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(57) Abstract: The present invention relates to the use of atomic layer deposition (ALD) techniques to enhance the acid catalytic activity of nanoporous materials.



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ENHANCING CATALYTIC ACTIVITY OF NANOPOROUS MATERIALS

FIELD OF THE INVENTION

- 5 The present invention relates to the use of atomic layer deposition (ALD) techniques to enhance the catalytic activity of nanoporous materials.

BACKGROUND OF THE INVENTION

10 Overview of nanoporous materials

There exists a wealth of inorganic nanoporous materials. Nanoporous materials can be unordered, such as pillared clays and silica gels, or ordered. The ordered porous materials comprise zeolites and zeolite like materials, ordered mesoporous materials and hierarchical materials presenting more than one level of porosity and structural order. Among the ordered nanoporous materials, ordered microporous and mesoporous materials attract a lot of attention by the materials science community (ref.1). Ordered microporous and mesoporous materials can be described in terms of a host structure, which defines a pore structure, which may contain guest species. The voids between the linked atoms have a free volume larger than a sphere with a 0.25 nm diameter. Pores with free diameters of less than 2 nm are called micropores, and those in the range of 2 to 50 nm mesopores (ref.2).

When the atoms of the host as well as the voids are arranged periodically with long-range order (at least 10 repeats in all directions) the materials produce sharp maxima in a diffraction experiment. These materials are crystalline. Zeolites and zeolite like materials are such crystalline materials based on a 3-dimensional 4 connected inorganic frameworks. Generally they contain silicon, aluminum and oxygen in their framework and exchangeable cations, water and/or other guest molecules within their pores. The framework structure may contain linked cages, cavities or channels, which are of the right size to allow small molecules to enter. The limiting pore sizes are roughly between 0.3 and 1 nm in diameter. Because of their unique porous properties, zeolites are used in a variety of applications with a global market of several million tons per annum. Major

zeolite uses are in catalytic petrochemical processes such as cracking, hydrocracking, alkylation, isomerization, in cation-exchange (water softening and water purification), and in molecular separations and purification of gases and solvents.

Another class of nanoporous materials displays short range order only. They are amorphous with respect to diffraction experiments. When such materials are ordered, the pores are of uniform size with long-range order and produce diffraction maxima at d-values reflecting the pore-to-pore distance. In such ordered mesoporous materials, the pore structure is "crystalline". Examples include MCM-41 (ref.3), MCM-48 (ref.4), SBA-15 (ref.5), FSM-16 (ref.6), TUD-1 (ref.7).

Next to crystalline microporous materials and ordered mesoporous materials both having only one type of pores, poly-porous materials exist. A distinction can be made according to the ordering of the different types of porosity. Mesoporous zeolites having a secondary porosity composed of irregular mesopores in addition to the micropores are e.g. applied as Fluid Catalytic Cracking catalysts. The ultrastable Y zeolite as a result of dealumination and partial structure degradation presents intracrystalline mesopores in addition to micropores (ref.8). The presence of mesopores is important in catalytic applications. These larger pores facilitate the diffusion of larger molecules into the interior of the zeolite crystals.

Mesoporous zeolites can be obtained using the replica technique, whereby the zeolite is grown within the pores of various kinds of carbon template (ref.9-11). Another approach for building poly-porous materials involves the linking of microporous building units into materials that are ordered at the mesoscale. Zeolites are examples of such hierarchical materials (ref.12 and 13). Zeolites are robust materials capable of withstanding higher temperatures and combine the advantages of both micro and mesoporous materials (ref.12 and 13).

Functionalization of nanoporous materials

For application in catalysis, nanoporous materials need to be functionalized. In silicate frameworks, the introduction of trivalent elements such as aluminum, gallium or iron (but not limited to these elements) generates positive charge deficiencies in the oxide framework that needs to be compensated by cations in the pores. Charge compensation with a proton generates Brönsted acidity in the material.

The conversion of an as-synthesized zeolite into a Brönsted acid zeolite can be obtained via different routes. When the lattice charge is compensated by organic cations, calcination to remove the organic molecules converts the as-synthesized zeolite into an acid zeolite. Alkali and alkaline earth metal cation can be replaced with protons through cation exchange with an ammonium salt and deammoniation via heating, or else through contacting of the zeolite with diluted acid. Cation exchange with multivalent cations such as La^{3+} followed by calcination is another method known in the art to generate Brönsted acid sites in a zeolite.

Nanoporous materials often have insufficient Brönsted acidity for a desired catalytic application. Many kinds of modifications have been reported to enhance the Brönsted acidity and the catalytic activity. Other modifications aim at altering the porosity and surface chemistry.

Post synthesis modifications of zeolites include a lot of techniques to further control the acidity or the shape selectivity of a specific zeolite structure. There are three main types of post synthesis modification which can be applied to a zeolite (ref.14): (i) structural modification in which the framework $\text{SiO}_2/\text{M}_2\text{O}_3$ molar ratio (where $\text{M} = \text{Al}$ or another trivalent metal cation) is altered resulting in a change in acidity; (ii) modification of the surface of the zeolite crystal to adapt the size of the pore opening; (iii) internal pore modification which block or alter the acid sites or restrict the internal pore diameter.

If the material is meant for catalytic application then it has to maintain a sufficient structural integrity.

There are several ways to decrease the aluminum content of a zeolite, e.g. by steaming, acid leaching or contacting the zeolite with an aluminum complexing agent such as ethylene diamine tetra acetate.

For enhancing the content of trivalent elements such as Al^{3+} there are several options. The incorporation of trivalent elements directly during the crystallization of the zeolite is sometimes difficult. In the so-called high silica zeolites, the acid catalytic activity is limited because of the small percentage of aluminum incorporated in the zeolite framework during crystallization. Imparting greater activity for those zeolites can be achieved by inserting aluminum atoms into the framework in a post-synthesis operation. Several methods have been used to incorporate trivalent elements such as aluminum or gallium into high silica zeolites (ref.14). A first method is the hydrothermal treatment of

the zeolite material with aqueous aluminate solution. The zeolite to be aluminated is then treated with an aqueous solution of aluminate salt under hydrothermal conditions. The aluminate reacts with the silanol groups of a hydroxyl defect site inside the zeolite channels. Sometimes an aluminum atom is inserted into a tetrahedral vacancy where it substitutes for a framework silicon atom. For example, ZSM 5 zeolite with enhanced n-hexane cracking activity can be obtained by treating essentially inactive high silica ZSM 5 zeolite with sodium aluminate solution in an autoclave (ref 15).

Treatment with Aluminum halide vapors is another proven method for aluminum incorporation into zeolites. It has been confirmed by ^{27}Al magic angle spinning NMR and IR spectroscopy that when highly siliceous zeolite such as Silicalite is treated with AlCl_3 vapor at elevated temperature (500-600°C), aluminum atoms take the position of silicons in the zeolite framework. Through such modification, a considerable amount of aluminum is also incorporated in the pores outside of the framework, where it adopts an octahedral coordination (ref.16). The aluminum insertion can be obtained by reaction of silanol groups with AlCl_3 or by the substitution reaction of silicon atoms of the framework by aluminum atoms provided as AlCl_3 reagent. Strong acid sites including both Brönsted and Lewis acid sites were generated together with the acid sites of normal strength observed for ordinary ZSM-5 zeolite. (ref.17)

AlO_x coating of the pores of ultrastable zeolite Y (USY) has proposed as a possible method for vanadium passivation of Fluid Catalytic Cracking catalysts. Two coating methods were presented: (i) the deposition of the $[\text{Al}_{13}\text{O}_4(\text{OH})_{24}(\text{H}_2\text{O})_{12}]^{7+}$ ($[\text{Al}_{13}]$) complex from aqueous solutions and (ii) the anchoring of alumoxane by in situ triisobutylaluminum hydrolysis followed by calcination. (ref.18)

Various ways for post synthesis incorporation of aluminum in ordered mesoporous materials have been reported. Post synthesis alumination of siliceous ordered mesoporous materials in principle offers advantages over the direct incorporation during synthesis. Aluminum often interferes with the ordering process during the formation process of the ordered mesoporous material. The accessibility to active aluminum sites incorporated during synthesis may be limited owing to pore blockage. In post synthesis alumination, the challenge is to obtain a well dispersed and uniform distribution of aluminum over all mesopores of the material. Aluminum reagents when contacted with

the ordered mesoporous silica tend to react and be deposited in the pore openings. The presence of long, monodimensional mesopores hinders the spreading of the aluminum over the internal body of the material. Techniques which can uniformly disperse aluminum into the mesopores are of great interest (ref.19).

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In the literature, the preparation of aluminum-containing mesoporous MCM-41 materials was obtained by post-synthesis modification of a purely siliceous MCM-41 using different Al sources: AlCl_3 , aluminum isopropoxide and NaAlO_2 . The structure, thermal stability and acidity of these materials have been investigated and compared with Al-MCM-41 prepared by direct hydrothermal synthesis. Irrespective of the preparation method, the surface area, pore diameter, crystallinity and thermal stability of Al-MCM-41 decreased with increasing Al content. Post-synthesis modified materials possessed better thermal stability, and this method allows for the incorporation of more aluminum without disintegration of the mesoporous structure as compared to Al-MCM-41 prepared by direct hydrothermal synthesis. The post-synthesized Al-MCM-41 had a moderate acidity, comparable to that of the direct hydrothermally-synthesized material. (ref.20)

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The alumination of siliceous MCM-48 containing organic templates with sodium aluminate solution has been reported (ref.21) The modification altered the porosity quite significantly.

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Aluminium chlorohydrate solution which contains Al polycations was reported to be an efficient source of Aluminum for post-synthesis alumination of purely siliceous MCM-41. The material retained excellent structural integrity and showed enhanced acidity and catalytic activity. The amount of Al incorporated into the MCM-41 framework was dependent on the concentration of Al in the grafting solution; ^{27}Al MAS NMR confirmed that a large proportion of the Al atoms was inserted into tetrahedral positions within the framework. TEM and XPS indicated that there were no separate surface alumina phases. The pore wall thickness increased with Al content, but pore size uniformity was maintained. Alumination generated Brønsted acid sites which increase in population as the Al content rose. Those materials exhibited considerable catalytic activity for cumene cracking and were superior to AlCl_3 -grafted MCM-41 or aluminum chlorohydrate grafted amorphous silica. (ref.22)

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O'Neil et al. investigated the use of supercritical solvents for post synthesis alumination of ordered mesoporous silica. O'Neil et al. prepared aluminum grafted MCM-41 material by reacting pure silica MCM-41 with aluminum isopropoxide in supercritical CO_2 or

propane. The supercritical fluid was shown to provide efficient transport of the aluminating agent into the mesoporous material. (ref.19)

In another investigation, dry MCM-41 sample was dispersed in dry toluene containing various amounts of trimethylaluminum (TMA). The resulting mixture was maintained at room temperature for 48 h without stirring. Aluminum was found to be inserted into tetrahedral positions within the framework at room temperature. No further calcination was required. It was decided that TMA is an efficient aluminum source for the post-synthesis alumination. (ref.23)

This literature overview teaches that alumination of mesoporous silicate-based materials can be achieved. The methods currently applied require the use of an aqueous medium, or of organic or supercritical solvents. The use of gaseous reagents such as AlCl_3 appeared to be less successful.

Atomic layer deposition (ALD) technique

Atomic layer deposition (ALD) is a process for depositing highly uniform and conformal thin films by alternating exposures of a surface to vapors of two chemical reactants (ref.24). Atomic Layer Deposition (ALD) is used to deposit thin films with special features. The technology was originally developed for the fabrication of polycrystalline luminescent ZnS:Mn and amorphous Al_2O_3 insulator films for electroluminescent flat panel displays. Even though the ALD technology showed some benefits, the deposition rate was too low to make it economical at that time. Due to its complex surface chemistry, no real break-through involving ALD was achieved until 1985.

The decreasing device dimensions and increasing aspect ratios in the micro-electronics industry increased interest towards the ALD technique during the 1990s. ALD processes are attractive for a variety of applications in micro-electronics: deposition of diffusion barriers, dielectric films and electrodes for DRAM capacitors and thin dielectric films for gate stack applications. ALD has been used to deposit various materials, including several oxides, nitrides and pure metals. Since this is a layer-by-layer deposition technique it produces films of uniform thickness and excellent conformality.

Different from chemical vapor deposition (CVD), ALD technology is based on saturated surface reactions. The principle of ALD is based on sequential pulsing of chemical precursor vapors, which form about one atomic layer each pulse. This generates pinhole free coatings that are extremely uniform in thickness, even deep inside pores, trenches and cavities. (ref.25)

The intrinsic surface control mechanism of the ALD process is based on the saturation of sequentially performed surface reaction between the substrate and precursor. The saturation mechanism makes the material growth rate directly proportional to the numbers of reaction cycles instead of the reactant concentration or time of growth.

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The advantages of atomic layer deposition technique can be enumerated as follows:

1. Digital thickness control to atomic level (no rate monitor needed, just set the number of atomic layers).
2. Perfect 3D conformality, 100% step coverage: uniform coatings on flat, inside porous and around particle samples.
3. Large area thickness uniformity.
4. Potential for batch scalability (precursor sources are small and stacking of substrates is possible).
5. Pinhole free films, even over very large areas.
6. Excellent repeatability (wide process windows: many ALD processes are not very sensitive to temperature or precursor dose variations).
7. Low defect density.
8. Excellent adhesion due to chemical bonds at the first layer.
9. Digital control of sandwiches, heterostructures, nanolaminates, mixed oxides, graded index layers and doping.
10. Gentle deposition process for sensitive substrates (although a plasma may be used to enhance the deposition rate for certain processes, thermal ALD is often sufficient).
11. Low temperature deposition possible (RT-400C).
12. Atomically flat and smooth coating, copies shape of substrate perfectly.
13. Low stress because of molecular self assembly.
14. 100% film density guarantees ideal material properties (n, Ebd, k, etc).
15. Insensitive to dust (grows underneath dust!).
16. The deposition of thin films of a variety of materials has been reported (oxides, nitrides, metals and semiconductors).
17. The deposited film can be either amorphous or crystalline depending on the substrate and the deposition temperature.
18. Coatings have been reported on a variety of substrates (glass, plastics, Si, metals etc).
19. High production yields due to all these process benefits.

There are two fundamental self-limiting mechanisms in ALD: chemisorption saturation process followed by exchange reaction (CS-ALD) and sequential surface chemical reaction (RS-ALD).

5 The treatment of materials by ALD typically proceeds as follows.

First the material needs to be pretreated to bring the surface in a reactive state. This is typically carried out by heat treatment, although the use of a plasma may also be beneficial. Physisorbed molecules, most often water adsorbed from ambient air, are removed.

10 Step 1: Saturating reaction of a gaseous reactant (reactant 1, typically a metal compound) with the reactive sites on the support surface. The reaction is allowed to proceed until the surface is saturated with the adsorbing species and no more reaction takes place. Thereafter, excess reactant and possible gaseous reaction products are removed by an inert gas purge or by evacuation.

15 Step 2: Saturating reaction of another reactant (reactant 2, typically a non-metal compound) with the reactive sites on the support. The adsorbed species left behind by the first reactant form a major part of the reactive sites. Excess reactant and the gaseous reaction products are removed. The steps are schematically presented in the following Figure 1 (ref.26).

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The atomic layer deposition technique has been applied in the area of catalyst preparation. Atomic layer deposition was used to prepare aluminum nitride on porous silica and alumina supports and to deposit catalytically active components on the obtained AlN/oxide supports. There are reports on aluminum nitride grown on porous
25 silica by atomic layer deposition from trimethylaluminum and ammonia precursors. The ALD growth is based on altering, separated saturating reactions of the gaseous precursors with the solid substrate. The growth and the surface reactions were investigated by elemental analysis and solid state NMR measurements for ^{27}Al and ^{29}Si (ref.26-27).

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Active transition metal catalysts have been produced by ALD for a variety of purposes. They are listed in Table 1 (ref.26).

Table 1. Examples of reactions for which catalysts have been prepared by ALD and description of the catalyst (ref.26)

Reaction	Catalyst	Support	Reactants
Alkane dehydrogenation	CrO _x	Alumina	Cr(acac) ₃ , ^a air
	VO _x	Silica, alumina	VO(acac) ₂ , air
Ethene hydroformylation	Co	Silica	Co(acac) ₃ , air
Toluene hydrogenation	Ni	Alumina	Ni(acac) ₂ , air
	Co	Silica	Co(acac) ₃ , air ^b
	Co	Alumina	Co(acac) ₂ , air ^b
Alkene metathesis	WO _x	Silica, alumina, magnesia	WOCl ₄ or WCl ₆ , air
Methane oxidation	CoO _x	Zirconia	Co(acac) ₃ , air ^b
Methanol oxidation	TaO _x	Silica, alumina, zirconia	Ta(OC ₂ H ₅) ₅ , air
	VO _x	Silica, alumina, zirconia	VO(acac) ₂ , air
Alkene polymerisation	CrO _x	Silica	Cr(acac) ₃ , air
	CrO _x	Silica	CrO ₂ Cl ₂
Alcohol dehydration	ZrO ₂	Alumina	ZrCl ₄ , H ₂ O

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ALD is reported to be used for the modification of zeolite or molecular sieve membranes to decrease the effective pore size for molecular separation purposes. (ref.28, ref.40)

Uniform nanostructured catalytic membranes had been fabricated by a combination of anodic aluminium oxidation and atomic layer deposition. The ALD method makes it possible to control pore diameters on the angstrom scale. (ref.29)

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Spatially controlled atomic layer deposition of ZnO, TiO₂, V₂O₅ and Nb₂O₅ in anodized aluminum membranes have been reported (ref.30). Conformal coating of metals over nanoporous AAO and SiO₂ aerogels which can have applications in catalysis and gas sensors is known in the art. (ref.31)

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A plasma-assisted ALD process has been developed in which the ALD precursors are chosen to be nonreactive unless triggered by plasma, so that ALD can be spatially defined by the supply of plasma irradiation. Since plasma cannot penetrate within the internal porosity of mesoporous silica, ALD has been successfully confined to the immediate surface. This technique is useful for sealing of porous low dielectric constant films with a conformal layer and for progressive reduction of the pore size of mesoporous membranes. (ref.32)

Several studies reported that ALD mediated grafting of vanadium and other elements, such as molybdenum and tungsten, on mesoporous silica by keeping the system in rigorous dry and unhydrated conditions resulted in superior catalytic performance in redox reactions (ref. 37-38).

Mahurin et al. (ref.39) described the atomic layer deposition of TiO_2 on mesoporous silica by ALD using TiCl_4 and water reactants as a means to functionalize the mesoporous material. However, this will not significantly improve the activity of the mesoporous material in reactions demanding acid catalytic sites.

SUMMARY OF THE INVENTION

The present invention relates to methods for increasing the catalytic activity of a silicate-based nanoporous material comprising the use of atomic layer deposition to incorporate a chemical element in said material, wherein said element is provided for ALD in a gaseous compound comprising said element. ALD under conditions favoring the hydrolysis of a compound comprising said chemical element was found to be an advantageous method for introducing aluminum into silicate-based nanoporous materials and enhancing the catalytic activity of said material. The method is particularly suited for introducing aluminum into ordered mesoporous materials, hierarchical materials and mesoporous zeolites. The incorporation of aluminum in four-, five- and sixfold coordination detected via ^{27}Al MAS NMR enhances the acidity of the modified materials. The method is practical for enhancing the catalytic activity of nanoporous materials in which the incorporation of aluminum through direct synthesis is difficult to achieve. Using the new method, zeolites that became deactivated during operation because of dealumination can be reactivated in a convenient way. The external surface of nanozeolites can be aluminated selectively.

DETAILED DESCRIPTION OF THE INVENTION

Legends to the figures

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Fig.1. Schematic illustration of the steps leading to growth of MZx materials (M denotes metal, Z non-metal) by ALD.

Fig.2. Schematic diagram of ALD reactor.

Fig.3. Decane conversion as a function of temperature over CBV-712 (●) and TMA 30 Cycles – 120s (▲).

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Fig.4. Yield as a function of decane conversion over parent CBV-712 (iso:●; crack: ○) ALD modified CBV-712 30 cycles – 120 s (iso: ▲; crack:Δ).

Fig.5. ^{27}Al MAS NMR spectra of ultrastable Y zeolite subjected to different alumination treatments using the ALD treatment of example 3.

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Fig.6. ^{27}Al MAS NMR spectra of aluminated (a) Zeotile-4 sample and (b) Silicalite-1 nanozeolite.

Fig.7. Nitrogen adsorption isotherms on parent ultrastable Y zeolite and aluminated specimens.

Fig.8. Evolution of the micropore volume with relative aluminum content introduced via ALD.

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Fig.9. Dependence of mesopore and external surface area with relative aluminum content of ultrastable Y zeolite.

Fig.10. Adsorption – Desorption Isotherms for the aluminated Zeotile-4(Al-ZT-4) and Silicalite-1(Al-S-1).

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Fig.11. Decane conversion as a function of temperature over Pt/Al-Zeotile-4 (■).

Fig.12. Yield of skeletal isomers and cracked products as a function of decane conversion over Pt/Al-Zeotile-4 (iso:■; crack:□).

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Description

In the context of the present invention the term "silicate based nanoporous material" refers to porous material with a matrix based on silicon oxide with pore diameter less than 100 nm. Ordered microporous and mesoporous materials can be described in terms of a host structure, which defines a pore structure, which may contain guest species. The voids between the linked atoms have a free volume larger than a sphere with a 0.25 nm diameter. Pores with free diameters of less than 2 nm are called micropores, and those in the range of 2 to 50 nm mesopores (ref.2). For pore shapes deviating from the cylinder, the above ranges of diameter of micropores and mesopores refer to equivalent cylindrical pores.

In the context of the present invention the term 'zeolite' refers to a crystalline microporous material comprising coordination polyhedra formed only of silicon, aluminum and oxygen. Non-aluminosilicate analogs of microporous crystals such as pure silicates, titanosilicates, silicoaluminophosphates and borosilicates, ferrosilicates, germanosilicates and gallosilicates, that exhibit the characteristic molecular-sieving properties similarly to zeolites, are referred to as zeolite-like' materials. In the present invention both zeolites and zeolite-like materials are encompassed by the term 'zeolite'. A publication entitled "Atlas of Zeolite Structure Types", 5th Revised Edition (2001) by authors W. M. Meier, D. H. Olson and Ch. Baerlocher, is a good source of the known zeolites and zeolite-like materials. More particularly the term "zeolite" refers to zeolites and zeolite-like material having a zeolite framework of the type AEI, AEL, AFI, AFO, AFR, AFX, ATN, ATO, BEA, CDO, CFI, CHA, CON, DDR, DON, EMT, EON, EUO, FAU, FER, IFR, IHW, ISV, ITE, ITH, ITW, IWR, IWV, IWW, LEV, LTA, LTL, MAZ, MEI, MEL, MER, MFI, MFS, MOR, MOZ, MSE, MSO, MTF, MTN, MTT, MTW, MWW, NON, RRO, RTE, RTH, RWR, SFE, SFF, SFG, SFH, SFN, SGT, SSY, STF, STT, TON or TUN (<http://izasc.ethz.ch/fmi/xsl/IZA-SC/ft.xsl>). In the context of the present invention the term nanozeolites refer to nanosized zeolites with particle size of less than 300nm, preferably less than 200 nm. The term "hierarchical material" as used in the present invention means a material having a double porosity on the scale of each of its particles: mesoporosity [i.e. a porosity organized on the mesopore scale], and a zeolitic type microporosity.

It was found that incorporating aluminum in various silicate based nanoporous materials using an atomic layer deposition process resulted in an unexpected spectacular gain in catalytic activity. Without being bound by theory, this surprising gain in catalytic activity can at least in part be explained by a reinforcement of the acid strength by introducing tetrahedral, distorted tetrahedral, pentacoordinated and octahedrally coordinated aluminum into said nanoporous material.

The present invention provides a method for increasing the acidic catalytic activity of a silicate-based nanoporous material, said method comprising the incorporation of a chemical element in said material using an atomic layer deposition (ALD) process under conditions favoring the hydrolysis of a compound comprising said chemical element, most preferably using water as one of the reactants of said ALD process.

Said atomic layer deposition process may be a thermal ALD or a plasma-enhanced ALD, comprising:

(i) a first saturating reaction of a gaseous reactant, preferably a metal compound coordinated with ligand groups, with the reactive sites (hydroxyl groups) of said silica based nanoporous material to form molecular bonded structures on said nanoporous material that comprise the metal atoms coordinated with the ligand group or with a modified ligand group that results from the reaction and bonded to oxygen atoms that are bonded to said nanoporous substrate atoms (e.g., silicon atoms),

(ii) removal of the excess reactant and possible gaseous reaction products by inert gas purge or by evacuation,

(iii) a second saturating reaction of another gaseous reactant, preferably water, with the reactive sites on the support, with the adsorbed metal left behind by the first reactant forming a major part of said reactive sites. This reaction comprises the hydrolysis of the bonds between the metal atom and the ligand or modified ligand group.

(iv) removal of the excess reactant and gaseous reaction products,

In a preferred embodiment of the present invention, the nanoporous material is selected out of the group consisting of mesoporous zeolites, nanozeolites, ordered mesoporous materials and hierarchical materials.

In a preferred embodiment the element which is incorporated is a trivalent element, such as Aluminum, Gallium, Boron or Iron, most preferably Aluminum. In a particular embodiment of the present invention Aluminum is incorporated in said silicate-based materials using ALD cycles with trimethylaluminum and water reactants.

5 A particular embodiment of the present invention relates to the use of an ALD process with trimethylaluminum and water reactants for reactivating silicate-based nanoporous materials, most preferably zeolites, that became deactivated during operation because of dealumination.

10 Another aspect of the present invention relates to the use of a silicate-based nanoporous material with enhanced acidic catalytic activity obtained by said method for the hydroconversion of hydrocarbons.

A third aspect of the present invention relates to the use of said method with aluminum and water reactants for selectively aluminating the external surface of nanozeolites.

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It is recognized that ALD reaction conditions (such as number of ALD cycles, ALD cycle time, ALD temperature) may be varied in the various embodiments of the invention, as known by a person skilled in the art. The choice of said reaction conditions will depend in part upon the desired porosity and catalytic activity of the treated material.

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EXAMPLES

EXAMPLE 1. Preparation of Silicalite-1 (nanozeolite)

25 37.32g TEOS (Acros, 98 %) was hydrolyzed in 32.13g aqueous TPAOH solution (Alfa, 40 wt %) under stirring. Initially, a separated layer of TEOS was formed on top of the TPAOH solution. Upon vigorous stirring, the mixture turned into an emulsion and, as the TEOS was hydrolyzed, gradually transformed into a clear sol. Then 30.55 g of water was added and the stirring continued for another 24 hours. The clear precursor sol (CS)
30 was then refluxed at 95°C for three days. The products were cooled to room temperature. The colloidal particles produced were then separated from the mother liquor by centrifugation (15 000 rpm, 15 min). The supernatant liquid was removed and

the zeolite product redispersed in water. The powder was washed until the pH of the supernatant was lower than pH 9. The dried powder material was calcined at 550°C. The particle size of such silicalite material typically is below 200 nm (ref.33).

5 **EXAMPLE 2. Synthesis of Zeolite-4**

A clear solution (CS) was prepared by mixing 37.32g TEOS (Acros, 98 %) and 32.13g aqueous TPAOH solution (Alfa, 40 wt %) under stirring. The mixture upon stirring turned into an emulsion and, as the TEOS was hydrolyzed, gradually transformed into a clear sol. To this 30.55 g of water was added and stirring continued for another 24 hours. Next, 10 g of pluronic 123 triblock copolymer from BASF (EO₂₀PO₇₀EO₂₀) was dissolved in 90 g water under stirring. An amount of 24 g of this template solution was combined with 8 g of 5 M HCl solution. 18 g of clear solution (CS) was combined with another 9g 5 M HCl under vigorous stirring. Subsequently, it is combined with the acidic triblock copolymer solution. Then the mixture was heated at 90 °C under quiescent conditions for 96 h. A solid product was formed and separated from the liquid by centrifugation at 12 000 rpm. The product was washed with water until the pH exceeded the value of 3. The sample was dried at 60 °C for 24 h and finally calcined at 350°C for 24 h with a heating rate of 0.5 °C min⁻¹ under air atmosphere. The XRD pattern confirmed the successful synthesis of Zeolite-4 like in reference 13.

EXAMPLE 3. Alumination of ultrastable Y zeolite (mesoporous zeolite) using ALD

The ultrastable Y zeolite was a commercial powder sample with code name CBV-712 from PQ Corporation.

The ALD reactor was a home-built pump-type reactor (see figure 2). The stainless steel walls of the reactor can be either watercooled, or intentionally heated up to 200°C. The ALD chamber is continuously pumped by a turbomolecular pump. The flow gases are controlled by needle valves and computer controlled pneumatic valves. The reaction gases are either directly injected into the chamber (thermal ALD), or can flow through an ICP-RF plasma source (plasma-enhanced ALD). For the present experiments, TMA and water were used as reagents, and no plasma was used. Since

the vapor pressure of TMA is sufficiently high, no Ar flow was required through the precursor bottle. During deposition, the chamber walls were heated to 80°C.

The ultrastable Y zeolite powder (350mg) was introduced in an Al vessel, which was placed on top of a resistive heater. The zeolite contained ca. 20% water. During a first series of experiments, the powder was loaded overnight in the ALD reactor at a temperature of 100°C, resulting in a base pressure of $1 \cdot 10^{-7}$ mbar. Alternatively, water desorption could be achieved by heating the powder in a tube furnace for 3 hours at 150°C. After loading the powder in the ALD chamber, a base pressure of $2 \cdot 10^{-6}$ mbar could be achieved.

An amount of ca.300 mg of zeolite powder was subjected to ALD cycles at 200°C. Two different types of cycles were used.

(1) Cycles of 480s, comprising 120 s of exposure to TMA, 120 s evacuation, 120 s exposure to H₂O pulse and 120 s evacuation: different samples were subjected to 5 (Z5), 10(Z3) and 30(Z1) cycles.

(2) Cycles of 120s, comprising 30 s of exposure to TMA, 30 s evacuation, 30 s exposure to H₂O and 30 s evacuation. Zeolite samples were exposed to 10 (Z4) and 30 (Z2) cycles.

EXAMPLE 4. Alumination of silicalite-1 (nanozeolite material) using ALD

The ALD experiment was similar to that performed on the ultrastable Y zeolite in example 3. For this powder, no water desorption step was required. Aluminum deposition on silicalite-1 powder sample from example 1 was done at 200°C in 10 cycles. A cycle comprised 30s TMA exposure, 30s evacuation, 30s H₂O exposure and 30s evacuation.

EXAMPLE 5. Alumination of Zeotile-4 (hierarchical material) using ALD

The ALD treatment was performed on the Zeotile-4 sample from example 2. The zeotile sample was initially heated to 200°C for 2 h in vacuum to desorb the water. The base pressure after 2 h was $2 \cdot 10^{-6}$ mbar. ALD deposition was also performed at 200°C.

The treatment consisted of 10 cycles, each comprising 30s exposure to TMA, 30s evacuation, 30s H₂O exposure and 30s evacuation.

5 **EXAMPLE 6. Decane hydroconversion over aluminated ultrastable Y zeolite**

The catalytic activity of the aluminated zeolites was evaluated using the decane hydroconversion as probe reaction.

10 The aluminated ultrastable Y zeolite from example 3, subjected to 30 cycles of 120 s (Z2) was impregnated with an aqueous Pt(NH₄)₃Cl₂ solution to obtain a loading of 0.5 wt. %.

For comparison purposes, a parent CBV-712 zeolite sample was loaded with 0.5 wt. % of Pt metal.

15 Catalyst pellets with a size between 125 and 250 µm were obtained by compressing the Pt-impregnated USY zeolite powder, crushing into flakes and sieving. Amounts of 35 mg of catalyst pellets were loaded in a microreactor of a high throughput reactor unit described in Ref.34. The catalyst pretreatment procedure comprised heating to 400 °C at 5 °C/min under oxygen flow for 1 h, flushing with nitrogen for 25 min, and finally a reduction under flowing hydrogen at 400 °C for 1 h without intermittent cooling.
20 The reactor was cooled to the reaction temperature of 150 °C. The unit is operated at a total pressure of 0.45 MPa and a hydrogen to hydrocarbon molar ratio of 375. The contact time was 2522 kg.s/mol. Reaction product analysis was done using online gas chromatography.

25 The conversion of decane at increasing reaction temperature is shown in Figure 3. The aluminated zeolite sample converts decane at substantially lower temperatures compared to the parent sample. The conversion curve is shifted by more than 30°C to lower temperatures by ALD of aluminum. The yields of decane skeletal and of cracked products are plotted against decane conversion in Fig.4. The parent zeolite and the ALD modification display the same yields for isomers and cracked products (Fig.4).

30

EXAMPLE 7. ^{27}Al MAS NMR Analysis for aluminated ultrastable Y zeolite

Aluminated ultrastable Zeolite Y samples from example 3 were characterized by ^{27}Al MAS NMR. The spectra were recorded on a Bruker DSX400 spectrometer (9.4 T). 12000 scans were accumulated with a recycle delay of 100 ms. The samples were packed in 2.5 mm rotors. The spinning frequency of the rotor was 20 kHz. 0.1 M aqueous solution of $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ was used as shift reference.

The ^{27}Al MAS NMR spectra present essentially three signals (Fig 5). The signal around 60 ppm is due to aluminum atoms in tetrahedral coordination incorporated in the zeolite framework. The signal around 30 ppm is due to distorted tetrahedral aluminum atoms and pentacoordinated aluminum atoms partially attached to the silicate framework (ref.35). The signal around 0 ppm is due to extraframework aluminum in octahedral coordination.

The signal of tetrahedral aluminum was little influenced by the ALD treatment. There was a substantial gain in intensity for the 30 ppm and 0 ppm signals. The spectacular gain in catalytic activity (Fig. 3) must be due to a reinforcement of the acid strength by introducing distorted tetrahedral, pentacoordinated and octahedrally coordinated aluminum into the zeolite. The NMR spectrometer was run under experimental conditions such that absolute signal intensities can be compared (Table 2). The ^{27}Al MAS NMR signal of the parent zeolite was taken as reference. The ^{27}Al MAS NMR signal in all samples subjected to ALD was higher than in the parent zeolite. The sequence of ^{27}Al MAS NMR intensity of $\text{Z0} < \text{Z4} < \text{Z5} < \text{Z2} < \text{Z3} < \text{Z1}$ reflect the integrated exposure time to TMA over the cycles the sample was subjected to.

(Z0 = Parent zeolite CBV 712; Z1 = 30cycles of 480s; Z2= 30cycles of 120s; Z3=

10cycles of 480s; Z4 = 10 cycles of 120s; Z5= 5cycles of 480s).

Table 2. Total signal intensity of ^{27}Al MAS NMR spectra of ultrastable Y zeolites (spectra shown in Fig.5)

sample	Area(a.u.)
Z0	1.0000
Z1	1.8772
Z2	1.4094
Z3	1.5725
Z4	1.2614
Z5	1.3748

EXAMPLE 8. ^{27}Al MAS NMR of aluminated zeotile-4 (hierarchical material) and (S-1) Silicalite-1 sample (nanazeolite)

The ^{27}Al MAS NMR spectra of aluminated zeotile-4 (hierarchical material) from example 5 and (S-1) Silicalite-1 sample (Nanazeolite) from example 4 are shown in Figure 6. These materials in their parent form do not contain any aluminum and show no signal in the ^{27}Al MAS NMR experiment. The ALD of aluminum results in the formation of tetrahedral aluminum (55 ppm), distorted tetrahedral and pentacoordinated aluminum (30 ppm) and extraframework octahedral aluminum (0 ppm). The two samples were subjected to a same exposure to TMA (same number of cycles of a same duration). Nevertheless, the ^{27}Al MAS NMR signal in the silicalite-1 sample is weaker than in the Zeotile-4 sample. The zeotile-4 sample is a hierarchical material with mesopores and micropores. The surfaces of the mesopores are hydroxylated and provide reactive sites for aluminum binding.

The silicalite-1 is a microporous material with small particle size (nanazeolite). The majority of hydroxyl groups suitable for ALD are located on the external surface of the zeolite particles. The aluminations is expected to occur especially on the external surface. Quantification of the ^{27}Al MAS NMR signals (Table.3) confirms the lower NMR signal intensity in the aluminated silicalite-1 nanazeolite compared to the aluminated Zeotile-4 sample.

Table 3.Relative intensity of ^{27}Al MAS NMR signal of aluminated Zeotile-4 sample and Silicalite-1 nanazeolite (spectra shown in Fig.5) Same reference as in Table 2

Sample	Area (a.u.)
Aluminated Zeotile-4	0.72636
Aluminated Silicalite-1	0.16925

EXAMPLE 9. Characterization of the porosity of aluminated ultrastable Y zeolites using nitrogen adsorption

Adsorption – desorption isotherms of nitrogen gas at -196°C on the parent ultrastable Y zeolite and the ALD modified specimen are presented in Fig.7. Aluminations

leads to a decrease of the nitrogen adsorption capacity. The samples show some hysteresis between adsorption and desorption branches of the isotherm. This hysteresis is caused by capillary condensation in mesopores. The ALD treatment does not eliminate the mesopores. The surface area (mesoporous + external) and micropore volume of the ultrastable Y zeolite samples has been calculated from t-plots using as reference, the Hakins-Jura equation to calculate the thickness of adsorbed nitrogen layer as a function of P/P_0 . The calculated values are listed in Table 4.

Table 4. Texture of ultrastable Y zeolites aluminated via ALD

Sample code	Al content	Mesopore and external surface area (m ² /g)	micropore volume (mL/g)
Z0	1	102	0.27
Z4	1.2614	64	0.23
Z5	1.3748	76	0.24
Z2	1.4094	64	0.23
Z3	1.5725	77	0.23
Z1	1.8772	32	0.16

The parent sample (Z0) has the highest microporosity. The introduction of aluminum via ALD leads to a moderate loss of microporosity. In the most loaded Z1 sample the microporosity loss is more pronounced. This decrease in microporosity can be explained by two effects. First, the introduced aluminum will occupy space inside the micropores. Second, the aluminum introduction causes an increase in weight of the zeolite. The CBV-712 zeolite has a Si/Al ratio of ca. 6/1. For an increase of the Al content by 40%, and taking an Al_2O_3 formula to represent the incorporated aluminum, a weight gain of the sample by 10% can be expected. As the introduced alumina is not expected to create additional pores, a decrease of the porosity by 10% can be explained by the weight gain. In conclusion, the ALD treatment did not close off micropores in Z2-Z5 samples. In the most severely treated sample (Z1), there is a significant loss of microporosity that may be due to pore blocking by aluminum incorporated via ALD. The evolution of micropore volume with alumination of the ultrastable Y zeolites is plotted in Fig.8.

The parent zeolite (Z0) has largest surface area in mesopores and on the external crystal surface (Table 4). The external surface area of these Y zeolites is quite small, so that the determined surface area is due to mesopores mainly. The surface area in the mesopores of Z2-5 samples having a similar alumination level is similar. The most

strongly aluminated sample has the lowest mesopore surface area (Z1). The mesopore surface area per gram of ultrastable Y zeolite gradually decreases with Al content (Fig.9). This is due to the weight gain and to the coverage of the mesoporous cavities with alumina species, decreasing the surface area.

5

EXAMPLE 10. Nitrogen adsorption measurements on Zeotile-F (Al-ZT-4) and Silicalite-1 (Al-S-1) samples

10 Adsorption – desorption Isotherms for the aluminated Zeotile-4 (Al-ZT-4) and Silicalite-1 (Al-S-1) are shown in Figure 10. The Zeotile-4 sample presents an hysteresis loop with parallel branches owing to the presence of well defined mesopores after ALD treatment.

The Silicalite-1 zeolite is a microporous material with strong nitrogen adsorption at low relative pressure followed by a plateau.

15

EXAMPLE 11. Decane catalytic test over bifunctional silicalite (Al-S-1) and Zeotile-4 (Al-ZT-4) samples

The catalytic activity of the aluminated zeolites was evaluated using the decane hydroconversion as probe reaction.

20 The aluminated zeolite-4 and the silicalite-1 and the parent samples were loaded with platinum metal and evaluated in decane hydroconversion as explained for the ultrastable Y zeolites in example 6. The parent samples were inactive at reaction temperatures below 350°C. The aluminated zeotile-4 material was active starting at 220°C (Figure 11). Decane isomerization and cracking are consecutive reactions (Figure 25 12), indicating that the platinum loaded aluminated Zeotile-4 is a bifunctional catalyst presenting a well balanced acid and hydrogenation-dehydrogenation function (ref.36).

30

References cited

- [1] L.B. McCusker *et al.*, Pure Appl.Chem. 2001, 73, 381-394.
- [2] J. Rouquerol *et al.*, Pure Appl.Chem. 1994, 66, 1739-1758.
- 5 [3] C.T. Kresge *et al.*, Nature 1992, 359, 710-712.
- [4] A. Monnier *et al.*, Science 1993, 261, 1299-1303.
- [5] D.Zhao *et al.*, Science 1998, 279, 548.
- [6] S. Inagaki *et al.*, Bull.Chem.Soc.Jpn. 1996, 69, 1449-1457.
- [7] J.C. Jansen *et al.*, Chem.Comm. 2001, 8, 713-714.
- 10 [8] A.H. Janssen, Angew.Chem.Int.Ed. 2001, 40, 1102-1104.
- [9] Jacobsen *et al.*, J.Am.Chem.Soc. 2000, 112, 7116-7117.
- [10] Kim *et al.*, Chem.Mater. 2003, 15, 1932-1934.
- [11] Y. Tao *et al.*, J. Phys.Chem.B 2003, 107, 10974-10976.
- [12] S P B Kremer *et al.*, Adv. Mater. 2003, 15, 1705-1707.
- 15 [13] J.A. Martens *et al.*, PCT Int. Appl. 2005, WO 2005 000740 A2.
- [14] R.Szostak, in H.van Bekkum, E.M. Flanigen, J.C. Jansen (Eds.), Introduction to zeolite science and practice, Stud. Surf. Sci. catal. 58, Elsevier, 1991, pp.153-192.
- [15] Gunter H Kuhl, in J. Weitkamp, L. Puppe (Eds) Catalysis and Zeolites, Fundamentals and Applications, Springer 1999, pp 81-179.
- 20 [16] M W Anderson *et al.*, Chem Commun. 1984, 23, 1596-1597
- [17] T.Yashima *et al.*, in P.J. Grobet *et al.* (Eds) Innovation in zeolite materials science, Stud. Surf. Sci. catal. 37, Elsevier 1988, pp. 175-182.
- [18] Catana, G. *et al.*, J. Phys. Chem. B 2000, 104, 9195 – 9202.
- [19] A.S. O'Neil *et al.*, J.Am.Chem.Soc. 2002, 124, 10636-10637
- 25 [20] L.Y.Chen *et al.*, Microporous and Mesoporous Materials 1999, 27, 231-242.
- [21] L.C. Guan *et al.*, J. Phys. Sci. 2006, 17, 65-75.
- [22] R. Mokaya and W. Jones, J. Mater. Chem. 1999, 9, 555 - 561
- [23] Y. Oumi *et al.*, Microporous and Mesoporous Materials 44-45, 2001, 267-274
- [24] Lim *et al.*, Nature Materials 2003, 2, 749-54.
- 30 [25] www.cambridgenanotech.com.
- [26] Riikka Puurunen, PhD Thesis, Department of Chemical Technology, Helsinki University of Technology (Espoo, Finland), 2002
- [27] R.L Pruunen *et al.*, Applied Surface Science 2000, 165, 193-202
- [28] Falconer *et al.*, US Patent ,US006043177A

- [29] P C Stair *et al.*, Topics in catalysis 2006, 39, 181-186.
- [30] Elam, J.W *et al.*, ECS Transactions 2007, 11, 177-184
- [31] Elam, J.W *et al.*, Journal of Nanomaterials 2006.
- [32] Jiang *et al.*, J.Am.Chem.Soc. 2006, 128, 11018-1101.
- 5 [33] Ravishankar *et al.*, J. Phys. Chem. B 1998,102, 2633-2639.
- [34] Huybrechts W. *et al.*, Appl. Cat A Gen. 2003, 243, 1-13
- [35] Grobet *et al.*, chemm. Commun. 1987, 22, 1688-90
- [36] Weitkamp J, Ind. Eng. Chem. Prod. Res. Dev. 1982, 550-558.
- [37] Herrera *et al.*, Topics in Catalysis, 2006, 39: 3-4
- 10 [38] Du *et al.*, J. Catal 2008, 253, 74-90
- [39] Mahurin *et al.*, Journal of Non-Crystalline Solids 2006, 352, 3280-3284
- [40] Funke *et al.* US Patent ,US006051517A

CLAIMS

- 5 1. A method for increasing the acid catalytic activity of a silicate based nanoporous material, said method comprising the incorporation of a chemical element in said material using an atomic layer deposition process under conditions favoring the hydrolysis of a compound comprising said chemical element.
2. A method according to claim 1, wherein the atomic layer deposition process is performed with a gaseous metal compound and water reactants
- 10 3. The method according to claims 1 or 2 wherein said silicate based nanoporous material is selected out of the group consisting of mesoporous zeolites, nanozeolites, ordered mesoporous materials and hierarchical materials.
4. A method according to any of the claims 1 to 3 wherein the element is a trivalent element
- 15 5. A method according to claims 1 to 4 wherein the trivalent element is Aluminum, Gallium, Iron or Boron.
6. A method according to any of the claims 1 to 5 wherein Aluminum is incorporated in said silicate based nanoporous materials using atomic layer deposition cycles with trimethylaluminum and water reactants.
- 20 7. The use of a silicate-based nanoporous material with enhanced acid catalytic activity obtained by the method according to any of the claims 1 to 6 for the hydroconversion of hydrocarbons.
8. The use of the method according to claim 6 for reactivating silicate-based nanoporous materials that became deactivated during operation because of dealumination
- 25 9. The use of of the method according to claim 6 for selectively aluminating the external surface of nanozeolites.

FIGURES

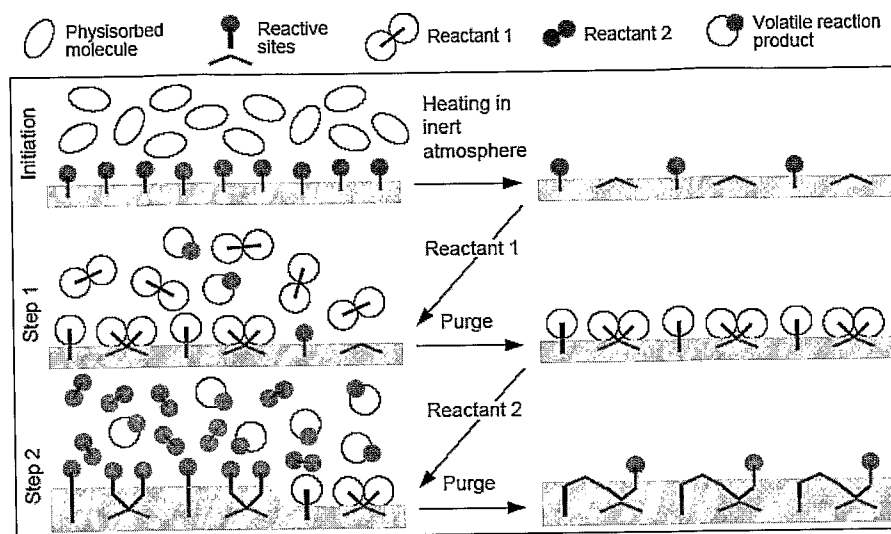


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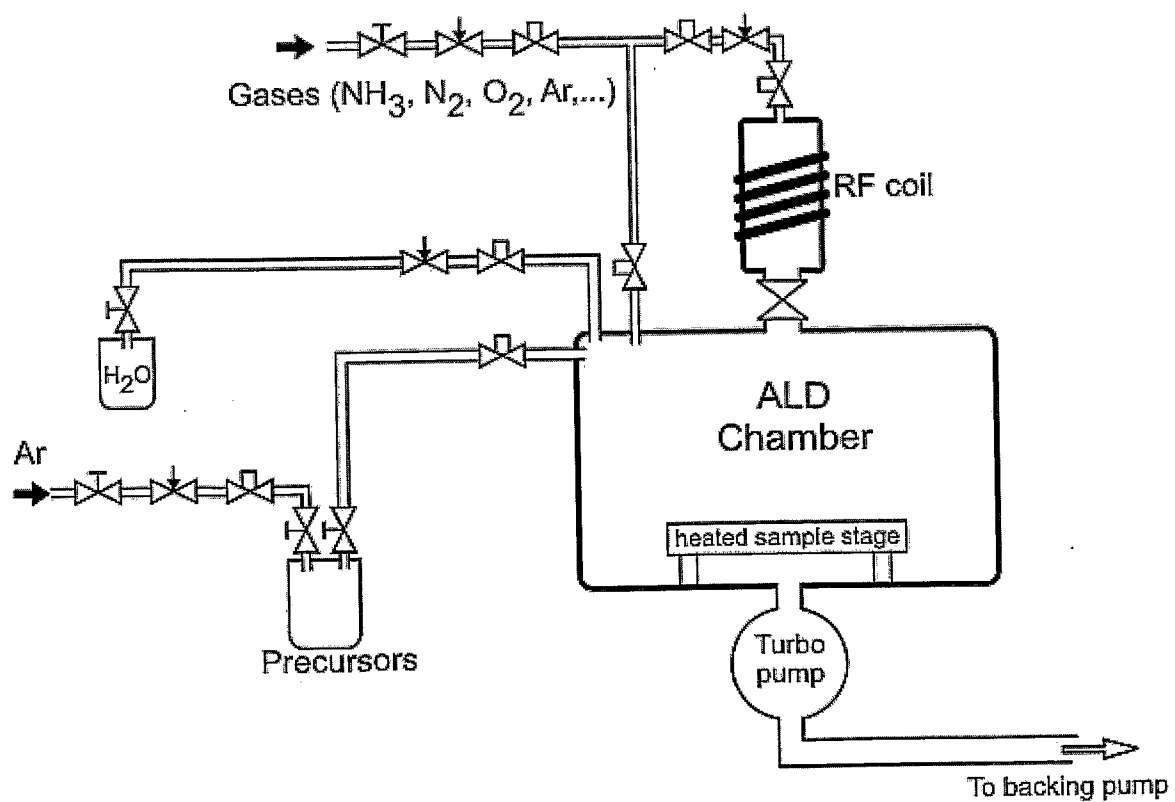


Figure 2

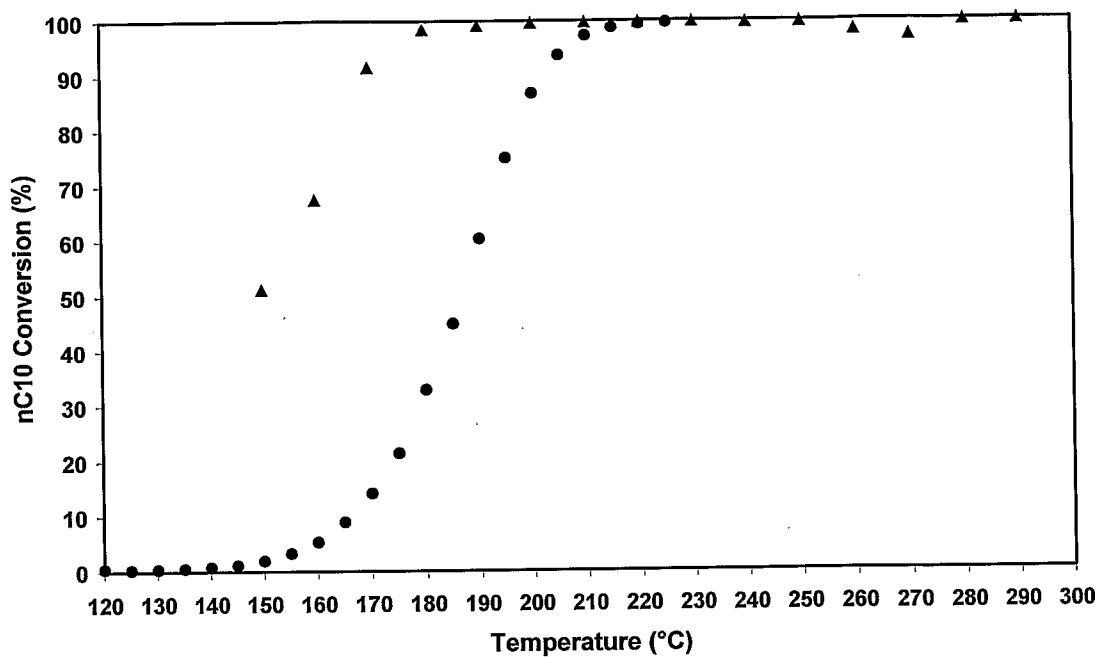


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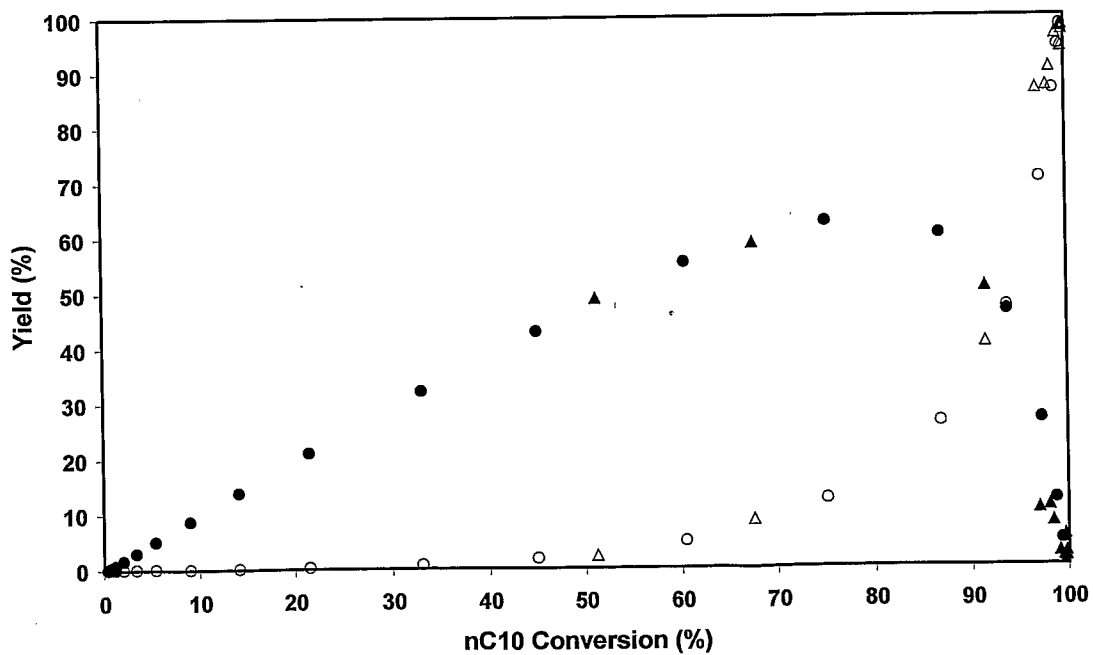


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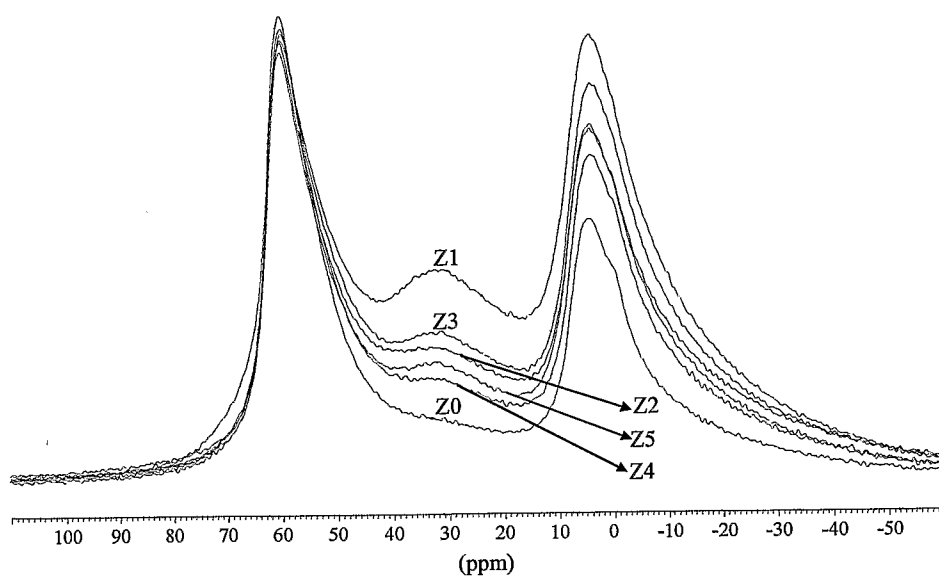
^{27}Al MAS NMR

Figure 5

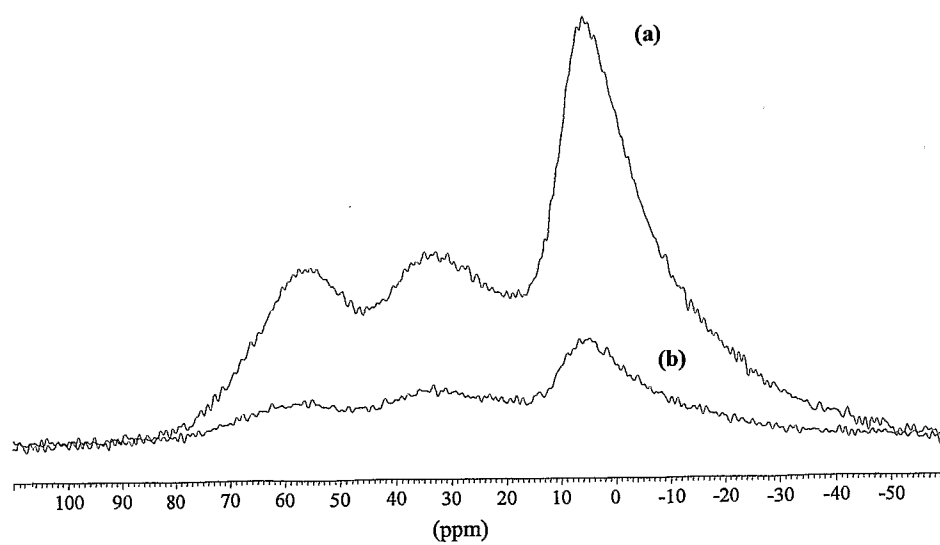
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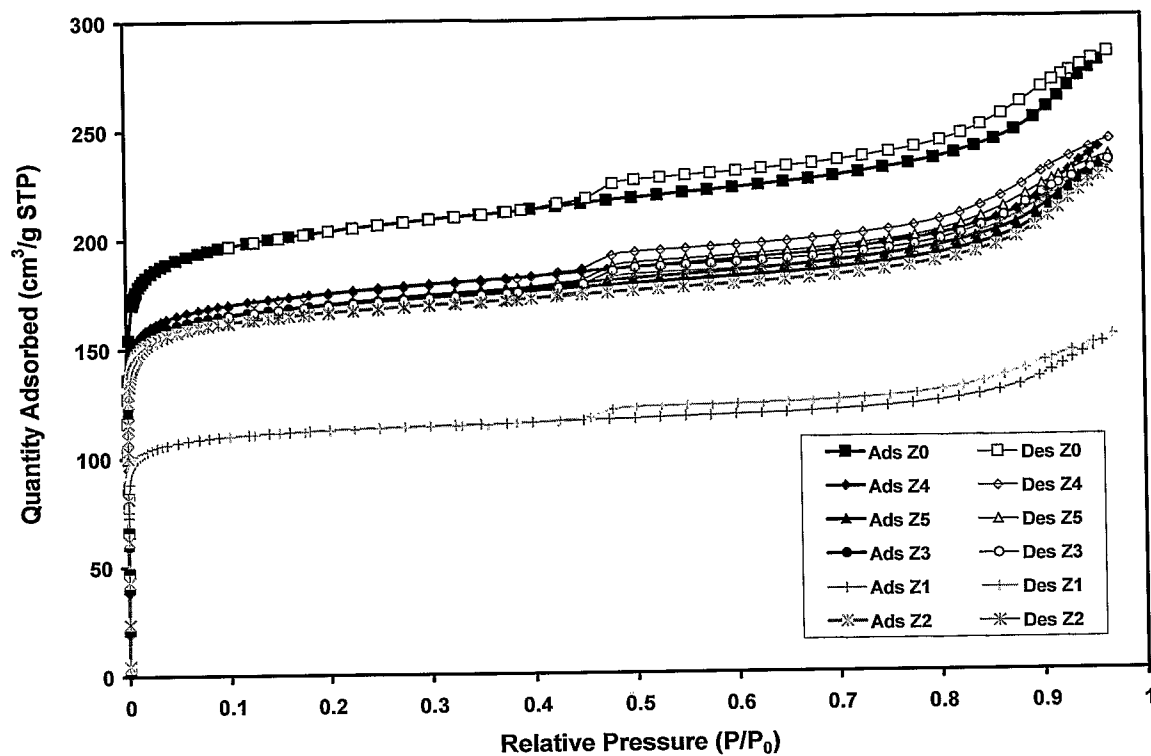


Figure 7

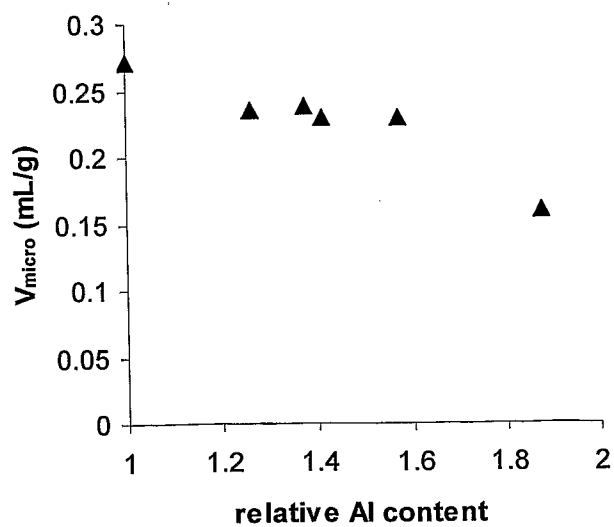


Figure 8

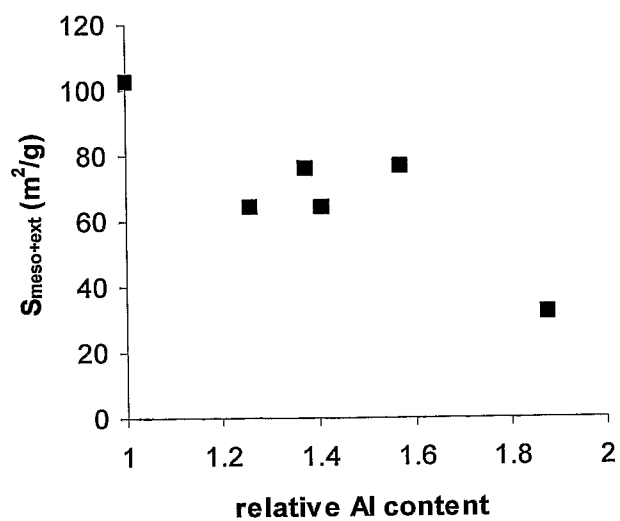


Figure 9

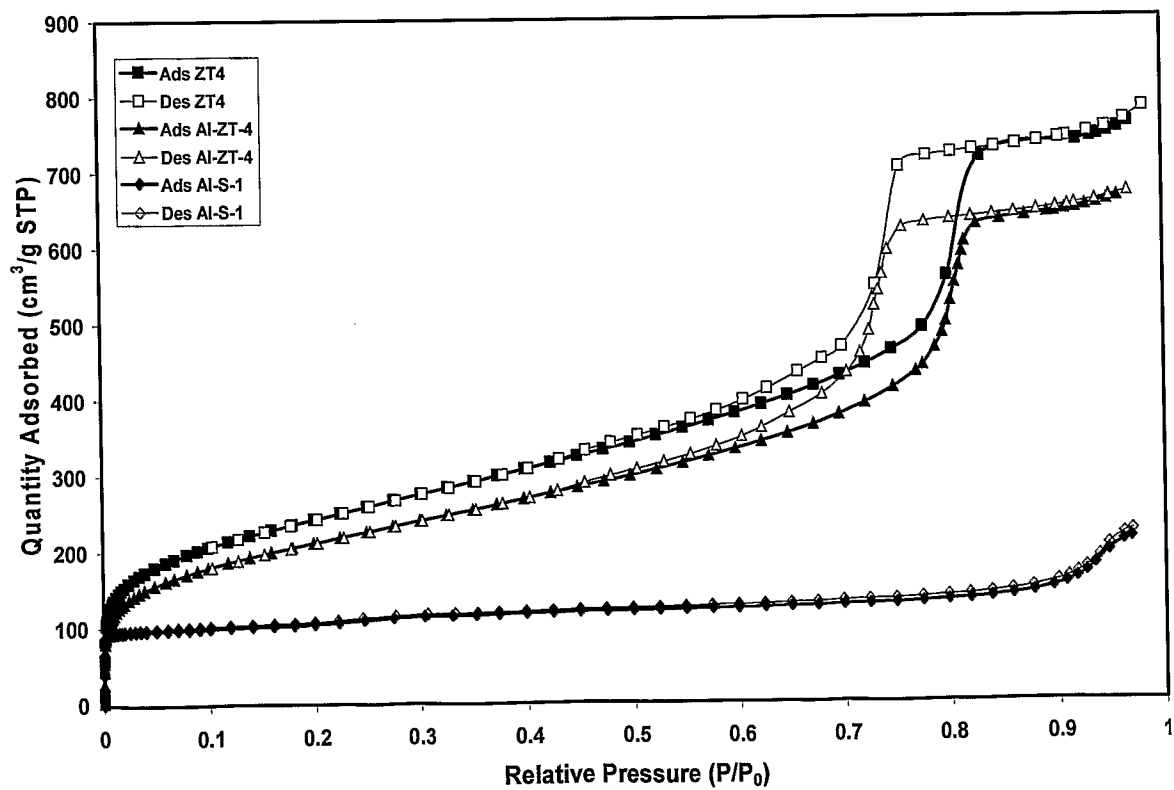


Figure 10

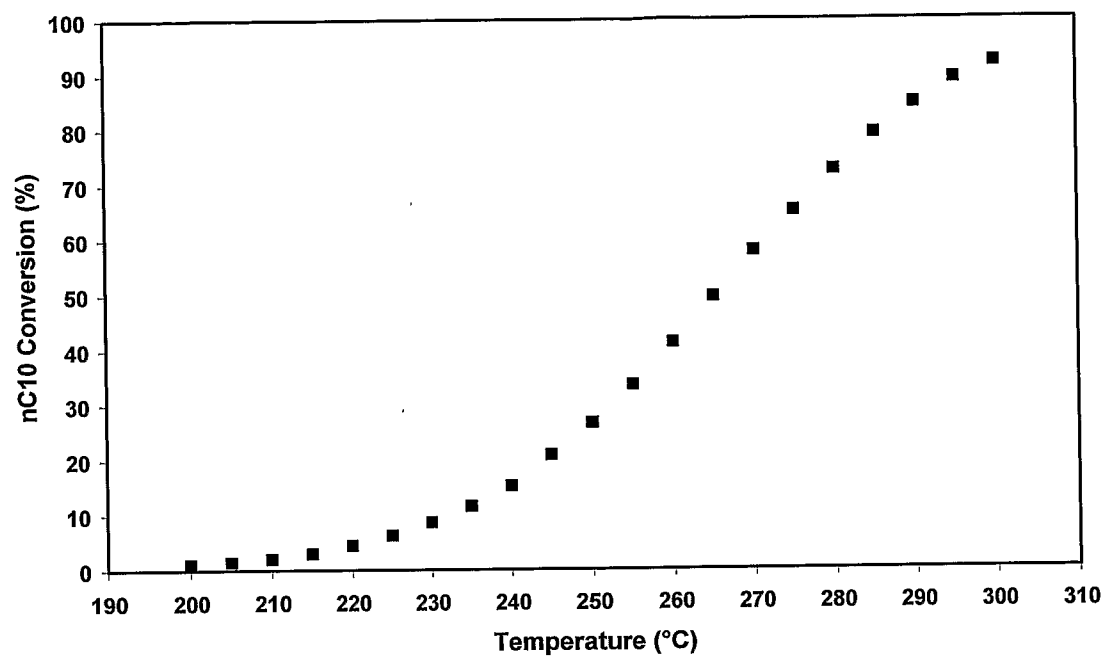


Figure 11

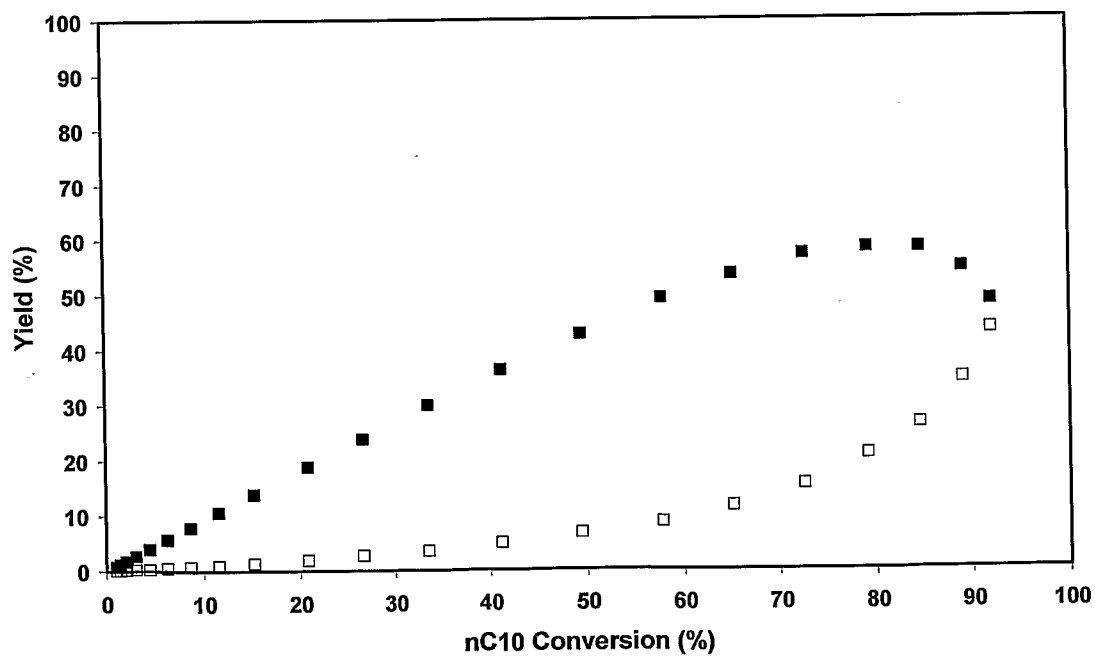


Figure 12