630286

FORM 1
REGULATION 9

COMMONWEALTH OF AUSTRALIA

PATENTS ACT 1952-1973

APPLICATION FOR A PATENT

We UNITED KINGDOM ATOMIC ENERGY AUTHORITY

of 11 Charles II Street, LONDON SW1Y 4QP, ENGLAND

hereby apply for the grant of a Patent for an invention entitled:

PRECIPITATION APPARATUS AND METHOD

which is described in the accompanying complete specification. This Application is a Convention Application and is based on the Application numbered: 90 07027.7 for a Patent or similar protection made in United Kingdom on 29 March 1990.

Our address for service is:

GRIFFITH HACK & CO
71 YORK STREET
SYDNEY NSW 2000

DATED this 25th day of March 1991

UNITED KINGDOM ATOMIC ENERGY AUTHORITY
By their Patent Attorney

GRIFFITH HACK & CO

TO: THE COMMISSIONER OF PATENTS
COMMONWEALTH OF AUSTRALIA

8020730 25/03/91

3739A:rk

DECLARATION FORM FOR COMPANY APPLICATIONS, AUSTRALIA

Form 6, 7. Regulations 11(1) and 11(2)
COMMONWEALTH OF AUSTRALIA PATENTS ACT 1952

DECLARATION IN SUPPORT OF AN APPLICATION FOR A PATENT.

In support of the Application made by United Kingdom Atomic Energy Authority, of 11 Charles II Street, London, SW1Y 4QP. England. for a patent for an invention entitled:-
Precipitation Apparatus and Method
I, Marcus John Lofting
of United Kingdom Atomic Energy Authority, Patents Branch, B.329, Harwell Laboratory, Oxon, OX11 0RA, United Kingdom, do solemnly and sincerely declare as follows:

1. I am authorised by the applicant for the patent to make this Declaration on its behalf.

2. The Applicant is in possession of the invention, the subject of the application.

3. Michael Joseph Bowe and John William Stairmand

of United Kingdom Atomic Energy, Patents Branch, B. 329, Harwell Laboratory, Oxfordshire, Ox11 0RA, England.

is the actual inventor(s) of the invention which belongs to the Applicant by virtue of a contract of employment between the inventor(s) and the Applicant.

4. The basic application, as defined by Section 141 of the Act, was made in the United Kingdom under Application No. 90 07027.7 on the 29th March 1990 by United Kingdom Atomic Energy Authority.

5. The basic application referred to in paragraph 4 of this Declaration was the first application made in a Convention country in respect of the invention, the subject of this application.

Declared at Harwell, Oxfordshire, United Kingdom

this Seventh day of March 1991

M. J. Lofting

To: The Commissioner of Patents, CANBERRA

Note: Initial all deletions and alterations.

(12) PATENT ABRIDGMENT (11) Document No. AU-B-73800/91
(19) AUSTRALIAN PATENT OFFICE (10) Acceptance No. 630286

(54) Title
PRECIPITATION APPARATUS AND METHOD

International Patent Classification(s)
(51)[5] **B01D 021/26** **B01J 019/00**

(21) Application No. : **73800/91** (22) Application Date : **25.03.91**

(30) Priority Data

(31) Number	(32) Date	(33) Country
9007027	**29.03.90**	**GB UNITED KINGDOM**

(43) Publication Date : **03.10.91**

(44) Publication Date of Accepted Application : **22.10.92**

(71) Applicant(s)
UNITED KINGDOM ATOMIC ENERGY AUTHORITY

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(56) Prior Art Documents
GB 2200574
EP 72737

(57) Claim

1. An apparatus for on-line precipitation comprising a flow line for a reagent flow, a vortex mixer in the flow line for combining and mixing the reagent flow with at least one further reagent flow, a pulser in the flow line to cause pulsing of the mixed flow from the vortex mixer and a vessel having an array of vortex cells to receive the pulsing mixed flow and to cause development and growth of precipitate under narrow residence time distribution conditions.

7. A method of on-line precipitation which comprises thoroughly mixing a flow of reagents to initiate precipitation, pulsing the flow of admixed reagents and causing the pulsing mixed flow to swirl with constantly reversing rotational flow to achieve development and growth of precipitate.

COMMONWEALTH OF AUSTRALIA

PATENTS ACT 1952 Form 10

SUBSTITUTE COMPLETE SPECIFICATION

(ORIGINAL)

FOR OFFICE USE

Short Title:

Int Cl:

Application Number:
Lodged:

Complete Specification-Lodged:
Accepted:
Lapsed:
Published:

Priority:

Related Art:

TO BE COMPLETED BY APPLICANT

Name of Applicant: UNITED KINGDOM ATOMIC ENERGY AUTHORITY

Address of Applicant: 11 Charles II Street, LONDON SW1Y 4QP, ENGLAND

Actual Inventor: Michael Joseph Bowe and John William Stairmand

Address for Service: GRIFFITH HACK & CO
71 YORK STREET
SYDNEY NSW 2000

Complete Specification for the invention entitled:

PRECIPITATION APPARATUS AND METHOD

The following statement is a full description of this invention, including the best method of performing it known to us:-

GH&CO REF: 7154-LC:RPW:RK

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Precipitation Apparatus and Method

The present invention concerns apparatus and method for the on-line treatment of chemical reagents. In particular the invention concerns apparatus and method for mixing reagents to cause precipitation of particles with narrow size distribution with the facility for on-line changes in mixing intensity, to change particle mean size and size distribution.

According to one aspect of the present invention an apparatus for on-line precipitation comprises a flow line for a reagent flow, a vortex mixer in the flow line for combining and mixing the reagent flow with at least one further reagent flow, a pulser in the flow line to cause pulsing of the mixed flow from the vortex mixer and a vessel having an array of vortex cells to receive the pulsing mixed flow and to cause development and growth of precipitate under narrow residence time distribution conditions.

According to another aspect of the present invention a method of on-line precipitation comprises thoroughly mixing a flow of reagents to initiate precipitation, pulsing the flow of admixed reagents and causing the pulsing mixed flow to swirl with constantly reversing rotational flow to achieve development and growth of precipitate.

An embodiment of the invention is described, by way of example, with reference to the accompanying schematic diagram of an apparatus for on-line precipitation.

Reagents are pumped along a flow line 1 by, for example, a gear pump 2 to enter a first vortex mixer 3. The vortex mixer comprises a cylindrical vortex chamber having at least one tangential inlet port in the circumferential wall of the chamber and an axial outlet port in an end wall of the chamber. Flow enters tangentially to swirl through the chamber to emerge at the outlet and in so doing thorough mixing of the reagents in the flow takes place.

The flow from the vortex mixer 3 proceeds along conduit 4 to enter a second vortex mixer 5 at a tangential inlet port. A second reagent flow, which can be liquid or gas, along a conduit 6 and likewise pumped by, for example, a gear pump 7 enters the second vortex mixer 5 through a further tangential inlet port. The two flows from the conduits 4 and 6 swirl through the second vortex mixer 5 and in so doing are thoroughly mixed together such that the mixing time is less than or equal to the incubation period for the particle precipitation reaction.

A rapid and thorough mixing is necessary when the reagents react to form a precipitate within a very short time interval. It is therefore desirable to complete the mixing in a time not longer than the incubation time for precipitation so that nucleation occurs under conditions of uniform supersaturation.

The flow along the conduit 8 from the second vortex mixer 5 will comprise the admixed reagents with a precipitate resulting from the interaction of the reagents. A pH meter 9 can be included in the conduit 8. A pulser 10, which can be a mechanical or fluidic device, is also included in the conduit 8 so as to cause a pulsing or oscillating flow to emerge from the conduit 8 into a vessel 11 in which the precipitate is allowed to develop to a final state under narrow residence time distribution conditions. The pulsing flow serves to mix the fluid, minimise deposition of precipitate on the walls of the conduits and vessel 11 and also serves to re-disperse boundary layer fluids back into the bulk fluid. The vessel 11 can comprise a plurality of substantially circular radiused sections 12 forming an array of vortex cells connected together and connected back-to-back. The mean residence time of the flow in the vessel can be altered by changing the number of sections 12 as required. The distribution of residence time about the mean value and the degree of agitation in the vessel can be varied by variation of pulse amplitude and/or frequency and also the number of sections 12. The

pulsing flow passes gradually through the vessel 11 and the configuration of the sections 12 is such as to cause the flow to swirl through the sections forming the array of vortex cells with constantly reversing rotational direction.

The flow from the vessel 11 passes into a pulse dampener 13 which is basically a vessel having an enclosed gas volume acting as a buffer to dampen oscillations or pulses in the flow. From there the flow enters a centrifugal separator such as a low shear hydrocyclone 14 for segregation of ripened particle size.

Overflow from the hydrocyclone 14 substantially depleted in larger particles can be recycled along conduit 15 by means of a low shear mono pump or the like 16, the recycled flow being introduced tangentially into the vortex mixer 5 to serve as a seed stream to minimise homogenous nucleation. An extension 17 of the conduit 15, having a gear pump 18, conveys a part of the hydrocyclone overflow stream to a second tangential port at the first vortex mixer 3. This permits mixing with the incoming stream along the conduit 1. Ideally the particles in the recycle stream will re-dissolve and indeed in many hydrolysis reactions flow and pH can be adjusted so this will happen. The resulting single phase fluid can then be fed to the mixer valve 5 to provide the means for varying mixing intensity without providing seed particles to the system. By varying the recycle rate in the extension 17 it is possible to vary the mixing

intensity in the mixer valve on line and without adjusting the main feed flow rates. It is thereby possible to obtain on-line adjustment of particle size distribution, because variation in mixing intensity effects the range of supersaturation values present in the mixing volume at the onset of nucleation. This effects both the rate of generation of nuclei and the subsequent growth rate.

The recycled flow is then employed in 2 ways:

1. It can be employed in mixer valve 5 to act as a precipitate seed stream.

2. It can be mixed with incoming feed and the re-cycled particles dissolved in mixer 3. The single phase fluid can then be used to vary mixing intensity in mixer valve 5.

This allows seeding conditions and mixing intensity to be decoupled. The system as a whole can now provide 3 degrees of freedom.

1. Variation of mixing intensity to adjust initial nucleation and growth rate.

2. Variation of seed stream flowrate to control initial nucleation rate and particle morphology.

3. Variation in precipitate development or ripening conditions by variation in mixing intensity and by variation in residence time distribution (in vessel 11) to control final particle size and distribution.

~~claims~~ THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:

1. An apparatus for on-line precipitation comprising a flow line for a reagent flow, a vortex mixer in the flow line for combining and mixing the reagent flow with at least one further reagent flow, a pulser in the flow line to cause pulsing of the mixed flow from the vortex mixer and a vessel having an array of vortex cells to receive the pulsing mixed flow and to cause development and growth of precipitate under narrow residence time distribution conditions.

2. An apparatus according to Claim 1 comprising centrifugal separator means for receiving flow from the vessel.

3. An apparatus according to Claim 2 comprising a a pulse dampener in a flow line from the vessel to the separator means.

4. An apparatus according to Claim 2 or 3 in which the separator means comprises a hydrocyclone.

5. An apparatus according to Claim 2, 3 or 4 including a return flow conduit for recycling a part of the out flow from the separator means to the vortex mixer.

6. An apparatus according to any preceding claim comprising a further vortex mixer in the flow line upstream of the vortex mixer.

7. A method of on-line precipitation which comprises thoroughly mixing a flow of reagents to initiate precipitation, pulsing the flow of admixed reagents and causing the pulsing mixed flow to swirl with constantly reversing rotational flow to achieve development and growth of precipitate.

8. A method according to Claim 7 which comprises separating the precipitate and recycling a part of the separated flow for mixing with the incoming flow of reagents.

9. Apparatus for on-line precipitation arranged and adapted to operate substantially as herein described with reference to and as illustrated in the accompanying drawing.

10. A method of on-line precipitation substantially as herein described with reference to the accompanying drawing.

Dated this 25th day of March 1991

UNITED KINGDOM ATOMIC ENERGY AUTHORITY
By their Patent Attorney
GRIFFITH HACK & CO.

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