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Title: Polyester containing filament material.

This invention relates to a process for the manufacture of a polyester comprising filament material suitable for surgical application, as such or in woven, braided or knitted form, as well as reinforcing beads. The invention further relates to a synthetic surgical material that is biocompatible with a patient and is biodegradable.

The invented process of spinning a polyester material in the presence of a certain additive can be used in the production of highly fibrillated sutures, which due to their fibrillation exhibit a good resorption rate and flexibility important for handling the suture and tying the knot.

Regular structurization at the fibre surface, created in the present spinningprocess, and preserved in the fibre even after hot-drawing, provides to the fibre a high knot strength.

There exist a number of commercial biocompatible and biodegradable sutures based on polyglycolide (Dexon), copolymer of lactide and glycolide (Vicryl), or lactone of hydroxyethyl glycolic acid (PDS). These well known materials are convenient to handle, and have the required rate of bioresorption. However there still exists a need for new biocompatible and biodegradable suture materials.

As follows from literature data, polylactide fibers have already been produced, but the rate of degradation of these fibers is too low as compared with that of Vicryl, Dexon or PDS sutures.

While Vicryl, Dexon and PDS sutures respectively disappear after about 90, 120 and 180 days from implantation, the polylactide sutures are not resorbed until after about 8 to 17 months from implantation.

Thus although polylactide is a biocompatible, biodegradable and fiberforming polymer, the polylactide sutures have not so far found practical application in surgery.

It is an object of the present invention to provide sutures with adequate tensile strength, high dimensional stability and a rate of

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hydrolysis comparable to those of Vicryl, Dexon or PDS sutures. It is another object of the present invention to provide fibers which have a flexibility higher than those produced according to the standard methods, yet having high tensile strength and modulus. It is a further object of the present invention to provide sutures having a knot strength higher than that of fibers produced by standard spinning procedures.

These and other objects are attained by filament material produced by dry- or wet-spinning a spinning mixture comprising a polyester material and an additive, particularly a polyurethane material. When wet-spinning a coagulant material is needed. Preferred polyester materials are poly (L-lactide), (PLLA), poly(dL-lactide) (PdLLA), and combinations thereof, having a viscosity-average molecular weight of at least about 3 x 10 5 and preferably above 5.0 x 10 5 Kg/kmol, as calculated according to the formule: [n] = 5.45 x 10 $^{-4}$ M $_{_{\rm V}}^{0.73}$, for a viscosity measured at 25 °C in trichlormethane.

Examples of additives other than the polyurathane material which can be used in preparing the filament material of this invention, are glycolide, lactide, camphor, benzoic acid-2-hydroxyacetate, hexamethylbenzene, 1,2-cyclohexandione and other low-molecular weight organic compounds which are preferably soluble in trichlormethane and/or dichlormethane and ethanol, and have a melting temperature in the range of 40 to 180°C.

Polyurethane is a preferred additive in the spinning mixture, and as such may be used a polyester urethane based on hexamethylene diisocyanate, 1,4-butanediol and a copolymer of lactic acid and ethylene glycol, diethylene glycol or tetramethylene glycol; hexamethylene diisocyanate, 2,4,6-tris(dimethylaminomethyl)phenol and copolymer of lactic acid and diethylene glycol, ethylene glycol, or tetramethylene glycol, a polyester urethane based on hexamethylene diisocyanate, trimethylol propane and a copolymer of polylactic acid and tetramethylene glycol or a polyester urethane based on 4,4'-diphenylmethane diisocyanate, 1,4-butanediol and polytetramethylene adipate. The concentration of the additive in the polylactide material may be in the range of 1 to 45 % by weight.

Filament material prepared from this kind of polylactide/ additive mixtures are formed by dry-spinning the polymer from a solution



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in a well dissolving material, in particular in dichloromethane and/or trichloromethane at room temperature through a spinneret. The filament material obtained is thereafter, according to a particularly preferred embodiment of the process according to the invention, subjected to a hot-drawing operation applying a drawing ratio within a wide range, particularly up to about 25.

The resulting oriented filaments are strong and owing to their regularly structurized surface form strong knots.

Owing to extensive fibrillation by virtue of using an additive, the fibres are flexible and easy to handle upon suturing or knotting and hydrolyse much faster than the standard polylactide fibers.

The invented fibers, such as the polylactide comprising fibers, exhibit very little shrinkage when heated at 37°C in water for 30 hours, namely, about 1 to 5 percent of their initial length. The invented spinning process avoids degradation of the polymer during extrusion, resulting in fibers of higher tensile strength.

It is recommendable that ethylene oxide is applied for sterilization of the fibers, for example polylactide comprising fibers, as high-energy radiation may result in crosslinking and chain scission and some decrease in tensile strength.

After sterilization with ethylene oxide, the sutures in sealed packages, are subjected to a vacuum of 10^{-4} Torr at 70°C for 1 hour. This avoids absorption of sterilizing gas in the sutures.

The filaments according to the present invention have a good tensile strength of at least 0.4GPa, preferably 0.7 GPA. Some have tensile strengths as high as 0.8 to 1.0 GPa. The invented fibers are resorbed as to 50% after about 150 days, which rate of hydrolysis is comparable to that of PDS fibers with comparable thickness and strength.

The filaments according to the invention, such as the polylactide comprising fibers, may be woven, braided, knitted or used as monofilaments of general surgical application, may be used as reinforcing beads for the construction of biodegradable tracheal or vascular prostheses, especially for by-pass systems. The polymeric material, in particular when being PLLA and/or PdLLA, which can be converted to filaments particularly by dry-spinning may be present in a spinning



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solution, and this in a concentration of 10 to 40% by weight in dichloromethane and/or trichloromethane, as these two solvents easily dissolve the polylactide with the above viscosity-average molecular weight of about 3 x 10^5 Kg/kmol at room temperature. Spinning polylactide fibers from a solution with a concentration in the range of 10 to 40 % by weight provides a monofilament of reasonable tensile strength, which is in addition regularly structurized due to the melt fracture as schematically shown in the accompanying drawing as obtained (drawing ratio λ = 0) and after hot-drawing at drawing ratios λ of 6, 10 and 20, respectively. Even hot-drawing at high draw ratios does not completely remove the surface structure but results in an extension of the pitch of the helix structure.

The diameter of the resulting fibre will generally be in the range of 0.3 to 1 x 10^{-4} m. Preferred monofilaments have a diameter of about 0.4 to 1 x 10^{-4} m.

Spinnerets having orifice sizes of 0.2 to 1 mm and a length of the capillary of 10 mm are suitable for spinning the monofilaments. In dry-spinning from dichlormethane or trichlormethane solutions, the solution is extruded at room temperature at which the solvent evaporates slowly. A preferred polymer concentration is 15-25, in particular about 20 % by weight.

The filament is extruded at a speed in the range of 0.02 to 2 mm/min. This gives no orientation to the fibre as spun. After spinning the polylactide fibers are hot-drawn at a temperature in the range of 45 to 200°C, preferably at 110, 170, 180 or 200°C, which temperature depends on the additive concentration in the polymer and the melting temperature of the additive.

The draw ratio λ may be up to 25, preferably 14 to 18. Take-up speed may be in the range of 0.2 to 1 cm.sec⁻¹ with a strain rate in the range of 10^{-3} sec.

The hot-drawing of fibers may be carried out in an electric tube-furnace with a length of 60 cm under a dry, oxygen-free atmosphere. Hot-drawing at temperatures above $120\,^{\circ}$ C may reduce the molecular weight of the starting polymer by 1-2 percent.

The filament can be colored by adding an inert material, e.g. Cosmetic Violet No. 2, to the solvent before preparation of the



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spinning solution.

The invention is illustrated in and by the following examples:

EXAMPLE I

Filaments with a regularly structurized surface and having a diameter of 0.44×10^{-4} m, a tensile strength of 1 GPa, a modulus of 12 GPa, a strength of square knot of 0.6 GPa and an elongation at break of 18 % were prepared by spinning poly (L-lactide) from a 20 wt % solution in trichloromethane at room temperature.

The poly(L-lactide) had a viscosity-average molecular weight of 6.0×10^5 . The fibre as spun was hot-drawn at 200° C to a draw ratio of 20.

EXAMPLE II

Filaments with a regularly structurized surface and having a diameter of 0.6×10^{-4} m, a tensile strength of 0.8 GPa, a modulus of 9 GPa, a strength of a square knot of 0.5 GPa and an elongation at break of 17% were prepared by spinning poly(L-lactide) which contained 10% by weight of camphor, from a 20 wt% solution in trichloromethane at room temperature. The poly(L-lactide) had a viscosity-average molecular weight of 6.0×10^{5} . The fibre was drawn at $180 \, ^{\circ}\text{C}$ to a draw ratio of 4.

After hot-drawing the filaments were extracted in ethanol for 4 hours. No additive was present in the fibre after extraction. The filaments obtained turned out to have a highly fibrillated structure. EXAMPLE III

diameter of 0.7 x 10⁻⁴m, a tensile strength of 0.65 GPa, a modulus of 8 GPa, a strength of a square knot of 0.45 GPa and an elongation at break of 19 % were prepared by spinning poly(L-lactide) containing 5 % by weight of polyester urethane from an 18 wt % solution in an hydrous trichlormethane. The poly(L-lactide) had a viscosity-average molecular weight of 4.0 x 10⁵. The fibre was drawn at 150°C to a draw ratio of 24. The poly(L-lactide)/polyester urethane monofilament so obtained has a highly fibrillated structure.

EXAMPLE IV

Highly fibrillated filaments having a diameter of 0.6×10^{-4} m, a tensile strength at break of 0.7 GPa were kept in water at 37° C for 10 to 200 days. After about 150 days the filaments were hydrolysed as



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to 50 %. This rate of hydrolysis is comparable to that of PDS filaments of similar strength and thickness.

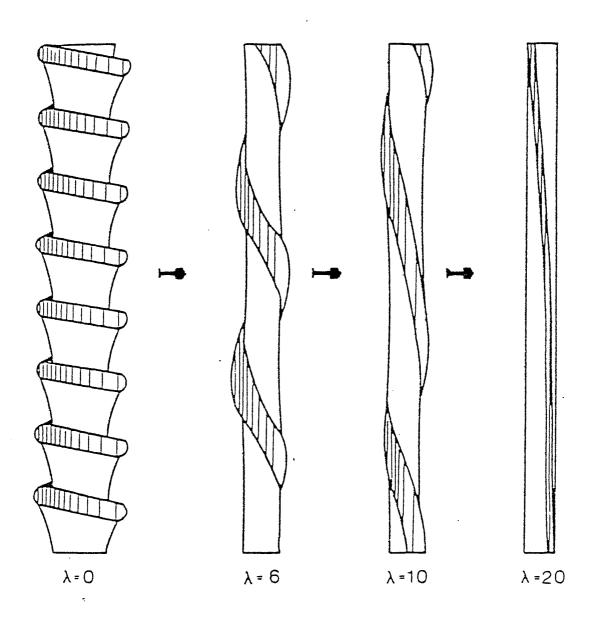


CLAIMS

- 1. A process for the manufacture of filament material by dryor wet-spinning a spinning mixture comprising a polyester material and an additive, particularly a polyurethane material.
- 2. A process according to claim 1, characterized in that the filament produced is subjected to a hot-drawing operation.
 - 3. A process according to claim 2, characterized in that the drawing operation is carried out applying a drawing ratio of up to about 25.
- 4. A process according to claim 1, characterized in that the

 filaments are prepared by dry-spinning, at room temperature, a solution
 of poly(L-lactide), PLLA, and/or poly(dL-lactide), PdLLA, in a
 concentration in the range of 5-70 % by weight in the presence of a
 biodegradable polyester urethane material.
- 5. A process according to claim 4, characterized in that the concentration is in the range of 10-40 % by weight, particularly about 20 % by weight.
 - 6. A process according to claims 4-5, characterized in that CHCL and/or ${\rm CH_2Cl_2}$ is used as the solvent material.
- 7. A process according to claims 1-6, characterized in that the additive material used is soluble in CHCl₃ and/or CH_2Cl_2 and/or $\text{C}_2\text{H}_5\text{OH}$ and has a melt temperature in the range of 40-180°C.
 - 8. A process according to claims 1-7, characterized in that the concentration of the additive material in the polylactide material is in the range of 1-45 % by weight.
- 9. Filament material produced by the process according to any of claims 1-8.







INTERNATIONAL SEARCH REPORT

International Application No PCT/NL 83/00028

	I. CLASSIFICATION OF SUBJECT MATTER (If several classification symbols apply, Indicate all) 3						
According to International Patent Classification (IPC) or to both National Classification and IPC							
IPC ³ : A 61 L 17/00; C 08 L 67/04; D 01 F 6/92							
II. FIELDS SEARCHED							
	Minimum Docun	nentation Searched 4					
Classificati	Classification System Classification Symbols						
IPC ³	0 4						
	Documentation Searched other to the Extent that such Document	er than Minimum Documentation nts are included in the Fields Searched ⁶					
III. DOCL	IMENTS CONSIDERED TO BE RELEVANT 14	17	Relevant to Claim No. 18				
Category *	Citation of Document, 16 with indication, where a	ppropriate, of the relevant passages 17	neterant to Claim 140. 44				
A	FR, A, 1461386 (DU F see abstract 2e	ONT) 9 December 1966	1				
,Λ,	FR, A, 1478694 (ETHI see page 6, line	CON) 28 April 1967 s 33-54	1				
A	FR, A, 2088548 (ETHI see page 14, lin		1				
A	FR, A, 2401185 (ETHI	CON) 23 March 1979					
A	FR, A, 2267748 (AMER 14 November 1975						
A	FR, A, 2440380 (F.E.	GOULD) 30 May 1980					
		UTU Jates decument sublished after the	s international filing date				
* Special categories of cited documents: 15 "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the claimed invention "X" document of particular relevance; the claimed invention cannot be considered to involve an inventive step document is combined with one or more other such documents, such combination being obvious to a person skilled in the art. "&" document member of the same patent family							
IV. CERTIFICATION Date of the Actual Completion of the International Search 2 Date of Mailing of this International Search Report 2							
Date of the Actual Completion of the International Search 3 10th October 1983 Date of Mailing of this International Search Report 3 0 8 NOV 1983							
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ANNEX TO THE INTERNATIONAL SEARCH REPORT ON

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This Annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the European Patent Office EDP file on 02/11/83

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Patent document cited in search report	Publication date	Patent family member(s)	Publication date
FR-A- 1461386		None	
FR-A- 1478694		NL-A- 6605197 BE-A- 679726 DE-A- 1642111 CH-A- 526963 GB-A- 1123445 SE-B- 353021	21/10/66 19/10/66 30/12/71 31/08/72 22/01/73
FR-A- 2088548	07/01/72	NL-A- 7103263 DE-A- 2062604 US-A- 3636956 US-A- 3797499 BE-A- 758156 CA-A- 982007 CH-A- 573752 SE-B- 361599	16/11/71 25/11/71 25/01/72 19/03/74 28/04/71 20/01/76 31/03/76 12/11/73
FR-A- 2401185	23/03/79	DE-A- 2827289 US-A- 4137921 US-A- 4157437 GB-A- 1595269 CA-A- 1124444	11/01/79 06/02/79 05/06/79 12/08/81 25/05/82
FR-A- 2267748	14/11/75	US-A- 3896802 NL-A- 7504655 BE-A- 828133 DE-A- 2515865 AU-A- 7899875 GB-A- 1476894 AT-B- 342214 JP-A- 50146181 AU-B- 498891 CA-A- 1059853 CH-A- 614123 SE-A- 7504547 SE-B- 411298 US-A- 3903882 CA-A- 1066579	29/07/75 21/10/75 20/10/75 30/10/75 16/09/76 16/06/77 28/03/78 22/11/75 29/03/79 07/08/79 15/11/79 23/12/75 17/12/79 09/09/75 20/11/79

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INTERNATIONAL APPLICATION NO. PCT/NL 83/00028 (SA 5480)

FR-A- 2440380	30/05/80	DE-A- US-A- US-A- JP-A- GB-A- GB-A-	2827450 4156066 4156067 54010398 1605079 1605080	11/01/79 22/05/79 22/05/79 25/01/79 16/12/81 16/12/81

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