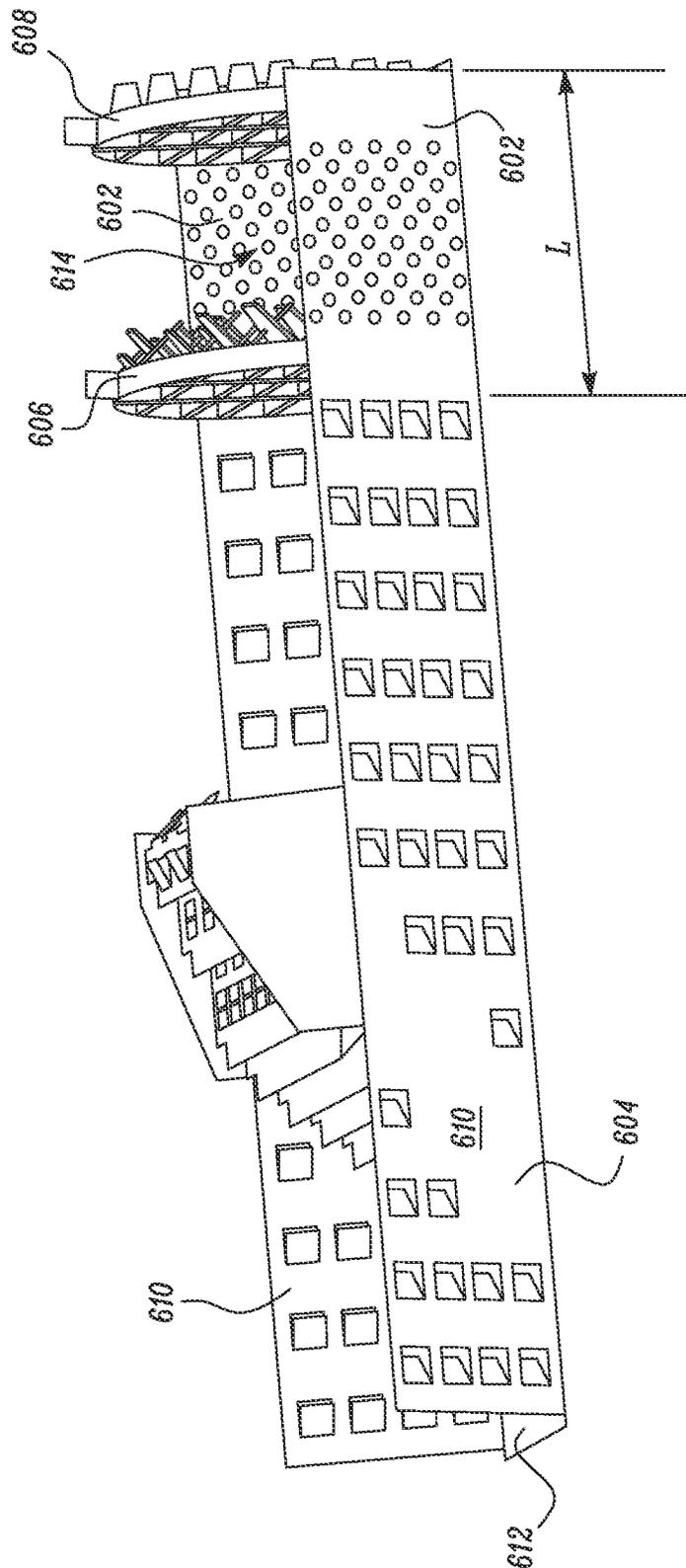


FIG. 6

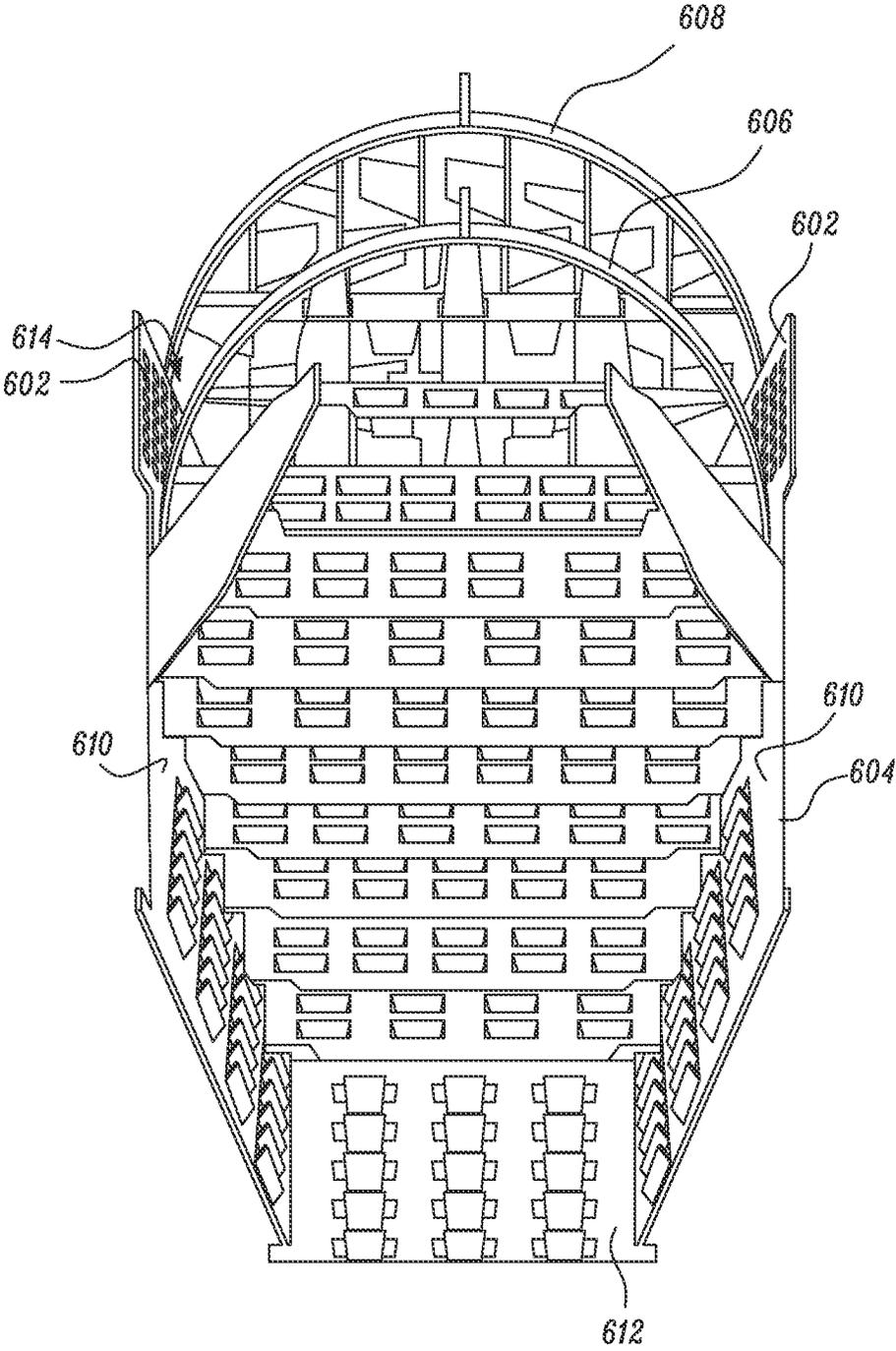


FIG. 7

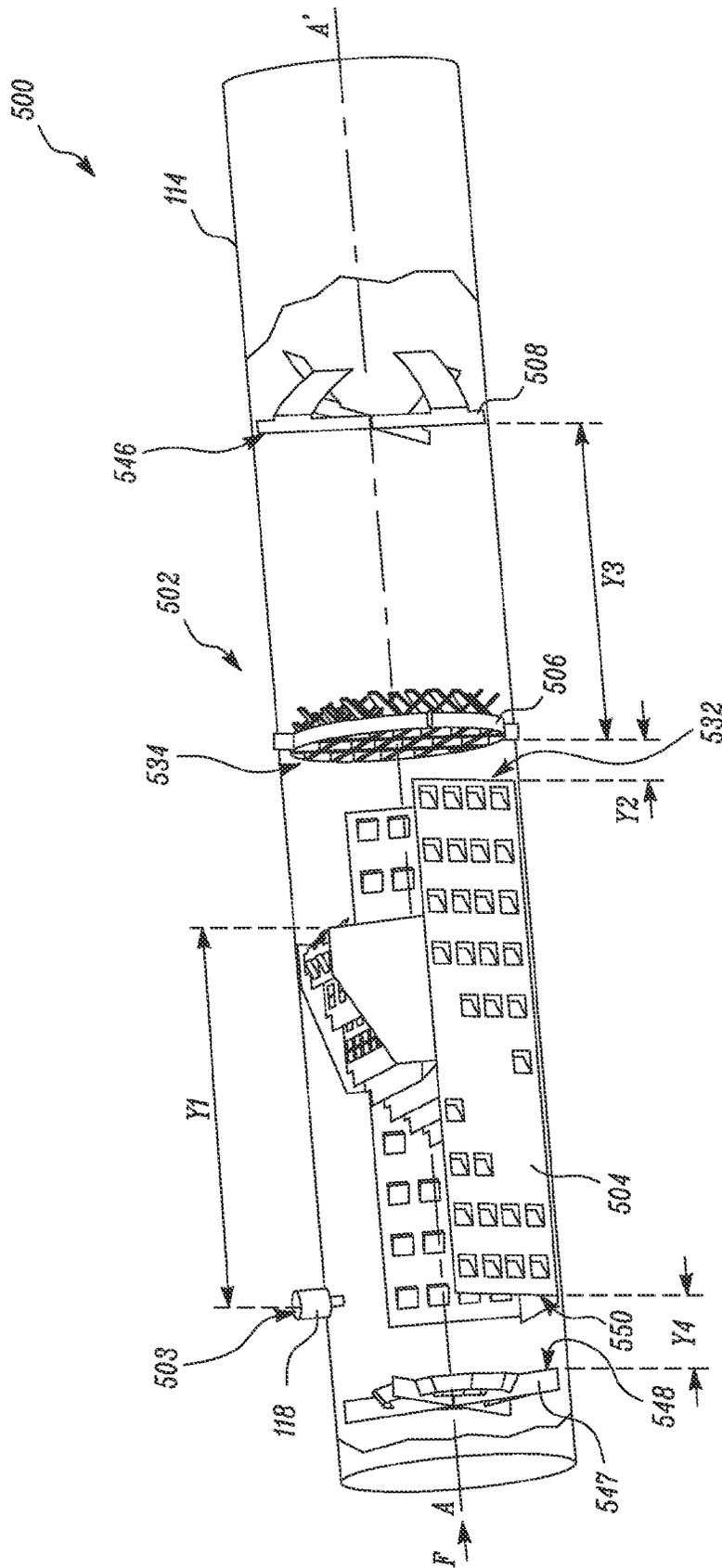


FIG. 8

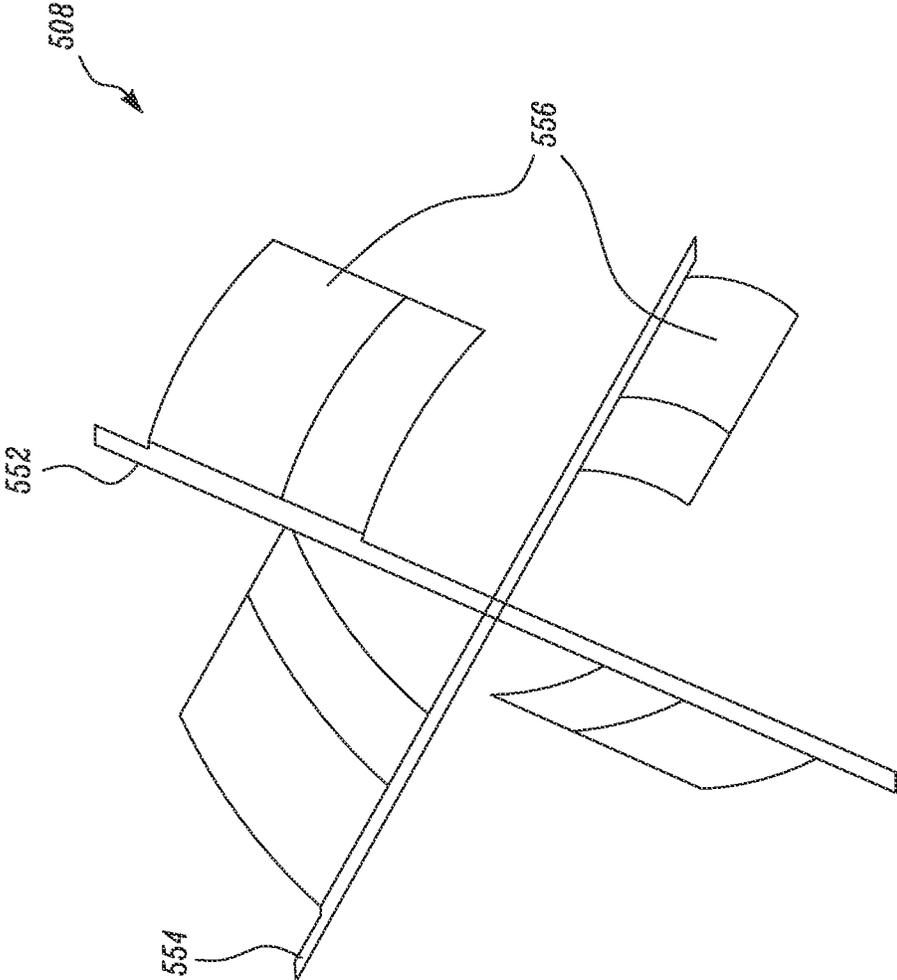


FIG. 9

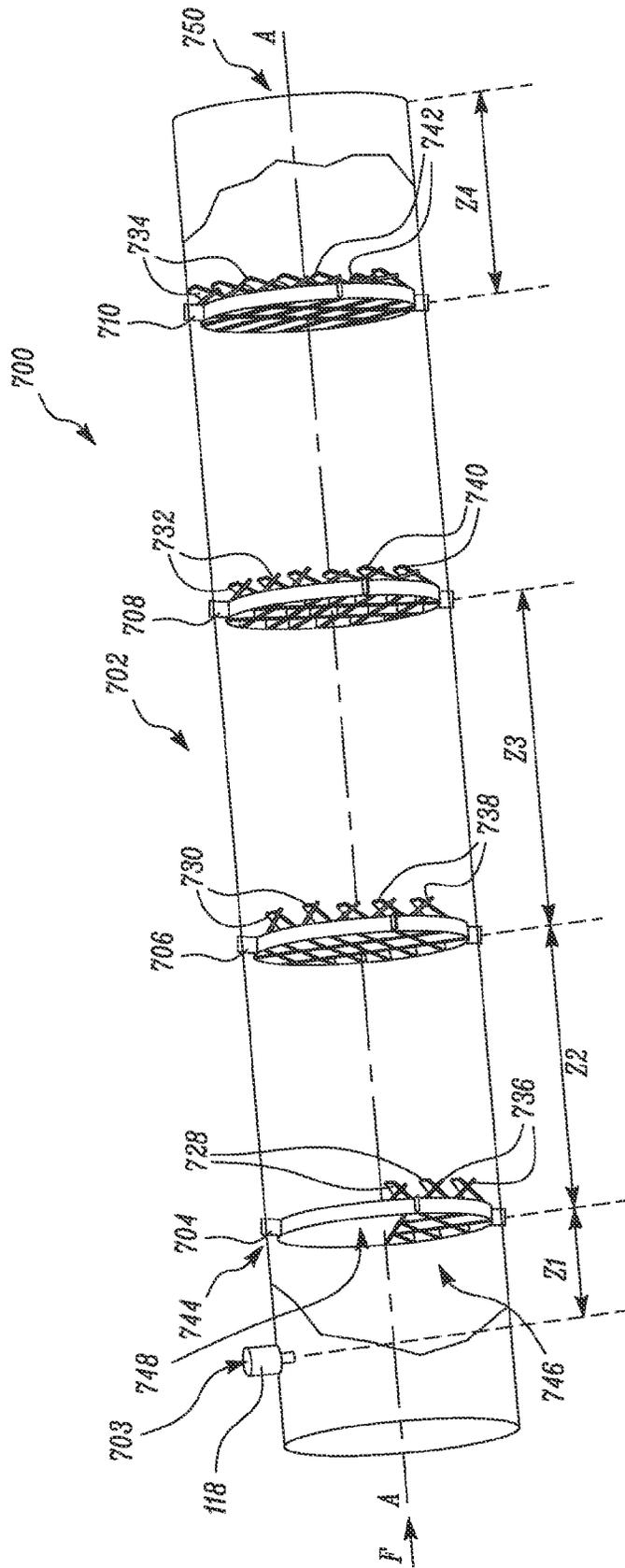


FIG. 10

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MIXING SYSTEM FOR AFTERTREATMENT SYSTEM

TECHNICAL FIELD

The present disclosure relates to a mixing system, more specifically to a mixing system for an aftertreatment system.

BACKGROUND

An aftertreatment system is associated with an engine system. The aftertreatment system is configured to treat and reduce oxides of nitrogen (NOx) present in an exhaust gas flow, prior to the exhaust gas flow exiting into the atmosphere. In order to reduce NOx, the aftertreatment system may include a reductant delivery module, a reductant injector, and a Selective Catalytic Reduction (SCR) module.

The reductant injector is configured to inject a reductant into the exhaust gas flowing through a mixing tube of the aftertreatment system. In order to achieve improved levels of NOx conversion, better flow distribution and mixing of the reductant with the exhaust gases must be achieved. A mixing element is affixed inside the mixing tube so that increased turbulence and improved distribution of the reductant within the exhaust gases may be achieved within a short length of the mixing tube.

However, sometimes the mixing element may provide a surface for the reductant particles to collect thereon, leading to formation of solid deposits. Deposit formation may in turn lead to increased back pressure on the engine and reduce an overall effectiveness of the mixing element. Further, the functioning of the aftertreatment system may be affected as well, causing a reduction in NOx conversion capability and increase in ammonia slip.

U.S. Pat. No. 8,272,777 describes a method for mixing an exhaust gas flow with a fluid in an exhaust gas pipe of an exhaust gas system, in which the fluid is injected by means of an injection device into the exhaust gas pipe. The exhaust gas flow is guided in the exhaust gas pipe in the area of the injection device in a direction of flow parallel to the exhaust gas pipe. The fluid is injected directly onto a deflection element which is arranged in the exhaust gas pipe in a central direction of injection which deviates from the direction of flow by an angle, wherein by means of at least one sheet metal part which is provided on the deflection element and which is raised at least partially at an angle with reference to the direction of flow, the exhaust gas flow is diverted with reference to the direction of flow from its direction of flow into a central direction of distribution.

SUMMARY OF THE DISCLOSURE

In one embodiment of the present disclosure, a mixing system for an aftertreatment system is disclosed. The mixing system includes a mixing tube. The mixing tube is provided in fluid communication with an exhaust conduit. The mixing system also includes a reductant injector positioned at an injection location on the mixing tube. The mixing system further includes a mixer assembly positioned downstream of the injection location. The mixer assembly includes a plurality of mixing elements provided in a series arrangement, such that each of the plurality of mixing elements is provided downstream of one another.

Other features and aspects of this disclosure will be apparent from the following description and the accompanying drawings.

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BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a schematic diagram of an exemplary engine system having an aftertreatment system associated therewithin, according to an embodiment of the disclosure;

FIG. 2 is a break away perspective view of a portion of a mixing tube of the aftertreatment system of FIG. 1, according to an embodiment of the disclosure;

FIGS. 3, 4, and 5 are perspective views of individual mixing elements associated with a mixing assembly of FIG. 2, according to some embodiments of the present disclosure;

FIGS. 6 and 7 are perspective views of a first mixing element, according to some embodiments of the present disclosure;

FIG. 8 is a break away perspective view of a portion of the mixing tube of FIG. 1 having another mixing assembly, according to other embodiments of the disclosure;

FIG. 9 is a perspective view of a mixing element associated with the mixing assembly of FIG. 8; and

FIG. 10 is a break away perspective view of a portion of the mixing tube of FIG. 1 having yet another mixing assembly, according to some other embodiments of the disclosure.

DETAILED DESCRIPTION

Wherever possible, the same reference numbers will be used throughout the drawings to refer to the same or the like parts. Referring to FIG. 1, a schematic diagram of an exemplary engine system **100** is illustrated, according to one embodiment of the present disclosure. The engine system **100** includes an engine **102**, which may be an internal combustion engine, such as, a reciprocating piston engine or a gas turbine engine. The engine **102** is a spark ignition engine or a compression ignition engine, such as, a diesel engine, a homogeneous charge compression ignition engine, or a reactivity controlled compression ignition engine, or other compression ignition engines known in the art. The engine **102** may be fueled by gasoline, diesel fuel, biodiesel, dimethyl ether, alcohol, natural gas, propane, hydrogen, combinations thereof, or any other combustion fuel known in the art.

The engine **102** may include other components (not shown), such as, a fuel system, an intake system, a drivetrain including a transmission system, and so on. The engine **102** may be used to provide power to any machine including, but not limited to, an on-highway truck, an off-highway truck, an earth moving machine, an electric generator, and so on. Accordingly, the engine system **100** may be associated with an industry including, but not limited to, transportation, construction, agriculture, forestry, power generation, and material handling.

Referring to FIG. 1, the engine system **100** includes an aftertreatment system **104** fluidly connected to an exhaust manifold of the engine **102**. The aftertreatment system **104** is configured to treat an exhaust gas flow exiting the exhaust manifold of the engine **102**. The exhaust gas flow contains emission compounds that may include oxides of nitrogen (NOx), unburned hydrocarbons, particulate matter, and/or other combustion products known in the art. The aftertreatment system **104** may be configured to trap or convert NOx, unburned hydrocarbons, particulate matter, combinations thereof, or other combustion products present in the exhaust gas flow, before exiting the engine system **100**.

In the illustrated embodiment, the aftertreatment system **104** includes a first module **106** that is fluidly connected to an exhaust conduit **108** of the engine **102**. During engine

operation, the first module **106** is arranged to internally receive engine exhaust gas from the exhaust conduit **108**. The first module **106** may contain various exhaust gas treatment devices, such as, a Diesel Oxidation Catalyst (DOC) **110** and a Diesel Particulate Filter (DPF) **112**, but other devices may be used. The first module **106** and the components found therein are optional and may be omitted for various engine applications in which the exhaust treatment function provided by the first module **106** is not required.

In the illustrated embodiment, the exhaust gas flow provided to the first module **106** by the engine **102** may first pass through the DOC **110** and then through the DPF **112** before entering a mixing tube **114**. The aftertreatment system **104** includes a reductant supply system **116**. A reductant is injected into the mixing tube **114** by a reductant injector **118**. The reductant may be a fluid, such as, Diesel Exhaust Fluid (DEF). The reductant may include urea, ammonia, or other reducing agent known in the art.

Referring to FIG. 1, the reductant supply system **116** includes a reductant tank **117**. The reductant is contained within the reductant tank **117**. Parameters related to the reductant tank **117** such as size, shape, location, and material used may vary according to system design and requirements. Further, the reductant injector **118** may be communicably coupled to a controller (not shown). Based on control signals received from the controller, the reductant from the reductant tank **117** is provided to the reductant injector **118** by a pump assembly **119**. As the reductant is injected into the mixing tube **114**, the reductant mixes with the exhaust gas flow passing therethrough, and is carried to a second module **124**. Further, the mixing tube **114** is configured to fluidly interconnect the first module **106** with the second module **124**, such that, the exhaust gas flow from the engine **102** may pass through the first and second modules **106**, **124** in series before being released at a stack **126** connected downstream of the second module **124**. The mixing tube **114** defines a longitudinal axis A-A'. The second module **124** encloses a Selective Catalytic Reduction (SCR) module **128** and an Ammonia Oxidation Catalyst (AMOX) **130**. The SCR module **128** operates to treat exhaust gases exiting the engine **102** in the presence of ammonia, which is provided after degradation of a urea-containing solution injected into the exhaust gases in the mixing tube **114**. The AMOX **130** is used to convert any ammonia slip from the downstream flow of the SCR module **128** before exiting the stack **126**.

Further, in order to promote mixing of the reductant with the exhaust gas flow, a mixing system **200** may be associated with the aftertreatment system **104**. The mixing system **200** is provided within a portion of the mixing tube **114**. The amount of the reductant that may be injected into the mixing tube **114** may be appropriately metered based on engine operating conditions. The aftertreatment system **104** disclosed herein is provided as a non-limiting example. It will be appreciated that the aftertreatment system **104** may be disposed in various arrangements and/or combinations relative to the exhaust manifold. These and other variations in aftertreatment system design are possible without deviating from the scope of the disclosure. The mixing system **200** will now be explained in detail with reference to FIGS. 2-7.

FIG. 2 illustrates a side perspective view of the portion of the mixing tube **114** having the mixing system **200** located therein, according to one embodiment of the present disclosure. The mixing system **200** includes a mixer assembly **202**. The mixer assembly **202** is positioned downstream of an injection location **203** and upstream of the SCR module **128** (see FIG. 1). The term "injection location" used herein refers

to a position on the mixing tube **114** at which the reductant injector **118** injects the reductant into the mixing tube **114**. The mixer assembly **202** includes a plurality of mixing elements.

As shown in FIG. 2, the mixer assembly **202** includes three mixing elements, namely a first mixing element **204**, a second mixing element **206**, and a third mixing element **208**. The mixing elements **204**, **206**, **208** are provided in a series arrangement, such that each of the mixing elements **204**, **206**, **208** is provided downstream of one another. The first, second, and third mixing elements **204**, **206**, **208** may be spaced apart from each other, such that distances "X1", "X2", "X3" respectively between consecutive mixing elements **204**, **206**, **208** may vary along an exhaust gas flow direction shown by arrow "F". Each of the first, second, and third mixing elements **204**, **206**, **208** are configured to assist in achieving improved mixing of the reductant with the exhaust gas flow on passage of the exhaust gas and the reductant therethrough.

It should be noted that the reductant injected in to the exhaust gas flow is generally in a liquid state. The each of the mixing elements **204**, **206**, **208** of the mixing system **200** is configured to break up and evaporate the reductant injected into the exhaust gas flow, such that before entering the SCR module **128**, the reductant is in a gaseous state and is homogeneously mixed with the exhaust gas flow.

The first mixing element **204** of the mixer assembly **202** is different from the second mixing element **206**. Referring to FIGS. 2 and 3, the first mixing element **204** is a primary mixing element, and is embodied as a flow convergent and impingement mixer. The first mixing element **204** includes a first pair of sidewalls **210** and a bottom wall **212**. The first pair of sidewalls **210** extends vertically upwards from the bottom wall **212**. Each of the first pair of sidewalls **210** and the bottom wall **212** of the first mixing element **204** includes a plurality of tabs **214** provided thereon. The tabs **214** open towards an inner side of the first mixing element **204**. The first mixing element **204** also includes a second pair of sidewalls **205**. The second pair of sidewalls **205** extending vertically upwards from an upper edge **207** of the first pair of sidewalls **210**.

FIG. 3 illustrates a front perspective view of the first mixing element **204**. The first mixing element **204** also includes a shelf arrangement **211** having a number of shelves **213**. The shelves **213** are arranged horizontally within the first mixing element **204**. Also, each of the shelves **213** is parallel to each other, and is also parallel to the bottom wall **212**. Some of the shelves **213** are mounted such that they extend between and are coupled to the first pair of sidewalls **210**. Whereas, remaining of the shelves **213** extend between and are coupled to the second pair of sidewalls **205**. Further, each of the shelves **213** include a plurality of tabs **215** provided thereon. Based on system requirements, the tabs **215** may either extend upwards or downwards with reference to a surface of the shelves **213**.

The first mixing element **204** also includes a plurality of attachment tabs **217**. The attachment tabs **217** may be provided at different positions on the first mixing element **204** in order to mount the first mixing element **204** within the mixing tube **114**. It should be noted that a number of shelves **213**, number and orientation of the tabs **215**, and the number of attachment tabs **217** may vary based on system requirements.

Referring now to FIG. 2, the first mixing element **204** is provided at the optimum distance "X1" from the injection location **203**, such that the reductant may contact the tabs **214**, **215** of the first mixing element **204** when injected into

the exhaust gas flow. The distance "X1" disclosed herein is defined as the distance between the injection location 203 and a downstream edge 219 of the shelf arrangement 211. In one example, the distance "X1" may approximately lie between 10 to 13 inches or 13 to 15 inches. For example, the distance "X1" may be approximately equal to 14 inches.

Referring now to FIGS. 2 and 4, the mixer assembly 202 includes the second mixing element 206. The second mixing element 206 is embodied as a flapper mixer. The second mixing element 206 is configured to mix the reductant and the exhaust gas flow in an up to down manner. Referring to FIG. 4, the second mixing element 206 includes a ring-shaped wall 216 having an inner surface 218 and an outer surface 220. The outer surface 220 of the wall 216 is provided with a plurality of projections 222. The projections 222 assist in mounting the second mixing element 206 within the mixing tube 114 (as shown in FIG. 2). In the illustrated embodiment, four projections 222 extend from the outer surface 220 of the wall 216. It should be noted that the number of projections 222 may vary based on system requirements.

The second mixing element 206 includes a plurality of first support members 224. The first support members 224 extend along a first direction B-B'. In this example, the first support members 224 are attached between inner surfaces 218 of the wall 216 of the second mixing element 206. Further, each of the plurality of first support members 224 is parallel to each other. The second mixing element 206 also includes second support members 226. The second mixing element 206 disclosed herein includes a pair of second support members 226, however the number of second support members 226 may vary as per operational requirements. The second support members 226 extend along a second direction C-C', such that the second direction C-C' is perpendicular to the first direction B-B'. The second support members 226 are also attached between the inner surfaces 218 of the wall 216 of the second mixing element 206, and are parallel to each other.

The second mixing element 206 further includes a first set of fin elements 228 and a second set of fin elements 230. The fin elements 228, 230 have a trapezoidal shape. Alternatively, the fin elements 228, 230 may have any other shape known in the art that serves the purpose of mixing. The fin elements 228, 230 are attached to and extend from the first support members 224 of the second mixing element 206. Further, each of the fin elements 228, 230 are attached to the first support members 224 in an angled manner. An inclination of the fin elements 228, 230 with respect to a vertical axis Y-Y' of the second mixing element 206 is defined as a fin angle " α ". Further, in the illustrated embodiment, the fin elements 228, 230 make an acute angle with respect to the axis Y-Y'. More specifically, the first set of fin elements 228 has the fin angle " α ", such that the fin elements 228 extend upwards from the first support members 224. Whereas the second set of fin elements 230 have the fin angle " α ", such that the fin elements 230 extend downwards from the first support members 224. In one example, the fin angle " α " may approximately lay between $\pm 1^\circ$ to 60° . However, the value of the fin angle " α " is not limited thereto, and may vary based on system requirements. It should be noted that the number of fin elements 228, 230 attached to the second mixing element 206 may also vary based upon a desired fin density. The term "fin density" used herein is calculated based upon the number of fin elements provided per unit area of a particular mixing element.

As shown in FIG. 2, the second mixing element 206 is provided downstream of the first mixing element 204 at a

location such that the reductant may contact the fin elements 228, 230 of the second mixing element 206. Accordingly, the second mixing element 206 is provided at the optimum distance "X2" from a downstream edge 232 of the first mixing element 204. The distance "X2" is defined as the distance between the downstream edge 232 of the first mixing element 204 and an upstream edge 234 of the second mixing element 206. In one embodiment, the distance "X2" may approximately lie between 0.5 to 2.5 inches or 2.5 to 5 inches. For example, the distance "X2" may be approximately equal to 2 inches.

Referring now to FIGS. 2 and 5, the mixer assembly 202 includes the third mixing element 208. The third mixing element 208 is mounted downstream of the second mixing element 206, along the exhaust gas flow direction "F" (see FIG. 2). The third mixing element 208 is configured to mix the reductant with the exhaust gas flow in a horizontal or side to side manner. The third mixing element 208 may be embodied as a flapper mixer, and has constructional features similar to the second mixing element 206 that is explained earlier in this section. As shown in FIG. 2, the third mixing element 208 is mounted in a different orientation as compared to that of the second mixing element 206 within the mixing tube 114. The third mixing element 208 is clocked by an angle of 90° with respect to the longitudinal axis A-A' of the mixing tube 114. The term "clocking" used herein is defined as an angular orientation of the mixing element with respect to an attachment of the mixing element with respect to the mixing tube 114.

Referring to FIG. 5, the clocking of the third mixing element 208 by 90° with respect to the longitudinal axis A-A' causes a first support members 236 of the third mixing element 208 to extend vertically along the second direction C-C', as against the first support members 224 of the second mixing element 206 which extend horizontally along the first direction B-B' (see FIG. 4). Also, the third mixing element 208 includes first and second set of fin elements 238, 240 that extend from the first support members 236, and are attached thereto. The first set of fin elements 238 and the second set of fin elements 240 are angled with respect to an axis Z-Z'. Further, second support members 242 of the third mixing element 208 extend along the first direction B-B'. The third mixing element 208 also includes projections 245 for mounting the third mixing element 208 within the mixing tube 114.

Further, in an exemplary embodiment, the fin density of the third mixing element 208 may be higher as compared to the fin density of the second mixing element 206, such that the third mixing element 208 includes higher number of fin elements 238, 240 compared to the number of fin elements 228, 230 of the second mixing element 206. In some embodiments, the fin angle " α " of the fin elements 228, 230, 238, 240 of each of the second and third mixing elements 206, 208 may also vary. In one example, the fin angle " α " of the fin elements 238, 240 of the third mixing element 208 may be lesser than the fin angle " α " of the fin elements 228, 230 of the second mixing element 206 (see FIGS. 4 and 5).

For better mixing and stratification of the reductant with the exhaust gas flow, the third mixing element 208 is provided at an optimum location within the mixing tube 114, so that the reductant may contact the fin elements 238, 240 of the third mixing element 208, instead of a wall 244 of the third mixing element 208. Accordingly, the third mixing element 208 is provided in the mixing tube 114 at the distance "X3" (see FIG. 2) from the second mixing element 206. More particularly, the distance "X3" is defined as the distance between the upstream edge 234 of the second

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mixing element **206** and an upstream edge **246** of the third mixing element **208**. In one embodiment, the distance “X3” may approximately lie between 5 to 7 inches or 7 to 10 inches. For example the distance “X3” may be approximately equal to 8 inches. In an exemplary embodiment, the mixing assembly **202** may also include a pre-mixer (not shown). The pre-mixer may be positioned upstream of the first mixing element **204**, and may be configured to impart slight turbulence to the exhaust gas flow entering the mixing tube **114**.

In an alternate embodiment of the present disclosure, as shown in FIGS. **6** and **7**, an attachment surface **602** is associated with a first mixing element **604**, a second mixing element **606**, and a third mixing element **608**. The attachment surface **602** is configured to couple the first mixing element **604**, the second mixing element **606**, and the third mixing element **608** with each other. Design features of the first mixing element **604**, the second mixing element **606**, and the third mixing element **608** are similar to the design features of the first, second, and third mixing elements **204**, **206**, **208** explained earlier with reference to FIGS. **2** to **5**. As shown in FIGS. **6** and **7**, the attachment surfaces **602** may be three in number, and are formed by extending a first pair of sidewalls **610** and a bottom wall **612** of the first mixing element **604**. The attachment surfaces **602** are provided such that a space **614** so formed and enclosed by each of the attachment surfaces **602** is configured to receive the second and third mixing elements **606**, **608** therein. Further, a length “L” of the attachment surfaces **602** may vary based on the mounting position of the second and third mixing elements **606**, **608**.

Alternatively, the attachment surface **602** may be shaped as a bar member. One or more such bar members may be associated with the mixing elements **604**, **606**, **608** in order to couple the mixing elements **604**, **606**, **608** with each other. Further, in another embodiment, the attachment surfaces **602** may be embodied by extending only the first pair of sidewalls **610** of the first mixing element **604**, and not the bottom wall **612** of the first mixing element **604**.

FIG. **8** illustrates another embodiment of the present disclosure in which each of the mixing elements is different from each other. In this embodiment, a mixer assembly **502** of a mixing system **500** includes first and second mixing elements **504**, **506** having constructional features similar to that of the first and second mixing elements **204**, **206** illustrated and explained with reference to FIGS. **2** to **4**. Also, the first mixing element **504** is provided at a distance “Y1” from an injection location **503**. The distance “Y1” may lie approximately between 10 to 12 inches or 12 to 15 inches. In one example the distance “Y1” may be approximately equal to 11.5 inches. Further, the second mixing element **506** is mounted at a distance “Y2”. The distance “Y2” is defined as the distance between a downstream edge **532** of the first mixing element **504** and an upstream edge **534** of the second mixing element **506**. The distance “Y2” may lie approximately between 1 to 2.5 inches or 2.5 to 5 inches. In one example, the distance “Y2” may be approximately equal to 4 inches.

In addition to the first and second mixing elements **504**, **506**, the mixer assembly **502** may include a pre-mixer **547**. The pre-mixer **547** is embodied as a booster. The pre-mixer **547** is configured to impart a slight turbulence to the exhaust gas flow entering the mixing tube **114**, before the reductant is injected therein. The pre-mixer **547** is provided at a distance “Y4” from the first mixing element **504**. More particularly, the distance “Y4” may be defined as the distance between a downstream edge **548** of the pre-mixer **547**

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and an upstream edge **550** of the first mixing element **504**. The distance “Y4” may lie approximately between 1 to 2 inches or 2 to 4 inches. In one example, the distance “Y4” may be approximately equal to 3 inches.

Referring now to FIGS. **8** and **9**, the mixer assembly **502** includes a third mixing element **508**. In this embodiment, the third mixing element **508** is embodied as a swirl mixer. As shown in FIG. **9**, the third mixing element **508** includes a first bar member **552** and a second bar member **554**. The first and second bar members **552**, **554** are connected in a scissor-type arrangement. Each end of the first and second bar members **552**, **554** includes blades **556** attached thereto. In the illustrated embodiment, the third mixing element **508** includes four such blades **556**; however, based on system requirements, the third mixing element **508** may include more than four blades **556**. Also, an angle of attachment of the blades **556** with the bar members **552**, **554** may vary in order to achieve optimum mixing of the reductant with the exhaust gas flow. It should be further noted that for better mixing of the reductant with the exhaust gas flow, the third mixing element **508** may be clocked differently from that shown in the accompanying figures.

As shown in FIG. **8**, the third mixing element **508** is mounted within the mixing tube **114** so as to achieve evaporation of the reductant and also to provide close to uniform mixing of the reductant with the exhaust gas flow. The third mixing element **508** is provided at a distance “Y3” from the second mixing element **506**. More particularly, the distance “Y3” is defined as the distance between an upstream edge **534** of the second mixing element **506** and an upstream edge **546** of the third mixing element **508**. The distance “Y3” may lie approximately between 10 to 15 inches or 15 to 25 inches. In one embodiment, the distance “Y3” may be approximately equal to 15 inches.

FIG. **10** illustrates yet another embodiment of the present disclosure. A mixer assembly **702** of a mixing system **700** includes four mixing elements, namely a first mixing element **704**, a second mixing element **706**, a third mixing element **708**, and a fourth mixing element **710**. The mixing elements **704**, **706**, **708**, **710** are provided downstream of an injection location **703**. Further, the mixing elements **704**, **706**, **708**, **710** are provided in a series arrangement, downstream of one another. Each of the mixing elements **704**, **706**, **708**, **710** is of the same type, and is embodied as a flapper mixer. The constructional features of the mixing elements **704**, **706**, **708**, **710** are similar to the constructional features of the flapper mixer explained earlier in this section. Accordingly, each of the mixing elements **704**, **706**, **708**, **710** respectively include a first set of fin elements **728**, **730**, **732**, **734**, and a second set of fin elements **736**, **738**, **740**, **742** respectively.

However, it should be noted that each of the mixing elements **704**, **706**, **708**, **710** are designed such that at least one parameter of the mixing elements **704**, **706**, **708**, **710** may change or be adjusted along the exhaust gas flow direction “F”. The parameter may include the fin density, the fin angle “ α ”, the clocking of the mixing elements **704**, **706**, **708**, **710** with respect to each other, or any combination of the parameters. The first mixing element **704** of the mixer assembly **702** is mounted within the mixing tube **114** at a distance “Z1” from the injection location **703**, so that the first mixing element **704** may capture reductant at low exhaust flow rates and may prevent the reductant from contacting a circular wall of the first mixing element **704**.

As shown in the accompanying figures, the first mixing element **704** is divided into portions, namely a top portion **744** and a bottom portion **746**. The top portion **744** of the

first mixing element **704** is embodied as an open space **748**. Further, the bottom portion **746** of the first mixing element **704** includes the fin elements **728**, **736** attached thereto. The first mixing element **704** is configured to break up large particles of the reductant at low exhaust gas flow rates while flowing through the fin elements **728**, **736**. Whereas, the reductant may be allowed to pass through the open space **748** of the first mixing element **704** during high exhaust flow rates.

The fin elements **728**, **736** of the first mixing element **704** have a shallow fin angle " α " as compared to the fin angle " α " of the remaining mixing elements **706**, **708**, **710** provided downstream of the first mixing element **704**. The fin angle " α " is decided such that, the fin elements **728**, **736** may promote a break up of large particles of the reductant and also promote mixing of the reductant with the exhaust gas flow. Further, the first mixing element **704** has relatively lower fin density as compared to fin densities of the remaining mixing elements **706**, **708**, **710**.

The second mixing element **706** of the mixer assembly **702** is mounted within the mixing tube **114** at a distance " $Z2$ " from the first mixing element **704**. The distance " $Z2$ " is decided such that the reductant particles, at high exhaust gas flow rates, hit the fin elements **730**, **738** instead of the circular wall of the second mixing element **706**. Further, the second mixing element **706** is configured to continue breaking of the reductant particles at low exhaust flow rates, and also to initiate the breaking of the large particles of the reductant at high exhaust flow rates. For this purpose, the second mixing element **706** is designed such that the fin elements **730**, **738** have a shallow fin angle " α " at a top portion of the second mixing element **706**. Also, the fin density of the second mixing element **706** may be lower at the top portion. In one embodiment, the fin density of the second mixing element **706** may be greater than the fin density of the first mixing element **704**. The arrangement of the fin elements **730**, **738** at the top portion of the second mixing element **706** may promote the breakup of the large particles of the reductant at high exhaust flow rates.

The fin angle " α " of the fin elements **730**, **738** may progressively get steeper towards a bottom portion of the second mixing element **706**. Also, the fin density of the second mixing element **706** may increase progressively towards the bottom portion of the second mixing element **706**. This arrangement may allow for the continual breakup of the small particles of the reductant that may have already passed through the first mixing element **704** at low exhaust gas flow rates.

The third mixing element **708** is mounted within the mixing tube **114** at a distance " $Z3$ " from the second mixing element **706**. The distance " $Z3$ " is optimized and decided such that minimal deposit formation may occur on the third mixing element **708** and close to uniform mixing of the reductant with the exhaust gas flow may be obtained. The third mixing element **708** is configured to break up the small particles of the reductant that may still exist in the exhaust gas flow and start a gaseous phase mixing of the reductant with the exhaust gas flow.

The third mixing element **708** includes the fin elements **732**, **740**. In the illustrated embodiment, the fin angle " α " of the fin elements **732**, **740** is steeper at a top portion of the third mixing element **708**, as compared to the fin angle " α " of the fin elements **730**, **738** of the second mixing element **706**. Further, the fin angle " α " may progressively get steeper towards a bottom portion of the third mixing element **708**. Also, the fin density of the third mixing element **708** may be optimally chosen in order to reduce or minimize back

pressure and promote uniform mixing of the reductant with the exhaust gas flow. The fin density may be constant from the top portion to the bottom portion of the third mixing element **708**; however, the fin density of the third mixing element **708** may be higher as compared to the fin density of the second mixing element **706**.

As shown in the accompanying figures, the third mixing element **708** is mounted within the mixing tube **114** at a different angular orientation within the mixing tube **114** as compared to the second mixing element **706**. More particularly, the third mixing element **708** is clocked at a certain angle about the longitudinal axis A-A'. In some examples, the fin angle " α " of the fin elements **732**, **740** may be optimized such that the third mixing element **708** may be clocked approximately up to 90° with respect to the second mixing element **706**, about the longitudinal axis A-A'. The clocking of the third mixing element **708** may promote the gaseous phase mixing of the reductant with the exhaust gas flow.

The mixer assembly **702** includes the fourth mixing element **710**. The fourth mixing element **710** may be configured to continue the breaking of the small particles of the reductant present in the exhaust gas flow, and may also promote gaseous mixing of the reductant with the exhaust gas flow. Further, the fourth mixing element **710** is mounted within the mixing tube **114** at a distance " $Z4$ " from an outlet **750** of the mixing tube **114**. The distance " $Z4$ " may be optimally decided so as to achieve maximum evaporation of the reductant and also promote close to uniform mixing of the reductant with the exhaust gas flow.

Further, the fin angle " α " of the fin elements **734**, **742** of the fourth mixing element **710** may be steeper as compared to the fin angle " α " of the fin elements **732**, **740** of the third mixing element **708**. The fin density of the fourth mixing element **710** may be optimized in order to minimize back-pressure and also to promote close to uniform mixing of the reductant with the exhaust gas flow. It should be noted that the fin density of the fourth mixing element **710** may be the highest as compared to the fin densities of the first, second, and third mixing elements **704**, **706**, **708**. Further, the fin density of the fourth mixing element **710** may be uniform from a top portion to a bottom portion of the fourth mixing element **710**. It should be further noted that the fin angle " α " of the fin elements **734**, **742** may be optimized such that the fourth mixing element **710** may be clocked approximately up to 90° with respect to the third mixing element **708**, about the longitudinal axis A-A'. The clocking of the fourth mixing element **710** may further promote the gaseous phase mixing of the reductant with the exhaust gas flow.

INDUSTRIAL APPLICABILITY

An optimum distribution of the reductant with the exhaust gas flow and the evaporation of the reductant in the mixing tube may be critical to the performance of the SCR module. Mixing systems are generally used for obtaining uniform flow distribution and thorough mixing of the reductant with the exhaust gas flow. However, an improper design of the mixing system may lead to increased formation of solid deposits of the reductant thereon. Deposit formation may lead to increased back pressure on the engine and reduce an effectiveness of the mixing system to blend the reductant with the exhaust gas flow, thereby leading to reduction in NOx conversion capability and increase in ammonia slip.

The present disclosure describes a low cost mixing system **200**, **500**, **700** which provides improved stratification of the reductant injected in the exhaust gas flow and also provides

optimum mixing of the reductant with the exhaust gas flow in a multi-stage reductant break up arrangement. The mixing system 200, 500, 700 may be capable of achieving improved levels of NOx conversion through close to uniform distribution of the reductant with the exhaust gas flow, with minimal or no formation of solid deposits. The positioning of each of the mixing elements 204, 206, 208, 504, 506, 508, 547, 604, 606, 608, 704, 706, 708, 710 within the mixing systems 200, 500, 700 respectively may be optimized in order to achieve the higher levels of NOx conversion through close to uniform distribution of the reductant. The positioning of the mixing elements 204, 206, 208, 504, 506, 508, 547, 604, 606, 608, 704, 706, 708, 710 with respect to each other and/or the injection locations 203, 503, 703 respectively may also be adjusted as a function of an exhaust gas flow velocity and reductant particle diameter in order to control the residence time and evaporation rate of the reductant.

Also, it is possible to adjust the fin angle “ α ”, fin density, and positioning of each of the mixing elements 204, 206, 208, 504, 506, 508, 547, 604, 606, 608, 704, 706, 708, 710 based on a function of a length of the mixing tube 114, in order to achieve optimum mixing of the reductant with the exhaust gas flow. Further, the process of designing the mixing systems 200, 500, 700 is simpler as compared to current designs because optimized mixing and distribution of the reductant with the exhaust gas flow may be achieved by breaking the function of uniform distribution into multiple mixing stages formed in each of the mixing assemblies 202, 502, 702.

Further, utilization of the multiple mixing elements 204, 206, 208, 504, 506, 508, 547, 604, 606, 608, 704, 706, 708, 710 may cause the engine system 100 to heat up faster as compared to the current designs. This may be beneficial from a reductant deposit formation perspective, especially when the engine system 100 is transitioning from a cold condition to a high temperature condition. A person of ordinary skill in the art will appreciate that mixing systems 200, 500, 700 of the present disclosure may be used across multiple platforms, apart from engine applications allowing for less development time and a consistent approach to mixing tube designs. The design may also allow for mixing of the reductant with the exhaust gas flow within shorter mixing tube lengths as compared to current designs.

While embodiments of the present disclosure have been particularly shown and described with reference to the embodiments above, it will be understood by those skilled in the art that various additional embodiments may be contemplated by the modification of the disclosed machines, systems and methods without departing from the spirit and scope of what is disclosed. Such embodiments should be understood to fall within the scope of the present disclosure as determined based upon the claims and any equivalents thereof.

What is claimed is:

1. A mixing system for an aftertreatment system, the mixing system comprising:
 - a mixing tube in fluid communication with an exhaust conduit;
 - a reductant injector positioned at an injection location on the mixing tube; and
 - a mixer assembly positioned downstream of the injection location, the mixer assembly including a plurality of mixing elements provided in a series arrangement;
 the plurality of mixing elements further including a first mixing element having a shelf arrangement with a plurality of shelves arranged horizontally and parallel

one another within the mixing tube, the plurality of shelves being located at a plurality of different shelf locations within a flow path of exhaust and reductant through the mixing tube such that a first one of the plurality of shelves is located upstream of a second one of the plurality of shelves;

the plurality of mixing elements further including a second mixing element at a second location that is downstream of the first mixing element to mix exhaust and reductant received from the first mixing element; and wherein the first mixing element is a flow convergent and impingement mixer comprising two sidewalls, each of the two sidewalls including a plurality of tabs provided thereon, and the second mixing element is one of a flapper mixer or a swirl mixer.

2. The mixing system of claim 1 further comprising a pre-mixer element positioned upstream of the injection location.

3. The mixing system of claim 1, wherein the plurality of mixing elements further includes a third mixing element, wherein the third mixing element is a flapper mixer.

4. The mixing system of claim 3, wherein at least one parameter of the third mixing element is different from that of the second mixing element, the at least one parameter including a fin density, a fin angle, an angle of attachment, a clocking of the flapper mixer about a longitudinal axis of the mixing tube, or a combination thereof.

5. The mixing system of claim 4, wherein at least one of the fin density or the fin angle increases from one mixing element to another along an exhaust flow direction.

6. The mixing system of claim 1, wherein the plurality of mixing elements further includes a third mixing element, wherein the third mixing element is a swirl mixer.

7. The mixing system of claim 1, wherein the plurality of mixing elements includes at least three mixing elements that are spaced apart such that a distance between each of the plurality of mixing elements increases along an exhaust flow direction.

8. The mixing system of claim 1, wherein the mixer assembly is positioned upstream of a selective catalytic reduction module.

9. A mixing system for an aftertreatment system, the mixing system comprising:

a mixing tube in fluid communication with an exhaust conduit;

a reductant injector positioned at an injection location on the mixing tube; and

a mixer assembly positioned downstream of the injection location, the mixer assembly including a plurality of mixing elements provided in a series arrangement, such that each of the plurality of mixing elements is provided downstream of one another;

wherein the plurality of mixing elements includes a first mixing element and a second mixing element;

wherein the first mixing element is a different type of mixing element from the second mixing element;

wherein the first mixing element is a flow convergent and impingement mixer comprising two sidewalls, each of the two sidewalls including a plurality of tabs provided thereon;

wherein the second mixing element is a flapper mixer; wherein the plurality of mixing elements further includes a third mixing element, wherein the third mixing element is a flapper mixer; and

wherein the mixing system further comprises at least one attachment surface, wherein the attachment surface is

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configured to connect the first mixing element, the second mixing element, and the third mixing element with each other.

10. The mixing system of claim 9, wherein at least one attachment surface is shaped as a bar member.

11. The mixing system of claim 9, wherein the at least one attachment surface is formed by extending at least one of the two sidewalls of the first mixing element.

12. A mixing system, for an aftertreatment system, the mixing system comprising:

a mixing tube in fluid communication with an exhaust conduit;

a reductant injector positioned at an injection location on the mixing tube; and

a mixer assembly positioned downstream of the injection location, the mixer assembly including a plurality of mixing elements provided in a series arrangement, such

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that each of the plurality of mixing elements is provided downstream of one another;

wherein each of the plurality of mixing elements is of a same type;

wherein the plurality of mixing elements includes a plurality of flapper mixers;

wherein at least one parameter of each of the plurality of flapper mixers is changed along an exhaust flow direction;

wherein the at least one parameter includes a fin density, a fin angle, an angle of attachment, a clocking of the flapper mixer about a longitudinal axis of the mixing tube, or a combination thereof; and

wherein at least one of the fin density or the fin angle increases from one flapper mixer to another along an exhaust flow direction.

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