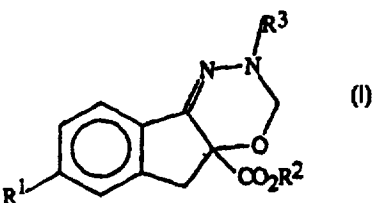
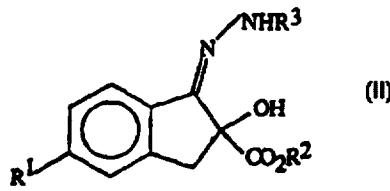




INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶: C07D 273/04 // A01N 47/38	A1	(11) International Publication Number: WO 98/05656 (43) International Publication Date: 12 February 1998 (12.02.98)
<p>(21) International Application Number: PCT/US97/13548</p> <p>(22) International Filing Date: 31 July 1997 (31.07.97)</p> <p>(30) Priority Data: 60/022,426 5 August 1996 (05.08.96) US</p> <p>(71) Applicant (for all designated States except US): E.I. DU PONT DE NEMOURS AND COMPANY [US/US]; 1007 Market Street, Wilmington, DE 19898 (US).</p> <p>(72) Inventor; and (75) Inventor/Applicant (for US only): DUMAS, Donald, J. [US/US]; 407 Baynard Boulevard, Wilmington, DE 19803 (US).</p> <p>(74) Agent: KATZ, Elliott, A.; E.I. du Pont de Nemours and Company, Legal Patent Records Center, 1007 Market Street, Wilmington, DE 19898 (US).</p>		<p>(81) Designated States: AL, AM, AU, AZ, BA, BB, BG, BR, BY, CA, CN, CU, CZ, EE, GE, HU, IL, IS, JP, KG, KP, KR, KZ, LC, LK, LR, LT, LV, MD, MG, MK, MN, MX, NO, NZ, PL, RO, RU, SG, SI, SK, SL, TJ, TM, TR, TT, UA, US, UZ, VN, YU, ARIPO patent (GH, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG).</p> <p>Published <i>With international search report.</i></p>
<p>(54) Title: PROCESSES FOR PREPARING INDENO[1,2-E][1,3,4]OXADIAZINE-DICARBOXYLATES</p>		
<div style="display: flex; justify-content: space-around; align-items: center;"> <div style="text-align: center;">  <p>(I)</p> </div> <div style="text-align: center;">  <p>(II)</p> </div> </div>		
<p>(57) Abstract</p> <p>Oxadiazines of formula (I), wherein R¹ is F, Cl or fluoralkoxy and R² is alkyl, are prepared by reacting hydrazine derivatives of formula (II) with a dialkoxymethane in the presence of a protic acid catalyst in an inert solvent under conditions which allow for the prompt removal of the alcohol by-product by distillation. The reaction can be combined with the preparation of the hydrazines derivatives (II) from the corresponding ketones and hydrazines NH₂-NHR³ in the presence of the same protic acid catalyst and an inert solvent. Oxadiazines I are useful as intermediates in the preparation of arthropodocidal agents.</p>		

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TITLE

PROCESSES FOR PREPARING INDENO[1,2-E][1,3,4]OXADIAZINE-DICARBOXYLATES

FIELD OF INVENTION

5 This invention relates to processes for preparing intermediates, particularly of dicarboxylate oxadiazines of Formula I and hydrazine carboxylates of Formula II, which are useful in the preparation of arthropodicidal oxadiazines.

BACKGROUND OF THE INVENTION

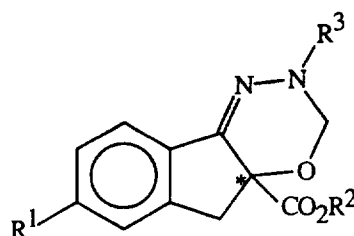
WO95/29171 discloses the preparation of arthropocidal oxadiazines from
10 dicarboxylate oxadiazines of Formula I and hydrazine carboxylates of Formula II.

In WO95/29171, compounds of Formula I are prepared by reacting compounds of Formula II with a di(C₁-C₃ alkoxy)methane in the presence of a Lewis acid, optionally in an inert solvent. The Lewis acids named are P₂O₅, BF₃, SO₃ (0.9 to 4.0 molar equivalent required) and metal trifluoromethanesulfonates (0.1 to 0.5 molar equivalent required). All of
15 the specifically named solvents for this transformation are halogenated (dichloromethane, 1,2-dichloroethane, chlorobenzene, a,a,a -trifluorotoluene). It is stated that when a metal trifluoromethanesulfonate is employed, it is preferable to continuously remove the byproduct alcohol by distillation. In contrast, the process of the present invention allows for the use of a protic acid such as *para*-toluene sulfonic acid in catalytic quantities, such as 0.1 molar
20 equivalent in a non-halogenated solvent (e.g. toluene) to provide good product quality in high chemical yield.

The need exists for a more efficient process to prepare oxadiazines of Formula I from hydrazine carboxylates of Formula II.

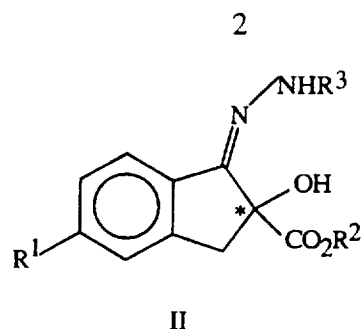
SUMMARY OF THE INVENTION

25 The present invention pertains to processes for preparing oxadiazine dicarboxylates of Formula I which are racemic or enantiomerically enriched at chiral center*



I

30 wherein R¹ is F, Cl, or C₁-C₃ fluoroalkoxy, R² is C₁-C₃ alkyl, and R³ is a protecting group such as CO₂CH₂(C₆H₅) comprising: reacting a compound of Formula II, which is racemic or enantiomerically enriched at*,

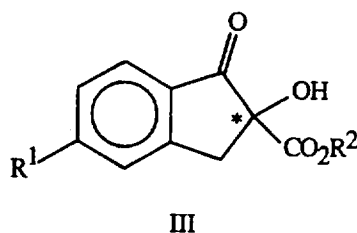


with a di(C₁-C₃ alkoxy)methane in the presence of a protic acid catalyst in an inert solvent under conditions which allow for the prompt removal of the by-product alcohol by

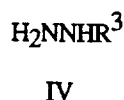
distillation.

This invention further pertains to processes for preparing compounds of Formula I as defined above comprising:

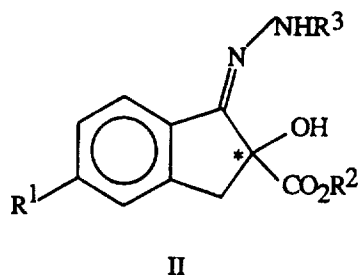
(a) reacting a compound of Formula III, which is racemic or enantiomerically enriched at*,



with the compound of Formula IV in the presence of a protic acid catalyst in an inert solvent



to form a compound of Formula II



and (b) reacting the compound of Formula II with a di(C₁-C₃ alkoxy)methane in the presence of the same protic acid catalyst and inert solvent as used in step (a) under conditions which allow for the prompt removal of the by-product alcohol by distillation.

In the above recitations, the term "C₁-C₃ fluoroalkoxy" refers to methoxy, ethoxy, *n*-propoxy and *iso*-propoxy which may be partially or fully substituted with fluorine atoms. Examples of "fluoroalkoxy" include CF₃O and CF₃CH₂O.

DETAILED DESCRIPTION OF THE INVENTION

The compounds of Formula I can be prepared by the process of this invention which comprises the process variations as described below.

Preferred compounds of Formula I are those where R¹ is F, Cl, CF₃O or CF₃CH₂O,
5 (more preferably Cl) and R² is CH₃.

Any protic acid can be used in the process of this invention as a catalyst. Suitable protic acid catalysts include mineral acids such as sulfuric acid and sulfonic acids such as aromatic, aliphatic and polymeric sulfonic acids. Preferred for reasons of greater commercial utility and/or ease of practice in the process for preparing compounds of Formula I are protic
10 acids which do not co-distill to any significant extent with the by-product alcohol and which do not react with the dialkoxymethane to form products which could co-distill with the by-product alcohol. The preferred acids are those which catalyze both the reaction of compounds of Formula III with compounds of Formula IV, to give compounds of Formula II, and the conversion of compounds of Formula II to compounds of Formula I. Examples of
15 the preferred acids are *para*-toluenesulfonic acid, mixtures of the isomeric toluenesulfonic acids, benzenesulfonic acid, naphthalene sulfonic acids, xylenesulfonic acids, methanesulfonic acid, sulfuric acid, and camphor sulfonic acids. Most preferred are *para*-toluenesulfonic acid and mixtures of isomeric toluenesulfonic acids.

While stoichiometric or greater amounts of the protic acid can be employed, it is
20 preferred for reasons of greater commercial utility and/or ease of practice in the process for preparing compounds of Formula I, from either compounds of Formula II or compounds of Formula III that a catalytic amount of the protic acid be employed. It is more preferred that a total of between 0.01 and 0.20 molar equivalent of protic acid, relative to the compound of Formula II or Formula III, be employed. Most preferred is the process in which between
25 0.05 to 0.10 molar equivalent of protic acid is employed. In general, the use of 0.05 to 0.10 molar equivalent of protic acid allows for useful reaction rates while minimizing acid use and waste generation.

The solvent used in the process of this invention can be any inert solvent which when combined with the reactants used in the process of the present invention forms a reaction
30 mixture from which the alcohol produced as a by-product in the process of this invention, such as ethanol, can be promptly separated by distillation. Depending on the specific reaction conditions, the alcohol can be removed as: (a) the alcohol; (b) an azeotrope or mixture of the alcohol and di(C₁-C₃ alkoxy)methane; (c) an azeotrope or mixture of the alcohol and solvent; or, (d) an azeotrope or mixture of the alcohol, di(C₁-C₃ alkoxy) methane
35 and solvent. Preferred for ease of operation, cost, toxicity and environmental reasons are non-halogenated solvents such as, aliphatic and aromatic hydrocarbons and alkyl nitriles. More preferred are aliphatic and aromatic hydrocarbons and alkyl nitriles with boiling points between 80 and 150°C. Most preferred are toluene, xylenes, heptane and acetonitrile.

The alcohol or alcohol-containing component can be distilled from the reaction mixtures using equipment and techniques known to those skilled the art. Equipment and procedures which allow for efficient removal of alcohol while minimizing co-distillation of di(C₁-C₃ alkoxy) methane and/or solvent are preferred. This can be achieved using conventional fractional distillation equipment.

The reaction of compounds of Formula II with a di(C₁-C₃ alkoxy)methane is most conveniently run at the boiling point of the reaction mixture at ambient pressure. Reaction temperatures need to be at least equal to the boiling point of the by-product alcohol (e.g., ethanol) or of the alcohol containing azeotrope or mixture being removed. Preferred for reasons of greater commercial utility and/or ease of practice in the process for preparing compounds of Formula I from compounds of Formula II is a reaction temperature from between about 40 and 150°C that allows for distillation of by-product alcohol. More preferred is a reaction temperature between 60 and 130°C. Most preferred is a reaction temperature between about 80 and 120°C. The reaction may also be carried out at elevated or reduced pressure. The use of reduced pressure can be particularly advantageous when using higher boiling solvents.

The reaction of compounds of Formula III with the compound of Formula IV is conducted at a reaction temperature from about 40 to 120°C. More preferred is a reaction temperature from about 50 to 90°C. Although the reaction can be carried out at ambient pressure, the reaction may also be carried out at elevated or reduced pressure. The use of reduced pressure can be particularly advantageous when using solvents that have boiling points higher than the desired reaction temperature. When preparing compounds of Formula II from compounds of Formula III and the compound of Formula IV, it is preferable that the by-product water be removed from the reaction mixture prior to combination of the reaction mixture with the di(C₁-C₃ alkoxy)methane. More preferably, the by-product water can be removed by distillation as it is formed.

In principle, only one molar equivalent of di(C₁-C₃ alkoxy) methane is needed. However, sufficient di(C₁-C₃ alkoxy) methane should be employed so as to allow for losses of di(C₁-C₃ alkoxy) methane via co-distillation. Any practical amount of the di(C₁-C₃ alkoxy)methane can be employed in the process of this invention and it can be used as the solvent for the reaction to convert compounds of Formula II to compounds of Formula I. For reasons of economy it is preferable to use between about 1 and 20 equivalents of the di(C₁-C₃ alkoxy)methane in conjunction with an inert solvent. More preferably between 1 and 10 equivalents of the di(C₁-C₃ alkoxy)methane can be employed, most preferably between 2 and 7 equivalents. Preferred are the di(C₂-C₃ alkoxy) methanes because they are higher boiling than the C₂-C₃ alcohols which they produce in the course of the reaction. This allows for removal of alcohol by distillation without removing large amounts of the

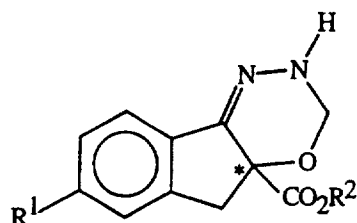
di(C₂-C₃ alkoxy)methane. Diethoxymethane is most preferred di (C₂ -C₃ alkoxy) methane because of availability and low cost.

In the reactions of compounds of Formula II with a di(C₁-C₃ alkoxy)methane, the reagents should be combined at a rate such that the by-product alcohol produced is promptly and efficiently removed to avoid the formation of side-reaction products which adversely affect the purity and yield of the desired product. In one embodiment, a slurry of the hydrazine carboxylate of Formula II containing all or part of the solvent and optionally containing all or part of the protic acid and all or part of the di (C₁-C₃ alkoxy) methane is added over time to a mixture of the balance of solvent, protic acid and di(C₁-C₃ alkoxy) methane which has been preheated to the appropriate reaction temperature. In an alternative embodiment, the di(C₁-C₃ alkoxy)methane can be added to a mixture of the hydrazine carboxylates of Formula II, solvent and protic acid which has been preheated to the appropriate reaction temperature. When the protic acid and the di(C₁-C₃ alkoxy)methane are combined and heated prior to combination with the hydrazine carboxylate of Formula II, it is preferable to distill out any alcohol produced by the reaction of the acid with the di(C₁-C₃ alkoxy)methane as it is formed.

The present invention further pertains to processes for preparing compounds of Formula I comprising: Step (a) preparing compounds of Formula II from compounds of Formula III and Step (b) reacting the compounds of Formula II with a di(C₁-C₃ alkoxy) methane under conditions which allow for prompt removal of the by-product alcohol by distillation wherein both steps are carried out in the presence of the same protic acid catalyst and inert solvent.

A compound of Formula I can be further converted to arthropodicidal oxadiazines of Formula VII by

(a) hydrogenating the compound of Formula I to form a compound of Formula V

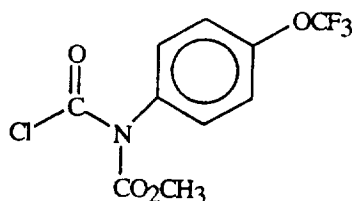


and

V

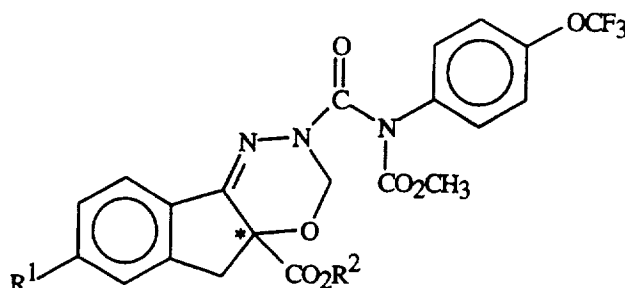
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(b) reacting the compound of Formula V with the compound of Formula VI



VI

to form a compound of Formula VII having substantially the same absolute configuration as the compound of Formula I.



VII

The preparation of the compound of Formula VI is described in WO 95/29171.

Without further elaboration, it is believed that one skilled in the art using the preceding description can utilize the present invention to its fullest extent. The following Examples are, therefore, to be construed as merely illustrative, and not limiting of the disclosure in any way whatsoever. Percentages are by weight except for the chromatographic solvent mixture which is by volume.

EXAMPLE 1

Preparation of 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e][1,3,4]oxadiazine-2,4a(3H,5H)-dicarboxylate

A 1 L, 4-neck round bottom flask (RBF) was equipped with an overhead stirrer with an oval paddle, thermometer, liquid feed line with an FMI (Fluid Metering Inc.) pump, 10 tray Oldershaw column equipped with a variable takeoff head, condenser and nitrogen inlet, and a heating mantel. The system was set up so that temperature could be monitored in the pot, at the 2, 4, 6, 8, 10 trays of the Oldershaw column and at the distillation head. Circulation of chilled water through the condenser was initiated. The flask was charged with 50 mL (0.4 mol) of Aldrich diethoxymethane and 100 mL of toluene and heated to reflux. The pot and head temperatures were 106°C and 83°C, respectively. Column temperatures at the second, forth, sixth, eighth and tenth trays (from bottom to top) were 97°C, 93°C, 90°C, 88°C and 83°C. In a separate flask, a mixture of 1.15 g of *para*-toluenesulfonic acid monohydrate and 125 mL of toluene was dried by azeotropic distillation of about 45 mL of

the solvent using a Dean-Stark trap. The resulting mixture was allowed to cool to ambient temperature and 24.56 g (0.06 mol, 94.8% assay) of racemic phenylmethyl[5-chloro-2,3-dihydro-2-hydroxy-2-(methoxycarbonyl)-1 H-inden-1-ylidene]hydrazinecarboxylate disclosed in WO95/29171 added to give a slurry. This slurry was then pumped into the refluxing mixture of diethoxymethane and toluene over 2 hours and 24 minutes and rinsed in with toluene. Once the temperature at the eighth tray (counting from the bottom) of the column dropped below 80°C, takeoff ethanol/diethoxymethane/toluene distillate was initiated at such a rate as to maintain the temperature at the fourth tray at 79-83°C. After the addition of the slurry was complete, the distillate was slowly collected until the temperature at the eighth tray reached 88°C. The rate of take off was then increased and distillation continued until the head temperature reached 110°C. A total of about 117 mL (99.0 g) of distillate was collected. The reaction mixture was allowed to cool, and concentrated using a rotary evaporator; the residue was dissolved in ethyl acetate, filtered, and the filtrate concentrated using a rotary evaporator to leave 29.12 grams of oil. The oil was slurried with 75 mL of methanol and cooled in an ice bath. The crystals which formed were collected, washed with two 10 mL portions of cold methanol, and dried in a vacuum oven to give 21.0 grams (87% yield) of product which assayed (HPLC, 4.6X250 mm 5-micron, Zorbax® SB-C8 column and eluting at 1.5 mL/min. with 60% acetonitrile/40% water, 40°C, UV detector set at 254 nm) as 98.99% 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e][1,3,4]oxadiazine-2,4a(3H,5 H)-dicarboxylate. m. p. 113-123°C.

EXAMPLE 2

Preparation of 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e][1,3,4]oxadiazine-2,4a(3H,5H)-dicarboxylate

A 1L, 4-neck RBF was equipped with an overhead stirrer with an oval paddle, thermometer, Dean-Stark trap, reflux condenser, and a heating mantle. The reactor was charged with 45.7 g (0.183 mol), 96.3% assay of racemic methyl 5-chloro-2,3-dihydro-2-hydroxy-1-oxo-1H-indene-2-carboxylate disclosed in WO 95/29171, 35.1 g (0.21 mol) of 99.4% phenylmethyl hydrazine carboxylate, 3.5 g (0.018 mol) of *para*-toluene sulfonic acid monohydrate, and 235 mL of toluene. The mixture was heated to reflux for 7 h under a vacuum (~168 to 205 mm) sufficient to maintain the boiling point of the mixture between 65 and 72°C. During this time, 3.4 mL of water was collected in the Dean-Stark trap. Heating was discontinued and the flask returned to atmospheric pressure. On cooling to ambient temperature, the Dean-Stark trap and reflux condenser were removed and replaced with a 5 tray Oldershaw column equipped with a variable takeoff head, condenser and nitrogen inlet. The flask was further equipped with a liquid feed line with an FMI (Fluid Metering Inc.) pump. The system was set up so that temperature could be monitored in the pot, at each tray of the Oldershaw column and at the distillation head. Circulation of chilled water through the condenser was initiated and the reaction mixture heated to reflux. The pot and head

temperatures were 113°C and 110°C, respectively. Column temperatures (from bottom to top) were 111°C, 110°C, 110°C, 110°C, and 110°C. Diethoxymethane (68 mL, 0.54 mol) was then pumped into the reaction mixture at a steady rate over 1 h and 6 min. Once the temperature at the fourth tray (counting from the bottom) of the column dropped below 80°C, takeoff of ethanol/diethoxymethane/toluene distillate was initiated at such a rate as to maintain the temperature at the fourth tray at 77-84°C. After the addition was complete, distillate was slowly collected over 50 min until the temperature at the fourth tray reached 91°C. The rate of take off was then increased and distillation continued until the head temperature reached 108°C. A total of about 104 mL (84.9 g) of distillate was collected. The reaction mixture was allowed to cool, concentrated using a rotary evaporator, the residue dissolved in 210 mL of methanol and cooled in an ice bath. The crystals which formed were collected, washed with three 30 mL portions of cold methanol, and dried in a vacuum oven to give 61.17 g (82% yield) of tan product which assayed (HPLC, 4.6X250 mm 5-micron, Zorbax® SB-C8 column and eluting at 1.5 mL/min. with 60% acetonitrile/40% water, 40°C, UV detector set at 254 nm) as 96.98% 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e][1,3,4]oxadiazine-2,4a(3H,5H)-dicarboxylate. m.p. 120-122°C

EXAMPLE 3

Preparation of 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e]-[1,3,4]oxadiazine-2,4a(3H,5 H)-dicarboxylate

Step A

A 2 L, 4-neck round bottomed flask was equipped with: an overhead stirrer with an oval paddle; thermometer; a Dean-Stark trap with a reflux condenser and nitrogen inlet; and a heating mantle. The reactor was purged with nitrogen and charged with 583 g of toluene, 120.7 g (0.50 mol, 99.68% assay) of 62% ee 5-chloro-2,3-dihydro-2-hydroxy-oxo-1H-indene-2-carboxylate, 94.13 g (0.55 mol) of 97% benzyl carbazate and 9.65 g (0.05 mol) of 98.5% *para*-toluene sulfonic. The mixture was heated to reflux under a vacuum (about 184 mm) sufficient to give a boiling point of 70°C. After a total of 6 h at reflux, the reaction mixture was allowed to cool to room temperature. Just prior to use in Step B, 131.5 g of diethoxymethane was added to the slurry.

Step B

A 3 L, 4-neck round bottomed flask was equipped with: an overhead stirrer with an oval paddle; thermometer; 5 tray Oldershaw column equipped with a variable take off head, condenser and nitrogen inlet; and a heating mantle. The system was set up so that temperature could be monitored in the pot, at each tray of the Oldershaw column and at the distillation head. Circulation of chilled water through the condenser was initiated. The flask was charged with 26.3 g (0.25 mol) of Aldrich diethoxymethane and 580 g of toluene and heated to reflux with a boil up of about 35 mL/min. The pot and head temperatures were 111°C and 102°C, respectively. Column temperatures at the first, second, third, forth, and

fifth trays (from bottom to top) were 109°C, 107°C, 106°C, 104°C and 102°C. The Step A slurry was then metered into the boiling solution over 6 h and 20 min and rinsed in with a mixture of 50 g of toluene and 26.3 g of diethoxymethane. As the addition proceeded, temperatures in the column and at the distillation head decreased. Once the temperature at the forth tray (counting from the bottom) of the column dropped to 80°C, takeoff off ethanol/diethoxymethane/toluene distillate was initiated at such a rate as to maintain the temperature at the fourth tray at about 80 to 84°C. After the addition was complete, distillate was slowly collected until the temperature at the forth tray reached 101°C. Take off of distillate was discontinued for 10 min during which time the temperature at the forth tray stayed at 101°C. Take off was then resumed at an increased rate until the head temperature reached 109°C. A total of about 328 mL (249 g) of distillate was collected. The reaction mixture was allowed to cool and the solvent then removed by distillation at 35 mm Hg until the pot temperature reached 70°C. Ethanol (360 mL) was then added and the mixture heated to reflux for 1 hour and allowed to cool. When the temperature reached 40°C, 30 mL of water was added and the mixture cooled to about 0°C. The product was collected by filtration, displacement washed with four cold 50 mL portions of ethanol, and dried on the filter to give 176.9 g (85% yield) of product which assayed (HPLC, 4.6X250 mm 5-micron, Zorbax® SB-C8 column and eluting at 1.5 mL/min. with 60% acetonitrile/40% water, 40°C, UV detector set at 254 nm) as 96.91% 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e][1,3,4]oxadiazine-2,4a(3H,5 H)-dicarboxylate with an ee of 70%. m. p. 103-120°C.

EXAMPLE 4

Preparation of 4a-methyl 2-(phenylmethyl)-7-chloroindeno- [1,2-e][1,3,4]oxadiazine-2,4a(3H,5 H)-dicarboxylate

Step A

A 2 L, 4-neck round bottomed flask was equipped with: an overhead stirrer with an oval paddle; thermometer; a Dean-Stark trap with a reflux condenser and nitrogen inlet; and a heating mantel. The reactor was purged with nitrogen and charged with 583 g of toluene, 120.7 g (0.50 mol, 99.68% assay) of 62% ee 5-chloro-2,3-dihydro-2-hydroxy-oxo-1H-indene-2-carboxylate, 94.13 g (0.55 mol) of 97% benzyl carbazate and 4.85 g (0.05 mol) of 99% methanesulfonic acid. The mixture was heated to reflux under a vacuum (about 184 mm) sufficient to give a boiling point of 70°C. After a total of 5.25 h at reflux, the reaction mixture was allowed to cool to room temperature. Just prior to use in Step B 131.5 g of diethoxymethane was added to the slurry.

Step B

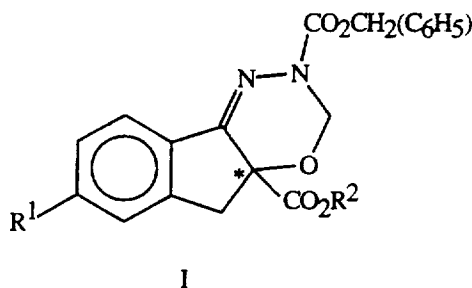
A 3 L, 4-neck round bottomed flask was equipped with: an overhead stirrer with an oval paddle; thermometer; 5 tray Oldershaw column equipped with a variable take off head, condenser and nitrogen inlet; and a heating mantel. The system was set up so that temperature could be monitored in the pot, at each tray of the Oldershaw column and at the

distillation head. Circulation of chilled water through the condenser was initiated. The flask was charged with 26.3 g (0.25 mol) of Aldrich diethoxymethane and 580 g of toluene and heated to reflux with a boil up of about 26 mL/min. The pot and head temperatures were 111°C and 102°C, respectively. Column temperatures at the first second, third, forth, and fifth trays (from bottom to top) were 108°C, 107°C, 106°C, 103°C and 102°C. The Step A slurry was then metered into the boiling solution over about 4 h and rinsed in with 50 g of toluene. As the addition proceeded, temperatures in the column and at the distillation head decreased. Once the temperature at the forth tray (counting from the bottom) of the column dropped to 80°C, takeoff off ethanol/diethoxymethane/toluene distillate was initiated at such a rate as to maintain the temperature at the fourth tray at about 78 to 82°C. After the addition was complete, distillate was slowly collected until the temperature at the forth tray reached 94°C. Take off was then resumed at an increased rate until the head temperature reached 108°C. A total of about 306 mL (234 g) of distillate was collected. The reaction mixture was allowed to cool and the solvent then removed by distillation at 35 mm Hg until the pot temperature reached 71°C. Ethanol (560 mL) was then added and the mixture heated to reflux until the all of the precipitated solids dissolved. The solution was then cooled to about 0°C. The product was collected by filtration, displacement washed with six cold 50 mL portions of ethanol, and dried to give 164.1 g of product 4a-methyl 2-(phenylmethyl)-7-chloroindeno[1,2-e][1,3,4]oxadiazine-2,4a(3H,5 H)-dicarboxylate with a m. p. 104-123°C.

CLAIMS

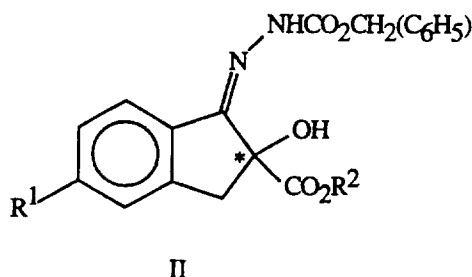
What is claimed is:

1. A process for the preparation of a dicarboxylate oxadiazine of Formula I



which is racemic or enantiomerically enriched at the chiral center*,
wherein:

R¹ is F, Cl or C₁-C₃ fluoroalkoxy and R² is C₁-C₃ alkyl comprising reacting a
hydrazine carboxylate of Formula II



with at least one molar equivalent of a di(C₁-C₃ alkoxy) methane in the presence of a protic
acid catalyst in an inert solvent under conditions which allow for the prompt removal of the
by-product alcohol by distillation.

2. A process of Claim 1 wherein R¹ is Cl and R² is CH₃.

3. A process of Claim 1 wherein the protic acid is selected from p-toluenesulfonic acid, mixtures of the isomeric toluene sulfonic acids, benzene sulfonic acid, naphthalene sulfonic acids, xylene sulfonic acids, methanesulfonic acid, sulfuric acid and camphor sulfonic acids.

4. A process of Claim 1 wherein a catalytic amount of the protic acid is used.

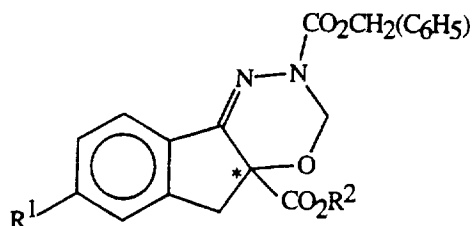
5. A process of Claim 1 wherein the dialkoxy methane used is a di(C₂-C₃ alkoxy) methane.

6. A process of Claim 1 wherein the reaction temperature is from about 40-150°C and at a pressure of about 1 atmosphere.

7. A process of Claim 1 wherein the solvent is an inert non-halogenated solvent.

8. A process for preparing a compound of Formula I

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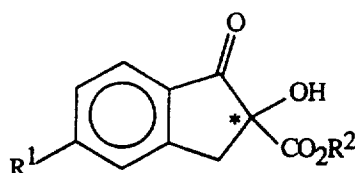


I

which is racemic or enantiomerically enriched at chiral center*

wherein: R¹ is F, Cl, or C₁-C₃ fluoroalkoxy, and R₂ is C₁-C₃ alkyl, comprising:

- 5 (a) reacting a compound of Formula III, which is racemic or enantiomerically enriched at*,



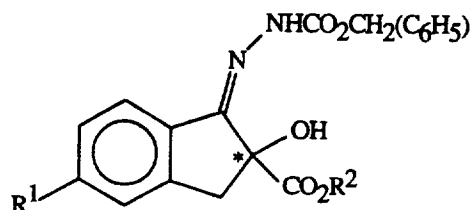
III

with the compound of Formula IV in the presence of a protic acid catalyst in an inert solvent



IV

10 to form a compound of Formula II



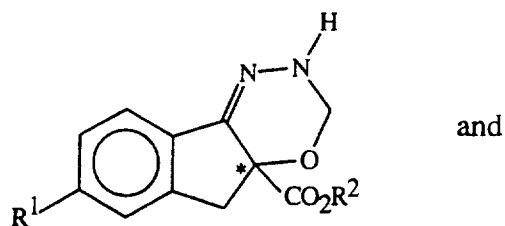
II

- 15 and (b) reacting the compound of Formula II with a di(C₁-C₃ alkoxy) methane in the presence of the same protic acid catalyst and inert solvent as used in step (a) under conditions which allow for the prompt removal of the by-product alcohol by distillation.

9. A process of Claim 1 further comprising the preparation of an arthropodocidal insecticide of Formula VII by
- 20

- (a) hydrogenating the compound of Formula I to form a compound of Formula V

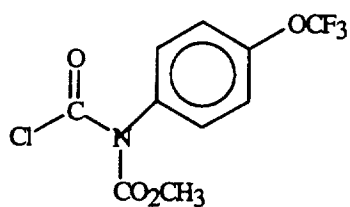
13



V

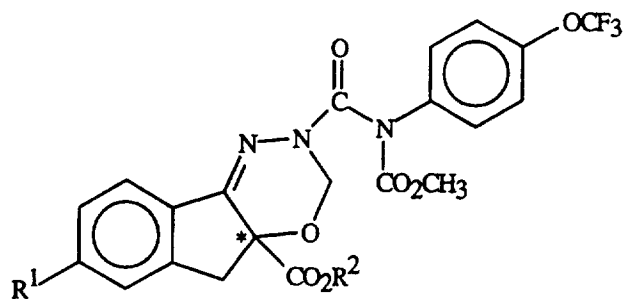
(b) reacting the compound of Formula V with the compound of Formula VI

5



VI

to form a compound of Formula VII having substantially the same absolute configuration as the compound of Formula I.



VII

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 97/13548

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 C07D273/04 //A01N47/38

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 C07D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category °	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 95 29171 A (E.I. DU PONT DE NEMOURS AND COMPANY) 2 November 1995 cited in the application see the whole document, particularly paragraph bridging pages 6 and 7 ---	1-9
Y	A. FRUCHIER ET AL.: "Ouverture d'époxydes par le N-hydroxycarbamates de méthyle; synthèses de tétrahydrodioxazine-1,4,2 ones-3 et de carbométhoxy-2 tétrahydrodioxazines-1,4,2" BULLETIN DE LA SOCIÉTÉ CHIMIQUE DE FRANCE, PARTIE II, 1984, PARIS, FR, pages II.173-II.182, XP002045208 see the whole document, particularly pages II-177 and II-181 --- -/--	1-9

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

° Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

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"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the international search

30 October 1997

Date of mailing of the international search report

13.11.97

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Allard, M

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 97/13548

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	<p>G. PICCIÒLA: "Sintesi di acidi chinazolinonici e benzossazinonici e studio delle loro proprietà antiinfiammatorie"</p> <p>IL FARMACO, EDIZIONE SCIENTIFICA, vol. 31, no. 9, 1976, PAVIA, IT, pages 655-64, XP002045209</p> <p>see the whole document, particularly page 663, method G</p> <p style="text-align: center;">-----</p>	1-9

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 97/13548

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 9529171 A	02-11-95	AU 2243295 A	16-11-95
		CA 2188400 A	02-11-95
		CN 1146205 A	26-03-97
		CZ 9603060 A	12-03-97
		EP 0756594 A	05-02-97
		HU 75052 A	28-03-97
		PL 316849 A	17-02-97
