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(54) **PROCESS FOR PREPARING A SOLUTION OF LIGNIN IN AN AQUEOUS MEDIUM**

VERFAHREN ZUR HERSTELLUNG EINER LIGNINLÖSUNG IN EINEM WÄSSRIGEN MEDIUM

PROCÉDÉ DE PRÉPARATION D'UNE SOLUTION DE LIGNINE DANS UN MILIEU AQUEUX

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- **DATABASE WPI Week 201329 Thomson Scientific, London, GB; AN 2013-E84666 XP002807340, & CN 102 848 443 A (ZHEJIANG ANJI DOUBLE TIGER BAMBOO & WOOD) 2 January 2013 (2013-01-02) & CN 102 848 443 B (ZHEJIANG ANJI DOUBLE TIGER BAMBOO & WOOD INDUSTRY CO LTD) 22 October 2014 (2014-10-22)**
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**EP 3 887 474 B1**

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## Description

### Field of the invention

[0001] The present invention relates to a process for lignin dissolution in which partial methylation of lignin is carried out during the step of preparing a solution of lignin in an aqueous medium comprising alkali and phenol.

[0002] The lignin prepared according to the process of the present invention can be used to manufacture lignin-based phenolic resins, which are particularly useful for example in the manufacture of laminates, plywood, laminated veneer lumber and oriented strand board.

### Background

[0003] Lignin, an aromatic polymer is a major constituent in e.g. wood, being the most abundant carbon source on Earth second only to cellulose. In recent years, with development and commercialization of technologies to extract lignin in a highly purified, solid and particularized form from the pulp-making process, it has attracted significant attention as a possible renewable substitute to primarily aromatic chemical precursors currently sourced from the petrochemical industry.

[0004] Lignin, being a polyaromatic network has been extensively investigated as a suitable substitute for phenol during production of phenol-formaldehyde adhesives. These are used during manufacturing of structural wood products such as plywood, oriented strand board and fiberboard. During synthesis of such adhesives, phenol, partially replaced by lignin, is reacted with formaldehyde in the presence of either basic or acidic catalyst to form a highly cross-linked aromatic resins termed novolacs (when utilizing acidic catalysts) or resoles (when utilizing basic catalysts). Currently, only limited amounts of the phenol can be replaced by lignin due to the lower reactivity of lignin. Lignin may be utilized as a powder at the time that it is incorporated into the resin formulation. Lignin can also be utilized in "liquid form" in an alkali solution in order to avoid lignin dust. If the moisture content of the powder lignin is relatively low (0-5%), it can be dusty and may create respiratory hazards. If the moisture content of the solids is relatively high (8-50%), it can be sticky or lumpy and difficult to transfer in reliable and quantitative manner.

[0005] One problem when preparing resins comprising lignin is to ensure that the inherent reactivity of the lignin is fully utilized by adequately dissolving it in a suitable liquid medium.

[0006] US4113675 is directed to a highly cross-linkable methylolated kraft lignin resin for use as a high wet strength adhesive.

[0007] Malutan et al. (2008), BioResources 3(1), 13-20, is directed to hydroxymethylation of lignin and aims at determining reaction conditions to improve the reactivity of lignin by fully methylating lignin.

[0008] CN104087219A discloses the preamble of claim 1.

[0009] There is a need to facilitate the process for preparing a solution of lignin in an aqueous medium, particularly for preparation of resins.

### Summary of the invention

[0010] It has now surprisingly been found that the solubility of lignin can be increased by partial methylation during the step of preparing a solution of lignin in an aqueous medium comprising phenol.

[0011] The present invention is thus directed to a method for dissolving lignin in an aqueous medium according to claim 1.

[0012] Preferably, the method for dissolving lignin in an aqueous medium comprises the steps of

- a) mixing lignin, alkali, phenol and formaldehyde in an aqueous medium;
- b) mixing until a solution of lignin in the aqueous medium has been obtained;

wherein the molar ratio between the formaldehyde and total amount of phenol and lignin monomer is 0.2 or less.

[0013] More preferably, the method for dissolving lignin in an aqueous medium comprises the steps of

- a) mixing lignin, alkali, phenol and formaldehyde in an aqueous medium;
- b) mixing until a solution of lignin in the aqueous medium has been obtained;

wherein the molar ratio between the formaldehyde and total amount of phenol and lignin monomer is 0.1 or less and in that the lignin has been isolated and/or purified before step a).

[0014] The lignin has been isolated from black liquor and purified before step a).

[0015] The present disclosure is also directed to a method for preparing a resin, comprising the steps of

- a) mixing lignin, alkali, phenol and formaldehyde in an aqueous medium;
- b) mixing until a solution of lignin in the aqueous medium has been obtained;
- c) keeping the mixture obtained in step b) at a temperature in the range of from 30°C to 95°C; and
- d) adding additional formaldehyde and phenol and maintaining the mixture at a temperature of from 30°C to 95°C for at least 30 minutes; wherein the molar ratio between the formaldehyde and total amount of phenol and lignin monomer in step a) is 0.4 or less.

[0016] The present disclosure is thus also directed to resins and the use of said resins in the manufacture of laminates, plywood, oriented strand board (OSB), laminated veneer lumber (LVL), insulation and other engi-

neered wood products. The present disclosure is also directed to such laminates and engineered wood products manufactured using said resins.

**[0017]** The present disclosure is also directed to a method for increasing the solubility of lignin in an aqueous medium comprising the steps of

- a) mixing lignin, alkali, phenol and formaldehyde in an aqueous medium;
- b) mixing until a solution of lignin in the aqueous medium has been obtained; wherein the molar ratio between the formaldehyde and lignin monomer is 0.4 or less.

### Detailed description

**[0018]** It is intended throughout the present description that the expression "lignin" embraces any kind of lignin, e.g. lignin originated from hardwood, softwood or annular plants. Preferably the lignin is an alkaline lignin generated in e.g. the Kraft process. The lignin has been purified and isolated before being used in the process according to the present invention. The lignin is isolated from black liquor and further purified before being used in the process according to the present invention. The purification is typically such that the purity of the lignin is at least 90%, preferably at least 95%, more preferably at least 97%, by dry weight. Thus, the lignin used according to the method of the present invention preferably contains less than 10%, preferably less than 5%, more preferably less than 3% impurities, by dry weight. The lignin may be separated from the black liquor by using the process disclosed in WO2006031175.

**[0019]** In one embodiment of the invention, an amount of alkali is added to the aqueous medium so that the aqueous medium comprises 1-30 wt% alkali, such as 1-20 wt% alkali, such as 1-15 wt% alkali. In one embodiment of the present invention the pH of the aqueous medium is at least pH 7, such as at least pH 8, such as at least pH 10 or at least pH 12 or at least pH 13.

**[0020]** The alkali is preferably sodium hydroxide, potassium hydroxide, calcium hydroxide, magnesium hydroxide or a mixture thereof.

**[0021]** In one embodiment of the present invention, the molar ratio between formaldehyde and total amount of phenol and lignin monomer in step a) is 0.4 or less, such as 0.35 or less or 0.30 or less or 0.25 or less or 0.20 or 0.15 or 0.10 or 0.08 or 0.06 or less. In one embodiment of the present invention the ratio between formaldehyde and total amount of phenol and lignin monomer in step a) is at least 0.01, such as at least 0.02 or at least 0.05. The molar ratio between formaldehyde and total amount of phenol and lignin monomer is calculated based on an average lignin monomer molecular weight of 190 g/mol.

**[0022]** The duration of step c) of the process described above is typically at least 5 minutes, such as at least 15 minutes or at least 30 minutes. The temperature used in step c) is in the range of 30-95°C, such as 40-80°C.

**[0023]** The mixing of lignin, alkali, phenol and formaldehyde in step a) can be carried out in any order. Each component may for example be added consecutively or at the same time as one or two of the other components. In one embodiment, the components are added in such a way that a part of the total amount of each component is added and one or more additional amounts of each component is subsequently added. In one embodiment, the alkali is added last, i.e. after addition of lignin, phenol and formaldehyde.

**[0024]** It is preferred that the solution in step b) comprises 5-50 wt%, such as 5-40 wt% lignin.

**[0025]** In one embodiment of the present invention, the mixing in step b) is carried out at room temperature, such as at a temperature of from 15°C to 25°C. In one embodiment of the present invention, the mixing in step b) is carried out at elevated temperature, such as from 25°C to 95°C, such as from 30°C to 80°C or from 50°C to 95°C.

**[0026]** The present disclosure also relates to a resin composition. The resin composition is preferably a lignin-phenol-formaldehyde resin. Said resin composition can be prepared by adding additional formaldehyde and optionally additional phenol to the solution described above and heating said mixture. The temperature at the time of adding additional formaldehyde and optionally additional phenol is typically in the range of from 40°C to 60°C, such as about 50°C. Typically, the total amount of lignin is approximately from 20% of the amount of phenol to the same as the amount of phenol, but it is appreciated that more or less phenol can be added depending on what type of resin composition is desired. The heating described in step d) is typically carried out at a temperature of 70-85°C for at least 30 minutes and typically for 4-8 hours. Typically, the viscosity increases during the heating in step d). Optionally, urea can also be added to the resin composition. The amount of urea is preferably 1-30 weight-% of the resin.

**[0027]** The resin obtained is useful for example in the manufacture of laminates. The resin is then impregnated into and/or applied between the sheets that should form the laminate and said sheets are pressed together and heated at a temperature of about 130-150 °C.

**[0028]** There are a number of advantages of the process described above, including:

- increased solubility of lignin in the aqueous medium
- shorter gel time / B time of a resin obtained using lignin that has been subjected to the process according to the present invention.

**[0029]** The present disclosure also relates to the use of the resin composition in engineered wood products such as plywood, particle board, wafer board, gluelam beams, structural composite lumber, oriented strand board (OSB), oriented strand lumber (OSL), laminated veneer lumber (LVL) and other applications such as laminates, insulation and molding compounds.

## Examples

Example 1:

**[0030]** Lignin based phenolic resin was prepared with a phenol replacement level of 25% with lignin for laminate application.

**[0031]** A liquid lignin composition was prepared by mixing 129.3 g of kraft lignin (solid content 97%), 380 g of phenol, 31.5 g of formalin (52.5%), 130 g of water and 42.7 g of 50% sodium hydroxide solution at room temperature in a 1 liter glass reactor equipped with overhead stirrer, condenser and temperature control unit. The composition was stirred for 10 minutes. The temperature of the mixture increase to 70 °C and the reaction mixture was stirred for 1 hour and the temperature of the lignin solution was decreased to 49°C.

**[0032]** In the next step, 372.5 g of formalin (concentration 52.5%) and 44.8 g of water were added to the reaction mixture. The temperature of the reaction mixture was increased to 85 °C and the reaction was continued for 30 minutes. The temperature was decreased to 75°C and the reaction was continued for further 20 minutes before cooling down to the room temperature. The reaction was monitored by measuring the viscosity at 25 °C using a Brookfield DV-II + LV viscometer.

**[0033]** The resin was analyzed and the results of the analysis are given in Table 1.

**Table 1**

Resin Properties	
Viscosity at 25°C (cP)	113
S.C (%)	57.7
pH at 23 °C	9.0
B Time (min) @130°C	5 min 44 sec

**[0034]** In view of the above detailed description of the present invention, which is defined in the appended claims, other modifications and variations will become apparent to those skilled in the art.

## Claims

1. A method for dissolving lignin in an aqueous medium comprising the steps of

- mixing lignin, alkali, phenol and formaldehyde in an aqueous medium;
- mixing until a solution of lignin in the aqueous medium has been obtained;

**characterized in that** the molar ratio between the formaldehyde and the total amount of phenol and lignin monomer is 0.4 or less, wherein the molar ratio

between formaldehyde and total amount of phenol and lignin monomer is calculated based on an average lignin monomer molecular weight of 190 g/mol and wherein the lignin has been isolated from black liquor and purified before step a).

- A method according to claim 1, wherein the molar ratio between the formaldehyde and the total amount of phenol and lignin monomer is in the range of from 0.01 to 0.3.
- A method according to claim 2, wherein the molar ratio between the formaldehyde and the total amount of phenol and lignin monomer is in the range of from 0.01 to 0.2.
- A method according to claim 3, wherein the molar ratio between the formaldehyde and the total amount of phenol and lignin monomer is in the range of from 0.01 to 0.1.
- A method according to any one of claims 1-4, wherein the alkali is sodium hydroxide, potassium hydroxide, calcium hydroxide, magnesium hydroxide or a mixture thereof.

## Patentansprüche

1. Verfahren zum Auflösen von Lignin in einem wässrigen Medium, umfassend die Schritte des

- Mischens von Lignin, Alkali, Phenol und Formaldehyd in einem wässrigen Medium;
- Mischens, bis eine Lösung von Lignin in dem wässrigen Medium erhalten wird;

**dadurch gekennzeichnet, dass** das Molverhältnis zwischen dem Formaldehyd und der Gesamtmenge an Phenol und Ligninmonomer 0,4 oder weniger beträgt, wobei das Molverhältnis zwischen Formaldehyd und der Gesamtmenge an Phenol und Ligninmonomer basierend auf einem durchschnittlichen Molekulargewicht des Ligninmonomers von 190 g/mol berechnet wird und wobei das Lignin vor Schritt a) aus Schwarzlauge isoliert und gereinigt wurde.

- Verfahren nach Anspruch 1, wobei das Molverhältnis zwischen dem Formaldehyd und der Gesamtmenge an Phenol und Ligninmonomer im Bereich von 0,01 bis 0,3 liegt.
- Verfahren nach Anspruch 2, wobei das Molverhältnis zwischen dem Formaldehyd und der Gesamtmenge an Phenol und Ligninmonomer im Bereich von 0,01 bis 0,2 liegt.

4. Verfahren nach Anspruch 3, wobei das Molverhältnis zwischen dem Formaldehyd und der Gesamtmenge an Phenol und Ligninmonomer im Bereich von 0,01 bis 0,1 liegt. 5
5. Verfahren nach einem der Ansprüche 1-4, wobei das Alkali Natriumhydroxid, Kaliumhydroxid, Calciumhydroxid, Magnesiumhydroxid oder ein Gemisch davon ist. 10

### Revendications

1. Procédé de dissolution de lignine dans un milieu aqueux comprenant les étapes de 15
- a) mélange de lignine, d'alcali, de phénol et de formaldéhyde dans un milieu aqueux ;
- b) mélange jusqu'à obtention d'une solution de lignine dans le milieu aqueux ; 20
- caractérisé en ce que** le rapport molaire entre le formaldéhyde et la quantité totale de phénol et de monomère de lignine est de 0,4 ou moins, dans lequel le rapport molaire entre le formaldéhyde et la 25
- quantité totale de phénol et de monomère de lignine est calculé sur la base d'un poids moléculaire moyen de monomère de lignine de 190 g/mol et dans lequel la lignine a été isolée à partir de liqueur noire et purifiée avant l'étape a). 30
2. Procédé selon la revendication 1, dans lequel le rapport molaire entre le formaldéhyde et la quantité totale de phénol et de monomère de lignine est dans la plage de 0,01 à 0,3. 35
3. Procédé selon la revendication 2, dans lequel le rapport molaire entre le formaldéhyde et la quantité totale de phénol et de monomère de lignine est dans la plage de 0,01 à 0,2. 40
4. Procédé selon la revendication 3, dans lequel le rapport molaire entre le formaldéhyde et la quantité totale de phénol et de monomère de lignine est dans la plage de 0,01 à 0,1. 45
5. Procédé selon l'une quelconque des revendications 1 à 4, dans lequel l'alcali est l'hydroxyde de sodium, l'hydroxyde de potassium, l'hydroxyde de calcium, l'hydroxyde de magnésium ou un mélange de ceux-ci. 50

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**REFERENCES CITED IN THE DESCRIPTION**

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