

(19)



(11)

EP 3 171 109 B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication and mention
of the grant of the patent:
14.11.2018 Bulletin 2018/46

(51) Int Cl.:
F26B 5/06 (2006.01)

(21) Application number: **16200274.5**

(22) Date of filing: **28.03.2012**

(54) **OPTIMIZATION OF NUCLEATION AND CRYSTALLIZATION FOR LYOPHILIZATION USING GAP FREEZING**

OPTIMIERUNG VON NUKLEIERUNG UND KRISTALLISIERUNG ZUR GEFRIERTROCKNUNG
MITTELS LÜCKENGEFRIERUNG

OPTIMISATION DE LA NUCLÉATION ET DE LA CRISTALLISATION POUR LA LYOPHILISATION
PAR CONGÉLATION AVEC SÉPARATION

(84) Designated Contracting States:
**AL AT BE BG CH CY CZ DE DK EE ES FI FR GB
GR HR HU IE IS IT LI LT LU LV MC MK MT NL NO
PL PT RO RS SE SI SK SM TR**

(43) Date of publication of application:
24.05.2017 Bulletin 2017/21

(62) Document number(s) of the earlier application(s) in
accordance with Art. 76 EPC:
12716817.7 / 2 831 526

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WO-A1-2012/054194 DE-A1- 2 235 483
US-A- 4 501 719 US-A- 4 953 299
US-A1- 2011 154 681

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Description**FIELD OF DISCLOSURE**

[0001] This disclosure relates to methods and apparatus used for lyophilizing liquid solutions of solutes. The disclosure provides a method for optimization of the nucleation and crystallization of the liquid solution during freezing to produce lyophilized cakes of the solutes with large, consistent pore sizes. The disclosure also provides a method for rapid lyophilization of the frozen liquid solution. The disclosure additionally provides apparatus for use with the method and lyophilization chambers.

BRIEF DESCRIPTION OF RELATED TECHNOLOGY

[0002] The preservation of materials encompasses a variety of methods. One important method, lyophilization, involves the freeze-drying of solutes. Typically, a solution is loaded into a lyophilization chamber, the solution is frozen, and the frozen solvent is removed by sublimation under reduced pressure.

[0003] One well known issue associated with the lyophilization of materials (e.g., sugars) is the formation of one or more layers of the solute (the dissolved materials) on the top of the frozen solution. In a worse case, the solute forms an amorphous solid that is nearly impermeable and eventually prevents sublimation of the frozen solvent. These layers of concentrated solute can inhibit the sublimation of the frozen solvent and may require use of higher drying temperatures and/or longer drying times. The higher drying temperatures may negatively impact the integrity of the solute and the longer drying time may have a negative effect on the economics of the process.

[0004] US 4,953,299 describes a process and apparatus for freeze-drying, said apparatus comprising freeze-drying shelves disposed inside a freeze-drying enclosure, on which may be placed products or solutions to be freeze-dried. The product or solutions may be contained in open recipients, as well as cooling and/or heating means associated with and preferably incorporated in said shelves. The means forming a thermal shield are disposed between said freeze-drying shelves, thus making it possible to slow down the heat exchanges between the surface of the product to be freeze-dried and the heating and/or cooling elements associated with the shelves.

[0005] DE 22 35 483 is concerned with a freeze drying apparatus configured to make better use of the available drying space when freeze drying plants to increase their drying capacity.

[0006] WO 2012/054194 discloses devices, articles, and methods useful for producing lyophilized cakes of solutes. The devices and articles provide for a method of freezing liquid solutions of the solute by the top and the bottom of the solution simultaneously. The frozen solution then provides a lyophilized cake of the solutes with large and uniform pores.

SUMMARY

[0007] The invention is set out in the appended claims.

BRIEF DESCRIPTION OF THE DRAWING FIGURES

[0008] For a more complete understanding of the disclosure, reference should be made to the following detailed description and accompanying drawing figures wherein:

Figure 1 is a drawing of the inside of a lyophilization device showing a lyophilization chamber and a plurality of heat sinks in a vertical arrangement;

Figure 2 is a composite drawing of an article showing an arrangement of a heat sink surface and a tray surface;

Figure 3 is another composite drawing of an article showing an arrangement of a plurality of heat sinks and the location and separation of the heat sink surface and the tray surface;

Figure 4 is illustrations of sample containers, here vials, (4a) positioned on a tray, (4b) positioned directly on a thermal insulator, or (4c) combined with a thermally insulating support;

Figure 5 is a drawing of a sample vial including a liquid solution showing the placement of thermocouples useful for the measurement of the temperatures of the top and the bottom of the solution;

Figure 6 is a plot of the temperatures of the top and the bottom of a 10 wt. % aqueous sucrose solution frozen using a 3mm gap between a heat sink surface and a tray (the tray having a thickness of about 1.2 mm) showing a nucleation event, the differences in temperatures between the top and the bottom of the solution, and the reduction in temperature of the top of the solution after the freezing point plateau;

Figure 7 is plots of the water-ice conversion indices for a 5 wt. % aqueous sucrose solution as a function of distance (air gap) from a heat sink surface to a tray (the tray having a thickness of about 1.2 mm);

Figure 8 is a plot of the internal temperatures of vials during a primary drying process illustrating the effect of gap-freezing on the product temperature during freeze-drying;

Figure 9 is a plot of effective pore radii for samples frozen on a 6 mm gapped tray and samples frozen directly on the heat sink surface;

Figures 10 and 11 are temperature probe diagrams for top shelf and bottom shelf vials according to Example 2;

Figures 12 and 13 are comparisons of approximate drying time for vials on the top shelf and bottom shelf, according to Example 2;

Figure 14 is a comparison of product temperatures of top shelf center vials and bottom shelf center vials during drying, according to Example 2;

Figure 15 is a comparison of product temperatures

of top shelf center vials and edge vials TP04 and TP07 during drying, according to Example 2; and Figure 16 is a comparison of product temperatures of bottom shelf center vials and edge vials during drying, according to Example 2.

[0009] While the disclosed methods and articles are susceptible of embodiments in various forms, there are illustrated in the examples and figures (and will hereafter be described) specific embodiments of the methods and articles, with the understanding that the disclosure is intended to be illustrative, and is not intended to limit the invention to the specific embodiments described and illustrated herein.

DETAILED DESCRIPTION

[0010] One well known issue associated with the lyophilization of materials (e.g., sugars) is the formation of one or more layers of the solute (the dissolved materials) on the top of the frozen solution. These layers form during the freezing of the solution because, typically, the solutions are positioned within the lyophilization chamber on a heat sink which rapidly decreases in temperature and causes the solution to freeze from the bottom up. This bottom up freezing pushes the solute in the liquid phase closer to the top of the solution and increases the solute concentration in the still liquid solution. The high concentration of solute can then form a solid mass that can inhibit the flow of gasses therethrough. In a worse case, the solute forms an amorphous solid that is nearly impermeable and prevents sublimation of the frozen solvent. These layers of concentrated solute can inhibit the sublimation of the frozen solvent and may require use of higher drying temperatures and/or longer drying times.

[0011] Disclosed herein is an apparatus for and method of freezing a material, e.g., for subsequent lyophilization, that can prevent the formation of these layers and thereby provide efficient sublimation of the frozen solvent.

[0012] The lyophilization or freeze drying of solutes is the sublimation of frozen liquids, leaving a non-subliming material as a resultant product. Herein, the non-subliming material is generally referred to as a solute. A common lyophilization procedure involves loading a lyophilization chamber with a container that contains a liquid solution of at least one solute. The liquid solution is then frozen. After freezing, the pressure in the chamber is reduced sufficiently to sublime the frozen solvent, such as water, from the frozen solution.

[0013] The lyophilization device or chamber is adapted for the freeze drying of samples in containers by including at least one tray for supporting the container and means for reducing the pressure in the chamber (e.g., a vacuum pump). Many lyophilization devices and chambers are commercially available.

[0014] With reference to Figures 1-3, the lyophilization chamber includes a heat sink **101** that facilitates the low-

ering of the temperature within the chamber. The heat sink **101** includes a heat sink surface **102** that is exposed to the internal volume of the lyophilization chamber and is in thermal communication with a refrigerant **103**. The refrigerant **103** can be carried in the heat sink **101** within a refrigerant conduit **104**. The refrigerant conduit **104** can carry the heat sink surface **102** or can be in fluid communication with the heat sink surface **102** for example through a heat sink medium **105**. The heat sink medium **105** is a thermal conductor, not insulator, and preferably has a thermal conductivity of greater than about 0.25, 0.5, and/or 1 W/mK at 25 °C.

[0015] According to the novel method described herein, the sample containers **106** do not sit on or in direct, substantial thermal conductivity with the heat sink **101** during freezing. In one embodiment, the sample containers **106** sit on or are carried by a tray surface **107** that is thermally insulated from the heat sink **101**. In another embodiment, the sample containers **106** are thermally insulated by being suspended above the heat sink **101**.

[0016] The tray surface **107** is thermally insulated from the heat sink **101** by a thermal insulator **108**. The thermal insulator **108** has a thermal conductivity of less than about 0.2, less than 0.1, and/or less than 0.05 W/mK at 25 °C. The thermal insulator **108** can be a gas, a partial or complete vacuum, a paper, a foam (e.g., a foam having flexibility at cryogenic temperatures), a polymeric material, or a combination or other mixture of thereof. The polymeric material can be free of or substantially free of open cells or can be a polymeric foam (e.g., a cured foam). As used herein, the thermal insulator **108** refers to the material, object and/or space that provides thermal insulation from the heat sink **101**. Air is still considered a thermal insulator in a method or apparatus wherein the pressure of the air is decreased due to evacuation of the lyophilization chamber.

[0017] The level of thermal insulation provided by the thermal insulator **108** can be dependent on the thickness of the thermal insulator **108**. This thickness can be measured by the distance **109** from the heat sink surface **102** to the tray surface **107**, for example. This distance **109**, limited by the internal size of the lyophilization chamber, can be in a range of about 0.5 to about 50 mm, for example, or smaller if the thermal isolation is very high. This distance **109** can be optimized for specific lyophilization chamber volumes and preferably is greater than about 0.5, 0.75, 1, 1.5, 2, 2.5, 3, 3.5, 4, 4.5, 5, 5.5, 6, 6.5, 7, 7.5, 8, 8.5, 9, 9.5, 10, 15, 20, 25, 30, 35, 40, 45, or 50 mm. While the distance **109** can be larger than about 10 mm, the volume within the lyophilization device is typically better used by optimizing the distances below about 20 mm. Notably, the distance between the heat sink surface **102** and the tray surface **107** is only limited by the distance between the heat sink surface **102** and the upper heat sink **101** minus the height of a vial **106**. The preferred distance **109** can be dependent on the specific model and condition of lyophilization chamber, heat sink, refrigerant, and the like, and is readily optimized by the person

of ordinary skill in view of the present disclosure to avoid uneven freezing from top and bottom surfaces of the solution in the container.

[0018] In an embodiment where the tray surface **107** is thermally insulated from the heat sink **101**, the tray surface **107** is carried by a tray **110**, preferably a rigid tray. Notably, the tray surface **107** can be a thermal insulator (e.g., foamed polyurethane) or a thermal conductor (e.g., stainless steel). In such an embodiment the thermal insulator **108** may comprise a gas, a partial vacuum, or a full vacuum.

[0019] The tray **110** is preferably maintained at a fixed distance between heat sink surface **102** and the tray surface **107** during freezing. The tray **110** can be spaced from the heat sink surface **102** by the thermal insulator **108** formed in an embodiment to include a spacer **111** positioned between the tray **110** and the heat sink surface **102** or can be spaced from the heat sink surface **102** to form the thermal insulator **108** by operationally engaging the tray **110** to a bracket **112** affixed to an internal surface **113** (e.g., wall) of the lyophilization chamber. In a further embodiment, the tray **110** is maintained at a distance from the heat sink surface **102** to form the thermal insulator **108** by a plurality of struts (not shown) that operationally engage the tray **110** and heat sink surface **102**. In an embodiment where a spacer **111** supports the tray **110**, the distance from the heat sink surface **102** to the tray surface **107** is the thickness of the spacer **111** plus the thickness of the tray **110**. In agreement with the distances disclosed above, the spacer **111** can have a thickness in a range of about 0.5 mm to about 10 mm, about 1 mm to about 9 mm, about 2 mm to about 8 mm, and/or about 3 mm to about 7 mm, for example. The tray **110** can be carried by one or more spacers **111** placed between the heat sink surface **102** and the tray **110**.

[0020] In another embodiment, the tray **110** can be carried by the thermal insulator **108** comprising a rigid thermal insulator. For example the tray **110** can be a thermal conductor (e.g., stainless steel) and supported by (e.g., resting on) a thermal insulator (e.g., foamed polyurethane). In a further embodiment the rigid thermal insulator can be combined with spacers to carry the tray. In agreement with the distances disclosed above, the rigid thermal insulator (with or without the spacer) can have a thickness in a range of about 0.5 mm to about 10 mm, about 1 mm to about 9 mm, about 2 mm to about 8 mm, and/or about 3 mm to about 7 mm, for example.

[0021] The lyophilization device can include a plurality of heat sinks **101** that individually have a heat sink surface **102** in thermal communication with a refrigerant **103**. In such a lyophilization device, the heat sinks **101** can be disposed vertically in the lyophilization chamber with respect to each other, forming upper and lower heat sinks **101** (see e.g., Figure 1). By convention, the lower heat sink surface **102** is disposed between the upper and lower heat sinks and the tray surface **107** is disposed between the upper heat sink **101** and the lower heat sink surface **102**. In this arrangement, the thermal insulator

108 is disposed between the tray surface **107** and the lower heat sink **101**.

[0022] In another embodiment, each individual sample container **106** can sit on or be carried by a thermal insulator **108** (see e.g., Figure 4b). For example, when the sample container is a vial having a top and a bottom the thermal insulator **108** can comprise a thermally insulating support **114** affixed to the bottom of the vial **115** (see e.g., Figure 4c). The thermally insulating support **114** can have a thermal conductivity less than about 0.2 W/mK, less than about 0.1 W/mK, and/or less than about 0.05 W/mK at 25 °C, for example. In one embodiment, the vial **106** and the insulating support **114** are different materials (e.g., the vial can comprise a glass and the insulating support can comprise a foam or a polymer). The vial can comprise a sealable vial.

[0023] The invention is directed to a method of freezing a liquid solution for subsequent lyophilization. In one embodiment of the method, the lyophilization chamber as described above is loaded with a liquid solution held in a container that includes an active pharmaceutical agent solute and a solvent. The liquid solution will have a top surface **116** and a bottom surface, wherein the bottom surface **117** is proximal to the heat sink **101** (see Figure 5). The container is separated from the heat sink **101** by providing a thermal insulator **108** between the container and the heat sink **101**, the thermal insulator having the characteristics described herein. Thus, the container is spaced vertically from the heat sink with an intervening thermal insulator **108**, the distance and thermal insulator **108** being selected to provide freezing of the liquid solution from the top and bottom surfaces at approximately the same rate. Having been loaded into the lyophilization chamber, the liquid solution can be frozen by lowering the temperature of the heat sink **101** and thereby the ambient temperature in the lyophilization chamber. The liquid solution advantageously can be frozen from the top and the bottom surfaces at approximately the same rate to form a frozen solution. A further advantage is that the concurrent water to ice conversion at the top and bottom of the solution avoids problematic freeze-concentration and skin formation observed when the bottom of the solution freezes more rapidly than the top.

[0024] A further embodiment of the inventions includes once frozen, the liquid solution (now the frozen solution) can be lyophilized to yield a lyophilized cake. In one type of embodiment, the solution is lyophilized without any significant change in the thermal insulator **108** such as by example maintaining the physical arrangement of the container and heat sink elements. In another type of embodiment, the container having the frozen liquid solution is placed in thermally-conductive contact with the heat sink during or following freezing, for example by removing the thermal insulator **108** and placing the tray **107** or containers directly on the shelf. Embodiments of the removal can comprise, removing the spacer **111**, moving the brackets **112** or altering the length of the struts (not shown). It is also envisioned that the thermal insulator

container not be placed in thermally conductive contact with the heat sink but the insulation characteristics of the thermal insulator 108 be altered such as by significantly lessening the insulation characteristics by reducing the spacing between the tray and heat sink to a minimal distance.

[0025] As noted in connection with Example 2 below, when freezing and drying an array of containers, containers placed at the edges of such an array, and those especially at the corners, can experience temperatures which deviate from those of center containers, due to radiant heat from side walls. Thus, in a method of freezing an array of containers, it is contemplated that the thermal insulator 108 or portions thereof between one or more of the container and heat sink can dimensionally vary from the thermal insulator or portions thereof between one or more remaining containers. In an embodiment, the thickness of the thermal insulator 108 can be reduced for edge and/or corner containers, relative to the thickness of the thermal insulator 108 between center containers and heat sink, in order to counter-balance the radiant heating experienced by such edge and corner containers from side walls and thus achieve more consistent temperature profiles across the array.

[0026] In this embodiment, the thermal insulator provides for the facile freezing of the liquid solution from the top and the bottom within the lyophilization chamber at approximately the same rate. The freezing of the liquid solution from the top and the bottom can be determined by measuring the temperature of the solution during the freezing process. The temperature can be measured by inserting at least two thermocouples into a vial containing the solution. A first thermocouple **118** can be positioned at the bottom of the solution, at about the center of the vial, for example, and a second thermocouple **119** can be positioned at the top of the solution, just below the surface of the solution, in about the center of the vial, for example. Once a freezing cycle has been optimized for a combination of liquid solution, container configuration, and lyophilization chamber, then in subsequent processing of additional batches temperature monitoring of the containers (e.g. vials) is not necessary.

[0027] To freeze the liquid solution from the top and the bottom surfaces at approximately the same rate, the thermal insulator (e.g., type and thickness) can be selected to provide a water-ice conversion index value in a range of about -2°C to about 2°C , or about -1°C to about 1°C , and/or about -0.5°C to about 0.5°C . Preferably, the water-ice conversion index is zero or a positive value. The water-ice conversion index is determined by a method including first plotting the temperatures reported by the thermocouples at the top (T_t) and at the bottom (T_b) of the solution as a function of time. The water-ice conversion index is the area between the curves, in $^{\circ}\text{C}\cdot\text{minute}$, between a first nucleation event and the end of water-ice conversion divided by the water-ice conversion time, in minutes. The water-ice conversion time is the time necessary for the temperature at the top (T_t) of

the solution to reduce in value below the freezing point plateau for the solution.

[0028] The temperature data are collected by loading solution-filled vials into a lyophilization chamber. The lyophilization tray, at $t=0$ min, is then cooled to about -60°C . The temperature can then be recorded until a time after which the top and the bottom of the solution cool to a temperature below the freezing point plateau.

[0029] The areas, positive and negative, are measured from the first nucleation event (observable in the plot of temperatures, e.g., such as in Figure 6) **122** until both temperature values cool below the freezing point plateau **123**. The sum of these areas provides the area between the curves. When calculating the area between the curves, the value is positive when the temperature at the bottom of the vial (T_b) is warmer than the temperature at the top of the vial (T_t) **120** and the value is negative when the temperature at the top of the vial (T_t) is warmer than the temperature at the bottom of the vial (T_b) **121**. Preferably, the water-ice conversion index is zero or a positive value. This condition will prevent the consequence that the freezing rate at the bottom of the solution is significantly higher than that at the top of the solution. Thus, for example, the water-ice conversion index value in one type of embodiment will be in a range of about 0°C to about 2°C , or about 0°C to about 1°C , or about 0°C to about 0.5°C . For a particular solution and container configuration, the cooling rate, temperature of the tray, and the thermal insulator can be optimized to provide an area between the curves at or near $0^{\circ}\text{C}\cdot\text{minute}$. For example, Figure 7 shows the water-ice conversion indices for 5 wt.% aqueous solutions of sucrose in vials on a stainless steel tray as a function of the distance from the heat sink surface to the stainless steel tray, with the thermal insulator 108 comprising air within a gap between the heat sink surface and the bottom of the stainless steel tray. The tray had a thickness of about 1.2 mm.

[0030] Still another embodiment of the invention is a lyophilized cake made by a method disclosed herein. The lyophilized cake can include a substantially dry lyophilized material and a plurality of pores in the lyophilized material having substantially the same pore size. In one embodiment, the lyophilized cake has a pore size that is substantially larger than the pore size of a reference lyophilized cake comprising the same material as the lyophilized cake but made by a standard lyophilization process (e.g., placing a vial **106** comprising a liquid solution onto a heat sink **101** within a lyophilization chamber, excluding a thermal insulator between the vial and the heat sink **101**, lowering the temperature of the heat sink **101** and thereby freezing the liquid solution, and then lyophilizing the frozen solution). The cross-sectional area of the cylindrical pores of the lyophilized cake is preferably at least 1.1, 2, and/or 3 times greater than the cross-sectional area of the reference lyophilized cake. In another embodiment the lyophilized cake has a substantially consistent pore size throughout the cake.

[0031] The size of pores in the lyophilized cake can be

measured by a BET surface area analyzer. The effective pore radius (r_e), a measure of the pore size, can be calculated from the measured surface area of the pores (SSA) by assuming cylindrical pores. The effective pore radius r_e can be determined by the equation $r_e = 2\varepsilon/SSA \cdot \rho_s \cdot (1-\varepsilon)$ where SSA is the surface area of the pores, ε is the void volume fraction or porosity ($\varepsilon = V_{\text{void}}/V_{\text{total}} = n \cdot r_e^2/V_{\text{total}}$), $(1-\varepsilon)$ is the solute concentration in the volume fraction units, and ρ_s is the density of the solid.

EXAMPLES

[0032] The following examples are provided to illustrate the invention, but are not intended to limit the scope thereof.

Example 1. Effect of Gap Freezing on Lowering Product Temperature and on Pore Enlargement

[0033] The effect of gap freezing on the pore enlargement for a lyophilized 10% aqueous sucrose solution was studied. Multiple 20 mL Schott tubing vials were filled with 7 mL of a 10% aqueous solution of sucrose. These filled vials were placed in a LyoStar II[tm] (FTS SYSTEMS, INC. Stone Ridge, NY) freeze dryer either directly in contact with a top shelf (heat sink surface) or on a 6mm gapped tray. See e.g., Fig. 1. Multiple probed vials were produced by inserting two thermocouples into the solutions, one at the bottom-center of the vial and the other one about 2mm below the liquid surface. See Fig. 5. The filled vials were then lyophilized by the following procedure:

- 1) the shelf was cooled to 5 °C and held at this temperature for 60 minutes; next
- 2) the shelf was cooled to -70 °C and held at this temperature for 200 minutes (the internal temperatures of the thermocouple-containing vials were recorded during freezing);
- 3) after freezing, the 6mm gapped tray was removed and these vials were placed directly on the bottom shelf (this provided the vials on the top and bottom shelves with the same shelf heat transfer rate during lyophilization, and thereby a direct comparison of the effect of different freezing methods could be performed); next
- 4) the lyophilization chamber was evacuated to a set-point of 9332.57 mPa (70 mTorr), and
- 5) a primary drying cycle, during which time the internal temperatures of the frozen samples were recorded, was started. The primary drying cycle involved (a) holding the samples for 10 minutes at -70 °C and 9332.57 (70 mTorr), then (b) raising the temperature at a rate of 1 °C/min to -40 °C while maintaining 9332.57 mPa (70 mTorr), then (c) holding the samples for 60 minutes at -40 °C and 9332.57 mPa (70 mTorr), then (d) raising the temperature at a rate

of 0.5 °C/min to -25 °C while maintaining 9332.57 mPa (70 mTorr), and then (e) holding the samples for 64 hours at -25 °C and 6666.12 mPa (50 mTorr); 6) a secondary drying followed, and involved raising the temperature at a rate of 0.5 °C/min to 30 °C and 13332.2 mPa (100 mTorr), and then holding the samples for 5 hours at 30 °C and 13332.2 mPa (100 mTorr).

[0034] The average product temperatures for the frozen samples in vials on the top and bottom (gapped-tray) shelves, during primary drying, are presented in Figure 8. It can be seen that the temperature profile of the samples on the bottom shelf is much lower than that of those on the top shelf, which implies that the pore size in the dry layer of the bottom shelf samples is much larger than those on the top shelf, due to the effect of "gap-freezing." Theoretically, the temperatures are different from the set point temperatures due to evaporative cooling and/or the insulative effect of larger pore sizes.

[0035] The effective pore radius, r_e , for the individual lyophilized cakes was determined by a pore diffusion model. See Kuu et al. "Product Mass Transfer Resistance Directly Determined During Freeze-Drying Using Tunable Diode Laser Absorption Spectroscopy (TDLAS) and Pore Diffusion Model." Pharm. Dev. Technol. (available online at: <http://www.ncbi.nlm.nih.gov/pubmed/20387998> and later published in Vol. 16, no. 4, p. 343-357, 2011). The results are presented in Figure 9, where it can be seen that the pore radius of the cakes on the bottom shelf is much larger than that on the top shelf. The results demonstrate that the 6mm gapped tray is very effective for pore enlargement.

Example 2. Acceleration of Drying Rate By Removing Gap Following Freezing

[0036] An alternative lyophilization procedure was developed to increase the rate of freeze-drying by removing the gap between heat sink shelf and container-loaded shelf following freezing.

[0037] Multiple 20 mL Schott tubing vials were filled with 5 mL of a 5% (w/v) aqueous solution of sucrose. Two trays containing these filled vials were placed in a LyoStar II™ (FTS SYSTEMS, INC. Stone Ridge, NY) freeze dryer in the upper and lower portions of the chamber. The trays were separated from contact with the heat sink shelves by a thermal insulator comprising a spacer made of plastic tubing placed on each heat sink shelf, to provide a gap of approximately 6.5mm between each tray and each heat sink shelf.

[0038] For monitoring the product temperature on each shelf, two thermocouples were placed in center vials and six thermocouples were placed on the edge locations of the shelves, as shown in Figures 10 and 11, wherein the numbers indicate temperature-probed vials.

[0039] The shelf temperature (each) was cooled to -70°

C, followed by holding the shelf at -70°C for 90 minutes. At this low shelf temperature, cooling of vials can be accelerated, since cooling with a gap is primarily driven by radiation. The shelf was then heated to -50°C, followed by holding the shelf at -50°C for 60 minutes. After the solution was frozen the shelf temperature was raised to a higher temperature of -50°C because after complete freezing of the solution it is not necessary to maintain it at -70°C for vacuum pulling. For one of the trays, the thermal insulator 108 was removed prior to vacuum pulling by removing the spacer.

[0040] For primary drying: (a) the lyophilization chamber was then evacuated to a set-point of 13332.2 mPa (100 mTorr), (b) the shelf temperature was held at -50°C (at 13332.2 mPa (100 mTorr)) for 30 minutes; (c) the shelf temperature was then ramped to -15°C (at 13332.2 mPa (100 mTorr)) at a rate of 0.5 °C/min; and (d) the shelf temperature was then held at -15°C (at 13332.2 mPa (100 mTorr)) until the end of primary drying.

[0041] For secondary drying: (e) the shelf temperature was ramped to 30 °C (at 13332.2 mPa (100 mTorr)), at a rate of 0.5 °C/min; and (f) the shelf temperature was then held at 30 °C (at 13332.2 mPa (100 mTorr)) until the end of secondary drying.

[0042] Only the temperature profiles of the center vials (TP01, TP02, TP09 and TP10) and the edge vials along the side walls (TP04, TP07, TP12, and TP15) are used for comparison. The product temperature profiles of the corner vials (TP03, TP05, TP06, TP08, TP11, TP13, TP14, and TP16) are not representative for a manufacturing scale freeze dryer due to the strong thermal radiation from the front and back walls to corner vials in this freeze dryer. The front wall of the LyoStar™ II freeze dryer is acrylic without insulation. The back wall of the chamber has insulation, but the large amount of heat produced by the fluid pump penetrates through the insulation and raises the product temperature to some extent.

Comparison for the approximate drying time for vials on the top shelf versus vials on the bottom shelf

[0043] As shown in Figs. 12 and 13, the drying time on the top shelf (Fig. 12, thermal insulator remaining during vacuum pulling) is much longer than that on the bottom shelf (Fig. 13, thermal insulator removed before vacuum pulling) due to the much higher heat transfer rate on the bottom shelf without a thermal insulator. It can be seen from Fig. 12 that after approximate 2670 minutes of cycle time, primary drying was still not complete, since the temperature in the center vial, TP02 did not move out of the plateau level during primary drying. On the other hand, Fig. 13 shows that after approximate 1690 minutes of cycle time, primary drying was complete, since the temperatures in the center vials, TP09 and TP10 moved out of the plateau levels of primary drying. Inlet temperatures of the shelf refrigerant fluids are plotted as Tf on each of Figures 12 and 13.

Comparison for the product temperatures of center vials. TP01 and TP02 on the top shelf with TP09 and TP10 on the bottom shelf

[0044] The comparison is shown in Fig. 14, in which the difference between TP02 and TP09 is about 1.7°C.

Comparison for the product temperatures of center vials TP01 and TP02 with the edge vials TP04 and TP07 on the top shelf

[0045] The comparison is shown in Fig. 15, in which the difference between TP02 and TP07 is about 1.5°C.

Comparison for the product temperatures of center vials TP09 and TP10 with the edge vials TP12 and TP15 on the bottom shelf

[0046] The comparison is shown in Fig. 16, in which the difference between TP09 and TP12 is only about 0.2°C, which is much smaller than 1.5°C on the top shelf.

[0047] Using the same lyophilization cycle, the vials on the tray without a thermal insulator between the tray and shelf during drying are dried much faster than those with a thermal insulator between the tray and shelf during drying. The tray without a thermal insulator during drying also has the advantage of reducing the temperature difference between the center and edge vials, which could be important for some temperature-sensitive formulations.

[0048] The foregoing description is given for clearness of understanding only, and no unnecessary limitations should be understood therefrom, as modifications within the scope of the invention may be apparent to those having ordinary skill in the art.

Claims

1. A method comprising:

providing a lyophilization chamber comprising a heat sink surface in thermal communication with a refrigerant (103);
loading a container (106) comprising a liquid solution into the lyophilization chamber above the heat sink surface, the liquid solution comprising an active pharmaceutical agent solute and a solvent, the liquid solution having a top surface (116) and a bottom surface (117);
forming a thermal conduction insulator (108) between the bottom of the container and the heat sink surface to isolate the container from thermal conductivity with the heat sink;
lowering the temperature of the heat sink and thereby the ambient temperature in the lyophilization chamber comprising the container to a temperature sufficient to freeze the liquid solu-

tion,

the thermal conduction insulator selected to provide freezing of the liquid solution from the top and the bottom surfaces at approximately the same temperature and thereby form a frozen solution; and reducing the ambient pressure in the chamber to lyophilize the frozen solution after altering the thermal conduction insulator;

characterised in that the method comprises: during or after freezing, altering the thermal conduction insulator.

2. The method of claim 1, wherein the thermal conduction insulator (108) comprises one of air, a gas, or vacuum space.
3. The method of claim 1, wherein the thermal conduction insulator has a thermal conductivity less than about 0.2 W/mK.
4. The method of claim 2, further comprising providing a tray (110) upon which the container rests between the container and thermal conduction insulator, the tray optionally being thermally conductive or thermally insulating.
5. The method of claim 1, wherein the heat sink comprises a refrigerant conduit in thermal communication with the heat sink surface.
6. The method of claim 1, wherein the container comprises a vial optionally, wherein the thermal conduction insulator (108) comprises a thermally insulating support member affixed to the bottom of the vial, and the thermally insulating support member rests on the heat sink.
7. The method of claim 1, wherein the lyophilization chamber includes at least two parallel heat sinks (101) and further comprising loading the container (106) comprising the liquid solution into the lyophilization chamber between the two parallel heat sinks at distances spaced vertically from each heat sink with an intervening thermal conduction insulator (108), the distances and thermal conduction insulator selected to provide freezing the liquid solution from the top (116) and the bottom (117) surfaces at approximately the same temperature and thereby form a frozen solution.
8. The method of claim 1, further comprising placing the container (106) on a tray (110) wherein the thermal conduction insulator (108) comprises a separation distance between the tray and heat sink (101) optionally, wherein the altering step comprises thermally contacting the tray (110) and heat sink (101).

9. The method of claim 1, wherein the altering step comprises placing the container (106) comprising frozen liquid solution in thermally-conductive contact with the heat sink (101).
10. The method of claim 1 wherein the forming step includes placing at least one spacer (111) between the container (106) and heat sink (101) and the altering step includes removing the at least one spacer.
11. The method of claim 10, further comprising placing the container (106) on a tray (110) wherein the thermal conduction insulator (108) comprises a separation distance between the tray and heat sink (101) and the at least one spacer (111) is disposed between the tray and heat sink.
12. The method of claim 8 wherein the contacting step comprises contacting after freezing.
13. The method of claim 1, wherein the thermal conduction insulator (108) is altered after freezing the liquid solution in the container (106).
14. The method of claim 1, wherein the thermal conduction insulator (108) is altered during freezing the liquid solution in the container (106).
15. The method of claim 1, wherein the thermal conduction insulator (108) is altered to lessen the insulation characteristics.

Patentansprüche

1. Verfahren, umfassend:

das Bereitstellen einer Lyophilisationskammer, die eine Kühlkörperoberfläche in thermischer Verbindung mit einem Kältemittel (103) umfasst; das Beladen eines Behälters (106), der eine flüssige Lösung in der Lyophilisationskammer oberhalb der Kühlkörperoberfläche umfasst, wobei die flüssige Lösung einen gelösten pharmazeutischen Wirkstoff und ein Lösungsmittel umfasst, wobei die flüssige Lösung eine obere Oberfläche (116) und eine untere Oberfläche (117) aufweist;

das Bilden eines Wärmeleitungsisolators (108) zwischen dem Boden des Behälters und der Kühlkörperoberfläche, um den Behälter von der Wärmeleitfähigkeit mit dem Kühlkörper zu isolieren;

das Absenken der Temperatur des Kühlkörpers und damit der Umgebungstemperatur in der Lyophilisationskammer, die den Behälter umfasst, auf eine Temperatur, die ausreicht, um die flüs-

- sige Lösung einzufrieren, wobei der Wärmeleitungsisolator so ausgewählt ist, dass er das Einfrieren der flüssigen Lösung von der oberen und der unteren Oberfläche bei etwa der gleichen Temperatur ermöglicht und dadurch eine gefrorene Lösung bildet; und das Verringern des Umgebungsdrucks in der Kammer, um die gefrorene Lösung nach Änderung Wärmeleitungsisolators zu lyophilisieren; **dadurch gekennzeichnet, dass** das Verfahren Folgendes umfasst: während oder nach dem Einfrieren, Ändern des Wärmeleitungsisolators.
2. Verfahren nach Anspruch 1, wobei der Wärmeleitungsisolator (108) einen von Luft-, einem Gas- oder einem Vakuumraum umfasst.
 3. Verfahren nach Anspruch 1, wobei der Wärmeleitungsisolator eine Wärmeleitfähigkeit von weniger als etwa 0,2 W/mK aufweist.
 4. Verfahren nach Anspruch 2, ferner umfassend das Bereitstellen einer Platte (110), auf der der Behälter zwischen dem Behälter und dem Wärmeleitungsisolator aufliegt, wobei die Platte wahlweise wärmeleitend oder wärmeisolierend ist.
 5. Verfahren nach Anspruch 1, wobei der Kühlkörper eine Kältemittelleitung in thermischer Verbindung mit der Kühlkörperoberfläche umfasst.
 6. Verfahren nach Anspruch 1, wobei der Behälter optional ein Gefäß umfasst, wobei der Wärmeleitungsisolator (108) ein wärmeisolierendes Stützelement umfasst, das am Boden des Gefäßes befestigt ist, und das wärmeisolierende Stützelement auf der Wärmesenke aufliegt.
 7. Verfahren nach Anspruch 1, wobei die Lyophilisationskammer mindestens zwei parallele Kühlkörper (101) beinhaltet und ferner das Beladen des Behälters (106), der die flüssige Lösung umfasst, in die Lyophilisationskammer zwischen den beiden parallelen Kühlkörpern in Abständen umfasst, die vertikal von jedem Kühlkörper mit einem dazwischenliegenden Wärmeleitungsisolator (108) beabstandet sind, wobei die Abstände und der Wärmeleitungsisolator so gewählt sind, dass das Einfrieren der flüssigen Lösung von der oberen (116) und der unteren (117) Oberfläche bei etwa derselben Temperatur bereitgestellt wird und dadurch eine gefrorene Lösung gebildet wird.
 8. Verfahren nach Anspruch 1, ferner umfassend Anordnen des Behälters (106) auf einer Platte (110), wobei der Wärmeleitungsisolator (108) optional einen Trennungsabstand zwischen der Platte und dem Kühlkörper (101) umfasst, wobei der Änderungsschritt das thermische Inkontaktbringen der Platte (110) und des Kühlkörpers (101) umfasst.
 9. Verfahren nach Anspruch 1, wobei der Änderungsschritt das Anordnen des Behälters (106), der eine gefrorene flüssige Lösung umfasst, in wärmeleitendem Kontakt mit dem Kühlkörper (101) umfasst.
 10. Verfahren nach Anspruch 1, wobei der Formgebungsschritt das Anordnen mindestens eines Abstandshalters (111) zwischen dem Behälter (106) und dem Kühlkörper (101) beinhaltet und der Änderungsschritt das Entfernen des mindestens einen Abstandshalters beinhaltet.
 11. Verfahren nach Anspruch 10, ferner umfassend das Anordnen des Behälters (106) auf einer Platte (110), wobei der Wärmeleitungsisolator (108) einen Trennungsabstand zwischen der Platte und dem Kühlkörper (101) umfasst und der mindestens eine Abstandshalter (111) zwischen der Platte und dem Kühlkörper angeordnet ist.
 12. Verfahren nach Anspruch 8, wobei der Schritt des Inkontaktbringens das Inkontaktbringen nach dem Einfrieren umfasst.
 13. Verfahren nach Anspruch 1, wobei der Wärmeleitungsisolator (108) nach dem Einfrieren der flüssigen Lösung in dem Behälter (106) verändert wird.
 14. Verfahren nach Anspruch 1, wobei der Wärmeleitungsisolator (108) während des Einfrierens der flüssigen Lösung in dem Behälter (106) verändert wird.
 15. Verfahren nach Anspruch 1, wobei der Wärmeleitungsisolator (108) verändert wird, um die Isolations-eigenschaften zu verringern.

Revendications

1. Procédé comprenant :

- l'utilisation d'une chambre de lyophilisation comprenant une surface de puits de chaleur en communication thermique avec un réfrigérant (103) ;
- le chargement d'un récipient (106) contenant une solution liquide dans la chambre de lyophilisation au-dessus de la surface du puits de chaleur, la solution liquide contenant un soluté d'agent pharmaceutiquement actif et un solvant, la solution liquide présentant une surface supérieure (116) et une surface intérieure (117) ;
- la formation d'un isolant thermoconducteur (108) entre le fond du récipient et la surface du

- puits de chaleur pour isoler le récipient d'une conductivité thermique avec le puits de chaleur ; l'abaissement de la température du puits de chaleur et ainsi de la température ambiante dans la chambre de lyophilisation comprenant le récipient à une température suffisante pour congeler la solution liquide, l'isolant thermoconducteur étant choisi pour réaliser la congélation de la solution liquide depuis les surfaces supérieure et inférieure à approximativement la même température et ainsi former une solution congelée ; et la réduction de la pression ambiante dans la chambre pour lyophiliser la solution congelée après modification de l'isolant thermoconducteur ;
- caractérisé en ce que** le procédé comprend : pendant ou après la congélation, la modification de l'isolant thermoconducteur.
2. Procédé selon la revendication 1, dans lequel l'isolant thermoconducteur (108) comprend un parmi un espace contenant de l'air, un gaz ou du vide.
 3. Procédé selon la revendication 1, dans lequel l'isolant thermoconducteur présente une conductivité thermique inférieure à environ 0,2 W/mK.
 4. Procédé selon la revendication 2, comprenant en outre un plateau (110) sur lequel repose le récipient entre le récipient et l'isolant thermoconducteur, le plateau étant éventuellement thermoconducteur ou calorifugé.
 5. Procédé selon la revendication 1, dans lequel le puits de chaleur comprend une conduite réfrigérante en communication thermique avec la surface de puits de chaleur.
 6. Procédé selon la revendication 1, dans lequel le récipient comprend un flacon, l'isolant thermoconducteur (108) comprenant éventuellement un élément de support à isolation thermique apposé au fond du flacon, et l'élément de support à isolation thermique reposant sur le puits de chaleur.
 7. Procédé selon la revendication 1, dans lequel la chambre de lyophilisation comprend au moins deux puits de chaleur parallèles (101) et comprenant en outre le chargement du récipient (106) comprenant la solution liquide dans la chambre de lyophilisation entre les deux puits de chaleur parallèles à des distances espacées verticalement du puits de chaleur avec un isolant thermoconducteur intercalé (108), les distances et l'isolant thermoconducteur intercalé étant choisis pour réaliser la congélation de la solution liquide depuis les surfaces supérieure (116) et inférieure (117) à approximativement la même température et ainsi former une solution congelée.
 8. Procédé selon la revendication 1, comprenant en outre le placement du récipient (106) sur un plateau (110), l'isolant thermoconducteur (108) comprenant une distance de séparation entre le plateau et le puits de chaleur (101), l'étape de modification comprenant éventuellement la mise en contact thermique du plateau (110) avec le puits de chaleur (101).
 9. Procédé selon la revendication 1, dans lequel l'étape de modification comprend le placement du récipient (106) comprenant une solution liquide congelée en contact thermoconducteur avec le puits de chaleur (101).
 10. Procédé selon la revendication 1, dans lequel l'étape de formation comprend le placement d'au moins un espaceur (111) entre le récipient (106) et le puits de chaleur (101) après que l'étape de modification comprend l'élimination de l'au moins un espaceur.
 11. Procédé selon la revendication 10, comprenant en outre le placement du récipient (106) sur un plateau (110), l'isolant thermoconducteur (108) comprenant une distance de séparation entre le plateau et le puits de chaleur (101) et l'au moins un espaceur (111) étant disposé entre le plateau et le puits de chaleur.
 12. Procédé selon la revendication 8, dans lequel l'étape de mise en contact comprend la mise en contact après la congélation.
 13. Procédé selon la revendication 1, dans lequel l'isolant thermoconducteur (108) est modifié après la congélation de la solution liquide dans le récipient (106).
 14. Procédé selon la revendication 1, dans lequel l'isolant thermoconducteur (108) est modifié pendant la congélation de la solution liquide dans le récipient (106).
 15. Procédé selon la revendication 1, dans lequel l'isolant thermoconducteur (108) est modifié pour diminuer les caractéristiques d'isolation.

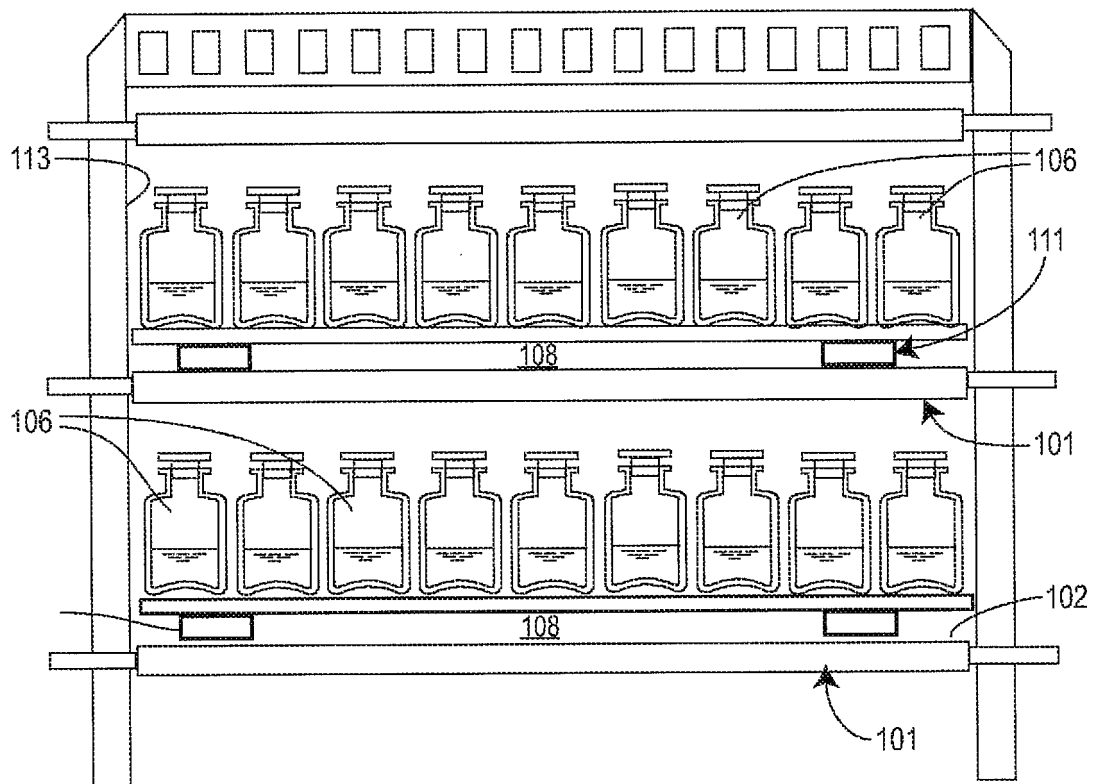


FIG. 1

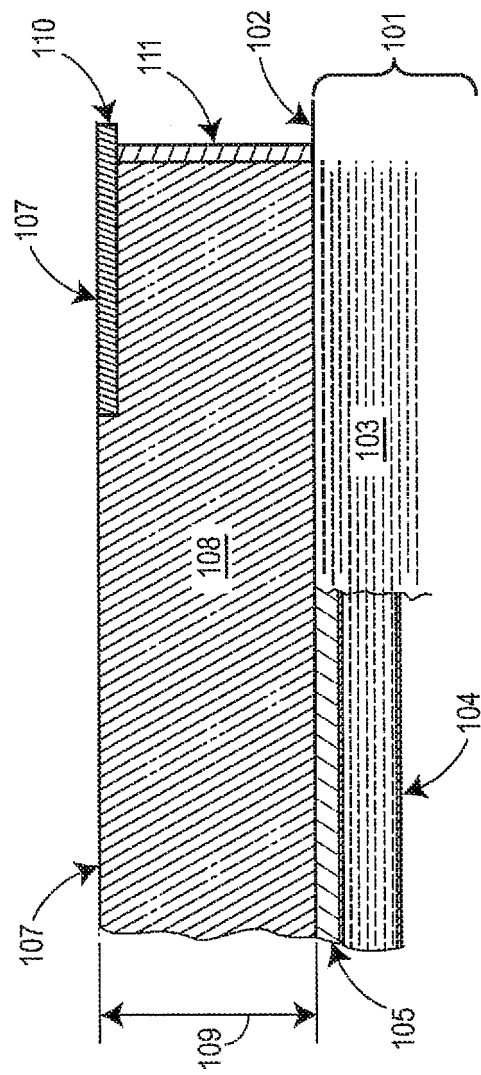


FIG. 2

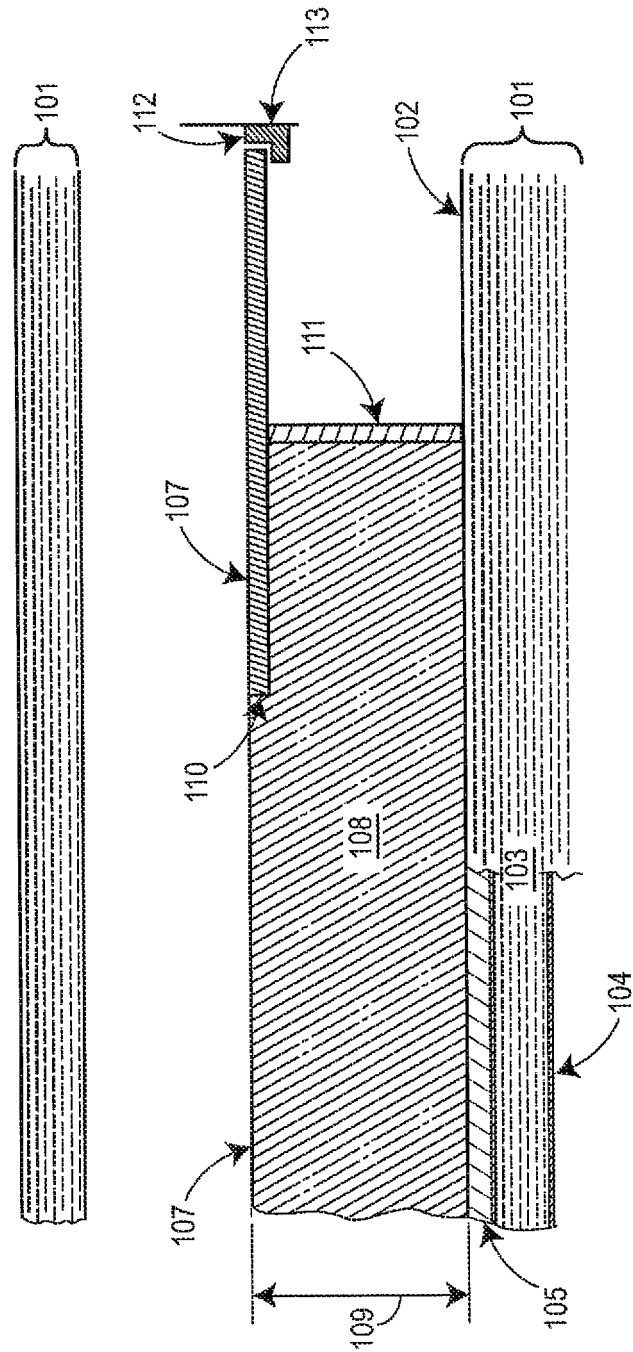


FIG. 3

A **FIG. 4**

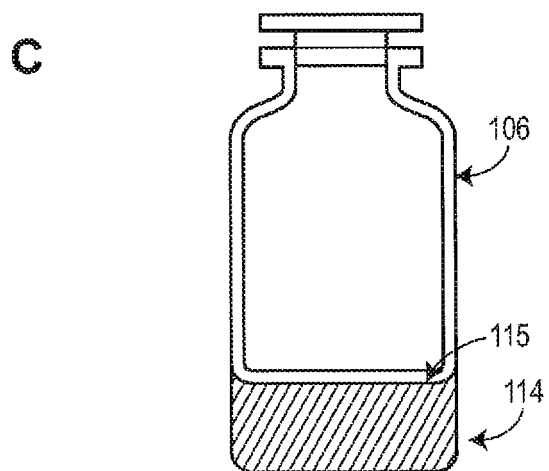
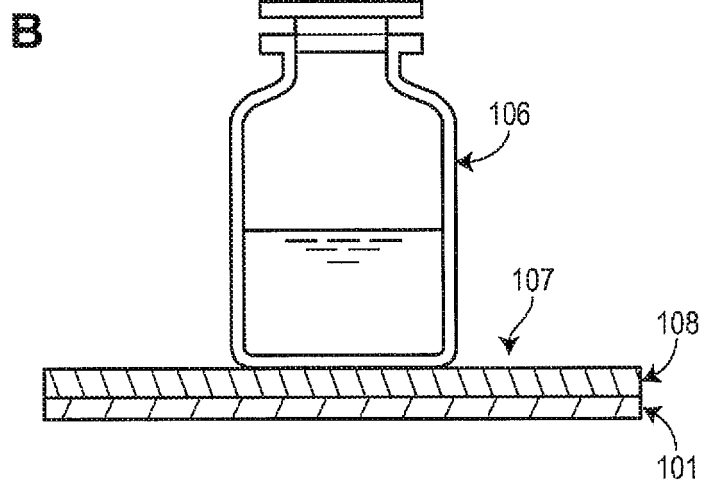
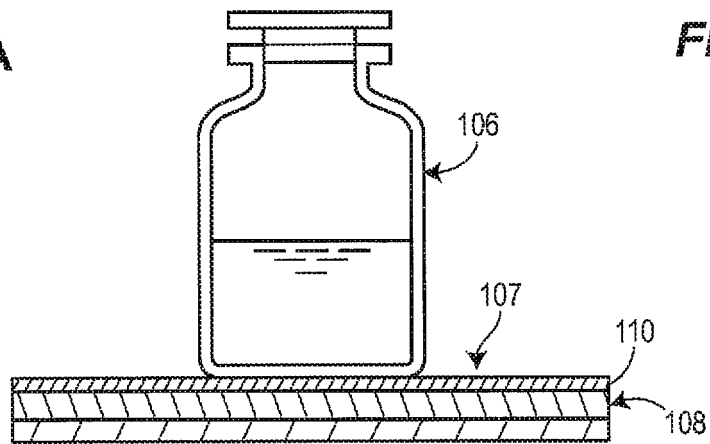


FIG. 5

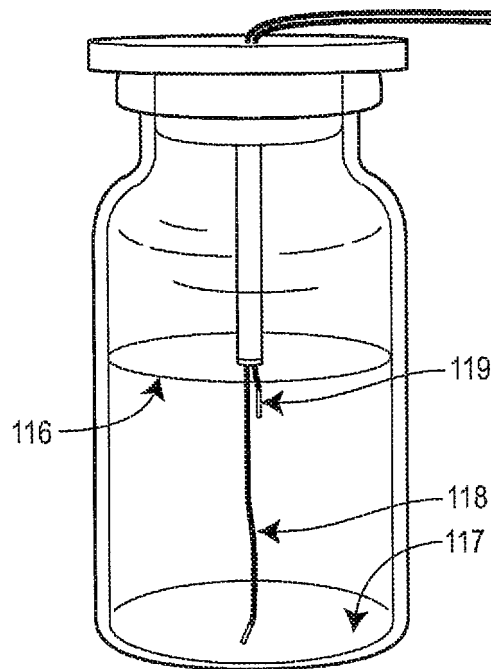


FIG. 6

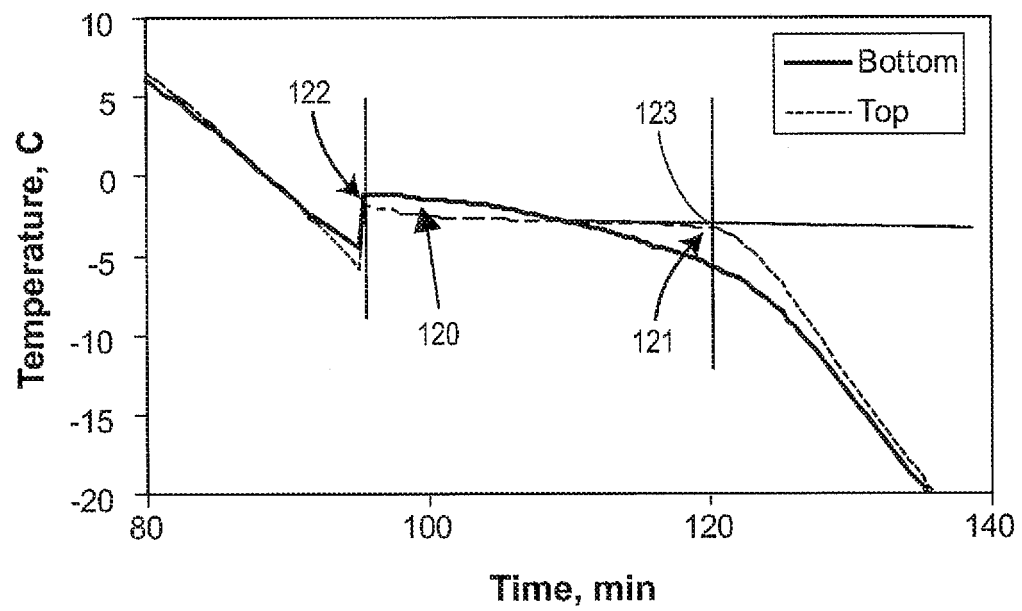
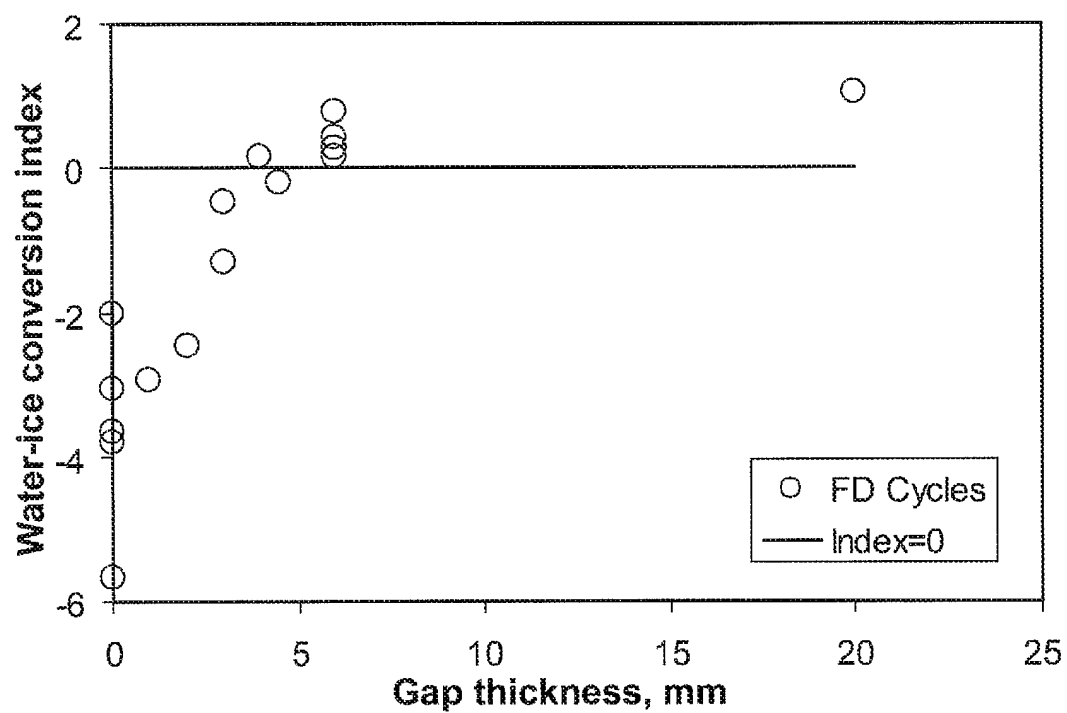
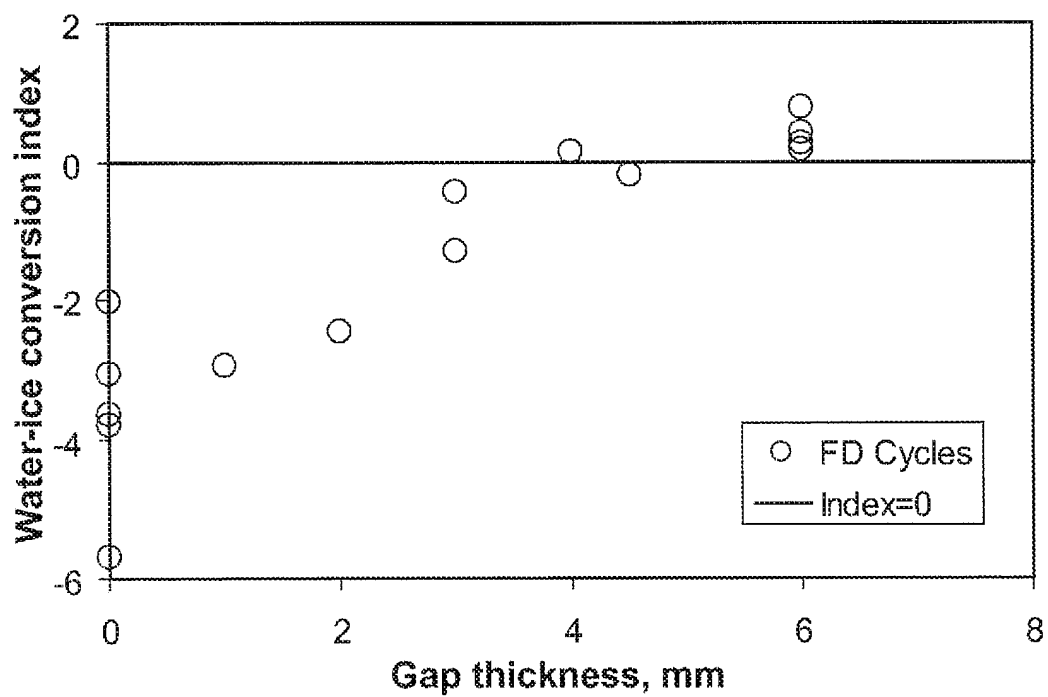


FIG. 7A**FIG. 7B**

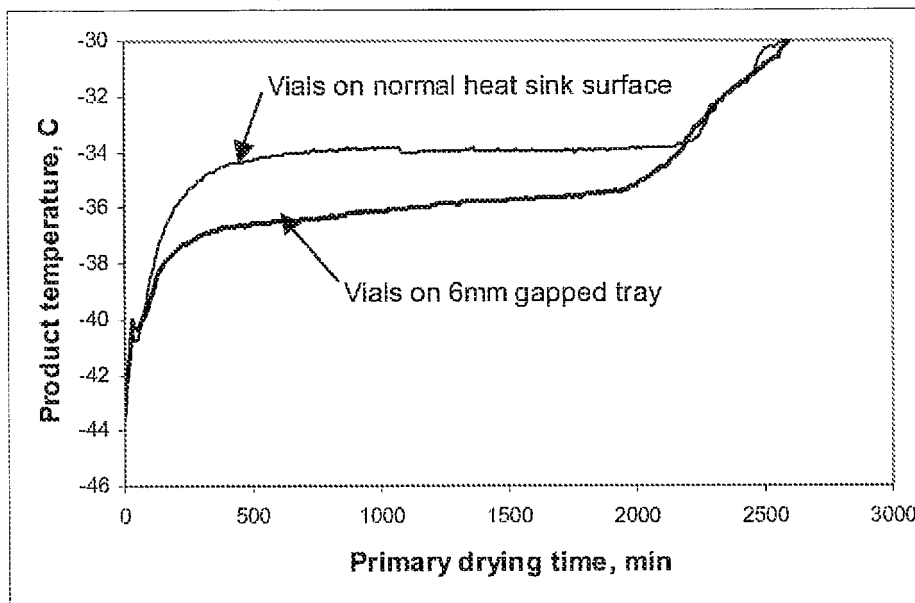


FIG. 8

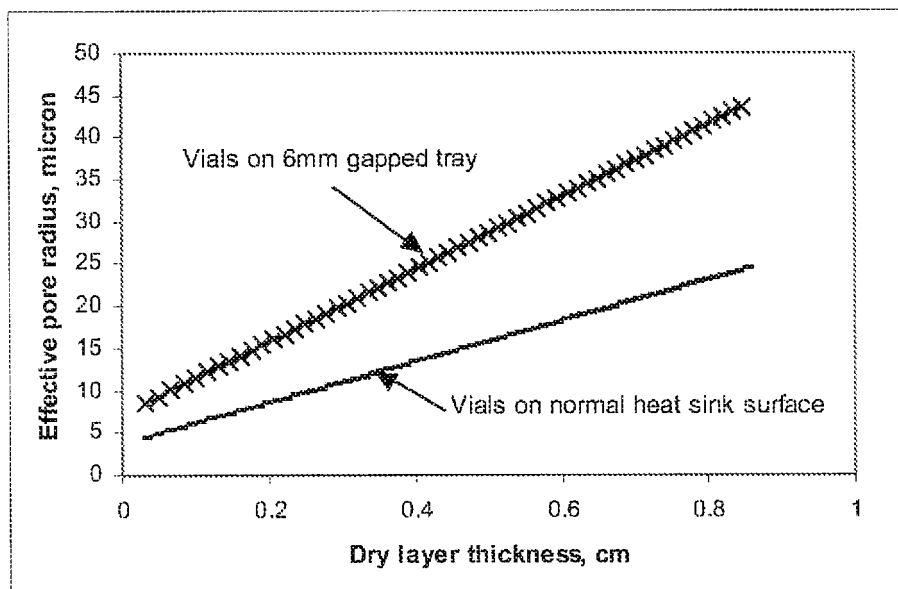


Fig. 9

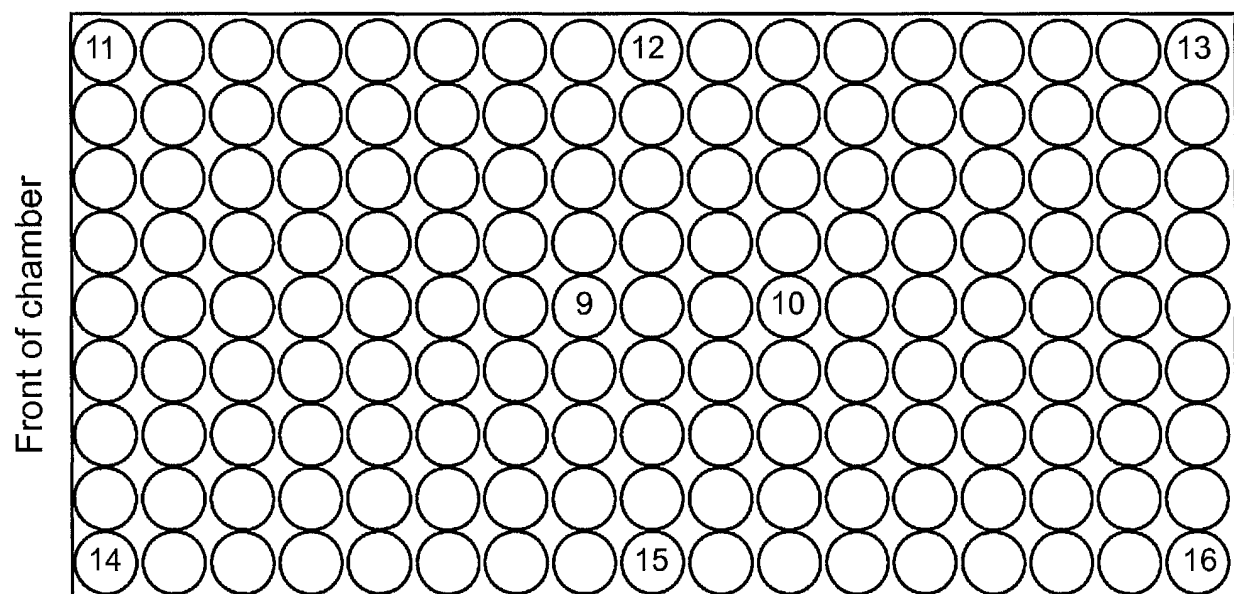
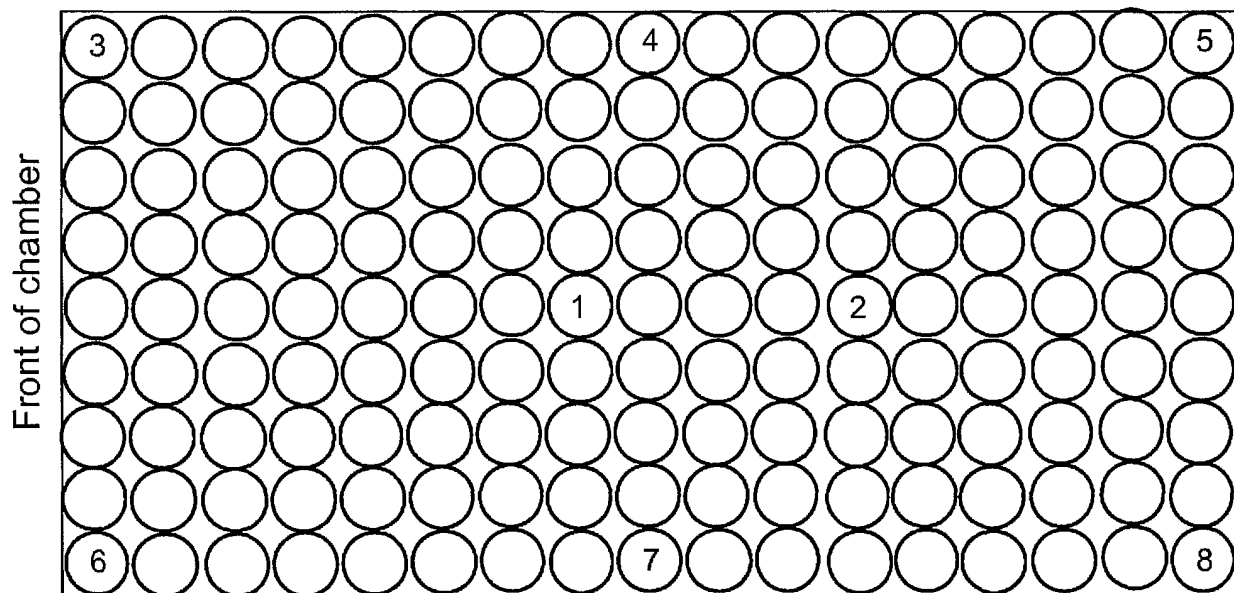


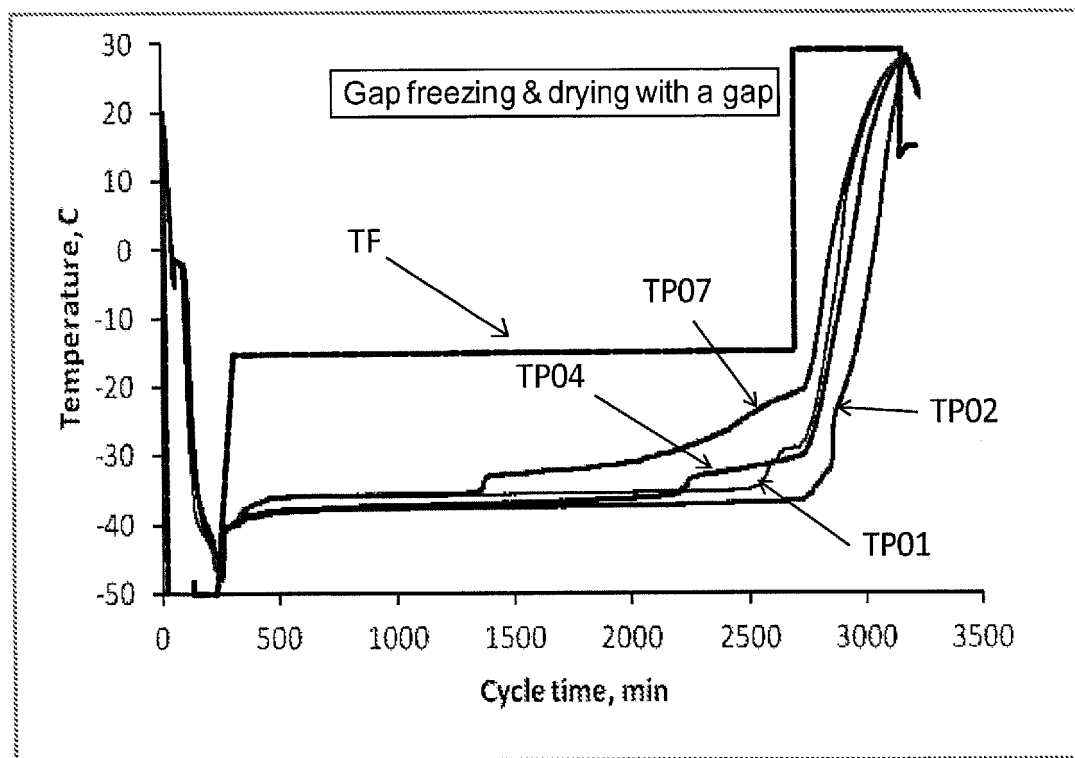
FIG. 12

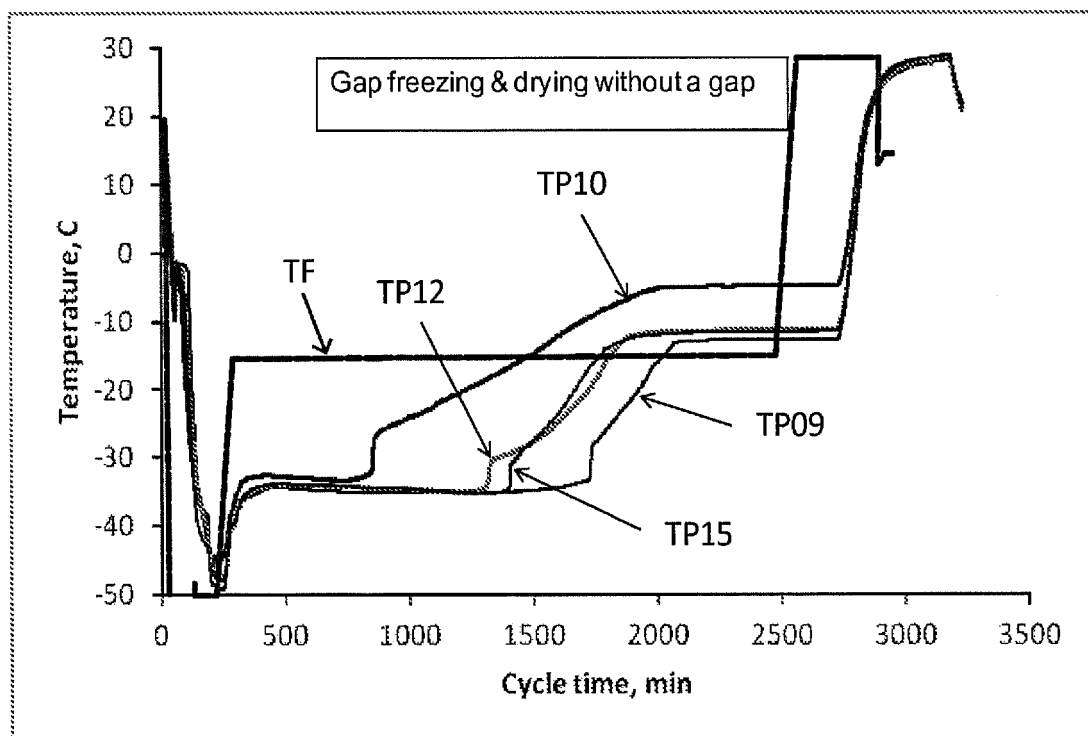
FIG. 13

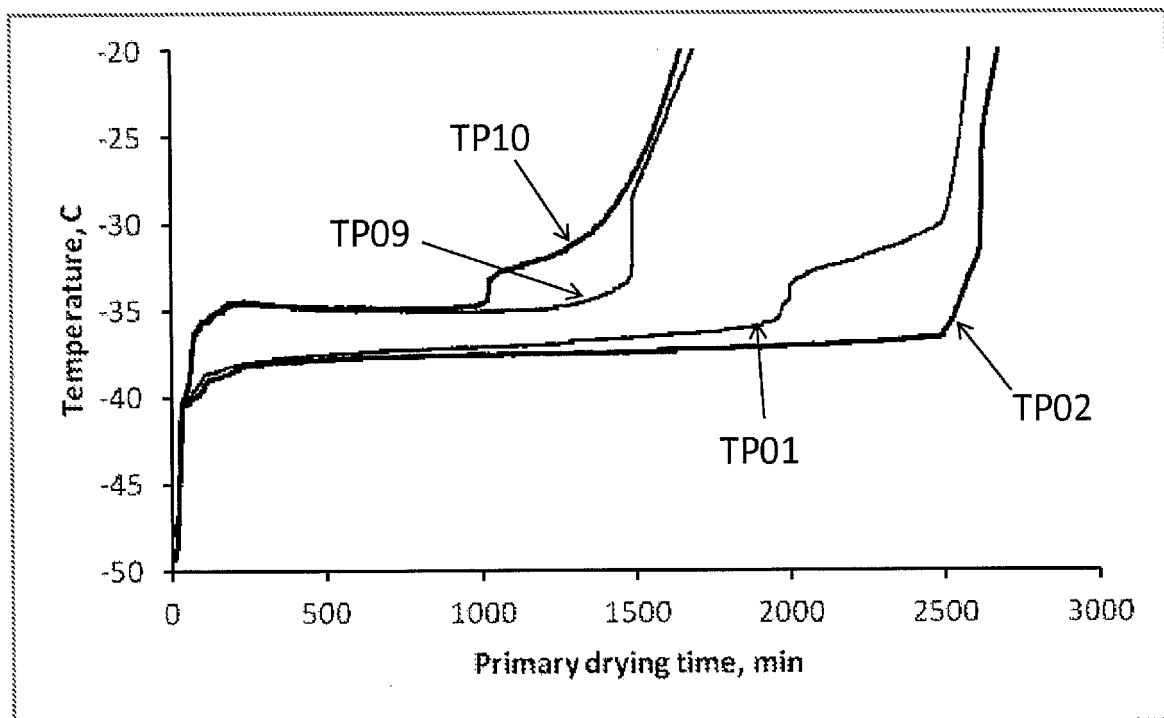
FIG. 14

FIG. 15

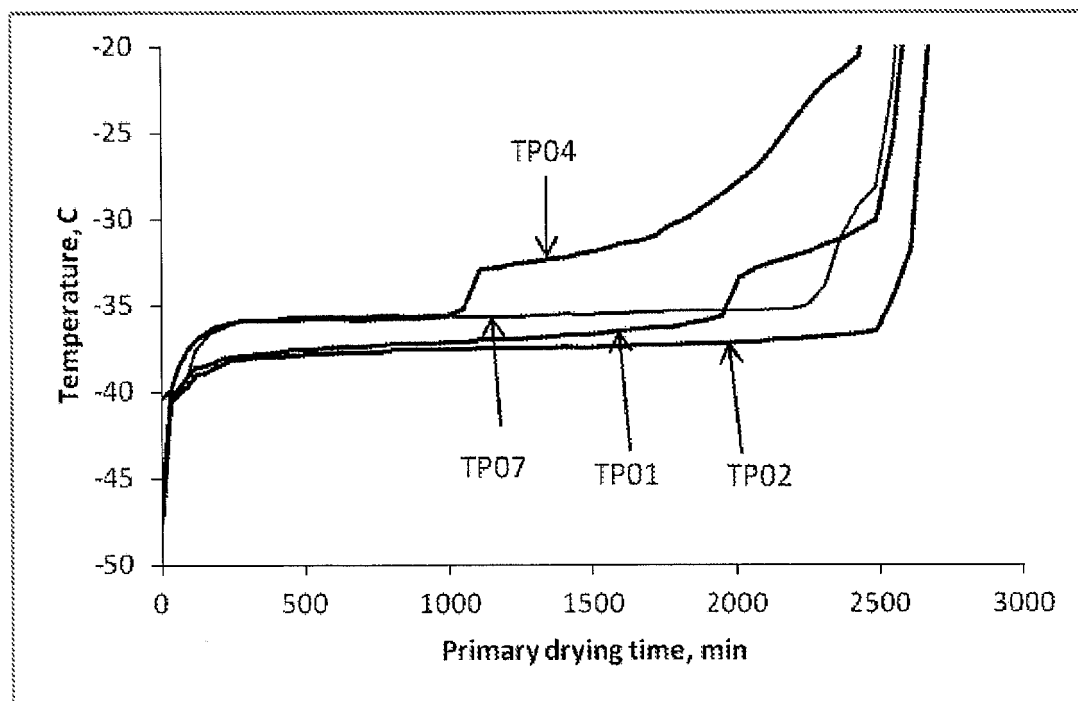
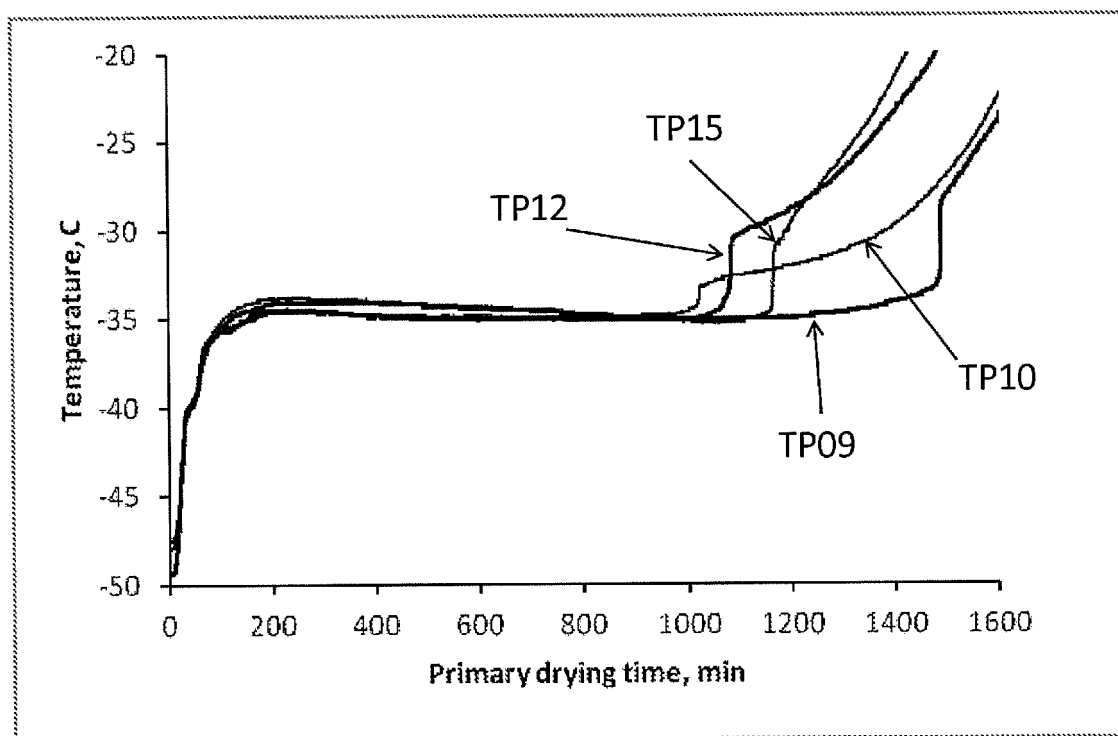


FIG. 16



REFERENCES CITED IN THE DESCRIPTION

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