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⑤4 METHOD OF PRODUCING CEMENTED CARBIDE OR CERMET ALLOY.

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Description

Field of the Invention

5 The present invention relates to a method of preparing a cemented carbide or a cermet alloy, and more particularly, it relates to a method of preparing a cemented carbide or a cermet alloy by shaping cemented carbide powder or cermet alloy powder into a prescribed configuration by an injection molding method, thereafter removing an organic binder and sintering the compact.

10 Background Art

A cemented carbide and a cermet alloy are materials having high melting points. In order to obtain a cemented carbide sintered compact or a cermet alloy sintered compact, therefore, a powder metallurgy method of press-molding or CIP-molding a powder raw material and thereafter sintering the same has 15 generally been employed. In this method, however, manufacturable configurations are significantly restricted. In order to obtain a complicated final configuration, it is necessary to grind the sintered compact with a diamond grindstone after sintering, leading to an extremely high cost.

20 A technique of molding plastic by an injection molding method is widely known. Japanese Patent Publication No. 62-33282 discloses a method of kneading metal powder or ceramics powder with an organic binder and shaping the same into an article having a complicated configuration by injection molding.

25 When such a powder injection molding technique is applied to a cemented carbide or a cermet alloy, however, the following problems take place: Cemented carbide powder or cermet alloy powder is fine powder whose particle diameter is about 1 μm . Further, such an alloy has large gravity. In addition, tolerance for carbon concentration in the alloy is small. Due to such material properties of the cemented carbide or the cermet alloy, deformation and imperfection are easily caused during debinder processing. Besides, it is impossible to obtain an alloy of good quality, due to an influence exerted by residual carbon which is caused by decomposition of the organic binder. In order to avoid such problems, it is necessary to perform debinder processing for an extremely long time. Due to presence of the aforementioned problems, an injection molding technique for a cemented carbide and a cermet alloy has not yet been substantially 30 put into practice.

Disclosure of the Invention

An object of the present invention is to provide a method which can obtain a cemented carbide or a 35 cermet alloy of high quality by efficiently shaping cemented carbide powder or cermet alloy powder by an injection molding method, and through subsequent debinder processing and sintering processing.

Another object of the present invention is to provide a method which causes no deformation and imperfection of a compact in debinder processing.

Still another object of the present invention is to provide a method which can perform debinder 40 processing in a short time.

In accordance with claim 1, the method of preparing a cemented carbide or a cermet alloy to be the premise for the present invention comprises a step of mixing/kneading cemented carbide powder or cermet alloy powder with an organic binder, a step of shaping this mixed powder into a prescribed configuration by an injection molding method, and a step of thereafter removing the organic binder from the compact and 45 sintering the same. In such a method, the removal of the organic binder is first performed in an inert gas atmosphere as a first removal step, and then performed in a vacuum with a pressure of less than 1 Torr (1.3 10^{-3} bar) in continuation as a second removal step.

According to one aspect of the present invention, the organic binder contains a plurality of types of 50 binders, which are divided into a group removable under a low temperature and a group removed under a high temperature. Compositions of the respective binders contained in the organic binder are selected to satisfy such a condition that the loss rate of the high-temperature removal group is within 5 % when the low-temperature removal group is lost by 30 % of the whole in an inert gas atmospheric pressure heating loss test (TG) for only the organic binder. Preferably the rate of the binder belonging to the low-temperature removal group with respect to the overall organic binder is set to be at least 30 % and not more than 90 %.

55 According to another aspect of the present invention, a temperature for transition from the first removal step to the second removal step is selected to satisfy the following condition: The condition is such a condition that the amount of removal of the binder belonging to the low-temperature removal group is at least 30 % with respect to the overall organic binder, while the residual rate of the binder belonging to the

high-temperature removal group is at least 5 % with respect to the overall organic binder. A binder for serving as the main component of the low-temperature removal group is preferably prepared from wax having hydrophilic polar groups, with a melting point of not more than 80 °C. Sintering is preferably performed in a vacuum under a pressure of not more than 0.05 Torr (6.6 10⁻⁵ bar).

5 After the organic binder is removed from the compact by the aforementioned method, sintering processing may be performed in continuation. Alternatively, the compact may be once cooled after the organic binder is removed, to be thereafter sintered.

An injection-molded compact is formed by powder and a binder, substantially with no voids. When the compact is subjected to temperature rising in this state, the binder first escapes by expansion of the binder, 10 and then debinding progresses due to evaporation from the surface. When debinding of 30 % progresses by such a process, pores communicating with the surface are formed in the interior of the compact. Gas generated in the interior of the compact is removed through the pores, to further promote debinding. However, if the gas is generated in the interior of the compact in a debinding state of less than 30 %, the compact is cracked or blistered. In order to prevent such cracking or blistering of the 15 compact, it is necessary to suppress generation of the gas in the interior of the compact with a loose programming rate. Therefore, a long time is required for the debinder processing. Wax for serving as a plasticizer and high polymer resin for serving as a binder are required as the binders. Since wax evaporates at a low temperature with no decomposition, it is possible to relatively easily perform debinding. On the other hand, high molecular weight polymer resin is apt to cause imperfection in the compact in an initial 20 stage of debinding, since the same generates a large quantity of gas by decomposition.

The inventors have noted the aforementioned points, to achieve the present invention. In more concrete terms, selected is high molecular weight polymer resin which will start no decomposition even if the temperature reaches such a level that the wax is removed by at least 30 % of the whole, and this high molecular weight polymer resin is mixed with the wax. In an initial state of debinder processing, debinding 25 of at least 30 % is facilitated by evaporation of the wax alone, to form continuous pores in the interior of the compact. After the pores are formed, decomposition of the high polymer resin is made to start.

Hoechst wax, carnauba wax, montan wax, ozokerite wax, auriculine wax, candelilla wax, beeswax, microcrystalline wax and the like can be cited as major wax materials of the low-temperature removal group. Low density polyethylene, low molecular weight polyethylene, ethylene-vinyl acetate, polypropylene, acrylic 30 resin and the like can be cited as binders of the high-temperature removal group.

In the initial state of debinder processing, the atmosphere pressure is maintained in excess of the atmospheric pressure, thereby preventing the compact from imperfection. After continuous pores are formed in the interior of the compact, the atmosphere pressure is brought into a decompressed state, or a state close to a vacuum, thereby facilitating evaporation of gas from the surface and desorption of gas 35 generated in the interior of the compact.

Note the strength of the injection-molded compact. When the high molecular weight resin serving as a bonding agent is removed, bonding strength between the powder particles is extremely reduced, such that a cemented carbide etc. having high specific gravity inevitably collapses. In order to prevent this, it is necessary to attain strength by bonding powder materials for forming the alloy. However, since the surfaces 40 of the alloy powder materials are covered with thin oxide films, bonding is hardly caused by diffusion. The inventors have found that, when removal of the binder is performed in a vacuum state, the surfaces of the alloy powder materials are deoxidized by ambient carbon, whereby bonding strength is attained between the alloy powder materials. Thus, according to the present invention, debinding in the vacuum state is facilitated thereby bonding the powder particles with each other. When the powder particles are bonded 45 with each other, the compact will not collapse until debinding is terminated. In a preferred embodiment of the present invention, the debinder processing is performed in two stages of a first removal step and a second removal step. The first removal step is carried out under an atmospheric pressure atmosphere, and the second removal step is carried out under a vacuum atmosphere. In transition from the first removal step to the second removal step, the bonding agent must be left by at least 5 %. If the residual amount of the 50 bonding agent is not more than 5 %, the compact will collapse before bonding strength is attained between the powder particles.

The atmosphere for the debinder processing is now described. The first removal step is carried out in an atmosphere of inert gas such as N₂ or Ar. If the debinder processing is performed in an oxidizing atmosphere such as the air, surface oxidation of Co, Ni and the like inevitably progresses during progress 55 of the debinding. If such surface oxidized layers are present, bonding strength by reduction is inevitably lowered in the second removal step. Further, since oxidation of only a portion exposed to the ambient atmosphere progresses with progress of debinding, carbon concentration in the alloy is ununiformized and a liquid phase appearance temperature in sintering is ununiformized, to significantly reduce dimen-

sional accuracy. Contrary to the invention, it would be conceivable to attain reduction of the oxide films on the surfaces of the alloy powder materials, by carrying out the second removal step not in a vacuum but in an H₂ atmosphere. If debinder processing is performed in an H₂ atmosphere, however, simultaneously caused is such reaction that carbide C, which is a hard phase forming component of the cemented carbide or the cermet alloy, reacts with hydrogen to form CH₄. Thus, the carbon content of the alloy is reduced.

The types of wax are now described. The surface of cemented carbide powder or cermet alloy powder is hydrophilic. On the other hand, wax such as n-paraffin is hydrophobic. Therefore, wettability between wax such as n-paraffin and cemented carbide powder or cermet alloy powder is inferior. In order to attain viscosity which is required for injection molding, therefore, it is necessary to use a larger amount of wax.

10 The inventors have studied various wax materials, to find that the amount of the binder can be reduced by employing a certain type of natural wax having hydrophilic polar groups. When the compact is taken out from a metal mold in injection molding, the compact is easily broken since wax is friable. In order to prevent such breakage, it is preferable to use wax at least having a melting point of not more than 80 °C. So far as the wax has hydrophilic polar groups with a melting point of not more than 80 °C, its effect remains

15 unchanged whether the same is a synthetic or natural one. While stearic acid or the like may be employed as a lubricant, the effect of the present invention remains unchanged even if such a minor additive is employed.

Best Modes for Carrying Out the Invention

20 Example 1

80 % of WC powder having a particle diameter of 2 to 4 µm, 10 % of TiC powder having a particle diameter of 1 to 2 µm, and 10 % of Co powder having a particle diameter of 2 to 4 µm were mixed in a wet ball mill for 3 hours, and dried. 6.0 % of beeswax and 1.0 % of low molecular weight polyethylene were added to 100 % of this mixed powder, and these were kneaded at 120 °C for 30 minutes. Then, this raw material mixture was cooled/solidified and thereafter pulverized, to prepare raw material particles of 0.5 to 2.0 mm in particle diameter. Then, injection molding was performed with a mold (20 × 20 × 6 mm) having the configuration of a throw-away tip, to prepare a compact. The compact was arranged in a furnace, and the interior of the furnace was held at 1 atm. (1 bar) in an Ar atmosphere. The temperature in the furnace was raised up to 425 °C at a programming rate of 8 °C/h. under a condition of an Ar flow rate of 3 l/min., to perform debinder processing. Then the temperature in the furnace was raised up to 700 °C at a programming rate of 50 °C/h. in a state maintaining the interior of the furnace not more than 0.5 (0.7 mbar) Torr with a vacuum pump, and the furnace was held at the temperature for one hour, and thereafter cooled.

30 Thus, the debinder processing was terminated. Then, the interior of the furnace was brought into a vacuum state of 0.05 (0.07 mbar) Torr and the temperature was raised up to 1400 °C at 200 °C/h., and the furnace was held at the temperature for one hour, and thereafter cooled. The as-formed sintered body had absolutely no imperfection, and was excellent in view of alloy characteristics. A heating loss test for the binders used in this Example was carried out whereby the beeswax was lost by 95 % before reaching

35 425 °C under conditions of N₂ and 1 atm (1 bar). On the other hand, the loss of the low molecular weight polyethylene was 13 % at 425 °C.

Example 2

45 90 % of WC powder having a particle diameter of 0.5 to 2 µm and 10 % of Co powder having a particle diameter of 2 to 4 µm were mixed in a wet ball mill for 20 hours, and dried. 5.5 % of carnauba wax and 1.0 % of low molecular weight polypropylene were added to 100 % of this mixed powder, and kneaded at 140 °C for 30 minutes. Then, this raw material mixture was cooled/solidified and thereafter pulverized, to prepare raw material particles of about 0.5 to 2.0 mm in particle diameter. Then, injection molding was

50 performed in a mold (20 × 20 × 6 mm) having the configuration of a throw-away tip. This compact was arranged in a furnace. The interior of the furnace was under an Ar atmosphere of 1 atm. (1 bar), and its temperature was raised up to 430 °C at a programming rate of 10 °C/h. under a condition of a flow rate of 3 l/min., to perform initial debinder processing. Then, the temperature was raised up to 700 °C at a programming rate of 50 °C/h. while maintaining the interior of the furnace not more than 0.2 Torr (0.3 mbar)

55 with a vacuum pump, and the furnace was held at the temperature for one hour. Thus, the debinder processing was terminated. Thereafter the temperature in the furnace was raised up to 1350 °C at 200 °C/h. in a vacuum of 0.05 Torr (0.07 mbar), and the furnace was cooled after the same was held at the temperature for one hour. The as-formed sintered body had absolutely no imperfection, and was excellent

in view of alloy characteristics. A heating loss test was performed on the binders employed in this Example, whereby the carnauba wax was lost by 92 % before reaching 430 °C under conditions of N₂ and 1 atm (1 bar). On the other hand, loss of the low molecular weight polypropylene was 8 % at 430 °C.

5 Example 3

88 % of WC powder having a particle diameter of 0.1 to 1 μm, 6 % of Co powder having a particle diameter of 2 to 4 μm and 6 % of Ni powder having a particle diameter of 2 to 4 μm were mixed in a wet ball mill for 25 hours, and dried. 0.5 % of beeswax, 4.5 % of n-paraffin, 0.2 % of stearic acid, 0.5 % of ethylene-vinyl acetate and 1.0 % of low molecular weight polyethylene were added to 100 % of this mixed powder, and kneaded at 120 °C for 30 minutes. Then this raw material mixture was cooled/solidified and thereafter pulverized, to prepare raw material particles of about 0.5 to 2.0 mm in particle diameter. Then, injection molding was performed with a mold (20 × 20 × 6 mm) having the configuration of a throw-away tip. This compact was arranged in a furnace. The interior of the furnace was set in an N₂ atmosphere of 1 atm. (1 bar), and its temperature was raised up to 380 °C at a programming rate of 13 °C/h. under a condition of a flow rate of 2 l/min., to perform initial debinder processing. Then, the temperature was raised up to 700 °C at a programming rate of 50 °C/h. while maintaining the interior of the furnace not more than 0.5 Torr (0.7 mbar) with a vacuum pump, and the furnace was cooled after the same was held at the temperature for one hour. Thus, the debinder processing was terminated. Then, the interior of the furnace was brought into a vacuum of 0.05 Torr (0.07 mbar), and its temperature was raised up to 1350 °C at 200 °C/h., and cooled after the same was held at the temperature for one hour. The as-formed sintered body had absolutely no imperfection, and was excellent in view of alloy characteristics. A heating loss test was performed on the binders employed in this Example, whereby the beeswax was lost by 60 % and the n-paraffin was lost by 100 % before reaching 380 °C under conditions of N₂ and 1 atm (1 bar). On the other hand, loss of the low molecular weight polyethylene was 7.0 % and loss of the ethylene-vinyl acetate was 10 % at 380 °C.

Example 4

30 88 % of WC powder having a particle diameter of 1 to 2 μm and 12 % of Co powder were mixed in a wet ball mill for 15 hours, and dried. 5.5 % of montan wax and 0.8 % of low density polyethylene were added to 100 % of this mixed powder, and kneaded at 120 °C for 3 hours. Then, this raw material mixture was cooled/solidified and thereafter pulverized, to prepare raw material particles of about 0.5 to 2.0 mm in particle diameter. Then injection molding was performed with a mold (20 × 20 × 6 mm) having the configuration of a throw-away tip. This compact was arranged in a furnace. The interior of the furnace was set in an Ar atmosphere of 1 atm. (1 bar), and its temperature was raised up to 350 °C at a programming rate of 10 °C/h. under a condition of a flow rate of 3 l/min., to perform initial debinder processing. Then, the temperature was raised up to 650 °C at a programming rate of 50 °C/h. while maintaining the interior of the furnace not more than 0.5 Torr (0.7 mbar) with a vacuum pump, and the furnace was cooled after the same was held at the temperature for one hour, to terminate the debinder processing. Then, the interior of the furnace was brought into a vacuum of 0.05 Torr (0.07 mbar), the temperature was raised up to 1400 °C at 200 °C/h., and the furnace was cooled after the same was held for one hour. The as-formed sintered body had absolutely no imperfection, and was excellent in view of alloy characteristics. A heating loss test was performed on the binders employed in this Example, whereby loss of the montan wax was 93 % before reaching 350 °C under conditions of N₂ and 1 atm. (1 bar), while loss of the low density polyethylene was 0 % on measurement at 350 °C.

Example 5

50 Cermet powder (50 % of TiCN, 10 % of TaC, 12 % of Mo₂C, 13 % of WC, 5 % of Ni and 10 % of Co) having a particle diameter of 0.5 to 1 μm was mixed in a wet ball mill for 10 hours, and dried. 7.8 % of montan wax, 2.7 % of n-paraffin, 2.7 % of low density polyethylene and 0.3 % of stearic acid were added to 100 % of this mixed powder, and kneaded at 120 °C for 3 hours. Then, this raw material mixture was cooled/solidified and thereafter pulverized, to prepare raw material particles of about 0.5 to 2.0 mm in particle diameter. Then, injection molding was made into a mold having a ball end mill configuration of 10 mm in diameter, to obtain a compact. This compact was arranged in a furnace. The interior of the furnace was set in an Ar atmosphere of 1 atm. (1 bar), and its temperature was raised up to 350 °C at a programming rate of 10 °C/h. under a condition of a flow rate of 3 l/min., to perform initial debinder

processing. Then, the temperature was raised up to 650 °C at a programming rate of 50 °C/h. while maintaining the interior of the furnace not more than 0.5 Torr (0.7 mbar) with a vacuum pump, and the furnace was cooled after the same was held at the temperature for one hour, to terminate the debinder processing. Then, the interior of the furnace was brought into a vacuum of 0.05 Torr (0.07 mbar) and the 5 temperature was raised up to 1400 °C at 200 °C/h., and the furnace was cooled after the same was held for one hour, and thereafter HIP processing was performed at 1350 °C. The as-formed sintered body had absolutely no imperfection, and was excellent in view of alloy characteristics. A heating loss test was performed on the binders employed in this Example, whereby loss of the montan wax was 93 % under conditions of N₂ and 1 atm. (1 bar) before reaching 350 °C and loss of the n-paraffin was 100 %, while loss 10 of the low density polypropylene was 0 % on measurement at 350 °C.

Example 6

A plurality of raw material particle compacts were prepared under the same conditions as those in 15 Example 1. With respect to these compacts, the programming rate in the first removal step of debinder processing and a transition temperature to the second removal step were changed, to examine states after debinding. Table 2 shows the results. Table 1 shows results of heating loss tests of beeswax and low molecular weight polyethylene (PE). As obvious from the results of Tables 1 and 2, excellent states are attained after debinding according to the inventive method, and debinding times can be shortened.

20

Table 1

Heating Loss Rate (N ₂ 1 atm (1 bar), Temperature Rising at 10 °C/min.)									
	T	250 °C	300 °C	350 °C	375 °C	400 °C	425 °C	450 °C	475 °C
	Beeswax (xT)	0.03	0.12	0.32	0.50	0.74	0.95	0.99	1.00
	Low Molecular Weight PE (yT)	0.01	0.03	0.05	0.07	0.09	0.13	0.30	0.85

30

Table 2

Test Result of Transition Temperature to Second Removal Step					
Test No.	Transition Temperature to 2nd Removal step	1st Removal Step Programming Rate	Beeswax Loss Rate a × xT	PE Residual Rate b × (1-yT)	State After Debinding
1	300	8 °C/h.	0.10	0.14	bursting state
2	300	4	0.10	0.14	significantly cracked and blistered
3	350	8	0.27	0.14	5 cracks
4	350	4	0.27	0.14	good
⑤	375	8	0.43	0.13	good
⑥	400	8	0.64	0.13	good
⑦	425	8	0.81	0.12	good
⑧	450	8	0.85	0.10	good
9	475	8	0.86	0.02	collapsed

O: Inventive Method
a = 0.86
b = 0.14

Example 7

8 types of samples were prepared by using alloy powder which was similar to that of Example 1 and changing the rate of beeswax to low molecular weight polyethylene (PE) as to binder compositions (tests

Nos. 10 to 17), to perform debinding tests. Table 3 shows the results. The transition temperature from the first removal step to the second removal step was set at 450 °C. As obvious from the results of Table 3, it is recognized that the inventive compositions are excellent.

5

Table 3
Test Condition and Result

Test No.	Binder Composition Beeswax/Low Molecular Weight PE	1st Removal Step Programming Rate	Beeswax Loss Rate axx_{450}	PE Residual Rate $b \times (1 - y_{450})$	$bxyT$ ($axxT=0.3$)	State after Debinding
10	6.5/0.5	10 °C/h.	0.92	0.05	0.005	partially deformed
11	6.0/1.0	10 °C/h.	0.85	0.10	0.008	good
12	5.0/2.0	10 °C/h.	0.71	0.20	0.018	good
13	4.0/3.0	10 °C/h.	0.57	0.30	0.032	good
14	3.0/4.0	10 °C/h.	0.42	0.40	0.045	good
15	3.0/4.0	4 °C/h.	0.42	0.40	0.045	good
16	2.0/5.0	10 °C/h.	0.28	0.50	not reaching $axxT=0.3$	significantly cracked
17	2.0/5.0	4 °C/h.	0.28	0.50	not reaching $axxT=0.3$	2 cracks

0: Inventive Method

Binder Composition: Rate with respect to 100% of Alloy Powder

35 Example 8

Alloy powder similar to that of Example 3 was used and debinding tests were performed by changing types and compositions of binders. Table 4 shows the results. Debinding conditions were identical to those of Example 3. Good injection and debinding were possible in the tests Nos. 18 to 20. In the test No. 40 21 employing n-paraffin, however, it was impossible to make good injection unless the amount of n-paraffin was increased. In the test No. 22, on the other hand, distortion was caused in debinder processing. In the test No. 23 of mixing beeswax and n-paraffin at 1/1, no deformation was recognized in debinding although it was necessary to add a slight amount of the binder.

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50

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Table 4
Wax Type and Result

Test No.	Wax Type	Binder Composition Wax/Low Molecular Weight PE	Injection	Debinder State
18	Carnauba Wax	5.0/1.5	possible	good
19	Beeswax	5.0/1.5	possible	good
20	Montan Wax	5.0/1.5	possible	good
21	n-Paraffin	5.0/1.5	impossible	---
22	n-Paraffin	7.0/1.5	possible	distorted
23	Beeswax + n-Paraffin	3+3/1.5	possible	good

0: Inventive Method

Binder Composition: Rate with respect to 100% of Alloy Powder

Example 9

In a preparation method similar to the test No. 5 of Table 2, atmospheres for the first removal step and the second removal step were varied as shown at tests Nos. 24 to 30 in Table 5. As obvious from the results of Table 5, it is recognized that the inventive atmospheres are effective. It was impossible to advance the samples of the tests Nos. 26 and 29 to sintering steps, since the same collapsed in debinding. Other samples were capable of progressing to sintering steps.

Table 5

Test No.	1st Removal Step: up to 350°C			2nd Removal Step: 350 to 700°C			Result (Sintered Body)
	Gas	Flow Rate	Pressure	Atmosphere	Flow Rate	Pressure	
5	Ar	3t/min.	Atmospheric Pressure	Vacuum		0.5Torr (0.7 mbar)	good
24	Ar	0.1t/min.	Atmospheric Pressure	Vacuum		0.5Torr	good
25	N ₂	3t/min.	Atmospheric Pressure	Vacuum		0.5Torr	good
26	N ₂	3t/min.	Atmospheric Pressure	N ₂	3t/min.	Atmospheric Pressure	Collapsed (in debinding)
27	N ₂	3t/min.	600Torr (0.8 bar)	Vacuum		0.5Torr	good
28	Air	3t/min.	Atmospheric Pressure	Vacuum		0.5Torr	distorted, cracked
29	Ar	3t/min.	Atmospheric Pressure	Ar		5Torr (7 mbar)	collapsed
30	N ₂	3t/min.	Atmospheric Pressure	H ₂	3t/min.	Atmospheric Pressure	low carbon abnormal phase caused

0: Inventive Method

Industrial Availability

The present invention is effectively applied to a method of preparing a cemented carbide or a cermet alloy by shaping cemented carbide powder or cermet alloy powder into a prescribed configuration by an injection molding method and thereafter sintering the compact upon removal of an organic binder.

Claims

1. A method of preparing cemented carbide or a cermet alloy by mixing/kneading cemented carbide powder or cermet alloy powder with an organic binder containing a plurality of types of binders being divided into a group removable under a low temperature and a group removed at a high temperature, shaping this mixed powder into a prescribed configuration by an injection molding method and thereafter removing said organic binder from this compact and sintering the same in order to obtain a dense alloy, characterized by
 removal of said organic binder being first performed in an inert gas atmosphere of N_2 or Ar under a pressure of not less than 600 Torr (0.8 bar) as a first removal step and then performed in a pressure range below 1 Torr (1.3 mbar) in continuation as a second removal step,
 and assuming that a_1, a_2, \dots, a_i represent rates of respective binders of said low-temperature removal group including j types of binders with respect to overall said organic binder, b_1, b_2, \dots, b_j represent rates of respective binders of said high temperature removal group including j types of binders with respect to overall said organic binder ($\sum a_i + \sum b_j = 1$) xT_i, xT_2, \dots, xT_i represent loss rates of a single substance of respective said binders belonging to said low-temperature removal group at a certain temperature T in inert gas atmospheric pressure heating loss tests (TG), and yT_1, yT_2, \dots, yT_j represent loss rates of a single substance of respective said binders belonging to said high-temperature removal group at said certain temperature T in inert gas atmospheric pressure heating loss tests, compositions of respective said binders contained in said organic binder are selected to satisfy the following conditions:

$$\sum (b_j \times yT_j) \leq 0.05$$

$$\sum b_j \geq 0.1$$
 at said temperature T for which $\sum (a_i \times xT_i) = 0.3$, and selecting said temperature T for transition from said first removal step to said second removal step to satisfy the following conditions:

$$\sum (a_i \times xT_i) > 0.3$$

$$\sum \{b_j \times (1 - yT_j)\} > 0.05$$

2. The method of preparing a cemented carbide or a cermet alloy in accordance with claim 1, wherein said low-temperature removal group includes wax having hydrophilic polar groups with a melting point of not more than 80 °C.
3. The method of preparing a cemented carbide or a cermet alloy in accordance with claim 1, wherein said sintering is performed in a vacuum of a not more than 0.05 Torr (0.07 mbar).

45 Patentansprüche

1. Verfahren zum Herstellen von gesintertem Karbid oder einer Cermetlegierung durch Mischen/Kneten von gesintertem Karbidpulver oder gesintertem Cermetlegierungspulver mit einem organischen Bindemittel, welches eine Anzahl von Typen von Bindemittel enthält, die unterteilt werden können in eine Gruppe entfernbare unter niedriger Temperatur und einer Gruppe entfernbare bei hoher Temperatur,
 Formen dieses gemischten Pulvers in eine vorgegebene Konfiguration durch ein Spritzgußverfahren und anschließendem Entfernen des organischen Bindemittels aus dem Kompaktmaterial und Sintern desselben, um eine dichte Legierung zu erhalten,
 dadurch gekennzeichnet, daß die Entfernung des organischen Bindemittels zuerst durchgeführt wird in einer Inert-Gas-Atmosphäre von N_2 oder Ar unter einem Druck von nicht weniger als 600 Torr (0,8 bar) als einen ersten Entfernschritt und anschließend Durchführen in einem Druckbereich unter 1 Torr (1,3 mbar) in Fortsetzung als ein zweiter Entfernschritt, wobei angenommen wird, daß a_1, a_2, \dots, a_i , die

Anteile der jeweiligen Bindemittel der Niedertemperatur-Entfernungsgruppe einschließlich von i-Typen von Bindern mit Bezug auf das gesamten organischen Bindemittel darstellen,

b_1, b_2, \dots, b_j die Anteile der jeweiligen Bindemittel der Hochtemperatur-Entfernungsgruppe einschließlich j-Typen von Bindern mit Bezug auf das gesamte organische Bindemittel ($\sum a_i + \sum b_j = 1$) wiedergeben,

5 xT_1, xT_2, \dots, xT_i die Verlustraten einer einzelnen Substanz des jeweiligen Bindemittels sind, welches zur Niedertemperatur-Entfernungsgruppe bei einer bestimmten Temperatur T in den Hitzeverlusttesten (TG) unter Inert-Gas-Umgebungsdruck gehören, und

10 yT_1, yT_2, \dots, yT_j die Verlustraten der einer einzelnen Substanz des jeweiligen Bindemittels sind, welches zur Hochtemperatur-Entfernungsgruppe gehört, bei einer bestimmten Temperatur T in den Hitzeverlusttesten des Inert-Gas-Umgebungsdruckes, wobei

15 Zusammensetzungen der jeweiligen Binder, die in dem organischen Bindemittel enthalten sind, so ausgewählt werden, daß die folgenden Bedingungen erfüllt sind:

$$\sum (b_j \times yT_j) \leq 0,05$$

15 $\sum b_j \geq 0,1$

bei der Temperatur T für welche $\sum (a_i \times xT_i) = 0,3$,

und Auswählen der Temperatur T für den Übergang vom ersten Entfernungschnitt zum zweiten Entfernungschnitt, um die folgenden Bedingungen zu erfüllen:

20 $\sum (a_i \times xT_i) > 0,3$

$\sum \{b_j \times (1 - yT_j)\} > 0,05$

25 2. Verfahren zum Herstellen von gesintertem Karbid oder Cermetlegierung gemäß Anspruch 1, worin die Niedertemperatur-Entfernungsgruppe Wachs umfaßt, welches hydrophile Polargruppen mit einem Schmelzpunkt von nicht mehr als 80 ° C umfaßt.

30 3. Verfahren zum Herstellen von gesintertem Karbid oder Cermetlegierung nach Anspruch 1, worin die Sinterung in einem Vakuum von nicht mehr als 0,05 Torr (0,07 mbar) durchgeführt wird.

Revendications

1. Procédé pour la préparation de carbure cémenté ou d'un alliage cermet ou céramométallique caractérisé par les étapes consistant à mélanger/malaxer de la poudre de carbure cémenté ou une poudre d'alliage cermet avec un liant organique contenant une pluralité de types de liants répartis dans un groupe extractable à basse température et un groupe extrait à température élevée, à façonner cette poudre mélangée en une configuration prescrite par un procédé de moulage par injection puis à extraire ce liant organique de ce corps compacte et à friter celui-ci pour obtenir un alliage dense, caractérisé par

40 l'extraction de ce liant organique étant d'abord effectuée dans une atmosphère de gaz inerte de N_2 ou d'Ar sous pression non inférieure à 600 Torr (0,8 bar) en tant que première étape d'extraction, puis à effectuer dans une plage de pression inférieure à 1 Torr (1,3 mbar) en continu en tant que seconde étape d'extraction,

45 et à partir du principe que a_1, a_2, \dots, a_i représentent les taux de liants respectifs du groupe d'extraction basse température comprenant les types i de liant par rapport à l'ensemble de ce liant organique, b_1, b_2, \dots, b_j représentent les taux de liants respectifs de ce groupe d'extraction haute température incluant les types j de liant par rapport à l'ensemble de ce liant organique ($\sum a_i + \sum b_j = 1$) xT_1, xT_2, \dots, xT_i représentent les taux de perte de substance unique de ces liants respectifs faisant partie du groupe d'extraction basse température à une certaine température T dans des tests de perte calorifique à pression atmosphérique gaz inerte (TG), et yT_1, yT_2, \dots, yT_j représentent les taux de perte d'une seule substance de ces liants respectifs faisant partie du groupe d'extraction haute température à une certaine température T dans des tests de perte calorifique sous pression atmosphérique en gaz inerte, les compositions de ces liants respectifs contenus dans le liant organique étant choisies pour satisfaire les conditions suivantes:

55 $\sum (b_j \times yT_j) \leq 0,05$

$\sum b_j \geq 0,1$

à cette température T pour laquelle $\Sigma (a_i \times xT_i) = 0,3$ et à choisir cette température T pour la transition à partir de la première étape d'extraction à la seconde étape d'extraction pour satisfaire les conditions suivantes:

5 $\Sigma (a_i \times xT_i) > 0,3$
 $\Sigma \{b_j \times (1 - yT_j)\} > 0,05$

10 2. Procédé pour la préparation de carbure cémenté ou d'un alliage cermet selon la revendication 1, dans lequel ce groupe d'extraction basse température comprend de la cire ayant des groupes polaires hydrophiles d'un point de fusion non supérieur à 80 °C.

15 3. Procédé pour la préparation d'un carbure cémenté ou d'un alliage cermet selon la revendication, dans lequel le frittage s'effectue sous vide à une pression non supérieure à 0,05 Torr (0,07 m bar).

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