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WO-A1-99/13521
US-A1- 2004 062 973
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DESCRIPTION

[0001] The present invention relates to a solid oxide fuel cell system and in particular to a solid oxide fuel cell system comprising a solid oxide fuel cell stack and a gas turbine engine.

[0002] WO2004032273A2 discloses a solid oxide fuel cell system comprising a solid oxide fuel cell stack and a gas turbine engine in which a portion of the unused oxidant leaving the cathodes of the solid oxide fuel cell stack is recycled with fresh oxidant supplied to the cathodes of the solid oxide fuel cell stack to preheat the fresh oxidant supplied to the cathodes of the solid oxide fuel cell stack. An oxidant ejector driven by the fresh oxidant is used to recycle the unused oxidant back to the cathodes of the solid oxide fuel cell stack.

[0003] A problem with this solid oxide fuel cell system is that the location of the oxidant ejector is between a compressor of the gas turbine engine and the expander, turbine, produces a very large pressure loss and this requires a specific gas turbine engine to be designed for the solid oxide fuel cell system. The specific design of gas turbine engine increases the total cost of the solid oxide fuel cell system.

[0004] Accordingly the present invention seeks to provide a solid oxide fuel cell system which reduces, preferably, overcomes the above mention problem.

[0005] EP 0 496 011 discloses a power generation system using molten carbonate fuel cells. A reformer includes a reforming chamber for reforming raw material and a heating chamber for heating the reforming chamber. Exhaust gas from a cathode chamber of a fuel cell is directly introduced to the heating chamber such that the exhaust gas is combusted, or the exhaust gas from the cathode chamber is introduced to a catalyst combustor together with exhaust gas discharged from the anode chamber such that these gases undergo combustion. Combustion exhaust gas is introduced to the heating chamber and sensible heat of the cathode exhaust gas is effectively used as heat source for a reforming reaction in the reforming chamber.

[0006] Viewed from one aspect, there is provided a solid oxide fuel cell system comprising a solid oxide fuel cell stack and a gas turbine engine, the solid oxide fuel cell stack comprising at least one solid oxide fuel cell, each solid oxide fuel cell comprising an electrolyte, an anode and a cathode, the gas turbine engine comprising a compressor and a turbine arranged to drive the compressor, the compressor being arranged to supply oxidant to the cathode of the at least one solid oxide fuel cell via an oxidant mixer, the oxidant mixer being arranged to supply a portion of the unused oxidant from the cathode of the at least one solid oxide fuel cell back to the cathode of the at least one solid oxide fuel cell with the oxidant from the compressor, characterised in that the solid oxide fuel cell system further comprises an additional compressor and an electric motor arranged to drive the additional compressor, the compressor being arranged to supply oxidant to the additional compressor, the additional compressor being arranged to supply oxidant to the oxidant mixer, the solid oxide fuel cell stack being arranged to supply exhaust gases to the turbine, and in that the oxidant mixer is an oxidant ejector.

[0007] The solid oxide fuel cell system may further comprise a cooler and a recuperator, the compressor may be arranged to supply oxidant via the cooler to the additional compressor, the additional compressor may be arranged to supply oxidant to the oxidant mixer via the recuperator, the solid oxide fuel cell stack may be arranged to supply exhaust gases to the turbine and the turbine may be arranged to supply the exhaust gases through the recuperator to heat the oxidant flowing through the recuperator.

[0008] The cathode of the at least one solid oxide fuel cell may be arranged to supply a portion of the unused oxidant to a combustor, the anode of the at least one solid oxide fuel cell is arranged to supply a portion of the unused fuel to the combustor and the combustor is arranged to supply at least a portion of the combustor exhaust gases to the turbine.

[0009] The combustor may be arranged to supply a portion of the combustor exhaust gases to the turbine.

[0010] The combustor may be arranged to supply the portion of the combustor exhaust gases to a first flow path through a heat exchanger and the oxidant mixer is arranged to supply the portion of the unused oxidant from the cathode of the at least one solid oxide fuel cell back to the cathode of the at least one solid oxide fuel cell with the oxidant from the compressor through a second flow path through the heat exchanger.

[0011] The additional compressor may be arranged to supply oxidant to an additional mixer via the recuperator, the combustor is arranged to supply the combustor exhaust gases to the additional mixer, the additional mixer is arranged to supply oxidant and the combustor exhaust gases to the first flow path through the heat exchanger.

[0012] The heat exchanger may be arranged to supply a first portion of the combustor exhaust gases and oxidant leaving the first flow path through the heat exchanger to the combustor and the heat exchanger is arranged to supply a second portion of the combustor exhaust gases and oxidant leaving the first flow path through the heat exchanger to the turbine.

[0013] The additional compressor may be a fan or a blower.

[0014] The additional mixer may be an additional ejector.

[0015] The present invention will be more fully described by way of example with reference to the accompanying drawings, in which:

Figure 1 is a solid oxide fuel cell system according to the present invention.

[0016] A solid oxide fuel cell system 10, as shown in figure 1, according to the present invention comprises a solid oxide fuel cell stack 12 and a gas turbine engine 14. The solid oxide fuel cell stack 12 comprises at least one solid oxide fuel cell 16 and each solid oxide fuel cell 16 comprises an electrolyte 18, an anode 20 and a cathode 22. The anode 20 and the cathode 22 are arranged on oppositely directed surfaces of the electrolyte 18.

[0017] The gas turbine engine 14 comprises a compressor 24 and a turbine 26 arranged to drive the compressor 24 via a shaft 28. The turbine 26 of the gas turbine engine 14 is also arranged to drive an electrical generator 27 via a shaft 29.

[0018] The anodes 20 of the solid oxide fuel cells 16 are supplied with a fuel for example hydrogen, by a fuel manifold 30 and a fuel supply 32, for example hydrogen, is arranged to supply fuel to the fuel manifold 30 via duct 34. The cathodes 22 are supplied with an oxidant, for example oxygen, air etc, by an oxidant manifold 36 and an oxidant supply 38 is arranged to supply oxidant to the oxidant manifold 36 via a duct 40. The compressor 24 is located in the duct 40 and pressurises the supply of oxidant to the oxidant manifold 36.

[0019] The anodes 20 are provided with an unused fuel collection manifold 42 into which unused fuel is discharged. The unused fuel collection manifold 42 is connected to the duct 34 via ducts 44 and 46 such that a portion of the unused fuel is supplied, recirculated, to the fuel manifold 30. A fuel ejector 48 is provided to induce the supply, recirculation, of unused fuel from the unused fuel collection manifold 42 to the fuel manifold 30. The ducts 44, 46 and the fuel ejector 48 form means 50 to supply, recirculate, unused fuel from the anodes 20 of the solid oxide fuel cells 16 back to the anodes 20 of the solid oxide fuel cells 16. The fuel ejector 48 pressurises the unused fuel and mixes the unused fuel with the fuel supplied by the fuel supply 32 through the duct 34 to the fuel manifold 30. Only fuel from the fuel supply 32 flows in a first portion 34A of the duct 34 between the fuel supply 32 and the fuel ejector 48. The fuel from the fuel supply 32 and the portion of the unused fuel from the anodes 20 of the solid oxide fuel cells 16 after mixing by the fuel ejector 48 is supplied through a second portion 34B of the duct 34 to the fuel manifold 30.

[0020] The unused fuel collection manifold 42 is also connected to a combustor 52 via the duct 44 and a further duct 54 such that a second portion of the unused fuel is supplied to the combustor 52.

[0021] The cathodes 22 of the solid oxide fuel cells 16 are provided with an unused oxidant collection manifold 56 into which unused oxidant is discharged. The unused oxidant collection manifold 56 is connected to the duct 40 via duct 58 such that a portion of the unused oxidant is supplied, recirculated, to the oxidant manifold 36. An oxidant ejector 60 is provided to induce the supply, recirculation, of unused oxidant from the unused oxidant collection manifold 56 to the oxidant manifold 36. The ducts 40 and 58 and the oxidant ejector 60 form means 61 to supply, recirculate, unused oxidant from the cathodes 22 of the solid oxide fuel cells 16 back to the cathodes 22 of the solid oxide fuel cells 16. The oxidant ejector 60 pressurises the unused oxidant and mixes the unused oxidant with the oxidant supplied by the compressor 24 through the duct 40 to the oxidant manifold 36. The compressor 24 is arranged to supply oxidant to the cathodes 22 of the solid oxide fuel cells 12 via the oxidant ejector 60, the oxidant ejector 60 is arranged to supply a portion of the unused oxidant from the cathodes 22 of the solid oxide fuel cell cells 16 back to the cathodes 22 of the solid oxide fuel cells 16 with the oxidant from the compressor 24.

[0022] The unused oxidant collection manifold 56 is connected to the combustor 52 via the duct 58 and a further duct 62 such that a second portion of the unused oxidant is supplied to the combustor 52.

[0023] The solid oxide fuel cell system 10 further comprises an additional compressor 64, an electric motor 66, a cooler 70 and a recuperator 72. The electric motor 66 is arranged to drive the additional compressor 64 via a shaft 68. The compressor 24 is arranged to supply the oxidant via a portion 40A of the duct 40, the cooler 70 and a portion 40B of the duct 40 to the additional compressor 64. A coolant C is supplied to the cooler 70 to cool the oxidant as it flow through the cooler 70.

[0024] The additional compressor 64 is arranged to supply the oxidant via a portion 40C of the duct 40 to the recuperator 72 to heat the oxidant. A first portion of the heated oxidant is supplied from the recuperator 72 via a portion 40D of the duct 40 to the oxidant ejector 60 and a second portion of the heated oxidant is supplied from the recuperator 72 via a duct 76 to an additional ejector 74. The combustor 52 is arranged to supply hot exhaust gases via a duct 78 to a secondary inlet of the additional ejector 74. The additional ejector 74 mixes the portion of oxidant supplied from the recuperator 72 and the hot exhaust gases from the combustor 52. The outlet of the additional ejector 74 is arranged to supply the mixture of oxidant and exhaust gases via a duct 80 to a heat exchanger 82. The hot exhaust gases are supplied to a first inlet 84 of the heat exchanger 82 and flow thought a first path 86 within the heat exchanger 82 to a first outlet 88 of the heat exchanger 82. A portion of the mixture of hot exhaust gases and oxidant is then supplied from the first outlet 88 of the heat exchanger 82 to the turbine 26 through a duct 90. The hot exhaust gases drive the turbine 26 and then the hot exhaust gases flow through a duct 92 to the recuperator 72 and are discharged through an exhaust 94. A further portion of the mixture of oxidant and hot exhaust gases is supplied from the first outlet 88 of the heat exchanger 82 to the combustor 52 via a duct 96.

[0025] The oxidant ejector 60 is arranged to supply the oxidant supplied by the additional compressor 64 via the recuperator 72 and a portion 40D of the duct 40 and the unused oxidant supplied from the oxidant collection manifold 56 and the duct 58 via a portion 40E of the duct 40 to a second inlet 98 of the heat exchanger 82 and flows thought a second path 100 within the heat exchanger 82 to a second outlet 102 of the heat exchanger 82. The oxidant from the additional compressor 64 and the portion of the unused oxidant from the cathodes 22 of the solid oxide fuel cells 16 is then supplied from the second outlet 102 of the heat exchanger 82 to the oxidant manifold 36 via a portion 40F of the duct 40.

[0026] The solid oxide fuel cell stack 12 is arranged to supply exhaust gases to the turbine 26 and the turbine 26 is arranged to supply the exhaust gases through the recuperator 72 to heat the oxidant flowing through the recuperator 72.

[0027] The advantage of the present invention is that the use of the additional compressor, electric motor, cooler and recuperator allows the use of a commercially available gas turbine engine rather than the development of a specific gas turbine engine to operate with a large pressure loss produced by an oxidant ejector recycling unused oxidant from the cathodes of the solid oxide fuel cells back to the cathodes of the solid oxide fuel cells. The additional compressor in particular increases the oxidant pressure, air pressure, at the inlet to the solid oxide fuel cell system and this allows the use of the oxidant ejector to drive the recycling of the unused oxidant, unused air, from the cathodes of the solid oxide fuel cells back to the cathodes of the solid oxide fuel cells. The use of the additional compressor enables a conventional gas turbine engine in which the compression ratio of the compressor is equal to the expansion ratio of the turbine compared to the development of an unconventional gas turbine engine in which the compression ratio of the compressor is greater than the expansion ratio of the turbine. The cooler reduces the additional power required by the additional compressor, for example reduces the power required by about 60%.

[0028] Although the present invention has been described with reference to a cooler in the flow path for the oxidant between the additional compressor and the compressor and a recuperator in the flow path for the exhaust gases from the turbine and in the flow path for the oxidant from the additional compressor to the oxidant ejector the present invention may equally well be used without the cooler, without the recuperator or without both the cooler and the recuperator. Alternatively if the cooler and recuperator are provided it may be possible to supply a portion of the oxidant from the additional compressor 64 directly through the duct 76 to the additional ejector 74 without flowing through the recuperator 72 and to supply a portion of the oxidant from the additional compressor 64 to the recuperator 72 and then through duct 40D to the oxidant ejector 60.

[0029] It may be possible in the present invention, if the fuel supply 22 is a supply of a hydrocarbon fuel, e.g. an alkane, an alkene, an alcohol etc, for example methane, butane, propane, natural gas, ethanol etc, to provide a fuel reformer in the second portion 34B of the duct 34 supplying fuel to the fuel manifold 30 and the anodes 20 of the solid oxide fuel cells 16. The fuel reformer may be arranged to be heated by unused oxidant exiting the cathodes 22 of the solid oxidant fuel cells 16 for example in the oxidant collection manifold 56 or the duct 58 etc.

[0030] Although the present invention has been described with reference to an oxidant ejector, it may be possible to use another type of oxidant mixer which mixes unused oxidant supplied from the unused oxidant collection manifold with fresh oxidant supplied by the compressor from the oxidant supply. Although the present invention has been described with reference to an additional ejector it may be possible to use another type of additional mixer. Although the present invention has been described with reference to a fuel ejector it may be possible to another type of fuel mixer which mixes unused fuel from the unused fuel collection

manifold with fresh fuel from the fuel supply.

REFERENCES CITED IN THE DESCRIPTION

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Patent documents cited in the description

- WO2004032273A2 [0002]
- EP0496011A [0005]

PATENTKRAV

1. Keramisk brændselscellesystem (10) omfattende en keramisk brændselscellestak (12) og en gasturbinemotor (14), hvor den keramiske brændselscellestak (12) omfatter mindst én keramisk brændselscelle (16), hvor hver keramisk brændselscelle (16) omfatter en elektrolyt (18), en anode (20) og en katode (22), hvor gasturbinemotoren (14) omfatter en kompressor (24) og en turbine (26), der er tilvejebragt til at drive kompressoren (24), hvor kompressoren (24) er tilvejebragt til at levere oxidationsmiddel til den mindst ene keramiske brændselscelles (16) katode (22) via en oxidationsmiddelblander (60), hvor oxidationsmiddelblander (60) er tilvejebragt til at levere en del af katodens (22) ikke-anvendte oxidationsmiddel fra den mindst ene keramiske brændselscelle (16) tilbage til den mindst ene keramiske brændselscelles (16) katode (22) med oxidationsmidlet fra kompressoren (24), kendetegnet ved, at det keramiske brændselscellesystem (10) endvidere omfatter en supplerende kompressor (64) og en elektrisk motor (66), der er tilvejebragt til at drive den supplerende kompressor (64), hvor kompressoren (24) er tilvejebragt til at levere oxidationsmiddel til den supplerende kompressor (64), hvor den supplerende kompressor (64) er tilvejebragt til at levere oxidationsmiddel til oxidationsmiddelblander (60), hvor den keramiske brændselscellestak (12) er tilvejebragt til at levere udstødningsgasser til turbinen (26), og ved, at oxidationsmiddelblander (60) er en oxidationsmiddelejektor.
2. Keramisk brændselscellesystem ifølge krav 1, hvor det keramiske brændselscellesystem (10) endvidere omfatter en køler (70) og en rekuperator (72), hvor kompressoren (24) er tilvejebragt til at levere oxidationsmiddel via køleren (72) til den supplerende kompressor (64), hvor den supplerende kompressor (64) er tilvejebragt til at levere oxidationsmiddel til oxidationsmiddelblander (60) via rekuperatoren (72), hvor den keramiske brændselscellestak (12) er tilvejebragt til at levere udstødningsgasser til turbinen (26), og hvor turbinen (26) er tilvejebragt til at levere udstødningsgasserne gennem rekuperatoren (72) for at opvarme oxidationsmidlet, der strømmer gennem rekuperatoren (72).
3. Keramisk brændselscellesystem ifølge krav 1 eller krav 2, hvor katoden (22) i den mindst ene keramiske brændselscelle (16) er tilvejebragt til at levere en del af det ikke-anvendte oxidationsmiddel til et forbrændingskammer (52), anoden (22) i den mindst ene keramiske brændselscelle (16) er tilvejebragt til at levere en del af det ikke-anvendte brændstof til forbrændingskammeret (52) og forbrændingskammeret (52) er tilvejebragt til at levere mindst en del af forbrændingskammerets (52) udstødningsgasser til turbinen (26).
4. Keramisk brændselscellesystem ifølge krav 3, hvor forbrændingskammeret (52) er tilvejebragt til at levere en del af forbrændingskammerets (52) udstødningsgasser til turbinen (26).
5. Keramisk brændselscellesystem ifølge krav 4, hvor forbrændingskammeret (52) er tilvejebragt

til at levere delen af forbrændingskammerets (52) udstødningsgasser til en første strømningsbane (86) gennem en varmeveksler (82) og oxidationsmiddelblanderen (60) er tilvejebragt til at levere delen af katodens (22) ikke-anvendte oxidationsmiddel i den mindst ene keramiske brændselscelle (16) tilbage til katoden (22) i den mindst ene keramiske brændselscelle (16) med oxidationsmidlet fra kompressoren (24) gennem en anden strømningsbane (100) gennem varmeveksleren (82).

6. Keramisk brændselscellesystem ifølge krav 5, hvor den supplerende kompressor (64) er tilvejebragt til at levere oxidationsmiddel til en supplerende blander (74) via rekuperatoren (72), forbrændingskammeret (52) er tilvejebragt til at levere forbrændingskammerets (52) udstødningsgasser til den supplerende blander (74), den supplerende blander (74) er tilvejebragt til at levere oxidationsmiddel og forbrændingskammerets (52) udstødningsgasser til den første strømningsbane (86) gennem varmeveksleren (82).

7. Keramisk brændselscellesystem ifølge krav 6, hvor varmeveksleren (82) er tilvejebragt til at levere en første del af forbrændingskammerets (52) udstødningsgasser og oxidationsmiddel, der forlader den første strømningsbane (86), gennem varmeveksleren (82) til forbrændingskammeret (52) og varmeveksleren (82) er tilvejebragt til at levere en anden del af forbrændingskammerets (52) udstødningsgasser og oxidationsmiddel, der forlader den første strømningsbane (86), gennem varmeveksleren (82) til turbinen (26).

8. Keramisk brændselscellesystem ifølge krav 6 eller krav 7, hvor den supplerende blander (74) er en supplerende ejektor.

9. Keramisk brændselscellesystem ifølge et hvilket som helst af kravene 1 til 8, hvor den supplerende kompressor (64) er en ventilator eller en blæser.

DRAWINGS

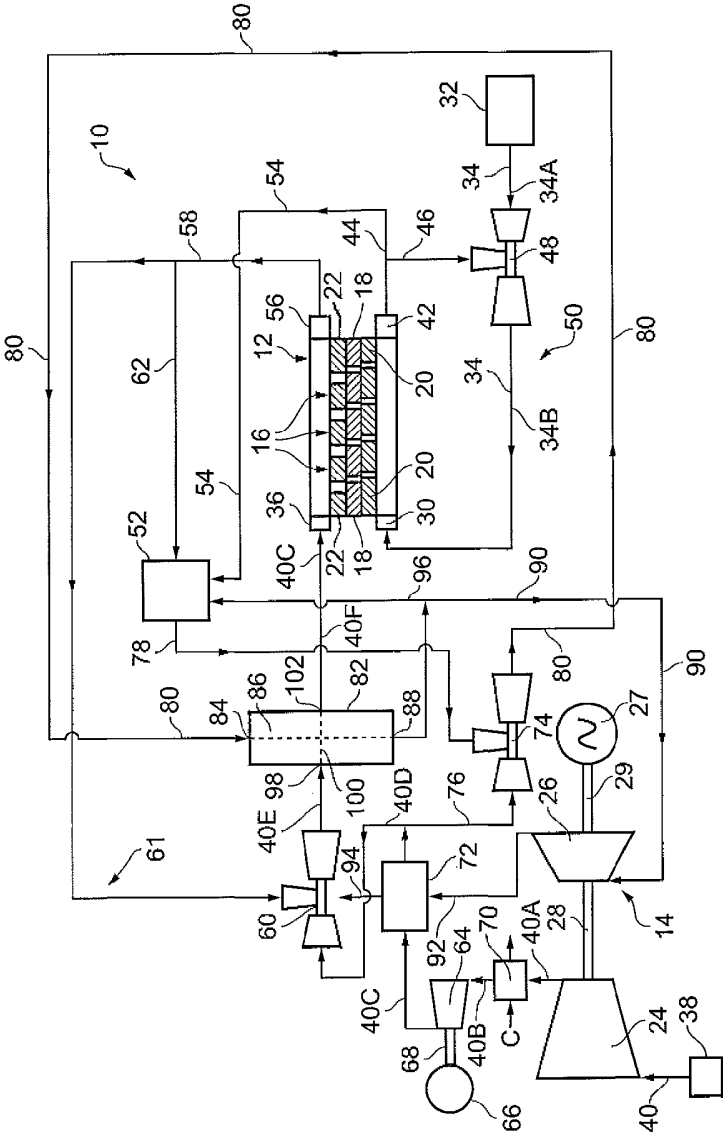


FIG. 1