

(19) AUSTRALIAN PATENT OFFICE

(54) Title
Methods and apparatus for removing solids from a membrane module

(51)⁶ International Patent Classification(s)
B01D 65/02 (2006.01) 20060101AFI2006051
B01D 65/02 7BHAU
PCT/AU2005/001396

(21) Application No: 2005284677 (22) Application Date: 2005 .09 .13

(87) WIPO No: W006/029456

(30) Priority Data

(31) Number	(32) Date	(33) Country
2004905292	2004 .09 .14	AU

(43) Publication Date : 2006 .03 .23

(71) Applicant(s)
Siemens Water Technologies Corp.

(72) Inventor(s)
Beck, Thomas William, Johnson, Warren Thomas

(74) Agent/Attorney
Shelston IP, Level 21 60 Margaret Street, Sydney, NSW, 2000

(56) Related Art
US-A-5 607 593
WO 2000/018498 A1
EP 280052 B
WO 2004/050221 A1
JP 10076144 A
US 2004/0217053 A1
JP 09 038470 A
WO 2003/024575

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
23 March 2006 (23.03.2006)

PCT

(10) International Publication Number
WO 2006/029456 A1

(51) International Patent Classification: **B01D 65/02**
(21) International Application Number:
PCT/AU2005/001396

(22) International Filing Date:
13 September 2005 (13.09.2005)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
2004905292 14 September 2004 (14.09.2004) AU

(71) Applicant (for all designated States except US): U. S. FILTER WASTEWATER GROUP, INC. [US/US]; 181 Thorn Hill Road, Warrendale, PA 15086 (US).

(72) Inventors; and

(75) Inventors/Applicants (for US only): BECK, Thomas, William [AU/AU]; 121 Keda Circuit, North Richmond, NSW 2756 (AU). JOHNSON, Warren, Thomas [AU/AU]; 87 Avoca Road, Grose Wold, NSW 2753 (AU).

(74) Agent: SHELSTON IP, 60 Margaret Street, Sydney, NSW 2000 (AU).

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NA, NG, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SM, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM, ZW.

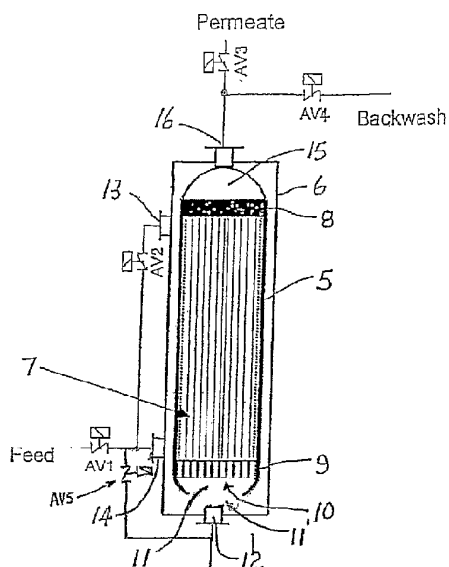
(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IS, IT, LT, LU, LV, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Declaration under Rule 4.17:

— of inventorship (Rule 4.17(iv)) for US only

[Continued on next page]

(54) Title: METHODS AND APPARATUS FOR REMOVING SOLIDS FROM A MEMBRANE MODULE



(57) Abstract: A method of operating a membrane filtration module (5), the module (5) including one or more membranes (7) extending longitudinally between vertically spaced upper and lower headers (8, 9) into which the ends of the membranes (7) are potted. The membranes (7) have a permeable wall which is subjected to a filtration operation wherein feed containing contaminant matter is applied to one side of the membrane wall and filtrate is withdrawn from the other side of the membrane wall. At least one of the upper and/or lower headers (8, 9) has one or more openings (10) therein and the method including flowing the feed, at least in part, through the one or more openings (10) for application to the membrane wall. Apparatus for performing the method is also disclosed.

WO 2006/029456 A1



Published:

— with international search report

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

**METHODS AND APPARATUS FOR REMOVING SOLIDS FROM A
MEMBRANE MODULE**

FIELD OF THE INVENTION

The present invention relates to membrane filtration systems and, more
5 particularly, to a method and apparatus for improving the filtration efficiency of such
systems by providing an improved cleaning system for the membranes.

BACKGROUND ART

Any discussion of the prior art throughout the specification should in no way be
considered as an admission that such prior art is widely known or forms part of common
10 general knowledge in the field.

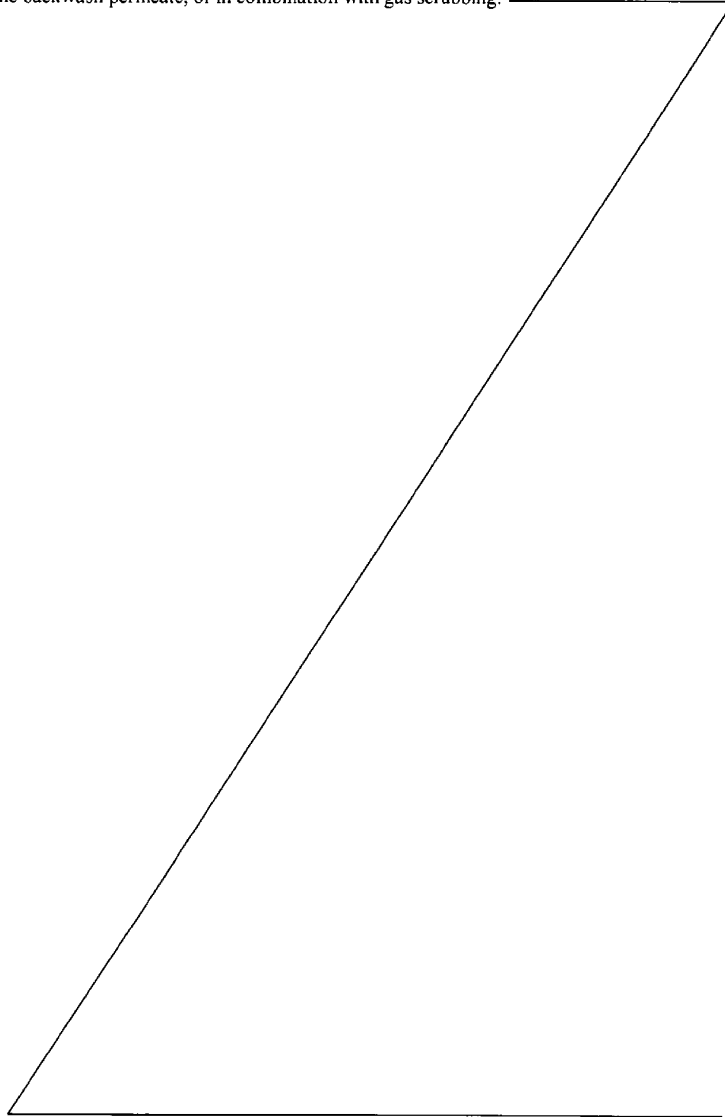
In a membrane filtration process, the method used to physically clean membranes
is of vital importance. An efficient membrane cleaning strategy can maintain a stable
permeability of the membrane and reduce the frequency of chemical cleans. A
commonly used method to physically clean membranes is a backwash (also called
15 "backflush" or "backpulse") with the permeate/filtrate or a gas. The backwash method is
typically used to eject solids blocking the membrane pores and partly dislodge the cake
that may have formed on the membrane surface. In a system exposed to a feed
containing a high concentration of solids, the fouling occurs more quickly and more
severely, in particular, where membranes are densely packed in a module.

20 Backwash with pressurized gas has proved a very efficient cleaning method and is
now widely used in the field of microfiltration processes. The limitation to this method
is the membrane pore size. Backwash of membranes with permeate has no limitations to
the pore size, but the backwash efficiency is generally lower than gas backwash and the
transmembrane pressure (TMP) recovery is not enough to offset the fouling rate. Further

2005284677 25 Sep 2008

- 1a -

means are employed to enhance the backwash efficiency, such as dosing chemicals to the backwash permeate, or in combination with gas scrubbing.



Maruyama et al in Japanese Patent No. JP2031200 discloses a hollow fibre membrane backwashing method. The method involves the following sequence: stop filtration, air-scour membrane, fill the membrane vessel, backwash with permeate under pressurized air and drain the waste. This procedure is repeated to achieve a higher efficiency. Sunaoka et al in a United States Patent No. 5,209,852 describes a process for scrubbing hollow fibre membranes in modules. This process is composed of a two-stage air scrubbing and draining to clean the membranes.

In order to minimise footprint and cost, membrane modules are typically manufactured with a high packing density of membranes, usually in the form of fibres. This increases the amount of membrane area for filtration within a module. However, the higher the packing density the more difficult it is to effectively flush solids captured during the filtration process from the membrane bundle. Therefore, improvement in the efficiency of solids removal during backwash allows either higher solids levels to be processed, or higher membrane packing densities to be used, reducing the cost of treatment.

In prior art fibre membrane systems, removal of solids is usually effected by sweeping with feedwater from one end of the module to the other and then out of the module through a side exit port. In this case, solids are first swept along the fibres to the exit end of the module, but must then cross the fibre bundle to exit the module. In many applications this requirement for the flow to change direction and pass perpendicular to the fibre bundle to exit the module can lead to accumulation of solids near the exit due to the tendency for the fibres to act like a string filter and capture or hinder the exit of solids from the module at this point.

DISCLOSURE OF THE INVENTION

The present invention seeks to overcome or at least ameliorate one or more of the disadvantages of the prior art or at least provide a useful alternative.

According to one aspect, the present invention provides a method of
5 operating a membrane filtration module, said module including one or more
membranes extending longitudinally between vertically spaced upper and lower
headers into which the ends of the membranes are potted, the membranes
having a permeable wall which is subjected to a filtration operation wherein feed
containing contaminant matter is applied to one side of the membrane wall and
10 filtrate is withdrawn from the other side of the membrane wall, at least one of
said upper and/or lower headers having one or more openings therein, the
method including flowing said feed, at least in part, through said one or more
openings for application to said membrane wall.

According to another aspect, the present invention provides a method of
15 cleaning a membrane filtration module, said module including one or more
membranes located in a feed-containing vessel and extending longitudinally
between vertically spaced upper and lower headers into which the ends of the
membranes are potted, the membranes having a permeable wall which is
subjected to a filtration operation wherein feed containing contaminant matter is
20 applied to one side of the membrane wall and filtrate is withdrawn from the other
side of the membrane wall, at least one of said upper and/or lower headers
having one or more openings therein, the method including:

- a) performing a filtration operation wherein said feed, at least in part, is
flowed through said one or more openings for application to said
25 membrane wall;

- 4 -

- b) suspending the filtration operation;
- c) performing a cleaning process on the membrane wall to dislodge contaminant matter therefrom into liquid surrounding the membrane;
- d) performing a sweep of the feed-containing vessel substantially parallel to the longitudinally extending membranes to remove the liquid containing the dislodged contaminant matter, at least in part, through the openings in the header; and
- e) recommencing the filtration operation.

For further preference, the openings are provided in the lower header and filtrate is withdrawn from the upper header. Preferably, the openings may also be used to introduce gas into the module to produce bubbles for scouring the surface of the membranes during said cleaning process. The sweep may be performed concurrently with the cleaning process. Preferably, the sweep is a high velocity sweep.

The present invention provides for holes or openings in one of the module pots so that during filtration at least part of the feed liquid will also be drawn in through the openings in the bottom pot and flow into the depths of the membrane bundle, reducing shell side pressure drop and generating some crossflow over the membrane surface. The use of these holes or openings for waste flow also allows solids swept along the membranes during the backwash process to continue to flow parallel to the membranes as they exit the module. The requirement for the solids to cross over the fibre bundle to exit at a side port is substantially reduced or eliminated.

The same concept may be applied to submerged membranes operated in an open tank. In the prior art, solids are typically removed by draining the tank.

- 5 -

As the feed containing the solids drains from the module it must change direction near the bottom to flow out of the module and drain from the tank. By providing holes or openings in the bottom of the module, solids can continue to flow substantially parallel to the fibres as they pass out of the module. This uninterrupted flow provides for more efficient removal of solid from the module and tank.

According to a further aspect, the present invention provides a method of operating a membrane filtration module, said module including one or more membranes extending vertically from an upper header into which proximal ends of the membranes are potted, the membranes having a permeable wall which is subjected to a filtration operation wherein feed containing contaminant matter is applied to one side of the membrane wall and filtrate is withdrawn from the other side of the membrane wall, the method including during said filtration operation flowing said feed, at least in part, through one or more openings in the module below said membranes for application to said membrane wall.

According to yet a further aspect, the present provides a method of cleaning a membrane filtration module, said module including one or more membranes located in a feed-containing vessel and extending vertically from an upper header into which proximal ends of the membranes are potted, the membranes having a permeable wall which is subjected to a filtration operation wherein feed containing contaminant matter is applied to one side of the membrane wall and filtrate is withdrawn from the other side of the membrane wall, the method including:

- 6 -

- a) performing a filtration operation wherein said feed, at least in part, is flowed through one or more openings in the module below said membranes for application to said membrane wall;
- b) suspending the filtration operation;
- 5 c) performing a cleaning process on the membrane wall to dislodge contaminant matter therefrom into liquid surrounding the membrane;
- d) performing a sweep or drain-down of the feed-containing vessel substantially parallel to the vertically extending membranes to
10 remove the liquid containing the dislodged contaminant matter, at least in part, through said opening or openings in the module beneath said membranes; and
- e) recommencing the filtration operation.

Apparatus for performing the above methods is also included within the
15 scope of the present invention.

BRIEF DESCRIPTION OF THE DRAWING

Embodiments of the invention will now be described, by way of example only, with reference to the accompanying drawings in which:

Figure 1 shows a schematic sectional view of a membrane module
20 according to one embodiment;

Figure 2 shows a schematic sectional view of a membrane module according to further embodiment; and

Figures 3a and 3b show an enlarged schematic sectional view of the lower header of a non-pressurized filtration system during the aeration and drain-down
25 phases, respectively.

- 7 -

DESCRIPTION OF PREFERRED EMBODIMENTS

Referring to the Figure 1, the filtration module 5 is mounted within a housing vessel 6 which contains the feed to be filtered. The filtration module 5 contains a bundle or bundles of hollow fibre membranes 7 extending between upper and lower headers 8 and 9, respectively. The lower header 9 is provided with a number of openings 10 communicating with the interior of the fibre bundle and an open-ended plenum chamber 11 having an opening 11'. An inlet/outlet port 12 is provided at the base of the module 5. Feed is supplied through ports 12, 13 and 14 under the control of valves AV5, AV1 and AV2.

Permeate/filtrate is withdrawn through chamber 15 and port 16 under control of valve AV3. A backwash may also be applied through port 16 under the control of valve AV4.

Figure 2 shows a similar arrangement to Figure 1, however, in this embodiment the hollow fibre membranes 7 are suspended vertically from the upper header 8 and are not potted at their lower distal ends 19. The distal ends 19 of each fibre membrane 7 are closed and filtrate withdrawn through the upper header 8.

In use, solids accumulated within the modules 5 following filtration and backwash are flushed or swept from the modules 5 through the openings 10 by opening port 12 and applying a suitable pressure to the feed within the module 5. The waste is flushed through the opening 11' in the plenum chamber 11 and removed through open port 12.

Figures 3a and 3b show an enlarged view of the lower headers 9 of a pair of modules 5 connected to a single plenum chamber 11 in a non-pressurized filtration system. The modules 5 in this embodiment are mounted in an open

- 8 -

vessel (not shown) and the waste liquid containing solids accumulated within the modules 5 following filtration and backwash is drained through the openings 10 under force of gravity, as shown in Figure 3b.

As best shown in Figure 3a, port 17 connected to a gas supply manifold 18 may also be used to supply gas to openings 10 to provide scouring bubbles within the module 5 to assist cleaning of the fibre membrane surfaces.

Systems embodying the invention may provide a number of benefits including:

1. Enhanced solids removal during backwash due to sweeping action along the fibre surface rather than across multiple fibres.
2. Easier contact of feed liquid with the inside of the membrane bundle during filtration (feed liquid can be drawn into the centre of the bundle through the same holes during filtration). This also induces a form of crossflow during filtration.
3. Rack inserts containing sets of membrane modules can be lowered down closer to the bottom of the module as an open area is no longer required beneath the modules to accommodate manifolds and piping used for solids removal and feed inlet, this now takes place through the openings in the pot. The result is better void space reduction efficiency as well as less space for drainage.
4. The plenum chambers can be connected to a pipe or manifold and the backwash waste pumped out of the module rather than gravity flowed, and/or the feedwater pumped in during filtration.

- 9 -

It will be appreciated that further embodiments and exemplifications of the invention are possible with departing from the spirit or scope of the invention described.

THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:-

1. A method of cleaning a membrane filtration module, said module
5 including one or more membranes located in a feed-containing vessel and
extending longitudinally between vertically spaced upper and lower headers into
which the ends of the membranes are potted, the membranes having a
permeable wall which is subjected to a filtration operation wherein feed
10 filtrate is withdrawn from the other side of the membrane wall, the lower header
having one or more openings therein, the method including:
- a) performing a filtration operation wherein said feed, at least in part, is
flowed through said one or more openings for application to said
membrane wall;
 - 15 b) suspending the filtration operation;
 - c) performing a cleaning process on the membrane wall to dislodge
contaminant matter therefrom into liquid surrounding the membrane;
 - d) performing a sweep or drain-down of the feed-containing vessel
20 substantially parallel to the longitudinally extending membranes to
remove the liquid containing the dislodged contaminant matter, at
least in part, through the openings in the lower header; and
 - e) recommencing the filtration operation.
2. A method of cleaning a membrane filtration module according to claim 1
wherein filtrate is withdrawn from the upper header.
- 25 3. A method of cleaning a membrane filtration module according to claim 1
or claim 2 wherein the openings are used to introduce gas into the module to

produce bubbles for scouring the surface of the membranes during said cleaning process.

4. A method of cleaning a membrane filtration module according to any one of the preceding claims wherein the sweep is performed concurrently with the
5 cleaning process.

5. A method of cleaning a membrane filtration module according to any one of the preceding claims wherein the sweep is a high velocity sweep.

6. A method of cleaning a membrane filtration module according to any one of the preceding claims wherein the feed-containing vessel is open to
10 atmosphere.

7. A membrane filtration module including one or more membranes extending longitudinally between vertically spaced upper and lower headers into which the ends of the membranes are potted, the membranes having a permeable wall which is subjected to a filtration operation wherein feed
15 containing contaminant matter is applied to one side of the membrane wall and filtrate is withdrawn from the other side of the membrane wall, said lower header having one or more openings therein and means for flowing said feed, at least in part, through said one or more openings for application to said membrane wall and further including means for performing a cleaning process
20 on the membrane wall to dislodge contaminant matter therefrom into liquid surrounding the membrane; and means for removing said contaminant matter containing liquid through one or more of said openings.

8. A membrane filtration module according to claim 7 wherein filtrate is
25 withdrawn from the upper header.

9. A membrane filtration module according to claim 7 or claim 8 wherein the openings are used to introduce gas into the module to produce bubbles for scouring the surface of the membranes during said cleaning process.

10. A membrane filtration system including a membrane filtration module, the
 5 membrane filtration module including one or more membranes located in a feed-containing vessel and extending longitudinally between vertically spaced upper and lower headers into which the ends of the membranes are potted, the membranes having a permeable wall which is subjected to a filtration operation wherein feed containing contaminant matter is applied to one side of the
 10 membrane wall and filtrate is withdrawn from the other side of the membrane wall, said lower header having one or more openings therein, the membrane filtration system further including:

- a) means for performing a filtration operation wherein said feed, at least in part, is flowed through said one or more openings for application to
 15 said membrane wall;
- b) means for suspending the filtration operation;
- c) means for performing a cleaning process on the membrane wall to dislodge contaminant matter therefrom into liquid surrounding the membrane;
- 20 d) means for performing a sweep or drain-down of the feed-containing vessel substantially parallel to the longitudinally extending membranes to remove the liquid containing the dislodged contaminant matter, at least in part, through the openings in the lower header; and
- e) means for recommencing the filtration operation.

11. A membrane filtration system according to claim 10 wherein filtrate is withdrawn from the upper header.
12. A membrane filtration system according to claim 10 or claim 11 wherein the openings are used to introduce gas into the module to produce bubbles for
5 scouring the surface of the membranes during said cleaning process.
13. A membrane filtration system according to any one of claims 10 to 12 wherein the sweep is performed concurrently with the cleaning process.
14. A membrane filtration system according to any one of claims 10 to 13 wherein the feed-containing vessel is open to atmosphere.
- 10 15. A method of cleaning a membrane filtration module substantially as herein described with reference to any one of the embodiments of the invention illustrated in the accompanying drawings and/or examples.
16. A membrane filtration module according to claim 7 substantially as herein described with reference to any one of the embodiments of the invention
15 illustrated in the accompanying drawings and/or examples.
17. A membrane filtration system substantially as herein described with reference to any one of the embodiments of the invention illustrated in the accompanying drawings and/or examples.

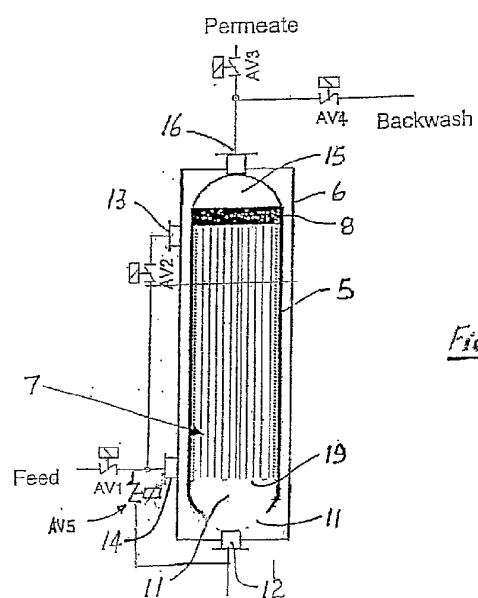
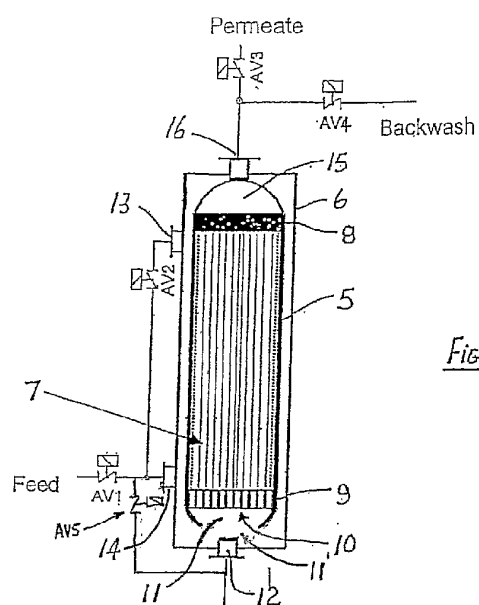


Fig. 3a

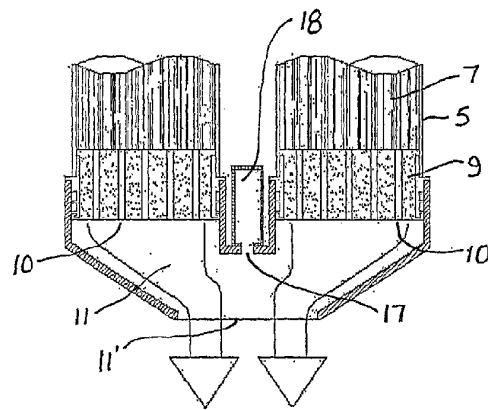
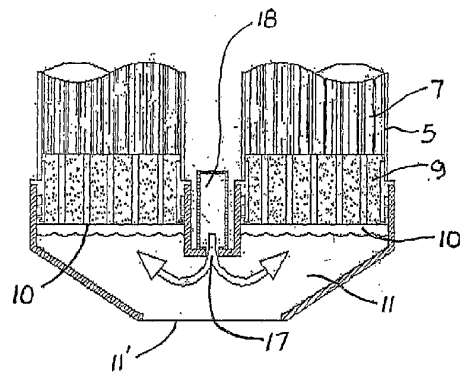


Fig. 3b