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(57) Abstract: Systems and methods for the performance of kidney replacement therapy having or using a dialyzer, control components, sorbent cartridge and fluid reservoirs configured to be of a weight and size suitable to be worn or carried by an individual requiring treatment are disclosed. The system for performing kidney replacement therapy has a controlled compliance dialysis circuit, where a control pump controls the bi-directional movement of fluid across a dialysis membrane. The dialysis circuit and an extracorporeal circuit for circulating blood are in fluid communication through the dialysis membrane. The flux of fluid moving between the extracorporeal circuit and the dialysis circuit is modified by the rate at which the control pump is operating such that a rate of ultra-filtration and convective clearance can be controlled. The system provides for the monitoring of an inlet and outlet conductivity of the sorbent cartridge to provide a facility to quantify or monitor the removal of urea by the sorbent cartridge.



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## HEMODIALYSIS SYSTEM HAVING A FLOW PATH WITH A CONTROLLED COMPLIANT VOLUME

### CROSS-REFERENCE TO RELATED APPLICATIONS

[0001] This application claims benefit of priority to U.S. Provisional Patent Application No. 61/514,469 filed on August 2, 2011, which is incorporated herein by reference.

### FIELD OF THE INVENTION

[0002] This disclosure relates to an apparatus for hemodialysis and hemofiltration for the treatment of pathological conditions such as End Stage Renal Disease (ESRD) on a frequent or continuous basis. The systems and methods include a system having a dialyzer, control components, dialysate regeneration cartridge and fluid reservoirs configured to be of a weight and size to be worn or carried by an individual requiring treatment. The disclosure further relates to the treatment of Chronic Kidney Disease (CKD) through methods and apparatuses that allow an individual to remain ambulatory during treatment. The disclosure further relates to the treatment of ESRD through methods and apparatuses that are small, lightweight, and portable.

### BACKGROUND

[0003] Chronic Kidney Disease (CKD), also known as chronic renal disease, is a progressive loss in renal function over a period of months or years. As the disease progresses, a patient with severe renal failure can develop many symptoms that if left untreated may eventually result in death. The most severe stage of CKD is End Stage Renal Disease (ESRD), which occurs when the glomerular filtration rate (GFR) is lower than about 15ml/min/1.73m<sup>2</sup>. ESRD, also referred to as kidney failure or renal failure, is the medical condition wherein a person's kidneys fail to sufficiently remove toxins, waste products, and excess fluid, and to maintain proper electrolyte levels. In the US, the two main causes of

CKD are diabetes and high blood pressure, which are responsible for up to two-thirds of the cases. Heart disease is the leading cause of death for all people having CKD.

[0004] Current treatments for CKD seek to manage comorbidities and, if possible, slow the progression of the disease. However, as the disease progresses, renal function decreases and eventually renal replacement therapy is employed to compensate for lost kidney function. Renal replacement therapy typically entails transplantation of a new kidney, or dialysis. Kidney dialysis is a medical procedure that is performed to aid or replace some of the kidney functions in severe renal failure. Hemodialysis, hemofiltration, hemodiafiltration, and peritoneal dialysis are all replacement therapies for patients who have lost most or all of their kidney function. Dialysis can remove many of the toxins and wastes that the natural kidney would remove. In addition, these therapies are used to balance the electrolyte or blood salt levels and to remove excess fluid that accumulates in patients with renal failure.

[0005] Hemodialysis treatment can be performed to remove waste products from the blood that are no longer being effectively removed by the kidneys, such as urea, creatinine and phosphates. Although the population of patients afflicted with CKD grows each year, there is no cure. The excess fluid accumulated in patients suffering from renal failure is generally removed by direct ultrafiltration or by the ultrafiltration action of a dialysis procedure.

[0006] Hemodialysis procedures are usually carried out three times a week in three to five hour sessions. Dialysis emulates kidney function by removing waste solutes, excess electrolytes and excess fluid from a patient's blood. During dialysis, the patient's blood that contains a high concentration of waste solutes is exposed to a semi-permeable membrane in contact with a solute-deficient dialysis solution (dialysate). Solute removal and electrolyte balancing is accomplished via diffusion across the membrane, while fluid removal is

accomplished via pressure-driven ultrafiltration. Once the blood is purified, it is then returned to the patient. Although effective at removing wastes from blood, dialysis treatments are administered intermittently and therefore do not emulate the continuous function of a natural kidney. Moreover, there are many inconveniences associated with dialysis, such as the necessity of committing to time consuming, thrice-weekly treatments.

[0007] The mortality rate of ESRD patients who receive traditional hemodialysis therapy is 23% per year with an even higher mortality rate among diabetic patients. Excessive fluid can accumulate in patients suffering from ESRD. Fluid accumulates in ESRD patients because the kidneys can no longer effectively remove water and other compounds from the body. The fluid accumulates first in the blood and then accumulates throughout the body resulting in swelling of the extremities and other tissues as edema. This accumulation of fluid causes increased stress on the heart, in turn causing significant increases in blood pressure or hypertension, which can lead to heart failure.

[0008] Although hemodialysis removes excess fluid, the thrice-weekly hemodialysis schedule creates variations in the patient's waste removal, impurity removal, fluid removal and electrolyte balance. These variations result in patient complications and the high rates of patient morbidity and mortality. Since the mid 1990s a number of physicians have prescribed treatment regimens with increased dialysis frequency and treatment time to try to eliminate the problems associated with the thrice-weekly hemodialysis schedule. Two recent randomized controlled clinical studies have shown statistically significant benefits of a more frequent dialysis regimen. Culleton *et al.* (Culleton, BF *et al.* Effect of Frequent Nocturnal Hemodialysis vs. Conventional Hemodialysis on Left Ventricular Mass and Quality of Life. 2007 Journal of the American Medical Association 298 (11)) reported that when compared with conventional hemodialysis (3 times weekly) daily nocturnal hemodialysis improved left ventricular mass (a surrogate for mortality), reduced the need for blood pressure medications

and improved some measures of mineral metabolism. The FHN trial (The FHN Trial Group. In-Center Hemodialysis Six Times per Week versus Three Times per Week, New England Journal of Medicine, 2010) was a comparison of increased treatment frequency of 5.2 hemodialysis treatments a week compared with the traditional thrice-weekly regimen: “Frequent hemodialysis, as compared with conventional hemodialysis, was associated with favorable results with respect to the composite outcomes of death or change in left ventricular mass and death or change in a physical-health composite score.” Based on this data it would be desirable to have a hemodialysis system that would allow kidney patients to dialyze from five to seven days a week if not continuously.

[0009] Despite the clinical results from the Culleton and FHN research, few patients presently undergo a higher frequency of dialysis treatment. More frequent hemodialysis is only used on a small part of the patient population due to the burden and cost of more frequent therapies. Even the thrice weekly-regime is a significant burden to ESRD patients, and an increase in treatment frequency can often be difficult due to the deficiencies in known devices and the cost of the additional treatments. Most dialysis is performed in a dialysis center; hence, there is a need for the practical implementation of more frequent hemodialysis using a simple, wearable/portable, and safe technology that can be used by a patient at home.

[0010] Although dialysis equipment for home use is available, a patient must still remain relatively immobile during the course of treatment due to the non-portable nature of such dialysis equipment. Typical home-dialysis equipment employs an amount of dialysis fluid greater than 20 liters and typically up to 120 to 200 liters that require a dedicated water system. Due to the volume and weight requirements of the needed dialysis fluid, even during home-based dialysis treatment a patient is not ambulatory during treatment, which may affect how often treatment is undertaken.

[0011] The large volume of dialysate fluid required for dialysis is in part attributable to the large quantity of solution necessary for the diffusion of waste products removed and the balancing of electrolytes within the dialysate from the blood of a dialysis patient. Regeneration of spent dialysate is one way to reduce the total volume of a dialysis system by eliminating the need for a large reserve of fresh dialysate. In order for spent dialysate to be reused, accumulated waste products and impurities must be removed from the spent dialysate, and the composition and pH of the regenerated dialysate must be regulated for physiological compatibility. Devices that regenerate spent dialysis fluid are primarily directed toward the removal of urea, ammonium ions, uric acid, creatinine, and phosphate via various sorbents. For example, the Recirculating Dialysate System (“REDY system”), which was introduced in the 1970s, employs a sorbent cartridge through which spent dialysate is recirculated and regenerated. However, the regenerated dialysate produced by REDY systems is subject to variations in pH and sodium concentrations non-conducive to physiological norms. Additionally, REDY systems have limited or no ability to remove sulfates, and are not portable.

[0012] Moreover, traditional dialysis systems employing sorbent technology, such as the REDY system usually employ low-flux dialyzers and adjust dialysate pressure to achieve net patient fluid removal. The UF coefficient of a dialyzer specifies the rate of filtration through the dialyzer due to pressure differences across the dialyzer membrane, typically called the trans-membrane pressure. The trans-membrane pressure is calculated by the formula  $TMP = ((\text{Blood Inlet Pressure} + \text{Blood Outlet Pressure})/2) - ((\text{Dialysate Inlet Pressure} + \text{Dialysate Outlet Pressure})/2)$ . This formula is usually shortened to  $TMP = \text{Venous Return Pressure} - \text{Dialysate Pressure}$ . Low flux hemodialyzers have a UF coefficient of less than 8 ml of water flux per hour per mmHg of trans-membrane pressure. To illustrate fluid removal with the traditional sorbent system, a typical low flux dialyzer could have a UF coefficient of

4 mL/hr/mmHg. To calculate the pressure necessary to achieve the rate of fluid removal, the desired hourly fluid removal is divided by the dialyzer UF coefficient. For example, an hourly rate of 0.5 L/hr yields a required trans-membrane pressure (TMP) of 125 mmHg if the UF coefficient is 4 mL/hr/mmHg. 125 mmHg is the trans-membrane pressure required to remove fluid at a rate of 0.5 L per hour. The venous pressure is a function of the blood flow rate and the blood return restriction (needle and access). As the Venous Return Pressure cannot be set, to control the fluid removal rate it is necessary calculate the required dialysate pressure. The operator calculates dialysate pressure via the formula  $\text{Dialysate Pressure} = \text{Venous Pressure} - \text{TMP}$ , if the venous return pressure were 75mmHg, ( $\text{DP} = 75 - 125 = -50$  mmHg). In this example the user must adjust the dialysate pressure to -50 mmHg to achieve the TMP of 125 mmHg. The venous pressure fluctuates during treatment so the operator must adjust the dialysate pressure on a regular basis, which is not suitable for a non-medical professional or a home patient. With high-flux dialyzers, pressure alone is not accurate enough to control ultrafiltration because fluid moves more freely across the dialyzer membrane. To control ultrafiltration in conventional hemodialysis using high-flux dialyzers, balancing chambers, flow sensors or other methods to balance flow to and from the dialyzer are employed. In CRRT (continuous blood purification machine) equipment, pumps controlled by precise scales are required to control the flow to and from the dialyzer very accurately.

[0013] Development of dialysate recirculating techniques has resulted in systems that employ a variety of sorbent media, including activated carbon, urease, and zirconium-, aluminum-, and magnesium-based materials. Yet one of the problems associated with sorbent regeneration of spent dialysate is the buildup of sodium ions released as a byproduct of the adsorption process, thus necessitating a high degree of sodium concentration control which has yet to be achieved by current wearable or portable dialysis systems. Deionization

resins have been explored to combat the buildup of sodium ions with mixed results. Further, electrolytes such as calcium, magnesium, and potassium are removed from spent dialysate by sorbent and deionization media and must be added back to the dialysate prior to reuse. Additionally, carbon dioxide gas is generated during the absorption process, especially in systems employing urease, and accumulates in the dialysate. Accordingly, sorbent-based dialysis regeneration systems typically must maintain large reservoirs of electrolytic solutions to regulate sodium concentration and maintain electrolyte concentration, and must also include a means for removing accumulated carbon dioxide gas, thus defeating the intended purpose of reducing total system volume and size.

[0014] Some systems have attempted to address the volume and weight problems by allowing for external connections to a tap water source in order to replenish system volume as needed. However, the introduction of tap water into a dialysis system necessitates additional purification measures, thus adding to system complexity and size. As a result, such systems may not be useful for mobile or portable use.

[0015] Sorbent-based dialysate regeneration systems can be found in U.S. Patent No. 3,669,878 Marantz *et al.*, which describes sorbent removal of urea and ammonium ions from spent dialysate via urease, ammonium carbonate, and zirconium phosphate; U.S. 3,669,880 Marantz *et al.*, which describes directing a controlled volume of dialysate through zirconium phosphate, activated carbon, and hydrated zirconium oxide columns; U.S. 3,850,835 Marantz *et al.*, which describes production of a zirconium hydrous oxide ion exchange media; and U.S. 3,989,622 Marantz *et al.*, which describes adsorption of urease on aluminum oxide and magnesium silicate media to convert liquid urea to ammonium carbonate.

[0016] U.S. 4,581,141 Ash, describes removal of uremic substances from dialysate via a calcium-based cation exchanger, urease, and aliphatic carboxylic acid resin. U.S. 4,826,663 Alberti *et al.* describes a method of preparing a zirconium phosphate ion

exchanger. U.S. 6,627,164 Wong describes production of sodium zirconium carbonate for ion exchange in renal dialysis, and U.S. 7,566,432 Wong describes production of zirconium phosphate particles for ion exchange in regenerative dialysis. U.S. 6,818,196 Wong, U.S. 7,736,507 Wong, U.S. Application Publication 2002/0112609 Wong, U.S. Application Publication 2010/0078387 Wong, and U.S. Application Publication 2010/00784330 Wong, describe cartridges for purification of dialysis solutions using sodium zirconium carbonate.

[0017] U.S. 6,878,283 Thompson, U.S. 7,776,210 Rosenbaum *et al.*, U.S. Application Publication 2010/0326911 Rosenbaum *et al.*, U.S. Application Publication 2010/0078381 Merchant, U.S. Application Publication 2009/0127193 Updyke *et al.* and U.S. Application Publication 2011/0017665 Updyke *et al.* describe filter cartridges having a plurality of types of filter media including zirconium compounds, urease, and alumina for dialysis systems. WO 2009/157877 A1 describes a urease material having urease immobilized on a substrate intermixed with a cation exchange material or zirconium phosphate material to improve workability for the reduction of clogging and to improve absorption of ammonium ions generated by the urease.

[0018] Management of impurities in regenerated dialysate can be found in U.S. 4,460,555 Thompson and U.S. 4,650,587 Polak *et al.*, which describes magnesium phosphate media for removal of ammonia from aqueous solutions. U.S. Application Publication 2009/0282980 Gura *et al.* describes degassing devices for use in dialysate systems having urease media.

[0019] However, none of the dialysis systems known in the art and commercialized are mobile such that the weight and volume of the system is sufficiently appropriate to be used by a patient while ambulatory. Hence, there is a need for such devices, which can facilitate regular usage, but is also conducive to operation by a patient without the assistance of a medical professional. Accordingly, there remains a need for a patient-friendly wearable

and/or portable dialysis system that is capable of operating on a small volume of dialysate and suitable for daily continuous or short-term dialysis.

### SUMMARY OF THE INVENTION

[0020] The invention is directed to a hemodialysis system having a size and weight suitable to be carried or worn by a patient during a dialysis treatment. It is to be understood by one skilled in the art that hemodialysis can include hemodialysis, hemofiltration, and hemodiafiltration. In certain embodiments, a system for kidney replacement therapy has a sorbent cartridge for regenerating a dialysate or replacement fluid and a dialyzer or hemofilter for performing hemodialysis and/or hemofiltration wherein water, urea, NaCl, electrolytes, and waste substances are removed from the blood and water can also be removed from the blood during treatment. The dialyzer is incorporated in a housing having a blood inlet and a blood outlet, and a dialysate inlet and a dialysate outlet of the housing in fluid communication with the sorbent cartridge. The hemofilter is housed in a housing having a blood inlet and a blood outlet and an outlet for ultrafiltrate to exit the hemofilter.

[0021] In any embodiment, a system for performing kidney replacement therapy has a dialysis system having a controlled compliance dialysis circuit, a dialyzer having a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane. Blood is circulated through the dialyzer with an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to a subject, a blood pump for conveying blood from the subject through the extracorporeal circuit and the dialyzer, wherein blood is conveyed from the subject, to the dialyzer and back to the subject. Dialysate is conveyed through the dialyzer with a dialysis circuit having a sorbent cartridge for removing impurities from the dialysate, one or more

conduits for carrying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate input end and a dialysate output end. A control pump controls the bi-directional movement of fluid into and out of the dialysis circuit, where a flux of fluid moving between the extracorporeal circuit and the dialysis circuit is changed by the rate at which the control pump is operating, and a first control reservoir stores fluid removed from the dialysis circuit by the control pump or stores fluid that can be added to the dialysis circuit by the control pump. One or more controllers are provided with the system for controlling the rate of the dynamic control pump, a rate of the blood pump, and a rate of the dialysate pump. Optionally, a second control reservoir can store fluid such as tap water that can be added to the dialysis circuit by the control pump when the first control reservoir is used only for storing fluid from the dialysis circuit by the control pump.

[0022] In any embodiment, the system has an infusate reservoir containing an infusate containing one or more electrolytes selected from potassium ions, calcium ions, and magnesium ions. The infusate is added to the dialysate under the control of a controller in order to maintain the concentration of potassium ion, calcium ion and/or magnesium ion within predetermined ranges.

[0023] In any embodiment, the dialysate is conveyed through the dialysis system by a dialysate pump, where the rate of the dialysate pump is controlled by a controller.

[0024] In any embodiment, blood from a patient is conveyed through the dialysis system by a blood pump, wherein the blood pump is controlled by a controller.

[0025] In any embodiment, the pressure of blood entering the dialyzer forming part of the dialysis system is measured entering the dialyzer by a pressure meter and/or the pressure of the blood exiting the dialyzer is measured by a pressure meter.

[0026] In any embodiment, the pressure of the dialysate entering the dialyzer forming part of the dialysis system is measured entering the dialyzer by a pressure meter and/or the pressure of the dialysate exiting the dialyzer is measured by a pressure meter.

[0027] In any embodiment, the dialysis circuit comprises a first pathway for conveying the dialysate between the sorbent cartridge, the dialysate pump, and the dialyzer, and a second bypass pathway for conveying the dialysate between the dialysis output end of the sorbent cartridge and the dialysis input end of the sorbent cartridge without the dialysate passing through the dialyzer. A controller controls the conveyance of the dialysate through either the first pathway or the second bypass pathway based at least in part upon the conductivity of the dialysate.

[0028] In any embodiment, the hemodialysis system has a bicarbonate container containing a solution having a bicarbonate salt and a bicarbonate pump for adding the bicarbonate solution to the dialysis circuit. The bicarbonate is added to the dialysate under the control of a controller in order to maintain the concentration of bicarbonate ion within predetermined ranges.

[0029] In any embodiment, a system is prepared for operation by priming the system. A container containing a priming fluid is attached to the system, the system having an external circuit having a first end that draws the priming fluid from the container and a second end that allows priming fluid to exit the external circuit; and a dialysis circuit, the external circuit and the dialysis circuit being in fluid communication through a dialysis membrane. A first pump is operated to convey the priming fluid from the container and through the external circuit to fill the external circuit with the priming fluid. The first and second ends of the external circuit are attached to draw a biological fluid and the dialysate pump is operated to draw the priming fluid across the dialysis membrane from the external circuit into the dialysis circuit and to draw the biological fluid into the extracorporeal circuit

such that the biological fluid reaches an inlet of a dialyzer housing the dialysis membrane; and after the biological fluid reaches the inlet, the first pump, ultrafiltrate pump, and the dialysate pump are operated where the ultrafiltrate pump is operated at a rate sufficient to transfer the volume of priming fluid present in the external circuit into the dialysis circuit through the dialysis membrane. When the external circuit is filled with biological fluid, the ultrafiltrate pump is operated at a rate sufficient to draw fluid from the external circuit into the dialysis circuit to complete filling the dialysis circuit with fluid.

[0030] In any embodiment, a use of a sorbent is providing a system having a controlled compliance circuit for controlling the movement of fluid volume from an external fluid. The use includes conveying the external fluid through an external circuit and a dialyzer, where the external circuit is in fluid communication with a controlled compliance dialysis circuit through a dialysis membrane housed in the dialyzer. A dialysate is conveyed through the dialysis circuit such that the dialysate moves from a sorbent cartridge, to the dialyzer and back to the sorbent cartridge, where at least one species diffuses from the external fluid to the dialysate through the dialysis membrane and the sorbent cartridge substantially removes at least species from the dialysate. A control pump, which adds fluid from a control reservoir to the dialysis circuit in an influx direction via a conduit or removes fluid from the dialysis circuit to the control reservoir in an efflux direction via the conduit, is operated to intermittently switch the control pump between the efflux direction to move fluid across the dialysis membrane from the external circuit to the dialysis circuit and the influx direction to move fluid across the dialysis membrane from the dialysis circuit to the external circuit. The intermittent switching of the control pump accomplishes the convective clearance of at least one species. Optionally, the at least one species has a molecular weight less than albumin, about 66000 g/mol.

[0031] In any embodiment, a use of a sorbent is providing a system having a controlled compliance circuit for controlling the movement of fluid volume from an external fluid. The use includes conveying the external fluid through an external circuit and a dialyzer, where the external circuit is in fluid communication with a controlled compliance dialysis circuit through a dialysis membrane housed in the dialyzer. A dialysate is conveyed through the dialysis circuit such that the dialysate moves from a sorbent cartridge, to the dialyzer and back to the sorbent cartridge, where at least one waste species diffuses from the external fluid to the dialysate through the dialysis membrane and the sorbent cartridge substantially removes at least one impurity or waste species from the dialysate. A control pump, which adds fluid from a control reservoir to the dialysis circuit in an influx direction via a conduit or removes fluid from the dialysis circuit to the control reservoir in an efflux direction via the conduit, is operated to intermittently switch the control pump between the efflux direction to move fluid across the dialysis membrane from the external circuit to the dialysis circuit and the influx direction to move fluid across the dialysis membrane from the dialysis circuit to the external circuit. A volume of fluid added to the dialysis circuit by the control pump results in substantially the same volume of fluid transferred to the external circuit, and a volume of fluid removed from the dialysis circuit by the control pump results in substantially the same volume of fluid transferred from the external circuit.

[0032] In any embodiment, a use of a sorbent is providing a system having a controlled compliance circuit and monitoring the removal of a waste species from an external fluid. The use includes conveying the external fluid through an external circuit and a dialyzer, where the extracorporeal circuit is in fluid communication with a controlled compliance dialysis circuit through a dialysis membrane housed in the dialyzer. Dialysate is conveyed through the dialysis circuit such that the dialysate moves from a sorbent cartridge, to the dialyzer and back to the sorbent cartridge, wherein urea diffuses from the external fluid

to the dialysate through the dialysis membrane. The conductivity of the dialysate is monitored at an inlet end of the sorbent cartridge and at an outlet end of the sorbent cartridge. The amount of urea absorbed by the sorbent cartridge is calculated based at least in part upon the conductivity measured at the inlet end of the sorbent cartridge and at the outlet end of the sorbent cartridge.

[0033] In any embodiment, a system for kidney replacement therapy to quantify urea removal has a dialyzer with a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane. An extracorporeal circuit has a conduit for receiving blood from a subject and a conduit for returning blood to a subject and a blood pump for conveying blood from the subject, to the dialyzer and back to the subject. A dialysis circuit has a sorbent cartridge for removing urea from the dialysate, one or more conduits for carrying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate input end and a dialysate output end. A first conductivity meter is present for measuring the conductivity of the dialysate at the dialysate input end of the sorbent cartridge. A second conductivity meter is present for measuring the conductivity of the dialysate at the dialysate output end of the sorbent cartridge. One or more controllers compare the conductivity measured by the first conductivity meter and the second conductivity meter and calculate the amount of urea absorbed by the sorbent cartridge.

[0034] In any embodiment, the system has a relative blood volume monitor for monitoring changes in the relative blood volume hydration status of the subject's blood over the course of treatment.

[0035] In any embodiment, a system for performing kidney replacement therapy has a dialysis system having a controlled compliance dialysis circuit, a dialyzer having a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane. Blood is circulated through the dialyzer with an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to a subject, a blood pump for conveying blood from the subject through the extracorporeal circuit and the dialyzer, wherein blood is conveyed from the subject, to the dialyzer and back to the subject. Dialysate is conveyed through the dialyzer with a dialysis circuit having a sorbent cartridge for removing impurities from the dialysate, one or more conduits for carrying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate input end and a dialysate output end. A control pump moves fluid between the dialysis circuit and the extracorporeal circuit by removing fluid from the dialysis circuit, where a flux of fluid moving between the extracorporeal circuit and the dialysis circuit is changed by the rate at which the control pump is operating, and a first control reservoir stores fluid removed from the dialysis circuit by the control pump. A second reservoir and a second reservoir pump is present to add water to the dialysis circuit, where fluid added to the dialysis circuit causes movement of fluid from the dialysis circuit to the extracorporeal circuit. In any embodiment, the second reservoir can store water, tap water or purified water. One or more controllers are provided with the system for controlling a rate of the control pump, a rate of the blood pump, a rate of the second reservoir pump and a rate of the dialysate pump. This second reservoir can be located either before the dialysate pump, after the dialysate pump or after the sorbent cartridge.

[0036] In any embodiment of a system, device or use described herein, a dialysis chamber is a selective diffusion chamber.

[0037] In any embodiment of a system, device or use described herein, a dialysis membrane is a selectively permeable membrane.

[0038] In any embodiment of a system, device or use described herein, an external fluid is not a fluid derived from the human body.

[0039] In any embodiment of a device or use described herein, the control pump is used to maintain control over the net movement of fluid between a controlled compliance circuit and an external circuit via the control pump adding or removing fluid from the controlled compliance circuit.

[0040] In any embodiment of a system, device or use described herein, the external fluid is a suspension or solution of biomolecules with the proviso that the suspension or solution is not a bodily fluid.

[0041] In any embodiment of a system, device or use described herein, a use of a sorbent is provided in the manufacturing of an apparatus for removing waste or impurity species from a fluid in a controlled compliance circuit.

[0042] In any embodiment of system, device or use described herein, a use of a sorbent is provided for absorbing an impurity or waste species originating from an external circuit using an apparatus having a controlled compliance circuit, wherein the apparatus has a control pump to maintain control over the net movement of fluid between the controlled compliance circuit and an external circuit via the control pump adding or removing fluid from the controlled compliance circuit.

[0043] In any system, device or use described herein, a use of a device having a dialyzer is provided for controlling the net movement of fluid through the dialyzer between a

controlled compliance circuit and an external circuit via a control pump adding or removing fluid from the controlled compliance circuit.

[0044] Other objects, features and advantages of the present invention will become apparent to those skilled in the art from the following detailed description. It is to be understood, however, that the detailed description and specific examples, while indicating some embodiments of the present invention are given by way of illustration and not limitation. Many changes and modifications within the scope of the present invention may be made without departing from the spirit thereof, and the invention includes all such modifications.

#### BRIEF DESCRIPTION OF THE DRAWINGS

[0045] Figure 1A shows a hemodialysis device having a controlled compliant dialysis circuit operating in accordance with certain embodiments.

[0046] Figure 1B shows a hemofiltration device having a controlled compliant filtration circuit operating in accordance with certain embodiments.

[0047] Figure 2 shows a hemodialysis device having a controlled compliant dialysis circuit and a mixed bed deionization column operating in accordance with certain embodiments.

[0048] Figures 3A through 3E show sorbent cartridges in accordance with certain embodiments. Figure 3A shows a sorbent cartridge having multiple sorbent materials in a single housing. Figure 3B shows a schematic for a sorbent cartridge having sorbent materials housed in several housings. Figure 3C shows a side view of an individual housing from the sorbent cartridge depicted in Figure 3B. Figure 3D shows a top view of an individual housing from the sorbent cartridge depicted in Figure 3B and a top view of a spacer frit. Figure 3E shows a bottom view of an individual housing from the sorbent cartridge depicted in Figure 3B and a bottom view of a spacer frit.

[0049] Figures 4A, 4B and 4C depict a sorbent cartridge with a carrier. Figure 4A shows a top view of a carrier for sorbent housings. Figure 4B shows a top view of the carrier of Figure 4A with several sorbent housings placed within the carrier. Figure 4C shows a side view of a sorbent cartridge having five separate sorbent housings.

[0050] Figure 5 shows a hemodialysis device having a controlled compliant dialysis circuit and a bicarbonate cartridge operating in accordance with certain embodiments.

[0051] Figure 6 shows a hemodialysis device having a controlled compliant dialysis circuit and a bicarbonate infusion pump operating in accordance with certain embodiments.

[0052] Figure 7 shows a hemodialysis device having a controlled compliant dialysis circuit and a bicarbonate infusion pump operating in accordance with certain embodiments.

[0053] Figure 8 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to remove air from the extracorporeal circuit.

[0054] Figure 9 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to remove air from a portion of the dialysis circuit.

[0055] Figure 10 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to remove air from the dialysis circuit.

[0056] Figure 11 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to remove air from the dialysis circuit and reconstitute infusate salts.

[0057] Figure 12 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to remove air from the dialysis circuit and to adjust the composition of the dialysate.

[0058] Figure 13 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to displace a priming fluid from an extracorporeal circuit to the dialysis circuit with blood from a patient.

[0059] Figure 14 shows a hemodialysis device having a controlled compliant dialysis circuit undergoing a priming operation to displace a priming fluid from an extracorporeal circuit to the dialysis circuit with blood from a patient.

[0060] Figure 15 shows a hemodialysis device having a controlled compliant dialysis circuit and an extracorporeal circuit undergoing a priming operation to fill a void volume in the dialysis circuit with fluid originating from a patient's blood.

[0061] Figure 16 shows a hemodialysis device having a controlled compliant dialysis circuit and an extracorporeal circuit undergoing a priming operation.

[0062] Figure 17 shows a hemodialysis device having a controlled compliant dialysis circuit and an extracorporeal circuit undergoing a priming operation to reconstitute an infusate solution and a bicarbonate solution.

[0063] Figure 18 shows a hemodialysis device having a controlled compliant dialysis circuit and an extracorporeal circuit undergoing a priming operation and adjustment of the composition of a dialysate.

[0064] Figure 19 shows a primed hemodialysis device that is ready for operation.

[0065] Figure 20 shows a hemodialysis device having a controlled compliant dialysis circuit, an extracorporeal circuit and a deionization column undergoing a priming operation.

[0066] Figure 21 shows a hemodialysis device having a controlled compliant dialysis circuit and a deionization column, where effluent from the deionization column is used to reconstitute a bicarbonate solution.

[0067] Figure 22 shows a hemodialysis device having a controlled compliant dialysis circuit, an extracorporeal circuit and a deionization column undergoing a priming operation by purging air from a dialyzer.

[0068] Figure 23 shows a hemodialysis device having a controlled compliant dialysis circuit, an extracorporeal circuit and a bicarbonate column undergoing a priming operation.

[0069] Figure 24 shows a hemodialysis device having a controlled compliant dialysis circuit, an extracorporeal circuit and a bicarbonate column undergoing a priming operation by purging air from a dialyzer.

[0070] Figure 25 shows a hemodialysis device having a controlled compliant dialysis circuit and an extracorporeal circuit undergoing an operation to return blood from the extracorporeal circuit to the patient.

[0071] Figure 26 shows a hemodialysis device having a controlled compliant dialysis circuit and an extracorporeal and at least two conductivity meters for determining an amount of urea absorbed by a sorbent cartridge.

[0072] Figure 27 shows a schematic for a hematocrit detector.

[0073] Figure 28 shows a schematic for an impedance detector.

[0074] Figure 29 shows a hemodialysis device illustrating a second control reservoir containing a fluid such as water.

[0075] Figure 30 shows a schematic for a controller in communication with various system components.

#### DETAILED DESCRIPTION OF THE INVENTION

[0076] Dialysis is the most commonly applied physical principle to address the build-up of urea and other toxins, to balance electrolytes, and to remove excess fluid in patients with kidney failure. Dialysis as a renal or kidney replacement therapy can include hemodialysis, hemodiafiltration, or hemofiltration to remove toxins and impurities from a patient's blood. Dialysis membranes employed in dialysis treatment are typically only selective toward molecular weight and not toward other properties such as electrical charge. As such, urea, ions and other small molecules can move across the dialysis membrane unimpeded from a higher concentration to a lower concentration via diffusion thereby

lowering the concentration of such species in the patient's blood through the process of hemodialysis.

[0077] Hemofiltration and hemodiafiltration employ techniques involving removing fluid from the patient by drawing bulk fluid across the dialysis membrane thereby pulling out waste products with a solute drag effect. Further, both hemofiltration and hemodiafiltration can be employed for ultrafiltration to accomplish the removal of accumulated fluid from a subject. Hemofiltration and hemodiafiltration are more effective for removing mid-weight and other impurities that otherwise have a low coefficient of diffusion and cannot be efficiently removed by hemodialysis.

[0078] During operation of typical dialysis machines to perform hemodiafiltration, blood is passed through a dialysis chamber on one side of a dialysis membrane and a dialysate is passed on the other side of the dialysis membrane. In addition to diffusion of solutes across the dialysis membrane, a difference in pressure between the blood-side and the dialysate-side of the dialysis membrane drives the bulk movement of water from higher pressure to lower pressure. This flow is in excess to the patient's net fluid removal requirements, so the blood must be rehydrated with a sterile substitution or replacement solution. The pressure generated on a particular side of the dialysis membrane depends on several factors including flow rate, viscosity of the fluid, geometry of the dialyzer and the physiological condition of the patient. Pressure and the subsequent net movement of water across the dialysis membrane requires large and expensive equipment to control with a high degree of accuracy.

[0079] A system or apparatus for kidney replacement therapy can also be configured to perform hemofiltration. Blood is passed through a hemofilter having a hemofiltration membrane to contact one side of the hemofiltration membrane. A negative pressure is applied to the side of the hemofiltration membrane not in contact with the blood to draw the

movement of water from the blood across the hemofiltration membrane. The amount or volume of water transversing the hemofiltration membrane also depends on several factors including the blood flow rate, viscosity, geometry of the hemofilter and the physiological condition of the patient. Removal of impurities from the blood by convection during hemofiltration is usually only accomplished by the removal of a large volume of fluid from the blood. Substitution or replacement fluid needs to be introduced to the subject. Expensive equipment is normally required to balance fluid removal with replacement or substitution fluid.

[0080] A portable dialysis system is contemplated herein having a controlled compliance dialysis circuit. In general, portable dialysis systems rely upon the regeneration of spent dialysate (*i.e.* dialysate having urea and/or other waste species therein) to form refreshed dialysate that can be reused to perform dialysis or to dialyze the patient utilizing a smaller dialysate volume. Regeneration of the dialysate allows for the volume of fluid that needs to be supplied to perform a session of dialysis treatment to be limited and enable a portable system. The systems of the invention can employ a reservoir of working dialysate solution that varies in volume depending upon bulk movement of water across the dialysis membrane and/or water added to dilute sodium ion concentration and reduce conductivity. Further, a system for kidney replacement therapy employing hemofiltration is contemplated wherein ultrafiltrate is treated to generate a replacement solution for reintroduction to the subject. Use of the ultrafiltrate to generate a replacement solution simplifies the balancing of fluid removal with the replacement solution; specifically, scales or gravimetric methods are not required to balance fluid removal with fluid replacement. Systems where the volume of working dialysate and/or ultrafiltrate vary during the course of treatment complicate accurate control over removal of fluid from a patient through techniques such as ultrafiltration and hemodiafiltration. In the present invention, a controlled compliance dialysis circuit is

provided for conveying and re-circulating a dialysate between a dialyzer, where the dialysate picks up impurities such as urea, and a sorbent cartridge where waste species are removed from the dialysate to form refreshed dialysate after the addition of cation electrolytes. The dialysate flow path described herein has active control of fluid flow entering and exiting the flow path in a manner that allows for the accurate performance of ultrafiltration, the quantization of urea removal and the performance of conductive clearance of mid-weight uremic impurities without an excessive risk for blood clotting.

[0081] Alternatively, a controlled compliance hemofiltration circuit is provided for conveying an ultrafiltrate from a hemofilter to a sorbent cartridge where waste species are removed from the ultrafiltrate. The ultrafiltrate with the impurities removed can then be reintroduced to the subject as a replacement fluid. The controlled compliance hemofiltration circuit provides for the accurate control of fluid removal and introduction of replacement fluid to the subject without the use of scales or gravimetric methods. The controlled compliance dialysis circuit described herein controls the inputs and outputs of fluid to the dialysis circuit by using a flow path having a substantially inflexible volume wherein all of the complexity associated with scale control is eliminated. Fluid balancing is accomplished very accurately. In any embodiment described herein, an operator or user need only set the fluid removal rate and the device can control the fluid removal accurately without the use of scales or balancing chambers to control flow.

### *Definitions*

[0082] Unless defined otherwise, all technical and scientific terms used herein generally have the same meaning as commonly understood by one of ordinary skill in the relevant art.

[0083] The articles “a” and “an” are used herein to refer to one or to more than one (*i.e.*, to at least one) of the grammatical object of the article. By way of example, “an element” means one element or more than one element.

[0084] The term “activated carbon” refers to a porous carbon material having a surface area greater than 500 m<sup>2</sup> per gram. Activated carbon can be capable of absorbing several species including heavy metals such as lead, mercury, arsenic, cadmium, chromium and thallium among others, oxidants such as chlorine and chloramine, fluoride ions, and waste species such as phosphate and certain nitrogen-containing waste species such as creatinine and uric acid

[0085] The terms “administering,” “administer,” “delivering,” “deliver,” “introducing,” “bolus,” and “introduce” can be used interchangeably to indicate the introduction of water or an agent into the body of a patient, including electrolytes and alkali and/or alkali earth ions, to a patient in need thereof, and can further mean the introduction of water, any agent or alkali and/or alkali earth ions to a dialysate or dialysis circuit where such water, agent or alkali and/or alkali earth ion will enter the blood of the patient by diffusion, transversal of a diffusion membrane or other means.

[0086] The term “air trap” refers to a structure for separating a gas from a mixture of a gas and a liquid or any other separation means known in the art. An air trap can include a hydrophobic membrane for allowing gases to pass and for preventing the passage of water.

[0087] The term “anticoagulant” is a substance that prevents or delays the clotting of blood, such as heparin, fragmin, and sodium citrate.

[0088] A “biocompatible material” is a material that has the ability to interface with living biological tissues with an acceptable host response in any of specific medical systems, methods of treatment or delivery contemplated herein. The biocompatible material can

consist of synthetic, natural or modified natural polymers intended to contact or interact with the biological systems during application of any of the inventions contained herein.

[0089] The term “conduit” refers to a vessel or passageway having a void volume through which a fluid can travel or move. A conduit can have a dimension parallel to the direction of travel of the fluid that is significantly longer than a dimension orthogonal to the direction of travel of the fluid.

[0090] “Chronic kidney disease” (CKD) is a condition characterized by the slow loss of kidney function over time. The most common causes of CKD are high blood pressure, diabetes, heart disease, and diseases that cause inflammation in the kidneys. CKD can also be caused by infections or urinary blockages. If CKD progresses, it can lead to end-stage renal disease (ESRD), where the kidneys fail to function at a sufficient level.

[0091] The terms “communicate” and “communication” include, but are not limited to, the connection of system electrical elements, either directly or remotely, for data transmission among and between said elements. The terms also include, but are not limited, to the connection of system fluid elements enabling fluid interface among and between said elements.

[0092] The term “comprising” includes, but is not limited to, whatever follows the word “comprising.” Thus, use of the term indicates that the listed elements are required or mandatory but that other elements are optional and may or may not be present.

[0093] The term “conductivity meter” or “conductivity sensor” refers to a device for measuring the electrical conductance of a solution.

[0094] The term “consisting of” includes and is limited to whatever follows the phrase “consisting of.” Thus, the phrase indicates that the limited elements are required or mandatory and that no other elements may be present.

[0095] The term “consisting essentially of” includes whatever follows the term “consisting essentially of” and additional elements, structures, acts or features that do not affect the basic operation of the apparatus, structure or method described.

[0096] The term “control pump” refers to a pump that is operable to pump fluid bi-directionally to actively control the transfer of fluid volume into or out of a compartment or circuit.

[0097] The term “control reservoir” refers to a substantially inflexible, or non-flexible vessel or container accessible by the control pump that contains a variable amount of fluid.

[0098] A “control system” consists of combinations of components that act together to maintain a system to a desired set of performance specifications. The control system can use processors, memory and computer components configured to interoperate to maintain the desired performance specifications. It can also include fluid control components, and solute control components as known within the art to maintain the performance specifications.

[0099] A “controller,” “control unit,” “processor,” or “microprocessor” is a device which monitors and affects the operational conditions of a given system. The operational conditions are typically referred to as output variables of the system, which can be affected by adjusting certain input variables.

[00100] The terms “controlled compliance” and “controlled compliant” describe the ability to actively control the transfer of fluid volume into or out of a compartment or circuit. In certain embodiments, the variable volume of fluid in a dialysate circuit expands and contracts via the control of one or more pumps. The volume of fluid in the system minus the attached reservoirs once the system is in operation is generally constant. The attached reservoirs allow the system to adjust the patient fluid volume by withdrawing fluid and storing the desired amount in an attached control reservoir and/or by providing rebalanced fluids to the patient and removing waste products. Alternatively, the fluid stored in a control

reservoir attached to the dialysate circuit can be used for ultrafiltration (UF) and/or delivery of an infusate. The terms “controlled compliance” and “controlled compliant” are not to be confused with the term “non-compliant volume,” which simply refers to a vessel, conduit, container, pathway or cartridge that resists the introduction of a volume of fluid after air has been removed from a defined space such as a vessel, conduit, container, pathway or cartridge.

[00101] The term “convective clearance” refers to the movement of solute molecules or ions across a semi-permeable barrier due to force created by solvent molecules moving across the semi-permeable barrier.

[00102] The term “dialysate” describes a fluid into which solutes from a fluid to be dialyzed diffuse through a membrane. A dialysate typically contains electrolytes that are close in concentration to the physiological concentration of electrolytes found in blood.

[00103] “Dialysis” is a type of filtration, or a process of selective diffusion through a membrane. Dialysis removes solutes of a specific range of molecular weights via diffusion through a membrane from a fluid to be dialyzed into a dialysate. During dialysis, a fluid to be dialyzed is passed over a filter membrane, while dialysate is passed over the other side of that membrane. Dissolved solutes are transported across the filter membrane by diffusion between the fluids. The dialysate is used to remove solutes from the fluid to be dialyzed. The dialysate can also provide enrichment to the other fluid.

[00104] The term “dialysis membrane” or “hemofiltration membrane” can refer to a semi-permeable barrier selective to allow diffusion of solutes of a specific range of molecular weights through the barrier, or optionally a high permeability membrane, which is a type of semipermeable membrane that is more permeable to water than the semipermeable membrane of a conventional hemodialysis system, which has a semipermeable membrane that has a sufficiently low permeability to water such that an ultrafiltration controller is not required to prevent excessive loss of water from the patient's blood. During high

permeability hemodialysis, the system removes toxins or excess fluid from the patient's blood using the principles of convection (via a high ultrafiltration rate) and/or diffusion (via a concentration gradient in dialysate). In certain non-limiting examples, the semipermeable membrane during high permeability hemodialysis or hemofiltration has an *in vitro* ultrafiltration coefficient (Kuf) greater than 8 milliliters per hour per conventional millimeter of mercury, as measured with bovine or expired human blood.

[00105] The term “diluent” refers to a fluid having conductivity less than a fluid to which the diluent is added.

[00106] The term “electrolyte” refers to an alkali or alkali earth cation dissolved in an aqueous medium.

[00107] The term “filtration” refers to a process of separating solutes from a fluid, by passing the fluid through a filter medium across which certain solutes or suspensions cannot pass. Filtration is driven by the pressure difference across the membrane.

[00108] The term “substantially inflexible volume” refers to a three-dimensional space within a vessel or container that can accommodate a maximum amount of non-compressible fluid and resists the addition of any volume of fluid above the maximum amount. The presence of a volume of fluid less than the maximum amount will fail to completely fill the vessel or container. Those skilled in the art will recognize that a minimal amount of expansion or contraction of the vessel or container can occur in a substantially inflexible volume; however, the addition or subtraction of a significant volume of fluid over a maximum or minimum will be resisted.

[00109] The term “fluid communication” refers to at least two fluids that are contained in separated compartments that are able to exchange matter, either solvent or solute molecules or ions, through a semi-permeable barrier.

[00110] The terms “frit” and “spacer frit” refer to a material that is biocompatible and has a porosity between about 1  $\mu\text{m}$  and 300  $\mu\text{m}$ . The material can be one or more of biocompatible, compressible, an open cell polymer or foam or similar material.

[00111] “Hemofiltration” is a therapy in which blood is filtered across a semi-permeable membrane. Water and solutes are removed from the blood via pressure-driven convection across the membrane. In hemofiltration, solutes small enough to pass through the membrane in proportion to their plasma concentration are removed. The driving force is a pressure gradient rather than a concentration gradient. A positive hydrostatic pressure drives water and solutes across the filter membrane from the blood compartment to the filtrate compartment, from which it is drained. Solute, both small and large, get dragged through the membrane at a similar rate by the flow of water that has been engineered by the hydrostatic pressure. Hence, convection overcomes the reduced removal rate of larger solutes (due to their slow speed of diffusion) observed in hemodialysis. The rate of solute removal is proportional to the amount of fluid removed from the blood circuit, which can be adjusted to meet the needs of a clinical situation. In general, the removal of large amounts of plasma water from the patient requires volume substitution. Substitution fluid, typically a buffered solution close to the plasma water composition a patient needs, can be administered pre or post filter (pre-dilution mode, post-dilution mode).

[00112] “Hemodialysis” is a technique where blood and a “cleansing fluid” called dialysate are exposed to each other separated by a semi-permeable membrane. Solute within the permeability range of the membrane pass while diffusing along existing concentration gradients. The dialysate employed during hemodialysis has soluble ions such as sodium, calcium and potassium ions and is not pure water. The sieving properties of the membrane exclude all solutes above a certain threshold from crossing the membrane. One common sieving property is “albumin sieving.” In most situations it is not desirable to remove

Albumin during renal replacement therapy, as lower blood serum Albumin is associated with increased mortality rates.

[00113] The term “albumin sieving coefficient” can be used to describe the amount of albumin that will cross a membrane.

[00114] The term “hematocrit” refers to the fraction of blood volume occupied by erythrocytes.

[00115] “Hemodiafiltration” is a therapy that combines hemofiltration and hemodialysis.

[00116] The term “impedance meter” refers to a device for measuring the opposition of an object or structure to an alternating current.

[00117] The term “impurity species” refers to a molecular or ionic species that originates from tap water, a sorbent cartridge or a source other than a patient’s or subject’s blood including chlorine, fluoride ions, and aluminum-containing species.

[00118] The term “infusate container” refers to a vessel, which can be substantially inflexible or non-flexible for holding a solution of one or more salts for the adjustment of the composition of a dialysate.

[00119] The term “infusate solution” refers to a solution of one or more salts for the adjustment of the composition of a dialysate, such as salts of calcium, magnesium and potassium.

[00120] The term “waste species” or “waste products” refer to any molecular or ionic species originating from the patient or subject, including metabolic wastes, molecular or ionic species including nitrogen or sulfur atoms, mid-weight uremic wastes and nitrogenous waste. Waste species are kept within a specific homeostasis range by individuals with a healthy renal system. For example, nitrogen-containing waste products are generally at a level less than 30 mg/dL in the blood for individuals with a healthy renal system and inorganic

phosphate can be generally in a range between 2.5-4.5 mg/dL but not necessarily limited to this range. The level of waste products in the blood is elevated for individuals with impaired kidney function.

[00121] The term “nitrogenous waste” refers to any non-polymeric nitrogen-containing organic compound originating from the blood of a patient. Nitrogenous waste includes urea and creatinine.

[00122] The term “oximeter” refers to a device for measuring the amount of oxygen carried by a volume of blood.

[00123] The term “luer connector” or “luer adapter” refers to adapters or connectors conforming with International Standards Organization (ISO) standards 594-2.

[00124] The term “memory” refers to a device for recording digital information that can be accessed by a microprocessor, such as RAM, Dynamic RAM, microprocessor cache, FLASH memory, or memory card.

[00125] The term “mid-weight uremic wastes” refers to substances that can pass through a dialysis membrane that have a molecular weight less than about 66,000 g/mol and greater than about 1000 g/mol.

[00126] The term “moving fluid bi-directionally” refers to the ability to move a fluid across a barrier, such as a semi-permeable membrane, in either direction.

[00127] “Osmolarity” is defined as the number of osmoles of a solute per liter of solution. Thus, a “hyperosmolar solution” represents a solution with an increase in osmolarity compared to physiologic solutions. Certain compounds, such as mannitol, may have an effect on the osmotic properties of a solution as described herein.

[00128] A “patient” or “subject” is a member of any animal species, preferably a mammalian species, optionally a human. The subject can be an apparently healthy individual, an individual suffering from a disease, or an individual being treated for a disease.

[00129] The terms “pathway” and “conveyance pathway” refer to the route through which a fluid, such as dialysate or blood travels.

[00130] The term “peristaltic pump” refers to a pump that operates by compression of a flexible conduit or tube through which the fluid to be pumped passes.

[00131] The terms “portable system” or “wearable system” refers to a system in whole or in part having a mass and dimension to allow for transport by a single individual by carrying the system or wearing the system on the individual’s body. The terms are to be interpreted broadly without any limitation as to size, weight, length of time carried, comfort, ease of use, and specific use by any person whether man, woman or child. The term is to be used in a general sense wherein one of ordinary skill will understand that portability as contemplated by the invention encompasses a wide range of weights, geometries, configurations and size.

[00132] The terms “pressure differential” and “pressure drop” refer to the difference in pressure measurements of a fluid between two points of measurement.

[00133] The term “pressure meter” refers to a device for measuring the pressure of a gas or liquid in a vessel or container.

[00134] The terms “processor,” “computer processor,” and “microprocessor” as used herein are broad terms and are to be given their ordinary and customary meaning to a person of ordinary skill in the art. The terms refer without limitation to a computer system, state machine, processor, or the like designed to perform arithmetic or logic operations using logic circuitry that responds to and processes the basic instructions that drive a computer. In some embodiments, the terms can include ROM (“read-only memory”) and/or RAM (“random-access memory”) associated therewith.

[00135] The term “programmable” as used herein refers to a device using computer hardware architecture with a stored program and being capable of carrying out a set of commands, automatically that can be changed or replaced.

[00136] The term “pulsatile pump” refers to a pump that mimics the action of a mammalian heart where the pumped fluid undergoes periodic variation in velocity.

[00137] The term “pump” refers to any device that causes the movement of fluids or gases by the application of suction or pressure.

[00138] The term “quick connector” refers to any structure for making an attachment that is operable by an individual using their hands or fingers without the assistance of additional tools. The quick connector may have a valve that shuts off flow when the connector is disconnected.

[00139] The term “relative blood volume monitor” refers to any device measuring the concentration of any solute or solid material in the blood. Non-limiting examples of relative blood volume monitors include devices for measuring the concentration of oxyhemoglobin, deoxyhemoglobin, hematocrit or red blood cell count, osmolarity or total protein concentration of the blood.

[00140] The term “relative blood volume hydration status” refers to the relative change in the level of any target solute or solid material in the blood over a period of time. Non-limiting examples of target solute or solid materials include oxyhemoglobin, deoxyhemoglobin, hematocrit or red blood cell count, osmolarity or total protein concentration of the blood. Relative blood volume hydration status can be monitored by observation of a change in a signal responsive to the level of any target solute or solid material in the blood without a requirement that the absolute concentration of the target solute or solid material be determined.

[00141] The term “spent dialysate” refers to a dialysate that has been contacted with blood through a dialysis membrane and contains one or more impurity, or waste species, or waste substance, such as urea.

[00142] The term “sorberent cartridge” refers to a cartridge containing one or more sorberent materials for removing specific solutes from solution, such as urea.

[00143] The terms “treating” and “treatment” refer to the management and care of a patient having a pathology or condition by administration of one or more therapy contemplated by the present invention. Treating also includes administering one or more methods of the present invention or using any of the systems, devices or compositions of the present invention in the treatment of a patient. As used herein, “treatment” or “therapy” refers to both therapeutic treatment and prophylactic or preventative measures. “Treating” or “treatment” does not require complete alleviation of signs or symptoms, does not require a cure, and includes protocols having only a marginal or incomplete effect on a patient.

[00144] The term "ultrafiltration" refers to subjecting a fluid to filtration, where the filtered material is very small; typically, the fluid comprises colloidal, dissolved solutes or very fine solid materials, and the filter is a microporous, nanoporous, or semi-permeable medium. A typical medium is a membrane. During ultrafiltration, a “filtrate” or “ultrafiltrate” that passes through the filter medium is separated from a feed fluid. In general, when transport across a membrane is predominantly diffusive as a result of a concentration driving force, the process is described herein as dialysis. When transport is primarily convective as a result of bulk flow across the membrane induced by a pressure driving force, the process is ultrafiltration or hemofiltration depending on the need for substitution solution as the membrane passes small solutes but rejects macromolecules. The term “ultrafiltration” can also refer to the fluid removal from blood during a dialysis or a hemofiltration process. That is, ultrafiltration refers to the process of passing fluid through a selective membrane,

such as a dialysis or hemofiltration membrane, in either a dialysis, hemodiafiltration, or filtration process.

[00145] The term “void volume” refers to a specific volume that can be occupied by a fluid in a defined space such as a dialysate circuit of the invention including all components contained therein.

[00146] “Diffusive permeability” is a property of a membrane describing permeation by diffusion. Diffusion is the process of solutes moving from an area of higher concentration to an area of lower concentration

[00147] The term “porosity,” as used herein describes the fraction of open pore volume of a membrane.

[00148] The term “shunt,” as used herein describes a passage between channels, such as blood vessels, where the shunt diverts or permits flow from one pathway or region to another.

[00149] The term “plumbing,” as used herein generally describes any system of valves, conduits, channels, and lines for supplying any of the fluids used in the invention.

[00150] The term “extracorporeal,” as used herein means situated or occurring outside the body.

[00151] The term “effluent dialysate,” as used herein describes the discharge or outflow after the dialysate has been used for dialysis.

[00152] The term “metabolic waste species,” as used herein describes organic and inorganic components generated by a patient. They can be metabolic products such as urea, uric acid, creatinine, chlorides, inorganic sulfates and phosphate, or excess electrolytes such as sodium, potassium, *etc.* It will be understood that the specific “metabolic waste species” can vary between individuals depending on diet and environmental factors. Hence, the term

is intended to encompass any waste component that is normally removed by a kidney or by dialysis without restriction on the specific type of waste substance.

[00153] The term “working dialysate solution” refers to a dialysate solution that is undergoing active circulation or movement through a system including conduits, pathways, dialyzers and cartridges.

*Controlled Compliance Dialysis Circuit and Portable Dialysis System*

[00154] In the controlled compliance dialysis circuit disclosed herein, passive movement of fluid across the dialysis membrane due to operational pressure change is eliminated. The invention provides for the ability to accurately control net patient fluid status, and/or diffusion combined with increased clearance via convection, and/or active provisioning of extra fluid to a patient. The invention can actively provide fluid to the patient when the patient becomes hypotensive or hypovolemic, and replace a blood circuit with a physiological solution when a patient is taken off a system. The invention can also provide for adjusting convective clearance. Any combination of the above mentioned features is contemplated by the invention. The system allows for the return of blood from the system back to the patient without necessarily providing for additional fluids. The system can optionally account for an infusate volume, provide additional convective clearance, and/or provide control of the entire process. In contrast, non-expandable volume systems do not allow for ultrafiltration (UF), the ability to give fluid to the patient, convective clearance or return of blood to the patient without additional fluids. Instead of a fixed or non-compliant volume used in known systems, the present invention can intentionally change a volume to push fluid to or from the patient where the system controls volume and compliance (both of which are dynamic and changing) to achieve the desired goals of a therapy. The controlled compliance dialysis circuit also simplifies the entire system. Specifically, scales or gravimetric methods are not required to balance fluid removal with fluid replacement.

[00155] In certain embodiments, the controlled compliance dialysis circuit has two points where fluid can enter the dialysate flow path: 1) infusate pumps and 2) a control pump that controls the movement of fluid across the dialysis membrane. The controlled compliance dialysis circuit operates by employing two principle components: 1) an extracorporeal circuit that is attached to the vasculature and the circulation of a patient, and 2) a dialysis circuit having a limited void volume for the circulation of a dialysate. The extracorporeal circuit is an extension of the patient's circulatory system external to the patient's body. Any fluid added to the dialysate circuit can enter the patient's body; likewise, any fluid drawn out of the extracorporeal circuit can originate from the patient's body. Due to the connection between the extracorporeal circuit and the vascular system, there is freedom of movement for fluid to flow into and out of the extracorporeal circuit due to the relatively large volume of the patient's body to accommodate an influx of fluid or to serve as a reservoir of fluid.

[00156] The extracorporeal circuit is maintained such that a point of exit or entry of a significant fluid volume to the extracorporeal circuit, other than the patient's body, can be the movement of fluid across a dialysis membrane allowing for the diffusion of solutes between the patient's blood and the dialysate present in the dialysis circuit. A small volume of heparin or other anticoagulant can be added to the extracorporeal circuit to prevent clotting. The components of the dialysis circuit have a controlled compliant volume. Fluid is blocked from passively flowing from the extracorporeal circuit to the dialysis circuit due to the controlled compliant volume of the dialysis circuit. Fluid is prevented from passively flowing from the dialysis circuit to the extracorporeal circuit since such a movement of fluid will leave a vacuum in the dialysate circuit. Since the dialyzer can be a high-flux type there is some fluid flux back and forth across the dialyzer membrane due to the pressure differential on the blood and dialysate sides of the membrane. This is a localized

phenomenon due to the low pressure required to move solution across the membrane and is called backfiltration, however results in no net fluid gain or loss by the patient.

[00157] While the components forming the dialysis circuit have a controlled compliant volume, the dialysis circuit further incorporates a control pump that can be operated to selectively adjust the volume of the dialysis circuit. Specifically, the action of typical pumps functions by expanding or contracting a space. When the control pump is provided on the dialysate circuit, the volume of the dialysate circuit can be expanded or contracted in a controlled fashion allowing for the movement of fluid across the dialysis membrane to be actively controlled by the user or a programmed controller. The control pump allows for fluid to move from the dialysate circuit to the extracorporeal circuit without creating a vacuum, wherein the operation of the control pump is controlled. Likewise, the control pump allows for fluid to move from the extracorporeal circuit, and hence the patient's body via the action of the control pump by selectively expanding the volume of the dialysis circuit. Movement of fluid between the extracorporeal circuit and the dialysis circuit can be accurately controlled and metered.

[00158] In certain embodiments, a control pump used in the invention can be a peristaltic pump, a volumetric metering pump, diaphragm pump, or a syringe style pump. During operation, the volume of the dialysate circuit changes continually during the treatment even when the system does not push fluid back into the patient. This volume changes in a controlled way. One typical dialysis blood pump peristaltic segment is 8 mm wherein during one rotation of the pump, two rollers can move approximately 14 mL. Depending on the position of the roller with this segment, there is 0 mL to 7 mL difference in dialysate flow path volume with this pump segment. This pump description is for illustration purposes and is non-limiting. The amount of the stroke volume will be dependent on the specific pump segment and the length of the blood pump race. A syringe pump can also always have a

changing volume, as can a simple metering device such as a diaphragm flow meter. As the flow path volume changes, the volume will expand and contract based on the stroke of the pumps. This change can be controlled. Hence, the dialysate circuit has substantially a substantially inflexible volume except for controlled changes in volume modulated by the control pump, the infusion pump(s) and optionally a second control reservoir pump that reflect the changes in volume due to the position of the peristaltic roller, syringe plunger or meter diaphragm and whether the pump is run forward or in reverse. In another embodiment, the blood pump and dialysate pump can be run in-phase, or not run 180 degrees out-of-phase. In contrast, known systems run the blood pump and dialysate pump 180 degrees out-of-phase, *i.e.*, when the blood pump pumps, the dialysate is stopped and vice versa. However, because the amount of water crossing into the blood during the dialysate stroke must be removed during the blood pump stroke, there is a tendency for the blood to hemoconcentrate and violate the blood filtration fraction. The ultrafiltration rate cannot exceed the acceptable filtration fraction. Filtration fraction (FF) is defined as  $FF(\%) = (\text{Ultrafiltration Rate} \times 100) / \text{Plasma flow}$ . Plasma flow ( $Q_p$ ) is defined as  $Q_p = \text{Blood Flow Rate} \times (1 - \text{hematocrit})$ . The maximum ultrafiltration rate cannot be greater than plasma flow  $\times 30\%$ . The invention can also be programmed to have a physician prescribed maximum ultrafiltration rate which is lower than the filtration fraction derived maximum ultrafiltration rate. In the invention, the fluid flows, into and out of the circuits, are controlled so that the blood pump is running when the fluid is removed to avoid violation of the filtration fraction, and to avoid hemoconcentration for less clotting.

[00159] In certain embodiments, the invention contemplates a volume of dialysate less than about 1 L being conveyed through the dialysis system at any one time. In other embodiments, less than is 0.5 L is contemplated. Figure 1A shows a system for circulating blood and a dialysate through a dialyzer **130**. A shunt such as a needle or catheter is

connected to a patient's vasculature to draw blood and circulate the patient's blood through an extracorporeal circuit **140**. The portion of the extracorporeal circuit **140** that contains drawn blood from the patient can be referred to as the arterial line **610**, which by convention is understood to mean a line for transporting blood from the patient regardless of whether blood is drawn from an artery or vein of the patient. Similarly, the portion that returns blood to the patient can be referred to as the venous line **620**. In certain embodiments, the arterial line **610** and the venous line **620** connect with one or more veins of the patient. Locomotive power for moving the blood through the extracorporeal circuit **140** is provided by a blood pump **125**, which is typically located along the arterial **610** line. Blood is typically conveyed through the extracorporeal circuit **140** at a rate of 50 to 600 mL/min and can be adjusted by a controller to any required rate suitable for a procedure performed by the invention. Blood pump **125** can be a peristaltic pump, although those skilled in the art will readily understand that other types of pumps can be used including diaphragm pumps, centrifugal pumps, and shuttle pumps. In certain embodiments, the blood pump **125** conveys blood through the dialyzer **130** where the blood is contacted with a blood side of a high permeability dialysis membrane **135**. Blood enters the dialyzer **130** through a blood inlet **161** and exits through a blood outlet **162**. The pressure of the blood prior to the blood pump **125** is measured by a pressure meter **133** and post dialyzer **130** by a pressure meter **134**. The pressure at pressure meter **133** provides an indication of the adequacy of the blood flow into the circuit where increased vacuum is an indication of a less adequate access flow. The pressure indication at pressure meter **134** can serve to detect obstructions in the venous bloodline. An air trap **500** is placed along the extracorporeal circuit **140** to prevent the introduction of air into the circulatory system of the patient. The air trap **500** is not limited to a particular design. Typical air traps employ a hydrophobic membrane that allows air to be separated from an air-liquid mixture by allowing air to pass through the membrane and retaining water-based

fluids. Alternatively the air trap **500** can be run full, where a pressure meter can use a flexible impermeable membrane to transmit pressure pulses to a pressure transducer such that there is no direct air blood interface. Air-fluid detectors **201** and **202** are present to confirm that air is not present in the extracorporeal circuit **140**. Air fluid detectors **201** and **202** can be ultrasonic sensors that can detect a change in solution density or scattering due the presence of air or air bubbles.

[00160] During the course of conveyance of blood along the extracorporeal circuit **140**, heparin or other anticoagulant is added to the blood to prevent clotting of blood within the dialyzer **130** or blood conveyance pathway/extracorporeal circuit **140**. Heparin or another anticoagulant is added from an anticoagulant container **185** at a metered rate using an anticoagulant pump **186**. The anticoagulant pump **186** can be any pump capable of accurately metering heparin.

[00161] Dialysate within the system is conveyed through one of a first dialysate pathway **108** in the dialysate circuit, which carries dialysate to the dialyzer **130**, or a second bypass pathway **136** shown in a dashed line, which serves to bypass the dialyzer **130**. The first and second pathways **108** and **136** have one or more conduits for conveying the dialysate. Access to the second bypass pathway **136** is controlled by valve **150**. It is understood by one skilled in the art that three-way valve **150** can be replaced with a two-way valve with the same result to control the flow through the dialyzer **130** or bypass pathway **136**. The first dialysate pathway **108**, the second bypass pathway **136**, and residual volume in the dialyzer **130** including conduits for conveying the dialysate together form a dialysis circuit **141** that houses the circulating volume of the dialysate present in the system. It is understood by one skilled in the art that three-way valve **150** could be replaced with two-way valves with the same result to control the flow through the dialyzer or bypass loop.

[00162]       Dialysate that is conveyed through the dialyzer **130** on the dialysate side of the dialysis membrane **135** picks up waste products from the blood, including urea, by diffusion, hemofiltration or hemodiafiltration. Dialysate enters the dialyzer at a dialysate inlet end **194** and exits at an outlet end **196**. The dialysate exiting the dialyzer **130** passes through a blood leak detector **560** that can determine the presence of blood in the dialysate indicating a breach in the dialysis membrane **135**. Flow of dialysate from the dialyzer **130** can be stopped or controlled through the operation of valve **158** as well as to prevent the backup of dialysate into the dialyzer **130**. The dialysate is conveyed through a sorbent cartridge **102** to remove waste products before being re-conveyed through the dialyzer **130**. The dialysate enters the sorbent cartridge **102** at a dialysate inlet end **197** and exits at an outlet end **195**. An air trap **501** can be positioned before or after outlet end **195** to remove gasses introduced into the dialysate by the sorbent cartridge **102**. The volume of actively circulating dialysate is determined by the total void volume of the conduits and the sorbent cartridge **102** forming both the dialysis circuit **141**. The void volumes of the conduits and of the sorbent cartridge **102** forming the dialysis circuit **141** have a non-expandable or substantially inflexible volume.

[00163]       The total void volume of the conduits having a substantially inflexible volume prevents the passive inflow and outflow of fluid volume due to pressure changes that can occur over the course of treatment. This results in a benefit because not all of the pressure changes during treatment are under precise control by a user or operator. A controlled compliance dialysis circuit is achieved by actively controlling the inflow (influx) and outflow (efflux) of fluid to and from the dialysis circuit **141** and the extracorporeal circuit **140**. In this manner, the volume of fluid crossing the dialysate membrane **135** is under direct control and can be accurately determined. In certain embodiments, the dialysis circuit **141** has a void volume from about 0.15 L to about 0.5 L. In other embodiments, the dialysis circuit **141** has

a void volume from about 0.2 L to about 0.4 L or from 0.2 L to about 0.35 L. Other volumes can be envisioned by those of ordinary skill in the art depending on parameters such as patient weight, size, and health condition. The system can be designed to be a portable system, a desktop system or a large system suitable for heavy use in a clinical setting. Hence, both large volumes greater than 0.5 L to about 5L, and micro-volumes from as small as 0.1 L to about 0.5 L such as 0.1 L to 0.2 L, 0.1 L to 0.3 L, 0.1 L to 0.4 L, 0.2 L to 0.3 L, 0.3 L to 0.4 L, or 0.3 L to 0.5 L are contemplated by the invention.

[00164] The controlled compliance dialysis circuit can be accurately controlled to precisely remove or add fluid to the dialysis circuit. Due to the substantially inflexible void volume of the conduits, the sorbent cartridge **102** and other components of the dialysis circuit **141**, the net movement of fluid over any time interval across the dialysate membrane can be accurately controlled by creating a means to accurately introduce or remove fluid from the patient. This capability is used to enhance the convective clearance of the system while controlling the net fluid removed from the patient.

[00165] As shown in Figure 1, the dialysate is moved along the dialysis circuit **141** by a dialysate pump **138**. When the control pump **190** is not operating, fluid along the length of the dialysis circuit **141** flows at a rate determined by the dialysate pump **138**. When the control pump **190** is operating, fluid exiting the dialyzer **130** and traveling toward the conduit **191** is flowing at a rate that is the combination of the rates of the control pump **190** and the dialysate pump **138**. However, the fluid traveling from the entry point of conduit **191** into the dialysis circuit **141** to the dialyzer **130** is traveling at the rate of the dialysate pump **138**. As such, the rate of fluid traveling to the dialyzer **130** is not affected by the operation of the control pump **190**. The dialysate pump can be operated at a rate from about 10 to about 400 mL/min, the specific rate being dependent on the rate of the blood pump **125** at the desired contact time with the dialysis membrane **125** to achieve diffusion of impurities from blood to

the dialysate. The rate of the dialysate pump **138** and the blood pump **125** can be controlled by a controller **801** (shown in Figure 30).

[00166] Refreshed dialysate exiting an outlet end of the sorbent cartridge **102** can be monitored by a conductivity meter **104**. The design of any conductivity meter employed in embodiments described herein is not particularly limited; however, a typical conductivity meter has two electrodes where a current between the two electrodes is monitored. The presence of sodium ions in the dialysate is the major contributor to the conductivity measured by conductivity meter **104**. Conductivity is continually monitored and reported to the controller to assess the quality and safety of the dialysate. When the conductivity of the dialysate falls within a predetermined range, the dialysate is directed by valve **150** to a dialysate inlet end **194** of the dialyzer **130**; the valve **150** is located between an outlet end **195** of the sorbent cartridge **102** and the dialysate inlet end **194** of the dialyzer **130**. In certain embodiments, the valve **150** is a three-way valve. Optionally, the dialysate can be filtered through a microbial filter **512**. The pressure of the dialysate entering the dialysate inlet end of the dialyzer **130** is measured by a pressure meter **137**. In certain embodiments, the predetermined range for the conductivity of the dialysate is from about 12.6 to about 15.4 mS/cm.

[00167] When the conductivity measured by meter **104** is outside of the predetermined range, the valve **150** directs the dialysate to be conveyed through the second dialysis flow path **136** shown as a dashed line. Further, valve **158** can be closed to prevent the dialysate from backing up into the dialyzer **130**. As such, the dialysate can be circulated through the sorbent cartridge **102** while bypassing the dialyzer **130** and preventing contact with the patient's blood when required. Since the dialysis circuit **141** is isolated from the extracorporeal circuit **140** when valve **158** is closed, the control pump **190** is not operated when valve **158** is in a closed position during normal operation. When the system is being

primed, control pump **190** can operate to vent air from the dialysis circuit **141**, as described below.

[00168] Due to the substantially inflexible void volume of the conduits and the sorbent cartridge **102**, bulk fluid or water is prevented from moving across the membrane **135** from the extracorporeal circuit **140** of the dialyzer **130** to the dialysate circuit **141** of the dialyzer **130**. Specifically, due to the controlled compliant feature of the void volume of the dialysis circuit **141**, water cannot passively move from the extracorporeal side to the dialysate side through the dialysis membrane. In the event of factors that tend to increase pressure on the extracorporeal side of the dialysis membrane, such as increased blood flow rate or blood viscosity, pressure across the membrane will automatically be equalized due to the limited volume of the dialysis circuit **141** and the non-compressible nature of the dialysate. In the event of factors that tend to increase pressure on the dialysate side of the dialysis membrane **135**, such as increased dialysis flow rate, net movement of water from the dialysis circuit **141** to the extracorporeal circuit **140** is prevented by a vacuum that would form in the dialysate circuit **141** in the event of such a movement. Since the dialyzer can be a high flux type, there is some fluid flux back and forth across the dialyzer membrane due to the pressure differential on the blood and dialysate sides of the membrane. This is a localized phenomenon due to the low pressure required to move solution across the membrane and is called backfiltration, however results in no net fluid gain or loss by the patient.

[00169] Using the controlled compliance dialysis circuit described herein, net movement of water across the dialysis membrane occurs under active control rather than passively due to pressure differences that develop across the dialysis membrane due to normal operations. A control pump **190** is present and accesses the controlled compliance dialysis circuit **141** through a conduit **191**. In certain embodiments, the conduit **191** joins with the controlled compliance dialysis circuit **141** at a point downstream from the dialyzer

**130.** The control pump **190** can be operated in an influx direction that moves fluid from a control reservoir **192** to the controlled compliance dialysis circuit **141** or in an efflux direction that moves fluid from the controlled compliance dialysis circuit **141** into the control reservoir **192**. Due to the substantially inflexible volume of the dialysis circuit **141**, volume added to the controlled compliance dialysis circuit when the control pump **190** operates in the influx direction causes net movement of fluid from the dialysate side of the dialysis membrane **135** to the extracorporeal side of the dialysis membrane **135**. When the control pump **190** is operated in the efflux direction, fluid is drawn from the extracorporeal side of the dialysis membrane into the controlled compliance dialysis circuit. In certain embodiments, the control pump **190** can be operated at a rate from 0 to about 500 mL/min in either direction. In certain embodiments, the control pump **190** can be operated at a rate from 0 to about 200 mL/min in either direction. In certain other embodiments, the control pump **190** can be operated at a rate from 0 to about 100 mL/min or 0 to 50 mL/min in either direction. Any range from about 0 to about 200 mL/min is contemplated by the invention such as about 15 to about 185 mL/min, about 25 to about 175 mL/min, about 5 to about 75 mL/min, about 61 to about 183 mL/min, about 156 to about 193 mL/min, about 32 to about 63 mL/min, about 145 to about 199 mL/min, about 16 to about 93 mL/min or, about 29 to about 124 mL/min.

[00170] In embodiments where the control pump **190** is operated in the influx direction, the dialysate pump **138** operates at a rate higher than the control pump **190** to prevent flow of the used dialysate back into the dialyzer **130**. The dialysate pump **138** functions to convey the dialysate from the point where line **191** joins the dialysis circuit **141** to the sorbent cartridge **102**. A rate of the dialysate pump **138** operating faster than the control pump **191** in the influx direction ensures that the contents of the control reservoir **192** are conveyed to the sorbent cartridge **102** and do not reach the dialyzer **130** without first

passing through the sorbent cartridge. In certain embodiments, the dialysate pump **138** operates at a rate that is about 100 mL/min greater and at rates greater than the rate of the control pump **190**, when the control pump **190** is operating in the influx direction. For example, if the rate of the control pump **190** is 10 mL/min, the dialysate pump **138** can operate at rates greater than about 110 mL/min such as 130 mL/min, 175 mL/min, 210 mL/min, 510 mL/min, 760mL/min, 1L/min, and 1.6 L/min. If the rate of the control pump **190** is 25 mL/min, the dialysate pump **138** can operate at rates greater than about 125 mL/min such as 130 mL/min, 175 mL/min, 210mL/min, 510 mL/min, 760 mL/min, 1 L/min, and 1.6 L/min. In one embodiment, the dialysate pump **138** operates at a rate that is about 20 mL/min greater and at rates greater than the rate of the control pump **190** or higher, when the control pump **190** is operating in the influx direction. In other embodiments, the dialysate pump **138** operates at a rate that is about twice the rate and at rates greater than that of the control pump **190**, when the control pump **190** is operating in the influx direction. In certain embodiments, the dialysate pump **138** operates at a rate that is about 5% higher and at rates higher than the rate of the control pump **190**, when the control pump **190** is operating in the influx direction. For example, the dialysate pump **138** can operate at 6%, 7%, 8%, 10%, 15%, 45%, 63%, 75%, 100%, 200%, 500%, 2000%, or any higher percentage than the rate of the control pump **190**. The pump rates described herein are also applicable to the controlled compliance hemofiltration circuit **142** configured for use in a hemofiltration system as shown in Figure 1B.

[00171] The control reservoir **192** is not limited to any particular structure. In certain embodiments, the control reservoir **192** can be made from a flexible or collapsible material that expands depending on the volume held. In certain embodiments, the control reservoir **192** can be substantially inflexible. The control reservoir **192** can include a hydrophobic 0.2 micron ( $\mu\text{m}$ ) sterile, non-pyrogenic, and non-toxic air filter **300** to prevent the entry of

bacteria or endotoxin into the control reservoir **192** and dialysis circuit **141**. The air filter **300** also sterilizes air exhaust and intake from the control reservoir **192** into the system. Further, the air filter **300** can release air pressure present in the control reservoir **192**. The material of air filter **300** may be Millipore Dualex<sup>TM</sup> filter or an equivalent known to one of ordinary skill. In certain embodiments, the control reservoir **192** can have a valve that allows the patient or subject to empty the volume of the control reservoir **192** without interrupting treatment.

[00172] Several sensors and monitors can be employed to determine the state of the dialysis system, as shown in Figure 1A. Blood leaks across the dialysis membrane **135** can be detected by a blood leak detector **560**. The blood leak detector **560** can be an optical detector having a light source and photo detector allowing for the observation of a red color in the dialysate. The presence of air or fluid in the extracorporeal **140** and dialysis circuits **141** can be determined by air-fluid detectors **201**, **202**, and **203**, which can be ultrasonic sensors that can detect a change in solution density or scattering due to the presence of air or air bubbles. Conductivity meters **101**, **104** and **160** can be present to monitor the composition of the dialysate within the dialysis circuit. Pressure meters **133**, **134** and **137** can be present to determine unsafe operating pressure and/or fluid leak from the system. The pressure meter can be a transducer device that operates through capacitive or piezoelectric principles to convert the amount of force applied to a surface to an electronic signal.

#### *Controlled Compliance Hemofiltration Circuit for Hemofiltration System*

[00173] As described above, the controlled compliance dialysis circuit **141** is configured to control fluid flow through a dialysis membrane **135**. A controlled compliance hemofiltration circuit **142** is similarly configured for use in a hemofiltration system, as shown in Figure 1B. The controlled compliance hemofiltration circuit **142** has a flow path with a substantially inflexible volume between the ultrafiltrate outlet **198** of a hemofilter **199** and a

point of introduction of replacement fluid **155** into the extracorporeal circuit **140**. The conduits, sorbent cartridge **102** and other components for conveying fluid between ultrafiltrate outlet **198** and point of introduction of replacement fluid **155** into the extracorporeal circuit **140** have a substantially inflexible volume. A control pump **190** and a filtrate pump **139** can accurately control the removal of fluid and the introduction of a replacement fluid due to the controlled compliant properties of the hemofiltration circuit **142**.

[00174] In traditional hemofiltration systems, fluid is removed from the blood of a subject through the application of a negative pressure to a hemofilter to draw off an ultrafiltrate. Hemofiltration serves to remove waste species from the blood by convection or solute drag, which has greater effect in removing mid-weight and heavier waste species compared with dialysis methods. However, the human body on average contains about 5 L of blood volume. As such, it is necessary to balance the volume of fluid removed from the extracorporeal circuit **140** with a volume of replacement solution that is added to the extracorporeal circuit **140** to prevent concentration of the blood and hypovolemic episodes. In traditional systems, the replacement solution is separately prepared and infused into the extracorporeal circuit **140**, and the filtered volume and the infused/replacement volume is balanced by either gravimetric, volumetric or flow cell techniques to avoid rapid changes in blood volume and concentration while performing hemofiltration.

[00175] As shown in Figure 1B, the controlled compliance filtration circuit **142** eliminates the need for complicated gravimetric (*e.g.* scales) and volumetric equipment to balance the rate and volume of filtrate removal with the rate and volume of replacement fluid infusion into the extracorporeal circuit. In Figure 1B, an extracorporeal circuit **140** is provided having a similar configuration as the extracorporeal circuit **140** shown in Figure 1A, except the dialyzer **130** is replaced with a hemofilter **199** having a hemofiltration membrane

**200.** Blood enters the hemofilter **199** at a blood inlet **163** and exits at a blood outlet **164** while contacting one side of the hemofiltration membrane **200**.

[00176] Operation of a filtrate pump **139** generates a negative pressure at the ultrafiltrate outlet **198** of the hemofilter **199**. The extracorporeal circuit **142** can be pre-primed or filled with fluid prior to operation and the hemofiltration membrane **200** can be a high-flux type membrane, such that application of negative pressure to the ultrafiltrate outlet **198** does not result in the formation of a vacuum. Operation of the filtrate pump **139** at a specific rate will result in substantially the same rate of ultrafiltrate removal from the extracorporeal circuit **140** to the hemofiltration circuit **142**. The rate of ultrafiltration or flux of fluid across the hemofiltration membrane **200** can be precisely controlled due to the substantially inflexible volume of the hemofiltration circuit **142**. The ultrafiltrate is conveyed by the filtration pump **139** to a sorbent cartridge **102** that removes waste species, such as urea, from the ultrafiltrate as will be described in greater detail below. The sorbent cartridge **102** also removes electrolytes (*e.g.*  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ ,  $\text{K}^{+}$ ) found in the ultrafiltrate. An infusate pump **181** is used to add a cation infusate **180** into the hemofiltration circuit **142** to generate a fluid having a proper physiological composition to serve as a replacement fluid for introduction into the extracorporeal circuit **140**. A bicarbonate solution in a container **504** can further be added by a pump **505** to maintain a physiological pH in the fluid prior to introduction to the extracorporeal circuit as described below. The operation of the valve **150**, bypass pathway **136**, conductivity meters **102** and **160**, air trap **501** and other like elements sharing an element number with those elements found in Figure 1A have similar structure and operation to element features described elsewhere in this document.

[00177] As described, the filtrate pump **139** controls the rate and volume of ultrafiltration occurring during the hemofiltration treatment and further controls the rate of generated replacement fluid infused into the extracorporeal circuit **140**. Since the

replacement solution is generated from the filtrate, the rate of fluid removal and infusion of replacement infusion is substantially balanced without the use of scales and/or volumetric devices. However, it should be noted that operation of pumps **181** and **505** add a small volume to the replacement fluid for infusion.

[00178] It is also possible to perform ultrafiltration with net fluid removal from the patient through use of the control pump **190**. Where the filtrate pump **139** and the control pump **190** are used simultaneously, the combined rate of the filtrate pump **139** and the control pump **190** controls the rate of filtration or fluid removal from the extracorporeal circuit. For example, if the filtrate pump **139** is operated at a rate of 50 mL/min and the control pump **190** operates at 12 mL/min, then the rate of fluid removal at ultrafiltrate outlet **198** is 62 mL/min. The control pump **190** drains a portion of the total ultrafiltrate into a control reservoir **192** to be discarded later. The rate of the control pump **190** controls the net volume of fluid removed from the patient over the time course of treatment, since this removed fluid is not infused into the extracorporeal circuit **140** as replacement fluid.

[00179] In situations where the filtrate pump **139** and the control pump **190** are used simultaneously, the rate of conveyance of fluid to the sorbent cartridge **102** for treatment to generate a replacement fluid will be the rate of the filtrate pump **139**. It should be noted that the rate of the control pump **190** can be adjusted by a controller **801** to compensate for any volume addition by pumps **181** and **505**. In the example above where the filtrate pump **139** is operated at a rate of 50 mL/min and the control pump **190** operates at 12 mL/min, filtrate is removed from the subject at a rate of 62 mL/min and replacement fluid is added to the extracorporeal circuit **140** at a rate of 52 mL/min (assuming pumps **181** and **505** operate at 1 mL/min), where net fluid removal from the subject is 10 mL/min or 600 mL over an hour of treatment. One having skill in the art will be able to determine and understand the resultant effects of the rate of ultrafiltrate generation, rate of fluid replacement, and rate and net

amount of fluid removal caused by operating any of pumps **505**, **181**, **190**, and **139** at any specific rate.

[00180] The same rules for filtration fraction discussed above for the hemodialysis circuit **141** are applicable to the hemofiltration circuit **142**. It is desirable to limit the rate of filtration or fluid removal through ultrafiltration port **198** to avoid problems of hemoconcentration and blood clotting. The ultrafiltration rate should not exceed an acceptable filtration fraction. Filtration fraction (FF) is defined as  $FF(\%) = (\text{Ultrafiltration Rate} \times 100) / \text{Plasma flow}$ . Plasma flow ( $Q_p$ ) is defined as  $Q_p = \text{Blood Flow Rate} \times (1 - \text{hematocrit})$ . The maximum ultrafiltration rate cannot be greater than plasma flow  $\times 30\%$ .

[00181] For example, Figure 1B shows a system where hemofiltration occurs at a point prior the addition of replacement fluid at point **155**. If blood hematocrit is 30% and blood flow through the hemofilter **199** is 300 mL/min, then  $Q_p = 300 \text{ mL/min} \times (1 - 0.3) = 210 \text{ mL/min}$ . The maximum rate of ultrafiltration can then be set at 30% of  $Q_p$  or 63 mL/min. As such, the control pump **190** and the filtrate pump **139** should not be operated at a combined rate higher than 63 mL/min.

[00182] In an alternate embodiment, the replacement fluid can be added to the extracorporeal circuit **140** prior to the hemofilter **199**. The replacement solution can be added to the arterial line **610** of the extracorporeal circuit **140**. Under a scenario where hematocrit is 30% and blood flow rate is 300 mL/min, hematocrit will be reduced to 25.7% upon addition of the replacement fluid, where 50 mL/min of replacement solution is added to the blood flow. Where the total flow rate through the hemofilter **199** is 350 mL/min due to the addition of the replacement fluid,  $Q_p$  will be equal to  $350 \text{ mL/min} \times (1 - 0.257)$  or 260 mL/min  $Q_p$ , which allows for a maximum ultrafiltration rate of 78 mL/min under such a scenario. These examples are provided for illustrative purposes and are not limiting. One having skill

in the art can easily calculate  $Q_p$  for any combination of blood flow rate and hematocrit and set a maximum ultrafiltration rate accordingly.

*Ultrafiltration and Increased Convective Clearance*

[00183] With regard to the systems configured as shown in Figures 1A and 1B, the compliance control pump **190** is operated by a controller **801** that accurately accounts for the volume of fluid being removed from the circulation of the patient and/or being infused into the circulation of the patient. As described above, the control pump **190** controls the movement of fluid across the dialysis membrane **135** due to the controlled compliant volume of dialysis circuit **141** or together with the filtrate pump **139** for the hemofiltration circuit **142**. In the configurations shown in Figures 1A and 1B, operation of the control pump **190** controls the rate and amount of net removal of fluid from the subject during treatment. Many kidney failure patients can have fluid build-up that may be addressed by ultrafiltration, where bulk fluid is removed via the circulatory system. The control pump **190** can be accurately used to determine the precise volume of fluid removed from the patient. In addition to accurately controlling the net fluid removed and the convective clearance of a patient, accurate control of the efflux or influx of fluid via the control pump **190** allows for the amount of sodium removed ( $\text{mEq Na}^+$ ) during a course of treatment to be determined, where such result can be calculated and stored in the memory of a controller **801** and/or be displayed on a control panel (not shown).

[00184] In the dialysis system of Figure 1A, accurate control of bulk fluid movement across the dialysis membrane can further be used to enhance clearance of mid-weight impurities by convective clearance, which is particularly beneficial for mid-weight impurities such as  $\beta_2$ -microglobulin that are not removed very well by hemodialysis and for which higher serum blood levels are associated with higher patient mortality. To be able to control net patient fluid removal, any fluid removed in excess of the desired patient fluid loss must be

reinfused to the blood. This is accomplished in one embodiment by running a control pump in reverse during the treatment and then compensating by ultrafiltration (UF): Control Pump Control = Net patient UF + Convective UF. Control pump backfiltration is controlled to Convective UF volume. For example, a desired 200 mL net patient fluid loss per hour and 1000 ml of convection per hour requires a control pump running at a UF (efflux) rate of 1000 mL/hr and at a backfiltration (influx) rate of 800 mL/hr to achieve the net fluid loss and the desired convective clearance. These same mechanisms allow one to give fluid to the patient when necessary, return blood to the patient and control fluid removal accurately.

[00185] The rate of diffusion of a solute is dependent upon the molecular weight of that solute. Small molecules, such as urea, can effectively diffuse from the extracorporeal side of the dialysis membrane to the dialysate side of the dialysis membrane in the absence of net movement of fluid. However, larger, “mid-weight uremic impurities”, having a lower rate of diffusion may not be removed as effectively. As used herein, the term “mid-weight uremic impurities” refers to an impurity having a molecular weight less than about 66000 g/mol and greater than about 1000 g/mol and includes uremic toxins, B12, C reactive protein, and  $\beta$ 2-microglobulin.

[00186] During periods of net movement of fluid from the extracorporeal side to the dialysate side of the dialysis membrane **135**, solutes can be dragged across the dialysis membrane **135** along with the net movement of fluid. This process, referred to as convective clearance, removes mid-weight impurities from the patient’s blood, which are absorbed by the sorbent cartridge **102**. Some convective clearance occurs during the course of ultrafiltration as described above. However, the amount of convective clearance is limited by the volume of fluid that is removed by ultrafiltration. For example, if 1 L of fluid is to be removed from the patient over the course of a 4-hour treatment, then the amount of convective clearance that occurs due to 1 L of fluid crossing the dialysis membrane **135** is the

maximum amount of convective clearance that occurs during the treatment regimen. Without infusing the patient with additional fluid, the amount of fluid that can be removed is limited considering that the average individual has about 5 L of blood. Further, it may be desirable to achieve convective clearance without the removal of a large amount of fluid from the patient.

[00187] To achieve convective clearance in accordance with certain embodiments, the control pump **190** is operated in the efflux direction to pull fluid from the extracorporeal circuit **140**, and hence from the patient, across the dialysis membrane **135**. During the net efflux for fluid across the membrane **135**, mid-weight solutes and impurities are carried into the circulating dialysate where they can be absorbed by the sorbent cartridge **102**. The control pump **190** is periodically reversed to the influx direction to force fluid from the control reservoir **192** into the controlled compliance dialysis circuit and thereby force a corresponding volume of fluid into the extracorporeal circuit **140** and into the patient. During influx, fluid from control reservoir **192** is not returned to the dialyzer **130** and must first pass through the sorbent cartridge **102**. As discussed herein, pressures, rates, and control means are adjusted to ensure that used dialysate is not returned to the dialyzer **130** from the dialysate circuit **141**.

[00188] Under a regime where the control pump **190** is run in the efflux and influx directions for approximately equal amounts of time at the same pump rate, the amount of convective clearance will be approximately the efflux flow rate without causing any net addition or removal of fluid from the patient. For example, if the control pump **190** is run at 10 mL/min for a hour with periodic reversal between efflux and influx directions, then 300 mL of fluid is moved from the extracorporeal circuit into the controlled compliance dialysis circuit **141** to affect convective clearance where the same volume is returned to the patient resulting in no net fluid removal at the end of treatment. In the alternative, the time that the

control pump **190** is operated in the efflux or influx direction can be unequal to affect a net volume of ultrafiltration during the course of treatment. For example, if the control pump **190** is operated in the efflux direction for 18-second periods with intervening 12-second periods in the influx direction at a rate of 10 mL/min, then 360 mL/h of fluid is moved in the efflux direction to affect convective clearance and a net of 120 mL/h of fluid is removed from the patient. Those skilled in the art will understand that the interval at which the control pump **190** operates between efflux and influx directions can be modified to further effect the amount of convective clearance and net ultrafiltration occurring over the course of treatment.

[00189] The blood pump **125** and the dialysate pump **138** provide the majority of the energy to convey the blood through the extracorporeal circuit **140** and the dialysate through the controlled compliance dialysis circuit **141**, respectively. In certain embodiments, the blood pump and the dialysate pump can be independently operated at any rate in a range from about 50 mL/min to about 300 mL/min including from about 60 mL/min to about 295 mL/min. Other rates are contemplated, such as about 76 mL/min to about 185 mL/min, about 85 mL/min to about 287 mL/min, about 25 mL/min to about 115 mL/min, about 45 mL/min to about 273 mL/min, about 156 mL/min to about 293 mL/min, about 32 mL/min to about 163 mL/min, about 145 mL/min to about 199 mL/min, about 167 mL/min to about 193 mL/min or, about 29 mL/min to about 224 mL/min. In certain embodiments, the blood pump and/or the dialysate pump deliver a constant load pressure such that the conveyance rate is constant over at least short periods of times. Pumps that can deliver a constant load pressure include peristaltic pumps. The filtrate pump **139** can be operated at any of these rates as well.

[00190] The use of pulsatile pumps, that mimic the pulsing action of the human heart, has been proposed to enable convective clearance. As discussed herein, in known devices, the blood and the dialysate are conveyed by pulsatile pumps that are set 180 degree out of phase in order to achieve periodic filtering across the dialysis membrane. When the blood

pump is undergoing a pulse action and the dialysate pump is at rest, convective clearance can occur due to an increase in pressure difference across the dialysis membrane. Conversely, fluid is back filtered across the dialysis membrane when the dialysate pump is undergoing a pulse action and the blood pump is at rest. However, such systems have been subject to increased clotting. It is desirable to stop the administration of heparin or other anticoagulant 30 to 60 minutes prior to the end of dialysis to restore normal clotting by the time treatment ends. However, blood becomes significantly more viscous at low flow rates. In addition, protein coats the membrane surface, starting the clotting cascade. The periodic slow down of blood circulation caused by the action of a pulsatile pump contributes to clotting occurring in the extracorporeal circuit. Blood clotting prevents the completion of treatment.

[00191] In the invention, the method for performing convective clearance using pulsatile pumps requires the flow rate of the blood and the dialysate through the dialyzer to be similar to function properly. The pressure generated in the dialyzer on either side of the dialysis membrane is dependent upon the flow rate, where the flow rate of the dialysate and the blood should be close to achieve equal movements of fluid in both directions across the dialysis membrane. Specifically, the ratio of blood flow to dialysis flow has been recommended to be from 3:4 to 4:3 when employing pulsatile pumps to increase convective clearance. The use of pulsatile pumps to perform convective clearance also increases hemoconcentration, which increases the risk for blood clotting. As the flow rate of blood through a dialyzer is lowered relative to the flow rate of dialysate through the dialyzer, any particular volume of fluid pulled from the extracorporeal circuit during a unit value of time causes a greater amount of hemoconcentration. That is, the volume of fluid removed from the extracorporeal circuit is removed from a smaller volume of blood as the flow rate of blood is lowered. As described above, a ratio of blood flow to dialysis flow has been recommended to be from 3:4 to 4:3 when pulsatile pumps are used to create convective

clearance. Using the controlled compliance dialysis circuit described herein, the net flux of fluid across the dialysis membrane **135** is controlled by the control pump **190** rather than a ratio of flow rates between blood and dialysate. Hence, the ratio of blood flow to dialysate flow can be set at a value that reduces hemoconcentration as a result of pulling fluid from the extracorporeal circuit. In certain embodiments, the ratio of blood flow to dialysate flow through the dialyzer **130** is from about 1:1.5 to 3:1, and can include any range of ratios in between. In certain other embodiments, the rate of blood flow through the dialyzer **130** is at least about 50% greater than the rate of dialysate flow through the dialyzer **130**.

#### *Sodium and Cation Control*

[00192] As will be described in greater detail below, the sorbent cartridge acts as a cation exchanger to absorb ammonia ions and other cations (*e.g.*  $K^+$ ,  $Ca^{2+}$ , and  $Mg^{2+}$ ) and release sodium ions and hydrogen ions in a stoichiometric fashion. In certain embodiments, the dialysate cartridge passes dialysate entering an inlet end **197** of the sorbent cartridge through a flow path having a urease-containing material. The urease in the urease-containing material converts urea to ammonium ions and carbon dioxide. The ammonium ions created through the action of urease are absorbed by a zirconium phosphate material by cation exchange with sodium ions. In certain other embodiments, the sorbent cartridge contains an alternate flow path that allows at least part of the used dialysate from the dialyzer to pass through a mixed bed anion/cation exchange (mixed bed de-I) resin prior to entering the sorbent cartridge to control the concentration of sodium ions in the circulating dialysate. In any embodiment the zirconium phosphate may be replaced with magnesium phosphate.

[00193] Without adjustments, sodium ion concentration will increase to unsafe levels over the course of treatment due primarily to the function of the zirconium phosphate material. The normal constituents of the dialysate are  $Na^+$  from 137 to 142 mEq/L,  $K^+$  from 1 to 4 mEq/L,  $Ca^{2+}$  from 2 to 3 mEq/L,  $Mg^{2+}$  from 0.5 to 1 mEq/L and  $HCO_3^-$  from 32 to 40

mEq/L. There is also typically a small amount of acetic or citric acid and dextrose in the solution. Sodium ions ( $\text{Na}^+$ ) are the major ionic content of dialysis solution in the standard composition. Sodium is given off by the sorbent cartridge **102** as a result of the exchange of ammonium, carbonate, calcium, magnesium and potassium by the zirconium phosphate material of the sorbent cartridge **102**. To gain an estimate of the magnitude of sodium ions added to the dialysate over the course of a typical treatment, removal of 10 grams urea during a daily therapy would result in the subsequent exchange of ammonium for sodium equal to about 180 mEq of sodium. The further exchange of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^+$  for  $\text{Na}^+$  results in the production of about 240 mEq sodium. The sorbent cartridge **102** acts to remove urea by the conversion of the neutral urea molecule to ammonium ions that are removable by cation exchange. The generation and removal of ammonium ions causes the production of increasing amounts of  $\text{Na}^+$  ions as urea is removed from the dialysate.

[00194] The sorbent cartridge **102** functions to remove substantially all ammonium,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^+$  cations from the dialysate passing through the cartridge in exchange for  $\text{Na}^+$  and hydrogen ions. The concentration of cations  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^+$  is maintained at near the physiological concentration in the dialysate; therefore, the dialysis treatment does not have a significant effect on the concentration of these cations by dialysis across the dialysis membrane **138**. However,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^+$  must be replenished in the dialysate exiting the sorbent cartridge **102**, since the sorbent cartridge **102** removes these cations. Therefore, a concentrated cation solution is added to the dialysate from an infusate container **180** by means of a pump **181**. In certain embodiments, the pump **181** is operated at a constant rate to maintain stable amounts of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^+$ . The point at which the infusate (*i.e.* cation) solution is added to the dialysate can be between the sorbent cartridge **102** and the valve **150** in certain embodiments. It should be noted that since the amounts of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^+$

remain stable over the course of treatments, fluctuations in conductivity of the dialysate over the course of treatment is primarily attributable to changes in sodium ion concentration.

[00195] Some of the sodium ions produced by the sorbent cartridge **102** are removed by the control pump **190** operating to remove a net volume of fluid from the patient by means of the extracorporeal circuit **140**. Since the conductivity of the dialysate is monitored by conductivity meter **104**, the controller **801** operating the control pump **190** can calculate the amount of sodium ion removed with a net removal of fluid, since the conductivity contributed by other cations (*e.g.*  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{K}^{+}$ ) remains relatively constant during the course of treatment. For example, if the sodium ion concentration in the dialysate is at a normal physiological level, then each net liter removed by the control pump **190** removes **140** mEq of sodium ions. For a typical daily hemodialysis treatment, the average amount of ultrafiltration is 1 to 1.5 liters per session. In the controlled compliance hemofiltration circuit **142** shown in Figure 1B, the replacement fluid generated by the removal of waste species and impurities from the ultrafiltrate by sorbent cartridge **102** is directly infused to extracorporeal circuit **140** and the subject. Electrolytes are required to be infused into the replacement fluid prior to introduction to the extracorporeal circuit **140**. An infusate can be added by pump **181** as described above to generate a physiologically compatible infusate and/or valve **150** can be operated to bypass the replacement fluid through bypass pathway **136** as required if an unsafe conductivity is detected.

[00196] As required, the content and conductivity of the dialysate can be adjusted. This adjustment can occur without adding any volume of fluid to the dialysis circuit **141**. Figure 2 shows an apparatus sharing features with the apparatus of Figure 1A. In addition to the sorbent cartridge **102** that serves as a source of sodium ions from cation exchange, an optional deionization cartridge **210** can be placed in the dialysate flow path. The deionization cartridge **210** can be present to assist with the removal of sodium ions from the dialysate in

certain embodiments. In embodiments where the deionization cartridge is not present, sodium concentration in the dialysate can be reduced by operation of the control pump **190**, where fluid introduced into the dialysis circuit from the blood can act as a diluent. The deionization cartridge **210** has a mixed anion and cation de-ionization (mixed bed de-I) resin that is placed in series with the sorbent cartridge **102**. Dialysate that is circulated through the deionization cartridge **210** is outputted as substantially deionized purified water having low conductivity due to the action of the mixed anion/cation resins. Hence, the effluent from deionization cartridge **210** can act a diluent for sodium ion concentration in the dialysate.

[00197] A conductivity meter **101** can be present near deionization cartridge **210** for the purpose of controlling the setting of valve **212** for diverting at least a portion of the dialysate flow through deionization cartridge **210**. Alternatively, conductivity meter **104** and/or **160** can be used for determining the setting of valve **212**. When the conductivity measured by conductivity meters **101**, **104** and/or **160** is above a predetermined range, valve **212** is actuated to divert at least part of the dialysate flow through the deionized column prior to being passed to the sorbent cartridge **102**. The operation of the valve **212** is under control of the controller **801** monitoring the conductivity measured by conductivity meters **101**, **104** and/or **160**. If necessary, the valve **150** can be operated to divert dialysate flow through the second flow path **136** to protect the patient from an increase in dialysate conductivity. Flow through the deionization cartridge **210** is controlled in response to the conductivity of dialysate exiting the sorbent cartridge **102** and dialyzer **130**. When the conductivity of the dialysate is too high, the valve **212** is opened at least temporarily to divert at least a portion of the flow of dialysate through the deionization cartridge **210**. The mixed bed de-I resin removes the electrolytes, including sodium ions, and releases substantially deionized water that acts as a diluent in the system to control sodium ion concentration.

[00198] It should be noted that under treatment regimens where the control pump **190** removes a net amount of fluid from the dialysis circuit **141** through operation in the efflux direction, equivalents of  $\text{Na}^+$  are removed from the system. Operation of the control pump **190** in the efflux direction to remove a net amount of fluid also reduces the sodium level in the dialysate. Specifically, fluid moving from the blood across the dialysis membrane **135** into the dialysis circuit **141** acts as a diluent for  $\text{Na}^+$  concentration and conductivity. As described above, the controller **801** can calculate and monitor the removal of  $\text{Na}^+$  from the system. Hence, the deionization cartridge **210** is not the sole means for reducing the  $\text{Na}^+$  concentration and conductivity of the dialysate.

*Regeneration of Dialysate and Generation of Replacement Fluid*

[00199] The sorbent cartridge **102** acts to remove waste species and impurities in a similar manner for both the dialysis system of Figure 1A and the hemofiltration system of Figure 1B. For simplicity, the regeneration of a dialysate will be described where it is understood that the same principles apply to generation of a replacement fluid from a filtrate. The sorbent cartridge **102** removes impurity or waste species transferred to the dialysate in the dialyzer **130** prior to reuse as refreshed dialysate. Sorbent materials that can perform removal of waste products and regenerate the dialysate for use in the controlled compliance dialysis circuit **141** are known. Examples of useful sorbent materials include the REDY sorbent system and U.S. Patents 3,669,880; 3,989,622; 4,581,141; 4,460,555; 4,650,587; 3,850,835; 6,627,164; 6,818,196; and 7,566,432 and U.S. Patent Publications 2010/007838; 2010/0084330; and 2010/0078381 and International Patent Publication WO 2009/157877 A1, which are incorporated herein by reference. The sorbent cartridge **102** typically contains at least four different kinds of materials as follows: 1) a urease-containing material, where urease is an enzyme that catalyzes the conversion of urea to ammonium ions and carbon dioxide; 2) a zirconium phosphate (ZrP) material that has the capacity to act as a cation

exchanger by absorbing a large quantity of ammonium ions in exchange for sodium and hydrogen ions; 3) a zirconium oxide material (ZrO), which acts as an anion exchanger by exchanging phosphate for acetate; and 4) an activated carbon material that has a surface area for adsorption of wide range of impurities including metal ions and uremic toxins, such as uric acid, creatinine, and  $\beta$ 2-microglobulin. In some embodiments, the zirconium phosphate material can be replaced with a magnesium phosphate material.

[00200] In certain embodiments, the urease-containing material, the zirconium phosphate material, the zirconium oxide material, and the activated carbon material are arranged into discrete layers within the sorbent cartridge **102**. As will be described in more detail below, the various sorbent materials can be provided in separate housings or as discrete layers within such housings in certain embodiments. In certain embodiments, the urease-containing material and the zirconium phosphate material are intermixed in the same discrete layer within the sorbent cartridge **102**. The urease-containing material can be immobilized or covalently linked to a substrate material. The substrate material is not particularly limited, where suitable substrate materials include organic polymers, carbohydrate-based polymers, polyamides, polyesters, inorganic polymeric materials, chitosal and silica gel. The inclusion of the urease-containing material and the zirconium phosphate material in the same discrete layer can improve workability of the sorbent materials to prevent clogging of the sorbent cartridge **102** or improve absorption of ammonium ions by the zirconium phosphate material.

[00201] A typical sorbent cartridge **102** passes dialysate entering the cartridge **102** through the urease-containing material, the ZrP material, the ZrO material and the activated carbon material in that order. Some sorbent cartridges **102** can contain an additional activated carbon material that contacts the used dialysate prior to the urease-containing material to remove metal ions or fluorine ions that can damage the urease-containing

material. Still other sorbent cartridges **102** can contain more than one activated carbon layer including an activated carbon layer at the inlet and at the outlet of the sorbent cartridge.

[00202] Exemplary sorbent cartridges **102** are shown in Figures 3 and 4. The systems and controlled compliant dialysis circuit **141** disclosed herein are not particularly limited to the use of any particular sorbent cartridge. Figure 3A shows a sorbent cartridge having a conical-shaped body **235** in accordance with certain embodiments. The conical-shaped body **235** is desirable for imparting smooth flow characteristics for the used dialysate **230** entering the sorbent cartridge **102** and the regenerated effluent dialysate **250**. A urease-containing material **240**, a ZrP material **242**, a ZrO material **244** and an activated carbon material **246** are present inside the cartridge body **235**, as shown. Those skilled in the art will understand that various frits, baffles, and other internal elements can be present to support the sorbent materials, to compress the sorbent materials and to prevent the escape of fines.

[00203] Figure 3B shows an additional embodiment of a sorbent cartridge **102**. As shown in Figure 3B, the sorbent materials can be divided into five separate housings **210**, **256**, **257**, **258** and **259**. Housing **210** can serve as the deionization cartridge and contain a mixed bed de-I resin **255**. However, the use of a deionization cartridge is optional and can be omitted in certain embodiments. In such embodiments, housing **210** and valves **212** and **214** can be omitted from the sorbent cartridge **102** shown in Figure 3B. Housings **256**, **257**, **258** and **259** contain the urease-containing material **240**, the ZrP material **242**, the ZrO material **244**, and the activated carbon material **246**, respectively. As shown in Figure 3B, each housing **210**, **256**, **257**, **258** and **259** contains only one type of sorbent material. However, those skilled in the art will readily understand that more than one sorbent material can be present in any particular housing and that the number of housings can be reduced or increased, including the complete omission of a mixed bed de-I resin. Optionally, the sorbent cartridge **210** shown in Figure 3B can have a mechanism for dividing the used dialysate **230**

entering the sorbent cartridge between housing **256** and the deionization cartridge **210**. As described above, a conductivity meter **101**, **104** and/or **160** can control operation of a valve **212** that directs flow of the dialysate. Further, a valve **214** can be present to assist in controlling dialysate flow in addition to valve **212**. In Figure 2, effluent leaving deionization cartridge **210** is directed toward the sorbent cartridge **102**, where the effluent contacts all of the sorbent materials present in cartridge **102**. As shown in Figure 3B, the effluent from deionization cartridge **210** can be directed to bypass one or more of the sorbent housings **256**, **257**, **258** and **259**. Hence, the sorbent cartridge **102** can be designed to have two distinct flow paths for the conveyance of dialysate through the sorbent cartridge **102**.

[00204] Figure 3C shows a side view of one of the housings **210**, **256**, **257**, **258** and **259**. Each housing has a conical-shaped housing body **280**, but can be formed in any suitable shape having a variable or fixed cross section that is substantially circular, rectangular, or triangular. The sorbent material is placed inside the housing body **280** and held in place and/or compressed by a top frit **272** and a bottom frit **273**. The top of the housing body **280** is sealed with a top piece **270** that has an outlet port **278** for letting dialysate out of the housing body **280**. The bottom of the housing body **280** is sealed with a bottom piece **276** that has an inlet port **279** for letting dialysate into the housing body **280**. The housing body, bottom piece **276** and top piece **270** can have a notch **275** therein to facilitate the housing body **280** lying flush with the patient's body when worn.

[00205] Figure 3D shows a top view of the top piece **270** and the top frit **272**. Figure 3C shows a bottom view of the bottom piece **276** and the bottom frit **273**. The top frit **272** and the bottom frit **276** can be made out of sintered glass or an inert plastic material, such as polypropylene. The top frit **272** and the bottom frit **276** serve to compress the contents of the housing body **280** as well as to prevent the escape of fines.

[00206] Figure 4A shows a carrier **290** for organizing the individual sorbent housings **210**, **256**, **257**, **258** and **259**. The holder **290** has a plurality of arms **292** for holding the housings by compression arms. One of ordinary skill will understand that any other type of releasably fixing means known for holding the housings within the art is encompassed by the invention. Figure 4B shows a top view of carrier **290** having sorbent housings **210**, **256**, **257**, **258** and **259** placed therein.

[00207] Further shown in Figure 4C are housings **255**, **256**, **257**, **258** and **259** arranged with connecting tubing **295**. Keyed connectors **298** and **299** can be present to ensure that the sorbent cartridge **102** can only be incorporated into the dialysis circuit **141** in one orientation. As shown, fluid entering the sorbent cartridge is passed to either housing **256** having the urease-containing material or to housing/deionization cartridge **210** having the mixed bed de-I resin **255**. Fluid leaving the housing **210** can be passed to the housing **259** having the activated carbon material **246** via connecting tubing **295** or flow conduits fashioned by attaching two molded pieces forming a fluid path(s). Fluid leaving the housing **256** is passed through the remaining housings.

[00208] The zirconium oxide and zirconium phosphate materials, as well as the optional mixed bed de-I resin, remove substantially all of the  $Mg^{2+}$ ,  $Ca^{2+}$ , and  $K^{+}$  cations from the dialysate exiting the sorbent cartridge. Hence, a concentrated infusate solution of the relevant cations is added by an infusate pump **181** from an infusate reservoir **180** as shown in Fig. 5. Since the concentrations of  $Mg^{2+}$ ,  $Ca^{2+}$ , and  $K^{+}$  in the dialysate are desired to be near physiological levels, the concentration of such cations are not largely affected during kidney replacement therapy. In certain embodiments, the infusate solution can be added to the dialysate at a constant or near constant rate during treatment. The addition of the infusate pump **181** is under the control of a controller **801** and the rate of the infusate pump can be modified during treatment.

[00209] Due to the nature of the controlled compliance dialysis circuit, the volume of the infusate solution added by the infusate pump **181** drives the flux of the same volume of fluid from the dialysis circuit into the extracorporeal circuit **140**. The controller **801** that controls the control pump **190** operates at a rate that compensates for the fluid volume added by the infusate pump. For example, if the infusate pump **181** adds the infusate solution at a rate of 0.5 mL/min, then the control pump **190** will operate at an efflux rate of 0.5 mL/min in order to maintain a net zero flux of fluid exchange between the dialysis circuit and the extracorporeal circuit **140**. If, however, the system operates to remove 2 mL/min of fluid from the extracorporeal circuit, then the control will send instructions to the control pump **190** to operate at an efflux rate of 2.5 mL/min to compensate for the fluid volume being added by the infusate pump at a rate of 0.5 mL/min. The operation of the control pump **190** can be modified to adjust for any fluid volume being added by the infusate pump **181** in order to achieve a control flux of fluid between the dialysis circuit and the extracorporeal circuit.

#### *Control of pH*

[00210] Constant pH in the blood is maintained by the presence of bicarbonate which is equilibrated with CO<sub>2</sub> through the action of carbonic anhydrase. Systems employing a sorbent cartridge **102** have a tendency to induce mild acidosis, particularly toward the beginning of treatment, due to adsorption of bicarbonate by the sorbent cartridge **102**, where bicarbonate freely diffuses across the dialysis membrane. After the initial loss of bicarbonate to the sorbent cartridge, the sorbent cartridge will add bicarbonate to the dialysate due to hydrogen ion added to the dialysate in exchange for ammonium carbonate.

[00211] In certain embodiments, a bicarbonate cartridge containing sodium bicarbonate or another bicarbonate-containing salt can be provided within the system, where dialysate solution can be diverted through the bicarbonate cartridge as required. As shown in Figure 5, the bicarbonate cartridge **302** is present in the second bypass pathway **136** attached

to 3-way valve **150**, wherein a portion of the dialysate flow can bypass the dialyzer **130** and be passed through the bicarbonate cartridge **302**. The bicarbonate cartridge **302** can contain an amount of solid sodium bicarbonate or another bicarbonate-containing salt that is reconstituted to form a saturating solution during a priming cycle, as described below. Changing the state of the 3-way valve **150** will direct flow to the bicarbonate cartridge **302** to release bicarbonate into the system. Dialysate flow can be diverted through the bicarbonate cartridge **302** as needed to adjust the pH of the dialysate. Further, the bicarbonate cartridge **302** at the beginning of treatment can be used to preload the sorbent cartridge **102** so that the bicarbonate level will not significantly decrease at the beginning of treatment due to absorption of bicarbonate ions by the sorbent cartridge **102**. In certain other embodiments, the contents of the bicarbonate cartridge **302** is completely dissolved in the priming process rather than forming a saturated solution. The dissolved bicarbonate can then preload the sorbent cartridge **102** at the beginning of treatment to prevent an excessive drop in pH at the beginning of treatment.

[00212] In certain other embodiments, a bicarbonate containing solution can be added via a bicarbonate pump **505**, as shown in Figure 1A. In Figure 1A, a bag or container **504** containing sodium bicarbonate is attached to the system via a pump **505**. The bag or container **504** can contain a premeasured solid amount of sodium bicarbonate that is reconstituted during the priming process by running the pump **505** in reverse. Alternatively, a premade bicarbonate solution can be provided. Bicarbonate infusion is controlled by the pump **505** to maintain a constant and physiological pH in the system. Adjustment of pH using pump **505** is also shown for the hemofiltration system in Figure 1B.

[00213] Figures 6 and 7 show alternate embodiments for the location of the bicarbonate pump **505**. As shown in Figure 6, the pump **505** can be used to introduce bicarbonate into a side port of the sorbent cartridge **102**. Preferably, the bicarbonate solution

is introduced at a point after the zirconium phosphate and zirconium oxide materials. Bicarbonate ion can form insoluble salts in the presence of  $Mg^{2+}$  and  $Ca^{2+}$  ions. Therefore, pH may be more adequately controlled when added at a location where cations have been removed by action of the zirconium phosphate material, and  $Mg^{2+}$  and  $Ca^{2+}$  ions have not yet been infused into the dialysate. As shown in Figure 7, certain embodiments can have the pump **505** positioned to deliver bicarbonate ions to spent dialysate prior to entering the sorbent cartridge **102**.

[00214] The rate of addition of bicarbonate ions to the dialysis circuit **141** can be at a constant rate over the course of treatment in accordance with some embodiments. In certain embodiments, a pH meter can be located within the system to measure the pH of the dialysate within the dialysis circuit **141**, where a controller **801** monitoring the pH meter can make appropriate adjustment to the rate of bicarbonate addition to the dialysis circuit **141**. Since bicarbonate solutions are conductive, the pH meter may be replaced by a conductivity sensor. As will be described below, certain embodiments allow for the amount of urea absorbed by the sorbent cartridge **102** to be quantified by a controller **801**. In certain embodiments, the controller **801** can adjust the rate of bicarbonate addition to the dialysis circuit **141** based up the amount of urea calculated to be absorbed by the sorbent cartridge **102**, where there is no requirement for the pH of the dialysate to be directly measured.

#### *Priming of the Portable Kidney Replacement System*

[00215] The systems and methods described herein are designed for home use outside of a clinical setting with trained medical staff. Further, many users of kidney replacement therapy are in poor health and may have limited vision and manual dexterity due to disease or age. Since dialysis systems require preparation prior to use, set-up can be difficult for some patients. Further, the system has to be properly purged of air (*i.e.* primed) prior to use such that the various pumps function properly and to protect the patient from an air embolism. In

certain embodiments, the systems described herein can be primed and prepared for operation through the provision of only one fluid provided in a single container. This “one-fluid” priming feature is enabled by the nature of the controlled compliance dialysis circuit **141** and the ability to accurately control the movement of fluid between the extracorporeal circuit **140** and the dialysis circuit **141** due to the controlled compliance nature of the dialysis circuit **141**.

[00216] In certain embodiments, the systems described herein have quick connectors, such as luer connectors, that are large and operable with little force or dexterity. With reference to Figures 8 through 12, methods for priming the hemodialysis systems disclosed herein will be described. Reference numbers in Figures 8 through 12 equate to like elements in Figure 1A. Solid-lined areas in the extracorporeal circuit **140** or the dialysis circuit **141** refer to areas containing fluid (*e.g.* blood, saline, water, etc.) undergoing active flow or conveyance during a stage of priming the hemodialysis system with the direction of movement indicated by arrows. Dashed-line areas indicate areas in the extracorporeal circuit **140** or the dialysis circuit **141** containing air or a non-moving fluid during a stage of priming. Valves are shown as “bowtie-shaped” symbols, where closed valves are shaded and open valves are unshaded.

[00217] With reference to Figure 8, a single source of saline **400** can be attached to the extracorporeal circuit **140** to provide fluid to prime the system. The manner in which the saline **400** is attached to the extracorporeal circuit **140** is not particularly limiting. In certain embodiments, quick connectors located on the extracorporeal circuit **140** can incorporate spikes that can be used to puncture the saline container **400**, or quick connectors can be attachable to other luer adapters and tubing that lead to the saline container **400**. The same quick connectors can be used to attach to the shunt for accessing a patient’s vascular system.

[00218] In certain embodiments, the extracorporeal circuit **140** and the dialyzer **130** are provided sterile. After the saline container **400** is attached to the extracorporeal circuit **140**,

the first step in priming the system is to flush the extracorporeal circuit **140**, including the extracorporeal side of the dialyzer **130** with the saline solution. This is accomplished by running the blood pump **125** until all of the air is pushed out of the extracorporeal circuit **140**, as shown in Figure 8. The saline container **400** can contain from about 250 to 1000 mL of saline solution; however, the volume of saline provided is not limited to any particular amount. Saline or another priming fluid is circulated in the extracorporeal circuit **140** until there is no indication of air in the extracorporeal circuit **140** as indicated by air-fluid detectors **201** and **202**. Valves **158** and **150** are kept in a closed position that prevents saline for accessing the dialysis circuit **141**. The saline container **400** can be placed higher than the extracorporeal circuit **140** flow path such that hydrostatic pressure is provided in addition to the blood pump **125** and to facilitate the removal of air.

[00219] With reference to Figure 9, after the extracorporeal circuit **140** is free from air, the dialysis circuit **141** is primed. Valve **158** is placed in an open position allowing for flow from the dialyzer **130** to access the dialysis circuit **141**; valve **150** is kept in a closed position. The control pump **190** is run in an efflux direction to pull saline solution across the dialysis membrane **135**, into the portion of the dialysis circuit **141** shown in solid lines. Air from the dialysis circuit **141** is vented into the control reservoir **192**. Air-fluid detector **203** is located in the vicinity of the union of the dialysis circuit **141** and the control pump conduit **191**. The control pump **190** is operated in the efflux direction until air-fluid detector **203** indicates that air and bubbles are removed.

[00220] With reference to Figure 10, valves **158** and **150** are both placed in an open position to allow access to the dialysis circuit **141** after air is cleared from air-fluid detector **203**. The dialysate pump **138** is run to circulate the saline through the dialysis circuit **141**, where additional saline solution is pulled across the dialysis membrane **135**. During priming of the dialysis circuit **141** as shown in Figure 10, the control pump **190** is occasionally

operated to remove or vent air from the dialysis circuit **141** that is being displaced by saline solution. In certain embodiments, the control pump **190** is operated in the efflux direction whenever air is detected at air-fluid detector **203**. The three-way valve **150** is occasionally operated to direct saline flow through the second bypass pathway **136** to accomplish priming of the second bypass pathway **136**. Similarly, if an in-series deionization cartridge **210** is present (not shown in Fig. 10), then valve **212** can be opened intermittently to prime the deionization cartridge **210** and tubing associated therewith.

[00221] After air is removed from the dialysis circuit **141**, the saline solution can be used to reconstitute a bicarbonate salt and/or infusate salts containing  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$ , ions that can be provided in solid form. As shown in Figure 11, the bicarbonate pump **505** and the infusate pump **181** can be run in a “reverse” direction to drawn saline solution from the dialysis circuit **141** into the bicarbonate reservoir **504** and the infusate reservoir **180**, respectively. Pumps **505** and **181** can be used to meter a predetermined volume of saline solution into the bicarbonate reservoir **504** and the infusate reservoir **180**, respectively, such that the formed bicarbonate and infusion solutions have a known concentration.

[00222] Prior to readying the system for hemodialysis, the saline solution in the now primed system is to be modified to have an appropriate composition to serve as a dialysate. As shown in Figure 12, the infusate pump **505** and the bicarbonate pump **181** are run in their normal operating direction while the solution within the dialysate circuit **141** is circulated to adjust the cation (*e.g.*  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ ,  $\text{K}^{+}$ , etc.) concentration and the pH to form a functional dialysate. After the priming process is complete, the extracorporeal circuit **140** can be connected to the vasculature of the patient and treatment commenced. If the patient does not attach to the extracorporeal circuit **140** within a brief, predetermined period of time, the dialysate pump **138** can be stopped to prevent the consumption of zirconium phosphate within the sorbent cartridge **102** due to absorption of cations from the dialysate. In certain

embodiments, the dialysis circuit **141** can include a bypass around the sorbent cartridge in order to preserve the zirconium phosphate therein during priming.

[00223] The process to prime the system described in Figures 8 through 12 necessitates that the saline solution or other priming fluid used to prime the extracorporeal circuit **140** is introduced into the patient at the beginning of the treatment. With reference to Figures 13 through 15, a priming method having the advantages of requiring only one priming solution and avoiding introduction of the priming solution to the patient will be described.

[00224] The extracorporeal circuit **140** is attached to a saline container **400** and flushed with saline solution as described above in Figure 8. Optionally, the control pump **190** can be operated in the efflux direction to draw saline solution into a portion of the extracorporeal circuit as described in Figure 9. After flushing of the extracorporeal circuit **140** with saline solution, the saline container **400** is removed and the extracorporeal circuit **140** is attached to patient's vascular system, as shown in Figure **13**. Normally, all pumps within the system are stopped during the period when connections are made between the subject and the extracorporeal circuit **140** and valve **515** is placed in a closed position to prevent unpriming of the system.

[00225] During normal operation of the system to perform kidney replacement therapy, the blood and the dialysate are passed through the dialyzer **130** in opposite directions. The portion of the extracorporeal circuit **140** between the subject and the dialyzer **130** can be referred to as the arterial line **610** that carries blood from the patient to the dialyzer **130** during normal operation. The portion of the extracorporeal circuit **140** between the dialyzer **130** and the subject can be referred to as the venous line **620** that returns blood to the patient. Once the patient is connected to the extracorporeal circuit **140** and the extracorporeal circuit **140** is flush with saline, the dialysate pump **138** and the blood pump **125** are run at the same rate with valve **158** in the open position. As a result, blood is drawn

into the venous line **610** to the dialyzer **130** and the saline solution that was present in the venous line **610** is transferred to the dialysate circuit **141**, as shown in Figure 13. The valve **150** is kept in a position to direct flow through the second bypass pathway **136** to avoid pushing air into the dialyzer **130**.

[00226] At the time that blood fills the arterial line **610**, the blood pump **125** is turned off and the dialysate pump **138** and the control pump **190** are run to draw blood into the venous line **620**. Control pump **190** is run in the efflux direction to provide an outlet for air in the system. In certain embodiments, the control pump **190** can be run when air is detected at air-fluid detector **203**. As shown in Figure 14, the location of the stopped blood pump **125** in the arterial line **610** acts as a valve that prevents the passage of blood in either direction. Valve **515** is placed in an open position to allow blood to be drawn into the venous line **620** by action of the dialysate pump **138** and the control pump **190**. At the same time, the saline solution that was present in the venous line **620** is transferred to the dialysis circuit **141**. Valve **150** is kept in a position to direct flow through the bypass loop **136** to prevent contact or reintroduction of saline into the dialyzer **130** until conductivity is adjusted to a safe level. The bicarbonate pump **505** and the infusate pump **181** are run to adjust the composition of the fluid within the dialysis circuit **141**. When the dialysate composition is within an acceptable range, the valve **150** can be adjusted to allow flushing of the dialysis circuit **141** between the valve **150** and the dialyzer **130** with dialysate.

[00227] At the time that the extracorporeal circuit **140** is filled with blood, the entire volume of saline has been transferred from the extracorporeal circuit **140** to the dialysis circuit **141**. The volume of the dialysis circuit **141** is typically larger than the volume of the extracorporeal circuit **140**. In certain embodiments, the volume of the dialysate circuit **141** can be from about 100 mL to about 200 mL larger than the extracorporeal circuit **140**. To fill the remaining volume of the dialysate circuit **141** and complete the priming process, blood is

circulated through the extracorporeal circuit **140** through operation of the blood pump **125** and an anticoagulant is added to the blood from the container **185** by means of the anticoagulant pump **186**, as shown in Figure 15. In the event that the dialysis circuit **141** is not completely primed, the action of the dialysate pump **138** will draw fluid from the blood plasma into the dialysis circuit **141** by ultrafiltration across the dialysis membrane **135**. In certain embodiments, the dialysis pump **138** is slowed down to operate at a rate less than the rate of the blood pump **125**. In certain embodiments, the dialysis pump is run at a rate that is no more than about 66% of the rate of the blood pump **125**. Running at a lower rate, the dialysate pump **138** draws fluid volume from the extracorporeal circuit **140**, such fluid volume originating from the patient's blood, to fill the remaining volume of the dialysate circuit **141**. The volume of fluid removed from the extracorporeal circuit **140** can be calculated by a controller **801** and taken into account for quantifying the total volume of fluid removed from the patient over the course of treatment. When the system is fully primed, the control pump **190** can then be used to control the flux of fluid between the extracorporeal **140** and the dialysate circuits **141**.

[00228] As indicated above, the above-described priming operation has several benefits. The patient does not need to connect and disconnect a priming fluid source other than the saline container **400**. Further, the initial saline prime is not given to the patient. A controller **801** is able to account for the volume of fluid removed from the patient (*i.e.* from extracorporeal circuit **140**) needed to complete priming of the dialysis circuit and to incorporate such volume into fluid removal or addition calculations.

[00229] Figures 16 through 19 demonstrate a third alternative priming embodiment for the system. The dialysis circuit can include a pair of quick connectors **550** that are connected during normal operation to form the dialysis circuit **141** in a closed loop. The method illustrated by Figure 16 requires both a saline solution **400** and water or other aqueous fluid

present in container **630** (*e.g.* water with  $\text{NaHCO}_3$  and dilute  $\text{NaCl}$  solution) to be provided to prime the extracorporeal circuit **140** and the dialysis circuit **141**, respectively. As shown in Figure 16, the blood pump **125** is run to fill the extracorporeal circuit **140** including the extracorporeal side of the dialyzer **130** with saline and the dialysate pump **138** is run to fill the dialysis circuit **141** with the fluid from container **630**. The valve **150** is set to divert flow in the dialysate circuit **141** through the second bypass pathway **136**.

[00230] After the extracorporeal circuit **140** and the dialysate circuit **141**, except for the dialyzer **130**, are flushed with fluid, the bicarbonate pump **505** and the infusate pump **181** are run in a reverse direction to reconstitute a solid bicarbonate salt and solid infusate salts present in containers **504** and **180**, respectively. The operation of pumps **505** and **181** is illustrated in Figure 17. When the solid bicarbonate salt and the infusate salts are properly reconstituted, the bicarbonate pump **505** and the infusate pump **181** are run in their normal operating direction to adjust the composition of the priming fluid in the dialysis circuit **141**, as shown in Figure 18. After the composition of the dialysate is adjusted, the dialysis circuit side of the dialyzer **130** can be flushed with dialysate by operation of the valve **150**.

[00231] After the extracorporeal circuit **140** and the dialysis circuit **141** are flushed with fluid having the correct composition, all pumps are stopped and the extracorporeal circuit is connected to the patient and the system is ready for operation. Optionally, tap water can be used to prime the dialysis circuit **141**, where the action of the sorbent cartridge can remove impurity species from the tap water and the dialysis system can adjust the composition of the tap water to a composition suitable for use as a dialysate. The abilities of the described dialysis systems to adjust pH and electrolyte concentration in the dialysate can be used to prepare a dialysate from tap water used to prime the dialysis circuit **141**.

[00232] The extracorporeal circuit and the dialyzer are typically provided sterile to the patient/user, while the dialysis circuit **141** and the sorbent cartridge **102** do not typically need

to be provided sterile. Typically, the output of the sorbent cartridge in prior art sorbent systems meets the Association for the Advancement of Medical Instrumentation's (AAMI) Water for Hemodialysis standard but does not meet the AAMI standard for microbiologically ultrapure dialysate. It has been shown in the medical literature that ultrapure dialysate is desirable in reducing the inflammatory response in the ESRD patient. Desirable quality for ultrapure dialysate is less than about 0.1 colony forming unit (cfu)/mL where cfu is the number of viable cells per unit volume, and detectable endotoxins less than about 0.03 ELISA unit (EU/mL). In certain embodiments, the dialysate passing through the dialyzer **130** has low levels of both active bacteria and endotoxins. In one embodiment, a microbial filter **512** placed in the dialysis circuit **141** can be present to prevent bacteria and endotoxin from reaching the patient. Suitable filters include ultrafilters and microfilters manufactured or supplied by Minntech, Medica, Nikkiso, Pall Corporation or Millipore®, however any known by those of ordinary skill for the intended purpose can be used. Further, the sorbent cartridge **102** can include a spacer frit, which is a membrane or material that is designed to prevent fines from leaving the cartridge. After this spacer frit, an endotoxin or retentive membrane can be placed to prevent the passage of endotoxins and bacterial. Examples of an endotoxin or retentive membrane include quaternized amine charged surface membranes such as those manufactured or supplied by Pall Corporation (Ann Arbor, MI). Endotoxin levels can be measured using a qualified assay with limulus amebocyte lysate assay using blood from the horseshoe crab through guidelines promulgated by the U.S. Food and Drug Administration or dialysis standards such as AAMI/ANSI/ISO 23500 Guidance for the preparation and quality management of fluids for hemodialysis and related therapies.

[00233] Figures 20 through 22 demonstrate a fourth alternative priming embodiment. As shown in Figure 20, the dialysis circuit **141** has a deionization cartridge containing a mixed bed de-I resin **210**, where flow of fluid through the deionization cartridge **210** is

controllable by valve **212**. The dialysis circuit can include a pair of quick connectors **550** that are connected during normal operation to form the dialysis circuit **141** in a closed loop. The method illustrated by Figure 20 requires both a saline solution **400** and water or other aqueous fluid present in container **630** (*e.g.* water with  $\text{NaHCO}_3$  and dilute  $\text{NaCl}$  solution) to be provided to prime the extracorporeal circuit **140** and the dialysis circuit **141**, respectively. For some sorbents that can be present in the sorbent cartridge **102**, a weak saline solution in container **630** to maintain efficiency of the sorbents is desirable. If tap water is used for the fluid in container **630**, then an activated carbon layer should be present as the first layer at the inlet of the sorbent cartridge **102** to absorb any metals and fluoride ions present in the tap water. The urease enzyme can be deactivated by metals and fluorides. As shown in Figure 20, the blood pump **125** is run to fill the extracorporeal circuit **140** including the extracorporeal side of the dialyzer **130** with saline from container **400** and the dialysate pump **138** is run to fill the dialysis circuit **141** with fluid from container **630**. The valve **150** is set to divert flow in the dialysate circuit **141** through the bypass loop **136** during this stage of priming.

[00234] As shown in Figure 21, valve **212** is adjusted to allow the priming fluid from container **630** to fill and prime the mixed bed de-I cartridge **210** and associated tubing. Due to the action of the mixed bed de-I resin, fluid eluting from the cartridge **210** is substantially deionized. If the fluid from container **630** does not contain any substantial non-ionic impurities, then the fluid eluting from the mixed bed de-I cartridge **210** is substantially pure water. During this stage of the system priming, it is feasible to run the carbonate pump **181** and the infusate pump **505** in reverse to reconstitute the contents of the carbonate container **180** and the infusate container **504**, as previously described. At this stage, the bicarbonate salt and infusate salts can be reconstituted with the pure or deionized water eluting from deionization cartridge **210**.

[00235] In Figure 22, the valve **150** is adjusted to divert flow from the container **630** through the dialyzer **130**. Fluid is pumped through the dialyzer **130** by the dialysate pump **136** until all of the air is removed from the dialysis circuit **141** as indicated by air-fluid detector **203**. When air is indicated to be removed from the system, the pumps **125** and **138** will stop and the system will alert the patient or another individual. The quick connector **550** can be reconnected and the extracorporeal circuit **140** attached to the vasculature of a patient to begin treatment.

[00236] Figures 23 and 24 demonstrate priming of the system where a bicarbonate cartridge **302** is present in the dialyzer bypass loop **136**. The dialysis circuit **141** can include a pair of quick connectors **550** that are connected during normal operation to form the dialysis circuit **141** in a closed loop. The method illustrated in Figure 23 requires both a saline solution **400** and water or other aqueous fluid in container **630** (*e.g.* water with  $\text{NaHCO}_3$  and dilute  $\text{NaCl}$  solution) to be provided to prime the extracorporeal circuit **140** and the dialysis circuit **141**, respectively. For some sorbents that can be present in the sorbent cartridge **102**, a weak saline solution in container **630** is retained to maintain efficiency of the sorbents. If tap water is used for the fluid in container **630**, then an activated carbon layer should be present at the first layer at the inlet of the sorbent cartridge **102** to absorb any metals and fluoride ions present in the tap water. The urease enzyme can be deactivated by metals and fluorides. As shown in Figure 23, the blood pump **125** is run to fill the extracorporeal circuit **140** including the extracorporeal side of the dialyzer **130** with saline from container **400** and the dialysate pump **138** is run to fill the dialysis circuit **141** with fluid from container **630**. The valve **150** is set to divert flow in the dialysate circuit **141** through the bypass loop **136** during this stage of priming. The solid or powder bicarbonate salt will then dissolve in the fluid originating from container **630**. When using the priming embodiment shown in Figure 23, fluid passing through the bicarbonate cartridge **302** can

form a saturating bicarbonate solution that will be available for use after hemodialysis treatment begins. If a less than saturating amount of bicarbonate is present in the cartridge **302**, then the bicarbonate may be completely dissolved or excess powder may be lost to waste.

[00237] As shown in Figure 24, the quick connector **550** can be reconnected after the bicarbonate cartridge **302** is full. This act is done to prevent wasting the contents of the bicarbonate cartridge. Valve **150** is set to divert the flow through the dialysis circuit **141** through the dialyzer **130** and remove air there from. The control pump **190** can be operated in an efflux direct to vent remaining air from the system as necessary or detected by air-fluid sensor **203**. After air is removed from the extracorporeal circuit **140** and the dialysate circuit **141** as indicated by air-fluid sensors **201**, **202** and **203**, the infusate **505** and bicarbonate **181** pumps can be operated to adjust the composition of the fluid within the dialysis circuit **141**.

#### *Blood Return*

[00238] After priming of the system as described above, the system is used in normal operation to accomplish the removal of impurities from the blood. However, blood in the extracorporeal circuit is preferentially returned to the body of the patient prior to disconnection of the extracorporeal circuit from the patient. With reference to Figure 25, the return of blood to the patient at the end of treatment will be described.

[00239] The control pump **190** is run in the influx direction and the blood pump **125** is run in reverse at the same rate as the control pump **190**. Through this operation, blood is forced down the arterial line **610** to return blood to the patient, where dialysate moves across the dialysis membrane **135** to fill the arterial line **610**. An optical sensor **202** can be present to determine the presence of blood in the arterial line **610**. Such an optical sensor **202** can function by passing a beam of light through the line to determine the amount of absorption to determine the presence of blood.

[00240] After the arterial line **610** is cleared of blood, the blood pump **125** is stopped while the control pump **190** continues to run in the influx direction. Since fluid cannot pass through the stopped blood pump **125** that is present along the arterial line **610**, dialysate entering the extracorporeal circuit **140** pushes blood in the venous line **620** of the extracorporeal circuit **140** to return to the patient. In certain embodiments, an optical sensor **201** similar to the optical sensor present **202** on the arterial line **610** can determine if blood has been returned to the patient through the venous line **620**. In certain other embodiments, the control pump **190** is run for an appropriate amount of time to return the volume of blood in the venous line to the patient without relying on information provided from optical sensors **201** and/or **202**.

#### *Quantization of Urea Removal*

[00241] The blood of patients undergoing a regime of renal replacement therapy typically has blood chemistry determined by laboratory testing on a monthly basis to determine the effectiveness of treatment. Such testing is undertaken by a trained healthcare professional on a separate basis from the renal replacement therapy. Based upon lab results, various treatment metrics can be adjusted. For a patient utilizing the wearable sorbent system described herein without the aid of a healthcare professional, it is desirable to have a facility to determine the accuracy of treatment during therapy.

[00242] During treatment, the sorbent cartridge acts as a cation exchanger and releases sodium ions. The release of sodium by the sorbent cartridge has two principal sources:

1) Urea is converted to ammonium carbonate by the urease layer of the sorbent cartridge. The ammonium carbonate is exchanged to sodium and hydrogen in the zirconium phosphate layer(s) of the sorbent cartridge. The stoichiometry of the amount of sodium given off in this exchange is dependent on the processing of the zirconium phosphate layer; however, each process provides uniform results. Once the stoichiometry of ammonium/hydrogen/sodium

exchange is known, the amount of sodium released from the sorbent cartridge can be used to quantify the amount of ammonium ion absorbed. By means of example, a representative example of the zirconium phosphate can operate to exchange 1 mEq Ammonium for 0.15 mEq sodium and 0.85 mEq hydrogen. In this example, if the cartridge removed 20 grams of urea during a treatment, it would require that the zirconium phosphate remove 1400 mEq ammonium, which would produce about 210 mEq of sodium. Those skilled in the art will readily recognize that other zirconium phosphate materials having a different stoichiometry of ammonium/hydrogen/sodium exchange can also be used to calculate the amount of urea converted to ammonium ion and absorbed.

2) The dialysis solution contains electrolytes such as calcium ( $\text{Ca}^{2+}$ ), magnesium ( $\text{Mg}^{2+}$ ) and potassium ( $\text{K}^+$ ). These electrolytes remain in a stable range and close to constant in the dialysate during treatment. These electrolytes are totally removed from the spent dialysate by the sorbent cartridge. To ensure that there is a stable and correct concentration of electrolytes in the refreshed dialysate prior to reaching the dialyzer, zirconium phosphate exchanges these electrolytes with sodium. Then, the electrolytes are re-infused via an infusate pump to the correct concentrations. The amount of sodium produced from the zirconium phosphate layer due to this exchange is dependent on the dialysis solution flow rate, the time of treatment and the concentration values of these cations in the dialysis solution. For example, if the  $\text{Ca}^{2+}$  were 3 mEq, the  $\text{Mg}^{2+}$  1 mEq, and the  $\text{K}^+$  1 mEq, the sorbent cartridge would produce approximately 240 mEq of sodium at a 20 mL/min flow rate and a total volume of 48 liters through the cartridge.

[00243] Due to the near constant amounts of ( $\text{Ca}^{2+}$ ), magnesium ( $\text{Mg}^{2+}$ ) and potassium ( $\text{K}^+$ ) ions being exchanged by the sorbent cartridge, the conductivity difference between dialysate containing urea entering the sorbent cartridge compared with the refreshed dialysate exiting the sorbent cartridge can be used to quantify the amount of urea converted to

ammonium ions and absorbed by the sorbent cartridge. If the temperature and composition of an electrolyte solution are constant, the resulting conductivity of the solution is constant. At the ranges of typical dialysis solutions, any change in sodium concentration will result in a linear increase or decrease in dialysate conductivity. The table below shows the concentration and conductivity of a typical dialysis solution at 25°C. Even though sodium is not the only contributor to conductivity in dialysis solution, NaCl and NaHCO<sub>3</sub> make up approximately 94% of the conductivity of a typical dialysate solution.

[00244] Table 1: Composition of a typical dialysate solution and conductivity contributed by individual species.

| Substance               | mmol/L | mS/cm |
|-------------------------|--------|-------|
| NaCl                    | 103    | 10.68 |
| NaHCO <sub>3</sub>      | 34.0   | 2.47  |
| KCl                     | 2.00   | 0.26  |
| CaCl                    | 1.75   | 0.35  |
| MgCl                    | 0.50   | 0.09  |
| NaCH <sub>3</sub> COO   | 3.00   | 0.21  |
| Total Conductivity 25°C |        | 14.05 |

[00245] Sodium concentration increases in the dialysate due to the exchange of ammonium to sodium, which can be used to verify if the urea was removed during the course of treatment. As shown in Figure 26, conductivity meters **101**, **104** and **160** can be incorporated into the system at the inlet and outlet of the sorbent cartridge. In certain embodiments, a conductivity meter can be present within the sorbent cartridge at the outlet of the zirconium phosphate layer. A conductivity at the inlet of the sorbent cartridge **102** is measured at a location between the dialysate outlet **196** of the dialyzer **130** and the sorbent cartridge **102**. A conductivity at the outlet of the sorbent cartridge **102** is measured at a location between the sorbent cartridge **102** and the dialysate inlet **194** of the dialyzer **130**. A microprocessor or controller can monitor the conductivity measured by the conductivity meters to analyze the changes in conductivity brought about by the following:

- 1) Conversion of urease to ammonium carbonate and subsequent exchange of ammonium carbonate to sodium, and
- 2) Any net change in conductivity due to the exchange of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  into sodium, which can be treated as a constant value. The change due to removal of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  is known and the increase due to sodium is known. In the example dialysis solution of Table 1, the  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  contribute 0.7 mS/cm of conductivity.

[00246] The change in conductivity due to the loss of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  and the increase of sodium ions due to this exchange will be relatively constant during the treatment. From this information, a controller can then calculate the amount of conductivity increase due to the urea removal via the following sources:

Inlet Conductivity – Conductivity Contribution of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  = Starting Conductivity  
 Outlet Conductivity – Increase in Conductivity due to exchange of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  to  $\text{Na}^{+}$  = Corrected Outlet Conductivity  
 Corrected Outlet Conductivity - Starting Conductivity = Conductivity Increase due to Conversion of  $\text{NH}_4^{+}$  to  $\text{Na}^{+}$

[00247] The following example quantization is based upon 48 liters of regenerated dialysis solution used during the course of treatment having typical concentrations of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$ :

Inlet Conductivity = 14.04 mS/cm    Outlet Conductivity = 14.32 mS/cm

1. 14.05 mS/cm – 0.7 mS/cm = 13.35 mS/cm Starting Conductivity
2. 14.32 mS/cm – 0.5 mS/cm = 13.8 mS/cm Corrected Outlet Conductivity
3. 13.8 mS/cm – 13.35 mS/cm = 0.45 mS/cm Conductivity Increase due to Conversion of  $\text{NH}_4^{+}$  to  $\text{Na}^{+}$
4. 0.45 mS/cm / 0.1037 mS·L/mEq·cm = 4.34 mEq/L  $\text{Na}^{+}$  due to Urea Removal
5. 0.4 g urea per liter

[00248] In hemodialysis, urea removal depends on the diffusive gradient across the dialyzer membrane. This gradient will be much higher at the beginning of treatment than at the end of treatment when typically 50 to 60 percent of the patient's urea has been removed.

In certain embodiments, the conductivity values can be averaged so the curve of urea removal is understood and a continuous calculation need not be made. For example, conductivity can be sampled four or five times per treatment session for the purposes of quantifying urea removal. Early during a treatment session, a quantization of urea removal can be performed to verify that urea is being removed and that the  $\text{Na}^+$  increase is relatively high. Later, quantization measurements can be performed to calculate a curve for urea removal and to predict total expected urea removal based on this curve. Hence, the amount of urea removed during treatment can be either accurately measured or estimated with a high degree of certainty.

#### *Detection of Significant Clearance Problems*

[00249] The urea removal monitoring facility described above can be used to indicate the proper operation of the system and to alert the patient to significant problems that would interrupt the waste removal process. This problem could be communicated automatically via WiFi™, the internet, or other communication means to a doctor or healthcare professional. For instance, a patient with impaired blood access flow would have little urea removed. In instances where low urea removed is monitored toward the beginning of treatment, an alarm can be communicated indicating a potential malfunction.

[00250] Access to the patient's vasculature can fail due to a buildup of plaque in the access stent. This plaque creates a stenosis at the distal end of the anastomosis where the stent or graft is sutured to the vascular system of the patient. When this occurs, the blood tends to recirculate within the access area and there is a lack of adequate flow of fresh blood into the extracorporeal circuit, which can result in the same blood being repeatedly dialyzed. Since little blood entering the dialyzer is from the systemic circulation, there is less urea in the blood and hence less sodium is produced from the cartridge due to urea/ammonium to sodium exchange. The lack of an adequate increase in conductivity can be detected by the

system and an alert can be sent indicating a potential malfunction or problem accessing the patient's vascular system. This alert can indicate a lowered waste clearance, but the alert does not necessarily specify if the cause of the lowered waste clearance is due to a vascular access problem or due to a problem in dialysis flow, *etc.* A skilled medical professional can analyze the event to determine the cause of the alert in some embodiments.

#### *Detection of Zirconium Exhaustion*

[00251] After an extended period of use, the ability of the zirconium phosphate to adsorb urea can be exhausted. Exhaustion of zirconium phosphate leads to ammonium release into the dialysate, which can lead to ammonium intoxication in the patient. As discussed above, the exchange of urea/ammonium to sodium affects the output conductivity of the sorbent cartridge. Monitoring the inlet and outlet conductivities of the cartridge thus provides a method to detect ammonium breakthrough in the sorbent cartridge. An equilibration of the sorbent cartridge inlet conductivity with the output conductivity over a short time period indicates that the zirconium phosphate layer within the sorbent cartridge is exhausted. In certain embodiments, the conductivities pre- and post-sorbent cartridge are monitored. If an increase in sodium concentration is not detected by the controller, then the system will send an alert and prevent the dialysate from reaching the dialyzer, thus protecting the patient from ammonia intoxication.

#### *Detection of Patient Hydration Status*

[00252] The portable dialysis described herein can be used to perform ultrafiltration on a patient. During ultrafiltration, fluid is drawn out from the serum of the blood in the extracorporeal circuit through the dialysis membrane **135** by means of the control pump **190** as shown in Fig. 1A. Fluid removed by the control pump **190** is removed to the control reservoir **192**. Ultrafiltration can be performed alone or in conjunction with convective clearance, as described above.

[00253] Patients having kidney failure may have an undesirable accumulation of fluid in body tissues that is called edema. As fluid (*e.g.* water) is removed from the patient's plasma, the volume of the patient's plasma is replaced by infusion of fluid from the patient's tissues. That is, the portable dialysis system does not directly access fluids stored in the patient generally but only directly accesses the patient's vascular system. Humans typically only have 5 to 6 L of plasma volume at any one time, where a significant time lapse can be required for plasma volume to be replaced by transfer to fluid from surrounding tissues.

[00254] During ultrafiltration, fluid can be removed too rapidly resulting in the patient becoming hypovolemic, which can cause several serious effects including hypotension, cramping, nausea and vomiting. To avoid instances of hemoconcentration due to excessive fluid removal, the rate of ultrafiltration is limited to a percentage of the blood flow through the extracorporeal circuit **140**. In certain embodiments, the rate of ultrafiltration is limited to be no greater than about 30% of the plasma flow through the extracorporeal circuit **140**. Plasma flow ( $Q_p$ ) is defined as  $Q_p = \text{Blood flow rate} \times (1 - \text{hematocrit})$ , where blood flow rate is in units of volume divided by time (*e.g.* mL/min) and hematocrit is the unitless fraction of blood volume occupied by red blood cells. For example, if the blood flow rate is 60 mL/min and the hematocrit is 40%, then the maximum rate of ultrafiltration is set to be equal to about 10.8 mL/min or less.

[00255] The portable dialysis system can have a hematocrit detector to determine the hematocrit of blood containing within the extracorporeal circuit **140** of Fig. 1A. In certain embodiments, the hematocrit detector is a light source and a photodetector, wherein light emanating from the light source is passed through the blood in the extracorporeal circuit **140** and detected by the photodetector. The absorption of one or more wavelengths of light can indicate the level of hematocrit in blood entering the dialyzer **130** in the arterial line **610**. In certain embodiments, the hematocrit detector gives an indication if the hematocrit trend is

unsafe rather than giving a precise numerical quantification. In certain additional embodiments, the hematocrit detector can also determine if blood is present in the extracorporeal circuit **140**, which can be useful during the processes of priming the system or returning blood to the patient as described above. A simple optical detector with a light source and a photodetector can also be used to detect whether there is blood in the system.

[00256] In most renal diseases, the kidneys fail to produce erythropoietin, a hormone that stimulates red blood cell production. Most ESRD patients take an erythropoietin stimulation drug to help produce red blood cells. These drugs are dosed to maintain a pre-treatment serum hematocrit of 32%. During the course of the dialysis treatment, the hematocrit can change due to the removal of fluid from the blood. Hematocrit level changes over the course of the treatment are an indication of relative blood volume changes over treatment. Fluid removal by ultrafiltration removes fluid from the blood plasma; however, red blood cells are left in the circulatory system. Depending on the rate of vascular fluid refilling from the tissues, the hematocrit will increase or decrease. A flat hematocrit indicates that the patient is most likely fluid overloaded even at the end of therapy. A steep increase in the slope of the hematocrit during fluid removal may portend a hypovolemic event prior to initiating a hypotensive episode. A gradual increase in hematocrit during the course of treatment is most likely indicative of a well-dialyzed patient.

[00257] Hematocrit level is proportional to hemoglobin concentration. Therefore, any suitable sensor can be used to measure hemoglobin concentration, such as sensors used in pulse oximeters which measure adsorption of red and infrared light to determine concentration of oxygenated hemoglobin and deoxyhemoglobin, respectfully. The hematocrit/hemoglobin sensors, which may include the associated light source(s), can be placed in any suitable location. Placement of the hematocrit/hemoglobin sensor along the arterial line **610** of the extracorporeal circuit **140** will indicate the status of blood volume

within the circulation of the patient. Placement of the hematocrit/hemoglobin sensor along the venous line **620** of the extracorporeal circuit **140** will indicate the extent of hemoconcentration occurring within the dialyzer **130**. Measurement of hematocrit within the arterial line **610** can be used to calculate  $Q_p$  as described above. Other optical based technologies that can determine the relative blood volume changes during the course of treatment can also be used to determine hydration status of the patient and whether the appropriate amount of fluid has been removed

[00258] Figure 27 shows a schematic for a hematocrit/hemoglobin/relative blood volume sensor. A light source **713** of appropriate wavelength (red or infrared) is positioned on one side of the tubing of extracorporeal circuit **140** such that the light passing through tubing hits detector **715**. More light is absorbed (and less hits the detector **715**) if a higher concentration of hemoglobin is present in the extracorporeal circuit **140**. A lead **712** carries power and other electrical signals, if appropriate, to the light source **713** from the sensor device body **711**, which may contain the power source and other control or detecting electronics. Lead **717** carries electrical signals from detector **715** to the components housed in sensor device body **711**. Suitable hematocrit sensors are known, such as a CRIT-LINE monitor from HEMAMETRICS (see, HEMAMETRICS, CRIT-LINE hematocrit accuracy, Vol. 1, Techn Note No. 11 (Rev. D) February 24, 2003).

[00259] In other embodiments, hemoconcentration and blood hydration status can be detected and monitored by a relative blood volume monitor. The relative blood volume monitor can detect a change in the concentration of measured solute, solid material or group of solutes and solid materials in the blood that are too large to cross the dialysis **135** or hemofiltration **200**, which indicates a change in blood volume. The volume of blood typically is not measured by the relative blood volume monitor. The relative blood volume monitor measures the change in water content of the blood over the course of treatment, as

implicated by a change in solute concentration, and does not require an absolute quantization of any particular solute in the blood. The relative blood volume monitor determines the relative blood volume hydration status (RBVHS) of the subject by measuring the level of one or more blood solutes or solid materials at a time close to the beginning of treatment, which can be assigned a value  $C_0$ . The level of the one or more blood solutes does not require an absolute quantification; rather the level of the one or more blood solutes or solid materials can be reported as the magnitude of a signal generated by the relative blood volume monitor. The level of the one or more solutes is measured periodically at a second later time, which can be assigned a value  $C_t$ . The relative blood volume hydration status can then be determined by the formula  $RBVHS = C_0/C_t$ .

[00260] In certain embodiments, the relative blood volume monitor is a hematocrit sensor and the one or more solutes measured by the relative blood volume monitor are oxygenated or deoxygenated hemoglobin. In certain other embodiments, the relative blood volume monitor is a device that measures the velocity of ultrasonic sound waves in the blood. Ultrasonic sound waves are defined as sound waves having a frequency above 20,000 Hz. The velocity of ultrasonic sound waves in blood is an indication of the total protein concentration in the blood.

[00261] The relative blood volume hydration status can be used in the same manner as hematocrit, described above, to determine the effectiveness of ultrafiltration. It is important to note that when using relative blood volume the trend slope is inverse to the trend slope when using a hematocrit sensor, i.e. as hematocrit increases, relative blood volume decreases. A flat relative blood volume hydration status indicates that the patient is most likely fluid overloaded even at the end of therapy. A steep decrease in the slope of the relative blood volume hydration status during fluid removal can portend a hypovolemic event prior to initiating a hypotensive episode. A gradual decrease in relative blood volume

hydration status during the course of treatment is most likely a well-dialyzed patient. In certain further embodiments, the relative blood volume hydration status determined by the relative blood volume monitor can be correlated to a fluid volume of the blood.

[00262] In the event that an unsafe level of hydration status is indicated by hematocrit level or by relative hydration status, a controller **801** associated with the system can stop the fluid removal and alert the patient. Controller **801** can be programmed to remove fluid via a gradual slope down in relative blood volume or up when monitoring hematocrit. Additionally, the controlled compliant nature of the dialysis circuit can be used to administer a bolus transfer of fluid to the patient. As described above, operation of the control pump **190** in the influx direction will cause a transfer of fluid volume from the control reservoir **191** to the extracorporeal circuit **140**. The system can be preprogrammed to transfer a certain bolus volume to the patient upon detection of an unsafe trend in hematocrit or relative blood volume hydration status.

[00263] In certain embodiments, the control reservoir **191** is empty at the beginning of a treatment session wherein volume enters the control reservoir during treatment including ultrafiltration. As such, a bolus infusion in response to trend in hematocrit or relative blood volume hydration status is a return of fluid volume removed from the patient during treatment back to the patient. Any volume returned to the patient from the control reservoir **191** is cleaned by the sorbent cartridge **102** prior to introduction to the extracorporeal circuit **140**. However, in other embodiments the control reservoir **191** can contain a volume of fluid at the beginning of treatment that can be used for a net infusion of fluid into the patient during the course of treatment.

[00264] Hypovolemia can further be guarded against by simultaneously monitoring body fluid level of the patient undergoing hemodialysis treatment. The amount of fluid stored in body tissues outside the blood is proportional to the impedance that can be

measured from the patient's body. As depicted in Fig. 28, impedance can be monitored between two electrodes **703** and **705** that are attached to the torso **10** of a human patient. The electrodes **703** and **705** are operably coupled to control and processing electronics **701** via leads. The electronics **701** are configured to generate a voltage differential between the electrodes **703** and **705**, and current can be measured and impedance calculated. The measurement can be done in either DC or AC mode. Impedance or phase angle can be correlated to tissue fluid volume. Suitable external impedance monitors **700** and components that can be used in accordance with the teachings described herein are known. In certain other embodiments, electrodes **703** and **705** can be implanted within the patient.

[00265] One example of a well studied system that can be used or modified for use herein is Medtronic, Inc.'s OptiVol® fluid status monitoring system. Such a system, or other similar systems, have well-documented procedures for determining acceptable ranges of tissue impedance and thus fluid volume. *See, e.g.,* Siegenthaler, et al. Journal of Clinical Monitoring and Computing (2010): 24:449-451, and Wang, Am. J. Cardiology, 99(Suppl):3G-1-G, May 21, 2007. Alternatively or in addition, tissue impedance can be monitored for a suitable period of time to establish a suitable baseline, and patient markers can be used to instruct whether the patient is fluid overloaded or under-loaded. The data acquired by impedance sensor and input data regarding fluid status of the patient at the time the sensor data is acquired may be used to establish suitable ranges for impedance values.

[00266] One or more controllers **801** associated with the hemodialysis system can monitor the hematocrit/relative blood volume hydration status and impedance/body fluid level of the patient undergoing hemodialysis treatment. A typical hematocrit level for a dialysis patient is about 32%. Prior to a treatment session, the fluid volume of blood of a kidney disease patient can be elevated, thus hematocrit levels can be lower than desired. The one or more controllers **801** monitoring hematocrit levels can adjust the rate of fluid removal

or end ultrafiltration treatment when hematocrit level reaches the desired, predetermined range.

[00267] Fluid within a person's body is capable of moving from the body tissue to the blood and vice versa. As such, proper fluid levels in a patient can be described in terms of a ratio of tissue fluid to blood volume, as measured by hematocrit level. Hematocrit level of body fluid level can be monitored independently as described above. In general, blood is about 7% of body weight and total tissue fluid is about 60% of the body weight (including blood, extracellular and intracellular fluid). As such, a typical tissue fluid to blood fluid volume ratio of a healthy individual is in the range from about 6:1 to about 9:1 or can be in a range from 5:1 to 9:1. A measured ratio above this range indicates that blood is being withdrawn too quickly to allow for adequate equilibration of fluid between the blood and tissues of the patient. Fluid removal can be modified, stopped, or a fluid bolus administered as appropriate and preprogrammed into the one or more controllers **801** of the hemodialysis system.

#### *Detection of Needle or Catheter Disconnection*

[00268] It is well established in the art that pressure is not always a reliable means to detect separations of the venous blood return from the access of the patient. If this event occurs there is the risk of a life threatening blood loss and possible exsanguination. A conductive mat or holder can be used to detect blood leaks to the controller. The controller can then take the appropriate means to protect the patient by stopping the blood pump and alerting the patient. Other means to detect needle or catheter disconnections can be incorporated into the system such as monitoring of the impedance through the two needles or using pressure pulses.

*Infusate Control*

[00269] As discussed above, a bicarbonate buffer can be added to the dialysate circuit **141** to maintain physiological pH and an infusate container can add cations to replace necessary electrolytes removed by the sorbent cartridge **102**. In some embodiments, the second reservoir is a water reservoir **173** and the second reservoir pump is a water pump **174** that can also be present for adding water, tap water or purified water to the dialysis circuit **141** (or hemofiltration circuit **142**) as necessary, as shown in Figure 29. For example, water can be added as a diluent as needed to dilute conductivity and sodium ion concentration if other methods to reduce sodium ion concentration are unsatisfactory. The addition of water as a diluent can be particularly appropriate when it is necessary to divert dialysate and/or filtrate through the bypass pathway **136** due to conductivity being outside an acceptable range. Alternatively, reservoir **173** can contain a solution having a compatible physiological composition to be used as a dialysate or replacement fluid that can be added to the dialysis circuit **141** and/or hemofiltration circuit **174** as needed. Those skilled in the art will recognize that the inclusion of water reservoir **173** and pump **174** are optional and that container **173** and pump **174** can be included with any embodiment of a hemodialysis or hemofiltration system described herein. Conductivity of the ultrafiltrate or replacement fluid in hemofiltration circuit **142** can be monitored by conductivity meters **104** and **160** as described. As shown in Figure 29, water can be added by a pump **174** at a position after the sorbent cartridge **102**; however, those skilled in the art will recognize that water can be added to the dialysis circuit **141** and/or hemofiltration circuit **174** at any convenient location, and more particularly prior to the sorbent cartridge wherein such placement could be safer from a risk standpoint due to the possible risk of hemolysis.

*Water Reservoir for Control of Convective Clearance*

[00270] As described above, the water reservoir **173** and pump **174** can be present in any embodiment of the systems described herein, including the systems of Figure 1A and B. As described above, the control pump **190** can be operated in a bidirectional fashion to assist in the performance of convective clearance. Specifically, the control pump can be operated in the efflux direction to cause the movement of fluid from the extracorporeal circuit **140** into the dialysis circuit **141** and in the influx direction to cause the movement of fluid from the dialysis circuit **141** into the extracorporeal circuit **141**.

[00271] In certain embodiments, operation of the control pump **190** in the influx direction can be substituted with operation of the pump **174** to drive liquid from the reservoir **173** into the dialysis circuit **141** and subsequently cause movement of fluid from the dialysis circuit **141** to the extracorporeal circuit across the dialysis membrane **135**. The control pump **190** can be used for the movement of fluid in the opposite direction across the dialysis membrane **135**. The pump **174** and reservoir **173** is used for the performance of convective clearance in embodiments of the invention where the total void volume of the dialysis circuit and working dialysate is less than about 0.5 L, or in embodiments where the void volume of the dialysis circuit and working dialysate is less than 1 L.

[00272] In certain embodiments, the volume of fluid held by reservoir **173** is about 1 L or less, or about 0.5 L or less. In certain embodiments, the volume of the fluid held by the reservoir is from about 0.1 L to about 1 L, from about 0.2 L to about 0.8 L, from about 0.5 L to about 1 L, from about 0.6 L to about 1 L, from about 0.5 L to about 0.8 L or from about 0.2 L to about 0.8 L.

*Further Applications and Uses*

[00273] One having skill in the art will readily recognize that the innovations disclosed herein are not limited to any specific application including not being limited to the removal of

impurity or waste species from blood or any other biological or bodily fluid. The system having a controlled compliance dialysis circuit **141** and an additional circuit without a requirement for specifically controlled compliance (*e.g.* extracorporeal circuit **140**) can be applied to any application where membrane-based diffusion or purification is applied. That is, dialysis or selective diffusion through a selectively permeable membrane is used in numerous applications where at least two fluids are contacted across a selectively permeable membrane to allow for exchange of material between the fluids. The innovations disclosed herein allow for a selective diffusion process to occur while allowing for precise control of net fluid flow across the selectively permeable membrane.

[00274] Those skilled in the art will understand that extracorporeal circuit **140** for conveying blood can be substituted with another circuit **140** for circulating any suitable fluid, wherein the volume of fluid transferred between the external fluid and the fluid in the dialysis circuit **141** can be controlled. For example, the described systems can be applied to buffer exchange for pharmaceutical compositions, such as aqueous suspensions of biomolecules including oligonucleotides, proteins, and/or peptides, etc. Specifically, the circuit **140** can be adapted to be an external circuit **140** that is configured to circulate a pharmaceutical composition containing a solution or suspension of biomolecules. Concentrating a solution or suspension containing biomolecules is often problematic; however, it is often a requirement for pharmaceutical compositions to be provided at very specific concentrations. A common procedure for concentrating such solutions and suspensions is ultrafiltration, where a solution or suspension of biomolecules is contacted with an ultrafiltration membrane with centrifugal force used to drive water through the ultrafiltration membrane to generate a more concentrated solution or suspension. However, ultrafiltration is expensive and often solubility problems develop during the process where expensive biomolecules are lost during

the process. As such, once a solution or suspension of biomolecules is prepared at a desired concentration, it is advantageous to avoid further changes in concentration.

[00275] Several techniques are known to achieve buffer exchange for a pharmaceutical or other aqueous solution or suspension of biomolecules. However, common techniques often lead to uncontrollable changes in volume and concentration, such as size exclusion chromatography. The systems described herein can be used to affect buffer exchange without any further changes in concentration or with a controlled change in concentration.

[00276] An external fluid being a solution or suspension of biomolecules in a first buffer can be provided and conveyed through the external circuit **140**. A second buffer can be provided and conveyed in the dialysis circuit **141**. The movement of fluid across the dialyzer **130** can be prevented to maintain the concentration of the solution or suspension of biomolecules during buffer exchanged. Alternatively, the solution or suspension of biomolecules can be selectively diluted to a desired concentration by operation of the control pump **190** to allow for a controlled movement of a volume of the second buffer across the membrane in the dialyzer **130**. The second buffer present in the dialysis circuit **141** can be regenerated during operation through any suitable technique. For example, a mixed anion/cation deionization resin can be provided in the sorbent cartridge **102** to remove all buffer salts followed by regeneration of the second buffer by infusing of a concentrated buffer using infusate pump **180**, as described above.

#### *System Control*

[00277] As described above, the systems described herein have several dynamic components including pumps and valves as well as detectors that determine the state of the system. As applied throughout this disclosure, operation of the system under the control of controller can refer to a single controller or multiple controllers having separate or

overlapping function. A controller refers to a device having a programmable microprocessor and associated memory.

[00278] Figure **30** shows one or more controllers **801** capable of sending and receiving data or instructions from several system components. The one or more controllers **801** can be more than one microprocessor unit. Specifically, the one or more controllers **801** are capable of controlling the pump rate and pumping direction of the blood pump **125**, the dialysate pump **138**, the filtrate pump **139** and the control pump **190** along with the operating of valve **150**, valve **158**, valve **212**, and valve **515**. The operation of heparin pump **181**, bicarbonate pump **505** and infusate pump **181** is further under control of the one or more controllers **801**. In two controller systems, one controller can be used to control the process and the other controller may be used to monitor the system and protect if the control is not correct. Alternatively in one controller systems, the processes that control or protect may be separate processes within the same controller.

[00279] The one or more controllers **801** also receives data from the various meters and detectors incorporated in the system including pressure meters **134**, **135**, and **137**, optical and/or air-fluid detectors **201**, **202**, and **203**, conductivity detectors **101**, **104** and **160** and blood leak detector **560**. Optionally, a detector, such as a pressure switch-type detector, a magnetic switch, or an optical detector, can be present to determine the connection state of quick connector **550**. The one or more controllers **801** are capable of stopping or modifying operation of the system to protect the patient from an unsafe pressure reading indicating a malfunction or the presences of air in the extracorporeal circuit **140**, an unsafe conductivity level or detection of a blood leak in the dialyzer **130**. The one or more controllers are capable of stopping any of the pumps of the systems or operating valve **150** to bypass the dialyzer **130**. Further, the one or more controllers **801** can modify or stop the operation of the system based upon the conductivity readings from the conductivity meters **101** and **104** as well as

calculating an amount of urea absorption by the sorbent cartridge **102** and/or sodium entering or leaving the system through control pump **190**. In two controller systems, one controller may be used to control the process and the other controller may be used to monitor and protect if the control is not correct.

[00280] In certain embodiments, the one or more controllers **801** are located remote from the dialysis and extracorporeal circuits. One of the controllers **801** can be a device that can send and receive data and instructions through a wired or wireless connection with the portable dialysis system. This data can be transferred automatically to an electronic medical record for automatic recording of patient data or a diagnostic device if the system malfunctions. Certain controller functions, for example, can be performed by an application that runs on a multipurpose computing device such as a cell phone, tablet, PC or PDA. In certain embodiments, a controller **801** that is remote to the portable dialysis system is capable of operating through a wired connection to the portable dialysis system to enable operation in hospital environments or airplanes where the use of wireless technology is restricted.

[00281] By locating one or more of the controllers **801** remote from the portable dialysis system, the majority of processing power does not have to be carried by the patient thereby lowering the weight of the device. Devices and methods for controlling a device through wireless technology are known in the art. The wireless signals can employ signal confirmation, digital encoding algorithms, checksums and other verifications to minimize the effects of interference and to allow similar systems to operate in the same area. The system can have a safety feature to stop the device if the wireless control signal is interrupted or compromised.

[00282] It will be apparent to one skilled in the art that various combinations and/or modifications and variations can be made to the portable dialysis system depending upon the

specific needs for operation. Moreover, features illustrated or described as being part of one embodiment may be used on another embodiment to yield a still further embodiment.

We claim:

1. A system for performing kidney replacement treatment, comprising:
  - a hemodialysis system having a controlled compliance dialysis circuit, a dialyzer with a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane;
  - an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to the subject, and a blood pump for conveying blood from the subject, to the dialyzer and back to the subject;
  - a dialysis circuit having a sorbent cartridge for removing at least one impurity or waste species from the dialysate, one or more conduits for conveying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate inlet end and a dialysate outlet end;
  - a control pump for moving fluid bi-directionally between the dialysis circuit and the extracorporeal circuit, and where a flux of fluid moving between the extracorporeal circuit and the dialysis circuit is changed by the rate at which the control pump is operating;
  - a first control reservoir for storing fluid removed from the dialysis circuit by the control pump or for storing fluid that can be added to the dialysis circuit by the control pump;
  - and
  - one or more controllers for controlling a rate of the control pump, a rate of the blood pump, and a rate of the dialysate pump.
2. The system of claim 1, wherein one or more of the blood pump and the dialysate pump are peristaltic pumps.
3. The system of claim 1, with the proviso that the blood pump and the dialysate pump are not pulsatile pumps.
4. The system of claim 1, further comprising an infusate container containing an infusate solution, the infusate solution comprising a potassium salt, and an infusate pump for adding the solution to the dialysis circuit.
5. The system of claim 4, wherein the infusate solution further comprises a magnesium salt and a calcium salt.
6. The system of claim 1, further comprising an infusate container containing fresh water.

7. The system of claim 1, further comprising a second control reservoir for storing fluid that can be added to the dialysis circuit by the control pump when the first control reservoir is used only for storing fluid from the dialysis circuit by the control pump.
8. The system of claim 1, further comprising an infusate container containing bicarbonate or buffer.
9. The system of claim 1, further comprising a conductivity meter for measuring the conductivity of the dialysate in the dialysis circuit.
10. The system of claim 1, wherein the dialysis membrane has high permeability.
11. The system of claim 9, wherein the conductivity meter measures the conductivity of the dialysate at a position located between the dialysate outlet end of the sorbent cartridge and the dialyzer.
12. The system of claim 9, wherein the one or more controllers calculate and store in a memory the amount of conductivity entering and leaving the dialysis circuit.
13. The system of claim 4, further comprising a conductivity meter for measuring the conductivity of the dialysate in the dialysis circuit.
14. The system of claim 13, wherein the one or more controllers calculate and store in a memory the amount of sodium ions entering and leaving the dialysis circuit by accounting for the amount of conductivity of the infusate solution entering the dialysis circuit.
15. The system of claim 1, further comprising an anticoagulant container containing a solution comprising an anticoagulant and an anticoagulant pump for adding the anticoagulant solution to the extracorporeal circuit.
16. The system of claim 15, wherein the anticoagulant is heparin.
17. The system of claim 1, wherein heparin is covalently bonded to a surface of the extracorporeal circuit.
18. The system of claim 1, wherein a volume of fluid added to the dialysis circuit by the control pump results in substantially the same volume of fluid transferred to the body of the subject.
19. The system of claim 1, wherein a net volume of fluid removed from the dialysis circuit by the control pump results in substantially the same volume of fluid transferred from the body of the subject to the system for performing kidney replacement treatment.
20. The system of claim 1, wherein the dialysis circuit comprises a first pathway for conveying the dialysate between the sorbent cartridge, the dialysate pump, and the

dialyzer, and a second bypass pathway for conveying the dialysate between the dialysis outlet end of the sorbent cartridge and the dialysis inlet end of the sorbent cartridge without the dialysate passing through the dialyzer.

21. The system of claim 20, wherein the one or more controllers direct the conveyance of the dialysate through the second bypass pathway when the conductivity of the dialysate is above a predetermined level.

22. The system of claim 20, wherein the one or more controllers direct the conveyance of the dialysate through the second bypass pathway when the conductivity of the dialysate is below a predetermined level.

23. The system of claim 20, wherein the one or more controllers direct the conveyance of the dialysate through the first pathway when the conductivity of the dialysate is within a predetermined range.

24. The system of claim 1, wherein the dialysate pump operates at a rate from about 10 to about 400 mL/min.

25. The system of claim 1, wherein the blood pump operates at a rate from about 50 to about 600 mL/min.

26. The system of claim 1, wherein the control pump operates at a rate from about 0 to about 200 mL/min.

27. The system of claim 1, wherein the control pump operates at a rate from about 0 to about 100 mL/min.

28. The system of claim 1, wherein the control pump operates at a rate from about 0 to about 50 mL/min.

29. The system of claim 1, further comprising one or more pressure meters for measuring the pressure of the dialysate in the dialysis circuit, and one or more pressure meters for measuring the pressure of the blood entering the dialyzer at the blood inlet end and the pressure of the blood exiting the dialyzer at the blood outlet end.

30. The system of claim 1, wherein the total volume of dialysate within the dialysis circuit is less than about 1 L.

31. The system of claim 1, wherein the volume of the dialysate within the dialysis circuit is a substantially inflexible volume.

32. The system of claim 1, wherein a void volume space for accommodating the dialysate in the sorbent cartridge, the dialyzer, and conduits comprising the dialysis circuit has a substantially inflexible volume.

33. The system of claim 1, wherein the dialysis circuit further comprising an air trap for removing air from the dialysate, the air trap located between the dialysate outlet end of the sorbent cartridge and the dialyzer.

34. The system of claim 33, wherein the air trap further comprises a hydrophobic membrane for allowing air to pass through the membrane and blocking the movement of fluid across the membrane.

35. The system of claim 1, wherein the sorbent cartridge comprises urease and zirconium phosphate.

36. The system of claim 1, further comprising a hematocrit sensor to determine a hematocrit level of the blood in the extracorporeal circuit, the hematocrit sensor configured to send information to the one or more controllers.

37. The system of claim 1, further comprising a relative blood volume monitor to determine the relative blood volume hydration status (RBVHS) of the blood in the extracorporeal circuit, the relative blood volume monitor configured to send information to the one or more controllers.

38. The system of claim 37, wherein the relative blood volume monitor determines the level of one or more solutes in the blood at a first time ( $C_0$ ) and determines the level of the one or more solutes in the blood at a second time later than the first time ( $C_t$ ), and the relative blood volume hydration status is calculated by the formula  $RBVHS = C_0/C_t$ .

39. The system of claim 37, wherein the relative blood volume monitor is a hematocrit sensor.

40. The system of claim 39, wherein the hematocrit sensor is an oximeter.

41. The system of claim 40, wherein the hematocrit sensor comprises a light source for emitting red or infrared light and a detector for detecting the emitted light.

42. The system of claim 37, wherein the relative blood volume monitor measures the velocity for ultrasonic sound waves in the blood in the extracorporeal circuit.

43. The system of claim 42, wherein the velocity for ultrasonic sound waves indicates the level of protein concentration in the blood.

44. The system of claim 37, further comprising an impedance detector for determining a tissue fluid volume in the subject, the impedance detector configured to send information to the one or more controllers.

45. The system of claim 37, wherein the relative blood volume monitor is configured to determine the fluid volume of the blood at a position prior to the blood entering the dialyzer.

46. The system of claim 44, wherein the one or more controllers operates the control pump to maintain a ratio of tissue fluid volume to blood fluid volume in the range from about 5:1 to about 9:1.

47. The system of claim 36, wherein the one or more controllers are configured to operate the control pump at a rate not exceeding the rate of the blood pump.

48. The system of claim 36, wherein the hematocrit sensor is an oximeter.

49. The system of claim 36, wherein the hematocrit sensor comprises a light source for emitting red or infrared light and a detector for detecting the emitted light.

50. The system of claim 1, further comprising an impedance detector for determining a tissue fluid volume in the subject, the impedance detector configured to send information to the one or more controllers.

51. The system of claim 50, further comprising a hematocrit sensor to determine the fluid volume of the blood in the extracorporeal circuit.

52. The system of claim 51, wherein the hematocrit sensor determines the fluid volume of the blood at a position prior to the blood entering the dialyzer.

53. The system of claim 51, wherein the one or more controllers operates the control pump to maintain a ratio of tissue fluid volume to blood fluid volume in the range from about 5:1 to about 9:1.

54. The system of claim 1, wherein the sorbent cartridge contains a zirconium phosphate material intermixed with a urease-containing material.

55. A medical device for performing kidney replacement treatment with enhanced convective clearance and reduced blood clotting risk, comprising:

a hemodialyzer having a controlled compliance dialysis circuit, a dialyzer with a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane;

an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to the subject and a blood pump for conveying blood from the subject, to the dialyzer and back to the subject;

a dialysis circuit having a sorbent cartridge for removing at least one impurity or waste species from the dialysate, one or more conduits for carrying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the

sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate inlet end and a dialysate outlet end;

a first control reservoir for storing fluid removed from the dialysis circuit by a control pump or for storing fluid that can be added to the dialysis circuit by the control pump; and

one or more controllers for controlling the operation of the control pump, the blood pump and the dialysate pump.

56. The medical device of claim 55, wherein the one or more controllers control operation of the control pump to intermittently switch between an efflux direction to move fluid across the dialysis membrane from the extracorporeal circuit to the dialysis circuit and a second influx direction to move fluid across the dialysis membrane from the dialysis circuit to the extracorporeal circuit.

57. The medical device of claim 55, wherein the one or more controllers control the blood pump and the dialysate pump such that a ratio of the flow rate of blood to dialysate through the dialyzer is from about 1:1.5 to about 3:1.

58. The medical device of claim 55, wherein one or more of the blood pump and the dialysate pump are peristaltic pumps.

59. The medical device of claim 55, with the proviso that the blood pump and the dialysate pump are not pulsatile pumps.

60. The medical device of claim 55, further comprising an infusate container containing an infusate solution comprising a potassium salt and an infusate pump for adding the solution to the dialysis circuit.

61. The medical device of claim 60, wherein the infusate solution further comprises a magnesium salt and a calcium salt.

62. The medical device of claim 55, further comprising an infusate container containing fresh water.

63. The medical device of claim 55, further comprising an infusate container containing bicarbonate or buffer.

64. The medical device of claim 55, further comprising a conductivity meter for measuring the conductivity of the dialysate in the dialysis circuit.

65. The medical device of claim 62, wherein the conductivity meter measures the conductivity of the dialysate at a position located between the dialysate outlet end of the sorbent cartridge and the dialysate inlet end of the dialyzer.

66. The medical device of claim 55, further comprising a bicarbonate container containing a bicarbonate solution comprising a bicarbonate salt and a bicarbonate pump for adding the bicarbonate solution to the dialysis circuit.

67. The medical device of claim 55, wherein a volume of fluid added to the dialysis circuit by the control pump results in substantially the same volume of fluid transferred to the body of the subject.

68. The medical device of claim 55, wherein operation of the control pump in the influx direction removes protein present on a surface of the dialysis membrane.

69. The medical device of claim 55, wherein a volume of fluid removed from the dialysis circuit by the control pump results in substantially the same volume of fluid transferred from the body of the subject to the medical device for performing kidney replacement treatment.

70. The medical device of claim 55, wherein the sorbent cartridge contains a zirconium phosphate material intermixed with a urease-containing material.

71. The medical device of claim 55, further comprising a second control reservoir for storing fluid that can be added to the dialysis circuit by the control pump when the first control reservoir is used only for storing fluid from the dialysis circuit by the control pump.

72. Use of preparing a system or medical device for operation, the use comprising priming the system or medical device by:

attaching a container containing a priming fluid to the system of claim 1 or the medical device of claim 55, the system or medical device having an extracorporeal circuit having a first end that draws the priming fluid from the container and a second end that allows the priming fluid to exit the extracorporeal circuit, where the extracorporeal circuit is in fluid communication with a dialysis circuit through a dialysis membrane;

operating a first pump that conveys the priming fluid from the container and through the extracorporeal circuit to fill the extracorporeal circuit with the priming fluid;

attaching the first and second ends of the extracorporeal circuit to the cardiovascular system of a subject;

operating a dialysate pump to draw the priming fluid across the dialysis membrane from the extracorporeal circuit into the dialysis circuit and to draw a biological fluid into the extracorporeal circuit such that the biological fluid reaches an inlet of a dialyzer housing the dialysis membrane; and after the biological fluid reaches the inlet, operating the first pump and the dialysate pump, the dialysate pump at a lower speed than the first pump, to transfer

the volume of priming fluid present in the extracorporeal circuit into the dialysis circuit through the dialysis membrane; and

when the extracorporeal circuit is filled with the biological fluid, operating the dialysate pump at a rate lower than the first pump to draw fluid from the extracorporeal circuit into the dialysis circuit to complete filling the dialysis circuit with fluid.

73. The use of claim 72, wherein the lower rate of the dialysis pump is about 66% or less than the rate of the first pump.

74. The use of claim 72, wherein the lower rate of the dialysis pump is less than 60% of the rate of the first pump.

75. The use of claim 72, wherein the first pump and the dialysate pump are independently selected from the group consisting of peristaltic pumps, diaphragm pumps, centrifugal pumps and shuttle pumps.

76. The use of claim 72, with the proviso that the first pump and the dialysate pump are not pulsatile pumps.

77. The use of claim 72, wherein a void volume of the dialysis circuit has a substantially inflexible volume.

78. The use of claim 72, wherein a void volume space for accommodating the dialysate for the sorbent cartridge, dialyzer, and conduits comprising the dialysis circuit has a substantially inflexible volume.

79. The use of claim 72, wherein a volume of the dialysis circuit is larger than the volume of the extracorporeal circuit.

80. The use of claim 72, wherein the priming fluid is a saline solution.

81. The use of claim 72, wherein the system is primed without introducing any of the priming fluid to the extracorporeal circuit.

82. The use of claim 72, wherein the first pump and the dialysate pump are controlled by one or more controllers.

83. The use of claim 72, wherein the one or more controllers calculate the volume of fluid transferred from the extracorporeal circuit to the dialysis circuit and stores the value of the volume in memory selected from one or more of RAM, Dynamic RAM, microprocessor cache, FLASH memory and memory card.

84. The use of claim 72, wherein the first pump pumps fluids through the dialyzer in a first direction and the dialysate pump pumps fluids through the dialyzer in a second direction opposite to the first direction.

85. Use of preparing a system or medical device for operation, the use comprising priming the system or medical device by:

attaching a container containing a priming fluid to the system of claim 1 or the medical device of claim 55, the system or medical device having an extracorporeal circuit having a first end that draws the priming fluid from the container and a second end that discharges the priming fluid from the extracorporeal circuit, where the extracorporeal circuit is in fluid communication with a dialysis circuit through a dialysis membrane;

operating a first pump to convey the priming fluid from the container and through the extracorporeal circuit to fill the extracorporeal circuit with the priming fluid, and operating a dialysate pump to draw the priming fluid across the dialysis membrane from the extracorporeal circuit into the dialysis circuit until the dialysis circuit is filled with the priming solution; and

venting air from the dialysis circuit to allow the priming fluid to enter the dialysis circuit.

86. The use of claim 85, further comprising adding one or more of potassium ion, calcium ions, magnesium ions and bicarbonate ions to convert the priming fluid in the dialysis circuit to a physiologically compatible dialysate.

87. The use of claim 85, wherein the lower rate of the dialysis pump is about 66% or less than the rate of the first pump.

88. The use of claim 85, wherein the lower rate of the dialysis pump is less than 60% of the rate of the first pump.

89. The use of claim 85, wherein the first pump and the dialysate pump are independently selected from the group consisting of peristaltic pumps, diaphragm pumps, centrifugal pumps and shuttle pumps.

90. The use of claim 85, with the proviso that the first pump and the dialysate pump are not pulsatile pumps.

91. The use of claim 85, wherein a void volume of the dialysis circuit has a substantially inflexible volume.

92. The use of claim 85, wherein a void volume space for accommodating the dialysate for the sorbent cartridge, dialyzer, and conduits comprising the dialysis circuit has a substantially inflexible volume.

93. The use of claim 85, wherein a void volume of the dialysis circuit is larger than the volume of the extracorporeal circuit.

94. The use of claim 85, wherein the priming fluid is a saline solution.

95. The use of claim 85, wherein the system or medical device is primed without introducing any of the priming fluid to the extracorporeal circuit.

96. The use of claim 85, wherein the first pump and the dialysate pump are controlled by one or more controllers.

97. The use of claim 85, wherein the first pump pumps fluids through the dialyzer in a first direction and the dialysate pump pumps fluids through the dialyzer in a second direction opposite to the first direction.

98. The use of claim 85, wherein the sorbent cartridge contains a zirconium phosphate material intermixed with a urease-containing material.

99. Use of a sorbent for providing a system having a controlled compliance circuit for controlling the movement of fluid volume from an external fluid or for performing enhanced convective clearance of a waste species from the external fluid, the use comprising:

operating the system to convey the external fluid through an external circuit and a dialyzer, where the external circuit is in fluid communication with a controlled compliance dialysis circuit through a dialysis membrane housed in the dialyzer;

conveying a dialysate through the controlled compliance dialysis circuit such that the dialysate moves from a sorbent cartridge containing the sorbent, to the dialyzer and back to the sorbent cartridge, where at least one waste species diffuses from the external fluid to the dialysate through the dialysis membrane and the sorbent cartridge substantially removes at least one impurity or waste species from the dialysate; and

operating a control pump that adds fluid from a control reservoir to the dialysis circuit in an influx direction via a conduit or removes fluid from the dialysis circuit to the control reservoir in an efflux direction via the conduit, and intermittently switching the control pump between the efflux direction to move fluid across the dialysis membrane from the external circuit to the dialysis circuit and the influx direction to move fluid across the dialysis membrane from the dialysis circuit to the external circuit,

wherein the intermittent switching of the pump accomplishes the convective clearance of at least one waste species from the external fluid.

100. The use of claim 99, wherein the waste species has a molecular weight less than about 66000 g/mol.

101. The use of claim 99, wherein the waste species removed by the sorbent cartridge is urea.

102. The use of claim 99, wherein the sorbent comprises urease and zirconium phosphate.

103. The use of claim 102, wherein the sorbent further comprises one or more components selected from the group consisting of zirconium oxide and activated carbon.

104. The use of claim 102, wherein the sorbent comprises urease and magnesium phosphate.

105. The use of claim 99, wherein the sorbent comprises one or more components selected from the group consisting of zirconium oxide and activated carbon.

106. The use of claim 99, wherein the total volume of dialysate within the dialysis circuit is less than about 1 L.

107. The use of claim 99, wherein the volume of the dialysate within the dialysis circuit has a substantially inflexible volume.

108. The use of claim 99, wherein a void volume space for accommodating the dialysate for the sorbent cartridge, dialyzer, and conduits comprising the dialysis circuit has a substantially inflexible volume.

109. The use of claim 99, wherein the control pump is intermittently switched between the efflux direction and the influx direction at least once every minute.

110. The use of claim 99, wherein the control pump is intermittently switched between the efflux direction and the influx direction such that the pump is not operated in either the efflux or influx direction for a time period exceeding about 2 minutes.

111. The use of claim 99, wherein the control pump is intermittently switched between the efflux direction and the influx direction such that the pump is not operated in either the efflux or influx direction for a time period exceeding about 45 seconds.

112. The use of claim 99, wherein the control pump is intermittently switched between the efflux direction and the influx direction such that the pump is not operated in either the efflux or influx direction for a time period exceeding about 30 seconds.

113. The use of claim 99, wherein the control pump is intermittently switched between the efflux direction and the influx direction such that the pump is not operated in either the efflux or influx direction for a time period exceeding about 15 seconds.

114. The use of claim 99, wherein the control pump does not operate in the efflux direction and the influx direction for equal period of times.

115. The use of claim 99, wherein the control pump does not operate to pump an equal volume in the efflux direction and the influx direction over a period of time.

116. The use of claim 99, wherein the control pump operates to pump a larger volume in the efflux direction compared with the influx direction over a period of time.

117. The use of claim 99, wherein the control pump operates to pump a volume in the efflux direction that is at least about 10% greater compared to a volume pumped in the influx direction over a period of time.

118. The use of claim 99, wherein the control pump operates to pump a volume in the efflux direction that is at least about 20% greater compared to a volume pumped in the influx direction over a period of time.

119. The use of claim 99, wherein the control pump operates to pump a volume in the efflux direction that is at least about 30% greater compared to a volume pumped in the influx direction over a period of time.

120. The use of claim 99, wherein the control pump operating in the efflux direction to pump a volume into the control reservoir causes substantially the same volume of fluid to be removed from the external fluid.

121. The use of claim 99, wherein the control pump operating in the influx direction to pump a volume from the control reservoir causes substantially the same volume of fluid to be introduced into the external fluid.

122. The use of claim 99, wherein the control pump operates in a manner to cause the net removal of about 100 to about 1000 mL per hour of fluid from the external fluid.

123. The use of claim 99, where the control pump operates in a manner such that the net removal of fluid from the external circuit does not exceed about 30% of  $Q_p$ , where  $Q_p = \text{External Fluid Flow Rate} \times (1 - \text{hematocrit})$ .

124. The use of claim 99, the ratio of rates of conveyance of the external fluid to dialysate through the dialyzer is from about 1:1.5 to about 3:1.

125. The use of claim 99, wherein the sorbent cartridge contains a zirconium phosphate material intermixed with a urease-containing material.

126. A use of a sorbent for providing a system having a controlled compliance circuit for purifying an external fluid and for controlling the movement of fluid volume from the external fluid, the use comprising:

operating the system to convey the external fluid through an external circuit and a dialyzer, where the external circuit is in fluid communication with a controlled compliance dialysis circuit through a dialysis membrane housed in the dialyzer;

conveying a dialysate through the controlled compliance dialysis circuit such that the dialysate moves from a sorbent cartridge containing the sorbent, to the dialyzer and back to the sorbent cartridge via a dialysate pump, where at least one waste species diffuses from the

external fluid to the dialysate through the dialysis membrane and the sorbent cartridge substantially removes at least one impurity or waste species from the dialysate; and

operating a control pump that adds fluid from a control reservoir to the dialysis circuit in an influx direction via a conduit or removes fluid from the dialysis circuit to the control reservoir in an efflux direction via the conduit, and intermittently switching the control pump between the efflux direction to move fluid across the dialysis membrane from the external circuit to the dialysis circuit and the influx direction to move fluid across the dialysis membrane from the dialysis circuit to the external circuit,

wherein a volume of fluid added to the controlled compliance dialysis circuit by the control pump results in substantially the same volume of fluid transferred to the external circuit; and

wherein a volume of fluid removed from the dialysis circuit by the control pump results in substantially the same volume of fluid transferred from the external circuit to the controlled compliance dialysis circuit.

127. The use of claim 126, wherein the dialysate and the external fluid are conveyed independently by one or more selected from the group consisting of peristaltic pumps, diaphragm pumps, centrifugal pumps, and shuttle pumps.

128. The use of claim 126, with the proviso that the external fluid and the dialysate are not conveyed by a pulsatile pump.

129. The use of claim 126, further comprising calculating the volume of fluid added to or removed from the external circuit during a period of time.

130. The use of claim 129, wherein the volume of fluid entering or leaving the external circuit during a period of time is calculated by a controller and stored in a memory of the controller.

131. The use of claim 126, further comprising adding an infusate solution to the dialysate in the dialysis circuit, the infusate solution comprising one or more ions selected from the group consisting of potassium ions, calcium ions and magnesium ions.

132. The use of claim 131, further comprising calculating the volume of fluid added to or removed from the external circuit during a period of time, wherein the volume of fluid pumped by the control pump and the volume of fluid pumped by the infusate pump is considered in calculating the volume of fluid added to or removed from the external circuit.

133. The use of claim 126, further comprising measuring the conductivity of the dialysate using a conductivity meter.

134. The use of claim 133, wherein the conductivity meter measures the conductivity of the dialysate at a position located between the dialysate outlet end of the sorbent cartridge and the dialysate inlet end of the dialyzer.

135. The use of claim 133, further comprising calculating the amount of conductive species entering and leaving the dialysis circuit by operation of the control pump and storing the value in a memory of a controller.

136. A system for monitoring the performance of kidney replacement treatment, comprising:

- a hemodialysis system having a controlled compliance dialysis circuit, and a dialyzer having a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane;

- an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to the subject, and a blood pump for conveying blood from the subject, to the dialyzer and back to the subject;

- a dialysis circuit having a sorbent cartridge for removing urea from the dialysate, one or more conduits for carrying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate inlet end and a dialysate outlet end;

- a first conductivity meter for measuring the conductivity of the dialysate at a position between the dialyzer and the dialysate inlet end of the sorbent cartridge;

- a second conductivity meter for measuring the conductivity of the dialysate at a position between the dialysate outlet end of the sorbent cartridge and the dialyzer; and

- one or more controllers for comparing the conductivity measured by the first conductivity meter and the second conductivity meter and calculating the amount of urea absorbed by the sorbent cartridge.

137. The system of claim 136, wherein the one or more controllers calculates the amount of urea absorbed by the sorbent cartridge by:

- calculating a starting conductivity by subtracting a conductivity attributed to a substantially constant concentration of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  ions in the dialysate from a conductivity measured by the first conductivity meter;

calculating a corrected outlet conductivity by subtracting an increase in conductivity attributed to an exchange  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  ions for  $\text{Na}^{+}$  ions by the sorbent cartridge from a conductivity measured by the second conductivity meter; and

calculating a conductivity increase from the exchange of  $\text{NH}_4^{+}$  for  $\text{Na}^{+}$  ions by the sorbent cartridge by subtracting the starting conductivity from the corrected outlet conductivity.

138. The system of claim 136, wherein the one or more controllers calculates the amount of urea absorbed by the sorbent cartridge over a course of kidney replacement treatment.

139. The system of claim 136, wherein the one or more controllers displays the amount of urea absorbed by the sorbent cartridge to the subject or other individual.

140. The system of claim 136, wherein the dialysis membrane has high permeability.

141. The system of claim 136, wherein the one or more controllers signals an alert if the difference between the conductivity measured by the first conductivity meter and the second conductivity meter are substantially equal.

142. The system of claim 141, wherein the system has a means for preventing the conveyance of dialysate to the dialyzer.

143. Use of a sorbent for providing a system having a controlled compliance circuit and for monitoring the removal of a waste species from an external fluid, the use comprising:

operating the system to convey the external fluid through an external circuit and a dialyzer, where the external circuit is in fluid communication with a controlled compliance dialysis circuit through a dialysis membrane housed in the dialyzer;

conveying a dialysate through the controlled compliance dialysis circuit such that the dialysate moves from a sorbent cartridge containing the sorbent, to the dialyzer and back to the sorbent cartridge, wherein urea diffuses from the external fluid to the dialysate through the dialysis membrane;

monitoring the conductivity of the dialysate at a first position between the dialyzer and an inlet end of the sorbent cartridge;

monitoring the conductivity of the dialysate at a second position between an outlet end of the sorbent cartridge and the dialyzer; and

calculating an amount of urea absorbed by the sorbent cartridge based at least in part upon the conductivity measured at the inlet end of the sorbent cartridge and at the outlet end of the sorbent cartridge.

144. The use of claim 143, wherein the amount of urea absorbed by the sorbent cartridge is calculated by:

calculating a starting conductivity by subtracting a conductivity attributed to a substantially constant concentration of  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  ions in the dialysate from a conductivity measured at the first position;

calculating a corrected outlet conductivity by subtracting an increase in conductivity attributed to an exchange  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ , and  $\text{K}^{+}$  ions for  $\text{Na}^{+}$  ions by the sorbent cartridge from a conductivity measured at the second position; and

calculating a conductivity increase from the exchange of  $\text{NH}_4^{+}$  for  $\text{Na}^{+}$  ions by the sorbent cartridge by subtracting the starting conductivity from the corrected outlet conductivity.

145. The use of claim 143, further comprising calculating the amount of urea absorbed by the sorbent cartridge over a time period.

146. The use of claim 143, further comprising communicating the amount of urea absorbed by the sorbent cartridge.

147. The use of claim 143, further comprising signaling an alert if the difference between the conductivity measured by the first position and the second position are substantially equal.

148. The use of claim 147, further comprising preventing conveyance of dialysate to the dialyzer.

149. A system for performing kidney replacement treatment, comprising:

a hemofiltration system having a controlled compliance filtration circuit, a hemofilter with a hemofiltration membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the hemofilter, and an ultrafiltration outlet for allowing an ultrafiltrate out of the hemofilter;

an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to the subject, and a blood pump for conveying blood from the subject, to the hemofilter and back to the subject;

a hemofiltration circuit having a sorbent cartridge for removing at least one impurity or waste species from the ultrafiltrate to generate a replacement fluid, wherein the ultrafiltrate enters an inlet end of the sorbent cartridge and a replacement fluid exits an outlet end of the sorbent cartridge, the hemofiltration circuit having one or more conduits and a filtrate pump for conveying the ultrafiltrate from the hemofilter to the sorbent cartridge and for infusing the replacement solution into the extracorporeal circuit; and

one or more controllers for controlling a rate of the blood pump and a rate of the filtrate pump.

150. The system of claim 149, wherein a rate of conveyance of the replacement solution is substantially equal to the rate of operation of the filtrate pump.

151. The system of claim 149, wherein a rate of conveyance of the replacement solution is substantially equal to the rate of operation of the filtrate pump within about 5 mL/min.

152. The system of claim 149, further comprising a control pump for removing a portion of the ultrafiltrate from the hemofiltration circuit, such that the removed portion of the ultrafiltrate is not generated into the replacement fluid and infused into the extracorporeal circuit.

153. The system of claim 149, further comprising an infusate container containing an infusate solution, the infusate solution comprising a potassium salt, and an infusate pump for adding the solution to the replacement fluid in the hemofiltration circuit.

154. The system of claim 153, wherein the infusate solution further comprises a magnesium salt and a calcium salt.

155. The system of claim 153, further comprising an infusate container containing fresh water.

156. The system of claim 153, further comprising an infusate container containing bicarbonate or buffer.

157. The system of claim 149, wherein the sorbent cartridge comprises urease and zirconium phosphate.

158. The system of claim 149, wherein the hemofiltration membrane has high permeability.

159. The system of claim 149, wherein a void volume space for accommodating the ultrafiltrate and replacement fluid in the sorbent cartridge, the hemofilter, and conduits comprising the hemofiltration circuit has a substantially inflexible volume.

160. A use of a sorbent for providing a system having a controlled compliance circuit for purifying an external fluid and for controlling the movement of fluid volume from the external fluid, the use comprising:

operating the system to convey the external fluid through an external circuit and a filter having a filtration membrane, the filter attached to a controlled compliance filtration circuit; operating a filtrate pump that draws an ultrafiltrate from the external fluid in the filter and passes the ultrafiltrate through a sorbent cartridge containing the sorbent for removing

one or more waste species or impurities from the ultrafiltrate to generate a replacement fluid; and

transferring the replacement fluid into the external circuit.

161. The use of claim 160, where the control pump operates in a manner such that the rate of ultrafiltration removal from the external circuit does not exceed about 30% of  $Q_p$ , where  $Q_p = \text{External Fluid Flow Rate} \times (1 - \text{hematocrit})$ , where the external fluid flow rate is the rate of external fluid conveyance through the filter.

162. The use of claim 160, further comprising operating a control pump that removes a portion of the ultrafiltrate from the filtration circuit, such that the removed ultrafiltrate is not generated into the replacement fluid.

163. The use of claim 160, wherein a rate of conveyance of the replacement solution is substantially equal to the rate of operation of the filtrate pump.

164. The use of claim 160, wherein a rate of conveyance of the replacement solution is substantially equal to the rate of operation of the filtrate pump within about 5 mL/min.

165. The use of claim 160, further comprising infusing an infusate solution from a container, the infusate solution comprising a potassium salt, and an infusate pump for adding the solution to the replacement fluid in the filtration circuit.

166. The use of claim 165, wherein the infusate solution further comprises a magnesium salt and a calcium salt.

167. The use of claim 160, further comprising an infusate container containing fresh water.

168. The use of claim 160, further comprising an infusate container containing bicarbonate or buffer.

169. The use of claim 160, wherein the sorbent comprises urease and zirconium phosphate.

170. The use of claim 160, wherein the filtration membrane has high permeability.

171. The use of claim 160, wherein a void volume space for accommodating the ultrafiltrate and replacement fluid in the sorbent cartridge, the filter, and conduits comprising the filtration circuit has a substantially inflexible volume.

172. A system for performing kidney replacement treatment, comprising:  
a hemodialysis system having a controlled compliance dialysis circuit, a dialyzer with a dialysis membrane, a blood inlet end for receiving blood, a blood outlet end for allowing blood out of the dialyzer, a dialysate inlet end for receiving dialysate and a dialysate outlet

end for allowing dialysate out of the dialyzer, wherein the blood and the dialysate contact different sides of the dialysis membrane;

an extracorporeal circuit having a conduit for receiving blood from a subject and a conduit for returning blood to the subject, and a blood pump for conveying blood from the subject, to the dialyzer and back to the subject;

a dialysis circuit having a sorbent cartridge for removing at least one impurity or waste species from the dialysate, one or more conduits for conveying dialysate between the sorbent cartridge and the dialyzer, and a dialysate pump for conveying dialysate from the sorbent cartridge, to the dialyzer and back to the sorbent cartridge, the sorbent cartridge having a dialysate inlet end and a dialysate outlet end;

a control pump for moving fluid between the dialysis circuit and the extracorporeal circuit, and where a flux of fluid moving between the extracorporeal circuit and the dialysis circuit is changed by the rate at which the control pump is operating;

a first control reservoir for storing fluid removed from the dialysis circuit by the control pump or for storing fluid that can be added to the dialysis circuit by the control pump;

a second reservoir and a second reservoir pump wherein the second reservoir holds a fluid that can be added to the dialysis circuit by operation of the second reservoir pump, where addition of the fluid by the second reservoir pump causes the movement of fluid from the dialysis circuit to the extracorporeal circuit; and

one or more controllers for controlling a rate of the control pump, a rate of the second reservoir pump, a rate of the blood pump, and a rate of the dialysate pump.

173. The system of claim 172, wherein the control pump operates in a bidirectional fashion to move fluid between the dialysis circuit and the extracorporeal circuit.

174. The system of claim 172, wherein the second reservoir contains water, tap water or purified water.

175. Any system, device or use described herein wherein a dialysis chamber is a selective diffusion chamber.

176. Any system, device or use described herein wherein a dialysis membrane is a selectively permeable membrane.

177. Any system, device or use described herein wherein an external fluid is not a fluid derived from the human body.

178. Any system, device or use described herein wherein the control pump is used to maintain control over the net movement of fluid between a controlled compliance circuit

and an external circuit via the control pump adding or removing fluid from the controlled compliance circuit.

179. Any system, device or use described herein wherein the external fluid is a suspension or solution of biomolecules with the proviso that the suspension or solution is not a bodily fluid.

180. Any system, device or use described herein wherein a use of a sorbent is provided in the manufacturing of an apparatus for removing waste or impurity species from a fluid in a controlled compliance circuit.

181. Any system, device or use described herein wherein a use of a sorbent is provided for absorbing an impurity or waste species originating from an external circuit using an apparatus having a controlled compliance circuit, the apparatus having a control pump to maintain control over the net movement of fluid between the controlled compliance circuit and an external circuit via the control pump adding or removing fluid from the controlled compliance circuit.

182. Any system, device or use described herein wherein a use of a device having a dialyzer is provided for controlling the net movement of fluid through the dialyzer between a controlled compliance circuit and an external circuit via a control pump adding or removing fluid from the controlled compliance circuit.

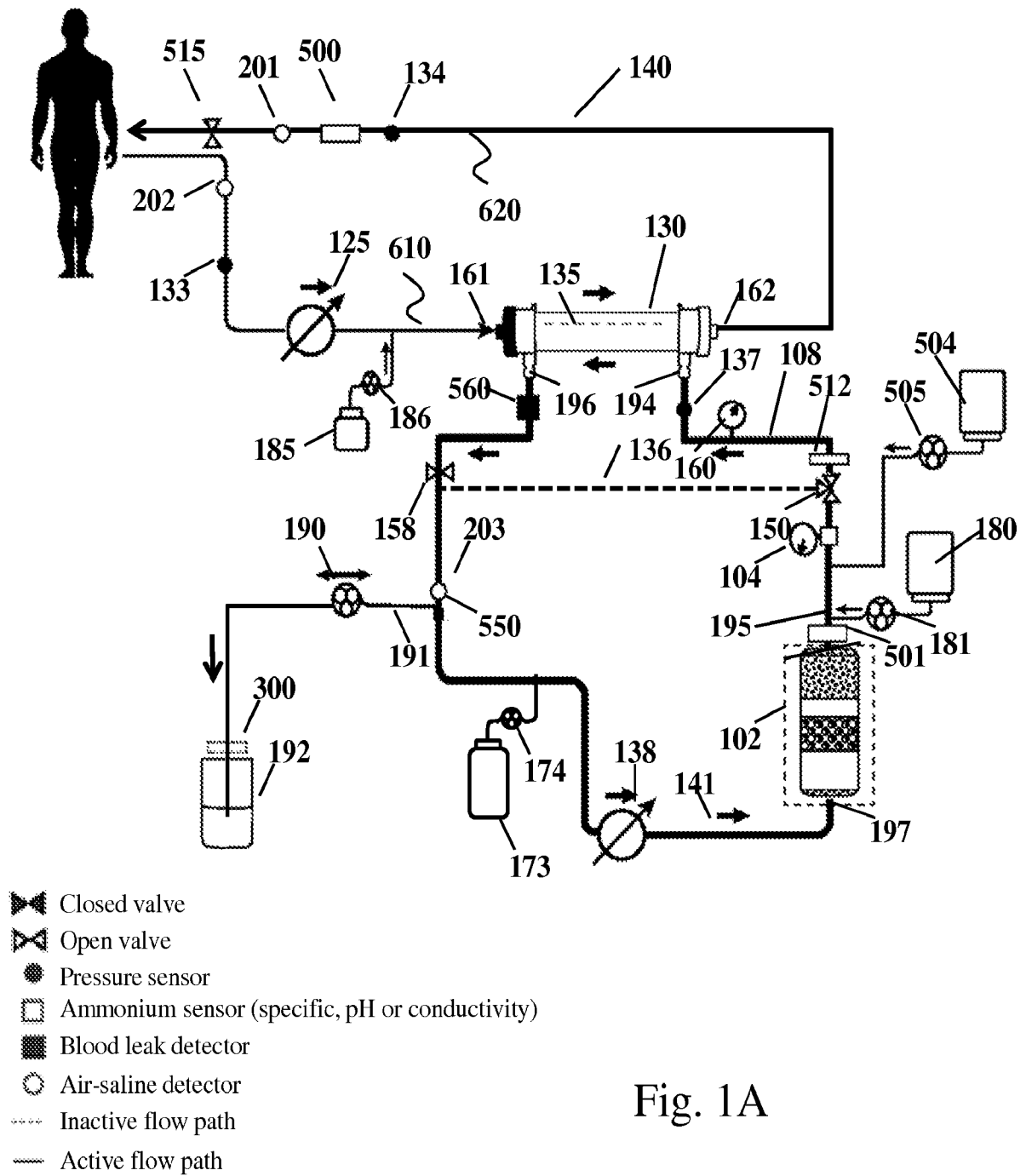


Fig. 1A

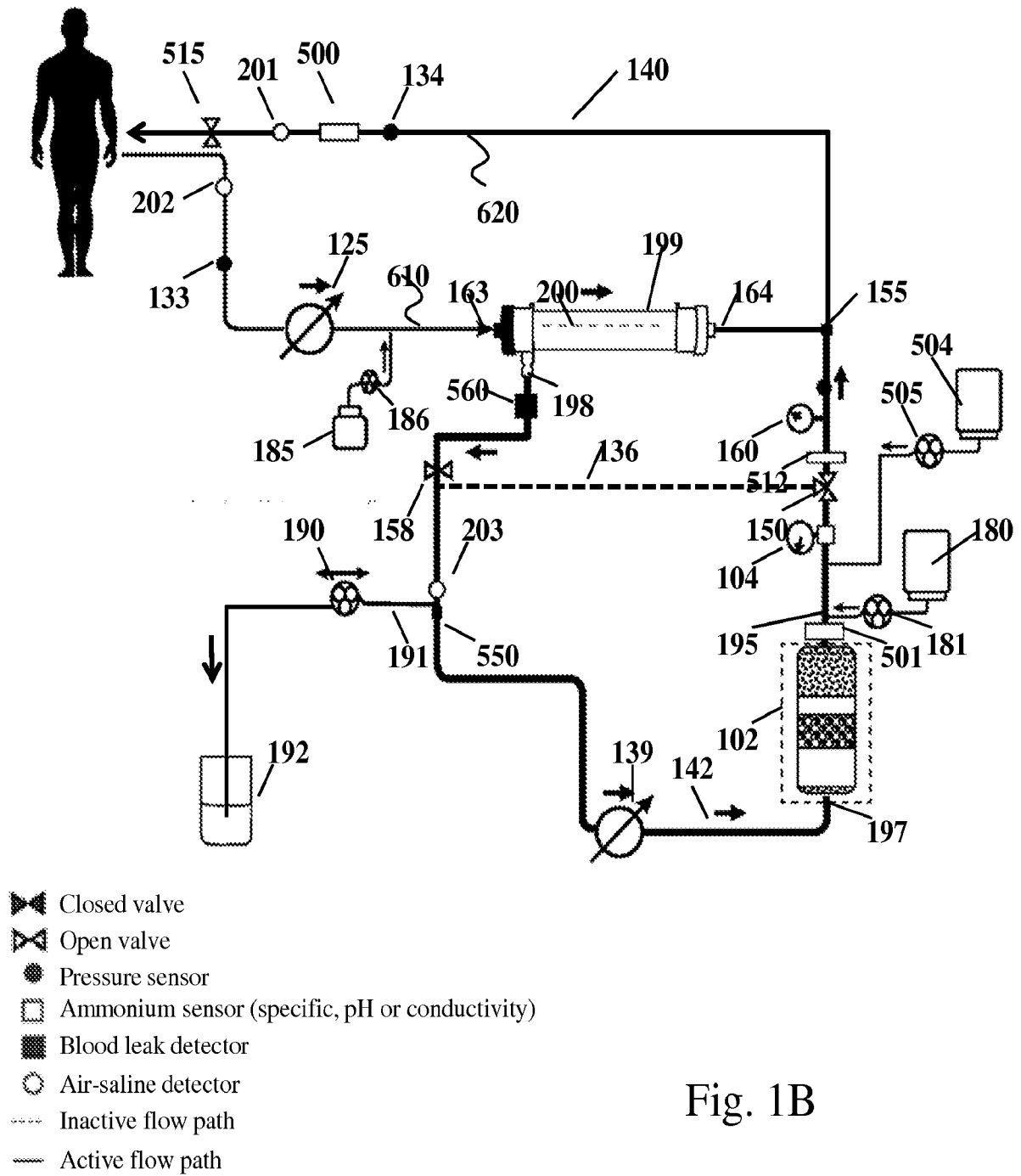


Fig. 1B

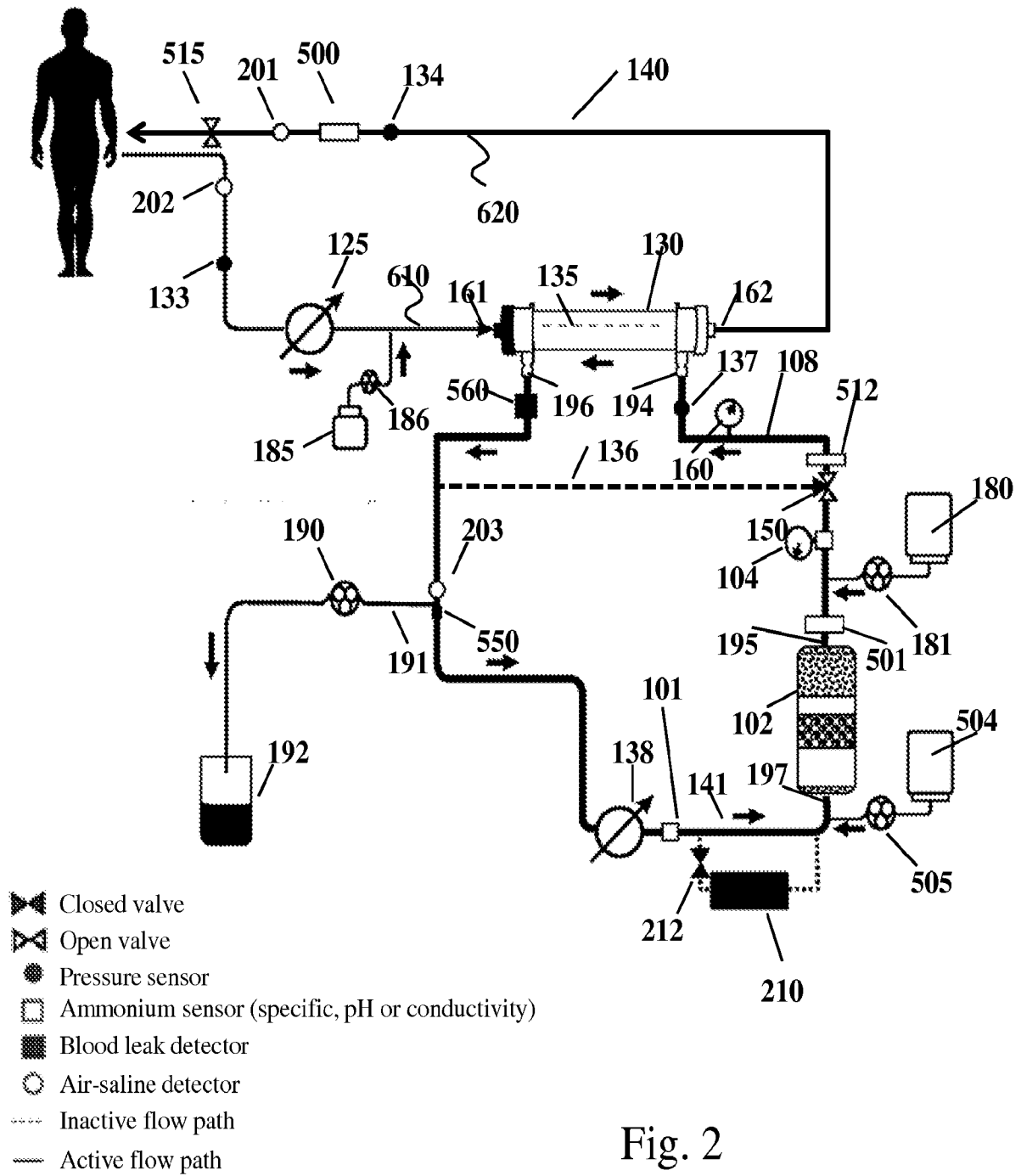


Fig. 2

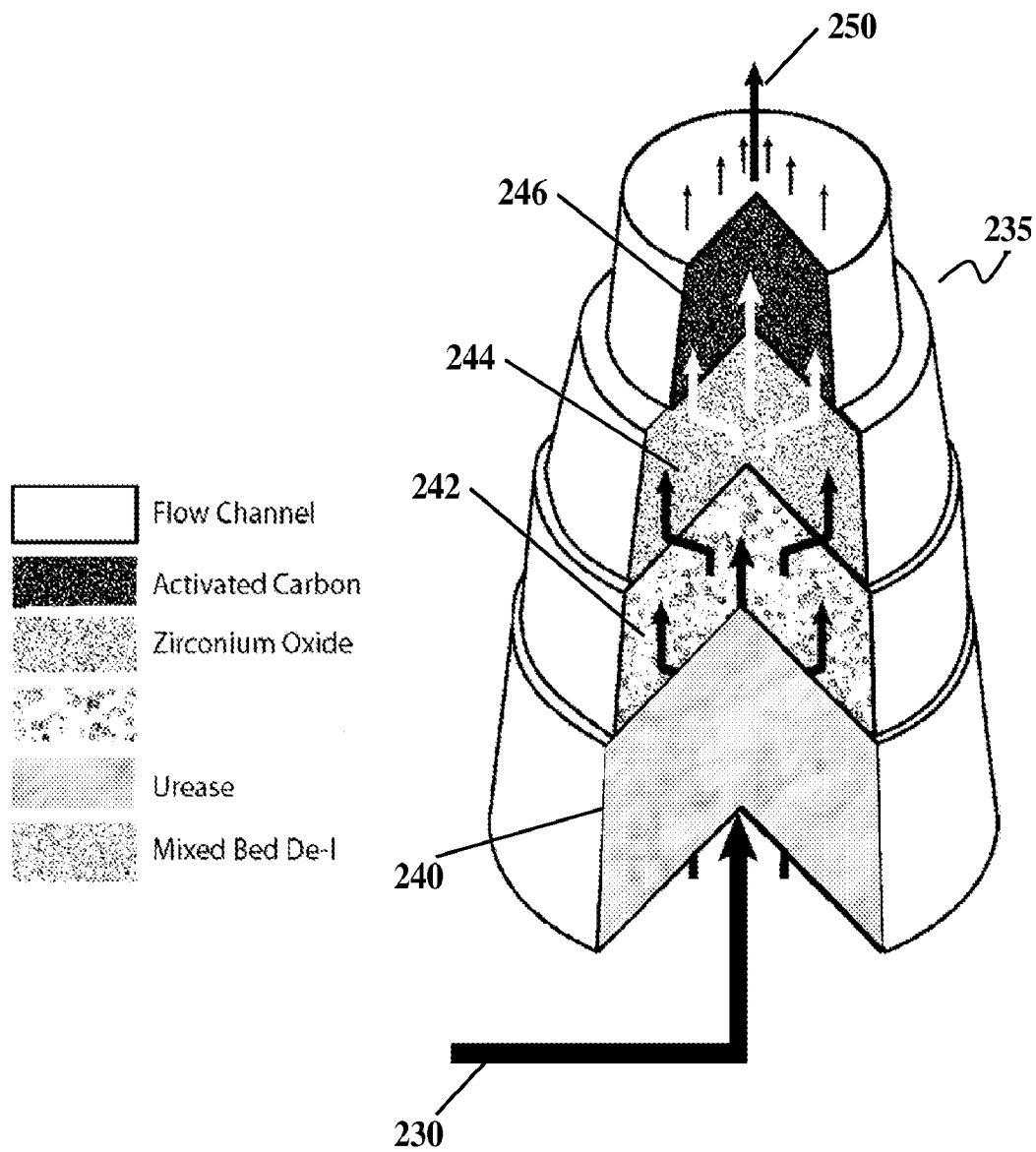


Fig. 3A

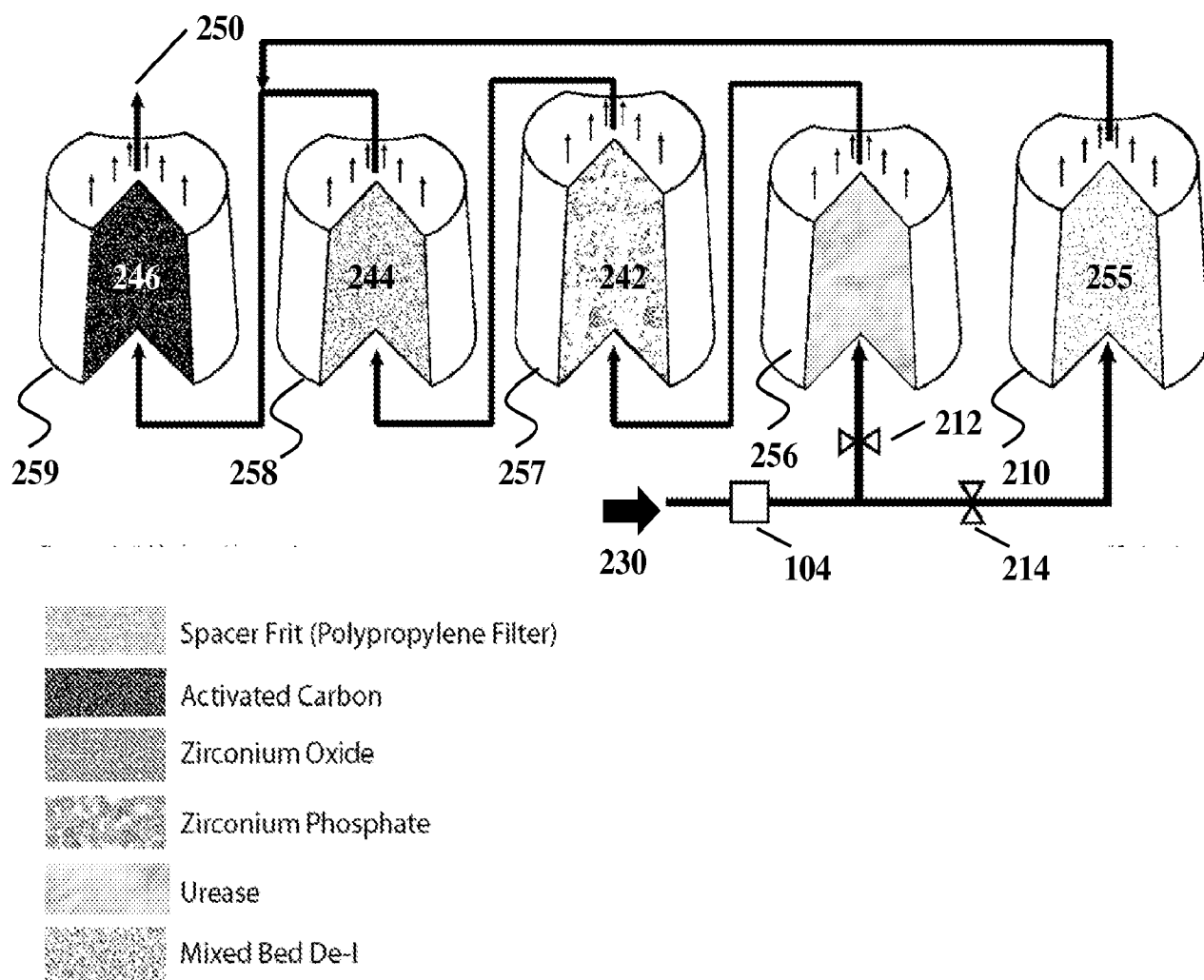


Fig. 3B

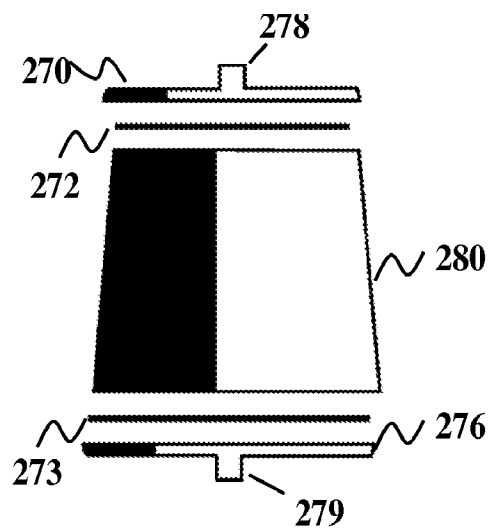


Figure 3C

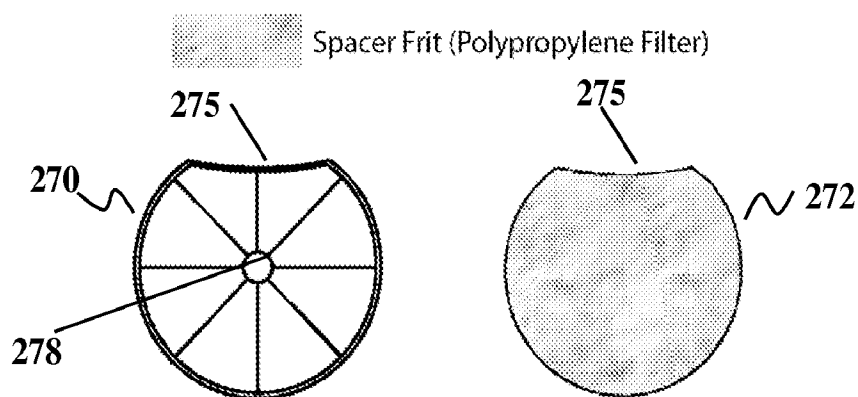


Figure 3D

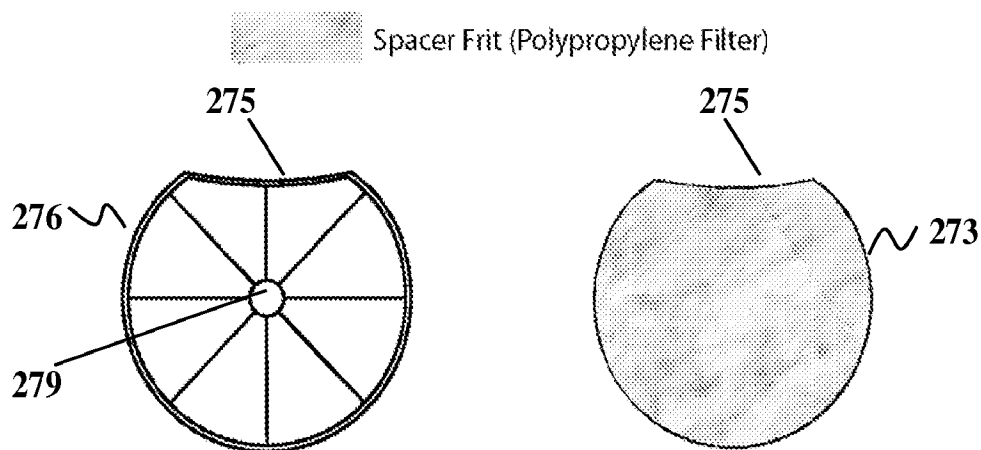


Fig. 3E

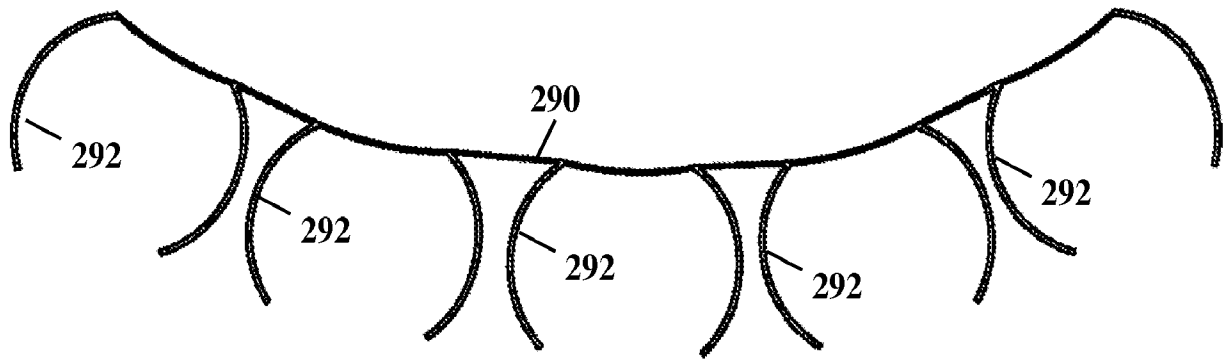


Figure 4A

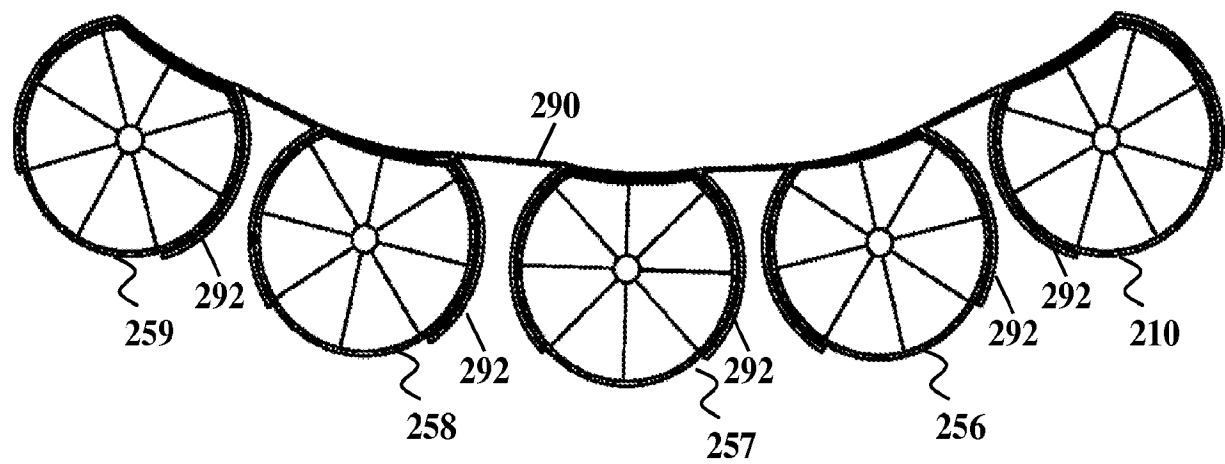


Figure 4B

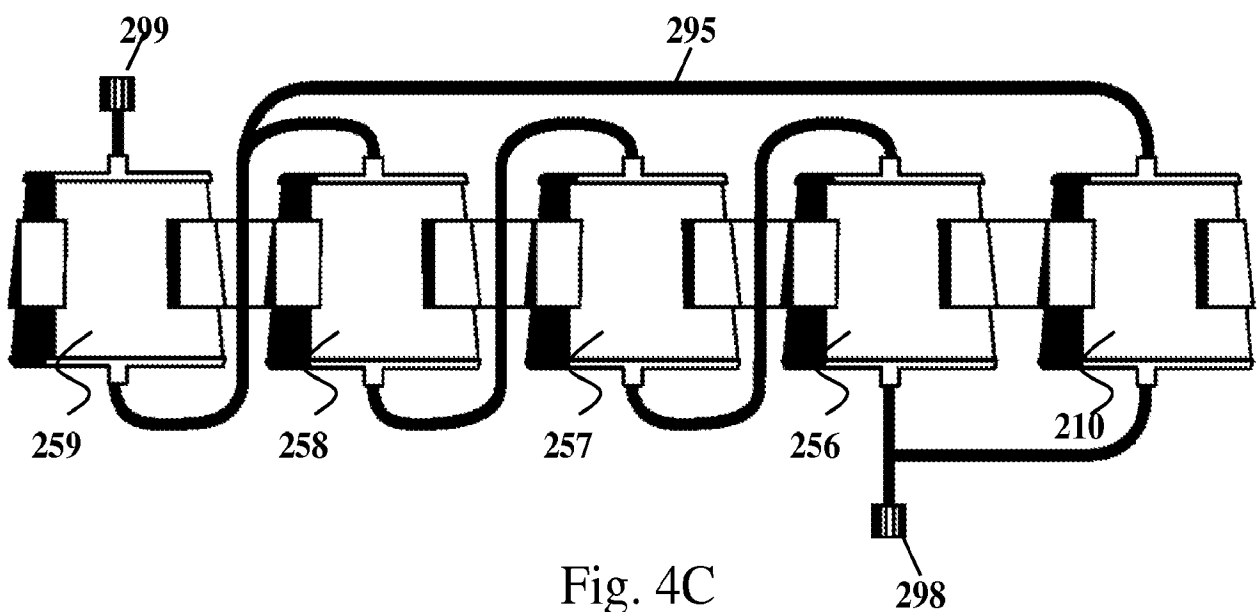


Fig. 4C

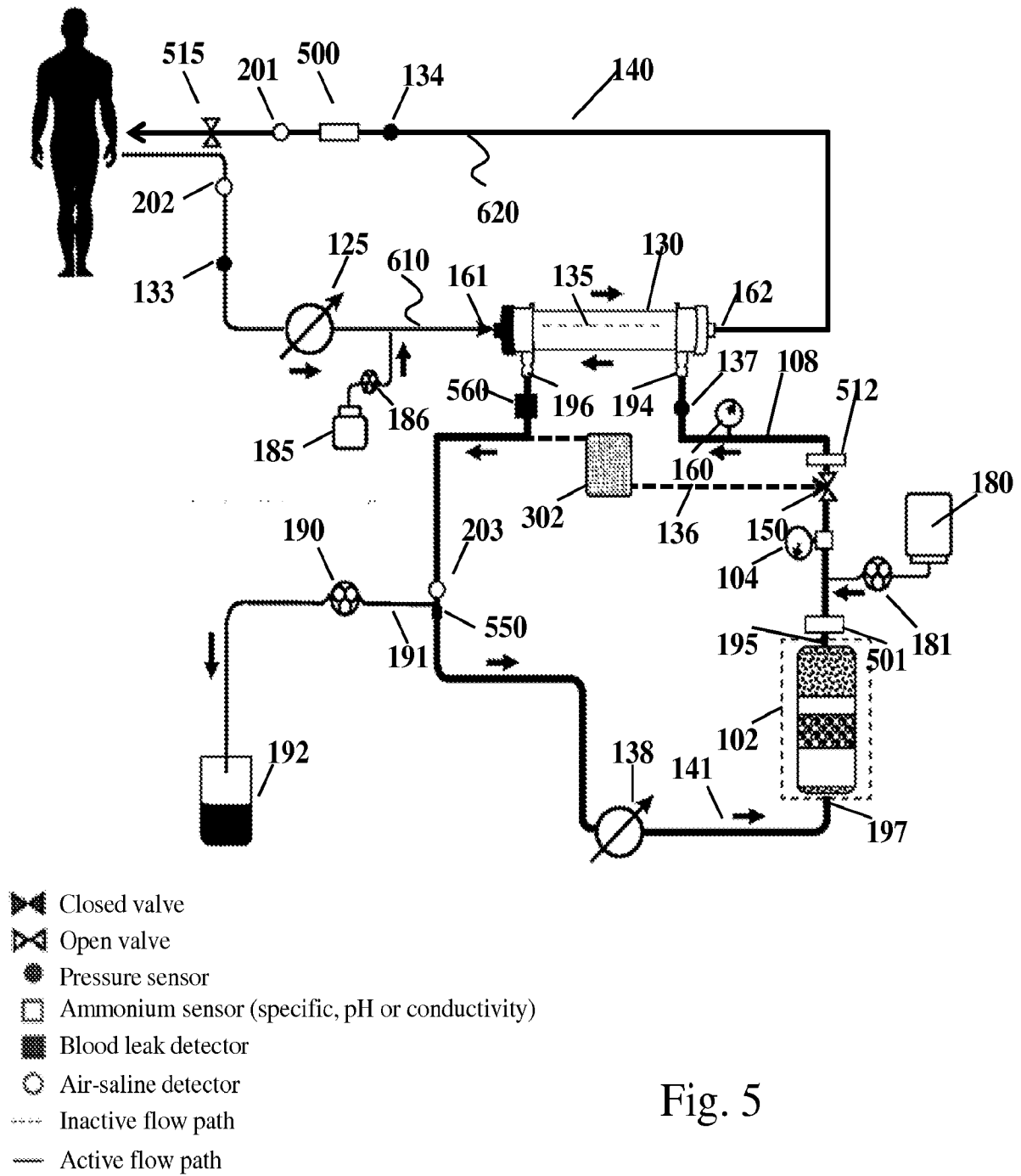
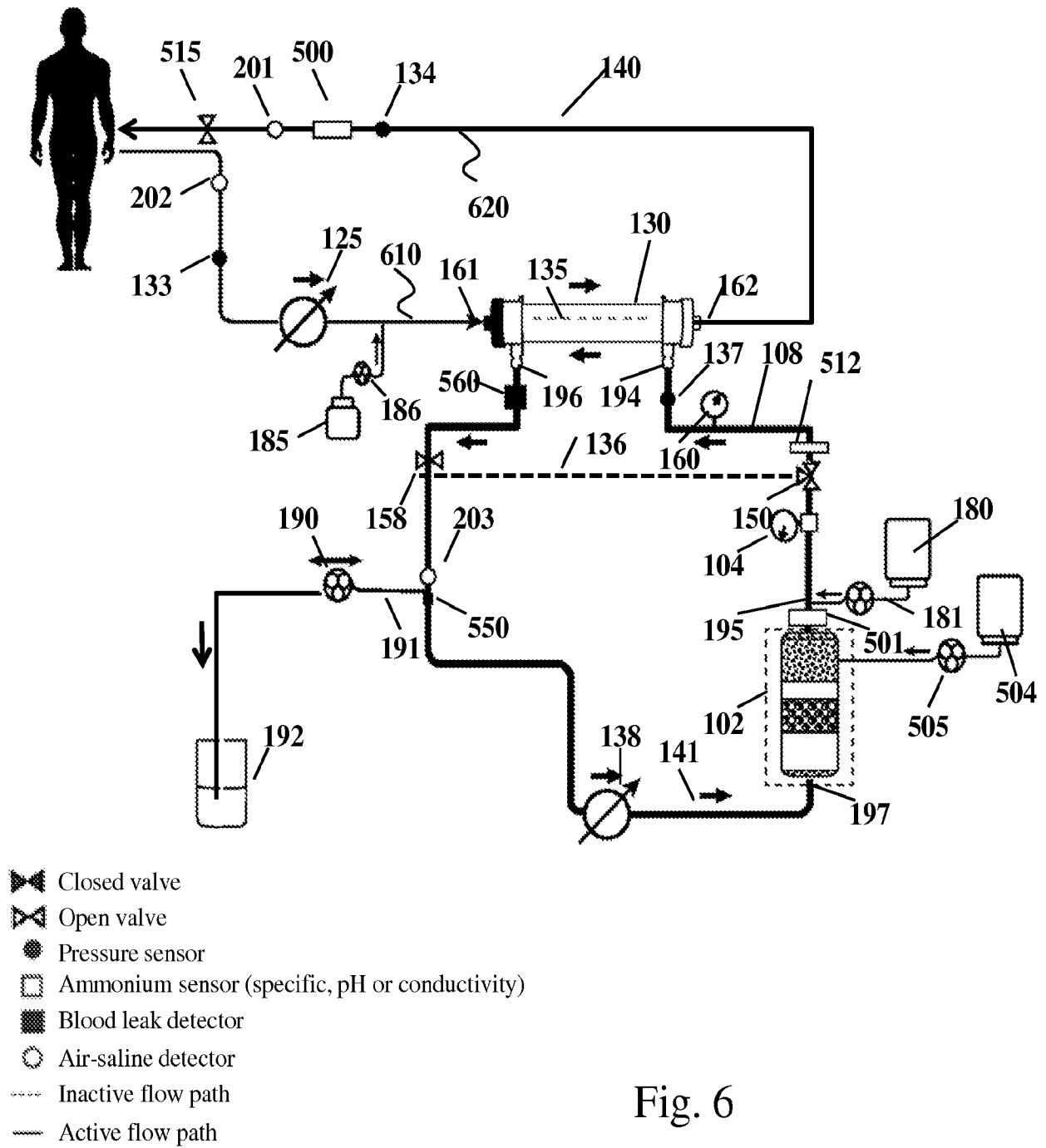


Fig. 5



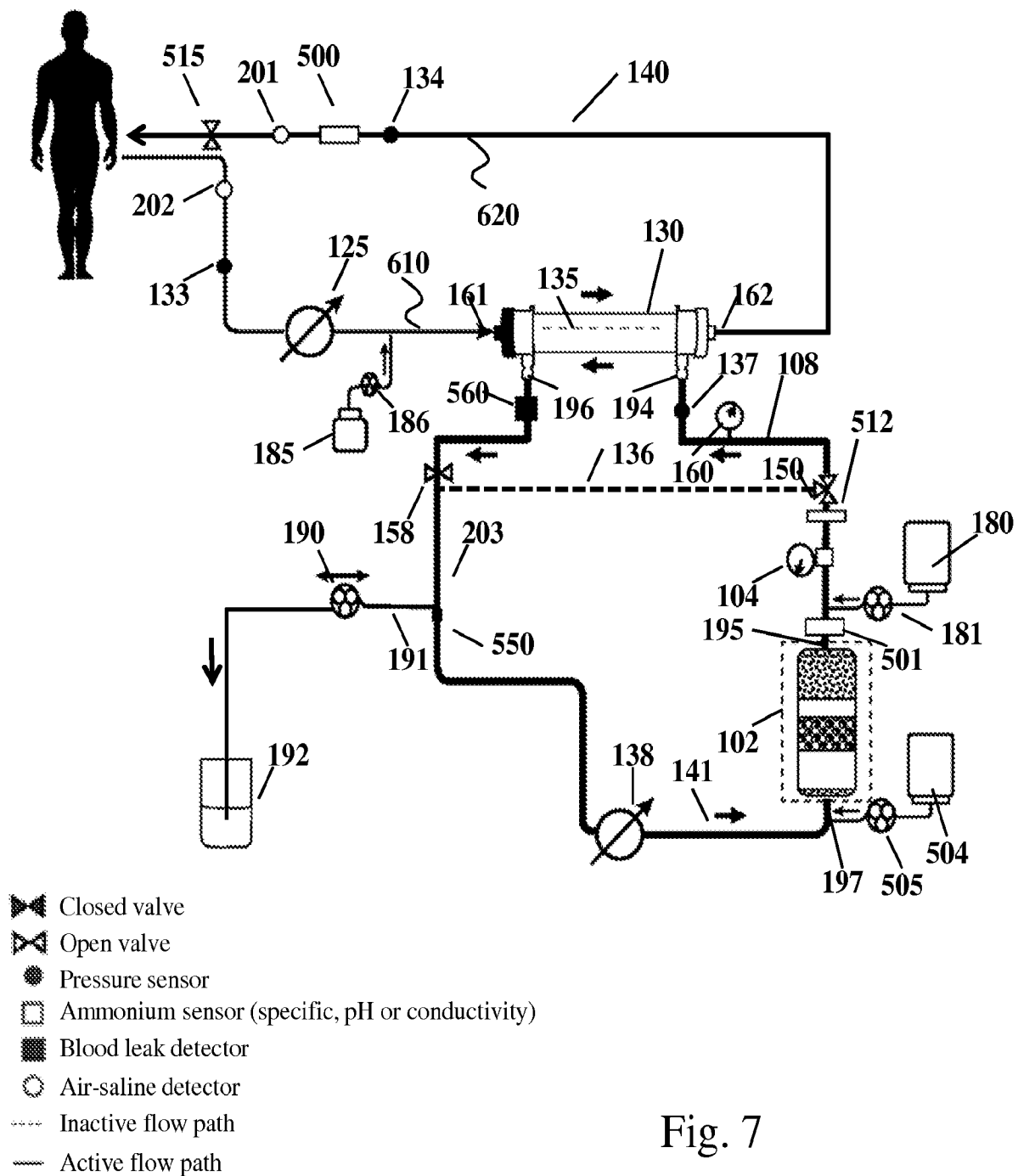


Fig. 7

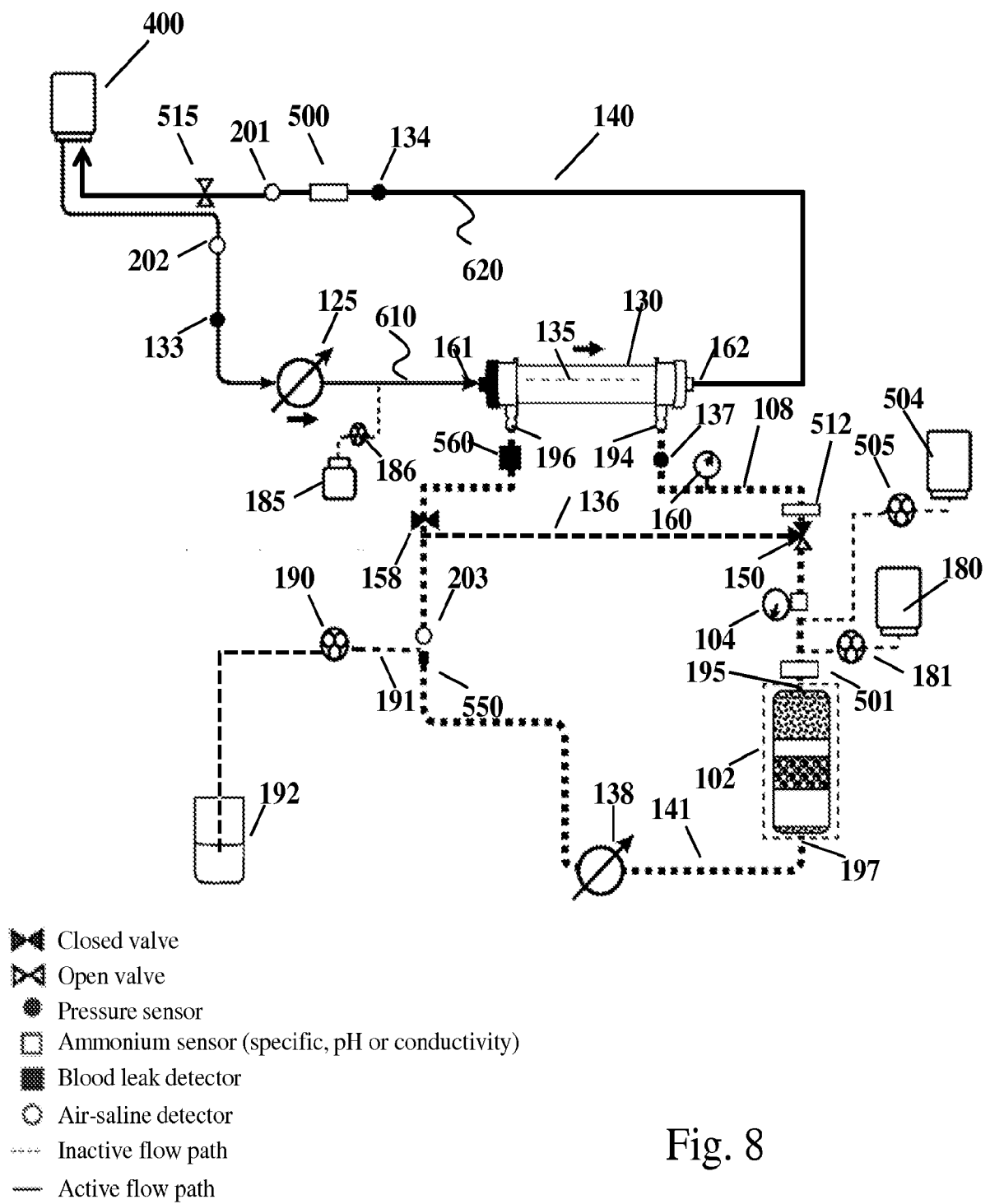
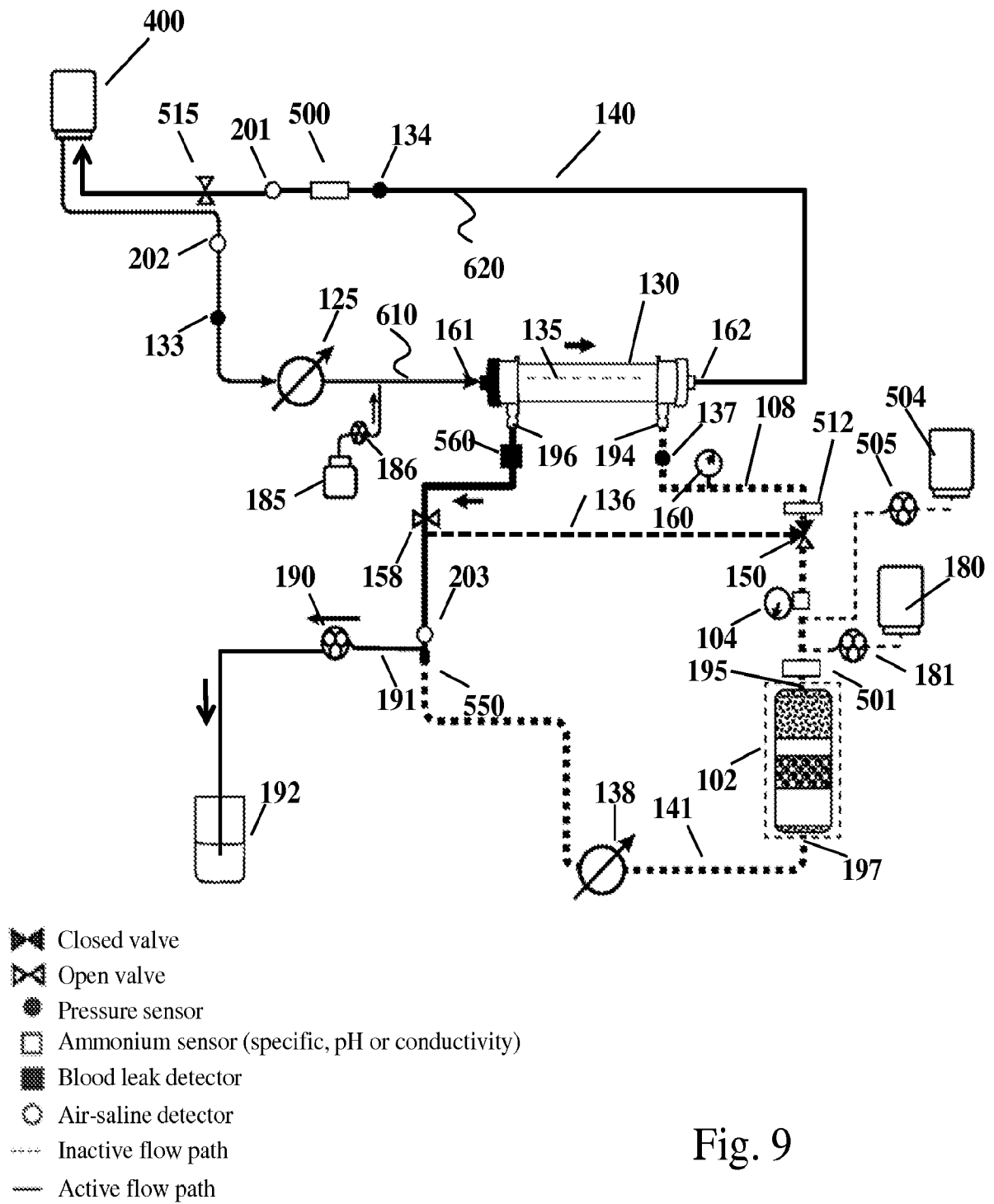
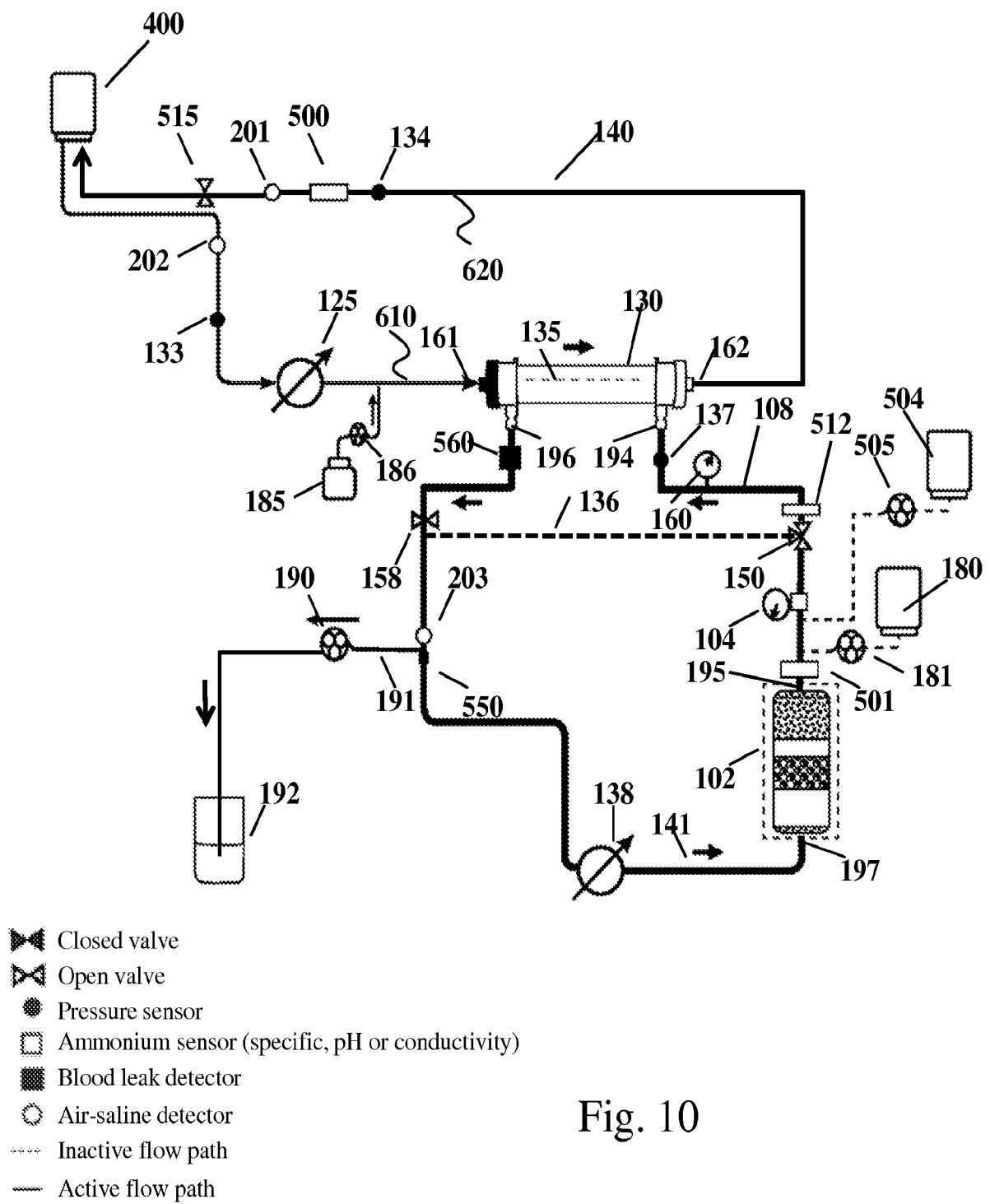


Fig. 8





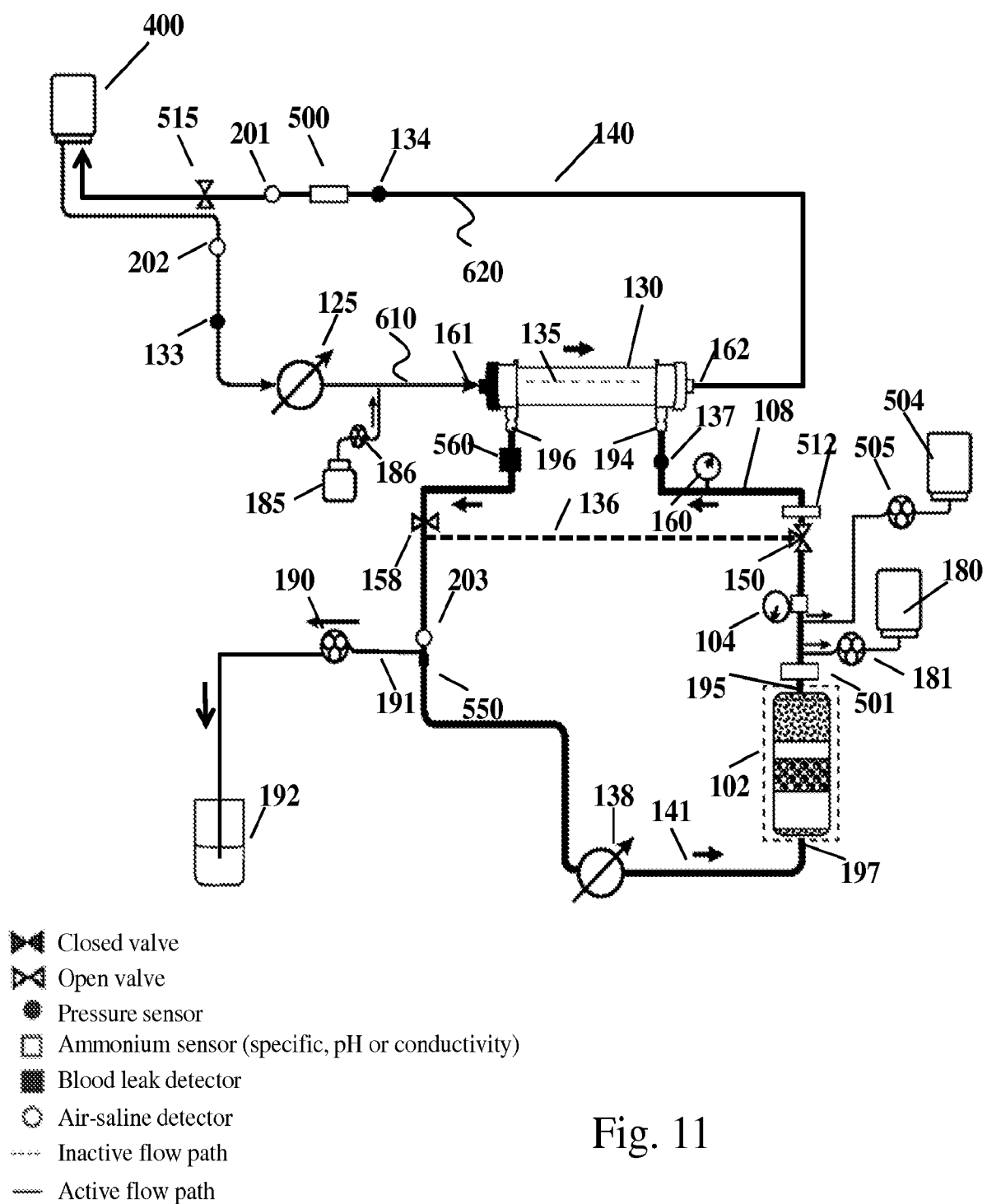
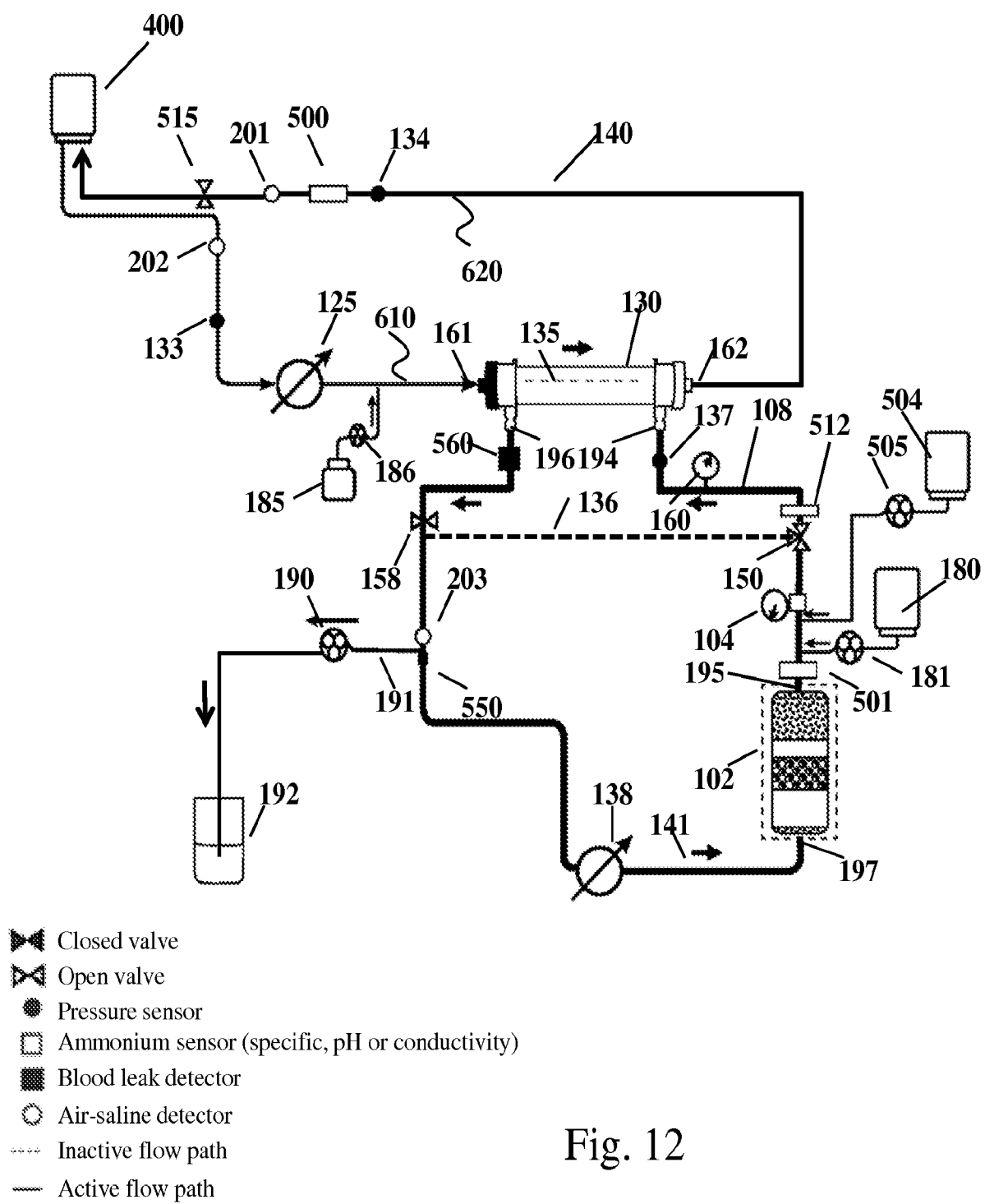
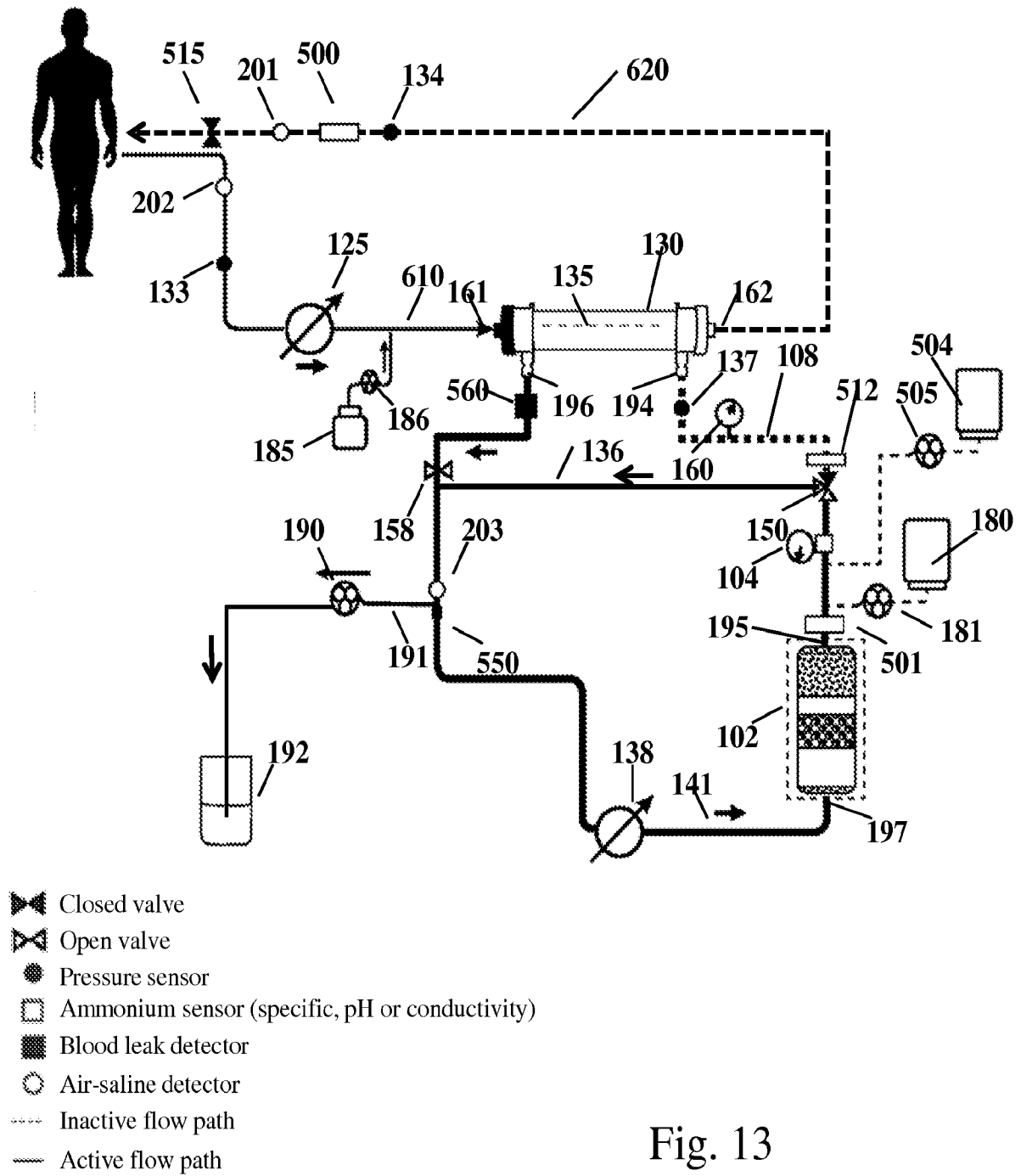


Fig. 11





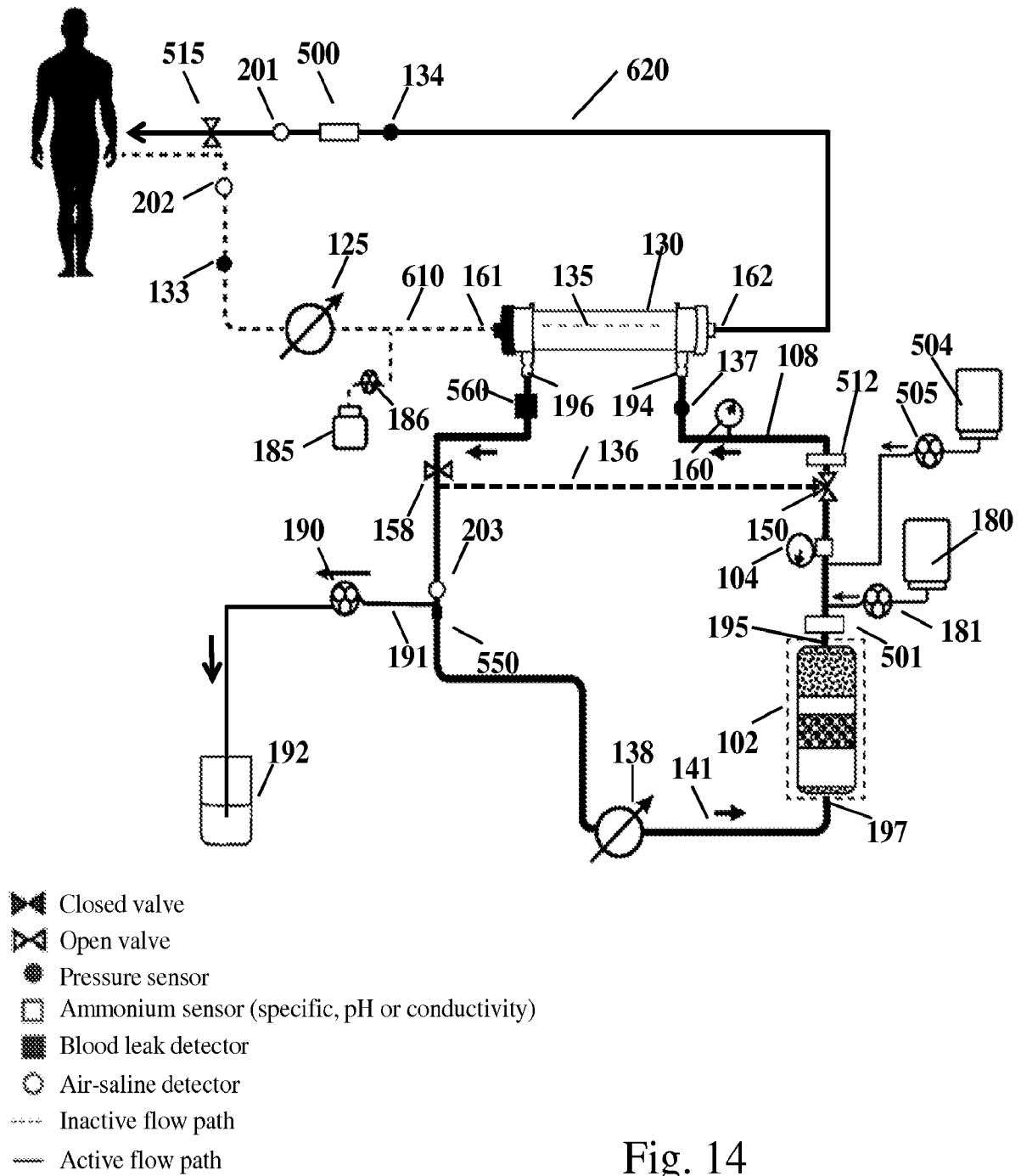


Fig. 14

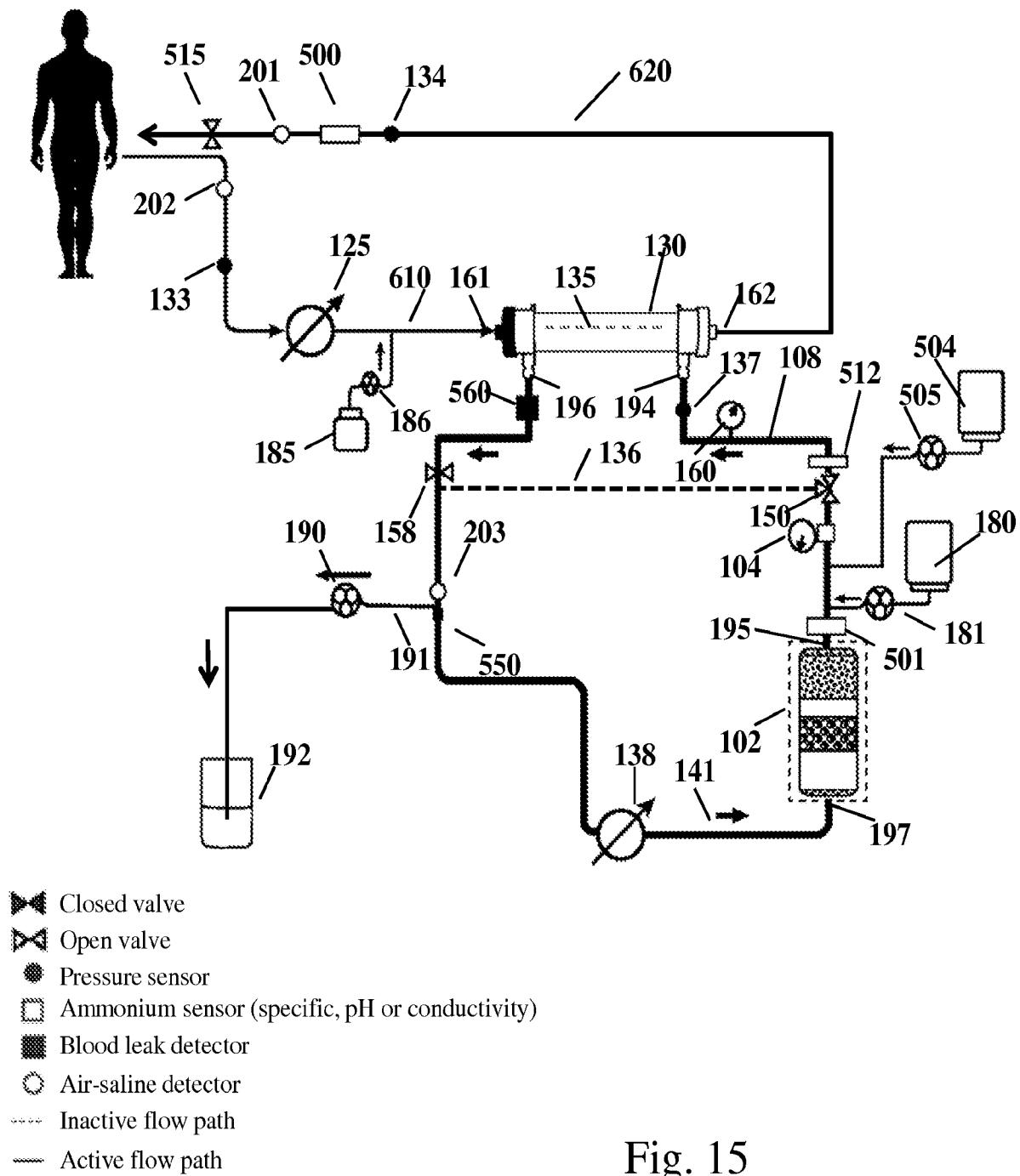


Fig. 15

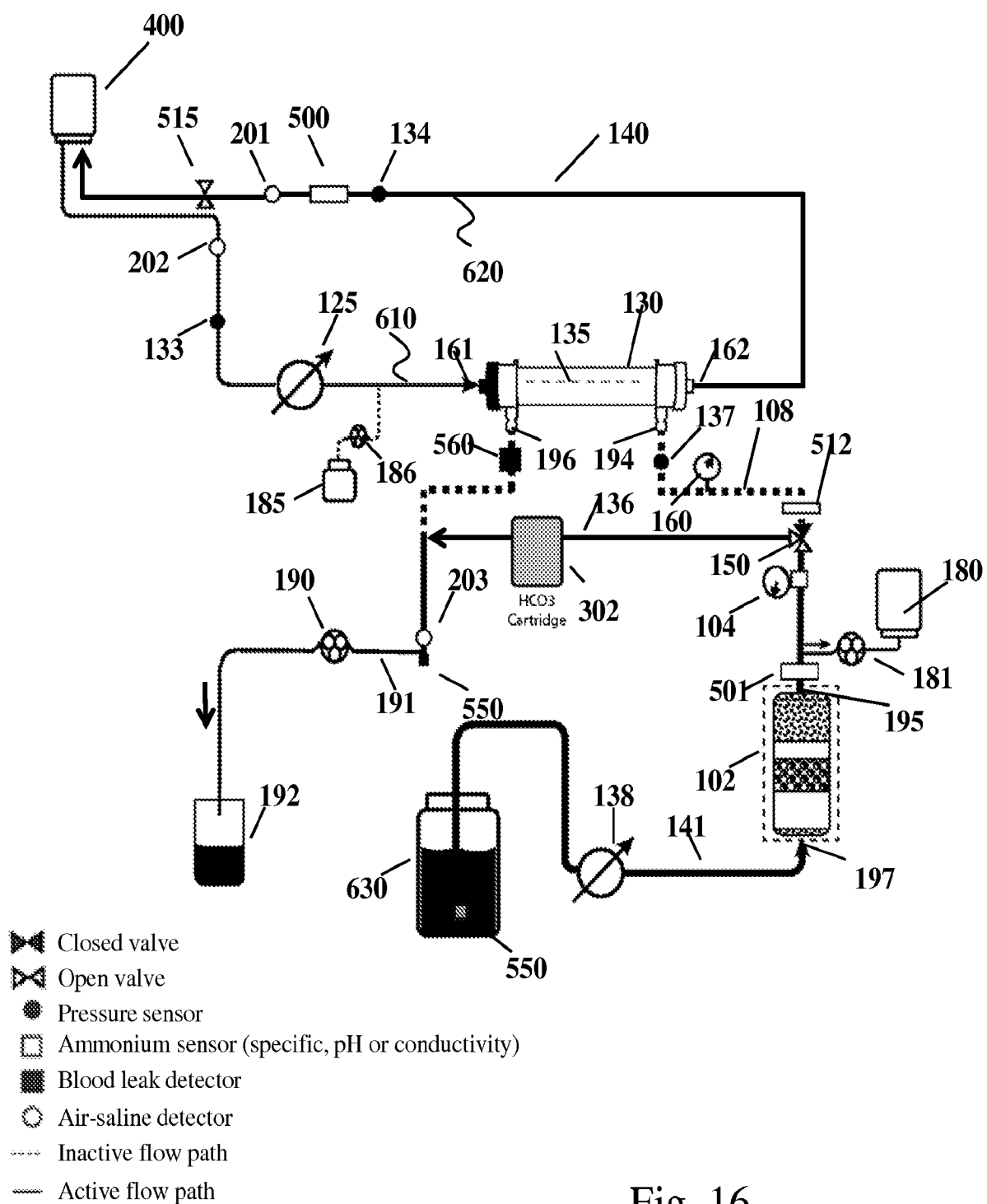


Fig. 16

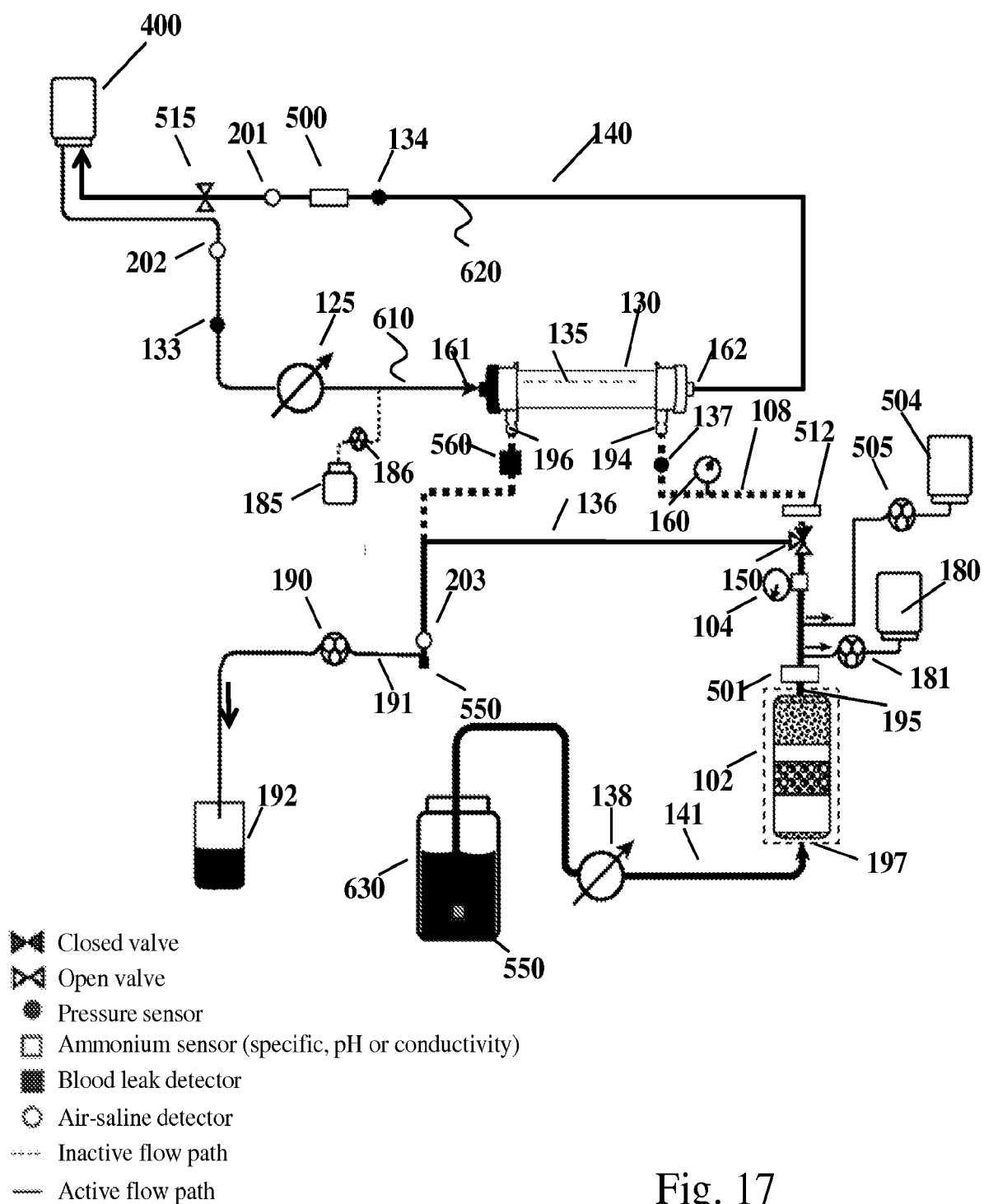


Fig. 17

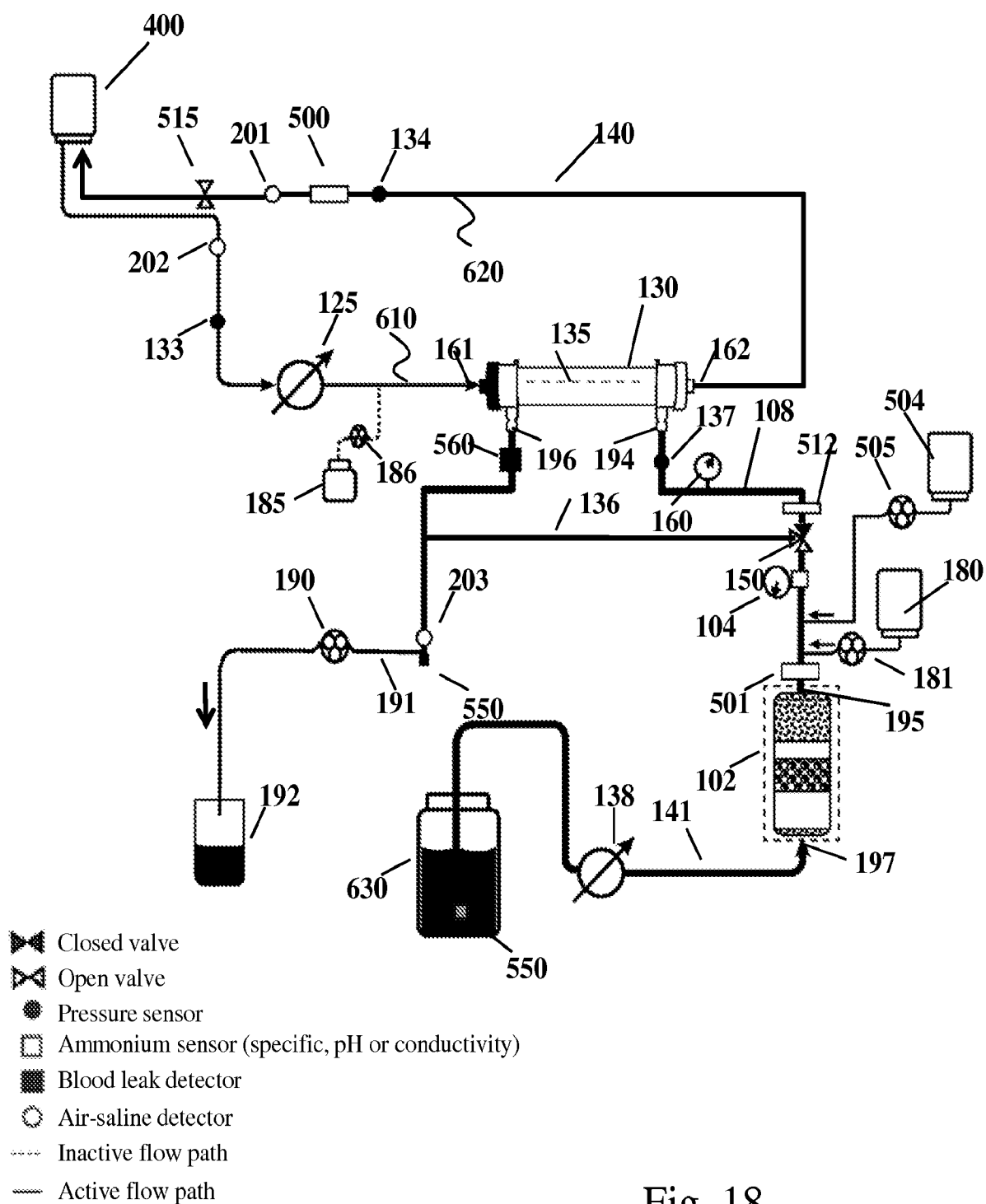


Fig. 18

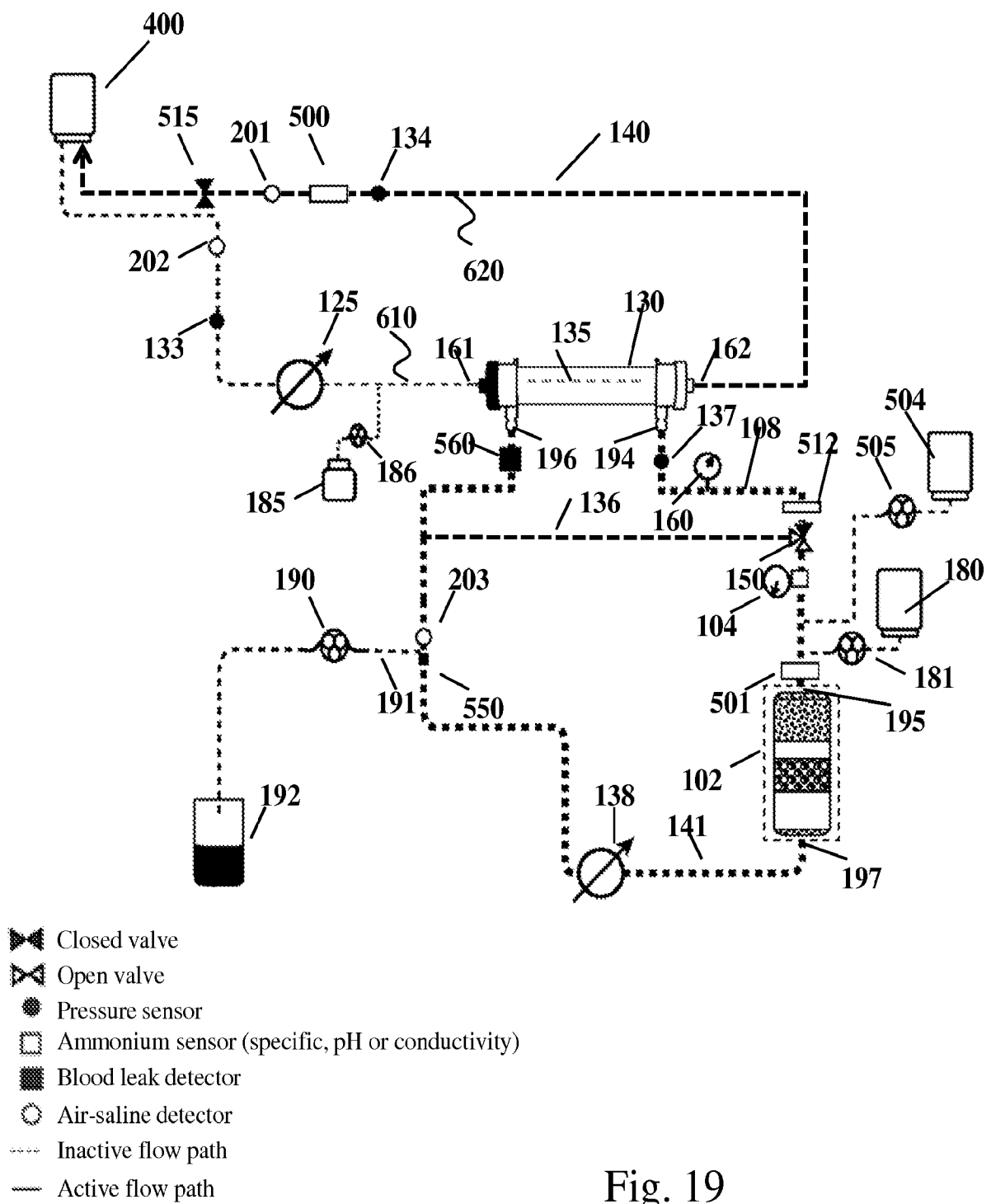
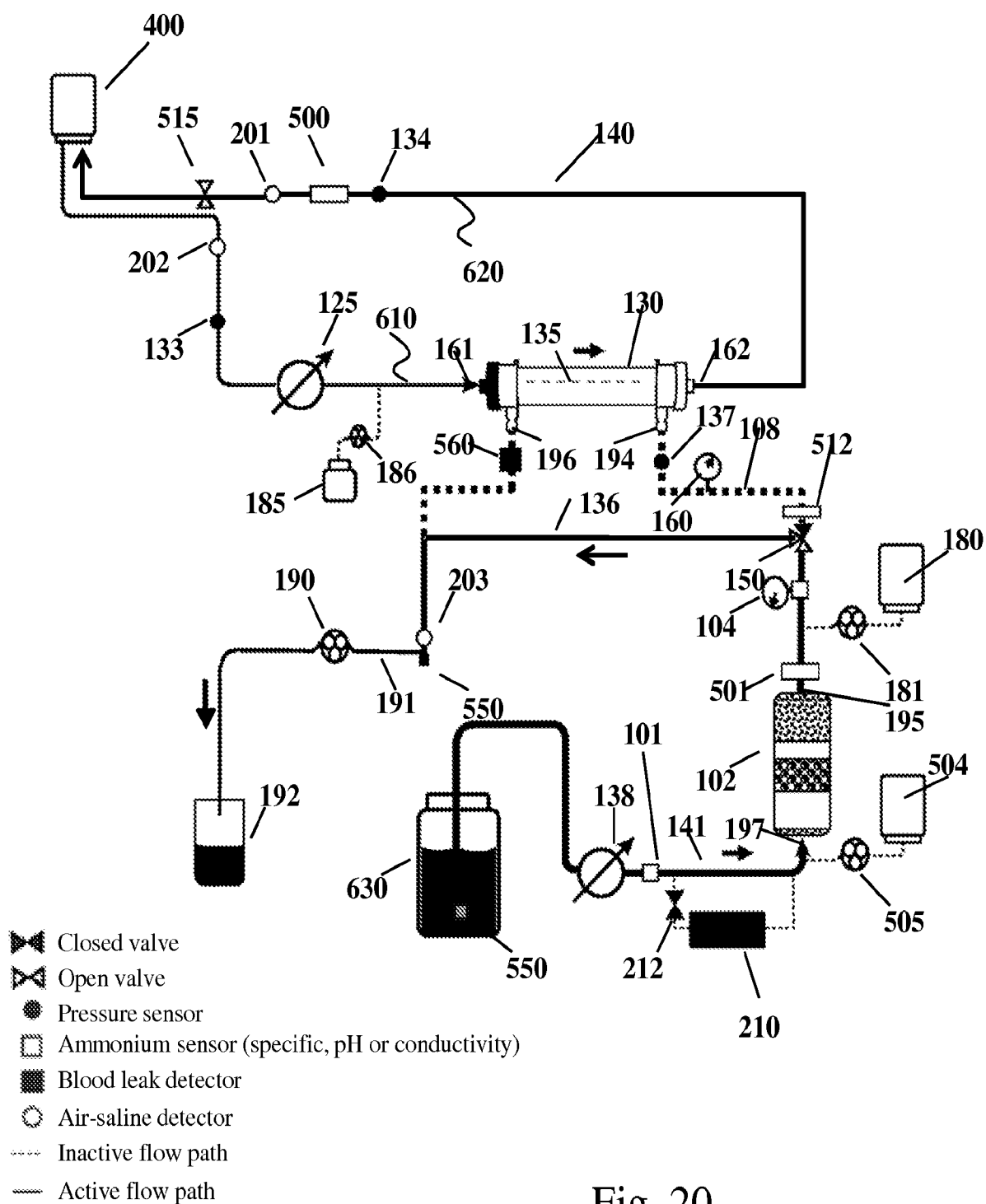
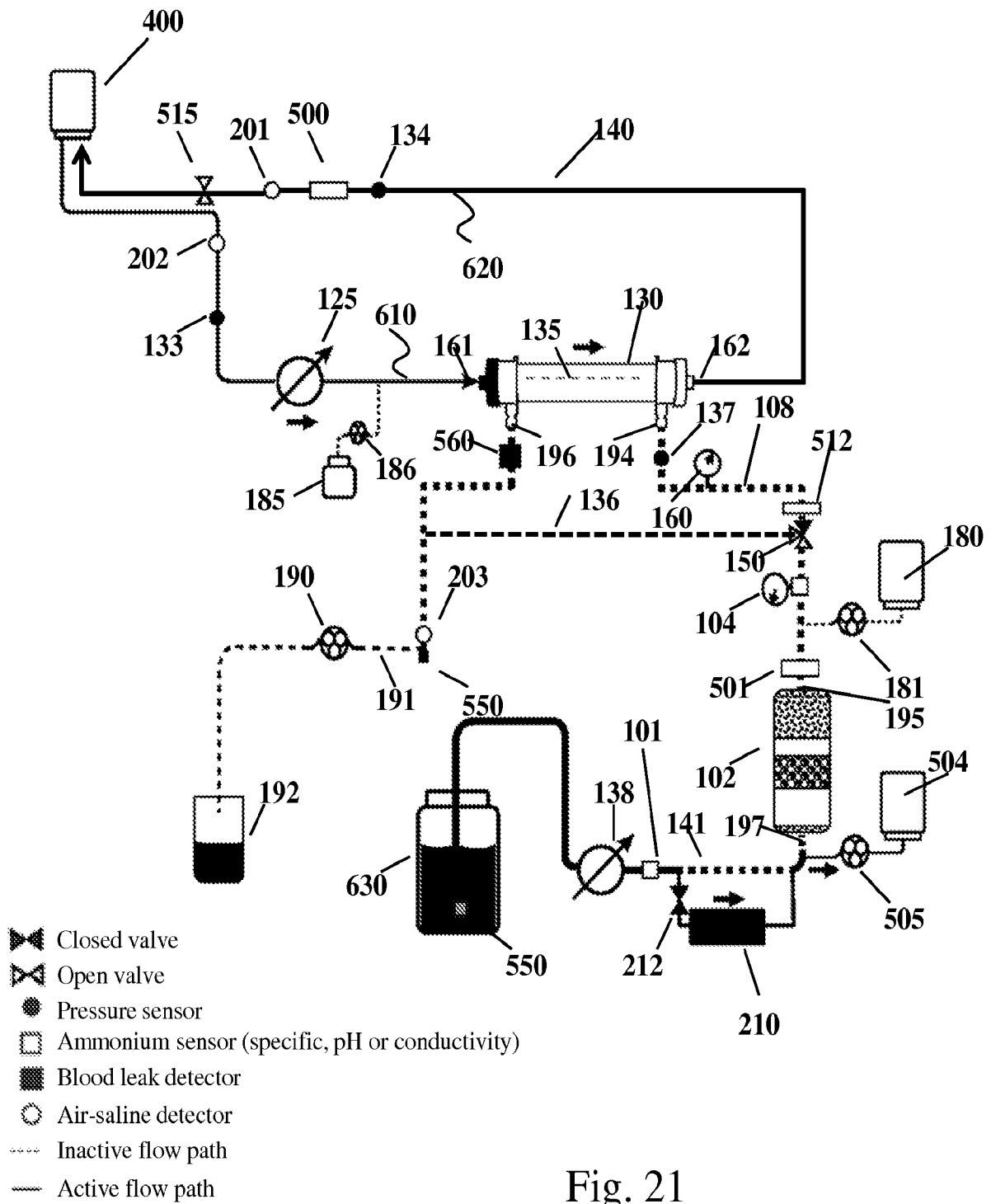


Fig. 19





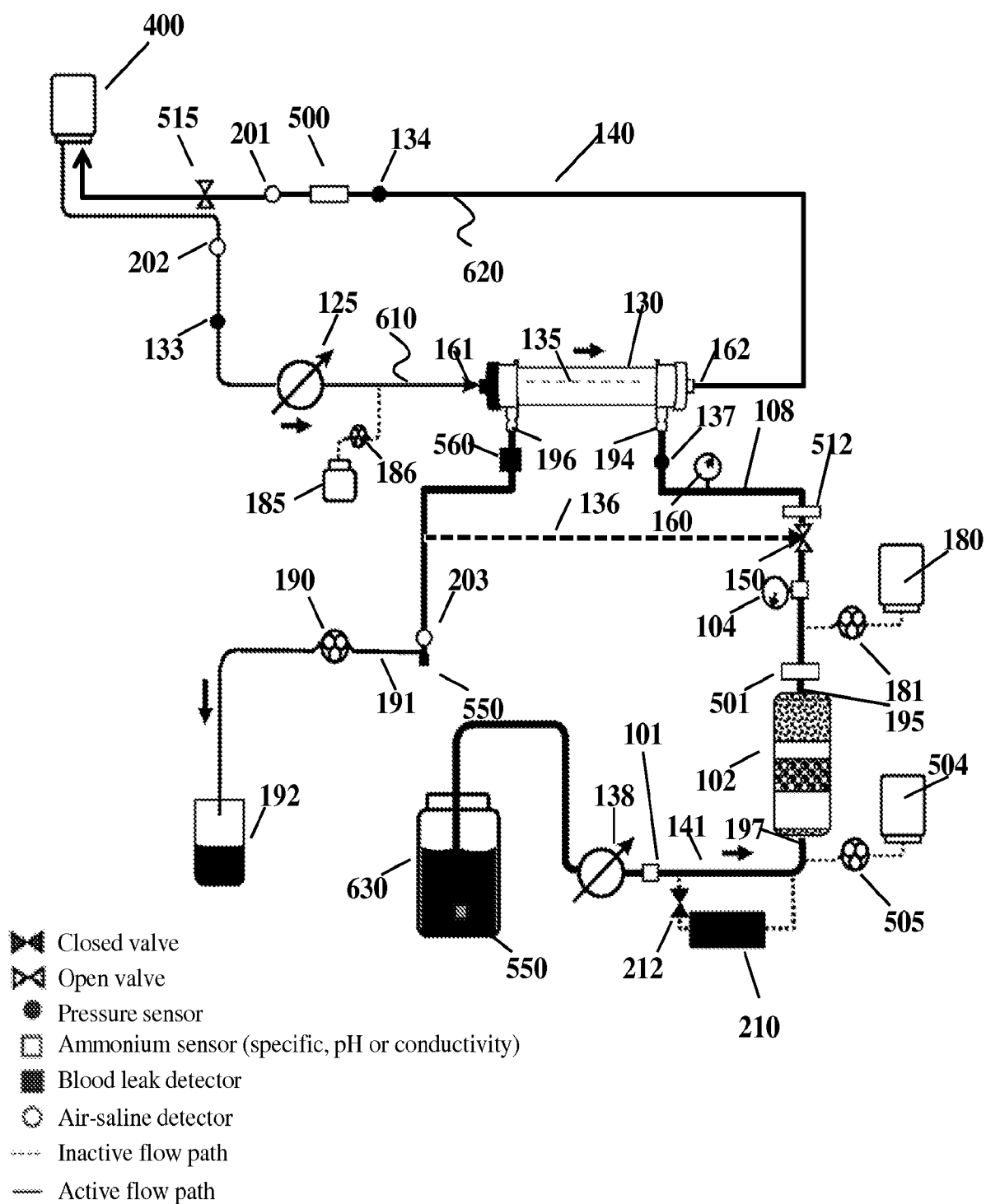


Fig. 22

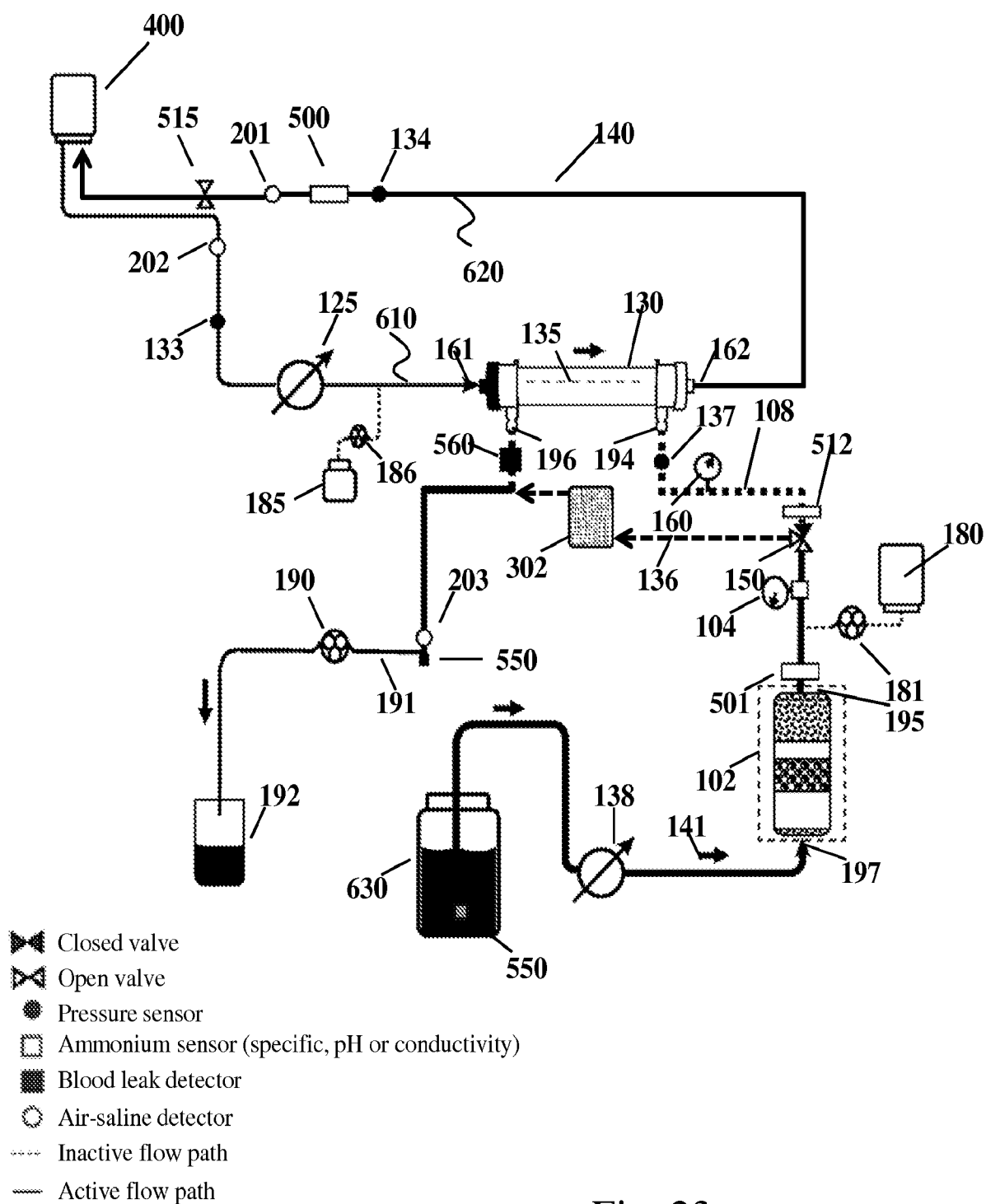
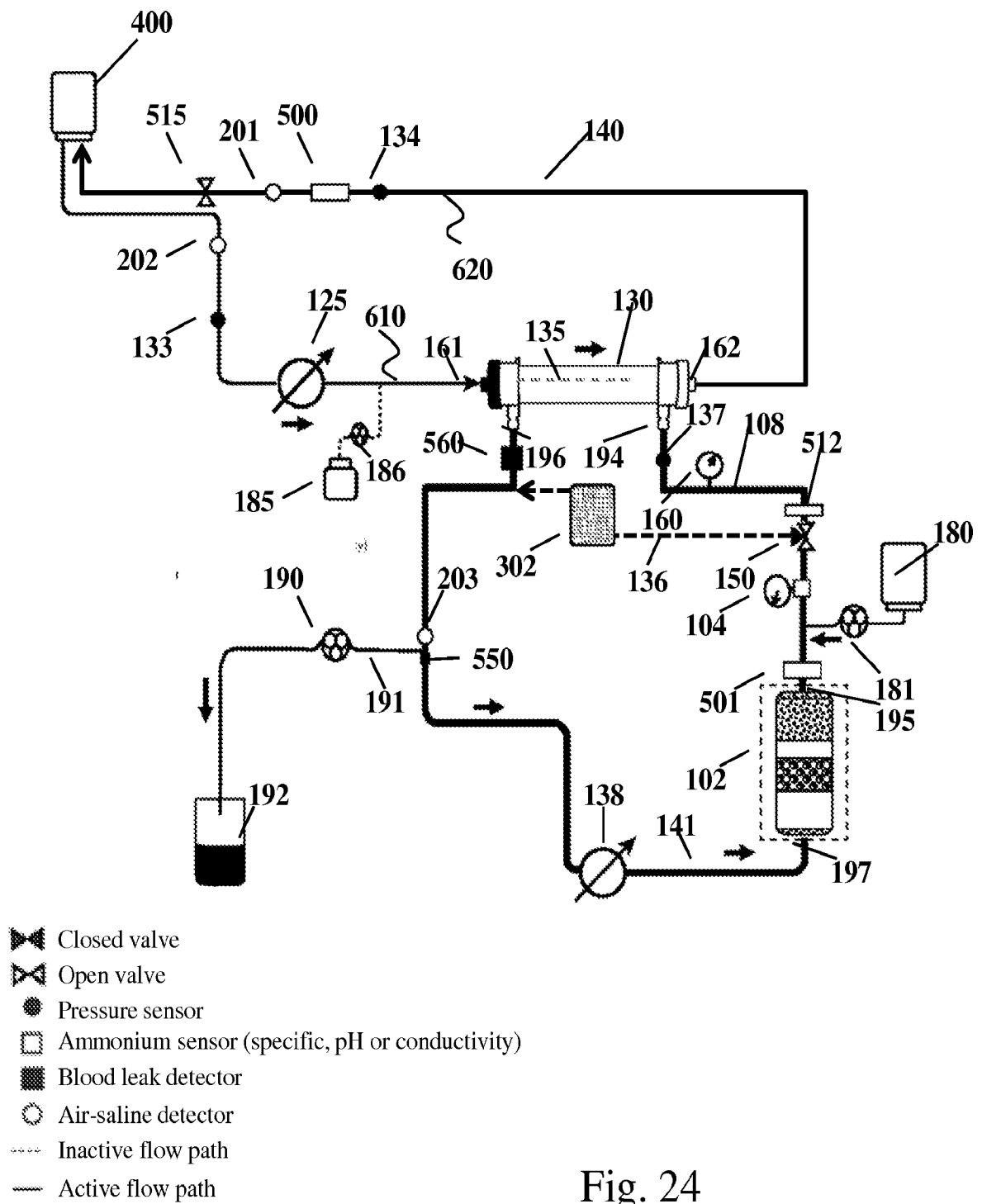


Fig. 23



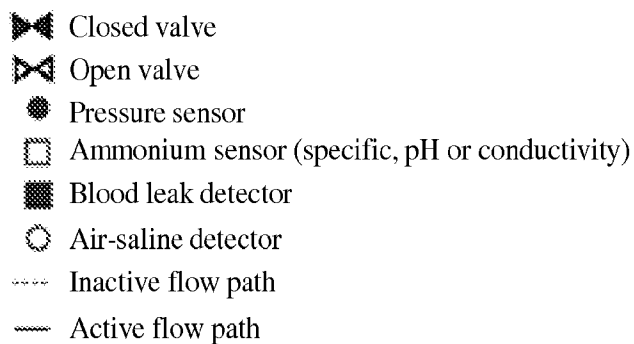
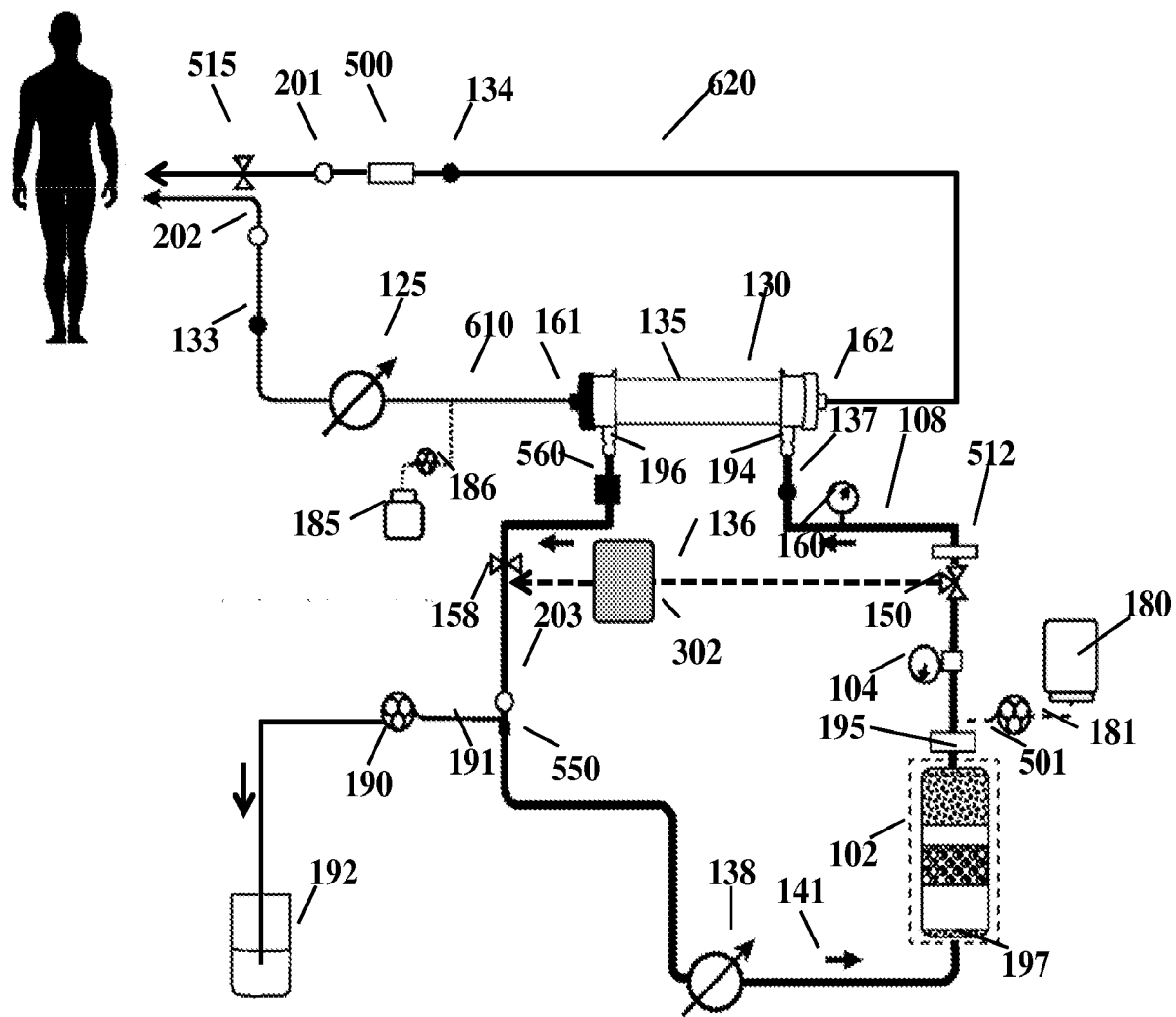


Fig. 25

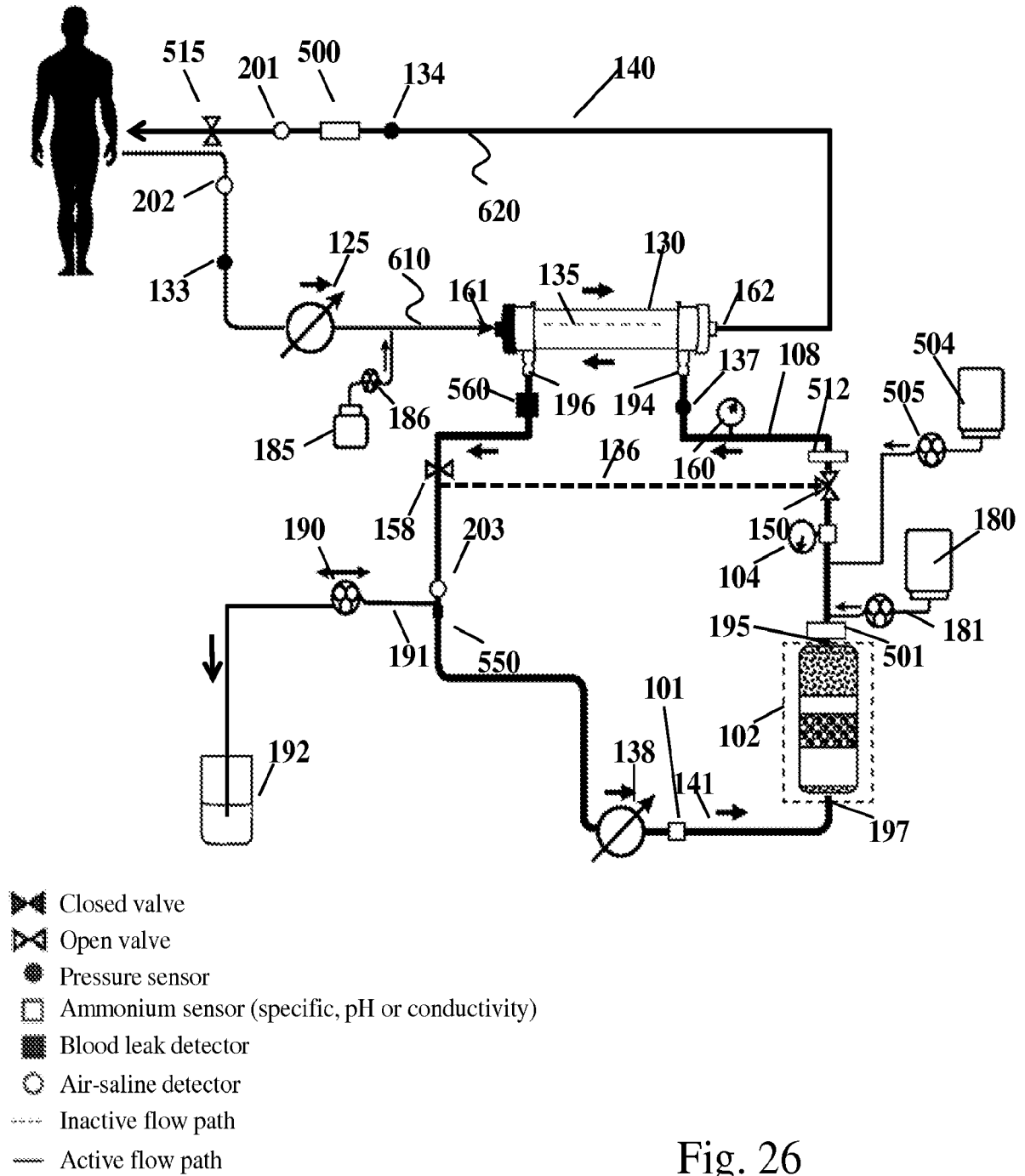


Fig. 26

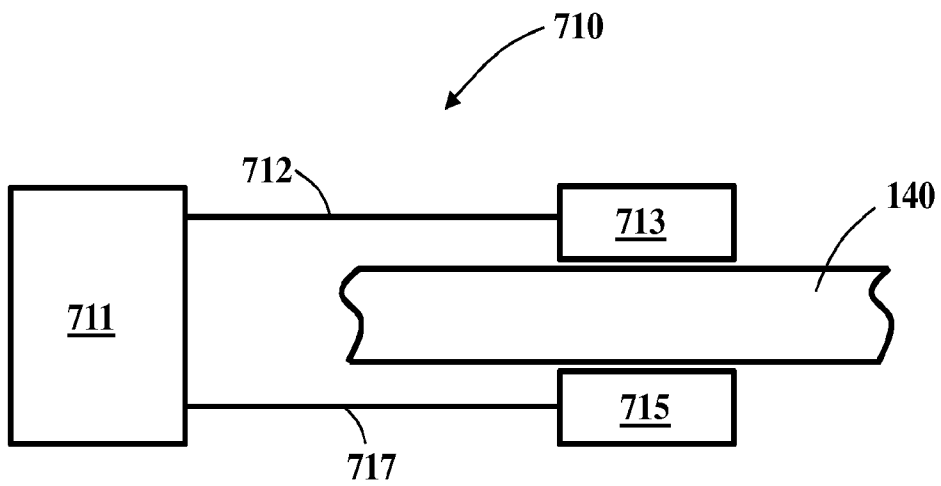


Fig. 27

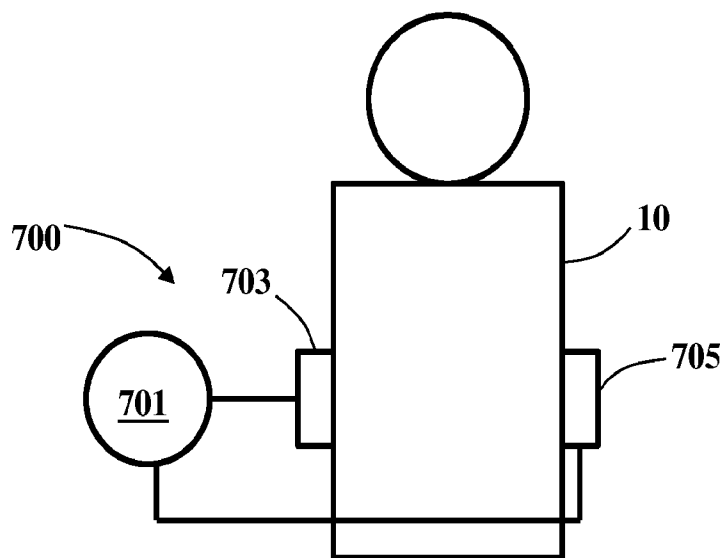


Fig. 28

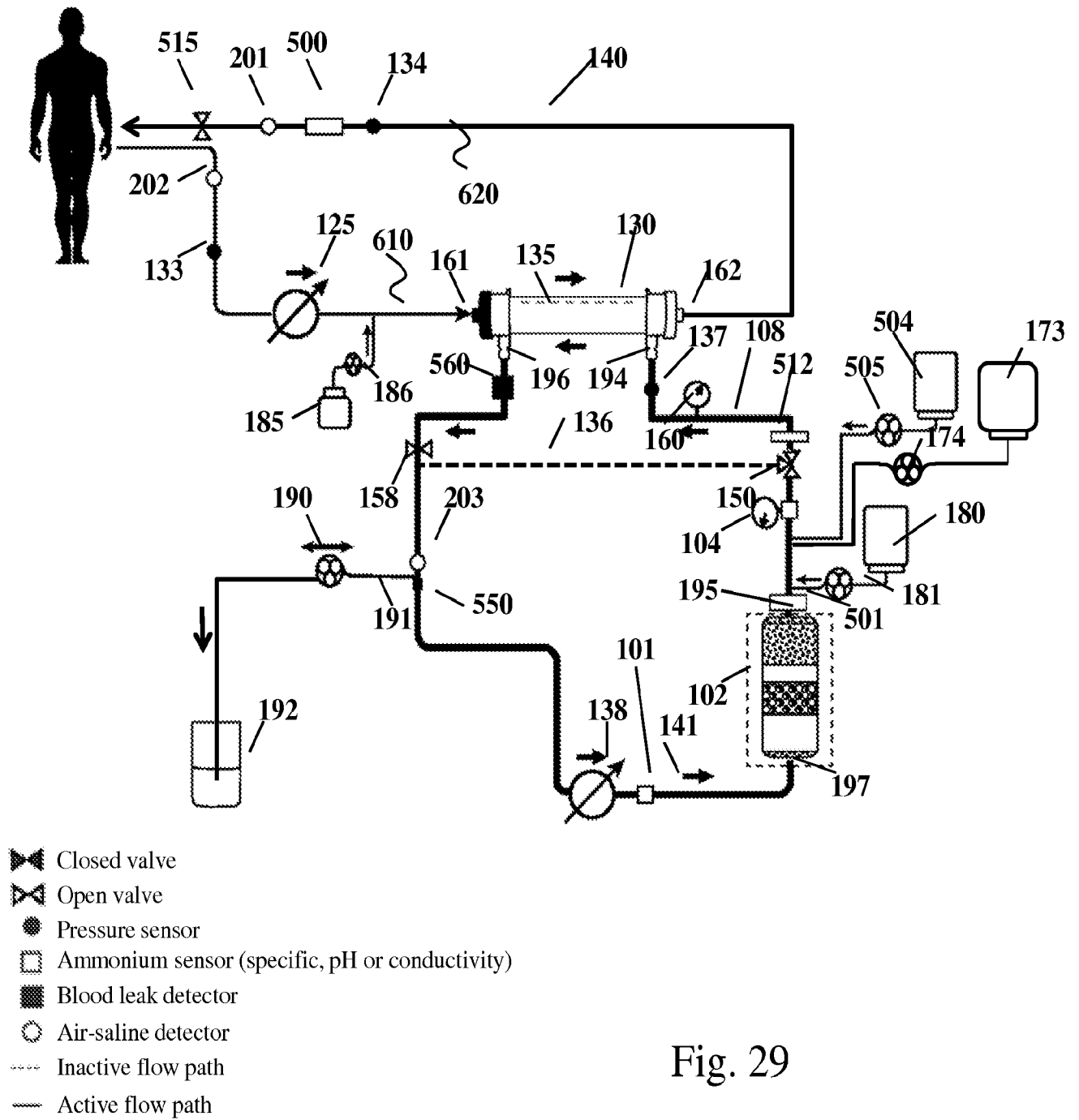


Fig. 29

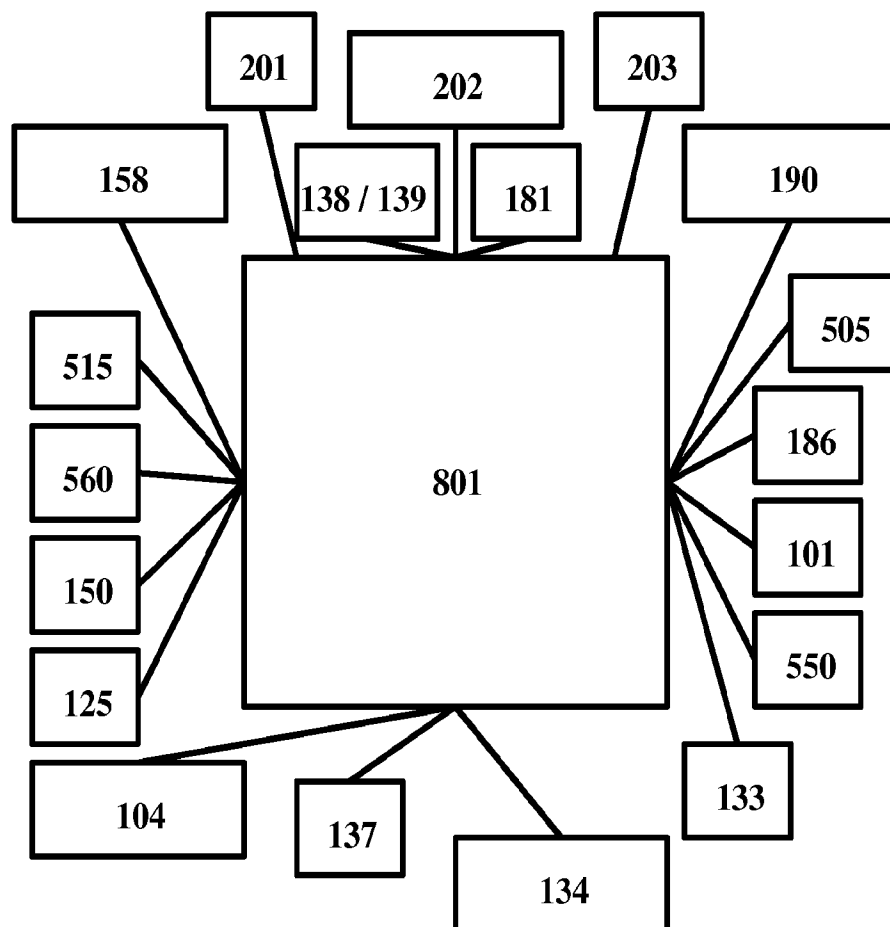


Fig. 30