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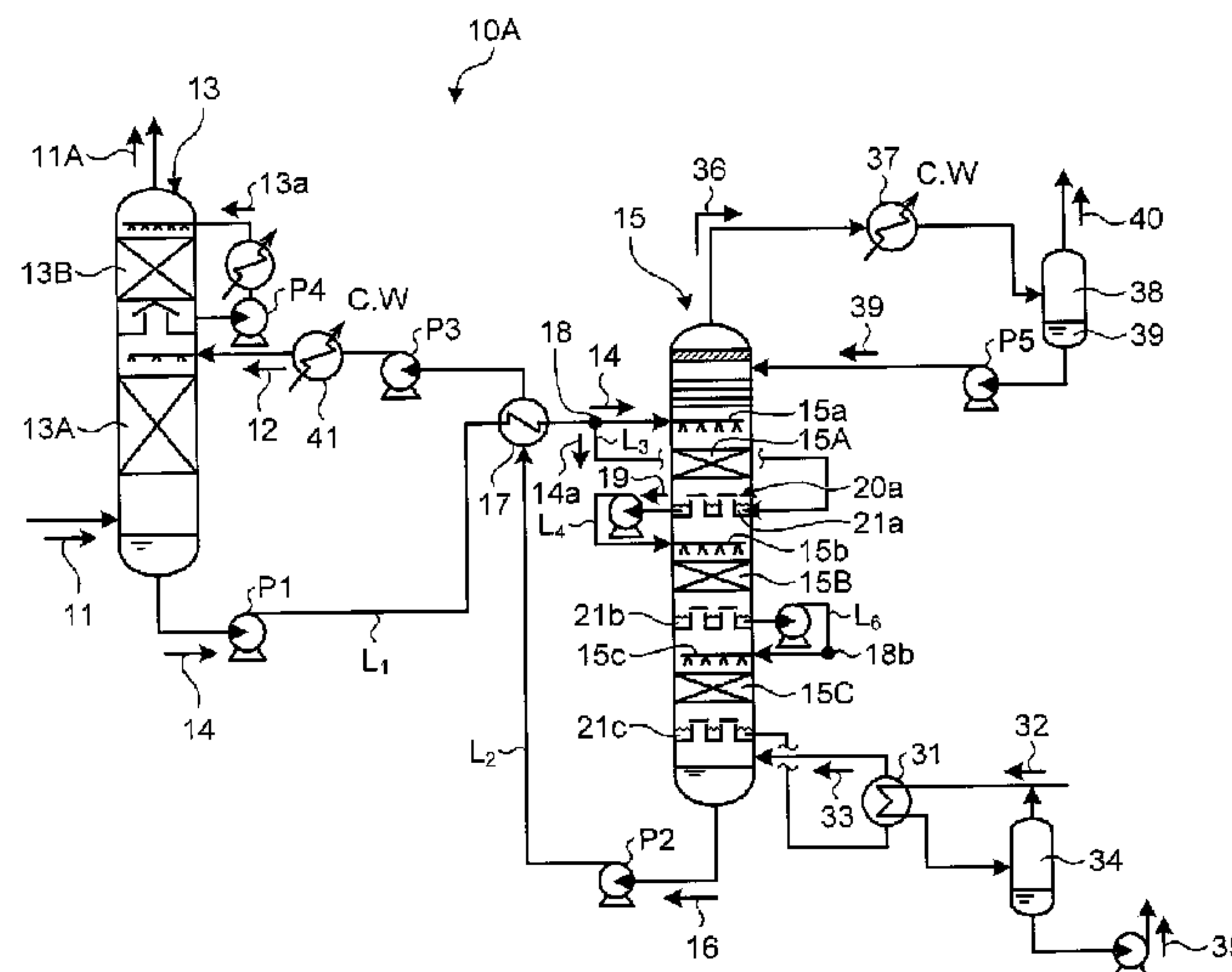
(72) Inventeurs/Inventors:
TANAKA, HIROSHI, JP;
HIRATA, TAKUYA, JP;
OISHI, TSUYOSHI, JP;
ENDO, TAKAHIKO, JP;
ITO, HIROAKI, JP

(73) Propriétaires/Owners:
MITSUBISHI HEAVY INDUSTRIES, LTD., JP;
THE KANSAI ELECTRIC POWER CO., INC., JP

(74) **Agent:** SMART & BIGGAR

(54) Titre : DISPOSITIF DE RECUPERATION DE CO₂

(54) Title: CO₂ RECOVERY UNIT



(57) Abrégé/Abstract:

An absorbent regenerator 15 is divided into at least two parts and includes: a rich solution supply line L_1 through which a rich solution 14 is supplied to the absorbent regenerator 15 from a CO_2 absorber 13; a lean solution supply line L_2 through which a lean solution 16 is supplied to the CO_2 absorber 13 from the absorbent regenerator 15; a lean-rich solution heat exchanger 17 that is provided at an intersection of the lean solution supply line L_2 and the rich solution supply line L_1 to exchange heat between the lean solution 16 and the rich solution 14; a branch portion 18 that branches some 14a of the rich solution 14 at a downstream side of the lean-rich solution heat exchanger 17 on the rich solution supply line L_1 ; and a first mixing portion 20a that mixes the some 14a of the rich solution 14 branched at the branch portion 18 with a semi-lean solution 19 in which CO_2 has been partially removed from the rich solution 14 in the absorbent regenerator 15.

ABSTRACT

An absorbent regenerator 15 is divided into at least two parts and includes: a rich solution supply line L_1 through which a rich solution 14 is supplied to the absorbent regenerator 15 from a CO_2 absorber 13; a lean solution supply line L_2 through which a lean solution 16 is supplied to the CO_2 absorber 13 from the absorbent regenerator 15; a lean-rich solution heat exchanger 17 that is provided at an intersection of the lean solution supply line L_2 and the rich solution supply line L_1 to exchange heat between the lean solution 16 and the rich solution 14; a branch portion 18 that branches some 14a of the rich solution 14 at a downstream side of the lean-rich solution heat exchanger 17 on the rich solution supply line L_1 ; and a first mixing portion 20a that mixes the some 14a of the rich solution 14 branched at the branch portion 18 with a semi-lean solution 19 in which CO_2 has been partially removed from the rich solution 14 in the absorbent regenerator 15.

DESCRIPTION

CO₂ RECOVERY UNIT

Field

[0001] The present invention relates to a CO₂ recovery
5 unit capable of reducing the amount of water vapor at the
time of regeneration of a CO₂ absorbent.

Background

[0002]

Recently, a greenhouse effect caused by CO₂ is noted
10 as one reason of having global warming phenomenon. Thus, a
solution for protecting earth and environment is urgently
needed all over the world. As a source for generating CO₂,
there is every human activity which is involved with
combustion of fossil fuel, and thus a demand for inhibited
15 emission tends to increase more than ever. Accordingly,
for power generating facilities like thermoelectric power
station which uses a large amount of fossil fuel, extensive
studies are made on a method of removing and recovering CO₂
in flue gas by bringing flue gas from a boiler into contact
20 with an amine-based CO₂ absorbent and a method of storing
recovered CO₂ without release to air. Furthermore, as a
process used for removing and recovering CO₂ in flue gas by
using an CO₂ absorbent, there is a process in which flue
gas is brought into contact with a CO₂ absorbent in an
25 absorber, the absorbent after absorption of CO₂ is heated
in a regenerator, and with release of CO₂, the absorbent is
regenerated and recycled to the absorber for reuse (for
example, see Patent Literature 1).

[0003] According to a method of removing and recovering
30 CO₂ from CO₂ containing gas like flue gas by using an CO₂
absorbent and the process described above, the process is
annexed to facilities for combustion, and thus the cost
related to the operation should be reduced as much as

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possible. Among the above processes, the regeneration process particularly consumes a large amount of heat energy, and thus it needs to be provided as a process which can save the energy as much as possible.

- 5 [0004] Accordingly, a suggestion has been made in a related art that part of a semi-lean solution is discharged to the outside from a regenerator for heat exchange with a lean solution in a heat exchanger, subjected to heat exchange with steam condensate in a heat exchanger, and returned to a lower
10 side than the extraction area, and by increasing the temperature of a semi lean solution fed to the bottom side of a regenerator, steam consumption amount is reduced (for example, see Patent Literature 2 (Example 8 and FIG. 17)).

Citation List

15 Patent Literature

[0005] Patent Literature 1: Japanese Laid-open Patent Publication No. 7-51537

Patent Literature 2: Japanese Laid-open Patent Publication No. 2005-254212

20 Summary

- [0006] By the way, a CO₂-absorbed rich solution to be introduced into an absorbent regenerator exchanges heat with a lean solution regenerated by the absorbent regenerator and is introduced into an upper part of the absorbent regenerator at a
25 high temperature of 100°C, for example, the total amount of rich solution being introduced into the upper part of the

absorbent regenerator at a time. As a result, CO₂ and water vapor are flushed from the rich solution introduced into the absorbent regenerator, and then the CO₂ gas and the water vapor are together released to the outside from the top of the

5 regenerator. After the CO₂ gas and the water vapor are cooled in a condenser provided at a downstream side of the top of the regenerator, moisture is separated in a separation drum for a gas-solution separation. However, at this time, because a rich solution is introduced at a time, the flush amount and the

10 amount of moisture to be separated increase, and the amount of water vapor to be consumed increases to that extent. As a result, there are problems that an excessive CO₂ dissipation load and an imbalance heat distribution occur at the top side of the regenerator and energy saving of renewable energy cannot

15 be achieved.

[0007] Accordingly, the reduction of the amount of water vapor is further desired to reduce the consumption of heat energy in the regeneration process of the absorbent.

[0008] An aspect of the present invention has been achieved

20 to solve the above problems, and an object thereof is to provide a CO₂ recovery unit capable of significantly reducing the amount of water vapor and further improving energy efficiency.

[0008a] According to an aspect of the present invention,

25 there is provided a CO₂ recovery unit comprising: a CO₂ absorber in which a CO₂-containing gas comes into contact with a CO₂ absorbent to remove CO₂; an absorbent regenerator which includes an upper stage and a lower stage and in which a CO₂-absorbed rich solution is regenerated by a regenerating heater,

thereby reusing a lean solution in which CO_2 has been removed in the absorbent regenerator, in the CO_2 absorber as the CO_2 absorbent; a rich solution supply line through which the rich solution is supplied to a topside of the upper stage of the

5 absorbent regenerator from the CO_2 absorber; a lean solution supply line through which the lean solution is supplied to the CO_2 absorber from the absorbent regenerator; a lean-rich solution heat exchanger that is provided at an intersection of the lean solution supply line and the rich solution supply line

10 to exchange heat between the lean solution and the rich solution; a branch portion that branches some of the rich solution at a downstream side of the lean-rich solution heat exchanger on the rich solution supply line; and a mixing portion that mixes the some of the rich solution branched at

15 the branch portion with a semi-lean solution in which CO_2 has been partially removed from the rich solution in the absorbent regenerator, wherein a front end of a branch line through which the some of the branched rich solution is supplied is connected to a solution storage portion of the semi-lean solution which

20 is located at a bottom of the upper stage of the regenerator to mix the some of the branched rich solution with the semi-lean solution.

[0008b] According to another aspect of the present invention, there is provided a CO_2 recovery unit comprising: a CO_2

25 absorber in which a CO_2 -containing gas comes into contact with a CO_2 absorbent to remove CO_2 ; an absorbent regenerator which includes an upper stage and a lower stage and in which a CO_2 -absorbed rich solution is regenerated by a regenerating heater, thereby reusing a lean solution in which CO_2 has been removed

30 in the absorbent regenerator, in the CO_2 absorber as the CO_2

absorbent; a rich solution supply line through which the rich solution is supplied to a topside of the upper stage of the absorbent regenerator from the CO₂ absorber; a lean solution supply line through which the lean solution is supplied to the CO₂ absorber from the absorbent regenerator; a lean-rich solution heat exchanger that is provided at an intersection of the lean solution supply line and the rich solution supply line to exchange heat between the lean solution and the rich solution; a branch portion that branches some of the rich solution at a downstream side of the lean-rich solution heat exchanger on the rich solution supply line; and a line mixing portion that mixes the some of the rich solution branched at the branch portion with a semi-lean solution in which CO₂ has been partially removed from the rich solution in the absorbent regenerator, wherein the line mixing portion is provided with a semi-lean solution extracting line through which the semi-lean solution is extracted from a solution storage portion of the semi-lean solution located at a bottom of the upper stage of the absorbent regenerator to be supplied to a lower stage of the absorbent regenerator, and a front end of a branch line through which the some of the rich solution is supplied is connected to the semi-lean solution extracting line to form the line mixing portion.

[0009] A first aspect provides a CO₂ recovery unit including a CO₂ absorber in which a CO₂-containing gas comes into contact with a CO₂ absorbent to remove CO₂, and an absorbent regenerator in which a CO₂-absorbed rich solution is regenerated by a regenerating heater, thereby reusing a lean solution in which CO₂ has been removed in the absorbent regenerator, in the CO₂ absorber as the CO₂ absorbent, wherein

the absorbent regenerator is divided into at least two parts and has a rich solution supply line through which the rich solution is supplied to the absorbent regenerator from the CO₂ absorber, a lean solution supply line through which the lean
5 solution is supplied to the CO₂ absorber from the absorbent regenerator, a lean-rich solution heat exchanger that is provided at an intersection of the lean solution supply line and the rich solution supply line to exchange heat between the lean solution and the rich solution, a branch portion that
10 branches some of the rich solution at a downstream side of the lean-rich solution heat exchanger on the rich solution supply line, and a mixing portion that mixes the some of the rich solution branched at the branch portion with a semi-lean solution in which CO₂ has been partially removed from the rich
15 solution in the absorbent regenerator.

[0010] A second aspect is the CO₂ recovery unit according to the first aspect, wherein a front end of a branch line through which the some of the branched rich solution is supplied is connected to a solution storage portion of the semi-lean
20 solution which is located at an upper stage side of the absorbent regenerator divided into parts to mix the some of the branched rich solution with the semi-lean solution.

[0011] A third aspect is the CO₂ recovery unit according to the first aspect, wherein the mixing portion is provided with a
25 semi-lean solution extracting line through which the semi-lean solution is extracted from the solution storage portion located at the upper stage side of the absorbent regenerator divided into parts and the extracted semi-lean solution is supplied to a lower stage side of the absorbent regenerator, and the front

end of the branch line through which the some of the branched rich solution is supplied is connected to the semi-lean solution extracting line to form a mixing portion in which the some of the branched rich solution is mixed with the semi-lean
5 solution.

[0012] In one embodiment, a fourth aspect is the CO₂ recovery unit according to the third aspect, wherein at an upstream side of the lean-rich solution heat exchanger interposed on the lean solution supply line, a lean and semi-lean solution heat
10 exchanger is provided at an intersection of the lean solution supply line and the semi-lean solution extracting line, and after the some of the branched rich solution and the semi-lean solution are mixed with each other in the mixing portion, the mixed solution exchanges heat with the lean solution in the lean
15 and semi-lean solution heat exchanger.

[0013] In another embodiment, a fifth aspect is the CO₂ recovery unit according to the fourth aspect, including a steam condensate heat exchanger that is interposed at a downstream side of the mixing portion on the semi-lean solution extracting
20 line to heat the mixed solution of the some of the branched rich solution and the semi-lean solution using residual heat of steam condensate from a regenerating heater of the absorbent regenerator.

[0014] According to one aspect, some of a rich solution are
25 branched before being introduced into an absorbent regenerator, and some of the branched rich solution are mixed with a semi-lean solution obtained by a removal of some of CO₂ from the rich solution in the absorbent regenerator, whereby an excessive dissipation load of CO₂ is prevented and heat

distribution is improved at the top side of the regenerator,
and thus energy saving can be achieved.

Brief Description of Drawings

[0015] FIG. 1 is a schematic view illustrating a
5 configuration of a CO₂ recovery unit according to a first
embodiment.

FIG. 2 is a schematic view illustrating a configuration of another CO₂ recovery unit according to the first embodiment.

FIG. 3 is a schematic view illustrating a configuration of a CO₂ recovery unit according to a second embodiment.

FIG. 4 is a schematic view illustrating a configuration of a CO₂ recovery unit according to a third embodiment.

FIG. 5 is a schematic view illustrating a configuration of another CO₂ recovery unit according to a fourth embodiment.

FIG. 6 is a diagram illustrating a relation between a rich-solution branch supply rate (%) and a CO₂ recovery heat quantity reduction rate according to the first embodiment.

FIG. 7 is a diagram illustrating a relation between a rich-solution branch supply rate (%) and a CO₂ recovery heat quantity reduction rate according to the second embodiment.

FIG. 8 is a diagram illustrating a relation between a rich-solution branch supply rate (%) and a CO₂ recovery heat quantity reduction rate according to the third embodiment.

Description of Embodiments

[0016] Hereinafter, preferred embodiments of the present invention will be described in detail with reference to the accompanying drawings. The present invention is not limited by these embodiments, but may be constituted in combination with each of embodiments when several embodiments are presented.

First Embodiment

[0017] CO₂ recovery units according to embodiments of

the present invention will be described with reference to FIG. 1.

FIG. 1 is a schematic view illustrating a configuration of a CO₂ recovery unit according to a first embodiment. As illustrated in FIG. 1, a CO₂ recovery unit 10A according to the first embodiment is a CO₂ recovery unit including: a CO₂ absorber 13 (hereinafter, also referred to as an "absorber") in which a CO₂-containing flue gas (hereinafter, also referred to as a "flue gas") 11 comes into contact with a CO₂ absorbent 12 to remove CO₂, and an absorbent regenerator (hereinafter, also referred to as a "regenerator") 15 in which a CO₂-absorbed rich solution 14 is regenerated by a regenerating heater, thereby reusing a lean solution 16, which is obtained by a partial removal of CO₂ in the absorbent regenerator 15, in the CO₂ absorber 13 as a CO₂ absorbent. In the CO₂ recovery unit, the absorbent regenerator 15 is divided into at least two parts (three parts in this embodiment), and includes: a rich solution supply line L₁ through which the rich solution 14 is supplied to the absorbent regenerator 15 from the CO₂ absorber 13; a lean solution supply line L₂ through which the lean solution 16 is supplied to the CO₂ absorber 13 from the absorbent regenerator 15; a lean-rich solution heat exchanger 17 that is provided at an intersection of the lean solution supply line L₂ and the rich solution supply line L₁ to exchanges heat between the lean solution 16 and the rich solution 14; a branch portion 18 that branches some 14a of the rich solution 14 at a downstream side of the lean-rich solution heat exchanger 17 on the rich solution supply line L₁; and a first mixing portion 20a that mixes some 14a of the rich solution branched at the branch portion 18 with a semi-lean solution 19 which is obtained by the partial removal of CO₂ from the

rich solution 14 in the absorbent regenerator 15.

In the drawings, reference numeral 15A represents a first division portion of the regenerator 15, reference numeral 15B represents a second division portion, reference numeral 15C represents a third division portion, reference numeral 15a represents a first solution dispersion portion, reference numeral 15b represents a second solution dispersion portion, and reference numeral 15c represents a third solution dispersion portion.

10 [0018] In a CO₂ recovery method using the CO₂ recovery unit, first, a flue gas 11 containing CO₂ released from a boiler, a gas turbine, or the like is cooled by a gas cooling system (not illustrated) and is then sent to the CO₂ absorber 13.

15 [0019] In the CO₂ absorber 13, for example, the flue gas 11 comes into countercurrent contact with an amine-based CO₂ absorbent 12, and the CO₂ contained in the flue gas 11 is absorbed by the CO₂ absorbent 12 through a chemical reaction.

20 A CO₂-removed flue gas obtained after CO₂ is removed by a CO₂ recovery portion 13A comes into gas-solution contact with circulation washing water 13a supplied from a solution distributor in a water washing portion 13B provided in the CO₂ absorber 13, the CO₂ absorbent 12
25 accompanied with the CO₂-removed flue gas is recovered, and then a CO₂-removed flue gas 11A obtained by the removal of CO₂ is released to the outside of the unit. The circulation washing water 13a is circulated by a solution circulating pump P4.

30 In addition, a rich solution 14 serving as the CO₂ absorbent 12 which has absorbed CO₂ is pressurized by a rich solution pump P1, heated by a lean solution 16 serving as the CO₂ absorbent 12 regenerated by the regenerator 15

in the lean-rich solution heat exchanger 17, and supplied to the regenerator 15.

[0020] The rich solution 14 released to the inside from an upper part of the regenerator 15 absorbs heat by water vapor supplied from the bottom and releases most of CO₂. The CO₂ absorbent from which some or most of CO₂ are released in the inside of the regenerator 15 is called the "semi-lean solution 19". The semi-lean solution 19 becomes the CO₂ absorbent 12 from which almost all CO₂ are removed when reaching the bottom of the regenerator 15. Out of the lean solution 16 from which most of CO₂ are removed, some are heated by water vapor 32 in a regenerating heater 31, and water vapor 33 is supplied into the regenerator 15. In the drawings, reference numeral 34 represents a gas-liquid separator, and reference numeral 35 represents steam condensate.

[0021] Meanwhile, a CO₂ gas 36 is guided from the top of the regenerator 15, the CO₂ gas 36 being released from the rich solution 16 and the semi-lean solution 19 in the regenerator and accompanying with the water vapor, the water vapor is condensed by a condenser 37, and water is separated by a separation drum 38. A CO₂ gas 40 separated by the separation drum 38 is released to the outside of the unit, and is recovered after being compressed by a separate compressor. The recovered CO₂ gas 40 is pressed into an oil field using, for example, an enhanced oil recovery (EOR) or is stored in an aquifer as a measure for dealing with global warming.

[0022] Reflux water 39, which is separated and refluxed from the CO₂ gas 36 in the separation drum 38, is supplied to the upper part of the regenerator 15 by a reflux water circulating pump P5.

The regenerated CO₂ absorbent (lean solution 16) is

cooled by a heat exchange with the rich solution 14 in the lean-rich solution heat exchanger 17. Subsequently, the cooled CO₂ absorbent is pressurized by a lean solution pump P3, and is supplied into the CO₂ absorber 13 after being
5 further cooled by a lean solution cooler 41.

[0023] In this embodiment, some of the rich solution 14 heated by the heat exchange with the lean solution 16 in the lean-rich solution heat exchanger 17 are branched at a branch portion 18, a front end of a branch line L₃ branched
10 from the branch portion 18 is connected to a first solution storage portion 21a of the semi-lean solution 19, which is located at an upper stage side of the regenerator 15 divided into a plurality of stages, and thus some 14a of the branched rich solution 14 and the semi-lean solution 19
15 are mixed by a first mixing portion 20a.

[0024] The mixed solution is extracted from the first solution storage portion 21a, introduced into a second solution dispersion portion 15b of a second division portion 15B located at a lower stage side by a first semi-
20 lean solution extracting line L₄, and comes into contact with a gas containing water vapor, whereby CO₂ is released. In addition, a second semi-lean solution extracted from a second solution storage portion 21b is introduced into a third solution dispersion portion 15c of a third division
25 portion 15C located at a further lower stage side by a second semi-lean solution extracting line L₆, and comes into contact with a gas containing water vapor, whereby CO₂ is released.

[0025] As a result, since some of the rich solution 14
30 are branched, it is possible to prevent the increase of the flush amount of CO₂ and water caused by the introduction of the total amount of the rich solution 14 heated by the heat exchange in the lean-rich solution heat exchanger 17 into

the upper part of the regenerator 15 as in the related art,
and to achieve energy saving by the prevention of the
dissipation load of the excessive CO₂ and the improvement
of the heat distribution at the top side of the regenerator
5 15.

[0026] In this embodiment, the mixing portion is defined
by the introduction of the front end of the line into a
sidewall of the regenerator 15, but a line mixing portion
may be provided to directly mix with the semi-lean solution
10 extracting line L₄.

[0027] FIG. 6 is a diagram illustrating a relation
between a rich-solution branch supply rate (%) and a CO₂
recovery heat quantity reduction rate according to the
first embodiment. Here, a case where the rich solution is
15 not branched (branch supply rate is 0%) is set as a
reference. As illustrated in FIG. 6, when the branch
supply rate exceeds 20%, a branch effect is exhibited.

[0028] FIG. 2 is a schematic view illustrating a
configuration of another CO₂ recovery unit according to the
20 first embodiment. As illustrated in FIG. 2, in a CO₂
recovery unit 10B according to a second embodiment, a
regenerator 15 is divided into three parts, a first semi-
lean solution extracting line L₄ is provided to extract a
semi-lean solution 19 existing in a first division portion
25 from a first solution storage portion 21a, a first branch
portion 18a is provided on the first semi-lean solution
extracting line L₄ to branch a semi-lean solution 19, some
of the branched semi-lean solution 19 are introduced into a
second solution storage portion 21b of a second division
30 portion by a branch line L₅, and thus a second mixing
portion 20b is formed.

In addition, a second semi-lean solution extracting
line L₆ is provided to extract a semi-lean solution 19

existing in a second division portion 15B from the second solution storage portion 21b, a second branch portion 18b is provided on the second semi-lean solution extracting line L_6 to branch the semi-lean solution 19, some of the branched semi-lean solution 19 are introduced into a third solution storage portion 21c in a third division portion 15C by a branch line L_7 , and thus a third mixing portion 20c is formed.

[0029] In this way, after a rich solution 14 obtained by a heat exchange in a lean-rich solution heat exchanger 17 is branched by a branch portion 18, the first branch portion 18a and the second branch portion 18b are provided on the semi-lean solution extracting lines L_4 and L_6 , respectively, to further extract the semi-lean solution 19, some of the semi-lean solution are introduced into the second solution storage portion 21b and the third solution storage portion 21c and mixed with each other, and thus distribution efficiency is further improved in the regenerator 15.

20 Second Embodiment

[0030] A CO_2 recovery unit according to an embodiment of the present invention will be described with reference to FIG. 3. The same members as in the configuration of the first embodiment are denoted by the same reference numerals, and the duplicated description thereof will not be presented.

FIG. 3 is a schematic view illustrating a configuration of a CO_2 recovery unit according to a second embodiment. As illustrated in FIG. 3, a CO_2 recovery unit 10C according to the second embodiment includes: a semi-lean solution extracting line L_4 through which a semi-lean solution 19 is extracted from a first solution storage portion 21a, which is located at an upper stage side of a

divided absorbent regenerator 15 and stores the semi-lean solution 19, and is supplied to a lower stage side of the absorbent regenerator 15; and a line mixing portion 20A that is provided on the semi-lean solution extracting line L_4 and connects with a front end of a branch line L_3 through which some 14a of the branched rich solution 14 is supplied, thereby mixing some 14a of the branched rich solution 14 with the semi-lean solution 19.

[0031] In addition, at an upstream side of the lean-rich solution heat exchanger 17 interposed in a lean solution supply line L_2 , a lean and semi-lean solution heat exchanger 51 is provided at an intersection of the lean solution supply line L_2 and the semi-lean solution extracting line L_4 , some 14a of the branched rich solution 14 and the semi-lean solution 19 are mixed with each other in the line mixing portion 20A, and then the mixed solution exchanges heat with the lean solution 16 in the lean and semi-lean solution heat exchanger 51.

[0032] In the related art, the semi-lean solution 19 was extracted through the semi-lean solution extracting line L_4 , and the semi-lean solution 19 was heated by exchanging heat in the lean and semi-lean solution heat exchanger 51. In this case, however, the heat of the heat exchange in the lean-rich solution heat exchanger 17 installed at the downstream side of the lean solution supply line L_2 was lowered, the heat held by the rich solution 14 was not sufficient to a dissipation load of CO_2 .

In contrast, as in this embodiment, some 14a of the rich solution 14 are branched by a branch portion 18 and are mixed with the semi-lean solution 19, whereby the rich solution 14 is distributed. Thus, the dissipation load of CO_2 can be equalized, and energy saving of renewable energy can be achieved.

[0033] FIG. 7 is a diagram illustrating a relation between a rich-solution branch supply rate (%) and a CO₂ recovery heat quantity reduction rate according to the second embodiment. Here, a case where the rich solution is not branched (branch supply rate is 0%) is set as a reference. As illustrated in FIG. 7, when the branch supply rate exceeds 20%, a branch effect is exhibited.

Third Embodiment

[0034] A CO₂ recovery unit according to an embodiment of the present invention will be described with reference to FIG. 4. The same members as in the configuration of the first embodiment are denoted by the same reference numerals, and the duplicated description thereof will not be presented.

FIG. 4 is a schematic view illustrating a configuration of a CO₂ recovery unit according to a third embodiment. As illustrated in FIG. 4, compared to the CO₂ recovery unit 10C of the second embodiment, a CO₂ recovery unit 10D according to the third embodiment is further configured to have a regenerator 15 divided into three parts, a first semi-lean solution extracting line L₄ through which a semi-lean solution 19 existing in a first division portion 15A is extracted from a first solution storage portion 21a, and a second semi-lean solution extracting line L₆ through which a semi-lean solution 19 existing in a second division portion 15B is extracted from a second solution storage portion 21b.

[0035] In addition, steam condensate and semi-lean solution heat exchangers 52A and 52B are provided to exchange heat of the semi-lean solution 19 extracted through the first semi-lean solution extracting line L₄ and heat of the semi-lean solution 19 extracted through the second semi-lean solution extracting line L₆ by a steam

condensate 35 of a regenerating heater 31, respectively.

[0036] In this embodiment, the steam condensate and semi-lean solution heat exchangers 52A and 52B are interposed in series with lean solution and semi-lean solution heat exchangers 51A and 51B through the semi-lean solution extracting lines L_4 and L_6 , respectively, such that the semi-lean solution 19 passes through each of the lean solution and semi-lean solution heat exchangers 51A and 51B after passing through each of the steam condensate and semi-lean solution heat exchangers 52A and 52B.

[0037] According to this embodiment, since the semi-lean solution 19 exchanges heat in series between the steam condensate and semi-lean solution heat exchanger 52A and the lean solution and semi-lean solution heat exchanger 51A after being joined with some 14a of a rich solution 14, an excessive dissipation load of CO_2 can be prevented and heat distribution can be improved at the top side of the regenerator 15, thereby achieving energy saving.

[0038] FIG. 8 is a diagram illustrating a relation between a rich-solution branch supply rate (%) and a CO_2 recovery heat quantity reduction rate according to the third embodiment. Here, a case where the rich solution is not branched (branch supply rate is 0%) is set as a reference. As illustrated in FIG. 8, when the branch supply rate exceeds 20%, a branch effect is exhibited.

Fourth Embodiment

[0039] A CO_2 recovery unit according to an embodiment of the present invention will be described with reference to FIG. 5. The same members as in the configuration of the first embodiment are denoted by the same reference numerals, and the duplicated description thereof will not be presented.

As illustrated in FIG. 5, a CO_2 recovery unit 10E

according to the fourth embodiment is further configured to include a first semi-lean solution extracting line L_{4A} and a first semi-lean solution extracting line L_{4B} which are branched from a first semi-lean solution extracting line L_4 and a second semi-lean solution extracting line L_{6A} and a second semi-lean solution extracting line L_{6B} which are branched from a second semi-lean solution extracting line L_6 in the fourth embodiment.

[0040] Then, a steam condensate and semi-lean solution heat exchanger 52A is interposed on the first semi-lean solution extracting line L_{4A} to be branched at a downstream side of a mixing portion of a line mixing portion 20A on the first semi-lean solution extracting line L_4 , and a lean solution and semi-lean solution heat exchanger 51A is interposed on the first semi-lean solution extracting line L_{4B} which is branched.

A semi-lean solution 19 is joined after exchanging heat in the steam condensate and semi-lean solution heat exchanger 52A and the lean solution and semi-lean solution heat exchanger 51A, and is then supplied to a second solution dispersion portion 15b of a second division portion 15B.

[0041] Similarly, a steam condensate and semi-lean solution heat exchanger 52B is interposed on the second semi-lean solution extracting line L_{6A} branched from the second semi-lean solution extracting line L_6 , and a lean solution and semi-lean solution heat exchanger 51B is interposed on the second semi-lean solution extracting line L_{6B} which is branched.

A semi-lean solution 19 is joined after exchanging heat in the steam condensate and semi-lean solution heat exchanger 52B and the lean solution and semi-lean solution heat exchanger 51B, and is then supplied to a third

solution dispersion portion 15c of a third division portion 15C.

[0042] According to this embodiment, since the semi-lean solution 19 exchanges heat in parallel between the steam
5 condensate and semi-lean solution heat exchanger 52A and the lean solution and semi-lean solution heat exchanger 51A after being joined with some 14a of a rich solution 14, an excessive dissipation load of CO₂ can be prevented and heat distribution can be improved at the top side of the
10 regenerator 15, thereby achieving energy saving.

Reference Signs List

[0043] 10A to 10E CO₂ RECOVERY UNIT

	11	CO ₂ -CONTAINING GAS
	12	CO ₂ ABSORBENT
15	13	CO ₂ ABSORBER (ABSORBER)
	14	RICH SOLUTION
	15	ABSORBENT REGENERATOR (REGENERATOR)
	16	LEAN SOLUTION
	20A	LINE MIXING PORTION
20	20a	FIRST MIXING PORTION
	20b	SECOND MIXING PORTION
	20c	THIRD MIXING PORTION
	21a	FIRST SOLUTION STORAGE PORTION
	21b	SECOND SOLUTION STORAGE PORTION
25	21c	THIRD SOLUTION STORAGE PORTION

CLAIMS:

1. A CO₂ recovery unit comprising:
 - a CO₂ absorber in which a CO₂-containing gas comes into contact with a CO₂ absorbent to remove CO₂;
 - 5 an absorbent regenerator which includes an upper stage and a lower stage and in which a CO₂-absorbed rich solution is regenerated by a regenerating heater, thereby reusing a lean solution in which CO₂ has been removed in the absorbent regenerator, in the CO₂ absorber as the CO₂
10 absorbent;
 - a rich solution supply line through which the rich solution is supplied to a topside of the upper stage of the absorbent regenerator from the CO₂ absorber;
 - a lean solution supply line through which the lean
15 solution is supplied to the CO₂ absorber from the absorbent regenerator;
 - a lean-rich solution heat exchanger that is provided at an intersection of the lean solution supply line and the rich solution supply line to exchange heat between the lean
20 solution and the rich solution;
 - a branch portion that branches some of the rich solution at a downstream side of the lean-rich solution heat exchanger on the rich solution supply line; and
 - a mixing portion that mixes the some of the rich
25 solution branched at the branch portion with a semi-lean solution in which CO₂ has been partially removed from the rich

solution in the absorbent regenerator, wherein a front end of a branch line through which the some of the branched rich solution is supplied is connected to a solution storage portion of the semi-lean solution which is located at a bottom of the upper stage of the regenerator to mix the some of the branched rich solution with the semi-lean solution.

2. A CO₂ recovery unit comprising:

a CO₂ absorber in which a CO₂-containing gas comes into contact with a CO₂ absorbent to remove CO₂;

10 an absorbent regenerator which includes an upper stage and a lower stage and in which a CO₂-absorbed rich solution is regenerated by a regenerating heater, thereby reusing a lean solution in which CO₂ has been removed in the absorbent regenerator, in the CO₂ absorber as the CO₂ 15 absorbent;

a rich solution supply line through which the rich solution is supplied to a topside of the upper stage of the absorbent regenerator from the CO₂ absorber;

20 a lean solution supply line through which the lean solution is supplied to the CO₂ absorber from the absorbent regenerator;

a lean-rich solution heat exchanger that is provided at an intersection of the lean solution supply line and the rich solution supply line to exchange heat between the lean 25 solution and the rich solution;

a branch portion that branches some of the rich solution at a downstream side of the lean-rich solution heat exchanger on the rich solution supply line; and

5 a line mixing portion that mixes the some of the rich solution branched at the branch portion with a semi-lean solution in which CO₂ has been partially removed from the rich solution in the absorbent regenerator, wherein the line mixing portion is provided with a semi-lean solution extracting line through which the semi-lean solution is extracted from a
10 solution storage portion of the semi-lean solution located at a bottom of the upper stage of the absorbent regenerator to be supplied to a lower stage of the absorbent regenerator, and

a front end of a branch line through which the some of the rich solution is supplied is connected to the semi-lean
15 solution extracting line to form the line mixing portion.

3. The CO₂ recovery unit according to claim 2, wherein

at an upstream side of the lean-rich solution heat exchanger interposed on the lean solution supply line, a lean and semi-lean solution heat exchanger is provided at an
20 intersection of the lean solution supply line and the semi-lean solution extracting line, and

after the some of the branched rich solution and the semi-lean solution are mixed with each other in the mixing portion, the mixed solution exchanges heat with the lean
25 solution in the lean and semi-lean solution heat exchanger.

4. The CO₂ recovery unit according to claim 3, comprising a steam condensate heat exchanger that is interposed

at a downstream side of the mixing portion on the semi-lean solution extracting line to heat the mixed solution of the some of the branched rich solution and the semi-lean solution using residual heat of steam condensate from a regenerating heater of
5 the absorbent regenerator.

FIG.1

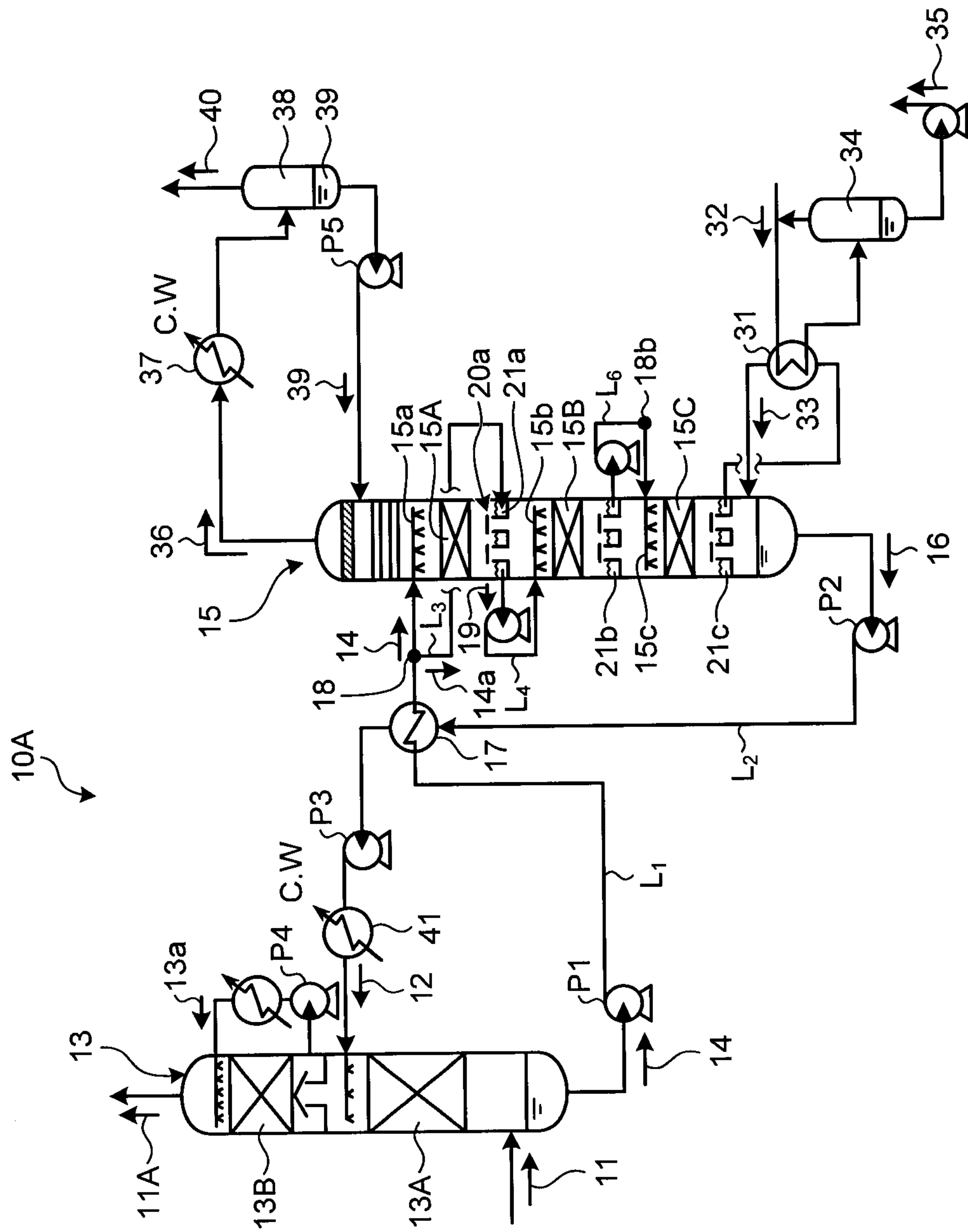


FIG.2

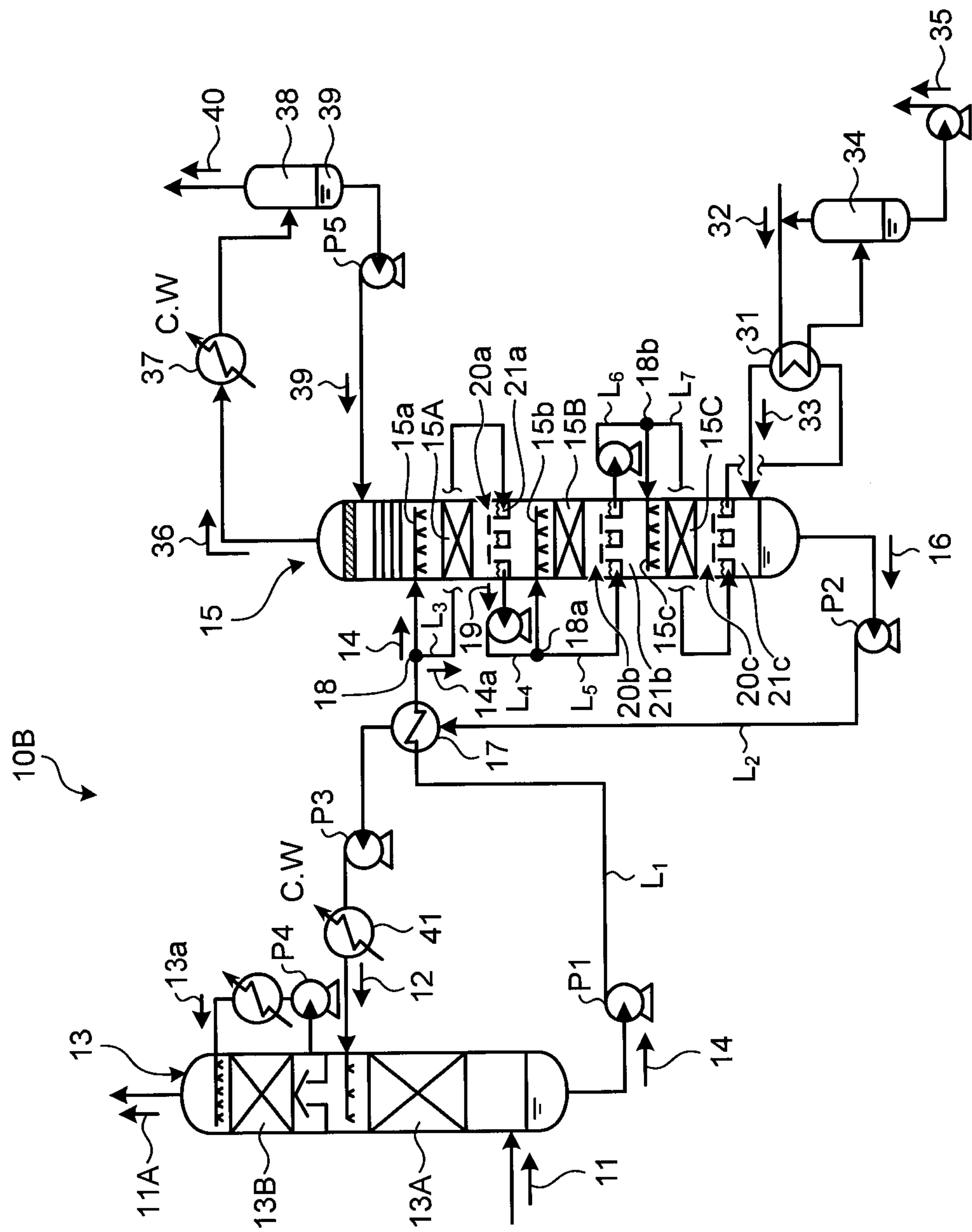


FIG.3

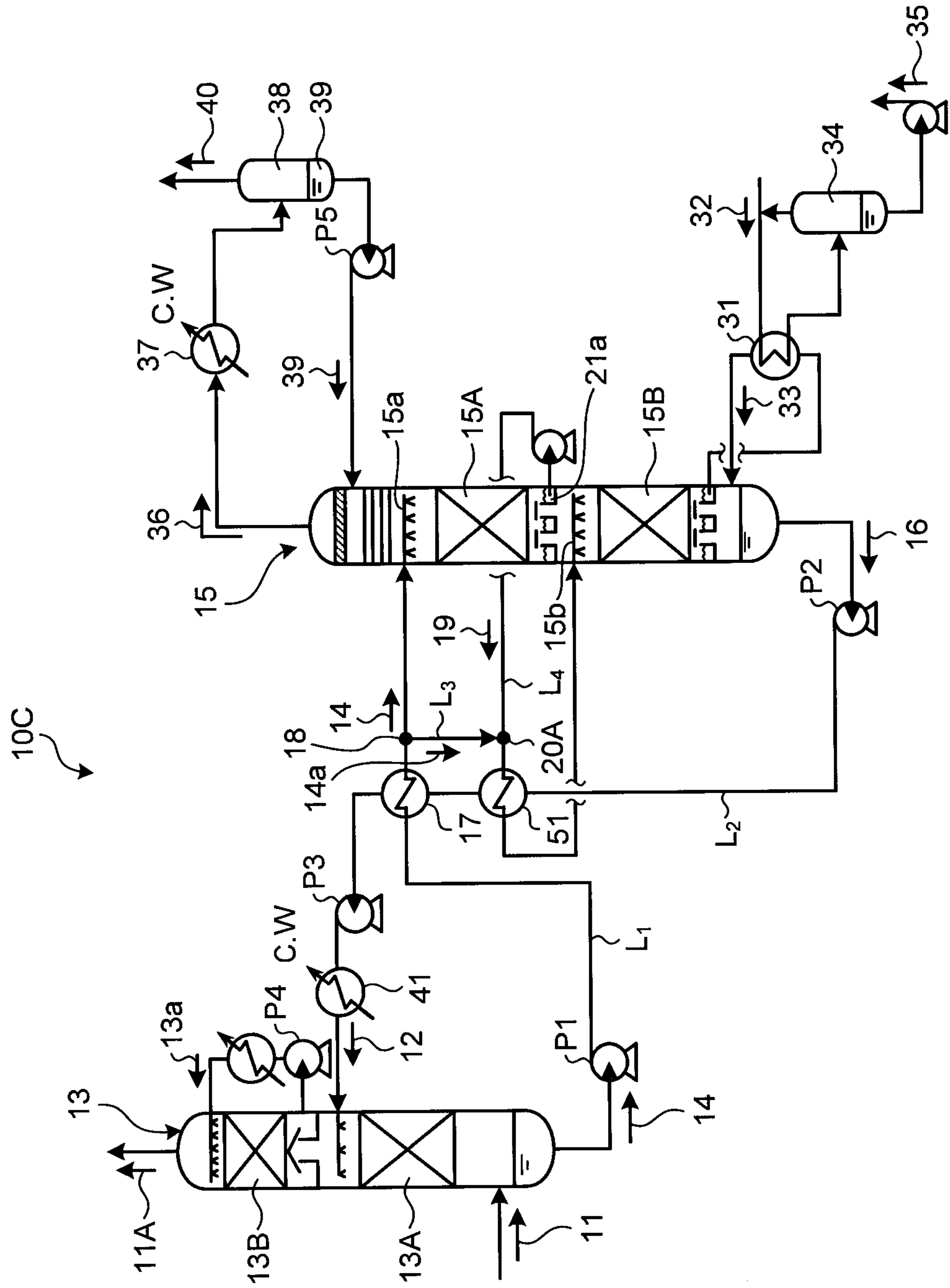


FIG.4

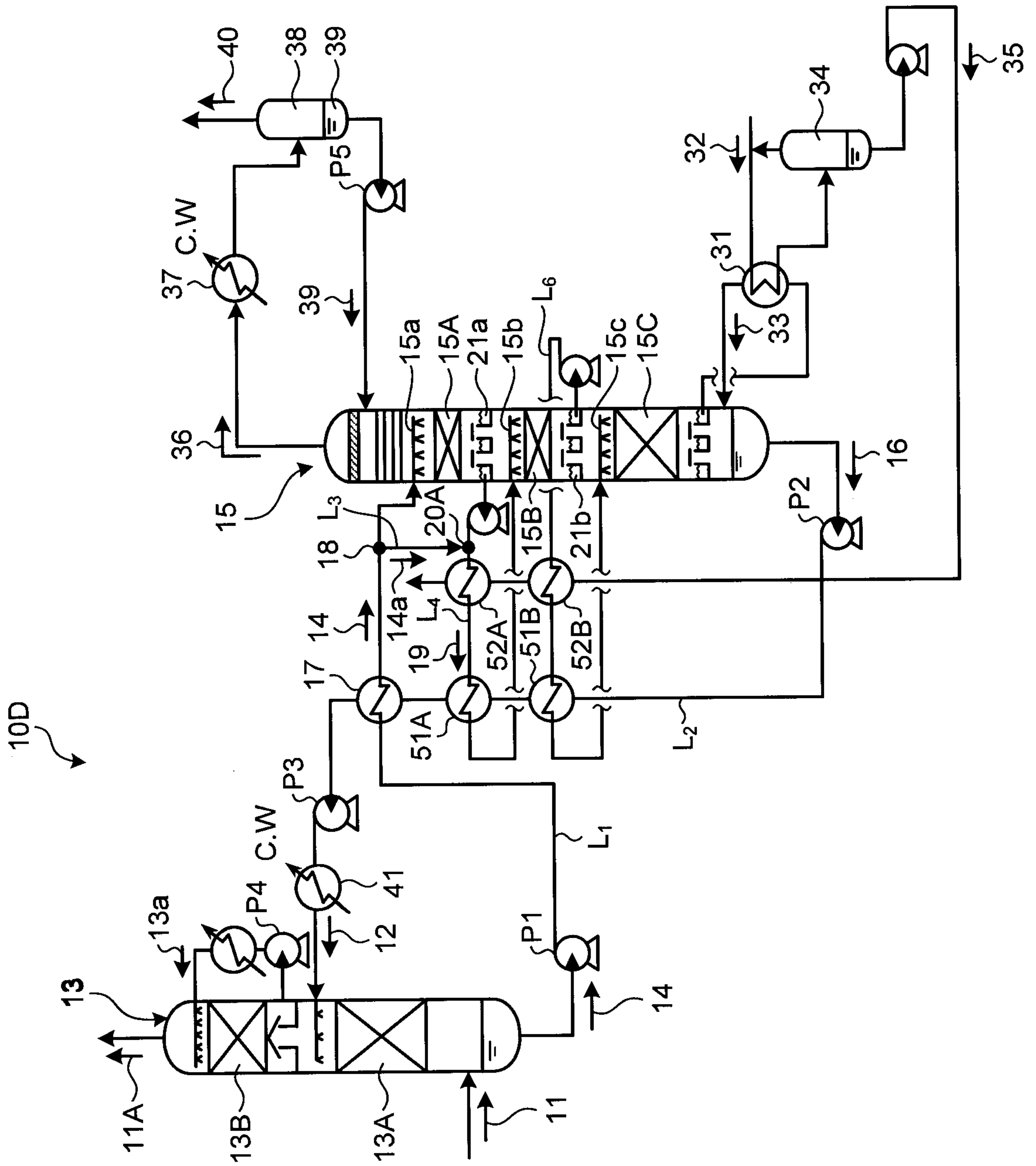
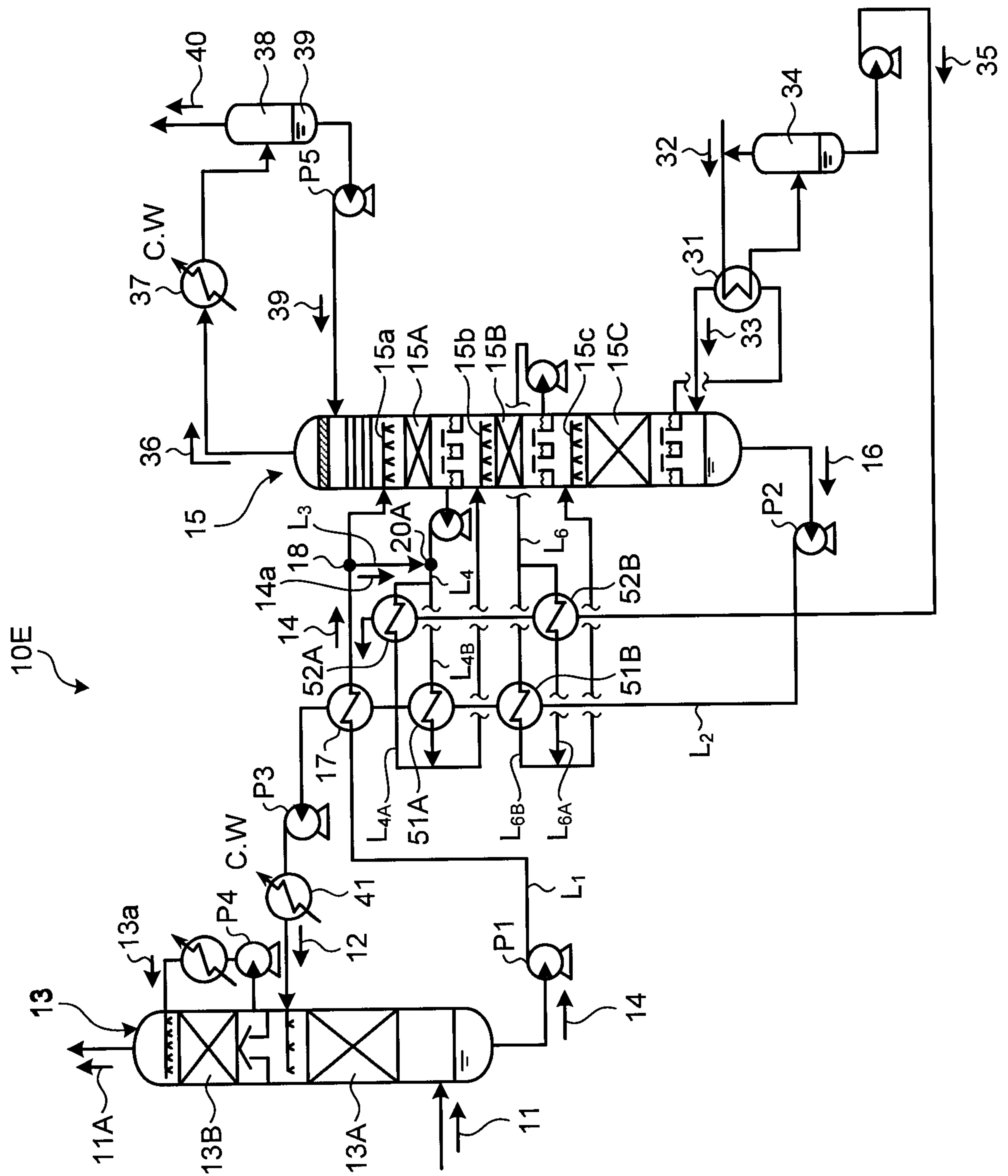
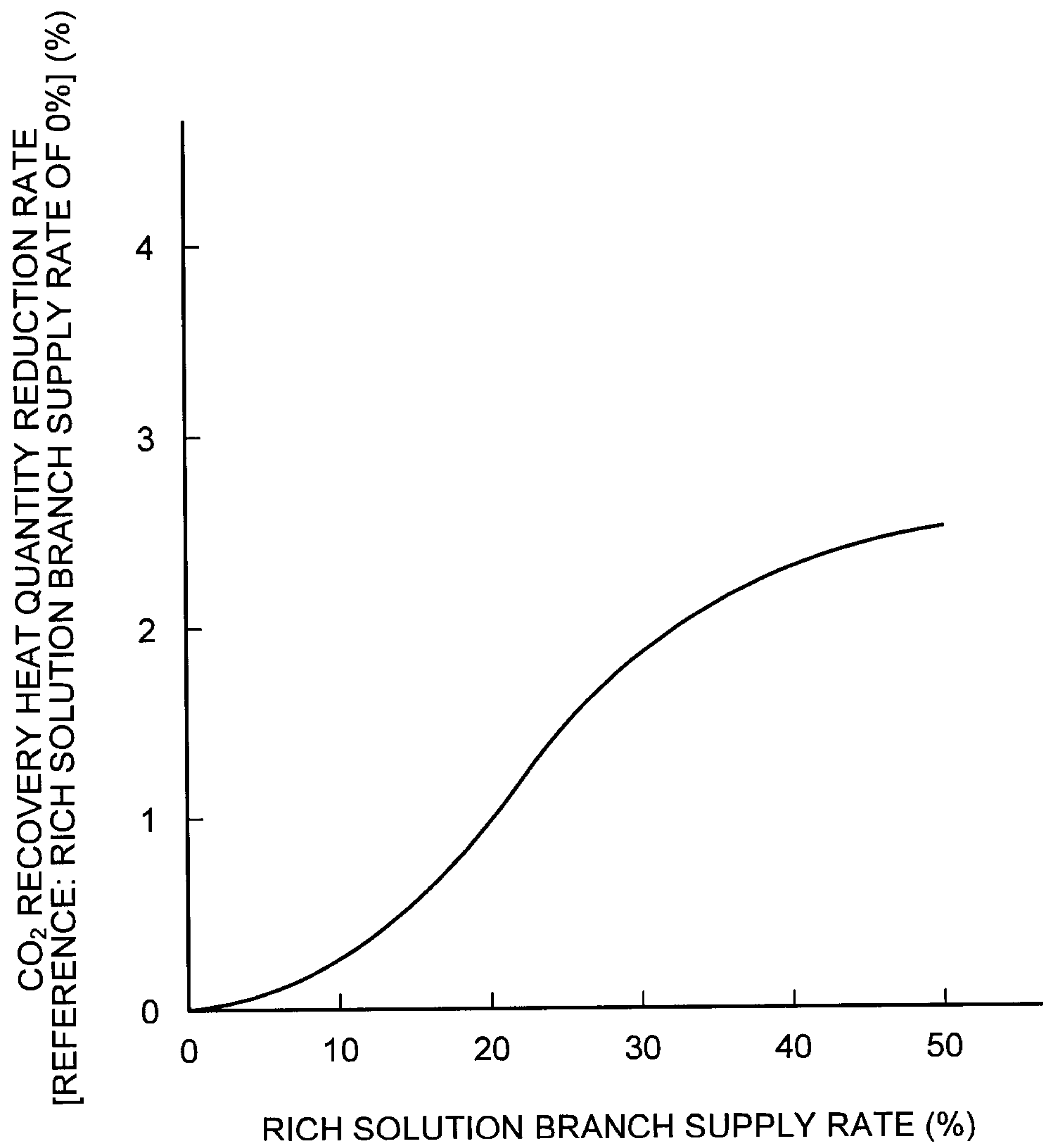


FIG.5



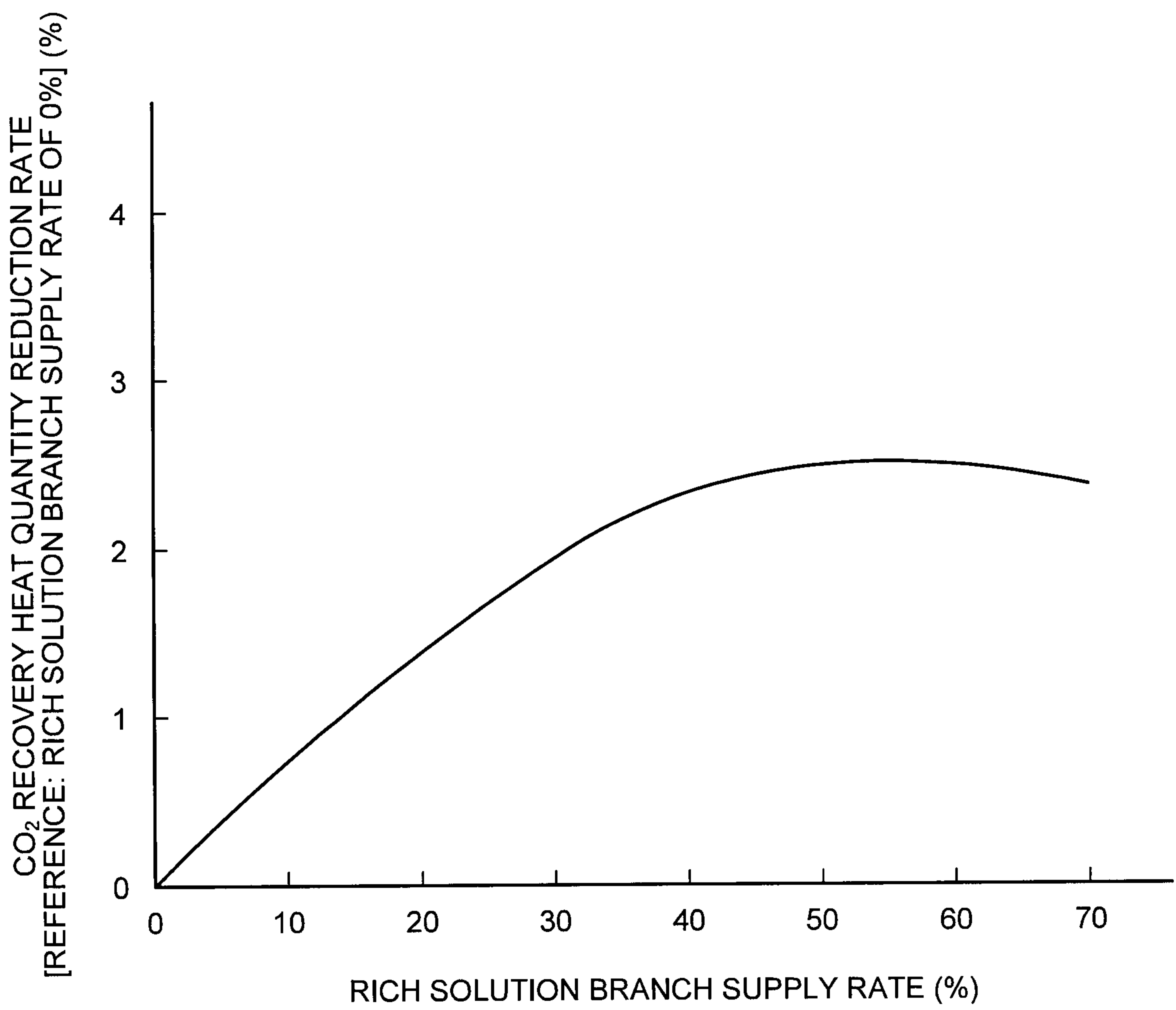
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FIG.6



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FIG.7



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FIG.8

