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DESCRIPTION

CROSS REFERENCE TO RELATED APPLICATION

[0001] The present application is a Non-Provisional and claims priority from U.S. Provisional Application Serial No. 61/774,192 filed March 7, 2013, entitled "Liquid Panel Assembly", which related and claims priority from U.S. Provisional Application Serial No. 61/692,798 filed August 24, 2012, entitled "Liquid Panel Assembly,".

BACKGROUND OF THE DISCLOSURE

[0002] Embodiments of the present disclosure generally relate to a liquid panel assembly, and more particularly, to a liquid panel assembly configured for use with an energy exchanger. DE 10143092 A1 discloses a liquid panel assembly having the features in the preambles of claims 1 and 14.

[0003] Enclosed structures, such as occupied buildings, factories and the like, generally include a heating/ventilation/air conditioning (HVAC) system for conditioning outdoor ventilated and/or recirculated air. The HVAC system includes a supply air flow path and an exhaust air flow path. The supply air flow path receives pre-conditioned air, for example outside air or outside air mixed with re-circulated air, and channels and distributes the pre-conditioned air into the enclosed structure. The pre-conditioned air is conditioned by the HVAC system to provide a desired temperature and humidity of supply air discharged into the enclosed structure. The exhaust air flow path discharges air back to the environment outside the structure. Without energy recovery, conditioning the supply air typically requires a significant amount of auxiliary energy, particularly in environments having extreme outside air conditions that are much different than the required supply air temperature and humidity. Accordingly, energy exchange or recovery systems are used to recover energy from the exhaust air flow path. Energy recovered from air in the exhaust flow path is utilized to reduce the energy required to condition the supply air.

[0004] Conventional energy exchange systems may utilize energy recovery devices (for example, energy wheels and permeable plate exchangers) or heat exchange devices (for example, heat wheels, plate exchangers, heat-pipe exchangers and run-around heat exchangers) positioned in both the supply air flow path and the return air flow path. Liquid-to-air membrane energy exchangers (LAMEEs) may be fluidly coupled so that a desiccant liquid flows between the LAMEEs in a run-around loop, similar to run-around heat exchangers that typically use aqueous glycol as a coupling fluid.

[0005] In general, a LAMEE transfers heat and moisture between a liquid desiccant solution and air through a thin flexible membrane. A flat plate LAMEE includes a series of alternating

liquid desiccant and air channels separated by the membrane. Typically, the pressure of the liquid within a liquid channel between membranes is higher than that of the air pressure outside of the membranes. As such, the flexible membranes tend to outwardly bow or bulge into the air channel(s).

[0006] In order to avoid excessive restriction of the air flow due to membrane bulge, air channels of a LAMEE are relatively wide compared to the liquid channels. Moreover, a support structure is generally provided between membranes to limit the amount of membrane bulge. However, the relatively wide air channels and support structures typically diminish the performance of the LAMEE. In short, resistance to heat and moisture transfer in the air channel is relatively high due to the large air channel width, and the support structure may block a significant amount of membrane transfer area. Accordingly, a large amount of membrane area is needed to meet performance objectives, which adds costs and results in a larger LAMEE. Moreover, the support structure within an air channel may produce an excessive pressure drop, which also adversely affects operating performance and efficiency of the LAMEE.

[0007] Typically, desiccant flows through a solution panel, which may include membranes that contain the desiccant between air channels. In general, the solution panel is uniformly full of desiccant during operation. Known energy exchangers force flow of desiccant upwardly through the solution panel, against the force of gravity. As such, the desiccant is typically pumped from the bottom of the solution panel to the top with enough pressure to overcome the relatively large amount of static head pressure, as well as the friction in the panel. However, the pumping pressure causes the membranes of the solution panel to outwardly bow or bulge. Moreover, the pumping pressure is often great enough to cause leaks in the membranes. Further, the pressure of the desiccant being pumped through the solution panel often causes membrane creep and degradation over time.

[0008] A typical solution panel also includes a filler material, such as a wick or woven plastic screen, configured to ensure proper spacing between membrane surfaces within the solution panel. The flow of the desiccant through the filler material is generally uncontrolled. For example, the filler material is generally unable to direct the desiccant over a particular path. Instead, the flow of desiccant through the filler material follows the path of least resistance, which generally follows a Hele-Shaw pattern between closed-spaced plates. Further, the flow pattern of the desiccant is sensitive to variations in the spacing within the solution panel caused by even small amounts of membrane bulge. Also, fluid instabilities from concentration and temperature gradients may cause additional flow irregularities and mal-distributions. The winding flow pattern within a typical solution panel produces flow dead zones at or proximate corners of the solution panel.

[0009] As noted, in order to ensure that desiccant completely fills the solution panel from bottom to top, a relatively high pumping pressure is used. However, the pumping pressure may often generate membrane bulge and bowing, which may adversely affect the energy exchanger.

[0010] DE 101 43 092 A1 discloses a coolant recirculation system for a passenger compartment air heater, which includes three cross flow heat exchangers in an arrangement promoting thermal stratification. WO 2011/161547 A2 discloses a liquid-to-air membrane energy exchanger. US 2008/099184 A1 discloses a heater core and air conditioner for an automobile equipped with same. EP 1 108 575 A1 discloses an air conditioner for a vehicle. US 2008/023182 A1 discloses a dual mode heat exchanger assembly.

SUMMARY OF THE DISCLOSURE

[0011] Certain embodiments of the present disclosure provide a liquid panel assembly, which may be configured to be used with an energy exchanger, for example. The liquid panel assembly may include a support frame having one or more fluid circuits and at least one membrane secured to the support frame. Each fluid circuit may include an inlet channel connected to an outlet channel through one or more flow passages, such as counterflow passages (in that liquid in the counterflow passages counterflows with respect to another fluid, such as air, outside of the at least one membrane). A liquid, such as a desiccant, is configured to flow through the fluid circuit(s) and contact interior surfaces of the membrane(s). The fluid circuit(s) is configured to offset hydrostatic pressure gain with friction pressure loss of the liquid that flows within the one or more fluid circuits to reduce pressure within the liquid panel assembly.

[0012] The shape, porosity, and/or hydraulic diameter of one or both of the inlet and outlet channels may be determined by a weight, viscosity, and/or flow speed of the liquid that is configured to flow through the fluid circuit(s). For example, if the liquid is heavy, the diameters of the channels may be reduced in order to promote faster liquid flow therethrough, which generates increased friction that offsets the liquid hydrostatic pressure.

[0013] The flow passages may include a set of a plurality of flow passages connected to the inlet channel and the outlet channel. A number of flow passages within the set of a plurality of flow passages may be determined by a weight and/or viscosity of the liquid that is configured to flow through the fluid circuit(s).

[0014] The fluid circuit(s) may include a plurality of fluid circuits. The lengths of each of the fluid circuits may be equal. The plurality of fluid circuits may include a first set of a plurality of flow passages connected to a first inlet channel and a first outlet channel, and a second set of a plurality of flow passages connected to a second inlet channel and a second outlet channel. The first set of a plurality of flow passages may be staggered with respect to the second set of a plurality of flow passages.

[0015] Each of the inlet and outlet channels may provide a flow alignment vane configured to direct the liquid to flow along a particular path. The inlet and outlet channels may be configured to provide support to the membrane(s). The inlet and outlet channels may be configured to

provide a sealing surface for at least a portion of the membrane(s). The inlet and outlet channels may be configured to maximize a length of the flow passages.

[0016] The membrane(s) may be continuously bonded around a perimeter of the support frame. The fluid circuits may be configured to provide uniform liquid flow distribution across and/or through the liquid panel assembly. The support frame and the membrane may be configured to be vertically oriented within an energy exchange cavity of an energy exchanger.

[0017] The inlet channel may be disposed at an upper corner of the support frame. The outlet channel may be disposed at a lower corner of the support frame. The upper corner may be diagonally located from the lower corner. The inlet and outlet channels may be vertical and the flow passages(s) may be horizontal. A horizontal length of the flow passage(s) may exceed half a total horizontal length of the support frame. The assembly may also include inlet and outlet members, such as headers, connected to the fluid circuit(s). The inlet and outlet members may include a liquid delivery channel and a liquid passage channel, respectively. The inlet member may be configured to modularly engage another inlet member, and the outlet member may be configured to modularly engage another outlet member. At least a portion of the membrane(s) may sealingly engage the inlet and outlet members.

[0018] Alternatively, the support frame and the membrane may be configured to be horizontally oriented within an energy exchange cavity of an energy exchanger.

[0019] The inlet channel may be disposed at one corner of the support frame. The outlet channel may be disposed at another corner of the support frame. The first corner may be diagonally located from the second corner. The inlet and outlet channels may be vertical and the flow passages(s) may be horizontal. A horizontal length of the flow passage(s) may exceed half a total horizontal length of the support frame.

[0020] The assembly may also include inlet and outlet members, such as headers, connected to the fluid circuit(s). The inlet member may fluidly engage all inlet channels and the outlet member may fluidly engage all outlet channels.

[0021] Alternatively, the flow passages in one or more panels can be fluidly connected to members, such as headers. One or more of these members can be fluidly connected to flow channels. Inlet channels can be fluidly connected to inlet members which can, in turn, be connected to flow passages. The flow passages can be fluidly connected to outlet members, such as headers, which are, in turn, connected to outlet channels.

[0022] Certain embodiments of the present disclosure provide an energy exchange system that may include a plurality of air channels configured to allow air to pass therethrough, and a plurality of liquid panel assemblies alternately spaced with the plurality of liquid panel assemblies. The system may also include a plurality of membrane support assemblies disposed within the plurality of air channels. Air within the air channels may be configured to counterflow with respect to the liquid within the one or more flow passages.

BRIEF DESCRIPTION OF THE DRAWINGS**[0023]**

Figure 1 illustrates a schematic view of an energy exchange system, according to an embodiment of the present disclosure.

Figure 2 illustrates a side perspective view of a liquid-to-air membrane energy exchanger, according to an embodiment of the present disclosure.

Figure 3 illustrates a cut-away front view of panels within an energy exchange cavity of a liquid-to-air membrane energy exchanger, according to an embodiment of the present disclosure.

Figure 4 illustrates an exploded isometric top view of an energy exchange cavity, according to an embodiment of the present disclosure.

Figure 5 illustrates a front view of a support frame of a liquid panel assembly, according to an embodiment of the present disclosure.

Figure 6 illustrates an isometric top view of an inlet member, according to an embodiment of the present disclosure.

Figure 7 illustrates an internal view of an inlet member, according to an embodiment of the present disclosure.

Figure 8 illustrates an isometric view of an area proximate an upper corner of a support frame of a liquid panel assembly, according to an embodiment of the present disclosure.

Figure 9 illustrates a chart of fluid pressure levels within a liquid panel assembly, according to an embodiment of the present disclosure.

Figure 10 illustrates a front view of a support frame of a liquid panel assembly, according to an embodiment of the present disclosure.

Figure 11 illustrates an isometric top view of liquid distribution channels formed in a support frame, according to an embodiment of the present disclosure.

Figure 12 illustrates an isometric top view of liquid distribution channels formed in a support frame, according to an embodiment of the present disclosure.

Figure 13 illustrates a simplified view of a liquid circuit, according to an embodiment of the present disclosure.

Figure 14 illustrates a simplified view of a liquid circuit, according to an embodiment of the present disclosure.

Figure 15 illustrates a simplified view of a liquid circuit, according to an embodiment of the

present disclosure.

Figure 16 illustrates an isometric view of horizontal liquid panel assemblies connected to combined inlet channels and combined outlet channels, according to an embodiment of the present disclosure.

Figure 17 illustrates an isometric view of horizontal liquid panel assemblies connected to individual inlet channels and individual outlet channels, according to an embodiment of the present disclosure.

Figure 18 illustrates an isometric view of stacked horizontal liquid panel assemblies connected to inlet headers, according to an embodiment of the present disclosure.

Figure 19 illustrates an isometric view of stacked horizontal liquid panel assemblies with external pressure balancing, according to an embodiment of the present disclosure.

DETAILED DESCRIPTION OF THE DRAWINGS

[0024] The foregoing summary, as well as the following detailed description of certain embodiments will be better understood when read in conjunction with the appended drawings. As used herein, an element or step recited in the singular and proceeded with the word "a" or "an" should be understood as not excluding plural of said elements or steps, unless such exclusion is explicitly stated. Furthermore, references to "one embodiment" are not intended to be interpreted as excluding the existence of additional embodiments that also incorporate the recited features. Moreover, unless explicitly stated to the contrary, embodiments "comprising" or "having" an element or a plurality of elements having a particular property may include additional such elements not having that property.

[0025] As explained in detail below, embodiments of the present disclosure provide liquid panel assemblies that are configured to balance internal liquid hydrostatic pressure and frictional forces. As such, the total pressure within the liquid panel assemblies may be reduced, negated or otherwise neutralized. Embodiments of the present disclosure provide a liquid panel assembly that may be configured, through selection of a number, orientation, shape, and/or the like of flow channels or passages, to ensure that pressure within the assembly is substantially reduced, negated, or otherwise neutralized. That is, the pressure may be reduced, negated, or otherwise neutralized to a greater extent than a negligible amount. Thus, membrane bulge is substantially reduced (that is, more than a negligible amount) or eliminated, which reduces the potential for leaks and membrane creep.

[0026] Figure 1 illustrates a schematic view of an energy exchange system 100, according to an embodiment of the present disclosure. The system 100 is configured to partly or fully condition air supplied to a structure 101. The system 100 may include an inlet 102 for a pre-

conditioned air flow path 104. The pre-conditioned air flow path 104 may include outside air, air from a building adjacent to the enclosed structure 101, or air from a room within the enclosed structure 101. Airflow in the pre-conditioned air flow path 104 may be moved through the pre-conditioned air flow path 104 by a fan 106. The fan 106 directs the pre-conditioned air flow through path 104 to a supply air liquid-to-air membrane energy exchanger (LAMEE) 108. The supply air LAMEE 108 conditions the pre-conditioned air flow in path 104 to generate a change in air temperature and humidity (i.e. to pre-condition the air partly or fully) toward that which is required for a supply air flow condition to be discharged into the enclosed space 101. During a winter mode operation, the supply air LAMEE 108 may condition the pre-conditioned air flow path 104 by adding heat and moisture to the pre-conditioned air in flow path 104. In a summer mode operation, the supply air LAMEE 108 may condition the pre-conditioned air flow path 104 by removing heat and moisture from the pre-conditioned air in flow path 104. The pre-conditioned air 110 may be channeled to an HVAC system 112 of the enclosed structure 101. The HVAC system 112 may further condition the pre-conditioned air 110 to generate the desired temperature and humidity for the supply air 114 that is supplied to the enclosed structure 101.

[0027] As shown in Figure 1, one fan 106 may be located upstream of the LAMEE 108. Optionally, the pre-conditioned air flow path 104 may be moved by a down-stream fan and/or by multiple fans or a fan array or before and after each LAMEE in the system.

[0028] Return air 116 is channeled out of the enclosed structure 101. A mass flow rate portion 118 of the return air 116 may be returned to the HVAC system 112. Another mass flow rate portion 119 of the return air 116 may be channeled to a return air or regeneration LAMEE 120. The portions 118 and 119 may be separated with a damper 121 or the like. For example, 80% of the return air 116 may be channeled to the HVAC system 112 and 20% of the return air 116 may be channeled to the return air LAMEE 120. The return air LAMEE 120 exchanges energy between the portion 119 of the return air 116 and the preconditioned air 110 in the supply air LAMEE 108. During a winter mode, the return air LAMEE 120 collects heat and moisture from the portion 119 of the return air 116. During a summer mode, the return air LAMEE 120 discharges heat and moisture into the portion 119 of the return air 116. The return air LAMEE 120 generates exhaust air 122. The exhaust air 122 is discharged from the structure 101 through an outlet 124. A fan 126 may be provided to move the exhaust air 122 from the return air LAMEE 120. The system 100 may include multiple fans 126 or one or more fan arrays located either up-stream or down-stream (as in Figure 1) of the return air LAMEE 120.

[0029] A liquid, such as a desiccant fluid 127, flows between the supply air LAMEE 108 and the return air LAMEE 120. The desiccant fluid 127 transfers the heat and moisture between the supply air LAMEE 108 and the return air LAMEE 120. The system 100 may include desiccant storage tanks 128 in fluid communication between the supply air LAMEE 108 and the return air LAMEE 120. The storage tanks 128 store the desiccant fluid 127 as it is channeled between the supply air LAMEE 108 and the return air LAMEE 120. Optionally, the system 100 may not include both storage tanks 128 or may have more than two storage tanks. Pumps 130 are provided to move the desiccant fluid 127 from the storage tanks 128 to one of the supply air

LAMEE 108 or the return air LAMEE 120. The illustrated embodiment includes two pumps 130. Optionally, the system 100 may be configured with as few as one pump 130 or more than two pumps 130. The desiccant fluid 127 flows between the supply air LAMEE 108 and the return air LAMEE 120 to transfer heat and moisture between the conditioned air 110 and the portion 118 of the return air 116.

[0030] Figure 2 illustrates a side perspective view of a LAMEE 300, according to an embodiment. The LAMEE 300 may be used as the supply air LAMEE 108 and/or the return or exhaust air LAMEE 120 (shown in Figure 1). The LAMEE 300 includes a housing 302 having a body 304. The body 304 includes an air inlet end 306 and an air outlet end 308. A top 310 extends between the air inlet end 306 and the air outlet end 308. While not shown, a stepped-down top may be positioned at the air inlet end 306. The stepped-down top may be stepped a distance from the top 310. A bottom 316 extends between the air inlet end 306 and the air outlet end 308. While not shown, a stepped-up bottom may be positioned at the air outlet end 308. The stepped-up bottom may be stepped a distance from the bottom 316. In alternative designs the stepped-up bottom or stepped-down top sections may have different sizes of steps or no step at all.

[0031] An air inlet 322 is positioned at the air inlet end 306. An air outlet 324 is positioned at the air outlet end 308. Sides 326 extend between the air inlet 322 and the air outlet 324.

[0032] An energy exchange cavity 330 extends through the housing 302 of the LAMEE 300. The energy exchange cavity 330 extends from the air inlet end 306 to the air outlet end 308. An air stream 332 is received in the air inlet 322 and flows through the energy exchange cavity 330. The air stream 332 is discharged from the energy exchange cavity 330 at the air outlet 324. The energy exchange cavity 330 may include a plurality of panels 334, such as liquid panels configured to receive desiccant and direct the flow of the desiccant therethrough.

[0033] A desiccant inlet reservoir 352 may be positioned on the top 310. The desiccant inlet reservoir 352 may be configured to receive desiccant, which may be stored in a storage tank 128 (shown in Figure 1). The desiccant inlet reservoir 352 may include an inlet in fluid communication with the storage tank 128. The desiccant is received through the inlet. The desiccant inlet reservoir 352 may also include an outlet that is in fluid communication with desiccant channels 376 of the panels 334 in the energy exchange cavity 330. The liquid desiccant flows through the outlet into the desiccant channels 376. The desiccant flows along the panels 334 through the desiccant channels 376 to a desiccant outlet reservoir 354, which may be positioned at or proximate the bottom 316. Accordingly, the desiccant may flow through the LAMEE 300 from top to bottom. For example, the desiccant may flow into the desiccant channels 376 proximate the desiccant inlet reservoir 352, through the desiccant channels 376, and out of the LAMEE 300 proximate to the desiccant outlet reservoir 354. In an alternative embodiment, the desiccant may flow through the LAMEE 300 from bottom to top.

[0034] Figure 3 illustrates a cut-away front view of the panels 334 within the energy exchange cavity 330 of the LAMEE 300, according to an embodiment. The panels 334 may be solution or

liquid panels configured to direct the flow of liquid, such as desiccant, therethrough, as explained below. The panels 334 form a liquid desiccant flow path 376 that is confined by semi-permeable membranes 378 on either side and is configured to carry desiccant therethrough. The membranes 378 may or may not be porous or able to transfer mass. Each membrane 378 may be any flexible structure that may generally bulge under fluid pressure. The semi-permeable membranes 378 are arranged in parallel to form air channels 336 with an average flow channel width of 337 and liquid desiccant channels 376 with an average flow channel width of 377. In one embodiment, the semi-permeable membranes 378 are spaced to form uniform air channels 336 and liquid desiccant channels 376. The air stream 332 (shown in Figure 2) travels through the air channels 336 between the semi-permeable membranes 378. The desiccant in each desiccant channel 376 exchanges heat and moisture with the air stream 332 in the air channels 336 through the semi-permeable membranes 378. The air channels 336 alternate with the liquid desiccant channels 376. Except for the two side panels of the energy exchange cavity, each air channel 336 may be positioned between adjacent liquid desiccant channels 376.

[0035] In order to minimize or otherwise eliminate the liquid desiccant channels 376 from outwardly bulging or bowing, membrane support assemblies may be positioned within the air channels 336. The membrane support assemblies are configured to support the membranes, and may promote turbulent air flow between the air channels 336 and the membranes 378.

[0036] As an example, the LAMEE 300 may be similar to a LAMEE as described in WO 2011/161547, entitled "Liquid-To-Air Membrane Energy Exchanger," filed June 22, 2011, which is hereby incorporated by reference in its entirety.

[0037] Figure 4 illustrates an exploded isometric top view of an energy exchange cavity 400, according to an embodiment. The energy exchange cavity 400 may include a plurality of liquid panel assemblies 402 spaced apart from one another by membrane support assemblies 404, such as those described in U.S. Patent Application No., entitled "Membrane Support Assembly for an Energy Exchanger," filed, which claims priority to U.S. Provisional Application No. 61/692,793, entitled "Membrane Support Assembly for an Energy Exchanger," filed August 24, 2012, both of which are hereby incorporated by reference in their entireties. The membrane support assemblies 404 may reside in air channels 406. For example, the membrane support assemblies 404 may prevent membranes 418 of the solution panel assemblies 402 from outwardly bulging or bowing into the air channels 406. Airflow 408 is configured to pass through the air channels 406 between liquid panel assemblies 402. As shown, the airflow 408 may generally be aligned with a horizontal axis 410 of the energy exchange cavity 400. Thus, the airflow 408 may be horizontal with respect to the energy exchange cavity 400. Notably, however, the membrane support assemblies 404 may include turbulence promoters configured to generate turbulence, eddies, and the like in the airflow 408 within the energy exchange cavity 400.

[0038] Each liquid panel assembly 402 may include a support frame 412 connected to an inlet member 414 at an upper corner 415 and an outlet member 416 at a lower corner 417 that may

be diagonal to the upper corner 415. Further, membranes 418 are positioned on each side of the support frame 412. The membranes 418 are formed of a liquid impermeable, but air permeable, material. The membranes 418 sealingly engage the support frame 412 along outer edges in order to contain liquid within the liquid panel assembly 402. Alternatively, a single membrane may sealingly wrap around an entirety of the support frame 412.

[0039] Each inlet member 414 may include a liquid delivery opening 420, while each outlet member 416 may include a liquid passage opening 422. The liquid delivery openings 420 may be connected together through conduits, pipes, or the like, while the liquid passage openings 422 may be connected together through conduits, pipes, or the like. Optionally, the inlet members 414 and outlet members 416 may be sized and shaped to directly mate with one another so that a liquid-tight seal is formed therebetween. Accordingly, liquid, such as desiccant may flow through the liquid delivery openings 420 and the liquid passage openings 422. The inlet members 414 and outlet members 416 may be modular components configured to selectively couple and decouple from other inlet members 414 and outlet members 416, respectively. For example, the inlet members 414 and outlet members 416 may be configured to securely mate with other inlet members 414 and outlet members 416, respectively, through snap and/or latching connections, or through fasteners and adhesives.

[0040] As shown, the liquid panel assemblies 402, the membrane support assemblies 404, and the air channels 406 may all be vertically oriented. The liquid panel assemblies 402 may be flat plate exchangers that are vertically-oriented with respect to a base that is supported by a floor, for example, of a structure.

[0041] Alternatively, the liquid panel assemblies 402, the membrane support assemblies 404, and the air channels 406 may all be horizontally oriented. For example, the liquid panel assemblies 402 may be flat plate exchangers that are horizontally-oriented with respect to a base that is supported by a floor, for example, of a structure.

[0042] In operation, liquid, such as desiccant, flows into the liquid delivery openings 420 of the inlet members 414. For example, the liquid may be pumped into the liquid delivery openings 420 through a pump. The liquid then flows into the support frames 412 through a liquid path 424 toward the outlet members 416. As shown, the liquid path 424 includes a vertical descent 426 that connects to a horizontal, flow portion, such as a flow portion 428, which, in turn, connects to a vertical descent 430 that connects to the liquid passage opening 422 of the outlet member 416. The vertical descents 426 and 430 may be perpendicular to the horizontal, flow portion 428. As such, the liquid flows through the solution panel assemblies 402 from the top corners 415 to the lower corners 417. As shown, the length of the horizontal, flow portion 428 substantially exceeds half the length L of the liquid panel assemblies 402. The horizontal, flow portion 428 provides liquid, such as desiccant, that may counterflow with respect to the airflow 408. Alternatively, the flow portion may be a crossflow, parallel-aligned flow, or other such flow portion, for example.

[0043] The airflow 408 that passes between the liquid panel assemblies 402 exchanges

energy with the liquid flowing through the liquid panel assemblies 402. The liquid may be a desiccant, refrigerant, or any other type of liquid that may be used to exchange energy with the airflow 408.

[0044] The energy exchange cavity 400 may include more or less liquid panel assemblies 402, membrane support assemblies 404, and air channels 406 than those shown in Figure 4. The inlet and outlet members 414 and 416 may be modular panel headers that are configured to selectively attach and detach from neighboring inlet and outlet members 414 and 416 to provide a manifold for liquid to enter into and pass out of the liquid panel assemblies 402. Sealing agents, such as gaskets, silicone gel, or the like, may be disposed between neighboring inlet members 414 and neighboring outlet members 416. At least a portion of the membrane sealingly engages the inlet and outlet members 414 and 416. The liquid panel assembly 402 formed in this manner provides a fully-sealed, stand-alone unit having openings at the inlet and outlet members 414 and 416, notably the openings 420 and 422, respectively. Accordingly, the liquid panel assembly 402 may be pre-tested for leaks and membrane holes prior to being positioned within an energy exchange cavity, for example.

[0045] Figure 5 illustrates a front view of the support frame 412 of the liquid panel assembly 400, according to an embodiment. For the sake of clarity, the membranes 418 secured to the liquid panel assembly 400 are not shown. However, it is to be understood that at least one membrane 418 is bonded to the front and back surfaces of the support frame 412. For example, the membrane 418 may be continuously bonded around the perimeter of the support frame 412, thereby creating a robust external seal.

[0046] The support frame 412 includes a main body 438 having a lower edge 440 connected to an upper edge 442 through lateral edges 444. The support frame 412 may be formed of various materials, such as injection molded plastic, metal, or a combination thereof. The support frame 412 may be integrally formed and manufactured as a single piece through a single molding process, for example. For example, the inlet and outlet members 414 and 416, respectively, may be integrally molded with the support frame 412. Optionally, the support frame 412 may be formed as separate and distinct pieces. For example, the support frame 412 may be extruded and assembled from various parts.

[0047] The inlet member 414 includes a base 446 that connects to a support inlet 448 proximate the upper corner 415. The upper corner 415 may include a channel configured to receive and retain the base 446. For example, the base 446 may fit into the channel and be securely fastened therein, such as through fasteners, adhesives, or the like. Optionally, as noted above, the base 446 may simply be integrally formed and molded with the upper corner 415. The base 446 supports and connects to an upper wall 449 through lateral walls 450. The base 446, the upper wall 449, and the lateral walls 450 define the liquid-delivery opening 420. Liquid passages (hidden from view in Figure 5) are formed through the base 446 and connect the liquid-delivery opening 420 to a liquid-reception area 452 formed at the upper corner 415 of the support frame 412.

[0048] Figure 6 illustrates an isometric top view of the inlet member 414, according to an embodiment. As shown, a lower edge 460 of the base 446 may be tapered or beveled, which allows the base 446 to be easily mated into a reciprocal channel of the support inlet 448 (shown in Figure 5). An opening 462 is formed at a terminal end of the beveled lower edge 460. The opening 462 connects to liquid passages (hidden from view in Figure 6) that connect to an opening (hidden from view in Figure 6) that connects to the liquid delivery opening 420. Accordingly, liquid may pass from the liquid delivery opening 420, out through the opening 462 of the base 446 and into the support inlet 448 of the support frame 412.

[0049] Figure 7 illustrates an internal view of the inlet member 414, according to an embodiment. As shown in Figure 7, the opening 462 is in communication with a plurality of liquid passages 470 separated by guide ribs 472. The liquid passages 470 are configured to align with liquid inlet channels of the support frame 412. While eight liquid passages 470 are shown in Figure 7, more or less liquid passages 470 may be used, depending on the number of liquid inlet channels of the support frame 412.

[0050] Referring again to Figure 5, the outlet member 416 is similarly constructed to the inlet member 414. The inlet and outlet members 414 and 416 are both liquid connection members configured to deliver and/or pass liquid to and/or from the support frame 412. Accordingly, similar to the inlet member 414, the outlet member 416 includes a base 446 that connects to a support outlet 480 of the support member 412 proximate the lower corner 417. The lower corner 417 may include a channel configured to receive and retain the base 446. For example, the base 446 may fit into the channel and be securely fastened therein, such as through fasteners, adhesives, or the like. Optionally, as noted above, the base 446 may simply be integrally formed and molded with the lower corner 417. The base 446 supports and connects to an upper wall 449 through lateral walls 450. The base 446, the upper wall 449, and the lateral walls 450 define the liquid-delivery opening 422. Liquid passages (hidden from view in Figure 5) are formed through the base 446 and connect the liquid-delivery opening 422 to a liquid-passage area 482 formed at the lower corner 417 of the support frame 412. The outlet member 416 may be constructed as shown in Figures 6 and 7.

[0051] The inlet and outlet members 414 and 416 provide panel headers that are configured to provide passageways for liquid, such as desiccant, to pass into and out of the liquid panel assembly 402. The inlet and outlet members 414 and 416 may also provide mating surfaces to neighboring panels to create a manifold to distribute liquid to all solution panels within an energy exchanger.

[0052] Figure 8 illustrates an isometric view of an area proximate the upper corner 415 of the support frame 412 of the liquid panel assembly 402. Referring to Figures 5 and 8, the support frame 412 includes vertical inlet channels 490 connected to vertical outlet channels 492 through horizontal flow passages 494. As shown, the support frame 412 may include eight vertical inlet channels 490 and eight vertical outlet channels 492. However, the support frame 412 may include more or less inlet and outlet channels 490 and 492 than those shown. Each inlet channel 490 may connect to five horizontal flow passages 494. For example, the

innermost inlet channel 490a connects to the top five horizontal flow passages 494a. Similarly, the inlet channel 490b connects to the five horizontal flow passages 494 below the top five horizontal flow passages 494a. Similarly, the top five flow passages 494a connect to an outermost vertical outlet channel 492a. Accordingly, the horizontal flow passages 494 may be staggered in sets of five with respect to the support frame 412. For example, inlet ends 498 of the horizontal flow passages 494a are farther away from the lateral edge 444a of the support frame 412 than the inlet ends 498 of the set of horizontal flow passages 494 immediately below the set of horizontal flow passages 494a. However, outlet ends 500 of the horizontal flow passages 494a are closer to the lateral edge 444b of the support frame 412 than the outlet ends 500 of the set of horizontal flow passages 494 immediately below the set of horizontal flow passages 494a. Further, the length of the inlet channel 490a is shorter than the length of the inlet channel 490b adjacent the inlet channel 490a. The length of the inlet channel 490b is longer in order to connect to the set of five horizontal flow passages 494 underneath the set of five horizontal flow passages 494a. Conversely, the length of the vertical outlet channel 492a is longer than the length of the vertical outlet channel 492b immediately adjacent the vertical distribution channel 492a.

[0053] The vertical inlet and outlet channels 490 and 492, respectively, provide continuous flow alignment vanes. Each channel 490 and 492 may be an isolated duct that allows the pressure of liquid in neighboring channels 490 and 492 to vary in order to evenly split the flow of liquid among the channels 490 and 492. As noted, each vertical distribution and passage channel 490 and 492 may feed a single horizontal flow passage 494, or a set or bank of horizontal flow passages 494. The membrane 418 (shown in Figure 4) may also be bonded to internal edge surfaces of the support frame 412 to separate each vertical channel 490 and 492 from one another, as well as to separate each horizontal flow passage 494 from one another. Therefore, each fluid circuit, which includes an inlet channel 490, one or more flow passages 494, and an outlet channel 492, may be a separate, sealed duct.

[0054] Each of the inlet and outlet channels 490 and 492 may provide a flow alignment vane configured to direct liquid to flow along a particular path. The inlet and outlet channels 490 and 492 may be configured to provide support to the membrane. The inlet and outlet channels may be configured to provide a sealing surface for at least a portion of the membrane.

[0055] As shown in Figures 5 and 6, the horizontal flow passages 494 are grouped in sets of five, which are staggered with respect to one another. The sets of horizontal flow passages 494 are staggered so that the overall length of each horizontal flow passage 494 is the same. Indeed, the total length of each liquid circuit, which includes a vertical inlet channel 490 that connects to a horizontal flow passage 494, which in turn connects to a vertical outlet channel 492, is the same due to the staggered nature of the sets of horizontal flow passages 494 and the different lengths of each of the vertical inlet channels 490 and the vertical outlet channels 492. The total vertical height H of a liquid circuit is the length of a vertical inlet channel 490 plus the length of a vertical outlet channel 492 that connects to the vertical inlet channel 490 through a horizontal flow passage 494. The vertical inlet channel 490a is the shortest, while the vertical outlet channel 492a (which connects to the inlet channel 490a through the fluid

passages 494a) is the longest. Conversely, the vertical inlet channel 490n is the longest, while the vertical outlet channel 492n (which connects to the inlet channel 490n through the fluid passages 494n) is the shortest. Further, the length of the vertical inlet channel 490a may equal the length of the vertical outlet channel 492n, while the length of the vertical inlet channel 490n may equal the length of the vertical outlet channel 492a. In short, the total vertical lengths for each liquid circuit may sum to H. Moreover, the total length of each liquid circuit, which includes a vertical inlet channel 490 that connects to a vertical outlet channel 492 through a horizontal fluid passage 494, may be equal.

[0056] While particular inlet and outlet channels 490 and 492, respectively, are each shown connecting to a set of five horizontal fluid passages 494, the inlet and outlet channels 490 and 492, respectively, may connect to more or less than five horizontal fluid passages 494. For example, the sets of horizontal fluid passages 494 may be two, three, six, seven, and the like. Further, each distribution and passage channel 490 and 492, respectively, may alternatively connect to only one horizontal fluid passage 494.

[0057] The liquid circuits are of equal length in order to provide for even distribution of liquid flow through the liquid panel assembly 402. The liquid panel assembly 402 is configured to operate at low pressure. That is, the liquid panel assembly 402 provides a low pressure assembly. The liquid that flows through the liquid panel assembly 402 has a particular weight and viscosity. For example, a desiccant is a dense fluid. The weight of the liquid creates fluid pressure. As the liquid flows from the top of the liquid panel assembly 402 to the bottom, the pressure from the weight of the liquid builds. As the liquid moves through the liquid panel assembly 402, the pressure is reduced through friction, for example. For example, the faster the speed of the liquid within a liquid circuit, the greater the friction between the liquid and walls of channels and passages that define the liquid circuit. Therefore, increasing the speed of the liquid, such as through pumping, increases the frictional force. Embodiments of the present disclosure provide a liquid panel assembly that balances the loss of pressure from friction with the pressure of the weight of the liquid.

[0058] The friction head loss, h_f , of a fluid flowing in a channel of length L is given by the following:

$$\frac{h_f}{L} = \frac{C\mu V}{2g\rho D_h^2}$$

where C is a coefficient that depends on the duct geometry (and may also be used to represent the friction of porous material in the duct), μ is the molecular viscosity of the fluid, V is the bulk speed of the fluid in the duct, g is the acceleration due to gravity, ρ is the density of the fluid, and D_h is the hydraulic diameter of the duct. The friction head loss may be synonymous with pressure drop ("head" refers to the height of a column of fluid that would produce the pressure), that is, $\Delta P = -\rho gh_f$.

[0059] Embodiments of the present disclosure provide a liquid panel assembly in which friction head loss may be the same or approximately the same as a drop in vertical elevation of the fluid as it flows downward in the channels, due to the gain in static pressure, which is given by

$\Delta P = \rho g \Delta z$, where Δz is the drop in vertical elevation (in the direction of gravity). Therefore, adding the two pressure changes together gives $\Delta P_{net} = \rho g(\Delta z - h_f)$. A closely balanced flow with low pressure would have $\Delta z \approx h_f$. Embodiments of the present disclosure provide pressure balancing channels at the ends of the panel that are oriented vertically, therefore, $\Delta z = L$. As such, the following may be consulted when selecting the size, shape, orientation, and the like of the fluid circuits:

$$\frac{h_f}{L} = \frac{C\mu V}{2g\rho D_h^2} \approx 1$$

[0060] However, complete balance as shown in the above equation is not necessarily required. Instead, the gauge pressure may be kept low enough to meet structural limitations of the membrane and support design (keeping membrane strain and stress within acceptable limits).

[0061] In an example, the weight of the liquid produces pressure in the vertical inlet and outlet channels 490 and 492, respectively. However, it has been found that increasing the number of horizontal fluid passages 494 connecting to particular inlet and outlet channels 490 and 492 increases the rate of fluid flow within the vertical inlet and outlet channels 490 and 492, respectively. Fluid velocity is directly proportional to friction. Thus, with increased fluid velocity, friction increases. The friction diminishes the overall pressure of the liquid within the liquid panel assembly 402. Therefore, by increasing the friction of the fluid with the walls of the channels and passages of the liquid panel assembly 402, the pressure is reduced. As an example, it has been found that connecting single vertical inlet and outlet channels 490 and 492, respectively, to sets of four or five horizontal fluid passages 494 may substantially or completely offset the pressure caused by the weight of a desiccant. Because different liquids have different densities and weights, the liquid panel assembly 402 may be configured to account for the differences in densities and weights. For example, the sets of horizontal flow passages 494 may be smaller, such as set of 2 or 3, for lighter liquids, than for heavier liquids. Therefore, a number of flow passages 494 within a set of multiple flow passages 494 connected to individual channels 490 and 492 may be based on and/or determined by a weight of the liquid that is configured to flow through fluid circuits that include the sets of liquid passages and channels 490 and 492. In general, embodiments of the present disclosure are configured to offset hydrostatic pressure gain of the liquid with friction pressure loss of the flowing liquid within one or more fluid circuits to minimize or eliminate pressure within a liquid panel assembly.

[0062] Additionally, the hydraulic diameters of the inlet and outlet channels 490 and 492, as well as the hydraulic diameters of the horizontal fluid passages 494, may be adjusted to balance liquid hydrostatic pressure with friction. For example, the hydraulic diameter of each channel or passage may be directly proportional to the velocity of liquid flowing therethrough. Thus, decreasing the hydraulic diameter of the channel or passage leads to an increased velocity of pumped liquid therethrough. As noted, increasing liquid velocity increases friction, which reduces the net pressure. Therefore, the hydraulic diameter of the channels 490 and 492 may be based on and/or determined, in part, by a weight of the liquid that is configured to

flow through fluid circuits that include the channels 490 and 492. In addition to the number of horizontal flow passages 494 in a set that connect to individual vertical inlet and outlet channels 490 and 492, respectively, the hydraulic diameter of the channels 490 and 492, as well as the flow passages 494 may be sized and shaped to generate a desired friction with respect to a particular liquid.

[0063] Thus, the liquid panel assembly 402 includes liquid circuits that are configured to balance the force of liquid hydrostatic pressure and friction by adjusting the number of horizontal flow passages 494 that connect to the vertical inlet and outlet channels 490 and 492, respectively, and/or the hydraulic diameter of the channels and/or passages, in order to reduce the net pressure within the liquid panel assembly 402.

[0064] The hydraulic diameters of the horizontal fluid passages 494 may be relatively wide compared to the vertical inlet and outlet channels 490 and 492, respectively. As such, the friction in relation to the liquid in the horizontal fluid passages 494 may be relatively small compared to the vertical inlet and outlet channels 490 and 492, respectively. The pressure drop in the horizontal fluid passages 494 may be relatively small. Because less friction in the horizontal flow passages 494 may be desired, the hydraulic diameters of the flow passages 494 may be wider than the hydraulic diameters of the vertical inlet and outlet channels 490 and 492, respectively. Therefore, the balancing of liquid hydrostatic pressure and friction may be achieved through the velocity of liquid through the vertical inlet and/or outlet channels 490 and 492, respectively, which may be controlled through the number of horizontal flow passages 494 connecting to each channel 490 and 492, and/or the hydraulic diameters of the channels 490 and 492.

[0065] Referring to Figures 4, 5, and 8, the lengths of the horizontal flow passages 494 may be substantially longer than half the length L of the support frame 412. Indeed, the lengths of the horizontal flow passages may be almost as long as the length L of the support frame 412. For example, the horizontal flow passages 494 may be the length of the support frame 412 minus the horizontal area occupied by the inlet and outlet channels 490 and 492, respectively. Accordingly, each fluid circuit may have a substantial length along a horizontal orientation. The linear, horizontal distances of the horizontal flow passages 494 increase the efficiency of energy exchange between the liquid flowing therethrough, and the airflow on either side of the membranes of the solution panel assemblies 402. As shown in Figure 5, the horizontal flow passages 494 increase the flow of liquid in the horizontal direction so that the direction of liquid flow D_L is counter to the direction of airflow D_A . It has been found that increasing the distance of counterflow between the liquid in the fluid circuits and the airflow increases the efficiency of energy exchange therebetween. A counterflow arrangement of the air and liquid streams provides an efficient and highly effective energy exchanger. The horizontal flow passages 494 maximize the counterflow area, and allow the liquid to distribute evenly. As noted above, however, the flow passages 494 may be alternatively be configured to provide crossflow, parallel-aligned flow, or other such flow.

[0066] Figure 9 illustrates a chart of fluid pressure levels within a liquid panel assembly 402,

according to an embodiment. As shown in Figure 9, the pressure level of liquid through an inlet length L_i (over the length of the vertical inlet channel 490) increases until the liquid passes into the horizontal flow passage 494, through which the pressure level L_C remains constant. The pressure of the liquid in the vertical outlet channel 492 increases. However, as shown in Figure 9, the friction of the liquid with respect to the liquid panel assembly 402 offsets the pressure levels of the liquid. As such, the pressure force 902 of the liquid is offset by the frictional force 904, thereby yielding a neutral pressure 906 within the liquid panel assembly 402. The vertical inlet and outlet channels 490 and 492, respectively, may be considered friction control members that are used to balance the pressure within the liquid panel assembly 402.

[0067] Figure 10 illustrates a front view of a support frame 1000 of a liquid panel assembly 1002, according to an embodiment. The support frame 1000 may include end sections 1004 and 1006 and an intermediate body 1008. The end section 1004 may provide vertical inlet channels 1010, while the end section 1006 may provide vertical outlet channels 1012, or vice versa. The intermediate body 1008 may provide horizontal flow passages 1014. The intermediate body 1008 includes flow passage sets 1016-1030 that are staggered and/or offset with one another with respect to a vertical axis 1040 of the intermediate body 1008. Each of the end sections 1004 and 1006, as well as the intermediate body 1008 may be formed from extruded parts and assembled together, such as through fasteners, bonding, and the like. The end sections 1004, 1006, and the intermediate body 1008 may be formed by extruding a flat sheet of plastic or metal, and then embossing the channel shapes using grooved rollers, for example.

[0068] Alternatively, any of the liquid panel assemblies described above may be formed through injection molding either as separate sub-parts that are later bonded together, or as a single, unitary piece. Injection molding the liquid panel assembly as a single piece, for example, eliminates the potential for joint failure or leakage at bonded seams.

[0069] Figure 11 illustrates an isometric top view of liquid inlet channels 1100 formed in a support frame 1102, according to an embodiment. As shown, the inlet channels 1100 may be grooves formed between ridges 1104 in the support frame 1102. The liquid outlet channels may be formed in a similar manner.

[0070] Figure 12 illustrates an isometric top view of liquid inlet channels 1200 formed in a support frame 1202, according to an embodiment. In this embodiment, the inlet channels 1200 may be cut completely through the support frame 1202, thereby forming a planar channel through the support frame 1202. The liquid outlet channels may be formed in a similar manner.

[0071] Referring to Figures 4-12, as explained above, the inlet channels and the outlet channels of the support frame may be vertical and linear, while the flow passages may be horizontal and linear. It has been found that the linear vertical and horizontal configuration of each liquid circuit provides for efficient pressure balancing within the solution panel assemblies. However, the liquid circuits may be various other shapes and sizes. As discussed above, a liquid circuit may include a vertical inlet channel, one or a set of horizontal flow passages, and

a vertical outlet channel.

[0072] Figure 13 illustrates a simplified view of a liquid circuit 1300, according to an embodiment. The liquid circuit 1300 includes a vertical inlet channel 1302 connected to a vertical outlet channel 1306 through a flow passage 1304. The flow passage 1304 may include a first horizontal portion 1308 connected to a second horizontal portion 1310 through a vertical drop 1312. The vertical drop 1312 may be configured to balance liquid hydrostatic pressure, similar to the vertical inlet and outlet channels, as explained above.

[0073] Figure 14 illustrates a simplified view of a liquid circuit 1400, according to an embodiment. The liquid circuit 1400 includes a vertical inlet channel 1402 connected to a vertical outlet channel 1404 through a flow passage 1406. The flow passage 1406 may include a first horizontal portion 1408 connected to a second horizontal portion 1410 through a vertical drop 1411. The liquid flow passage 1406 may also include a third horizontal portion 1412 connected to the second horizontal portion 1410 through a vertical drop 1413. The vertical drops 1411 and 1413 may be configured to balance liquid hydrostatic pressure, similar to the vertical inlet and outlet channels, as explained above. The flow passage 1406 may include more vertical drops than those shown.

[0074] Figure 15 illustrates a simplified view of a liquid circuit 1500, according to an embodiment. In this embodiment, a vertical inlet channel 1502 is connected to a vertical outlet channel 1504 through a flow passage 1506, which may be non-linear. When non-linear, the flow passage 1506 may include offsetting portions such that a trough 1508 is offset by a peak 1510. That is, the depth of the trough 1508 may be the same absolute distance as the height of the peak 1510.

[0075] Referring to Figures 13-15, for example, the liquid circuits may or may not include horizontal passages. For example, the liquid circuits may include vertical flow channels connected to one another through various passages. Pressure balancing may occur directly in the vertical flow channels. Additionally, the liquid circuits may be angled with respect to horizontal and vertical orientations.

[0076] Figure 16 illustrates an isometric view of horizontal liquid panel assemblies connected to combined inlet channels and combined outlet channels 1600 according to an embodiment of the present disclosure. One or more panel assemblies 1602 may be stacked horizontally to form a panel stack 1640. The panel assemblies 1602 may be separated by membrane support assemblies, such as described with respect to Figure 4. The panel assemblies 1602 may be fluidly connected proximate the left corner 1606 to an inlet channel 1608. The inlet channel 1608 may be fluidly connected to an inlet header 1610. The panel assemblies are fluidly connected proximate the right corner 1616 to an outlet channel 1618. The outlet channel 1618 is fluidly connected to an outlet header 1620. Liquid, such as a desiccant, flows from the inlet header 1610 into the inlet channel 1608 and into the panel assembly 1602 at the corner 1606. The liquid passes through the panel assembly 1602 by traveling along a liquid path, such as described with respect to Figure 4. The liquid exits the panel assembly 1602 at the corner

1616 and flows into the outlet channel 1618 and into the outlet header 1620. The inlet channel 1608 may provide a pressure balancing function for low pressure supply to every panel assembly 1602 in the panel stack 1640. The outlet channel 1618 may provide a pressure balancing effect for low back pressure to every panel assembly 1602 in the panel stack 1640.

[0077] Figure 17 illustrates an isometric view of horizontal liquid panel assemblies connected to individual inlet channels and individual outlet channels 1700 according to an embodiment of the present disclosure. One or more panel assemblies 1702 may be stacked horizontally to form a panel stack 1740. The panel assemblies 1702 may be separated by membrane support assemblies, such as described with respect to Figure 4. The panel assemblies 1702 may be fluidly connected proximate the right corner 1706 to an inlet channel 1708. The inlet channel 1708 may be fluidly connected to an inlet header 1710. The panel assemblies may be fluidly connected proximate the left corner 1716 to an outlet channel 1718. The outlet channel 1718 may be fluidly connected to an outlet header 1720. Liquid, such as a desiccant, flows flow from the inlet header 1710 into the inlet channel 1708 and into the panel assembly 1702 at the corner 1706. The liquid passes through the panel assembly 1702 by traveling along a liquid path, such as described with respect to Figure 4. The liquid exits the panel assembly 1702 at the corner 1716 and flows into the outlet channel 1718 and into the outlet header 1720. The inlet channel 1708 may provide a pressure balancing function for low pressure supply to every panel assembly 1702 in the panel stack 1740. The outlet channel 1718 may provide a pressure balancing effect for low back pressure to every panel assembly 1702 in the panel stack 1740.

[0078] Figure 18 illustrates an isometric view of stacked horizontal liquid panel assemblies connected to inlet headers 1800 according to an embodiment of the present disclosure. One or more panel assemblies 1802 may be stacked horizontally to form a panel stack 1850. One or more panel stacks 1850 may be stacked to form a stack of panel stacks 1840. The panel assemblies 1802 may be separated by membrane support assemblies, such as described with respect to Figure 4. All panel assemblies 1802 in one panel stack 1850 may be fluidly connected proximate the right corner 1806 to one inlet header 1808. The inlet header 1808 may be fluidly connected to an inlet channel 1810. The panel assemblies may be fluidly connected proximate the left corner 1816 to an outlet header 1818. The outlet header 1818 may be fluidly connected to an outlet channel 1820. Liquid, such as a desiccant, flows to flow along a fluid path 1860 from the inlet channel 1810 into the inlet header 1808 and into each panel assembly 1802 in the panel stack 1850 at the corner 1806. The liquid passes through the panel assemblies 1802 by traveling along a liquid path, such as described with respect to Figure 4. The liquid exits the panel assemblies 1802 at the corner 1816 and flows into the outlet header 1818 and into the outlet channel 1820. The inlet channel 1810 may provide a pressure balancing function for low pressure supply to every panel stack 1850 in the stack of panel stacks 1840. The outlet channel 1820 may provide a pressure balancing effect for low back pressure to every panel stack 1850 in the stack of panel stacks 1840.

[0079] Figure 19 illustrates an isometric view of stacked horizontal liquid panel assemblies with external pressure balancing 1900 according to an embodiment of the present disclosure. One

or more panel assemblies 1902 may be stacked horizontally to form a panel stack 1950. One or more panel stacks 1950 may be stacked to form a stack of panel stacks 1940. The panel assemblies 1902 may be separated by membrane support assemblies such as described with respect to Figure 4. All panel assemblies 1902 in one panel stack 1950 may be fluidly connected proximate the right corner 1906 to one inlet header 1908. The inlet header 1908 may be fluidly connected to a pressure control device such as an inline regulating valve, a pressure regulating pump or other such device capable of supplying fluid to all inlet headers at the same pressure. The panel assemblies may be fluidly connected proximate the left corner 1916 to an outlet header 1918. The outlet header 1918 may be fluidly connected to a pressure control device such as an inline regulating valve, a pressure regulating pump or other such device capable of retrieving fluid from all outlet headers at the same pressure. Fluid, such as a desiccant, flows along a fluid path 1960 from the pressure control device into the inlet header 1908 and into each panel assembly 1902 in the panel stack 1950 at the corner 1906. The liquid passes through the panel assemblies 1902 by traveling along a liquid path, such as described with respect to Figure 4. The liquid exits the panel assemblies 1902 at the corner 1916 and flows into the outlet header 1918 and into the pressure control device. The inlet pressure control device may provide low pressure supply to every panel stack 1950 in the stack of panel stacks 1940. The outlet pressure control device may provide low back pressure to every panel stack 1950 in the stack of panel stacks 1940.

[0080] Embodiments of the present disclosure may be used with various types of energy exchangers, such as liquid-to-air or liquid-to-liquid membrane energy exchangers.

[0081] Embodiments of the present disclosure provide liquid panel assemblies that are configured to balance internal liquid hydrostatic pressure and frictional forces. As such, the total pressure within the liquid panel assemblies may be reduced, negated or otherwise neutralized. Thus, membrane bulge is substantially reduced or eliminated, which reduces the potential for leaks and membrane creep.

[0082] Embodiments of the present disclosure provide a liquid panel assembly divided into a plurality of separate liquid circuits, each of equal length and friction, so that liquid divides itself evenly among the liquid circuits and the flow through the liquid circuits is uniform. The fluid circuits promote uniform flow distribution across the liquid panel assembly, thereby providing efficient operation and performance.

[0083] Embodiments of the present disclosure provide a liquid panel assembly that creates pathways for controlled, uniform, flow distribution (such as counterflow distribution) of liquid, such as desiccant, over an internal membrane area. Further, the liquid panel assembly provides low operating pressure by offsetting the static pressure gain and friction pressure loss as the liquid moves through the liquid circuits. The vertical flow of liquid may be confined to small high speed channels, thereby reducing or eliminating the potential for buoyancy-driven mal-distribution of liquid. The flow passages may be open (no filler wick or mesh), thereby allowing for good contact of the liquid and membrane, and low friction loss.

[0084] Embodiments of the present disclosure are not restricted to energy exchangers. Instead, embodiments of the present disclosure may be used with respect to any liquid panel frame that exchanges heat and/or mass through a membrane, and where liquid pressure and flow distribution are controlled. For example, the liquid panel assemblies described above may be used with desalination systems, water purification systems, evaporative cooling systems, systems configured to transfer heat/mass between a liquid and a gas through a membrane, systems configured to transfer heat/mass between two liquid streams through a membrane, and the like.

[0085] While various spatial and directional terms, such as top, bottom, lower, mid, lateral, horizontal, vertical, front and the like may be used to describe embodiments of the present disclosure, it is understood that such terms are merely used with respect to the orientations shown in the drawings. The orientations may be inverted, rotated, or otherwise changed, such that an upper portion is a lower portion, and vice versa, horizontal becomes vertical, and the like.

[0086] It is to be understood that the above description is intended to be illustrative, and not restrictive. For example, the above-described embodiments (and/or aspects thereof) may be used in combination with each other. In addition, many modifications may be made to adapt a particular situation or material to the teachings of the various embodiments of the disclosure without departing from their scope. While the dimensions and types of materials described herein are intended to define the parameters of the various embodiments of the disclosure, the embodiments are by no means limiting and are exemplary embodiments. Many other embodiments will be apparent to those of skill in the art upon reviewing the above description. The scope of the various embodiments of the disclosure should, therefore, be determined with reference to the appended claims, along with the full scope of equivalents to which such claims are entitled. In the appended claims, the terms "including" and "in which" are used as the plain-English equivalents of the respective terms "comprising" and "wherein." Moreover, in the following claims, the terms "first," "second," and "third," etc. are used merely as labels, and are not intended to impose numerical requirements on their objects. Further, the limitations of the following claims are not written in means-plus-function format and are not intended to be interpreted based on 35 U.S.C. § 112, sixth paragraph, unless and until such claim limitations expressly use the phrase "means for" followed by a statement of function void of further structure.

[0087] This written description uses examples to disclose the various embodiments of the disclosure, including the best mode, and also to enable any person skilled in the art to practice the various embodiments of the disclosure, including making and using any devices or systems and performing any incorporated methods. The patentable scope of the various embodiments of the disclosure is defined by the claims, and may include other examples that occur to those skilled in the art. Such other examples are intended to be within the scope of the claims if the examples have structural elements that do not differ from the literal language of the claims, or if the examples include equivalent structural elements with insubstantial differences from the literal languages of the claims.

[0088] According to further embodiments of the invention, there is provided:

1. 1. A liquid panel assembly comprising:

a support frame having one or more fluid circuits, wherein each of the one or more fluid circuits comprises an inlet channel connected to an outlet channel through one or more flow passages; and

at least one membrane secured to the support frame, wherein a liquid is configured to flow through the one or more fluid circuits and contact interior surfaces of the at least one membrane, and wherein the one or more fluid circuits are configured to at least partially offset hydrostatic pressure gain with friction pressure loss of the liquid that flows within the one or more fluid circuits to reduce pressure within the liquid panel assembly.
2. 2. The liquid panel assembly of clause 1, wherein the one or more flow passages comprises one or more counterflow passages.
3. 3. The liquid panel assembly of clause 1, wherein a shape, porosity, or hydraulic diameter of one or both of the inlet and outlet channels is determined by a weight, viscosity, or flow speed of the liquid that is configured to flow through the one or more fluid circuits.
4. 4. The liquid panel assembly of clause 1, wherein the inlet channel is disposed at an upper corner of the support frame, and the outlet channel is disposed at a lower corner of the support frame.
5. 5. The liquid panel assembly of clause 4, wherein the upper corner is diagonally located from the lower corner.
6. 6. The liquid panel assembly of clause 1, wherein the inlet and outlet channels are vertical and the one or more flow passages are horizontal.
7. 7. The liquid panel assembly of clause 5, wherein a horizontal length of the one or more flow passages exceeds half a total horizontal length of the support frame.
8. 8. The liquid panel assembly of clause 1, wherein the one or more flow passages comprises a set of a plurality of flow passages connected to the inlet channel and the outlet channel.
9. 9. The liquid panel assembly of clause 8, wherein a number of flow passages within the set of a plurality of flow passages is determined by a weight of the liquid that is configured to flow through the one or more fluid circuits.
10. 10. The liquid panel assembly of clause 1, wherein the one or more fluid circuits comprises a plurality of fluid circuits.
11. 11. The liquid panel assembly of clause 10, wherein lengths of each of the one or more fluid circuits are equal.
12. 12. The liquid panel assembly of clause 10, wherein the plurality of fluid circuits comprises: a first set of a plurality of flow passages connected to a first inlet channel and a first outlet channel; and a second set of a plurality of flow passages connected to a second inlet channel and a second outlet channel.
13. 13. The liquid panel assembly of clause 12, wherein the first set of a plurality of flow passages is staggered with respect to the second set of a plurality of flow passages.

14. 14. The liquid panel assembly of clause 1, wherein the support frame and the at least one membrane are configured to be vertically oriented within an energy exchange cavity of an energy exchanger.
15. 15. The liquid panel assembly of clause 1, further comprising inlet and outlet members connected to the at least one fluid circuit.
16. 16. The liquid panel assembly of clause 15, wherein the inlet and outlet members comprise a liquid delivery channel and a liquid passage channel, respectively.
17. 17. The liquid panel assembly of clause 16, wherein the inlet member is configured to modularly engage another inlet member, and wherein the outlet member is configured to modularly engage another outlet member.
18. 18. The liquid panel assembly of clause 1, wherein at least a portion of the at least one membrane sealingly engages the inlet and outlet members.
19. 19. The liquid panel assembly of clause 1, wherein each of the inlet and outlet channels provides a flow alignment vane configured to direct the liquid to flow along a particular path, wherein the inlet and outlet channels are configured to provide support to the at least one membrane, and wherein the inlet and outlet channels are configured to provide a sealing surface for at least a portion of the at least one membrane.
20. 20. The liquid panel assembly of clause 1, wherein the inlet and outlet channels are configured to maximize a length of the one or more flow passages.
21. 21. The liquid panel assembly of clause 1, wherein the at least one membrane is continuously bonded around a perimeter of the support frame.
22. 22. The liquid panel assembly of clause 1, wherein the one or more fluid circuits are configured to provide uniform liquid flow distribution across the liquid panel assembly.
23. 23. The liquid panel assembly of clause 1, wherein the one or more fluid circuits are configured to substantially offset the hydrostatic pressure gain with the friction pressure loss of the liquid that flows within the one or more fluid circuits to reduce pressure within the liquid panel assembly.
24. 24. An energy exchange system comprising:
 - a plurality of air channels configured to allow air to pass therethrough;
 - a plurality of liquid panel assemblies alternately spaced with the plurality of air channels,
 - wherein each of the plurality of liquid panel assemblies comprises:
 - a support frame having one or more fluid circuits, wherein each of the one or more fluid circuits comprises an inlet channel connected to an outlet channel through one or more flow passages; and
 - at least one membrane secured to the support frame, wherein a liquid is configured to flow through the one or more fluid circuits and contact interior surfaces of the at least one membrane, and wherein the one or more fluid circuits are configured to at least partially offset hydrostatic pressure gain with friction pressure loss of the liquid that flows within the one or more fluid circuits to reduce pressure within the liquid panel assembly.
25. 25. The energy exchange system of clause 24, wherein the one or more flow passages

comprise one or more counterflow passages.

26. 26. The energy exchange system of clause 24, further comprising a plurality of membrane support assemblies disposed within the plurality of air channels.
27. 27. The energy exchange system of clause 24, wherein a shape, porosity, or hydraulic diameter of one or both of the inlet and outlet channels is determined by a weight, viscosity, or flow speed of the liquid that is configured to flow through the one or more fluid circuits.
28. 28. The energy exchange system of clause 24, wherein the inlet channel is disposed at an upper corner of the support frame, and the outlet channel is disposed at a lower corner of the support frame.
29. 29. The energy exchange system of clause 28, wherein the upper corner is diagonally located from the lower corner.
30. 30. The energy exchange system of clause 24, wherein the inlet and outlet channels are vertical and the one or more flow passages are horizontal.
31. 31. The energy exchange system of clause 24, wherein a horizontal length of the one or more flow passages exceeds half a total horizontal length of the support frame.
32. 32. The energy exchange system of clause 24, wherein the one or more flow passages comprises a set of a plurality of flow passages connected to the inlet channel and the outlet channel.
33. 33. The energy exchange system of clause 32, wherein a number of flow passages within the set of a plurality of flow passages is determined by a weight and/or viscosity of the liquid that is configured to flow through the one or more fluid circuits.
34. 34. The energy exchange system of clause 24, wherein the one or more fluid circuits comprises a plurality of fluid circuits.
35. 35. The energy exchange system of clause 34, wherein lengths of each of the one or more fluid circuits are equal.
36. 36. The energy exchange system of clause 34, wherein the plurality of fluid circuits comprises:

a first set of a plurality of flow passages connected to a first inlet channel and a first outlet channel; and

a second set of a plurality of flow passages connected to a second inlet channel and a second outlet channel.
37. 37. The energy exchange system of clause 36, wherein the first set of a plurality of flow passages is staggered with respect to the second set of a plurality of flow passages.
38. 38. The energy exchange system of clause 24, wherein the support frame and the at least one membrane are configured to be vertically oriented within an energy exchange cavity of the energy exchanger.
39. 39. The energy exchange system of clause 24, further comprising inlet and outlet members connected to the at least one fluid circuit.
40. 40. The energy exchange system of clause 24, wherein the inlet and outlet members comprise a liquid delivery channel and a liquid passage channel, respectively.
41. 41. The energy exchange system of clause 40, wherein the inlet member is configured

to modularly engage another inlet member, and wherein the outlet member is configured to modularly engage another outlet member.

42. 42. The energy exchange system of clause 24, wherein air within the plurality of air channels is configured to counterflow with respect to the liquid within the one or more flow passages.
43. 43. The energy exchange system of clause 24, wherein at least a portion of the at least one membrane sealingly engages the inlet and outlet members.
44. 44. The energy exchange system of clause 24, wherein each of the inlet and outlet channels provides a flow alignment vane configured to direct the liquid to flow along a particular path, wherein the inlet and outlet channels are configured to provide support to the at least one membrane, and wherein the inlet and outlet channels are configured to provide a sealing surface for at least a portion of the at least one membrane.
45. 45. The energy exchange system of clause 24, wherein the inlet and outlet channels are configured to maximize a length of the one or more flow passages.
46. 46. The energy exchange system of clause 24, wherein the at least one membrane is continuously bonded around a perimeter of the support frame.
47. 47. The energy exchange system of clause 24, wherein the one or more fluid circuits are configured to substantially offset the hydrostatic pressure gain with the friction pressure loss of the liquid that flows within the one or more fluid circuits to reduce pressure within the liquid panel assembly.

REFERENCES CITED IN THE DESCRIPTION

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Patentkrav**1.** Væskepanelsamling (402) omfattende:

5 ene eller flere fluidkredsløb omfatter en indløbskanal (490) forbundet med en udløbskanal (492) gennem en eller flere strømningspassager (494); og mindst en membran (418) fastgjort på støtterammen (412), hvor en væske er konfigureret til at strømme gennem det ene eller flere fluidkredsløb og komme i kontakt med indvendige overflader på den mindst ene membran (418), og hvor det ene eller flere fluidkredsløb er konfigureret til mindst delvist at afbalancere hydrostatisk trykstigning med friktionstryktab af væsken, der strømmer inden i det ene eller flere fluidkredsløb for at reducere tryk inden i væskepanelsamlingen (402),

kendetegnet ved, at hver af indløbs- og udløbskanalerne (490, 492)

15 tilvejebringer en strømningsstilpasningsvinge konfigureret til at lede væsken til at strømme langs en bestemt bane, hvor indløbs- og udløbskanalerne (490, 492) er konfigureret til at tilvejebringe støtte til den mindst ene membran (418), og hvor indløbs- og udløbskanalerne (490, 492) er konfigureret til at tilvejebringe en tætningsoverflade for mindst en del af den mindst ene membran (418).

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2. Væskepanelsamling ifølge krav 1, hvor den ene eller flere strømningspassager (494) omfatter en eller flere modstrømsplassager.

3. Væskepanelsamling ifølge et hvilket som helst af kravene 1-2, hvor en form, porøsitet eller hydraulisk diameter af en af eller begge indløbs- og udløbskanalerne (490, 492) bestemmes ved en vægt, viskositet eller strømningshastighed af væsken, der er konfigureret til at strømme gennem det ene eller flere fluidkredsløb.

30 **4.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-3, hvor indløbskanalen (490) er anbragt i et øverste hjørne (415) af støtterammen (412), og udløbskanalen (492) er anbragt i et nederste hjørne (417) af støtterammen,

- 5.** Væskepanelsamling ifølge krav 4, hvor det øverste hjørne (415) er placeret diagonalt i forhold til det nederste hjørne (417).
- 6.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-5, hvor indløbs- og udløbskanalerne (490, 492) er vertikale, og den ene eller flere strømningspassager er horisontale.
- 7.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-7, hvor en horisontal længde af den ene eller flere strømningspassager (494) overstiger halvdelen af en samlet horisontal længde af støtterammen (412).
- 8.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-7, hvor den ene eller flere strømningspassager (494) omfatter et sæt af en flerhed af strømningspassager (494n) forbundet med indløbskanalen (490) og udløbskanalen (492).
- 9.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-8, hvor det ene eller flere fluidkredsløb omfatter en flerhed af fluidkredsløb.
- 10.** Væskepanelsamling ifølge krav 9, hvor længderne af hver af det ene eller flere fluidkredsløb er ens.
- 11.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-10, hvor flerheden af fluidkredsløb omfatter:
- et første sæt af en flerhed af strømningspassager forbundet med en første indløbskanal og en første udløbskanal; og
 - et andet sæt af en flerhed af strømningspassager forbundet med en anden indløbskanal og en anden udløbskanal.
- 12.** Væskepanelsamling ifølge krav 11, hvor det første sæt af en flerhed af strømningspassager er forskudt i forhold til det andet sæt af en flerhed af strømningspassager.
- 13.** Væskepanelsamling ifølge et hvilket som helst af kravene 1-12, endvidere omfattende indløbs- og udløbselementer (414, 416) forbundet med det mindst

ene fluidkredsløb, hvor indløbs- og udløbselementerne (414, 416) omfatter henholdsvis en væsketilførelseskanal og en væskepassagekanal, hvor hvert af indløbselementerne (414) er konfigureret til modulvist at gribe ind i et andet af indløbselementerne, og hvor hvert af udløbselementerne (416) er konfigureret til modulvist at gribe ind i et andet af udløbselementerne.

14. Væskepanelsamling (402) omfattende:

en støtteramme (412) med et eller flere fluidkredsløb, hvor hvert af det ene eller flere fluidkredsløb omfatter en indløbskanal (490) forbundet med en udløbsskanal (492) gennem en eller flere strømningspassager (494); og mindst en membran (418) fastgjort på støtterammen (412), hvor en væske er konfigureret til at strømme gennem det ene eller flere fluidkredsløb og komme i kontakt med indvendige overflader på den mindst ene membran (418), og hvor det ene eller flere fluidkredsløb er konfigureret til mindst delvist at afbalancere hydrostatisk trykstigning med friktionstryktab af væsken, der strømmer inden i det ene eller flere fluidkredsløb for at reducere tryk inden i væskepanelsamlingen (402), **kendetegnet ved, at** flerheden af fluidkredsløb omfatter:

et første sæt af en flerhed af strømningspassager forbundet med en første indløbskanal og en første udløbsskanal; og

et andet sæt af en flerhed af strømningspassager forbundet med en anden indløbskanal og en anden udløbsskanal, og

hvor det første sæt af en flerhed af strømningspassager er forskudt i forhold til det andet sæt af en flerhed af strømningspassager.

15. Energiudvekslingssystem (100) omfattende:

en flerhed af luftkanaler (406) konfigureret til at tillade at der passerer luft derigennem;

en flerhed af væskepanelsamlinger (402) skiftevis anbragt med mellemrum med flerheden af luftkanaler (406), hvor hver af flerheden af væskepanelsamlingerne ifølge et hvilket som helst af kravene 1-14.

DRAWINGS

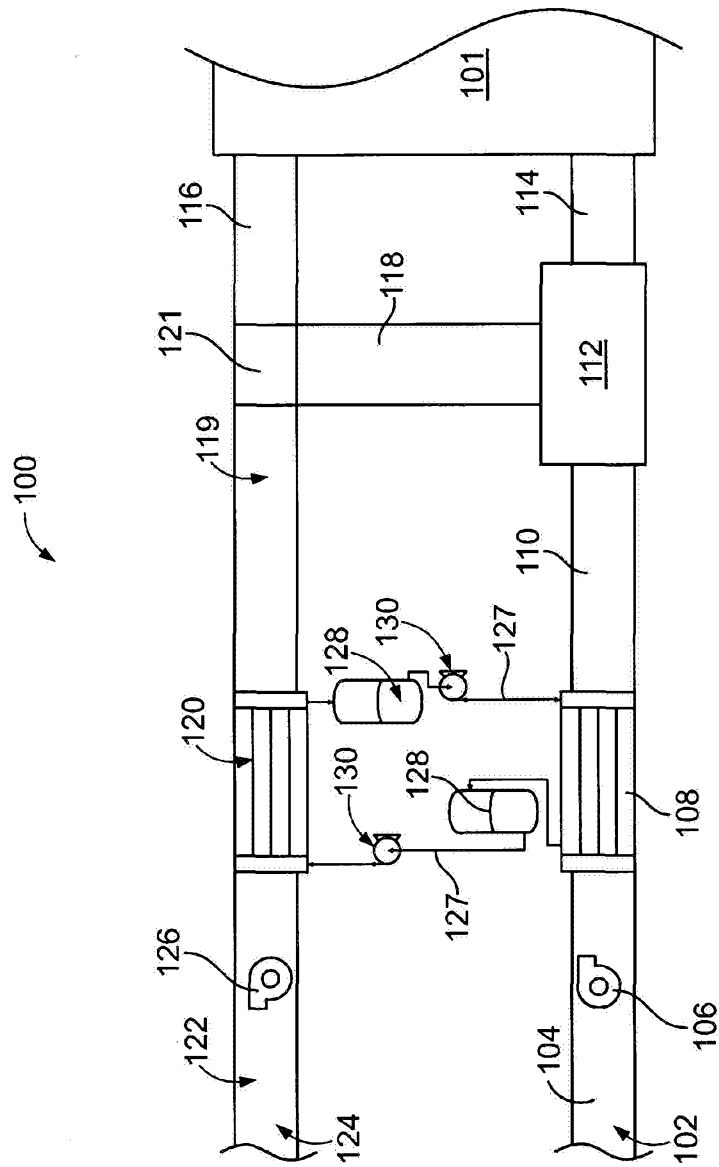


FIG. 1

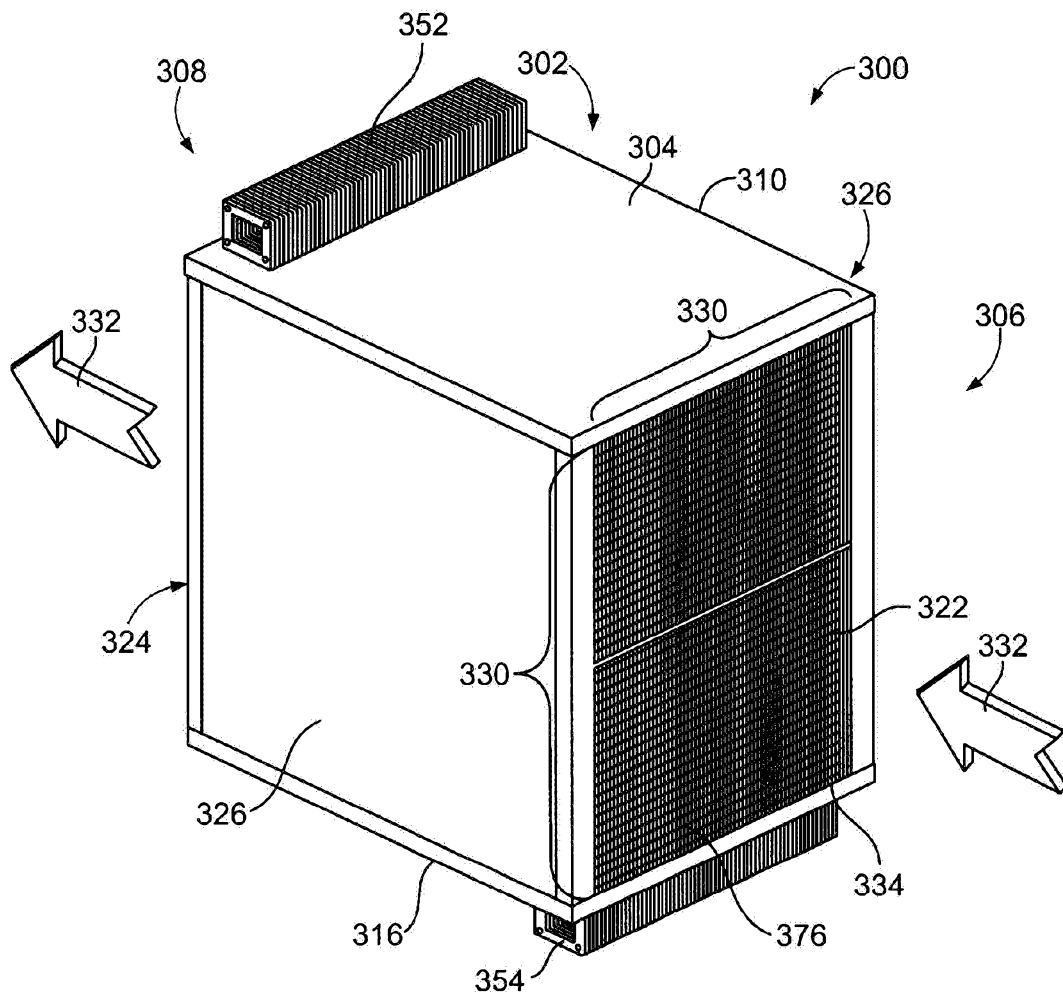


FIG. 2

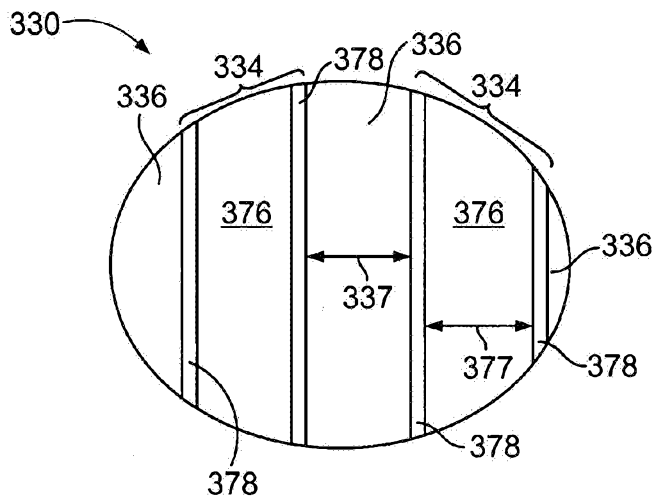


FIG. 3

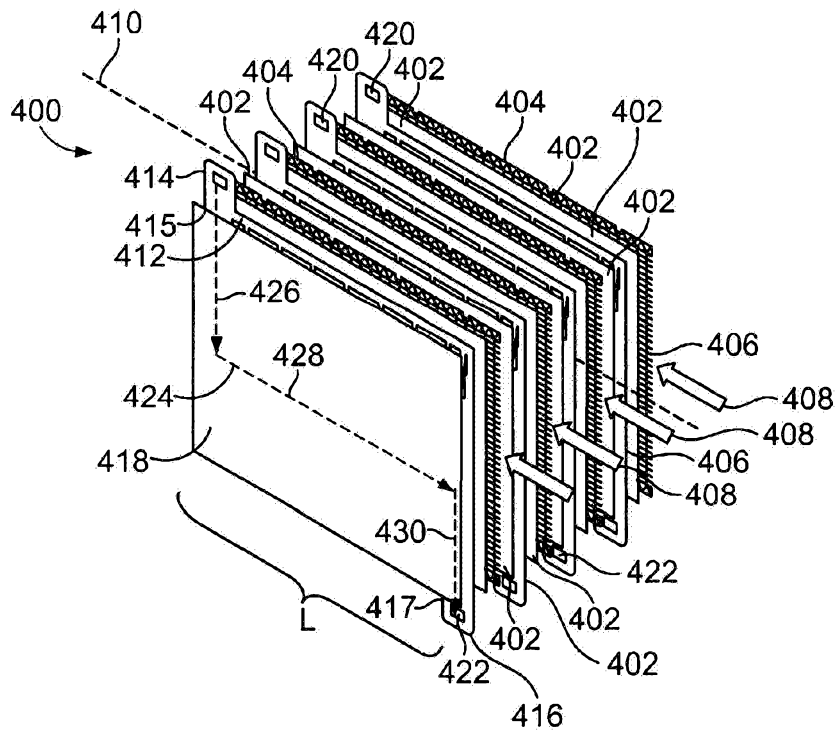
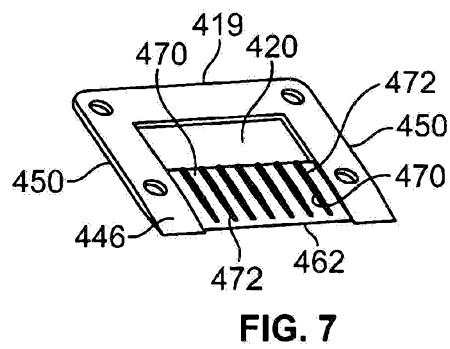
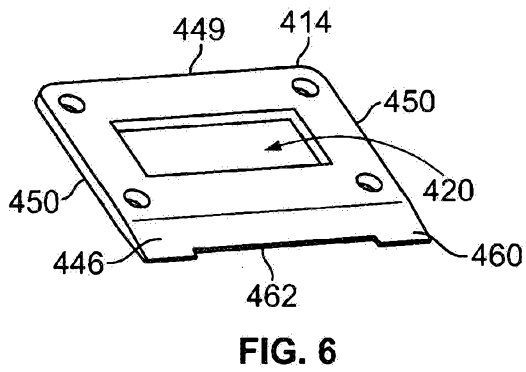
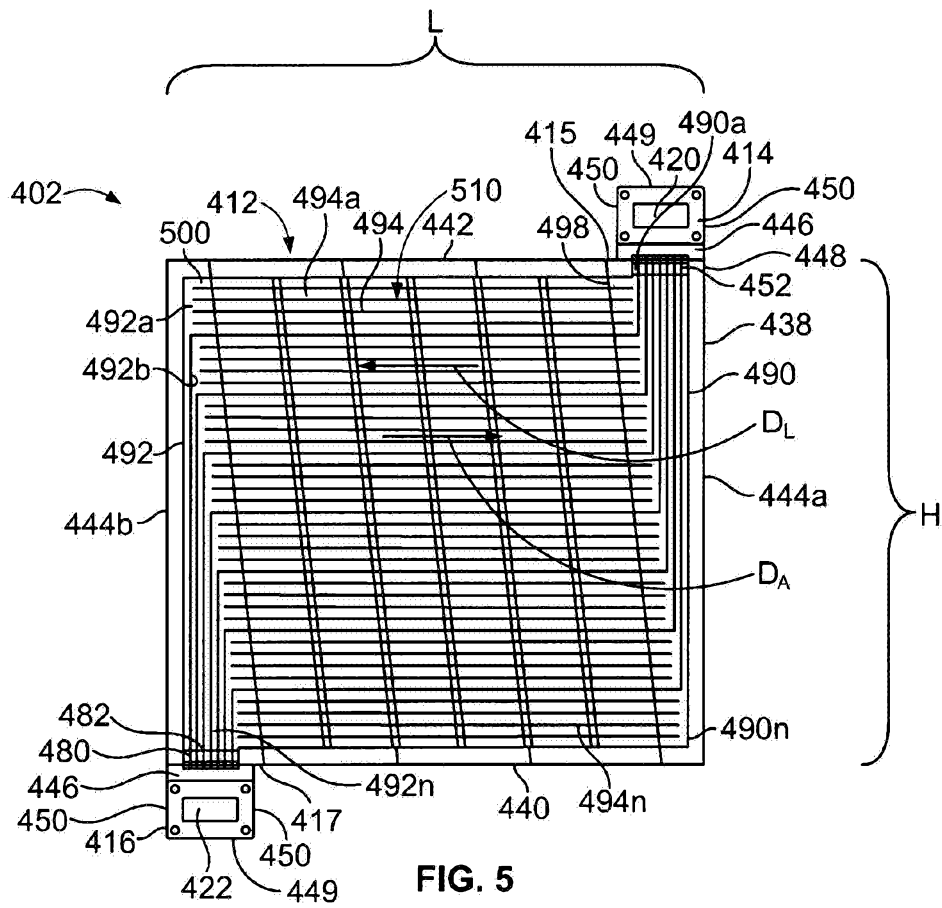


FIG. 4



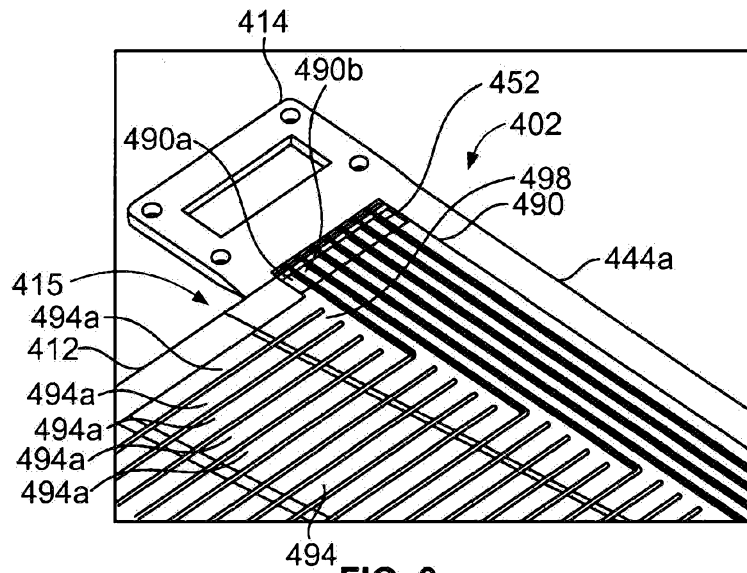


FIG. 8

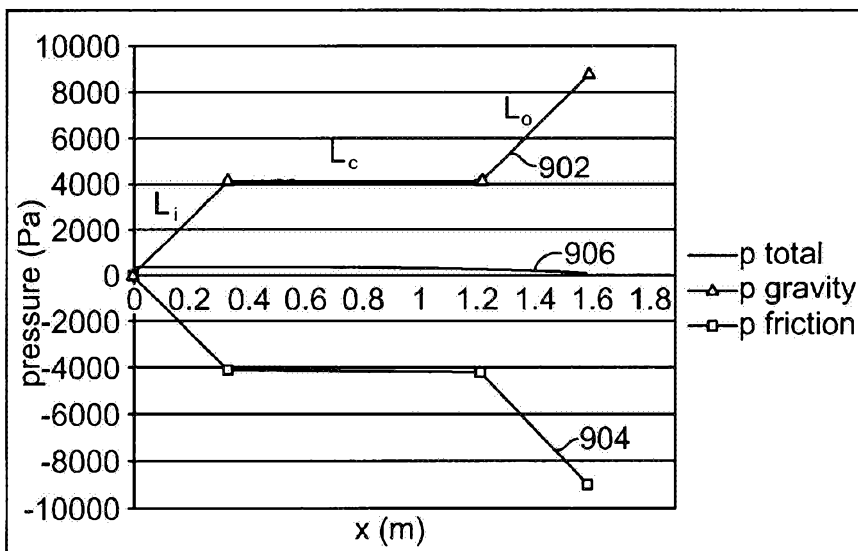
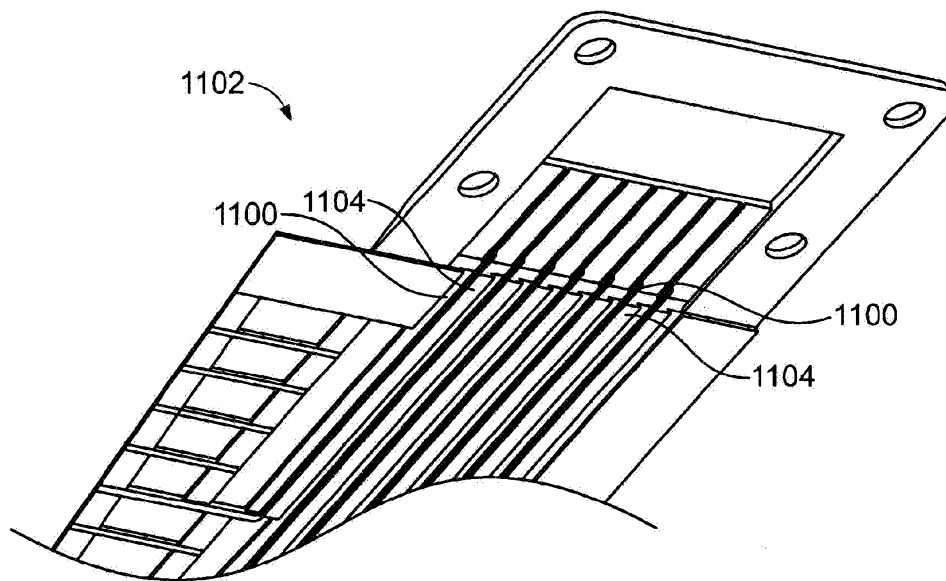
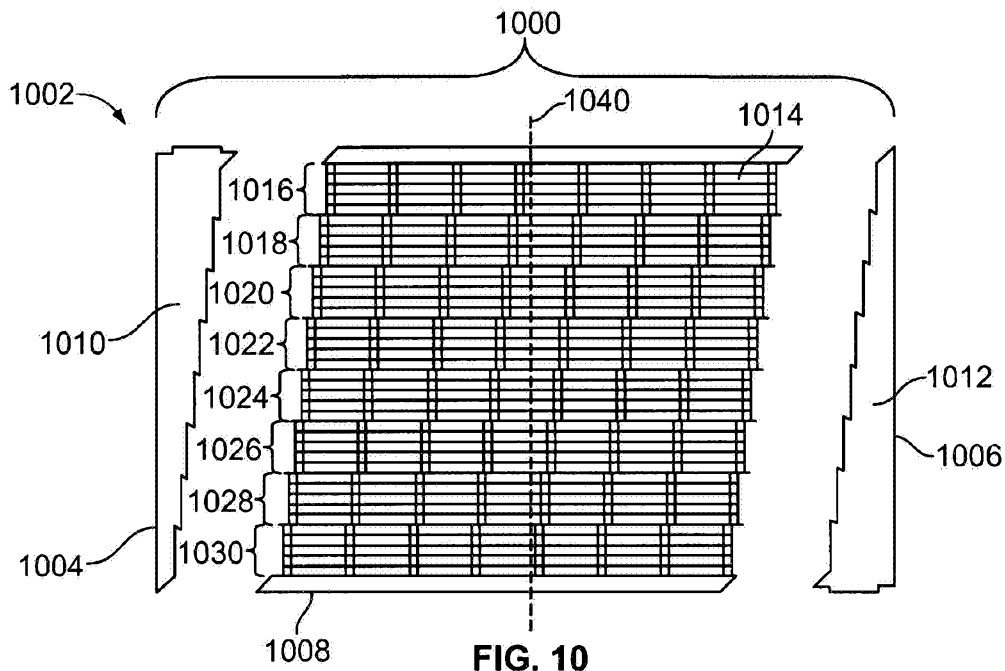


FIG. 9



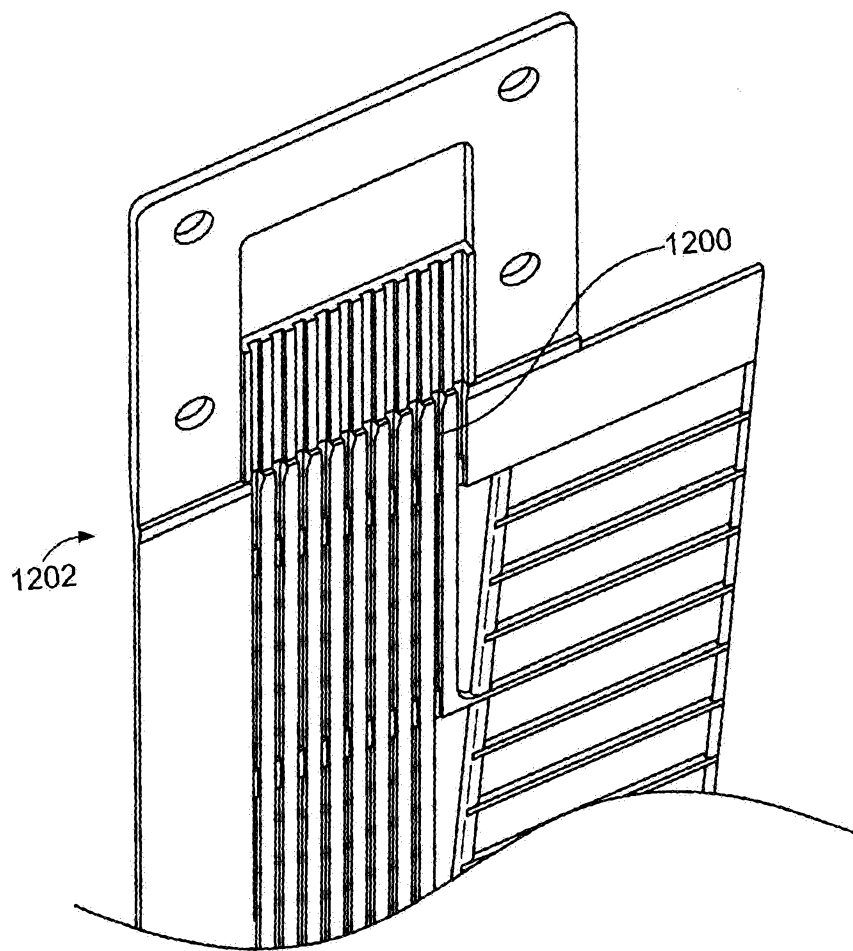


FIG. 12

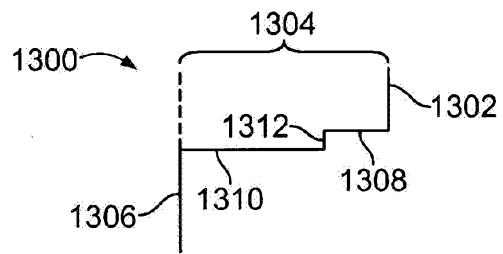


FIG. 13

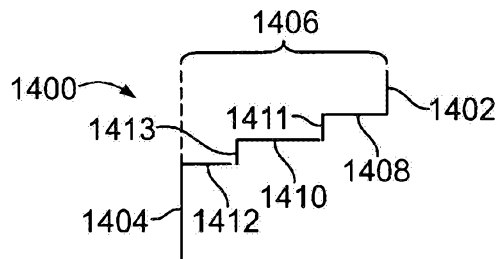


FIG. 14

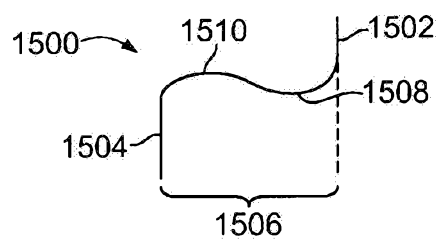


FIG. 15

1600

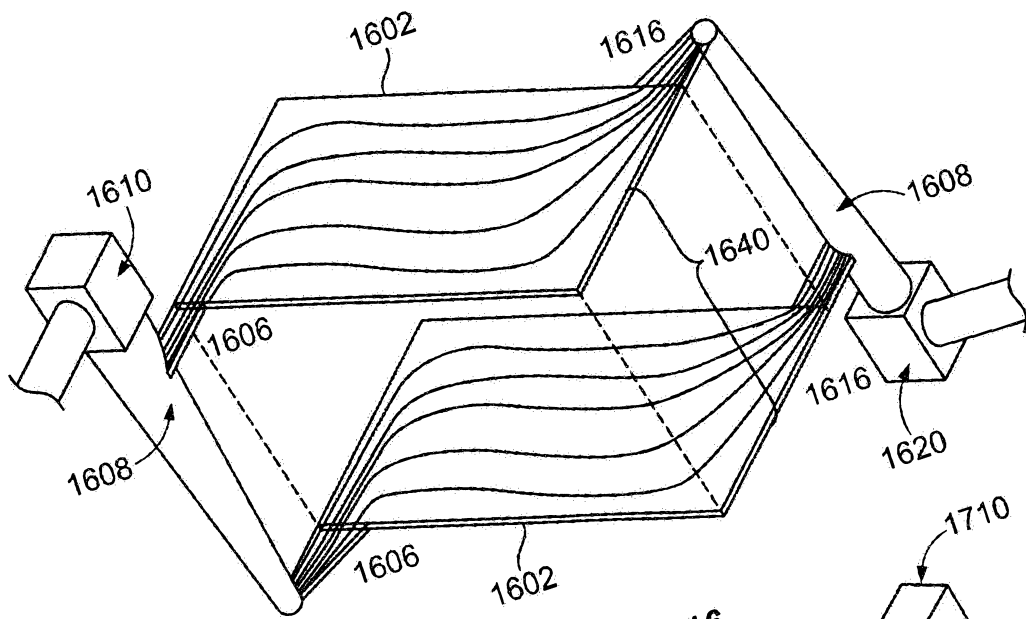


FIG. 16

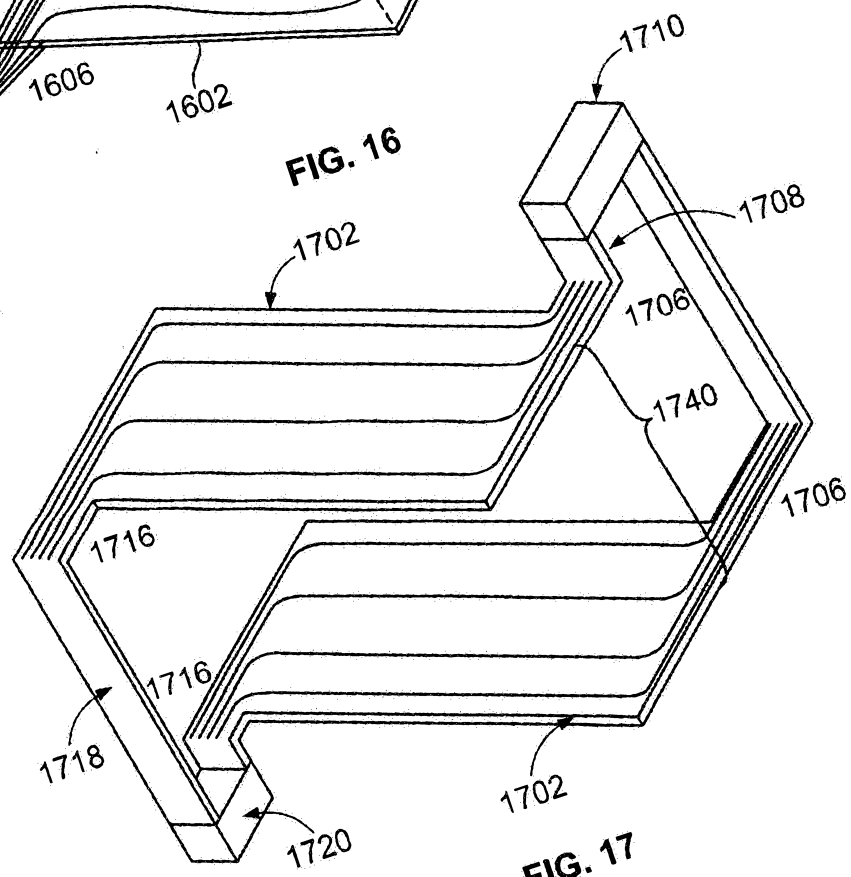


FIG. 17

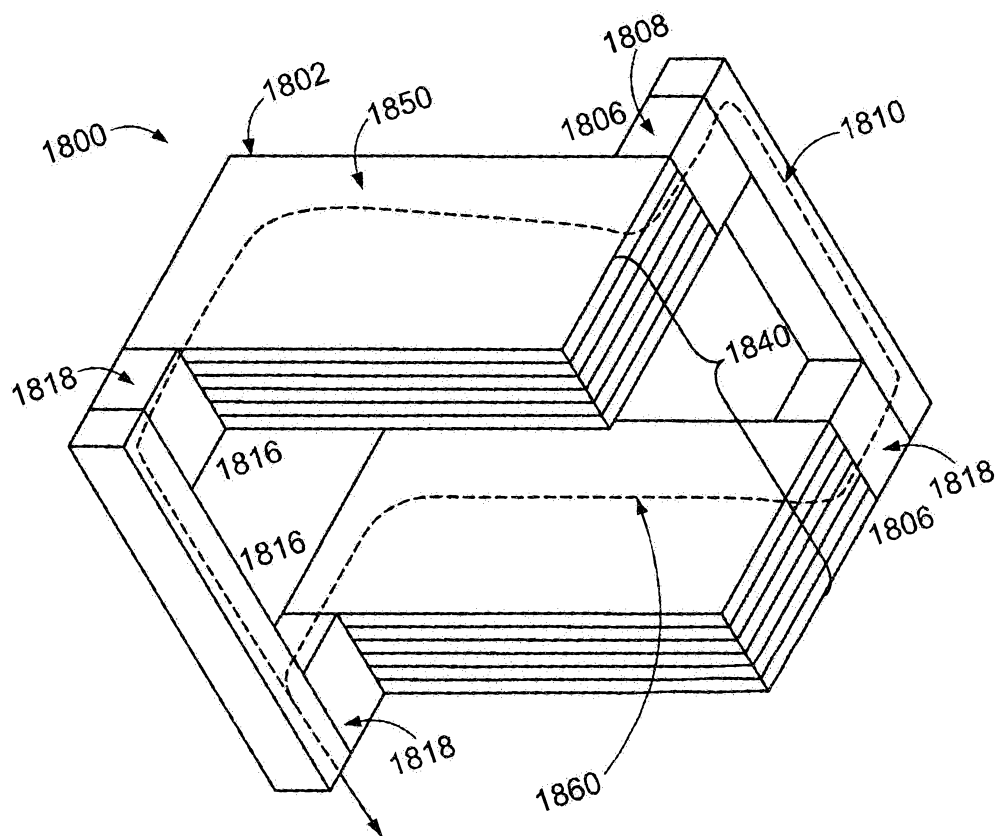


FIG. 18

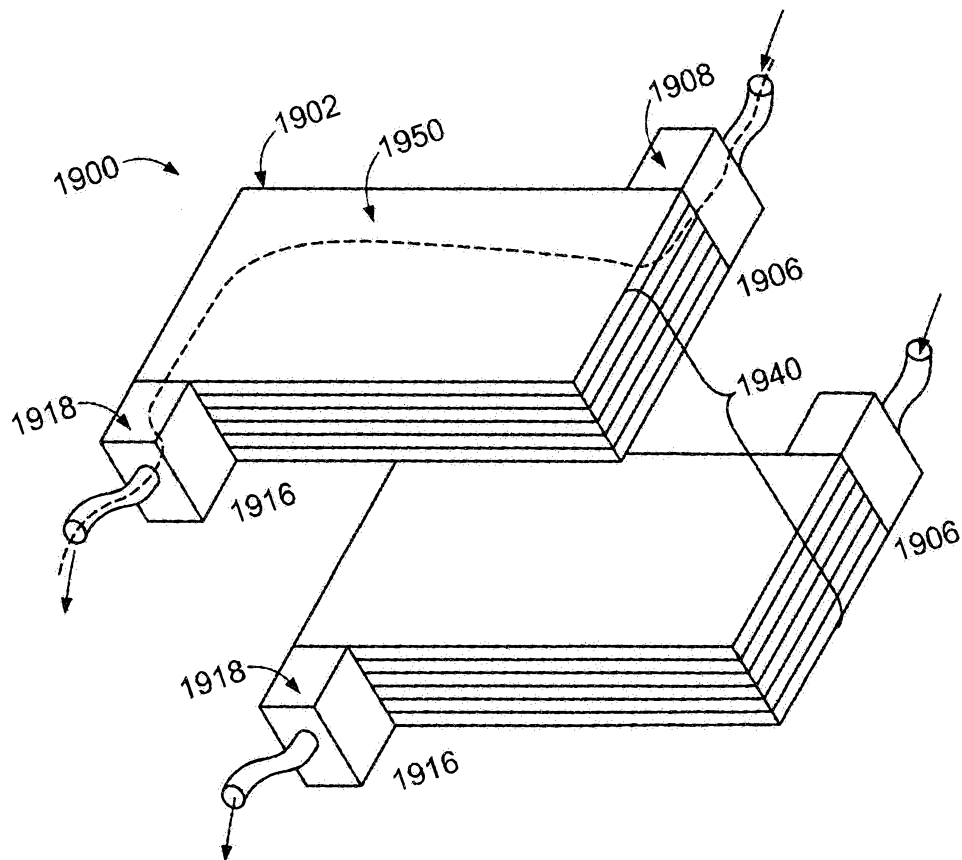


FIG. 19