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(57) **Abrégé/Abstract:**

A paint composition comprising microfibrillated cellulose, binder and solvent. The microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10 % by weight based on the total weight of the paint composition.

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(54) **Title:** COMPOSITIONS FOR PAINT(57) **Abstract:** A paint composition comprising microfibrillated cellulose, binder and solvent. The microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10 % by weight based on the total weight of the paint composition.

COMPOSITIONS FOR PAINT

TECHNICAL FIELD

5 The present invention relates to a mill-base for paint including microfibrillated cellulose and optionally co-processed inorganic particulate material as pigment or extender, and to a paint composition comprising microfibrillated cellulose and optionally co-processed inorganic particulate material.

10 BACKGROUND

Paints, including water-based decorative paints, contain many ingredients. The main ingredients are pigments, such as TiO₂, and extenders such as kaolin, talc or calcium carbonate, which are added to generate light scattering and give the paint its whiteness and opacity, and in the case of coloured paints to provide strong, bright colours. These are accompanied by one or more binders, typically synthetic latex polymers, which bond to the pigments and extenders to provide a strong and coherent dried film. Other minor additives such as co-solvents, plasticisers, defoamers, biocides and rheology modifiers are also common. Conventional rheology modifiers, such as hydroxyethyl cellulose, are used to prevent the sedimentation of the pigments and extenders in the can, in order to give the product a long shelf life and to avoid the need for extensive and rigorous stirring prior to use, as well as to prevent the dripping of the paint once applied to a substrate. These additives give the paint a highly shear-thinning or pseudoplastic rheological profile; the paint is viscous or even semi-solid at rest but its viscosity is reduced substantially by the shearing action of a brush or roller so that it can be easily transferred from the can to the substrate. For example, a solution of up to 5% by weight hydroxyethyl cellulose in the makedown water of a paint is normally sufficient to impart the desired rheology to the paint formulation.

30 Hydroxyethyl cellulose (and related products such as carboxymethyl cellulose) is typically produced from a bleached chemical pulp source. However, its production requires reaction and dissolution of the cellulose in concentrated and caustic solutions, and is an inherently expensive paint component. Thus, there is a need for new and less-expensive rheology modifiers for paint, particularly those which may impart other benefits to the paint, such as improved whiteness, opacity, gloss and wet scrub resistance.

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The present invention seeks to provide alternative and/or improved components such as rheology modifiers for paint products which may be incorporated in the paint in addition to or in replacement of conventional rheology modifiers such as hydroxyethyl cellulose whilst maintaining or even improving the physical/mechanical, optical and post-application properties of the paint product. As such, the present inventors have surprisingly found that a composition comprising microfibrillated cellulose and optionally a co-processed inorganic particulate material can be used as a rheology modifier in paint whilst maintaining or even improving the physical/mechanical, optical and/or post-application properties of the paint.

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SUMMARY OF THE INVENTION

In accordance with a first aspect, there is provided a mill-base for paint, which comprises microfibrillated cellulose. The microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10 % by weight based on the total weight of a paint composition formulated from said mill base. In an embodiment, the mill-base further comprises co-processed inorganic particulate material as primary pigment and/or extender pigment, wherein said inorganic particulate material is co-processed with a fibrous substrate comprising cellulose during the preparation of said microfibrillated cellulose.

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In accordance with a second aspect, there is provided a paint composition comprising microfibrillated cellulose, binder and solvent. The microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10 % by weight based on the total weight of the paint composition. In an embodiment, the paint composition is formulated from the mill-base of the first aspect of the invention.

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According to a third aspect, the present invention is directed to the use of microfibrillated cellulose as disclosed herein as a rheology modifier in a mill-base for paint or paint composition.

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According to a fourth aspect, the present invention is directed to the use of microfibrillated cellulose as disclosed herein as a replacement or partial replacement for conventional cellulose-derived rheology modifier in a mill-base for paint or paint composition.

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According to a sixth aspect, there is provided a substrate coated with the paint composition of the second aspect of the invention.

5 According to a seventh aspect, there is provided a canned paint comprising the paint composition of the second aspect of the invention.

10 According to an eighth aspect, there is provided a paint composition comprising at least one rheology modifier, a binder, a solvent, a primary pigment, and, at least one extender pigment, wherein the at least one extender pigment is one or more of, kaolin, calcium carbonate and talc, wherein the at least one rheology modifier comprises a microfibrillated cellulose, wherein the paint composition is free of cellulose-derived rheology modifier other than the microfibrillated cellulose, and wherein the microfibrillated cellulose is present in an amount of from about 0.1 % to about 10 % by weight based on the total weight of the paint composition, comprising co-processed
15 inorganic particulate material as at least one of the primary pigment and the extender pigment, wherein the inorganic particulate material is co-processed with a fibrous substrate comprising cellulose during the preparation of the microfibrillated cellulose, wherein the microfibrillated cellulose has a d_{50} of from about 5 μm to about 500 μm as measured by laser light scattering, wherein the microfibrillated cellulose has a fibre steepness of from about 20 to about 50, and wherein the microfibrillated cellulose
20 improves one or more of the properties of the paint composition selected from the group consisting of improvement in wet scrub resistance of a dry film of no more than 45 μm determined in accordance with ISO 11998; a reduction in gloss at 85 degree of less than 7.0 determined in accordance with ISO 2813; a reduction in burnish of less
25 than 5.8; and mud cracking thickness of at least 1,000 μm , compared to an equivalent paint composition not comprising microfibrillated cellulose as a rheology modifier.

BRIEF DESCRIPTION OF THE FIGURES

Figure 1 shows the rheology profiles (viscosity as a function of shear rate) of various comparative and exemplary paint formulations.

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Figure 2 shows the rheology profiles (viscosity as a function of shear rate) of further comparative and exemplary paint formulations.

DETAILED DESCRIPTION

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The terms "mill-base" or "mill-base for paint" used herein means a composition which may be formulated into paint. A mill-base will typically comprise a portion of liquid paint components as well as primary pigment and optional extender pigment components, and other conventional additives as described later. Thus, a mill-base includes components of fully formulated paint, other than the majority of the solvent (e.g., water) and binder (e.g., a latex).

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The terms "paint" or "formulated paint" or "fully formulated paint" used herein means a composition comprising primary pigment, optional extender pigment, solvent and binder, and other optional additives suitable for use in paint, which is in a form suitable for application to a substrate, e.g., an article of manufacture (e.g., a handy-craft item, piece of furniture or an automobile, and the like) or a surface, e.g., the surface of a constructional element (e.g., interior walls, ceilings and floors of a dwelling place), and the like.

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By microfibrillating is meant a process in which microfibrils of cellulose are liberated or partially liberated as individual species or as smaller aggregates as compared to the fibres of the pre-microfibrillated pulp. Typical cellulose fibres (i.e., pre-microfibrillated pulp) include larger aggregates of hundreds or thousands of individual cellulose microfibrils. By microfibrillating the cellulose, particular characteristics and properties, including but not limited to the characteristic and properties described herein, are

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imparted to the microfibrillated cellulose and the compositions including the microfibrillated cellulose.

As used herein “co-processed inorganic particulate material” refers to inorganic
5 particulate material produced by the methods for microfibrillating fibrous substrates comprising cellulose in the presence of an inorganic particulate material as described herein.

Unless otherwise stated, the particle size properties referred to herein for the inorganic
10 particulate materials are as measured by the well known conventional method employed in the art of laser light scattering, using a Malvern Mastersizer S machine as supplied by Malvern Instruments Ltd (or by other methods which give essentially the same result). In the laser light scattering technique, the size of particles in powders, suspensions and emulsions may be measured using the diffraction of a laser beam,
15 based on an application of Mie or Fraunhofer theory. Such a machine provides measurements and a plot of the cumulative percentage by volume of particles having a size, referred to in the art as the ‘equivalent spherical diameter’ (e.s.d), less than given e.s.d values. The mean particle size d_{50} is the value determined in this way of the particle e.s.d at which there are 50% by volume of the particles which have an
20 equivalent spherical diameter less than that d_{50} value.

Alternatively, where stated, particle size properties referred to herein for the inorganic
particulate materials are as measured in a well known manner by sedimentation of the
particulate material in a fully dispersed condition in an aqueous medium using a
25 Sedigraph 5100 machine as supplied by Micromeritics Instruments Corporation, Norcross, Georgia, USA (telephone: +1 770 662 3620; web-site: www.micromeritics.com), referred to herein as a “Micromeritics Sedigraph 5100 unit”. Such a machine provides measurements and a plot of the cumulative percentage by
weight of particles having a size, referred to in the art as the ‘equivalent spherical
30 diameter’ (e.s.d), less than given e.s.d values. The mean particle size d_{50} is the value determined in this way of the particle e.s.d at which there are 50% by weight of the particles which have an equivalent spherical diameter less than that d_{50} value.

Unless otherwise stated, particle size properties of the microfibrillated cellulose
35 materials are as measured by the well known conventional method employed in the art of laser light scattering, using a Malvern Mastersizer S machine as supplied by Malvern

Instruments Ltd (or by other methods which give essentially the same result). Details of an exemplary procedure used to characterise the particle size distributions of mixtures of inorganic particle material and microfibrillated cellulose using a Malvern Mastersizer S machine are provided in WO-A-2010/131016 at page 40, line 32 to page 41, line 34.

Mill-base

The mill-base comprises microfibrillated cellulose, wherein the microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10 % by weight based on the total weight of a paint composition formulated from said mill-base and including solvent, binder and any other additives. Thus, based on the total weight of the mill-base, the microfibrillated cellulose may be present in amount of from about 0.1 to about 20 % by weight.

In an embodiment, the microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 8 % by weight based on the total weight of a paint composition formulated from said mill base, for example, from about 0.1 % to about 6 % by weight, or from about 0.2 to about 5 % by weight, or from about 0.3 % to about 5 % by weight, or from about 0.4 % to about 5 % by weight, or from about 0.4 % to about 4.5 % by weight, or from about 0.4 % to about 4 % by weight, or from about 0.4 % to about 3.5 % by weight, or from about 0.4 % to about 3 % by weight, or from about 0.4% to about 2.5 % by weight, or from about 0.4 % to about 2 % by weight.

Thus, based on the total weight of the mill-base, the microfibrillated cellulose may be present in an amount of from about 0.1 % to about 18 % by weight, for example, from about 0.2 % to about 16 % by weight, or from about 0.3 to about 14 % by weight, or from about 0.4 % to about 12 % by weight, or from about 0.5 % to about 10 % by weight, or from about 0.5 % to about 9 % by weight, or from about 0.5 % to about 8 % by weight, or from about 0.5 to about 7 % by weight, or from about 0.5 % to about 6 % by weight, or from about 0.5 % to about 5 % by weight, or from about 0.5 % to about 4 % by weight, or from about 0.5 % to about 3 % by weight.

The microfibrillated cellulose may be included as a rheology modifier.

In an embodiment, the microfibrillated cellulose is obtainable by a method comprising microfibrillating a fibrous substrate comprising cellulose in a suitable environment, advantageously an aqueous environment, by grinding in the presence of a grinding medium which is to be removed after the completion of grinding. The grinding is carried out in the absence of grindable inorganic particulate material. A grindable inorganic particulate material is a material which would be ground in the presence of the grinding medium. In an embodiment, the grinding is performed in a tower mill, a screened grinder, a stirred media mill, or stirred media detritor. Suitable methods for preparing microfibrillated cellulose are described in WO-A-2010/131016, see in particular pages page 33, line 17 to page 40, line 24.

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The particulate grinding medium may be of a natural or a synthetic material. The grinding medium may, for example, comprise balls, beads or pellets of any hard mineral, ceramic or metallic material. Such materials may include, for example, alumina, zirconia, zirconium silicate, aluminium silicate or the mullite-rich material which is produced by calcining kaolinitic clay at a temperature in the range of from about 1300°C to about 1800°C. For example, in some embodiments a Carbolite® grinding media is preferred. Alternatively, particles of natural sand of a suitable particle size may be used.

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Generally, the type of and particle size of grinding medium to be selected for use in the invention may be dependent on the properties, such as, e.g., the particle size of, and the chemical composition of, the feed suspension of material to be ground. Preferably, the particulate grinding medium comprises particles having an average diameter in the range of from about 0.5 mm to about 6 mm. In one embodiment, the particles have an average diameter of at least about 3 mm.

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The grinding medium may comprise particles having a specific gravity of at least about 2.5. The grinding medium may comprise particles have a specific gravity of at least about 3, or least about 4, or least about 5, or at least about 6.

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The grinding medium (or media) may be present in an amount up to about 70% by volume of the charge. The grinding media may be present in amount of at least about 10% by volume of the charge, for example, at least about 20% by volume of the charge, or at least about 30% by volume of the charge, or at least about 40% by volume of the charge, or at least about 50% by volume of the charge, or at least about 60 % by volume of the charge.

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The mill-base may further comprise co-processed inorganic particulate material as pigment and/or extender. In this embodiment, the inorganic particulate material is co-processed with a fibrous substrate comprising cellulose during the preparation of said microfibrillated cellulose. In an advantageous embodiment, the microfibrillated cellulose is obtainable by a method
5 comprising microfibrillating a fibrous substrate comprising cellulose in a suitable environment, advantageously an aqueous environment, in the presence of said inorganic particulate material. In a further embodiment, the microfibrillating step comprises grinding the fibrous substrate comprising cellulose in the presence of the inorganic particulate material. The grinding may be performed in a tower mill, a screened grinder, a stirred media mill or a stirred
10 media detritor. Suitable methods for preparing microfibrillated cellulose in the presence of an inorganic particulate material are described in WO-A-2010/131016, see in particular page 9, line 19 to page 22, line 12.

In this embodiment, a particulate grinding medium may be present. As described above, by
15 grinding medium is meant a medium other than the inorganic particulate material which is co-ground with the fibrous substrate comprising cellulose. The particulate grinding medium, when present, may be of a type, form and size as described above in connection with the embodiment in which grinding is carried out in the absence of grindable inorganic particulate material.

20 The fibrous substrate comprising cellulose may be derived from any suitable source, such as wood, grasses (e.g., sugarcane, bamboo) or rags (e.g., textile waste, cotton, hemp or flax). The fibrous substrate comprising cellulose may be in the form of a pulp (i.e., a suspension of cellulose fibres in water), which may be prepared by any suitable chemical or mechanical
25 treatment, or combination thereof. For example, the pulp may be a chemical pulp, or a chemithermomechanical pulp, or a mechanical pulp, or a recycled pulp, or a papermill broke, or a papermill waste stream, or waste from a papermill, or a combination thereof. The cellulose pulp may be beaten (for example in a Valley beater) and/or otherwise refined (for example, processing in a conical or plate refiner) to any predetermined freeness, reported in
30 the art as Canadian standard freeness (CSF) in cm^3 . CSF means a value for the freeness or drainage rate of pulp

measured by the rate that a suspension of pulp may be drained. For example, the cellulose pulp may have a Canadian standard freeness of about 10 cm³ or greater prior to being microfibrillated. The cellulose pulp may have a CSF of about 700 cm³ or less, for example, equal to or less than about 650 cm³, or equal to or less than about 600 cm³, or equal to or less than about 550 cm³, or equal to or less than about 500 cm³, or equal to or less than about 450 cm³, or equal to or less than about 400 cm³, or equal to or less than about 350 cm³, or equal to or less than about 300 cm³, or equal to or less than about 250 cm³, or equal to or less than about 200 cm³, or equal to or less than about 150 cm³, or equal to or less than about 100 cm³, or equal to or less than about 50 cm³. The cellulose pulp may then be dewatered by methods well known in the art, for example, the pulp may be filtered through a screen in order to obtain a wet sheet comprising at least about 10% solids, for example at least about 15% solids, or at least about 20% solids, or at least about 30% solids, or at least about 40% solids. The pulp may be utilised in an unrefined state; that is to say without being beaten or dewatered, or otherwise refined.

The fibrous substrate comprising cellulose may be added to a grinding vessel or homogenizer in a dry state. For example, a dry paper broke may be added directly to the grinder vessel. The aqueous environment in the grinder vessel will facilitate the formation of a pulp.

The grinding may be carried out in one or more stages. For example, a coarse inorganic particulate material may be ground in the grinder vessel to a predetermined particle size distribution, after which the fibrous material comprising cellulose is added and the grinding continued until the desired level of microfibrillation has been obtained.

In one embodiment, the mean particle size (d_{50}) of the inorganic particulate material is reduced during the co-grinding process. For example, the d_{50} of the inorganic particulate material may be reduced by at least about 10%, for example, the d_{50} of the inorganic particulate material may be reduced by at least about 20%, or reduced by at least about 30%, or reduced by at least about 40%, or reduced by at least about 50%, or reduced by at least about 60%, or reduced by at least about 70%, or reduced by at least about 80%, or reduced by at least about 90%. For example, an inorganic particulate material having a d_{50} of 2.5 μm prior to co-grinding and a d_{50} of 1.5 μm post co-grinding will have been subject to a 40% reduction in particle size. In embodiments, the mean particle size of the inorganic particulate material is not significantly reduced

during the co-grinding process. By 'not significantly reduced' is meant that the d_{50} of the inorganic particulate material is reduced by less than about 10%, for example, the d_{50} of the inorganic particulate material is reduced by less than about 5%.

- 5 The fibrous substrate comprising cellulose may be microfibrillated in the presence of an inorganic particulate material to obtain microfibrillated cellulose having a d_{50} ranging from about 5 to μm about 500 μm , as measured by laser light scattering. The fibrous substrate comprising cellulose may be microfibrillated in the presence of an inorganic particulate material to obtain microfibrillated cellulose having a d_{50} of equal to or less than about 400 μm , for example equal to or less than about 300 μm , or equal to or less than about 200 μm , or equal to or less than about 150 μm , or equal to or less than about 125 μm , or equal to or less than about 100 μm , or equal to or less than about 90 μm , or equal to or less than about 80 μm , or equal to or less than about 70 μm , or equal to or less than about 60 μm , or equal to or less than about 50 μm , or equal to or less than about 40 μm , or equal to or less than about 30 μm , or equal to or less than about 20 μm , or equal to or less than about 10 μm .

The fibrous substrate comprising cellulose may be microfibrillated in the presence of an inorganic particulate material to obtain microfibrillated cellulose having a modal fibre particle size ranging from about 0.1-500 μm and a modal inorganic particulate material particle size ranging from 0.25-20 μm . The fibrous substrate comprising cellulose may be microfibrillated in the presence of an inorganic particulate material to obtain microfibrillated cellulose having a modal fibre particle size of at least about 0.5 μm , for example at least about 10 μm , or at least about 50 μm , or at least about 100 μm , or at least about 150 μm , or at least about 200 μm , or at least about 300 μm , or at least about 400 μm .

The fibrous substrate comprising cellulose may be microfibrillated in the presence of an inorganic particulate material to obtain microfibrillated cellulose having a fibre steepness equal to or greater than about 10, as measured by Malvern. Fibre steepness (i.e., the steepness of the particle size distribution of the fibres) is determined by the following formula:

$$\text{Steepness} = 100 \times (d_{30}/d_{70})$$

The microfibrillated cellulose may have a fibre steepness equal to or less than about 100. The microfibrillated cellulose may have a fibre steepness equal to or less than about 75, or equal to or less than about 50, or equal to or less than about 40, or equal to or less than about 30. The microfibrillated cellulose may have a fibre steepness
5 from about 20 to about 50, or from about 25 to about 40, or from about 25 to about 35, or from about 30 to about 40.

The grinding is suitably performed in a grinding vessel, such as a tumbling mill (e.g., rod, ball and autogenous), a stirred mill (e.g., SAM or IsaMill), a tower mill, a stirred
10 media detritor (SMD), or a grinding vessel comprising rotating parallel grinding plates between which the feed to be ground is fed.

The fibrous substrate comprising cellulose and inorganic particulate material may be present in the aqueous environment at an initial solids content of at least about 4 wt %, of which at least about 2 % by weight is fibrous substrate comprising cellulose. The
15 initial solids content may be at least about 10 wt%, or at least about 20 wt %, or at least about 30 wt %, or at least about at least 40 wt %. At least about 5 % by weight of the initial solids content may be fibrous substrate comprising cellulose, for example, at least about 10 %, or at least about 15 %, or at least about 20 % by weight of the initial
20 solids content may be fibrous substrate comprising cellulose.

As the suspension of material to be ground may be of a relatively high viscosity, a suitable dispersing agent may preferably be added to the suspension prior to grinding. The dispersing agent may be, for example, a water soluble condensed phosphate,
25 polysilicic acid or a salt thereof, or a polyelectrolyte, for example a water soluble salt of a poly(acrylic acid) or of a poly(methacrylic acid) having a number average molecular weight not greater than 80,000. The amount of the dispersing agent used would generally be in the range of from 0.1 to 2.0% by weight, based on the weight of the dry inorganic particulate solid material. The suspension may suitably be ground at a
30 temperature in the range of from 4°C to 100°C.

Other additives which may be included during the microfibrillation step include: carboxymethyl cellulose, amphoteric carboxymethyl cellulose, oxidising agents, 2,2,6,6-Tetramethylpiperidine-1-oxyl (TEMPO), TEMPO derivatives, and wood
35 degrading enzymes.

The pH of the suspension of material to be ground may be about 7 or greater than about 7 (i.e., basic), for example, the pH of the suspension may be about 8, or about 9, or about 10, or about 11. The pH of the suspension of material to be ground may be less than about 7 (i.e., acidic), for example, the pH of the suspension may be about 6,
5 or about 5, or about 4, or about 3. The pH of the suspension of material to be ground may be adjusted by addition of an appropriate amount of acid or base. Suitable bases included alkali metal hydroxides, such as, for example NaOH. Other suitable bases are sodium carbonate and ammonia. Suitable acids included inorganic acids, such as hydrochloric and sulphuric acid, or organic acids. An exemplary acid is
10 orthophosphoric acid.

The amount of inorganic particulate material and cellulose pulp in the mixture to be co-ground may vary in a ratio of from about 99.5:0.5 to about 0.5:99.5, based on the dry weight of inorganic particulate material and the amount of dry fibre in the pulp, for
15 example, a ratio of from about 99.5:0.5 to about 50:50 based on the dry weight of inorganic particulate material and the amount of dry fibre in the pulp. For example, the ratio of the amount of inorganic particulate material and dry fibre may be from about 99.5:0.5 to about 70:30. In an embodiment, the ratio of inorganic particulate material to dry fibre is about 80:20, or for example, about 85:15, or about 90:10, or about 91:9, or
20 about 92:8, or about 93:7, or about 94:6, or about 95:5, or about 96:4, or about 97:3, or about 98:2, or about 99:1. In a preferred embodiment, the weight ratio of inorganic particulate material to dry fibre is about 95:5. In another preferred embodiment, the weight ratio of inorganic particulate material to dry fibre is about 90:10. In another preferred embodiment, the weight ratio of inorganic particulate material to dry fibre is about 85:15. In another preferred embodiment, the weight ratio of inorganic particulate
25 material to dry fibre is about 80:20.

The total energy input in a typical grinding process to obtain the desired aqueous suspension composition may typically be between about 100 and 1500 kWh^t⁻¹ based
30 on the total dry weight of the inorganic particulate filler. The total energy input may be less than about 1000 kWh^t⁻¹, for example, less than about 800 kWh^t⁻¹, less than about 600 kWh^t⁻¹, less than about 500 kWh^t⁻¹, less than about 400 kWh^t⁻¹, less than about 300 kWh^t⁻¹, or less than about 200 kWh^t⁻¹. As will be apparent, the total energy input per tonne of dry fibre in the fibrous substrate comprising cellulose will be less than
35 about 10,000 kWh^t⁻¹, for example, less than about 9000 kWh^t⁻¹, or less than about 8000 kWh^t⁻¹, or less than about 7000 kWh^t⁻¹, or less than about 6000 kWh^t⁻¹, or less

than about 5000 kWh^t⁻¹, for example less than about 4000 kWh^t⁻¹, less than about 3000 kWh^t⁻¹, less than about 2000 kWh^t⁻¹, less than about 1500 kWh^t⁻¹, less than about 1200 kWh^t⁻¹, less than about 1000 kWh^t⁻¹, or less than about 800 kWh^t⁻¹. The total energy input varies depending on the amount of dry fibre in the fibrous substrate being
5 microfibrillated, and optionally the speed of grind and the duration of grind.

Alternatively, or additionally, microfibrillation of the fibrous substrate comprising cellulose may be effected under wet conditions in the presence of the inorganic particulate material by a method in which the mixture of cellulose pulp and inorganic
10 particulate material is pressurized (for example, to a pressure of about 500 bar) and then passed to a zone of lower pressure. The rate at which the mixture is passed to the low pressure zone is sufficiently high and the pressure of the low pressure zone is sufficiently low as to cause microfibrillation of the cellulose fibres. For example, the pressure drop may be effected by forcing the mixture through an annular opening that
15 has a narrow entrance orifice with a much larger exit orifice. The drastic decrease in pressure as the mixture accelerates into a larger volume (i.e., a lower pressure zone) induces cavitation which causes microfibrillation. In an embodiment, microfibrillation of the fibrous substrate comprising cellulose may be effected in a homogenizer under wet conditions in the presence of the inorganic particulate material. In the homogenizer,
20 the cellulose pulp-inorganic particulate material mixture is pressurized (for example, to a pressure of about 500 bar), and forced through a small nozzle or orifice. The mixture may be pressurized to a pressure of from about 100 to about 1000 bar, for example to a pressure of equal to or greater than 300 bar, or equal to or greater than about 500, or equal to or greater than about 200 bar, or equal to or greater than about 700 bar. The
25 homogenization subjects the fibres to high shear forces such that as the pressurized cellulose pulp exits the nozzle or orifice, cavitation causes microfibrillation of the cellulose fibres in the pulp. Additional water may be added to improve flowability of the suspension through the homogenizer. The resulting aqueous suspension comprising microfibrillated cellulose and inorganic particulate material may be fed back into the
30 inlet of the homogenizer for multiple passes through the homogenizer. The inorganic particulate material may be a naturally platy mineral, such as kaolin. As such, homogenization not only facilitates microfibrillation of the cellulose pulp, but also facilitates delamination of the platy particulate material.

35 A platy particulate material, such as kaolin, is understood to have a shape factor of at least about 10, for example, at least about 15, or at least about 20, or at least about 30,

or at least about 40, or at least about 50, or at least about 60, or at least about 70, or at least about 80, or at least about 90, or at least about 100. Shape factor, as used herein, is a measure of the ratio of particle diameter to particle thickness for a population of particles of varying size and shape as measured using the electrical conductivity methods, apparatuses, and equations described in U.S. Patent No. 5,576,617.

5 A suspension of a platy inorganic particulate material, such as kaolin, may be treated in the homogenizer to a predetermined particle size distribution in the absence of the fibrous substrate comprising cellulose, after which the fibrous material comprising cellulose is added to the aqueous slurry of inorganic particulate material and the combined suspension is processed in the homogenizer as described above. The homogenization process is continued, including one or more passes through the homogenizer, until the desired level of microfibrillation has been obtained. Similarly, the platy inorganic particulate material may be treated in a grinder to a predetermined particle size distribution and then combined with the fibrous material comprising cellulose followed by processing in the homogenizer. An exemplary homogenizer is a Manton Gaulin (APV) homogenizer.

10 After the microfibrillation step has been carried out, the aqueous suspension comprising microfibrillated cellulose and inorganic particulate material may be screened to remove fibre above a certain size and to remove any grinding medium. For example, the suspension can be subjected to screening using a sieve having a selected nominal aperture size in order to remove fibres which do not pass through the sieve. Nominal aperture size means the nominal central separation of opposite sides of a square aperture or the nominal diameter of a round aperture. The sieve may be a BSS sieve (in accordance with BS 1796) having a nominal aperture size of 150µm, for example, a nominal aperture size 125µm, or 106µm, or 90µm, or 74µm, or 63µm, or 53µm, 45µm, or 38µm. In one embodiment, the aqueous suspension is screened using a BSS sieve having a nominal aperture of 125µm. The aqueous suspension may then be optionally dewatered.

25 30 In certain embodiments, the microfibrillated cellulose is obtained by grinding the fibrous substrate comprising cellulose in the presence of a grinding medium, and optionally in the presence of an inorganic particulate material, to obtain said microfibrillated cellulose, for example, microfibrillated cellulose having a fibre steepness equal to or

greater than about 10, as measured by Malvern, as described above, or from about 20 to about 50, and then the microfibrillated cellulose (optionally including co-processed inorganic particulate material) is further treated in a homogenizer under wet conditions. In the homogenizer, the microfibrillated cellulose is pressurized (for example, to a
5 pressure of about 500 bar), and forced through a small nozzle or orifice. The mixture may be pressurized to a pressure of from about 100 to about 1000 bar, for example to a pressure of equal to or greater than 300 bar, or equal to or greater than about 500, or equal to or greater than about 200 bar, or equal to or greater than about 700 bar. Additional water may be added to improve flowability of the suspension through the
10 homogenizer. The resulting aqueous suspension comprising microfibrillated cellulose and optional inorganic particulate material may be fed back into the inlet of the homogenizer for multiple passes through the homogenizer.

For use in the mill-base of the present invention, the microfibrillated cellulose and co-
15 processed inorganic particulate material may be provided in the form of an aqueous slurry or damp pressed cake.

In embodiments in which the microfibrillation is conducted in the absence of grindable inorganic particulate material, the fibrous substrate comprising cellulose may be
20 microfibrillated to obtain microfibrillated cellulose having a d_{50} ranging from about 5 to about 500 μm , as measured by laser light scattering. The fibrous substrate comprising cellulose may be microfibrillated to obtain microfibrillated cellulose having a d_{50} of equal to or less than about 400 μm , for example equal to or less than about 300 μm , or equal to or less than about 200 μm , or equal to or less than about 150 μm , or
25 equal to or less than about 125 μm , or equal to or less than about 100 μm , or equal to or less than about 90 μm , or equal to or less than about 80 μm , or equal to or less than about 70 μm , or equal to or less than about 60 μm , or equal to or less than about 50 μm , or equal to or less than about 40 μm , or equal to or less than about 30 μm , or equal to or less than about 20 μm , or equal to or less than about 10 μm .

30 The fibrous substrate comprising cellulose may be microfibrillated to obtain microfibrillated cellulose having a modal fibre particle size ranging from about 0.1-500 μm . The fibrous substrate comprising cellulose may be microfibrillated to obtain microfibrillated cellulose having a modal fibre particle size of at least about 0.5 μm , for
35 example at least about 10 μm , or at least about 50 μm , or at least about 100 μm , or at

least about 150 μm , or at least about 200 μm , or at least about 300 μm , or at least about 400 μm .

The fibrous substrate comprising cellulose may be microfibrillated to obtain microfibrillated cellulose having a fibre steepness equal to or greater than about 10, as measured by Malvern. Fibre steepness (i.e., the steepness of the particle size distribution of the fibres) is determined by the following formula:

$$\text{Steepness} = 100 \times (d_{30}/d_{70})$$

10

The microfibrillated cellulose may have a fibre steepness equal to or less than about 100. The microfibrillated cellulose may have a fibre steepness equal to or less than about 75, or equal to or less than about 50, or equal to or less than about 40, or equal to or less than about 30. The microfibrillated cellulose may have a fibre steepness from about 20 to about 50, or from about 25 to about 40, or from about 25 to about 35, or from about 30 to about 40.

15

As noted above, the grinding is performed in the presence of a grinding medium. In an embodiment, the grinding medium is a coarse media comprising particles having an average diameter in the range of from about 1 mm to about 6 mm, for example about 2 mm, or about 3 mm, or about 4 mm, or about 5 mm.

20

In another embodiment, the grinding media has a specific gravity of at least about 2.5, for example, at least about 3, or at least about 3.5, or at least about 4.0, or at least about 4.5, or at least about 5.0, or at least about 5.5, or at least about 6.0.

25

As described above, the grinding medium (or media) may be in an amount up to about 70% by volume of the charge. The grinding media may be present in amount of at least about 10% by volume of the charge, for example, at least about 20 % by volume of the charge, or at least about 30% by volume of the charge, or at least about 40 % by volume of the charge, or at least about 50% by volume of the charge, or at least about 60 % by volume of the charge.

30

In one embodiment, the grinding medium is present in amount of about 50% by volume of the charge.

35

By 'charge' is meant the composition which is the feed fed to the grinder vessel. The charge includes water, grinding media, the fibrous substrate comprising cellulose and any other optional additives (other than as described herein).

5 The fibrous substrate comprising cellulose may be present in an aqueous environment at an initial solids content of at least about 1 wt %. The fibrous substrate comprising cellulose may be present in the aqueous environment at an initial solids content of at least about 2 wt %, for example at least about 3 wt %, or at least about at least 4 wt %. Typically the initial solids content will be no more than about 10 wt%.

10

For use in the mill-base of the present invention, the microfibrillated cellulose prepared in the absence of grindable inorganic particulate material may be provided in the form of an aqueous slurry or damp pressed cake.

15 - *co-processed inorganic particulate material*

In accordance with the present invention, the co-processed inorganic particulate material may be included in the mill-base and paint composition as primary pigment or extender pigment (as described later).

20

The inorganic particulate material may, for example, be an alkaline earth metal carbonate or sulphate, such as calcium carbonate, magnesium carbonate, dolomite, gypsum, a hydrous kandite clay such as kaolin, halloysite or ball clay, an anhydrous (calcined) kandite clay such as metakaolin or fully calcined kaolin, talc, mica, perlite or
25 diatomaceous earth, or magnesium hydroxide, or aluminium trihydrate, or combinations thereof. The inorganic particulate material may also be a conventional mineral pigment, such as titanium dioxide, calcium sulphate and iron oxide, preferably titanium dioxide.

30 In an embodiment, the inorganic particulate material is an alkaline earth metal carbonate, for example, calcium carbonate. The inorganic particulate material may be ground calcium carbonate (GCC) or precipitated calcium carbonate (PCC), or a mixture of GCC and PCC. In another embodiment, the inorganic particulate material is a naturally platy mineral, for example, kaolin. The inorganic particulate material may be
35 a mixture of kaolin and calcium carbonate, for example, a mixture of kaolin and GCC, or a mixture of kaolin and PCC, or a mixture of kaolin, GCC and PCC.

The particulate calcium carbonate used in the present invention may be obtained from a natural source by grinding. Ground calcium carbonate (GCC) is typically obtained by crushing and then grinding a mineral source such as chalk, marble or limestone, which may be followed by a particle size classification step, in order to obtain a product
5 having the desired degree of fineness. Other techniques such as bleaching, flotation and magnetic separation may also be used to obtain a product having the desired degree of fineness and/or colour. The particulate solid material may be ground autogenously, i.e. by attrition between the particles of the solid material themselves, or, alternatively, in the presence of a particulate grinding medium comprising particles of a
10 different material from the calcium carbonate to be ground. These processes may be carried out with or without the presence of a dispersant and biocides, which may be added at any stage of the process.

Precipitated calcium carbonate (PCC) may be used as the source of particulate
15 calcium carbonate in the present invention, and may be produced by any of the known methods available in the art. TAPPI Monograph Series No 30, "Paper Coating Pigments", pages 34-35 describes the three main commercial processes for preparing precipitated calcium carbonate which is suitable for use in preparing products for use in the paper industry, but may also be used in the practice of the present invention. In all
20 three processes, a calcium carbonate feed material, such as limestone, is first calcined to produce quicklime, and the quicklime is then slaked in water to yield calcium hydroxide or milk of lime. In the first process, the milk of lime is directly carbonated with carbon dioxide gas. This process has the advantage that no by-product is formed, and it is relatively easy to control the properties and purity of the calcium carbonate
25 product. In the second process the milk of lime is contacted with soda ash to produce, by double decomposition, a precipitate of calcium carbonate and a solution of sodium hydroxide. The sodium hydroxide may be substantially completely separated from the calcium carbonate if this process is used commercially. In the third main commercial
30 process the milk of lime is first contacted with ammonium chloride to give a calcium chloride solution and ammonia gas. The calcium chloride solution is then contacted with soda ash to produce by double decomposition precipitated calcium carbonate and a solution of sodium chloride. The crystals can be produced in a variety of different shapes and sizes, depending on the specific reaction process that is used. The three
35 main forms of PCC crystals are aragonite, rhombohedral and scalenohedral, all of which are suitable for use in the present invention, including mixtures thereof.

Wet grinding of calcium carbonate involves the formation of an aqueous suspension of the calcium carbonate which may then be ground, optionally in the presence of a suitable dispersing agent. Reference may be made to, for example, EP-A-614948 for more information regarding the wet grinding of calcium carbonate.

5

Kaolin clay used in this invention may be a processed material derived from a natural source, namely raw natural kaolin clay mineral. The processed kaolin clay may typically contain at least about 50% by weight kaolinite. For example, most commercially processed kaolin clays contain greater than about 75% by weight kaolinite and may contain

10

greater than about 90%, in some cases greater than about 95% by weight of kaolinite. Kaolin clay used in the present invention may be prepared from the raw natural kaolin clay mineral by one or more other processes which are well known to those skilled in the art, for example by known refining or beneficiation steps.

15

For example, the clay mineral may be bleached with a reductive bleaching agent, such as sodium hydrosulfite. If sodium hydrosulfite is used, the bleached clay mineral may optionally be dewatered, and optionally washed and again optionally dewatered, after the sodium hydrosulfite bleaching step.

20

The clay mineral may be treated to remove impurities, e. g. by flocculation, flotation, or magnetic separation techniques well known in the art. Alternatively the clay mineral used in the first aspect of the invention may be untreated in the form of a solid or as an aqueous suspension.

25

The process for preparing the particulate kaolin clay used in the present invention may also include one or more comminution steps, e.g., grinding or milling. Light comminution of a coarse kaolin is used to give suitable delamination thereof. The comminution may be carried out by use of beads or granules of a plastic (e. g. nylon), sand or ceramic grinding or milling aid. The coarse kaolin may be refined to remove impurities and improve physical properties

30

using well known procedures. The kaolin clay may be treated by a known particle size classification procedure, e.g., screening and centrifuging (or both), to obtain particles having a desired d50 value or particle size distribution.

The particle size distribution of the inorganic particulate materials will be that which is suitable for use in paint. Suitable particle sizes are described below in connection with the primary pigment and extender pigment.

5 In one embodiment, the inorganic particulate material used during the microfibrillating step may have a particle size distribution in which at least about 10% by weight of the particles have an e.s.d of less than 2 μm , for example, at least about 20% by weight, or at least about 30% by weight, or at least about 40% by weight, or at least about 50% by weight, or at least about 60% by weight, or at least about 70% by weight, or at least
10 about 80% by weight, or at least about 90% by weight, or at least about 95% by weight, or about 100% of the particles have an e.s.d of less than 2 μm .

The amount of co-processed inorganic particulate material in the paint composition of the present invention may range from about 0.1 to about 30 % by weight, based on the
15 total weight of the paint composition. In embodiments, the amount of co-processed inorganic particulate material in the paint composition may be from about 0.2 to about 20 % by weight, for example, from about 0.2 to about 10% by weight, for example, from about 0.2 to about 5 % by weight, for example, from about 0.3 to about 5 % by weight, for example, from about 0.4 to about 4 % by weight, for example, from about 0.4 to
20 about 3 % by weight, or from about 0.4 to about 2 % by weight.

Advantageously, the co-processed inorganic particulate material is suitable for use as primary pigment or extender pigment, which means the amount of primary pigment and/or extender pigment that would otherwise have been added separately to the mill-
25 base may be reduced. In one embodiment, the co-processed inorganic particulate constitutes all of the primary pigment and/or extender pigment comprised in the mill-base and/or paint composition of the present invention.

- *primary pigment and extender pigment*

30

In another embodiment, the mill-base comprises primary pigment and/or extender pigment, other than the co-processed inorganic particulate material described above. A primary pigment is that which provides the primary colouration of a paint, whether white or a colour shade. The term includes finely ground, natural or synthetic,
35 inorganic or organic, insoluble dispersed particles which, when dispersed in a liquid vehicle, i.e., solvent, may provide, in addition to colour, many of the desired properties

of paint, such as opacity, hardness, durability and corrosion resistance. Extender pigments are the filler used in paints. Extender pigments generally do not hide as well as primary pigments and their presence may affect the overall characteristics and performance of a paint. Primary pigment is generally more expensive than extender pigment.

Thus, by way of example, the mill-base may comprise titanium dioxide as primary pigment, optionally co-processed calcium carbonate as extender pigment, and other inorganic particulate material as extender pigment, such as calcium carbonate, kaolin and/or talc, which is not derived from the processes disclosed herein for preparing microfibrillated cellulose.

Suitable primary pigment include, but are not limited to, titanium dioxide, carbon black, calcium sulphate, iron oxide, and the copper-complex phthalo blue. Other suitable primary pigments for providing colour will be readily apparent to persons skilled in the art.

Extender pigments include, but are not limited to, an alkaline earth metal carbonate or sulphate, such as calcium carbonate, magnesium carbonate, dolomite, gypsum, a hydrous kandite clay such as kaolin, halloysite or ball clay, an anhydrous (calcined) kandite clay such as metakaolin or fully calcined kaolin, talc, mica, perlite, feldspars, nepheline syenite, wollastonite, diatomaceous earth, barite, glass, and natural or synthetic silica or silicates. The mill-base and paint composition may include one or more or a mixture of the aforementioned extender pigments.

For paint applications in which a lesser degree of whiteness and/or lower opacity may be tolerated or even desired, an extender pigment such as, for example, calcium carbonate, may be utilised as a primary pigment.

In one embodiment, the mean particle size (d_{50}) of the primary pigment and/or extender pigment (and the co-processed inorganic particulate material described above) may be from about 0.1 μm to about 20 μm , as determined by Sedigraph. For example, the d_{50} may be from about 0.2 μm to about 15 μm , or from about 0.3 μm to about 12 μm , or from about 0.4 μm to about 10 μm , or from about 0.6 μm to about 10 μm , or from about 0.8 μm to about 10 μm , or from about 1 μm to about 10 μm , or from about 1.5 μm to about 10 μm , or from about 2 μm to about 10 μm , or from about 2.5 to about 10 μm . The d_{50} of the primary pigment and/or extender pigment may be up to about 9 μm , for

example, up to about 8 μm , or up to about 7 μm , or up to about 6 μm , or up to about 5 μm , or up to about 4 μm , or up to about 3 μm , or up to about 2 μm .

In an embodiment, the primary pigment is titanium dioxide, for example, rutile TiO_2 or
5 anatase TiO_2 . Titanium oxide may be prepared from the mineral ilmenite, or rutile ore.
The particles of titanium oxide may be coated, for example, with alumina, silica and/or
zirconia. Advantageously, the titanium oxide has an oil absorption in the range from
about 10 to about 30 $\text{cm}^3/100 \text{ g pigment}$, for example, about 20 $\text{cm}^3/100 \text{ g pigment}$, as
determined in accordance with ISO 787/11 (palette knife method). Advantageously,
10 the mill-base comprises one or more of the aforementioned primary pigments,
advantageously titanium dioxide, and one or more of, or advantageously all of, kaolin,
calcium carbonate and talc as extender pigment.

The kaolin may be a hydrous kaolin may have a d_{50} of from about 0.2 μm to about 10
15 μm , for example, from about 0.3 μm to about 5 μm , or from about 0.4 μm to about 5
 μm , or from about 0.4 μm to about 3.5 μm , as determined by Sedigraph. The kaolin
may have an oil absorption (ISO 787/5) of from about 30 to about 50 g oil/100g
pigment.

The calcium carbonate may have a d_{50} of from about 0.5 μm to 12 μm , for example,
20 from about 0.8 μm to about 10 μm , as determined by Sedigraph. The calcium
carbonate may have an oil absorption of from about 15 to about 30 (ISO 787/5). In
certain embodiments, the mill base or paint composition may comprise a mixture of
coarse and fine calcium carbonate. For example, a mixture of calcium carbonate
25 having a d_{50} of from about 0.5 to about 4 μm , for example, from about 1.0 to about 3
 μm , and calcium carbonate having a d_{50} of from about 5 to about 8 μm , for example,
from about 5.5 to about 7 μm .

The talc may have a d_{50} of from about 1 μm to about 15 μm , for example, from about 1
30 to about 12 μm , or from about 1 to about 10 μm , or from about 1 to about 9 μm , or from
about 2 to about 12 μm , or from about 5 to about 12 μm , as determined by Sedigraph.
The talc may have an oil absorption of from about 30 to about 80 (ISO 787/5). In
certain embodiments, the amount of talc in the paint composition is from about 0.1
about 10 wt. %, for example, from about 0.5 to about 8 wt. %, or from about 2 to about
35 8 wt. %, or from about 4 wt. %. In certain embodiments, for example, embodiments in
which the paint comprises a mixture of fine and coarse calcium carbonate, as

described above, the amount of talc in the paint composition is from about 0.1 to about 4 wt. %, for example, from about 1.0 to about 3 wt. %.

The amount of primary pigment in the paint composition of the invention formulated from the mill-base may be from about 1 % to about 50 % by weight, based on the total weight of the paint composition. In an embodiment, the amount of primary pigment is from about 5 % to 40 % by weight, or from about 5 % to about 30 % by weight, or from about 5 % to about 20 % by weight, or from about 5 % to about 15 % by weight, or from about 6 % to about 12 % by weight, or from about 8 % to about 12 % by weight, based on the total weight of the paint composition.

The total amount of extender pigment in the paint composition of the invention formulated from the mill-base may be from about 1 % to about 60 % by weight, based on the total weight of the paint composition. In an embodiment, the amount of extender pigment is from about 1 % to about 50 % by weight, or from about 5 % to about 40 % by weight, or from about 10 % to about 40 % by weight, or from about 15 % to about 40 % by weight, or from about 15 % to about 35 % by weight, or from about 20 % to about 35 % by weight, or from about 25 % to about 35 % by weight, based on the total weight of the paint composition.

The total amount of primary pigment, extender pigment and co-processed inorganic particulate material in the paint composition of the invention formulated from the mill-base may be from about 2% to about 80% by weight, based on the total weight of the paint composition. In an embodiment, the amount of extender pigment is from about 5 % to 70 % by weight, or from about 10 % to about 70 % by weight, or from about 15 % to about 70 % by weight, or from about 15 % to about 60 % by weight, or from about 20 % to about 50 % by weight, or from about 25 % to about 45 % by weight, or from about 30 % to about 60 % by weight, or from about 40 % to about 50 % by weight, based on the total weight of the paint composition.

- rheology modifiers

The mill-base and paint composition may comprise rheology modifier other than said microfibrillated cellulose. Said other rheology modifier may be a cellulose-derived rheology modifier, for example, hydroxymethyl cellulose, hydroxyethyl cellulose, hydroxypropyl cellulose, hydroxypropylmethyl cellulose, carboxymethyl cellulose or a

mixture thereof. In a further embodiment, the mill-base and paint composition (optionally formulated from said mill-base), is free of cellulose-derived rheology modifier other than said microfibrillated cellulose. Thus, in embodiments the weight ratio of said microfibrillated cellulose to cellulose-derived rheology modifier other than

5 said microfibrillated cellulose is from about ∞ to about 1:5, for example, from about 1000:1 to about 1:4, or from about 100:1 to about 1:4, or from about 10:1 to about 1:4, or from about 1000:1 to about 1:3, or from about 1000:1 to about 1:2, or from about 1000:1 to about 1:1, or from about 1000:1 to about 3:2, or from about 1000:1 to about 3:1, or from about 1000:1 to about 4:1, or from about 1000:1 to about 5:1. In other

10 embodiments, the weight ratio of said microfibrillated cellulose to cellulose-derived rheology modifier other than said microfibrillated cellulose is about 1:5, or about 1:4, or about 1:3, or about 1:2, or about 1:1, or about 2:1, or about 3:2, or about 3:1, or about 4:1, or about 5:1, or about 6:1, or about 7:1, or about 8:1, or about 9:1, or about 10:1, or about 20:1, or about 50:1, or about 100:1, or about 1000:1.

15 In a further embodiment, the mill base or paint composition comprises non-cellulose-derived rheology modifier. Such rheology modifiers include one or more of acrylic associative thickeners, polyacrylates, emulsion copolymers, dicyanamide, triols, polyoxyethylene ether, urea, sulphated castor oil, polyvinyl pyrrolidone, sodium

20 alginate, xanthan gum, sodium silicate and acrylic acid copolymers. Such non-cellulose derived rheology modifier may be present in amount up to about 5 % by weight based on the total weight of the paint composition, for example, from about 0.1 to about 4 % by weight, or from about 0.2 to about 3 % by weight, or from about 0.2 to about 2 % by weight based on the total weight of the paint composition.

25 In an embodiment, the mill-base or paint composition (optionally formulated from said mill-base), does not contain microfibrillated cellulose which is produced by at least partly enzymatic treatment of cellulose fibers.

30 *Paint composition*

In accordance with the second aspect, the paint composition comprises microfibrillated cellulose as disclosed herein, binder and solvent, wherein the microfibrillated cellulose is present in an amount ranging from 0.1 % to 10 % by weight based on the total

35 weight of the paint composition.

In an embodiment, the paint composition further comprises co-processed inorganic particulate material, as disclosed herein, as primary pigment and/or extender pigment, wherein said inorganic particulate material is co-processed with a fibrous substrate comprising cellulose during the preparation of said microfibrillated cellulose. In another
5 embodiment, the paint composition further comprises primary pigment and/or extender pigment as disclosed herein, other than the co-processed inorganic particulate material.

In embodiment, the microfibrillated cellulose is obtainable by the methods disclosed
10 herein comprising microfibrillating a fibrous substrate comprising cellulose in an aqueous environment by grinding in the presence of a grinding medium which is to be removed after the completion of grinding, wherein the grinding is carried out in the absence of grindable inorganic particulate material.

15 In an embodiment, the microfibrillated cellulose is obtainable by the methods disclosed herein comprising microfibrillating a fibrous substrate comprising cellulose in an aqueous environment in the presence of said inorganic particulate material. The microfibrillating step may comprise grinding the fibrous substrate comprising cellulose in the presence of the inorganic particulate material

20

In an embodiment, the paint composition is formulated from the mill-base of the first aspect of the invention and embodiments thereof.

The paint may be formulated as a decorative paint, including matt and gloss paints, an
25 industrial paint, including protective paints and paints for sanitation, and the like, and other paints such as paints for identification, e.g., signage, and the like. Advantageously, the paint is a water-based paint, for example, a water-based decorative paint, for example, water-based decorative matt paint.

30 The solvent is any suitable substance which can act as a carrier for the pigment and binder. Once on the substrate being painted, the solvent evaporates through drying and/or curing and leaves behind a dry paint film on the painted substrate. In embodiment, the solvent comprises water and optional dispersing chemicals. Organic solvents include mineral spirits, e.g., white sprits, petroleum distillate, esters, glycol
35 ethers, and the like.

The amount of solvent in the paint composition will vary depending on the particular form of paint and its intended use. In an embodiment, the amount of solvent is present in an amount of from about 5 % to about 90 % by weight, based on the total weight of the paint composition. For example, the amount of solvent may be from about 10 % to about 90 % by weight, or from about 15 % to about 90 % by weight, or from about 20 % to about 90 % by weight, or from about 25 % to about 90 % by weight, or from about 30 % to about 90 % by weight, or from about 35 % to about 90 % by weight or from about 40 % to about 90 % by weight, or from about 10 % to about 80 % by weight, or from about 20 % to about 80 % by weight, or from about 30 % to about 80 % by weight, or from about 30 % to about 70 % by weight, or from about 30 % to about 60 % by weight, or from about 40 % to about 60 % by weight, or from about 5 % to about 80 % by weight, or from about 5 % to about 70 % by weight, or from about 5 % to about 60 % by weight, or from about 5 % to 50 % by weight, or from about 5 % to about 40 % by weight, or from about 5 % to about 30 % by weight, or from about 5 % to about 25 % by weight, or from about 5 % to about 20 % by weight, or from about 5 % to about 15% by weight, or from about 10 % to about 30 % by weight, or from about 10 to about 25 % by weight, or from about 10 to about 20 % by weight, based on the total weight of the paint composition.

Binders are film-forming components of paint, which impart adhesion and bind the pigments together. Thus, the binder is any suitable material which is capable of binding the pigments together and providing adhesion to the substrate that is painted with the paint. The binder may be a natural and/or synthetic resin such as, for example, latex-based binders such as polymers and copolymers based on acrylics and/or vinyls, polyurethanes, polyesters, melamine resins, epoxies, and/or oils and other suitable monomeric species. In one embodiment, the binder comprises or consists of 100 % acrylic latex or polyvinyl acetate (PVA) latex. For oil-based paints, suitable binders include linseed oil, tung oil or alkyd resins.

The amount of binder in the paint composition will vary depending on the particular form of paint and its intended use. In an embodiment, the amount of binder is present in an amount of from about 5 % to about 30 % by weight, based on the total weight of the paint composition. For example, the amount of solvent may be from about 5 % to about 25 % by weight, or from about 5 % to about 20 % by weight, or from about 5 % to about 15% by weight, or from about 10 % to about 30 % by weight, or from about 10 to

about 25 % by weight, or from about 10 to about 20 % by weight, based on the total weight of the paint composition.

5 The amounts of co-processed inorganic particulate material (when present), primary pigment and extender pigment (when present) in the paint composition is disclosed above.

Other optional additives

10 The mil-base and paint composition may include at least one further additive chosen from conventional additives, such as, for example, pigments other than those disclosed herein, surfactant, thickener, defoamer or anti-foamer, wetting agent, dispersant, biocide, pH adjustor, co-solvent, and antifreeze coalescent, as well as other functional
15 additives. These additives may be included in any suitable amount, which will vary depending on the composition of the paint and relative amounts of pigment, solvent and binder. These amounts are readily determinable by a person skilled in the art. Generally, these additives may be included, on an individual basis, in the paint in an amount up to about 1 % by weight, based on the total weight of the fully formulated paint. Co-solvent may be present in an amount up to about 5 % by weight based on
20 the total weight of the fully formulated paint composition, for example, up to about 4 % by weight, or up to about 3 % by weight, or up to about 2 % by weight.

Suitable dispersants include, for example, polyelectrolytes such as polyacrylates and copolymers containing polyacrylate species, especially polyacrylate salts (e.g., sodium
25 and aluminium optionally with a group II metal salt), sodium hexametaphosphates, non-ionic polyol, polyphosphoric acid, condensed sodium phosphate, non-ionic surfactants, alkanolamine and other reagents commonly used for this function. The dispersant may, for example, be selected from conventional dispersant materials commonly used in the processing and grinding of inorganic particulate materials. Such dispersants will
30 be well recognised by those skilled in this art. They are generally water-soluble salts capable of supplying anionic species which in their effective amounts can adsorb on the surface of the inorganic particles and thereby inhibit aggregation of the particles. The unsolvated salts suitably include alkali metal cations such as sodium. Solvation may in some cases be assisted by making the aqueous suspension slightly alkaline.
35 Examples of suitable dispersants include: water soluble condensed phosphates, e.g., polymetaphosphate salts [general form of the sodium salts: $(\text{NaPO}_3)_x$] such as

tetrasodium metaphosphate or so-called "sodium hexametaphosphate" (Graham's salt); water-soluble salts of polysilicic acids; polyelectrolytes; salts of homopolymers or copolymers of acrylic acid or methacrylic acid, or salts of polymers of other derivatives of acrylic acid, suitably having a weight average molecular mass of less than about
5 20,000.

Suitable antifoamers and defoamers include, for example, blends of surfactants, tributyl phosphate, fatty polyoxyethylene esters plus fatty alcohols, fatty acid soaps, silicone emulsions and other silicone containing compositions, waxes and inorganic particulates
10 in mineral oil, blends of emulsified hydrocarbons and other compounds sold commercially to carry out this function.

Suitable biocides include, for example, oxidizing biocides such as chlorine gas, chlorine dioxide gas, sodium hypochlorite, sodium hypobromite, hydrogen, peroxide, peracetic
15 oxide, ammonium bromide/sodium hypochlorite, or non-oxidising biocides such as GLUT (Glutaraldehyde, CAS No 90045-36-6), ISO (CIT/MIT) (Isothiazolinone, CAS No 55956-84-9 & 96118-96-6), ISO (BIT/MIT) (Isothiazolinone), ISO (BIT) (Isothiazolinone, CAS No 2634-33-5), DBNPA, BNPD (Bronopol), NaOPP, CARBAMATE, THIONE (Dazomet), EDDM - dimethanol (O-formal), HT - Triazine (N-formal), THPS - tetrakis
20 (O-formal), TMAD - diurea (N-formal), metaborate, sodium dodecylbenene sulphonate, thiocyanate, organosulphur, sodium benzoate and other compounds sold commercially for this function, e.g., the range of biocide polymers sold by Nalco.

The paint composition may further include dye. The distinction between powders
25 which are pigments and those which are dyes is generally considered to be on the basis of solubility: pigments being insoluble and dispersed in the material, dyes being soluble or in solution when used.

Paint properties

30 The present inventors have unexpectedly found that microfibrillated cellulose, optionally co-processed in the presence of an inorganic particular material, may be used as a rheology modifier in a paint composition in addition to or in (partial) replacement of conventional rheology modifiers such as, for example, hydroxyethyl
35 cellulose and the like, whilst maintaining or even improving the physical/mechanical, optical and post-application properties of the paint product.

In embodiments, the use of microfibrillated cellulose, optionally co-processed in the presence of an inorganic particular material, in addition to or in partial or total replacement of conventional cellulose-derived rheology modifiers, such as, for example, hydroxyethyl cellulose and the like, maintains the paint viscosity (as may be
5 determined in accordance with ISO 2884-1) at high shear rate (1/s), for example, a shear rate of at least about 100, but significantly increases paint viscosity at low shear rate, for example, a shear rate of no more than about 10. This may have the effect of improving the stability and drip-resistance of the paint whilst remaining easy to apply, e.g., brush or roller). Further, conventional cellulose-derived rheology modifiers such
10 as hydroxyethyl cellulose and the like, are relatively more expensive to produce than the microfibrillated cellulose disclosed herein. Thus, cost-savings may be achieved by using the microfibrillated cellulose disclosed herein in partial or total replacement of conventional cellulose-derived rheology modifiers, such as hydroxyethyl cellulose and the like.

15 According to some embodiments, dry paint film produced from the exemplary paints disclosed herein may exhibit desirable optical properties. For example, in some embodiments the use of microfibrillated cellulose, optionally co-processed in the presence of an inorganic particular material, in partial or total replacement of
20 conventional cellulose-derived rheology modifiers, such as, for example, hydroxyethyl cellulose and the like, may improve one or more of the opacity (contrast ratio) of the dry film (determined in accordance with ISO 6504-1, ISO 6504-3 or ISO 2814), and the wet scrub resistance of the dry film (determined in accordance with ISO 11998). Further, the use of microfibrillated cellulose, optionally co-processed in the presence of an
25 inorganic particular material, in partial or total replacement of conventional cellulose-derived rheology modifiers, such as, for example, hydroxyethyl cellulose and the like, may provide a significant reduction in gloss at 85° (determined in accordance with ISO 2813), which is important for a matt paint of this type.

30 In some embodiments, dry paint film obtained from the paint composition of the invention has a gloss at 85° of less than about 7.0, for example, less than about 6.5, or less than about 6.0, or less than about 5.5, or less than about 5.0.

In further embodiments, dry paint film obtained from the paint composition of the
35 invention has a wet-scrub resistance of no more than about 45 μm , for example, no more than about 40 μm , or no more than about 35 μm , or no more than about 30.

In further embodiments, dry paint film obtained from the paint composition has a Burnish (at 85°) of less than about 5.8, for example, less than about 5.5, or less than about 5.0, or less than about 4.5. Typically, the burnish will be greater than about 1.0, for example, greater than about 2.0. In other words, an effect of including
5 microfibrillated cellulose has the effect of reducing burnish. Burnish may be determined in accordance with the method described in the Examples below.

In further embodiments, dry paint film obtained from the paint composition has a mud cracking thickness of at least about 1,000 μm , for example, at least about 1050 μm , or
10 at least about 1100 μm , or at least about 1150 μm . In other words, an effect of including microfibrillated cellulose has the effect of reducing the mud cracking propensity of the dry paint film. Mud cracking thickness may be determined in accordance with the method described in the Examples below.

15 *Preparative methods*

Certain embodiments of the mill-base and paint composition of the present invention may be prepared in accordance with conventional methods known in the art. This comprises combining, e.g., mixing, and processing mill-base and/or paint components
20 in appropriate amounts (depending on the desired paint composition) and under suitable conditions to obtain a mill-base or paint composition. The mill-base and/or paint components may be processed by milling or in a high-speed dispersion tank in which the premixed components are subjected to high-speed agitation by a circular, toothed blade attached to a rotating shaft. The processed composition is then typically
25 thinned by agitation with a suitable amount of solvent for the type of paint desired to produce the final paint product.

Applications

30 The paint composition of the present invention may be applied to a substrate, e.g., an article of manufacture which are many and various, (e.g., a handy-craft item, a piece of furniture, a vehicle or sea-going vessel, piping, and the like) or a surface, e.g., the surface of a constructional element (e.g., interior/exterior walls, ceilings and floors of a dwelling place, outside fencing and trimming, and the like).

35

Also provided is a canned paint comprising the paint composition of the second aspect of the invention. The term 'canned' is used herein to refer to any container suitable for paint, for example, a can, tub, bottle or pouch. The container may be formed from any material suitable for containing paint such as, for example, metal, plastic and glass.

5 For the avoidance of doubt, the present application is directed to the subject-matter defined in the following numbered paragraphs:

1. A mill-base for paint, which comprises microfibrillated cellulose, wherein the microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10
10 % by weight based on the total weight of a paint composition formulated from said mill base.

2. A mill-base according to paragraph 1, further comprising co-processed inorganic particulate material as primary pigment and/or extender pigment, wherein said
15 inorganic particulate material is co-processed with a fibrous substrate comprising cellulose during the preparation of said microfibrillated cellulose.

3. A mill-base according to paragraph 1 or 2, comprising primary pigment and/or extender pigment, other than the co-processed inorganic particulate material of claim 2.
20

4. A mill-base according to paragraph 1 or 3, wherein said microfibrillated cellulose is obtainable by a method comprising microfibrillating a fibrous substrate comprising cellulose in an aqueous environment by grinding in the presence of a grinding medium which is to be removed after the completion of grinding, wherein the grinding is carried
25 out in the absence of grindable inorganic particulate material.

5. A mill-base according to paragraph 2 or 3, wherein said microfibrillated cellulose is obtainable by a method comprising microfibrillating a fibrous substrate comprising cellulose in an aqueous environment in the presence of said inorganic particulate
30 material, optionally wherein the microfibrillating step comprises grinding the fibrous substrate comprising cellulose in the presence of the inorganic particulate material.

6. A mill-base according to paragraph 4 or 5, wherein the grinding is performed in a tower mill, screened grinder, stirred media mill or stirred media detritor.
35

7. A mill-base according to any preceding numbered paragraph comprising rheology modifier other than said microfibrillated cellulose.
8. A mill-base according to paragraph 7, wherein said rheology modifier is a cellulose-derived rheology modifier, for example, hydroxyethyl cellulose, hydroxymethyl cellulose, hydroxypropyl cellulose, hydroxypropylmethyl cellulose, carboxymethyl cellulose or a mixture thereof.
9. A mill-base according to paragraph 8, wherein the weight ratio of microfibrillated cellulose to said cellulose-derived rheology modifier is from about 1000:1 to about 1:4.
10. A mill-base according to any one of paragraphs 1-7, wherein said mill-base is free of cellulose-derived rheology modifier other than said microfibrillated cellulose.
11. A mill-base according to any one of paragraphs 1-10, comprising titanium dioxide as a primary pigment.
12. A mill-base according to any one of paragraphs 2-11, wherein said extender pigment is selected from one or more of an alkaline earth metal carbonate or sulphate, such as calcium carbonate, magnesium carbonate, dolomite, gypsum, a hydrous kandite clay such as kaolin, halloysite or ball clay, an anhydrous (calcined) kandite clay such as metakaolin or fully calcined kaolin, talc, mica, perlite, feldspars, nepheline syenite, wollastonite, diatomaceous earth, barite, glass, and natural or synthetic silica or silicates
13. A mill-base according to any one of paragraphs 2-11, wherein said co-processed inorganic particulate material is selected from one or more of an alkaline earth metal carbonate or sulphate, such as calcium carbonate, magnesium carbonate, dolomite, gypsum, a hydrous kandite clay such as kaolin, halloysite or ball clay, an anhydrous (calcined) kandite clay such as metakaolin or fully calcined kaolin, talc, mica, perlite, feldspars, nepheline syenite, wollastonite, diatomaceous earth, barite, glass, and natural or synthetic silica or silicates
14. A paint composition comprising microfibrillated cellulose, binder and solvent, wherein the microfibrillated cellulose is present in an amount ranging from about 0.1 % to about 10 % by weight based on the total weight of the paint composition.

15. The paint composition according to paragraph 14, which is formulated from the mill-based according to any one of paragraphs 1-13.
16. The paint composition according to paragraph 14 or 15, wherein the binder is a latex binder.
17. The paint composition according to any one of paragraphs 14-16, wherein the solvent is water.
18. The paint composition according to any one of paragraphs 14-17, wherein said paint is formulated for use as a decorative paint, for example, a matt paint.
19. A mill base or paint composition according to any preceding numbered paragraph, wherein said microfibrillated cellulose and optionally co-processed inorganic particulate material is provided in the form of an aqueous slurry or damp pressed cake.
20. Use of microfibrillated cellulose as defined in paragraph 4 and/or paragraph 5 as a rheology modifier in a-mill base for paint or a paint composition.
21. Use of microfibrillated cellulose as defined in paragraph 4 and/or paragraph 5 as a replacement or partial replacement for conventional cellulose-derived rheology modifier in a mill-base for paint or a paint composition.
22. Use according to paragraph 20, wherein said conventional cellulose-derived rheology modifier is selected from hydroxyethyl cellulose, hydroxymethyl cellulose, hydroxypropyl cellulose, hydroxypropylmethyl cellulose, carboxymethyl cellulose and mixtures thereof.
23. Use according to any one of paragraphs 20 -22 for one or more of:
- (i) increasing hiding power;
 - (ii) increasing opacity (contrast ratio);
 - (iii) reducing gloss at 85°; and
 - (iv) improving wet scrub resistance.

24. A substrate coated with a paint composition according to any one of paragraphs 14-19.

25. The coated substrate of paragraph 23, wherein the substrate is an article of
5 manufacture or the surface of one or more constructional elements.

26. The coated substrate of paragraph 25, wherein said constructional element is a wall or floor or ceiling.

27. The coated substrate of paragraph 25, wherein said constructional elements form
10 the interior of a dwelling.

28. A canned paint comprising the paint composition according to any one of paragraphs 14-18.

15 Embodiments of the present invention will now be described by way of illustration only, with reference to the following examples.

EXAMPLES

20 *Example 1*

A series of paint formulations were mixed under high shear in which the standard hydroxyethyl cellulose component was progressively replaced by microfibrillated cellulose. Details of the formulations are shown in Table 1. The microfibrillated
25 cellulose (MFC) sample was made by co-grinding a ground calcium carbonate having a d_{50} of 1.4 μm with Botnia northern bleached sulphate pulp in a stirred media mill at a specific energy of 2500 kWh/tonne of pulp. The MFC used in the paint formulation was provided in the form of an aqueous slurry comprising 2 % by weight microfibrillated cellulose and 8 % by weight ground calcium carbonate.

30

Figure 1 shows the rheology profiles (viscosity as a function of shear rate) of the formulations used. Replacement of the hydroxyethyl cellulose rheology modifier with microfibrillated cellulose prepared in accordance with the methods described herein maintains the paint viscosity at high shear rate approximately constant, but significantly
35 increases viscosity at low shear rate. This will have the effect of making the paint more stable and drip-resistant whilst remaining easy to brush.

Table 1.

	Control	Formulation A	Formulation B	Formulation C	Formulation D
Rutile pigment coated with alumina (TiO ₂ content – 94 %)	10	10	10	10	10
Refined kaolin having a d ₅₀ of 0.7 µm	10	10	10	10	10
CaCO ₃ having a d ₅₀ of 2.6 µm	18	18	18	18	18
Talc having a d ₅₀ of 9 µm	6	6	6	6	6
MFC (2% microfibrillated cellulose, 8% co-processed CaCO ₃)	0	5	10	15	20
Natrosol 250MR (2% hydroxyethyl cellulose solution in water)	20	15	10	5	0
Defoamer (Dispclair CF24)	0.3	0.3	0.3	0.3	0.3
Dispersant (Dispex A40 and 10% Calgon)	0.85	0.85	0.85	0.85	0.85
Biocide (Acticide BX(N))	0.2	0.2	0.2	0.2	0.2
pH adjustor (Ammonia 0.880)	0.05	0.05	0.05	0.05	0.05
Binder (PVA latex)	14	14	14	14	14
Rheology modifier (Acrysol TT935 diluted 1:2)	2.25	2.25	2.25	2.25	2.25
Water	18.35	18.35	18.35	18.35	18.35
Total	100	100	100	100	100

Table 2 shows the properties of drawdown films of the paint formulations described in Table 1. Substitution of hydroxyethyl cellulose increases the light scattering coefficient of the film, thus improving its opacity and hiding power. It also results in a significant reduction in gloss at 85°, which is important for a matt paint. It can also be seen that the substitution results in an improvement in the wet scrub resistance of the paint, since the loss of film thickness in the standard scrubbing test used is lower for formulations containing microfibrillated cellulose prepared in accordance with the methods described herein. Opacity (contrast ratio) and hiding power (which is the spreading rate required to obtain a contrast ratio of 98%) were determined in accordance with ISO 6504-1. Gloss was determined in accordance with ISO 2813. Wet scrub resistance was determined in accordance with ISO 11998.

Table 2.

Paint	Scattering Coefficient	Absorption Coefficient	Contrast Ratio at 20 m ² /l	Hiding Power V _{0.98}	Gloss %			Wet Scrub Resistance
	mm ⁻¹	mm ⁻¹	%	m ² /l	20°	60°	85°	Average Loss in Film Thickness, μm
Control	96.06	0.40	92.90	10.04	1.4	2.6	8.1	45
Formulation A	98.87	0.41	93.20	10.32	1.4	2.5	6.0	45
Formulation B	102.01	0.41	93.51	10.61	1.4	2.5	5.4	not measured
Formulation C	104.11	0.41	93.71	10.80	1.4	2.5	4.8	29
Formulation D	115.15	0.42	94.61	11.80	1.4	2.5	4.5	31

Example 2

- 5 A second series of paint formulations, this time with a portion of the talc replaced with a coarse calcium carbonate (having a d₅₀ of 6.5 μm, were mixed under high shear in which the standard hydroxyethyl cellulose component was progressively replaced by microfibrillated cellulose. Details of the formulations are shown in Table 3, and properties of the paint films in Tables 4a and 4b.

10

The mud cracking propensity of these paints was assessed by the drawdown of films which increase in thickness across their width, and recording of the film thickness in microns at which cracking after drying first appears. The higher the thickness at which cracking is observed, the lower is the tendency of the paint to give cracking problems in

15

use.

Mud cracking was determined in the following manner:

Materials and apparatus:

20

- Substrate: gypsum plasterboard
- Wedge applicator (300 to 1500 μm wet film thickness)
- Series of bar applicators (1500, 1750, 2000, 2250 and 2500 μm wet film thickness)

25

- Ruler (0 to 300 mm)

Procedure:

- The paint is applied onto the plasterboard substrate (before Rotothinner analysis to eliminate further introduction of air into the paint) using either the wedge applicator or the series of bars or both if the approximate end result is not known. The applicator is slowly drawn down across the substrate to allow any air bubbles to disperse.
 - The coatings are dried at 23°C +/- 2°C and 50% +/- 5% relative humidity and left for 24 hours. The plasterboard should be laid flat on a shelf or similar and left to reduce the risk of premature cracking.
- 10 - *measurement - wedge applicator*
- The result quoted is the point on the paint film where cracks appear within every 1 cm all the way down the film; a line should be drawn along the cracks. Cracks that have formed as a result of air bubbles should be excluded.
 - The distance between the left hand edge of the film (300 µm edge) and the line is measured.
- 15 - *calculation of the result*
- As the distance between 300 µm and 1500 µm wet film thickness is 10 cm, the actual film thickness where the line is drawn can be calculated by:
- $$\text{Mud Crack } (\mu\text{m}) = (\text{Distance of line from 300 } \mu\text{m thickness (cm)} \times 120) + 300$$
- 20 - *measurement – bar applicators*
- Record the thinnest wet film thickness that shows evidence of mud cracking (excluding any cracking caused as a result of air bubbles) as the final result.
- 25 The mud crack results present below were determined in accordance with the wedge applicator measurement.

The propensity of these paint films to burnish – i.e., to increase in gloss when rubbed – was also determined, and the results recorded as the increase in 85° gloss after 50 rubbing cycles.

30

Burnish was determined in the following manner.

Materials and apparatus:

- Substrate: glass panel, 4mm thick, dimensions 30 cm x 10 cm
- Block applicator with a gap of 100µm
- 5 - Erichsen Automatic Film Applicator (509 mk111)
- Glossmeter: Sheen Tri Glossmaster 20/60/85°
- Erichsen Scrub Tester
- Sponge holder, stainless steel, weight 360g
- Sponge pad plus abrasive pad
- 10 - Cloth, similar to J cloth

Procedure:

- The test film is applied onto the glass substrate using the Erichsen automatic applicator.
- 15 • The coated panel is dried at 23°C +/- 2°C and 50% +/- 5% relative humidity and left for 24 hours.
- The gloss is measured (normally at 85°; 5 separate areas down the length of the panel, quoting the average value). This is the 'initial gloss'.
- The glass panel is placed on the scrub tester and secured.
- 20 • The cloth is wrapped around the sponge pad and abrasive pad and placed into the sponge holder, ensuring that the pad/cloth is protruding approximately 5 mm out of the bottom of the sponge holder.
- The sponge holder is secured on top of the glass panel with the cloth in contact with the paint film.
- The paint film is rubbed/scrubbed for 50 cycles.
- 25 • The gloss over the area rubbed by the cloth is re-measured (in the same manner as the initial gloss. The re-measured gloss is the 'final gloss'.

- The burnish result quoted is the increase in gloss (final gloss - initial gloss).

A new piece of cloth should be used for each rubbing, The same side of the cloth should be used each time. If the cloth has a noticeable pile this should always be placed around the sponge so that the pile will rub in the same direction.

Table 3.

	Control 2	Formulation E	Formulation F	Formulation G
Rutile pigment coated with alumina (TiO ₂ content – 94 %)	10	10	10	10
Refined kaolin having a d ₅₀ of 0.7 μm	10	10	10	10
CaCO ₃ having a d ₅₀ of 2.6 μm	18	18	18	18
CaCO ₃ having a d ₅₀ of 6.5 μm	4	4	4	4
Talc having a d ₅₀ of 9 μm	2	2	2	2
MFC (2% microfibrillated cellulose, 8% co-processed CaCO ₃)	0	5	10	15
Natrosol 250MR (2% hydroxyethyl cellulose solution in water)	20	15	10	5
Defoamer (Dispelair CF24)	0.3	0.3	0.3	0.3
Dispersant (Dispex A40 and 10% Calgon)	0.85	0.85	0.85	0.85
Biocide (Acticide BX(N))	0.2	0.2	0.2	0.2
pH adjustor (Ammonia 0.880)	0.05	0.05	0.05	0.05
Binder (PVA latex)	14	14	14	14
Rheology modifier (Acrysol TT935 diluted 1:2)	2.25	2.25	2.25	2.25
Water	18.35	18.35	18.35	18.35
Total	100	100	100	100

Table 4a.

Paint	Scattering Coefficient	Absorption Coefficient	Contrast Ratio at 20m ² /l	Hiding Power V _{0.98}	Gloss %		
	mm ⁻¹	mm ⁻¹	%	m ² /l	20°	60°	85°
Control 2	74.59	0.32	89.73	7.82	1.4	2.5	7
Formulation E	75.62	0.32	89.93	7.94	1.4	2.5	6.0
Formulation F	77.38	0.32	90.23	8.10	1.4	2.5	5.2
Formulation G	81.10	0.34	90.86	8.48	1.4	2.5	4.7

Table 4b.

Paint	Mudcrack	Burnish Resistance
	μm	Difference in 85 degree gloss
Control 2	940	6
Formulation E	910	5.3
Formulation F	1100	4.7
Formulation G	1190	4.4

Example 3

- 5 The sample of microfibrillated cellulose from Example 1 was diluted to 2.5 wt% total solids and passed once through a GEA Niro Soavi homogeniser (model: Pony NS2006L) at 500 bar pressure. The product from the homogenizer was then concentrated back to 10% solids (2% microfibrillated cellulose) by centrifuge and used progressively to substitute hydroxyethyl cellulose in the equivalent formulation as used
- 10 in Example 2. Formulation details are provided in Table 5.

The optical properties of the paint films made from these formulations are summarized in Table 6. As can be seen, the further treatment leads to a greater enhancement of the light scattering and, thus, opacity of the paint. Rheology profiles are shown in

15 Figure 2 – again the microfibrillated cellulose enhances the viscosity of the formulation at low shear.

20

25

Table 5.

	Control 3	Formulation H	Formulation I	Formulation J	Formulation K
Rutile pigment coated with alumina (TiO ₂ content – 94 %)	10	10	10	10	10
Refined kaolin having a d ₅₀ of 0.7 µm	10	10	10	10	10
CaCO ₃ having a d ₅₀ of 2.6 µm	18	18	18	18	18
CaCO ₃ having a d ₅₀ of 6.5 µm	4	4	4	4	4
Talc having a d ₅₀ of 9 µm	2	2	2	2	2
MFC (2% microfibrillated cellulose, 8% co-processed CaCO ₃)	0	5	10	15	20
Natrosol 250MR (2% hydroxyethyl cellulose solution in water)	20	15	10	5	0
Defoamer (Dispelair CF24)	0.3	0.3	0.3	0.3	0.3
Dispersant (Dispex A40 and 10% Calgon)	0.85	0.85	0.85	0.85	0.85
Biocide (Acticide BX(N))	0.2	0.2	0.2	0.2	0.2
pH adjustor (Ammonia 0.880)	0.05	0.05	0.05	0.05	0.05
Binder (PVA latex)	14	14	14	14	14
Rheology modifier (Acrysol TT935 diluted 1:2)	2.25	2.25	2.25	2.25	2.25
Water	18.35	18.35	18.35	18.35	18.35
Total	100	100	100	100	100

Table 6.

Paint	Scattering Coefficient	Absorption Coefficient	Contrast Ratio at 20m ² /l	Hiding Power V _{0.98}	Gloss %		
	mm ⁻¹	mm ⁻¹	%	m ² /l	20°	60°	85°
Control 3	77.52	0.35	90.30	8.19	1.3	2.4	5.1
Formulation H	91.96	0.36	92.36	9.51	1.4	2.4	5.6
Formulation I	97.96	0.36	93.03	10.07	1.4	2.5	5.4
Formulation J	97.46	0.36	92.98	10.02	1.4	2.4	5.2
Formulation K	94.69	0.37	92.70	9.81	1.4	2.4	4.7

What is claimed is:

1. A paint composition comprising at least one rheology modifier, a binder, a solvent, a primary pigment, and, at least one extender pigment, wherein the at least one extender pigment is one or more of, kaolin, calcium carbonate and talc, wherein the at least one rheology modifier comprises a microfibrillated cellulose, wherein the paint composition is free of cellulose-derived rheology modifier other than the microfibrillated cellulose, and wherein the microfibrillated cellulose is present in an amount of from about 0.1 % to about 10 % by weight based on the total weight of the paint composition, comprising co-processed inorganic particulate material as at least one of the primary pigment and the extender pigment, wherein the inorganic particulate material is co-processed with a fibrous substrate comprising cellulose during the preparation of the microfibrillated cellulose, wherein the microfibrillated cellulose has a d_{50} of from about 5 μm to about 500 μm as measured by laser light scattering, wherein the microfibrillated cellulose has a fibre steepness of from about 20 to about 50, and wherein the microfibrillated cellulose improves one or more of the properties of the paint composition selected from the group consisting of improvement in wet scrub resistance of a dry film of no more than 45 μm determined in accordance with ISO 11998; a reduction in gloss at 85 degree of less than 7.0 determined in accordance with ISO 2813; a reduction in burnish of less than 5:8; and mud cracking thickness of at least 1,000 μm , compared to an equivalent paint composition not comprising microfibrillated cellulose as a rheology modifier.
2. The paint composition according to claim 1, wherein the binder is a latex binder, and the solvent is water.

3. The paint composition according to claim 1 or 2, wherein the paint composition is formulated for use as a decorative paint comprising matte paint.
4. The paint composition according to any one of claims 1 to 3, wherein the microfibrillated cellulose maintains the paint viscosity, at high shear rate 1/s of at least 100 and significantly increases paint viscosity at low shear rate of no more than 10, thereby improving the stability and drip-resistance of the paint composition.
5. The paint composition according to claim 4, wherein the paint viscosity is determined in accordance with ISO 2884-1.
6. The paint composition according to any one of claims 1 to 5, further comprising a rheology modifier other than microfibrillated cellulose which is a non-cellulose derived rheology modifier.
7. The paint composition according to claim 6, wherein the non-cellulose derived rheology modifier is selected from the group consisting of an acrylic associative thickener, polyacrylate, emulsion copolymer, dicyanamide, triol, polyoxyethylene ether, urea, sulphated castor oil, polyvinyl pyrrolidone, sodium alginate, xanthan gum, sodium silicate, acrylic acid copolymer and mixtures thereof.
8. The paint composition according to claim 6 or 7, wherein the non-cellulose derived rheology modifier is present in an amount up to 5% by weight.
9. The paint composition according to any one of claims 1 to 8, wherein the primary pigment is selected from the group consisting of ground, natural,

inorganic, insoluble dispersed particles; ground, natural, organic, insoluble dispersed particles; ground, synthetic, inorganic, insoluble dispersed particles; and ground, synthetic, organic, insoluble dispersed particles;

which, when dispersed in a liquid vehicle, provide color.

10. The paint composition according to any one of claims 1 to 8, wherein the primary pigment is selected from the group consisting of titanium dioxide, carbon black, calcium sulphate, iron oxide, and a copper-complex phthalo blue.

11. The paint composition according to any one of claims 1 to 10, wherein the primary pigment has a mean particle size d_{50} of from about 0.1 μm to about 20 μm , as determined by Sedigraph™.

12. The paint composition according to any one of claims 1 to 11, wherein the extender pigment has a mean particle size d_{50} of from about 0.1 μm to about 20 μm , as determined by Sedigraph™.

13. The paint composition according to any one of claims 1 to 12, wherein the co-processed inorganic particulate material has a mean particle size d_{50} of from about 0.1 μm to about 20 μm , as determined by Sedigraph™.

14. The paint composition according to any one of claims 1 to 13, wherein the co-processed inorganic particulate material is selected from the group consisting of an alkaline earth metal carbonate and sulphate.

15. The paint composition according to any one of claims 1 to 13, wherein the co-processed inorganic particulate material is selected from the group consisting of calcium carbonate, magnesium carbonate, dolomite, gypsum, a hydrous kandite clay, kaolin, halloysite, ball clay, an anhydrous calcined kandite clay, metakaolin, fully calcined kaolin, talc, mica, perlite, feldspars, nepheline syenite, wollastonite, diatomaceous earth, barite, glass, natural silica, synthetic silica, natural silicates and synthetic silicates.

16. The paint composition according to any one of claims 1 to 15, wherein the microfibrillated cellulose is further treated in a homogenizer under wet conditions.

17. A canned paint comprising the paint composition according to any one of claims 1 to 16.

Figure 1

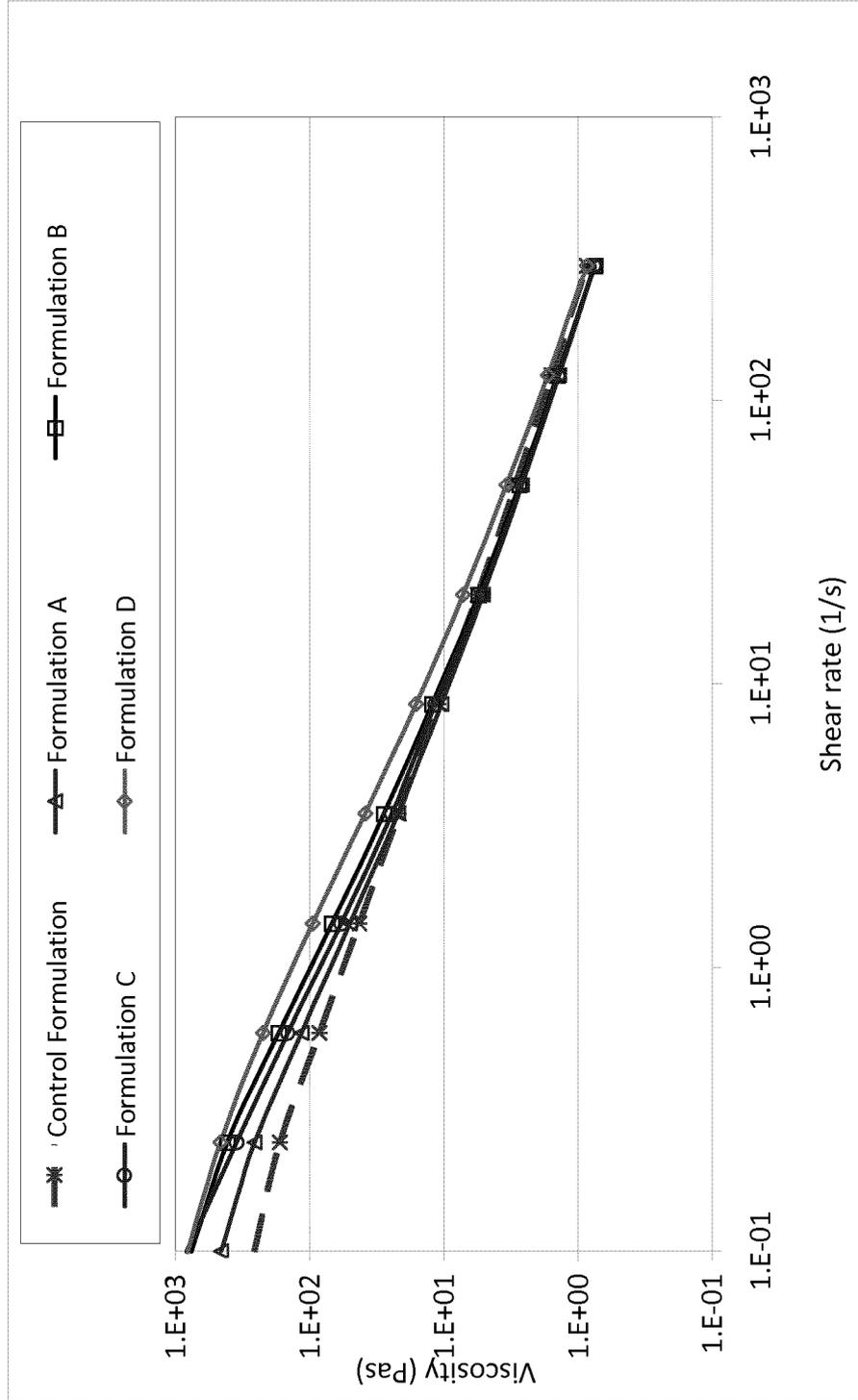


Figure 2

