

**METHOD FOR COMBUSTION OF A LIQUID FUEL WITH STAGED  
ATOMIZATION**

The present invention **relates**, on the one hand, to a **method** for combustion of a liquid fuel comprising the **steps** for producing a spray (10) of the liquid fuel by injecting a main stream (3) of an **atomizing gas** in contact with the liquid fuel (4), the said **method** being **characterized** in that at least one secondary **stream** (11) of **atomizing gas** is **injected** close to the **spray** (10) in order to produce a **secondary** atomization of the said spray (10) prior to its contact with a jet of **oxidizer** in order to carry out the combustion of **the** spray, and, on the **other**, to a burner **impl** such a combustion method.

Figure 1

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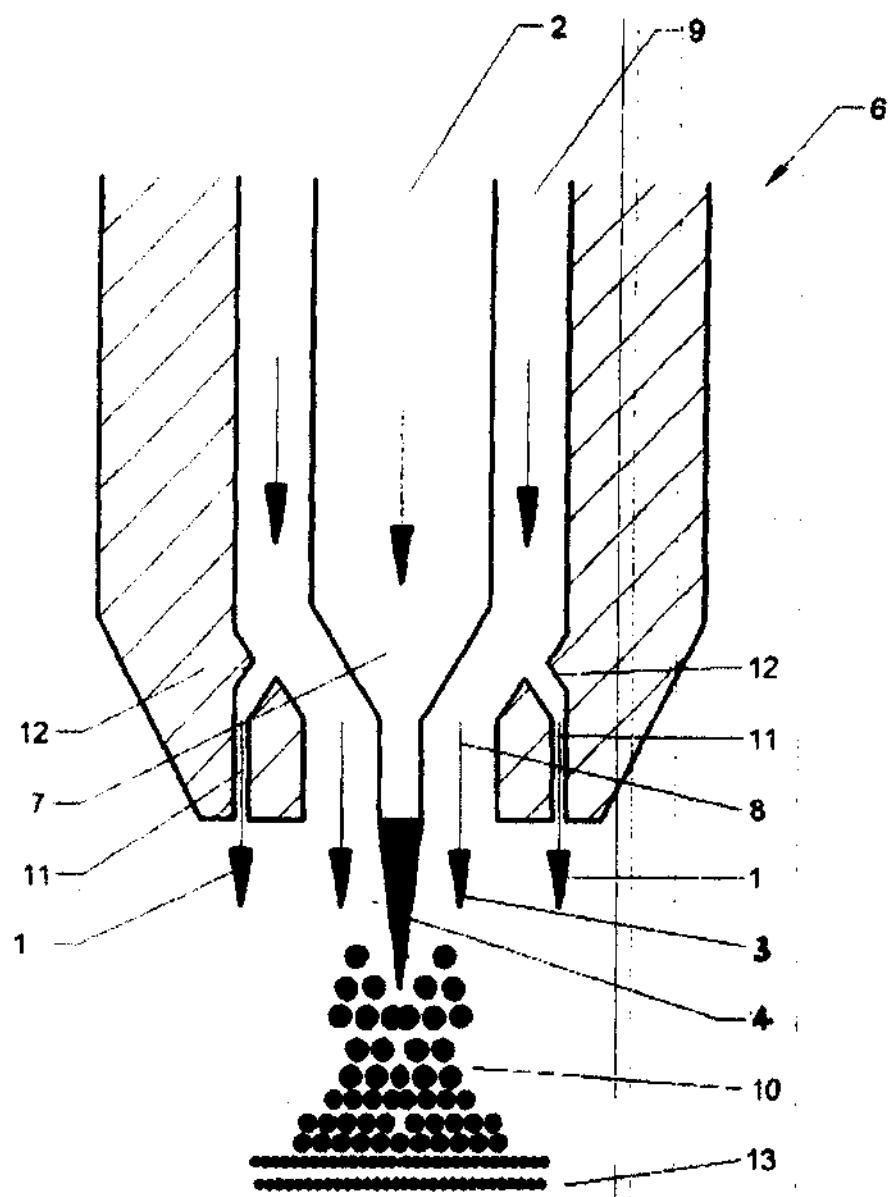


Fig. 1

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CLAIMS

1. Method for combustion of a liquid fuel comprising the steps for producing a spray (10) of the liquid fuel by injecting a main stream (3) of an atomizing gas in contact with the liquid fuel (4), the said method being characterized in that at least one secondary stream (1, 5) of atomizing gas is injected close to the spray (10) in order to produce a secondary atomization of the said spray (10) prior to its contact with a jet of oxidizer in order to carry out the combustion of the fuel.
2. Combustion method according to Claim 1, characterized in that the secondary stream (1) of atomizing gas is injected in a direct parallel to the injection direction of the liquid fuel.
3. Combustion method according to Claim 1, characterized in that the secondary stream (5) of atomizing gas is injected in an oblique direction converging towards the injection direction of the liquid fuel.
4. Combustion method according to any one of Claims 1 to 3, characterized in that the secondary stream (1, 5) of atomizing gas is injected so as to produce a turbulent flow.
5. Combustion method according to any one of Claims 1 to 4, characterized in that the atomizing gas flow rate in the secondary stream (1, 5) of atomizing gas represents between 20% and 70% of the total flow rate of atomizing gas.
6. Combustion method according to any one of Claims 1 to 5, characterized in that the secondary stream (1, 5) of atomizing gas is divided into a

plurality of streams injected in a uniformly distributed manner and equidistant around the liquid fuel stream (4).

7. Combustion method according to any one of Claims 1 to 6, characterized in that the oxidizer jet is divided into a primary oxidizer jet and a secondary oxidizer jet, the primary oxidizer jet being injected close to the liquid fuel spray in order to cause a first incomplete combustion, the gases issuing from this first combustion still comprising at least part of the fuel, while the secondary oxidizer jet is injected at a distance  $l$ , from the fuel spray which is higher than the distance between the liquid fuel jet and the primary oxidizer jet closest to the liquid fuel spray, in order to enter into combustion with the part of the fuel present in the gases issuing from the first combustion.

8. Burner comprising at least one liquid fuel injection means (7) combined with at least one atomizing gas injection means (8) in order to produce a fuel spray (10), and at least one oxidizer injection means, characterized in that it comprises at least one secondary atomizing gas injection means (11, 12, 14) arranged close to the fuel injection means.

9. Burner according to Claim 8, characterized in that the secondary atomizing gas injection means (11, 12, 14) is obtained by bypassing a common atomizing gas feed (9).

10. Burner according to either of claims 8 and 9, characterized in that the secondary means (11, 12, 14) is oriented parallel to or obliquely to the fuel injection means (7).

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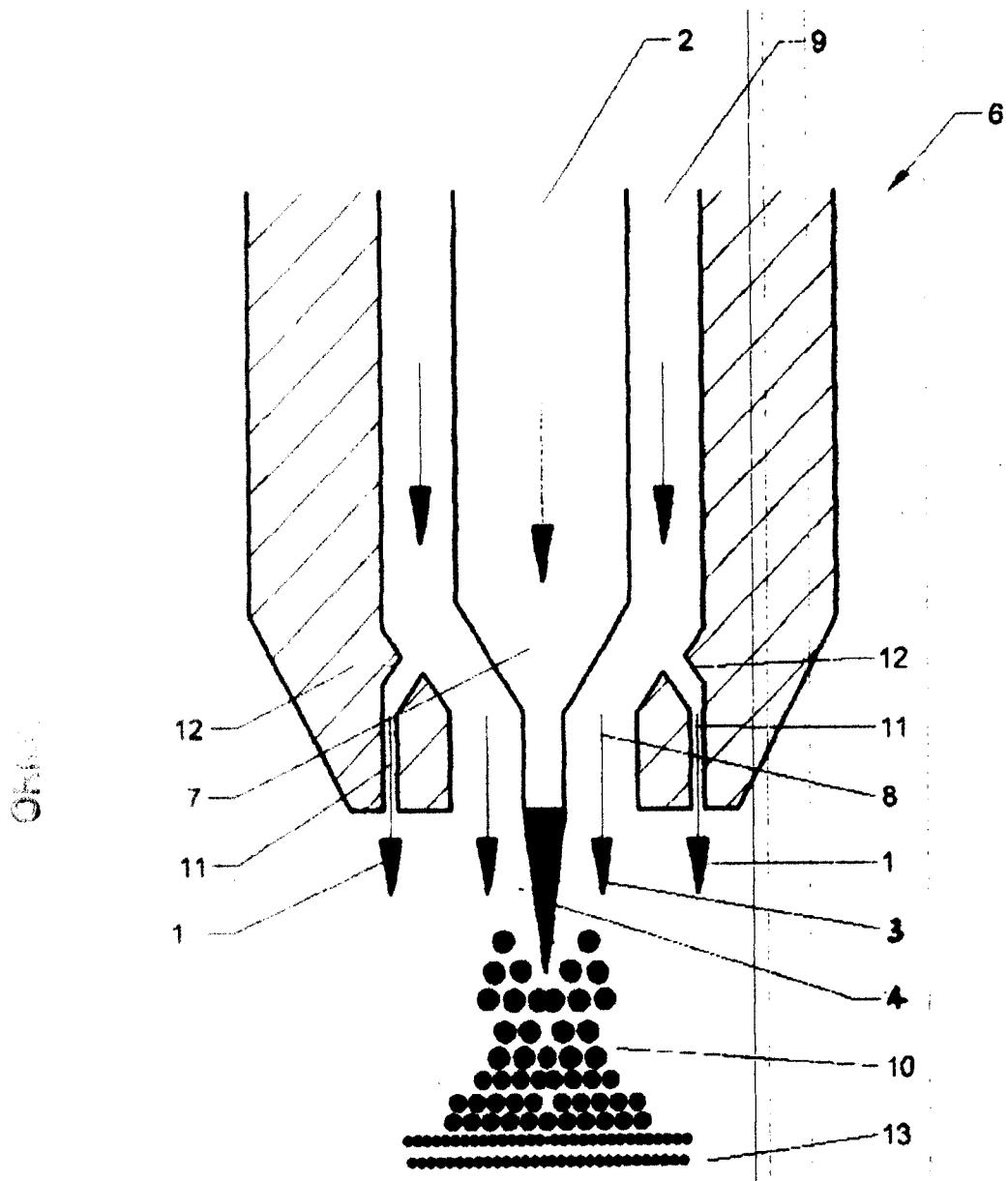


Fig. 1

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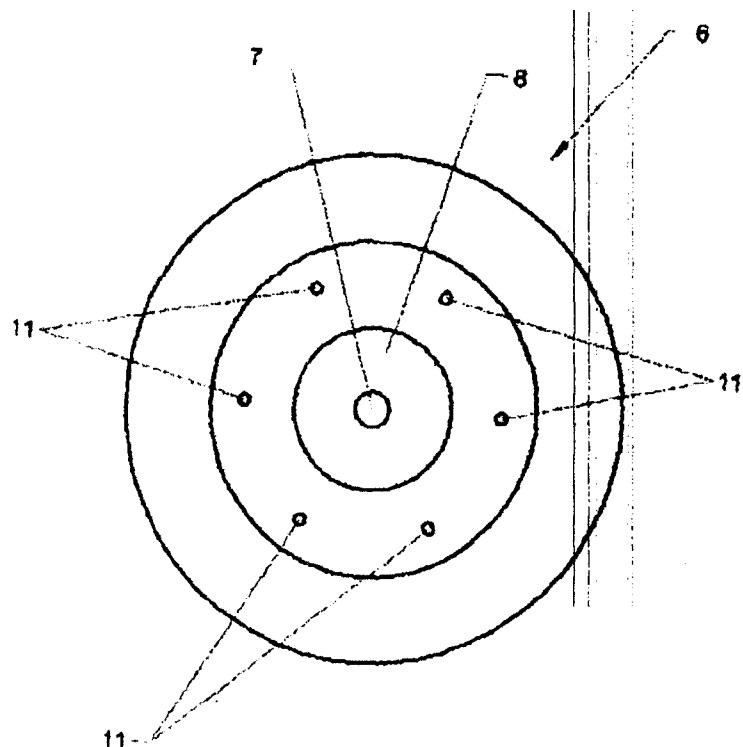


Fig. 2

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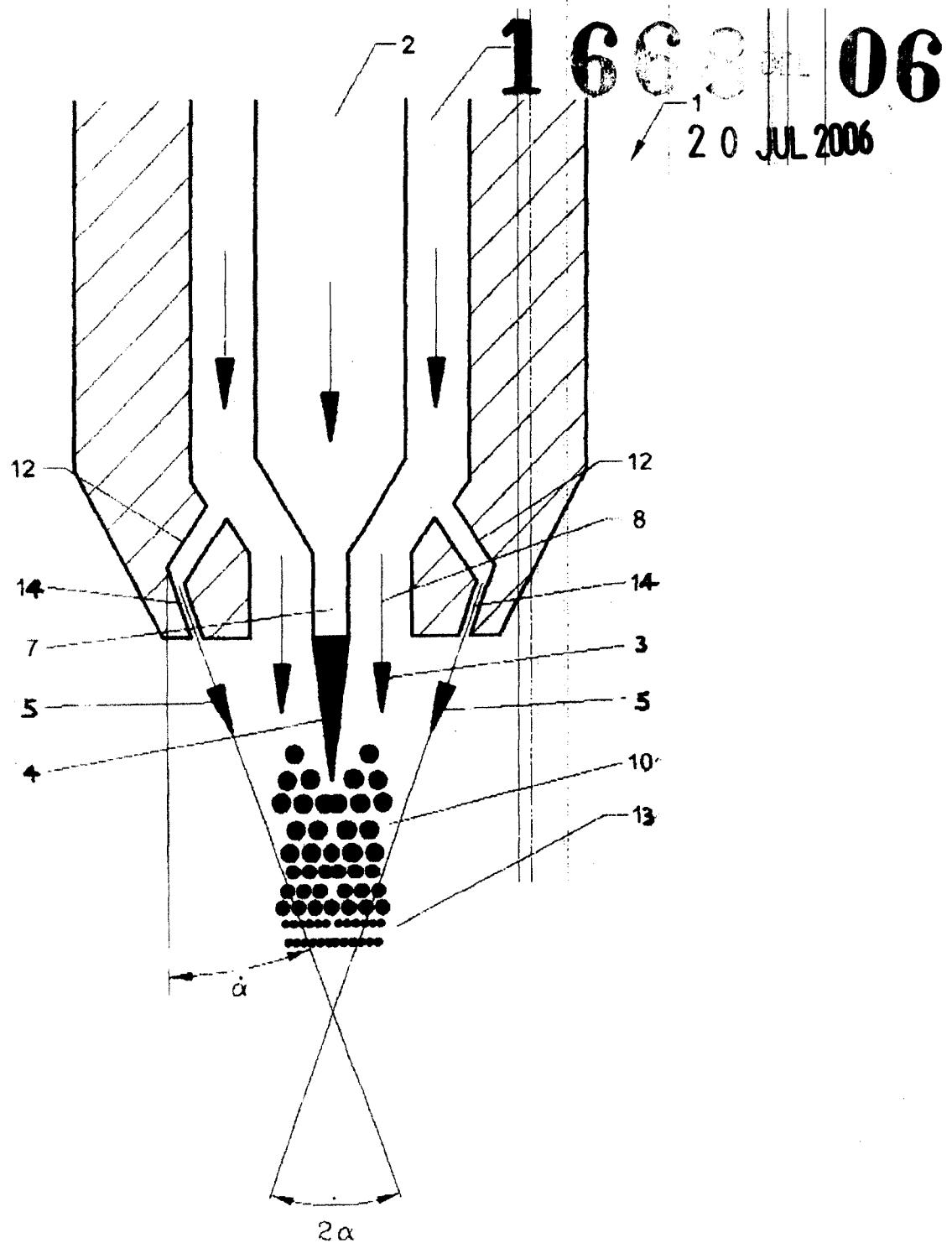


Fig. 3

  
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The present invention **relates** to a method for combustion of a liquid **fuel**, and to a burner implementing the **same**.

During the installation of a **combustion system** for an industrial furnace, for example, one of the major concerns **is** to **optimize** the combustion efficiency by optimally controlling the **flame properties**, while **meeting** the needs of the heated **method** in terms of heat transfers and minimizing air pollutant releases.

The **two-phase** combustion of a liquid fuel by an **oxidizing gas** comprises two main **steps** before the actual combustion takes **place**. In the first step, it is **necessary** to **atomize** the liquid **fuel** using an **atomizing gas injected** so as to **destabilize** the liquid fuel stream and to form a **fuel spray** with a **high** contact surface area with the **oxidizer** in order to promote the combustion. The **atomizing gas used** may be air, oxygen, steam or even natural **gas**, for example. It **is** then **necessary** for the liquid **fuel** drops thus formed to evaporate before the **fuel burns** with the **oxidizer**. Since the fuel drop vaporization time is **longer** than the reaction time, the **mixture** of the reagents and, **in consequence**, the combustion properties, essentially depend on the **characteristics** of the fuel spray, particularly the size of the fuel drops **formed**.

The **spray characteristics** depend on the type of injector used. Most injectors use a high **speed** differential between the **atomizing gas** and the liquid fuel to destabilize the fuel and **for the spray**. Two types of injector are available **according** to whether a high speed **flow** is imposed on the fuel or the **atomizing gas**, that is, mechanical injectors in which the fuel is subjected to high pressure and **flow** at high **speed** through a small-diameter orifice, and injectors called "dual fluid" injectors in which a **fuel** jet **flows** at a

relatively low **speed** and is destabilized by a high **speed** flow of atomizing gas. However, **mechanical** injectors are little **used because**, on the one hand they incur higher risks of **blocking** of the fuel injection orifice by **deposits**, and on the other, limited flow range due to the **high** cost of the **compressors** needed to reach high liquid **pressures**.

Dual fluid **injectors** can allow for very **high atomizing** **flow speeds**. In this category, a distinction is made between **air-assisted** atomizers, **operating** with low flow rates of gas ejected at very high **speed**, and spray **atomizers** characterized by lower **atomizing** gas flow speeds but higher flow rates. Two **fluids** can be **mixed** in a **confined environment** (internal **mixing** injector) or **outside** the injection **system** (**external** **mixing** injector).

Furthermore, the liquid fuel flow **may optionally** be oriented to form a film on an appropriate surface before its contact with the **atomizing gas** flow. In this case, the injector is called a **prefilmed atomizer**, with prior formation of a **liquid** film, and in the opposite case, a plain jet **atomizer**, with full liquid flow.

The most commonly **used** injectors in **oxy-combustion** are **injectors** of the dual flow type **with** spraying with an atomizing gas **speed** lower than 200 m. **with** **external** **air** **mixing**, and plain jet **injectors**.

The combustion properties of a spray **produced** by such injectors are mainly controlled by changing the relative **atomizing gas** and **liquid** **flow speeds**. In doing so, the mean drop **size** of the fuel spray is modified, and consequently, the **vaporization** time compared with the combustion reaction time is also changed. The drop size and **vaporization** time control the mixing of the evaporated fuel **with** the **oxidizer**.

and are hence very important **combustion parameters**, determining particularly whether the combustion **is** complete or **not**. **However**, although **controlling** the injection speeds **serves** to **adjust** the **properties** of the spray and of the two-phase combustion **to** adapt them to the heated **process**, **such injectors still** have a lack of **flexibility**.

For example, it is difficult to **effectively** control the cooling of the injector. In fact, an **increase** in the **atomizing gas** flow rate **results** in a **reduction** in the mean drop size, and consequently, a closer reaction zone and hence **overheating** of the **injector**.

Moreover, for an excessively high **atomizing** gas flow rate, the **atomization** mode may go from a **fibre mode**, that is, with a fully developed **liquid** cone, to a **superpulse** mode, that **is**, with a **short and truncated** liquid cone. In this case, the **reactio** zone is liable to **stabilize** in the immediate **neighbourhood** of the **burner** and cause its **destruction**. Moreover, an excessively high atomizing gas **speed** can also **cause** instability of the flame. In **fact**, it has been demonstrated that the stability of the **flame** could be related to the ratio of the **mixing** time to the characteristic time of the **combustion** chemistry, the flame being stable when this ratio is above 1. In the case of an excessive **increase in the atomizing ga** **speed**, the **mixing time** becomes shorter than the **characteristic** time of the **combustion chemistry**, and the stability condition is no longer **satisfied**.

Another drawback is that the **spray characteristic** affect **several** parameters which **ar** therefore not possible to control independently **f** one another. Thus, **it** is not possible to control the **spray** drop size and spray angle independently, **characteristic** bot **dependent** on the ratio of the **momentu** of atomizing gas to that of the **fuel**. More **particularly**, if this

momentum ratio is lower than 5, an increase in the atomizing gas flow rate simultaneously results in a decrease in the drop size and a widening of the spray angle, the flame being liable to interact with those of adjacent burners.

Another drawback appears in the case in which a high viscosity fuel is used. In this case, a simple atomizing gas stream injected in a ring around the liquid fuel stream does not permit uniform atomization producing a spray with uniform drop sizes. This causes irregular combustion and problems of flame stabilization.

It is the object of the present invention to overcome the abovementioned drawbacks and therefore consists of a method for combustion of a liquid fuel comprising the steps for producing a spray of the liquid fuel by injecting a main stream of an atomizing gas in contact with the liquid fuel, the said method being characterized in that at least one secondary stream of atomizing gas is injected close to the spray in order to produce a secondary atomization of the said spray prior to its contact with a jet of oxidizer in order to carry out the combustion of the fuel.

Thus, for the same total atomizing gas flow rate, the flow rate of the first atomizing stream is decreased, causing the formation of a spray with a higher size of the drops formed in the neighbourhood of the injector. The fuel drops of the first spray then undergo a second atomization, leading to a modified spray with smaller drops. A first spray having already been formed, the secondary atomization is more effective, particularly in the case of a high viscosity fuel, and entrains the drops of the modified spray further from the injector. Due to this staged atomization of the liquid fuel, the combustion reaction takes place further from the injector, thereby decreasing the risks of burner

overheating and destruction. It is important to observe that in the case in which a burner has a retractable injection head, the secondary atomization allows it to operate with a higher retraction. Moreover, the atomizing gas flows thereby multiply permit more effective cooling of the burner. The injector service life is thereby increased and its maintenance reduced.

This improvement in cooling the injector is particularly advantageous in the case in which the atomizing gas used is oxygen, a gas for which the risks of overheating are high.

Furthermore, the presence of a secondary atomization stream reduces the dependence between the drop size (flame length) and the spray angle (flame width) by limiting the increase of the latter. The flame length can therefore be controlled more easily, while limiting the risks of interaction with adjacent burner flames.

A further advantage of the invention is the reduction of emissions of NOx compounds. In fact, the flame temperature obtained is more uniform, so that NOx formation is reduced. This process is accentuated by a better dilution of the reagents and combustion products thanks to the secondary atomizing gas stream.

According to a first exemplary embodiment of the method, the secondary stream of atomizing gas is injected in a direction parallel to the injection direction of the liquid fuel.

According to a second exemplary embodiment of the method, the secondary stream of atomizing gas is injected in an oblique direction converging towards the injection direction of the liquid fuel. This makes it possible to control the spray angle more accurately, the modified spray angle being equal to twice the angle

between the **secondary** atomizing gas stream injection direction and the fuel flow direction. **Advantageously**, the secondary atomizing **gas** stream is **injected** at an angle of between 0 and 60°, preferably at an angle of between 0 and 30°.

Optionally, adjusting **means** can be provided for orienting the secondary atomizing gas **an** injection direction **as regards** the liquid fuel injection direction in order to increase the **flame** width, and consequently, the heat **transfer** to the **heated process**, if necessary.

**Advantageously**, the secondary **stream** of atomizing gas is injected so as to produce a **turbulent** flow. Thus, the turbulent flow improves the dilution of the reagents and **combustion** products and **rther** reduces the **emissions** of NOx compounds.

Preferably, the **secondary** atomizing **ga** flow rate **represents** between 20% and 70% of the **total** flow **rate** of atomizing **gas**.

**Advantageously**, the secondary **stream** of atomizing gas is divided into a plurality of **streams** injected in a uniformly distributed manner and **equidistant around** the liquid fuel stream. The injection can be carried out *inter alia*, by a concentric flow **around** the fuel injection or by a plurality of **openings** terminating in the burner head and uniformly **distributed** around the fuel injection. More precisely, the **ma** atomizing gas stream is **injected** coaxially **around** the liquid fuel while the secondary stream is **ected** via the plurality of openings.

The method according to the invention **is** ideal for the **staged** combustion process in **which** the **oxidizer** is **injected** and divided into several streams **introduced** at various **distances** from the fuel **spray**, as **described** in

particular in WO 2004/094902. Thus, the oxidizer jet can be divided into a primary oxidizer jet and a secondary oxidizer jet, the primary oxidizer jet being injected close to the fuel spray in order to cause first incomplete combustion, the gases issuing from this first combustion still comprising at least part of the fuel, while the secondary oxidizer jet is injected at a distance  $l$  from the fuel spray which is higher than the distance between the fuel spray and the primary oxidizer jet closest to the fuel spray, in order to enter into combustion with the part of the fuel present in the gases issuing in the first combustion. The invention also covers the case in which a third oxidizer jet is injected at a distance  $l$  from the fuel spray which is longer than the distance  $l_1$ .

The method according to the invention is ideal for two phase burners in which the atomizing gas is injected on the one hand, at a speed at least 10 times higher than the fuel injection speed, and on the other, with an atomizing gas mass flow rate higher than 10% of the fuel mass flow rate.

The present invention further relates to a burner implementing the preceding two-phase method, the said burner comprising at least one fuel injection means combined with at least one atomizing gas injection means in order to produce a fuel spray, and at least one oxidizer injection means characterized in that it comprises at least one secondary atomizing gas injection means arranged close to the fuel injection means. It should be observed that in the case of a burner with highly separated jets, such a burner comprises a primary oxidizer injection means, a secondary oxidizer injection means arranged at a distance from the fuel injection means that is longer than that of the primary injection means, and optionally, a tertiary oxidizer injection means.

arranged at the edge of the burner.

Advantageously, the **secondary** atomizing gas injection means is obtained by bypassing a common **atomizing gas** feed. The choice of the bypass **diameter** serves to define a ratio **between** the primary atomizing gas stream and the main stream. Further advantageously, the **secondary** injection means is **oriented** parallel to or obliquely to the fuel injection means.

The **implementation** of the invention will be better understood from the detailed **description** given below with reference to the drawing appended here to in which:

Figure 1 is an enlarged **partial** schematic representation of a longitudinal **cross section** of an **atomization head** of a burner according to the invention;

- Figure 2 is a front view of the **atomization head** in Figure 1; and

- Figure 3 is an enlarged **partial** schematic representation of a longitudinal **cross section** of another **atomization head** of a burner according to the invention.

A combustion method according to the invention is implemented by a burner comprising a **spray-guide** **atomization head** 6 with external **mixing** as shown in Figures 1 and 2. This **atomization head** 6 comprises:

- an ejection line 7 for a **liquid fuel** stream 4; delivered by a fuel feed 2; and

- an atomizing gas ejection line 8 concentric with the fuel ejection line 7 and connected to an atomizing gas feed 9 and terminating in contact with the fuel stream 4 in order to produce a liquid fuel spray 10 under the action of a **main** atomizing **gas** stream 3.

Furthermore, the atomization head 6 has six **secondary** ejection channels 11 oriented **parallel** to the fuel

ejection line 7 and to the atomizing gas ejection line 8. These six secondary ejection channels 11 are uniformly distributed around the ejection lines 8 and are designed to create secondary atomizing gas streams 1 tapped off from the atomizing gas feed 9 by bypass channels 12. Under the effect of these secondary atomizing gas streams 1, the liquid fuel spray 10 thereby undergoes a second atomization producing a modified spray 13. This modified spray 13 is then contacted with an oxidizer stream (not shown), optionally divided into a primary stream and a secondary stream, to carry out the combustion of the fuel. A tertiary oxidizer feed may also be located at a relatively long distance from the atomization head 6 and is used to inject oxygen at high speed in order to obtain a sufficient dilution of the reagents before the main combustion zone and thereby to prevent an excessive formation of thermal NOx compounds. Experiments have demonstrated that such a burner, in which 50% of the total oxygen was injected at the tertiary feed level, served, all other things remaining equal, to obtain a flame stabilization distance equal to about four times the flame stabilization distance of a conventional injector without secondary atomizing gas stream. This longer stabilization distance serves to reduce the overheating of the atomization head 6. Furthermore, it has also been demonstrated that the flame obtained was more uniform and longer due to the delayed atomization, the spray 10 having a larger drop size than a spray issuing from a conventional burner while the modified spray 13 has a smaller drop size and better diluted and hence more uniformly distributed drops.

The more uniform flame thus obtained consequent reduces the temperature difference between the hot spots and the cold spots.

A significant reduction of NOx compound emissions by a

burner equipped with an atomization head 6 according to the invention has also been demonstrated. A reduction by a factor of between 1.2 and 1.5, depending on the oxidizer distribution selected, can be obtained for the same total atomizing gas flow rate. This reduction can be explained by the law of the reaction explained by the invention.

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As a variant, an atomization head 1, as shown in, Figure 1, differs from the atomization head 6 only in the fact that it comprises secondary ejection lines 14 obliquely oriented by an angle  $\alpha$  to the fuel flow direction. The angle  $\alpha$  is advantageously between 0 and  $60^\circ$ , preferably between 0 and  $30^\circ$ . These secondary ejection lines 14 deliver secondary atomizing gas stream 5 which, with the spray 10, form a modified spray 13 having a spray angle of  $2\alpha$ . Such an atomization head 1 is suitable for more accurate adjustment of the flame width.

Although the invention has only been described in connection with particular embodiments, it is quite obvious that it is not limited thereby and that it comprises all the technical equivalents of the means described and of their combinations if these fall within the scope of the invention.