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(54) Titre : METHODE DE PURIFICATION DE LA PREPROINSULINE

(54) Title: A METHOD FOR PURIFYING PREPROINSULIN

(57) **Abrégé/Abstract:**

The invention relates to a method for the chromatographic purification of preproinsulins, according to which higher-molecular substances are separated from an aqueous solution of the preproinsulin by means of a first chromatography on an anion exchanger in through-flow mode and a subsequent second chromatography on a cation exchanger in adsorption mode, and a method for the production of insulins, which comprises the method for producing preproinsulins.

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(54) Title: METHOD FOR PURIFYING PREPROINSULIN

(54) Bezeichnung: VERFAHREN ZUR REINIGUNG VON PREPROINSULIN

(57) Abstract: The invention relates to a method for the chromatographic purification of preproinsulins, according to which higher-molecular substances are separated from an aqueous solution of the preproinsulin by means of a first chromatography on an anion exchanger in through-flow mode and a subsequent second chromatography on a cation exchanger in adsorption mode, and a method for the production of insulins, which comprises the method for producing preproinsulins.

(57) Zusammenfassung: Die Erfindung bezieht sich auf ein Verfahren zur chromatographischen Reinigung von Preproinsulinen bei dem höhermolekulare Substanzen aus einer wässrigen Lösung des Preproinsulins durch eine erste Chromatographie an einem Anionenaustauscher im Durchflussmodus und eine anschließende zweite Chromatographie an einem Kationenaustauscher im Adsorptionsmodus abgetrennt werden, sowie auf ein Verfahren zur Herstellung von Insulinen, welches das Verfahren zur Herstellung von Preproinsulinen miteinschließt.



WO 2004/013176 A1

Description

A method for purifying preproinsulin

Approximately 12 million people worldwide suffer from type 1 diabetes mellitus which
5 is characterized by an insufficient indigenous production of the hormone insulin.
Substitution of the lack of endocrine insulin secretion by applying insulin preparations
is the only possible form of therapy for this type of diabetes mellitus.

10 Insulin preparations are pharmaceutical preparations whose active substance is the
hormone insulin. Here, insulin analogs and insulin derivatives are used in addition to
naturally occurring insulins.

Human insulin which is produced in the human pancreas is a polypeptide comprising
15 51 amino acid residues which divide into two peptide chains: the A chain having 21
amino acid residues and the B chain having 30 amino acid residues. The sequence
of the amino acid residues in both peptide chains has been genetically determined
and is known. Both chains are connected to one another by two disulfide bridges. In
addition, the A chain also contains an intrachain disulfide bridge.

20 Insulin analogs differ from human insulin by substitution of at least one amino acid
residue and/or addition or removal of at least one amino acid residue. Insulin
analogues may either occur naturally in species other than humans or may have been
prepared artificially. Insulin derivatives contain chemically modified amino acid
residues which contain, for example, additional ester or amido groups but otherwise
25 show the human or an analog amino acid sequence.

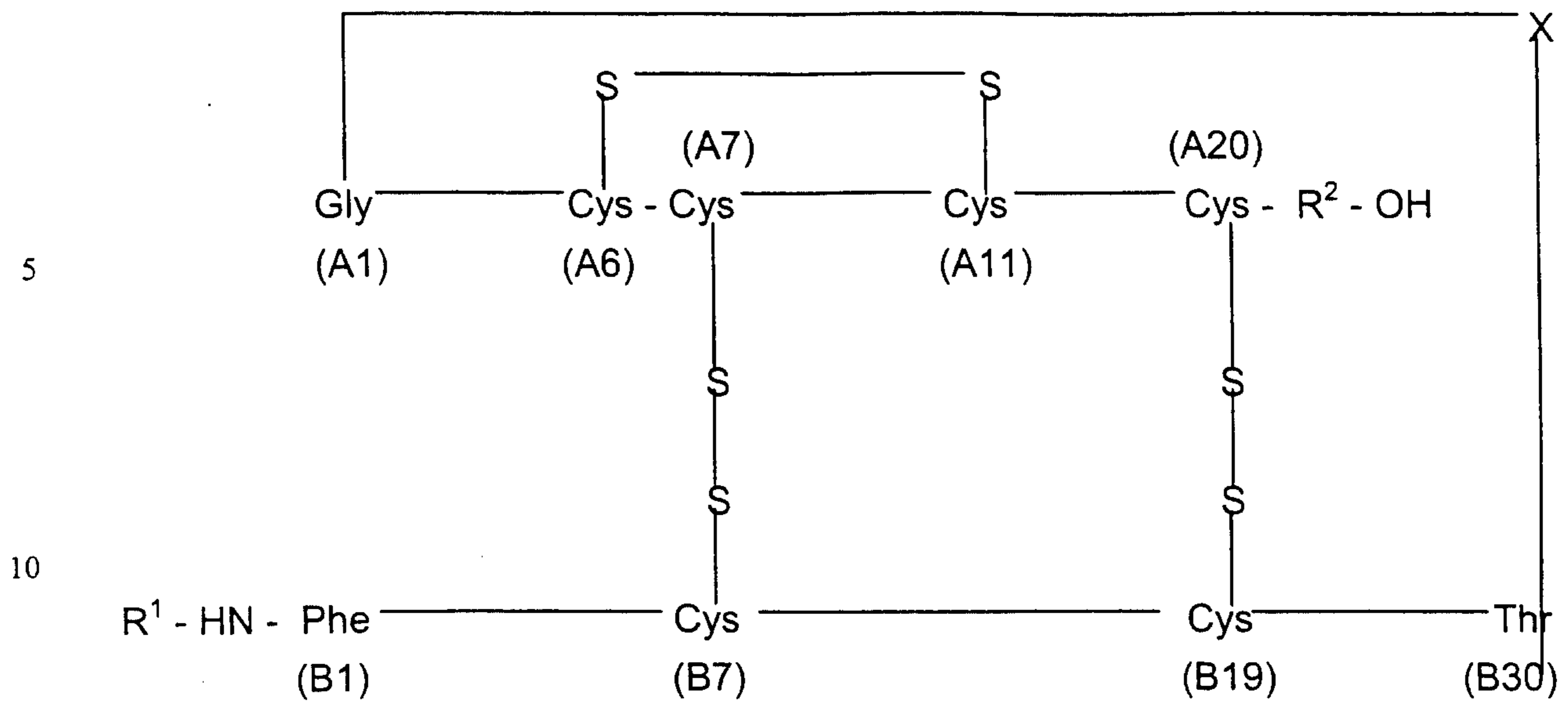
Normally, insulin analogs or insulin derivatives exhibit an altered action kinetics
compared to unmodified human insulin.

30 For some years, human insulin and the insulin analogs or insulin derivatives have
been prepared by recombinant DNA technology. In industrial methods, for example,
first an appropriate precursor of the formula 1, the preproinsulin (PPI), is prepared
from which human insulin or the insulin analogs are prepared by enzymic cleavage.
For example, a genetic method for preparing human insulin comprises the following
35 method steps:

- a) Fermentation of the genetically modified microorganisms,
 - b) Harvesting said microorganisms and cell disruption,
 - c) Isolating the inclusion bodies containing the undissolved fusion protein,
 - d) Dissolving said fusion protein with correct folding of the peptide chain and with
5 simultaneous closure of the disulfide bridges to give preproinsulin,
 - e) Enzymic cleavage of preproinsulin to give human insulin,
 - f) Purification of human insulin,
 - g) Crystallization of human insulin and drying of the obtained product.
- 10 When preparing an insulin analog, the amino acid sequence (of the A and B chains) in the appropriate regions of preproinsulin has already been predetermined. Enzymic cleavage of the various preproinsulins is carried out using proteases such as, for example, the enzyme trypsin and in addition, if necessary, the enzyme carboxypeptidase B.

15

The preproinsulin is a protein of the formula 1,



in which

X

20

- a) is a genetically encodable amino acid residue or
 b) is a peptide having from 2 to 35 amino acid residues, which starts and ends with in each case a basic amino acid residue, in particular Arg, and which, if it consists of more than 3 amino acid residues, starts and ends with in each case two basic amino acid residues, in particular Arg and/or Lys,

25

R¹

- a) is hydrogen,
 b) is a genetically encodable amino acid residue or
 c) is a peptide having from 2 to 15 amino acid residues,

30

R²

- is a genetically encodable amino acid residue, and

and the residues A1 – A20 correspond to the amino acid sequence of the A chain of human insulin or of an insulin analog and the residues B1 – B30 correspond to the amino acid sequence of the B chain of human insulin or of an insulin analog.

35

The preproinsulin is preferably a protein of the formula 1 in which

X is a peptide having 35 amino acid residues with the C-chain sequence of human insulin or simian insulin or is a peptide having 29 amino acids of the sequence:

Arg-Asp-Val-Pro-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-
5 Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg (SEQ ID NO: 1)

R¹ is a peptide having from 2 to 15 amino acid residues, whose carboxyl-terminal amino acid residue is Arg,

R² is the amino acid residue Asn or Gly,

and the residues A1 – A20 correspond to the amino acid sequence of the A chain of human insulin and the residues B1 – B30 correspond to the amino acid sequence of the B chain of human insulin or of an insulin analog in which Lys replaces Asn in position B3 and Glu replaces Lys in position B29.

The process stage - dissolving the fusion protein with correct folding of the peptide chain and with simultaneous closure of the disulfide bridges to give preproinsulin - produces, in addition to the desired monomeric preproinsulin, also polymeric forms of preproinsulin in a competing reaction. Said polymeric preproinsulins can be detected, owing to their higher molecular weight, by HPLC-GPC analysis or by the method of dynamic light scattering. In order to repress this undesired competing reaction, the initial concentration of the fusion protein needs to be as low as possible (De Bernadez et al., Meth. Enzym. 309:217, 1999). In practice, this process stage produces preproinsulin at a concentration of from approx. 0.5 to 1 g/l, with approx. 40% of higher molecular weight proportions being found in addition. The higher molecular weight proportions include the polymeric preproinsulins.

Surprisingly, it was found within the framework of the present invention that the polymeric forms of preproinsulins adversely affect the stability of the insulins in the subsequent process stages by inducing the denaturation of the native insulins. It is known that, during the denaturation reaction chain, a first reversible step produces, from the dissolved monomeric insulin molecules, linear aggregates in which physical adhesive forces hold together the repeated units. An irreversible subsequent reaction produces, from the dissolved aggregates, stable insoluble aggregate bundles (fibrils) which in turn induce the denaturation of native insulins in an autocatalytic process. These insoluble insulin fibers are not only biologically inactive

but may also cause blockage of injection needles during application of the pharmaceutical insulin preparations. In addition, they are also held responsible for immunological incompatibility reactions which can occasionally occur during therapy with insulin preparations (J.Bränge et al, J. Pharm. Sc. 1997, 86, 517-525; R.E. Ratner et al., Diabetes, 39, 728-733, 1990).

In the subsequent part of the insulin preparation process, preproinsulin is converted to human insulin with the aid of the enzymes trypsin and carboxypeptidase B (see Kemmler, W., Peterson, J.D., and Steiner, D.F., J. Biol. Chem., 246 (1971) 6786-6791). Here, the linker peptide between the A and B chains (X in the formula 1) and the pre part at the amino end of the B chain (R^1 in the formula 1) are removed. The enzymic reaction with trypsin cleaves not only those peptide bonds whose cleavage produces human insulin but also, in a competing reaction, other peptide bonds whose cleavage produces a plurality of undesired byproducts. The formation of de-Thr insulin due to additional cleavage between amino acid residues B29 and B30 in formula 1 (see EP 0 264 250 B1) is particularly undesired. The removal of this byproduct in the subsequent purification stages results in large losses of product. In order to repress this undesired side reaction, the initial concentration of preproinsulin needs to be as high as possible, i.e. in the range from 8 – 25 g/l, corresponding to 1 – 3 mM (see EP 0 264 250 B1). This requirement contrasts with the requirement mentioned in the last but one paragraph.

From the above, it is evident that it is advantageous to introduce, between production of preproinsulin and cleavage of preproinsulin to insulin, an additional process step which removes the polymeric preproinsulins as completely as possible and, at the same time, increases the concentration of monomeric preproinsulin as much as possible. An additional condition is the need to ensure a very high yield in this process step.

It has therefore been proposed (EP 0 600 372 B1) to concentrate preproinsulin on a hydrophobic adsorber resin. The applicant was able to show in his own experiments that, although a high concentration factor of $F = 10 - 15$ can be achieved, there is virtually no removal of polymeric preproinsulins. Another proposal (D.F. Steiner et al., Diabetes, 17 (1968), 725-736) mentions chromatographic purification of preproinsulin with the aid of an ion exchanger resin. In our own experiments, we were only able to achieve a concentration factor of $F = 5$ and a removal of the higher molecular weight proportions to approx. 5%, using an anion exchanger resin. Although using a cation exchanger resin removed the higher molecular weight

proportions to approx. 1%, the binding capacity of the resin for preproinsulin proved to be unsatisfactory.

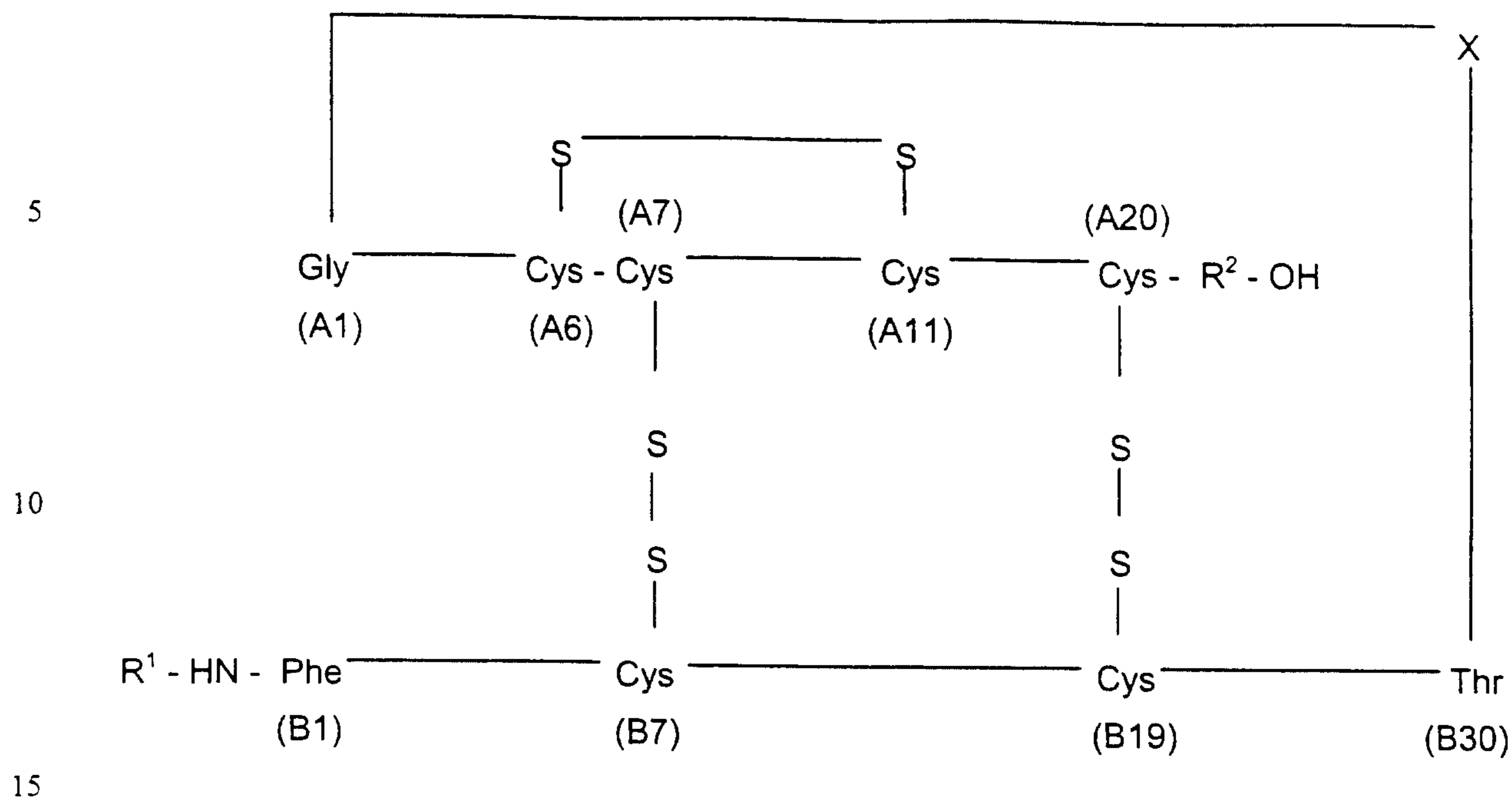
Surprisingly, it was then found that the combination of a chromatography on an anion exchanger resin in flow-through mode with an immediately following chromatography on a cation exchanger resin in adsorption mode provided distinctly superior results. The present invention therefore relates to a method for effectively removing the higher molecular weight substances from an aqueous solution of preproinsulin with simultaneous high concentration of the monomeric preproinsulin.

According to the invention, a diluted aqueous solution of a preproinsulin, as is produced during the preparation process of insulin, is pumped at pH 7.0 to 9.0, preferably at pH 7.5 to 8.5, and a conductivity of from 5 to 7 mS/cm through a precolumn packed with an anion exchanger resin, for example Source 30TM Q. In this case, the monomeric preproinsulin is not bound to the resin but runs through the column together with the permeate. In contrast, the majority of the higher molecular weight substances, including the polymeric preproinsulins, is adsorbed to the resin and thus removed from preproinsulin. The permeate from this precolumn, which contains the substance of interest, is adjusted in line to pH 3.0 to 5.5, preferably to pH 4.0 to 5.0, using hydrochloric acid and then pumped directly onto a second column packed with a cation exchanger resin, for example Source 30TM S.

Preproinsulin adsorbs to this resin and impurities are washed out of the column together with the permeate. Preproinsulin is desorbed with the aid of an elution buffer containing sodium chloride at a linearly increasing concentration of from 1 to 20 g/l, preferably 2.5 to 15.0 g/l. The purified preproinsulin is collected in a main fraction, whereas further impurities are removed in a prefraction and a postfraction. In the main fraction which contained > 90% of the initial amount of preproinsulin, a concentration of from 15 to 20 g/l was measured (concentration factor $F = 20 - 25$). The higher molecular weight substances were removed to a proportion of < 0.1%.

The preproinsulin purified in this way can be isolated from the solution intermediately by crystallization or the solution can be fed directly to the enzymic cleavage process stage.

The present invention thus relates to a method for the chromatographic purification of preproinsulin of the formula 1,



20 in which

X

25 a) is a genetically encodable amino acid residue or
 b) is a peptide having from 2 to 35 amino acid residues, which starts and ends with in each case a basic amino acid residue, in particular Arg, and which, if it consists of more than 3 amino acid residues, starts and ends with in each case two basic amino acid residues, in particular Arg and/or Lys,

R¹

30 a) is hydrogen,
 b) is a genetically encodable amino acid residue or
 c) is a peptide having from 2 to 15 amino acid residues,

R² is a genetically encodable amino acid residue, and

35 and the residues A1 – A20 correspond to the amino acid sequence of the A chain of human insulin or of an insulin analog and the residues B1 – B30 correspond to the amino acid sequence of the B chain of human insulin or of an insulin analog;

in which method higher molecular weight substances are removed from an aqueous solution of said preproinsulin by means of a first chromatography on an anion exchanger in flow-through mode and a subsequent second chromatography on a cation exchanger in adsorption mode;

5

wherein said preproinsulin can have the following amino acid sequence:

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Asn-Gln-His-Leu-Cys-Gly-
Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-
10 Thr-Pro-Lys-Thr-Arg-Arg-Glu-Ala-Glu-Asp-Pro-Gln-Val-Gly-Gln-Val-Glu-Leu-
Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-
Gln-Lys-Arg-Gly-Ile-Val-Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-
Leu-Glu-Asn-Tyr-Cys-Asn; (SEQ ID NO: 2)

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Asn-Gln-His-Leu-Cys-Gly-
Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-
15 Thr-Pro-Lys-Thr-Arg-Arg-Glu-Ala-Glu-Asp-Pro-Gln-Val-Gly-Gln-Val-Glu-Leu-
Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-
Gln-Lys-Arg-Gly-Ile-Val-Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-
20 Leu-Glu-Asn-Tyr-Cys-Gly; (SEQ ID NO: 3)

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Lys-Gln-His-Leu-Cys-Gly-
Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-
Thr-Pro-Glu-Thr-Arg- Asp-Val-Pro-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-
25 Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg-Gly-Ile-Val-
Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Asn
(SEQ ID NO: 4).

The invention further relates to a method as described above for separating foreign
30 substances from the solutions of preproinsulins which induce insulin denaturation.

The invention further relates to a method as described above, wherein the second
chromatography is carried out at a pH of from 3.0 to 5.5.

35 The invention further relates to a method as described above, wherein the second
chromatography is carried out under a pressure of from 1 to 30 bar.

The invention further relates to a method for preparing insulin by expressing nonfolded preproinsulin, comprising the steps:

- a) fermentation of genetically modified microorganisms which express nonfolded preproinsulin,
- 5 b) harvesting the microorganisms and cell disruption,
- c) isolating the inclusion bodies containing undissolved, nonfolded preproinsulin,
- d) dissolving the preproinsulin with correct folding of the peptide chain and simultaneous closure of the disulfide bridges to give preproinsulin, and subsequently running a method for chromatographic purification of preproinsulin
- 10 of the formula 1 as described above,
- e) enzymic cleavage of preproinsulin to give human insulin,
- f) purification of human insulin,
- g) crystallization of human insulin and drying.

15

The invention is illustrated in more detail below, without being limited thereto.

Examples:

20

The starting solution for the purification of various preproinsulins of the formula 1, described in the following examples 1 to 3, was prepared in the known manner (EP 0 489 780 and EP 0 600 372) as follows, according to the abovementioned process stages a, b, c and d:

25

During fermentation of the microorganisms (process stage a), the E.coli cells formed inclusion bodies which contained the fusion protein having the amino acid sequence of the preproinsulin. After finishing the fermentation, the cells are isolated by centrifugation and disrupted by means of the usual high-pressure homogenization (process stage b). The insoluble inclusion bodies released in the process were

30 isolated by centrifugation and washed with water in the centrifuge (process stage c). In the subsequent process stage d, the fusion protein inclusion bodies were dissolved in an 8 M guanidine hydrochloride solution at pH 10.8. After diluting with water and adding cysteine hydrochloride, the fusion protein was folded with closure of the 3 disulfide bridges at pH 10.8 and 4°C to give preproinsulin of the formula 1.

35

The solution was then adjusted to pH 5 using 10% strength hydrochloric acid, as a result of which foreign proteins were precipitated which were removed by centrifugation. The supernatant after centrifugation contained 0.6 to 0.8 g/l monomeric preproinsulin. The purity of preproinsulin, as determined by HPLC-RP

analysis, was approx. 65% by area. HPLC-GPC analysis determined a proportion of approx. 45% by area higher molecular weight impurities.

HPLC-RP analysis

5

Column: LiChroCARTTM 250-4 from Merck (SuperspherTM 100-RP18e)
Instrument: WatersTM 2690
Software: Waters Millenium
Gradient: A: 25% by volume acetonitrile, 0.3 M NaCl in 0.05 M phosphate
10 buffer
pH 2.5
B: 65% by volume acetonitrile, 0.05 M NaCl in 0.05 M
phosphate buffer
pH 2.5

15

The gradient is characterized by the following amounts of
buffer B according to the corresponding run times:
0 min 4.0%; 20 min 17.0% ; 30 min 37.0%; 40 min 4.0%

Temperature: 35 °C
Loading volume: 10 µl
20 Total run time: 55 min
Flow rate: 1.0 ml/min
Detection: 214 nm (Waters 2487)

25

In order to determine the preproinsulin content in the loading solution, the peak area
of preproinsulin in the analyzed sample was divided by the corresponding peak area
of a standard substance. In order to determine the degree of purity, the peak area of
preproinsulin was divided by the sum of the peak areas of all elutable substances in
the analyzed sample.

30

HPLC-GPC analysis

Column: 2 columns in series, stainless steel L = 300 mm; ID = 7.8 mm
Instrument: pump: Waters 510 / autosampler: Wisp 717
35 Software: Waters Millenium
Stationary phase: ShodexTM Protein KW 802.5 120-7 diol
Separation limits: 2 000 to 80 000 dalton
Mobile phase: 30% by volume acetonitrile, 3.5 M acetic acid, pH 3.0

adjusted with aqueous ammonia

Gradient: isocratic

Temperature: room temperature

Loading volume: 100 μ l

5 Total run time: 65 min

Flow rate: 0.5 ml/min

Detection: 276 nm (Waters 2487)

10 In order to determine the proportion of higher molecular substances, the peak areas of all higher molecular substances which were eluted prior to monomeric preproinsulin were divided by the sum of the peak areas of all elutable substances. The retention time for monomeric preproinsulin was determined using a standard substance.

15 Example 1

After completion of the abovementioned process stages a, b, c and d, a solution of preproinsulin having the following amino acid sequence was obtained from the appropriately genetically modified E.coli cells:

20

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Asn-Gln-His-Leu-Cys-Gly-Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-Thr-Pro-Lys-Thr-Arg-Arg-Glu-Ala-Glu-Asp-Pro-Gln-Val-Gly-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg-Gly-Ile-Val-25 Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Asn (SEQ ID NO: 2)

Said preproinsulin corresponds to the formula 1, in which

30

X is a peptide chain having 35 amino acid residues with the sequence of simian C peptide,

R1 is a peptide chain having 10 amino acid residues of the sequence: Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg (SEQ ID NO: 5)

R2 is the amino acid residue Asn (identical to A21 of the A chain of human insulin)

35

A1-A20 is the peptide chain having the sequence (only A1 to A20) of the A chain of human insulin

B1-B30 is the peptide chain having the sequence of the B chain of human insulin.

5 The preproinsulin solution was purified using an apparatus which comprised primarily two chromatography columns arranged in series and a stirred vessel arranged in between. The stirred vessel was used to change the pH of the solution in line between the two columns.

10 In the first chromatography column (manufacturer: Pharmacia, diameter: 5 cm), a gel bed (bed height: 14 cm, bed volume: 275 ml) was prepared using the anion exchanger resin DEAE-SepharoseTM fast flow (manufacturer: Pharmacia Biotech; Prod. No. 17-0709-05). The column was operated from top to bottom and at atmospheric pressure of 1 bar. The flow rate was 2 000 ml/h. A multiway valve, a
15 loading pump (IsmatecTM MV) and a bubble trap were installed upstream of the column. The following solutions were pumped onto the column successively via the multiway valve:

20 8.1 l of loading solution,
2.3 l of displacement buffer,
1.4 l of washing buffer,
1.4 l of regenerating solution,
2 l of equilibration buffer.

25 A UV probe (275 nm, with data recording) and another multiway valve were installed downstream of the column. Via the second multiway valve, approx. 10.2 l of permeate fraction were conducted into the abovementioned stirred vessel and, subsequently, approx. 1 l of washing fraction was conducted into a collecting vessel. The remaining permeates were discharged into the biological waste channel via the
30 multiway valve.

The anion exchange chromatography was operated in flow-through mode, i.e. the conditions (pH 8.3; conductivity = 6.1 mS/cm) were chosen such that the valuable substance preproinsulin was not bound to the gel but washed through the column
35 together with the permeate during product application. In contrast, contaminations were adsorbed to the gel and removed with the washing buffer and the regenerating solution.

The solutions used had the following composition:

Starting solution for column 1:

Starting solution (supernatant from centrifugation)		8.0	l	
Sodium chloride solution, 25% strength (w/w)		100	ml	12.5 ml/l
Sodium hydroxide solution, 10% (w/w)	approx.	4.5	ml	0.6 ml/l
	pH	8.3		
Conductivity		6.1	mS/cm	
Temperature	approx.	5	°C	

Purified water		1	l	
Tris(hydroxymethyl)aminomethane		4.0		g/l
Sodium chloride		2.5		g/l
Hydrochloric acid, 25% strength (w/w)	approx.	2.5		ml/l
	pH	8.0		
Conductivity	approx.	5.7		mS/cm
Temperature				room temperature

5

Purified water		1	l	
Tris(hydroxymethyl)aminomethane		5.0		g/l
Sodium chloride		15		g/l
Hydrochloric acid, 25% strength (w/w)	approx.	3		ml/l
	pH	8.0		
Conductivity	approx.	24		mS/cm
Temperature				room temperature

Regenerating solution for columns 1 and 2:

Purified water		0.91	L	
Sodium chloride		40	g	40 g/l
Sodium hydroxide solution 33% strength (w/w)		0.09	l	1 mol/l

Equilibration buffer for column 1:

Purified water		1	l
Tris(hydroxymethyl)aminomethane		5.0	g/l
Sodium chloride		2.0	g/l
Hydrochloric acid, 25% strength (w/w)	approx.	3	ml/l
	pH	8.0	
Conductivity	approx.	5.1	mS/cm
Temperature			room temperature

5 The permeate fraction containing the valuable substance preproinsulin and the washing fraction containing the majority of the higher molecular weight impurities were collected at the column outlet:

- 10 1. approx. 10.2 l permeate fraction
(at start of loading solution, from UV value 20% (ascending) to UV value 35% (descending), during product displacement)
- 15 2. approx. 1 l washing fraction
(during loading of washing buffer, from UV value 30% (ascending slope) to UV value 40% (descending))

All other permeates were discharged into the biological waste channel.

20 Figure 1 depicts the UV diagram measured at the outlet of column 1.

The permeate fraction of the first column was adjusted to pH 3.5 with 90% strength lactic acid inline in the intermediate vessel (nominal volume: 4 l, with stirrer, pH probe and inlet tube) and then pumped directly onto the second chromatography
25 column.

In the second chromatography column (manufacturer: Pharmacia, diameter: 5 cm), a gel bed (bed height: 10.5 cm, bed volume: 206 ml) was prepared using the cation exchanger resin Source 30 S (manufacturer: Pharmacia Biotech; Prod. No. 17-1273-
30 04). The column was operated from top to bottom and at atmospheric pressure of 1

bar. The flow rate was likewise 2 000 ml/h. A multiway valve, a loading pump and a bubble trap were installed upstream of the column. The following solutions were pumped onto the column successively via the multiway valve:

- 5 10.2 l loading solution (= permeate fraction of column 1, adjusted to pH 3.5)
 0.5 l displacement buffer
 3.0 l elution buffer A/B (equal amounts of A and B)
 2.3 l regenerating solution
 2 l equilibration buffer

10

A UV probe (275 nm, with data recording) and another multiway valve were installed downstream of the column. Approx. 1 l of the main fraction was conducted via the second multiway valve into a collecting vessel. The remaining permeates were discharged via the multiway valve into the biological waste channel.

15

The cation exchanger chromatography was operated in adsorption mode, i.e. the valuable substance preproinsulin was adsorbed to the gel during product application and (after displacing the loading solution) desorbed again using the elution buffer A/B. In order to achieve an optimal purification effect, a linearly increasing sodium chloride gradient was

20 applied in the elution buffer.

The solutions used had the following composition:

Loading solution for column 2:

Permeate fraction of column 1	approx.	10.2	l	
Lactic acid, 90% strength		14.3	ml	1.4 ml/l
	pH	3.5		
Conductivity	approx.	6.3	mS/cm	
Temperature	approx.	5	°C	

25

Displacement buffer for column 2:

Purified water		1	l	
Lactic acid, 90% strength		8.3	ml	0.1 mol/l
Sodium chloride		2.5	g	2.5 g/l
Sodium hydroxide solution, 10% strength (w/w)	approx.	8	ml	

	pH	3.5		
Conductivity	approx.	8	mS/cm	
Temperature		room temperature		

Elution buffer A for column 2:

The elution buffer A is identical to the displacement buffer for column 2.

Elution buffer B for column 2:

Purified water		1	l	
Lactic acid, 90% strength		8.3	ml	0.1 mol/l
Sodium chloride		15.0	g	15.0 g/l
Sodium hydroxide solution, 10% strength (w/w)	approx.	7	ml	
	pH	3.5		
Conductivity	approx.	25	mS/cm	
Temperature		room temperature		

5

Regeneration solution for columns 1 and 2:

Purified water		0.91	l	
Sodium chloride		40	g	40 g/l
Sodium hydroxide solution, 33% strength (w/w)		0.09	l	1 mol/l

Equilibrium buffer for column 2:

Purified water		1	l	
Lactic acid, 90% strength		8.3	g	0.1 mol/l
Sodium chloride		2.9	g/l	
Sodium hydroxide solution 10% strength (w/w)	approx.	9	ml	
	pH	3.5		
Conductivity	approx.	8.5	mS/cm	
Temperature		room temperature		

The main fraction which contained the valuable substance preproinsulin was collected at the column outlet:

5

approx. 1.0 l main fraction
(during elution, from UV value 65% (ascending) to UV
value 76% (descending))

10 All other permeates were discharged into the biological waste channel.

Figure 2 depicts the UV diagram measured at the outlet of column 2.

15 In the purified solution (main fraction column 2), 15 g/l preproinsulin with a degree of
purity of 89% by area were measured (HPLC-RP analysis). The yield was 91%,
based on the amount of preproinsulin in the starting solution. Higher molecular
proportions of 0.2% by area were determined by HPLC-GPC analysis.

20 Example 2

After completion of the abovementioned process stages a, b, c and d, a solution of
preproinsulin having the following amino acid sequence is obtained from the
appropriately genetically modified E.coli cells:

25

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Asn-Gln-His-Leu-Cys-Gly-Ser-
His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-Thr-Pro-
Lys-Thr-Arg-Arg-Glu-Ala-Glu-Asp-Pro-Gln-Val-Gly-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-
Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg-Gly-Ile-Val-
30 Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Gly (SEQ
ID NO: 3)

Said preproinsulin corresponds to the formula 1, in which

35

X is a peptide chain having 35 amino acid residues with the sequence of
simian C peptide,

R1 is a peptide chain having 10 amino acid residues of the sequence:
Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg (SEQ ID NO: 5)

R2 is the amino acid residue Gly
A1-A20 is the peptide chain having the sequence (only A1 to A20) of the A chain of human insulin
B1-B30 is the peptide chain having the sequence of the B chain of human insulin.

5

The preproinsulin solution was purified by again using an apparatus which comprised primarily two chromatography columns arranged in series and a stirred vessel arranged in between. The stirred vessel was used to change the pH of the solution inline between the two columns. The apparatuses for the second chromatography stage were designed for pressure stability.

10

The chromatography on column 1 and the pH-switching in the intermediate vessel were carried out as described in example 1 so that the description and the values will not be repeated here.

15

In the second chromatography column (manufacturer: Prochrom, diameter: 5 cm, material: stainless steel), a gel bed (bed height: 10 cm, bed volume: 196 ml) was prepared using the cationic exchanger Source 30 S (manufacturer: Pharmacia Biotech; prod. No.: 17-1273-04). The column was operated from top to bottom and at a working pressure of 10 bar. The flow rate was 3 500 ml/h. A multiway valve, a loading pump (manufacturer: Besta; type: HD2-300) were installed upstream of the column. The following solutions were pumped onto the column successively via the multiway valve:

20

25

- 10.2 l loading solution (= permeate fraction of column 1, adjusted to pH 4.6)
- 0.5 l displacement buffer
- 3.0 l elution buffer A/B (equal amounts of A and B)
- 2.3 l regenerating solution
- 2 l equilibration buffer

30

A UV probe (275 nm, with data recording) and another multiway valve were installed downstream of the column. The main fraction containing the purified preproinsulin was conducted via the second multiway valve into a collecting vessel. The remaining permeates were discharged via the multiway valve into the biological waste channel.

35

The cation exchanger chromatography was operated in adsorption mode, i.e. the valuable substance preproinsulin was adsorbed to the gel during product application and (after

displacing the loading solution) desorbed again using the elution buffer A/B. In order to achieve an optimal purification effect, a linearly increasing sodium chloride gradient was applied in the elution buffer.

5 The solutions used had the following composition:

Loading solution for column 2:

Permeate fraction of column 1	approx.	10.2	l	
Lactic acid, 90% strength		12.2	ml	1.2 ml/l
	pH	4.6		
Conductivity	approx.	6.7	mS/cm	
Temperature	approx.	5	°C	

Displacement buffer for column 2:

Purified water		1	l	
Lactic acid, 90% strength		8.3	ml	0.1 mol/l
Sodium chloride		2.5	g	2.5 g/l
Sodium hydroxide solution, 10% strength (w/w)	approx.	27	ml	
	pH	4.6		
Conductivity	approx.	8	mS/cm	
Temperature			room temperature	

10

Elution buffer A for column 2:

The elution buffer A is identical to the displacement buffer for column 2.

Elution buffer B for column 2:

Purified water		1	l	
Lactic acid, 90% strength		8.3	ml	0.1 mol/l
Sodium chloride		15.0	g	15.0 g/l
Sodium hydroxide solution, 10% strength (w/w)	approx.	27	ml	
	pH	4.6		

Conductivity	approx.	25	mS/cm
Temperature		room temperature	

Regeneration solution for columns 1 and 2:

Purified water		0.91	l		
Sodium chloride		40	g	40	g/l
Sodium hydroxide solution, 33% strength (w/w)		0.09	l	1	mol/l

Equilibrium buffer for column 2:

Purified water		1	l		
Lactic acid, 90% strength		8.3	g	0.1	mol/l
Sodium chloride		2.9	g/l		
Sodium hydroxide solution 10% strength (w/w)	approx.	26	ml		
	pH	4.6			
Conductivity	approx.	8.7	mS/cm		
Temperature		room temperature			

5

The main fraction which contained the valuable substance preproinsulin was collected at the column outlet:

10	approx.	0.9	l	main fraction (during elution, from UV value 65% (ascending) to UV value 76% (descending))
----	---------	-----	---	---

All other permeates were discharged into the biological waste channel.

15 In the purified solution (main fraction from column 2), 17 g/l preproinsulin with a degree of purity of 93% by area were measured (HPLC-RP analysis). The yield was 92%, based on the amount of preproinsulin in the starting solution. Higher molecular weight proportions of <0.1% by area were determined by HPLC-GPC analysis.

20

Example 3

After completion of the abovementioned process stages a, b, c and d, a solution of preproinsulin having the following amino acid sequence is obtained from the
5 appropriately genetically modified E.coli cells:

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Lys-Gln-His-Leu-Cys-Gly-Ser-
His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-Thr-Pro-
Glu-Thr-Arg- Asp-Val-Pro-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-
10 Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg-Gly-Ile-Val-Glu-Gln-Cys-Cys-Thr-Ser-
Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Asn (SEQ ID NO: 4)

Said preproinsulin corresponds to the formula 1, where

- 15 X is a peptide chain having 29 amino acid residues with the sequence:
Arg- Asp-Val-Pro-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-
Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg (SEQ ID NO:
1)
- R1 is a peptide chain having 10 amino acid residues with the sequence:
20 Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg (SEQ ID NO: 5),
- R2 is the amino acid residue Asn (A21 of the A chain of human insulin),
- A1-A20 is a peptide chain with the sequence (only A1 to A20) of the A chain of
human insulin,
B1-B30 [lacuna] peptide chain with a sequence similar to the B chain of
25 human insulin, i.e. with Lys replacing Val in position B3 and Glu
replacing Lys in position B29.

The preproinsulin solution was purified using the same apparatus used in example 1.

30 This time, the anion exchanger resin Source 30 Q (manufacturer: Pharmacia
Biotech; Prod.-No.: 17-1275-04) was used for the chromatography on column 1.
Regeneration of this gel required twice the amount of regenerating solution
compared to examples 1 and 2. The remaining parameters of the first
chromatography, such as composition and volumes of the solutions, were the same
35 as those described in examples 1 and 2.

Likewise, the pH-switching in the intermediate vessel was carried out as described in
example 1.

The second chromatography was this time carried out with a working pressure of 15 bar. All other parameters of the second chromatography were identical to those described in example 2.

5

In the purified solution (main fraction from column 2), 17 g/l preproinsulin with a degree of purity of 92.5% by area were measured (HPLC-RP analysis). The yield was 91%, based on the amount of preproinsulin in the starting solution. Higher molecular weight proportions of <0.1% by area were determined by HPLC-GPC analysis.

10

Denaturation assay

The denaturation assay (table 1) shows that the higher molecular weight, polymeric forms of preproinsulins, as produced during the folding reaction, can induce denaturation of native insulin.

15

In the denaturation assay, native insulin glargine, an Aventis Deutschland GmbH product, which is obtained after enzymic cleavage of the preproinsulin described in example 2, was crystallized. Surprisingly, we were able to show in all experiments that, under the conditions of insulin glargine crystallization (pH 6.1 and 26°C), denaturation of native insulin occurs when substances which can induce insulin denaturation are added to the crystallization mixture.

20

A standard solution of the following composition was prepared for the crystallization mixtures:

25

	Insulin glargine	5	g/l
	Citric acid	5.2	mmol/l
30	Zinc chloride	3	mmol/l
	Sodium chloride	0.5	g/l
	n-Propanol	7	%(v/v)
	Purified water to	500	ml
	using 1 N hydrochloric acid, pH	3	

35

The solution was filtered through a membrane filter with a pore width of 0.1 µm.

In the denaturation assay, this acidic standard solution was admixed with solutions of the various assay substances: the washing fraction of column 1 which contained the

removed polymeric forms of preproinsulins at a concentration of 5 g/l or the main fraction of column 2 which contained purified preproinsulin at a concentration of 15 and, respectively, 17 g/l. For further proof that the phenomena observed were caused by insulin denaturation, 10 ml of a 0.1% strength aqueous stock solution of PoloxamerTM 171 were added. Poloxamer 171 is known to be able to suppress insulin denaturation at hydrophobic interfaces (H. Thurow and K. Geisen, Diabetologia (1984) 27, 212-218 and EP 0 018 609).

The solutions were then heated to 26°C and adjusted to pH 6.1 with 10% strength sodium hydroxide solution with stirring, resulting in the precipitation of amorphous insulin. The amorphous suspension was stirred at 26°C for 50 hours. After this time, all mixtures contained insulin crystals.

The mixtures were analyzed by evaluating samples under the microscope, looking for the appearance of amorphous particles (veils) in the background or between the insulin crystals. In addition, each mixture was divided into two parts of approximately the same size. The first part was introduced into a 250 ml measuring cylinder in order to investigate the sedimentation behavior, and after leaving the mixtures at room temperature for 60 min, sediment volume and supernatant clarity were evaluated. The second part was adjusted to pH 3 with 1 N hydrochloric acid, and, after the insulin crystals had dissolved, the clarity of the resulting solution was evaluated.

Table 1 shows the result of the denaturation assay. In the control samples 174 A and 188 A without addition of the polymer fraction, no denaturation had been observed. Under the microscope, crystals were visible against a clear background. After 60 minutes, the crystals had sedimented, resulting in a compact sediment and a clear supernatant. After dissolving the crystals at pH 3, a clear solution had been produced. In contrast, the samples 174 B, 188 B and 174 C, in the case of which 1 ml and, respectively, 5 ml of polymer fraction had been added to the crystallization mixture, showed a distinct denaturation of insulin glargine. Under the microscope, an amorphous veil was visible between the crystals. In the sedimentation assay, voluminous sediments having a sediment volume of from 50 to 90 ml (from 250 ml of crystal suspension) had been produced. After redissolving the crystals at pH 3, more or less opaque amorphous suspensions had been produced. In the presence of 20 ppm of Poloxamer 171, no denaturation had been observed with the addition of 1 ml of polymer solution (188 C). In the assay mixtures 174 D, 174 E and 174 F

which had been admixed with purified preproinsulins (main fraction of column 2 from examples 1, 2 and 3), likewise no denaturation of insulin glargine was observed.

Similar results, not shown here, were obtained in an analogous denaturation assay
5 in which human insulin was crystallized.

Table 1
Influence of higher molecular weight impurities on insulin glargine denaturation

Crystallization mixture No.	Additions to the crystallization mixture	Microscopic image background appearance (between rhombohedral crystals)	Appearance after dissolving the crystals at pH 3	Sedimentation behavior of crystal suspension
174 A	None	clear	clear	+++
174 B	1 ml of washing fraction, column 1 *	amorphous particles	slightly opaque	+ - -
174 C	5 ml of washing fraction, column 1 *	more amorphous particles	opaque	- - -
174 D	1 ml of main fraction, example 1 **	clear	clear	+++
174 E	1 ml of main fraction, example 2 ***	clear	clear	+++
174 F	1 ml of main fraction, example 3 ****	clear	clear	+++
188 A	None	clear	clear	+++
188 B	1 ml of washing fraction, column 1 *	amorphous particles	opaque	- - -
188 C	1 ml of washing fraction, column 1 * and 20 ppm Poloxamer 171	occasional amorphous particles	clear	+++

Crystallization mixtures of in each case 500 ml with 2 500 mg of insulin glargine (= 5 g/l).

contains 5 g/l protein.

+ + + = After approx. 60 min, 3 to 5 ml of sediment from 250 ml of suspension.

15 g/l preproinsulin

- - - = After approx. 60 min, up to 90 ml of sediment from 250 ml of suspension.

17 g/l preproinsulin

* The washing fraction of column 1 from example 2

** The main fraction of column 2 from example 1 contains

*** The main fraction of column 2 from example 2 contains

**** The main fraction of column 2 from example 3 contained 17 g/

SEQUENCE LISTING

<110> Aventis Pharma Deutschland GmbH

<120> A method for purifying preproinsulin

<130> 9982-863

<140> CA 2,493,539

<141> 2003-07-18

<150> DE10235168.6

<151> 2002-08-01

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<170> PatentIn Ver. 2.1

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Leu Gln Pro Leu Ala Leu Glu Gly Ser Leu Gln Lys Arg
20 25

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20 25 30

Gly Phe Phe Tyr Thr Pro Lys Thr Arg Arg Glu Ala Glu Asp Pro Gln
35 40 45

Val Gly Gln Val Glu Leu Gly Gly Gly Pro Gly Ala Gly Ser Leu Gln
50 55 60

Pro Leu Ala Leu Glu Gly Ser Leu Gln Lys Arg Gly Ile Val Glu Gln
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 20 25 30
 Gly Phe Phe Tyr Thr Pro Lys Thr Arg Arg Glu Ala Glu Asp Pro Gln
 35 40 45
 Val Gly Gln Val Glu Leu Gly Gly Gly Pro Gly Ala Gly Ser Leu Gln
 50 55 60
 Pro Leu Ala Leu Glu Gly Ser Leu Gln Lys Arg Gly Ile Val Glu Gln
 65 70 75 80
 Cys Cys Thr Ser Ile Cys Ser Leu Tyr Gln Leu Glu Asn Tyr Cys Gly
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 1 5 10 15
 Cys Gly Ser His Leu Val Glu Ala Leu Tyr Leu Val Cys Gly Glu Arg
 20 25 30
 Gly Phe Phe Tyr Thr Pro Glu Thr Arg Asp Val Pro Gln Val Glu Leu
 35 40 45

28

Gly Gly Gly Pro Gly Ala Gly Ser Leu Gln Pro Leu Ala Leu Glu Gly
50 55 60

Ser Leu Gln Lys Arg Gly Ile Val Glu Gln Cys Cys Thr Ser Ile Cys
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Ser Leu Tyr Gln Leu Glu Asn Tyr Cys Asn
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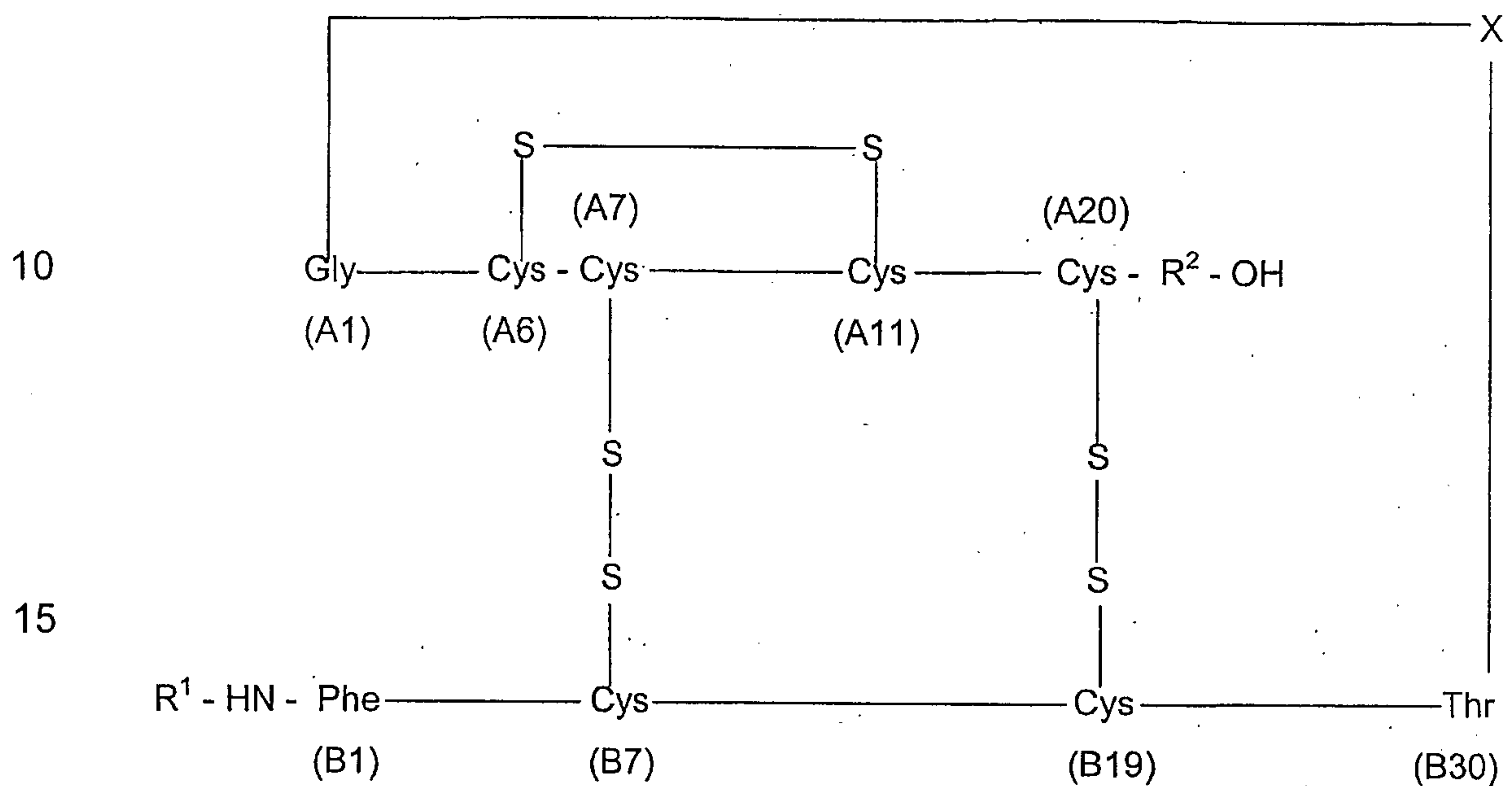
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Ala Thr Thr Ser Thr Gly Asn Ser Ala Arg
1 5 10

Claims:

1. A method for the chromatographic purification of preproinsulin of the formula 1,

5



in which

25 X a) is a genetically encodable amino acid residue or
 b) is a peptide having from 2 to 35 amino acid residues, which starts and ends with a basic amino acid residue,

30 R¹ a) is hydrogen,
 b) is a genetically encodable amino acid residue or
 c) is a peptide having from 2 to 15 amino acid residues,

R² is a genetically encodable amino acid residue, and

and the residues A1 - A20 correspond to the amino acid sequence of the A chain of human insulin or of an insulin analog and the residues B1 - B30 correspond to the amino acid sequence of the B chain of human insulin or of an insulin analog;

5

wherein said method for chromatographic purification of preproinsulin comprises: removing higher molecular weight substances from an aqueous solution of said preproinsulin by means of a first chromatography on an anion exchanger in flow-through mode and a subsequent second chromatography on a cation exchanger in adsorption mode.

10

2. The method for the chromatographic purification of preproinsulin according to claim 1, wherein said preproinsulin of the formula 1 has the following amino acid sequence:

15

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Asn-Gln-His-Leu-Cys-Gly-Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-Thr-Pro-Lys-Thr-Arg-Arg-Glu-Ala-Glu-Asp-Pro-Gln-Val-Gly-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg-Gly-Ile-Val-Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Asn (SEQ ID NO: 2).

20

3. The method for the chromatographic purification of preproinsulin according to claim 1, wherein said preproinsulin of the formula 1 has the following amino acid sequence:

25

Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Ala-Arg-Phe-Val-Asn-Gln-His-Leu-Cys-Gly-Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-Thr-Pro-Lys-Thr-Arg-Arg-Glu-Ala-Glu-Asp-Pro-Gln-Val-Gly-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-

30

Ala-Leu-Glu-Gly-Sec-Leu-Gln-Lys-Arg-Gly-Ile-Val-Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Gly (SEQ 1D NO: 3).

4. The method for the chromatographic purification of preproinsulin according to claim 1, wherein said preproinsulin of the formula 1 has the following amino acid sequence:
- Ala-Thr-Thr-Ser-Thr-Gly-Asn-Ser-Afa-Arg-Phe-Val-Lys-Gln-His-Leu-Cys-Gly-Ser-His-Leu-Val-Glu-Ala-Leu-Tyr-Leu-Val-Cys-Gly-Glu-Arg-Gly-Phe-Phe-Tyr-Thr-Pro-Glu-Thr-Arg-Asp-Val-Pro-Gln-Val-Glu-Leu-Gly-Gly-Gly-Pro-Gly-Ala-Gly-Ser-Leu-Gln-Pro-Leu-Ala-Leu-Glu-Gly-Ser-Leu-Gln-Lys-Arg-Gly-Ile-Val-Glu-Gln-Cys-Cys-Thr-Ser-Ile-Cys-Ser-Leu-Tyr-Gln-Leu-Glu-Asn-Tyr-Cys-Asn (SEQ ID NO: 4).
5. The method for the chromatographic purification of preproinsulin according to claim 1 wherein in the formula 1, X is a peptide having from 2 to 35 amino acid residues which starts and ends with the basic amino acid residue Arg.
6. The method for the chromatographic purification of preproinsulin according to claim 1 wherein in the formula 1, X is a peptide having from 4 to 35 amino acid residues starts and ends with in each case two basic amino acid residues.
7. The method for the chromatographic purification of preproinsulin according to claim 6 wherein the two basic amino acid residues are independently selected from Arg and Lys.
8. The method as claimed in any one of claims 1 to 7 for separating foreign substances which induce insulin denaturation from the solution of preproinsulin.

9. The method as claimed in any one of claims 1 to 8, wherein the second chromatography is carried out at a pH of from 3.0 to 5.5.
10. The method as claimed in any one of claims 1 to 9, wherein the second chromatography is carried out under a pressure of from 1 to 30 bar.
11. A method for preparing insulin by expressing nonfolded preproinsulin, comprising the steps:
- a) fermenting of genetically modified microorganisms which express nonfolded preproinsulin,
 - b) harvesting the microorganisms and disrupting cells of the microorganisms,
 - c) isolating inclusion bodies containing undissolved, nonfolded preproinsulin,
 - d) dissolving the preproinsulin with correct folding of the peptide chain and simultaneous closure of the disulfide bridges to give preproinsulin,
 - e) purifying the preproinsulin using the method of any one of claims 1 to 10;
 - f) enzymatically cleaving the preproinsulin to give human insulin,
 - g) purifying human insulin,
 - h) crystallizing the human insulin and drying.