



- (51) **International Patent Classification:**
C07C 2/58 (2006.01) *C10G 50/00* (2006.01)
- (21) **International Application Number:**
PCT/EP20 13/0766 10
- (22) **International Filing Date:**
13 December 2013 (13. 12.2013)
- (25) **Filing Language:** English
- (26) **Publication Language:** English
- (30) **Priority Data:**
PCT/CN20 12/0866 17
14 December 2012 (14. 12.2012) CN
- (71) **Applicant (for all designated States except US):** SHELL
INTERNATIONALE RESEARCH MAATSCHAPPIJ
B.V. [NL/NL]; Carel van Bylandtlaan 30, NL-2596 HR
The Hague (NL).
- (71) **Applicant (for US only):** SHELL OIL COMPANY
[US/US]; PO Box 2463, One Shell Plaza, Houston, Texas
77252-2463 (US).
- (71) **Applicant:** CHINA UNIVERSITY OF PETROLEUM
[CN/CN]; Fuxue Road 18, Beijing 102249 (CN).
- (72) **Inventors:** KLUSENER, Peter Anton August; Grasweg
31, NL-103 1 HW Amsterdam (NL). ZHANG, Rui; Fuxue
Road 18, Changping, Beijing 102249 (CN).
- (74) **Agent:** MATTHEZING, Robert Maarten; PO Box 384,
NL-2501 CJ The Hague (NL).
- (81) **Designated States (unless otherwise indicated, for every
kind of national protection available):** AE, AG, AL, AM,
AO, AT, AU, AZ, BA, BB, BG, BH, BN, BR, BW, BY,
BZ, CA, CH, CL, CN, CO, CR, CU, CZ, DE, DK, DM,
DO, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT,
HN, HR, HU, ID, IL, IN, IR, IS, JP, KE, KG, KN, KP, KR,
KZ, LA, LC, LK, LR, LS, LT, LU, LY, MA, MD, ME,
MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ,
OM, PA, PE, PG, PH, PL, PT, QA, RO, RS, RU, RW, SA,
SC, SD, SE, SG, SK, SL, SM, ST, SV, SY, TH, TJ, TM,
TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM,
ZW.
- (84) **Designated States (unless otherwise indicated, for every
kind of regional protection available):** ARIPO (BW, GH,
GM, KE, LR, LS, MW, MZ, NA, RW, SD, SL, SZ, TZ,
UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, RU, TJ,
TM), European (AL, AT, BE, BG, CH, CY, CZ, DE, DK,
EE, ES, FI, FR, GB, GR, HR, HU, IE, IS, IT, LT, LU, LV,
MC, MK, MT, NL, NO, PL, PT, RO, RS, SE, SI, SK, SM,
TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW,
KM, ML, MR, NE, SN, TD, TG).

Declarations under Rule 4.17 :

- *as to applicant's entitlement to apply for and be granted a
patent (Rule 4.1 7(H))*

Published:

- *with international search report (Art. 21(3))*

(54) **Title:** SOLIDS CONTENT CONTROL IN IONIC LIQUID ALKYLATION PROCESS

(57) **Abstract:** The present invention relates to a continuous or non- continuous ionic liquid alkylation process comprising a step for solids removal, the process further comprising the steps (a) measuring the solids content in the ionic liquid alkylation process stream by on line (in situ) or offline sampling; (b) in response to the solids measurement signal, regulating the flow of the ionic liquid side stream to be sent to the solids removal device; (c) regulating the flow of the fresh ionic liquid inlet stream, for controlling the solids content in the ionic liquid alkylation process to a pre-defined level. The process of the invention provides a means to more efficiently run an ionic liquid alkylation process.



SOLIDS CONTENT CONTROL IN IONIC LIQUID ALKYLATION PROCESS

Field of the invention

The present invention provides a means and a process for controlling the solids content in an ionic liquid alkylation process.

5 Background of the invention

Recently, new ionic liquid alkylation processes have been disclosed for the production of alkylates, in particular fuel-blending components like trimethylpentanes (TMPs), which have research octane numbers (RONs) of greater than 100. In such processes isoparaffins are alkyated with olefins using an acidic ionic liquid catalyst .

For instance, US7285698 discloses a process in which a composite ionic liquid catalyst is used to react isobutane with a butane under alkylation conditions. The reactor effluent is separated and the ionic liquid phase is recycled to the reactor while the hydrocarbon phase is treated to retrieve the alkylate. It has however been found that during operation of such an ionic liquid alkylation process, solids are formed. As the reaction progresses, these solids accumulate in the reaction zone and may lead to blockage of pathways and/or valves. In WO2011/015639 a process is described for removal of the solids formed during the ionic liquid alkylation process. It is important to maintain the solids content in the ionic alkylation process at pre-defined levels thereby minimizing the need for addition of fresh ionic liquid catalyst .

Summary of the invention

30 It has been found that the solids content in an ionic liquid alkylation process can be followed by

measuring the solids content in the ionic liquid alkylation process stream by on line (in situ) or off line sampling.

Accordingly, the present invention provides a continuous or non-continuous ionic liquid alkylation process comprising a step for solids removal, the process further comprising the steps

(a) measuring the solids content in the ionic liquid alkylation process stream by on line (in situ) or off line sampling;

(b) in response to the solids measurement signal, regulating the flow of the ionic liquid side stream to be sent to the solids removal device;

(c) regulating the flow of the fresh ionic liquid inlet stream,

for controlling the solids content in the ionic liquid alkylation process to a pre-defined level.

Particularly useful is a continuous alkylation process wherein Focused Beam Reflectance Measurement (FRBM^(R)) technology is used for on line measurement of solids content in step (a).

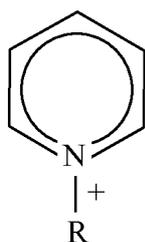
By controlling the solids content in the process streams, the process is more efficient, requires less materials and produces higher yields.

Detailed description of the invention

The solids, the content of which is measured according to the process of this invention, are formed in a process wherein an alkylate is prepared by reacting an isoparaffin with an olefin, in particular isobutane and a butene. The obtained alkylate is particularly suitable for gasoline blending purposes or for use in aviation gasoline production. In the alkylation process, the isoparaffin and the olefin are provided to a reaction

zone. In the reaction zone a hydrocarbon mixture comprising isoparaffin and olefin is contacted with a catalyst suitable for alkylation. The hydrocarbon mixture comprises olefin typically supplied externally, i.e. fresh olefin, and comprises isoparaffin. The isoparaffin may be externally supplied isoparaffin, i.e. fresh isoparaffin, and/or isoparaffin which is recycled from any other part of the process. The (fresh) isoparaffin and olefin may be supplied to the process separately, however typically the (fresh) isoparaffin and the (fresh) olefin are provided to the reaction zone as a mixture comprising isoparaffin and olefin.

In the present alkylation process the catalyst is a composite mixture comprising the ionic liquid (herein below also referred to a catalyst) . Ionic liquids are known in the art for their ability to catalyse alkylation reactions. The catalyst used in the present alkylation process is a composite ionic liquid comprising ammonium cations and anions which are composite coordinate anions derived from two or more metal salts. In particular, the cations are derived from a hydrohalide of an alkyl-containing amine, imidazolium or pyridine. Preferably, the cations comprise cations of ammonium salts, for example nitrogen atoms, which are saturated with four substituents , among which there is at least one hydrogen atom and one alkyl group. More preferably, the alkyl substituent is at least one selected from methyl, ethyl, propyl, butyl, amyl, and hexyl groups. Examples of preferred ammonium cations include triethylammonium (NEt_3H^+) and methyldiethyl-ammonium cations (MeNEt_2H^+), cations in which the nitrogen is part of a cyclic structure (e.g. like in piperidine and pyrrolidine) or



The anions of the composite ionic liquid are preferably derived from aluminium based Lewis acids, in particular aluminium halides, preferably aluminium (III) chloride. Due the high acidity of the aluminium chloride Lewis acid it is preferred to combine the aluminium chloride, or other aluminium halide, with a second or more metal halide, sulfate or nitrate to form a coordinate anion, in particular a coordinate anion derived from two or more metal halides, wherein at least one metal halide is an aluminium halide. Suitable further metal halides, sulfates or nitrates, may be selected from halides, sulfates or nitrates of metals selected from the group consisting of Group IB elements of the Periodic Table, Group IIB elements of the Periodic Table and transition elements of the Periodic Table. Preferred metals include copper, iron, zinc, nickel, cobalt, molybdenum, silver or platinum. Preferably, the metal halides, sulfates or nitrates, are metal halides, more preferably chlorides or bromides, such as copper (I) chloride, copper (II) chloride, nickel (II) chloride, iron (II) chloride. Preferably, the molar ratio of the aluminium compound to the other metal compounds in the range of from 1:100-100:1, more preferably of from 1:1-100:1, or even more preferably of from 2:1-30:1. By using a coordinate anion comprising aluminium and another metal, an improved alkylate product may be obtained. A method for preparing such catalyst is for instance

described in US7285698. Particularly preferred catalysts are acidic ionic liquid catalysts comprising a coordinate anion derived from aluminium (III) chloride and copper (II) chloride or aluminium (III) chloride and copper (I) chloride.

As mentioned herein above, the hydrocarbon mixture comprising isoparaffin and olefin is contacted with the catalyst in the reaction zone. The hydrocarbon mixture is mixed in the reaction zone with the catalyst to form a reaction mixture. As the reaction progresses the reaction mixture will, besides hydrocarbon reactants and acidic ionic liquid, additionally comprise products. Mixing of the hydrocarbon mixture and the catalyst may be done by any suitable means for mixing two or more liquids, including dynamic and static mixers. In contact with the catalyst, the isoparaffins and olefins react under alkylation conditions to form an alkylate.

The formed alkylate is obtained from the reaction zone in the form of an alkylate-comprising effluent. The alkylate-comprising effluent still comprises a substantial amount of unreacted isoparaffin. Therefore, part of the alkylate-comprising effluent may be recycled to the reaction zone to maintain a high ratio of isoparaffin to olefin in hydrocarbon mixture in the reaction zone.

At least part of the alkylate-comprising effluent of the reaction zone is separated in a separator unit into a hydrocarbon-rich phase and an ionic liquid catalyst-rich phase. At least part of the hydrocarbon-rich phase is treated and/or fractionated (e.g. by distillation) to retrieve the alkylate and optionally other components in the hydrocarbon phase, such as unreacted isoparaffin or n-paraffins. Preferably, such isoparaffin is at least

partly reused to form part of the isoparaffin feed provided to the process. This may be done by recycling at least part of the isoparaffin, or a stream comprising isoparaffin obtained from the fractionation of the hydrocarbon-rich phase, and combining it with the isoparaffin feed to the process.

Reference herein to a hydrocarbon-rich phase is to a phase comprising more than 50 mol% of hydrocarbons, based on the total moles of hydrocarbon and ionic liquid catalyst.

Reference herein to an ionic liquid catalyst-rich phase is to a phase comprising more than 50 mol% of ionic liquid catalyst, based on the total moles of hydrocarbon and ionic liquid catalyst.

Due to the low affinity of the ionic liquid for hydrocarbons and the difference in density between the hydrocarbons and the ionic liquid catalyst, the separation between the two phases is suitably done using for example well known settler means, wherein the hydrocarbons and catalyst separate into an upper predominantly hydrocarbon phase and lower predominantly catalyst phase or by using any other suitable liquid/liquid separator. Such liquid/liquid separators are known to the skilled person and include cyclone and centrifugal separators. The catalyst phase is generally recycled back to the reactor.

As described herein before, during the alkylation reaction solids are formed in the reaction zone. Reference herein to solids is to non-dissolved solid particles. The solids predominantly consist out of metals, metal compounds and/or metal salts which were originally comprised in the composite ionic liquid catalyst. Preferably, the solids comprise at least 10wt%

metal, i.e. either in metallic, covalently bound or ionic form, based the total weight of the solids, wherein the metal is a metal that was introduced to the process as part of the acidic ionic liquid catalyst. The solids may also comprise contaminant components, which were introduced into the reaction mixture as contaminants in the hydrocarbon mixture or the composite ionic liquid. Alternatively, the solids may be the product of a chemical reaction involving any of the above-mentioned compounds.

The solids may have any size, however the solids typically have an average size of in the range of from 0.1 to 100µm. In particular, at least 50% of the solids have a particle size below 5µm, more particular 80% of the solids have a particle size below 5µm based on the total number of solid particles.

In WO2011015639 it is described that although during mixing these solids are dispersed throughout the reaction mixture, upon separation of the alkylate-comprising effluent it was found that the solids, to a large extent, accumulate in the composite ionic liquid catalyst-rich phase. If the catalyst-rich phase is subsequently recycled to the reaction zone to become part of the reaction mixture in the reaction zone, the solids accumulate in the reaction zone, resulting in undesirably high solids content in the reaction zone. A high solids content in the reaction zone may for instance result in blockage of pathways or valves in the reactor zone and pipes to and from the separation unit, due to precipitation of solids. In addition, at high solids content the solids may agglomerate to form large aggregates, resulting in increased blockage risk. Therefore, (at least part of) the solids are removed from

the reaction zone. It is not required to remove all solids from the reaction zone. Preferably, solids are removed from the reaction zone to an extent that the reaction mixture (i.e. a mixture comprising hydrocarbon
5 reactants, composite ionic liquid and products) comprises in the range of from 0.05 to 5wt%, more preferably at most 2wt% of solids, based on the total weight composite ionic liquid in the reaction zone.

The solids may be removed from the reaction zone by
10 withdrawing at least part of the reaction mixture from the reaction zone as a solids-comprising effluent. This solids-comprising effluent comprises next to the solid also hydrocarbons and composite ionic liquid, wherein the hydrocarbons typically include isoparaffins and alkylate.
15 Subsequently, (at least part of) the solids in at least part of the solids-comprising effluent are removed. After the removal of solids a solids-depleted effluent is obtained. Preferably, at least part of the solids-depleted effluent is recycled to the reactor for
20 efficient use of the materials.

The solids-comprising effluent is first separated in a typical separator unit into a catalyst-rich phase and a hydrocarbon-rich phase and the solids are subsequently removed from the catalyst-rich phase. Subsequently, the
25 solids-depleted catalyst can be reintroduced into the reaction zone.

The solids may be removed by any suitable means for removing solids from liquids, including but not limited to filtration, precipitation (e.g. in a settler unit) and
30 centrifugation processes, and processes using a cyclone. Such processes are well known in the art. In view of process efficiency, centrifugation is the preferred

process for removing the solids from the catalyst-rich phase .

Due to the specific nature of ionic liquids it is preferred that the removal of the solids is performed at such a temperature that the acidic ionic liquid catalyst is liquid. In particular, it is preferred to remove the solids at a temperature in the range of from 5 to 80°C, more preferably of from 20 to 60°C, while ensuring that the temperature is such that the ionic liquid remains a liquid. By removing the solids at elevated temperatures, the viscosity of the ionic liquid is lower while the density is reduced, which may be beneficial in view of decreased time and power input required to obtain separation of the solids from the liquid.

The solids may be removed from the process in any form, however typically the solids are removed in the form of a paste of solids. Such a paste may comprise next to solid particles for instance some residual ionic liquid and/or hydrocarbons (which may be for instance some polymeric material formed as side product during the reaction) . Depending on the amount of residual ionic liquid, the solids may also be removed from the process in the form of a slurry. In this text, the term "paste" is meant to also refer to "slurry". Typically, a paste contains at least 30 % of solid particles.

According to an embodiment of the invention, the signal produced by the device measuring the solids content, preferably a Focused Beam Reflectance Measurement (FRBM[®]) device, controls the pump that regulates the flow of the ionic liquid side stream to be sent to the solids removal device.

Preferably, the solids content is measured by the measuring device in the inlet line for introducing ionic liquid into the reaction zone.

5 In a further embodiment, through the inlet line a combined stream of fresh and recycled ionic liquid is introduced into the reaction zone.

10 In an embodiment of the invention, the signal produced by the device measuring the solids content, preferably a Focused Beam Reflectance Measurement device, controls the pump that pumps fresh ionic liquid into the system. Introduction of fresh ionic liquid to make up for loss of ionic liquid in the process, e.g. due to solid formation and bleed.

15 In a further embodiment of the invention, the signal produced by the device measuring the solids content, preferably a Focused Beam Reflectance Measurement device, controls a valve that controls the flow of spent ionic liquid bleed. This bleed is necessary to balance with the introduction of fresh ionic liquid into the system.

20 In the alkylation process, an isoparaffin and an olefin are reacted to form an alkylate by contacting the hydrocarbon mixture comprising isoparaffin and olefin with the catalyst under alkylation conditions. Preferably, the hydrocarbon mixture comprises at least
25 isobutane and optionally isopentane, or a mixture thereof, as an isoparaffin. The hydrocarbon mixture preferably comprises at least an olefin comprising in the range of from 2 to 8 carbon atoms, more preferably of from 3 to 6 carbon atoms, even more preferably 4 or 5
30 carbon atoms. Examples of suitable olefins include, propene, 1-butene, 2-butene, isobutene, 1-pentene, 2-pentene, 2-methyl-1-butene, 3-methyl-1-butene, 2-methyl-2-butene .

Isoparaffins and olefins are supplied to the process in a molar ratio, which is preferably 1 or higher, and typically in the range of from 1:1 to 40:1, more preferably 1:1 to 20:1. In the case of a continuous
5 process, excess isoparaffin can be recycled for reuse in the hydrocarbon mixture.

The alkylation conditions (or process conditions) are those known in the art for this type of alkylation processes. Actual operational process conditions are for
10 example dependent of the exact composition of the hydrocarbon mixture and catalyst, and the like.

The temperature in the alkylation reactor is preferably in the range of from -20 to 100°C, more preferably in the range of from 0 to 50°C. In any case
15 the temperature must be high enough to ensure that the ionic liquid catalyst is in the liquid state.

To suppress vapour formation in the reactor, the process may be performed under pressure; preferably the pressure in the reactor is in the range of from 0.1 to
20 1.6 MPa.

Preferably, the composite ionic liquid catalyst to hydrocarbon ratio in the alkylation reaction zone is at least 0.5, preferably 0.9 more preferably at least 1. Preferably, the composite ionic liquid catalyst to
25 hydrocarbon ratio in the reaction zone is in the range of from 1 to 10.

The hydrocarbon mixture may be contacted with the catalyst in any suitable alkylation reactor. This may be done in a batch-wise, a semi-continuous or continuous
30 process. Reactors such as used in liquid acid catalysed alkylation can be used (see L.F. Albright, Ind. Eng. Res. 48 (2009)1409 and A. Corma and A. Martinez, Catal. Rev. 35 (1993) 483); alternatively the reactor is a loop

reactor, optionally with multiple injection points for
the hydrocarbon feed, optionally equipped with static
mixers to ensure good contact between the hydrocarbon
mixture and catalyst, optionally with cooling in between
5 the injection points, optionally by applying cooling via
partial vaporization of volatile hydrocarbon components
(see Catal. Rev. 35 (1993) 483), optionally with an
outlet outside the reaction zone (see WO2011/015636). In
the prior art diagrams are available of alkylation
10 process line-ups which are suitable for application in
the process of this invention, e.g. in US7285698, Oil &
Gas J., vol 104 (40) (2006) p 52-56 and Catal. Rev. 35
(1993) 483.

Description of the drawings.

15 In Figure 1 a schematic representation is given of a
process according to the invention.

A mixture, comprising olefin and isoparaffin is
provided to reactor 100 through line 105. Also ionic
liquid catalyst is provided to reaction zone 100, through
20 inlet line 110. In reaction zone 100, the hydrocarbon
mixture and catalyst are mixed under alkylation
conditions. Through line 115, a solids-comprising
effluent comprising hydrocarbons and acidic ionic liquid
is withdrawn from the reaction zone. Part of this
25 effluent may be directly recycled to the reactor or
combined with line 105 via a recycle line (not shown). At
least part of the effluent is supplied to liquid/liquid
separation unit 120, e.g. a settler unit. In
liquid/liquid separation unit 120, a hydrocarbon-rich
30 phase and catalyst-rich phase separate under influence of
gravity or centrifugal forces. Part of the hydrocarbon-
rich phase may be directly recycled to the reactor or
combined with line 105 via a recycle line (not shown). At

least part of the hydrocarbon-rich phase is provided to fractionator 125 through line 130. From the bottom of fractionator 125, an alkylate-comprising product is retrieved through line 135. The alkylate-comprising product can be used for instance for fuel blending purposes. Additionally, an isoparaffin-comprising stream is retrieved from fractionator 125, which is recycled via line 140 to become part of the mixture in line 105. Other hydrocarbon-comprising streams (not shown) may also be retrieved from fractionator 125.

The ionic liquid catalyst phase, containing solids, can be recycled via line 145 to reactor 100. Part or all of the catalyst can be diverted from line 145 via pump 175 by line 150 to centrifuge 155. In centrifuge 155, solids are removed from the ionic liquid catalyst phase under influence of the centrifugal forces, and are retrieved through a flow meter of solids concentrate 200 and further via line 160. The remaining acidic ionic liquid catalyst phase exits centrifuge 155 via line 165. Optionally, hydrochloride gas is provided to the ionic liquid catalyst phase in line 165 (not shown) for which optionally a mixing device (not shown), e.g. a venturi absorber, is used to mix the hydrogen chloride gas into the ionic liquid.

A Focused Beam Reflectance Measurement (FRBM^(R)) device 210 is located in the process stream at a position downstream in the line after the point where lines 165 and 145 come together. The FRBM^(R) device measures the solids content in ionic liquid feed line 110. Through line 145 the remainder of the ionic liquid catalyst phase is pumped, via recycle pump 190, and in addition fresh ionic liquid catalyst may be introduced into line 145 via line 180, through pump 185.

The FRBM^(R) device 210 sends via computer control system 250 a control signal to the pump 175 controlling the flow to the centrifuge 155. The centrifuge produces a slurry or paste containing solids and liquid, the flow of the slurry or paste being dependent on both the pump rate of pump 175 and the solids content of the feed to the centrifuge 155. The computer control system 250 sends a control signal to the pump 185 which pumps fresh ionic liquid into the system. Also the materials balance is controlled by computer control system 250, which sends a signal to valve 230 to control spent ionic liquid bleed flow. Optionally also a level control meter in liquid/liquid separation unit 120 sends a signal to the computer control system 250 to adjust the feed of fresh ionic liquid by pump 185 or the bleed of spent ionic liquid by control valve 230. The spent ionic liquid flows through line 170 and is measured by flow meter 220.

The (partially recycled) ionic liquid catalyst phase is subsequently directed back to reaction zone 100.

Computer control system 250 can be controlled automatically or manually.

The invention is illustrated by the following examples.

Examples

An FMBR apparatus from Mettler Toledo was used. The cord length determined with FBRM is a measure for the particle size .

Ionic liquid was prepared according to the procedures described in US7285698.

Examples 1-3

The graph in Figure 2 shows three FBRM graphs .

Example 1) shows fresh ionic liquid.

Example 2) shows a mixture of fresh and reused ionic
5 liquid.

Example 3) shows the ionic liquid from example 2 after
144 h runtime in an alkylation process according to
US7285698 .

The graphs indicate that solids content as well as the
10 particle size increases as function of runtime. In
examples 1 and 2 the solids were isolated and the solids
fraction was 0.5 and 1.5 w%, respectively.

Example 4

The graph of Figure 3 shows the FBRM curve of a non-
15 centrifuged ionic liquid sample (example 4), taken from
an alkylation process according to US7285698.

Example 5 shows the FBRM curve of the sample ex example 4
after centrifuge and solids removal, also in Figure 3 .

The spikes in example 5 for cord lengths above 10 microns
20 are artefacts as ingress of air bubbles occurred during
the measurement due to the small sample size and can be
ignored .

These examples show that FBRM can be used to measure
solids content as well as particle size. FBRM apparatus
25 is commercially available and can be applied for in situ
measurement. The application of FBRM is just one example
of in situ solids measurement. Any method a known by
those skilled in the art to be applied on line (in situ)
or off line sampling and analysis is part of the
30 invention.

C L A I M S

1. A continuous or non-continuous ionic liquid alkylation process comprising a step for solids removal, the process further comprising the steps
- 5 (a) measuring with a measuring device the solids content in the ionic liquid alkylation process stream by on line (in situ) or off line sampling;
- (b) in response to the solids measurement signal, regulating the flow of the ionic liquid side stream to be sent to the solids removal device;
- 10 (c) regulating the flow of the fresh ionic liquid inlet stream, for controlling the solids content in the ionic liquid alkylation process to a pre-defined level.
2. The process according to claim 1, wherein the process is a continuous process and wherein Focused Beam Reflectance Measurement (FRBM^(R)) technology is used for on line measurement of solids content in step (a) .
3. The process according to claim 1 or 2, wherein the solids content is measured in the inlet line for
- 20 introducing ionic liquid into the reaction zone.
4. The process according to claim 3, wherein through the inlet line a combined stream of fresh and recycled ionic liquid is introduced into the reaction zone.
5. The process according to any one of the preceding
- 25 claims, wherein the signal produced by the device measuring the solids content, preferably a FRBM^(R) device, controls a pump that regulates the flow of the ionic liquid side stream to be sent to the solids removal device .
- 30 6. The process according to any one of the preceding claims, wherein the signal produced by the device

measuring the solids content, preferably a FRBM^(R) device, controls a pump that pumps fresh ionic liquid into the system.

5 7. The process according to any one of the preceding claims, wherein the signal produced by the device measuring the solids content, preferably a FRBM^(R) device, controls a valve that controls the flow of spent ionic liquid bleed.

10 8. The process of any one of the preceding claims, wherein the ionic liquid is a composite ionic liquid comprising ammonium cations and anions being composite coordinate anions derived from two or more metal salts.

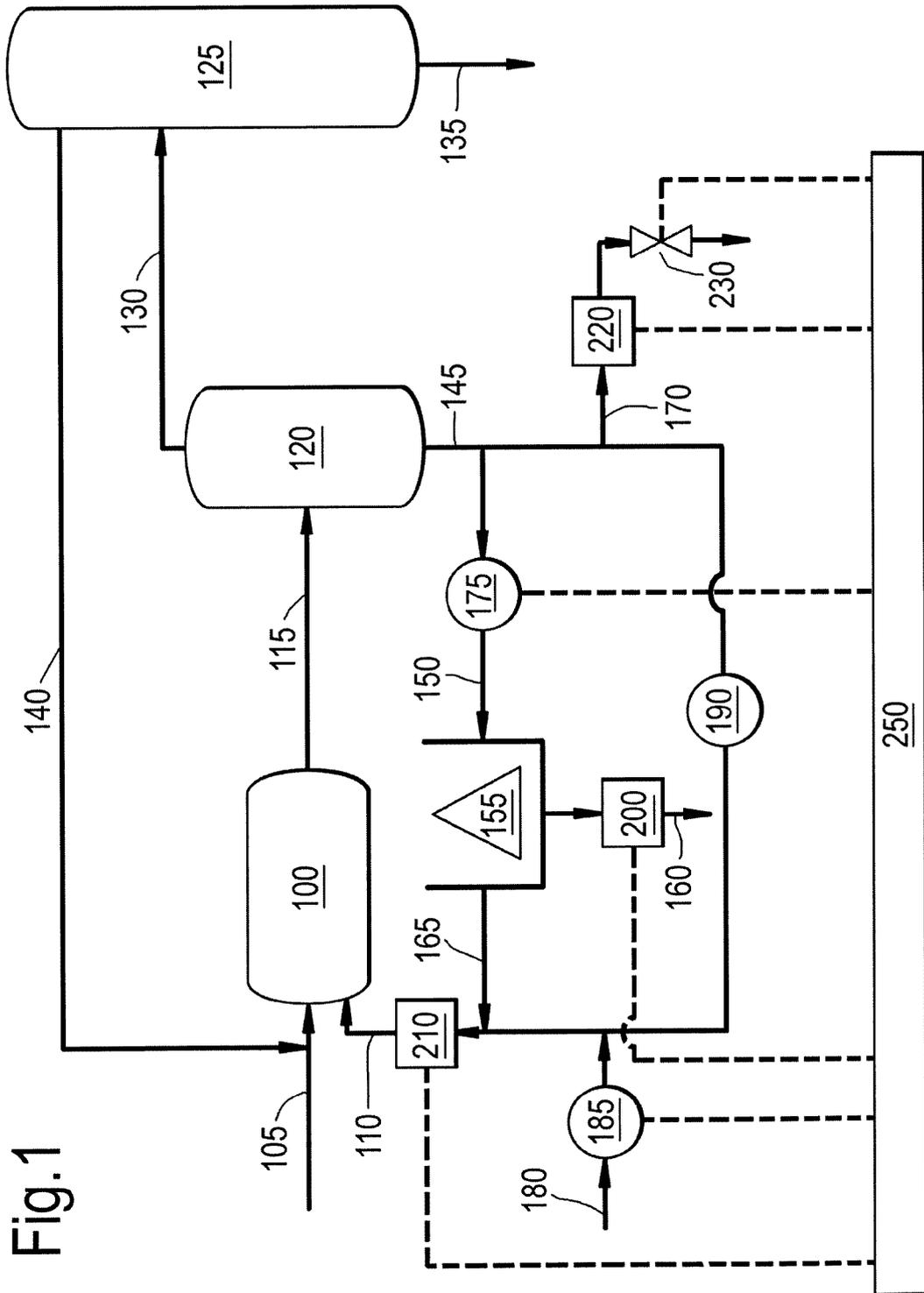


Fig.1

Fig.2

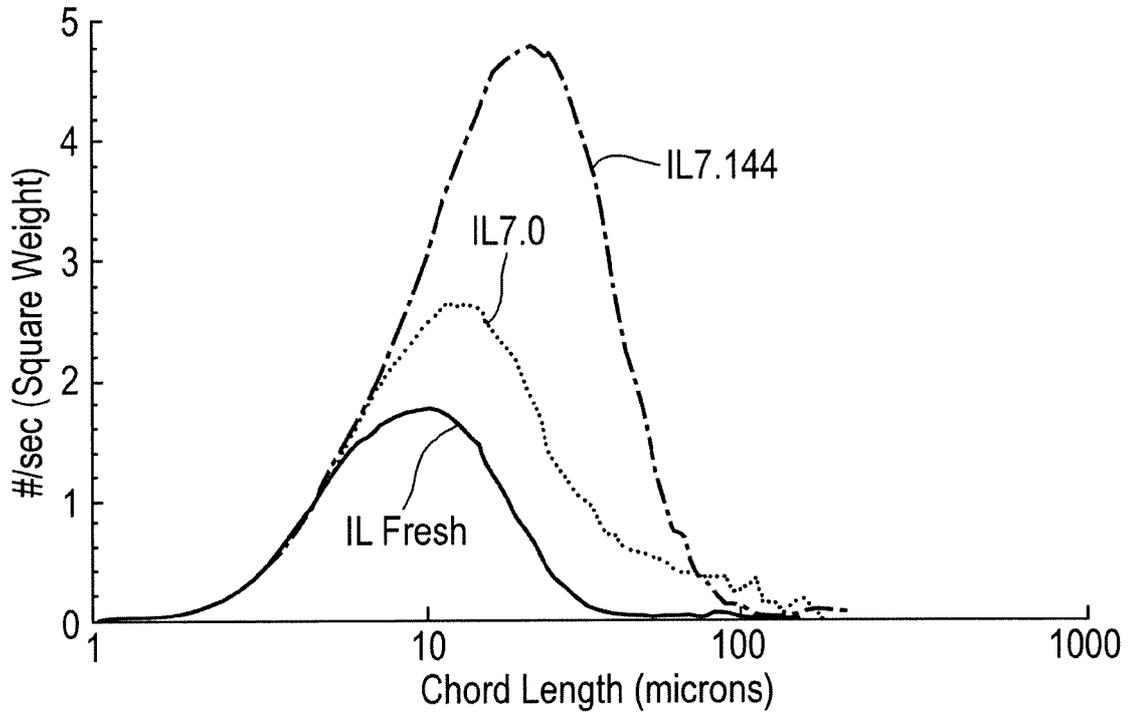
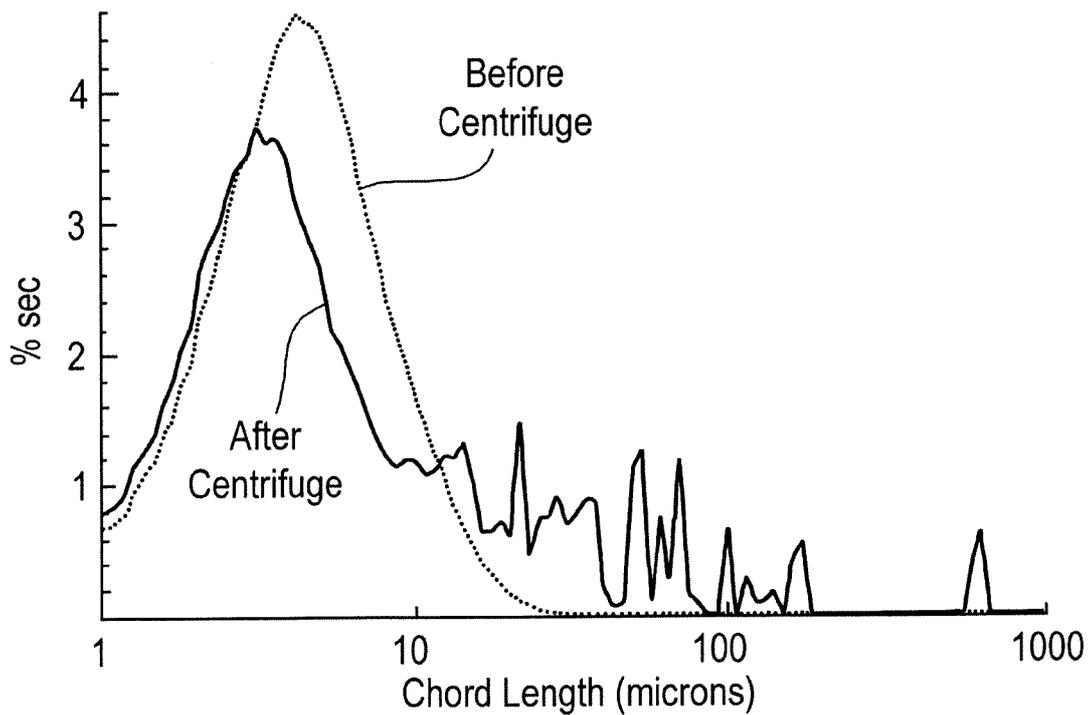


Fig.3



INTERNATIONAL SEARCH REPORT

International application No
PCT/EP2013/076610

A. CLASSIFICATION OF SUBJECT MATTER
INV. C07C2/58 C10G50/00
ADD.
According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED
Minimum documentation searched (classification system followed by classification symbols)
C07C C10G
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)
EPO-Internal

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	wo 2011/015639 A2 (SHELL INT RESEARCH [NL]; UNIV CHINA PETROLEUM [CN]; LIU ZHICHANG [CN];) 10 February 2011 (2011-02-10) cited in the application the whole document -----	1-8
A	wo 2010/062902 A2 (CHEVRON USA INC [US]; AHMED MOINUDDIN [US]; LUO HUPING [US]; PARIMI KR) 3 June 2010 (2010-06-03) the whole document -----	1-8

Further documents are listed in the continuation of Box C.

See patent family annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance
"E" earlier application or patent but published on or after the international filing date
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
"O" document referring to an oral disclosure, use, exhibition or other means
"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"&" document member of the same patent family

Date of the actual completion of the international search 29 January 2014	Date of mailing of the international search report 10/02/2014
--	--

Name and mailing address of the ISA/ European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016	Authorized officer Cooper, Simon
--	---

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No PCT/EP2013/076610
--

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
w0 2011015639	A2	10-02-2011	AU 2010280693 AI 16-02 -2012 EP 2462091 A2 13-06 -2012 SG 178155 AI 29-03 -2012 US 2012165590 AI 28-06 -2012 Wo 2011015639 A2 10-02 -2011

w0 2010062902	A2	03-06-2010	AU 2009319862 AI 30-06 -2011 CN 102272056 A 07-12 -2011 KR 20110103979 A 21-09 -2011 SG 171818 AI 28-07 -2011 US 2010130799 AI 27-05 -2010 US 2013274533 AI 17-10 -2013 US 2014024874 AI 23-01 -2014 Wo 2010062902 A2 03-06 -2010
