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(54) **Title:** APPARATUS AND SYSTEMS HAVING COMPACT CONFIGURATION MULTIPLE SWING ADSORPTION BEDS AND METHODS RELATED THERETO

(57) **Abstract:** A compact configuration for a plurality of swing adsorption beds. The beds are configured within a single vessel such that one or more beds of adsorbent material are positioned as successive rings about a first, or core, bed of adsorbent material.



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**APPARATUS AND SYSTEMS HAVING COMPACT CONFIGURATION
MULTIPLE SWING ADSORPTION BEDS AND METHODS RELATED THERETO**

CROSS REFERENCE TO RELATED APPLICATIONS

5 **[0001]** This application claims the benefit of U.S. Patent Application No. 61/448,125 entitled APPARATUS AND SYSTEMS HAVING COMPACT CONFIGURATION MULTIPLE SWING ADSORPTION BEDS AND METHODS RELATED THERETO, filed March 1, 2011, the entirety of which is incorporated by reference herein.

10 **[0002]** This application is related to U.S. Patent Application No. 61/448,117 entitled APPARATUS AND SYSTEMS HAVING AN ENCASED ADSORBENT CONTACTOR AND SWING ADSORPTION PROCESSES RELATED THERETO, filed March 1, 2011; U.S. Patent Application No. 61/448,120 entitled APPARATUS AND SYSTEMS HAVING A RECIPROCATING VALVE HEAD ASSEMBLY AND SWING ADSORPTION PROCESSES RELATED THERETO, filed March 1, 2011; U.S. Patent Application No.
15 61/448,121 entitled METHODS OF REMOVING CONTAMINANTS FROM A HYDROCARBON STREAM BY SWING ADSORPTION AND RELATED APPARATUS AND SYSTEMS, filed March 1, 2011; and U.S. Patent Application No. 61/448,123 entitled APPARATUS AND SYSTEMS HAVING A ROTARY VALVE ASSEMBLY AND SWING ADSORPTION PROCESSES RELATED THERETO, filed March 1, 2011, and
20 U.S. Patent Application No. 61/594,824 entitled METHODS OF REMOVING CONTAMINANTS FROM A HYDROCARBON STREAM BY SWING ADSORPTION AND RELATED APPARATUS AND SYSTEMS, filed February 3, 2012, each of which is herein incorporated by reference in its entirety.

FIELD OF THE INVENTION

25 **[0003]** The present invention relates to a compact configuration for a plurality of swing adsorption beds. The beds are configured within a single vessel such that one or more beds of adsorbent material are positioned as successive rings about a first, or core, adsorbent bed of adsorbent material.

BACKGROUND OF THE INVENTION

30 **[0004]** Gas separation is important in many industries and can typically be accomplished by flowing a mixture of gases over an adsorbent of an adsorbent contactor that preferentially

adsorbs more readily adsorbed components relative to less readily adsorbed components of the mixture. One of the more important types of gas separation technology is swing adsorption.

[0005] Conventional swing adsorption processes typically take place in a cylindrical vessel containing a plurality of adsorbent beds. Some swing adsorption processes are performed in a plurality of adsorbent beds, each within its own vessel. Such designs may be useful when gas processing requires only small diameter beds or when a large equipment footprint is available. However, such designs are generally not desirable for large scale operations that require large diameter adsorbent beds or where a small footprint is critical, such as on off-shore platforms or in arctic or desert environments. Therefore, there is a need in the art for swing adsorption apparatus that can be used for large scale gas separations and which occupy a small footprint.

SUMMARY OF THE INVENTION

[0006] In accordance with the present invention there is provided an adsorbent bed system comprising: (a) a first bed of adsorbent material capable of selectively removing a target gas from a gaseous mixture, which adsorbent bed is substantially cylindrical shape; and (b) a second bed of adsorbent material capable of selectively removing a target gas from a gaseous mixture, which second adsorbent bed has a substantially cylindrical shape and being disposed about the first bed of adsorbent material and is substantially the same cross-sectional area as the cross-sectional area of the first adsorbent bed.

[0007] In a preferred embodiment, a third bed of adsorbent bed material capable of selectively removing a target gas from a gaseous mixture and being substantially annular in shape and being disposed about the second bed of adsorbent material, the third bed of adsorbent material having approximately the same cross-sectional area as the cross-sectional area of the first and second beds of adsorbent material.

[0008] In another preferred embodiment, a fourth bed of adsorbent material which has selectivity to a target gas in a gaseous mixture and having a substantially cylindrical shape and being disposed about the third bed of adsorbent material, the fourth bed of adsorbent material having approximately the same cross-sectional area as the cross-sectional area of the first, second and third beds of adsorbent material.

BRIEF DESCRIPTION OF THE FIGURES

[0009] Figure 1 hereof is a plan view representation of a conventional two adsorbent bed pressure swing adsorption apparatus showing two vessels, one for each adsorbent bed, which is typical in the art.

5 [0010] Figure 2 hereof is a cross-sectional view taken along a horizontal plane in a single adsorption vessel of the present invention containing two beds of adsorbent material with a first bed comprising the core and a second bed is positioned annular about the first bed.

[0011] Figure 3 hereof is a plan view representation of a conventional four adsorbent bed pressure swing adsorption apparatus showing four vessels, each containing a bed of adsorbent
10 material.

[0012] Figure 4 hereof is a cross-sectional view taken along a horizontal plane in a single adsorption vessel of the present invention containing four beds of adsorbent material with a first bed comprising the core and the remaining three beds positioned in rings about the first bed.

15 [0013] Figure 5 hereof is a perspective representation of a cross-section taken along a horizontal plane of the four adsorbent bed system of the present invention showing how all four adsorbent beds can share a common actuator drive assembly.

DETAILED DESCRIPTION OF THE INVENTION

[0014] Unless otherwise explained, all technical and scientific terms used herein have the
20 same meaning as commonly understood by one of ordinary skill in the art to which this disclosure pertains. The singular terms "a," "an," and "the" include plural referents unless the context clearly indicates otherwise. Similarly, the word "or" is intended to include "and" unless the context clearly indicates otherwise. The term "includes" means "comprises." All patents and publications mentioned herein are incorporated by reference in their entirety,
25 unless otherwise indicated. In case of conflict as to the meaning of a term or phrase, the present specification, including explanations of terms, will control. Directional terms, such as "upper," "lower," "top," "bottom," "front," "back," "vertical," and "horizontal," are used herein to express and clarify the relationship between various elements. It should be understood that such terms do not denote absolute orientation (e.g., a "vertical" component
30 can become horizontal by rotating the device). The materials, methods, and examples recited herein are illustrative only and not intended to be limiting.

[0015] Other applications in the technical area include U.S. Patent Application Nos. 61/447,806, 61/447,812, 61/447,824, 61/447,848, 61/447,869, 61/447,835, and 61/447,877, each of which is herein incorporated by reference in its entirety.

[0016] The present invention relates to compact configurations for swing adsorption equipment suitable for use at remote locations where space is at a premium. For example, there is a great need for compact equipment designs for equipment used on off-shore platforms. Any swing adsorption equipment used off-shore should fit within a defined compact space allotted to it on the platform. The only conventional swing adsorption systems that can presently be used off-shore are systems containing only a few relatively small adsorbent beds capable of processing only a relatively small volume of feed gas. Consequently, large volumes of gases to be separated typically cannot be performed off-shore. The present invention allows for smaller swing adsorption equipment sizes, but without any appreciable sacrifice to performance capacity when compared to conventional swing adsorption equipment of comparable performance capacity. The present invention incorporates a compact design for multiple adsorbent beds that can be encased in a single vessel to form the adsorbent bed unit, each bed sharing a common actuator system with the other beds of the vessel. All vessel walls in the concentric arrangements are preferably of suitable thickness to withstand pressures in the range of 100 bar to 200 bar. The vessel walls are preferably multi-layered to facilitate drop-in or change-out of adsorbent beds, as well as for increasing durability for cyclic pressure swing conditions. These wall may be cylindrically shapped or other suitable geometric shapes. The vessels walls can also be suitably corrugated or stiffened in sections by any conventional means known in art.

[0017] Non-limiting swing adsorption processes include pressure swing adsorption (PSA), vacuum pressure swing adsorption (VPSA), temperature swing adsorption (TSA), partial pressure swing adsorption (PPSA), rapid cycle pressure swing adsorption (RCPSA), rapid cycle thermal swing adsorption (RCTSA), rapid cycle partial pressure swing adsorption (RCPPSA), as well as combinations of these processes such as pressure/ temperature swing adsorption.

[0018] PSA processes rely on the phenomenon of gases being more readily adsorbed within the pore structure or free volume of an adsorbent material when the gas is under pressure, i.e., the higher the gas pressure, the greater the amount readily-adsorbed gas adsorbed. When the pressure is reduced, the adsorbed component is released, or desorbed.

Accordingly, the process may include one or more of these steps to separate certain gases from a stream.

[0019] PSA processes may be used to separate gases of a gas mixture because different gases tend to fill the micropore of the adsorbent to different extents. If a gas mixture, such as natural gas, is passed under pressure through a vessel containing a polymeric or microporous adsorbent that is more selective towards carbon dioxide than it is for methane, at least a portion of the carbon dioxide is selectively adsorbed by the adsorbent, and the gas exiting the vessel is enriched in methane. When the adsorbent reaches the end of its capacity to adsorb carbon dioxide, it is regenerated by reducing the pressure, thereby releasing the adsorbed carbon dioxide. The adsorbent is then typically purged and repressurized and ready for another adsorption cycle.

[0020] TSA processes rely on the phenomenon that gases at lower temperatures are more readily adsorbed within the pore structure or free volume of an adsorbent material compared to higher temperatures, i.e., when the temperature of the adsorbent is increased, the adsorbed gas is released, or desorbed. By cyclically swinging the temperature of an adsorbent bed, TSA processes can be used to separate gases in a mixture when used with an adsorbent that is selective for one or more of the components of a gas mixture.

[0021] Swing adsorption processes typically take place in a vessel containing one or more adsorbent beds. In multi-bed systems, each adsorbent bed may undergo a different step in an adsorption cycle, such as an adsorption step, one or more depressurization/desorption steps, one or more blow-down steps, and one or more repressurization steps. The flow of fluid to and from each bed is typically controlled by either a poppet valve and/or a rotary valve assembly.

[0022] Any suitable adsorbent bed material that can be used for the separation of a target gas from a gaseous mixture can be used for the adsorbent bed system of the present invention. The adsorbent is typically comprised of an adsorbent material supported on a non-adsorbent support, or contactor. Non-limiting examples of the form of the adsorbent bed of the present invention include beds of: beaded or pelletized adsorbent particles; an adsorbent material on a structured contactor, such as a parallel channel contactor. Preferred structured contactors may contain substantially parallel flow channels wherein 20 volume percent, preferably 15 volume percent or less of the open pore volume of the contactor, excluding the flow channels, is in pores greater than about 20 angstroms. Flow channels, as used herein,

means that portion of the contactor in which gas flows when a steady state pressure difference is applied between the point, or place, at which a feed stream enters the contactor and the point, or place, at which a product stream leaves the contactor. In a parallel channel contactor, the adsorbent is typically incorporated into or onto the wall of the flow channel.

5 Non-limiting examples of geometric shapes of parallel channel contactors include various shaped monoliths having a plurality of substantially parallel channels extending from one end of the monolith to the other; a plurality of tubular members, stacked layers of adsorbent sheets with and without spacers between each sheet; multi-layered spiral rolls, spiral wound adsorbent sheets, bundles of hollow fibers, as well as bundles of substantially parallel solid

10 fibers. "Parallel channel contactors" are defined as a subset of adsorbent contactors comprising structured (engineered) adsorbents in which substantially parallel flow channels are incorporated into the adsorbent structure. Parallel flow channels are described in detail in United States Patent Applications US 2008/0282892 and US 2008/0282886, both of which are herein incorporated by reference in their entirety. These flow channels may be formed by

15 a variety of means and in addition to the adsorbent material, the adsorbent structure can contain items such as, but not limited to, support materials, heat sink materials, void reduction components, and heating/cooling passages.

[0023] In preferred embodiments, adsorbent materials that can be used include high surface area (>10 meters squared per gram (m^2/gm) and preferably $>75 \text{ m}^2/\text{gm}$) alumina,

20 microporous zeolites (preferably zeolites with particle sizes < 1 millimeter (mm)), other microporous materials, mesoporous materials and ordered mesoporous materials. Non-limiting examples of these materials include carbons, cationic zeolites, high silica zeolites, highly siliceous ordered mesoporous materials, sol gel materials, ALPO materials (microporous and mesoporous materials containing predominantly aluminum phosphorous

25 and oxygen), SAPO materials (microporous and mesoporous materials containing predominantly silicon aluminum phosphorous and oxygen), MOF materials microporous and mesoporous materials comprised of a metal organic framework) and ZIF materials (microporous and mesoporous materials comprised of zeolitic imidazolate frameworks). Other materials include microporous and mesoporous sorbents functionalized with functional

30 groups. Examples of functional groups include primary, secondary, tertiary and other non protogenic basic groups such as amidines, guanidines and biguanides.

[0024] The present invention can be better understood with reference to the figures hereof. Figure 1 hereof is plan representation of conventional two adsorbent bed swing

adsorption equipment **10** showing the need for two separate adsorption vessels **12, 14**. Each vessel contains an adsorbent bed of adsorbent material. Each vessel **12, 14** requires its own actuator assembly and fluid communication conduits A, D, E between vessels. Also shown bordering this figure is a footprint **20** of the space such a conventional system requires. In contrast to this conventional two adsorbent bed system is the adsorbent bed structure of the present invention shown in Figure 2 hereof. Figure 2 shows a first bed **22** at the core of a vessel with a second bed **24** forming a ring about the first adsorbent bed **22** (e.g., may be annularly positioned). The border of Figure 2 also shows a footprint **26** for this two adsorbent bed system, which footprint **26** is about 40% less than the footprint **20** required for the conventional two adsorbent bed system shown in Figure 1. The second adsorbent bed **24**, which may have the same adsorbent material as the first bed **22**, has the same face cross-sectional area of first bed **22**. Therefore, second bed **24** has the same capacities/production (for the same cycle and flow rates) as first bed **22**. The first adsorbent bed **22** and the second adsorbent bed **24** may be separated by a material that is non-permeable to the gas flowing through the adsorbent beds. This prevents the leakage of gas from one adsorbent bed to the other.

[0025] Figures 3 and 4 are similar to Figures 1 and 2, but these figures compare a four bed system for conventional swing adsorption technology and that of the present invention. Referring to Figure 3, each vessel **30, 32, 34** and **36** contains a bed of adsorbent material. Each vessel **30, 32, 34** and **36** requires its own actuator assembly and fluid communication conduits between vessels. For simplicity purposes, the entire conduit system for communication between the four vessels is not shown. Also, shown bordering this figure is a footprint **38** of the space such a conventional system requires. In contrast to this conventional four adsorbent bed, is the adsorbent bed system of the present invention shown in Figure 4. Figure 4 shows a first adsorbent bed **40** at the core of a vessel with a second adsorbent bed **42** forming a ring (e.g., annularly positioned) about the first adsorbent bed **40**. About the second adsorbent bed **42** is a third adsorbent bed **44** annularly positioned, or forming a ring, about the second adsorbent bed **42**. About the third adsorbent bed **44** is a fourth adsorbent bed **46** annularly positioned, about the third adsorbent bed **44**. Each adsorbent bed may preferably be separated from the other beds by a material that is non-permeable to the gas flowing through it to prevent leakage to other adsorbent beds and to contain pressure within the respective beds. The border of Figure 4 also shows a footprint **48** for this four adsorbent bed system, which footprint **48** is approximately 50 % less than the footprint **38** required for a

convention four adsorbent bed system shown in Figure 3. The second adsorbent bed **42**, the third adsorbent bed **44** and the fourth adsorbent bed **46** have substantially the same face cross-sectional area as the first adsorbent bed **40**. Therefore, each of the second adsorbent bed **42**, the third adsorbent bed **44** and the fourth adsorbent bed **46** have the same capacities or production (for the same cycle and flow rates) as the first adsorbent bed **40**. It is noted that the drawings are not drawn to scale, and that the second adsorbent bed **42** has a larger radial dimension than the third adsorbent bed **44**. Likewise, the third adsorbent bed **44** has a larger radial dimension than the fourth adsorbent bed **46**. One skilled in the art readily recognizes that more than four beds can be used in accordance with the present invention. Any additional beds may have the same face cross-sectional area as the first bed **40**.

[0026] Again, it can be seen that the adsorbent bed configurations of the present invention require a substantially smaller footprint than a conventional swing adsorption system comprised of the same number of adsorbent beds, each requiring its own actuator system.

[0027] Figure 5 is a perspective representation of a cross-section of a four adsorbent bed system of the present invention. This representation shows that the size of the system may be further reduced because multiple poppet valves **52** can share the same actuator drive apparatus **50**, as opposed to conventional systems that require a separate actuator drive for each adsorbent bed. It is noted that only a few drives are sketched in Figure 5 for clarity. This feature also allows for better gas distribution since additional ports can be distributed around the annular regions.

[0028] The direction of flow of the gas streams through the different adsorbent beds may be configured to facilitate transfer of heat between the adsorbent beds. For example, the direction of gas flow in beds 1 and 3 could be opposite to the direction of gas flow in beds 2 and 4.

[0029] Practice of the present invention also has the advantages of: reduced equipment weight and complexity; more efficient manufacture and assembly of the adsorbent beds; and maintaining uniformity and identical nature of each bed, which are important to separation performance. If structured materials are used for the adsorbent beds of the present invention their assembly is facilitated by the multiple/distributed concentric shapes. For example, in spiral wound structures, each concentric shell provides the core around which the spiral winding for each bed can be initiated, but it is difficult to maintain a proper tension during

spiral winding of large-diameter conventional, (non-annular) cross-section vessels. For monolithic structures as well, the processes of forming uniform structures, are greatly improved when a single structure is made, rather than when separate structures are independently made. Accordingly, by using a single block of material, the multiple vessels
5 are assembled in-situ by suitable introduction of the successive vessels walls, taking advantage of the configuration provided by the present invention. One preferred way of assembling the multiple adsorbent bed system of the present invention is to place annular grooves into an adsorbent monolith and sliding annular rings of impermeable material into the grooves running the length of the monolith material.

10 **[0030]** Adsorptive kinetic separation processes, apparatus, and systems, as described above, are useful for development and production of hydrocarbons, such as gas and oil processing. Particularly, the provided processes, apparatus, and systems are useful for the rapid, large scale, efficient separation of a variety of target gases from gas mixtures. The provided processes, apparatus, and systems may be used to prepare natural gas products by
15 removing contaminants and heavy hydrocarbons, i.e., hydrocarbons having at least two carbon atoms.

[0031] The provided processes, apparatus, and systems are useful for preparing gaseous feed streams for use in utilities, including separation applications such as dew point control, sweetening/detoxification, corrosion protection/control, dehydration, heating value,
20 conditioning, and purification. Examples of utilities that utilize one or more separation applications include generation of fuel gas, seal gas, non-potable water, blanket gas, instrument and control gas, refrigerant, inert gas, and hydrocarbon recovery. Exemplary "not to exceed" product (or "target") gas specifications include: (a) 2 volume percent (vol.%) CO₂, 4 parts per million (ppm) H₂S, (b) 50 ppm CO₂, 4 ppm H₂S, or (c) 1.5 vol.% CO₂, 2 ppm
25 H₂S.

[0032] The provided processes, apparatus, and systems may be used to remove acid gas from hydrocarbon streams. Acid gas removal technology becomes increasingly important as remaining gas reserves exhibit higher concentrations of acid gas, i.e., sour gas resources. Hydrocarbon feed streams vary widely in amount of acid gas, such as from several parts per
30 million acid gas to 90 vol.% acid gas. Non-limiting examples of acid gas concentrations from exemplary gas reserves include concentrations of at least: (a) 1 vol.% H₂S, 5 vol.%

CO₂, (b) 1 vol.% H₂S, 15 vol.% CO₂, (c) 1 vol.% H₂S, 60 vol.% CO₂, (d) 15 vol.% H₂S, 15 vol.% CO₂, and (e) 15 vol.% H₂S, 30 vol.% CO₂.

[0033] One or more of the following Concepts A-O may be utilized with the processes, apparatus, and systems, provided above, to prepare a desirable product stream while
5 maintaining high hydrocarbon recovery:

Concept A: using one or more kinetic swing adsorption process, such as pressure swing adsorption (PSA), thermal swing adsorption (TSA), calcination, and partial pressure swing or displacement purge adsorption (PPSA), including combinations of these processes; each swing adsorption process may be utilized with rapid cycles, such as
10 using one or more rapid cycle pressure swing adsorption (RC-PSA) units, with one or more rapid cycle temperature swing adsorption (RC-TSA) units or with one or more rapid cycle partial pressure swing adsorption (RC-PPSA) units; exemplary kinetic swing adsorption processes are described in U.S. Patent Application Publication Nos. 2008/0282892, 2008/0282887, 2008/0282886, 2008/0282885, and 2008/0282884 which
15 are each herein incorporated by reference in its entirety;

Concept B: removing acid gas with RC-TSA using advanced cycles and purges as described in U.S. patent application no. 61/447848, filed March 1, 2011, which is herein incorporated by reference in its entirety;

Concept C: using a mesopore filler to reduce the amount of trapped methane in the adsorbent
20 and increase the overall hydrocarbon recovery, as described in U.S. Patent Application Publication Nos. 2008/0282892, 2008/0282885, 2008/0282886, each of which is herein incorporated by reference in its entirety. The non-sweepable void space present within the adsorbent channel wall is can be defined by the total volume occupied by mesopores and macropores. Mesopores are defined by the IUPAC to be pores with sizes in the 20
25 to 500 angstrom size range. Macropores are defined herein to be pores with sizes greater than 500 angstrom and less than 1 micron. Because the flow channels are larger than 1 micron in size, they are not considered to be part of the macropore volume. The non-sweepable void space is defined herein as the open pore volume occupied by pores in the absorbent that are between 20 angstroms and 10,000 angstroms (1 micron) in diameter
30 divided by the total volume of the contactor that is occupied by the absorbent material including associated mesopores and macropores in the absorbent structure. The non-sweepable void space can be reduced by filling the mesopores and macropores between

the particles to reduce the open volume while allowing rapid gas transport throughout the adsorbent layer. This filling of the non-sweepable void, which may be referred to as mesopore filling, space is desired to reduce to acceptable levels the quantity of desired product, lost during the rapid desorption step as well as to allow a high degree of adsorbent bed purity following desorption. Such mesopore filling can be accomplished in a variety of ways. For example, a polymer filler can be used with rapid diffusion of H₂S and CO₂, such as a silicon rubber or a polymer with intrinsic porosity. Alternatively, a pyrolytic carbon having mesoporosity and/or microporosity could be used to fill the void space. Still another way may be by filling the void space with inert solids of smaller sizes, or by filling the void space with a replenishable liquid through which the desired gases rapidly diffuse (such as water, solvents, or oil). Preferably, the void space within the adsorbent wall may be reduced to less than 40 volume percent (vol.%), preferably to less than 30 vol.%, and more preferably to less than 20 vol.%, and even more preferably to less than 10 vol.% and most preferably less than about 5 vol.% of the open pore volume.;

Concept D: Choosing an appropriate adsorbent materials to provide high selectivity and minimize adsorption (and losses) of methane and other hydrocarbons, such as one or more of the zeolites described in U.S. Patent Application Publication Nos. 2008/0282887 and 2009/0211441, each of which is herein incorporated by reference in its entirety.

Preferred adsorbents for the removal of acid gases are selected from a group consisting of mesoporous or microporous materials, with or without functionality for chemical reactions with acid gases. Examples of materials without functionality include cationic zeolites and stannosilicates. Functionalized materials that chemically react with H₂S and CO₂ exhibit significantly increased selectivity for H₂S and CO₂ over hydrocarbons. Furthermore, they do not catalyze undesirable reactions with hydrocarbons that occur on acidic zeolites. Functionalized mesoporous adsorbents are also preferred, wherein their affinity toward hydrocarbons is further reduced compared to unfunctionalized smaller pore materials, such as zeolites.

Alternatively, adsorption of heavy hydrocarbons can be kinetically suppressed by using small-pore functionalized materials, in which diffusion of heavy hydrocarbons is slow compared to H₂S and CO₂. Care should also be taken to reduce condensation of

hydrocarbons with carbon contents equal to or above about 4 (i.e., C₄+ hydrocarbons) on external surfaces of H₂S and CO₂ selective adsorbents.

Non-limiting example of functional groups suitable for use herein include primary, secondary, tertiary and other non-protogenic, basic groups such as amidines, guanidines and biguanides. Furthermore, these materials can be functionalized with two or more types of functional groups. To obtain substantially complete removal of H₂S and CO₂ from natural gas streams, an adsorbent material preferably is selective for H₂S and CO₂ but has a low capacity for both methane and heavier hydrocarbons (C₂+). In one or more embodiments, it is preferred to use amines, supported on silica based or other supports because they have strong adsorption isotherms for acid gas species. They also have high capacities for such species, and as a consequence of their high heats of adsorption, they have a relatively strong temperature response (i.e. when sufficiently heated they readily desorb H₂S and CO₂ and can thus be used without excessive temperature swings). Preferred are adsorbents that adsorb in the 25 °C to 70 °C range and desorb in the 90 °C to 140 °C range. In systems requiring different adsorbents for CO₂ and H₂S removal, a layered bed comprising a suitable adsorbent for the targeted species may be desirable.

For CO₂ removal from natural gas, it is preferred to formulate the adsorbent with a specific class of 8-ring zeolite materials that has a kinetic selectivity. The kinetic selectivity of this class of 8-ring zeolite materials allows CO₂ to be rapidly transmitted into zeolite crystals while hindering the transport of methane so that it is possible to selectively separate CO₂ from a mixture of CO₂ and methane. For the removal of CO₂ from natural gas, this specific class of 8-ring zeolite materials preferably has a Si/Al ratio from about 1 to about 25. In other preferred embodiments, the Si/Al ratio of the zeolite material is from 2 to about 1000, preferably from about 10 to about 500, and more preferably from about 50 to about 300. It should be noted that as used herein, the term Si/Al is defined as the molar ratio of silica to alumina of the zeolitic structure. This preferred class of 8-ring zeolites that are suitable for use herein allow CO₂ to access the internal pore structure through 8-ring windows in a manner such that the ratio of single component diffusion coefficients for CO₂ over methane (i.e., DCO₂/DCH₄) is greater than 10, preferably greater than about 50, and more preferably greater than about 100 and even more preferably greater than 200.

In many instances, nitrogen also has to be removed from natural gas or gas associated with the production of oil to obtain high recovery of a purified methane product from nitrogen containing gas. There have been very few molecular sieve sorbents with significant equilibrium or kinetic selectivity for nitrogen separation from methane. For N₂ separation from natural gas it is also preferred to formulate the adsorbent with a class of 8-ring zeolite materials that has a kinetic selectivity. The kinetic selectivity of this class of 8-ring materials allows N₂ to be rapidly transmitted into zeolite crystals while hindering the transport of methane so that it is possible to selectively separate N₂ from a mixture of N₂ and methane. For the removal of N₂ from natural gas, this specific class of 8-ring zeolite materials also has a Si/Al ratio from about 2 to about 1000, preferably from about 10 to about 500, and more preferably from about 50 to about 300. This preferred class of 8-ring zeolites that are suitable for use herein allow N₂ to access the internal pore structure through 8-ring windows in a manner such that the ratio of single component diffusion coefficients for N₂ over methane (i.e., DN₂/DCH₄) is greater than 5, preferably greater than about 20, and more preferably greater than about 50 and even more preferably greater than 100. Resistance to fouling in swing adsorption processes during the removal N₂ from natural gas is another advantage offered by this class of 8-ring zeolite materials.

In a preferred embodiment, H₂S is selectively removed with a non-aqueous sorbent comprising a basic non-protogenic nitrogenous compound supported on a macroporous, mesoporous, or microporous solid. The non-protogenic nitrogenous compound selectively reacts with at least a portion of the H₂S in the feed gas mixture. Examples of suitable porous solid supports include activated charcoal or solid oxides (including mixed oxides), such as alumina, silica, silica-alumina or acidic or non-acidic zeolites. The basic non-protogenic nitrogenous compound may simply be physically sorbed on the support material (e.g. by impregnation or bonded with or grafted onto it by chemical reaction with the base itself or a precursor or derivative in which a substituent group provides the site for reaction with the support material in order to anchor the sorbent species onto the support). Bonding is not, however, required for an effective solid phase sorbent material. Support materials which contain reactive surface groups, such as the silanol groups found on zeolites and the M41S silica oxides are capable of reacting with siloxane groups in compounds, such as trimethoxysilylpropyldimethylamine. Non-protogenic nitrogenous compounds do not enter into chemisorption reactions with CO₂

in the absence of water although they do undergo reaction with H₂S. This differential chemical reactivity is used to make the separation between the H₂S and the CO₂. A wide variety of basic nitrogen-containing compounds may be used as the essential sorbent. If desired, a combination of such compounds may be used. The requirement for the desired selectivity for H₂S adsorption is that the nitrogenous groups be non-protogenic, that is, incapable of acting as a proton donor. The nitrogenous groups therefore do not contain an acidic, dissociable hydrogen atom, such as nitrogen in a primary or secondary amine. It is not required that the whole compound be aprotic, only that the nitrogen-containing groups in the compound be non-protogenic. Non-protogenic nitrogen species cannot donate an H⁺ (proton), which is a prerequisite for the formation of carbamates as a route for the CO₂ chemisorption reaction in the absence of water; they are non-nucleophilic under the prevailing reaction conditions. Suitable nitrogenous compounds include tertiary amines such as triethylamine, triethanolamine (TEA), methyldiethanolamine (MDEA), *N*-methyl diethanolamine (CH₃N(C₂H₄OH)₂), NNN'N' – tetrakis (2 - hydroxyethyl) ethylenediamine as well as non-protogenic nitrogenous bases with cyclic, multicyclic, and acyclic structures, such as imines, heterocyclic imines and amines, amidines (carboxamidines) such as dimethylamidine, guanidines, triazabicyclodecenes, imidazolines, and pyrimidines. Compounds such as the *N,N*-di(lower alkyl) carboxamidines where lower alkyl is preferably C₁-C₆ alkyl, *N*-methyltetrahydropyrimidine (MTHP), 1,8-diazabicyclo[5.4.0]-undec-7-ene (DBU), 1,5,7-triazabicyclo[4.4.0]dec-5-ene (TBD), 7-methyl-1,5,7-triazabicyclo[4.4.0]dec-5-ene (MTBD), 1,5-diazabicyclo[4.3.0]non-5-ene (DBN), substituted guanidines of the formula (R¹R²N)(R³R⁴N)C=N-R⁵ where R¹, R², R³ and R⁴ are preferably lower alkyl (C₁-C₆) and R⁵ is preferably H or lower alkyl (C₁-C₆), such as 1,1,3,3-tetramethylguanidine and biguanide, may also be used. Other substituent groups on these compounds such as higher alkyl, cycloalkyl, aryl, alkenyl, and substituted alkyl and other structures may also be used.

Another class of materials that is capable of removing H₂S and CO₂, from natural gas streams is cationic zeolites. Selectivity of these materials for H₂S and CO₂ depends on the framework structure, choice of cation, and the Si/Al ratio. In a preferred embodiment the Si/Al ratio for cationic materials is in a range from 1 to 50 and more preferably a range from 1 to 10. Examples of cationic zeolite include zeolites, 4A, 5A

and faujasites (Y and X). It is preferred to use these materials for selectively removing H₂S and CO₂ after the feed stream has been dehydrated.

Other non-limiting examples of preferred selective adsorbent materials for use in embodiments herein include microporous materials such as zeolites, AIPOs, SAPOs, MOFs (metal organic frameworks), ZIFs (zeolitic imidazolate frameworks, such as ZIF-7, ZIF-8, ZIF-22, etc.) and carbons, as well as mesoporous materials such as the amine functionalized MCM materials. For the acidic gases such as hydrogen sulfide and carbon dioxide which are typically found in natural gas streams, adsorbent such as cationic zeolites, amine-functionalized mesoporous materials, stannosilicates, carbons are also preferred.;

Concept E: depressurizing one or more RC-PSA units in multiple steps to intermediate pressures so that the acid gas exhaust can be captured at a higher average pressure, thereby decreasing the compression required for acid gas injection. Pressure levels for the intermediate depressurization steps may be matched to the interstage pressures of the acid gas compressor(s) to optimize the overall compression system;

Concept F: using exhaust or recycle streams to minimize processing and hydrocarbon losses, such as using exhaust streams from one or more RC-PSA units as fuel gas instead of re-injecting or venting;

Concept G: using multiple adsorbent materials in a single bed to remove trace amounts of a first contaminant, such as H₂S, before removal of a second contaminant, such as CO₂; such segmented beds may provide rigorous acid gas removal down to ppm levels with RC-PSA units with minimal purge flow rates;

Concept H: using feed compression before one or more RC-PSA units to achieve a desired product purity;

Concept I: contemporaneous removal of non-acid gas contaminants such as mercaptans, COS, and BTEX; selection processes and materials to accomplish the same;

Concept J: using structured adsorbents for gas-solid contactors to minimize pressure drop compared to conventional packed beds;

Concept K: selecting a cycle time and cycle steps based on adsorbent material kinetics;

Concept L: using a process and apparatus that uses, among other equipment, two RC-PSA units in series, wherein the first RC-PSA unit cleans a feed stream down to a desired

product purity and the second RC-PSA unit cleans the exhaust from the first unit to capture methane and maintain high hydrocarbon recovery; use of this series design may reduce the need for a mesopore filler;

5 **Concept M:** using parallel channel contactors, wherein gas/solid contacting takes place in relatively small diameter adsorbent lined channels. This structure of the contactor provides the benefits of rapid adsorption kinetics through minimization of gas film resistance and high gas solid communication. A preferred adsorber design generates a sharp adsorption front.

10 It is preferred to have very rapid gas to adsorbent kinetics, i.e. the length through which the target species (e.g., target gas) diffuses to make contact with the adsorbent wall is kept short, preferably less than 1000 microns, more preferably less than 200 microns, and most preferably less than 100 microns. Favorable adsorbent kinetics may be realized by, while limiting bed pressure drop to acceptable values, utilizing parallel channel contactors wherein the feed and purge gases are confined to a plurality of very
15 narrow (1000 to 30 micron diameter) open channels that are lined to an effective thickness of the adsorbent material.

By “effective thicknesses”, we mean a range of about 500 microns to 5 microns for most applications. In the most limiting case of laminar gas flow, the very narrow channels limit the maximum diffusion distance for a trace species to no more than $\frac{1}{2}$ the
20 diameter of the channel. Even when adsorbing the desired species at the leading edge of the adsorption front, where their concentrations approach zero in the gas phase, a sharp adsorption front can be maintained by using such small diameter parallel channel structured adsorption bed configurations. Such a configuration can be in the form of multiple independent parallel channels, or in the form of very wide, very short channels
25 as may be achieved by using a spiral wound design.

Concept N: A means for rapidly heating and cooling the adsorbent bed structure so that adsorption can occur at a lower temperature and desorption at a higher temperature. The adsorption step then occurs at high pressure and the higher temperature desorption step can optionally take place at a reduced pressure in order to increase adsorbent swing
30 capacity. Depending upon adsorbent properties, it may be desirable to use a bed architecture suitable for either an externally temperature controlled or internally temperature controlled scheme.

By “internal temperature control”, we mean the use of a heating and cooling fluid media, either gaseous or liquid, preferably liquid, that can be circulated through the same adsorbent lined channels that are utilized for the gaseous feed flow. Internal temperature control requires that the adsorbent material not be adversely affected by the temperature control fluid and that the temperature control fluid be easily separated from the previously adsorbed species (H_2S and CO_2) following the heating step. Further, for internal temperature control, the pressure drop across each of the parallel channels in the structured bed during the gaseous feed adsorption step is preferably sufficiently high to clear each channel (or the single channel in the case of spiral wound designs) of the temperature control fluid. Additionally, internal fluid flow temperature designs preferably utilizes an adsorbent that does not strongly adsorb the temperature control fluid so that H_2S and CO_2 may be usefully adsorbed even in the presence of the temperature control fluid.

Non-limiting examples of such adsorbents include amine functionalized microporous and mesoporous adsorbents. A non-limiting example of such a system may be the use of supported amines on a water stable support with the use of hot and cold water (pressurized liquid or used as steam for heating) for heating and cooling. Whereas liquid water is left within the adsorbent wall during the adsorption step, if the thickness of the adsorbent wall is kept small (less than 1000 microns, preferably less than 200 microns, and most preferably less than 100 microns) it may be possible for H_2S and CO_2 to diffuse through the liquid water in time scales less than 1 minute, more preferred less than 10 seconds to become adsorbed by the supported amine. Following the desorption step, H_2S and CO_2 can be easily separated using distillation or other methods known to those skilled in the art.

By “external temperature control” we mean an adsorbent bed structure where the heating and cooling fluid is kept from contact with the gas carrying adsorbent channels. Such a structure can resemble a tube and shell heat exchanger, plate and frame heat exchanger or hollow fibers with a fluid impermeable barrier layer on the outer diameter or on the inner diameter, or any other suitable structures. In order to obtain rapid heating and cooling, the distance through which the heat diffuses from the temperature control fluid to the adsorbent layer should be kept to a minimum, ideally less than 10,000 microns, more preferably less than 1000 microns, most preferably less than 200 microns.

A non-limiting example of such an external temperature control bed design may

be the use of hollow fibers with a fluid impermeable barrier layer on the outer diameter wherein the hollow fibers are comprised of a mixed matrix system of polymeric and supported amine adsorbents. Feed gas is passed through the inner diameter of the porous fiber to be adsorbed by the adsorbent at lower temperatures, while cool temperature
5 control fluid is flowing over the fibers outer diameters. Desorption may be accomplished by passing hot temperature control fluid, preferably in a counter-current direction over the fibers outer diameter, thus heating the adsorbent. The cycle is completed by exchanging the hot temperature control fluid with cold fluid to return the fiber containing the adsorbent to the desired adsorption temperature.

10 In a preferred embodiment, the rate of heat flow in the system may be such that a sharp temperature gradient in the temperature control fluid may be established during heating and cooling such that the sensible heat of the system can be recuperated within the adsorbent bed structure. For such a non-limiting hollow fiber example, the useful fiber outer diameter dimension is less than 20,000 microns, preferably less than 2000
15 microns, and most preferably less than 1000 microns. The useful hollow fiber inner diameters (the feed gas channels) is less than 10,000 microns, preferably less than 1000 microns, and most preferably less than 500 microns as suitable based on the desired adsorption and desorption cycle times, feed adsorbed species concentrations, and adsorbent layer swing capacity for those species.

20 In one or more embodiments, it is advantageous to keep the ratio of non-adsorbing thermal mass in the adsorbent bed to adsorbent as low as possible. This ratio may preferably be less than 20, more preferably less than 10, and most preferred less than 5. In this manner, the sensible heat of the system that must be swung in each cycle may be kept to a minimum.

25 **Concept O:** A relatively low flow of about 0.01 to 5 % of the total feed of a clean gas substantially free of H₂S or CO₂ is utilized as a purge gas. Non-limiting examples of such gases (i.e., "clean gas") include methane and nitrogen that are maintained flowing through the parallel channels in a direction counter-current to the feed direction during at least a portion of the desorption steps of the process. It is preferred that the flow rate of
30 this clean gas be sufficient to overcome the natural diffusion of the desorbing H₂S and CO₂ to maintain the product end of the adsorbing channel in a substantially clean condition. That is, the purge stream should have sufficient flow rate to sweep the

desorbing CO₂ and H₂S from the channels and/or pores. It is this counter-current purge flow during desorption that ensures that on each subsequent adsorption cycle there may be no bleed-through of target species, such as H₂S or CO₂ into the product stream. A further benefit or objective of the clean purge is to assist in desorption of contaminants by reducing the partial pressure of contaminants in the flow channels of the adsorbent bed. This lessening of the partial pressure may be utilized to drive the contaminants from the adsorbent bed.

A preferred cycle and bed design for the practice of the present invention is that the product end of the adsorbent channels, i.e. the end opposite the end where feed gases enter) have a low, or ideally essentially zero concentration of adsorbed H₂S and CO₂. In this manner, and with suitable structured channels as described above, the H₂S and CO₂ may be rigorously removed from the feed gas stream. The downstream end of the bed can be kept clean as described by maintaining a low flow of a clean fluid substantially free of H₂S and CO₂, in a counter-current direction relative to the feed direction, during the desorption step(s), or more preferably, during all the heating and cooling steps in the cycle. It is further preferred that during the adsorption step, the adsorption part of the cycle be limited to a time such that the advancing adsorption front of H₂S and CO₂ loaded adsorbent not reach the end of the channels, i.e. adsorption to be halted prior to H₂S and/or CO₂ breakthrough so that a substantially clean section of the adsorbent channel remains substantially free of target species. With reasonably sharp adsorption fronts, this may allow more than 50 vol.% of the adsorbent to be utilized, more preferred more than 75 vol.%, and most preferred more than 85 vol.%.

[0034] The processes, apparatus, and systems provided herein are useful in large gas treating facilities, such as facilities that process more than five million standard cubic feet per day (MSCFD) of natural gas, or more than 15 MSCFD of natural gas, or more than 25 MSCFD of natural gas, or more than 50 MSCFD of natural gas, or more than 100 MSCFD of natural gas, or more than 500 MSCFD of natural gas, or more than one billion standard cubic feet per day (BSCFD) of natural gas, or more than two BSCFD of natural gas.

[0035] Compared to conventional technology, the provided processes, apparatus, and systems require lower capital investment, lower operating cost, and less physical space, thereby enabling implementation offshore and in remote locations, such as Arctic

environments. The provided processes, apparatus, and systems provide the foregoing benefits while providing high hydrocarbon recovery as compared to conventional technology.

[0036] Additional embodiments are provided in the following Embodiments A-Q:

Embodiment A: An adsorbent bed system comprising:

5 a first adsorbent bed of adsorbent material capable of selectively removing a target gas from a gaseous mixture, which adsorbent bed is substantially cylindrical shape;

 a second adsorbent bed of adsorbent material capable of selectively removing a target gas from a gaseous mixture, which second adsorbent bed has a substantially cylindrical shape (or other suitable geometric shape) and being disposed about the first bed of adsorbent material and is substantially the same cross-sectional area (e.g., face cross sectional area) as
10 the cross-sectional area (e.g., face cross sectional area) of the first adsorbent bed.

Embodiment B: The adsorbent bed system of Embodiment A, further comprising:

 a third adsorbent bed of adsorbent material capable of selectively removing a target gas from a gaseous mixture and being substantially cylindrical in shape and being
15 disposed about the second adsorbent bed of adsorbent material, the third adsorbent bed of adsorbent material having approximately the same cross-sectional area (e.g., face cross sectional area) as the cross-sectional area of the first and second beds of adsorbent material (e.g., face cross sectional area).

Embodiment C: The adsorbent bed system of Embodiment B, further comprising:

20 one or more additional beds of adsorbent material which have selectivity to a target gas in a gaseous mixture and having a substantially cylindrical shape and being disposed about the third adsorbent bed of adsorbent material, the fourth adsorbent bed of adsorbent material having approximately the same cross-sectional area (e.g., face cross sectional area) as the cross-sectional area (e.g., face cross sectional area) of the first, second
25 and third adsorbent beds of adsorbent material.

Embodiment D: The adsorbent bed system of any of Embodiments A-C, wherein the beds are connected at feed and product ends via rotary valving or non-rotary valving or a combination of these.

Embodiment E: The adsorbent bed system of any of Embodiments A-D, wherein the adsorbents are structured materials or combinations of structured materials and gas flow through the structured materials is substantially axial-flow.

5 **Embodiment F:** The adsorbent bed system of any of Embodiments A-D, wherein the adsorbents are non-structured materials or combinations of non-structured materials.

Embodiment G: The adsorbent bed system of Embodiment D, wherein the non-rotary valving comprises poppet valves, at least some of which share a common actuator.

10 **Embodiment H:** The adsorbent bed system of any of Embodiments A-G, which is assembled by introducing annular grooves into an adsorbent monolith and sliding annular rings of impermeable material into said grooves, said grooves running the length of the monolith material.

Embodiment I: The adsorbent bed system of Embodiment H, wherein the grooves are introduced using extrusion techniques or cutting techniques including lasers.

15 **Embodiment J:** The adsorbent bed system of any of Embodiments A-I, which is assembled by rolling/winding an adsorbent coated sheet on the outside of a cylinder containing a rolled adsorbent sheet of similar material as said adsorbent, and subsequently encasing said first rolled sheet in an annular cylinder of impermeable material,

Embodiment K: The adsorbent bed system of Embodiment J, wherein encasing also uses additional sealing and filling means.

20 **Embodiment L:** The adsorbent bed system of Embodiment J or K, wherein additional adsorbent sheets are successively wound and then encased to obtain multiple concentric vessels greater in number in than two.

Embodiment M: A method of processing hydrocarbons comprising the steps of:

25 (a) providing the adsorbent bed system of any of embodiments A-L or shown in the attached figures,

(b) recovering at least 5 million, or at least 15 million, or at least 25 million, or at least 50 million, or at least 100 million, or at least 500 million, or at least 1 billion, or at least 2 billion standard cubic feet per day (SCFD) of natural gas.

30 **Embodiment N:** The method of Embodiment M, wherein one or more additional steps utilize a kinetic swing adsorption process selected from the group consisting of: pressure

swing adsorption (PSA), thermal swing adsorption (TSA), calcination, partial pressure swing or displacement purge adsorption (PPSA), and combinations of these processes.

Embodiment O: The method of Embodiment N, wherein one or more swing adsorption process utilizes rapid cycles.

- 5 **Embodiment P:** The method of an of Embodiments M-O, wherein a gaseous feed stream is processed to achieve: (a) a desired dew point, (b) a desired level of detoxification, (c) a desired corrosion protection composition, (d) a desired dehydration level, (e) a desired gas heating value, (f) a desired purification level, or (g) combinations thereof.

Embodiment Q: A hydrocarbon treating apparatus comprising:

- 10 the adsorbent bed system of any of embodiments A-L or shown in the attached figures, wherein the hydrocarbon treating apparatus capacity is at least 5 million, or at least 15 million, or at least 25 million, or at least 50 million, or at least 100 million, or at least 500 million, or at least 1 billion, or at least 2 billion standard cubic feet per day (SCFD) of natural gas.

- 15 **Embodiment R:** The adsorbent bed system of any of the Embodiments A to Q, wherein the flow of streams through the first adsorbent bed and another adsorbent bed (e.g., the second, third or fourth bed) are configured to flow in opposite directions relative to each other.

- 20 **[0037]** In view of the many possible embodiments to which the principles of the disclosed invention may be applied, it should be recognized that the illustrative embodiments are only preferred examples of the invention and should not be taken as limiting the scope of the invention.

CLAIMS

What is claimed is:

1. An adsorbent bed system comprising:
 - a first adsorbent bed of adsorbent material capable of selectively removing a target
5 gas from a gaseous mixture, which adsorbent bed is substantially cylindrical shape;
 - a second adsorbent bed of adsorbent material capable of selectively removing a target
gas from a gaseous mixture, which second adsorbent bed has a substantially cylindrical shape
and being disposed about the first bed of adsorbent material and is substantially the same face
cross-sectional area as the face cross-sectional area of the first adsorbent bed.
- 10 2. The adsorbent bed system according to claim 1, further comprising:
 - a third adsorbent bed of adsorbent material capable of selectively removing a target
gas from a gaseous mixture and being substantially annular in shape and being disposed
about the second adsorbent bed of adsorbent material, the third adsorbent bed of adsorbent
material having approximately the same face cross-sectional area as the face cross-sectional
15 area of the first and second beds of adsorbent material.
3. The adsorbent bed system according to claim 2, further comprising:
 - a fourth adsorbent bed of adsorbent material which has selectivity to a target gas in a
gaseous mixture and having a substantially cylindrical shape and being disposed about the
third bed of adsorbent material, the fourth bed of adsorbent material having approximately
20 the same face cross-sectional area as the face cross-sectional area of the first, second and
third beds of adsorbent material.
4. The adsorbent bed system according to claims 1, 2 and 3 where the beds are
connected at feed and product ends via rotary valving or non-rotary valving or a combination
of these.
- 25 5. The adsorbent bed system of claim 4 where the adsorbents are structured materials or
combinations of structured materials and gas flow through the structured materials is
substantially axial-flow.
6. The adsorbent bed system of claim 4 where the adsorbents are non-structured
materials or combinations of non-structured materials.

7. The adsorbent bed system of claim 4 where the non-rotary valving comprises poppet valves, at least some of which share a common actuator.
8. The adsorbent bed system of claim 4, 5, 6 where the beds, valves and interconnections are used to deploy a swing adsorption process to separate components of a feed stream, such
5 that at least one resultant product stream is enriched preferentially in one of the feed components.
9. The adsorbent bed system of claim 4 where the swing adsorption process is a fast cycled pressure swing adsorption process.
10. The adsorbent bed system of claim 4 where the swing adsorption process is a thermal
10 swing process or a combination of thermal swing and pressure swing processes.
11. The adsorbent bed system of claim 1 which is assembled by introducing annular grooves into an adsorbent monolith and sliding annular rings of impermeable material into said grooves, said grooves running the length of the monolith material.
12. The adsorbent bed system of claim 11 where the grooves are introduced using
15 extrusion techniques or cutting techniques including lasers.
13. The adsorbent system of claim 1 which is assembled by rolling/winding an adsorbent coated sheet on the outside of a cylinder containing a rolled adsorbent sheet of similar material as said adsorbent, and subsequently encasing said first rolled sheet in an annular cylinder of impermeable material,
- 20 14. The adsorbent bed system of claim 13 where encasing also uses additional sealing and filling means.
15. The adsorbent bed system of claims 13 and 14 where additional adsorbent sheets are successively wound and then encased to obtain multiple concentric vessels greater in number in than two.
- 25 16. The adsorbent bed system of any one of claims 1 to 15, wherein the flow of streams through the first adsorbent bed and the second adsorbent bed are configured to flow in opposite directions relative to each other.

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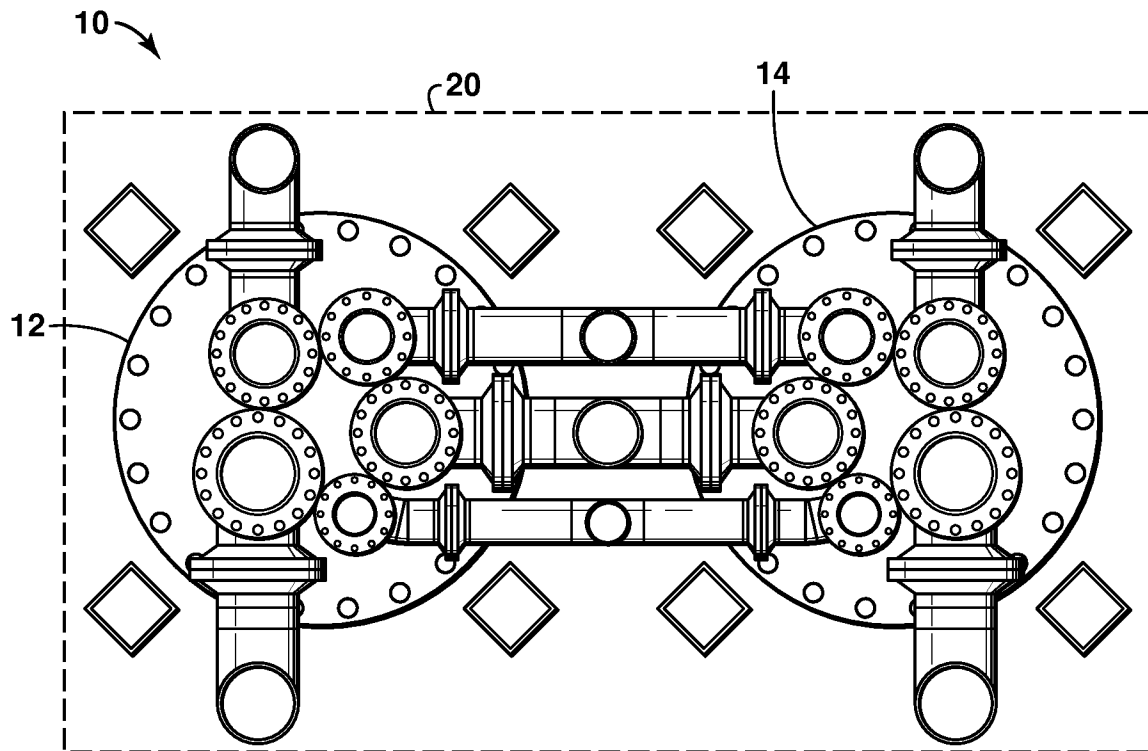


FIG. 1

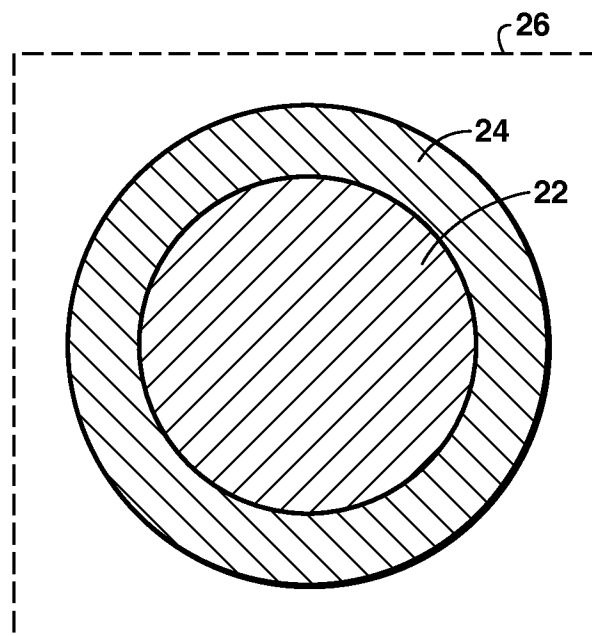


FIG. 2

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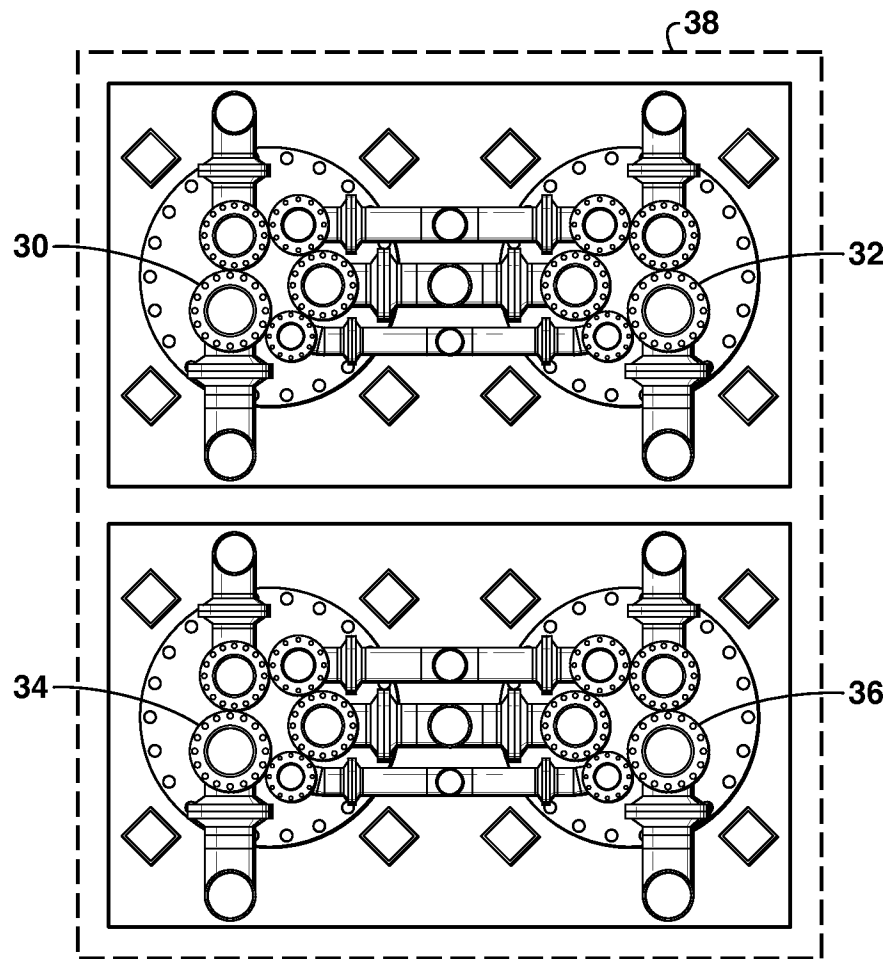


FIG. 3

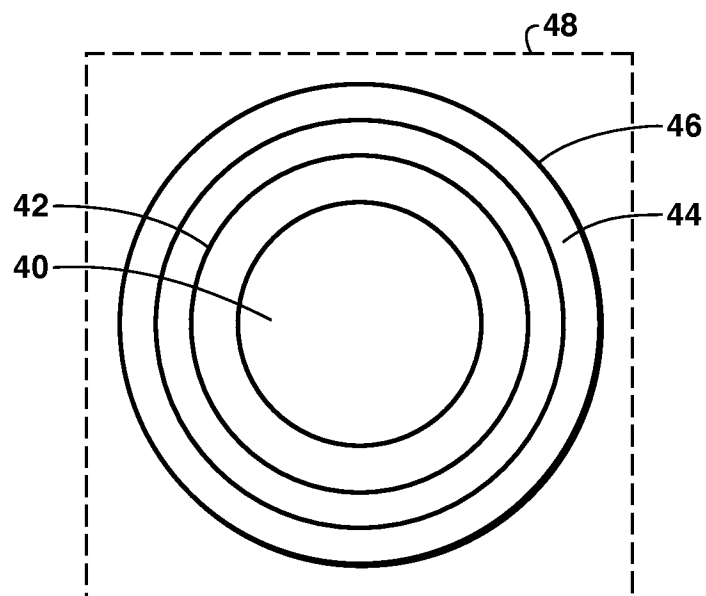


FIG. 4

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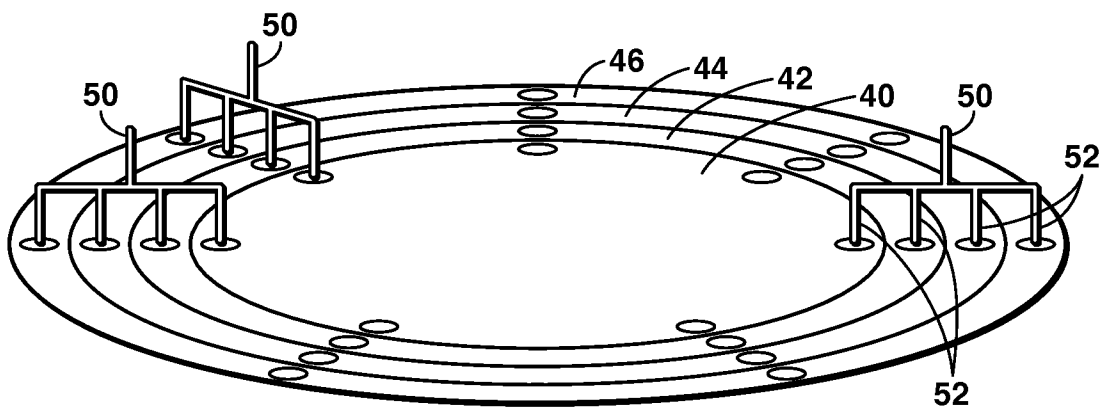


FIG. 5