

- [54] **METHOD FOR INJECTION MOLDING A FOAMED THERMOPLASTIC POLYMER ARTICLE SUBSTANTIALLY FREE FROM SWIRL-PATTERNS IN ITS SURFACE**
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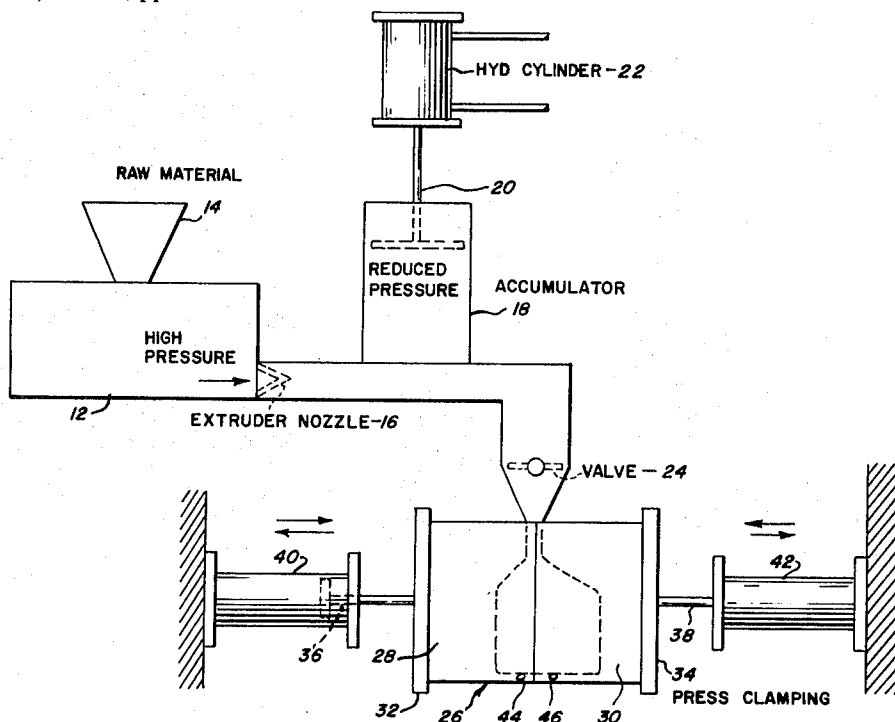
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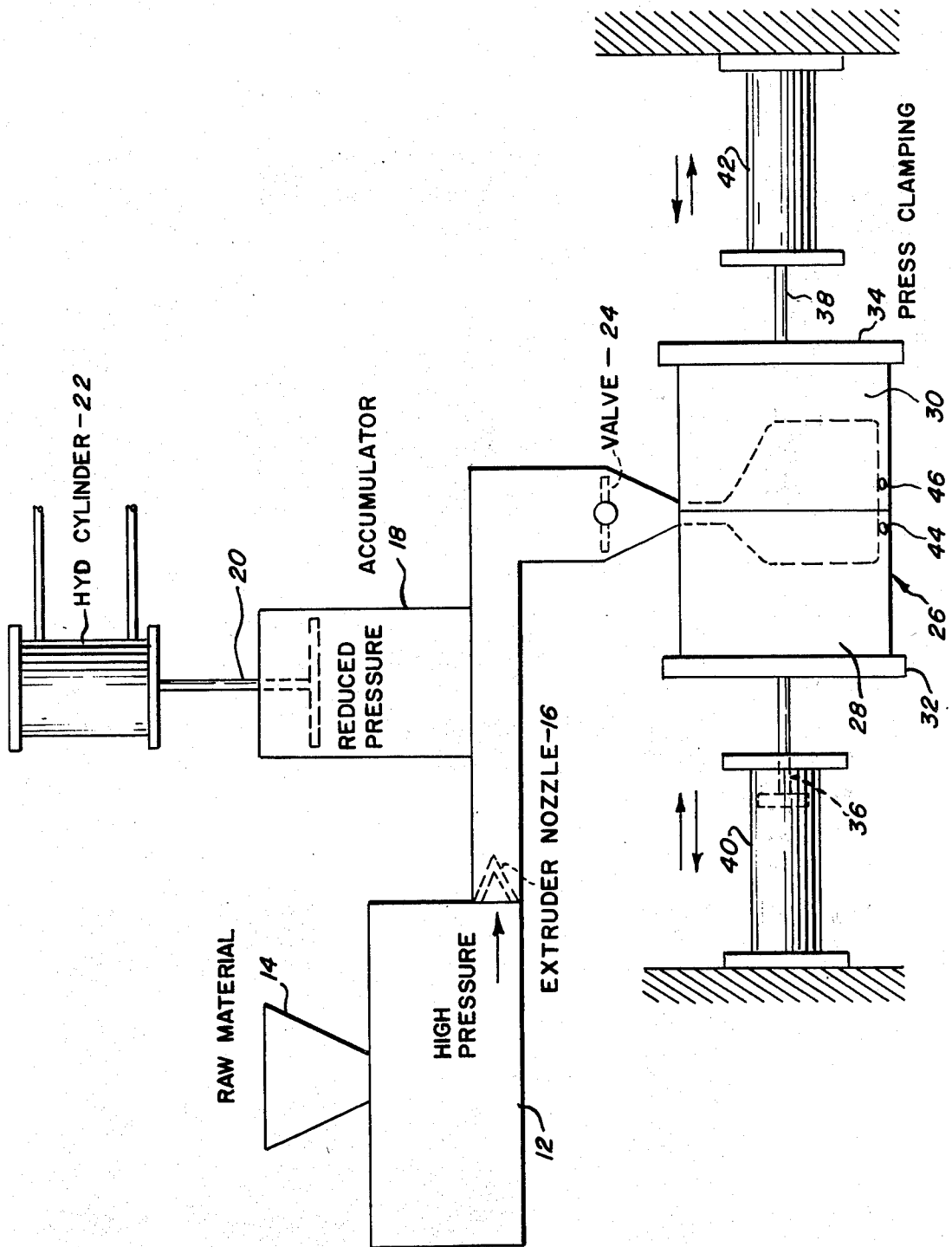
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[57] **ABSTRACT**
 A method for producing an improved molded thermoplastic polymeric resinous article comprising: introducing a heat plastified thermoplastic polymeric resinous material into a mold in the presence of a finely divided inorganic material; cooling the heat plastified thermoplastic polymeric resinous material; removing from the mold the cooled mold-shaped thermoplastic polymeric resinous article having finely divided inorganic material incorporated therein.

6 Claims, 1 Drawing Figure





METHOD FOR INJECTION MOLDING A FOAMED THERMOPLASTIC POLYMER ARTICLE SUBSTANTIALLY FREE FROM SWIRL-PATTERNS IN ITS SURFACE

This is a continuation-in-part of Ser. No. 149,022, filed June 1, 1971 and now abandoned.

BACKGROUND

Plastic has been used as a material of construction for various articles. Perhaps one of the more recent applications for plastic is its use as a material of construction for furniture and the like. It has been found that plastic can be molded to have a grained surface which is imperceptively different from that of wood. Generally for these applications the plastic is foamed rather than solid. A method of injection molding foamed plastics to produce fabricated articles is disclosed in U.S. Pat. No. 3,268,636, entitled "Method and Apparatus for Injection Molding Foamed Plastic Articles", issued Aug. 23, 1966. That patent teaches a process for molding foamed thermoplastic articles which includes the steps of mixing a blowing agent and a thermoplastic material, maintaining at a temperature at least equal to the melting temperature of the thermoplastic material, and a pressure and temperature above the pressure and temperature at which the mixture foams. A mold which is maintained at a pressure below the pressure at which the mixture foams is rapidly filled with the mixture which then foams and expands and fills out the mold.

Two problems have arisen in using foamed plastics as materials of construction for various molded articles. The first of these problems is that when plastics are molded, especially foamed plastics, there results a swirl-pattern in the surface of the finished article. Frequently when the finished article is furniture the swirl-pattern is noticeable in spite of the fact that the article is molded to have a grained surface.

The second problem is present when foamed articles are being produced by injection molding. More specifically, when a heat plastified plastic material which is being foamed by an active foaming agent is injected into a mold, a surface skin is formed by virtue of the fact that the heat plastified material contacts the mold walls which are below the heat plastifying temperature of the thermoplastic resin. However, after the mold has filled and the surface skin has formed, the foaming agent in the thicker uncooled section continues to produce gas. Concomitant with this continued gas production, small cells already formed migrate toward each other and combine to form larger cells. The end result, quite frequently, is that large voids are formed internally in the foamed article. These large voids are undesirable for two reasons. The first reason is that they frequently occur too close to the skin surface of the foamed article, and thus the skin surface is easily punctured. The second reason is that the voids substantially reduce the strength of the foamed article.

The invention of this disclosure allows the production of polymeric resinous articles, especially foamed polymeric thermoplastic articles which are substantially free of swirl-patterns in their surface as well as substantially free of large voids within the articles themselves.

SUMMARY OF THE INVENTION

A method for producing an improved molded thermoplastic polymeric resinous article comprising: intro-

ducing a heat plastified thermoplastic polymeric resinous material into a mold in the presence of a finely divided inorganic material; cooling the heat plastified thermoplastic polymeric resinous material; removing from the mold the cooled mold shaped thermoplastic polymeric resinous material having finely divided inorganic material incorporated therein.

The invention of this disclosure has been found to be effective in substantially reducing swirl-patterns in the surface of polymeric resinous articles, especially injection molded foamed polymeric resinous articles. In addition, the invention of this disclosure was found to be effective in promoting a more uniform cell size in injection molded foamed polymeric resinous articles.

BRIEF DESCRIPTION OF THE DRAWING

The FIGURE represents one form of injection molding apparatus.

A screw extruder 12 having a hopper 14 communicates, with or without valving, through extruder nozzle 16 with an accumulator 18 equipped with a hydraulic cylinder 22 and piston 20. The accumulator 18 communicates through valve 24 with split injection mold 26 composed of mold halves 28 and 30 which are attached to press clamping platens 32 and 34. The platens are moved in the direction of the arrows with the aid of pistons 36 and 38 operating in hydraulic cylinders 40 and 42 to open and close the mold halves 28 and 30. The mold 26 also has conventional vents 44 and 46 which aid in the removal of the gases released by the breaking of bubbles adjacent to the mold walls.

PREFERRED EMBODIMENTS

The invention of this disclosure, in its most preferred form, includes injecting a heat plastified thermoplastic polymeric resinous material into a mold in the presence of a finely divided inorganic material.

Thermoplastic polymeric resinous materials include chlorinated rubber, cellulose ethers and esters, e.g., ethyl cellulose, cellulose acetate, cellulose acetate-butyrate, homopolymers and interpolymers of monomeric compounds containing the $\text{CH}_2=\text{C}$ grouping, such as olefins, e.g. ethylene, propylene, isobutylene, butene-1, vinyl halides, e.g., vinyl chloride and vinyl fluoride, vinylidene chloride; vinyl esters of carboxylic acids, e.g., vinyl acetate, vinyl stearate, vinyl benzoate, vinyl ethers, e.g., vinyl methyl ether, vinyl ethyl ether, vinyl isobutyl ether; chlorotrifluoroethylene, hexafluoropropylene, unsaturated carboxylic acids and derivatives thereof, e.g., acrylic acid, methacrylic acid, methyl acrylate, methyl alpha chloracrylate, methyl methacrylate, acrylamide, acrylonitrile, methacrylonitrile, and interpolymers of the above-mentioned vinylidene monomers with alpha, beta-unsaturated polycarboxylic acids and derivatives thereof, e.g. maleic anhydride, diethyl maleate, dibutyl fumarate, diallyl maleate, dipropyl maleate, polyolefin, monopolymers, copolymers and terpolymers, etc. A preferred class of materials with which optimum results are obtained are rigid, relatively nonelastic, thermoplastic polymeric resinous materials such as homopolymers and interpolymers of vinyl chloride, e.g., polyvinyl chloride, vinyl chloride-vinyl acetate copolymer (87:13), vinyl chloride, acrylonitrile copolymer (80:20); homopolymers of vinylidene aromatic hydrocarbons and ring halogenated derivatives thereof, e.g. styrene, o-chlorostyrene, p-chlorostyrene, 2,5-dichlorostyrene, 2,4-dichlorostyrene, p-methylstyrene, p-ethylstyrene,

alphanaphthylstyrene, vinyl naphthalene and interpolymers of such vinylidene monomers with each other and with other vinylidene monomers in which the interpolymers contain at least 70% of the vinylidene aromatic hydrocarbon compound, e.g., a copolymer of 70% styrene and 30% acrylonitrile. As previously indicated, for many uses the most preferred resins are thermoplastic styrene polymers containing at least 70% by weight styrene in the structure.

Additional suitable thermoplastic resins include polycarbonates, e.g., the polymer from bisphenol A and diphenyl carbonate; polyoxymethylene (Delrin), oxymethylene-alkylene oxide copolymers, e.g., oxymethylene-ethylene oxide (95:5); or glycerine-propylene adduct molecular weight 3000 or butanediol 1,4-adipic acid polyester; Dacron (polyethylene terephthalate), nylon (e.g., polymeric hexamethylene adipamide), ABS terpolymers can be used, e.g., the terpolymer of 25% butadiene, 15% acrylonitrile and 60% styrene (a rigid ABS terpolymer), as well as other terpolymers containing 25 to 60% butadiene, 10 to 20% acrylonitrile, and 20 to 60% styrene.

The present invention is of particular value in preparing foamed articles from polyethylene (of high density, e.g., 0.960, medium density, e.g., 0.935 or low density, e.g., 0.914), polypropylene, copolymers of ethylene and propylene (e.g., 50:50 copolymer, 60:40 copolymer and 20:80 copolymer), regular or high impact polystyrene, acrylonitrile-butadiene-styrene terpolymer, polyvinyl chloride (preferably rigid polyvinyl chloride), copolymers of ethylene with minor amounts of alpha olefins having 4 to 10 carbon atoms such as butene-1 (e.g., 90:10 and 97.5:2.5) or octene-1 (96:4); terpolymers of ethylene, propylene and up to 5% of a nonconjugated polyolefin such as pentadiene-1,4 and dicyclopentadiene, e.g., a terpolymer of 60% ethylene, 39% propylene and 1% dicyclopentadiene or pentadiene-1,4.

There can also be prepared foamed articles from fluorocarbon polymers such as, polyhexafluoropropylene and tetrafluoroethylene-hexafluoro-propylene copolymers (e.g., 50:50).

When employing polystyrene there can be employed normal crystal grade polystyrene or high impact polystyrene or a mixture containing 5 to 95% normal crystal grade polystyrene and the balance high impact polystyrenes. When employing a thermoplastic styrene polymer it normally contains greater than 50% by weight of styrene and preferably at least 70% by weight of styrene in its structure. Preferably, the polystyrene is at least 10% high impact polystyrene. High impact polystyrenes are frequently prepared by polymerizing monomeric styrene in the presence of 2 to 15% by weight of a rubbery diene polymer or by polymerizing styrene in the presence of such amounts of a difunctional material. Examples of high impact styrene include a terpolymer of 5% acrylonitrile, 5% butadiene and 90% styrene; a copolymer of 5% butadiene and 95% styrene; the product made by polymerizing 95% of styrene in the presence of 5% polybutadiene; a copolymer of 5% chlorosulfonated polyethylene and 95% styrene; a blend of 97.5% polystyrene and 2.5% polybutadiene; a blend of 95% polystyrene and 5% hydrogenated polybutadiene containing 35.4% residual unsaturation; polystyrene formed in the presence of 5% hydrogenated polybutadiene containing 4.5% of residual unsaturation, a blend of 95% polystyrene and 5% polyisoprene, a blend of 98% polystyrene with 2% rubbery butadiene-

styrene copolymer, a blend of 85% polystyrene with 15% rubbery butadiene-styrene copolymer, and a copolymer of 99.5% styrene with 0.5% divinyl benzene.

Unless otherwise indicated, all parts and percentages are by weight.

Generally, before it is heat plastified, the thermoplastic polymeric resinous material is in pellet form. The finely divided inorganic material is preferably mixed with such pellets in a drum type blender. Usually such mixing is done dry and without the use of an amordant. The mixture of finely divided inorganic material and thermoplastic polymeric resinous material pellets is then heat plastified and injected into a mold under typical operating conditions.

In the most preferred method of operating, a foaming agent is employed in conjunction with the finely divided inorganic material to obtain a foamed thermoplastic polymeric resinous material. The foaming agent may be a volatile liquid adsorbed on an adsorbent. As the adsorbent there can be employed any conventional adsorbent in finely divided form, such as silica gel, e.g., Cab-O-Sil, and Hi-Sil, activated alumina, and activated carbon. The adsorbent is usually used in an amount of 0.1 to 15%, preferably 0.5 to 10% by weight of the polymeric resinous material, although up to 25 or 30% of adsorbent can be employed. The adsorbent is an inert filler of large surface area but small particle size, e.g., 200 mesh or below.

As the volatile liquid there can be used aliphatic hydrocarbons boiling between 10° and 150°C. and preferably between 30° and 90°C., e.g., petroleum ether (containing primarily pentane or hexane or a mixture of these hydrocarbons), pentane, hexane, isopentane, heptane, cyclohexane, cyclopentane, pentadiene and neopentane. Other volatile liquids include methanol, ethanol, methyl acetate, ethyl acetate, butane, acetone, methyl formate, ethyl formate, dichloroethylene, trichloromonofluoromethane, perchloroethylene, dichlorotetrafluoroethane, isopropyl chloride, carbon tetrachloride, monochlorotrifluoroethylene, propionaldehyde, diisopropyl ether, dichloro-difluoromethane, a mixture of pentane with 5 to 30% of methylene chloride or other volatile lower halogenated hydrocarbon.

The amount of volatile liquid adsorbed on the adsorbent can vary from 5 to 150% or more based on the weight of the adsorbent. The amount of liquid adsorbed will depend upon the capacity of the adsorbent for the particular liquid. Normally, the adsorbent containing the volatile liquid will appear to be a dry powder. The volatile liquid employed should be one which is nonreactive with the particular polymeric resinous material to be expanded. The amount of volatile liquid will depend upon the extent of foaming desired. In general, the greater the amount of adsorbed volatile liquid in the polymer adsorbent mixture the more the expansion. It has been found that good expansion can be obtained using very small amounts of the volatile liquid.

Instead of adsorbing the volatile liquid on a filler, there can be employed conventional expansible thermoplastic materials such as expansible polystyrene containing 1 to 9% of one of the volatile liquids, e.g., Dow Pelespan 101 expansible polystyrene beads containing 6% pentane).

Various suitable chemical foaming or blowing agents and their gas release (i.e. decomposition) temperatures are set forth in the following table:

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TABLE

Foaming agent:	Gas release temperature, °C.
Azobisisobutyronitrile	115
N,N'-dimethyl-N,N'-dinitrosoterephthal- amide	105
p,p'-Oxybis(benzenesulfonyl hydrazide)	150
Dinitrosopentamethylenetetramine	185
Azodicarbonamide	200
Sodium bicarbonate citric acid (4:3)	140
Urea-biuret (33:67)	135
Diazoaminobenzene	100
1,6-di-n-decyl azobisformamide	145
1,6-di-phenyl azobisformamide	176
Diphenyl 4,4'-di(sulfonyl azide)	145
p,p'-Oxybis(N-nitroso-N-methyl benzenesulfonamide)	130
Tetramethylene dinitrosodimethyl urethane	125
p,p'-Oxybis(benzenesulfonyl semicarbazide)	210
Benzene sulfonic acid hydrazide	104
B-naphthalene sulfonic acid hydrazide	138
Diphenyl sulfone-3,3'-disulfonyl hydrazide	150
Benzene 1,3-disulfonic acid dihydrazide	145
Benzene sulfonic acid N-phenyl hydrazide	146
95% sodium bicarbonate and 5% melamine	140
Barium azodicarboxylate	250

Additionally there can be used materials such as trihydrazine-triazine, sodium bicarbonate, benzene sulfonyl hydrazine, ammonium carbonate, ammonium bicarbonate and potassium bicarbonate.

Also in forming a foamed thermoplastic polymeric resinous material, there is preferably utilized a nucleating agent, e.g., in an amount of from 0.02 to 10%, preferably 0.4 to 5% of the weight of the polymer.

Conventionally, the nucleating agents are made up of two materials which react to form carbon dioxide and water. The two materials are normally used in approximately equivalent amounts. As the carbon dioxide liberating materials there can be used ammonium, alkali and alkaline earth carbonates or bicarbonates, e.g., ammonium bicarbonate, sodium bicarbonate, sodium carbonate, potassium bicarbonate, calcium carbonate. The other material is an acid or acid-reacting salt, preferably solid, which is sufficiently strong to liberate the carbon dioxide from the carbonate or bicarbonate. Generally, the acid has at least 3.0 milliequivalents of acidic hydrogen, and preferably at least 10.0 milliequivalents, per gram. The acid can be organic or inorganic. Suitable acidic materials include boric acid, sodium dihydrogen phosphate, fumaric acid, malonic acid, oxalic acid, citric acid, tartaric acid, potassium acid tartrate, chloroacetic acid, maleic acid, succinic acid, glutaric acid and phthalic acid. In place of the anhydrous acids or salts there can be used the solid hydrates, e.g., oxalic acid hydrate and citric acid monohydrate.

While not essential, there can also be added a wetting agent such as Bayol 35 (a petroleum aliphatic hydrocarbon white oil), kerosene having an average of at least 8 carbon atoms in the molecule, alkylphenoalkene oxide adducts, e.g., Triton X-100 (t-octylphenol-ethylene oxide adduct having 10 ethylene oxide units in the molecule), sodium lauryl sulfate and sodium dodecylbenzene sulfonate. The wetting agent can be non-ionic or anionic.

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One mode of incorporating the foaming agent and the nucleating agent into the polymeric resinous material is by premixing the pelletized, solid, thermoplastic polymeric resinous material, e.g., high impact styrene polymer, with a minor amount of the nucleating agent and a minor amount of the adsorbent having adsorbed thereon a volatile liquid (i.e., the foaming agent) which is nonreactive with and which has not more than a slight solvent action on the polymer. The volatile liquid should volatilize below the softening point of the polymer.

Generally, the concentration of finely divided inorganic material is found to be effective in the range of between about 0.001 to about 50% based upon the total weight of finely divided inorganic material and polymeric resinous material. The preferred concentration of finely divided inorganic material was found to be in the range of between 1.0 to about 10% based upon the total weight of finely divided inorganic material and polymeric resinous material. The most preferred concentration was about 5.0 to about 10.0% finely divided inorganic material based upon the weight of finely divided inorganic material and polymeric resinous material.

The term "finely divided" as used herein is intended to mean particles of a size which will pass through a 10 mesh sieve. However, preferred for this invention is a finely divided inorganic material which will pass through a 60 mesh sieve, and most preferred is a finely divided inorganic material which is about the size which will pass through a 200 mesh sieve.

Generally any finely divided inorganic material is found to effect the benefits earlier described. However, most preferred as inorganic materials are those selected from the group consisting of minerals containing naturally occurring silicates; a mixture of about 30% zinc sulfide and about 70% barium sulfate commonly known as Lithopone; calcium carbonate; and barium sulfate. The minerals of this invention containing naturally occurring silicates should contain a substantial amount of such silicates and preferably they should contain a major portion of naturally occurring silicates. The following table is a representative example of several finely divided inorganic materials which were found to give the desired improvements. Specifically Lithopone, comprising about 30% zinc sulfide and 70% barium sulfate, was the most preferred inorganic material to reduce the swirl-patterns in the surface of an article, while 5% mica was most preferred to give a more uniform cell structure. The following Table I shows the various finely divided inorganic materials which were used and the effectiveness of each. Table I was generated from results obtained with additives to the basic process described in Example IV of the herein above cited U.S. Pat. No. 3,268,636 on a 375 ton model Jarecki Structural Foam injection molding machine. Accordingly, the mixture of finely divided inorganic material and thermoplastic polymeric resinous pellets was charged into the extruder where it was worked and heated, and nitrogen gas was slowly fed into the barrel of the extruder and therein mixed with the molten mixture. The accumulator was filled at a pressure high enough to prevent foaming and then the mold was rapidly filled where foaming commenced.

TABLE I

Additive	Evaluation of injection molded foamed polymeric resinous articles.					
	Impact Polystyrene		High Density Polyethylene		Polypropylene	
	Cell Structure	Surface	Cell Structure	Surface	Cell Structure	Surface
Clay (ASP-200)	Same	Same	Same	Same	Better	Same
Clay (ASP-101)	Same	Same	Same	Same	Same	Same
Talc (Emtal 5 gg)	Same	Slightly Better	Same	Better	Same	Same
Diatomaceous Earth	Same	Slightly Better	Same	Same	Better	Same
Lithopone						
30% zinc sulfide, 70% barium sulfate	Same	Better	Better	Much Better	Same	Slightly Better
Barium Sulfate						
Barimite		Slightly Better				
XF	Same		Better	Better	Same	Same
Calcium Carbonate						
Chem Carb 44	Slightly Better	Same	Better	Better	Same	Same
Aluminum Silicate						
AFTON	Same	Same	Same	Better	Same	Same
Calcium Silicate		Slightly Better				
SILENE EF	Same		Same	Better	Same	Same
Bentonite	Slightly Better					
Clay		Same	Same	Same	Same	Same
Mica (Alisbronz) No.12	Same	Slightly Better	Better	Same	Same	Same
Mica (Alisbronz) No.21	Slightly Better	Slightly Better	Better	Same	Same	Same
Allen-R	—	—	—	—	Same	Same
Arosil	—	—	—	—	Same	Same

"Same" means not significantly improved over articles molded from the same polymeric resinous material without the finely divided inorganic material. "Slightly Better", "Better" and "Much Better" indicate an increasing improvement over articles molded from the same polymeric resinous material without the finely divided mineral powder.

EXAMPLE I

There is provided a screw extruder. Into the hopper of the extruder there is added the thermoplastic foamable composition (e.g., a mixture of polystyrene with a blowing agent such as 1.3% of citric acid and 1.7% sodium bicarbonate and 0.2% of Bayol 35 based on the polystyrene). The solid mixture is heated under high pressure in the extruder to above the decomposition temperature of the blowing agent, e.g. to 150°C., and the foamable mixture under high pressure, e.g. 1000 p.s.i. (although it can be much more, e.g. 2500 p.s.i. or 5000 p.s.i.) is passed through a nozzle into an accumulator (or transfer pot). The foamable composition then commences to foam in the accumulator under a pressure of 5 to 250 p.s.i., e.g. 50 p.s.i.

In place of the nozzle the extruder can be provided with a screen pack or other device which permits the foamable composition to enter the accumulator. A piston is slidably located between the accumulator and a hydraulic cylinder, as the foamable composition expands in the accumulator it forces the piston to go further up into the hydraulic cylinder. In this phase of the operation cycle the entrance to the mold is closed. Two platens are moved with the aid of pistons operating in hydraulic cylinders to open and close the mold halves. The mold also has conventional vents which aid in the removal of the gases released by the breaking of the bubbles adjacent the mold walls. The mold walls are at lower temperature than the foamed material entering the mold from the accumulator, e.g. 175°C. in the case of polypropylene.

When sufficient foamed plastic has formed in the accumulator mold the halves are brought together, the entrance to the mold is opened and a low pressure, e.g. 100 p.s.i. is applied from the hydraulic cylinder via the piston to force foamed plastic into the mold and form a container. Since the foamable plastic is being extruded at a much greater pressure from the extruder nozzle none of the foamed plastic is forced back into the extruder but instead it is forced into the injection mold. After formation of the container the mold halves are opened and the container removed.

In one specific instance in which polypropylene containing 1% of azobisisobutyronitrile and 10% Lithopone is extruded at a pressure of 1000 p.s.i. and a temperature of 182°C. the temperature of the foamed polypropylene in the accumulator at the time of injection of the foamed polypropylene into the mold is 175°C. The mold walls are at 20°C. The container has a wall thickness of 60 mils, the skin being 8 mils thick and the foamed portion 52 mils thick. The transfer molded foam has a density of 35 lbs./cu. ft. while the skin has a density of 52 lbs./cu. ft.

In another instance there is produced an injection molded foamed polystyrene article containing 5% Mica having an unfoamed skin with a density of 56 lbs./cu. ft. (The same as the starting polystyrene) while the foamed portion of the article (90% of the total thickness) has a density of 45.6 lbs./cu. ft.

In a third specific instance there is employed Pelespan 101 (polystyrene containing 6% pentane and 10% Lithopone).

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The pressure at the extruder die is 1000 p.s.i. and the extrusion temperature is 160°C. The polystyrene is allowed to foam in the accumulator and is then injection molded into a cabinet door at a pressure of 100 p.s.i. The temperature of the foamed polystyrene going into the mold is about 150°C. and the mold is cooled to 10°C. by cooling water running through ducts in the mold. In this case the foamed polystyrene is forced into a cabinet door shaped channel in the mold so that both the inner and outer surfaces of the cabinet door as it is being formed are cooled by the mold. Thus there is formed a foamed polystyrene cabinet door having inner and outer external skins integral with the foamed core. The cabinet door is composed of a 4 mil thick impervious, unfoamed outer skin and a foamed core. The foamed core has a density of 30 lbs./cu. ft. and the skin a density of slightly over 60 lbs./cu. ft.

Having thus described the invention what is claimed is:

1. A method for producing a foamed thermoplastic polymeric resinous article substantially free from swirl-patterns in its surface comprising:

injecting a heat plastified thermoplastic polymeric resinous material into a mold in the presence of a foaming agent and finely divided lithopone particles comprising about 30% zinc sulfide and about 70% barium sulfate and being of a size such that

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the lithopone particles will pass through a 10 mesh sieve; cooling the heat plastified thermoplastic polymeric resinous material; removing the cooled, foamed, moldshaped, thermoplastic polymeric resinous article having the finely divided lithopone particles incorporated therein from the mold.

2. The method of claim 1 wherein the finely divided lithopone particles are combined with the thermoplastic polymeric resinous material before the thermoplastic polymeric resinous material is heat plastified and injected into a mold.

3. The method of claim 1 wherein the thermoplastic polymeric resinous material is impact polystyrene.

4. The method of claim 1 wherein the thermoplastic polymeric resinous material is high density polyethylene.

5. The method of claim 1 wherein the thermoplastic polymeric resinous material is polypropylene.

6. A method for injection molding foamed thermoplastic polymeric resinous articles wherein the improvement comprises: admixing into the plastifiable resin finely divided lithopone particles capable of passing through a 10 mesh sieve, the lithopone particles comprising about 30% zinc sulfide and about 70% barium sulfate, to produce articles which are substantially free from swirl-patterns in the surface.

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