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61/309,782 2 March 2010 (02.03.2010) US(71) Applicant (for all designated States except US): **MAS-
SACHUSETTS INSTITUTE OF TECHNOLOGY**
[US/US]; 77 Massachusetts Avenue, Cambridge, MA
02139 (US).

(72) Inventors; and

(75) Inventors/Applicants (for US only): **STEPHANOPOU-
LOS, Gregory** [US/US]; 4 Russet Lane, Winchester, MA
01890 (US). **ABIDI, Syed, Hussain Imam** [PK/US]; 124
Peterborough Street, Apt. D, Boston, MA 02120 (US).(74) Agent: **VAN AMSTERDAM, John, R.**; Wolf, Green-
field & Sacks, P.C., 600 Atlantic Avenue, Boston, MA
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(54) Title: MICROBIAL ENGINEERING FOR THE PRODUCTION OF FATTY ACIDS AND FATTY ACID DERIVATIVES

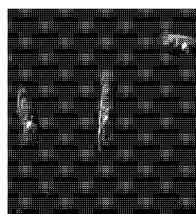
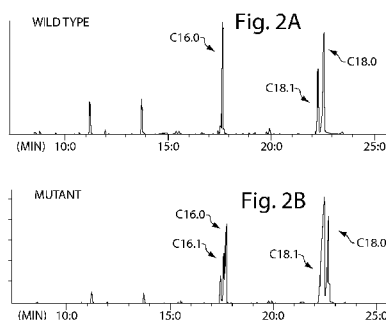


Fig. 2C

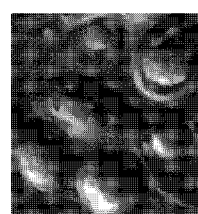


Fig. 2D

(57) Abstract: Some aspects of this invention relate to methods useful for the conversion of a carbon source to a biofuel or biofuel precursor using engineered microbes. Some aspects of this invention relate to the discovery of a key regulator of lipid metabolism in microbes. Some aspects of this invention relate to engineered microbes for biofuel or biofuel precursor production.

MICROBIAL ENGINEERING FOR THE PRODUCTION OF FATTY ACIDS AND
FATTY ACID DERIVATIVES

RELATED APPLICATION

5 This application claims priority under 35 U.S.C. § 119(e) to United States provisional patent application, U.S.S.N. 61/309,782, filed March 2, 2010, the entire contents of which are incorporated herein by reference.

FIELD OF THE INVENTION

10 The invention, at least in part, relates to the field of converting a carbohydrate source into a biofuel or a biofuel precursor, for example, a fatty acid or fatty acid derivative, such as a triacylglycerol, using an engineered cell or microbe.

FEDERALLY SPONSORED RESEARCH

15 Research leading to certain aspects of the invention(s) disclosed herein was supported, at least in part, by Department of Energy grant 69106899. The United States Government has certain rights in the invention.

BACKGROUND OF THE INVENTION

20 Sustainably produced biofuels are an alternative to fossil fuels and may help to alleviate the depletion of easily accessible fossil fuel stocks while avoiding fossil fuel-associated pollution and greenhouse gas emission, thus satisfying a rising demand for affordable energy in a sustainable way. However, the widespread implementation of biofuel production has been thwarted by several drawbacks of current production methods, for
25 example the competition of biofuel-producing plants with food crops for agriculturally valuable acreage, or the use of industrial substrates with only limited supply as carbon sources.

SUMMARY OF THE INVENTION

30 The growing concerns over the sustainability and renewability of fossil fuels have led to the development of a wide spectrum of alternative biofuels of various origins, including lipids synthesized from renewable resources by microbes such as bacteria or yeast. Lipids

useful as biofuel or biofuel precursors include, for example, fatty acids and their derivatives (e.g., triacylglycerols).

The economical viability of microbe-synthesized biofuels or biofuel precursors is dependent on employing a suitable microbe of a phenotype including a combination of multiple beneficial traits, for example, a metabolism allowing for efficient carbon to biofuel or biofuel precursor conversion, high biomass formation rate, high productivity of biofuel or biofuel precursor, high levels of intracellular accumulation or secretion of biofuel or biofuel precursor, good tolerance to feedstock (carbon source and associated substances) and synthesized product (e.g., fatty acid or triacylglycerol), and stability of the biofuel or biofuel precursor, for example, at low carbon source concentrations. The conversion yield (gram of oil produced per gram of substrate, e.g., glucose) is of particular importance. Microbes commonly employed in biofuel or biofuel precursor production do not conform to the required phenotype in a way sufficient to allow for economical industrial-scale production of biofuel.

Some aspects of this invention relate to the engineering of required traits in a microorganism for biofuel or biofuel precursor production. While lipid and fatty acid metabolism has been studied in microbes from the 1930s and 1940s onward (see, e.g. Woodbine, M. 1959, *Microbial fat: Microorganisms as potential fat producers*. Prog. Ind. Microbiol.1:181), little progress has been made toward engineering desirable phenotypes related to biofuel production in microbes despite numerous efforts to genetically engineer a microbe or to optimize the conditions of the production process. So far, genetic engineering efforts have mainly been directed to the manipulation of a gene target upstream of or within the fatty acid synthesis pathway and the optimization of fermentation or growth conditions, for example, by supplementing growth media with fatty acids.

One major obstacle to genetic engineering of microbes is the lack of genomic information and annotation of key metabolic pathway regulators in target microbes, for example, in oleaginous yeast. As a result, functional identification and annotation of a key regulator governing carbohydrate to lipid conversion is still lacking in microbes for biofuel production.

Some aspects of this invention relate to the identification of the oleaginous yeast *Y. lipolytica* as a microbe for biofuel or biofuel precursor production. Some aspects of this invention relate to the discovery of a key regulator of fatty acid metabolism in a microbe.

Some aspects of this invention relate to the discovery of stearoyl-CoA desaturase (SCD) as a key regulator of carbohydrate to lipid conversion in a microbe. Some aspects of this invention relate to an isolated nucleic acid encoding a key regulator of fatty acid metabolism in a microbe. Some aspects of this invention provide an isolated nucleic acid encoding a key
5 regulator of fatty acid metabolism, for example, a SCD gene product, of an oleaginous microbe.

Some aspects of this invention relate to the engineering of a microbe for the production of biofuel by manipulating the activity of a regulator of fatty acid metabolism, for example, by genetic manipulation. Some aspects of this invention relate to an isolated
10 microbe engineered for biofuel or biofuel precursor production. Some aspects of this invention relate to an isolated microbe optimized for the conversion of a carbohydrate source to a biofuel or biofuel precursor, for example, an oleaginous microbe comprising an increased activity of a SCD gene product. Some aspects of this invention relate to a culture of a microbe engineered for biofuel or biofuel precursor production. Some aspects of this
15 invention relate to methods of converting a carbohydrate source into a fatty acid or fatty acid derivative using a microbe engineered for biofuel production. Some aspects of this invention relate to a bioreactor for carbohydrate to fatty acid or fatty acid derivative conversion using a microbe engineered for biofuel production. Some aspects of this invention provide a method to convert a carbohydrate source, at least partially, into a biofuel or biofuel precursor using an
20 engineered microbe.

Some aspect of this invention relate to an isolated oleaginous cell, comprising a genetic modification that increases expression of one or more genes chosen from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC, SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA synthetase, Pyruvate carboxylase, and AMPK genes,
25 and/or a genetic modification that reduces expression of a gene chosen from the group of JNK2 and delta-12 desaturase. In some embodiments, the isolated oleaginous cell comprises a nucleic acid construct comprising (a) an expression cassette comprising a nucleic acid encoding the gene product under the control of a suitable homologous or heterologous promoter; (b) an expression cassette comprising a nucleic acid encoding an interfering RNA
30 targeting the gene product under the control of a heterologous promoter; and/or (c) a nucleic acid construct inserted into the genome of the cell, the construct comprising a nucleic acid sequence that increases or decreases the expression of the gene product. In some

embodiments, the heterologous promoter is an inducible or a constitutive promoter. In some embodiments, the nucleic acid construct inhibits or disrupts the natural regulation of a native gene encoding the gene product resulting in overexpression of the native gene. In some embodiments, the nucleic acid construct inhibits or abolishes expression of the native gene.

- 5 In some embodiments, inhibition or disruption of the natural regulation of the native gene is mediated by deletion, disruption, mutation and/or substitution of a regulatory region, or a part of a regulatory region regulating expression of the gene, or inhibition or abolition of the expression of a native gene is mediated by deletion, disruption, mutation and/or substitution of a coding sequence of the native gene, or of a regulatory region, or a part of a regulatory region regulating expression of the native gene. In some embodiments, the decreased
- 10 expression of the JNK2 and/or delta-12 desaturase gene is mediated by constitutive or inducible expression of a nucleic acid targeting a JNK2 and/or delta-12 desaturase gene product and inhibiting the expression of the gene. In some embodiments, the nucleic acid targeting the JNK2 and/or delta-12 desaturase transcript inhibits expression of the transcript
- 15 via an RNAi pathway. In some embodiments, the nucleic acid targeting the JNK2 and/or delta-12 desaturase transcript is an siRNA, an shRNA, or a microRNA. In some embodiments, a decrease of expression of JNK2 or delta-12 desaturase is achieved by knocking out the wild type gene in the microbe, for example, by homologous recombination of a nucleic acid construct, e.g., a targeting vector, with the genomic JNK2 or delta-12
- 20 desaturase locus, thus disrupting the expression of the wild type gene. In some embodiments, the nucleic acid construct is inserted into the genome of the cell. In some embodiments, the increased or decreased expression of the gene product confers a beneficial phenotype for the conversion of a carbohydrate source to a fatty acid, fatty acid derivative and/or TAG to the cell. In some embodiments, the beneficial phenotype is a modified fatty acid profile, a
- 25 modified triacylglycerol profile, an increased fatty acid and/or triacylglycerol synthesis rate, an increase conversion yield, an increased triacylglycerol accumulation in the cell, and an increased tolerance of osmotic stress, an increased proliferation rate, an increased cell volume, and/or an increased tolerance of a substance at a concentration lethal to and/or inhibiting proliferation of unmodified cells of the same cell type, by the cell. In some
- 30 embodiments, the modified fatty acid profile or the modified triacylglycerol profile of the cell exhibits at least a 2-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type. In some embodiments, the modified fatty

acid profile or the modified triacylglycerol profile of the cell exhibits at least an 2.5-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type. In some embodiments, the modified fatty acid profile or the modified triacylglycerol profile of the cell exhibits at least a 5-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type. In some embodiments, the modified fatty acid profile or the modified triacylglycerol profile of the cell exhibits at least a 6.5-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type. In some embodiments, the cell is viable under conditions of osmotic stress lethal to unmodified cells. In some embodiments, the cell is viable under conditions of osmotic stress at a level of 200% of the highest level tolerated by unmodified cells. In some embodiments, the cell is viable under conditions of osmotic stress at a level of 300% of the highest level tolerated by unmodified cells. In some embodiments, the cell is viable under conditions of osmotic stress at a level of 400% of the highest level tolerated by unmodified cells. In some embodiments, the cell proliferation rate is at least 5-fold, at least 10-fold, at least 20-fold, at least 25-fold, or at least 30-fold increased as compared to unmodified cells of the same cell type. In some embodiments, the volume of the cell is at least 2-fold increased as compared to unmodified cells of the same cell type. In some embodiments, the cell tolerates a substance at a concentration lethal to and/or inhibiting proliferation of unmodified cells of the same cell type. In some embodiments, the substance is a fermentable sugar and the concentration is at least 80g/l, at least 100g/l, at least 150g/l, at least 200g/l, at least 300g/l. In some embodiments, the synthesis rate of a fatty acid or a triacylglycerol of the cell is at least 5-fold, or at least 10-fold, increased as compared to unmodified cells of the same cell type. In some embodiments, the cell converts a carbohydrate source to a fatty acid or a triacylglycerol at a conversion rate of at least about 20g/g, at least about 25g/g, or at least about 30g/g. In some embodiments, the cell is a prokaryotic cell or a eukaryotic cell. In some embodiments, the cell is a bacterial cell, an algal cell, a fungal cell, or a yeast cell. In some embodiments, the cell is an oleaginous yeast cell. In some embodiments, the cell is a *Y. lipolytica* cell.

Some aspects of this invention relate to a culture, comprising an isolated oleaginous cell, comprising a genetic modification that increases expression of one or more genes chosen from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC, SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA synthetase, Pyruvate

carboxylase, and AMPK genes, and/or a genetic modification that reduces expression of a JNK2 and/or delta-12 desaturase gene product, and a carbohydrate source. In some embodiments, the isolated oleaginous cell is an engineered microbe as provided herein. In some embodiments, the carbohydrate source is a fermentable sugar. In some embodiments, the carbohydrate source is a monomeric sugar. In some embodiments, the carbohydrate source is glucose and glycerol. In some embodiments, the carbohydrate source is not sterilized. In some embodiments, the culture is maintained under non-sterile conditions. In some embodiments, the culture does not comprise an antibiotic or antiproliferative agent selective for the isolated oleaginous cell. In some embodiments, the carbohydrate source is derived from plant or algal biomass. In some embodiments, the carbohydrate source is derived from cellulose, hemi-cellulose, starch, glycerol, or a derivative thereof. In some embodiments, the culture further comprises a cellulose- or hemi-cellulose-hydrolyzing enzyme. In some embodiments, the biomass or the cellulose or hemi-cellulose is pretreated in a hot water or dilute acid or ammonia fiber expansion procedure, with a hydrolyzing enzyme, with a steam pre-treatment, and/or a lime pre-treatment. In some embodiments, the culture comprises a substance at a concentration lethal to unmodified wild type, unmodified cells of the same cell type as the isolated oleaginous cell. In some embodiments, the substance is a toxic substance generated during pretreatment of the carbohydrate source such as acetic acid, furfural or aromatic compounds. In some embodiments, the substance is the carbohydrate source. In some embodiments, the substance is a fermentable sugar. In some embodiments, the substance is a monomeric sugar. In some embodiments, the culture comprises the fermentable sugar at a concentration of at least 80g/l, at least 100g/l, at least 150g/l, at least 200g/l, at least 250g/l, or at least 300g/l.

Some aspects of this invention relate to a method, comprising contacting a carbohydrate source with an isolated oleaginous cell, the cell comprising a genetic modification that increases expression of one or more genes chosen from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC, SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA synthetase, Pyruvate carboxylase, and AMPK gene products, and/or a genetic modification that reduces expression of a JNK2 and/or a delta-12 desaturase gene, and incubating the carbohydrate source contacted with the cell under conditions suitable for at least partial conversion, of the carbohydrate source into a fatty acid or a triacylglycerol by the cell. In some embodiments, the isolated oleaginous cell is an

engineered microbe as provided herein. In some embodiments, the carbohydrate source is a sugar, such as glucose, xylose etc or starches derived from plant or algal biomass. In some embodiments, the carbohydrate source is derived from cellulose or hemi-cellulose. In some embodiments, the carbohydrate source is contacted with the cell in the presence of a cellulose- or hemi-cellulose-hydrolyzing enzyme. In some embodiments, the carbohydrate source is contacted with the cell in the presence of about 15 IU of cellulose- or hemi-cellulose-hydrolyzing enzyme per g of biomass at 55°C for 48 hours. In some embodiments, the biomass or the cellulose or hemi-cellulose is pretreated with hot water or dilute acid or ammonia fiber expansion procedure and/or a hydrolyzing enzyme. In some embodiments, the carbohydrate source contacted with the isolated oleaginous cell comprises a substance at a concentration lethal to unmodified cells of the same cell type as the isolated oleaginous cell. In some embodiments, the substance is a toxic substance generated during pretreatment of the carbohydrate source, for example, acetic acid. In some embodiments, the substance is the carbohydrate source. In some embodiments, the carbohydrate source is a fermentable sugar and the concentration of the fermentable sugar is at least 80g/l, at least 100g/l, at least 200g/l, or at least 300g/l after contacting with the oleaginous cell. In some embodiments, the carbohydrate source is contacted with the isolated oleaginous cell under non-sterile conditions. In some embodiments, the carbohydrate source contacted with the isolated oleaginous cell is incubated under non-sterile conditions. In some embodiments, the carbohydrate source contacted with the isolated oleaginous cell is incubated in an open reactor. In some embodiments, the carbohydrate source is contacted with the isolated oleaginous cell and incubated for conversion of the carbohydrate source to a fatty acid or a triacylglycerol in a fed batch process. In some embodiments, the carbohydrate source is contacted with the isolated oleaginous cell and incubated for conversion of the carbohydrate source to a fatty acid or a triacylglycerol in a continuous process. In some embodiments, the fatty acid or the triacylglycerol is extracted from the carbohydrate source contacted with the isolated oleaginous cell by solvent extraction. In some embodiments, the solvent extraction is a solvent hexane extraction. In some embodiments, the fatty acid or the triacylglycerol is separated from the carbohydrate source contacted with the isolated oleaginous cell and subsequently refined by transesterification.

Some aspects of this invention relate to a method, comprising modifying the fatty acid profile, the triacylglycerol profile, the fatty acid synthesis rate, the triacylglycerol synthesis

rate, the extent of fatty acid derivative accumulation in the cell, the rate of fatty acid derivative secretion, the rate of carbohydrate to fatty acid or fatty acid derivative conversion, the efficient yield of carbohydrate to fatty acid or fatty acid derivative conversion, the tolerance of osmotic stress, the proliferation rate, the cell volume, or the tolerance of a toxic substance of a cell for use in the conversion of a carbohydrate source into a fatty acid or triacylglycerol by increasing the expression of one or more gene product(s) chosen from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC, SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, and AMPK gene products, and/or decreasing expression of a JNK2 and/or a delta-12 desaturase gene. In some embodiments, modifying the fatty acid profile, the triacylglycerol profile, the fatty acid synthesis rate, the triacylglycerol synthesis rate, the extent of fatty acid derivative accumulation in the cell, or the rate of fatty acid derivative secretion of the cell is increasing the amount of a fatty acid, a fatty acid derivative, and/or a triacylglycerol is synthesized, accumulated, or secreted by the cell. In some embodiments, modifying the efficiency of carbohydrate to fatty acid or fatty acid derivative conversion of the cell is increasing the efficiency of conversion by at least 2-fold, at least 3-fold, at least 4-fold, or at least 5-fold. In some embodiments, the fatty acid derivative is a triacylglycerol. In some embodiments, modifying the tolerance of osmotic stress, or the tolerance of a toxic substance of the cell is conferring tolerance of osmotic stress or of a toxic substance at a level lethal to unmodified cells of the same cell type. In some embodiments, modifying the proliferation rate is increasing the proliferation rate at least 2-fold, at least 5-fold, at least 10-fold, at least 20-fold, or at least 30-fold. In some embodiments, modifying the cell volume is increasing the cell volume at least 2-fold. In some embodiments, the cell is a yeast cell. In some embodiments, the yeast is an oleaginous yeast. In some embodiments, the oleaginous yeast is *Y. lipolytica*.

Some aspects of this invention relate to an isolated nucleic acid molecule comprising a) a nucleotide sequence that encodes SEQ ID NO:1 (*Y. lipolytica* SCD), or b) a nucleotide sequence that is at least 85% identical to the nucleotide sequence of (a). In some embodiments, the nucleotide sequence that encodes SEQ ID NO:1 is SEQ ID NO:2. In some embodiments, the nucleotide sequence is at least 85% identical to the nucleotide sequence of SEQ ID NO:2. In some embodiments, the nucleotide sequence is at least 90% identical to the nucleotide sequence of SEQ ID NO:2. In some embodiments, the nucleotide sequence is at least 95% identical to the nucleotide sequence of SEQ ID NO:2. In some embodiments, the

nucleotide sequence is at least 97.5% identical to the nucleotide sequence of SEQ ID NO:2. In some embodiments, the nucleotide sequence is at least 99% identical to the nucleotide sequence of SEQ ID NO:2. In some embodiments, a nucleic acid construct is provided that comprises an isolated nucleic acid molecule as described herein, for example, an isolated nucleic molecule as described in this paragraph, and a heterologous isolated promoter. In some embodiments, the promoter is a constitutive promoter or an inducible promoter. In some embodiments, the constitutive promoter is a Translation Elongation Factor (TEF) promoter. In some embodiments, the inducible promoter is a drug-inducible promoter. In some embodiments, the isolated nucleic acid molecule includes a modified SCD promoter. In some embodiments, the modification is a deletion, complete or partial, and/or a mutation of a wild-type SCD promoter sequence resulting in a disruption of the feedback inhibition of said SCD promoter in response to high levels of a fatty acid, a fatty acid derivative, and/or a triacylglycerol. In some embodiments, the modification is an insertion of a heterologous sequence into a wild-type SCD promoter region, optionally associated with a deletion, complete or in part, and/or a mutation of a wild-type SCD promoter sequence, resulting in a disruption of the feedback inhibition of said SCD promoter in response to high levels of a fatty acid, a fatty acid derivative, and/or a triacylglycerol.

Some aspects of this invention relate to a vector comprising an expression cassette, for example any of the expression cassettes mentioned herein. Some aspects of this invention relate to a cell comprising an expression cassette as described herein or at least a part of a vector as described herein.

The subject matter of this application may involve, in some cases, interrelated products, alternative solutions to a particular problem, and/or a plurality of different uses of a single system or article.

Other advantages, features, and uses of the invention will become apparent from the following detailed description of non-limiting embodiments of the invention when considered in conjunction with the accompanying drawings. In cases where the present specification and a document incorporated by reference include conflicting disclosure, the present specification shall control.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1: Fatty acid profiling of *Yarrowia lipolytica*. A) a log phase culture of *Y.*

lipolytica grown in minimal media was assayed for total free fatty acid (FFA) using gas chromatography-mass spectroscopy (GC-MS) in a shake flask experiment. B) Total FFA was assayed in the same culture under same conditions during the stationary growth phase. C) Total lipids (FFA and esterified fatty acids) were assayed in the same culture during stationary phase.

Figure 2: Analysis of total lipids in *Yarrowia lipolytica*. A) Wild type *Y. lipolytica* strain grown in minimal media until 72-hour stationary phase culture and assayed for total lipids using GC-MS in a shake flask experiment. B) Total lipids were assayed in the mutant strain grown to stationary phase (72 hours) and over-expressing SCD, a native $\Delta 9$ desaturase under the control of a quasi-constitutive promoter. C) Confocal microscopy on wild type strain grown to stationary phase was stained with Nile red. D) Mutant strain grown to stationary phase was stained with Nile red and analyzed with confocal microscope.

Figure 3: Glucose consumption of *Y. lipolytica* mutant-1 (overexpressing cytochrome B, hemoglobin, Glut1, and $\Delta 9$ -desaturase (SCD), (D9, ■)); and the wild type (LS, ♦) on pure glucose in shake flask. *Y. lipolytica* mutant-1 exhibits a faster glucose consumption characteristics as compared to wild type *Y. lipolytica* and also a complete glucose consumption as compared to the incomplete consumption observed in the wild type.

Figure 4: A) Sugar consumption in *Y. lipolytica* mutant 1 (overexpressing cytochrome B, hemoglobin, Glut1, and $\Delta 9$ -desaturase (SCD)), and mutant 2 (overexpressing cytochrome B, hemoglobin, and Glut1) in 72 hours in corn stover hydrolyzate (Hz). B) Oil production in mutant 1 and mutant 2 hours in corn stover Hz.

Figure 5: Comparison of growth characteristics of wild type and engineered microbes. YL-eng: mutant *Y. lipolytica* overexpressing $\Delta 9$ -desaturase (SCD). YL-wild: wild-type *Y. lipolytica*. Cells were grown in minimal media containing a sugar concentration of 250 g/l. While the wild type cells failed to grow under these conditions, the mutant cells were able to tolerate the high level of sugars and grew well, suggesting that higher biofuel or biofuel precursor productivity can be achieved in processes using mutant strains. Y-axis: OD values. X-axis: time in hours.

Figure 6: Sugar consumption and growth characteristics of a *Y. lipolytica* mutant overexpressing $\Delta 9$ -desaturase (SCD). Cells were grown in media containing 160 g/l sugar and OD and sugar consumption of the culture were monitored. The mutant cells consumed the supplied sugar within 48 hours, and continued to grow after fed-batch replenishment of

sugars. This figure exemplifies an embodiment useful for fed-batch operations and semi-continuous biofuel production processes.

Figure 7: Lipid production of engineered *Y. lipolytica* (overexpressing $\Delta 9$ -desaturase (SCD), Cytochrome B and hemoglobin).

5 Figure 8: Fatty acid profiles of mutant strain (overexpressing $\Delta 9$ -desaturase (SCD), cytochrome B and hemoglobin; left bar in each set) and wild type *Y. lipolytica* strain (right bar in each set) after 72h of culture.

Figure 9: Growth kinetics of different mutant *Y. lipolytica* strains compared to wild type *Y. lipolytica*. CB: cytochrome B overexpressor. D9: SCD overexpressor.

10 Figure 10: Growth kinetics of different mutant *Y. lipolytica* strains compared to wild type *Y. lipolytica* at different glucose levels. Wild: wild-type *Y. lipolytica*; C18: mutant *Y. lipolytica* overexpressing $\Delta 9$ -desaturase (SCD).

Figure 11: Growth and lipid production kinetics of mutant (overexpressing $\Delta 9$ -desaturase (SCD)) and wild type *Y. lipolytica*.

15 Figure 12: pYLEX1, an expression vector useful for transgene expression in *Y. lipolytica* (A). The vector, which is well known to those of skill in the art, may include a selection marker, or a defective URA3 marker, which is derived from the URA3 gene of *Y. lipolytica*, which allows complementation of auxotrophy for uracil, such as the URA3d markers described by LE DALL et al., Curr. Genet., 26, 38-44 (1994). The sequences for
20 controlling the expression are, for example, promoter and terminator sequences which are active in *Yarrowia*. In some embodiments, the vector comprises an inducible or constitutive promoter. In some embodiments, genes can be overexpressed in microbes from pYLEX1, for example, by cloning a construct of interest, e.g., a SCD cDNA under the control of a promoter, into pYLEX1. Exemplary cloning of cytochrome B and hemoglobin cDNAs under
25 the control of a TEF promoter are shown (B, C).

Figure 13: Growth of engineered microbe on algal biomass. Dried algae was obtained and autoclaved to break cells and gelatinize starches. The autoclaved cells were enzymatically treated with alpha-amylase to release glucose. The resulting media was inoculated with our mutant yeast cells containing $\Delta 9$ -desaturase and Cytochrome, Glut1, and
30 hemoglobin. The chart shows robust growth of *Yarrowia* mutant in fermentation media without any additive. The cells obtained OD 43 in 4-5 days. This shows there is no inhibition on growth of mutant yeast.

Figure 14: Microscopy of the yeast cells grown in algae hydrolysates. Cells were grown in the conditions described in Figure 13. Cells were harvested and stained with Nile Red to identify oil. The droplets inside the yeast cells represents oil.

Figure 15: Microscopy of the yeast cells grown in crude glycerol. Cells were harvested and stained with Nile Red to identify oil. The droplets inside the yeast cells represent oil.

Figure 16: Schematic structure of a delta-12 desaturase knockout construct containing delta-12 desaturase gene flanking regions and antibiotic resistance sequence, that is used to generate delta-12 desaturase knockout strains.

Figure 17: Growth of engineered microbes on 3% acetate with addition of 2% glycerol at 84 hrs.

DETAILED DESCRIPTION

INTRODUCTION

In view of diminishing fossil fuel resources, numerous research efforts have been directed to develop renewable alternatives. One promising approach is to engineer microbes for the production of biofuels, for example, biodiesel or biodiesel precursors, such as triacylglycerols, from renewable carbon sources, for example, by using microbes that produce fatty acids or fatty acid derivatives. Microalgae as a raw material for biofuels production (Gouveia L, Oliveira AC. *J Ind Microbiol Biotechnol*. 2009 Feb;36(2):269-74). While some aspects of this invention relate to the use of photosynthetic microbes, such as algae, for biofuel or biofuel precursor production, the use of photosynthetic microbes creates a set of technological challenges (Cadoret JP, Bernard O. *J Lipid biofuel production with microalgae: potential and challenges* Soc Biol. 2008; 202(3):201-11). The focus of research efforts is shifting towards the engineering of microbes for converting renewable carbon sources, for example, biomass-derived fermentable sugars (e.g., glucose or sugars from corn or sugarcane) or non-fermentable carbohydrate polymers (e.g. cellulose or hemicellulose) to biofuel or biofuel precursors in dark fermentation processes.

Economically viable production of biofuel requires (i) the identification of a suitable microbe, and (ii) the engineering of a required and/or desirable phenotype, which may include multiple traits, in the microbe. Examples of such required and/or desirable traits in such a phenotype include, but are not limited to, rapid and efficient biomass production,

growth advantage over undesired microbes, efficient, ideally near-theoretical carbohydrate to oil conversion, and high substrate and end-product tolerance. Some of these traits are prerequisites for economically viable, microbe-based biofuel production at an industrial-scale. Ideally, the engineered microbe should display a combination of beneficial traits

5 conferring a phenotype allowing for efficient conversion of an abundant carbon source to a biofuel or biofuel precursor in a scalable, cost-efficient manner.

MICROBIAL PRODUCTION OF A BIOFUEL OR BIOFUEL PRECURSOR

Some aspects of this invention relate to microbe-mediated production of biofuel or

10 biofuel precursor. The term "biofuel" refers to a fuel that is derived from a biological source, such as a living cell, microbe, fungus, or plant. The term includes, for example, fuel directly obtained from a biological source, for example, by conventional extraction, distillation, or refining methods, and fuel produced by processing a biofuel precursor obtained from a biological source, for example by chemical modification, such as transesterification

15 procedures. Examples of biofuels that are directly obtainable are alcohols such as ethanol, propanol, and butanol, fat, and oil. Examples of biofuels that are obtained by processing of a biofuel precursor (e.g., a lipid), are biodiesel (e.g., produced by transesterification of a lipid), and green diesel/modified oil fuels (e.g., produced by hydrogenation of an oil). Biodiesel, also referred to as fatty acid methyl (or ethyl) ester, is one of the economically most

20 important biofuels today and can be produced on an industrial scale by transesterification of lipids, in which sodium hydroxide and methanol (or ethanol) reacts with a lipid, for example, a triacylglycerol, to produce biodiesel and glycerol. Feedstocks for industrial-scale production of biodiesel include animal fats, vegetable oils, palm oil, hemp, soy, rapeseed, flax, sunflower, and oleaginous algae. In other approaches, biomass is converted by a

25 microbe into a biofuel precursor, for example, a lipid, that is subsequently extracted and further processed to yield a biofuel. The term "biomass" refers to material produced by growth and/or propagation of a living cell or organism, for example, a microbe. Biomass may contain cells, microbes and/or intracellular contents, for example cellular fatty acids and TAGS, as well as extracellular material. Extracellular material includes, but is not limited to,

30 compounds secreted by a cell, for example, secreted fatty acids or TAGs. Important types of biomass for biofuel production are algal biomass and plant-derived biomass, for example, corn stover and wood fiber. In some embodiments, biomass for biofuel or biofuel precursor

production may comprise plant derived sugars, for example, sugarcane or corn derived sugars.

Some aspects of this invention relate to the identification, engineering, and development of a microbial source of lipids for economically viable, industrial-scale biodiesel production, none of which has previously been reported. The term “lipid” refers to fatty acids and their derivatives. Accordingly, examples of lipids include fatty acids (FA, both saturated and unsaturated); glycerides or glycerolipids, also referred to as acylglycerols (such as monoglycerides (monoacylglycerols), diglycerides (diacylglycerols), triglycerides (triacylglycerols, TAGs, or neutral fats); phosphoglycerides (glycerophospholipids); nonglycerides (sphingolipids, sterol lipids, including cholesterol and steroid hormones, prenol lipids including terpenoids, fatty alcohols, waxes, and polyketides); and complex lipid derivatives (sugar-linked lipids or glycolipids, and protein-linked lipids). Lipids are an essential part of the plasma membrane of living cells and microbes. Some cells and microbes also produce lipids to store energy, for example in the form of triacylglycerols in lipid droplets.

Some aspects of this invention relate to the identification of a microbe for biofuel or biofuel precursor production based on a suitable lipid metabolism of the microbe. The term “lipid metabolism” refers to the molecular processes that involve the creation or degradation of lipids. Fatty acid synthesis, fatty acid oxidation, fatty acid desaturation, TAG synthesis, TAG storage and TAG degradation are examples of processes that are part of the lipid metabolism of a cell. Accordingly, the term “fatty acid metabolism” refers to all cellular or organismic processes that involve the synthesis, creation, transformation or degradation of fatty acids. Fatty acid synthesis, fatty acid oxidation, TAG synthesis, and TAG degradation are examples of processes are part of the fatty acid metabolism of a cell.

The term “triacylglycerol” (TAG, sometimes also referred to as triglyceride) refers to a molecule comprising a single molecule of glycerol covalently bound to three fatty acid molecules, aliphatic monocarboxylic acids, via ester bonds, one on each of the glycerol molecule’s three hydroxyl (OH) groups. Triacylglycerols are highly concentrated stores of metabolic energy because of their reduced, anhydrous nature, and are a suitable feedstock for biodiesel production.

Many cells and organisms store metabolic energy in the form of fatty acids and fatty acid derivatives, such as TAGs. Fatty acids and their derivatives, such as TAGs, provide an

ideal form to store metabolic energy. The energy contained in the C–C bonds can be efficiently released by β -oxidation, a reaction formally equivalent to the reverse of fatty acid biosynthesis, but mediated and regulated by different enzymes constituting a different molecular pathway. Microbes can derive fatty acids from external supply, endogenous turnover, and de novo synthesis. Some aspects of this invention relate to the identification of a microbe for biofuel or biofuel precursor production based on the microbe's ability to synthesize and store fatty acids or fatty acid derivatives, such as TAGs, efficiently from an externally supplied carbon source.

A MICROBE FOR BIOFUEL PRODUCTION

Some aspects of this invention relate to the identification of a suitable microbe for industrial-scale carbohydrate-to-lipid conversion for biofuel or biofuel precursor production. No suitable microbe has been identified so far that would allow for economically viable production of biofuel or a biofuel precursor from a carbohydrate source on an industrial scale.

Some aspects of this invention relate to the identification of an oleaginous yeast, *Y. lipolytica*, as an organism for biofuel or biofuel precursor production based on *Y. lipolytica*'s favorable base metabolism.

Y. lipolytica is a non-pathogenic oleaginous yeast that can use a variety of carbon sources, including organic acids, hydrocarbons and various fats and oils. The term "oleaginous" refers to a microbe that can accumulate more than 20% of its dry cell weight as lipid (see C. Ratledge et al., *Microbial routes to lipids*. Biochem Soc Trans. 1989 Dec;17(6):1139-41). According to some aspects of this invention, *Y. lipolytica* represents a microbe for biofuel or biofuel precursor production, because *Y. lipolytica* is an obligate aerobe with the ability to assimilate carbohydrates, for example, glucose, or glycerol as a sole carbon source, and, compared to other yeast strains, *Y. lipolytica* has a higher glucose to fatty acid and triacylglycerol (TAG) flux and higher lipid storage capacity. See, e.g., Beopoulos A, Cescut J, Haddouche R, Uribe Larrea JL, Molina-Jouve C, Nicaud JM, *Yarrowia lipolytica* as a model for bio-oil production. Prog Lipid Res. 2009 Nov;48(6):375-87. Further, *Y. lipolytica* is one of the more intensively studied 'non-conventional' yeast species and genome sequencing, including mitochondrial DNA, of *Y. lipolytica* was completed recently. Kerscher S, Durstewitz G, Casaregola S, Gaillardin C, Brandt U., *The complete mitochondrial genome of Yarrowia lipolytica*. Comp Funct Genomics. 2001;2(2):80-90. The availability of genomic

sequence data makes genetic manipulation more accessible., even though functional annotation of genomic sequences is not complete. See, e.g., Sokolova L, Wittig I, Barth HD, Schägger H, Brutschy B, Brandt U., *LILBID-mass spectrometry of protein complexes from blue-native gels, a sensitive top-down proteomic approach*. Proteomics. Published online
5 2010 Feb 1, PMID: 20127694.

In wild type *Y. lipolytica*, fatty acid and TAG synthesis from a carbon source is triggered during the stationary growth phase, suggesting a tight regulatory mechanism in place to control lipid metabolism. This regulatory mechanism controls the amount of lipids that can be synthesized and stored, which significantly limits the conversion yield of
10 feedstock to lipids. Accordingly, the metabolic parameters of wild type *Y. lipolytica* are not suitable for economically viable industrial-scale biofuel or biofuel precursor production.

A MICROBIAL KEY REGULATOR OF FATTY ACID METABOLISM

Some aspects of this invention relate to the surprising discoveries that (i) saturated
15 fatty acids inhibit de novo fatty acid synthesis and TAG storage via a feedback loop, and (ii) that overexpression of SCD, a $\Delta 9$ -desaturase, in a microbe suitable for biofuel or biofuel precursor production, for example, *Y. lipolytica*, is sufficient to override this feedback inhibition of fatty acid synthesis and TAG storage, resulting in significantly increased synthesis, storage of fatty acids and/or TAGs.

Some aspects of this invention relate to the surprising discovery that, in addition to effecting increased synthesis and storage of fatty acids and/or TAGs, overexpression of SCD in a microbe further confers a beneficial phenotype for biofuel or biofuel precursor production to a microbe, for example, *Y. lipolytica*, including but not limited to: (i)
20 hyperactivation of the TAG storage pathway, (ii) growth advantage, (iii) continuous oil production, (iv) elevated tolerance to carbohydrate source substances (e.g. glucose and other
25 sugars) in the culture medium and (v) fatty acid profile modification, e.g. a shift of the ratios of saturated to unsaturated fatty acids favorable for biofuel or biofuel precursor production.

The discovery of SCD as a key regulator of fatty acid metabolism and TAG synthesis in oleaginous microbes according to this invention has major implication for processes
30 aiming to convert renewable carbon sources into biofuel or biofuel precursor with the help of engineered cells. Based on some aspects of this invention it is now possible to modify the fatty acid and/or TAG profile of a microorganism, for example an oleaginous yeast such as *Y.*

lipolytica, in a way that confers highly desirable phenotypes for industrial-scale carbohydrate to biofuel or biofuel precursor conversion, such as remarkable increases in fatty acid synthesis, TAG synthesis, fatty acid and TAG, biomass production, and elevated tolerance of high substrate, product, and/or toxin concentration in the culture medium.

5 According to some aspects of this invention, modifying the lipid or fatty acid metabolism in a microbe in accordance with methods provided herein, for example by overexpressing SCD alone or in combination with other genetic or non-genetic modifications provided herein, allows for the generation of a microbe optimized for use in biofuel or biofuel precursor production processes. Some aspects of this invention relate to the engineering of
10 the fatty acid metabolism in a microbe, resulting in increased synthesis rate and accumulation of fatty acids and fatty acid derivatives in the microbe.

Natural fatty acid molecules commonly have an unbranched, aliphatic chain, or tail, of 4 to 28 carbon atoms. Fatty acids are referred to as “saturated”, if all carbon atoms of the aliphatic chain are connected via a C-C single bond, or as “unsaturated”, if two or more
15 carbon atoms are connected via a C-C double bond. Unsaturated fatty acids play important roles in the regulation of membrane fluidity, cellular activity, metabolism and nuclear events governing gene transcription.

The spectrum of fatty acids in yeast consists mostly of C16 and C18 fatty acids, for example palmitic acid (C16), palmitoleic acid (C16), stearic acid (C18) and oleic acid (C18).
20 Palmitic acid is an unbranched, saturated fatty acid, with an aliphatic chain of 16 carbon atoms (carbon atoms/unsaturated bonds: 16.0). Stearic acid is an unbranched, saturated fatty acid with an aliphatic chain of 18 carbon atoms (18.0). Palmitoleic acid is a monounsaturated fatty acid with an aliphatic chain of 16 carbon atoms (16.1). Oleic acid is a monounsaturated fatty acid with an aliphatic chain of 18 carbon atoms (18.1). Minor fatty acid species in yeast
25 include C14 and C26 fatty acids, which play essential functions in protein modification or as components of sphingolipids and GPI anchors, respectively.

De novo synthesis of fatty acids utilizes substantial amounts of metabolites, acetyl-CoA, ATP and NADPH, and thus competes with other cellular processes that are dependent on these compounds. NADPH is required for two reduction steps in the fatty acid elongation
30 cycle, linking fatty acid synthesis to the metabolic state of the cell and results in fatty acid synthesis being restricted to conditions of high energy load of the cells, indicated by increased ATP/AMP ratio, elevated reduction equivalents and elevated acetyl-CoA pool.

Almost all subcellular organelles are involved in fatty acid metabolism, indicating that maintenance of fatty acid homeostasis requires regulation at multiple levels.

Most organisms, including yeast, are able to synthesize fatty acids *de novo* from a variety of carbon sources. In an initial step, acetyl-CoA is carboxylated by the addition of CO₂ to malonyl-CoA, by the enzyme acetyl-CoA carboxylase (ACC; encoded by ACC1 and HFA1 in yeast). Biotin is an essential cofactor in this reaction, and is covalently attached to the ACC apoprotein, by the enzyme biotin:apoprotein ligase (encoded by BPL1/ACC2 in yeast). ACC is a trifunctional enzyme, harboring a biotin carboxyl carrier protein (BCCP) domain, a biotin-carboxylase (BC) domain, and a carboxyl-transferase (CT) domain. In most bacteria, these domains are expressed as individual polypeptides and assembled into a heteromeric complex. In contrast, eukaryotic ACC, including mitochondrial ACC variants (Hfa1 in yeast) harbor these functions on a single polypeptide. Malonyl-CoA produced by ACC serves as a two carbon donor in a cyclic series of reactions catalyzed by fatty acid synthase, FAS, and elongases.

In yeast, the individual functions involved in cytosolic fatty acid synthesis are represented as discrete domains on a single or on two different polypeptide chains, respectively. Yeast cytosolic fatty acid synthase (FAS) is a complex composed of two subunits, Fas1 (β subunit) and Fas2 (α subunit) which are organized as a hexameric $\alpha_6\beta_6$ complex. Fas1 harbors acetyl transferase, enoyl reductase, dehydratase, and malonyl-palmitoyl transferase activities; Fas2 contains acyl carrier protein, 3-ketoreductase, 3-ketosynthase and the phosphopantetheine transferase activities.

Mitochondrial fatty acid synthesis in yeast is carried out by a type II FAS system, harboring the individual enzymatic activities on distinct polypeptides: Acp1, acyl-carrier protein which carries the prosthetic phosphopantetheine group; Cem1, β -ketoacyl-ACP synthase; Oar1, 3-oxoacyl-[acyl-carrier-protein] reductase; Htd2, 3-hydroxyacyl-thioester dehydratase; Etr1, enoyl-ACP reductase. Ppt2 functions as the phosphopantetheine: protein transferase, catalyzing the attachment of the phosphopantetheine prosthetic group to the apoACP.

The immediate product of *de novo* fatty acid synthesis are saturated fatty acids. Saturated fatty acids are known to be the precursors of unsaturated fatty acids in eukaryotes, including yeast. Unsaturated fatty acids are generally produced by desaturation of C-C single bonds in saturated fatty acids by specialized enzymes, called desaturases. The control

mechanisms that govern the conversion of saturated fatty acids to unsaturated fatty acids are not well understood. In eukaryotes, unsaturated fatty acids play important roles in the regulation of membrane fluidity, cellular activity, metabolism and nuclear events that govern gene transcription. Typically, about 80% of yeast fatty acids are monounsaturated, meaning that they contain one unsaturated bond in their aliphatic chain.

A critical committed step in the biosynthesis of monounsaturated fatty acids is the introduction of the first cis-double bond in the $\Delta 9$ position (between carbons 9 and 10). This oxidative reaction is catalyzed by stearoyl-CoA desaturase (SCD, also known as delta-9-desaturase, or $\Delta 9$ -desaturase). Although the insertion of the double bond occurs in several different methylene-interrupted fatty acyl-CoA substrates, the preferred substrates of SCD are palmitoyl (16.0)- and stearoyl (18.0)-CoA which are converted to palmitoleoyl (16.1)- and oleoyl (18.1)-CoA, respectively (Ntambi, J. Lipid Res., 1999, 40, 1549-1558).

In *S. cerevisiae*, a stearoyl-CoA desaturase gene was identified as Ole1 in 1990 (Stukey JE, et al., J Biol Chem., 1990, 265(33):20144-9). The human stearoyl-CoA desaturase gene was partially characterized in 1994 via isolation of a 0.76 kb partial cDNA from human adipose tissue (Li et al., Int. J. Cancer, 1994, 57, 50 348-352). The gene was fully characterized in 1999 and it was found that alternative usage of polyadenylation sites generates two transcripts of 3.9 and 5.2 kb (Zhang et al., Biochem. J., 1999, 340, 255-264). In *S. cerevisiae*, fatty acid monodesaturation is catalyzed by the endoplasmic reticulum (ER)-resident and essential $\Delta 9$ -desaturase, Ole1 (Martin CE, Oh CS, Jiang Y, *Regulation of long chain unsaturated fatty acid synthesis in yeast.* Biochim Biophys Acta. 2007 Mar;1771(3):271-85. Epub 2006 Jul 13).

Some aspects of this invention relate, at least in part, to the identification of the *S. cerevisiae* Ole1 homologue SCD in *Y. lipolytica*, as described herein.

Non-limiting examples of representative sequences of *Y. lipolytica* SCD are given below:

>gil50548053|ref|XP_501496.1| YALI0C05951p [*Yarrowia lipolytica*]

MVKNVDQVDLSQVDTIASGRDVNYKVKYTSQVMSQAYDDKGRHISEQPFTWANWHQHINWLNFIILV
IALPLSSFAAAPFVSFNWKTAFAVGYYMCTGLGITAGYHRMWAHRAKAAALPVRIILALFGGGAVEG
SIRWWASSHRVHHRWTDNKPYPYDARKGFWFSHFGWMLLPNPKNKGRTDISDLNNDWVRLQHKYYV
YVLVFMAIVLPTLVCGFGWGDWKGGLVYAGIMRYTFVQQVTFVCVNSLAHWIGEQQPFDDRRTPRDHALT
ALVTFGEGYHNFHHEFPDYNRNALIWYQYDPTKWLIIWTLKQVGLAWDLQTFSSQNAIEQGLVQQRQKKL
DKWRNNLWNGIPIEQLPVIEFEFQEQAQKTRDLVLISGIVHDVSAFVEHHPGGKALIMSAVGKDGTA

FNGGVYRHSNAGHNLLATMRVSVIRGGMEVEVWKTAQNEKKDQNIIVSDESGNRIHRAGLQATRVENPG
MSGMAA (SEQ ID NO:1)

>gil50548052|reflXM_501496.1| *Yarrowia lipolytica* YALI0C05951p (YALI0C05951g)

5 mRNA, complete cds

ATGGTGAAAAACGTGGACCAAGTGGATCTCTCGCAGGTCGACACCATTGCCTCCGGCCGAGATGTCAA
CTACAAGGTCAAGTACACCTCCGGCGTTAAGATGAGCCAGGGCGCCTACGACGACAAGGGCCGCCACA
TTTCCGAGCAGCCCTTACCTGGGCCAACTGGCACCAGCACATCAACTGGCTCAACTTCATTCTGGTG
ATTGCGCTGCCTCTGTGTCCTTTGCTGCCGCTCCCTTCGTCTCCTTCAACTGGAAGACCGCCGCGTT
10 TGCTGTGCGCTATTACATGTGCACCGGTCTCGGTATCACCGCCGGCTACCACCGAATGTGGGCCCATC
GAGCCTACAAGGCCGCTCTGCCCCGTTTGAATCATCCTTGCTCTGTTTGGAGGAGGAGCTGTGAGGGC
TCCATCCGATGGTGGGCCTCGTCTCACCGAGTCCACCACCGATGGACCGACTCCAACAAGGACCCTTA
CGACGCCCCGAAAGGGATTCTGGTTCTCCCACTTTGGCTGGATGCTGCTTGTGCCCAACCCCAAGAACA
AGGGCCGAACTGACATTTCTGACCTCAACAACGACTGGGTTGTCCGACTCCAGCACAAGTACTACGTT
15 TACGTTCTCGTCTTCATGGCCATTGTTCTGCCCACCTCGTCTGTGGCTTTGGCTGGGGCGACTGGAA
GGGAGGTCTTGTCTACGCCGGTATCATGCGATACACCTTTGTGCAGCAGGTGACTTTCTGTGTCAACT
CCCTTGCCCACTGGATTGGAGAGCAGCCCTTCGACGACCGACGAACCTCCCCGAGACCACGCTCTTACC
GCCCTGGTCACCTTTGGAGAGGGCTACCACAACCTCCACCACGAGTTCCTTCGGACTACCGAAACGC
CCTCATCTGGTACCAGTACGACCCACCAAGTGGCTCATCTGGACCCTCAAGCAGGTTGGTCTCGCCT
20 GGGACCTCCAGACCTTCTCCCAGAACGCCATCGAGCAGGGTCTCGTGCAGCAGCGACAGAAGAAGCTG
GACAAGTGGCGAAACAACCTCAACTGGGGTATCCCCATTGAGCAGCTGCCTGTCAATTGAGTTTGAGGA
GTTCCAAGAGCAGGCCAAGACCCGAGATCTGGTTCTCATTTCTGGCATTGTCCACGACGTGTCTGCCT
TTGTGAGCACCACCCTGGTGGAAAGGCCCTCATTATGAGCGCCGTCGGCAAGGACGGTACCGCTGTC
TTCAACGGAGGTGTCTACCGACACTCCAACGCTGGCCACAACCTGCTTGCCACCATGCGAGTTTCGGT
25 CATTCGAGGCGGCATGGAGGTTGAGGTGTGGAAGACTGCCCAGAACGAAAAGAAGGACCAGAACATTG
TCTCCGATGAGAGTGGAAACCGAATCCACCGAGCTGGTCTCCAGGCCACCCGGGTCGAGAACCCCGGT
ATGTCTGGCATGGCTGCTTAG (SEQ ID NO:2)

Stearoyl-CoA desaturase, or SCD, introduces a double bond at the Δ^9 -C of its
30 substrate fatty acids esterified with CoA. This activity affects the ratio of saturated to
unsaturated fatty acids, for example of stearic acid to oleic acid. Stearic acid is the primary
substrate for SCD, however other chain length fatty acids can be processed as well by SCD.
In humans, Stearoyl-CoA desaturase has been viewed as a lipogenic enzyme not only for its
key role in the biosynthesis of monounsaturated fatty acids, but also for its pattern of
35 regulation by diet and insulin (Ntambi, Lipid Res., 1999, 40, 1549-1558). The regulation of

stearoyl-CoA desaturase is, therefore, of considerable physiologic importance and its activity is sensitive to dietary changes, hormonal imbalance, developmental processes, temperature changes, metals, alcohol, peroxisomal proliferators and phenolic compounds (Ntambi, Lipid Res., 1999, 40, 1549-1558).

Animal models have been very useful in investigations of the regulation of stearoyl-CoA desaturase by polyunsaturated fatty acids (PUFAs). For example, in adipose tissue of lean and obese Zucker rats, Jones et al. observed a 75% decrease in stearoyl-CoA desaturase mRNA when both groups were fed a diet high in PUFAs relative to a control diet (Jones et al, Am. J. Physiol., 1996, 271, E44-49). Similar results have been obtained with tissue culture systems. In the murine 3T3-L1 adipocyte cell line, arachidonic, linoleic, linolenic, and eicosapentanoic acids decreased stearoyl-CoA desaturase expression in a dose- dependent manner (Sessler et al, J. Biol. Chem., 1996, 271, 29854-29858).

The molecular mechanisms by which PUFAs regulate stearoyl-CoA desaturase gene expression in different tissues are still poorly understood. The current understanding of the regulatory mechanism involves binding of PUFAs to a putative PUFA-binding protein, after which repression of transcription occurs via binding of the PUFA-binding protein to a cis-acting PUFA response element of the stearoyl-CoA desaturase gene (SREBP) (Ntambi, Lipid Res., 1999, 40, 1549-1558; Zhang et al, Biochem. J., 2001, 357, 183-193).

While the regulation of the catalytic activity of the SCD gene has been investigated in different organisms, the implications of SCD gene expression and regulation on lipid metabolism itself have not been the subject of extensive study. It has been stated that SCD affects the ratio of saturated to unsaturated fatty acids, for example of stearic acid to oleic acid.

Some aspects of this invention relate to the surprising discovery that SCD also functions as a key regulator of fatty acid and TAG metabolism in microbes, for example, in *Y. lipolytica*. Some aspects of this invention relate to the surprising discovery that overexpression of a SCD gene product alone not only skews the ratio of saturated to unsaturated fatty acids in the affected cells, but is sufficient to trigger remarkable and unexpected increases in fatty acid and/or TAG synthesis rates and/or storage. The unexpected finding that manipulation of desaturase expression alone confers highly desirable phenotypes to microbes, for example, oleaginous yeast cells, for industrial-scale carbohydrate to lipid conversion has far-reaching implications for the efficient production of biofuels or biofuel

precursors from renewable carbon sources by microbe-mediated fermentation processes.

Overriding downregulation of fatty acid synthesis and storage by overexpressing SCD in a microbe not only confers increased fatty acid synthesis rate and accumulation in the microbe, but also overrides the restriction of FA/TAG synthesis to the stationary phase of a microbe in culture. Surprisingly, overexpression of SCD in a microbe, for example, a microbe for biofuel or biofuel precursor production, also confers increased tolerance to high concentrations of substrate, for example, of fermentable sugars, and to substrate-associated toxic substances, for example, by-products of substrate pre-treatment procedures, to the microbe. The phenotypes conferred by SCD overexpression, for example the improved tolerance phenotypes described above, allow for obtaining high concentrations of lipids in industrial fermentation processes converting sugars to lipids. (See figure 11 for override of negative FA synthesis regulation by SCD over-expression)

According to some aspects of this invention, the manipulation of additional genes may be beneficial for the large-scale production of biofuel or biofuel precursor from a carbon source by microbial fermentation. For example, genes that effect the diversion of carbon-containing substrates, for example, sugars, to fatty acid synthesis. Accordingly, some aspects of this invention provide methods to manipulate the expression of genes involved in regulating carbon flux into or out of lipid synthesis pathways to achieve an improvement in lipid production parameters.

Some aspects of this invention provide a method for the manipulation of the expression and/or activity of other gene products regulating the lipid metabolism of microbes for biofuel or biofuel precursor production. Manipulations according to aspects of this invention are targeted to increase carbohydrate to fatty acid and/or TAG conversion in order to optimize the manipulated organism for large-scale production of lipids from carbohydrate sources. Manipulations provided according to some aspects of this invention, for example, overexpression, knockout, knock-down, activation and/or inhibition of specific gene products, may be effected alone or in combination, and/or in combination with other manipulations known to those of skill in the art. The term “manipulation” refers to both genetic manipulation, for example, overexpression, knockout, knock-down, activation and/or inhibition of specific gene products, and non-genetic manipulation, for example, manipulation of the growth media, substrate, substrate pretreatment, pH, temperature, conversion process, etc.

A manipulation of gene expression, also referred to herein as a modulation of gene expression, can be a disruption or inhibition of the natural regulation of expression, an overexpression, an inhibition of expression, or a complete abolishment of expression of a given gene. The insertion of a heterologous promoter upstream of a native gene sequence, for example the native SCD gene sequence, or the deletion of regulatory sequences within a promoter, for example regulatory sequences that mediate the feedback inhibition of the SCD gene by saturated fatty acids, are examples of a disruption or inhibition of the natural regulation of expression. Strategies for the modulation of gene expression may include genetic alterations, for example by recombinant technologies, such as gene targeting or viral transductions, or non-genetic alterations, for example environmental alterations known to result in the up- or down-regulation of gene expression, or transient delivery of modulators, for example drugs or small RNA molecules to the target cells. Methods for genetic and non-genetic alterations of microbes are well known to those of skill in the art, and are described, for example, in J. Sambrook and D. Russell, *Molecular Cloning: A Laboratory Manual*, Cold Spring Harbor Laboratory Press; 3rd edition (January 15, 2001); David C. Amberg, Daniel J. Burke; and Jeffrey N. Strathern, *Methods in Yeast Genetics: A Cold Spring Harbor Laboratory Course Manual*, Cold Spring Harbor Laboratory Press (April 2005); John N. Abelson, Melvin I. Simon, Christine Guthrie, and Gerald R. Fink, *Guide to Yeast Genetics and Molecular Biology, Part A, Volume 194* (Methods in Enzymology Series, 194), Academic Press (March 11, 2004); Christine Guthrie and Gerald R. Fink, *Guide to Yeast Genetics and Molecular and Cell Biology, Part B, Volume 350* (Methods in Enzymology, Vol 350), Academic Press; 1st edition (July 2, 2002); Christine Guthrie and Gerald R. Fink, *Guide to Yeast Genetics and Molecular and Cell Biology, Part C, Volume 351*, Academic Press; 1st edition (July 9, 2002); Gregory N. Stephanopoulos, Aristos A. Aristidou and Jens Nielsen, *Metabolic Engineering: Principles and Methodologies*, Academic Press; 1 edition (October 16, 1998); and Christina Smolke, *The Metabolic Pathway Engineering Handbook: Fundamentals*, CRC Press; 1 edition (July 28, 2009), all of which are incorporated by reference herein.

The term “overexpression”, as used herein, refers to an increased level of expression of a given gene in a given cell, cell type or cell state, as compared to a reference cell, for example, a wild type cell of the same cell type or a cell of the same cell type but lacking a specific modification, for example, a genetic modification. Forced, continuous expression of

the SCD gene in *Y. lipolytica* cells exhibiting concentrations of saturated fatty acids that would inhibit SCD gene expression in wild-type cells is an example of gene overexpression.

The term “knockout”, as used herein, refers to the functional disruption of the expression of a gene product, for example a RNA or protein. This is normally achieved by targeting a respective genomic region with a targeting construct, which recombines with a specific part of said genomic region and either deletes a part of said region and/or inserts a heterologous nucleotide or nucleotide sequence, resulting in a complete inhibition of expression of a gene product, for example a mRNA or protein, from the recombined gene. In diploids, such homologous recombination events normally only affect one of the two alleles. Homozygosity can be achieved by various strategies, for example by breeding heterozygotes and screening the offspring. In diploid organisms, for example yeast, the term “knockout strain” generally refers to a strain homozygous for a non-functional allele.

The term “knock-down”, as used herein, refers to the partial inhibition of the expression of a gene product, for example a mRNA or protein. Various strategies for gene knockdown known in the art can be used to inhibit gene expression (for example expression of a gene inhibiting or diverting resources away from lipid synthesis pathways, such as ACS2, FAT1, PCS60, and/or AMPK in oleaginous yeast, for example in *Y. lipolytica*). For example, gene knockdown strategies may be used that make use of RNA interference (RNAi) and/or microRNA (miRNA) pathways including small interfering RNA (siRNA), short hairpin RNA (shRNA), double-stranded RNA (dsRNA), miRNAs, and other small interfering nucleic acid-based molecules known in the art. In one embodiment, vector-based RNAi modalities (e.g., shRNA or shRNA-mir expression constructs) are used to reduce expression of a gene (for example of a gene inhibiting or diverting resources away from lipid synthesis pathways, such as ACS2, FAT1, PCS60, and/or AMPK) in a cell (for example in an oleaginous yeast cell, such as a *Y. lipolytica* cell). Isolated plasmids according to aspects of this invention may comprise a promoter operably linked to a gene encoding a small interfering nucleic acid, for example an shRNA. In some embodiments, an isolated plasmid vector may be employed to generate a viral particle, for example a retrovirus or bacteriophage, capable of infecting a cell, for example a yeast cell or bacterial cell. Exemplary viruses include adenovirus, retrovirus, lentivirus, adeno-associated virus, phages and others that are known in the art and disclosed herein.

Some aspects of this invention provide a method for the manipulation of the activity of a stearoyl-CoA-desaturase (SCD) in a microbe for biofuel or biofuel precursor production. SCD is a $\Delta 9$ desaturase that inserts a double bond between C9 and C10 of stearic acid coupled to CoA, a key step in the generation of desaturated fatty acids and their derivatives, as described in more detail elsewhere herein. In some embodiments, the manipulation is an overexpression. In some embodiments, the manipulation is effected by contacting a microbe for biofuel or biofuel precursor production with an expression construct comprising a nucleic acid coding for a SCD gene product, for example, a SCD protein, operably linked to a heterologous promoter, for example, a constitutive or an inducible promoter. In some embodiments, the nucleic acid coding for a SCD gene product comprises the coding sequence of SEQ ID NO: 2. In some embodiments, the SCD is *Y. lipolytica* SCD, for example, *Y. lipolytica* SCD comprising the amino acid sequence of SEQ ID NO: 1. In some embodiments, the microbe is *Y. lipolytica*. In some embodiments, manipulation of the activity of a SCD in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. Stearoyl-CoA Desaturase gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 852825 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a c-Jun N-terminal kinase 2 (JNK2) gene product in a microbe for biofuel or biofuel precursor production. JNK2 is localized to the cytoplasm and catalyzes the breakdown of fatty acids for energy and carbon block generation during starvation. JNK2 is required for energy homeostasis and plays a crucial role in lipase activation in response to low cellular sugar levels. See, Grimard V, Massier J, Richter D, Schwudke D, Kalaidzidis Y, Fava E, Hermetter A, Thiele C., *siRNA screening reveals JNK2 as an evolutionary conserved regulator of triglyceride homeostasis*. J Lipid Res. 2008 Nov;49(11):2427-40. Epub 2008 Jul 8. In some embodiments, JNK2 activity is abolished or decreased in a microbe for biofuel or biofuel precursor production, for example, by knockout or knockdown, respectively. In some embodiment, JNK2 activity is decreased in a microbe for biofuel or biofuel precursor production in order to increase product stability and/or decrease product catabolism. In some

embodiments, a conditional repression system is used and JNK2 activity is repressed during a phase in the production process in which the carbohydrate source, for example, a fermentable sugar, is very low. In some embodiments, manipulation of the activity of a JNK2 gene product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. JNK2 gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 5601 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a delta-12 desaturase gene product in a microbe for biofuel or biofuel precursor production. Delta-12 desaturase is involved in the conversion of oleic acid containing lipids to higher chain lipids. In some embodiments, it is desirable to avoid or minimize the production of long-chain fatty acids for the production of biofuel, for example, in view of the cold flow properties of the resulting biofuel. In some embodiments, delta-12 desaturase activity is abolished or decreased in a microbe for biofuel or biofuel precursor production, for example, by complete (e.g., knockout) or partial gene deletion or knockdown, respectively. In some embodiments, delta-12 desaturase activity is decreased in a microbe for biofuel or biofuel precursor production in order to increase product stability, achieve a desirable TAG profile in the microbe and/or decrease product catabolism. In some embodiments, a conditional repression system is used for the repression of delta-12 desaturase activity. In some embodiments, manipulation of the activity of a delta-12 desaturase gene product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage, increased content of C18 fatty acids, increased percentage of C18 fatty acids of the whole fatty acid pool in the microbe, improved cold flow properties of the produced lipids, oils, or TAGs, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. Delta-12 desaturase gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 2909806 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a hemoglobin gene product in a microbe for biofuel or biofuel precursor production. For an overview of hemoglobin gene products, including hemoglobin gene products useful in some embodiments of this invention, see, Frey AD, Kallio PT. *Bacterial hemoglobins and flavohemoglobins: versatile proteins and their impact on microbiology and biotechnology*. FEMS Microbiol Rev. 2003 Oct;27(4):525-45. In some embodiments, the activity of a hemoglobin gene product, for example, a hemoglobin protein, is increased in the microbe, for example, by overexpression of a hemoglobin protein-encoding nucleic acid. In some embodiments, overexpression of hemoglobin in the microbe effects increased oxygen transfer in the microbe. In some embodiments, increased hemoglobin activity results in improved biofuel or biofuel precursor synthesis, due to increased flux of oxygen into a highly oxygen demanding synthesis pathway, for example, the fatty acid synthesis pathway. In some embodiments, manipulation of the activity of a hemoglobin gene product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. Hemoglobin gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 7738539 (Deide_12990) in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a cytochrome gene product in a microbe for biofuel or biofuel precursor production, such as a cytochrome B gene product, more specifically a cytochrome B5 gene product. In some embodiments, the activity of a cytochrome gene product, for example, a cytochrome protein, is increased in the microbe, for example, by overexpression of a cytochrome protein-encoding nucleic acid. In some embodiments, overexpression of cytochrome in the microbe effects increased oxygen transfer in the microbe. In some embodiments, increased cytochrome activity results in improved biofuel or biofuel precursor synthesis, due to increased flux of oxygen into a highly oxygen demanding synthesis pathway, for example, the fatty acid synthesis pathway. In some embodiments, manipulation of the activity of a cytochrome gene product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased

carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. Cytochrome gene and gene product sequences are well known to those of skill in the art. An exemplary, representative gene sequence can be found under the entry for GeneID: 1528 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a glucose transporter (GLUT) gene product, for example, a Glut1 gene product, in a microbe for biofuel or biofuel precursor production. In some embodiments, the activity of a GLUT gene product, for example, a GLUT protein, is increased in the microbe, for example, by overexpression of a GLUT protein-encoding nucleic acid. In some embodiments, overexpression of a GLUT protein encoding nucleic acid in the microbe effects increased glucose uptake by the microbe. In some embodiments, increased GLUT activity results in improved biofuel or biofuel precursor synthesis, due to increased uptake of glucose. In some embodiments, manipulation of the activity of a GLUT gene product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. GLUT gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 38109 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a Pyruvate Carboxylase (PC) gene product in a microbe for biofuel or biofuel precursor production. In some embodiments, the activity of a PC gene product, for example, a PC protein, is increased in the microbe, for example, by overexpression of a PC protein-encoding nucleic acid. In some embodiments, overexpression of a PC protein encoding nucleic acid in the microbe effects increased glucose uptake by the microbe. In some embodiments, increased PC activity results in improved biofuel or biofuel precursor synthesis, due to increased uptake of glucose. In some embodiments, manipulation of the activity of a PC gene product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. PC gene and gene product

sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID:5091 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a malic enzyme (ME) gene product in a microbe for biofuel or biofuel precursor production. ME catalyzes the oxidative decarboxylation of (S)-malate to pyruvate, with the concomitant release of carbon dioxide and conversion of NADP⁺ to NADPH. In some embodiments, the activity of a ME gene product, for example, a ME protein, is increased in the microbe, for example, by overexpression of a ME protein-encoding nucleic acid. In some
10 embodiments, overexpression of a ME protein encoding nucleic acid in the microbe effects increased NADPH levels in the microbe, resulting in sufficient levels of reducing metabolites, for example, NADPH, for increased fatty acid synthesis. In some embodiments, increased ME activity results in improved biofuel or biofuel precursor synthesis, due to increased NADPH levels. In some embodiments, manipulation of the activity of a ME gene
15 product in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. ME gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and
20 gene product sequences can be found under the entry for GeneID: 17436 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of an acetyl-CoA carboxylase (ACC) gene product in a microbe for biofuel or biofuel precursor production, for example, in *Y. lipolytica*. ACC gene products mediate the conversion of
25 acetyl-CoA, the main C2-precursor in fatty acid synthesis, to malonyl-CoA, which is considered the first committed step in fatty acid synthesis and has been suggested to also be the rate-limiting step in fatty acid synthesis (see Cao Y, Yang J, Xian M, Xu X, Liu W. *Increasing unsaturated fatty acid contents in Escherichia coli by coexpression of three different genes*. Appl Microbiol Biotechnol. 2010). In some embodiments, ACC activity
30 manipulation is ACC overexpression. In some embodiments, ACC overexpression in a microbe increases fatty acid synthesis rate and/or confers a beneficial phenotype for large-scale carbohydrate to biofuel or biofuel precursor conversion, for example increased lipid

synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. ACC gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 855750 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of an Acyl-CoA synthetase (ACS) in a microbe for biofuel or biofuel precursor production. ACSs are a family of enzymes catalyzing the thioesterification of fatty acids with CoA to form activated intermediates (see Lu X, Vora H, Khosla C., *Overproduction of free fatty acids in E. coli: implications for biodiesel production* Metab Eng. 2008 Nov;10(6):333-9). These intermediates are the precursors for phospholipids, fatty acid cholesterol esters, or fatty acid alcohol esters, such as TAGs. *Y. lipolytica* contains two known and two predicted Acyl-CoA synthetases. In some embodiments of this invention, overexpression of an ACS enzyme in a lipid producing organism is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and/or secretion, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. ACS gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 851245 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of acetyl-CoA synthetase 2 (ACS2), an enzyme localized in the peroxisome and involved in the degradation of fatty acids, in a microbe for biofuel or biofuel precursor production. In some embodiments, inhibition of ACS2 prevents or inhibits degradation of fatty acids by yeast catabolic metabolism and, in some embodiments, such inhibition complements an increase in FAA1 gene product activity for increased fatty acid secretion into the medium. *Y. lipolytica* contains ACS2 acetyl-CoA synthetase (see Beopoulos A, Cescut J, Haddouche R, Uribe-larrea JL, Molina-Jouve C, Nicaud JM., *Yarrowia lipolytica as a model for bio-oil production*. Prog Lipid Res. 2009 Nov;48(6):375-87). In some embodiments, knockout, knock-down, and/or inhibition of ACS2 gene product expression or activity in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to biofuel or biofuel

precursor conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. ACS2 gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 850846 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of the activity of a FAA1 gene product in a microbe for biofuel or biofuel precursor production. The FAA1 gene product catalyzes the cytoplasmic thioesterification of long-chain fatty acids with CoA to produce activated intermediates. *Y. lipolytica* FAA1 is a homologue of *S. cerevisiae* P30624 FAA1 long-chain-fatty-acid-CoA ligase. This enzyme is involved in the generation of the free fatty acid pool and fatty acid secretion. In some embodiments, overexpression of a FAA1 gene product in a microbe for biofuel or biofuel precursor production is effected to confer a beneficial phenotype for large-scale carbohydrate to lipid conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to elevated concentrations of a carbon source or a lipid product. FAA1 gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 854495 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of very long-chain-fatty-acid-CoA synthetase (FAT1) activity in a microbe for biofuel or biofuel precursor production. FAT1 is thought to control the fatty acid transport and thioesterification of very long chain fatty acids with CoA. *Y. lipolytica* contains a FAT1 very-long-chain-fatty-acid-CoA synthetase. In some embodiments, inhibition of FAT1 activity, for example, by genetic manipulation, prevents synthesis of very long fatty acid derivatives and/or increases the pool of free fatty acids. In some embodiments, knockout, knock-down, and/or inhibition of FAT1 gene product expression or activity in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to biofuel or biofuel precursor conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. FAT1 gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene

and gene product sequences can be found under the entry for GeneID: 852329 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the manipulation of PCS60, also known as FAT2, AMP-binding protein acyl-CoA synthetase, or peroxisomal-CoA synthetase, which is a peroxisomal acyl-CoA synthetase with undefined substrate specificity. *Y.*

lipolytica contains a *S. cerevisiae* PCS60 homolog. PCS60 inhibition will prevent synthesis of very long fatty acid derivatives and increase the pool of free fatty acid. In some embodiments of this invention, knockout, knock-down, and/or inhibition of PCS60 gene product expression or activity in a microbe is effected to confer a beneficial phenotype for large-scale carbohydrate to biofuel or biofuel precursor conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. FAT2 gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 852523 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the overexpression of ATP citrate lyase (ACLY) in a microbe, for example *Y. lipolytica*, for the large-scale production of a biofuel or biofuel precursor. Some microbes suitable for industrial scale biofuel or biofuel precursor production, including *Y. lipolytica*, commonly produce large amounts of citrate.

ACLY mediates the conversion of citrate to CoA, a reaction, which, according to some aspects of this invention, can be promoted by ACLY overexpression (see Holz M, Förster A, Mauersberger S, Barth G., *Aconitase overexpression changes the product ratio of citric acid production by Yarrowia lipolytica*. Appl Microbiol Biotechnol. 2009 Jan;81(6):1087-96). In

some embodiments, ACLY overexpression reduces the production of undesirable citrate and/or provides an additional source of acetyl-CoA for biofuel or biofuel precursor synthesis.

In some embodiments, excessive citrate production is inhibited in a microbe for biofuel or biofuel precursor production, including *Y. lipolytica*. In some embodiments, ACLY overexpression in a microbe, for example in *Y. lipolytica*, increases fatty acid synthesis rate and/or confers a beneficial phenotype for large-scale carbohydrate to biofuel or biofuel precursor conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and, increased growth rate, increased

tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. See also Lasserre JP, Nicaud JM, Pagot Y, Joubert-Caron R, Caron M, Hardouin J. Talanta. *First complexomic study of alkane-binding protein complexes in the yeast Yarrowia lipolytica*. 2010 Feb 15;80(4):1576-85. ACLY gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 108728 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the overexpression of Fatty Acid Synthase complex (FAS). While ACC is likely to be the rate-limiting enzyme in fatty acid synthesis, other steps have also been suggested to exercise control of this pathway, most notably, FAS (see Schweizer E, Köttig H, Regler R, Rottner G.J, *Genetic control of Yarrowia lipolytica fatty acid synthetase biosynthesis and function*. Basic Microbiol. 1988;28(5):283-92). This complex is a multifunctional polypeptide that elongates the fatty acid chain in the most substrate-intensive process in the entire lipid synthesis pathway. In some embodiments, ACLY overexpression in a microbe, for example in *Y. lipolytica*, increases fatty acid synthesis rate and/or confers a beneficial phenotypes for large-scale carbohydrate to biofuel or biofuel precursor conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and/or secretion, increased growth rate, increased tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. FAS gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entries for GeneID: 853653 and GeneID: 855845 in the NCBI database (www.ncbi.nlm.nih.gov).

Some aspects of this invention provide a method for the inhibition of AMP activated Protein Kinase (AMPK). AMPK is a regulatory enzyme that regulates the activity of other proteins by phosphorylation in response to cellular AMP:ADP ratio (see Lee-Young RS, Palmer MJ, Linden KC, LePlastrier K, Canny BJ, Hargreaves M, Wadley GD, Kemp BE, McConnell GK. *Carbohydrate ingestion does not alter skeletal muscle AMPK signaling during exercise in humans*. Am J Physiol Endocrinol Metab. 2006 Sep;291(3):E566-73). In yeast, AMPK was shown to target ACC as well as INO1, a gene required for an early step in lipid biosynthesis. Lack of ACC phosphorylation in AMPK knockout mutants results in hyperactive ACC and fatty acid overproduction. In some embodiments, inhibition of AMPK

in a microbe leads to hyperactivation of lipid synthesis. In some embodiments, AMPK activity is completely abolished in a microbe, for example, by knockout of the AMPK gene. In some embodiments, AMPK activity is inhibited in a microbe, for example, by genetic or non-genetic manipulation. Inhibition, as opposed to complete abolishment, of AMPK activity might avoid negative effects on other cellular processes regulated by AMPK. In some embodiments, knockout, knock-down, and/or inhibition of AMPK gene product expression or activity in a microbe, for example *Y. lipolytica*, is effected to confer a beneficial phenotype for large-scale carbohydrate to biofuel or biofuel precursor conversion, for example increased lipid synthesis rate, increased carbohydrate to lipid conversion efficiency, increased lipid storage and/or secretion, increased growth rate, increased tolerance to concentrations of a substance, e.g. a carbon source, a biofuel or biofuel precursor, or a toxic substance. AMPK gene and gene product sequences are well known to those of skill in the art. Exemplary, representative gene and gene product sequences can be found under the entry for GeneID: 100145903 in the NCBI database (www.ncbi.nlm.nih.gov).

ISOLATED NUCLEIC ACIDS

Some aspects of this invention provide nucleic acids coding for a gene product conferring a required and/or desired phenotype for biofuel or biofuel precursor production to a microbe, for example, *Y. lipolytica*. In some embodiments, the nucleic acid is a nucleic acid derived from *Y. lipolytica*. In some embodiments, the nucleic acid encodes a desaturase, for example a $\Delta 9$ desaturase. In some embodiments, the nucleic acid encodes *Y. lipolytica* $\Delta 9$ desaturase. In some embodiments, the nucleic acid comprises SEQ ID NO: 1. In some embodiments, the nucleic acid is SEQ ID NO: 1. In some embodiments, the nucleic acid encodes a gene product, for example, a protein, encoded by SEQ ID NO: 1.

Some aspects of this invention provide a gene product, for example, a protein, conferring a required and/or desirable phenotype for biofuel or biofuel precursor production to a microbe, for example, *Y. lipolytica*. In some embodiments, the protein is a protein from *Y. lipolytica*. In some embodiments, the protein is a desaturase, for example a $\Delta 9$ desaturase. In some embodiments, the protein is a *Y. lipolytica* $\Delta 9$ desaturase. In some embodiments, the amino acid sequence of the protein is the one provided in SEQ ID NO: 2.

The term “nucleic acid” refers to a molecule comprising multiple linked nucleotides. “Nucleic acid” and “nucleic acid molecule” are used interchangeably and refer to

oligoribonucleotides as well as oligodeoxyribonucleotides. The terms also include polynucleosides (i.e., a polynucleotide minus a phosphate) and any other organic base containing nucleic acid. The organic bases include adenine, uracil, guanine, thymine, cytosine and inosine. The nucleic acids may be single or double stranded. The nucleic acid may be naturally or non-naturally occurring. Nucleic acids can be obtained from natural sources, or can be synthesized using a nucleic acid synthesizer (i.e., synthetic). Isolation of nucleic acids are routinely performed in the art and suitable methods can be found in standard molecular biology textbooks. (See, for example, Maniatis' Handbook of Molecular Biology.) The nucleic acid may be DNA or RNA, such as genomic DNA, mitochondrial DNA, mRNA, cDNA, rRNA, miRNA, PNA or LNA, or a combination thereof, as described herein. Non-naturally occurring nucleic acids such as bacterial artificial chromosomes (BACs) and yeast artificial chromosomes (YACs) can also be used in accordance with some aspects of this invention.

Some aspects of this invention relate to the use of nucleic acid derivatives. As will be described herein, the use of certain nucleic acid derivatives may increase the stability of the nucleic acids of the invention by preventing their digestion, particularly when they are exposed to biological samples that may contain nucleases. As used herein, a nucleic acid derivative is a non-naturally occurring nucleic acid or a unit thereof. Nucleic acid derivatives may contain non-naturally occurring elements such as non-naturally occurring nucleotides and non-naturally occurring backbone linkages. Nucleic acid derivatives according to some aspects of this invention may contain backbone modifications such as but not limited to phosphorothioate linkages, phosphodiester modified nucleic acids, combinations of phosphodiester and phosphorothioate nucleic acid, methylphosphonate, alkylphosphonates, phosphate esters, alkylphosphonothioates, phosphoramidates, carbamates, carbonates, phosphate triesters, acetamides, carboxymethyl esters, methylphosphorothioate, phosphorodithioate, p-ethoxy, and combinations thereof. The backbone composition of the nucleic acids may be homogeneous or heterogeneous.

Nucleic acid derivatives according to some aspects of this invention may contain substitutions or modifications in the sugars and/or bases. For example, some nucleic acid derivatives may include nucleic acids having backbone sugars which are covalently attached to low molecular weight organic groups other than a hydroxyl group at the 3' position and other than a phosphate group at the 5' position (e.g., an 2'-O-alkylated ribose group). Nucleic

acid derivatives may include non-ribose sugars such as arabinose. Nucleic acid derivatives may contain substituted purines and pyrimidines such as C-5 propyne modified bases, 5-methylcytosine, 2-aminopurine, 2-amino-6-chloropurine, 2,6-diaminopurine, hypoxanthine, 2-thiouracil and pseudoisocytosine.

5 In some embodiments, a nucleic acid may comprise a peptide nucleic acid (PNA), a locked nucleic acid (LNA), DNA, RNA, or a co-nucleic acids of the above such as DNA-LNA co-nucleic acid.

As used herein the term "isolated nucleic acid molecule" refers to a nucleic acid that is not in its natural environment, for example a nucleic acid that has been (i) extracted and/or
10 purified from a cell or microbe, for example, a bacteria or yeast, by methods known in the art, for example, by alkaline lysis of the host cell and subsequent purification of the nucleic acid, for example, by a silica adsorption procedure; (ii) amplified *in vitro*, for example, by polymerase chain reaction (PCR); (iii) recombinantly produced by cloning, for example, a nucleic acid cloned into an expression vector; (iv) fragmented and size separated, for
15 example, by enzymatic digest *in vitro* or by shearing and subsequent gel separation; or (v) synthesized by, for example, chemical synthesis. In some embodiments, an isolated nucleic acid can readily be manipulated by recombinant DNA techniques well known in the art. Accordingly, a nucleic acid cloned into a vector, or a nucleic acid delivered to a host cell and integrated into the host genome is considered isolated but a nucleic acid in its native state in
20 its natural host, for example, in the genome of the host, is not. An isolated nucleic acid may be substantially purified, but need not be. For example, a nucleic acid that is isolated within a cloning or expression vector is not pure in that it may comprise only a small percentage of the material in the cell in which it resides. Such a nucleic acid is isolated, however, as the term is used herein.

25 Some aspects of this invention relate to nucleic acids encoding a gene product conferring a required or desirable phenotype to a microbe for biofuel or biofuel precursor production which are linked to a promoter or other transcription activating element. In some embodiments, the nucleic acid encoding the gene product and linked to a promoter is comprised in an expression vector or expression construct. As used herein, the terms
30 "expression vector" or "expression construct" refer to a nucleic acid construct, generated recombinantly or synthetically, with a series of specified nucleic acid elements that permit transcription of a particular nucleic acid in a host microbe, for example, an oleaginous yeast.

In some embodiments, the expression vector may be part of a plasmid, virus, or nucleic acid fragment. In some embodiments, the expression vector includes the coding nucleic acid to be transcribed operably linked to a promoter. A promoter is a nucleic acid element that facilitates transcription of a nucleic acid to be transcribed. A promoter is typically located on the same strand and upstream (or 5') of the nucleic acid sequence the transcription of which it controls. In some embodiments, the expression vector includes the coding nucleic acid to be transcribed operably linked to a heterologous promoter. A heterologous promoter is a promoter not naturally operably linked to a given nucleic acid sequence. For example, the SCD gene in *Y. lipolytica* is naturally operably linked to the *Y. lipolytica* SCD gene promoter. Any promoter other than the wildtype *Y. lipolytica* SCD gene promoter operably linked to the SCD gene, or parts thereof, for example in an expression construct, would, therefore, be a heterologous promoter.

In some embodiments, the expression vector includes the coding nucleic acid, for example, a nucleic acid encoding a SCD gene product, operably linked to a constitutive promoter. The term "constitutive promoter" refers to a promoter that allows for continual transcription of its associated gene. In some embodiments, the expression vector includes the coding nucleic acid, for example, a nucleic acid encoding a SCD gene product, operably linked to an inducible promoter. The term "inducible promoter", interchangeably used herein with the term "conditional promoter", refers to a promoter that allows for transcription of its associated gene only in the presence or absence of biotic or abiotic factors. Drug-inducible promoters, for example tetracycline/doxycycline inducible promoters, tamoxifen-inducible promoters, as well as promoters that depend on a recombination event in order to be active, for example the cre-mediated recombination of loxP sites, are examples of inducible promoters that are well known in the art.

Methods to deliver expression vectors or expression constructs into microbes, for example, into yeast cells, are well known to those of skill in the art. Nucleic acids, including expression vectors, can be delivered to prokaryotic and eukaryotic microbes by various methods well known to those of skill in the relevant biological arts. Methods for the delivery of nucleic acids to a microbe in accordance to some aspects of this invention, include, but are not limited to, different chemical, electrochemical and biological approaches, for example, heat shock transformation, electroporation, transfection, for example liposome-mediated transfection, DEAE-Dextran-mediated transfection or calcium phosphate transfection. In

some embodiments, a nucleic acid construct, for example an SCD expression construct, is introduced into the host microbe using a vehicle, or vector, for transferring genetic material. Vectors for transferring genetic material to microbes are well known to those of skill in the art and include, for example, plasmids, artificial chromosomes, and viral vectors. Methods for the construction of nucleic acid constructs, including expression constructs comprising constitutive or inducible heterologous promoters, knockout and knockdown constructs, as well as methods and vectors for the delivery of a nucleic acid or nucleic acid construct to a microbe are well known to those of skill in the art, and are described, for example, in J. Sambrook and D. Russell, *Molecular Cloning: A Laboratory Manual*, Cold Spring Harbor Laboratory Press; 3rd edition (January 15, 2001); David C. Amberg, Daniel J. Burke; and Jeffrey N. Strathern, *Methods in Yeast Genetics: A Cold Spring Harbor Laboratory Course Manual*, Cold Spring Harbor Laboratory Press (April 2005); John N. Abelson, Melvin I. Simon, Christine Guthrie, and Gerald R. Fink, *Guide to Yeast Genetics and Molecular Biology, Part A, Volume 194* (Methods in Enzymology Series, 194), Academic Press (March 11, 2004); Christine Guthrie and Gerald R. Fink, *Guide to Yeast Genetics and Molecular and Cell Biology, Part B, Volume 350* (Methods in Enzymology, Vol 350), Academic Press; 1st edition (July 2, 2002); Christine Guthrie and Gerald R. Fink, *Guide to Yeast Genetics and Molecular and Cell Biology, Part C, Volume 351*, Academic Press; 1st edition (July 9, 2002); Gregory N. Stephanopoulos, Aristos A. Aristidou and Jens Nielsen, *Metabolic Engineering: Principles and Methodologies*, Academic Press; 1 edition (October 16, 1998); and Christina Smolke, *The Metabolic Pathway Engineering Handbook: Fundamentals*, CRC Press; 1 edition (July 28, 2009), all of which are incorporated by reference herein.

In some embodiments, the native promoter of a gene encoding a gene product conferring a required or desirable phenotype to a microbe, for example, the native SCD promoter, is modified in the microbe to alter the regulation of its transcriptional activity. In some embodiment, the modified promoter exhibits an increased transcriptional activity as compared to its unmodified counterpart. The term “modified promoter”, as used herein, refers to a promoter the nucleotide sequence of which has been artificially altered. Nucleotide deletion(s), insertion(s) or mutation(s), alone or in combination, are examples of such artificial alterations. Artificial promoter alterations can be effected in a targeted fashion, for example by homologous recombination approaches, such as gene targeting, knockout, knock in, site-directed mutagenesis, or artificial zinc finger nuclease-mediated strategies.

Alternatively, such alterations may be effected by a random or quasi-random event, such as irradiation or non-targeted nucleotide integration and subsequent selection. Promoter modifications, in general, are fashioned in order to modulate the transcriptional activation properties of the respective promoter. For example, the disruption or deletion of a regulatory element mediating the repression of a SCD promoter in response to elevated intracellular fatty acid levels would lead to continued transcriptional activation of the SCD gene even under conditions of elevated intracellular fatty acid levels. Similarly, the insertion of a constitutively active transcriptional activator element into a conditional promoter region may effect overexpression of the respective gene under normally inhibitive conditions. Methods for the targeted disruption of a native promoter, for example, a native SCD promoter, in a microbe, for example, for targeted disruption resulting in an increased transcription rate, are well known to those of skill in the art.

In some embodiments, a nucleic acid construct is provided that is useful for the knockout of a delta-12 desaturase gene in a microbe for biofuel or biofuel precursor production. In some embodiments, the knockout construct comprises genomic sequences of a microbial delta-12 desaturase gene that flank a nucleotide sequence that, when inserted into the delta-12 desaturase gene, disrupts the expression of a delta-12 desaturase gene product. In some embodiments, the nucleic acid disrupting the delta-12 desaturase gene product expression is an antibiotic resistance marker, for example, a phleomycin resistance gene. In some embodiments, the delta-12 desaturase knockout vector comprises a sequence as provided in SEQ IDNO: 28. Methods of delivering knockout vectors to microbes are well known to those of skill in the art and methods to effect homologous recombination in microbes, for example, in yeasts, are well known to the skilled artisan as well. The invention is not limited in this respect.

MICROBE ENGINEERING METHODS

Some aspects of this invention relate to engineering of a microbe, for example, *Y. lipolytica*, to exhibit a required and/or desirable phenotype for large-scale production of a biofuel or biofuel precursor. Some aspects of this invention relate to the metabolic engineering of the SCD pathway in order to yield a microbe optimized for biofuel production. Some aspects of this invention relate to the metabolic engineering of a gene regulating carbon flux into or out of a fatty acid synthesis pathway in order to yield a microbe optimized for

biofuel production.

Some aspects of this invention provide methods to greatly increase the efficiency of *Y. lipolytica* mediated carbon source to lipid conversion by modulating *Y. lipolytica*'s native lipid metabolism. Some aspects of this invention relate to the discovery that an

5 overexpression of a gene increasing fatty acid or triacylglycerol accumulation, such as SCD, not only results in an increase in lipid accumulation, but also an increase of lipid synthesis rate, lipid content, and/or growth rate. Remarkably and unexpectedly, lipid metabolism modulation according to some methods provided by this invention also confers other beneficial characteristics, for example an increased tolerance to feedstock substances, 10 including high concentrations of substrate (e.g., glucose) and/or of toxic substances commonly found to contaminate feedstock, for example, pretreated feedstock. Some non-limiting examples of such contaminating substances are furfural, 5-hydroxymethylfurfural and acetic acid. Some non-limiting examples of feedstock materials that generate contaminating, toxic substances upon pre-treatment, are wood-derived feedstocks, corn 15 stover, and bagasse.

Some aspects of this invention relate to engineering required and/or desirable phenotypes in *Y. lipolytica* via overriding transcriptional inhibition of a key regulator of lipid metabolism, for example via overriding transcriptional inhibition of SCD. The manipulation of a key regulator of lipid metabolism, for example SCD, in other biofuel producing 20 microbes, for example yeast, bacteria, fungi, or algae, is also contemplated.

In order to engineer an organism, for example an oleaginous yeast, to be useful in the industrial-scale production of biofuels, a detailed understanding of the molecular mechanisms governing fatty acid and lipid metabolism in the respective organism is essential. Until the present invention, the identification and functional annotation of fatty acid and lipid 25 metabolism regulators in oil producing microorganisms for biofuel production, e.g. oleaginous yeast, remained unsolved. Some aspects of this invention provide the identification and functional annotation of key regulator gene, SCD, in the oleaginous yeast *Y. lipolytica*. Isolated SCD nucleic acid and protein molecules are also provided.

Some aspects of this invention relate to the engineering of a desirable phenotype for 30 biofuel or biofuel precursor production in a microbe by genetic engineering. Some aspects of this invention relate to the manipulation of a gene involved in the production of biofuel or a biofuel precursor, for example, a fatty acid or a triacylglycerol, in a microbe. Some aspects of

this invention relate to the manipulation of a plurality of genes involved in the production of biofuel or a biofuel precursor in parallel in a microbe.

In some embodiments, a microbe is engineered for biofuel or biofuel precursor production by manipulating a single gene according to methods provided by aspects of this invention, for example, a $\Delta 9$ desaturase (e.g., SCD), GLUT (e.g., Glut1), hemoglobin, cytochrome (e.g., cytochrome B5), malic enzyme, ACC, ACS, ACS2, FAA1, FAT1, FAT2, ACLY, FAS, AMPK, JNK2, or delta-12 desaturase. In some embodiments, a microbe is engineered for biofuel or biofuel precursor production by manipulating a plurality of genes according to methods provided by aspects of this invention, for example, any combination of two or more of a $\Delta 9$ desaturase (e.g., SCD), GLUT (e.g., Glut1), hemoglobin, cytochrome (e.g., cytochrome B5), malic enzyme, ACC, ACS, ACS2, FAA1, FAT1, FAT2, ACLY, FAS, JNK2, delta-12 desaturase, and/or AMPK. In some embodiments, a microbe is engineered to comprise an increased level of a SCD gene product and an additional manipulation, for example, a genetic manipulation, of the expression of an additional gene product, for example, a GLUT (e.g., Glut1), hemoglobin, cytochrome (e.g., cytochrome B5), malic enzyme, ACC, ACS, ACS2, FAA1, FAT1, FAT2, ACLY, FAS, JNK2, delta-12 desaturase, or AMPK gene product. In some embodiments, a microbe is engineered to comprise an increased level of a SCD gene product and of a hemoglobin gene product. In some embodiments, a microbe is engineered to comprise an increased level of a SCD gene product and of a GLUT gene product, for example, a Glut1 gene product. In some embodiments, a microbe is engineered to comprise an increased level of a SCD gene product, of a GLUT gene product, for example, a Glut1 gene product, and of a hemoglobin and/or a cytochrome gene product. In some embodiments, a microbe is engineered to comprise an increased level of a SCD gene product and of Glut1, hemoglobin and cytochrome b5, and optionally a delta-12 desaturase knockout. In some embodiments, the microbe is *Y. lipolytica*.

ENGINEERED MICROBES FOR BIOFUEL PRODUCTION

Some aspects of this invention relate to a microbe engineered and/or optimized for large-scale biofuel or biofuel precursor production. In some embodiments, an engineered microbe is provided that has been manipulated by a method or using a nucleic acid or protein provided by some aspects of this invention. In some embodiments, an engineered microbe is provided, that overexpresses a gene product that, according to some aspects of this invention,

confers a required and/or desirable phenotype for biofuel or biofuel precursor production to the microbe. In some embodiments, a microbe comprising an increased SCD gene product activity is provided. In some embodiments, the microbe exhibits an increased fatty acid synthesis rate, an increased TAG storage, and/or an additional required or desirable trait.

5 In some embodiments, the engineered microbe is an oleaginous yeast, for example, *Y. lipolytica*. In some embodiments, an engineered yeast provided by this invention exhibits one or more highly desirable and unexpected phenotypic characteristics, for example: increased carbon to oil conversion, e.g., at a rate approaching theoretical values, robust growth, continuous oil production, remarkable biomass production, and increased tolerance of the
10 carbon source and associated substances.

In some embodiments, the engineered microbe, for example, the engineered yeast, provided by aspects of this invention exhibits a carbon to oil conversion rate within the range of about 0.02g/g (g oil, lipid, or TAG produced/ g Glucose consumed) to about 0.3 g/g. In some embodiments, the engineered microbe, for example, the engineered yeast, provided by
15 aspects of this invention exhibits a carbon to oil conversion of about 0.010g/g (g TAG produced/ g Glucose consumed), about 0.02g/g, about 0.025g/g, about 0.03g/g, about 0.04g/g, about 0.05g/g, about 0.06g/g, about 0.07g/g, about 0.075g/g, about 0.08g/g, about 0.09g/g, about 0.1g/g, about 0.11g/g, about 0.12g/g, about 0.13g/g, about 0.14g/g, about
20 0.15g/g, about 0.16g/g, about 0.17g/g, about 0.18g/g, about 0.19g/g, about 0.2g/g, about 0.21g/g, about 0.22g/g, about 0.23g/g, about 0.24g/g, about 0.25g/g, about 0.26g/g, about 0.27g/g, about 0.28g/g, about 0.29g/g, or about 0.3g/g, or approaching theoretical values. In some embodiments, the engineered microbe, for example, the engineered yeast, provided by aspects of this invention exhibits a carbon to oil conversion rate of at least about 0.010g/g (g TAG produced/ g Glucose consumed), at least about 0.02g/g, at least about 0.025g/g, at least
25 about 0.03g/g, at least about 0.04g/g, at least about 0.05g/g, at least about 0.06g/g, at least about 0.07g/g, at least about 0.075g/g, at least about 0.08g/g, at least about 0.09g/g, at least about 0.1g/g, at least about 0.11g/g, at least about 0.12g/g, at least about 0.13g/g, at least about 0.14g/g, at least about 0.15g/g, at least about 0.16g/g, at least about 0.17g/g, at least about 0.18g/g, at least about 0.19g/g, at least about 0.2g/g, at least about 0.21g/g, at least
30 about 0.22g/g, at least about 0.23g/g, at least about 0.24g/g, at least about 0.25g/g, at least about 0.26g/g, at least about 0.27g/g, at least about 0.28g/g, at least about 0.29g/g, or at least about 0.3g/g, or approaching theoretical values.

In some embodiments, the engineered yeast provided by aspects of this invention exhibits a biomass production that is increased about 2-fold, about 2.5-fold, about 5-fold, about 7.5-fold, about 10-fold, about 15-fold, about 20-fold, about 25-fold, about 30-fold, about 32-fold, about 35-fold, or about 40-fold as compared to wild type yeast. In some
5 embodiments, the engineered yeast provided by aspects of this invention exhibits tolerance to the carbon source and/or associated substances at concentrations of up to about 150%, up to about 175%, up to about 200%, up to about 225%, up to about 250%, up to about 275%, up to about 300%, up to about 325%, up to about 350%, up to about 375%, up to about 400%, or up to about 500% of that of the highest concentrations tolerated by wild type yeast. Non-
10 limiting examples of carbon source associated substances include toxic substances contaminating the carbon source, for example, substances that are generated or used during pretreatment of the carbon source (e.g. acidic substances, such as acetic acid, or ammonia).

The data presented herein identify a novel rate-limiting step of lipid accumulation in oleaginous yeast, the engineering of which results in greatly improved characteristics of the
15 manipulated microbe in respect to biofuel generation from carbohydrate sources (e.g. glucose). Accordingly, methods and manufactures provided by the instant invention represent a significant advance towards an alternative production of biofuels from renewable carbohydrate sources using microbial, for example yeast, fermentation.

20 MICROBIAL CULTURES FOR BIOFUEL PRODUCTION

Some aspects of this invention relate to a culture of a microbe provided herein or engineered according to aspects of this invention or comprising an isolated nucleic acid or protein provided herein.

In some embodiments, the culture comprises a microbe provided herein or engineered
25 according to aspects of this invention or comprising an isolated nucleic acid or protein from the list provided herein and a medium, for example, a liquid medium.

In some embodiments, the culture comprises a microbe provided herein or engineered according to aspects of this invention or comprising an isolated nucleic acid or protein provided herein and a carbohydrate source.

30 In some embodiments, the culture comprises a microbe provided herein or engineered according to aspects of this invention or comprising an isolated nucleic acid or protein provided herein and a salt and/or buffer establishing conditions of salinity, osmolarity, and

pH, that are amenable to survival, growth, and/or carbohydrate to biofuel or biofuel precursor conversion by the microbe.

In some embodiments, the culture comprises an additional component, for example, an additive. Non-limiting examples of additives are nutrients, enzymes, amino acids, albumin, growth factors, enzyme inhibitors (for example protease inhibitors), fatty acids, lipids, hormones (e.g., dexamethasone and gibberellic acid), trace elements, inorganic compounds (e.g., reducing agents, such as manganese), redox-regulators (e.g., antioxidants), stabilizing agents (e.g., dimethylsulfoxide), polyethylene glycol, polyvinylpyrrolidone (PVP), gelatin, antibiotics (e.g., Brefeldin A), salts (e.g., NaCl), chelating agents (e.g., EDTA, EGTA), and enzymes (e.g., cellulase, dispase, hyaluronidase, or DNase). In some embodiments, the culture may comprise a drug inducing or inhibiting transcription from a conditional or inducible promoter, for example doxycycline, tetracycline, tamoxifen, IPTG, hormones, or metal ions.

While the specific culture conditions, for example, the concentration of the carbon source, will depend upon the respective engineered microorganism to be cultured, general methods and culture conditions for the generation of microbial cultures are well known to those of skill in the art, and are described, for example, in J. Sambrook and D. Russell, *Molecular Cloning: A Laboratory Manual*, Cold Spring Harbor Laboratory Press; 3rd edition (January 15, 2001); David C. Amberg, Daniel J. Burke; and Jeffrey N. Strathern, *Methods in Yeast Genetics: A Cold Spring Harbor Laboratory Course Manual*, Cold Spring Harbor Laboratory Press (April 2005); John N. Abelson, Melvin I. Simon, Christine Guthrie, and Gerald R. Fink, *Guide to Yeast Genetics and Molecular Biology, Part A, Volume 194* (Methods in Enzymology Series, 194), Academic Press (March 11, 2004); Christine Guthrie and Gerald R. Fink, *Guide to Yeast Genetics and Molecular and Cell Biology, Part B, Volume 350* (Methods in Enzymology, Vol 350), Academic Press; 1st edition (July 2, 2002); and Christine Guthrie and Gerald R. Fink, *Guide to Yeast Genetics and Molecular and Cell Biology, Part C, Volume 351*, Academic Press; 1st edition (July 9, 2002), all of which are incorporated by reference herein. For oil production, the cultures of engineered microbes described herein are cultured under conditions suitable for oil accumulation, as known in the art.

In some embodiments, an engineered microbe is provided that exhibits a growth advantage over wild type microbes of the same kind and/or over other microbes, for example,

microbes commonly found to contaminate microbial cultures for carbon source to biofuel or biofuel precursor conversion. For example, in some embodiments, a microbe is provided that exhibits an increased proliferation rate as compared to wild type microbes of the same kind or other microbes, and/or an increased tolerance to or viability under conditions that are toxic or restrict growth or proliferation to wild type microbes of the same kind and/or other microbes. In some embodiments, the growth and/or proliferation advantage of an engineered microbe provided by aspects of this invention translates into the possibility of using non-sterile culturing and fermentation conditions for biofuel or biofuel precursor production, because the problem of culture overgrowth by contaminating microbes is mitigated or completely abolished. In some embodiments, an engineered microbe provided by aspects of this invention is cultured under non-sterile conditions for biofuel or biofuel precursor production. For example, in some embodiments, non-sterilized feedstock, non-sterilized culture media, non-sterilized supplements, or a non-sterilized bioreactor (e.g. an open reactor under non-sterile conditions) is used for biofuel or biofuel precursor production.

METHODS FOR BIOFUEL PRODUCTION/FEEDSTOCK/BIOREACTORS

Some aspects of this invention relate to methods for the production of biofuel or biofuel precursor using modified microbes in accordance with this invention. In some embodiments, methods for biofuel or biofuel precursor production on an industrial scale are provided.

A variety of carbon sources can be converted into a biofuel or biofuel precursor using a method provided by some aspects of this invention. Sugars, starches, and fibers are non-limiting examples of carbohydrate sources suitable for conversion methods provided by some aspects of this invention. According to some aspects of this invention, a carbohydrate source may comprise a refined and/or unrefined sugar, starch, and/or fiber, or a combination of any of these. Non-limiting examples of sugars are fermentable sugars, such as glucose, fructose, sucrose, xylose, and lactose. Non-limiting examples of starches are amylose and amylopectin. Non-limiting examples of fibers are plant fibers, such as cellulose, hemicellulose and wood fibers. Some aspects of this invention relate to the use of industrial byproducts, intermediates, or waste products, for example raw plant extracts, molasses, stover, or sewage as a carbon source. In some embodiments, the carbon source is derived from algae. In some

embodiments, algal biomass is produced specifically for use as a carbon source in microbe-mediated biofuel or biofuel precursor production.

In some embodiments, methods for the production of biofuel or biofuel precursor are provided that include the use of a cheap, abundant, and readily available carbon source feedstock as the carbon source. In some embodiments, cellulose or hemicellulose is used as the carbon source. In some embodiments, the cellulose or hemicellulose is derived from industrial by- or waste products. In some embodiments, the cellulose or hemicellulose is derived directly from plant or algal biomass. Plant or algal biomass is one of the most abundant feedstocks and comprises a significant amount of non-fermentable sugars and fibers, for example, cellulose and hemi-cellulose. In some embodiments, biomass feedstock is pretreated to convert a non-fermentable sugar or fiber into a fermentable sugar, thus making them available for microbe growth and microbe-mediated biofuel or biofuel precursor production. In some embodiments, the pretreatment of biomass feedstock includes depolymerizing cellulose and/or hemicellulose components to monomeric sugars using a pretreatment method known to those of skill in the art, for example, a dilute acid or ammonia fiber expansion (AFEX) method (see, e.g., Yang B, Wyman CE. *Dilute acid and autohydrolysis pretreatment*. Methods Mol Biol. 2009;581:103-14; Balan V, Bals B, Chundawat SP, Marshall D, Dale BE, *Lignocellulosic biomass pretreatment using AFEX* Methods Mol Biol. 2009;581:61-77). Other methods for depolymerization of biomass polymers to monomeric sugars are well known to those of skill in the art and are contemplated to be used in some embodiments of this invention.

In some embodiments, a biomass feedstock containing non-fermentable sugars is pretreated using a dilute acid method to depolymerize a non-fermentable sugar to a monomeric, fermentable sugar. In some embodiments, biomass is treated with dilute sulphuric acid at moderately mild temperatures for a defined period of time. For example, in some embodiments, the biomass is treated with about 0.5%, about 1%, about 2%, about 3%, about 4%, about 5%, or about 6% sulphuric acid. In some embodiments, the biomass is treated at about 30°C, at about 37°C, at about 40°C, at about 50°C, at about 60°C, at about 70°C, at about 80°C, at about 90°C, at about 100°C, at about 110°C, at about 120°C, at about 130°C, at about 140°C, at about 150°C, at about 175°C, at about 200°C, or at above about 200°C.

In some embodiments, the resulting hydrolysate contains insoluble lignin and solubilized cellulosic and hemicellulosic polymers. The latter products can be further treated to generate hexose and pentose sugars such as glucose and xylose monomers by methods well known to those of skill in the art, for example, by treatment with cellulase or other

5 hydrolyzing enzymes. In some embodiments, the pretreatment of non-fermentable sugars with dilute acid results in the generation of by-products that include toxic compounds which inhibit growth, decrease viability, and/or inhibit biofuel or biofuel precursor production of microbes not engineered according to aspects of this invention. In some embodiments, the pre-treated feedstock is washed, supplemented with media supporting microbial growth and
10 biofuel or biofuel precursor production, and/or over-limed for detoxification.

In some embodiments, a biomass feedstock containing non-fermentable sugars is pretreated using an AFEX method to depolymerize a non-fermentable sugar to a monomeric, fermentable sugar. In some embodiments, biomass is treated with liquid ammonia at high temperature and pressure for a defined period of time. In some embodiments, biomass is
15 treated for about 10 minutes, about 20 minutes, about 30 minutes, about 40 minutes, about 50 minutes, about 60 minutes, about 70 minutes, about 80 minutes, about 90 minutes, or longer. In some embodiments, biomass is treated at about 30°C, at about 37°C, at about 40°C, at about 50°C, at about 60°C, at about 70°C, at about 80°C, at about 90°C, at about 100°C, at about 110°C, at about 120°C, at about 130°C, at about 140°C, at about 150°C, at about
20 175°C, at about 200°C, or at above about 200°C. In some embodiments, the AFEX pretreatment results in the conversion of crystalline cellulose contained in the feedstock into an amorphous, fermentable form. In some embodiments, the AFEX pre-treated biomass feedstock does not contain significant amounts of toxic byproducts that inhibit microbial growth and/or biofuel or biofuel precursor production, and is used without prior
25 detoxification for microbial biofuel or biofuel precursor production.

In some embodiments, biomass feedstock, with or without pre-treatment, is treated with an enzyme that hydrolyzes or depolymerizes sugar polymers, for example, with a cellulase or hemicellulase enzyme. In some embodiments, the feedstock is contacted with the enzyme in a liquid phase and incubated at a temperature allowing for the enzyme to catalyze
30 a depolymerization or hydrolyzation reaction for a time sufficient to hydrolyze or depolymerize a significant amount of the non-fermentable sugar or fiber in the biomass feedstock. In some embodiments, the liquid phase of the feedstock contacted with the

enzyme, which contains the soluble, fermentable sugar fraction, is separated from the solid phase, including non-fermentable sugars and fibers, after incubation for hydrolyzation and depolymerization, for example, by centrifugation. In some embodiments, the liquid fraction of the feedstock is subsequently contacted with a microbe, for example, a microbe provided by aspects of this invention, for conversion to biofuel or biofuel precursor. In some
5 embodiments, enzymatic conversion of non-fermentable sugars or fiber occurs in a consolidated bioprocess, for example, at the same time and/or in the same reactor as microbial conversion of the produced fermentable sugars to biofuel or biofuel precursor. In some embodiments, the enzymatic conversion is performed first, and the feedstock contacted
10 with enzyme is subsequently contacted with the microbe for biofuel or biofuel precursor production. In some embodiments, enzymatic and microbial conversion are performed at the same time and in the same reactor.

In some embodiments, an engineered microbe as provided herein, for example, a *Yarrowia lipolytica* overexpressing an SCD gene and, optionally, carrying additional
15 modifications as described herein, is grown on acetate as the main carbon source. For example, in some embodiments, the microbe is grown in a solution of acetic acid with a concentration of about 1%, about 2%, about 3%, about 4%, about 5%, about 6%, about 7%, about 8%, about 9%, or about 10%. In some embodiments, the acetate concentration is between about 3%-10%. In some embodiments, cell cultures comprising engineered
20 microbes as provided herein that are cultured on acetate as the main carbon source are contacted, or “spiked” with glycerol. In some embodiments, the microbes are intermittently contacted with glycerol. In some embodiments, the microbes are continuously or semi-continuously contacted with glycerol. In some embodiments, the microbes are contacted with glycerol at a concentration of about 0.5%, about 1%, about 2%, about 3%, about 4%, or about
25 5%. Contacting the engineered microbes provided herein with glycerol provides much needed metabolites for the production of TAGs, as well as reducing moieties needed in the production of fatty acids from carbohydrates. In some embodiments, glycerol spiking is performed in biofuel or biofuel precursor production methods using a carbon source other than acetate, for example, any carbon source described herein.

30 In some embodiments, fermentation processes for large-scale microbe-mediated carbohydrate to lipid conversion may be carried out in bioreactors. As used herein, the terms “bioreactor” and “fermentor”, which are interchangeably used, refer to an enclosure, or

partial enclosure, in which a biological and/or chemical reaction takes place, at least part of which involves a living organism or part of a living organism. A “large-scale bioreactor” or “industrial-scale bioreactor” is a bioreactor that is used to generate a product, for example a biofuel or biofuel precursor, for example a fatty acid and/or TAG, on a commercial or quasi-commercial scale. Large scale bioreactors typically have volumes in the range of liters, hundreds of liters, thousands of liters, or more.

A bioreactor in accordance with aspects of this invention may comprise a microbe or a microbe culture. In some embodiments, a bioreactor may comprise a spore and/or any kind of dormant cell type of any isolated microbe provided by aspects of this invention, for example, in a dry state. In some embodiments, addition of a suitable carbohydrate source to such bioreactors may lead to activation of the dormant cell, for example to germination of a yeast spore, and subsequent conversion of the carbohydrate source, at least in part, to a biofuel or biofuel precursor.

Some bioreactors according to aspects of this invention may include cell culture systems where microbes are in contact with moving liquids and/or gas bubbles. Microbes or microbe cultures in accordance with aspects of this invention may be grown in suspension or attached to solid phase carriers. Non-limiting examples of carrier systems include microcarriers (e.g., polymer spheres, microbeads, and microdisks that can be porous or non-porous), cross-linked beads (e.g., dextran) charged with specific chemical groups (e.g., tertiary amine groups), 2D microcarriers including cells trapped in nonporous polymer fibers, 3D carriers (e.g., carrier fibers, hollow fibers, multicartridge reactors, and semi-permeable membranes that can comprising porous fibers), microcarriers having reduced ion exchange capacity, encapsulation cells, capillaries, and aggregates. Carriers can be fabricated from materials such as dextran, gelatin, glass, and cellulose.

Industrial-scale carbohydrate to lipid conversion processes in accordance with aspects of this invention may be operated in continuous, semi-continuous or non-continuous modes. Non-limiting examples of operation modes in accordance with this invention are batch, fed batch, extended batch, repetitive batch, draw/fill, rotating-wall, spinning flask, and/or perfusion mode of operation.

In some embodiments, bioreactors may be used that allow continuous or semi-continuous replenishment of the substrate stock, for example a carbohydrate source and/or continuous or semi-continuous separation of the product, for example a secreted lipid, an

organic phase comprising a lipid, and/or cells exhibiting a desired lipid content, from the reactor.

Non-limiting examples of bioreactors in accordance with this invention are: stirred tank fermentors, bioreactors agitated by rotating mixing devices, chemostats, bioreactors agitated by shaking devices, airlift fermentors, packed-bed reactors, fixed-bed reactors, fluidized bed bioreactors, bioreactors employing wave induced agitation, centrifugal bioreactors, roller bottles, and hollow fiber bioreactors, roller apparatuses (for example benchtop, cart-mounted, and/or automated varieties), vertically-stacked plates, spinner flasks, stirring or rocking flasks, shaken multiwell plates, MD bottles, T-flasks, Roux bottles, multiple-surface tissue culture propagators, modified fermentors, and coated beads (e.g., beads coated with serum proteins, nitrocellulose, or carboxymethyl cellulose to prevent cell attachment).

Bioreactors and fermentors according to aspects of this invention may, optionally, comprise a sensor and/or a control system to measure and/or adjust reaction parameters. Non-limiting examples of reaction parameters are: biological parameters, for example growth rate, cell size, cell number, cell density, cell type, or cell state, chemical parameters, for example pH, redox-potential, concentration of reaction substrate and/or product, concentration of dissolved gases, such as oxygen concentration and CO₂ concentration, nutrient concentrations, metabolite concentrations, glucose concentration, glutamine concentration, pyruvate concentration, apatite concentration, concentration of an oligopeptide, concentration of an amino acid, concentration of a vitamin, concentration of a hormone, concentration of an additive, serum concentration, ionic strength, concentration of an ion, relative humidity, molarity, osmolarity, concentration of other chemicals, for example buffering agents, adjuvants, or reaction by-products, physical/mechanical parameters, for example density, conductivity, degree of agitation, pressure, and flow rate, shear stress, shear rate, viscosity, color, turbidity, light absorption, mixing rate, conversion rate, as well as thermodynamic parameters, such as temperature, light intensity/quality etc.

Sensors able to measure parameters as described herein are well known to those of skill in the relevant mechanical and electronic arts. Control systems able to adjust the parameters in a bioreactor based on the inputs from a sensor as described herein are well known to those of skill in the art of bioreactor engineering.

A variety of different microbes as provided by aspects of this invention can be cultured in a suitable bioreactor to perform large-scale carbohydrate to biofuel or biofuel precursor conversion in accordance with aspects of the invention, for example, microbes from various sources of yeast, such as oleaginous yeast, bacteria, algae and fungi.

5 Non-limiting examples of yeast cells are cells from *Yarrowia lipolytica*, *Hansenula polymorpha*, *Pichia pastoris*, *Saccharomyces cerevisiae*, *S. bayanus*, *S. K. lactis*, *Waltomyces lipofer*, *Mortierella alpine*, *Mortierella isabellina*, *Hansenula polymorpha*., *Mucor rouxii*, *Trichosporon cutaneu*, *Rhodotorula glutinis* *Saccharomyces diastasicus*, *Schwanniomyces occidentalis*, *S. cerevisiae*, *Pichia stipitis*, and *Schizosaccharomyces pombe*.

10 Non-limiting examples of bacteria are *Bacillus subtilis*, *Salmonella*, *Escherichia coli*, *Vibrio cholerae*, *Streptomyces*, *Pseudomonas fluorescens*, *Pseudomonas putida*, *Pseudomonas sp*, *Rhodococcus sp*, *Streptomyces sp*, and *Alcaligenes sp*.

Fungal cells can, for example, be cultured from species such as *Aspergillus shirousamii*, *Aspergillus niger* and *Trichoderma reesei*.

15 Non-limiting examples of algal cells are cells from *Neochloris oleoabundans*, *Scenedesmus obliquus*, *Nannochloropsis sp.*, *Dunaliella tertiolecta*, *Chlorella vulgaris*, *Chlorella emersonii*, and *Spirulina maxima*.

The type of carbohydrate source to be employed for conversion to a biofuel or biofuel precursor according to aspects of this invention depends on the specific microbe employed.

20 Some microbes provided by aspects of this invention may be able to efficiently convert a specific carbohydrate source, while a different carbohydrate source may not be processed by the same microbe at high efficiency or at all. According to aspects of this invention, the oleaginous yeast *Y. lipolytica*, for example, can efficiently convert sugars, such as glucose, fructose, sucrose, and/or lactose, and carbohydrate sources high in sugars, for example
25 molasses, and plant fibers into fatty acids and their derivatives.

In some embodiments, a biofuel or biofuel precursor, for example, a fatty acid or a triacylglycerol, generated from a carbon source feedstock is secreted, at least partially, by a microbe provided by aspects of this invention, for example, an oleaginous yeast, such as a *Y. lipolytica* cell. In some embodiments, a microbe provided by aspects of this invention is
30 contacted with a carbohydrate source in an aqueous solution in a bioreactor, and secreted biofuel or biofuel precursor forms an organic phase that can be separated from the aqueous phase. The term organic phase, as used herein, refers to a liquid phase comprising a non-

polar, organic compound, for example a fatty acid, TAG, and/or other non-polar lipid. And organic phase in accordance to this invention might further contain a microbe, a carbohydrate, or other compound found in other phases found in a respective bioreactor.

Methods useful for industrial scale phase separation are well known to those of ordinary skill in the art. In some embodiments, the organic phase is continuously or semi-continuously siphoned off. In some embodiments, a bioreactor is employed, comprising a separator, which continuously or semi-continuously extracts the organic phase.

In some embodiments, a biofuel or biofuel precursor is accumulated in cells according to aspects of this invention. In some embodiments, cells that have accumulated a desirable amount of biofuel or biofuel precursor, are separated continuously or semi-continuously from a bioreactor, for example, by centrifugation, sedimentation, or filtration. Cell separation can further be effected, for example, based on a change in physical cell characteristics, such as cell size or density, by methods well known to those skilled in the art. The accumulated biofuel or biofuel precursor can subsequently be extracted from the respective cells using standard methods of extraction well known to those skilled in the art, for example, solvent hexane extraction. In some embodiments, microbial cells are collected and extracted with 3 times the collected cell volume of hexane. In some embodiments, the extracted biofuel or biofuel precursor are further refined. In some embodiments, a biofuel precursor, for example a triacylglycerol is converted to a biofuel, for example, biodiesel, using a method well known to those of skill in the art, for example, a transesterification procedure.

The function and advantage of these and other embodiments of the present invention will be more fully understood from the examples below. The following examples are intended to illustrate the benefits of the present invention, but do not exemplify the full scope of the invention.

EXAMPLES

MATERIALS AND METHODS

Gene constructs: The respective genes, for example, GLUT1, hemoglobin, cytochrome, pyruvate carboxylase, SCD, etc., were cloned into plasmid YLEX (Figure 12) between PmlI and KpnI sites. The restrictions sites used were PmlI and KpnI. All cDNA were sequenced and mapped to genomic databases. Exemplary, representative sequence database entries that the cloned cDNAs were mapped to include: GLUT1: GeneID: 6513; Hemoglobin:

Vitreoscilla stercoraria bacterial hemoglobin gene, ACCESSION L77863; Cytochrome:

GeneID: 1528, CYB5A cytochrome b5 type A; Pyruvate carboxylase: GeneID: 5091; SCD
stearoyl-CoA desaturase (SCD): GeneID: 710155.

Representative sequences, for example coding sequences, useful for the generation of
overexpressing microbes are, for example:

HEMOGLOBIN (bacterial)

ATGTTAGACCAACAAACCGTAGACACCAGCAAAGCCACTGTTCTGTATTGAAAGAGCATGGCGTGACCATTACCACGACGTT
TTACCAAAATTTGTTTGCCAAACATCCTGAAGTACGACCTTTGTTTGACATGGGTGCGCAAGCATCTTTGGAACAGCCTAAGG
CTTTGGCGATGACGGTTGGGGCGGCGGCACAAAACATTGAAAAATTACCTGCAATTTTGCTGCGAGTACAAAAAATTGCCGTC
AAACATTGTCAAGCAGGCGTGGCGGCACGACATTATCCGATTGTGGGTCAAGAAATTGTTGGGTGCGATTAAAGAATTATTGGG
TGATGCGGCGACCGATGATATTTTGGATGCGTGGGGCAAGGCTTATGGCGTGATTGCCGATGTTTTATTCAAGTGGAAGCGG
ATTTGTACGCTCAAGACGCTGAATAA (SEQ ID NO: 3)

CYTOCROME B (Yarrowia)

ATGATCATCAACGGCAAGGTCTACGACATCTCCAGCTTCGTTGACGAGCATCCCGGTGGAGAGGAGGTTCTTCTTGATGCCGG
TGGAATGAGGCCACCAACGCTTTTCGACGACGTTGGACACTCTGAGGACGCTTACGGCATCCTTAACGACCTCTATGTCGGTG
AGGTTGACCCAGCGAGGACGTTATCCGAAAGACTCACACTGTCAAGACTTCTTACGAGGACGGCGAGTCTGTTGGTGATGAC
CACGGATCTTCTTCCATGATCTTCTCATTGTTGCTGCTGCTGTTGCCGCCGCTGCTTTCTTACCTCCAGGGTCAGAAATA
A (SEQ ID NO: 4)

GLUT (rat)

ATGGAGCCCAGCAGCAAGAAGGTGACGGGGCCGCTTATGTTGGCCGTGGGAGGGGCAGTGCTCGGATCCCTGCAGTTCCGGCTA
TAACACCGGTGTCTATCAACGCCCCCAGAAAGGTAATTGAGGAGTTCTACAATCAAACATGGAACACCGCTATGGAGAGTCCA
TCCCATGCCACACTCACACACTCTGGTCTCTCTCCGTGGCCATCTTCTCTGTGCGGGGCATGATTGGTTCCCTTCTCTGTG
GGCCTCTTTGTTAATCGCTTTGGCAGGCGGAACTCCATGCTGATGATGAACCTGTTGGCCTTTGTGTCTGCCGTGCTTATGGG
TTTCTCCAACTGGGCAAGTCCTTTGAGATGCTGATCCTGGGCCGCTTCATCATTGGAGTGTACTGTGGCCTGACCACCGGCT
TTGTGCCCATGTATGTGGGGAGGTGTACCCACAGCTCTTCGTGGAGCCCTGGGCACCTGCACAGCTGGGCATCGTCTGTT
GGGATCCTTATTGCCAGGTGTTCCGGCTTAGACTCCATCATGGGCAATGCAGACTTGTGGCCTCTACTGCTCAGTGTCTATCTT
CATCCCAGCCCTGCTACAGTGTATCCTGTTGCCCTTCTGCCCTGAGAGCCCCGCTTCCTGCTCATCAATCGTAACGAGGAGA
ACCGGGCCAAGAGTGTGCTGAAAAAGCTTCGAGGGACAGCCGATGTGACCCGAGACCTGCAGGAGATGAAAGAAGAGGGTCGG
CAGATGATCGGGAGAGAAGGTCAACATCTGGAGCTGTTCCGCTCACCCGCTACCGCCAGCCCATCCTCATCGCCGTGGT
GCTGCAGCTGTCCAGCAGCTGTGCGGCATCAATGCTGTGTTCTACTACTCAACGAGCATCTTCGAGAAGGCAGGTGTGCAGC
AGCCTGTGTATGCCACCATCGGCTCGGGTATCGTCAACACGGCCTTCACTGTGGTGTGCTGTTGCTGCTGGAGCGAGCTGGC
CGTCGGACCTGCACCTCATTTGGTCTGGCTGGCATGGCGGGCTGTGCTGTGCTCATGACCATCGCCCTGGCCCTGCTGGAGCA
GCTGCCCTGGATGTCTATCTGAGTATCGTGGCCATCTTTGGCTTTGTGGCCTTCTTTGAAGTAGGCCCTGGTCTATTCCAT
GGTTTATTGTGGCCGAGCTGTTTACGCCAGGGGCCCGACCTGCTGCTGTTGCTGTGGCTGGCTTCTTAACCTGGACCTCAAAC
TTCATCGTGGGCATGTGCTTCCAATATGTGGAGCAACTGTGTGGCCCTACGCTTTCATCATCTTCACGGTGTGCTGGTACT
CTTCTTTCATCTTACCTACTTCAAAGTTCTGAGACCAAAGGCCGACCTTCGATGAGATCGCTTCCGGCTTCCGGCAGGGGG
GTGCCAGCCAGAGCGACAAGACACCTGAGGAGCTCTTCCACCCTCTGGGGGCTGACTCCCAAGTGTGA (SEQ ID NO: 5)

Malic enzyme (Yarrowia)

ATGTTACGACTACGAACCATGCGACCCACACAGACCAGCGTCAGGGCGGCGCTTGGGCCACCAGCCGCGGCCGAAACATGTC
CTCCTCCAGCCCCCTCCAGCTTCGAATACTCGTCTACGTCAAGGGCACGCGGAAATCGGGCACCGAAAGGCGCCACAAACC
GTCTGTGCGTTGAGGGCCCCATCTACGTGGGCTTCGACGGCATTCGTCTTCTCAACCTGCGCATCTCAACAAGGGCTCGGGA
TTCCCCCTCAACGAGCGACGGGAATTACAGACTCAGTGGTCTTCTGCCCTCTGCCGAAGCCACCCTGGAGGAACAGGTGACCG
AGCATACCAACAATTCAAAAAGTGTGGCACTCCCTTAGCCAAAAACGGGTTCTGCACCTCGCTCAAGTTCAAAAACGAGGTGC
TCTACTACGCCCTGCTGTCTAAGCACGTTAAGGAGGTCTTCCCATCATCTATACACCGACTCAGGGAGAAGCCATTGAACAG
TACTCGCGCTGTTCCGGCGGCCCCGAAGGTGCTTTCCTCGACATCACCAGTCCCTACGACGTGGAGGAGCGTCTGGGAGCGTT
TGGAGACCATGACGACATTGACTACATTGTCGTGACTGACTCCGAGGGTATTCTCGGAATTGGAGACCAAGGAGTGGGCGGTA
TTGGTATTTCCATCGCCAAGCTGGCTCTCATGACTCTATGTGCTGGAGTCAACCCCTCACGAGTCAATTCCTGTGTTCTGGAT
ACGGGAACCAACAACAGGAGCTGCTGCACGACCCCTGTATCTCGGCCGACGAATGCCCCGAGTGCGAGGAAAGCAGTACGA
CGACTTCATCGACAACCTTTGTGCAGTCTGCCCGAAGGCTGTATCCCAAGGCGGTGATCCATTTTCGAGGACTTTGGGCTCGCTA
ACGCACACAAGATCCTCGACAAGTATCGACCGGAGATCCCTGCTTCAACGACGACATCCAGGCACTGGAGCCGCTCACTTTG
GCCTCCATCACGGCCGCTCTCAAGGTGCTGGGCAAAAATATCACAGATACTCGAATTCTCGTGTACGGAGCTGTTTCGGCCGG
CATGGGTATTGCTGAACAGGTCTATGATAACCTGGTTGCCAGGGTCTCGACGACAAGACTGCGCGACAAAACATCTTTCTCA
TGGACCGACCGGGTCTACTGACCACCGCACTTACCGACGAGCAGATGAGCGACGTGCAGAAAGCCGTTTGCCAAGGACAAGGCC
AATTACGAGGGAGTGGACACCAAGACTCTGGAGCAGTGGTTGCTGCCGTCAAGCCCATATTTCTATTGGATGTTCCACTCA
GCCCCGCGCCTTTAACGAGAAGGTGCTCAAGGAGATGCTCAAAACACACCCCTCGACCCATCATTCTCCCTCTTTCCAACCCCA
CACGTCTTCATGAGGCTGTCCCTGCAGATCTGTACAAGTGGACCGACGGCAAGGCTCTGGTTGCCACCGGCTCGCCCTTTGAC
CCAGTCAACGGCAAGGAGACGTCTGAGAACATAACTGCTTTGTTTTCCCGGAATCGGGCTGGGAGCCATTCTGTCTCGATC

AAAGCTCATCACCAACACCATGATTGCTGCTGCCATCGAGTGCCTCGCCGAACAGGCCCCCATTTCTCAAGAACCACGACGAGG
GAGTACTTCCCGACGTAGCTCTCATCCAGATCATTTCGGCCCGGGTGGCCACTGCCGTGGTTCTTCAGGCCAAGGCTGAGGGC
CTAGCCACTGTGCGAGGAAGAGCTCAAGCCCGGCACCAAGGAACATGTGCAGATTCCCGACAACCTTTGACGAGTGTCTCGCCTG
GGTCGAGACTCAGATGTGGCGGCCCGTCTACCGGCCTCTCATCCATGTGCGGGATTACGACTAG (SEQ ID NO: 6)

Yarrowia Delta(9)-desaturase (Stearoyl-CoA desaturase)

ATGGTGAAAAACGTGGACCAAGTGGATCTCTCGCAGGTGACACCATTTGCCCTCCGGCCGAGATGTCAACTACAAGGTCAAGTA
CACCTCCGGCGTTAAGATGAGCCAGGGCGCCTACGACGACAAGGGCCGCCACATTTCCGAGCAGCCCTTACCTGGGCCAACT
GGCACCAGCACATCAACTGGCTCAACTTCATTCTGTTGATTGCGCTGCCTCTGTCGTCCTTTGCTGCCGCTCCCTTCGTCTCC
TTCAACTGGAAGACCGCCGCTTTGCTGTGCGCTATTACATGTGCACCGGTCTCGGTATCACCGCCGGCTACCACCGAATGTG
GGCCCATCGAGCCTACAAGGCCGCTCTGCCGCTTCGAATCATCCTTGCTCTGTTTGGAGGAGGAGCTGTGAGGGCTCCATCC
GATGGTGGGCCTCGTCTCACCGGAGTCCACCACCGATGGACCGACTCCAACAAGGACCCTTACGACGCCCGAAAGGGATTCTGG
TTCTCCCACTTTGGCTGGATGCTGCTTGTGCCCAACCCCAAGAACAAGGGCCGAAGTACATTCTGACCTCAACAACGACTG
GGTTGTCCGACTCCAGCACAGTACTACGTTTACGTTTCTGCTTTCATGGCCATTGTTCTGCCACCCCTCGTCTGTGGCTTTG
CTGGGGCGCAGCTGGAAGGGAGGTCTTGTCTACGCCGGTATCATGCGATACACCTTTGTGACGAGGTGACTTTCTGTGTCAAC
TCCCTTGCCCACTGGATTGGAGAGCAGCCCTTCGACGACCGACGAACCTCCCGAGACCAGCTCTTACCGCCCTGGTCACCTT
TGGAGAGGGCTACCACAACCTCCACCACGAGTTCCCTTCGGACTACCGAAACGCCCTCATCTGGTACCAGTACGACCCACCA
AGTGGCTCATCTGGACCCTCAAGCAGGTTGGTCTCGCCTGGGACCTCCAGACCTTCTCCAGAACGCCATCGAGCAGGGTCTC
GTGCAGCAGCGACAGAAGAAGCTGGACAAGTGGCGAAACAACCTCAACTGGGGTATCCCCATTGAGCAGCTGCCTGTCAATTGA
GTTTGGAGAGTTCCAAGAGCAGGCCAAGACCCGAGATCTGGTTCTCATTTCTGGCATTGTCCACGACGTGTCTGCCTTTGTGCG
AGCACACCTTGGTGGAAAGGCCCTCATTATGAGCGCCGTGGCAAGGACGGTACCGCTGTCTTCAACGGAGGTGTCTACCGA
CACTCCAACGCTGGCCACAACTGCTTGGCACCATGCGAGTTTCGGTCAATTGAGGCGGCATGGAGGTTGAGGTGTGGAAGAC
TGCCCGAAGCAAGGAAGGACGAGAACATTGTCTCCGATGAGAGTGGAAACCGAATCCACCAGCTGGTCTCCAGGCCACCC
GGGTCGAGAACCCCGGTATGTCTGGCATGGCTGCTTAG (SEQ ID NO: 7)

Pyruvate carboxylase (human)

ATGCTGAAGTTCCGAACAGTCCATGGGGGCGCTGAGGCTCCTGGGAATCCGCCGAACCTCCACCGCCCCCGCTGCCTCCCCAAA
TGTCCGGCGCTGGAGTATAAGCCCATCAAGAAAGTCATGGTGGCCAAACAGAGGTGAGATTGCCATCCGTGTGTTCGGGGCT
GCACGGAGCTGGGCATCCGCACCGTAGCCATCTACTCTGAGCAGGACACGGGCCAGATGCACCGGCAGAAAGCAGATGAAGCC
TATCTCATCGGCCGCGGCTGGCCCCGCTGCAGGCCCTACCTGCACATCCAGACATCATCAAGGTGGCCAAGGAGAACAACGT
AGATGCAGTGCACCCTGGCTACGGGTTCTCTCTGAGCGAGCGGACTTCGCCCAGGCCTGCCAGGATGCAGGGGTCCGGTTTA
TTGGGCCAAGCCCAAGTGGTCCGCAAGATGGGAGACAAGGTGGAGGCCCGGGCCATCGCCATTGCTGCGGGTGTTCCTCGTT
GTCCCTGGCACAGATGCCCCATCACGTCCCTGCATGAGGCCACGAGTTCTCCAACACCTACGGCTTCCCCATCATCTTCAA
GCGCGCTATGGGGTGGAGGGCGTGGCATGAGGTTGGTGCACAGCTACGAGGAGCTGGAGGAGAATTACACCGGGCCTACT
CAGAGGCTCTGGCCGCTTTGGGAATGGGGCGCTGTTTGTGGAGAAGTTTCATCGAGAAGCCACGGCACATCGAGGTGCAGATC
TTGGGGGACCAGTATGGGAACATCCTGCACCTGTACGAGCGAGACTGCTCCATCCAGCGGGCGCACCAAGGTGGTTCGAGAT
TGCCCCCGCCGCCACCTGGACCCGACGTTCCGACTCGGCTACCAGCGACTCTGTGAAACTCGCTAAACAGGTGGGCTACG
AGAACGCAGGCACCGTGGAGTTCTTGGTGGACAGGCACGGCAAGCACTACTTCATCGAGGTCAACTCCCGCCTCGAGGTGGAG
CACACGGTACAGAGGAGATCACCGACGTAGACCTGGTCCATGCTCAGATCCACGTGGCTGAGGGCAGGAGCCTACCCGACCT
GGGCTTGGCGCAGGAGAATCCGCATCAACGGGTGTGCCATCCAGTGGCGGGTCAACACCGAGGACCCCGCGCAGCTTCC
AGCCGACACCGCGCGCATTTGAGGTGTTCCGGAGCGGAGAGGGCATGGGCATCCGCTGGATAATGCTTCCGCTTCCAAGGA
GCCGTCTATCTCGCCCCACTACGACTCCCTGCTGGTCAAAGTCAATTGCCACGGCAAGAACCCACCGCCGCCACCAAGAT
GAGCAGGGCCCTTGGGAGTTCCGCGTCCGAGGTGTGAAGACCAACATCGCCTTCTGTCAGAAATGTGCTCAACAACAGCAGT
TCCTGGCAGGCACGTGTGGACACCCAGTTTCATCGACGAGAACCAGAGCTGTTCCAGCTGCGGCCTGCACAGAACCGGGCCAA
AAGCTGTTGCACTACCTCGGCCATGTATGTTAAACGGTCCAACACCCCGATTCCCGTCAAGGCCAGCCCCAGCCCCACGGA
CCCCGTTGTCCTGTCAGTGCCATAGGCCCGCCCCCGGCTGGTTTCAGAGACATCTCTGCTGCGAGAGGGGCTGAGGGCTTTG
CTCGAGCTGTGCGGAACACCCGGGGCTGTGCTGATGGACACGACCTTCAGGGACGCCACCAGTCACTGCTGGCCACTCGT
GTGCGCACCCACGATCTCAAAAAGATCGCCCCCTATGTTTGCCCAACACTTCAGCAAGCTCTTCAGCATGGAGAATCGGGAGG
AGCCACGTTTGACGTCGCCATGCGCTTCTGTATGAGTGCCCTGGCGGCGGCTGCAGGAGCTCCGGGAGCTCATCCCCAACA
TCCCTTTCCAGATGCTGCTGCGGGGGGCCAATGCTGTGGGTACACCAACTACCCAGACAACGTGGTCTTCAAGTTCTGTGAA
GTGGCCAAAGAGAATGGCATGGATGCTTCCGTGTGTTTACTCCCTCAACTACTTGCCCAACATGCTGCTGGGCATGGAGGC
GGCAGGAAGTGCCGGAGGCGTGGTGGAGGCTGCCATCTCATACACGGGCGACGTGGCCGACCCAGCCGACCAAGTACTCAC
TGCAGTACTACATGGGCTTGGCCGAAGAGCTGGTGCAGCTGGCACCCACATCTGTGTCATCAAGGACATGGCCGGGCTGTG
AAGCCACCGGCTGCACCATGCTGCTCAGTCCCTCCGGGACCGCTTCCCGACCTCCACTGTCACATCCACACCCAGCAC
GTCAGGGGCGAGGCTGGCAGCCATGCTGGCCTGTGCCAGGCTGTCAGCTGATGTGGTGGATGTGGCAGCTGATTCCATGTCTG
GGATGACTTCACAGCCAGCATGGGGGCCCTGGTGGCCTGTACCAGAGGGACTCCCTGGACACAGAGGTGCCCATGGAGCGC
GTGTTTACTACAGTGAAGTACTGGGAGGGGCTCGGGGACTGTACGCGGCTTCGACTGCACGGCCACCATGAAGTCTGGCAA
CTCGGACGTGTATGAAAATGAGATCCCAGGGGGCCAGTACACCAACCTGCATTCAGGCCCCACGATGGGGCTTGGCTCCA
AGTTCAAGGAGGTCAAGAAGGCCATATGTGGAGGCCAACCAGATGCTGGGCGATCTCATCAAGGTGACGCCCTCTCCAAGATC
GTGGGGGACCTGGCCCAAGTTTATGGTGCAGAAATGGAATGAGCCGGGCGAGAGCCGAAGCTCAGGCGGAAGAGCTGTCTTTCC
CCGCTCCGTGGTGGATTCTCGCAGGGCTACATCGGTGTCGCCATGGGGGTTCCCGAACCCTTTCGCTCTAAGGTACTGA
AGGACCTGCCAAGGGTGGAGGGGCGGCTGGAGCCTCCCTCCCTCCCTGGATCTGCAGGCACTGGAGAAGGAGCTGGTAGAC
CGGCATGGGGAGGAGGTGACGCCGAAGATGTGCTCTCAGCAGCTATGTACCCCGATGTGTTTGGCCACTTCAAGGACTTCAC
TGCCACCTTTGGCCCCCTGGATAGCCTGAATACTCGCCTTCTCTGAGGACCCGAAGATCGCAGAGGAGTTTGGAGTGGAGC
TGGAGCGGGGCAAGACGCTGCACATCAAGCCCTGGCCGTGAGCGACCTGAACCGGGCCGGCCAGAGGCAGGTCTTCTTTGAG

CTCAATGGGCAGCTGCGGTCCATCTTGGTCAAGGACACCCAGGCCATGAAGGAGATGCACTTCCACCCCAAGGCCCTAAAGGA
CGTGAAGGGCCAGATCGGGGCGCCCATGCCCTGGGAAGGTGATAGACATCAAAGTGGTGGCAGGGGCCAAGGTGGCCAAGGGCC
AGCCCCCTGTGTGCTCAGTGCCATGAAGATGGAGACTGTGGTGACCTCACCCATGGAGGGTACTGTCCGCAAGGTTTCATGTG
ACCAAGGACATGACACTGGAAGGTGACGACCTCATCTGGAGATCGAGTGA (SEQ ID NO: 8)

ACC (*Saccharomyces cerevisiae*)

TTATTTCAAAGTCTTCAACAATTTTTCTTTATCATCGGTAGATAACATCTTGATAACTTCAGATAATCCATCAATAGCATTGT
CATGGTCGCTTCTGATCTTTTAGCTAAGCTTTGAGCGAATGACTCTAATTTCAAACCCTTTAGTTTATCGTCCAAAGTTTTG
TAGTTTTCTTCAATCCATGTTGCGACTTGCCATCATCTTCATGGTCCACTGAAGCAGGGTACCACGATCTAATCTTTCGAT
CTTTTCTAATCTTGATGCTTCGCCTACCTGATGGCTCAACCTTTTAATCAAATATTCTTCGTTCAATCTTCTTCTCAATCTCC
AGAAGAAGAAACGACGTGCCTCGGTCCATTCCAGTTCCTTAGAAAATAACACCCTTGGCCACCATACTGTAAGACCTATCGTGC
AAATCAGCAAATTGAAGACTGATTTGTCCGTAATTTGGCAATAGTTCTCTCTCAGCATCAGCTAATTGCTTGGATATTTGCTG
ATGTACTTCTGGAGCCAACTCTTGTGGATAATTGAGATCTCAATTCTCTGTACTTGTATCCAATCTGTTTCATGGTGTCCA
GCAATTTTCTCTACGGAACCTTGATACCAACCATACTTGTGGTTCCAAAACACCAGCTCTAGCGTTGACGTGCGCATACATT
TCCATTTGGTTCAGCGTTGATAGTTGGATCGACAACAACCCATGAACCACCTCTTAGTTTACCCGTTAGGTGGGATATAGATAAT
AATTGGTTGTTTGTAAATCCACCAATGCGTCAACAATAAACGAACCATACTTCAAGACTTCGTTGAACATATCACGTTGACCAC
CAGAGAAACCTCTCCAGTTGGCCAAAATCATCTTGGCAATTGTTTACCCTTGTAAAGTCATTGATAGCTTGAGCAGTCTTG
AAGGCGGAGTTTGGATGCCAACTTGACCAGGTTCTTGAATTAATGTTTCAGCACTATTTGGATTAGCTGGATCAGCAGGAAT
CAAGTTCTCGACAGTTCTTGTTCACACCAATAACACCCAGTGGAAATACCACCAAGACGGGCTCTACCAACGCAACACCTT
TGGCCCATCTGACAAAGTTTCAAAGAAAGACCTTTATCAAACAAACCATAATTCAAATCCACTTTCAGTCTCACGACCTTCA
ATCATCCATCTTACATGCTAAGTTTCATCATTAGTTGGAGTGAAATCAACTGGTCTATCCCATGTGCTCTTAGTTTCCAAGAT
AGGAATCGGCATATTACGCTTGGCTGGAACATAAGACATCATCAACAATCTTCTCTACACCACTAAATCGTCAACAGCAG
TCAAATGTGAAACACCGTTGTATACATGATTTGAGTACCACCAATTTGTAAGTTAGAAGTATAAACTTCTCTACCCAGCATT
TTGTTGATTGCGAGGACCAGTTAAAATAATTGGCTGGCCTTCGACCTGAATAGCTCTTTGACCCAAACGAACCAATAAGC
ACCGATACCGACGGATCTACAAGTGACTAAGGTGATAGTGAAGATATCGTGGTAAGCCCTTGACGTTGCACCAGCAATTAAC
CAGATCCACGTAGACATTCGACACCTAACCCATCTTCAGAACCAATAATTGCTTGTATGACAAATCTTTCTTACCCTTTTATA
ACAGTACGTTTCAGTGAGAACAGAATTTCTTTGTCAAATTTCTTTAAAGTTTCCATACCTTCACTTGTTAAGTATAAGTATTG
AAGGCCCTTGTCCGATTGGCAGCATCTCCATGCAACTTGAAATAGTGGAAACAATCTCTTACGCCATACCAATTCCTTGGCAG
CTGAGTTTGCAGCCAAGTAAATCTTGGGATACCACGCTTTCTAGCATATTCAGTAACCTTATTGAAGAATTCGCTTTCTTGT
GGACCAAGGAACCGATCTTGAATGTGATATCGTTAGCAACAACAACAATTTGACGGCCTCTTGGATATTCAGGAGTCTTTAC
AGTAATCTTAAAGGCAACCATAACCAATAGCGTTGGCACCAGGTTCTCTTTCCACCTCAGTTAATTCGCCGTTTTCTATCTTCAA
TCAACTCGTTGGAAATAAAGAAATCATCTGTTAACTTAACATCTGCAGAGAAATTTTCCATTGGGATGACGATGCTTGGCGG
AATAATTCGGGAAGTATAGACATATGTTGTACCCATCAAGTGTGCCTTATAACGTTTGGTTGCAACCATTCCCTTAACAGG
GTAAGGAGTAGCAATAGTGCTTAAATGCATGGATCCAGGTTTACCCAAGACTTAAATACCCATTCACCTTTTGGCTTCTTGA
CTTCGGTGTACATTTCTGTTTGTATAACATAACCGAAACGTTATTGATCAAGGCACGCAATGGTACTGGGGCACCTGTTTGA
GGATCTTTGATGATGATTCTAATTTCCGGCAGAAGAAACACGCAATCTCAACAATCTCTTACCAAACTTTTCTAAGAAACACC
GAAGGCGGCTTCGACATCTTCTGGAGAGATATCAAACACCGCAATGAAGTTGATGAAGATATGATTCAAATCAGAATTTGAAG
TGTCGGTGACTTCTAAATTTACCAATATATCACTCATCAATCTGTTAGCTTCAGAAGTCAGATATTCTTGAATGAAATGTCA
TCACGGATATGACCCGTTCTAATAATACCTCTTGTAAAGAAATCTCTTATCCAATGGAGAAGTCTTACTAACAGCTTCGTAGAC
ATGGATGTTTCTATTATCAGTGAAAAATTGGTTAATGTTGAGTTGGACAATCTTCTAATTTCCAGTTGGAAGGCCAAAGCCG
GCTCAATGTGACAAATGTTTCTAATTTTCGTTAATTTGGACCGTTAAAAGTATAATACTTTGGATAAGACCCATCTTTAAAA
CCGAACATAAATGTGATACGACGGATAGAAGCAATTGATTAATTCCTGCTTATTCAAATCCAAATTTCTCTCAACCTTACCAA
AATTTCTCTTTCAGATTCGAAACCTTCTGTAGAAGCAACACAAACATTAGCAACATTACTCAACGATGCGGAGCTACCAGAAC
GATCAGGAGCAGGTCCGTTAGAAGAAGATTGGTGACGAGGAATAACTTCCAACTTTGTGACAAAATTTTCATCAACATCATCT
AAATGATCCACAGCCATCAAAATACCTTCTCTAACGGAGATGACTGACTGTTGCAACATATGACAAATCTGAAACAGAAAC
AGCCCTGTTTCATACCCATTTTAGATTTAACAGTTGGAAAGGTGGAGAACGCAGCTGAAGGTAGTTGGAATTTCCATTCAACAA
TTGGAACGTGTGACACCTTCGTGAACCTTAATATCTCTATGGTGTAAGCACGATAAGCACGACGAATATAGACTTGAGCAGCT
GCAGCAGTCACAACCTGGGCTTGTATGGGTTAGGAATTTGAAGTAAAACATCGAACACAACGTAATTAGAATCGATCAAGTCCTT
CAAGATATTCAAATCTGGTTCAGAGCGCTTTGGATTGGATGAGCCATAGGCAACCTTCACAACAGAGGATTTTAAAGATATGTT
CAATTTGTTTCAGTTCTTTCTTGTACCGAAGGTAAAGCGCTTGAATCAAATTTCTCTTGTGTTGATAGCGACCTTAGCGGTA
GCCTTAGATCTAGTTCAACAATATGTTGTAGAGGAGTAGAGAAAATGGCAGAACTTTAGAAGATAACTTGCACAATGGTTG
ATAATGTTTCAAGATAGCTAGGATCAGGTTATTCTTCGCTGAAACTTTTCAATGAGACAAAACAGTTAGCGCAACTTTATCTA
GATCTTTAGGGTTTTTCATCAGCAATTTTCAAGATGATATTTTCTCAGCAACATTTGGACCATTGAATAACTTTTCAACTTCG
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FAA (*S. cerevisiae*)

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Acyl-CoA synthetase

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FAT

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NO: 12)

FAT

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GGAGGCGAACTTGAACTCACTGGTGGACAAGGACAATTACTGCAAAACCAACGTAAGTTGAGTAACTTGGAGGTTAACCAGC
GTCCAATTAGCTACACAGCAGTTCCAAATGACAACCTAGTCTGAGCAATAGGAATTTTGTAAATAACTTAGACATCTTGCGT
AGCTACGGTTCGGCCGGCGATGAACGGAATGTGCCATTGAGTACCAGAAGGTTAATCGAAACAAACAGCATGTGAACAT
AAACTCCTGCCATTCAACCGATGCAGATAATGCCACAAAGAAATGGTGCAGCAATGCATTTAAGAACCTTCAGTGAAA
20 ATAACTGAACAATGAACTTAAACGGGATTTCCGACCATCTGTGAGTCGCTTTTCAACTGGGAACTAATCCAAGTTGAAATG
CCCAAGTTGTGCCACTTTCCAGTGCGAATTTTCGTTGATTATTCAGTCTTTGCCAATGGTCAGTATCATTGGGACTGTTCCGA
CTGGGTTTCGCAAAAGCCATAATCCCTTGCCAGATATAACCGAAGTTCTCGGAGCAGAAATAGCTGATTCGTGAGCTTACACA
GCAACGATAGCAACGAGTCCAAGTCAAGAAAGCCTTTTTCGTGCACAGGGAAGACGGAGATGTTGATCCGACGAGGGATATA
GCCGCGTTGAATGAGGATATCGGATCGGAGTATTTGGACTCGGAGGCAGAGAGCTGCTTGGAGCCGTTTATGTTGCCAAGATC
25 AAGTAATCAGCCACTTTCAAGACTGAGTTCCTTTAATAATATCGAGAATGAAGACTATAAATCAAATACAGGCAAGATATATT
TAAGACATCTCTGATTTCGATTTTACCGACGATGCATTTTCCAAGTGAGACCGATGGGGAAAGCTCTATGACCGAGGGGCCGATT
TCTAGGATGGAATAAAAAACCAGGAGGACGATAAGTGAAAATTTCAGAGGAGGCATACCTATTTCCATGCATGTGCGAGAAAT
TGGATCCAACGACAACATTTCCGTTTCGACTGTGTGAAATTGAAGATTCTGAGTTGGAGGAGTTTTTACCACAACAACAAACAA
ACAATTAA (SEQ ID NO: 13)

PCS (*Saccharomyces cerevisiae*)

CTACAACCTACTCTTATTTCTGCTGCTCTTAGCAAAAGTTTCTGCGATAACTCTTCTCTGGATTTTACCTGTAGCGGTTTTTG
GTAGCTTATCAACAAAGTACACCTTGGTTGGAATTTTGAAGAGGCTAGGTGCTTCTTTAAGAAGTTCACCAGTTCTTCGTAG
35 GTCATTTTTCTCCCTTCTTCAAAACAATGGCGGCTTGAACCTACTTGGCCGTACATATCGTCGGGAACACCAATGCAACGGC
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AAGTTCTCTTGTAGCTTTTGGATTATTAGCATACCCCAAAGTGACGTTTTTCGCTCTGATGGAACCTTCGCCGACTTTGCC
CGGGGGCAAGACATTGTCTATGTCTATAGATGACGACGGTGACTCCTTGTGGCTGGCCACAGTACCAGGCTTCTCTTTTC
40 CTGGAGGCAGATTGTTTGGAGTCATTTGATGTGATGCTTCGGTCATCGCATAGGCCCTCCAAGACAGGTGCATTGAATTCCTTC
TCCAGCTTATGGAACGTTGCTGGAGCCAAAGCAGAAGAACAGATCTGATGAATCTAATGTGTGGGAAAGGGTTGGTTTGGG
CTGTTTCAGCATAATCATGTCTATTGTGGGAACGCAACTGAACCAATTACAGTTGTACTTAAACAAATTGGTCCAGATAACT
TTGGATGGAATCCATCGGGAACCAACAGAACCCCTGAGTTCTAAAGTGGAAGTAAACACCAATTAACCCATGGACGTGG
AAAAGAGGCATCAGACATAAGATCTGTCCAAGGGCGTTAGCTTGTAAGTGTAGCAATGTTCAACGTGCTTCTACAATGTT
45 CAAATGTAAACAAAGGCACCGTTTTTGGAGTGGAGGTGGTACCCTGGTATGCAAAATCAGGGCAACGTCACTGGAACGGGCAA
ACCCAGGGAAATTAACGGGATTTGTGTTGACAAATTTGGCGTGTGTTCAAAGACCGGTAAATAACCCTTTTGTAGTTGTCTCT
GGAGAGTATATATCACTCTACCCTAACCTGGTGCATCGAAGGCCAGCTCTACGATAAAACATCCAAACGTGGAGGCAGA
TTTTAGAAATTCAGAACTCTGTAACTTTGTGGTACCTTTTGGGACGCAATCGCCTTAGATTTCAGGTCAATCAATAAAAAAT
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50 TCCAGCCCATACGCATGGATATCGCCACTGTATCTTGTCTGAAAACAGCTCCGTACAATGGAGAATTAGGATTGTGAACAT
GGTCTGGAAGTGACCCACCATGTGGGATAGATCCCTGTAGGTACCTGAGTGTCCGTTTCAGGAACAATAACGGCGACATTAT
CGGATACGCTAAAAGTATCGTTGAACGAAGCAGTAACAGTAGCGGCACCTTGTCT (SEQ ID NO: 14)

ACLY (*Homo sapiens*):

CGAGCCGATGGGGGCGGGGAAAAGTCCGGCTGGGCCGGGACAAAAGCCGGATCCCGGAAGCTACCGGCTGCTGGGGTGCTC
55 CGGATTTTTCGGGGTTTCGTGGGCTGTGGAAGAAGCTGCCGCGCACGGACTTCGGCAGAGGTAGAGCAGGTCTCTCTGCAGC
CATGTCCGCCAAGGCAATTTAGAGCAGACGGGCAAGAAGCTCTTTACAAGTTTCATCTGTACCACCTCAGCCATCCAGAATC
GGTTCAAGTATGCTCGGGTCACTCTTGACACAGACTGGGCCCGCTTGTGTCAGGACCAACCCCTGGCTGCTCAGCCAGAATTTG
GTAGTCAAGCCAGACCACTGATCAACCGTCTGGAAGAACTTGGTCTCGTTGGGGTCAACCTCACTCTGGATGGGGTCAAGTC
60 CTGGCTGAAGCCACGGCTGGGACAGGAAGCCACAGTTGGCAAGGCCACAGGCTTCCTCAAGAACTTTCTGATCGAGCCCTTCG
TCCCCACAGTCAGGCTGAGGAGTTCTATGTCTGCATCTATGCCACCGAGAAGGGGACTACGTCTGTTCCACCACGAGGGG
GGTGTGGACGTGGGTGATGTGGACGCCAAGGCCAGAAGCTCTGTTGGCGTGGATGAGAACTGAATCCTGAGGACATCAA
AAAACACCTGTTGGTCCACGCCCTGAAGACAAGAAAGAAATTTTGCCAGTTTTATCTCCGGCTCTTCAATTTCTACGAGG
ACTTGTACTTCACTACCTCGAGATCAATCCCTTGTAGTGACCAAGATGGAGTCTATGTCTTGACTTGGCGGCCAAGGTG
65 GACGCCACTGCCACTACATCTGCAAGTGAAGTGGGGTGACATCGAGTTCCCTCCCCCTTCGGGCGGGAGGCATATCCAGA
GGAAGCCTACATTGCAGACCTCGATGCCAAAAGTGGGGCAAGCCTGAAGCTGACCTTGCTGAACCCCAAGGGAGGATCTGGA

CCATGGTGGCCGGGGTGGCGCCTCTGTCTGTACAGCGATACCATCTGTGATCTAGGGGGTGTCAACGAGCTGGCAAACATAT
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 CCCAGATGGCAAGATCCTCATCATTGGAGGCGAGCATCGCAAACCTTACCAACGTGGCTGCCACGTTCAAGGGCATCGTGAGAG
 CAATTCGAGATTACCAGGGCCCCCTGAAGGAGCACGAAGTCACAATCTTTGTCCGAAGAGGTGGCCCCAACTATCAGGAGGGC
 5 TTACGGGTGATGGGAGAAGTCGGGAAGACCACTGGGATCCCCATCCATGTCTTTGGCACAGAGACTCACATGACGGCCATTGT
 GGGCATGGCCCTGGGCCACCGGCCCATCCCCAACAGCCACCCACAGCGGCCACACTGCAAACCTTCCTCTCAACGCCAGCG
 GGAGCACATCGACGCCAGCCCCAGCAGGACAGCATCTTTTTCTGAGTCCAGGGCCGATGAGGTGGCGCCTGCAAGAAGGCC
 AAGCCTGCCATGCCACAAGATTCACTCCCAAGTCCAAGATCCCTGCAAGGAAAGAGCACCCTCTTCAGCCGCCACACCAA
 GGCCATTGTGTGGGCGATGCGAGACCCGGGCCGTGCAAGGCATGCTGGACTTTGACTATGTCTGCTCCCGAGACGAGCCCTCAG
 10 TGGCTGCCATGGTCTACCCCTTCACTGGGGACCACAAGCAGAAGTTTTACTGGGGGCACAAAGAGATCCTGATCCCTGTCTTC
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 CACCATGGAGACCATGAATATGCCAGATCCGGACCATCGCCATCATAGCTGAAGGCATCCCTGAGGCCCTCAGGAGAAAGC
 TGATCAAGAAGGCGGACCAGAAGGGAGTGACCATCATCGGACCTGCCACTGTTGGAGGCATCAAGCCTGGGTGCTTTAAGATT
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 15 AGGCATGTCCAACGAGCTCAACAATATCATCTCTCGGACCACGGATGGCGTCTATGAGGGCGTGGCCATTGGTGGGGACAGGT
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 TCTTGCCAGTTTATTGAGATGTGCTGATGGTGACAGCTGATCACGGGCCAGCGTCTCTGGAGCCACAAACCATCATTTG
 25 TGCGCGAGCTGGGAAAGACCTGGTCTCCAGCCTCACCTCGGGGCTGCTCACCATCGGGGATCGGTTTGGGGGTGCTTGGATG
 CAGCAGCCAGATGTTTCAAGACCTTTGACAGTGGCATTATCCCCATGGAGTTTGTGAACAGATGAAGAAGGAAGGGAAG
 CTGATCATGGGCATTGGTCAACGAGTGAAGTCGATAAACAACCCAGACATGCGAGTGCAGATCCTCAAAGATTACGTCAGGCA
 GCACTTCCCTGCCACTCCTCTGCTCGATTATGCATGGAAGTAGAGAAGATTACCACCTCGAAGAAGCCAAATCTTATCTGA
 ATGTAGATGGTCTCATCGGAGTGCATTTGTAGACATGCTTAGAAACTGTGGGTCTTTACTCGGAGGAAGCTGTGAATAT
 30 ATTGACATTGGAGCCCTCAATGGCATCTTTGTGCTGGGAAGGAGTATGGGGTTTATTGGACACTATCTTGATCAGAAGAGGCT
 GAAGCAGGGGCTGTATCGTCATCCGTGGGATGATATTTCATATGTTCTTCCGGAACACATGAGCATGTAA (SEQ ID NO:
 15)

FAS (Mycobacterium bovid subsp.bovis):

ATGAGTCAGACGGTGC CGGTGTGATCGCAGACAAAAGGGCGAACCCGTTGAGCTGGTGAACATTGTCTGCCGGATCCCGG
 35 ACCCGGCGAGGCCGTGGTTCAGCTCACCCTGCGGGGTATGCCATACCGACCTGACCTACCGCGAGGGCGGCAACAACGACG
 AATACCCTTTTCTGCTCGGACACGAGGCCGCGGGCATCATCGAGGCCGTGCGGCCGGGTGTAACCGCAGTCGAGCCCGGCGAC
 TTCGTGATCTGAACTGGCGTGCCGTGTGCGGCCAGTGCCGGGCTGCAAACGCGGACGGCCCCGCTACTGCTTCGACACCTT
 TAACGCCGAGACAGAAGATGACGCTGACCGACGGCACCAGCTCAGTGCAGGCGTGGGCATCGGGGCCCTTGGCGATAAGACGC
 TGGTGCATCTGGCCAGTGACAGAAGGTGATCCGGCTGCCGATCCCGCGGTGGCCGGCTGCTGGGTTGCGGGGTGATGGCC
 40 GGCTTGGGCGCCGCGATCAACACCGCGGGGTAAACCGCGACGACACCGTTCGCGGTGATCGGCTGCGGCGGCGTTGGCGATGC
 GCGATCGCCGGTCCGCGCTGGTTCGGCGCCAAACGGATCATCGCGGTCGACACCGATGACACGAAGCTTATGATGGGCGCGCA
 CCTTCGGCGCCACCCACACCGTCAACGCCCCGGAAGTCGACGCTCGTCCAGGCCATCGGCGGCCCTACGGATGGATTTCGGCGCG
 GACGTGGTGTGACGCGCGTGGCGGACCGGAAACCTACCAGCAGGCCTTCTACGCCCGCATCTCGCCGGAACCGTTGTGCT
 45 GGTGGGTGTTCCGACGCCGACATGCGCCTGGACATGCGCTGGTTCGACTTCTCTCTACGGCGGTGCGCTGAAGTCGTCGT
 GGTACGGCGATTGCTGCGCGAAAGCGACTTCCCCACGCTGATCGACCTTTACCTGCAGGGCCGGCTGCCGCTGCAGCGGTTT
 GTTCCGAACGCATCGGGCTCGAAGACGTCGAGGAGGCGTTCCACAAGATGCATGGCGGCAAGGTATTGCGTTCCGTTGGTGTAT
 GTTGTGA (SEQ ID NO: 16)

AMPK (Homo sapiens):

AGTTCTTGGAGAAAGATGGCGACAGCCGAGAAGCAGAAACACGACGGGCGGGTGAAGATCGGCCACTACATTCTGGGTGACAC
 50 GCTGGGGGTGCGCACCTTCGGCAAAGTGAAGGTTGGCAAACATGAATTGACTGGGCATAAAGTAGCTGTGAAGATACTCAATC
 GACAGAAGATTTCGAGCCTTGATGTGGTAGGAAAAATCCGACAGAGAAATTCAGAACCTCAAGCTTTTCAGGCATCCTCATATA
 ATTAACTGCACAGGTATCAGTACACCATCTGATATTTTATGGTGTGGAATATGTCTCAGGAGGAGAGCTATTTGATTA
 TATCTGTAAGAATGGAAGGAAATCTGATGTACCTGGAGTAGTAAAAACAGGCTCCACGAAGGAGCTGGATGAAAAAGAAAGTC
 55 GCGCTGTGTTCCAAACAGATCCTTTCTGGTGTGGATTATTGTACAGGCATATGGTGGTCCATAGAGATTGAAACCTGAAAAAT
 GTCCTGCTTGATGCACACATGAATGCAAAGATAGCTGATTTTGGTCTTTCAAACATGATGTGAGATGGTGAATTTTAAAGAAC
 AAGTTGTGGCTCACCAACTATGCTGCACCAAGATAATTTAGGAAGATTGTATGCAGGCCAGAGGTAGATATATGGAGCA
 GTGGGGTTATCTCTATGCTTTATTATGTGAACCTTCCATTTGATGATGACCATGTGCCAACTCTTTTAAAGAGATATGT
 GATGGGATCTTCTATACCCCTCAATATTTAAATCCTTCTGTGATTAGCCTTTTGAACATATGCTGCAGGTGGATCCCATGAA
 60 GAGGGCCACAATCAAAGATATCAGGGAACATGAATGGTTTAAACAGGACCTTCCAAAATATCTTTCTTCTGAGGATCCATCAT
 ATAGTTCAACCATGATTGATGATGAAGCCTTAAAGAGATGTGAAAAAGTTTGAAGTCTCAGAGAGGAAGTTCTCAGCTGT
 CTTTACAACAGAAATCACCAGGATCCTTTGGCAGTTGCCTACCATCTCATAATAGATAACAGGAGAATAATGAATGAAGCCAA
 AGATTTCTATTTGGCGACAAGCCACCTGATTCTTTTCTTGTGATGATCATCCTGACTCGGCCCCATCTGAAAGAGTACCAT
 65 TCTTGGTTGCTGAAACACCAAGGGCACGCCATACCCTTGTGATGAATTAATCCACAGAAATCCAAACACCAAGGTGTAAGGAAA
 GCAAAATGGCATTTAGGAATTAGAAGTCAAAGTCGACCAATGATATTATGGCAGAAGTATGTAGAGCAATCAAACAATTGGA

5

TTATGAATGGAAGGTTGTAAACCCATATTATTTCGCTGTACGAAGGAAGAATCCTGTGACAAGCACTTACTCCAAAATGAGTC
TACAGTTATACCAAGTGGATAGTAGAACTTATCTACTGGATTTCCTAGTATTGATGATGAAATTACAGAAGCCAAATCAGGG
ACTGCTACTCCACAGAGATCGGGATCAGTTAGCAACTATCGATCTTGCCAAAGGAGTGATTGAGATGCTGAGGCTCAAGGAAA
ATCCTCAGAAGTTTCTCTTACCTCATCTGTGACCTCACTTGACTCTTCTCCTGTTGACCTAACTCCAAGACCTGGAAGTCACA
CAATAGAATTTTTTGAGATGTGTGCAAATCTAATTAATAATCTTGACAATAA (SEQ ID NO: 17)

The vector was transformed in *Polg Yarrowia lipolytica* strain and selected on leucine deficient agar plates. The colonies were screened for the correct insert in the genome using PCR.

- 10 $\Delta 9$ -FW AATGGTGAAAAACGTGGACCAAGTGGA (SEQ ID NO: 18)
 $\Delta 9$ -REV ATGGATCCCTAAGCAGCCATGCCAGACATAC (SEQ ID NO: 19)
 GLUT1-FW AATGGAGCCCAGCAGCAAGAAGGTGA (SEQ ID NO: 20)
 GLUT1-REV AATGGGTACCTCACACTTGGGAGTCAGCC (SEQ ID NO: 21)
 Hemoglobin FW AGAGACCGGGTTGGCGGCGCA (SEQ ID NO: 22)
 15 Hemoglobin REV CAGCGTCTTGAGCGTACAAA (SEQ ID NO: 23)
 Cytochrome FW AATGATCATCAACGGCAAGGTCT (SEQ ID NO: 24)
 Cytochrome REV TTATTTCTGACCCTGGAGGTAGAAG (SEQ ID NO: 25)
 Pyruvate Carboxylase FW AATGCTGAAGTTCCGAACAGT (SEQ ID NO: 26)
 Pyruvate Carboxylase REV CGATGGTACCTCACTCGATCTCCAGGATG (SEQ ID NO:
 20 27)

The resulting colony was grown in YPD media (full media: yeast extract, peptone, dextrose) and YNB media (minimal media, containing all nutrients, but no amino acids, and no nitrogen or carbon source). When grown in YNB media was used, nitrogen was provided as ammonium sulphate and carbon was provided as glucose at a Carbon to Nitrogen ratio of
 25 150. This C/N ratio is necessary for triggering oil accumulation. Upon depletion of nitrogen excess sugar is channeled to oil accumulation in yeast.

Oil Harvesting: The cells were grown in nitrogen-restricted growth media. After 72 hours the cells are harvested and dried at 60°C for 2 days. The cells were directly treated with 1% sulphuric acid and methanol for 24 hours at 90°C. The oil was converted to FAME (fatty
 30 acid methyl esters) and extracted by hexane. The hexane extraction is repeated twice to recover 95% of FAME. The hexane fraction is evaporated and re-suspended in 5 ml of hexane. 10ul of the fraction is injected into GC-MS to quantify FAME.

Cell cultures were harvested and prepared for fatty acid analysis, as described earlier (Voelker and Davies, 1994). The fatty acid content of each sample was quantified by GC-MS
 35 using a single quadrupole MS with an electron impact ionization source. The GC column was

a 30m long HP-5 MS (5% phenyl)-methylpolysiloxane with a ID of 0.25mm and a film thickness of 25µm. The GC elution conditions were as follows: 100°C as the starting temperature (5min), a 15 min ramp to 250°C, hold at 250°C for 10 min.

5 EXAMPLE 1

A qualitative profile of total free fatty acid (FFA) pool was probed in *Y. lipolytica* culture grown in the log and stationary growth phases using GC-MS (Figure 1 A-C). The major FFA pool is comprised of saturated palmitic and stearic acids and unsaturated oleic acid. A comparison of the FFA profiles in the two growth phases revealed absence of oleic acid in the stationary phase while similar peak intensities of stearic and oleic acid were observed in the log phase (Fig.1 A, B). Analysis of the total lipids (FFA+lipids) during stationary phase recovered partial amount of the oleic acid suggesting that oleic acid is being routed for TAG formation (Fig. 1C). The remaining pool of oleic acid is utilized for downstream poly-unsaturated fatty acids and therefore cannot be rescued. Therefore, oleic acid is channeled to TAG formation in a temporal fashion during stationary growth phase that coincides with the timing of activation of intracellular TAG storage pathway. This suggests a checkpoint mechanism may exist to monitor oleic acid levels to regulate oil accumulation.

EXAMPLE 2

20 Since in mouse SCD is essential for lipogenesis (see, e.g. *Regulation of stearoyl-CoA desaturases and role in metabolism*. Prog Lipid Res. 2004 Mar;43(2):91-104) and is reported to be important for the synthesis of unsaturated fatty acids in most organisms, we tested the role of *Y. lipolytica* SCD as a rate limiting step in TAG accumulation. Protein sequence analysis of *Saccharomyces cerevisiae* OLE1 gene encoding SCD against *Y. lipolytica* protein sequences revealed a protein with 51% identity. The *Y. lipolytica* desaturase contains three histidine boxes and a cytochrome b5 domain typical to other stearoyl-CoA desaturases. Since desaturase enzymes are highly regulated at gene transcription level (see e.g., *Regulation of stearoyl-CoA desaturase by polyunsaturated fatty acids and cholesterol*. James M. Ntambi. Journal of Lipid Research, Vol. 40, 1549-1558, September 1999) and during the log and stationary phase of cell growth (see Mol Cell Biol Res Commun. 1999 Apr;1(1):36-43), we modulated the native *Y. lipolytica* desaturase gene expression with a quasi-constitutive promoter. A single copy of the modified gene was stably integrated into the genome. GC-MS

profile between the mutant and wild type strain showed a significant increase in the ratio between unsaturated to saturated fatty acids (Fig. 2 A, B). Confocal microscopy of intracellular lipids stained with Nile red showed a correlation between elevated unsaturated fatty acids and excess accumulation of TAG (Fig. 2C: wild type, Fig. 2D:SCD overexpressor). In most cases the entire cell volume of the SCD overexpressor cells is completely filled with TAG (Fig. 2D). These findings provide evidence of a key regulator gene that surprisingly is sufficient to induce over-accumulation of intracellular TAG by altering the ratio of unsaturated fatty acids to saturated fatty acids.

The confocal imaging of the growing and stationary cells revealed a striking difference in the pattern of oil accumulation. We tested the intracellular TAG mobility of stationary phase oil-rich mutant cells upon re-entry to mitotic cell cycle. We fed-batch stationary phase cells with minimal media containing higher concentration of sugars (300g/l). The cells efficiently re-enter the log phase and followed rapid growth and biomass production consuming all of the sugars within 96 hours. Interestingly, image analysis showed the mutant strain accumulating excess intracellular oil even during log phase, which is atypical to oleaginous yeast. Although the wild type cells were unable to grow in high sugar concentration, the continuous oil production and yeast-like bodies were absent in log phase even at sugar concentrations favorable to growth.

Taken together, these results establish a continuous fed-batch process using high concentration of sugars, and suggest that the engineered yeast strain is able to accumulate oil continuously during the log and stationary growth phases.

EXAMPLE 3

Two types of mutant yeast were generated, which overexpressed the following genes: Mutant 1: SCD, Hemoglobin, Glut1, Cytochrome; Mutant 2: Hemoglobin, Glut1, Cytochrome. The respective genes were cloned into plasmid YLEX between PmlI and Kpn sites. The vector was transformed in Po1g *Yarrowia lipolytica* strain and selected on Leucine-deficient agar plates. The colonies were screened for the correct insert in the genome using PCR. The resulting colony was grown in YPD media and YNB media with a carbon to nitrogen (C/N) ratio of 150. This C/N ratio is necessary for triggering oil accumulation. Upon depletion of nitrogen excess sugar is channeled to oil accumulation in yeast.

In order to measure maximum oil accumulation, the cells were grown in nitrogen restricted growth media. After 72 hours the cells were harvested and dried at 60°C for 2 days. The cells were directly treated with 1% sulphuric acid and methanol for 24 hours at 90°C. The oil was converted to FAME (fatty acid methyl esters) and extracted by hexane. The hexane extraction was repeated twice to recover 95% of FAME. The hexane fraction was evaporated and re-suspended in 5 ml of hexane. 10ul of the fraction was injected into GC-MS to quantify FAME. The maximum oil accumulation in the mutant strains was 80 grams/l.

The glucose uptake kinetics of mutant 1 ("D9") and wild type yeast ("LS") were compared. Figure 3 shows that mutant 1 consumed all sugar provided after 72 hours, whereas wild type yeast only consumed about 70% of the provided sugar. It was observed that wild type strains did not consume all sugars even at extended period of time.

It was next determined whether the mutant strains could use biomass hydrolyzate as a carbon source. A 2-L bioreactor was set up containing corn stover hydrolyzates (Hz) in the presence of 1% yeast extract. The Hz contains 20 gram of glucose. We added (fed-batch) 180g of glucose to final conc. of 200g/l. We determined that the wild type cannot grow in the toxic biomass Hz. Mutant 1 and mutant 2 cells were grown in shake flask to a final OD of 3 in 50ml. The overnight culture was added to the respective bioreactor and fermentation was carried out for 72 hours at 30°C. The two reactors, one with mutant 1 and the other with mutant 2, were run under identical conditions. The stirring was 800rpm and the pH was set at 5.5.

Both strains consumed around 50% of the supplied glucose in 72 hours due to limitation of some nutrient factors in the medium (Figure 4A, showing mutant 1 strain). The reason for 50% sugar consumption in both strains is due to the presence of Glut1 which is known to transport glucose into the cell. Mutant 1 consumed 123 gram of glucose whereas mutant 2 consumed 105 grams of sugar. This result shows that the mutant cells can consume almost 50% of the sugars and resist the toxicity of the Hz very well compared to wild type, which do not grow well and consume less than 10 gram of sugars in earlier experiments. The mutant strains showed robust growth and good consumption of sugars. The leftover sugars were not consumed due to some deprivation of nutrient factors (see Figure 5 and 6).

Mutant 1 (with combination of genes overexpressed) displayed increased oil synthesis as compared to mutant 2. Mutant-1 produced 26 grams of oil per liter (Figure 4B) and mutant-2 produced 14 grams of oil per liter. This suggests that overexpression of a

combination of genes not only results in the increased consumption of supplied sugars but also in the increased production of more oil, a useful biofuel precursor.

EXAMPLE 4

We next measured the growth advantage, total lipid production, conversion efficiency of carbohydrate substrate to lipid and substrate tolerance between the engineered and the wild type strain in a 2 liter fermentor vessel.

The total amount of lipid was measured using GC-MS (Figure 7). A 10 fold higher production of lipid (80g/l) was observed in the engineered strain as compared to the wild type strain, representing a 20 fold increase over the *Yarrowia lipolytica* strain described by others (S. Papanikolaou I. Chevalot, M. Komaitis, I. Marc G. Aggelis, *Single cell oil production by Yarrowia lipolytica growing on an industrial derivative of animal fat in batch cultures* Appl Microbiol Biotechnol. 2002 Mar;58(3):308-12.). The dominant species of mono-unsaturated fatty acid was oleic acid which increased 8.5 times (g/l) as compared to the control strain (Figure 8). The ratio of total unsaturated to saturated fatty acid was significantly increased, the total unsaturated fatty acids are not increased over saturated ones, however few of them are as in the case of c18.1 (see Figures 7 and 8). The sugar to oil conversion efficiency of the mutant strain was determined to be 0.28g/g, approaching near theoretical values when taking into consideration the sugar utilized for biomass production.

A remarkable and unexpected 32-fold growth advantage was observed between the engineered and wild type strain (Fig. 9). The growth characteristic of the mutant strain remains the same at sugar concentrations that were osmotic-lethal to wild type strain (Fig. 10). The higher sugar tolerance is particularly important for high gravity fermentation commonly employed in industrial biofuel production. Previously, an inverse correlation was observed between higher biomass production and lipid accumulation in *Yarrowia lipolytica* culture (Papanikolaou S, Chevalot I, Komaitis M, Marc I, Aggelis G. *Single cell oil production by Yarrowia lipolytica growing on an industrial derivative of animal fat in batch cultures*. Appl Microbiol Biotechnol. 2002 Mar;58(3):308-12.). Therefore, the link between higher biomass production and excess lipid accumulation in our engineered strain was unexpected. Since fat storage is primarily used for membrane synthesis and budding activities (FEBS J. 2008 Nov;275(22):5552-63), one possibility for the cells in log phase is to re-direct the excess lipid flux towards membrane synthesis via activation of cell division pathway

and/or secretion of lipid to extra-cellular medium. This would compensate for excess lipid production early on followed by intracellular accumulation of lipids upon entry to stationary phase of cell cycle. Indeed, the higher biomass production was coupled to secretion of lipid during early growth phase.

5 Figure 11 shows the growth and lipid production kinetics of mutant and wild type *Y. lipolytica*. Not only does the mutant strain exhibit a strong growth advantage, but it also produces a significantly higher amount of fatty acids as compared to the wild type (control) strain.

 Taken together, these results demonstrate efficient metabolic engineering of
10 oleaginous yeast to exhibit highly desirable multiple phenotypes on glucose as a sole carbon source.

EXAMPLE 5

 The regulatory mechanism of SCD underlying the diverse phenotypic traits of the
15 mutant strain was probed. Given the low sequence identity of *Yarrowia lipolytica* desaturase gene to similar functional genes in the nematode *Caenorhabditis elegans* and mouse, the cloned cross-species SCD for fatty acid specificity in *Yarrowia lipolytica* was tested. The SCD in *C. elegans* and mouse has similar specificity toward stearic acid, showed higher biomass production, similar to mutants over-expressing native *Yarrowia* gene. The confocal
20 imaging confirmed excess oil accumulation during stationary growth phase. These results suggest that desaturase activity towards oleic acid synthesis is linked to over-accumulation of TAG. Since SCD in baker's yeast is known to be regulated at the transcriptional and post-transcriptional level (see Tabor DE, Kim JB, Spiegelman BM, Edwards PA, *Identification of conserved cis-elements and transcription factors required for sterol-regulated transcription of stearoyl-CoA desaturase*. J Biol Chem. 1999 Jul 16;274(29):20603-10; Shimano H, *Sterol regulatory element-binding protein family as global regulators of lipid synthetic genes in energy metabolism*. Vitam Horm. 2002;65:167-94), the feedback inhibition of oleic acid on the desaturase gene was investigated as a possible regulatory niche. We stably integrated a
25 single copy of a native desaturase gene with a 1kb upstream sequence including the promoter
30 region. The mutant strain accumulated excessive oil and had growth advantage and sugar tolerance as with the earlier mutant. This shows that, unlike in baker's yeast, the oil accumulation is not modulated with promoter sequences driving desaturase expression. This

means the negative regulation of desaturase gene in *Yarrowia* is transcriptional independent and possibly occurs at the metabolite level. This data provide the first mechanistic insight of oil regulation via over-riding the inhibitory effects of oleic acid in the oleaginous yeast.

5 EXAMPLE 6

Engineered microbes provided herein can be grown on various substrates. Figure 13 shows robust growth of a mutant *Y. lipolytica* strain on algal biomass as the carbohydrate source. Figure 14 shows oil accumulation in engineered microbial cells grown on algal biomass. Figure 15 shows oil accumulation in engineered cells grown on crude glycerol.

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EXAMPLE 7

Delta-12 desaturase is responsible for converting oleic acid containing lipids to higher chain lipids. For the purpose of producing biofuels, C18 chain fatty acids such as stearic and oleic acids are preferred in view of the cold flow properties of diesel fuel. It is therefore desirable, in some embodiments, to block or inhibit the conversion of C18 fatty acids to longer chain fatty acids.

15

This can be achieved by inhibiting or blocking the expression of the wild type delta-12 desaturase gene in the host microbe, for example, a microbe overexpressing a $\Delta 9$ desaturase (SCD). To this end, a nucleic acid construct was generated to knock out wild type delta-12 desaturase in *Yarrowia lipolytica*. A schematic structure of the knockout construct is shown in Figure 16. The vector comprises genomic sequences of the delta-12 desaturase gene flanking a phleomycin (e.g., ZeocinTM) resistance gene. The sequence of the construct is shown below.

20

25 delta-12 desaturase Knockout vector sequence:

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CCAACAGACCGACCATAGAAATGGATTTCGACCACGCAGACCAACACCGGCACCGGCAAGGTGGCCGTGCAGCCCCACGGCC
TTCATTAAGCCCATTTGAGAAGGTGTCCGAGCCGTCTACGACACCTTTGGCAACGAGTTCACTCCTCCAGACTACTCTATCAA
GGATATTCTGGATGCCATTCCCCAGGAGTGCTACAAGCGGTCTACGTAAAGTCTACTCGTACGTGGCCCGAGACTGCTTCT
TTATCGCCGTTTTTGCCTACATGGCCTACGCGTACCTGCCTCTTATTCCCTCGGCTTCCGGCCGAGCTGTGGCCTGGGCCATG
30 TACTCCATTGTCCAGGGTCTGTTTGGCACCAGGTCTGTGGGTCTTGCCCACGAGTGTGGCCACTCTGCTTTCTCCGACTCTAA
CACCGAGAGACCGGGTTGGCGGCGCATTGTGTGCCAAAAACAGCCCCAATTGCCCAATTGACCCCAAATTGACCCAGTAG
CGGGCCCAACCCCGCGAGAGCCCCCTTACCCCCACATATCAAACCTCCCCCGGTTCACACTTGCCGTTAAGGGCGTAGGG
TACTGCAGTCTGGAATCTACGCTTGTTCAGACTTTGTACTAGTTTCTTTGTCTGGCCATCCGGGTAACCCATGCCGGACGCAA
AATAGACTACTGAAAATTTTTTGTCTTTGTGGTTGGGACTTTAGCCAAGGGTATAAAAGACCACCGTCCCCGAATTACCTTTC
35 CTCTTCTTTTCTCTCTCTCTCTTGTCAACTCACACCCGAAATCGTTAAGCATTTCCTTCTGAGTATAAGAATCATTCAAATGG
CCAAGTTGACCAGTGCCGTTCCGGTGCTCACCGCGCGACGTCGCCGAGCGGTGCGAGTTCTGGACCGACCGGCTCGGGTTC

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TCCCGGGACTTCGTGGAGGACGACTTCGCCGGTGTGGTCCGGGACGACGTGACCCTGTTTCATCAGCGCGGTCCAGGACCAGGT
 GGTGCCGGACAACACCCTGGCCTGGGTGTGGGTGCGCGGCCGTCGACGAGCTGTACGCCGAGTGGTCGGAGGTCTGTGTCCACGA
 ACTTCCGGGACGCCTCCGGGCCGGCCATGACCGAGATCGGCGAGCAGCCGTGGGGGCGGGAGTTGCCCTGCGGACCCGGCC
 GGCAACTGCGTGCACTTCGTGGCCGAGGAGCAGGACTGATCCATGGCCTGTCCCCACGTTGCCGGTCTTGCCCTCTACTACCT
 5 GTCCATCAATGACGAGGTTCTCACCCCTGCCCAGGTCGAGGCTCTTATTACTGAGTCCAACACCGGTGTTCTTCCCACCACCA
 ACCTCAAGGGCTCTCCCAACGCTGTTGCCTACAACGGTGTGGCATTAGGCAATTAACAGATAGTTTGCCGGTGATAATTCT
 CTTAACCTCCACACTCCTTTGACATAACGATTTATGTAAACGAACTGAAATTTGACCAGATATTGTTGTAAATAGAAAATCT
 GGCTTGTAGGTGGCAAAATGCGGCGTCTTTGTTTCATCAATTCCCTCTGTGACTACTCGTCATCCCTTTATGTTGACTGTCTGT
 ATTTCTTATTTTCCATACATATGCAAGTGAGATGCCCGTGTCTGGCCATCACCTACCTGCAGCACACCGACCCCACTCTGCC
 10 CCACTACCACGCCGACCAGTGGAACCTCACCCGAGGAGCCGCCACCATCGACCGAGAGTTTGGCTTCATCGGCTCCTTCT
 GCTTCCATGACATCATCGAGACCCACGTTCTGCACCACTACGTGTCTCGAATTCCCTTCTACAACGCCCGAATCGCCACTGAG
 AAGATCAAGAAGGTCATGGGCAAGCACTACCGACACGACGACACCAACTTCATCAAGTCTCTTTACACTGTCGCCCGAACCTG
 CCAGTTTGTGTAAGGTAAGGAAGGCATTGAGATGTTTAGAAACGTCAATGGAGTCGGAGTTGCTCCTGACGGCTGCCTTCTA
 AAAAGTAGAGCTAGAAATGTTATTTGATTGTGTTTTAACTGAACAGCA (SEQ ID NO: 28)

15 A series of genes including $\Delta 9$ desaturase, Glut1, hemoglobin and cytochrome b5, were overexpressed in delta-12 desaturase knockout cells of *Yarrowia lipolytica* to further increase the sugar flux into the cell and increase oil content. A marked increase in the size of the cells was observed with up to 95% by volume of cells filled with oil.

20 EXAMPLE 8

Yarrowia lipolytica overexpressing SCD was grown in 3% acetic acid solution for 148 hours (Figure 17). Cell cultures were spiked with 2% glycerol at about 84 hours to provide glycerol to drive fatty acid production. The latter is a bottleneck in the production of oil using acetate as feedstock. A marked increase in oil production was observed by confocal
 25 laser microscopy using a glycerol spike on acetate media showing a new process to efficiently produce oils with better economics.

While several embodiments of the present invention have been described and illustrated herein, those of ordinary skill in the art will readily envision a variety of other
 30 means and/or structures for performing the functions and/or obtaining the results and/or one or more of the advantages described herein, and each of such variations and/or modifications is deemed to be within the scope of the present invention. More generally, those skilled in the art will readily appreciate that all parameters, dimensions, materials, and configurations described herein are meant to be exemplary and that the actual parameters, dimensions,
 35 materials, and/or configurations will depend upon the specific application or applications for which the teachings of the present invention is/are used. Those skilled in the art will

recognize, or be able to ascertain using no more than routine experimentation, many equivalents to the specific embodiments of the invention described herein. It is, therefore, to be understood that the foregoing embodiments are presented by way of example only and that, within the scope of the appended claims and equivalents thereto, the invention may be practiced otherwise than as specifically described and claimed. The present invention is directed to each individual feature, system, article, material, kit, and/or method described herein. In addition, any combination of two or more such features, systems, articles, materials, kits, and/or methods, if such features, systems, articles, materials, kits, and/or methods are not mutually inconsistent, is included within the scope of the present invention.

All definitions, as defined and used herein, should be understood to control over dictionary definitions, definitions in documents incorporated by reference, and/or ordinary meanings of the defined terms.

The indefinite articles “a” and “an”, as used herein in the specification and in the claims, unless clearly indicated to the contrary, should be understood to mean “at least one.”

The phrase “and/or,” as used herein in the specification and in the claims, should be understood to mean “either or both” of the elements so conjoined, i.e., elements that are conjunctively present in some cases and disjunctively present in other cases. Other elements may optionally be present other than the elements specifically identified by the “and/or” clause, whether related or unrelated to those elements specifically identified unless clearly indicated to the contrary. Thus, as a non-limiting example, a reference to “A and/or B”, when used in conjunction with open-ended language such as “comprising” can refer, in one embodiment, to A without B (optionally including elements other than B); in another embodiment, to B without A (optionally including elements other than A); in yet another embodiment, to both A and B (optionally including other elements); etc.

As used herein in the specification and in the claims, “or” should be understood to have the same meaning as “and/or” as defined above. For example, when separating items in a list, “or” or “and/or” shall be interpreted as being inclusive, i.e., the inclusion of at least one, but also including more than one, of a number or list of elements, and, optionally, additional unlisted items. Only terms clearly indicated to the contrary, such as “only one of” or “exactly one of,” or, when used in the claims, “consisting of,” will refer to the inclusion of exactly one element of a number or list of elements. In general, the term “or” as used herein shall only be interpreted as indicating exclusive alternatives (i.e. “one or the other but not

both”) when preceded by terms of exclusivity, such as “either,” “one of,” “only one of,” or “exactly one of.” “Consisting essentially of”, when used in the claims, shall have its ordinary meaning as used in the field of patent law.

As used herein in the specification and in the claims, the phrase “at least one,” in reference to a list of one or more elements, should be understood to mean at least one element selected from any one or more of the elements in the list of elements, but not necessarily including at least one of each and every element specifically listed within the list of elements and not excluding any combinations of elements in the list of elements. This definition also allows that elements may optionally be present other than the elements specifically identified within the list of elements to which the phrase “at least one” refers, whether related or unrelated to those elements specifically identified. Thus, as a non-limiting example, “at least one of A and B” (or, equivalently, “at least one of A or B,” or, equivalently, “at least one of A and/or B”) can refer, in one embodiment, to at least one, optionally including more than one, A, with no B present (and optionally including elements other than B); in another embodiment, to at least one, optionally including more than one, B, with no A present (and optionally including elements other than A); in yet another embodiment, to at least one, optionally including more than one, A, and at least one, optionally including more than one, B (and optionally including other elements); etc.

It should also be understood that, unless clearly indicated to the contrary, in any methods claimed herein that include more than one act, the order of the acts of the method is not necessarily limited to the order in which the acts of the method are recited.

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All publications, patents and sequence database entries mentioned herein, including those items listed above, are hereby incorporated by reference in their entirety as if each individual publication or patent was specifically and individually indicated to be incorporated by reference. In case of conflict, the present application, including any definitions herein, will control.

CLAIMS

1. An isolated oleaginous cell, comprising
a genetic modification that increases expression of one or more genes selected from
the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC, SCD,
FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA synthetase,
Pyruvate carboxylase, and AMPK genes, and/or
a genetic modification that reduces expression of JNK2 and/or delta-12 desaturase.
2. The isolated oleaginous cell of claim 1, wherein the genetic modification comprises a
nucleic acid construct that increases or decreases the expression of the gene product, the
nucleic acid construct comprising
 - (a) an expression cassette comprising a nucleic acid encoding the gene product
under the control of a suitable homologous or heterologous promoter,
 - (b) an expression cassette comprising a nucleic acid encoding an interfering RNA
targeting the gene product under the control of a heterologous promoter,
and/or
 - (c) a nucleic acid sequence that modulates the level of expression of the gene
product when inserted into the genome of the cell.
3. The isolated oleaginous cell of claim 2, wherein the heterologous promoter is an
inducible or a constitutive promoter.
4. The isolated oleaginous cell of claim 2, wherein the nucleic acid construct inhibits or
disrupts the natural regulation of a native gene encoding the gene product resulting in
overexpression of the native gene.
5. The isolated oleaginous cell of claim 2, wherein the nucleic acid construct inhibits or
abolishes expression of the native gene.
6. The isolated oleaginous cell of claim 4 or 5,
wherein inhibition or disruption of the natural regulation of the native gene is

mediated by deletion, disruption, mutation and/or substitution of a regulatory region, or a part of a regulatory region regulating expression of the gene, or

wherein inhibition or abolition of the expression of a native gene is mediated by deletion, disruption, mutation and/or substitution of a coding sequence of the native gene, or of a regulatory region, or a part of a regulatory region regulating expression of the native gene.

7. The isolated oleaginous cell of any of claims 1-6, wherein the decreased expression of JNK2 and/or delta-12 desaturase is mediated by constitutive or inducible expression of a nucleic acid targeting a JNK2 and/or a delta-12 desaturase gene product and inhibiting the expression of the gene.

8. The isolated oleaginous cell of claim 7, wherein the gene product is a transcript and the nucleic acid targeting the JNK2 and/or the delta-12 desaturase transcript inhibits expression of the transcript via an RNAi pathway.

9. The isolated oleaginous cell of claim 8, wherein the nucleic acid targeting the JNK2 and/or the delta-12 desaturase transcript is an siRNA, an shRNA, or a microRNA.

10. The isolated oleaginous cell of claims 3-9, wherein the nucleic acid construct is inserted into the genome of the cell.

11. The isolated oleaginous cell of any of claims 1-10, wherein the increased or decreased expression of the gene product confers a beneficial phenotype for the conversion of a carbohydrate source to a fatty acid, fatty acid derivative and/or triacylglycerol (TAG) to the cell.

12. The isolated oleaginous cell of claim 11, wherein the beneficial phenotype is a modified fatty acid profile, a modified TAG profile, an increased fatty acid and/or triacylglycerol synthesis rate, an increase conversion yield, an increased triacylglycerol accumulation in the cell, and an increased tolerance of osmotic stress, an increased proliferation rate, an increased cell volume, and/or an increased tolerance of a substance at a

concentration lethal to and/or inhibiting proliferation of unmodified cells of the same cell type, by the cell.

13. The isolated oleaginous cell of claim 12, wherein the modified fatty acid profile or the modified TAG profile of the cell exhibits at least a 2-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type.

14. The isolated oleaginous cell of claim 12, wherein the modified fatty acid profile or the modified TAG profile of the cell exhibits at least an 2.5-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type.

15. The isolated oleaginous cell of claim 12, wherein the modified fatty acid profile or the modified TAG profile of the cell exhibits at least a 5-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type.

16. The isolated oleaginous cell of claim 12, wherein the modified fatty acid profile or the modified TAG profile of the cell exhibits at least a 6.5-fold increase of the ratio of C18 fatty acids over C16 fatty acids as compared to unmodified cells of the same cell type.

17. The isolated oleaginous cell of any of claims 12-16, wherein the cell is viable under conditions of osmotic stress lethal to unmodified cells.

18. The isolated oleaginous cell of any of claims 12-16, wherein the cell is viable under conditions of osmotic stress at a level of 200% of the highest level tolerated by unmodified cells.

19. The isolated oleaginous cell of any of claims 12-16, wherein the cell is viable under conditions of osmotic stress at a level of 300% of the highest level tolerated by unmodified cells.

20. The isolated oleaginous cell of any of claims 12-16, wherein the cell is viable under conditions of osmotic stress at a level of 400% of the highest level tolerated by unmodified cells.

5 21. The isolated oleaginous cell of any of claims 12-20, wherein the cell proliferation rate is at least 5-fold increased as compared to unmodified cells of the same cell type.

22. The isolated oleaginous cell of any of claims 12-20, wherein the cell proliferation rate is at least 10-fold increased as compared to unmodified cells of the same cell type.

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23. The isolated oleaginous cell of any of claims 12-20, wherein the cell proliferation rate is at least 20-fold increased as compared to unmodified cells of the same cell type.

15 24. The isolated oleaginous cell of any of claims 12-20, wherein the cell proliferation rate is at least 25-fold increased as compared to unmodified cells of the same cell type.

25. The isolated oleaginous cell of any of claims 12-20, wherein the cell proliferation rate is at least 30-fold increased as compared to unmodified cells of the same cell type.

20 26. The isolated oleaginous cell of any of claims 12-25, wherein the volume of the cell is at least 2-fold increased as compared to unmodified cells of the same cell type.

25 27. The isolated oleaginous cell of any of claims 12-26 wherein the cell tolerates a substance at a concentration lethal to and/or inhibiting proliferation of unmodified cells of the same cell type.

28. The isolated oleaginous cell of claim 27, wherein the substance is a fermentable sugar and the concentration is at least 80g/l.

30 29. The isolated oleaginous cell of claim 27, wherein the substance is a fermentable sugar and the concentration is at least 100g/l.

30. The isolated oleaginous cell of claim 27, wherein the substance is a fermentable sugar and the concentration is at least 150g/l.

31. The isolated oleaginous cell of claim 27, wherein the substance is a fermentable sugar and the concentration is at least 200g/l.

32. The isolated oleaginous cell of claim 27, wherein the substance is a fermentable sugar and the concentration is at least 300g/l.

33. The isolated oleaginous cell of any of claims 12-32, wherein the synthesis rate of a fatty acid or a TAG of the cell is at least 5-fold increased as compared to unmodified cells of the same cell type.

34. The isolated oleaginous cell of any of claims 12-33, wherein the synthesis rate of a fatty acid or a TAG of the cell is at least 10-fold increased as compared to unmodified cells of the same cell type.

35. The isolated oleaginous cell of any of claims 12-34, wherein the cell converts a carbohydrate source to a fatty acid or a TAG at a conversion rate within the range of about 0.025g/g to about 0.3g/g (g TAG produced/ g Glucose consumed).

36. The isolated oleaginous cell of any of claims 12-34, wherein the cell converts a carbohydrate source to a fatty acid or a TAG at a conversion rate of at least about 0.2g/g.

37. The isolated oleaginous cell of any of claims 12-34, wherein the cell converts a carbohydrate source to a fatty acid or a TAG at a conversion rate of at least about 0.3g/g.

38. The isolated oleaginous cell of any of claims 1-37, wherein the cell is a prokaryotic cell or a eukaryotic cell.

39. The isolated oleaginous cell of any of claims 1-38, wherein the cell is a bacterial cell, an algal cell, a fungal cell, or a yeast cell.

40. The isolated oleaginous cell of any of claims 1-39, wherein said cell is an oleaginous yeast cell.
- 5 41. The isolated oleaginous cell of any of claims 1-40, wherein said cell is a *Y. lipolytica* cell.
42. A culture, comprising the oleaginous cell of any of claims 1-41 or 138.
- 10 43. A culture, comprising
an isolated oleaginous cell, comprising
a genetic modification that increases expression of one or more genes selected
from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC,
SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA
15 synthetase, Pyruvate carboxylase, and AMPK genes, and/or
a genetic modification that reduces expression of a JNK2 and/or a delta-12
desaturase gene product; and
a carbohydrate source.
- 20 44. The culture of claim 42 or 43, wherein the carbohydrate source is a fermentable sugar.
45. The culture of any of claims 42-44, wherein the carbohydrate source is a monomeric sugar.
- 25 46. The culture of any of claims 42-45, wherein the carbohydrate source is glucose and/or glycerol
47. The culture of any of claims 42-46, wherein the carbohydrate source is not sterilized.
- 30 48. The culture of any of claims 42-47, wherein the culture is maintained under non-sterile conditions.

49. The culture of any of claims 42-48, wherein the culture does not comprise an antibiotic or antiproliferative agent selective for the isolated oleaginous cell.

50. The culture of any of claims 42-49, wherein the carbohydrate source is derived from plant or algal biomass.

51. The culture of any of claims 42-50, wherein the carbohydrate source is derived from cellulose, hemi-cellulose, starch, glycerol, or a derivative thereof.

52. The culture of claim 50 or 51, further comprising a cellulose-hydrolyzing enzyme or hemi-cellulose-hydrolyzing enzyme.

53. The culture of any of claims 50-52, wherein the biomass or the cellulose or hemi-cellulose is pretreated in a hot water or dilute acid or ammonia fiber expansion procedure, with a hydrolyzing enzyme, with a steam pre-treatment, and/or a lime pre-treatment.

54. The culture of any of claims 42-53, wherein the culture comprises a substance at a concentration lethal to unmodified wild type, unmodified cells of the same cell type as the isolated oleaginous cell.

55. The culture of claim 54, wherein the substance is a toxic substance generated during pretreatment of the carbohydrate source such as acetic acid, furfural or aromatic compounds.

56. The culture of claim 54 or 55, wherein the substance is the carbohydrate source.

57. The culture of any of claims 54-56, wherein the substance is a fermentable sugar.

58. The culture of any of claims 54-57, wherein the substance is a monomeric sugar.

59. The culture of any of claims 44-58, wherein the culture comprises the fermentable sugar at a concentration of at least 80g/l.

60. The culture of any of claims 44-59, wherein the culture comprises the fermentable sugar at a concentration of at least 100g/l.

61. The culture of any of claims 44-60, wherein the culture comprises the fermentable sugar at a concentration of at least 150g/l.

62. The culture of any of claims 44-61, wherein the culture comprises the fermentable sugar at a concentration of at least 200g/l.

63. The culture of any of claims 44-62, wherein the culture comprises the fermentable sugar at a concentration of at least 250g/l.

64. The culture of any of claims 44-64, wherein the culture comprises the fermentable sugar at a concentration of at least 300g/l.

65. A method, comprising
contacting a carbohydrate source with an isolated oleaginous cell, the cell comprising
a genetic modification that increases expression of one or more genes selected
from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC,
SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA
synthetase, Pyruvate carboxylase, and AMPK gene products, and/or
a genetic modification that reduces expression of a JNK2 and/or a delta-12
desaturase gene; and
incubating the carbohydrate source contacted with the cell under conditions suitable
for at least partial conversion of the carbohydrate source into a fatty acid or a triacylglycerol
by the cell.

66. The method of claim 65, wherein the isolated oleaginous cell is the isolated oleaginous cell of any of claims 1-41.

67. The method of claim 65 or 66, wherein the carbohydrate source is a fermentable sugar such as glucose or xylose or a carbohydrate starch derived from plant or algal biomass.

68. The method of any of claims 65-67, wherein the carbohydrate source is derived from cellulose or hemi-cellulose.

5 69. The method of any of claims 65-68, wherein the carbohydrate source is contacted with the cell in the presence of a cellulose-hydrolyzing enzyme or hemi-cellulose-hydrolyzing enzyme.

10 70. The method of any of claims 65-69, wherein the carbohydrate source is contacted with the cell in the presence of about 15 IU of cellulose-hydrolyzing enzyme or hemi-cellulose-hydrolyzing enzyme per g of biomass at 55°C for 48 hours.

15 71. The method of any of claims 67-70, wherein the biomass or the cellulose or hemi-cellulose is pretreated with hot water or dilute acid or ammonia fiber expansion procedure and/or a hydrolyzing enzyme.

20 72. The method of any of claims 65-71, wherein the carbohydrate source contacted with the isolated oleaginous cell comprises a substance at a concentration lethal to unmodified cells of the same cell type as the isolated oleaginous cell.

73. The method of claim 72, wherein the substance is a toxic substance generated during pretreatment of the carbohydrate source such as acetic acid, furfural or aromatic compounds.

25 74. The method of claim 72, wherein the substance is the carbohydrate source.

75. The method of claim 74, wherein the carbohydrate source is a fermentable sugar and the concentration of the fermentable sugar is at least 80g/l after contacting with the oleaginous cell.

30 76. The method of claim 74, wherein the carbohydrate source is a fermentable sugar and the concentration of the fermentable sugar is at least 80g/l after contacting with the oleaginous cell.

77. The method of claim 74, wherein the carbohydrate source is a fermentable sugar and the concentration of the fermentable sugar is at least 100g/l after contacting with the oleaginous cell.

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78. The method of claim 74, wherein the carbohydrate source is a fermentable sugar and the concentration of the fermentable sugar is at least 200g/l after contacting with the oleaginous cell.

10 79. The method of claim 74, wherein the carbohydrate source is a fermentable sugar and the concentration of the fermentable sugar is at least 300g/l after contacting with the oleaginous cell.

15 80. The method of any of claims 65-79, wherein the carbohydrate source is contacted with the isolated oleaginous cell under non-sterile conditions.

81. The method of any of claims 65-80, wherein the carbohydrate source contacted with the isolated oleaginous cell is incubated under non-sterile conditions.

20 82. The method of any of claims 65-81, wherein the carbohydrate source contacted with the isolated oleaginous cell is incubated in an open reactor.

25 83. The method of any of claims 65-82, wherein the carbohydrate source is contacted with the isolated oleaginous cell and incubated for conversion of the carbohydrate source to a fatty acid or a triacylglycerol in a fed batch process.

84. The method of any of claims 65-82, wherein the carbohydrate source is contacted with the isolated oleaginous cell and incubated for conversion of the carbohydrate source to a fatty acid or a triacylglycerol in a continuous process.

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85. The method of any of claims 65-84, wherein the fatty acid or the triacylglycerol is extracted from the carbohydrate source contacted with the isolated oleaginous cell by solvent extraction.

5 86. The method of claim 85, wherein the solvent extraction is a hexane extraction.

87. The method of any of claims 65-86, wherein the fatty acid or the triacylglycerol is separated from the carbohydrate source contacted with the isolated oleaginous cell and subsequently refined by transesterification

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88. A method, comprising

modifying in a cell the fatty acid profile, the triacylglycerol profile, the fatty acid synthesis rate, the triacylglycerol synthesis rate, the extent of fatty acid derivative accumulation, the rate of fatty acid derivative secretion, the rate of carbohydrate to fatty acid or fatty acid derivative conversion, the efficient yield of carbohydrate to fatty acid or fatty acid derivative conversion, the tolerance of osmotic stress, the proliferation rate, the cell volume, or the tolerance of a toxic substance of a cell for use in the conversion of a carbohydrate source into a fatty acid or triacylglycerol by

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increasing in the cell the expression of one or more gene product(s) selected from the group of Hemoglobin, Cytochrome, GLUT, Malic Enzyme, ACC, SCD, FAA1, ACS, ACS2, FAT1, FAT2, PCS60, ACLY, FAS, Acyl-CoA synthetase, Pyruvate carboxylase, and AMPK gene products, and/or decreasing in the cell expression of a JNK2 and/or a delta-12 desaturase gene.

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25 89. The method of claim 88, wherein modifying the fatty acid profile, the triacylglycerol profile, the fatty acid synthesis rate, the triacylglycerol synthesis rate, the extent of fatty acid derivative accumulation in the cell, or the rate of fatty acid derivative secretion of the cell is increasing the amount of a fatty acid, a fatty acid derivative, and/or a triacylglycerol is synthesized, accumulated, or secreted by the cell.

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90. The method of claim 88 or 89, wherein modifying the efficiency of carbohydrate to fatty acid or fatty acid derivative conversion of the cell is increasing the efficiency of conversion by at least 2-fold.

5 91. The method of claim 88 or 89, wherein modifying the efficiency of carbohydrate to fatty acid or fatty acid derivative conversion of the cell is increasing the efficiency of conversion by at least 3-fold.

10 92. The method of claim 88 or 89, wherein modifying the efficiency of carbohydrate to fatty acid or fatty acid derivative conversion of the cell is increasing the efficiency of conversion by at least 4-fold.

15 93. The method of claim 88 or 89, wherein modifying the efficiency of carbohydrate to fatty acid or fatty acid derivative conversion of the cell is increasing the efficiency of conversion by at least 5-fold.

94. The method of any of claims 88-93, wherein the fatty acid derivative is a triacylglycerol.

20 95. The method of any of claims 88-94, wherein modifying the tolerance of osmotic stress, or the tolerance of a toxic substance of the cell is conferring tolerance of osmotic stress or of a toxic substance at a level lethal to unmodified cells of the same cell type.

25 96. The method of any of claims 88-95, wherein modifying the proliferation rate is increasing the proliferation rate at least 2-fold.

97. The method of any of claims 88-95, wherein modifying the proliferation rate is increasing the proliferation rate at least 5-fold.

30 98. The method of any of claims 88-95, wherein modifying the proliferation rate is increasing the proliferation rate at least 10-fold.

99. The method of any of claims 88-95, wherein modifying the proliferation rate is increasing the proliferation rate at least 20-fold.

100. The method of any of claims 88-95, wherein modifying the proliferation rate is increasing the proliferation rate at least 30-fold.

101. The method of any of claims 88-100, wherein modifying the cell volume is increasing the cell volume at least 2-fold.

102. The method of any of claims 88-101, wherein the cell is a yeast cell.

103. The method of claim 102, wherein the yeast is an oleaginous yeast.

104. The method of claim 103, wherein the oleaginous yeast is *Y. lipolytica*.

105. An isolated nucleic acid molecule comprising:
a) a nucleotide sequence that encodes SEQ ID NO:1 (*Y. lipolytica* SCD), or
b) a nucleotide sequence that is at least 85% identical to the nucleotide sequence of a).

106. The isolated nucleic acid molecule of claim 105, wherein the nucleotide sequence that encodes SEQ ID NO:1 is SEQ ID NO:2.

107. The isolated nucleic acid molecule of claim 105, wherein the nucleotide sequence is at least 85% identical to the nucleotide sequence of SEQ ID NO:2.

108. The isolated nucleic acid molecule of claim 107, wherein the nucleotide sequence is at least 90% identical to the nucleotide sequence of SEQ ID NO:2.

109. The isolated nucleic acid molecule of claim 108, wherein the nucleotide sequence is at least 95% identical to the nucleotide sequence of SEQ ID NO:2.

110. The isolated nucleic acid molecule of claim 108, wherein the nucleotide sequence is at least 97.5% identical to the nucleotide sequence of SEQ ID NO:2.

111. The isolated nucleic acid molecule of claim 108, wherein the nucleotide sequence is at least 99% identical to the nucleotide sequence of SEQ ID NO:2.

112. An expression cassette, comprising the isolated nucleic acid molecule of any of claims 105-111 and a heterologous isolated promoter.

113. The expression cassette of claim 112, wherein the promoter is a constitutive promoter or an inducible promoter.

114. The expression cassette of claim 113, wherein the constitutive promoter is a Translation Elongation Factor (TEF) promoter.

115. The expression cassette of claim 113, wherein the inducible promoter is a drug-inducible promoter.

116. An expression cassette, comprising the isolated nucleic acid molecule of any of claims 105-111.

117. The expression cassette of claim 116, further comprising a modified SCD promoter.

118. The expression cassette of claim 117, wherein said modification is a deletion, complete or partial, and/or a mutation of a wild-type SCD promoter sequence resulting in a disruption of the feedback inhibition of said SCD promoter in response to high levels of a fatty acid, a fatty acid derivative, and/or a triacylglycerol.

119. The expression cassette of claim 117, wherein said modification is an insertion of a heterologous sequence into a wild-type SCD promoter region, optionally associated with a deletion, complete or in part, and/or a mutation of a wild-type SCD promoter sequence,

resulting in a disruption of the feedback inhibition of said SCD promoter in response to high levels of a fatty acid, a fatty acid derivative, and/or a triacylglycerol.

120. A vector comprising the expression cassette of any of claims 112-119.

5

121. A cell comprising the expression cassette of any of claims 112-119 or at least a part of the vector of claim 120.

122. The culture of claim 43, wherein the carbohydrate source is acetate.

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123. The culture of claim 122, wherein the acetate is at a concentration of at least 1%.

124. The culture of claim 122, wherein the acetate is at a concentration of at least 2%.

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125. The culture of claim 122, wherein the acetate is at a concentration of at least 3%.

126. The culture of claim 122, wherein the acetate is at a concentration of at least 4%.

127. The culture of claim 122, wherein the acetate is at a concentration of at least 5%.

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128. The culture of any of claims 122-127, wherein the culture further comprises glycerol.

129. The culture of claim 128, wherein the glycerol is at a concentration of 2%.

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130. The method of any of claims 65-74, wherein the carbohydrate source is acetate.

131. The method of claim 131, wherein the acetate is at a concentration of at least 1%.

132. The method of claim 131, wherein the acetate is at a concentration of at least 2%.

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133. The method of claim 131, wherein the acetate is at a concentration of at least 3%.

134. The method of claim 131, wherein the acetate is at a concentration of at least 4%.

135. The method of claim 131, wherein the acetate is at a concentration of at least 5%.

5 136. The method of any of claims 131-135, wherein the method further comprises contacting the cells with glycerol.

137. The method of claim 136, wherein the method comprises contacting the cells with glycerol at a concentration of about 2%.

10

138. The isolated oleaginous cell of any of claims 1-40, wherein the genetic modification that reduces expression of JNK2 and/or delta-12 desaturase is a gene disruption, optionally a complete or partial gene deletion.

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LOG PHASE

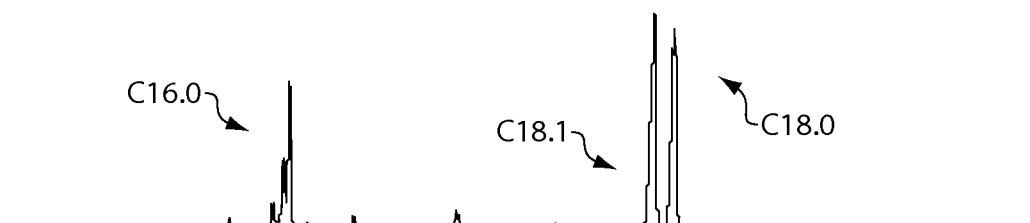


Fig. 1A

STATIONARY PHASE

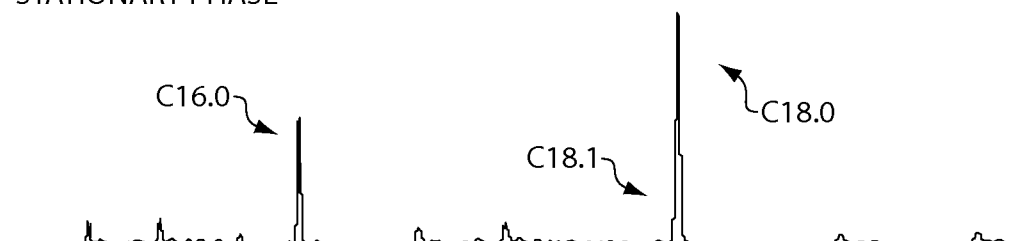


Fig. 1B

STATIONARY PHASE

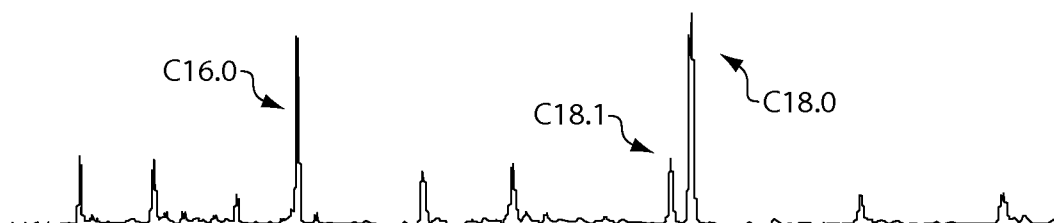


Fig. 1C

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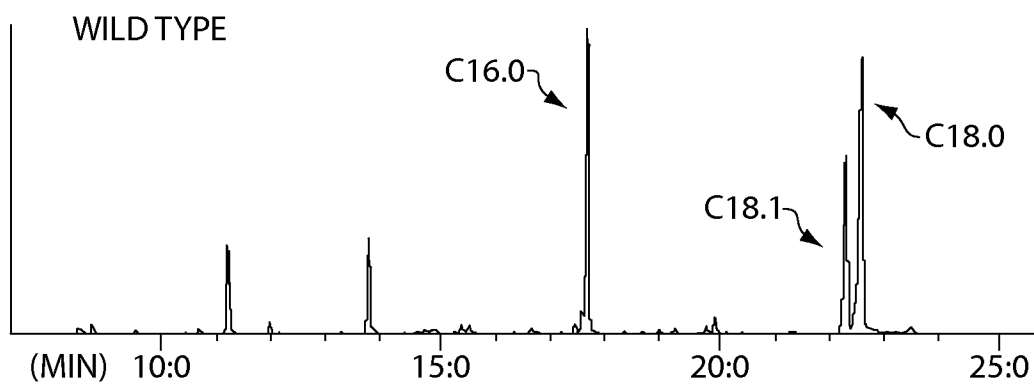


Fig. 2A

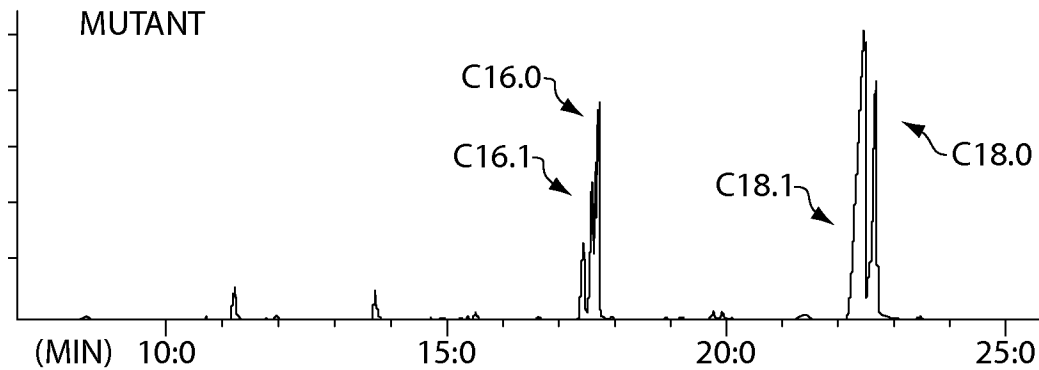


Fig. 2B

3/14

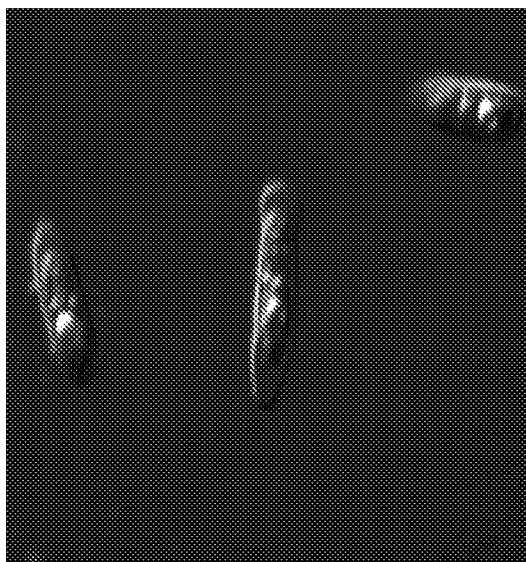


Fig. 2C



Fig. 2D

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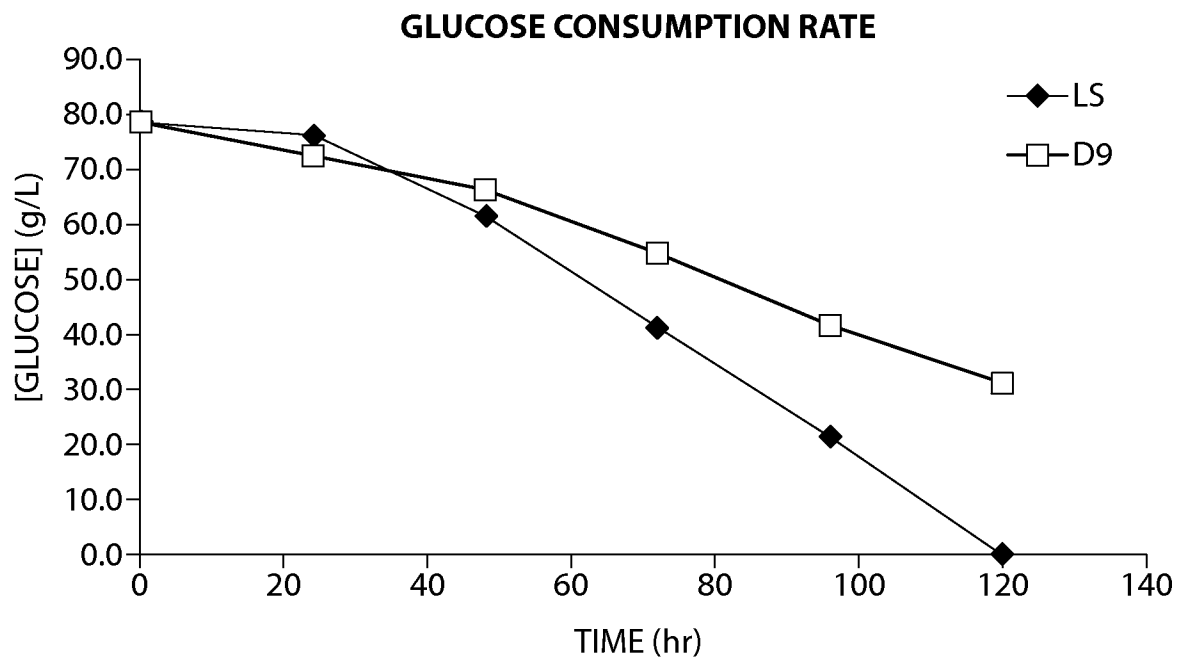


Fig. 3

5/14

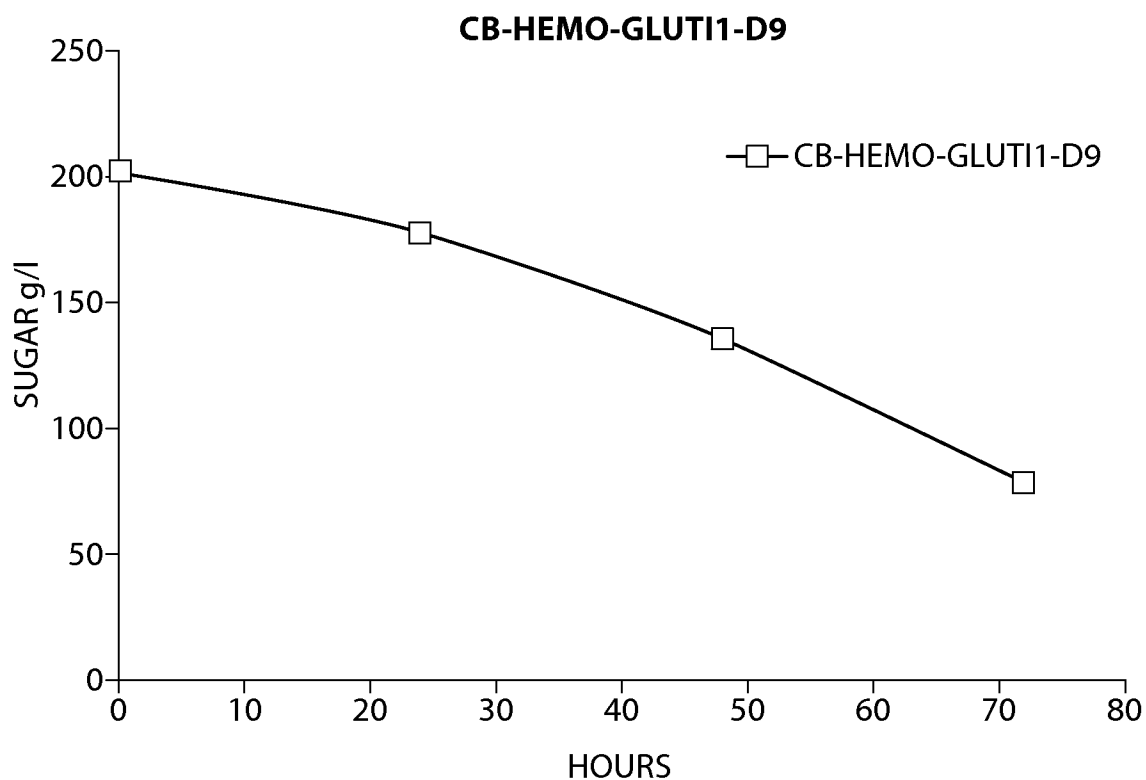


Fig. 4A

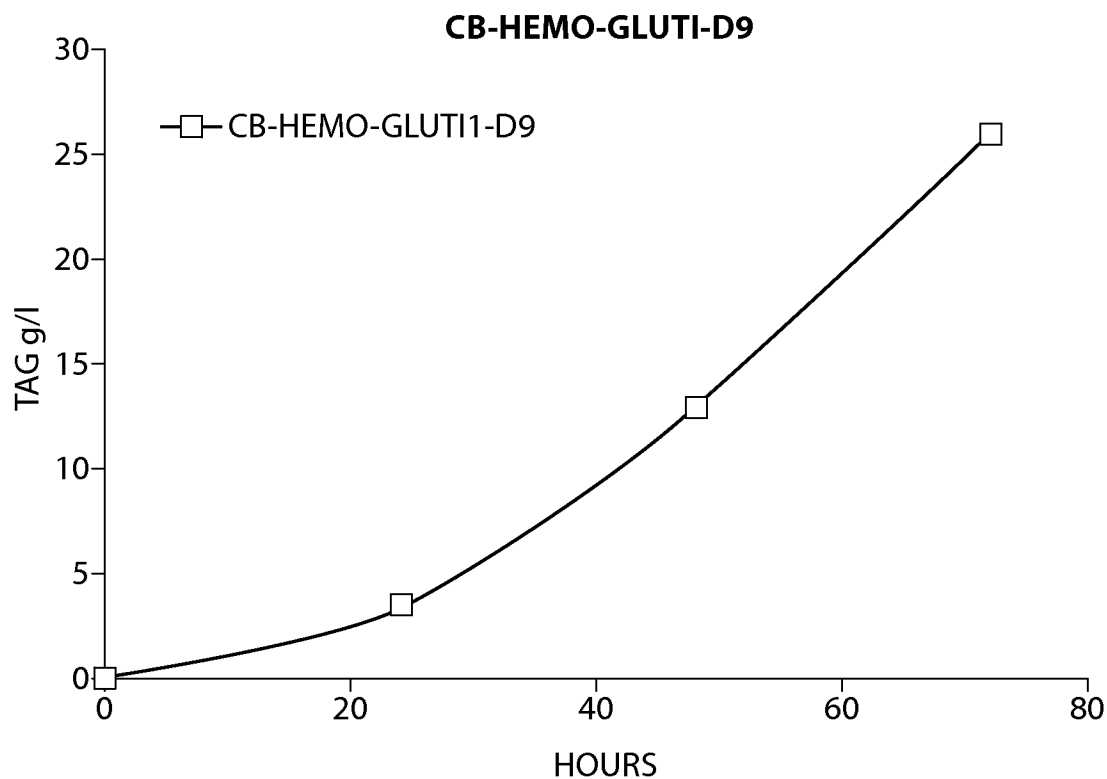


Fig. 4B

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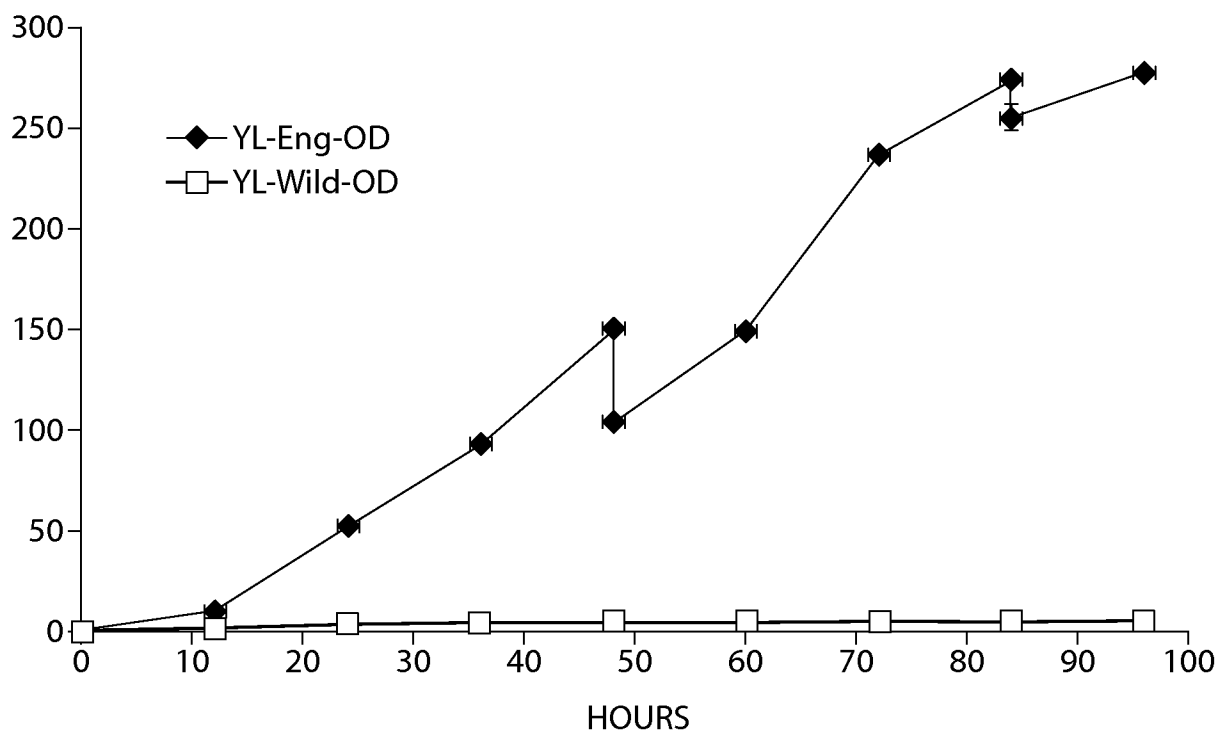


Fig. 5

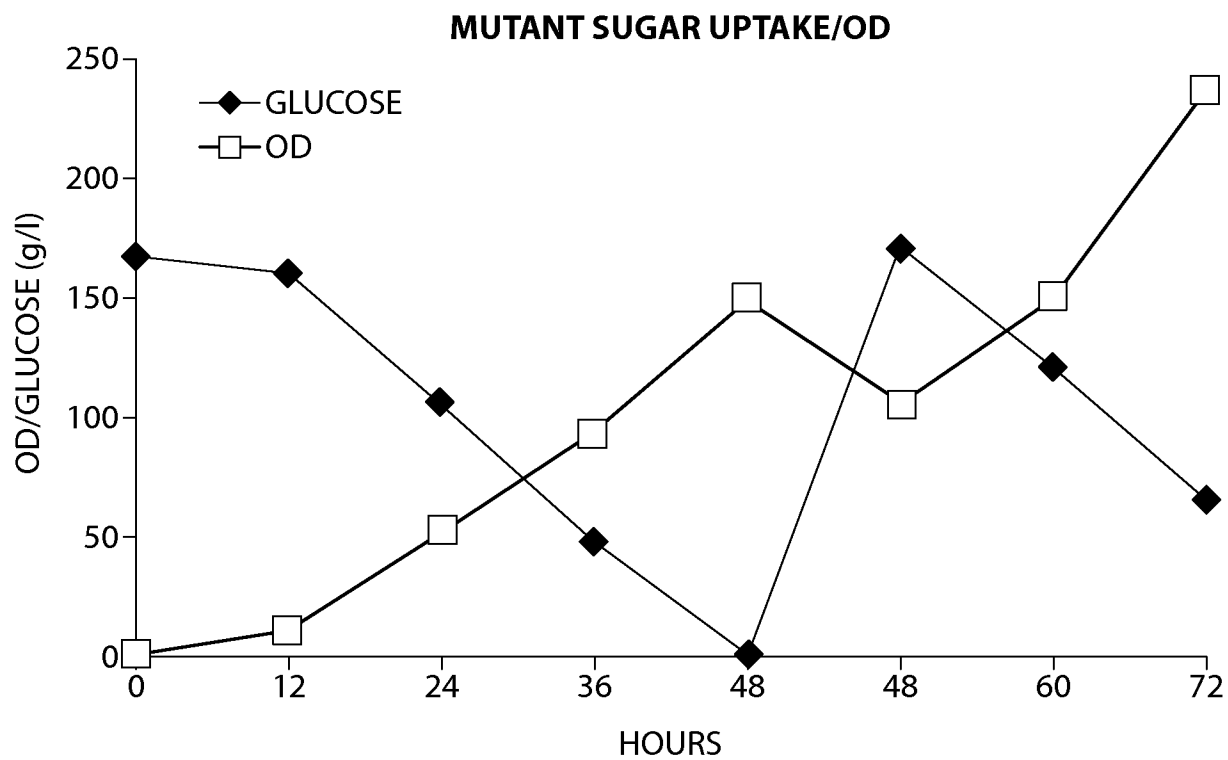


Fig. 6

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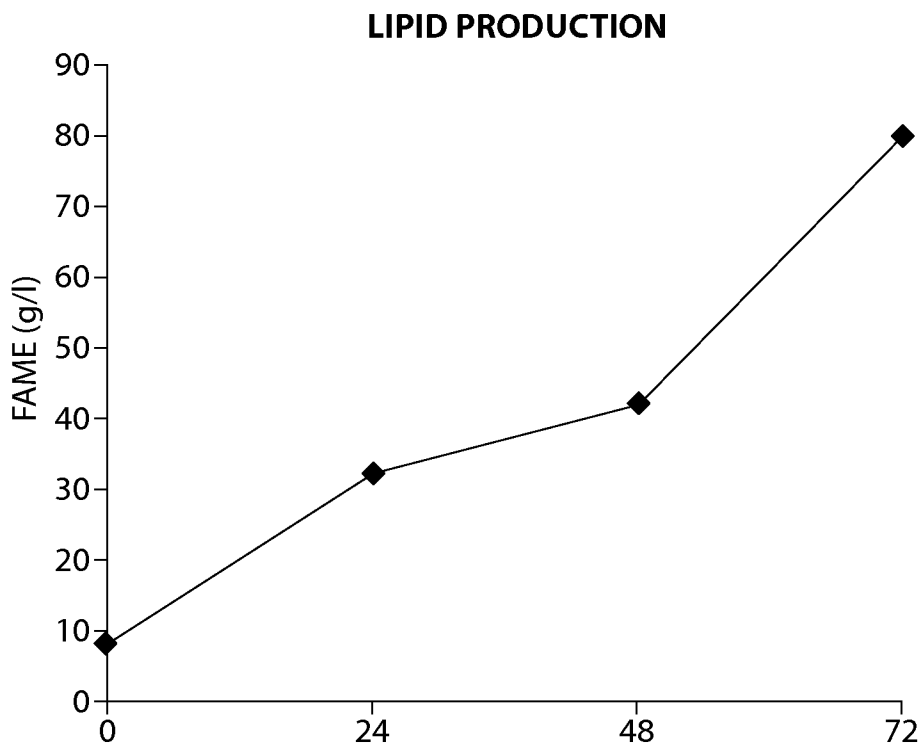


Fig. 7

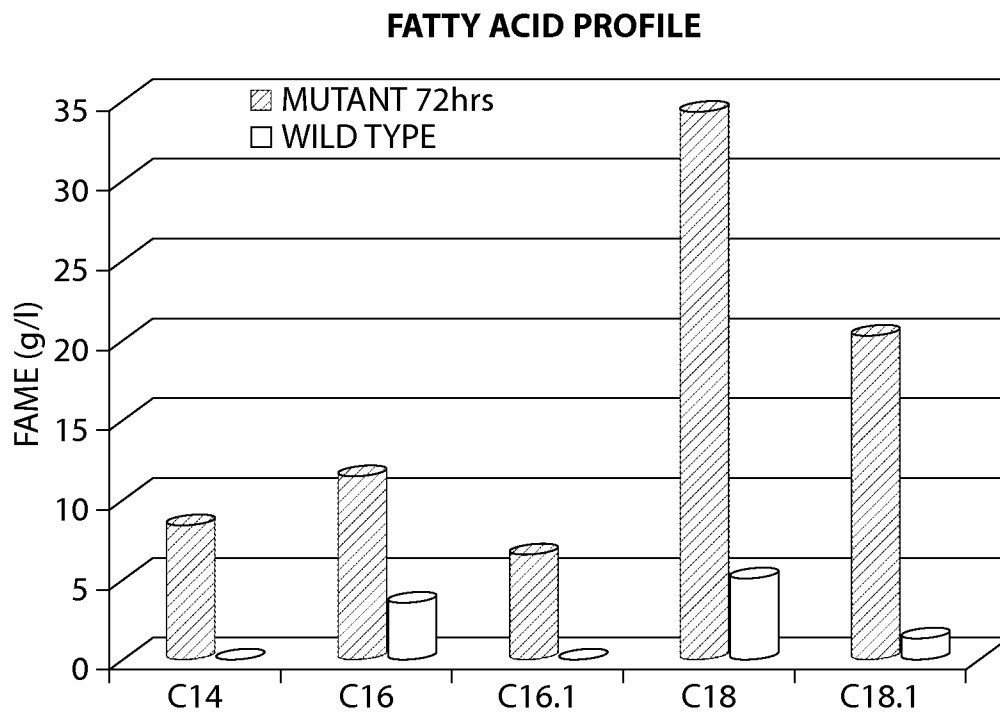


Fig. 8

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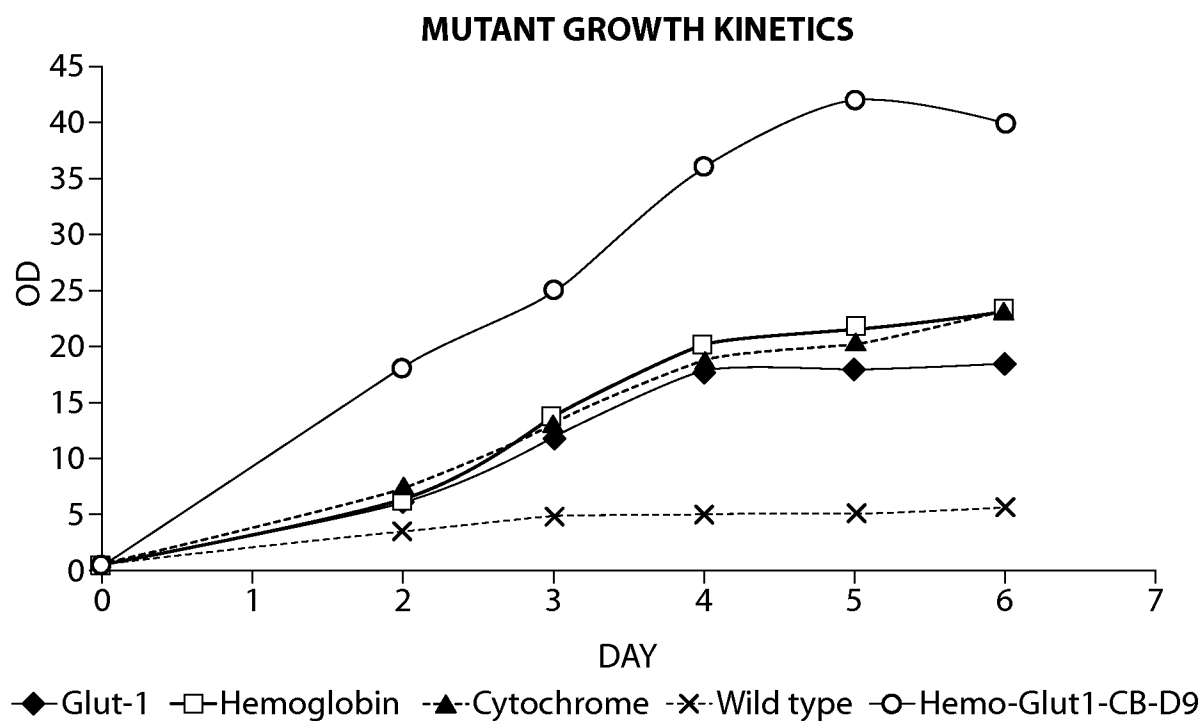


Fig. 9

**EFFECT OF EXTRACELLULAR GLUCOSE CONCENTRATION ON
Y. LIPOLYTICA BIOMASS FORMATION IN SHAKER FLASK CULTURES**

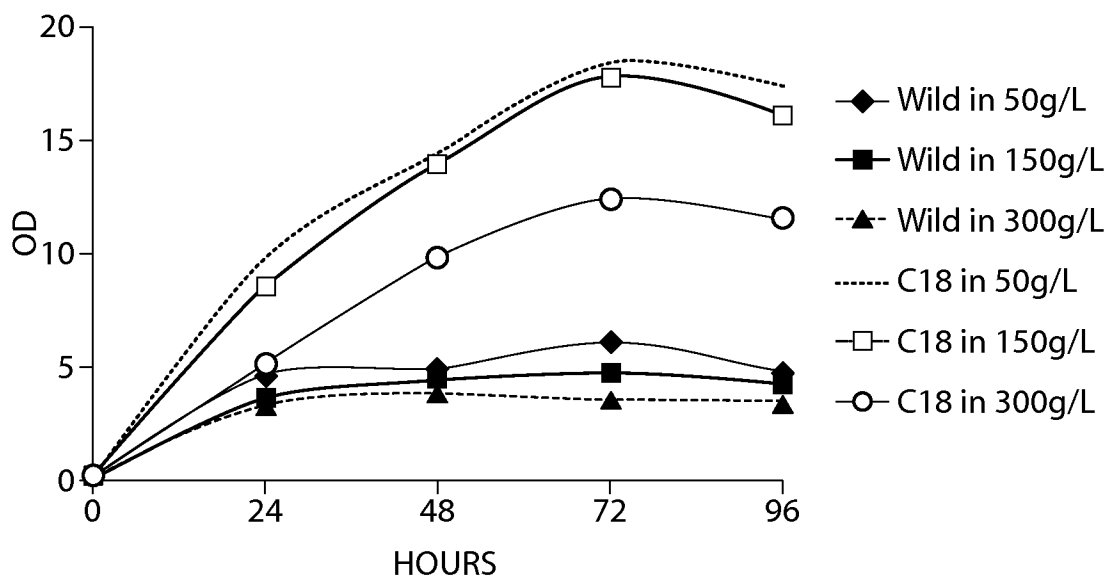


Fig. 10

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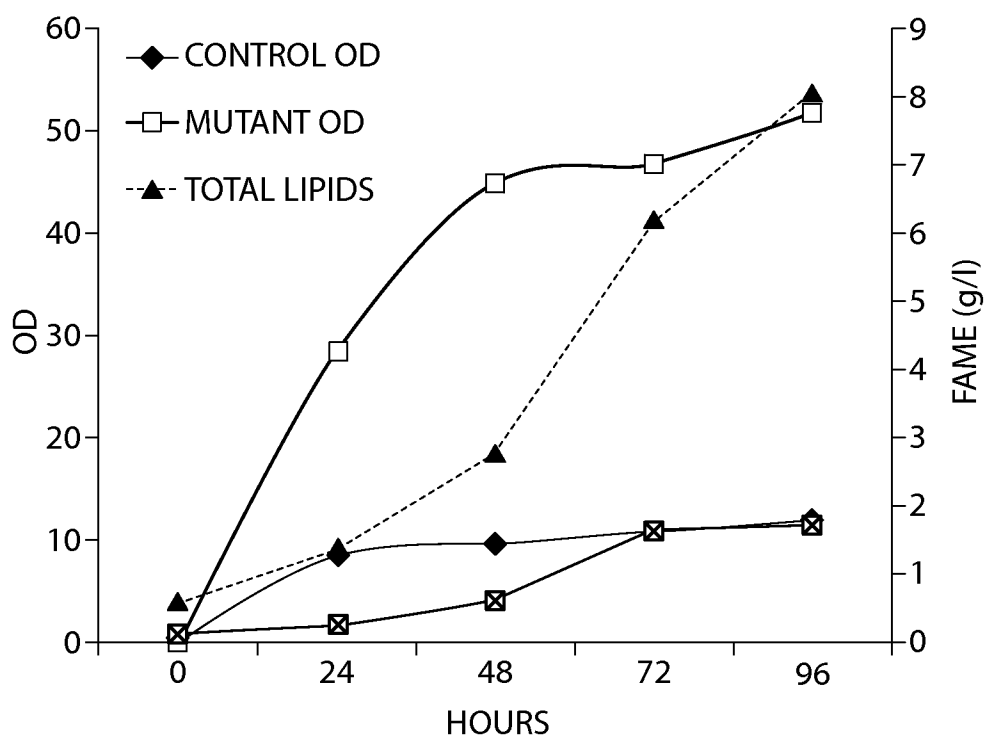


Fig. 11

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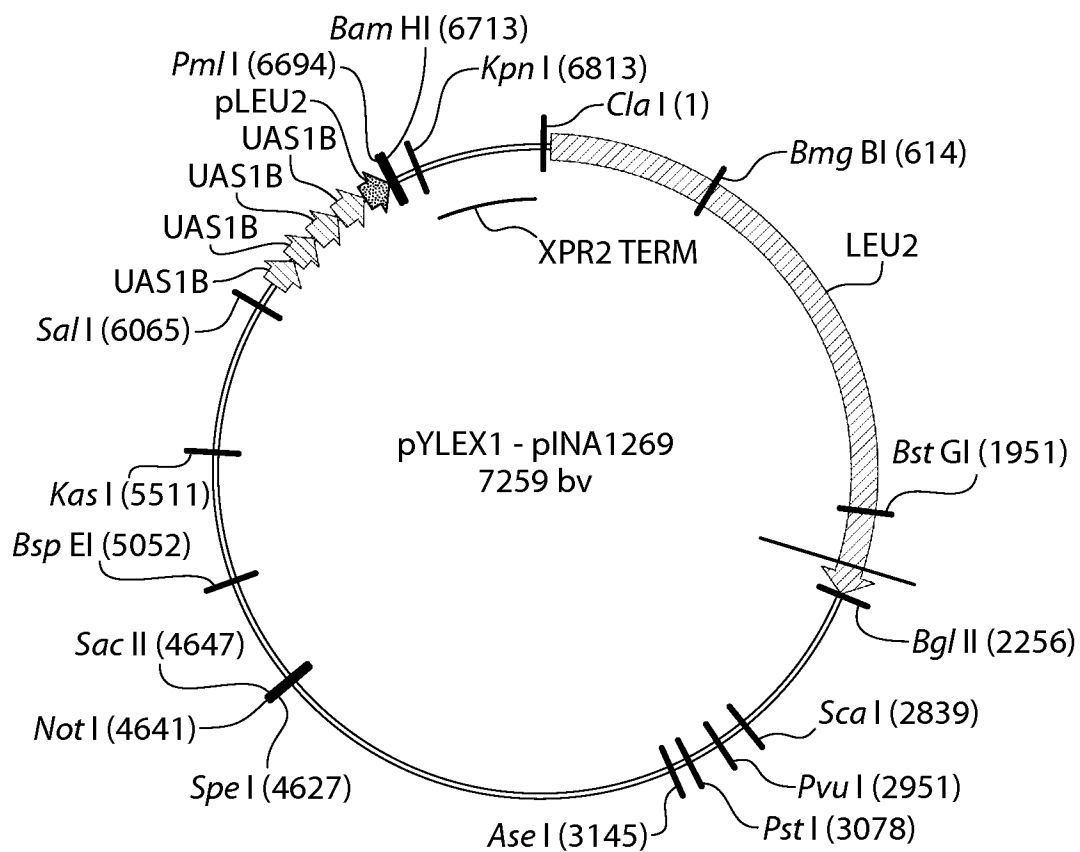


Fig. 12-1

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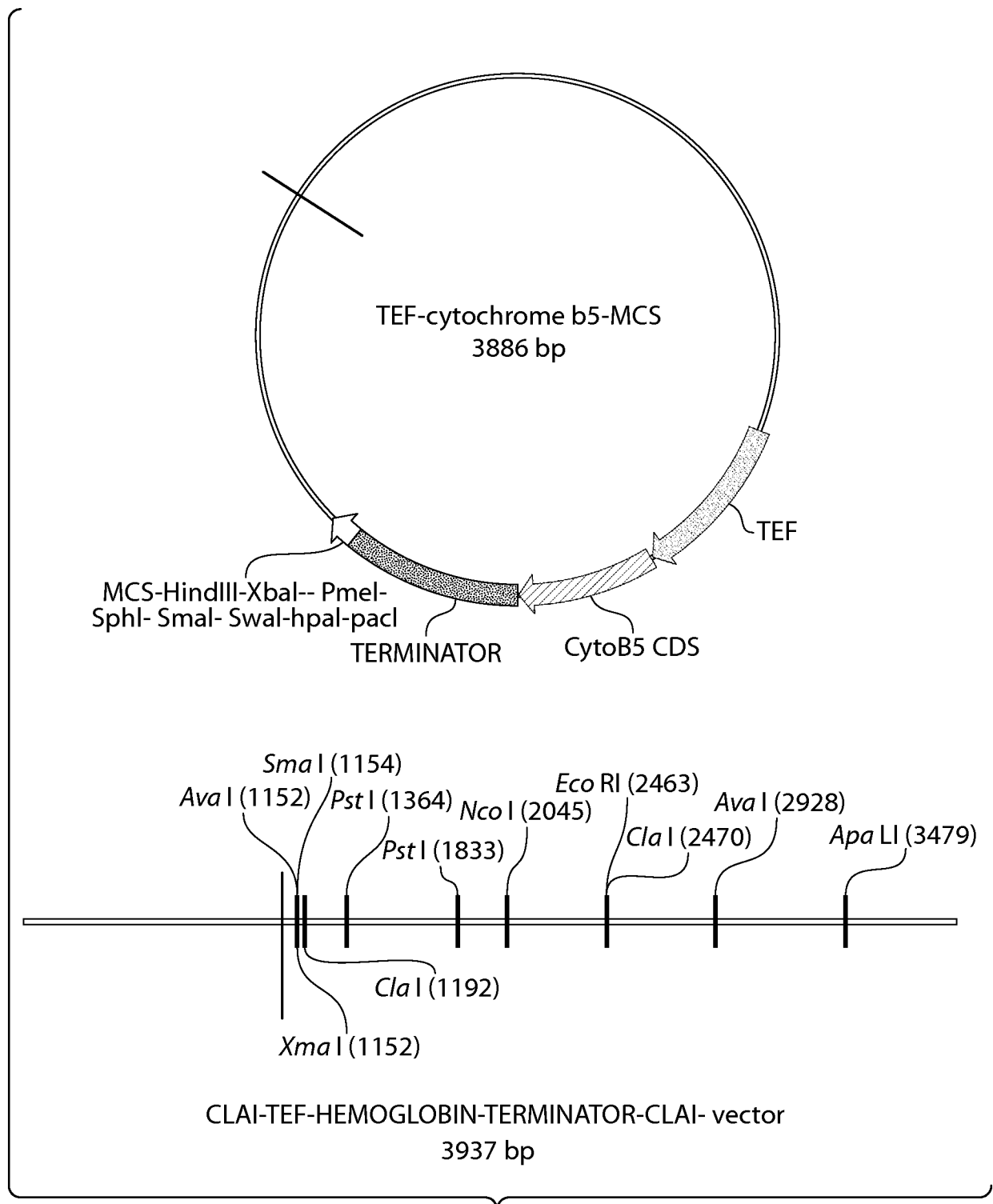


Fig. 12-2

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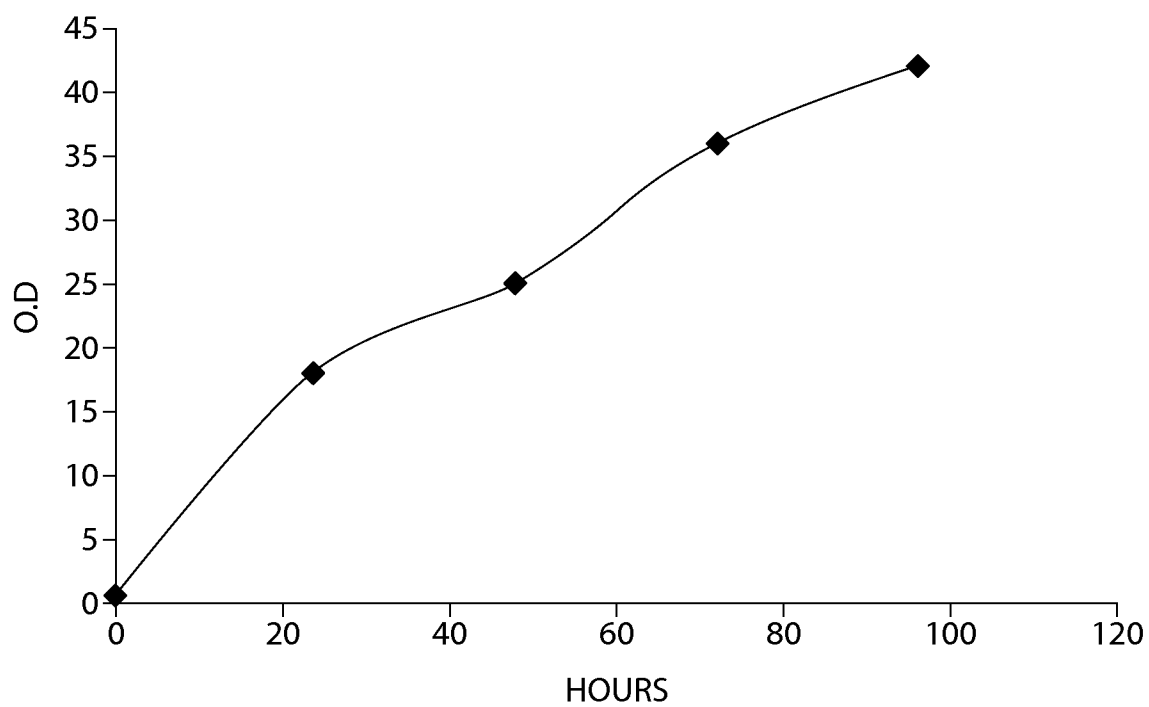


Fig. 13

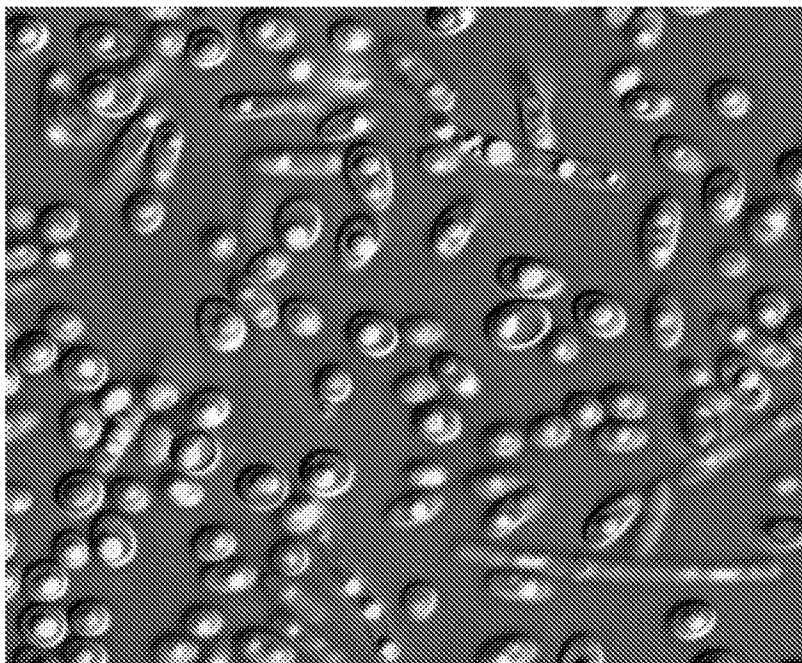


Fig. 14

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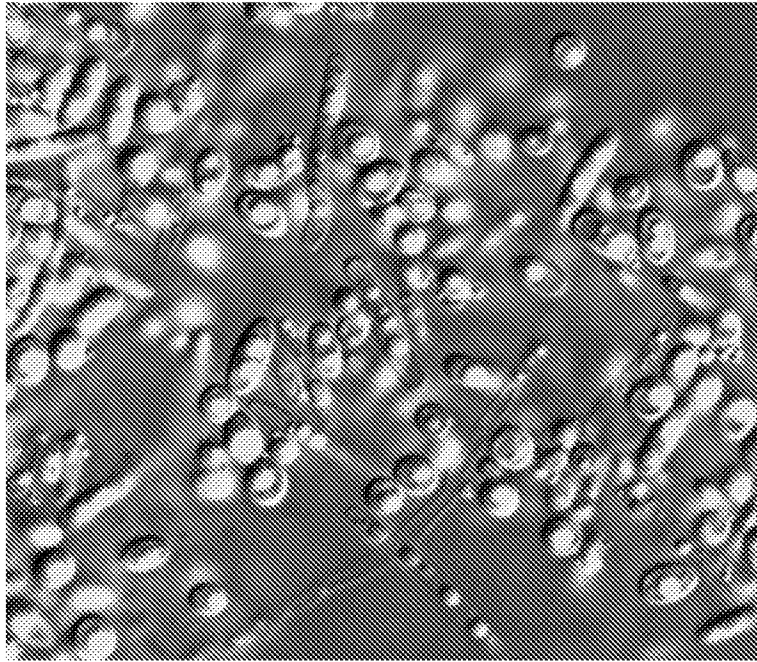


Fig. 15

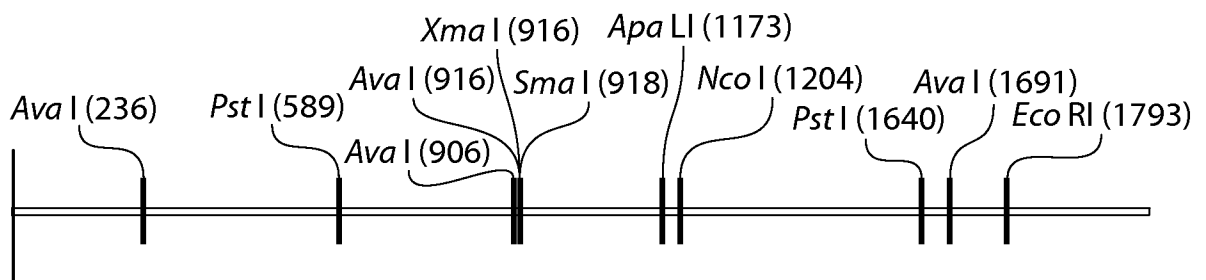


Fig. 16

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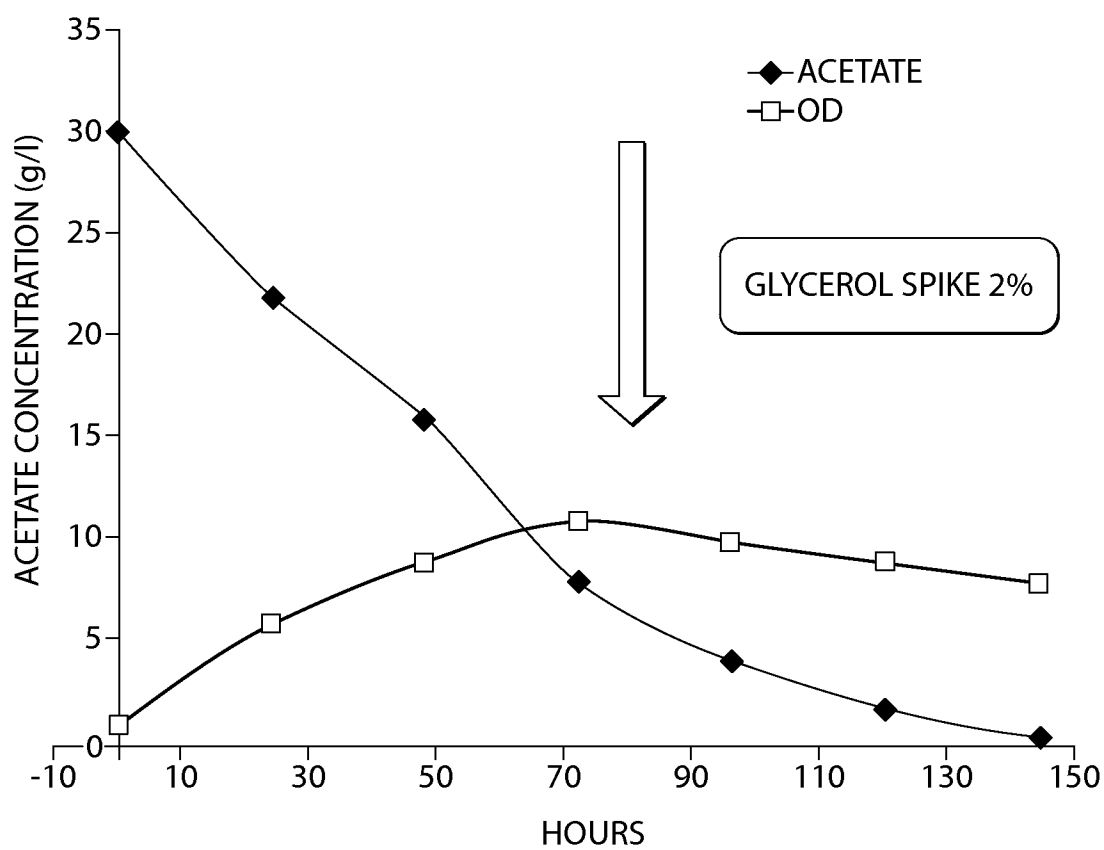


Fig. 17