COMMONWEALTH OF AUSTRALIA

The Patents Act 1952-1978

We, FAKOMBINAT SZOMBATHELY, a body corporate duly organized under the Laws of Hungary (formerly called NYUGAT-MAGYARORSZAGI FAGAZDASAGI KOMBINAT)

of Szombathely, Zanati ut 21, H-9700, Hungary,

hereby apply to the grant of a Patent for an invention entitled:

"PROCESS AND APPARATUS FOR THE PRODUCTION OF BODIES, EXPECIALLY BUILDING UNITS FROM AFTERHARDENING MATERIALS"

which is described in the accompanying complete specification. This application is a Convention application, and is based on an Application for a Patent or similar protection made under:-

Hungary Patent Application No. 2251-2004/87

Filed 5th May, 1987.

Our address for service is care of G.R. CULLEN & COMPANY, Patent Attorneys, of Dalgety House, 79 Eagle Street, Brisbane, in the State of Queensland, Commonwealth of Australia.

DATED this 14th day of April, 1988

FAKUM

FAKOMBINAT SZOMBATHELY
By their Patent Attorneys
G.R. CULLEN & CO.

APPLICATION ACCEPTED AND AMENDMENTS

ALC: 2 - 9 - 90

ONE HUNDRED DOLLARS

0 00 0 000

6 0 0 0 6 0 0

. O 9 O 9 O 9

0000

0 0 0 0 0 0 0 0

T.G. AHEARN

To: The Commissioner of Patents: AT SUB-OFFICE

Commmonwealth of Austral QBQED AT SUB-OFFICE

PATENT OFFICE PATENT OFFICE PATENT OF THE BRISDOM

BrisDom

BrisDom

APART 1988

BrisDom

BrisDom

BrisDom

APART 1988

BrisDom

BrisD

ONE HUNDRED DOLLARS FIFTY DOLLARS

COMMONWEALTH OF AUSTRALIA

DECLARATION IN SUPPORT OF AN APPLICATION FOR A PATENT

In support of the Application made for a patent

Insert Title of Invention for an invention entitled:

"PROCESS AND APPARATUS FOR THE PRODUCTION OF BODIES, ESPECIALLY BUILDING UNITS FROM AFTERHARDENING MATERIALS"

Insert

We, BELA MANDIK and LAJOS HORVATH,

Full Name(s) and Address(cs)

of C/- FAKOMBINAT SZOMBATHELY, Szombathely, Zanati Ut 21, H-9700 Hungary, do solemnly and sincerely declare as follows:—

1. xbanxwaxxxxxxxxxxxxxxxxxxxxxxxx

Insert Full Name(s)
of applicant(s)

(or, in the case of an application by a body corporate)

- 1. MXMMWWe are authorised by FAKOMBINAT SZOMBATHELY (formerly called NYUGAT-MAGYARORSZAGI FAGAZDASAGI KOMBINAT) the applicant(s) for the patent to make this declaration on its 外轮 behalf.

(or, where a person other than the inventor is the applicant)

Full Name(s) and Address(es) of Inventor(s) Dr. Tibor ALPAR, of Szombathely, Szekely Bertalan u. 20, 2. H-9700, Hungary, Janos GYORVARI, of Szombatheley, Levendula u. 8, H-9700, Hungary and Dr. Erno SCHMIDT, of Szombathely, Karpathi Kelemen u. 21, H-9700, Hungary

State how Applicant(s) Cerive title from inventor(s) e.g. The Applicant(s) is/are the assignee(s) of the invention from the inventor(s) শঙ্গare the actual inventor(s) of the invention and the facts upon which the applicant(s) is/are entitled to make the application are as follows:-

*Note: Paragraphs
3 and 4 need only be
acompleted for a
Convention Application

The said FAKOMBINAT SZOMBATHELY (formerly called NYUGAT-MAGYARORSZAGI FAGAZDASAGI KOMBINAT) is the assignee of the said DR. TIBOR ALPAR, JANOS GYORVARI and DR. ERNO SCHMIDT.

Basic Country (ies) Priority Date(s) Basic Applicant(s) 3. The basic application(x) as defined by Section 141 of the Act was tweeter made

The basic application(s) referred to in paragraph 3 of this Declaration was were the first application(s) made in a Convention country in respect of the invention(s) the subject of the application.

Declared at Szombathely this Hungary

To: The Commissioner of Patents

FAKOMBINAT

Mandik) (Lajos Horvát

Signature of Declarant(s)

G.R. CULLEN & COMPANY

(12) PATENT ABRIDGMENT (11) Document No. AU-B-15236/88 (19) AUSTRALIAN PATENT OFFICE (10) Acceptance No. 602764

(54) Title
PROCESS AND APPARATUS FOR THE PRODUCTION OF BODIES, ESPECIALLY
BUILDING UNITS FROM AFTERHARDENING MATERIALS

International Patent Classification(s)

- (51)⁴ C04B 040/02 B28B 003/24
- (21) Application No.: 15236/88 (22) Application Date: 28.04.88
- (30) Priority Data
- (31) Number (32) Date (33) Country 2251/87 05.05.87 HU HUNGARY
- (43) Publication Date: 10.11.88
- (44) Publication Date of Accepted Application: 25.10.90
- (71) Applicant(s) FAKOMBINAT SZOMBATHELY
- (72) Inventor(s)
 Dr. TIBOR ALPAR; JANOS GYORVARI; Dr. ERNO SCHMIDT
- (74) Attorney or Agent CULLEN & CO, GPO Box 1074, BRISBANE QLD 4001
- (56) Prior Art Documents AU 32105/84 B28B, C04B US 4117060
- (57) Claim
- 1. A process for the preparation of bodies or building units from an afterhardening mixture containing cement and/or lime as binding material, as well as additives and water, in the course of which the still not hardened mixture is admitted into a mould, where carbonation reaction is brought about by the injection of CO₂ gas into the mixture through a mould face and thereby the mixture is hardened, characterised by pressing the after hardening mixture continuously through a mould space in the mould which is open at both ends, while CO₂ gas is injected into the mixture under pressure reducing from an inlet port of the mould towards an outlet port of the mould, and a quasi gas tight plug of mixture is formed by compaction of the mixture within the mould in the vicinity of the inlet port, and a quasi gas tight condition is brought

(11) AU-B-15236/88 (10) 602764

about between this plug and the mould face, furthermore in the vicinity of the outlet port as much amount of CO_2 gas is injected into the mould as necessary for full completion or substantially full completion of the chemical reaction of carbonation.

An apparatus for the continuous production of bodies or building units from an afterhardening mixture containing cement and/or lime as binding material, as well as additive and water, by its carbonation, said apparatus being provided with a mould having a mould space, a CO, gas-source and holes in at least one wall of the mould, suitable for injection of CO, gas into said mould space, at a pressure exceeding atmospheric pressure, characterised by the mould having an inlet port for admitting the raw afterhardening mixture, and an outlet port for discharging the mixture hardened by carbonation, a plurality of separate zones disposed between said inlet port and said outlet port; a press mechanism situated in front of said inlet port for pressing the raw afterhardening mixture into the mould space and for forming a quasi gas tight plug of mixture within the mould in the vicinity of the inlet port, said press mechanism also adapted to press the raw afterhardening mixture into the mould space and moving said afterhardening mixture as well as said mixture hardened by carbonation through said mould space; the holes leading into the mould space serving for inlet of the CO, gas being divided into separate hole groups which communicate with gas injection devices suitable for ejecting CO, gas, at pressures to be separately controlled for each said zone.

This document contains the continuents of the conti

COMMONWEAT THE C

COMMONWEALTH OF AUSTRALIA

The Patents Act 1952-1969

Name of Applicant:

FAKOMBINAT SZOMBATHELY

Address of Applicant:

SZOMBATHELY, ZANATI UT 21, H-9700, HUNGARY

This document contains the amendments made under Section 49 and is correct for printing

Actual Inventor:

000000

0000

0 00

0000

000

00

00 1

DR. TIBOR ALPAR JANOS GYORVARI DR. ERNO SCHMIDT

Address for Service:

G.R. CULLEN & COMPANY,
Patent & Trade Mark Attorneys,
Dalgety House,
79 Eagle Street,
BRISBANE. QLD. 4000
AUSTRALIA

COMPLETE SPECIFICATION FOR THE INVENTION ENTITLED:

"PROCESS AND APPARATUS FOR THE PRODUCTION OF BODIES, ESPECIALLY BUILDING UNITS FROM AFTERHARDENING MATERIALS"

The following statement is a full description of the invention including the best method of performing it known to us:

The invention relates to a process for the production of bodies, especially building units from afterhardening materials containing hydraulic binder, particularly cement as setting agent.

known, at which hardening of the cement-set moulded

material is accelerated by injection of CO, gas into

4,093,690 and Swiss patent specification No. 1 460 284).

These methods are based on carbonation, i.e. a process

the cement mortar quickly changes over to limestone upon

to each other that the product, e.g. building panel may

minutes, though hydration of the binding material, e.g.

when the large amount of Ca(OH), compound present in

the effect of CO₂ gas. The limestone molecules being

formed during this process, become so tightly bonded

reach even 35-50 % of its 28-day-strength in 5 - 30

the raw mixture (e.g. US patent specification No.

Such building unit production methods are

5

10

.... 15

20

The carbonation takes places generally in a closed space containing the raw mixture to be set with cement by producing differential pressure, then a pressure exceeding the atmospheric one is brought about with the injection of CO_2 gas, as a result of which the CO_2 gas may penetrate into the pores of the raw mixture and chemical reaction takes place. The raw mixture is filled into a mould determining the shape

.

of the product to be produced and compacted, then placed into a closed space together with, or removed from the mould. These methods, however, are fairly costly, because the closed spaces require careful sealing to be realized with difficulty and at high cost. Apart from this, the alternating use of vacuum and high pressure is lengthy, thus, the techologies allowing only a step by step production carried out with several operations (filling into the mould and compacting; filling and discharging the carbonation space; carbonation) take fairly long time.

A building unit production technology combined with carbonation is described in the Hungarian patent specification No. 189.455 where elastic fibrous material as additive is used for the preparation of the cement-set raw mixture, and there is utilized the characteristic feature of this mixture for more or less elastic reversion after compaction, thus, its volume expands when the compressive force is stopped during the setting time of the hydraulic binding material, i.e. cement. The raw mixture placed between two press--plates is compressed in a greater degree in the vicinity along their flanges than the rest of the mixture - either by using a thicker part along the flanges of the press-plate or by applying a locally greater amount of raw mixture - thus, a strip of higher density, consequently of lower gas permeability is formed at the flanges, than within. This strip of

20

5

10

15

0 0 0 0 0 0

000000

0000

0000

of the state of th

higher density along the flanges functions as a seal, and prevents the CO₂ gas injected for carbonation from escaping from the mixture on the sides. Although this method is more favourable than the former ones its drawback resides firstly in its periodicity, thus in its relatively low productivity and in the fact that a solid end-product can be produced only from mixtures containing elastic fibrous material.

The invention aims at providing a process for the production of bodies, particularly building units from an afterhardening material by accelerating the setting with carbonation, which partly allows a continuous production thereby considerably improving the productivity and economic efficiency, and partly it is not restricted to the use of afterhardening mixtures prepared with an elastic fibrous additive as a starting material (to be moulded), whereby it substantially extends the choice of products to be economically produced with carbonation.

The invention is based on the recognition that when the afterhardening material is passed through a moulding space open at both ends, and escape of the CO_2 gas is prevented by a continuous mechanical compaction of the raw mixture in the vicinity of the point of inlet and by reducing the pressure of the CO_2 gas to a minimum - in the given case to the atmospheric pressure - in the vicinity of the point of outlet, and the CO_2 gas is injected between these two points into the mould space evenly distributed along the

0 00 8 0 0

5

@ # @ O O O

စ ဝဝ ဇ ၈ စ မ ၈ စ

9 G G

mould face(s), however under a pressure reduced from the inlet towards the outlet, the production may be made continuous, and the product emerging from the mould space will appear in a solid, moulded state as a result of carbonation taking place in the mould space.

On the basis of this recognition, the problem was solved by a process for the preparation of bodies or building units from an afterhardening mixture containing cement and/or lime as binding material, as well as additives and water, in the course of which the still not hardened mixture is admitted into a mould, where carbonation reaction is brought about by the injection of CO, gas into the mixture through a mould face and thereby the mixture is hardened, characterised by pressing the after hardening mixture continuously through a mould space in the mould which is open at both ends, while CO gas is injected into the mixture under pressure reducing from an inlet port of the mould towards an outlet port of the mould, and a quasi gas tight plug of mixture is formed by compaction of the mixture within the mould in the vicinity of the inlet port, and a qyasi gas tight condition is brought about between this plug and the mould face, furthermore in the vicinity of the outlet port as much amount of CO, gas is injected into the mould as necessary for full completion or substantially full completion of the chemical reaction of carbonation. afterhardening material is stamped-pressed into the mould

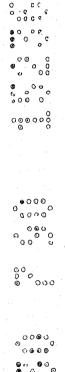


5

6000 6001 15

୍ଜନ୍ତ ଜୁନ୍ତ ଅଧ୍ୟୟର ବୃକ୍ତ ଅନ୍ୟୁଦ୍

space preferably with a recipricating device. ${\tt Expediently,\ the\ CO_{a}\ gas\ is\ injected\ into}$





the mould space through at least one of the confining surfaces under pressure exceeding the atmospheric pressure; and when passed throug the afterhardening material the gas of reduced pressure and quantity is discharged from the mould space through at least another mould face, and/or vacuum is applied to at least one face of the mould space, and this way the CO₂ gas is made flown through the material, or its flow is intensified.

According to another advantageous feature of the invention, in a zone following the compacted layer of material in the vicinity of the inlet port, CO, gas at a pressure of suitably 3-6 bar is injected into the pores of the mixture then - looking in the direction of the material's movement - in a second zone, where the instantaneous explosion-like reaction of carbonation takes place, CO, gas under a lower pressure of e.g. 2-3 bar is injected into the material, the quantity of which is essentially the same as that of the CO, gas consumed by the reaction, whereby the carbonation reaction is continued, then in a third zone co, gas under even lower pressure of e.g. 1-2 bar is injected into the mould space, whereby essentially full completion of the carbonation reaction is realized. A further embodiment of the process is characterized by creating a balancing zone in the mould space situated directly behind the outlet port of the material hardened by carbonation, where the gas outflow is checked, and in the zone(s) behind the balancing zone, gas is injec-

25

ted as a function of the quantity of the outflowing amount and/or pressure of the gas. It is generally advisable to cut to size - suitably by sawing - the carbonation-hardened body leaving the mould space, and to inject the CO_2 gas into the mould space with a gas mixture, containing suitably at least 30 % of CO_2 gas.

It may be advisable to inject the CO₂ gas into the raw mixture prior to feeding it into the mould. The setting proces can be accelerated by this carbonation pretreatment.

The apparatus according to the invention contains a mould, a CO, gas-source, e.g. gas bottle and openings e.g. holes in at least one wall of the mould, suitable for injection of CO2 gas into the mould space, the pressure of which exceeds the atmospheric pressure, and this apparatus is characterized in that the mould has an inlet port for feeding in the raw afterhardening mixture and an outlet port for discharging the body hardened by carbonation; a press mechanism situated in front of the inlet port for pressing the raw afterhardening mixture into the mould space, and moving the afterhardening mixture and the body hardened therefrom by carbonation through the mould space; and the holes leading into this mould space and used for injection of the CO, gas are divided into separate hole groups communicating with devices suitable for injecting CO2 gas, at pressures to be separately controlled for each zone. It is expedient when at

0 0 a

\$ 6 6 6 0 0 5 6

least one wall of the mould is provided with holes for outlet of the CO_2 gas remaining - in given case - after the completed chemical reaction of carbonation, which holes are expediently communicating with pipes connecting the CO_2 gas source, e.g. gas bottle with the mould plate containing the holes for injecting CO_2 gas into the mould space.

An embodiment of the apparatus is characterized by having a forward pipe for feeding the CO, gas into the mould space and a return pipe for feeding back into the forward pipe the CO2 gas remaining - in a given case - after the completed carbonation reaction; a gas pump being connected to the forward pipe into which also the return pipe is leading, and - in up-stream direction of the gas flow - a pipe containing shut-off means, leading out of the CO, gas supply source, e.g. gas bottle being joint to the return pipe before the pump, and the forward pipe being interconnected through leg pipes containing valves with separate hole groups on the gas inlet side, while leg pipes containing similarly valves and leading from the hole groups into the return pipe are provided for discharging the gas remaining - in a given case after the completed carbonation reaction. A vacuum pump be inserted into the return pipe.

According to a further feature of the invention the hole groups on both the gas inlet side and

_

10

15

20

the remaining gas outlet side is leading into separate closed chambers fitted expediently gastight to the outer face of the mould plates. Furthermore it may be of advantage, when the hole groups are leading from - e.g. meandering - ducts running inside the mould plates into the mould space, each duct communicating with one of the leg pipes emerging from the forward pipe or with one of the leg pipes leading into the return pipe.

5

10

15

20

25

According to another embodiment of the apparatus given by way of example, a device, e.g. a saw suitable for cutting up the carbonation-hardened body emerging from the mould space is arranged behind the outlet port of the mould.

According to another arrangement of the invention, chambers covering at least one of the hole groups are fitted to the outer side of the mould plates in the vicinity behind the outlet port of the mould, and gas outlet stubs containing control valves are leading out of the chambers.

A further embodiment of the apparatus is characterized by providing a press mechanism with a reciprocating beater, e.g. a piston, the cross sectional shape and size of which are the same or essentially the same as those of the mould's inlet port. In this case it is expedient, when the position of the mould and the path of the piston are vertical, the piston is fitted between guide rails, the guide rails are covered by a bell-shaped protective cover, the lower flange of which

is running in the vicinity of the lower edge of the guide rails and a gap is provided for between said lower flange and the guide rails; and the actuating mechanism together with the protective cover is situated in a hopper serving for feeding the raw afterhardening mixture into the mould, the hopper leading into the upper end of the mould space.

The invention will be described below in further details on the basis of the attached drawings illustrating a preferred embodiment of the apparatus by way of example, some of its structural details, graphs in connection with the exemplified process variants furthermore some of the building units producible with the method according to the invention, as follows:

Fig. 1 is a schematic vertical cross section of the apparatus;

Fig. 2 a horizontal section along line
A-A according to Fig. 1;

Fig. 3a an embodiment of one of the mould plates drawn to a larger scale, showing the sectional view along line B-B according to Fig. 3;

Fig. 3b a view from the direction of arrow C, marked in Fig. 3a;

Fig. 4 a graph illustrating the change of the pressure and the body's density within the mixture as a function of the time, taking place

10

5

15

20

during compression of the afterhardening mixture p. d with nonelastic additive;

Fig. 5 a characteristic curve related to the afterhardening mixture, same as the one shown in Fig. 4, but prepared with elastic additive;

Fig. 7 a set of curves different from the one shown in Fig. 6 in that it is formed by the curves shown in Fig. 5;

Fig. 8 a diagram showing the gas pressure, path and time;

Figs. 9a-9f building units of different cross sectional shapes prepared with the method according to the invention, to illustrate the extensive applicability of the invention;

Fig. 10 a production model of the building unit shown in Fig. 9f produced with carbonation method according to the invention.

The apparatus shown in Figs. 1 and 2 contains a mould designated as a whole with 1, a hopper 2 and a press mechanism 3 which in the present embodiment,

5

*. 10

£

20

comprises a piston 8 moving up and down as indicated by the double arrow \underline{b} , having an expanding neck-part, an actuating mechanism (not shown), and vertical guide rails 9 on both sides of the piston 8 for guiding it while moving up and down.

The mould space 5 of the mould 1 is confined by vertical mould plates 4a, 4b of width s (Fig. 2) situated at a distance a from each other (Fig. 1) and by similarly vertical, narrow walls (not shown) perpendicular to the mould plates; the apparatus according to Figs. 1 and 2 is namely used for the production of building panels 22 of thickness a, whose width perpendicular to the plane of the drawing (Fig. 1) is determined by the width of the mould plates 4a, 4b meassured in the same direction (value s in Fig. 2), whereas their other dimension, e.g. the length in the plane of the drawing (fig. 1) may optionally be selected between practical limits. The rould 1 is open on its top and bottom; the inlet port of the mould is marked with reference number 6, and its outlet port with 7. The hopper 2 (feed hopper) is leading into the upper open end of the mould 1, and the piston 8 in the hopper fits into the inlet port 6 of the mould 1, i.e.: its cross sectional shape and size are essentially identical with, suitably somewhat smaller than those of the outlet port 6.

A bell-shaped protective cover 10 with its open end 10a turned down is arranged in the hopper 2 above the mould 1, which covers the guide rails 9 and whose

.

5

10

15

. . .

20

lower flange is running in the vicinity of the lower ends of the vertical guide rails 9. The protective cover 10 is situated at a distance from the inner surface of the hopper 2 as well as from the outer surfaces of the guide rails 9, and its outer surface is suitably curved thereby facilitating downward movement of the raw mixture admitted in the direction of arrows \underline{c} toward the inlet port 6 in the hopper 2.

The apparatus includes a gas tank 14 shown in Fig. 1, containing CO, gas at a pressure exceeding the atmospheric pressure, said gas tank being connected through an intermediate pipe 15 fitted with a shut off means 15a to the return pipe 18 leading to the circulating gas pump 16. From the gas pump 16 a forward pipe 17 is leading out from which leg pipes 17a-17c are branching off fitted with valves 17a'-17c'. The leg pires 17a-17c are leading into distribution chambers 23-25 situated along the mould plate 4b above each other, one of their confining faces being formed by the outer side of the mould plate itself, and the chambers 23-25 are separated from each other by - expediently gastight - sealings 31. A further chamber 26 is arranged below the chamber 25, being separated from this latter similarly by sealing 31, and having a deacrating and gas pressure compensation stub leading out therefrom and fitted with valve 21a.

20

25

Four chambers are adjoining also the outer surface of the mould plate 4a marked " going downwards from the top - with reference numbers 27-30. Leg pipes

18a-18c are leading out from the chambers 27-29, a manometer 19 and one of the valves 18a'-18c' being built in each of the leg pipes. The leg pipes 18a-18c are connected to said return pipe 18 in which a vacuum pump 32 is inserted. A deacration and gas pressure compensation stub 20 fitted with valve 20a (contru? valve) is leading out of the lowest chamber 30. The chambers 27-30 are also separated from one another by sealings 31.

Holes 12 are passing through the mould plates 4a, 4b as clearly shown in Fig 2, while the same holes are illustrated with dotted lines in Fig. 1. Thus, the holes 12 establish gas passage connection between the mould space 5 and the chambers 23-26 and chambers 27-30, respectively (only chamber 23 is shown in Fig. 2).

15

25

The mould 1 is divided into technological zones designated - going downwards from the top - by I-IV, each comprising a pair of chambers 23, 27; 24, 28;, 25, 29; and 26, 30; the function of these zones will be described further in the part dealing with operation of the apparatus.

The gas can be injected into the mould space 5 not only as shown in Figs. 1 and 2 but also with the structural solution shown in Figs. 3a, 3b. In this case, the mould plates 4a, 4b contain a duct system formed according to the said technological zones I-IV. The uppermost zone I has two, and each of the zones II-IV has one meandering hole group 11 for transmitting the gas, whose holes 12 are leading out similarly from a meandering gas distributing duct 13, and which are running in the interior

of the mould plate 4b. (For the sake of better overview, only four holes 12 leading into the mould space 5 are shown in Fig. 3a.) Each gas distribution duct 13 has an inlet stub 32 connected to one of the leg pipes 17a...17n (in the present example to leg pipe 17a according to Fig. 3a) leading out of the forward pipe 17. Naturally, valves 17a'-17n' are installed in each leg pipe to adjust independently the gas pressure of CO₂ flowing out of each hole group 11. Duct and hole systems identical to those in Fig. 3a, 3b, are to be provided for in the mould plate 4a, where the return pipe 18 for each hole group is connected to the leg pipes 18a-18n.

The chambers 23-26 and 27-30 in Figs. 1 and 2, as well as the hole groups 11 connected to independent gas pipes according to Figs. 3a, 3b offer the possibility to inject the ${\rm CO}_2$ gas into the mould space 5 in the locally determined zones under different pressures.

Production of the building panel with the apparatus according to Figs. 1 and 2 (as well as Figs. 3a, 3b) is carried out as follows:

The afterhardening raw mixture containing cement as binding material is fed into the hopper 2 at a steady rate and continuously according to arrows \underline{c} shown in Fig. 1. The afterhardening material passes downwards to the inlet port 6 of the mould 1. The piston 8 is kept in reciprocating motion as indicated by the double arrow \underline{b} . The piston 8 performs about 15-300, mainly 100-150 compression steps per minute, i.e. the up-and-down motion

5

25

of the piston is variable - depending on the building unit to be produced and/or on the basic material - within wide limits and it may also be very fast. The cover 10 prevents the raw mixture from passing to the upper end of the guide rails 9, which would cause troubles in or inhibiting the run of the piston 8 pressing the afterhardening material from the hopper 2 in between the mould plates 4a, 4b, i.e. into the mould space 5. As a result of this pressing in, density of the raw mixture increases - due to the relaxation - to the multiple of the value preceding its compression. Part-quantities of the material in proportion with the stroke of the piston 8 fill up the mould space 5, and the carbonated cement-set material treated with ${\rm CO}_2$ gas (or with the ${\rm CO}_2$ component of a gas mixture) while passing through, leaves the outlet port 7 of the mould 1 in a hardened condition continuously.

The above production technology to be described subsequently in detail including its phases is enabled by the factors as follows:

- the cement-set raw mixture - prepared practically by any additive - is always of a porous texture. Extent of the porosity depends on the measure of additive components of the mixture (e.g. size of grain and/or fibre) and on the compression. Porosity means that the mixture is permeable to gas and this feature has an important role in the carbonation, because the CO₂ gas can only be injected in a gas-permeable composition of materials;

the mixture arises in the vicinity of the inlet port 6 of the mould 1, dropping as continuously going downwards in the mould space 5. As a result of the said maximum internal pressure, the material will become quasi gastight to such an extent, that the CO₂ gas injected into the mould space 5 can not escape from the mould through the inlet port 6. In other words: the gastight condition of the product is ensured by its still unhardened, but already compacted material.

Returning to the description of operation of the apparatus according to Fig. 1, the material passed downwards by the piston 8 through the mould space 5 is treated in the technological zones I - IV, the carbonation taking place mainly in zones I - III.

By stamping in the material in the uppermost part of the zone I in the vicinity of the inlet port 6, a quasi gastight condition is brought about in the material - as referred to above - i.e. mechanically by utilizing also the relaxation force of the compressed material, the CO₂ gas injected into the material in the mould space 5 is prevented from escaping through the chamber 23 and the holes 12 (see also Fig. 2). (Since both the feeding of the raw mixture and stamping-pressing are continuous, the quasi gastight core is constantly present in the upper part of the mould during the whole process of production, by way of continuous reproduction). Effect of

5

15

25

the mechanical compaction (though at a downwardly decreaseing extent) extends to the whole zone I, the value of the relaxation force is high, thus, a fairly high gas pressure and/or the use of vacuum from the wall 4b of the mould are required for injecting the CO2 gas into the pores of the raw mixture; so to say the CO2 gas has to be pressed into the pores of the mixture. The required gas pressure, e.g. 6 bar can be set with the valve 17a' (Fig. 1). The efficiency of injecting the CO₂ gas into the mixture can be improved by using the vacuum pump 32; in this case the valve 18a' is open. The pressure conditions of the gas flowing through can be controlled with the manometer 19 built into the leg pipe 18a, and the valves 17a', 18a' are adjustable as necessary. By use of a vacuum of e.g. 0.5 bar a differential pressure is brought about on the inner faces of the mould plates 4a, 4b, whereby the transversal gas flow from the mould plate 4b towards the mould plate 4a will obviously become more intensive, and the pores of the mixture will evenly be filled with CO2 gas in the whole cross section.

The pores of the mixture in zone I will be filled up with ${\rm CO}_2$ gas, while the unnecessary gas of lower pressure (e.g. 3 bar) entering the chamber 27 through the holes 12 of the mould plate 4b returns through the leg pipe 18a and the return pipe 18 into the gas cycle. Directions of the gas flow through the pipes shown in Fig. 1 are marked with arrows, while path of the gas passing from the leg pipe 17a into the chamber 23 in Fig. 2 is marked

by arrow e, and the path of the gas flowing through the holes 12 into the mould space 5 is marked by arrow f. The same marks \underline{e} and f were used in Figs. 3a and 3b accordingly. It is noted that the gas injection method according to Figs. 3a, 3b offers the possibility that it is sufficient to inject gas under a lower pressure, e.g. 5 bar into the mould space 5 through the second hole group 11 from above (Fig. 3) in the lower range of zone I, where the compacting effect of the piston 8 is less effective and the material has a less density (the internal stress of the compacted mixture - as referred to is at a maximum on the upper end of the zone I, then it gradually drops when going downwars); in this case, the pressure of the remaining discharge gas is about 2-3 bar. In any case, the pressure of the CO2 gas injected into the zone I has to be selected so as to prevent it from escaping through the compacted layer of material situated above the zone I in the vicinity of the inlet port 6 of the mould 1. Since a quasi gastight condition exists also between the inner faces of the mould plates 4a, 4b and the mixture, the CO2 gas can not escape from the mould space 5 along the mould plates either. Injecting the gas into the zone I under two different pressures has the further advantage that the low-pressure gas cannot flow from below upwards to the inlet port 6, because this is prevented by the higher pressure gas forcing the low pressure gas towards the opposite mould plate 4a, i.e. to a transversal passage through the mixture.

:... 10

5

15

20

5

15

25

The chemical reaction between the CO2 gas and the cement - i.e. the carbonation - just begins in zone I, but it takes place explosion-like (instantaneous reaction) in zone II. The chemical reaction consumes the CO, injected into the zone I, the pressure drops, and vacuum would develop in the material unless the ${\rm CO}_2$ is replaced. Therefore, continuing the injection of CO2 into the zone II through the leg pipe 17b and the chamber 24, the ${
m CO}_2$ gas consumed in the zone I during the chemical reaction, is replaced. In zone II, the ${\rm CO_2}$ gas is injected under a lower pressure still exceeding the atmospheric one e.g. at 4 bar (it is unnecessary to press the gas under into the pores of the mixture, at a higher pressure), which flowing through the material, passes into the chamber 28 under a pressure not more than about 2 bar and returns to the gas cycle through the leg pipe 18b and the return pipe 18. By correct adjustment of the valve 18b', vacuum can be applied also in the zone II, but this is not essential.

extent already in zone I, while in the zone II its intensity completely stops the relaxation force. Thus, the building panel 22 (Fig. 1) in state of hardening is capable to pass downwards in the mould 1 unobstructed and continuously, the material is not pressed against the walls of the mould as in the upper part of the zone I (where the compressive force produced by the piston 8 forces downwards the still unhardened raw mixture). As a result of the chemical reaction of carbonation, vacuum will develop

in the material.

10

15

20

25

The pressure of the ${\rm CO}_{2}$ gas injected into the zone III is further reduced, gas at a pressure of e.g. 1 bar is fed thereto. The carbonation process in this zone is practically completed. The amount of the gas admitted to the zone III shall cover the still missing gas required for the whole carbonation reaction. This way, the detrimental loss of ${\rm CO}_2$ - adversely influencing the economic efficiency of the process can be prevented at the lower end of the mould space 5, i.e. at the outlet port 7, where the compressed, already carbonated partly hardened material passes into the open air, merely by bringing about appropriate pressure conditions in the zone III, in other words: here is fed only a minimum amount (pressure) of the CO, gas. The pressure of the remaining CO2 gas flowing into the chamber 29 (if no vacuum exists) is not much lower than the pressure of the admitted gas, e.g. 0.8 - 0.9 bar. Thus the carbonation reaction is safely completed. It is noted, that a vacuum of e.g. 0.5 bar can be brought about with the pump 32 also in the zones II and III in order to intensify the transversal gas flow in the chambers 28, 29.

Zone IV is a balancing zone where no ${\rm CO}_2$ gas is fed to, here practically no chemical reaction takes place. Into the chambers 27 and 30 the ${\rm CO}_2$ gas flowing eventually hereto along the mould plates 4a, 4b flows outwards from within, the amount and pressure of which

were selected in the zone III so as to be sufficient for completing the carbonation reaction. If the pressure of gas was correctly selected in the zone III, the gas should just blow out through the control valves 20a, 21a. Thus, with the aid of these control valves 20a, 21a the pressure of the CO_2 gas can be balanced in the zone IV. Consequently the production technology does not entail any overconsumption of CO_2 , because practically no perceptible amount of gas escape either on the top or the bottom of the mould 1, which is a significant factor for the economic efficiency.

5

10,

.....

15

20

25

If, however not pure CO_2 gas but a gas mixture was used for the carbonation that contains CO_2 only in part (e.g. 30 %), the neutral gas component(s) is (are) not used up for the carbonation reaction. and in this case the amount of gas (air) emitted through the control valves 20a, 21a may also be fairly large, and in this case the valves 20a, 21a function as air vent.

Although the individual phases of the carbonation process are realized separately from one another in space and time, the whole process of production is continuous, since the material to be moulded and hardened to building panel passes through the mould space 5 continuously. The building panel 22 discharged continuously in infinite length through the outlet port 7 is cut to size by the transversal saw 21 its operation being synchronized with the pressing rate, thus, there are obtained partially hardened building panels - having e.g.

a strength representing about 30% of the 28-day-strength which can be further cured by any known method - by artificial ageing of by allowing to stand.

5

10

15

20

25

Cross section of the building panel 22 produced with the apparatus according to Figs. 1 and 2, is shown in Fig. 9a but it is easily conceivable that with the aid of the and apparatus according to the process invention, optional cross section of the building units can be produced - within practical limits - by an appropriate selection of the cross sectional shape of the mould space and the piston, Cross section of the building unit 30 according to Fig. 9b is wedge-shaped, while the building unit 31 shown in Fig. 9c is of wavy-sgape. A trapezoid building unit 32 is shown in Fig. 9d. In fact, the production of a hollow building unit is also possible with the aid of the invention. The element 33 shown in Fig. 9e has an annular cross section whose circular hole is marked with reference number 33a. The rectangular building unit shown in Fig. 9f has two cavities 34a and 34b. Naturally the production of hollow building units requires a suitable mould to form the cavities; the construction of the mould structure for the building element according to Fig. 9f is shown in Fig. 10. Ducts and holes are formed in the outer mould frame 34 as well as in the walls of the hollow internal mould cores 36, 37 (the cavities are marked with reference numbers 36a and 37a) - similarly as shown in Figs. 3a, 3bfor injection of the CO2 gas, or for putting it through the material passing through

the mould. A possible way of having the gas flown is shown in Fig. 1 by arrows, but for the better overview, illustration of the ducts and holes is omitted.

Moreover, the amount of ${\rm CO}_2$ gas required for carbonation is always proportionate to the quantity of cement used according to the given formula, making out about 8-10 mass % thereof. The gas mixture used for carbonation - if not pure ${\rm CO}_2$ is used - should contain expediently at least 30 % of ${\rm CO}_2$.

The invention is described in further details by way of examples as follows:

Example 1

5

15

25

20 mm thick, 60 x 100 cm building panels are produced with the process according to the invention using the apparatus shown in Figs. 1 and 2. Composition of the raw afterhardening mixture to be moulded by pressing and treated with carbonation is the following:

cement	4	2	mass	ç
caustic lime		2	ji L	
quartzsand	4	2	H .	
water	1	4	16	

Fig. 4 illustrates the trend of the internal stress (pressure) \underline{P} and the density \underline{R}_0 as a function of the time consequent upon compression in the mixture not containing elastic (organic) additive-component. In the initial phase of the pressing process both the internal stress and the density are rapidly increasing, but after a short time, increase of the density slows down, the curve

 \underline{R}_0 is nearly parallel to the axis of time (it hardly approches to the latter) while the internal stress \underline{P} upon reaching a maximum, remains essentially constant for a short time, then it rapidly draps. The internal stress at the intersection \underline{M} of the curves \underline{P} and \underline{R}_0 is only as high, at which the density \underline{R}_0 of the mixture practically would not change even if the compressive force was stopped. (Moreover, the pressure and density of all those afterhardening mixtures are characterized by curves similar to the graph in Fig. 4, the moisture content of which is at most 50 % and their additives are inorganic, rigid materials e.g. sandy gravel, gravel, siliceous earth, fibreglass etc.).

The pressure conditions - i.e. trend of the internal stresses - as a function of the time, arising while pressing in the mixture described in this example, with the reciprocating piston 8 of the apparatus as shown in Figs. 1-3, are illustrated with the set of curves according to Fig. 6. Each curve P represents the internal stress-influence line of the compression performed with each piston stroke. Fig. 6. clearly shows that in the uppermost layer of the mixture in the mould space 5 (Fig. 1) always the same - and maximum - internal stress prevails, and it exists continuously, because the upper horizontal parts of the curves P (see also Fig. 4) are practically passing into one another. Thus, as a result of the mechanical pressing process in this upper layer of the material, the quasi gastight condition is ensured until the piston 8 of the apparatus stamps the mixture

15

5

10

2 C

into the mould 1.

15

20

25

The ${\rm CO}_2$ gas is injected into the material being present in the mould 1 and moving downwards in zones I-III under the following Pressure:

Zone I: entry 6 bar 5 exit 3 bar Zone II: entry 2 bar 1 bar exit Zone III: 0.4 bar entry 0 bar 10 exit

The gas incidentally flowing down from zone III along the inner faces of the mould plates is emitted in the balancing zone IV; the amount of gas may be only at minimum.

The material passes through the mould space 5 continuously at a rate of 1.0 m/sec.

The gas pressure, path and time diagram in Fig. 8-where \underline{v} is the velocity of the material moving down in the mould, \underline{R}^O is the density of the afterhardening mixture, and \underline{d} is the thickness of the produced building panel - proves that the material passes through zone I - where the pressure of CO_2 gas is at the maximum (6 bar) - in about two minutes, whereas its passage through the zones II and III takes barely one minute, while the gas pressure gradually drops to zero, and the gas do not has any overpressure in zone IV. The curve in Fig. 8 represents the internal relaxation force proportional to the compressive force produced by the piston, in other words,

the intensity of the force required for compaction and passing on the material to be pressed is always proportional to the relaxation force affecting the sides of the mould.

The bending strength of the material leaving through the outlet port 7 of the mould 1 is about 35 kp/cm 2 (about 30 % of the final, 28-day-strength), and its density is 1250 kg/m 3 . The panel material continuously leaving the mould is cut according to the planned size with a cutting disc. The panels partly hardened by carbonation are stored standing on their edge.

Example 2

5

15

25

14 mm thick, 163 x 1250 x 4000 mm hollow building units are produced with the process according to the invention using the apparatus as shown in Fig. 1-3. Composition of the raw afterhardening mixture to be shaped by pressing and treated by carbonation is the following:

cement	58	mass%
waterglass	1	ir .
woodshavings	14	n
water	24	u
caustic lime	3	u u

Fig. 5 illustrates the trend of internal stress (pressure) \underline{P} and density \underline{R}_0 as a function of the time consequent upon compression of such mixture – not containing any elastic (organic) additive-component. (Similar curves are obtained if instead of woodshavings other

elastic, organic additive-components, e.g. cellulose, vegetable fibres, vegetable scrapings, synthetic fibres, etc., or a mixture containing their optional combination are used for preparation of the mixture.) In this case, the internal stress \underline{P} - upon reaching a maximum value and when the corresponding horizontal or essentially horizontal curve-section is longer than the corresponding part of curve \underline{P} in Fig. 4 - drops only at a slow rate, maintaining the compressive force over a longer time is required to keep the density R_0 on a constant value. When the compressive force is stopped (before hardening of the material) the internal stress existing in the mixture would result in a decrease of the density, because the material would spring back (relaxation effect).

If the raw mixture of above composition was pressed into the mould 1 with the reciprocating piston 8 of the apparatus shown in Figs. 1 and 2, the pressure conditions according to Fig. 7 develop in the mixture. The horizontal section of the internal stress-influence lines P corresponding to each piston stroke in this case, too will pass continuously into one another, i.e. always the same, maximum stress will prevail in the mixture in the vicinity of the inlet port 6 of the mould space 5 until the material is continuously stamped by the piston 8 into the mould 1. This way, due to the mechanical compaction, the quasi gastight condition is ensured during the process of production.

15

25

Pressure of the gas injected into and emerging

from the zones I-III is the same as the one shown in Example I and also the gas pressure, path and time diagram is similar to that of Fig. 8, however, the volume weight and strength of the end-product - consequent upon the difference appearing in the additive - are lower.

5

10

15

ໍເ 20

25

The main advantage of the invention is that it enables continuously the large-scale production of building units, the strength of which, when discharged from the mould, is at least 30% of the final (28-day) strength, thus, their production is extremely efficient and economical. A further advantage is the simplicity of the apparatus according to the invention, consequently its cost of investment is relatively low, and it is suitable for the production of units from a raw mixture containing either elastic (fibrous), or solid granular additive.

Naturally, the invention is not limited to described examples of the process and to the illustrated and explained embodiments of the apparatus, but it can be realized in many ways within the protective scope defined by the claims. The mould should not necessarily be of an upright position, the building units may be produced also in an inclined or even in a horizontal mould. can be realized according to several different from those described in the examples. The method of passing the gas through the material in motion is realizable in many ways different from the one described in the foregoing deviation from those described above is conceivable according to several other aspects, without overstepping the protective scope defined by the claims.

THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:

- A process for the preparation of bodies or building units from an afterhardening mixture containing cement and/or lime as binding material, as well as additives and water, in the course of which the still not hardened mixture is admitted into a mould, where carbonation reaction is brought about by the injection of CO2 gas into the mixture through a mould face and thereby the mixture is hardened, characterised by pressing the after hardening mixture continuously through a mould space in the mould which is open at both ends, while CO gas is injected into the mixture under pressure reducing from an inlet port of the mould towards an outlet port of the mould, and a quasi gas tight plug of mixture is formed by compaction of the mixture within the mould in the vicinity of the inlet port, and a quasi gas tight condition is brought about between this plug and the mould face, furthermore in the vicinity of the outlet port as much amount of CO, gas is injected into the mould as necessary for full completion or substantially full completion of the chemical reaction of carbonation.
- 2. Process according to claim 1, characterized by stamping-pressing the after hardening material into the mould space with a reciprocating device.
- 3. Process according to claim 1 or 2, characterised by injecting the ${\rm CO_2}$ gas into the mould space at least through one mould face under pressure exceeding the atmospheric



pressure, and when passed through the afterhardening material the gas of reduced pressure and amount is discharged from the mould space at least through another mould face, and/or vacuum is applied to at least one face of the mould space, and this way the CO_2 gas is made flow through the material, or its flow is intensified.

- 4. Process according to any of claims 1-3, characterised by injecting CO₂ gas at a pressure of between 3-6 bar into the pores of the mixture in a first zone (I) following the compacted layer of material in the vicinity of the inlet port, then looking in the direction of the material's movement in a second zone (II) where an instantaneous reaction of carbonation takes place CO₂ gas under a lower pressure of between 2-3 bar is injected, the amount of which is equivalent to the gas consumed by the reaction, thereby providing for the continuation of the carbonation reaction, then in a third zone (III) CO₂ gas under even lower pressure of 1-2 bar is injected into the mould space, whereby substantially full completion of the carbonation reaction is realised.
- 5. Process according to any of claims 1-4, characterised by creating a balancing zone (IV) in the mould space situated directly behind the outlet port of the material hardened by carbonation, where the gas outflow is checked, and the gas injection into the zones (I-III) behind the balancing zone (IV) is carried out as a function of the



outflowing amount and/or pressure of the gas.

- 6. Process according to any of claims 1-5, characterised by cutting to size the carbonation-hardened body leaving the mould space.
- 7. Process according to any of claims 1-6, characterised by injecting CO_2 gas into the mould space with a gas mixture, containing at least 30% of CO_2 gas.
- 8. Process according to any of claims 1-7, characterised by injecting ${\rm CO_2}$ gas into the raw mixture prior to feeding this latter into the mould.
- An apparatus for the continuous production of bodies or building units from an afterhardening mixture containing cement and/or lime as binding material, as well as additive and water, by its carbonation, said apparatus being provided with a mould having a mould space, a CO gas-source and holes in at least one wall of the mould, suitable for injection of CO, gas into said mould space, at a pressure exceeding atmospheric pressure, characterised by the mould having an inlet port for admitting the raw afterhardening mixture, and an outlet port for discharging the mixture hardened by carbonation, a plurality of separate zones disposed between said inlet port and said outlet port; a press mechanism situated in front of said inlet port for pressing the raw afterhardening mixture into the mould space and for forming a quasi gas tight plug of mixture within the mould in the vicinity of the inlet port, said press mechanism



also adapted to press the raw afterhardening mixture into the mould space and moving said afterhardening mixture as well as said mixture hardened by carbonation through said mould space; the holes leading into the mould space serving for inlet of the CO_2 gas being divided into separate hole groups which communicate with gas injection devices suitable for ejecting CO_2 gas, at pressures to be separately controlled for each said zone.

- 10. Apparatus according to claim 9, characterised by discharge holes provided in at least one wall of the mould, for emitting the CO_2 gas remaining in a given case after the completed carbonation reaction, said discharge holes expediently communicating with pipes connecting the CO_2 gas-source, with the mould containing the holes for injecting CO_2 gas into the mould space.
- 11. Apparatus according to claim 10, characterised by having a forward pipe for injecting CO_2 gas into the mould space, and a return pipe for recirculating into the forward pipe the CO_2 gas remaining in a given case after the completed carbonation reaction; a gas pump being connected to the forward pipe into which also the return pipe is leading, and in up-stream direction of the gas flow before the pump a pipe leading out of the CO_2 gas-source, and fitted with a shut-off means being joint to the return pipe; and the forward pipe being interconnected through leg pipes containing valves with separate hole groups on the gas-



injection side, while leg pipes fitted also with valves and leading from the hole groups into the return pipe are provided for discharging the gas remaining - in a given case - after the completed carbonation reaction.

- 12. Apparatus according to claim 11, characterised by a vacuum pump being inserted into the return pipe.
- 13. Apparatus according to claim 11 or 12, characterised in that the hole groups on both the gas inlet side and the remaining-gas outlet side are leading into separate closed chambers fitted expediently gastight to the outer face of the mould plates.
- 14. Apparatus according to any of claims 11-13, characterised in that the hole groups are leading from ducts running inside the mould plates into the mould space, each duct communicating with one of the leg pipes leading out of the forward pipe, and with one of the leg pipes leading into the return pipe, respectively.
- 15. Apparatus according to any of claims 9-14, characterised by means being provided behind the outlet port of the mould for cutting up the carbonation-hardened body leaving the mould space.
- 16. Apparatus according to any of claims 9-15, characterised in that chambers covering at least one of the hole groups are fitted to the outer side of the mould plates in the vicinity behind the outlet port of the mould.
- 17. Apparatus according to any of claims 9-16,



characterised by the press mechanism containing a reciprocating beater, the cross sectional shape and size of which is the same or essentially the same as those of the inlet port's of the mould.

- 18. Apparatus according to claim 17, characterised in that the mould is of vertical arrangement the reciprocating beater is fitted between guide rails, the guide rails are covered with a bell-shaped protective cover, the lower flange of which runs in the vicinity of the lower edge of the guide rails; and an opening is provided for between said lower flange and the guide rails; and the actuating mechanism together with the protective cover is situated in a hopper for feeding the raw afterhardening mixture into the mould, said hopper leading to the upper end of the mould space.
- 19. A process for the production of articles from a composition containing cement and/or lime substantially as hereinbefore described.
- 20. An apparatus for the production of articles from a composition containing cement and/or lime substantially as hereinbefore described with reference to the accompanying drawings.

DATED this twenty-sixth day of July

1990.

FAKOMBINAT SZOMBATHELY

By Their Patent Attorneys
CULLEN & CO



Fig. 1

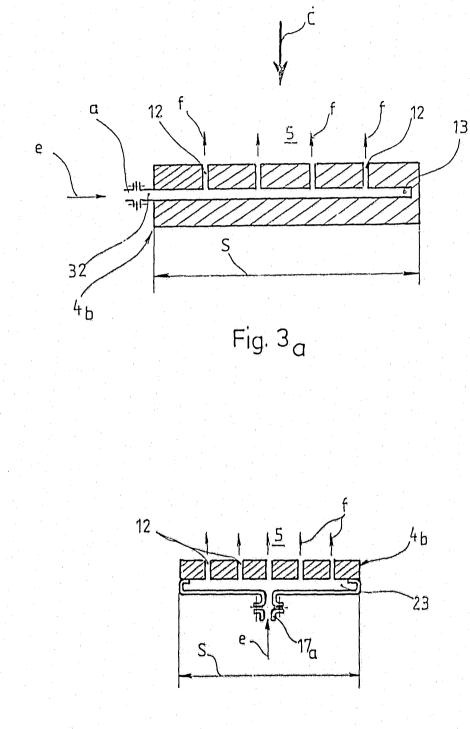


Fig 2

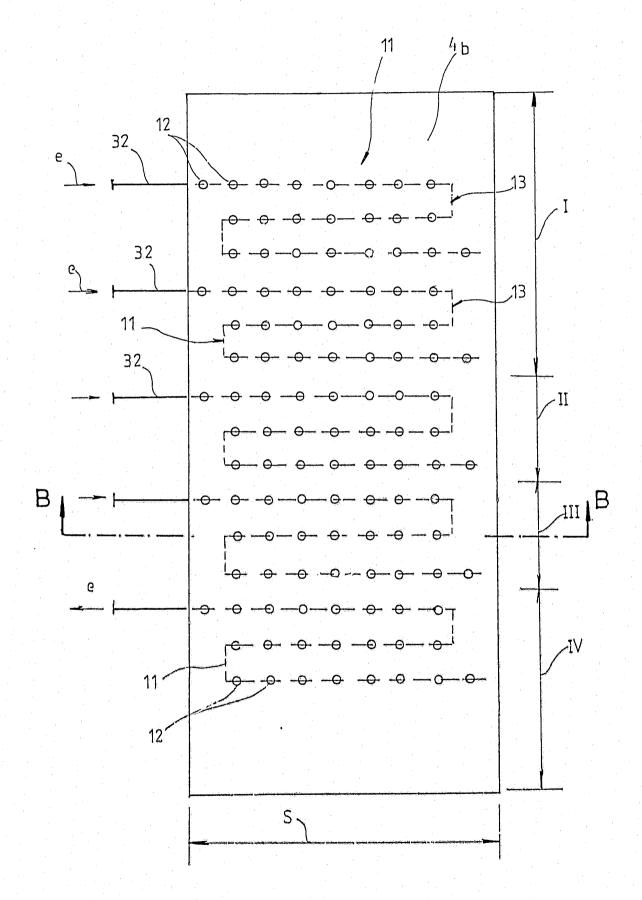
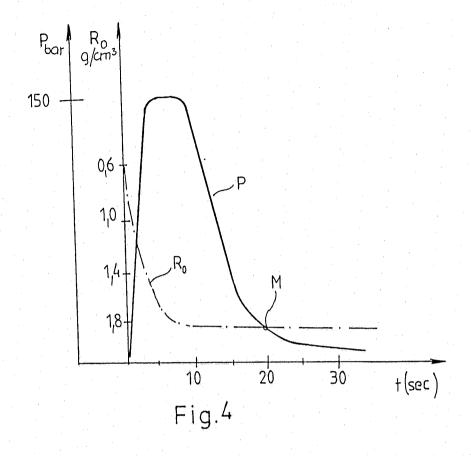


Fig. 3/b



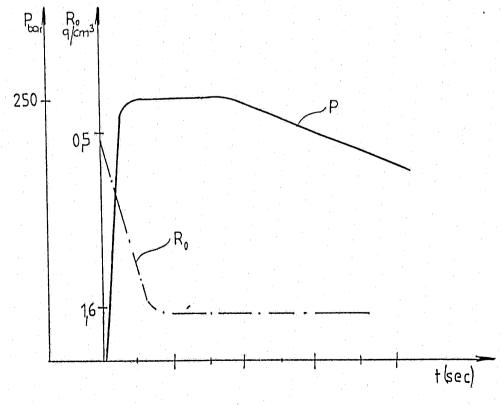


Fig. 5

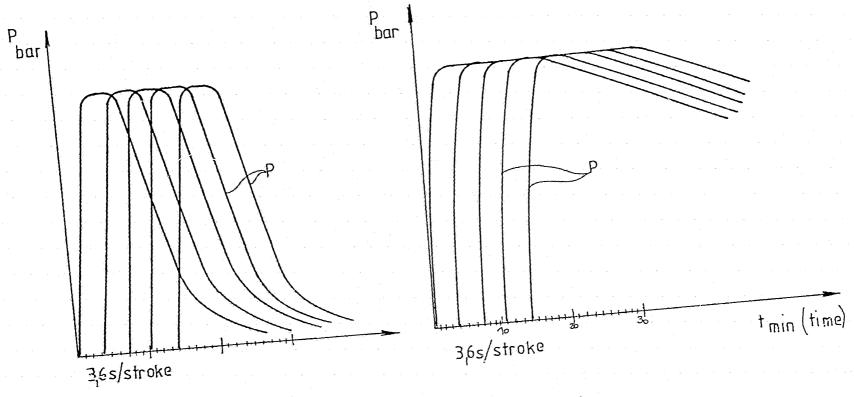
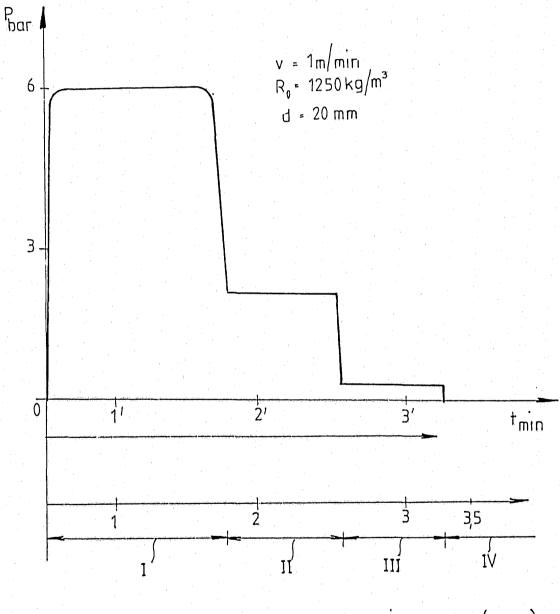


Fig. 6

Fig.7



length of pressing section (zones)

Fig.8

