



(22) Date de dépôt/Filing Date: 2007/11/16

(41) Mise à la disp. pub./Open to Public Insp.: 2008/01/30

(45) Date de délivrance/Issue Date: 2009/01/27

(30) Priorité/Priority: 2007/07/16 (US60/949,948)

(51) Cl.Int./Int.Cl. *C01F 7/56* (2006.01),
C01F 7/30 (2006.01), *C22B 3/08* (2006.01)

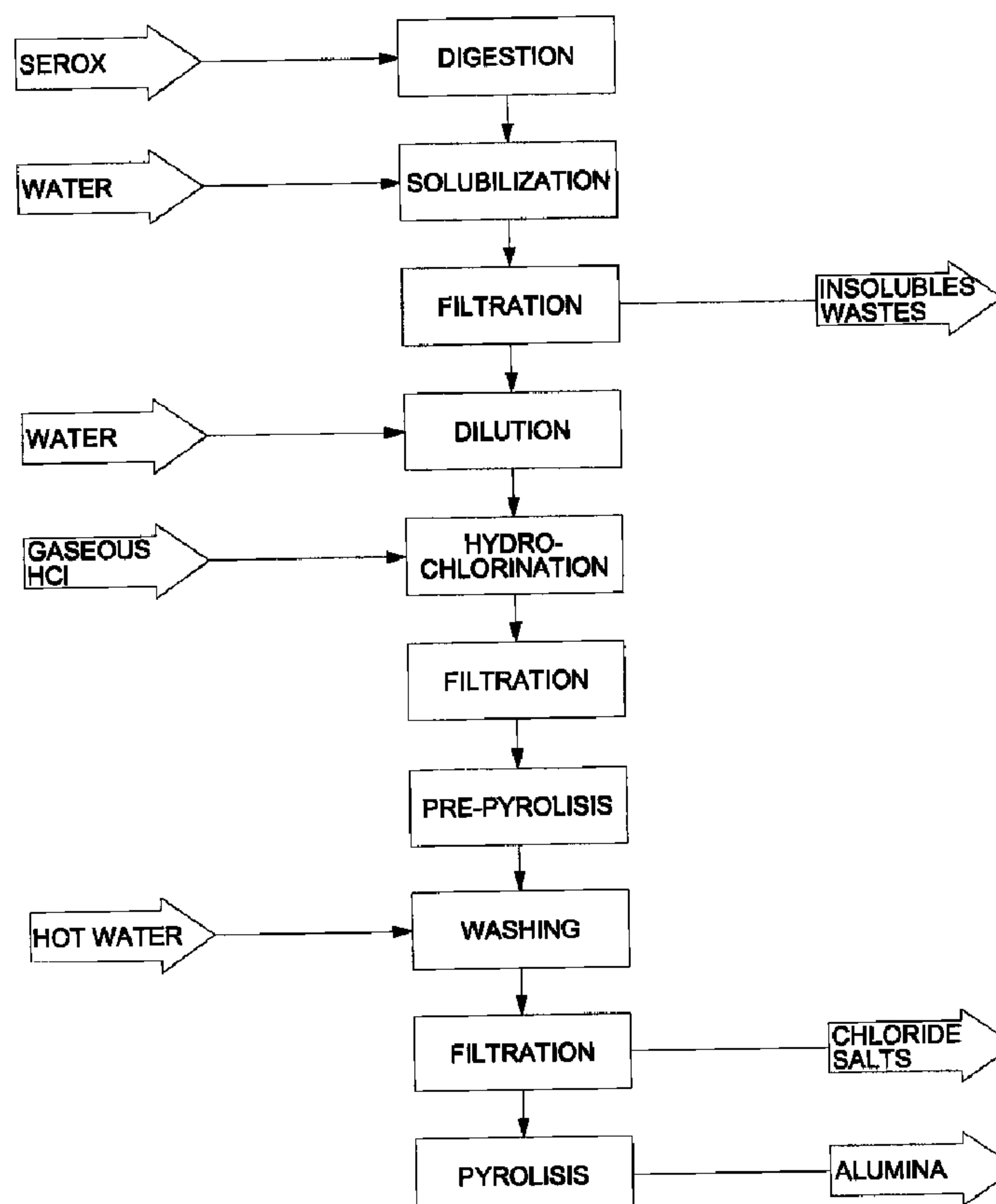
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(54) Titre : PROCESSUS DE TRAITEMENT DE RESIDUS D'ECUME D'ALUMINIUM

(54) Title: PROCESSES FOR TREATING ALUMINIUM DROSS RESIDUES



(57) Abrégé/Abstract:

There is provided a process for preparing aluminium chloride comprising leaching aluminium dross residues with H_2SO_4 so as to obtain a leachate; and hydrochlorinating the leachate so as to obtain aluminium chloride. If desired, aluminium chloride can then be converted into alumina.

ABSTRACT OF THE DISCLOSURE

There is provided a process for preparing aluminium chloride comprising leaching aluminium dross residues with H_2SO_4 so as to obtain a leachate; and hydrochlorinating the leachate so as to obtain aluminium chloride. If desired, aluminium chloride can then be converted into alumina.

PROCESSES FOR TREATING ALUMINIUM DROSS RESIDUES

TECHNICAL FIELD

The present invention relates to improvements in the field of inorganic chemistry applied to aluminium dross residues. In particular, this invention relates to processes for treating aluminium dross residues.

BACKGROUND OF THE INVENTION

In the production of aluminium (aluminium smelters) or melting of aluminium (eg. for manufacture of extrusions, ingots and billets) a by-product called aluminium dross is formed. Such a by-product is formed in molten aluminium in view of oxygen from environmental air as well as impurities present in aluminium. Aluminium dross generally comprises free metal and non-metallic substances (e.g. aluminium oxide and salts). Aluminium nitrides and carbides may also be present, as well as metals oxides derived from molten alloy. Aluminium dross does represent an interesting by-product to valorize in order to recuperate or recover the products contained therein.

It is known to process the dross first by separating aluminium from it to obtain aluminium dross residues, which are also known as non-metallic products (NMP). In other words it can be said that the aluminium dross residues are obtained by at least partially removing aluminium metallic from aluminium dross. Aluminium dross is normally treated either by a plasma or in a conventional furnace with a salt mixture, to remove recoverable aluminum metal, leaving a dross residue having reduced aluminum content.

The main components in aluminium dross residues generally include alumina, aluminum metallic and spinel. Other main components such as aluminum nitride, gibbsite ($\text{Al}(\text{OH})_3$), and diaoyudaoite ($\text{NaAl}_{11}\text{O}_{17}$) can also be present. Various minor components such as Fe_2O_3 , SiO_2 , MgO can also be present.

Dube et al. in U.S. Pat. Nos. 4,959,100 and 4,960,460 disclose treatment processes for recovering aluminum from aluminum dross hence producing aluminum dross residues. Such aluminium dross residues are also disclosed in U.S Pat. No. 5,407,459, and known as NOVAL™.

Formerly aluminium dross residues originating from known dross processing techniques in rotating salt furnaces were put in a landfill as waste. Such disposal is increasingly facing environmental problems or is even banned, since salts can leach from the aluminium dross residues and pass into the soil below. Aluminum dross residues are frequently classified as hazardous material. Therefore, the disposal, transformation or valorization of the aluminium dross residues is of prime economic and environmental importance.

Several solutions have been proposed for recuperating aluminium from aluminium dross but only few have been proposed for valorizing or treating aluminium dross residues i.e. residues that are obtained after removal of aluminium from aluminium dross.

It would thus be highly desirable to be provided with a process that would propose an alternative way for valorizing aluminium dross residues into a product, which is different than calcium aluminates.

SUMMARY OF THE INVENTION

According to one aspect of the invention, there is provided a process for preparing aluminium chloride comprising:

- leaching aluminium dross residues with H_2SO_4 so as to obtain a leachate; and
- hydrochlorinating the leachate so as to obtain aluminium chloride.

According to another aspect of the invention, there is provided a process for preparing aluminium chloride comprising:

- treating aluminium dross residues so as to reduce the amount of aluminium nitride present therein;
- leaching the aluminium dross residues with H_2SO_4 so as to obtain a leachate; and
- hydrochlorinating the leachate so as to obtain aluminium chloride.

According to another aspect of the invention, there is provided a process for preparing alumina comprising:

- optionally treating aluminium dross residues so as to reduce the amount of aluminium nitride present therein;
- leaching the aluminium dross residues with H_2SO_4 so as to obtain a leachate;
- hydrochlorinating the leachate so as to obtain aluminium chloride; and
- converting aluminium chloride into alumina.

The expression "aluminium dross residues" as used herein refers to residues that are obtained by substantially removing the recoverable aluminum metal from aluminium dross. For example, the aluminium dross residues comprise alumina, aluminium metal and spinel (MgAl_2O_4). Some other compounds such as aluminum nitride, gibbsite ($\text{Al}(\text{OH})_3$), and diaoyudaoite ($\text{NaAl}_{11}\text{O}_{17}$) can also be present at various proportions. Various minor components such as Fe_2O_3 , SiO_2 , MgO can also be present. For example, the dross residues can comprise NOVALTM, SEROXTM, or a mixture thereof.

The term "SEROXTM" as used herein refers, for example, to aluminium dross residues that comprise alumina, aluminium metal, spinel (MgAl_2O_4), and gibbsite ($\text{Al}(\text{OH})_3$). Such residues can also comprises various other compounds, such as diaoyudaoite ($\text{NaAl}_{11}\text{O}_{17}$), sylvite (KCl), Halite (NaCl), Cryolite (Na_3AlF_6), mica, sodalite ($\text{Na}_4\text{Al}_3\text{Si}_3\text{O}_{12}\text{Cl}$), Ca_2SiO_4 , albite ($\text{NaAlSi}_3\text{O}_8$), fluorite CaF_2 , or mixtures thereof.

The term "NOVALTM" as used herein refers, for example, to aluminium dross residues that comprise alumina, aluminium, aluminium nitride, sodium oxide and magnesium oxide.

The amount of aluminium nitride present in the aluminium dross residues can be reduced by converting aluminium nitride into aluminium hydroxide. For example, at least 80%, at least 85 %, at least 90 %, or at least 95 % of the aluminium nitride present in the aluminium dross residues can be converted into aluminium hydroxide. Aluminium nitride can be converted into aluminium hydroxide by reacting the aluminium dross residues with water having a temperature of at least 80 °C, at least 85 °C, at least 90 °C, or at least 95 °C. For example, the water temperature can be around its boiling point. A solid can be recovered after the conversion of aluminium nitride into aluminium hydroxide and the solid can be treated (for example leached with H_2SO_4) so as to solubilize at least a portion of the aluminium hydroxide, thereby obtaining a leachate and another solid. The solid can be treated with a solution comprising H_2SO_4 . The solution can further comprise aluminium sulfate. The other solid can also be leached with H_2SO_4 so as to obtain a leachate.

In the processes of the present invention, the leaching can be carried out at a temperature of at least 70 °C, at least 90 °C, at least 125 °C, at least 150 °C, at least 160 °C, at least 200 °C, at least 225 °C, or at least 250 °C .

For example, after the leaching step, a mixture comprising a solid phase and a liquid phase can be obtained. These two phases can eventually

be separated. They can be separated by various means including membranes, filtration means, for example under vacuum etc. The solid phase can be treated with water having a temperature of at least 30 °C so as to solubilize metals and minerals contained therein and to obtain the leachate.

For example, the solid phase can be treated with water having a temperature of at least 50 °C or of at least 70 °C so as to solubilize metals and minerals contained therein and to obtain the leachate. The leachate can be hydrochlorinated with gaseous HCl.

Hydrochlorination can be carried out at a temperature of about -10 °C to about 20 °C or at a temperature of about -10 °C to about 0 °C. The leachate can be hydrochlorinated with gaseous HCl.

Aluminium chloride can optionally be converted into alumina. The conversion of aluminium chloride into alumina can be, for example, carried out by pyrolyzing or pyrohydrolyzing the aluminium chloride so as to obtain alumina. Such a step can be, for example, carried out at a temperature of about 100 °C to about 1400 °C, about 200 °C to about 1300 °C, about 800 °C to 1200 °C, or at about 950 °C to 1150 °C. This step can be, for example, carried out over a period of about 0.5 to about 6 hours, about 1 hour to about 3 hours, or over a period of about 1.5 hours. For example, aluminium chloride can be converted into aluminium hydroxide by heating aluminium chloride at a temperature of at least 100 °C, at least 200 °C, at least 300 °C, at least 400 °C, at least 500 °C, at least 600 °C, at least 700 °C, at least 800 °C, at least 900 °C, or at least 950 °C. Then, aluminium hydroxide can be converted into alumina by heating aluminium hydroxide at a temperature of at least 450 °C, at least 550 °C, at least 650 °C, at least 750 °C, at least 850 °C, at least 950 °C, or at least 1000 °C. Conversion of aluminium chloride into alumina can further comprise washing the aluminium hydroxide so as to remove chloride salts.

For example, in the conversion from aluminium chloride to alumina, at least 50 %, at least 60 %, at least 70 %, at least 80 %, at least 90 %, at least 95 %, or at least 99 % by weight of the Al atoms contained in the aluminium dross residues can be obtained in the form of alumina. About 80 % to about 95 % by weight of the Al atoms contained in the aluminium dross residues can be obtained in the form of alumina. The alumina so-obtained can have a purity of at least 80 %, at least 85 %, at least 90 %, at least 93 %, at least 95 %, at least 98 %, at least 99 %, or of about 93 % to about 99 %.

The leaching step can be carried out using a H_2SO_4 solution having a concentration of about 50 % to about 98%, about 70 % to about 98%, or of about 98 %.

BRIEF DESCRIPTION OF DRAWINGS

In the following drawings, which represent by way of example only, various embodiments of the invention :

Fig. 1 shows a bloc diagram of a process according to one embodiment of the present invention; and

Fig. 2 shows a bloc diagram of a process according to another embodiment of the present invention.

DETAILED DESCRIPTION OF THE INVENTION

Further features and advantages of the invention will become more readily apparent from the following description of various embodiments as illustrated by way of non-limiting examples in the appended drawings.

Example 1

The following example (see Fig. 1) was carried out on aluminium dross residues, and more particularly on SEROXTM. The SEROX sample contained the following components: 32.4 % of alumina, 1.0 % of aluminium metal, 7.0 % of gibbsite ($\text{Al}(\text{OH})_3$), 20.0 % of diaoyudaoite ($\text{NaAl}_{11}\text{O}_{17}$), 0.5 % of sylvite

(KCl), 2.5 % of halite (NaCl), 2.0 % of cryolite (Na_3AlF_6), 3.1 % of mica, 0.5 % of sodalite ($\text{Na}_4\text{Al}_3\text{Si}_3\text{O}_{12}\text{Cl}$), 2.5 % of Ca_2SiO_4 , 1.8 % of albite ($\text{NaAlSi}_3\text{O}_8$), 1.0 % of fluorite CaF_2 and humidity. It was calculated that the theoretical yield of 100 % conversion of all the Al atoms contained in the dross residues into alumina would provide an amount of 24.9 g of alumina.

The process can comprise different amounts of steps and, in accordance with the steps carried out, different final products (aluminium chloride or alumina) will be obtained and the percentage of Al atoms recovered from the aluminium dross residues will also vary. As previously indicated, each process or treatment comprises at least one H_2SO_4 leaching step and one hydrochlorinating step. Optionally a conversion from aluminium chloride to alumina can be carried out when the desired final product is alumina.

H_2SO_4 leaching step

In the H_2SO_4 leaching step (or digestion), the aluminium dross residues were mixed with H_2SO_4 98 % at a temperature of about 275 °C under constant stirring for a period of about 8 hours. About 800.0 g of SEROX were introduced in a reactor with 8 liters of H_2SO_4 98 % and the mixture was kept under stirring at the aforesaid temperature. When the reaction was completed, the heating was stopped and the mixture was stirred until a temperature of about 70 °C was obtained. Then, the mixture was filtered under vacuum and about 5.4 liters of an aqueous phase (unreacted H_2SO_4) and a solid (for example a paste) containing residues (H_2SO_4 , minerals and metals (such as sulfates)) were recovered.

The paste was then mixed with about 13 liters of hot water and the so-obtained mixture was stirred and maintained at a temperature of about 80 °C in order to solubilize the metals and minerals contained therein. Then, the hot mixture was filtered under vacuum to obtain a leachate of a volume of about 13 liters and a solid residue of about 26 grams on a dry basis.

Hydrochlorination step

The leachate (about 13 liters) was cooled at $-10\text{ }^{\circ}\text{C}$. Then, it was treated with gaseous HCl and the reaction was carried out at a temperature of about $-4\text{ }^{\circ}\text{C}$ to about $-10\text{ }^{\circ}\text{C}$. The hydrochlorination was carried out until saturation of the solution. The gaseous HCl thereby introduced caused aluminium chloride to precipitate. Then, the so-obtained cold mixture was filtered under vacuum so as to provide about 2735 grams of aluminium chloride hydrate and about 12 liters of a waste liquid.

Pyrohydrolysis of aluminium chloride into alumina

The aluminium chloride so-obtained can then optionally be converted into alumina by means of a pyrohydrolysis.

The aluminium chloride was heated (pre-pyrolysis) at a temperature of about $500\text{ }^{\circ}\text{C}$ for a period of about 2 hours in order to convert the aluminium chloride into aluminium hydroxide and gaseous HCl. Then, the so-obtained material was washed with hot water at about $80\text{ }^{\circ}\text{C}$ to remove chloride salts. The product was then heated for 15 minutes at about $1050\text{ }^{\circ}\text{C}$ to convert aluminium hydroxide into gamma-alumina, thereby providing about 481 g of alumina having a degree of purity of at least 98 %. The 100 % theoretical yield of conversion of all the Al atoms contained in the SEROX should provide 544 g of alumina. Therefore, the yield for recovering the Al atoms of the dross residues into alumina was 88.4 %.

Example 2

The following example (see Fig. 2) was carried out on aluminium dross residues containing at least 15 % of aluminium nitride and more particularly on NOVALTM. The NOVAL sample contained the following components: 52 % of alumina (Al_2O_3), 42 % of sodium oxide (Na_2O), 3 % of silica (SiO_2), 9 % of magnesium oxide (MgO), 20 % of aluminium nitride (AlN), 12 % of aluminium metal, 1.7 % of calcium fluoride (CaF_2), 1.4 % of chloride expressed as sodium chloride, 4 % of total fluoride, 0.7 % of ferric oxide (Fe_2O_3) and 0.4 %

of manganese oxide (MnO). It was calculated that the theoretical yield of 100 % conversion of all the Al atoms contained in this dross residues into alumina would provide an amount of about 1 kg of alumina per kg of dross residues.

The process can comprise various amounts of steps and, in accordance with the steps carried out, different final products (aluminium chloride or alumina) will be obtained. As previously indicated, each process or treatment comprises at least one conversion of aluminium nitride into aluminium hydroxide step, one neutralization step, one H₂SO₄ leaching step and one hydrochlorinating step. Optionally, a conversion from aluminium chloride into alumina can be carried out when the desired final product is alumina.

Conversion of aluminium nitride

In the conversion of aluminium nitride in aluminium hydroxide, the aluminium dross residues were mixed with hot water at the boiling point for a period of 24 hours. About 1 kg of NOVAL was introduced in a reactor with about 2.5 liters of water. The mixture was kept under stirring at the aforesaid temperature. Water was added occasionally to keep the volume substantially constant.

During this step, the ammoniac so-produced was vented out the reactor. When the reaction was completed, the mixture was filtered to recover the solid fraction. The mass of this fraction was about 1300 g on a dry basis.

The so-obtained solid was added to the liquid fraction of the H₂SO₄ leaching step (digestion), which is the step that neutralizes this acid fraction.

Neutralization step

The solid fraction previously obtained in the conversion of aluminium nitride was mixed with the filtrate obtained from the H₂SO₄ leaching step at a temperature of about 100 °C for a period of about 2 hours. This liquid fraction contained sulfuric acid and aluminium sulfate in solution. The solid fraction will

react with the sulfuric acid contained in the solution to solubilize the aluminium hydroxide produced at the step of converting aluminium nitride into aluminium hydroxide. Then, when the reaction is completed, the mixture is filtered. The so-obtained solid (about 450 g) is kept to be treated at the H_2SO_4 leaching step of the process. The so-obtained liquid, which contains all the Al atoms, is diluted with water to obtain a total volume of about 21 liters to have a concentration in Al atoms of about 25 g/liter. This liquid (also called leachate) will be used in the hydrochlorination step of the process.

H_2SO_4 leaching step

The solid fraction coming from the neutralization step is mixed with about 3 liters of sulfuric acid 98% at a temperature of about 200 °C for about 2 hours. The mixture is under stirring during all this time in order to solubilize all the Al atoms. Then, when the leaching is completed, about 14 liters of water are added to the mixture to make sure that all the sulfates produced by the reaction are kept in solution. The mixture is stirred for about 2 hours at a temperature of about 100 °C in order to maximize the solubilization.

Then, when the mixture was back at room temperature, it was filtered under vacuum. The so-obtained liquid fraction was used in the neutralization step of the process to solubilize the aluminium hydroxide contained in the solid phase of the conversion step. The solid fraction, which is the solid residue of the process, has to be wasted.

Hydrochlorinating

The neutralization step liquid (about 21 liters) is cooled down to 0 °C . Then it was treated with gaseous HCl and the reaction was carried out at a temperature of about -4 °C to 4 °C. The hydrochlorination is carried out until the solution is saturated. The gaseous HCl thereby introduced causes aluminium chloride formation and precipitation. Then, the so-obtained cold mixture is filtered under vacuum so as to provide about 8 700 grams of

aluminium chloride hydrate and about 24 liters of a waste liquid. This liquid could be further distilled to recover sulfuric acid and hydrochloridric acid.

Pyrohydrolysis of aluminium chloride into alumina

The aluminium chloride obtained in the hydrochlorinating step is then optionally converted into alumina by means of a pyrohydrolysis.

The aluminium chloride is heated at a temperature of about 500 °C for about 2 hours in order to convert the aluminium chloride into aluminium hydroxide and gaseous HCl. Then, the so-obtained material is washed with hot water at about 80 °C to remove chloride salt. The product is then heated for 15 minutes at about 1050 °C to convert aluminium hydroxide into gamma-alumina thereby providing about 990 g of alumina having a degree of purity of at least 98 %. The 100 % theoretical yield of conversion of all the Al atoms contained in the Noval should provide 995 g the Al atoms of the dross residues into alumina was 99.5 %.

It was found that the processes described in the present document are quite simple and that they can be carried out at low costs. It was also found that such processes propose efficient ways to valorize aluminium dross residues by converting the Al atoms comprised therein into aluminium chloride. Such processes permit to recuperate, recover or extract very high yields of Al atoms from aluminium dross residues and convert them into aluminium chloride and optionally into alumina. It was found that by submitting aluminium dross residues with one leaching using H_2SO_4 , it was possible to valorize a very high percentage of the total weight aluminium dross residues and convert it in aluminium chloride and eventually, if desired, into alumina.

While the invention has been described in connection with specific embodiments thereof, it will be understood that it is capable of further modifications and this application is intended to cover any variations, uses, or adaptations of the invention following, in general, the principles of the invention and including such departures from the present disclosure as come

within known or customary practice within the art to which the invention pertains and as may be applied to the essential features hereinbefore set forth, and as follows in the scope of the appended claims.

WHAT IS CLAIMED IS:

1. A process for treating aluminium dross residues comprising:
 - leaching said aluminium dross residues with H_2SO_4 so as to obtain a leachate; and
 - hydrochlorinating said leachate so as to obtain aluminium chloride.
2. The process of claim 1, wherein said leaching is carried out at a temperature of at least 70 °C.
3. The process of claim 1, wherein said leaching is carried out at a temperature of at least 160 °C
4. The process of claim 1, wherein said leaching step is carried out at a temperature of at least 250 °C.
5. The process of claim 1, wherein after said leaching step a mixture comprising a solid phase and a liquid phase is obtained, and wherein said two phases are separated.
6. The process of claim 5, wherein said two phases are separated by means of a filtration under vacuum.
7. The process of claim 5 or 6, wherein the solid phase is treated with water having a temperature of at least 30 °C so as to solubilize metals and minerals contained therein and to obtain said leachate.
8. The process of claim 5 or 6, wherein the solid phase is treated with water having a temperature of at least 50 °C so as to solubilize metals and minerals contained therein and to obtain said leachate.

9. The process of claim 5 or 6, wherein the solid phase is treated with water having a temperature of at least 70 °C so as to solubilize metals and minerals contained therein and to obtain said leachate.
10. The process of any one of claims 1 to 9, wherein said leachate is hydrochlorinated with gaseous HCl.
11. The process of any one of claims 1 to 10, wherein said hydrochlorination is carried out at a temperature of about -10 °C to about 20 °C.
12. The process of any one of claims 1 to 10, wherein said hydrochlorination is carried out at a temperature of about -10 °C to about 0 °C.
13. The process of any one of claims 1 to 12, further comprising converting said aluminium chloride into alumina.
14. The process of claim 13, wherein the conversion from aluminium chloride to alumina is carried out at a temperature of about 100 °C to about 1400 °C.
15. The process of claim 13, wherein the conversion from aluminium chloride to alumina is carried out at a temperature of about 200 °C to about 1300 °C.
16. The process of claim 13, wherein the conversion from aluminium chloride to alumina is carried out at a temperature of about 950 °C to about 1150 °C.
17. The process of claim 13, wherein said aluminium chloride is converted into aluminium hydroxide by heating said aluminium chloride at a temperature of at least 100 °C, and then said aluminium

hydroxide is converted into alumina by heating said aluminium hydroxide at a temperature of at least 450°C.

18. The process of claim 17, further comprising washing said aluminium hydroxide so as to remove chloride salts.
19. The process of claim 17 or 18, wherein aluminium chloride is heated at a temperature of at least 650 °C.
20. The process of claim 17 or 18, wherein aluminium hydroxide is heated at a temperature of at least 950 °C.
21. The process of any one of claims 13 to 20, wherein in the conversion from aluminium chloride to alumina, at least 50 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
22. The process of any one of claims 13 to 20, wherein in the conversion from aluminium chloride to alumina, at least 70 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
23. The process of any one of claims 13 to 20, wherein in the conversion from aluminium chloride to alumina, at least 80 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
24. The process of any one of claims 13 to 20, wherein in the conversion from aluminium chloride to alumina, about 80 to about 95 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
25. The process of any one of claims 13 to 24, wherein the alumina obtained has a purity of at least 80 %.

26. The process of any one of claims 13 to 24, wherein the alumina obtained has a purity of at least 90 %.
27. The process of any one of claims 13 to 24, wherein the alumina obtained has a purity of about 93 to about 99 %.
28. The process of any one of claim 1 to 27, wherein said leaching step is carried out using a H_2SO_4 solution having a concentration of about 50 to about 98%.
29. The process of any one of claim 1 to 27, wherein said leaching step is carried out using a H_2SO_4 solution having a concentration of about 70 to about 98%.
30. The process of any one of claim 1 to 27, wherein said leaching step is carried out using a H_2SO_4 solution having a concentration of about 98%.
31. A process for treating aluminium dross residues comprising:
 - treating said aluminium dross residues so as to reduce the amount of aluminium nitride present therein;
 - leaching said aluminium dross residues with H_2SO_4 so as to obtain a leachate; and
 - hydrochlorinating said leachate so as to obtain aluminium chloride.
32. A process for treating aluminium dross residues comprising:
 - optionally treating said aluminium dross residues so as to reduce the amount of aluminium nitride present therein;
 - leaching said aluminium dross residues with H_2SO_4 so as to obtain a leachate;

- hydrochlorinating said leachate so as to obtain aluminium chloride; and
 - converting said aluminium chloride into alumina.
33. The process of claim 31 or 32, wherein the amount of aluminium nitride is reduced by converting aluminium nitride into aluminium hydroxide.
34. The process of claim 31 or 32, wherein at least 80% of the aluminium nitride present in the aluminium dross residues is converted into aluminium hydroxide.
35. The process of claim 31 or 32, wherein at least 95 % of the aluminium nitride present in the aluminium dross residues is converted into aluminium hydroxide.
36. The process of any one of claims 33 to 35, wherein aluminium nitride is converted into aluminium hydroxide by reacting said aluminium dross residues with water having a temperature of at least 80 °C.
37. The process of claim 36, wherein water is at a temperature around its boiling point.
38. The process of any one of claims 33 to 37, wherein a solid is recovered after said conversion of aluminium nitride into aluminium hydroxide and said solid is leached with H_2SO_4 so as to solubilize at least a portion of said aluminium hydroxide, thereby obtaining said leachate and another solid.
39. The process of claim 38, wherein said solid is treated with a solution comprising H_2SO_4 and aluminium sulfate.

40. The process of claim 38 or 39, wherein said another solid is leached with H_2SO_4 in order to obtain another leachate.
41. The process of any one of claims 31 to 40, wherein said leachate and said another leachate are hydrochlorinated with gaseous HCl .
42. The process of claim 41, wherein said hydrochlorination is carried out at a temperature of about $-10\text{ }^\circ\text{C}$ to about $20\text{ }^\circ\text{C}$.
43. The process of any one of claims 31 to 42, wherein said hydrochlorination is carried out at a temperature of about $-10\text{ }^\circ\text{C}$ to about $0\text{ }^\circ\text{C}$.
44. The process of claim 31, further comprising converting said aluminium chloride into alumina.
45. The process of claim 32 or 44, wherein the conversion from aluminium chloride to alumina is carried out at a temperature of about $100\text{ }^\circ\text{C}$ to about $1400\text{ }^\circ\text{C}$.
46. The process of claim 32 or 44, wherein the conversion from aluminium chloride to alumina is carried out at a temperature of about $200\text{ }^\circ\text{C}$ to about $1300\text{ }^\circ\text{C}$.
47. The process of claim 32 or 44, wherein the conversion from aluminium chloride to alumina is carried out at a temperature of about $950\text{ }^\circ\text{C}$ to about $1150\text{ }^\circ\text{C}$.
48. The process of claim 32 or 44, wherein said aluminium chloride is converted into aluminium hydroxide by heating said aluminium chloride at a temperature of at least $100\text{ }^\circ\text{C}$, and then said aluminium hydroxide is converted into alumina by heating said aluminium hydroxide at a temperature of at least $450\text{ }^\circ\text{C}$.

49. The process of claim 48, further comprising washing said aluminium hydroxide so as to remove chloride salts.
50. The process of claim 48 or 49, wherein aluminium chloride is heated at a temperature of at least 650 °C.
51. The process of claim 48 or 49, wherein aluminium hydroxide is heated at a temperature of at least 950 °C.
52. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, at least 50 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
53. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, at least 70 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
54. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, at least 80 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
55. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, at least 90 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
56. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, at least 95 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
57. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, at least 99 % by

weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.

58. The process of any one of claims 32 and 44 to 51, wherein in the conversion from aluminium chloride to alumina, about 80 to about 95 % by weight of the Al atoms contained in the aluminium dross residues are thereby obtained in the form of alumina.
59. The process of any one of claims 32 and 44 to 58, wherein the alumina obtained has a purity of at least 80 %.
60. The process of any one of claims 32 and 44 to 58, wherein the alumina obtained has a purity of at least 90 %.
61. The process of any one of claims 32 and 44 to 58, wherein the alumina obtained has a purity of about 93 to about 99 %.
62. The process of any one of claim 31 to 61, wherein said leaching step is carried out using a H_2SO_4 solution having a concentration of about 50 to about 98%.
63. The process of any one of claim 31 to 61, wherein said leaching step is carried out using a H_2SO_4 solution having a concentration of about 70 to about 98%.
64. The process of any one of claim 31 to 61, wherein said leaching step is carried out using a H_2SO_4 solution having a concentration of about 98%.

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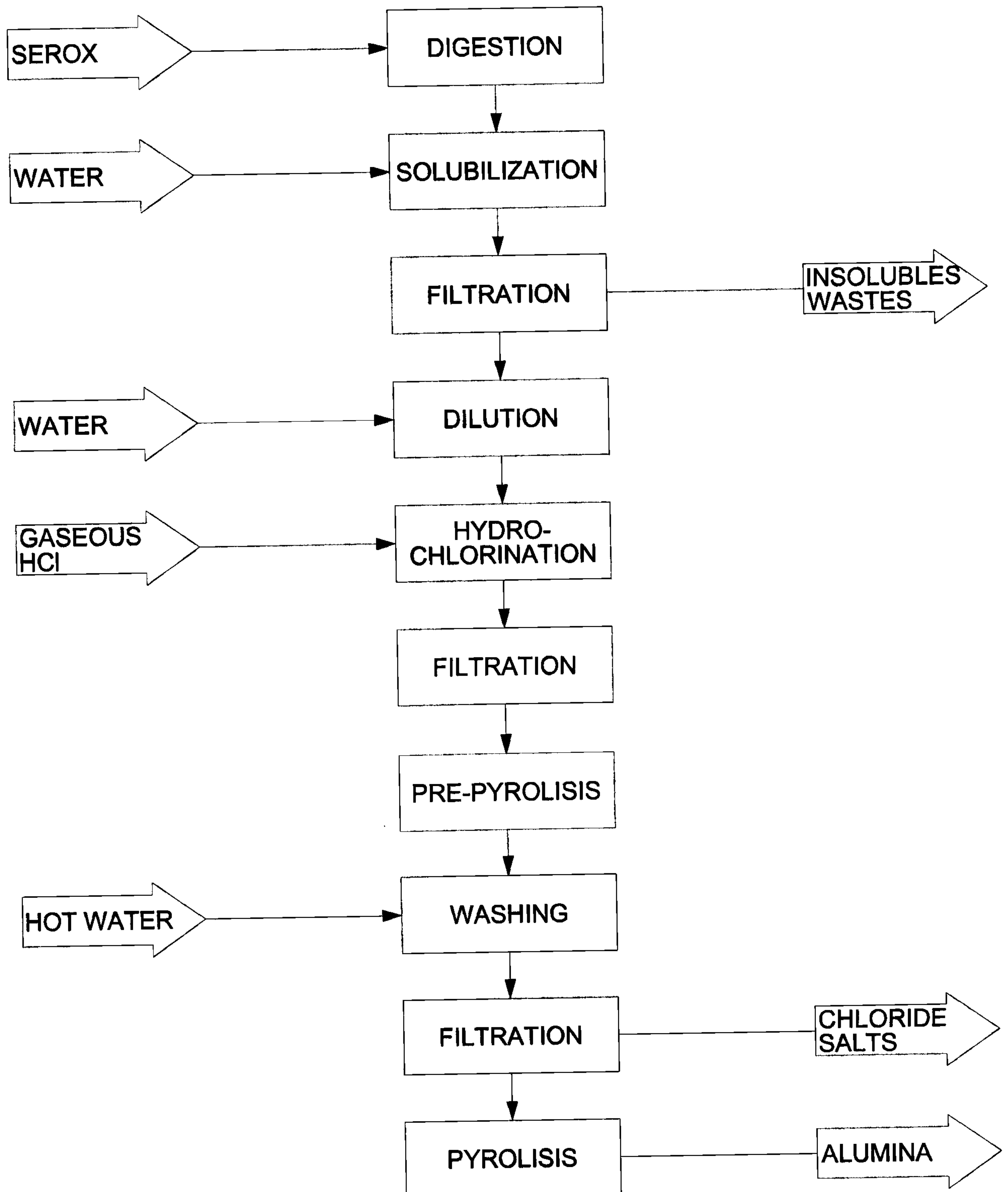


FIG.1

2/2

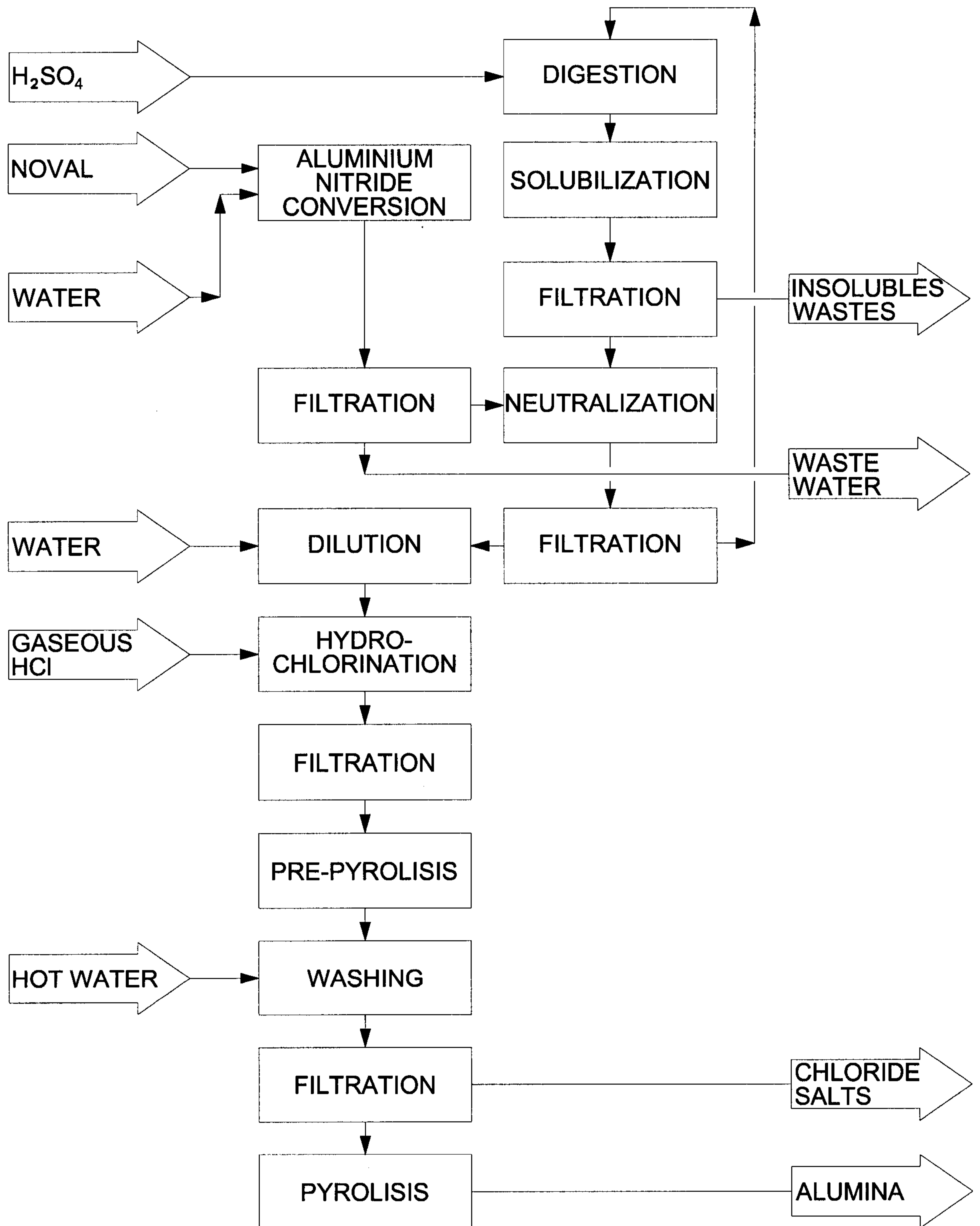


FIG.2

