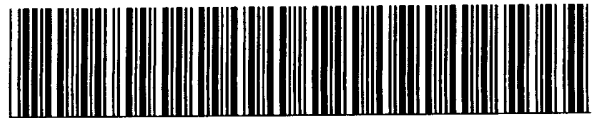


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WORLD INTELLECTUAL PROP
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INTERNATIONAL APPLICATION PUBLISHED UNDER

WO 9605256A1

<p>(51) International Patent Classification ⁶ : C09C 1/36, C09D 17/00</p>	<p>A1</p>	<p>(11) International Publication Number: WO 96/05256 (43) International Publication Date: 22 February 1996 (22.02.96)</p>
<p>(21) International Application Number: PCT/US94/08316 (22) International Filing Date: 11 August 1994 (11.08.94) (71) Applicant: E.I. DU PONT DE NEMOURS AND COMPANY [US/US]; 1007 Market Street, Wilmington, DE 19898 (US). (72) Inventors: OTT, Michael, W.; 14 Barnard Street, Newark, DE 19711 (US). SULLIVAN, Brian, W.; 250 Green Lane, Newark, DE 19711-6753 (US). (74) Agents: GOULD, David, J. et al.; E.I. du Pont de Nemours and Company, Legal/Patent Records Center, 1007 Market Street, Wilmington, DE 19898 (US).</p>		<p>(81) Designated States: European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). Published <i>With international search report.</i></p>

(54) Title: MEDIA MILLING PIGMENT SLURRIES TO ELIMINATE OR REDUCE OVERSIZE PARTICLES

(57) Abstract

Disclosed is a process for substantially increasing the content of particles having a size of less than 10 microns in a titanium dioxide slurry, comprising subjecting a starting material slurry containing at least 0.5 % by weight of titanium dioxide particles of at least about 10 microns to media milling, whereby the content of particles greater than 10 microns is reduced by a factor of 5.

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MEDIA MILLING PIGMENT SLURRIES TO ELIMINATE
OR REDUCE OVERSIZE PARTICLES

Background of the Invention

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The present invention relates to the preparation of a composition of titanium dioxide in an aqueous slurry suitable for production of coated boards, e.g., paperboards having high gloss characteristics and surface smoothness.

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Titanium dioxide slurries suitable for use in paper and paperboard manufacture are relatively well known. For example, Hall et al. disclose in USP 3,702,773, a stabilized titanium dioxide slurry of 60 to 82% by weight of TiO₂ for use in paper manufacturing. DeColibus 15 discloses in USP 4,177,081 titanium dioxide slurries imparting high gloss to water-based acrylic paint systems, and Glaeser discloses in USP 4,214,913 a process for producing rutile TiO₂ slurries which may be used in board coating.

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In order to produce coatings with sufficient gloss and smoothness, certain finishing steps are required to be performed on the slurries. Consequently, such steps as filtration, washing, drying, micronization and reslurrying are often performed. Other advantages such as improved tinctorial strength are achieved by a reduction in particle 25 size. As a result, various techniques are known for reduction of the particle size of such slurries, e.g., mechanical grinding (Whatley et al., USP 3,342,424), steam milling micronization (Baloga, USP 4,427,451), high shear milling (Gladu, USP 4,288,254, Hall et al., above, Slepety, USP 3,549,091, Jester et al., USP 3,380,665, micronizing process) and ball 30 milling (Jacobs et al., USP 3,313,492).

It is desirable, however, to have a production process that yields the improved coating smoothness of conventional finishing steps.

Summary of the Invention

5 The present invention concerns a process for reducing the amount of oversized particles greater than about 1 micron, especially those particles from about 10 to about 44 microns, in a rutile pigment slurry. The resultant slurry is particularly suitable for producing improved board coating grade titanium dioxide coatings. Reduction of the oversized particles is achieved preferably through media milling. In the following, all percentages are by weight unless otherwise indicated.

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Typical slurries produced conventionally have a particle size distribution such that about 5% of the particles have a size of about 1-10 microns, and about 1/2-2% of the particles have a size of 10-44 microns. It has now been discovered, for the first time, that reduction of these particles, particularly those of the 10-44 microns range, enables production of improved board coatings having the smoothness and gloss of slurries produced with more expensive and laborious conventional finishing steps. Typically, slurries processed according to the invention have, subsequent to media milling, about 0.1% particles 10-44 microns, with about 94% of the particles having a size of less than about 1 micron.

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Media milling is established technology for particle size reduction, with process equipment being commercially available. For example, in EP 298,777, a method of producing fine particles is disclosed involving media milling a suspension, separating a resultant slurry by size and recycling a coarse fraction to the mill. Further, JP 210,521 discloses media milling of calcium carbonate to a size below 15 microns. Pigments suitable for paper coating are obtained thereby.

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In the invention, the titanium dioxide slurry having particles greater than 10 microns is fed into a grind chamber which is filled with beads. Many types of media or different sizes may be used, with one of ordinary skill in the art being able to adjust the media to produce the desired result based on the size distribution of the particles in the starting material according to conventional protocols. The media is stirred in the grind chamber by a series of discs attached to a rotating shaft. The motion of the media is perpendicular to the direction in which the slurry is

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pumped, and therefore the TiO₂ particles are sheared by the media. Typically, a screen keeps the media inside the grind chamber but allows the TiO₂ slurry out of the mill. Optionally, the product of the mill can be further screened.

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Any titanium dioxide slurry with particles over 1 micron, preferably over 10 microns, is suitable for use in the present invention. Preferred starting materials include rutile pigment slurries as produced by Glaeser in USP 4,214,913. Typically, such slurries have on the order of 1% by weight of their particles about 10 microns, e.g., a "subgrit" level of from 10-44 microns.

10

Preferred is the chloride process for production of the starting material slurry. The process typically comprises oxidizing with oxygen or an oxygen containing gas, a mixture of TiCl₄ and AlCl₃, and after at least 80% of the TiCl₄ has been converted to TiO₂, the amount of AlCl₃ being sufficient to form 0.1-1.5% Al₂O₃ in the TiO₂. Preferably, the improved slurry for board coating is produced by (a) slurrying TiO₂ particles at a sufficiently high solids content so as to achieve deagglomeration of the slurry, while still permitting sufficient fluidity to permit dispersion thereof, (b) diluting the slurry to a point sufficient to permit slurry handling and transfer, and (c) media milling the slurry. Preferably the slurry is made from TiO₂ directly removed from the oxidation section of the process. (Sometimes referred to herein as base TiO₂.)

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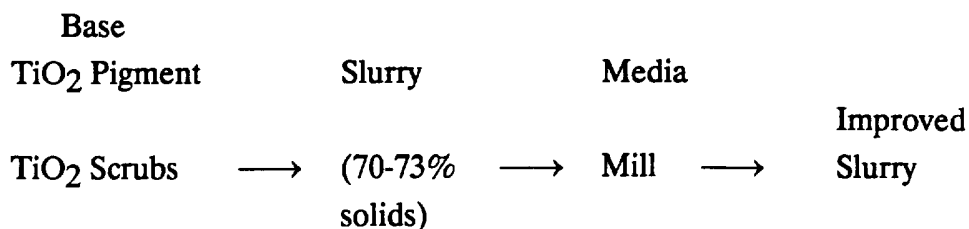
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Typically, such starting material slurries in (a) have about 79-83% by weight of solids. In (b), the slurry typically is diluted to about 70-73% solids, more preferably about 72%.

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A typical overall process is as follows:



By TiO₂ scrubs is meant the scrub solids, such as large particle size TiO₂, which is used to scrub and remove build-up from the interior of the flue pipes downstream from the TiO₂ oxidation section.

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The overall process may be conducted in a batch or continuous mode. Preferably, the process is conducted continuously.

Without further elaboration, it is believed that one skilled in the art can, using the preceding description, utilize the present invention to is fullest extent. The following preferred specific embodiments are, therefore, to be construed a merely illustrative, and not limitation of the remainder of the disclosure in any way whatsoever.

15 In the foregoing and in the following examples, all temperatures are set forth uncorrected in degrees Celsius and unless otherwise indicated, all parts and percentages are by weight.

20 The entire disclosures of all applications, patents and publications cited above and below are hereby incorporated by reference.

EXAMPLES

Base TiO₂ pigment is made as follows:

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A stream of oxygen preheated to a temperature of 980°C is introduced into one end of 10-inch inside diameter tubular, chlorine purged reactor operated at 1.76 kg/cm² gauge at a rate of 7730 kg per hour.

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A titanium tetrachloride stream containing sufficient aluminum trichloride to provide one percent Al₂O₃ in the titanium dioxide based on the titanium dioxide is preheated to 480°C and introduced into the reactor in vapor form through an annular ring and mixing tee to insure complete and uniform mixing with the preheated oxygen.

35

The temperature of the reaction gas stream is 1300°-1450°C after the addition of the titanium tetrachloride and aluminum trichloride is complete. PCl_3 is then added at a point where 92% of the TiCl_4 was converted to TiO_2 through a similar annular ring in sufficient quantity to provide 0.25% P_2O_5 on the titanium dioxide. The PCl addition is followed by scrub solids before the reaction stream exits the reactor into cooling ducts. The reaction stream with the scrub solids is cooled. The reaction produces pigmentary size 100% rutile TiO_2 .

Scrub solids are rutile TiO_2 particles of granular 20-40 mesh size that has been calcinated and is used to clean the walls of the reactor.

The base TiO_2 is made into rutile pigment slurry by the following process which disperses and deagglomerates the base pigment to produce a slurry product.

682 kg of H_2O are added to a slurry tank. 10.9 kg of powdered tetrapotassium pyrophosphate and 16.4 kg of liquid 2-amino-2methyl-1-propanol (AMP) are added to the H_2O and are stirred until dissolved. 2830 kg of TiO_2 prepared as described above are added over a period of 20 minutes to form a slurry. The slurry is ground for 30 minutes. The slurry contents are diluted to about 72% by adding 409 kg of H_2O . The slurry is screened to remove grit.

The above slurry was then fed to a 25 liter Drais media mill. The media mill's grind chamber is charged to 85% capacity with 107 lbs Zr_2SiO_2 media. The media nominal size range is 1.0-1.6 mm in diameter. The milling of the slurry is done in a continuous fashion. The flow rate of the slurry through the mill is adjusted to provide a 1.27 minute grinding residence time. After passing through the grind chamber, the product slurry is separated from the grinding media by a set of screens.

The particle size distribution between 10-44 microns is determined by laboratory screening operations. The data for unmilled and milled product is summarized below:

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wt. % of TiO₂ Particles

	<u>Unmilled</u>	<u>Milled</u>
%30 - 40 microns	0.163	0.010
5 %20 - 30 microns	0.183	0.008
<u>%10 - 20 microns</u>	<u>0.530</u>	<u>0.058</u>
Total	0.876	0.076

10 The particle size distribution between 1-10 microns is determined by Sedigraph analysis. The data for unmilled and milled product is summarized below:

wt. % of TiO₂ Particles

	<u>Unmilled</u>	<u>Milled</u>
15 5 - 10 microns	1	0.5
2 - 5 microns	3	1.5
1 - 2 microns	5	4

20 Other property improvements determined were:

	<u>Unmilled</u>	<u>Milled</u>
High Shear Visc. (cp)	34	23
Dry Film Drawdown Gloss	90	105

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The viscosity was measured at 4,000 reciprocal seconds shear rate using a Hercules High Shear Viscometer. Gloss is measured as a relative reflectance on a 0.02 inch thick dry slurry film.

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To further test milled pigment quality, its performance was tested by coating board samples at 40% solids loading. Coating quality was evaluated by counting the number of bumps observed per unit area at 19 x magnification. The milled product produces significantly smoother board as shown below:

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	<u>Unmilled</u>	<u>Milled</u>
Average number of bumps (square inch)	642	179

The preceding examples can be repeated with similar success by substituting the generically or specifically described reactant and/or operating conditions of this invention for those used in the preceding examples.

From the foregoing description, one skilled in the art can easily ascertain the essential characteristics of this invention, and without departing from the spirit and scope thereof, can make various changes and modifications of the invention to adapt it to various usages and conditions.

WHAT IS CLAIMED IS:

1. A process for the production of TiO₂ slurries, comprising (a) slurring chloride process TiO₂ particles without surface treatment at a sufficiently high solids contents so as to achieve deagglomeration of the slurry, while still permitting sufficient fluidity to permit dispersions thereof, (b) diluting the slurry to a point sufficient to permit slurry handling and transfer, (c) optionally removing any scrub solids from the TiO₂ process, and (d) media milling the slurry.
5
2. A process according to claim 1, wherein in (a) the solids content is about 79-83% by weight.
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3. A process according to claim 2, wherein in (b) the solids content is about 70-73% by weight.
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4. A process according to claim 1, wherein after step (b), the slurry has less than about 4% by weight of particles with a size greater than about 44 microns.
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5. A process for the production of a titanium dioxide slurry, comprising subjecting a starting material slurry containing at least 5.0% by weight of titanium dioxide particles of about 1 to 10 microns to media milling, wherein said starting material slurry is produced by a process comprising (a) slurring TiO₂ particles at a sufficiently high solids content so as to achieve deagglomeration of the slurry, while still permitting sufficient fluidity to permit dispersion thereof, and (b) diluting the slurry to a point sufficient to permit slurry handling and transfer.
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6. A process according to claim 5 wherein the starting material slurry contains greater than about one-half percent of particles having a size of about 10-44 microns.
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7. A process according to claim 5, wherein the starting material slurry contains about 5% by weight of particles having a size of about 1-10 microns and greater than about one-half percent of particles having a size of about 10-44 microns.
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8. A process for enhancing coatability of TiO₂ slurry on boards, comprising lowering to less than about 0.1% by weight the content in the slurry of TiO₂ particles having a size of about 10-44 microns.

INTERNATIONAL SEARCH REPORT

International Application No
PCT/Us 94/08316

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 C09C1/36 C09D17/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 6 C09C C09D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
E	US,A,5 356 470 (M. W. OTT ET AL.) 18 October 1994 see claim 1 see column 3, line 65 - column 4, line 18 see column 2, line 48 - line 52 see column 1, line 47 - line 59 ---	1-3,5-8
A	US,A,4 177 081 (R. L. DECOLIBUS) 4 December 1979 cited in the application see claims 1-5 ---	1,5
A	GB,A,2 057 409 (CANADIAN TITANIUM) 1 April 1981 see claim 1 ---	1
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Further documents are listed in the continuation of box C.

Patent family members are listed in annex.

- * Special categories of cited documents :
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Date of the actual completion of the international search 9 May 1995	Date of mailing of the international search report 23.05.95
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INTERNATIONAL SEARCH REPORT

International Application No
PCT/US 94/08316

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US,A,3 342 424 (W. R. WHATELY ET AL.) 19 September 1967 see claim 1 ---	1
A	DATABASE WPI Week 8718 Derwent Publications Ltd., London, GB; AN 87-127430 & SU,A,1 255 630 (BARSKII) , 7 September 1986 see abstract ---	1
A	DATABASE WPI Week 8329 Derwent Publications Ltd., London, GB; AN 83-714584 & JP,A,58 099 121 (ONAHAMA SAKAI KAGAK) , 13 June 1983 see abstract -----	1

INTERNATIONAL SEARCH REPORT

Information on patent family members

Internat	Application No
PCT/US	94/08316

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