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(72) Inventeurs/Inventors:

ZHENG, CUI, CN;  
ZHU, GUIXIANG, CN;  
LIU, LIZHI, CN;  
ZHANG, WEI, CN

(73) Propriétaires/Owners:

CHINA PETROLEUM & CHEMICAL CORPORATION,  
CN;  
BEIJING RESEARCH INSTITUTE OF CHEMICAL  
INDUSTRY, CHINA PETROLEUM & CHEMICAL  
CORPORATION, CN

(74) Agent: RIDOUT & MAYBEE LLP

(54) Titre : COMPOSITION DE POLYESTER ET PROCEDE DE PREPARATION ASSOCIE

(54) Title: POLYESTER COMPOSITION AND PREPARATION METHOD THEREFOR

(57) Abrégé/Abstract:

The present invention relates to a polyester composition and a preparation method therefor. The polyester composition provided by the present invention comprises polybutylene terephthalate and an aliphatic-aromatic copolyester, wherein based on the total weight of the polybutylene terephthalate and the aliphatic-aromatic copolyester, the content of the polybutylene terephthalate is from 50 to 99% by weight, and the content of the aliphatic-aromatic copolyester is from 1 to 50% by weight. Also provided are a method for preparing such a polyester composition and a toughened composite material prepared therefrom. The polyester composition provided by the present invention has an elongation at break of up to 230% or above, have significantly improved toughness without substantial loss of strength.

**Abstract**

The present invention relates to a polyester composition and a preparation method therefor. The polyester composition provided by the present invention comprises polybutylene terephthalate and an aliphatic-aromatic copolyester, wherein based on the total weight of the polybutylene terephthalate and the aliphatic-aromatic copolyester, the content of the polybutylene terephthalate is from 50 to 99% by weight, and the content of the aliphatic-aromatic copolyester is from 1 to 50% by weight. Also provided are a method for preparing such a polyester composition and a toughened composite material prepared therefrom. The polyester composition provided by the present invention has an elongation at break of up to 230% or above, have significantly improved toughness without substantial loss of strength.

## **Polyester Composition and Preparation Method Therefor**

### **Technical Field**

The present invention relates to the field of polymer, specifically to a polyester composition and a process for the preparation of the polyester composition, as well as a toughened composite material prepared from the polyester composition.

### **Background Art**

Polybutylene terephthalate (PBT) is one of the five major engineering plastics. It was first synthesized by German scientist P. Schlack in 1942 and then industrially developed by the US company Celanese (now Ticona) and marketed under the trade name Celanex. PBT has the characteristics of good dimensional stability, high-temperature resistance, excellent flame retardant and insulation properties, good fluidity, small linear thermal expansion coefficient, good chemical solvent resistance, etc. It has a wide range of applications in the fields of electrical and electronic industry, automotive industry and office machinery. However, PBT is very poor in terms of impact resistance, especially very sensitive to defects. A tiny notch on the surface of an article may cause the whole article to be fractured. Therefore, it is quite necessary to modify PBT by toughening.

The toughening modification of PBT is mainly modification by blending, which in turn is mainly divided into three categories. The first category is toughening with fibers, wherein mainly glass fibers are added to PBT, and other fibers such as carbon fibers, bamboo fibers or flax fibers may also be added. For example, in CN105086387A, glass fibers are added to the PBT in about half of the amount thereof, which can significantly increase the notched impact strength thereof. The main disadvantage of adding fibers is that the material can no longer be processed using a conventional injection molding process, but often additional matching process cost is required, especially for long fibers that significantly improve the properties, the process cost is significant. The second category is addition of high impact materials. Due to the relatively high processing temperature of PBT, it is often necessary to add materials that can withstand relatively high processing temperatures. A very common example is addition of PC (polycarbonate). For example, in CN104693759A, after about 100% to 200% of PC based on the amount of PBT is added to PBT, the toughness is improved. The disadvantage of adding high impact materials is that

almost all the current high impact materials are incompatible with PBT, they repel each other at the molecular level, and they are difficult to be completely mixed uniformly even after very strong blending conditions. Adding a large amount of a compatibilizer can partially solve this problem, but at the same time it will bring about a decline in material properties. The third category is the addition of other materials that are very similar to the PBT molecular structure but tougher than PBT to slightly improve the toughness of PBT. A typical example is PET (polyethylene terephthalate). For example, in CN104419125A, PBT and PET are blended in about equal amounts, the material obtained has stronger toughness than PBT. The disadvantage of this category is that even if the material similar to PBT in molecular structure has a better toughness than PBT, it is not better by a large margin, and the final result is that the toughness of the obtained composite material is not significantly improved.

Another effective method for the toughening modification of PBT by blending is to modify PBT by blending using a copolymer containing a group similar to the PBT in structure. However, although there are many copolymers containing PBT structure at present, due to various reasons, such as material properties and cost control, there is yet no modified material obtained by blending PBT and corresponding copolymer on the market. Therefore, at present, there is an urgent need to find a PBT product modified in terms of toughness.

#### Disclosure

#### Summary of the Invention

It is an object of the present invention to provide a polyester composition and a process for its preparation, as well as a toughened composite material prepared from the polyester composition, so as to overcome the above defects of the existing PBT products. Compared with PBT, the toughness of the polyester composition and the composite material of the present invention should be significantly improved without substantial loss of strength.

Another object of the invention is to improve the compatibility of PBT with other components in the polyester composition so that it is unnecessary to additionally add a compatibilizer.

Another object of the present invention is to provide a polyester composition which shall

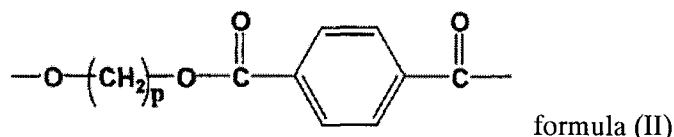
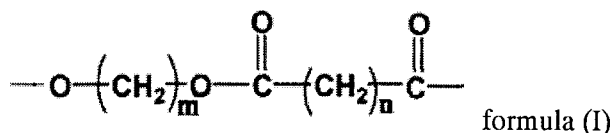
be processable using the same equipment as that for PBT, without the need for additional modifications to the processing equipment during its preparation.

According to the present invention, the above objects are achieved by a polyester composition comprising PBT and a specific aliphatic-aromatic copolyester.

Thus, the present invention provides a polyester composition comprising

(1) from 50 to 99% by weight, preferably from 70 to 95% by weight, more preferably from 80 to 90% by weight, of polybutylene terephthalate; and

(2) from 1 to 50% by weight, preferably from 5 to 30% by weight, more preferably from 10 to 20% by weight, of an aliphatic-aromatic copolyester, wherein the aliphatic-aromatic copolyester is a copolymer comprising a repeating unit A represented by formula (I) and a repeating unit B represented by formula (II),



wherein based on the total moles of the repeating unit A and the repeating unit B in the aliphatic-aromatic copolyester, the content of the repeating unit A is from 1 to 60 mol%, preferably from 20 to 55 mol%, and more preferably from 20 to 40 mol%, and the content of the repeating unit B is from 40 to 99 mol%, preferably from 45 to 80 mol%, and more preferably from 60 to 80 mol%; m is an integer of 2 to 10, n is an integer of 2 to 8, p is an integer of 2 to 10, preferably, m is an integer of 2 to 6, n is an integer of 2 to 4, p is an integer of 2 to 6, preferably 2 to 4; and m, n and p are the same or different;

wherein the % by weight is calculated based on the total weight of the polybutylene terephthalate and the aliphatic-aromatic copolyester.

Preferably, the aliphatic-aromatic copolyester has a weight average molecular weight of 50,000 to 900,000, preferably 100,000 to 500,000, as determined by GPC; preferably, the molecular weight distribution is from 1.2 to 3, as determined by GPC.

Preferably, the polybutylene terephthalate has a weight average molecular weight of 100,000 to 200,000, as determined by GPC.

5 The polyester composition may further comprise a nucleating agent; the content of the nucleating agent is from 0.01 to 10% by weight, preferably from 0.2 to 5% by weight, based on the total weight of the polyester composition.

10 The nucleating agent may be one or more selected from the group consisting of talc, calcium oxide, carbon black, calcium carbonate, inorganic pigments, kaolin, metal carboxylates, metal phosphates, dibenzyl sorbitol and derivatives thereof, polyvinylcyclohexane, polyvinylcyclopentane, low density polyethylene, hyperbranched polyamide and ethylene-methacrylic acid ionomer; preferably one or more selected from the group consisting of calcium carbonate, low density polyethylene, dibenzyl sorbitol and derivatives thereof and hyperbranched polyamide.

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The polyester composition may further comprise other additives such as erucylamide and/or white oil.

20 Further, the aliphatic-aromatic copolyester may be at least one selected from the group consisting of a random copolymer, an alternating copolymer, a block copolymer, and a graft copolymer.

25 Advantageously, the polyester composition according to the present invention may have an elongation at break of up to 230% or above, as measured by the method according to the standard GB/T 1040.2-2006.

30 The present invention also provides a process for the preparation of a polyester composition according to the present invention, which comprises: mixing polybutylene terephthalate and an aliphatic-aromatic copolyester and subjecting the resulting mixture to extrusion pelletization to obtain a polyester composition.

The mixing may be carried out under stirring; and the stirring rate may be from 6 to 60 rpm, and the stirring time may be from 2 to 30 min.

Advantageously, said extrusion pelletization is carried out in a twin-screw extruder; preferably, said extrusion pelletization conditions include: a temperature of 230 to 300 °C, a screw rotational speed of 10 to 70 rpm, and a torque of 2 to 80 N \*m.

5

Preferably, no compatibilizer is added during the mixing process.

In another aspect, the present invention further provides a toughened composite material prepared from the polyester composition, which toughened composite material may have an elongation at break of up to 230% or above, as measured by the method according to the standard GB/T 1040.2-2006.

The present invention achieves the object of toughening modification of PBT by blending PBT with an aliphatic-aromatic copolyester. Compared with PBT, the polyester composition provided by the present invention has significantly improved toughness without significant loss of strength; at the same time, in the preparation of the polyester composition, since PBT and the aliphatic-aromatic copolymer used in the present invention have good compatibility, it is unnecessary to additionally add a compatibilizer. In addition, the polyester composition provided by the present invention can be processed using the same equipment as that for PBT, without the need for additional modifications to the processing equipment during its preparation. Therefore, the polyester composition provided by the present invention has good industrial application prospects.

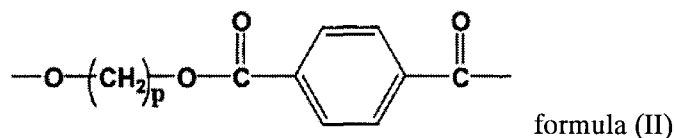
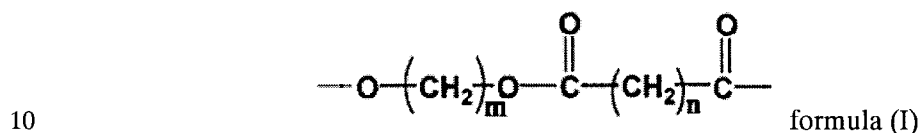
Other characters and advantages of the present invention will be described in detail under Detailed Description of the Invention below.

#### Detailed Description of the Invention

The present invention provides a polyester composition comprising polybutylene terephthalate and an aliphatic-aromatic copolyester, wherein the content of the polybutylene terephthalate is from 50 to 99% by weight, and the content of the aliphatic-aromatic copolyester is from 1 to 50% by weight, based on the total weight of the polybutylene terephthalate and the aliphatic-aromatic copolyester.

Preferably, the content of the polybutylene terephthalate is from 70 to 95% by weight, and the content of the aliphatic-aromatic copolyester is from 5 to 30% by weight, based on the total weight of the polybutylene terephthalate and the aliphatic-aromatic copolyester; more preferably, the content of the polybutylene terephthalate is from 80 to 90% by weight, and the content of the aliphatic-aromatic copolyester is from 10 to 20% by weight.

According to the present invention, the aliphatic-aromatic copolyester may be a copolymer comprising a repeating unit A represented by formula (I) and a repeating unit B represented by formula (II),



wherein based on the total moles of the repeating unit A and the repeating unit B in the aliphatic-aromatic copolyester, the content of the repeating unit A is from 1 to 60 mol%, and the content of the repeating unit B is from 40 to 99 mol%; m is an integer of 2 to 10, n is an integer of 2 to 8, p is an integer of 2 to 10; and m, n and p are the same or different, the aliphatic-aromatic copolyester may have a weight average molecular weight of 50,000 to 900,000.

Preferably, based on the total moles of the repeating unit A and the repeating unit B in the aliphatic-aromatic copolyester, the content of the repeating unit A is from 20 to 55 mol%, more preferably from 20 to 50 wt.%; the content of the repeating unit B is from 45 to 80 wt.%, more preferably from 50 to 80 wt.%; m is an integer of 2 to 6, n is an integer of 2 to 4, p is an integer of 2 to 6, preferably 2 to 4; and m, n and p are the same or different, the aliphatic-aromatic copolyester may have a weight average molecular weight of 100,000 to 500,000.

In the present invention, the weight average molecular weight of the polymer is determined by gel permeation chromatography (GPC).

In the present invention, the aliphatic-aromatic copolyester may be at least one selected from the group consisting of a random copolymer, an alternating copolymer, a block copolymer and a graft copolymer, preferably, a random copolymer and/or a block copolymer. The source of the aliphatic-aromatic copolyester in the present invention is not particularly limited, and it can be obtained by a conventional means in the art, for example, obtained commercially, or prepared by the process disclosed in CN100429256C.

Specifically, the process for preparing the aliphatic-aromatic copolyester may comprise the following steps:

(1) reacting monomer A with monomer B in the presence of a first catalyst in an inert atmosphere;

(2) reacting monomer C with monomer D in the presence of the first catalyst in an inert atmosphere;

(3) reacting the reaction product obtained in step (1) with the reaction product obtained in step (2) in the presence of a second catalyst;

wherein the monomer A is butanediol; the monomer B is terephthalic acid and/or an ester thereof, preferably, at least one selected from the group consisting of terephthalic acid, dimethyl terephthalate and diethyl terephthalate; the monomer C is a C2-C4 diol (particularly a saturated linear diol); the monomer D is a C4-C6 dibasic acid (particularly a saturated linear dibasic acid); the first catalyst is at least one selected from the group consisting of tetrabutyl titanate, titanium dioxide, diethoxy titanium and zinc acetate, preferably tetrabutyl titanate; the second catalyst is at least one selected from the group consisting of lanthanum acetylacetonate, lanthanum trichloride, triphenoxy lanthanum and lanthanum propionate, preferably lanthanum acetylacetonate.

In the present invention, in step (1), the molar ratio of the monomer B to the first catalyst is 1 : 0.0001-0.02 : 0.0001-0.02, more preferably 1 : 0.001-0.003 : 0.001-0.003.

In the present invention, in step (2), the molar ratio of the monomer D to the first catalyst is 1 : 0.0001-0.02 : 0.0001-0.02, more preferably 1 : 0.001-0.003 : 0.001-0.003.

Preferably, the molar ratio of the total amount of the first catalyst (the sum of the amount of the first catalyst in step (1) and the amount of the first catalyst in step (2)) to the amount

of the second catalyst is 1 : 0.5-1.5, preferably 1 : 0.8-1.2.

In the present invention, the kinds of the various reactive monomers can be adjusted correspondingly according to the composition and molecular weight of the target product, and the molecular weight of the product and the content of each repeating unit in the product are controlled by adjusting the feeding amount and the feeding ratio, respectively.

In the present invention, in step (1), the reaction temperature is preferably 160 to 220 °C; in the present invention, in step (2), the reaction temperature is preferably 160 to 220 °C; in the present invention, in step (3), the reaction temperature is preferably 180 to 240°C.

In a preferred embodiment of the present invention, when m1 is 4, the process for preparing the aliphatic-aromatic copolyester comprises the following steps:

(S1) reacting butanediol with monomer A' in the presence of a first catalyst in an inert atmosphere;

(S2) reacting the reaction product obtained in step (S1) with monomer B' in the presence of a second catalyst;

wherein A' is terephthalic acid and/or an ester thereof, preferably at least one selected from the group consisting of terephthalic acid, dimethyl terephthalate and diethyl terephthalate; the monomer B' is a C4-C6 dibasic acid (particularly a saturated linear dibasic acid); the first catalyst and the second catalyst are described as above and will not be further described herein.

In the present invention, in step (S1), the molar ratio of the monomer A' to the first catalyst is 1 : 0.0001-0.02 : 0.0001-0.02, more preferably 1 : 0.001-0.003 : 0.001-0.003.

Preferably, the molar ratio of the first catalyst to the second catalyst is 1 : 0.5-1.5, preferably 1 : 0.8-1.2.

In the present invention, the kinds of the various reactive monomers can be adjusted correspondingly according to the composition and molecular weight of the target product, and the molecular weight of the product and the content of each repeating unit in the product are controlled by adjusting the feeding amount and the feeding ratio, respectively.

In the present invention, in step (S1), the reaction temperature is preferably 160 to 220°C; in the present invention, in step (S2), the reaction temperature is preferably 180 to 240°C.

5 More specifically, the process for producing the aliphatic-aromatic copolyester may comprise the following steps: adding 1,4-butanediol, dimethyl benzoate and the catalyst as described in US11312373 to a reactor, heating and stirring under a nitrogen atmosphere until a clear solution is obtained; subsequently, increasing the temperature to 160 to 220 °C for reaction; adding succinic acid after most of the distilled methanol in the system is  
10 removed, and increasing the temperature to 180 to 240°C; removing most of the water by distillation, then slowly creating a vacuum environment, and increasing the temperature of the system to 220 to 280°C; after 3 to 6 hours, completing the reaction to obtain a product.

In the present invention, the polybutylene terephthalate is not particularly limited and may  
15 be a conventional selection in the art, for example, the polybutylene terephthalate may have a weight average molecular weight of 100,000 to 200,000, and can be obtained commercially as usual, such as Crastin SC164 NC010, available commercially from the company DuPont.

20 According to the present invention, the polyester composition may further comprise a nucleating agent; the content of the nucleating agent is from 0.01 to 10% by weight, preferably from 0.2 to 5% by weight, more preferably from 1 to 5% by weight, based on the total weight of the polyester composition.

25 According to the present invention, the nucleating agent may be those as conventionally selected in the art. For example, the nucleating agent may be one or more selected from the group consisting of talc, calcium oxide, carbon black, calcium carbonate, inorganic pigments (such as the yellow or green pigments purchased from Guangzhou Yingyi Plastic Pigment Co., Ltd.), kaolin, metal carboxylates, metal phosphates, dibenzyl sorbitol and  
30 derivatives thereof, polyvinylcyclohexane, polyvinylcyclopentane, low density polyethylene, hyperbranched polyamide and ethylene-methacrylic acid ionomer; preferably one or more selected from the group consisting of calcium carbonate, low density polyethylene, dibenzyl sorbitol and derivatives thereof, and hyperbranched polyamide;

more preferably, calcium carbonate and/or low density polyethylene.

In the present invention, the polyester composition may further comprise other additives, such as erucylamide and/or white oil.

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The present invention further provides a process for the preparation of the polyester composition according to the present invention, comprising: mixing all the components including polybutylene terephthalate and the aliphatic-aromatic copolyester, and subjecting the resulting mixture to extrusion pelletization to obtain the polyester composition.

10

According to the present invention, the above process may further comprise carrying out the process of mixing the polybutylene terephthalate and the aliphatic-aromatic copolyester in the presence of a nucleating agent; the nucleating agent may be used in an amount of 0.01 to 10% by weight, preferably 0.2 to 5% by weight, more preferably 1 to 5% by weight, based on the total weight of the polyester composition.

15

The types of the nucleating agent are described as above.

In the present invention, the process may further comprise: carrying out the process of mixing PBT and the aliphatic-aromatic copolyester in the presence of a nucleating agent and other additives, wherein the other additives may be erucylamide and/or white oil.

20

According to the present invention, the mixing can be carried out under stirring; the stirring rate can be 6 to 60 rpm, and the stirring time can be 2 to 30 min.

25

According to the present invention, the extrusion pelletization process can be carried out according to a conventional extrusion pelletization method, for example, the extrusion pelletization can be carried out in a twin-screw extruder; preferably, the extrusion pelletization conditions include: a temperature of 230 to 300°C, a screw rotational speed of 10 to 70 rpm, and a torque of 2 to 80 N\*m; more preferably, the twin-screw extruder includes six temperature sections, and the temperatures of various sections from the feed inlet to the extrusion outlet are successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C.

30

In the present invention, the inventors have unexpectedly found during the research that blending PBT with an aliphatic-aromatic copolyester can significantly improve the toughness of the product; and, the aliphatic-aromatic copolyester have good compatibility with the copolymer of PBT, the purpose of toughening modification of PBT material can be achieved under conventional blending conditions without the need of additionally adding a compatibilizer. Thus, in the present invention, the mixing process may be carried out without adding a compatibilizer.

In the present invention, the compatibilizer may be those conventionally selected in the art, and may be, for example, at least one selected from the group consisting of PE-g-ST, PP-g-ST, ABS-g-MAH, PE-g-MAH and PP-g- MAH.

The polyester composition according to the present invention may have an elongation at break of up to 230% or above, and has significantly improved toughness.

A toughened composite material can be prepared from the polyester composition of the present invention by a conventional molding process. The toughened composite material according to the present invention may have an elongation at break of up to 230% or above, measured by the method according to the standard GB/T 1040.2-2006.

#### Examples

The present invention will be described in detail below by way of examples. It shall be understood that the examples described herein are merely used to explain and illustrate the present invention and are not intended to limit the present invention.

In the following examples and comparative examples,

the weight average molecular weight of a polymer was determined by gel permeation chromatography (GPC) on Waters-208 (with a Waters 2410 RI detector, 1.5 mL/min flow rate, 30°C) instrument, using tetrahydrofuran (THF) as the solvent, and calibrated with polystyrene standard;

the microstructure of PBT and the aliphatic-aromatic copolyester was determined by an AVANCE DRX 400 MHz NMR spectrometer from the company Bruker, Switzerland, using deuterated chloroform as the solvent;

the constitution of the polyester composition was determined by the feeding of the starting materials;

the mechanical properties of the polyester composition were tested by the method according to the standard GB/T 1040.2-2006, and the gauge dimension of 5B was chosen;

5 unless otherwise specified, the aliphatic-aromatic copolyester used in the present invention was self-made according to the process disclosed in Examples B13-B21 of CN100429256C, wherein the kinds of the starting materials for reaction can be correspondingly adjusted according to the composition and molecular weight of the target product, and the molecular weight of the product and the content of each repeating unit in  
10 the product can be controlled by adjusting the feeding amount and the feeding ratio, respectively.

#### Example 1

180g of polybutylene terephthalate (available from the company DuPont, under the  
15 designation Crastin SC164 NC010, the same below), 20g of butylene terephthalate-butylene succinate copolyester (weight average molecular weight of 100,000, wherein based on the total moles of the butylene succinate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 80 mol%) and 2g of calcium carbonate were mixed under stirring, with the stirring rate of 10  
20 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections in the twin-screw extruder from the feed inlet to the extrusion outlet being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester  
25 composition A1.

#### Comparative example 1

A polyester composition was prepared according to the process of Example 1, except that the butylene terephthalate-butylene succinate copolyester used in Example 1 was not added,  
30 to obtain polyester composition D1.

#### Comparative example 2

A polyester composition was prepared according to the process of Example 1, except that

the amount of the polybutylene terephthalate was 20g, and the amount of the butylene terephthalate-butylene succinate copolyester was 180g, to obtain polyester composition D2.

5 Comparative example 3

A polyester composition was prepared according to the process of Example 1, except that the same weight of polybutylene succinate (available from the company BASF, under the designation 1111HTA4) was used instead of the butylene terephthalate-butylene succinate copolyester used in Example 1, to obtain polyester composition D3.

10

Comparative example 4

A polyester composition was prepared according to the process of Example 1, except that the same weight of polyethylene terephthalate (available from the company DuPont, under the designation FR530) was used instead of the butylene terephthalate-butylene succinate copolyester used in Example 1, to obtain polyester composition D4.

15

Example 2

180g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 20g of butylene terephthalate-butylene succinate copolyester (weight average molecular weight of 100,000, wherein based on the total moles of the butylene succinate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 60 mol%) and 2g of calcium carbonate were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester composition A2.

25

30 Example 3

180g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 20g of ethylene terephthalate- ethylene succinate copolyester (weight average molecular weight of 100,000, wherein based on the total

moles of the ethylene succinate repeating unit and the ethylene terephthalate repeating unit, the content of the ethylene terephthalate repeating unit is 80 mol%) and 2g of calcium carbonate were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester composition A3.

#### 10 Example 4

180g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 20g of butylene terephthalate-butylene adipate copolyester (weight average molecular weight of 100,000, wherein based on the total moles of the butylene adipate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 60 mol%) and 2g of calcium carbonate were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester composition A4.

#### Example 5

160g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 40g of butylene terephthalate-butylene adipate copolyester (weight average molecular weight of 100,000, wherein based on the total moles of the butylene adipate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 60 mol%) and 2g of calcium carbonate were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C,

260°C, 265°C, 260°C, to prepare polyester composition A5.

#### Example 6

160g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 40g of butylene terephthalate-butylene adipate copolyester (weight average molecular weight of 100,000, wherein based on the total moles of the butylene adipate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 60 mol%) and 10g of calcium carbonate were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester composition A6.

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#### Example 7

160g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 40g of butylene terephthalate-butylene adipate copolyester (weight average molecular weight of 100,000, wherein based on the total moles of the butylene adipate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 60 mol%) and 2g of a low density polyethylene (available from SINOPEC Yanshan Petrochemical Company, under the designation LD607) were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester composition A7.

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#### Example 8

180g of polybutylene terephthalate (available from the company DuPont, under the designation Crastin SC164 NC010), 20g of butylene terephthalate-butylene succinate copolyester (weight average molecular weight of 500,000, wherein based on the total

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moles of the butylene succinate repeating unit and the butylene terephthalate repeating unit, the content of the butylene terephthalate repeating unit is 80 mol%) and 2g of calcium carbonate were mixed under stirring, with the stirring rate of 10 rpm and for the time of 10 minutes. The resulting mixture was subjected to extrusion pelletization via a twin-screw extruder, with the rotational speed of the screw being controlled at 10 rpm, the screw torque being 20 N\*m, and the temperatures of various sections from the feed inlet to the extrusion outlet in the twin-screw extruder being successively 240°C, 250°C, 260°C, 260°C, 265°C, 260°C, to prepare polyester composition A8.

#### 10 Example 9

A polyester composition was prepared according to the process of Example 1, except that the calcium carbonate used in Example 1 was not added, to obtain polyester composition A9.

#### 15 Test examples

The polyester compositions prepared in Examples 1-9 and Comparative examples 1-4 were made into specimens, respectively, which were subjected to mechanical property tests such as tensile yield strength (MPa) and elongation at break (%). The results are shown in Table 1 below.

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Table 1

|                | Specimen material | Tensile yield strength (MPa) | Elongation at break (%) |
|----------------|-------------------|------------------------------|-------------------------|
| Test example 1 | A1                | 54                           | 320                     |
| Test example 2 | D1                | 58                           | 8                       |
| Test example 3 | D2                | 25                           | 520                     |
| Test example 4 | D3                | 50                           | 12                      |
| Test example 5 | D4                | 51                           | 10                      |
| Test example 6 | A2                | 53                           | 370                     |
| Test example 7 | A3                | 45                           | 230                     |
| Test example 8 | A4                | 53                           | 380                     |
| Test example 9 | A5                | 48                           | 520                     |

|                 |    |    |     |
|-----------------|----|----|-----|
| Test example 10 | A6 | 50 | 450 |
| Test example 11 | A7 | 51 | 480 |
| Test example 12 | A8 | 55 | 310 |
| Test example 13 | A9 | 52 | 320 |

It can be seen from the comparison of the results of the mechanical property tests of the specimens made from the above polyester compositions, which are prepared in Examples 1 to 9 and Comparative examples 1 to 4, that the polyester compositions provided by the present invention have an elongation at break as high as 230% or above, have significantly improved toughness without substantial loss of strength. Moreover, it is unnecessary to additionally add a compatibilizer during the preparation of the polyester compositions. In addition, the polyester compositions provided by the present invention can be processed using the same equipment as that for PBT, without the need for additional modifications to the processing equipment during its preparation. Therefore, the polyester compositions provided by the invention have good industrial application prospects.

The endpoints of the ranges and any values disclosed herein are not limited to the precise ranges or values, and these ranges or values shall be understood as including values that are close to the ranges or values. For numerical ranges, a combination may be made between the endpoint values of the various ranges, between the endpoint values of the various ranges and the individual point values, and between the individual point values to obtain one or more new numerical ranges. These numerical ranges shall be considered as specifically disclosed herein.

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The preferred embodiments of the present invention have been described in detail above, but the present invention is not limited to the specific details of the above embodiments. Within the scope of the technical concept of the present invention, various simple modifications can be made to the technical solutions of the present invention. These simple variants all fall within the protection scope of the present invention.

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It shall be further noted that the various specific technical features described in the above specific embodiments may be combined in any suitable manner without contradiction. In

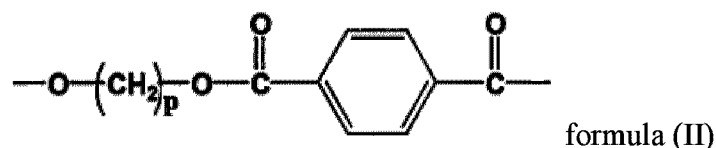
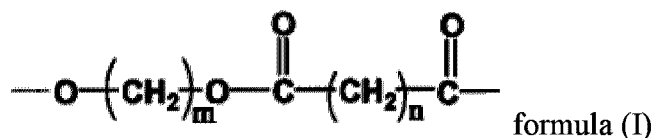
order to avoid unnecessary repetition, the present invention will not further describe the various possible combinations.

In addition, the various different embodiments of the present invention may be combined  
5 randomly. As long as such a combination does not deviate from the idea of the present invention, it shall also be regarded as the disclosure of the present invention.

## **WHAT IS CLAIMED IS:**

1. A polyester composition, comprising

- (1) from 80 to 90% by weight of polybutylene terephthalate; and
- (2) from 10 to 20% by weight of an aliphatic-aromatic copolyester, wherein the aliphatic-aromatic copolyester is a copolymer comprising a repeating unit A represented by formula (I) and a repeating unit B represented by formula (II),



wherein based on the total moles of the repeating unit A and the repeating unit B in the aliphatic-aromatic copolyester, the content of the repeating unit A is from 20 to 40 mol%, and the content of the repeating unit B is from 60 to 80 mol%; m is an integer of 2 to 6, n is 2, p is an integer of 2 to 4; and m, n and p are the same or different;

wherein the % by weight is calculated based on the total weight of the polybutylene terephthalate and the aliphatic-aromatic copolyester;

wherein the aliphatic-aromatic copolyester has a weight average molecular weight of 100,000 to 500,000, as determined by GPC.

2. The polyester composition according to claim 1, characterized in that the aliphatic-aromatic copolyester has a molecular weight distribution of 1.2 to 3, as determined by GPC.

3. The polyester composition according to claim 1 or 2, characterized in that the polybutylene terephthalate has a weight average molecular weight of 100,000 to 200,000, as determined by GPC.

4. The polyester composition according to any one of claims 1 to 3, characterized in that the polyester composition further comprises a nucleating agent; the content of the nucleating agent is

from 0.01 to 10% by weight, based on the total weight of the polyester composition.

5. The polyester composition according to claim 4, characterized in that the content of the nucleating agent is from 0.2 to 5% by weight, based on the total weight of the polyester composition.

6. The polyester composition according claim 4, characterized in that the nucleating agent is one or more selected from the group consisting of talc, calcium oxide, carbon black, calcium carbonate, inorganic pigments, kaolin, metal carboxylates, metal phosphates, dibenzyl sorbitol and derivatives thereof, polyvinylcyclohexane, polyvinylcyclopentane, low density polyethylene, hyperbranched polyamide and ethylene-methacrylic acid ionomer.

7. The polyester composition according to any one of claims 1 to 6, characterized in that the polyester composition further comprises erucylamide and/or white oil.

8. The polyester composition according to any one of claims 1 to 7, characterized in that the aliphatic-aromatic copolyester is a random copolymer, an alternating copolymer, a block copolymer, or a graft copolymer.

9. The polyester composition according to any one of claims 1 to 8, characterized in that the polyester composition has an elongation at break of equal to or greater than 230%, as measured by the method according to the standard GB/T 1040.2-2006.

10. A process for the preparation of a polyester composition according to any one of claims 1 to 9, characterized in that the process comprises: mixing all the components including polybutylene terephthalate and the aliphatic-aromatic copolyester, and subjecting the resulting mixture to extrusion pelletization to obtain the polyester composition.

11. The process according to claim 10, characterized in that the mixing is carried out under stirring with the stirring rate of 6 to 60 rpm and the stirring time of 2 to 30 min; said extrusion pelletization is carried out in a twin-screw extruder at a temperature of 230 to 300 °C,

with a screw rotational speed of 10 to 70 rpm, and with a torque of 2 to 80 N \*m.

12. The process according to claim 10 or 11, characterized in that no compatibilizer is added during the mixing process.

13. A toughened composite material, prepared from a polyester composition according to any one of claims 1 to 9.