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(54) **Titre : PROCÉDES D'AUGMENTATION DE LA CONCENTRATION D'UN CATALYSEUR LORS DE L'HYDROCRAQUAGE
D'HUILE LOURDE ET/OU DE RESIDUS DE CHARBON**
(54) **Title: METHODS FOR INCREASING CATALYST CONCENTRATION IN HEAVY OIL AND/OR COAL RESID HYDROCRACKER**

(57) **Abrégé/Abstract:**

Methods and systems for hydrocracking a heavy oil feedstock using a colloiddally or molecularly dispersed catalyst (e.g., molybdenum sulfide) which provide for concentration of the colloiddally dispersed catalyst within the lower quality materials requiring additional hydrocracking. In addition to increased catalyst concentration, the inventive systems and methods provide increased reactor throughput, increased reaction rate, and of course higher conversion of asphaltenes and lower quality materials. Increased conversion levels of asphaltenes and lower quality materials also reduces equipment fouling, enables the reactor to process a wider range of lower quality feedstocks, and can lead to more efficient use of a supported catalyst if used in combination with the colloiddal or molecular catalyst.



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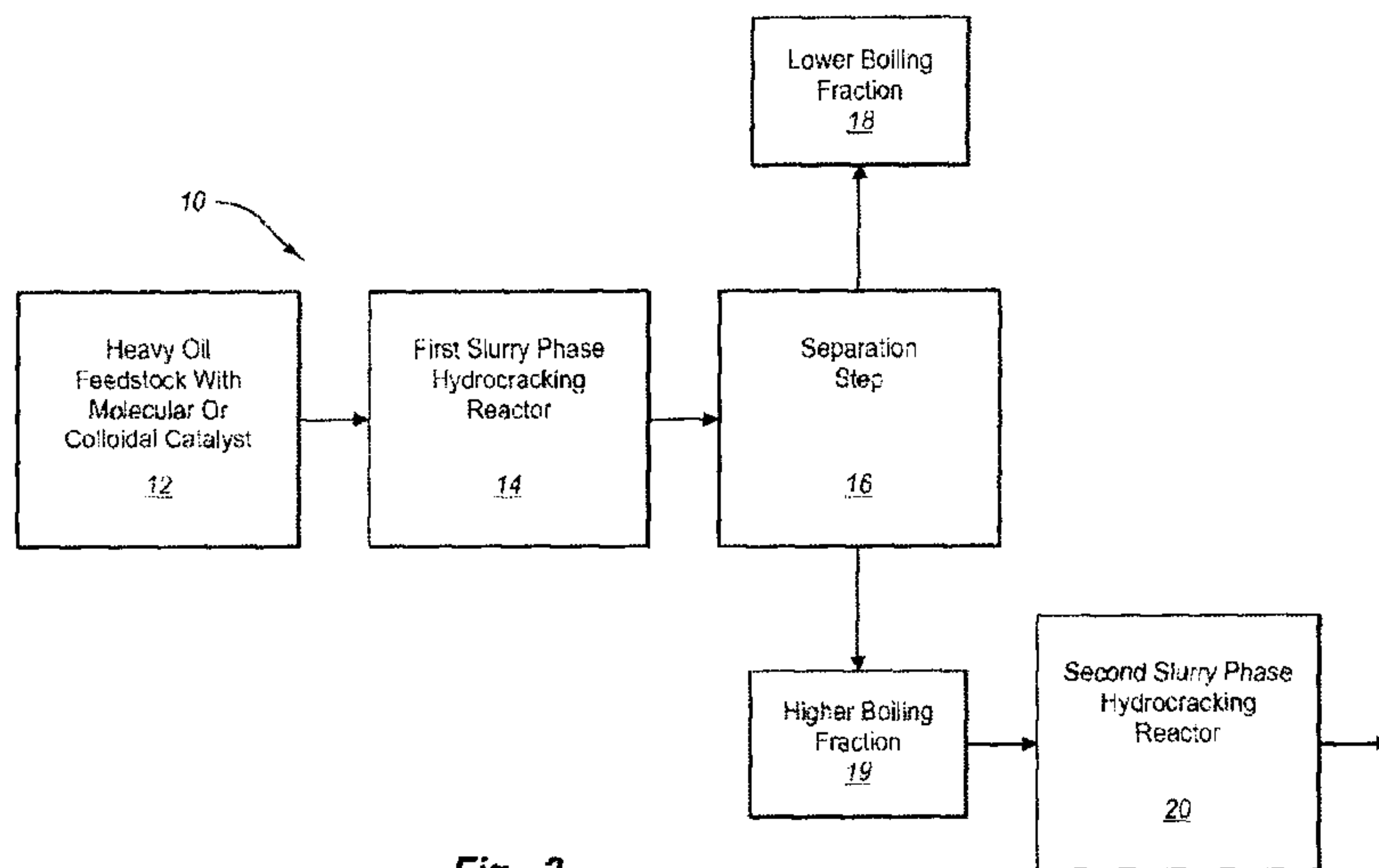


Fig. 2

(57) Abstract: Methods and systems for hydrocracking a heavy oil feedstock using a colloiddally or molecularly dispersed catalyst (e.g., molybdenum sulfide) which provide for concentration of the colloiddally dispersed catalyst within the lower quality materials requiring additional hydrocracking. In addition to increased catalyst concentration, the inventive systems and methods provide increased reactor throughput, increased reaction rate, and of course higher conversion of asphaltenes and lower quality materials. Increased conversion levels of asphaltenes and lower quality materials also reduces equipment fouling, enables the reactor to process a wider range of lower quality feedstocks, and can lead to more efficient use of a supported catalyst if used in combination with the colloidal or molecular catalyst.

METHODS FOR INCREASING CATALYST CONCENTRATION IN HEAVY OIL AND/OR COAL RESID HYDROCRACKER

1. The Field of the Invention

5 The present invention is in the field of upgrading heavy hydrocarbon feedstocks such as heavy oil and/or coal (*e.g.*, coal liquefaction) into lower boiling, higher quality materials.

2. Related Technology

World demand for refined fossil fuels is ever-increasing and will eventually
10 outstrip the supply of high quality crude oil. As the shortage of high quality crude oil increases there will be an increasing demand to find ways to better exploit lower quality feedstocks and extract fuel values from them.

Lower quality feedstocks are characterized as including relatively high quantities of hydrocarbons that have a boiling point of 524 °C (975 °F) or higher.
15 They also contain relatively high concentrations of sulfur, nitrogen and/or metals. High boiling fractions typically have a high molecular weight and/or low hydrogen/carbon ratio, an example of which is a class of complex compounds collectively referred to as “asphaltenes”. Asphaltenes are difficult to process and commonly cause fouling of conventional catalysts and hydroprocessing equipment.

20 Examples of lower quality feedstocks that contain relatively high concentrations of asphaltenes, sulfur, nitrogen and metals include heavy crude and oil sands bitumen, as well as bottom of the barrel and residuum left over from conventional refinery processes (collectively “heavy oil”). The terms “bottom of the barrel” and “residuum” (or “resid”) typically refer to atmospheric tower bottoms,
25 which have a boiling point of at least 343 °C (650 °F), or vacuum tower bottoms, which have an initial boiling point of at least 524 °C (975 °F). The terms “resid pitch” and “vacuum residue” are commonly used to refer to fractions that have an initial boiling point of 524 °C (975 °F) or greater.

Converting heavy oil into useful end products requires extensive processing,
30 including reducing the quantity of heavy oil by converting it to lighter, lower boiling petroleum fractions, increasing the hydrogen-to-carbon ratio, and removing impurities such as metals, sulfur, nitrogen and high carbon forming compounds.

When used with heavy oil, existing commercial catalytic hydrocracking processes become fouled or rapidly undergo catalyst deactivation. The undesirable reactions and fouling involved in hydrocracking heavy oil greatly increases the catalyst and maintenance costs of processing heavy oils, making current catalysts less economical for hydroprocessing heavy oil.

One promising technology for hydroprocessing heavy oils uses a hydrocarbon-soluble molybdenum salt that decomposes in the heavy oil during hydroprocessing to form, *in situ*, a hydroprocessing catalyst, namely molybdenum sulfide. One such process is disclosed in U.S. Patent No. 5,578,197 to Cyr et al.

Once formed *in situ*, the molybdenum sulfide catalyst is highly effective at hydrocracking asphaltenes and other complicated hydrocarbons while preventing fouling and coking.

A significant problem with commercializing oil soluble molybdenum catalysts is the cost of the catalyst. Even small improvements in catalyst performance can have a significant benefit to the economics of the hydrocracking process due to the increase in output and/or the reduced use of the catalyst.

The performance of oil soluble molybdenum catalysts depends significantly on how well the catalyst precursor can be dispersed in the heavy oil and/or other heavy hydrocarbon (*e.g.*, coal) feedstock and the concentration of the metal catalyst in the heavy hydrocarbon being cracked. It would be an improvement in the art to provide methods and systems that result in concentration of the metal catalyst within feed streams containing heavy hydrocarbon components requiring additional hydrocracking, which would minimize the overall quantity of catalyst used and improve the overall efficiency and conversion levels, all while minimizing processing costs.

SUMMARY OF THE PREFERRED EMBODIMENTS

The present invention relates to methods and systems for hydrocracking a heavy hydrocarbon (*e.g.*, heavy oil and/or coal) feedstock using a colloiddally or molecularly dispersed catalyst (*e.g.*, molybdenum sulfide). It is believed that the present systems and processes may be used to upgrade a coal feedstock and/or mixtures of heavy oil and coal feedstock as well as liquid heavy oil feedstocks. As such, the term heavy oil as used herein may broadly include coal, for example as used

in a coal liquefaction system to upgrade the coal feedstock (and/or a mixture of liquid heavy oil and coal) into higher quality, lower boiling hydrocarbon materials. The inventive methods and systems advantageously provide for concentration of the colloidally dispersed catalyst within the lower quality materials needing additional hydrocracking in order to form lower boiling higher value materials without expensive and complicated separation steps to remove the catalyst from product streams containing the desired product materials, and without requiring additional catalyst, both of which can be prohibitively expensive. In addition to increased catalyst concentration, the inventive systems and methods provide increased reactor throughput, increased reaction rate, and of course higher conversion levels of asphaltenes and high boiling lower quality materials. Increased conversion levels of asphaltenes and lower quality materials also reduces equipment fouling, enables the reactor to process a wider range of lower quality feedstocks, and can lead to more efficient use of a supported catalyst if such is used in combination with the colloidal or molecular catalyst.

An exemplary system includes a first gas-liquid two or more phase hydrocracking reactor (*e.g.*, a two-phase gas-liquid reactor) and at least a second gas-liquid two or more phase hydrocracking reactor arranged in series with the first two or more phase reactor. For simplicity, the gas-liquid two or more phase reactors are herein referred to as gas-liquid two-phase reactors or simply hydrocracking reactors, although it is to be understood that they may optionally comprise a third (*i.e.*, solid) phase comprising, for example coal particles and/or a supported catalyst. Although it may be possible to operate the reactor systems with an ebullated bed of solid supported catalyst in addition to the colloidal and/or molecular catalyst, preferred systems may employ only the colloidal and/or molecular catalyst. Each gas-liquid two-phase reactor operates at a respective pressure. An interstage pressure differential separator is disposed between the first and second gas-liquid two-phase reactors. The interstage separator provides a pressure drop from the operating pressure of the first gas-liquid two-phase reactor (*e.g.*, 2400 psig) down to a second, lower pressure (*e.g.*, the operating pressure of the second gas-liquid two-phase reactor, for example, 2000 psig). The pressure drop induced by the interstage separator allows the effluent from the first gas-liquid two-phase reactor to be

separated into a lighter lower boiling fraction (which volatilizes) and a higher boiling bottoms liquid fraction.

Advantageously, the colloidally dispersed catalyst remains with the higher boiling bottoms liquid fraction during the phase separation, resulting in a catalyst
5 concentration within the liquid fraction that is elevated as compared to the catalyst concentration within the overall effluent from the first gas-liquid two-phase hydrocracking reactor. In addition, the catalyst concentration within the liquid fraction is greater than the catalyst concentration of the heavy oil being fed into the first hydrocracking reactor. At least a portion of the higher boiling bottoms liquid
10 fraction is then introduced into the second gas-liquid two-phase hydrocracking reactor.

The pressure drop achieved upon entering the interstage separator may typically range between about 100 psi and about 1000 psi. Preferably, the pressure drop is between about 200 psi and about 700 psi, and more preferably the pressure
15 drop within the interstage separator is between about 300 and about 500 psi. Higher pressure drops result in a greater percentage of the first gas-liquid two-phase reactor effluent being volatilized and withdrawn with the lower boiling volatile gaseous vapor fraction. This, in turn, increases the efficiency of the second gas-liquid two-phase reactor by (1) increasing catalyst concentration; (2) reducing the volume of material
20 being hydrocracked so that a smaller second reactor may be employed; (3) withdrawing lighter boiling fraction materials (*e.g.*, C₁-C₇ hydrocarbons) which may otherwise tend to promote additional asphaltene and/or coke formation; and (4) increasing the concentration of materials in need of upgrading. Additional fresh hydrogen gas is introduced into the second reactor with the liquid effluent from the
25 interstage separator, such that the pressure within the second reactor may be higher than the pressure within the separator (*e.g.*, it may be pressurized back up to the operating pressure of the first reactor).

The molybdenum sulfide catalyst is concentrated within the higher boiling liquid fraction that is withdrawn out the bottom of the interstage pressure differential
30 separator. For example, the catalyst concentration within the higher boiling bottoms liquid fraction introduced into the second gas-liquid two-phase hydrocracking reactor may have a catalyst concentration that is at least about 10 percent higher than the

concentration of the catalyst present within the effluent from the first gas-liquid two-phase hydrocracking reactor, as a result of the lighter fraction (which is substantially free of catalyst) being separated and drawn off as vapor within the interstage separator. More preferably, the catalyst concentration within the higher boiling bottoms liquid fraction introduced into the second gas-liquid two-phase hydrocracking reactor is at least about 25 percent higher than the concentration of the catalyst present within the effluent from the first gas-liquid two-phase reactor, and most preferably the concentration within the higher boiling bottoms liquid fraction introduced into the second hydrocracking reactor is at least about 30 percent higher than the concentration of the catalyst present within the effluent from the first reactor.

Typically, the concentration of catalyst entering the second reactor may range between about 10 percent and about 100 percent higher than the catalyst concentration within the first reactor, more preferably between about 20 percent and about 50 percent higher, and most preferably between about 25 percent and about 40 percent higher. Stated another way, preferably about 10 percent to about 50 percent of the material is flashed off within the interstage separator, more preferably between about 15 percent and about 35 percent of the material is flashed off within the interstage separator, and most preferably between about 20 percent and about 30 percent of the material is flashed off within the interstage separator.

In one exemplary system and method, no recycle of the higher boiling bottoms liquid fraction from the interstage separator back into the first gas-liquid two-phase hydrocracking reactor (*e.g.*, as a source of feedstock and/or catalyst) is necessary, as the present system provides for higher boiling effluent material remaining from the first reactor to be sent to the second reactor. In other words, all of the liquid fraction from the interstage separator may be introduced into the second gas-liquid two-phase hydrocracking reactor.

The system may further include a third gas-liquid two-phase hydrocracking reactor and a second interstage separator disposed between the second gas-liquid two-phase reactor and the third gas-liquid two-phase reactor. Such a second interstage separator performs another separation between lighter lower boiling volatile gaseous vapor materials which are drawn off and a second higher boiling bottoms liquid fraction in which the colloidally and/or molecularly dispersed catalyst is even more

concentrated. Additional gas-liquid two-phase (or other type) reactors and interstage pressure differential or other type separators may also be provided, although such additional equipment may be unnecessary, as the inventors have found that systems that include two gas-liquid two-phase reactors and a single interstage separator
5 disposed therebetween can produce very high conversion levels of asphaltenes (*e.g.*, 60 to 80 percent or more). Of course, overall conversion level is dependent on catalyst concentration, reactor temperature, space velocity, and number of reactors, as well as other variables. Those skilled in the art will appreciate that reactor systems according to the present invention may be designed and configured to maximize
10 and/or minimize any desired variable within given constraints relative to the remaining variables.

An alternative exemplary system includes a first gas-liquid two-phase hydrocracking reactor and at least a second gas-liquid two-phase hydrocracking reactor arranged in series with the first reactor. Lower boiling volatile gaseous vapor
15 effluent from the first gas-liquid two-phase reactor is withdrawn from the top of the first gas-liquid two-phase reactor separately from the remaining effluent (which principally includes higher boiling liquid effluent) from the first gas-liquid two-phase reactor. In other words, the effluent is separated into two phases, but without a formal interstage separation unit. Advantageously, the colloidally and/or molecularly
20 dispersed catalyst remains with the higher boiling liquid effluent fraction, resulting in a catalyst concentration within this stream that is elevated as compared to the catalyst concentration within the heavy oil feedstock introduced into the first hydrocracking reactor. The higher boiling liquid fraction stream is then introduced into the second gas-liquid two-phase hydrocracking reactor to further upgrade this material. The
25 reactor effluent from the second gas-liquid two-phase reactor is fed along with the lower boiling gaseous vapor fraction withdrawn from the first gas-liquid two-phase reactor is sent downstream for further processing and recovery of valuable streams.

In each embodiment, the inventive systems and methods result in concentration of the catalyst within the higher boiling liquid fraction requiring
30 additional hydrocracking. Such increased catalyst concentration provides increased reactor throughput, increased reaction rate, and of course higher conversion of asphaltenes and lower quality materials, all without the addition of new catalyst.

69767-47

7

Increased conversion levels of asphaltenes and lower quality materials also reduce equipment fouling, enable the gas-liquid two-phase hydrocracking reactors to process a wider range of lower quality feedstocks, and can lead to more efficient use of a supported catalyst if used in combination with the colloidal or molecular catalyst (*e.g.*, in an example where the hydrocracking reactors comprise three-phase reactors). In addition, withdrawal of at least some of the lower boiling volatile gaseous vapor fraction before introducing the remaining effluent into the second gas-liquid two-phase reactor reduces the volume of material to be reacted within the second gas-liquid two-phase reactor (*i.e.*, the second reactor can be smaller than would otherwise be required, resulting in a cost savings).

By removing the vapor components from the products of first reactor, the liquid throughput through the second reactor can be significantly increased (if reactor diameter remains constant). Alternatively, for a given reactor diameter, the reduction in vapor flow rate results in reduced gas hold up within the second reactor so that the reactor can be shorter to achieve a desired conversion level, or with a longer reactor, higher conversion can be achieved. In other words, there are vapor products generated (*e.g.*, including, but not limited to C₁-C₄ light hydrocarbons) within the reactor that are simply taking up space. Removal of these components lowers gas hold up, which may be thought of as effectively increasing the size of the reactor.

A further embodiment relates to a method of hydrocracking a heavy oil feedstock using a colloiddally or molecularly dispersed catalyst comprising: introducing a heavy oil feedstock including a colloiddally or molecularly dispersed catalyst or catalyst precursor into a first gas-liquid two or more phase hydrocracking reactor, said first gas-liquid two or more phase hydrocracking reactor having a first concentration of colloiddally or molecularly dispersed catalyst and producing an effluent; separating, using a pressure differential interstage separator which induces a pressure drop of at least 100 psi, said effluent produced from said first hydrocracking reactor into a lower boiling volatile gaseous vapor fraction and a higher boiling liquid fraction; introducing at least a portion of said higher boiling liquid fraction into a second gas-liquid two or more hydrocracking reactor, wherein

69767-47

7a

said higher boiling liquid fraction has a second concentration of colloiddally or molecularly dispersed catalyst that is greater than the first concentration of colloiddally or molecularly dispersed catalyst within said first hydrocracking reactor.

A still further embodiment relates to a system for hydrocracking heavy oil

5 using a colloiddally or molecularly dispersed catalyst comprising: a series of gas-liquid two or more phase hydrocracking reactors including at least a first gas-liquid two or more phase hydrocracking reactor operating at a first pressure and a second gas-liquid two or more phase hydrocracking reactor operating at a second pressure, said first hydrocracking reactor having a first concentration of colloiddally or molecularly dispersed catalyst; and a pressure differential

10 interstage separator disposed between said first hydrocracking reactor and said second hydrocracking reactor, said interstage separator receiving an effluent from said first hydrocracking reactor at said first pressure and providing a pressure drop of at least 100 psi so as to separate a lower boiling volatile gaseous vapor fraction from a higher boiling bottoms liquid fraction, at least a portion of said higher boiling bottoms liquid fraction being

15 introduced into said second hydrocracking reactor and wherein said higher boiling bottoms liquid fraction has a second concentration of colloiddally or molecularly dispersed catalyst that is greater than the first concentration of colloiddally or molecularly dispersed catalyst within said first hydrocracking reactor.

These and other advantages and features of the present invention will become

20 more fully apparent from the following description and appended claims, or may be learned by the practice of the invention as set forth hereinafter.

BRIEF DESCRIPTION OF THE DRAWINGS

To further clarify the above and other advantages and features of the present invention, a more particular description of the invention will be rendered by reference to

25 specific embodiments thereof which are illustrated in the appended drawings. It is appreciated that these drawings depict only typical embodiments of the invention and are therefore not to be considered limiting of its scope. The invention will be described and

69767-47

7b

explained with additional specificity and detail through the use of the accompanying drawings, in which:

Figure 1 depicts a hypothetical chemical structure for an asphaltene molecule;

Figure 2 is a block diagram that schematically illustrates an exemplary

hydrocracking system according to the invention for upgrading a heavy oil feedstock;

Figure 3 schematically illustrates a refining system that includes an exemplary hydrocracking system according to the invention as a module within the overall system;

5 Figure 4 schematically illustrates an alternative hydrocracking system;

Figure 5 schematically illustrates another example of an inventive hydrocracking system;

Figure 6 schematically illustrates catalyst molecules or colloidal-sized catalyst particles associated with asphaltene molecules; and

10 Figures 7A and 7B schematically depict top and side views of a molybdenum disulfide crystal approximately 1 nm in size.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

I. Introduction

The present invention relates to methods and systems for hydrocracking a heavy oil feedstock using a colloiddally and/or molecularly dispersed catalyst (*e.g.*, molybdenum sulfide). The inventive methods and systems advantageously provide for concentration of the colloiddally dispersed catalyst within the lower quality materials needing additional hydrocracking in order to form higher value materials without expensive and complicated separation steps to remove the catalyst from product streams containing the desired product materials, and without requiring the addition of new catalyst during the process, all of which may be prohibitively expensive. In addition to increased catalyst concentration, the inventive systems and methods reduce the volume of material introduced into downstream reactors and other equipment, provide increased reactor throughput, increased reaction rate, and of course higher conversion of asphaltenes and lower quality materials. Increased conversion levels of asphaltenes and lower quality materials also reduces equipment fouling, enables the reactor to process a wider range of lower quality feedstocks, and can lead to more efficient use of a supported catalyst if used in combination with the colloiddal or molecularly dispersed catalyst.

30 In one embodiment, the methods and systems employ two or more gas-liquid two or more phase hydrocracking reactors in series and an interstage pressure differential separator arranged between the reactors. The interstage separator operates

by subjecting the effluent from the first hydrocracking reactor to a pressure drop (*e.g.*, across a valve as the material enters the separator), causing a phase separation between a gaseous and/or volatile lower boiling fraction and a higher boiling liquid fraction of the effluent. Advantageously, the catalyst remains in the liquid fraction, substantially increasing the catalyst concentration within this fraction. The liquid fraction is then introduced into the second gas-liquid two or more phase hydrocracking reactor. Such an increase in catalyst concentration, as well as the reduction in volume of material (as a result of the lower boiling volatile gaseous/vapor fraction being removed) provides increased conversion levels at overall reduced cost. Furthermore, removal of low boiling point components from the stream prior to introduction into the second reactor results in reduced gas hold up (*i.e.*, gases occupy less of the reactor volume, and the partial pressure and/or fraction of hydrogen gas as a fraction of total gas volume is increased).

An alternative exemplary system also includes at least two gas-liquid two or more phase hydrocracking reactors arranged in series. Lower boiling volatile gaseous vapor effluent from the first reactor is withdrawn separately from the higher boiling liquid effluent from the first reactor (*i.e.*, the effluent is separated into two phases, but without a formal separation unit). Advantageously, the colloidally and/or molecularly dispersed catalyst remains with the higher boiling liquid effluent fraction, resulting in a catalyst concentration within this stream that is elevated as compared to the catalyst concentration within the heavy oil feedstock introduced into the first hydrocracking reactor. The higher boiling liquid fraction is then introduced into the second hydrocracking reactor to further upgrade this material. The reactor effluent from the second reactor is fed along with the lower boiling gaseous vapor fraction withdrawn from the first reactor downstream within the hydroprocessing system for further treatment and/or processing.

In each embodiment the inventive systems and methods provide increased reactor throughput, increased reaction rate, and of course higher conversion of asphaltenes and lower quality materials. Increased conversion levels of asphaltenes and lower quality materials to higher quality materials also reduces equipment fouling (*e.g.*, due to coke and/or asphaltene deposition), enables the gas-liquid two or more phase reactor system to process a wider range of lower quality feedstocks, and can

lead to more efficient use of a supported catalyst if used in combination with the colloidal or molecular catalyst.

II. Definitions

The terms “colloidal catalyst” and “colloidally-dispersed catalyst” shall refer to catalyst particles having a particle size that is colloidal in size, *e.g.*, less than about 100 nm in diameter, preferably less than about 10 nm in diameter, more preferably less than about 5 nm in diameter, and most preferably less than about 1 nm in diameter. The term “colloidal catalyst” includes, but is not limited to, molecular or molecularly-dispersed catalyst compounds.

The terms “molecular catalyst” and “molecularly-dispersed catalyst” shall refer to catalyst compounds that are essentially “dissolved” or completely dissociated from other catalyst compounds or molecules in a heavy oil hydrocarbon feedstock, non-volatile liquid fraction, bottoms fraction, resid, or other feedstock or product in which the catalyst may be found. It shall also refer to very small catalyst particles that only contain a few catalyst molecules joined together (*e.g.*, 15 molecules or less).

The terms “blended feedstock composition” and “conditioned feedstock composition” shall refer to a heavy oil feedstock into which an oil soluble catalyst precursor composition has been combined and mixed sufficiently so that, upon decomposition of the catalyst precursor and formation of the catalyst, the catalyst will comprise a colloidal and/or molecular catalyst dispersed within the feedstock.

The term “heavy oil feedstock” shall refer to heavy crude, oils sands bitumen, bottom of the barrel and resid left over from refinery processes (*e.g.*, visbreaker bottoms), and any other lower quality material that contains a substantial quantity of high boiling hydrocarbon fractions (*e.g.*, that boil at or above 343 °C (650 °F), more particularly at or above about 524 °C (975 °F)), and/or that include a significant quantity of asphaltenes that can deactivate a solid supported catalyst and/or cause or result in the formation of coke precursors and sediment. As used herein, the term may also broadly include coal, for example as used in a coal liquefaction system to upgrade the coal feedstock into higher quality, lower boiling hydrocarbon materials. Examples of heavy oil feedstocks include, but are not limited to, Lloydminster heavy oil, Cold Lake bitumen, Athabasca bitumen, atmospheric tower bottoms, vacuum tower bottoms, residuum (or “resid”), resid pitch, vacuum residue, and higher-boiling

liquid fractions that remain after subjecting crude oil, bitumen from tar sands, liquefied coal, or coal tar feedstocks to distillation, hot separation, and the like and that contain higher boiling fractions and/or asphaltenes.

The term “asphaltene” shall refer to the fraction of a heavy oil feedstock that is typically insoluble in paraffinic solvents such as propane, butane, pentane, hexane, and heptane and that includes sheets of condensed ring compounds held together by hetero atoms such as sulfur, nitrogen, oxygen and metals. Asphaltenes broadly include a wide range of complex compounds having anywhere from 80 to 160,000 carbon atoms, with predominating molecular weights, as determined by solution techniques, in the 5000 to 10,000 range. About 80-90% of the metals in the crude oil are contained in the asphaltene fraction which, together with a higher concentration of non-metallic hetero atoms, renders the asphaltene molecules more hydrophilic and less hydrophobic than other hydrocarbons in crude. A hypothetical asphaltene molecule structure developed by A.G. Bridge and co-workers at Chevron is depicted in Figure 1.

The term “hydrocracking” shall refer to a process whose primary purpose is to reduce the boiling range of a heavy oil feedstock and in which a substantial portion of the feedstock is converted into products with boiling ranges lower than that of the original feedstock. Hydrocracking generally involves fragmentation of larger hydrocarbon molecules into smaller molecular fragments having a fewer number of carbon atoms and a higher hydrogen-to-carbon ratio. The mechanism by which hydrocracking occurs typically involves the formation of hydrocarbon free radicals during fragmentation followed by capping of the free radical ends or moieties with hydrogen. The hydrogen atoms or radicals that react with hydrocarbon free radicals during hydrocracking are generated at or by active catalyst sites.

The term “hydrotreating” shall refer to a more mild operation whose primary purpose is to remove impurities such as sulfur, nitrogen, oxygen, halides, and trace metals from the feedstock and saturate olefins and/or stabilize hydrocarbon free radicals by reacting them with hydrogen rather than allowing them to react with themselves. The primary purpose is not to change the boiling range of the feedstock. Hydrotreating is most often carried out using a fixed bed reactor, although other hydroprocessing reactors can also be used for hydrotreating, an example of which is

an ebullated bed hydrotreater.

Of course, “hydrocracking” may also involve the removal of sulfur and nitrogen from a feedstock as well as olefin saturation and other reactions typically associated with “hydrotreating”. The term “hydroprocessing” shall broadly refer to
5 both “hydrocracking” and “hydrotreating” processes, which define opposite ends of a spectrum, and everything in between along the spectrum.

The terms “solid supported catalyst”, “porous supported catalyst” and “supported catalyst” shall refer to catalysts that are typically used in conventional ebullated bed and fixed bed hydroprocessing systems, including catalysts designed
10 primarily for hydrocracking or hydrodemetallization and catalysts designed primarily for hydrotreating. Such catalysts typically comprise (i) a catalyst support having a large surface area and numerous interconnected channels or pores of uneven diameter and (ii) fine particles of an active catalyst such as sulfides of cobalt, nickel, tungsten, and molybdenum dispersed within the pores. For example a heavy oil hydrocracking
15 catalyst manufactured by Criterion Catalyst, Criterion 317 trilube catalyst, has a bi-modal pore size distribution, with 80% of the pores ranging between 30 to 300 Angstroms with a peak at 100 Angstroms and 20% of the pores ranging between 1000 to 7000 Angstroms with a peak at 4000 Angstroms. The pores for the solid catalyst support are of limited size due to the need for the supported catalyst to maintain
20 mechanical integrity to prevent excessive breakdown and formation of excessive fines in the reactor. Supported catalysts are commonly produced as cylindrical pellets or spherical solids.

The term “hydrocracking reactor” shall refer to any vessel in which hydrocracking (*i.e.*, reducing the boiling range) of a feedstock in the presence of
25 hydrogen and a hydrocracking catalyst is the primary purpose. Hydrocracking reactors are characterized as having an input port into which a heavy oil feedstock and hydrogen can be introduced, an output port from which an upgraded feedstock or material can be withdrawn, and sufficient thermal energy so as to form hydrocarbon free radicals in order to cause fragmentation of larger hydrocarbon molecules into
30 smaller molecules. Methods and systems of the present invention employ a series of at least two gas-liquid two or more phase hydrocracking reactors (*i.e.*, a two-phase, gas-liquid system or a three-phase gas-liquid-solid system). In each case, the reactor

includes at least a gas phase and a liquid phase. Although preferred embodiments of the invention may include at least two gas-liquid hydrocracking reactors that do not include any solid supported catalyst phase, in alternative embodiments one or both of the at least two hydrocracking reactors may comprise three-phase gas-liquid-solid hydrocracking reactors comprising a solid supported catalyst. Other three-phase
5 embodiments may include coal particles as a solid phase, which may or may not include a solid supported catalyst phase. Examples of three-phase hydrocracking reactors include, but are not limited to, ebullated bed reactors (*i.e.*, a gas-liquid-ebullated solid bed system), and fixed bed reactors (*i.e.*, a three-phase system that
10 includes a liquid feed trickling downward over a fixed bed of solid supported catalyst with hydrogen gas typically flowing cocurrently, but possibly countercurrently in some cases). In either case, although it may be possible to operate the reactor systems with ebullated bed solid supported catalyst in addition to the colloidal and/or molecular catalyst, preferred systems may employ only the colloidal and/or molecular
15 catalyst.

The term “hydrocracking temperature” shall refer to a minimum temperature required to effect significant hydrocracking of a heavy oil feedstock. In general, hydrocracking temperatures will preferably fall within a range of about 410 °C (770 °F) to about 460 °C (860 °F), more preferably in a range of about 420 °C (788 °F) to
20 about 450 °C (842 °F), and most preferably in a range of about 430 °C (806 °F) to about 445 °C (833 °F). It will be appreciated that the temperature required to effect hydrocracking may vary depending on the properties and chemical make up of the heavy oil feedstock. Severity of hydrocracking may also be imparted by varying the space velocity of the feedstock, *i.e.*, the residence time of feedstock in the reactor,
25 while maintaining the reactor at a fixed temperature. Milder reactor temperature and longer feedstock space velocity are typically required for heavy oil feedstock with high reactivity and/or high concentration of asphaltenes.

The terms “gas-liquid two or more phase hydrocracking reactor” “hydrocracking reactor” and “gas-liquid two-phase hydrocracking reactor” shall refer
30 to a hydroprocessing reactor that includes a continuous liquid phase and a gaseous dispersed phase within the liquid phase. The liquid phase typically comprises a hydrocarbon feedstock that may contain a low concentration of a colloidal catalyst or

molecular-sized catalyst, and the gaseous phase typically comprises hydrogen gas, hydrogen sulfide, and vaporized low boiling point hydrocarbon products. The term “gas-liquid-solid, 3-phase hydrocracking reactor” or “gas-liquid-solid, 3-phase slurry hydrocracking reactor” may be used when a solid catalyst and/or solid coal particles
5 are included as a solid phase along with liquid and gas. The gas may contain hydrogen, hydrogen sulfide and vaporized low boiling hydrocarbon products. The terms “gas-liquid two or more phase hydrocracking reactor” “hydrocracking reactor” and “gas-liquid two-phase hydrocracking reactor” shall broadly refer to both type of reactors (e.g., those with a gas phase and a liquid phase including a colloidal or
10 molecular catalyst, and which may optionally include solid coal particles and/or employ a micron-sized or larger solid/particulate catalyst in addition to the colloidal or molecular catalyst), although preferred embodiments may be substantially free of any solid phase. An exemplary gas-liquid two phase reactor is disclosed in U.S. Patent No. 6,960,325 entitled “APPARATUS FOR HYDROCRACKING AND/OR
15 HYDROGENATING FOSSIL FUELS”.

The terms “upgrade”, “upgrading” and “upgraded”, when used to describe a feedstock that is being or has been subjected to hydroprocessing, or a resulting material or product, shall refer to one or more of a reduction in the molecular weight
20 of the feedstock, a reduction in the boiling point range of the feedstock, a reduction in the concentration of asphaltenes, a reduction in the concentration of hydrocarbon free radicals, and/or a reduction in the quantity of impurities, such as sulfur, nitrogen, oxygen, halides, and metals.

The colloidal and/or molecular catalyst is typically formed *in situ* within the
25 heavy oil feedstock prior to, or upon commencing, hydroprocessing of the feedstock. The oil soluble catalyst precursor comprises an organo-metallic compound or complex, which is advantageously blended with and thoroughly dispersed within the heavy oil feedstock in order to achieve a very high dispersion of the catalyst precursor within the feedstock prior to heating, decomposition, and formation of the final
30 catalyst. An exemplary catalyst precursor is a molybdenum 2-ethylhexanoate complex containing approximately 15% by weight molybdenum.

In order to ensure thorough mixing of the catalyst precursor within the heavy

oil feedstock, the catalyst precursor can be mixed into the heavy oil feedstock through a multi-step blending process. According to one such process, the oil soluble catalyst precursor is pre-blended with a hydrocarbon oil diluent (*e.g.*, vacuum gas oil, decant oil, cycle oil, or light gas oil) to create a diluted catalyst precursor, which is thereafter
5 blended with at least a portion of the heavy oil feedstock so as to form a mixture of the catalyst precursor and the heavy oil feedstock. This mixture is blended with any remaining heavy oil feedstock in such a way so as to result in the catalyst precursor being homogeneously dispersed down to the molecular level within the heavy oil feedstock. The blended feedstock composition may then be heated to decompose the
10 catalyst precursor, forming a colloidal or molecular catalyst within the heavy oil feedstock.

III. Exemplary HydroProcessing Systems and Methods

Figure 2 depicts an exemplary hydroprocessing system 10 according to the invention comprising a heavy oil feedstock 12 having a colloidal or molecular catalyst
15 dispersed therein, a first gas-liquid two-phase hydrocracking reactor 14 within which an upgraded feedstock or material is produced from the heavy oil feedstock, a separation step 16 (*e.g.*, an interstage pressure differential separator) by which upgraded feedstock or material withdrawn from first gas-liquid two-phase hydrocracking reactor 14 is separated into a lower boiling gaseous and volatile liquid
20 fraction 18 and a higher boiling less-volatile liquid fraction 19, and a second gas-liquid two-phase hydrocracking reactor 20 into which the higher boiling less-volatile liquid fraction 19 is introduced, resulting in additional production of upgraded material from second gas-liquid two-phase hydrocracking reactor 20. The heavy oil feedstock 12 may comprise any desired fossil fuel feedstock and/or fraction thereof
25 including, but not limited to, one or more of heavy crude, oil sands bitumen, bottom of the barrel fractions from crude oil, atmospheric tower bottoms, vacuum tower bottoms, coal tar, liquefied coal, and other resid fractions.

A common characteristic of heavy oil feedstocks 12 that may advantageously be upgraded using the hydroprocessing methods and systems (according to the
30 invention) is that they include a significant fraction of high boiling point hydrocarbons (*i.e.*, at or above 343 °C (650 °F), more particularly at or above about 524 °C (975 °F)) and/or asphaltenes. Asphaltenes are complex hydrocarbon

molecules that include a relatively low ratio of hydrogen to carbon that is the result of a substantial number of condensed aromatic and naphthenic rings with paraffinic side chains (*see* Figure 1). Sheets consisting of the condensed aromatic and naphthenic rings are held together by heteroatoms such as sulfur or nitrogen and/or polymethylene bridges, thio-ether bonds, and vanadium and nickel complexes. The asphaltene fraction also contains a higher content of sulfur and nitrogen than does crude oil or the rest of the vacuum resid, and it also contains higher concentrations of carbon-forming compounds (*i.e.*, that form coke precursors and sediment).

A significant characteristic of the gas-liquid two-phase hydrocracking reactors 14 and 20 within hydroprocessing system 10 according to the invention is that the heavy oil feedstock 12 introduced into the hydrocracking reactor 14 includes the colloidal or molecular catalyst and/or a well-dispersed catalyst precursor composition capable of forming the colloidal or molecular catalyst *in situ* within the feed heaters and/or the first gas-liquid two-phase hydrocracking reactor 14. Similarly, the higher boiling less-volatile liquid fraction 19 introduced into second gas-liquid two-phase hydrocracking reactor 20 includes the colloidal or molecular catalyst, as the catalyst becomes increasingly concentrated within the higher boiling liquid fraction 19 (*i.e.*, lower boiling volatile fraction 18 is free or substantially free of catalyst). The colloidal or molecular catalyst, the formation of which is discussed in more detail below, is preferably used alone (*i.e.*, without any conventional solid supported catalysts, for example, porous catalysts with active catalytic sites located within the pores).

Separation step 16 preferably comprises a pressure differential interstage separator which subjects the product stream to a pressure drop in order to separate a lower boiling volatile fraction from a higher boiling less-volatile fraction. Differences between a pressure differential interstage separator at separation step 16 within hydroprocessing system 10 according to the invention and separators used in conventional systems include the fact that a pressure differential interstage separator operates by subjecting the product stream to a significant pressure drop (*e.g.*, across a valve as the material enters the separator) so as to force a more significant fraction of the product stream to volatilize than would otherwise occur. In other words, there is a significant intentionally induced pressure drop, for example, at least about 100 psi. In

addition, the upgraded feedstock or material that is introduced into the separator includes residual colloidal or molecular catalyst dispersed therein as well as dissolved hydrogen. As a result, any hydrocarbon free radicals, including asphaltene free radicals, that are generated within the separator and/or which persist within the
5 upgraded feedstock as withdrawn from the gas-liquid two-phase hydrocracking reactor 14 can be further hydroprocessed in the separator, reducing coke and/or asphaltene formation and deposition.

More particularly, the colloidal or molecular catalyst within the upgraded feedstock or material transferred from first gas-liquid two-phase hydrocracking
10 reactor 14 to an interstage separator is able to catalyze beneficial upgrading or hydrotreating reactions between the hydrocarbon free radicals and hydrogen within the interstage separator. The result is a more stable upgraded feedstock, decreased sediment and coke precursor formation, and decreased fouling of the separator compared to hydroprocessing systems that do not employ a colloidal or molecular
15 catalyst (*e.g.*, conventional ebullated bed systems which require quenching of a separator with cooler oil in order to reduce the tendency of free radicals within the upgraded material to form coke precursors and sediment in a separator in the absence of any catalyst). Furthermore, the induced pressure drop also results in a moderate temperature drop, which further decreases or eliminates any need for quench oil, as
20 well as decreasing any tendency of free radicals to form coke precursors and sediment.

In addition, because the colloidal or molecular catalyst remains with the higher boiling liquid fraction 19 as separated by separation step 16, the catalyst is easily passed forward with fraction 19 to second gas-liquid two-phase reactor 20 for further
25 processing. By separating the lower boiling, more volatile fraction 18 (which is not introduced into second gas-liquid two-phase reactor 20), the volume of material to be treated within second gas-liquid two-phase reactor 20 is less than if no separation were performed. By employing an interstage separator which induces and subjects the effluent from first gas-liquid two-phase reactor 14 to a significant pressure drop,
30 the lower boiling more volatile fraction 18 also represents a greater percentage of the effluent from first gas-liquid two-phase reactor 14 than it otherwise would if a different type separator were used in which no pressure drop is applied. Increasing

the percentage of the effluent which is separated with lower boiling volatile fraction 18 likewise further decreases the volume of higher boiling liquid fraction 19 to be further reacted within second gas-liquid two-phase reactor 20. Furthermore, removal of low boiling point components from the stream prior to introduction into second
5 reactor 20 results in reduced gas hold up (*i.e.*, gases occupy less of the reactor volume, and the partial pressure and/or fraction of hydrogen gas as a fraction of total gas volume is increased).

Although described in a preferred embodiment as including an interstage pressure differential separator, separation step 16 may alternatively comprise the step
10 of removing a lower boiling gaseous/vapor fraction 18 from first gas-liquid two-phase reactor 14, without the use of any particular separation unit (*i.e.*, a gaseous vapor fraction present at the top of first gas-liquid two-phase reactor 14 may simply be drawn off separately from the liquid effluent from gas-liquid two-phase reactor 14). Of course, another alternative may include both removing a lower boiling
15 gaseous/vapor fraction 18 from first gas-liquid two-phase reactor 14, without the use of any particular separation unit, followed by introducing the remaining higher boiling effluent from reactor one into a pressure differential separator so as to flash off an additional fraction of the effluent before introducing the bottom fraction from the separator into a second two-phase hydrocracking reactor.

20 Figure 3 depicts an exemplary refining system 100 that incorporates an exemplary hydrocracking system according to the invention. The refining system 100 may itself comprise a module within an even more detailed and complex oil refinery system, including a module that is added to a pre-existing refinery system as part of an upgrade. The refining system 100 more particularly includes a distillation tower
25 102 into which an initial feed 104 comprising a significant fraction of higher boiling hydrocarbons is introduced. By way of example and not limitation, gases and/or lower boiling hydrocarbons 106 having a boiling point less than 370 °C (698 °F) are separated from a higher boiling liquid fraction 108 comprising materials having a boiling point greater than 370 °C (698 °F). In this embodiment, the higher boiling
30 liquid fraction 108 comprises a “heavy oil feedstock” within the meaning of this term.

An oil soluble catalyst precursor composition 110 is preblended with a hydrocarbon oil fraction or diluent 111, and mixed for a period of time in a pre-mixer

112 to form a diluted precursor mixture 113 in which the precursor composition 110 is well-mixed with the diluent 111. By way of example and not limitation, the pre-mixer 112 may be a multistage in-line low shear static mixer. Examples of suitable hydrocarbon diluents 111 include, but are not limited to, start up diesel (which typically has a boiling range of about 150 °C or higher), vacuum gas oil (which typically has a boiling range of 360-524 °C) (680-975 °F), decant oil or cycle oil (which typically has a boiling range of 360-550 °C) (680-1022 °F), and/or light gas oil (which typically has a boiling range of 200-360 °C) (392-680 °F). In some embodiments, it may be possible to dilute the catalyst precursor composition with a small portion of the heavy oil feedstock 108. Although the diluent may contain a substantial fraction of aromatic components, this is not required in order to keep the asphaltene fraction of the feedstock in solution, as the well dispersed catalyst is able to hydrocrack the asphaltenes within the heavy oil feedstock as well as the other components of the feedstock.

The catalyst precursor composition 110 is mixed with the hydrocarbon diluent 111 at a temperature below which a significant portion of the catalyst precursor composition 110 starts to decompose, *e.g.*, in a range of about 25 °C (77 °F) to about 300 °C (572 °F), most preferably in a range of about 75 °C (167 °F) to about 150 °C (302 °F), to form the diluted precursor mixture. It will be appreciated that the actual temperature at which the diluted precursor mixture is formed typically depends largely on the decomposition temperature of the particular precursor composition that is used.

It has been found that pre-blending the precursor composition 110 with a hydrocarbon diluent 111 prior to blending the diluted precursor mixture with the heavy oil feedstock 108 greatly aids in thoroughly and intimately blending the precursor composition 110 within feedstock 108, particularly in the relatively short period of time required for large-scale industrial operations to be economically viable. Forming a diluted precursor mixture advantageously shortens the overall mixing time by (1) reducing or eliminating differences in solubility between the more polar catalyst precursor 102 and the heavy oil feedstock 108; (2) reducing or eliminating differences in rheology between the catalyst precursor composition 102 and the heavy oil feedstock 108; and/or (3) breaking up bonds or associations between clusters of

catalyst precursor molecules to form a solute within hydrocarbon oil diluent 104 that is much more easily dispersed within the heavy oil feedstock 108.

For example, it is particularly advantageous to first form a diluted precursor mixture in the case where the heavy oil feedstock 108 contains water (*e.g.*, condensed water). Otherwise, the greater affinity of the water for the polar catalyst precursor composition 110 can cause localized agglomeration of the precursor composition 110, resulting in poor dispersion and formation of micron-sized or larger catalyst particles. The hydrocarbon oil diluent 111 is preferably substantially water free (*i.e.*, contains less than about 0.5% water) to prevent the formation of substantial quantities of micron-sized or larger catalyst particles.

The diluted precursor mixture 113 is then combined with heavy oil feedstock 108 and mixed for a time sufficient and in a manner so as to disperse the catalyst precursor composition throughout the feedstock in order to yield a blended feedstock composition in which the precursor composition is thoroughly mixed within the heavy oil feedstock. In the illustrated system, heavy oil feedstock 108 and the diluted catalyst precursor 113 are blended in a second multistage low shear, static in-line mixer 114.

Second in-line static mixer 114 is followed by further mixing within a dynamic, high shear mixer 115 (*e.g.*, a vessel with a propeller or turbine impeller for providing very turbulent, high shear mixing). Static in-line mixer 114 and dynamic high shear mixer 115 may be followed by a pump around in surge tank 116, and/or one or more multi-stage centrifugal pumps 117. According to one embodiment, continuous (as opposed to batch) mixing can be carried out using high energy pumps having multiple chambers within which the catalyst precursor composition and heavy oil feedstock are churned and mixed as part of the pumping process itself used to deliver a conditioned heavy oil feedstock 118 to the hydroprocessing reactor system.

Although illustrated with a specific arrangement of inline mixers 112, 114, and high shear mixer 115 it is to be understood that the illustrated example is simply a non-limiting exemplary mixing scheme for intimately mixing the catalyst precursor with the heavy oil feedstock. Modifications to the mixing process are possible. For example, in one embodiment, rather than mixing the diluted precursor mixture with all of heavy oil feedstock 108 at once, only a portion of heavy oil feedstock 108 may

initially be mixed with the diluted catalyst precursor. For example, the diluted catalyst precursor may be mixed with a fraction of the heavy oil feedstock, the resulting mixed heavy oil feedstock can be mixed in with another fraction of the heavy oil feedstock, and so on until all of the heavy oil feedstock has been mixed with the diluted catalyst precursor. Additional details regarding processes for intimately mixing the catalyst precursor with the heavy oil feedstock are described in United States Patent Application Serial No. 11/374,369 filed March 13, 2006 and entitled METHODS AND MIXING SYSTEMS FOR INTRODUCING CATALYST PRECURSOR INTO HEAVY OIL FEEDSTOCK.

10 The finally conditioned feedstock 118 is introduced into a pre-heater or furnace 120 so as to heat the finally conditioned feedstock 118 to a temperature that is about 100 °C (212 °F), preferably about 50 °C (122 °F) below the temperature in first gas-liquid two-phase hydrocracking reactor 122. The oil soluble catalyst precursor composition 110 dispersed throughout the feedstock 108 decomposes and combines
15 with sulfur released from the heavy oil feedstock 108 to yield a colloidal or molecular catalyst as the conditioned feedstock 118 travels through the pre-heater of furnace 120 and is heated to a temperature higher than the decomposition temperature of the catalyst precursor composition.

This yields a prepared feedstock 121, which is introduced under pressure into
20 first gas-liquid two-phase hydrocracking reactor 122. Hydrogen gas 124 is also introduced into first gas-liquid two-phase reactor 122 under pressure in order to effect hydrocracking of the prepared feedstock 121 within first gas-liquid two-phase reactor 122. Heavy oil resid bottoms 126 and/or recycle gas 128 produced downstream from first gas-liquid two-phase hydrocracking reactor 122 may optionally be recycled back
25 into first gas-liquid two-phase reactor 122 with prepared feedstock 121. Any recycled resid bottoms 126 advantageously includes a relatively high concentration of residual colloidal and/or molecular catalyst dispersed therein, as will be apparent from the present disclosure. The recycle gas 128 advantageously includes hydrogen.

The prepared feedstock 121 introduced into first gas-liquid two-phase
30 hydrocracking reactor 122 is heated to or maintained at a hydrocracking temperature, which causes the prepared feedstock 121, in combination with catalyst and hydrogen in first gas-liquid two-phase reactor 122, to be upgraded so as to form an upgraded

feedstock 130 that is withdrawn at the top of first gas-liquid two-phase reactor 122. According to one embodiment, the upgraded feedstock 130 is transferred directly to pressure differential interstage separator 132 through a valve 133, optionally together with at least a portion of the lower boiling point fraction 106 from the distillation tower 102 and/or recycle gas 128 produced downstream. Interstage separator 132 operates by subjecting the feed components 130 and optionally 106 and 128 to a pressure drop (*e.g.*, across valve 133 as the material enters separator 132) relative to the pressure at which first gas-liquid two-phase reactor 122 operates. For example, in one embodiment the first gas-liquid two-phase hydrocracking reactor may operate at a pressure between about 1500 psig and about 3500 psig, more preferably between about 2000 psig and about 2800 psig, and most preferably between about 2200 and about 2600 psig (*e.g.*, 2400 psig). Valve 133 and interstage separator 132 induce a significant pressure drop to the incoming feed. For example, the pressure drop may be in a range between about 100 psi and about 1000 psi, more preferably between about 200 psi and about 700 psi, and most preferably between about 300 psi and about 500 psi.

Lower boiling volatile gaseous vapor fraction 134 (*e.g.*, including H₂, C₁-C₇ hydrocarbons, and other lower boiling components depending on the degree of the pressure drop) is removed from the top of interstage separator 132 and sent downstream for further processing. A higher boiling liquid fraction 136 is withdrawn from the bottom of interstage separator 132. The higher boiling liquid fraction 136 withdrawn from the bottom of interstage separator 132 has a concentration of colloidally or molecularly dispersed catalyst which is significantly higher than the catalyst concentration within effluent 130 from first gas-liquid two-phase hydrocracking reactor 122. The catalyst concentration is similarly significantly higher than the catalyst concentration of prepared feedstock 121. This is because the catalyst is not held within lower boiling volatile phase 134 withdrawn from interstage separator 132; rather substantially all of the catalyst concentrates within higher boiling liquid fraction 136.

This is advantageous as higher boiling liquid fraction 136 may then be reacted within a second gas-liquid two-phase hydrocracking reactor 138 to increase the overall conversion level of the heavy oil feedstock. Such a system allows for a

reduction in volume of material to be treated within the second gas-liquid two-phase hydrocracking reactor, does not require any complex or expensive separation scheme to retrieve catalyst from high quality lower boiling volatile fraction 134, does not require the addition of new catalyst (which would be an added expense), and provides
5 increased catalyst concentration within the material introduced into second gas-liquid two-phase hydrocracking reactor 138, as well as increased asphaltene/lower quality components concentration, which increase reaction rate and conversion levels. In addition, second gas-liquid two-phase hydrocracking reactor 138 may be of a smaller volume than first gas-liquid two-phase hydrocracking reactor 122 as the volume of
10 material stream 136 to be treated is relatively smaller, and the concentration of colloidally or molecularly dispersed catalyst is increased relative to the catalyst concentration within stream 121 introduced into first gas-liquid two-phase reactor 122.

Because of the pressure drop induced at interstage separator 132 and valve
15 133, second gas-liquid two-phase reactor 138 may operate at a lower pressure than first gas-liquid two-phase reactor 122. For example, in one embodiment first gas-liquid two-phase reactor 122 may operate at about 2400 psig, while second gas-liquid two-phase reactor 138 may operate at about 2000 psig, the pressure differential being a result of the pressure drop across valve 133 at interstage separator 132. Of course,
20 the operating pressure of second reactor 138 may be raised by the addition of more hydrogen gas 125. For example, sufficient hydrogen gas 125 may be added under pressure to second reactor 138 so that both reactors 122 and 138 operate at approximately the same pressure.

Second gas-liquid two-phase hydrocracking reactor 138 is maintained at a
25 hydrocracking temperature, which causes higher boiling liquid fraction 136, in combination with catalyst and hydrogen 125 in second gas-liquid two-phase reactor 138, to be upgraded so as to form an upgraded feedstock 140 that is withdrawn at the top of second gas-liquid two-phase reactor 138. According to one embodiment, the upgraded feedstock 140 is combined with the lighter lower boiling volatile gaseous
30 vapor fraction 134 removed from interstage separator 132, which combined stream may then be introduced into a hot separator 127 to separate out any remaining high boiling fraction materials that may either be used as a residue 126 or recycled back

into one or both of hydrocracking gas-liquid two-phase reactors 122 and/or 138. Hot separator 127 induces no significant pressure drop (*e.g.*, not more than about 25 psi, more typically not more than about 10 psi). The residue 126 may also be used as a feedstock to provide gaseous product in a gasification reactor.

5 The catalyst concentration within the higher boiling bottoms liquid fraction introduced into the second gas-liquid two-phase hydrocracking reactor 138 typically will have a catalyst concentration that is between about 10 percent and about 100 percent higher than the concentration of the catalyst present within the effluent from the first gas-liquid two-phase hydrocracking reactor 122. More preferably, the
10 catalyst concentration within the higher boiling bottoms liquid fraction introduced into the second gas-liquid two-phase hydrocracking reactor 138 is between about 20 percent and about 50 percent (*e.g.*, at least about 25 percent higher) than the concentration of the catalyst present within the effluent from the first gas-liquid two-phase reactor 122, and most preferably the concentration within the higher boiling
15 bottoms liquid fraction introduced into the second hydrocracking reactor 138 is between about 25 percent and about 40 percent (*e.g.*, at least about 30 percent higher) than the concentration of the catalyst present within the effluent from the first reactor.

 Stated another way, preferably about 10 percent to about 50 percent of the material is flashed off within interstage separator 132, more preferably between about
20 15 percent and about 35 percent of the material is flashed off within interstage separator 132, and most preferably between about 20 percent and about 30 percent of the material is flashed off within interstage separator 132.

 Stream 129 (optionally with all or a portion of stream 106) may then be introduced into a mixed feed hydrotreater 142. The mixed feed hydrotreater 142
25 comprises one or more beds of solid supported catalyst 144 that effects hydrotreatment of the materials introduced therein. Mixed feed hydrotreater 142 is an example of a fixed bed reactor.

 The hydrotreated material 146 is withdrawn from the hydrotreater 142 and then subjected to one or more downstream separation or cleaning processes 148.
30 Recycle gas 128 comprising hydrogen may be recycled back into the gas-liquid two-phase reactors 122 and/or 138 and/or interstage separator 132 and/or hot separator 127, as desired. Hydrogen containing recycle gas 128 acts to reduce coke formation

and fouling within separators 132 and 127. Wash water and lean amine 150 may be used to wash the hydrotreated material 146 in order to yield a variety of products, including fuel gas 152, synthetic crude oil 154, rich amine 156, and sour water 158. The amine is used to remove H_2S . The wash water is used to dissolve ammonium salts which otherwise may form crystals that can become deposited on the equipment, thereby restricting fluid flow.

Figure 4 illustrates an alternative hydroprocessing system that may form part of a larger refining process (*e.g.*, similar to the overall process illustrated in Figure 3). For example, reactors 122 and 138, valve 133, interstage separator 132, and hot separator 127 of Figure 3 may be replaced with the alternative hydroprocessing system shown in Figure 4. As shown in Figure 4, prepared feedstock 121 is introduced under pressure into first gas-liquid two-phase hydrocracking reactor 122'. Hydrogen gas 124' is also introduced into first gas-liquid two-phase reactor 122' under pressure in order to effect hydrocracking of the prepared feedstock 121 within first gas-liquid two-phase reactor 122'. Heavy oil resid bottoms 126' and/or recycle gas 128' produced downstream from first gas-liquid two-phase hydrocracking reactor 122' may optionally be recycled back into first gas-liquid two-phase reactor 122'. Within the inventive systems, any recycled resid bottoms 126' advantageously includes an extremely elevated concentration of residual colloidal or molecular catalyst dispersed therein. The recycle gas 128' advantageously includes hydrogen.

The prepared feedstock 121 within first gas-liquid two-phase hydrocracking reactor 122' is heated or maintained at a hydrocracking temperature and pressure (*e.g.*, about 2000 psig), which causes or allows the prepared feedstock 121, in combination with catalyst and hydrogen in first gas-liquid two-phase reactor 122', to be upgraded so as to form an upgraded feedstock that is withdrawn at the top of first gas-liquid two-phase reactor 122' as a liquid fraction stream 130a' and a gaseous vapor fraction stream 130b'. For example, vapor stream 130b' may be withdrawn through a pipe or other outlet which collects material from a vapor pocket at the top of gas-liquid two-phase reactor 138' – as compared to withdrawal of stream 130a', which may be accomplished by submerging the outlet pipe into the liquid phase within reactor 122' located below the vapor pocket from which stream 130b' is drawn. Although it may be possible for stream 130b' to bypass separator 127' and combine it directly with

stream 129', this is discouraged as the separation between vapor stream 130b' and liquid stream 130a' can be difficult, particularly under the temperatures and pressures at which first gas-liquid two-phase reactor 122' operates. In other words, there will likely be at least a small fraction of higher boiling liquid component contamination within stream 130b', and introducing stream 130b' into separator 127' removes any such constituents back to residue stream 126'. As illustrated, the volatile gaseous vapor fraction stream 130b' is transferred directly to a separator (*e.g.*, hot high pressure separator 127'), while liquid fraction stream 130a' is introduced into second gas-liquid two-phase hydrocracking reactor 138'.

10 Similar to the embodiment illustrated within Figure 3, a lower boiling volatile portion of the effluent from the first gas-liquid two-phase hydrocracking reactor is separated from the upgraded feedstream before introducing the liquid fraction of the upgraded material into the second gas-liquid two-phase hydrocracking reactor. A principal difference between the embodiments illustrated in Figures 3 and 4 is that the embodiment illustrated in Figure 3 includes a pressure differential interstage separator and associated valve through which all of the upgraded feedstock 130 is fed so as to separate a lower boiling volatile fraction from a higher boiling bottoms fraction. Because a significant pressure differential is applied to the feed, the low boiling volatile fraction that is separated removes materials having higher boiling points than the separation as illustrated in Figure 4 (because no pressure differential is applied in the separation of streams 130a' and 130b' illustrated in Figure 4). In other words, the pressure differential as applied in the process of Figure 3 forces the most volatile liquid components (*i.e.*, having the lowest boiling points) that would otherwise remain in the liquid stream 130a' of Figure 4 to volatilize into the vapor stream within the process of Figure 3. All other things being equal, the process of Figure 3 results in a greater reduction in the volume of material being introduced into the second gas-liquid two-phase hydrocracking reactor 138 and a greater increase in concentration of the catalyst within the liquid feedstock being introduced into that reactor. As such, the process of Figure 3 may be preferred, although the process of Figure 4 still provides some of the benefits of the system of Figure 3, just to a smaller degree, likely at a lower cost, and in a way that may easily accommodate retrofitting to an existing reactor system.

The higher boiling liquid fraction 130a' withdrawn from first gas-liquid two-phase reactor 122' has a concentration of colloidally or molecularly dispersed catalyst which is significantly higher (*e.g.*, at least about 10 percent higher) than the catalyst concentration within prepared feedstock 121 fed to first gas-liquid two-phase reactor 122'. This is because the catalyst is not held within volatile phase 130b' withdrawn from first reactor 122' so that substantially all of the catalyst concentrates within higher boiling liquid fraction 130a'. Higher boiling liquid fraction 130a' may then be reacted within second gas-liquid two-phase hydrocracking reactor 138' to increase conversion levels of the heavy oil feedstock within the overall process.

Similar to the system module within Figure 3, the system module of Figure 4 provides a reduced volume of material to be treated within the second gas-liquid two-phase hydrocracking reactor (*i.e.*, stream 130a' is smaller than stream 121), does not require any complex or expensive separation scheme to retrieve catalyst from lower boiling volatile fraction 130a' (in this regard it is even simpler than the system of Figure 3), does not require the addition of fresh catalyst (which would be an added expense), and provides increased catalyst concentration within the material introduced into second gas-liquid two-phase hydrocracking reactor 138', which increases reaction rate and overall conversion levels relative to a system that does not include such a reaction system in which a volatile fraction is removed before introduction of the effluent from the first gas-liquid two-phase reactor into the second gas-liquid two-phase reactor.

Similar to the system of Figure 3, second gas-liquid two-phase hydrocracking reactor 138' may be of a smaller volume than first gas-liquid two-phase hydrocracking reactor 122' as the volume of material stream 130a' to be treated is relatively smaller, and the concentrations of both the asphaltene/lower quality components, as well as the colloidally or molecularly dispersed catalyst are increased relative to the concentrations within stream 121 introduced into first gas-liquid two-phase reactor 122'.

Second gas-liquid two-phase hydrocracking reactor 138' is maintained at a hydrocracking temperature and pressure (*e.g.*, about 2000 psig), which causes higher boiling liquid fraction 130a', in combination with catalyst and hydrogen 125' in second gas-liquid two-phase reactor 138', to be upgraded so as to form an upgraded

feedstock 140' that is withdrawn at the top of second gas-liquid two-phase reactor 138'. The upgraded feedstock 140' is fed with lower boiling volatile gaseous vapor stream 130b' into hot high pressure separator 127' to separate out any remaining high boiling fraction materials that may either be used as a residue 126' or recycled back
5 into one or both hydrocracking gas-liquid two-phase reactors 122' and 138'. The residue 126' may also be used as a feedstock to provide gaseous product in a gasification reactor.

The overhead lower boiling volatile fraction 129' from hot high pressure separator 127' may then be introduced downstream for additional hydrotreating (*e.g.*,
10 fed into a mixed feed hydrotreater for further downstream treatment, for example as shown in Figure 3). Separator 127' operates without inducing any significant pressure drop (*e.g.*, not more than about 25 psi, more typically not more than about 10 psi). The embodiment illustrated in Figure 4 may be particularly advantageous in retrofitting an existing reactor system (*e.g.*, a three-phase ebullated bed reactor
15 system), as the vapor products may be withdrawn from first hydrocracking reactor 122', reducing gas hold up within both the first and second reactors. Such a retrofit to an existing reactor system allows for higher liquid flow rates or higher overall conversion levels to be achieved with a minimum of capital investment.

Figure 5 illustrates another exemplary hydrocracking system that may form
20 part of a larger refining process (*e.g.*, similar to the overall process illustrated in Figure 3). The system of Figure 5 is similar to that shown in Figure 4, except that the higher boiling effluent from the first two-phase hydrocracking reactor is fed through a valve 133 and interstage separator 132, effectively combining features from the systems of both Figure 3 and Figure 4. Similar to in Figure 4, prepared feedstock 121
25 is introduced under pressure into first gas-liquid two-phase hydrocracking reactor 122'. Hydrogen gas 124' is also introduced into first gas-liquid two-phase reactor 122' under pressure in order to effect hydrocracking of the prepared feedstock 121 within first gas-liquid two-phase reactor 122'. Heavy oil resid bottoms 126' and/or recycle gas 128' produced downstream from first gas-liquid two-phase hydrocracking reactor
30 122' may optionally be recycled back into first gas-liquid two-phase reactor 122'.

The higher boiling liquid fraction 130a' withdrawn from first gas-liquid two-phase reactor 122' has a concentration of colloidally or molecularly dispersed catalyst

which is significantly higher (*e.g.*, at least about 10 percent higher) than the catalyst concentration within prepared feedstock 121 fed to first gas-liquid two-phase reactor 122'. Higher boiling liquid fraction 130a' may then be introduced into pressure differential separator 132 through valve 133. A pressure drop is induced across valve 133, causing a separation between lower boiling volatile gaseous vapor fraction 131b' and a higher boiling liquid fraction 131a'. The higher boiling liquid fraction 131a' withdrawn from the bottom of interstage separator 132 has a concentration of colloidally or molecularly dispersed catalyst which is significantly higher than the catalyst concentration within effluent 130a' and prepared feedstock 121. Higher boiling liquid fraction 131a' is reacted within second gas-liquid two-phase hydrocracking reactor 138' to increase conversion levels of the heavy oil feedstock within the overall process. An upgraded feedstock 140' is withdrawn at the top of second gas-liquid two-phase reactor 138'. The upgraded feedstock 140' is fed with lower boiling volatile gaseous vapor stream 130b' and stream 131b' into hot high pressure separator 127' to separate out any remaining high boiling fraction materials that may either be used as a residue 126' or recycled back into one or both hydrocracking gas-liquid two-phase reactors 122' and 138'. The first and second hydrocracking gas-liquid two-phase reactors of Figures 3 through 5 and may contain a recycle channel, recycling pump, and distributor grid plate as in a conventional ebullated bed reactor to promote more even dispersion of reactants, catalyst, and heat (*e.g.*, in a manner similar to conventional ebullated bed reactors).

IV. Preparation and Characteristics of Colloidal/Molecular Catalyst

After the catalyst precursor composition has been well-mixed throughout the heavy oil feedstock so as to yield the blended feedstock composition, this composition is then heated to above the temperature where significant decomposition of the catalyst precursor composition occurs in order to liberate the catalyst metal therefrom so as to form the final active catalyst. According to one embodiment, the metal from the precursor composition is believed to first form a metal oxide, which then reacts with sulfur liberated from the heavy oil feedstock to yield a metal sulfide compound that is the final active catalyst. In the case where the heavy oil feedstock includes sufficient or excess sulfur, the final activated catalyst may be formed *in situ* by heating the conditioned heavy oil feedstock to a temperature sufficient to liberate the

sulfur therefrom. In some cases, sulfur may be liberated at the same temperature that the precursor composition decomposes. In other cases, further heating to a higher temperature may be required.

The oil soluble catalyst precursor preferably has a decomposition temperature
5 in a range from about 100 °C (212 °F) to about 350 °C (662 °F), more preferably in a range of about 150 °C (302 °F) to about 300 °C (572 °F), and most preferably in a range of about 175 °C (347 °F) to about 250 °C (482 °F). Examples of exemplary catalyst precursor compositions include organometallic complexes or compounds, more specifically, oil soluble compounds or complexes of transition metals and
10 organic acids. A currently preferred catalyst precursor is molybdenum 2-ethylhexanoate (also commonly known as molybdenum octoate) containing 15% by weight molybdenum and having a decomposition temperature or range high enough to avoid substantial decomposition when mixed with a heavy oil feedstock at a temperature below about 250 °C (482 °F). Other exemplary precursor compositions
15 include, but are not limited to, molybdenum naphthanate, vanadium naphthanate, vanadium octoate, molybdenum hexacarbonyl, vanadium hexacarbonyl, and iron pentacarbonyl.

The colloidal or molecular catalyst generally never becomes deactivated because it is not contained within the pores of a support material. Moreover, because
20 of intimate contact with the heavy oil molecules, the molecular catalyst and/or colloidal catalyst particles can rapidly catalyze a hydrogenation reaction between hydrogen atoms and free radicals formed from the heavy oil molecules. Although the molecular or colloidal catalyst leaves the hydroprocessing reactor with the liquid fraction of upgraded product effluent, it is constantly being replaced with fresh
25 catalyst contained in the incoming feedstock and/or recycled residue in which the catalyst has become highly concentrated. As a result, process conditions, throughput and conversion levels remain significantly more constant over time compared to processes that employ solid supported catalysts as the sole hydroprocessing catalyst. Moreover, because the colloidal or molecular catalyst is more freely dispersed
30 throughout the feedstock, including being intimately associated with asphaltenes, conversion levels and throughput can be significantly or substantially increased compared to conventional hydroprocessing systems.

The uniformly dispersed colloidal and/or molecular catalyst is also able to more evenly distribute the catalytic reaction sites throughout the reaction chamber and feedstock material. This reduces the tendency for free radicals to react with one another to form coke precursor molecules and sediment compared to ebullated bed
5 reactors that only use a relatively large (*e.g.*, 1/4" x 1/8" or 1/4" x 1/16") (6.35 mm x 3.175 mm or 6.35 mm x 1.5875 mm) supported catalyst, wherein the heavy oil molecules must diffuse into the pores of the catalyst support to reach the active catalyst sites. As will be apparent to one skilled in the art, a typical ebullated bed reactor inherently has catalyst free zones at the reactor bottom (plenum) and from
10 above the expanded catalyst level to the recycle cup. In these catalyst free zones the heavy oil molecules continue undergoing thermal cracking reactions so as to form free radicals that may react with one another to produce coke precursor molecules and sediment.

The benefits resulting from the use of the colloidal and/or molecular catalyst
15 and its concentration within the higher boiling effluent fraction and the residue within the inventive processing systems include increased hydrogen transfer to cracked hydrocarbon molecules enabling higher conversion levels and throughput, reduced volume of material requiring treatment within second gas-liquid two-phase reactor 138 or 138' relative to the volume of material treated within first gas-liquid two-phase
20 reactor 122 or 122', and more efficient use of catalyst (the same catalyst is used sequentially within both the first gas-liquid two-phase reactor (*i.e.*, reactor 122 or 122' and the second gas-liquid two-phase reactor (*i.e.*, reactor 138 or 138')).

If the oil soluble catalyst precursor is thoroughly mixed throughout the heavy oil feedstock, at least a substantial portion of the liberated metal ions will be
25 sufficiently sheltered or shielded from other metal ions so that they can form a molecularly-dispersed catalyst upon reacting with sulfur to form the metal sulfide compound. Under some circumstances, minor agglomeration may occur, yielding colloidal-sized catalyst particles. Simply mixing, while failing to sufficiently blend, the catalyst precursor composition with the feedstock typically causes formation of
30 large agglomerated metal sulfide compounds that are micron-sized or larger. However, it is believed that taking care to thoroughly mix the precursor composition throughout the feedstock (*e.g.*, with premixing processes as described above in

conjunction with Figure 3) will yield individual catalyst molecules rather than colloidal particles. In addition, it is believed that the molecularly dispersed catalyst remains molecularly dispersed when concentrated within the higher boiling liquid effluent fraction and residue 126, allowing this material to be further hydrocracked
5 without requiring any additional process to intimately disperse the catalyst within the material.

In order to form the metal sulfide catalyst, the blended feedstock composition is preferably heated to a temperature in a range of about 200 °C (392 °F) to about 500 °C (932 °F), more preferably in a range of about 250 °C (482 °F) to about 450 °C
10 (842 °F), and most preferably in a range of about 300 °C (572 °F) to about 400 °C (752 °F). According to one embodiment, the conditioned feedstock is heated to a temperature that is about 100 °C (212 °F) less than the hydrocracking temperature within the hydrocracking reactor, preferably about 50 °C (122 °F) less than the hydrocracking temperature. According to one embodiment, the colloidal or molecular
15 catalyst is formed during preheating before the heavy oil feedstock is introduced into the hydrocracking reactor. According to another embodiment, at least a portion of the colloidal or molecular catalyst is formed *in situ* within the hydrocracking reactor itself. In some cases, the colloidal or molecular catalyst can be formed as the heavy oil feedstock is heated to a hydrocracking temperature prior to or after the heavy oil
20 feedstock is introduced into a gas-liquid two-phase hydrocracking reactor. The initial concentration of the catalyst metal in the colloidal or molecular catalyst is preferably in a range of about 5 parts per million (ppm) to about 500 ppm by weight of the heavy oil feedstock, more preferably in a range of about 15 ppm to about 300 ppm, and most preferably in a range of about 25 ppm to about 175 ppm. As described above, the
25 catalyst becomes more concentrated as volatile fractions are removed from a higher boiling liquid bottoms fraction.

Notwithstanding the generally hydrophobic nature of heavy oil feedstocks, because asphaltene molecules generally have a large number of oxygen, sulfur and nitrogen functional groups, as well as associated metal constituents such as nickel and
30 vanadium, the asphaltene fraction is significantly less hydrophobic and more hydrophilic than other hydrocarbons within the feedstock. Asphaltene molecules therefore generally have a greater affinity for the polar metal sulfide catalyst,

particularly when in a colloidal or molecular state, compared to more hydrophobic hydrocarbons in a heavy oil feedstock. As a result, a significant portion of the polar metal sulfide molecules or colloidal particles tend to become associated with the more hydrophilic and less hydrophobic asphaltene molecules compared to the more hydrophobic hydrocarbons in the feedstock. The close proximity of the catalyst particles or molecules to the asphaltene molecules helps promote beneficial upgrading reactions involving free radicals formed through thermal cracking of the asphaltene fraction. This phenomenon is particularly beneficial in the case of heavy oils that have a relatively high asphaltene content, which are otherwise difficult, if not impossible, to upgrade using conventional hydroprocessing techniques due to the tendency of asphaltenes to deactivate porous supported catalysts and deposit coke and sediments on or within the processing equipment. Figure 6 schematically depicts catalyst molecules, or colloidal particles "X" associated with, or in close proximity to, the asphaltene molecules.

While the highly polar nature of the catalyst compound causes or allows the colloidal and/or molecular catalyst to associate with asphaltene molecules, it is the general incompatibility between the highly polar catalyst compound and the hydrophobic heavy oil feedstock that necessitates the aforementioned intimate or thorough mixing of the oil soluble catalyst precursor composition within the heavy oil feedstock prior to decomposition of the precursor and formation of the colloidal or molecular catalyst. Because metal catalyst compounds are highly polar, they cannot be effectively dispersed within a heavy oil feedstock in colloidal or molecular form if added directly thereto or as part of an aqueous solution or an oil and water emulsion. Such methods inevitably yield micron-sized or larger catalyst particles.

Reference is now made to Figures 7A and 7B, which schematically depict a nanometer-sized molybdenum disulfide crystal. Figure 7A is a top view, and Figure 7B is a side view of a molybdenum disulfide crystal. Molecules of molybdenum disulfide typically form flat, hexagonal crystals in which single layers of molybdenum (Mo) atoms are sandwiched between layers of sulfur (S) atoms. The only active sites for catalysis are on the crystal edges where the molybdenum atoms are exposed. Smaller crystals have a higher percentage of molybdenum atoms exposed at the edges.

The diameter of a molybdenum atom is approximately 0.3 nm, and the diameter of a sulfur atom is approximately 0.2 nm. The illustrated nanometer-sized crystal of molybdenum disulfide has 7 molybdenum atoms sandwiched in between 14 sulfur atoms. As best seen in Figure 7A, 6 out of 7 (85.7%) of the total molybdenum atoms will be exposed at the edge and available for catalytic activity. In contrast, a micron-sized crystal of molybdenum disulfide has several million atoms, with only about 0.2% of the total molybdenum atoms being exposed at the crystal edge and available for catalytic activity. The remaining 99.8% of the molybdenum atoms in the micron-sized crystal are embedded within the crystal interior and are therefore unavailable for catalysis. This means that nanometer-sized molybdenum disulfide particles are, at least in theory, orders of magnitude more efficient than micron-sized particles in providing active catalyst sites.

In practical terms, forming smaller catalyst particles results in more catalyst particles and more evenly distributed catalyst sites throughout the feedstock. Simple mathematics dictates that forming nanometer-sized particles instead of micron-sized particles will result in approximately 1000^3 (*i.e.*, 1 million) to 1000^6 (*i.e.*, 1 billion) times more particles depending on the size and shape of the catalyst crystals. That means there are approximately 1 million to 1 billion times more points or locations within the feedstock where active catalyst sites reside. Moreover, nanometer-sized or smaller molybdenum disulfide particles are believed to become intimately associated with asphaltene molecules, as shown in Figure 6. In contrast, micron-sized or larger catalyst particles are believed to be far too large to become intimately associated with or within asphaltene molecules. For at least these reasons, the distinct advantages associated with the mixing method and system that provides for formation of a colloidal and/or molecular catalyst will be apparent to one skilled in the art.

V. Examples

The following examples more particularly illustrate exemplary hydrocracking systems in which the upgraded effluent material from a first gas-liquid two-phase hydrocracking reactor is separated into a lower boiling volatile gaseous vapor fraction and a higher boiling liquid fraction before introducing the higher boiling liquid fraction into a second gas-liquid two-phase hydrocracking reactor, which causes the catalyst to concentrate within the liquid fraction in preparation for further

hydroprocessing of this fraction. All percentages are mole percent unless specified otherwise.

Comparative Example A

The effectiveness of the inventive hydroprocessing reactor system designs
5 were compared. The baseline comparison reactor system design is similar to that shown in Figure 4, except that all effluent from first reactor 122' is fed into second reactor 138' (i.e., no flow in stream 130b'). A heavy oil feedstock comprising 75 ppm of a molybdenum disulfide catalyst in colloidal or molecular form is introduced into a first gas-liquid two-phase reactor having dimensions of about 5.0 m OD and a
10 capacity of about 30,000 barrels per stream day (BPSD).

Example 1

A reactor system design similar to that shown in Figure 4 is evaluated. A heavy oil feedstock comprising about 75 ppm of a molybdenum disulfide catalyst in colloidal or molecular form is introduced into a first gas-liquid two-phase reactor
15 having dimensions of about 5.0 m OD and a capacity of about 30,000 barrels per stream day (BPSD). Effluent from second two-phase reactor 138' includes smaller fractions of lower boiling components, including less C₁ to C₄ hydrocarbons and H₂S relative to Comparative Example A. The catalyst concentration within stream 130a' is greater than the catalyst concentration exiting the first reactor of Comparative
20 Example A (e.g., at least about 10 percent higher). Within second reactor 138', there are less gaseous products, less required H₂ flow, less gas hold up (because a larger fraction of the material within the reactor are liquid components requiring hydrocracking), and higher catalyst concentration relative to the composition within the second reactor of Comparative Example A. In addition, second reactor 138' may
25 be smaller than in Comparative Example A, or alternatively, the system may be designed with the same reactor volume and increased conversion (i.e., lower fraction of unconverted asphaltene/resid material exiting from second reactor 138') as compared to Comparative Example A.

Example 2

30 A reactor system design similar to that shown in Figure 5 is evaluated. A heavy oil feedstock comprising about 75 ppm of a molybdenum disulfide catalyst in colloidal or molecular form is introduced into a first gas-liquid two-phase reactor

having dimensions of about 5.0 m OD and a capacity of about 30,000 barrels per stream day (BPSD). Stream 131a' introduced into second two-phase reactor 138' is much greater than the initial concentration of 75 ppm (*e.g.*, about 25 percent to about 40 percent higher). Effluent from second two-phase reactor 138' includes smaller
5 fractions of lower boiling components, including less C₁ to C₄ hydrocarbons and less H₂S relative to Comparative Example A and Example 1. Within second reactor 138', there are less gaseous products, less required H₂ flow, less gas hold up (because a larger fraction of the material within the reactor are liquid components requiring hydrocracking), and higher catalyst concentration relative to the compositions within
10 the second reactors of Comparative Example A and Example 1. In addition, second reactor 138' may be smaller than the second reactors in Comparative Example A and Example 1. Alternatively, the system may be designed with the same reactor volume and increased conversion (*i.e.*, lower fraction of unconverted asphaltene/resid material exiting from second reactor 138') as compared to Comparative Example A and
15 Example 1. The pressure of stream 130b' is significantly greater (*e.g.*, 100 to 1000 psi greater, for example 400 psi greater) than stream 131b', which is may be slightly greater (*e.g.*, less than 25 psi greater, more typically less than 10 psi greater) than the pressure of stream 129'.

Example 3

20 A reactor system design similar to that shown in Figure 3 is evaluated. A heavy oil feedstock comprising about 75 ppm of a molybdenum disulfide catalyst in colloidal or molecular form is introduced into a first gas-liquid two-phase reactor having dimensions of about 5.0 m OD and a capacity of about 30,000 barrels per stream day (BPSD). Stream 136 introduced into second two-phase reactor 138 is
25 much greater than the initial concentration of 75 ppm (*e.g.*, at least about 20 percent higher). Effluent 140 from second two-phase reactor 138 includes smaller fractions of lower boiling components, including less C₁ to C₄ hydrocarbons and less H₂S relative to Comparative Example A and Example 1. Within second reactor 138, there are less gaseous products, less required H₂ flow, less gas hold up (because a larger
30 fraction of the material within the reactor are liquid components requiring hydrocracking), and higher catalyst concentration relative to the compositions within the second reactors of Comparative Example A and Example 1. In addition, second

69767-47

37

reactor 138 may be smaller than the second reactors in Comparative Example A and Example 1. Alternatively, the system may be designed with the same reactor volume and increased conversion (*i.e.*, lower fraction of unconverted asphaltene/resid material 140 exiting from second reactor 138) as compared to Comparative Example A and
5 Example 1. The pressure of stream 134 is significantly (*e.g.*, about 400 psi greater) greater than streams 140 and 129.

The present invention may be embodied in other specific forms without departing from its scope. The described embodiments are to be considered in all respects only as illustrative and not restrictive. The scope of the invention is, therefore,
10 indicated by the appended claims rather than by the foregoing description. All changes which come within the meaning and range of equivalency of the claims are to be embraced within their scope.

69767-47

38

CLAIMS:

1. A method of hydrocracking a heavy oil feedstock using a colloiddally or molecularly dispersed catalyst comprising:

5 introducing a heavy oil feedstock including a colloiddally or molecularly dispersed catalyst or catalyst precursor into a first gas-liquid two or more phase hydrocracking reactor, said first gas-liquid two or more phase hydrocracking reactor having a first concentration of colloiddally or molecularly dispersed catalyst and producing an effluent;

10 separating, using a pressure differential interstage separator which induces a pressure drop of at least 100 psi, said effluent produced from said first hydrocracking reactor into a lower boiling volatile gaseous vapor fraction and a higher boiling liquid fraction;

15 introducing at least a portion of said higher boiling liquid fraction into a second gas-liquid two or more hydrocracking reactor, wherein said higher boiling liquid fraction has a second concentration of colloiddally or molecularly dispersed catalyst that is greater than the first concentration of colloiddally or molecularly dispersed catalyst within said first hydrocracking reactor.

2. A method as recited in claim 1, wherein substantially all of said higher boiling liquid fraction is introduced into said second hydrocracking reactor.

3. A method as recited in claim 1, further comprising:

20 introducing an effluent from said second hydrocracking reactor into a second interstage pressure differential separator which induces a second pressure drop so as to separate a second lower boiling volatile gaseous vapor fraction from a second higher boiling liquid fraction; and

25 introducing at least a portion of said second higher boiling liquid fraction into a third gas-liquid two or more phase hydrocracking reactor and wherein said second higher boiling liquid fraction has a third concentration of colloiddally or molecularly dispersed

69767-47

39

catalyst that is greater than said second concentration of colloidally or molecularly dispersed catalyst within said second hydrocracking reactor.

4. A method as recited in claim 1, wherein the pressure drop is between 100 psi to 1000 psi.
- 5 5. A method as recited in claim 1, wherein the pressure drop is between 200 psi to 700 psi.
6. A method as recited in claim 1, wherein the pressure drop is between 300 psi to 500 psi.
7. A method as recited in claim 1, wherein said colloidally or molecularly
10 dispersed catalyst comprises molybdenum sulfide and wherein said molybdenum sulfide has a concentration within said higher boiling liquid fraction introduced into said second hydrocracking reactor that is at least 10 percent higher than a molybdenum sulfide catalyst concentration within said first hydrocracking reactor.
8. A method as recited in claim 1, wherein said colloidally or molecularly
15 dispersed catalyst comprises molybdenum sulfide and wherein said molybdenum sulfide has a concentration within said higher boiling liquid fraction introduced into said second hydrocracking reactor that is at least 25 percent higher than a molybdenum sulfide catalyst concentration within said first hydrocracking reactor.
9. A method as recited in claim 1, wherein said colloidally or molecularly
20 dispersed catalyst comprises molybdenum sulfide and wherein said molybdenum sulfide has a concentration within said higher boiling liquid fraction introduced into said second hydrocracking reactor that is at least 30 percent higher than a molybdenum sulfide catalyst concentration within said first hydrocracking reactor.
10. A system for hydrocracking heavy oil using a colloidally or molecularly
25 dispersed catalyst comprising:

69767-47

40

a series of gas-liquid two or more phase hydrocracking reactors including at least a first gas-liquid two or more phase hydrocracking reactor operating at a first pressure and a second gas-liquid two or more phase hydrocracking reactor operating at a second pressure, said first hydrocracking reactor having a first concentration of colloiddally or
5 molecularly dispersed catalyst; and

a pressure differential interstage separator disposed between said first hydrocracking reactor and said second hydrocracking reactor, said interstage separator receiving an effluent from said first hydrocracking reactor at said first pressure and providing a pressure drop of at least 100 psi so as to separate a lower boiling volatile gaseous vapor
10 fraction from a higher boiling bottoms liquid fraction, at least a portion of said higher boiling bottoms liquid fraction being introduced into said second hydrocracking reactor and wherein said higher boiling bottoms liquid fraction has a second concentration of colloiddally or molecularly dispersed catalyst that is greater than the first concentration of colloiddally or molecularly dispersed catalyst within said first hydrocracking reactor.

11. A system as recited in claim 10, wherein said colloiddally or molecularly dispersed catalyst comprises molybdenum sulfide and wherein said molybdenum sulfide has a concentration within said higher boiling liquid fraction introduced into said second hydrocracking reactor that is at least 10 percent higher than a molybdenum sulfide catalyst concentration within said first hydrocracking reactor.

12. A system as recited in claim 10, wherein said colloiddally or molecularly dispersed catalyst comprises molybdenum sulfide and wherein said molybdenum sulfide has a concentration within said higher boiling liquid fraction introduced into said second hydrocracking reactor that is at least 25 percent higher than a molybdenum sulfide catalyst concentration within said first hydrocracking reactor.

13. A system as recited in claim 10, wherein said colloiddally or molecularly dispersed catalyst comprises molybdenum sulfide and wherein said molybdenum sulfide has a concentration within said higher boiling liquid fraction introduced into said second

69767-47

41

hydrocracking reactor that is at least 30 percent higher than a molybdenum sulfide catalyst concentration within said first hydrocracking reactor.

14. A system as recited in claim 10, wherein said series of gas-liquid two or more phase hydrocracking reactors further comprises:

5 a third gas-liquid two or more phase hydrocracking reactor operating at a third pressure; and

a second interstage separator disposed between said second hydrocracking reactor and said third hydrocracking reactor, said second interstage separator receiving an effluent from said second hydrocracking reactor at said second pressure and providing a
10 pressure drop so as to separate a second interstage separator lower boiling volatile gaseous vapor fraction from a second interstage separator higher boiling bottoms liquid fraction, at least a portion of said second interstage separator higher boiling bottoms liquid fraction being introduced into said third hydrocracking reactor and wherein said second interstage separator higher boiling bottoms liquid fraction has a third concentration of colloiddally or molecularly
15 dispersed catalyst that is greater than said second concentration of colloiddally or molecularly dispersed catalyst within said second hydrocracking reactor.

15. A system as recited in claim 10, wherein the first pressure is between 100 psi and 1000 psi higher than the second pressure.

16. A system as recited in claim 10, wherein the first pressure is between 200 psi
20 and 700 psi higher than the second pressure.

17. A system as recited in claim 10, wherein the first pressure is between 300 psi and 500 psi higher than the second pressure.

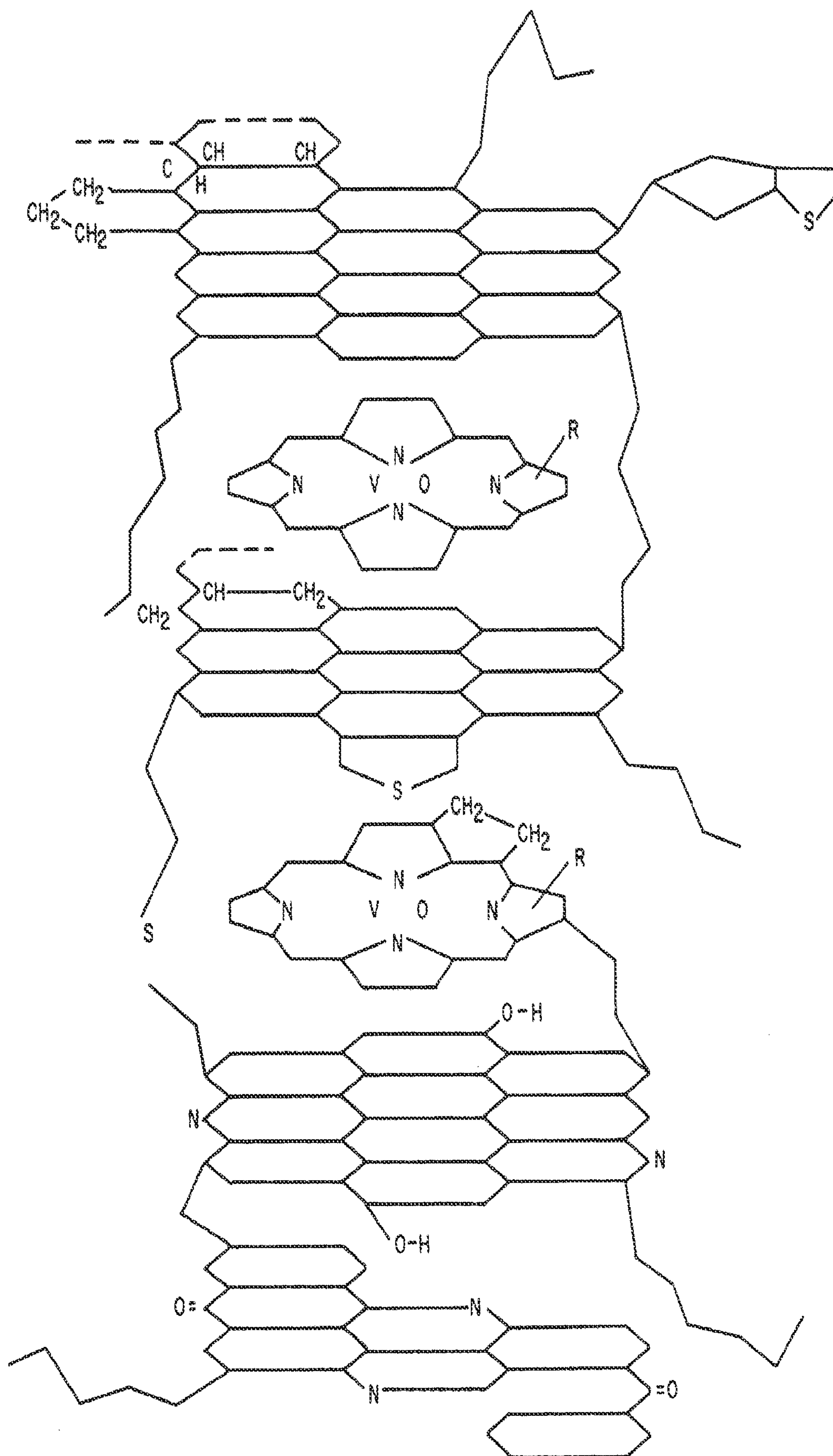


Fig. 1

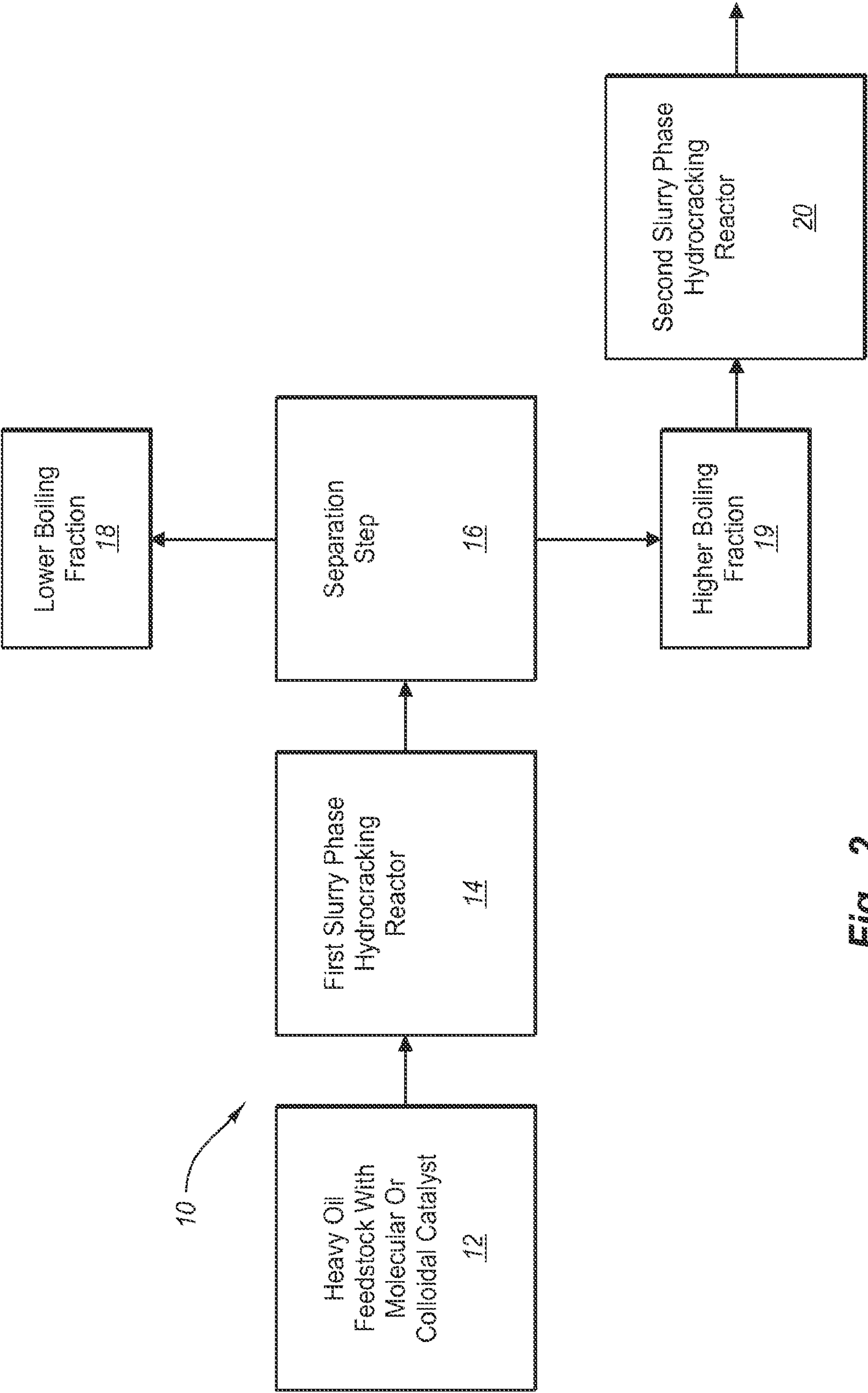
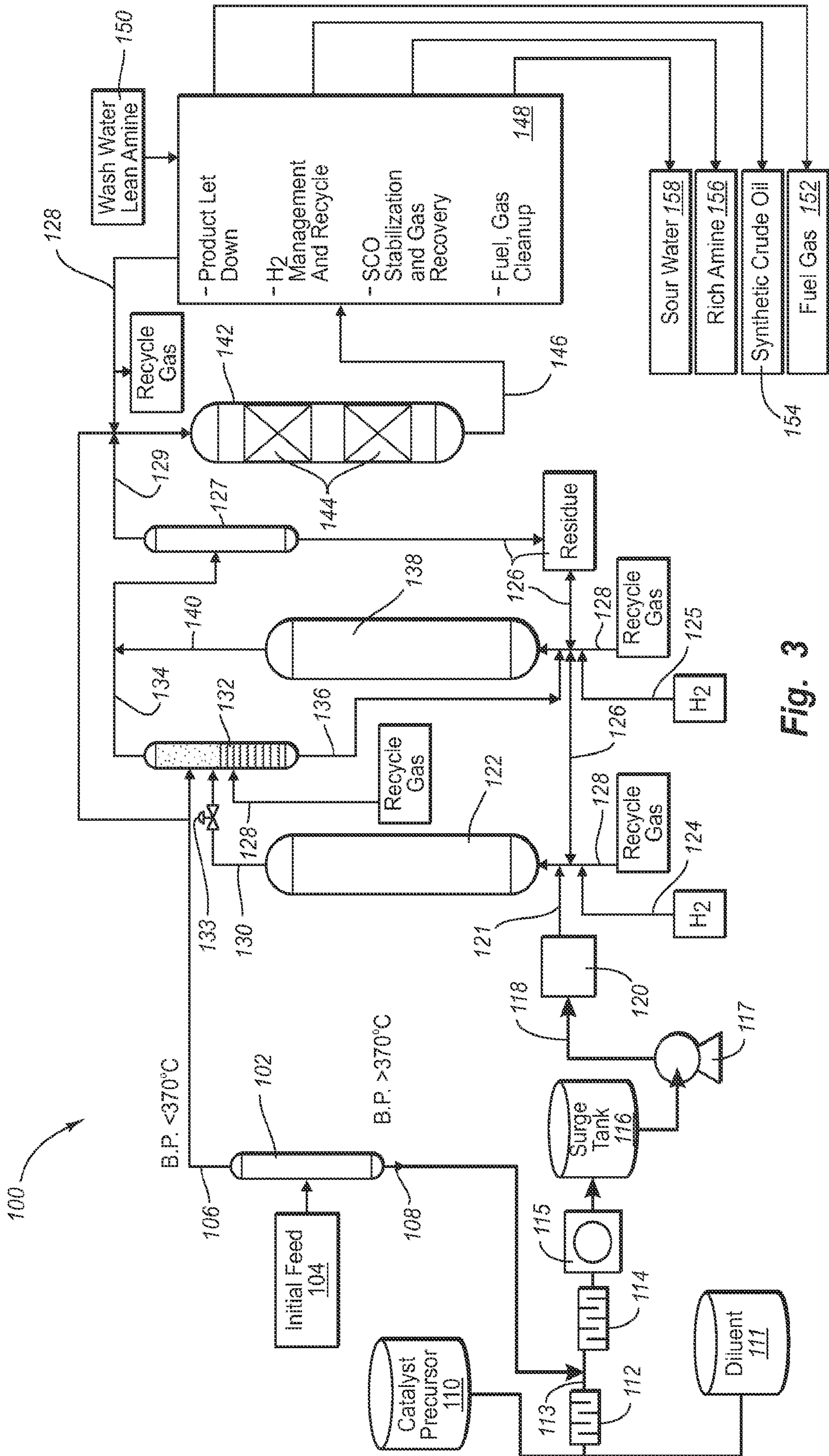


Fig. 2

3/7



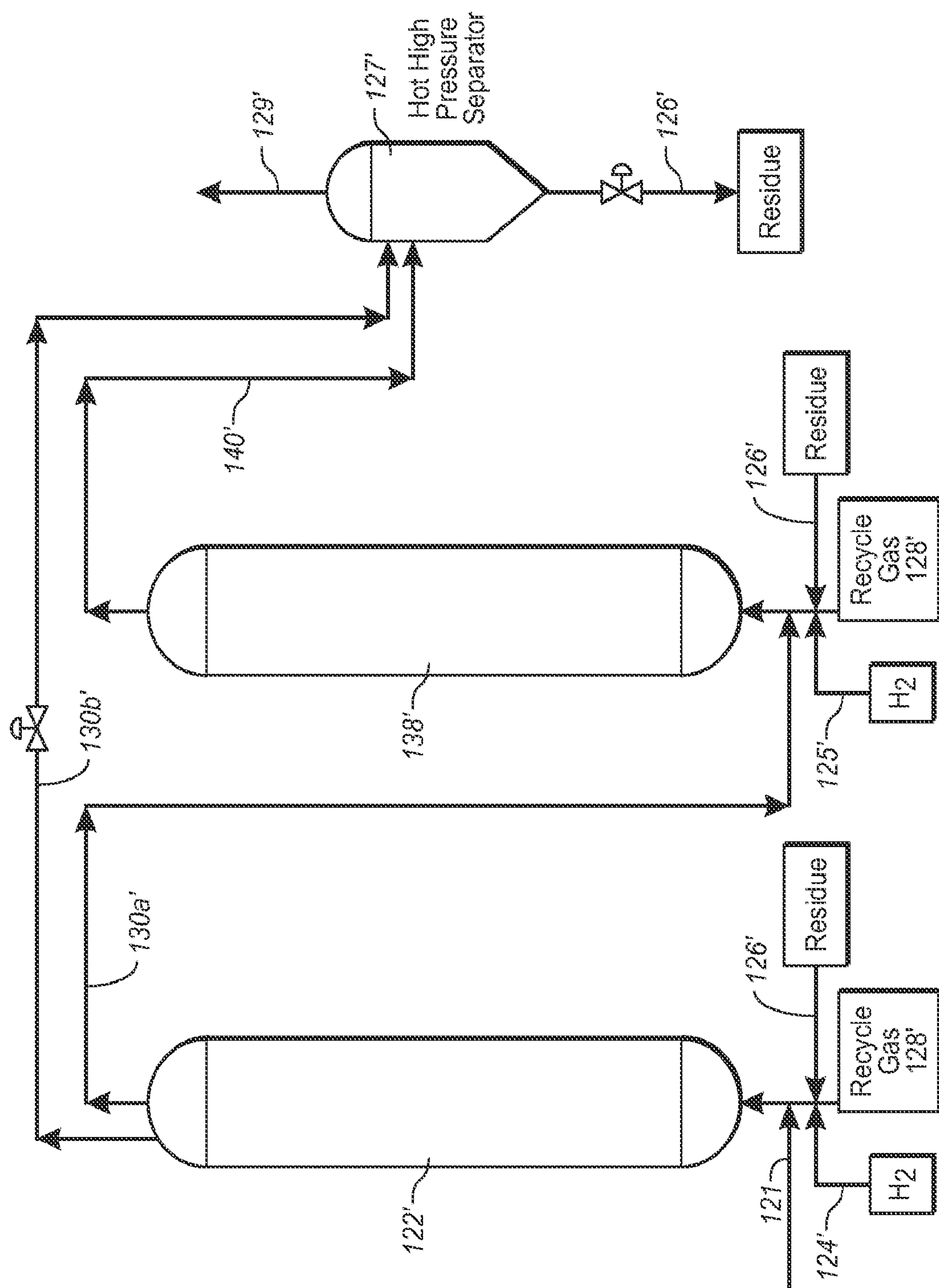


Fig. 4

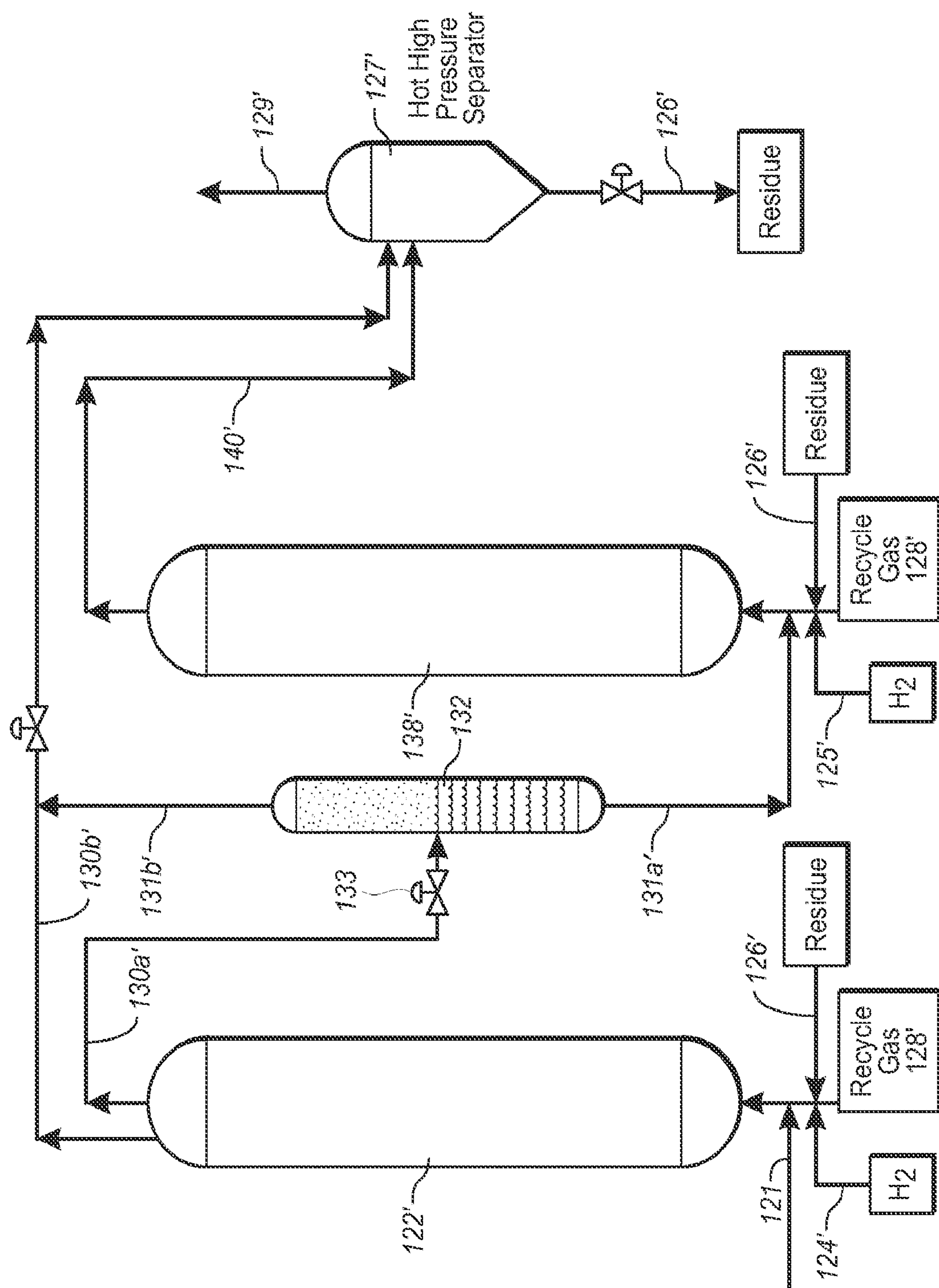
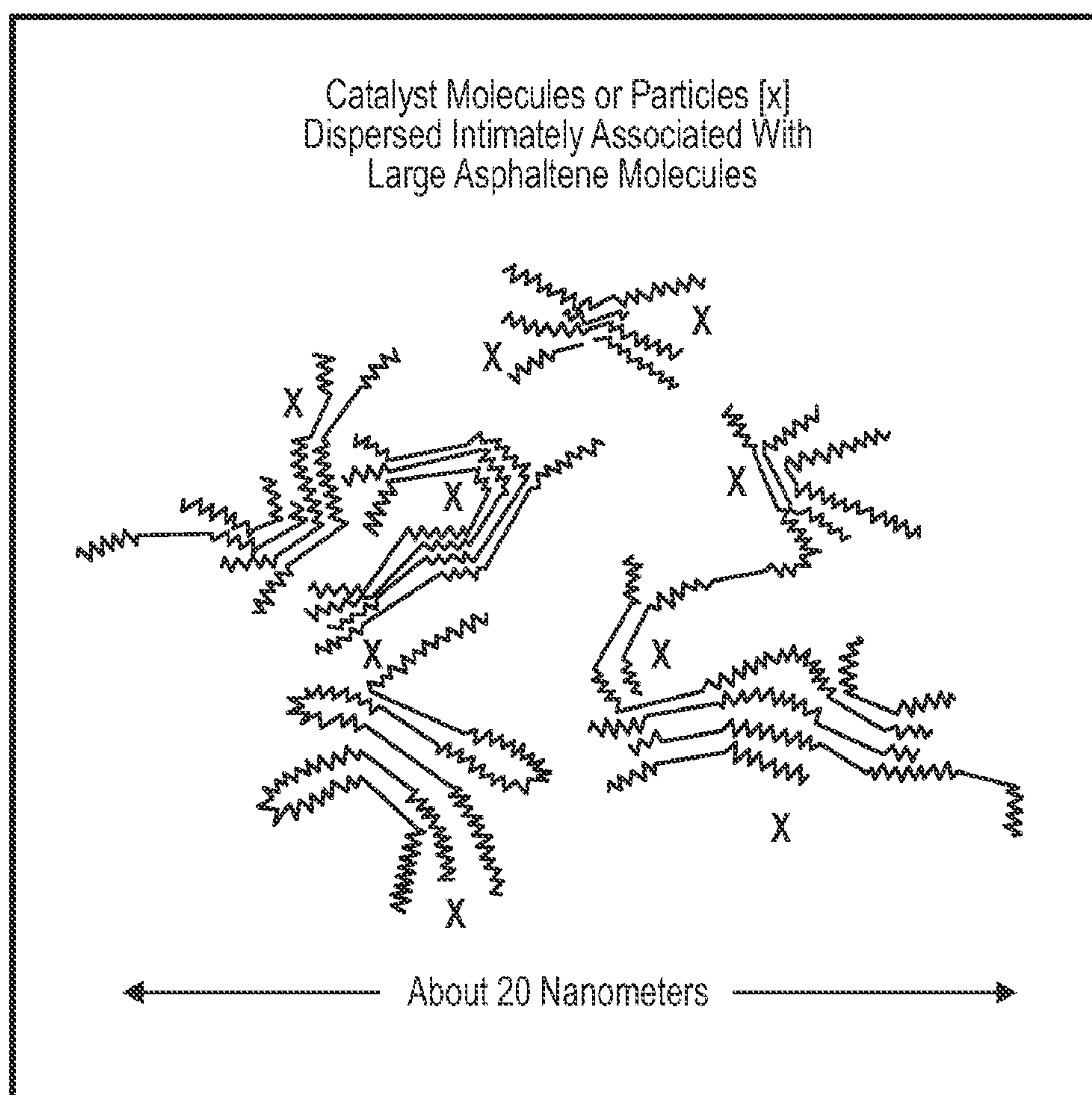
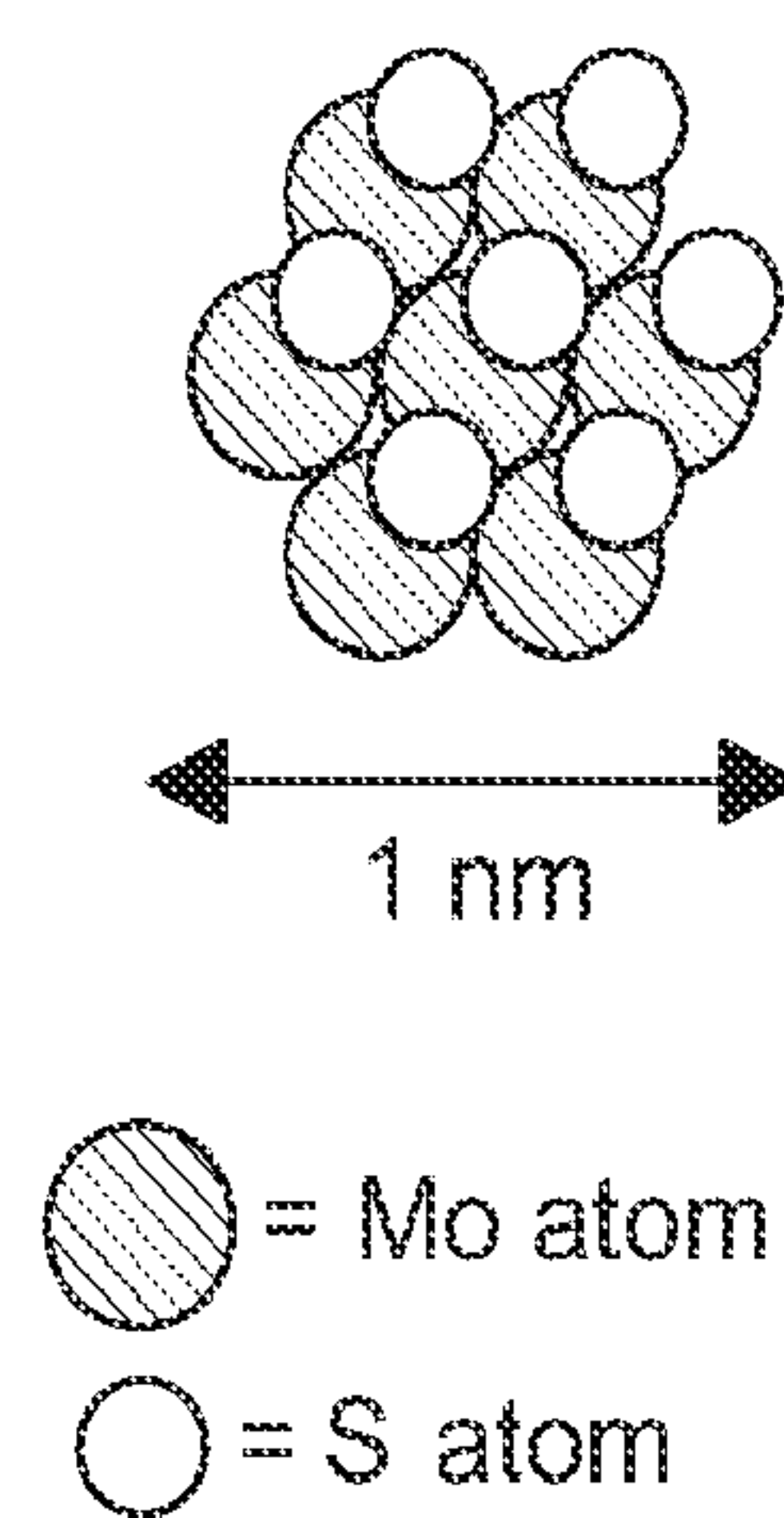
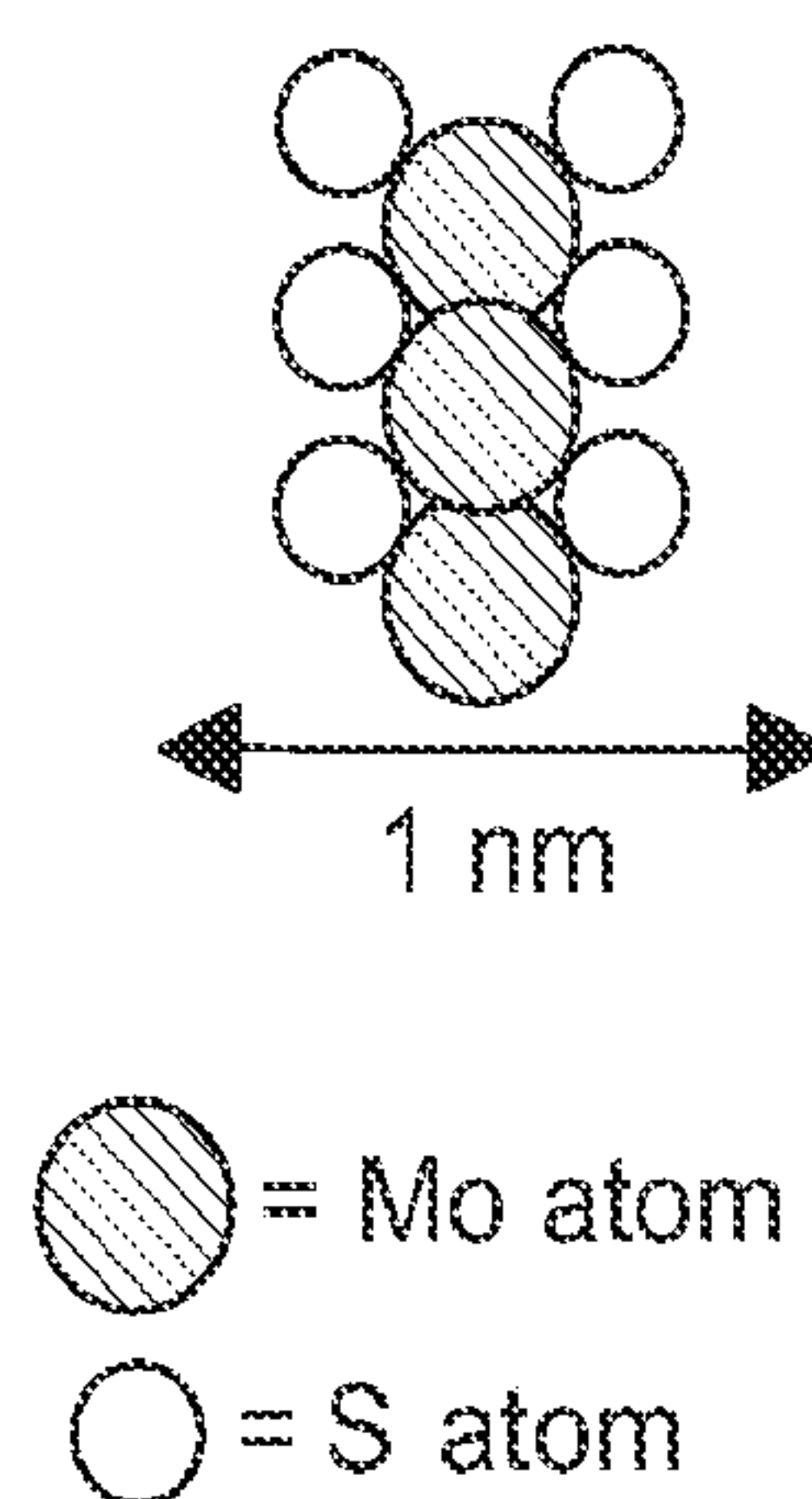


Fig. 5

*Fig. 6*

7/7

*Fig. 7A**Fig. 7B*

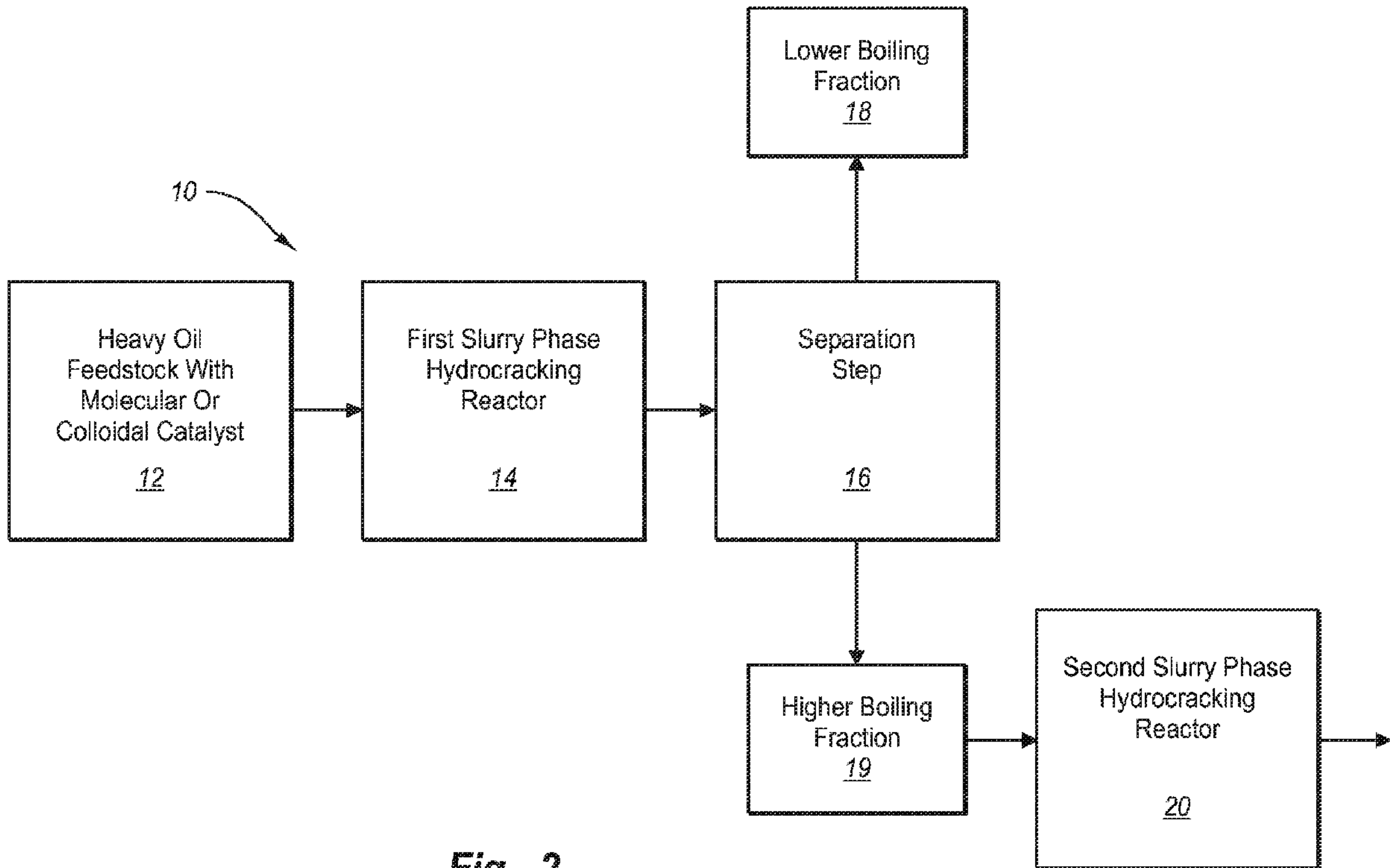


Fig. 2