

**(19) AUSTRALIAN PATENT OFFICE**

(54) Title  
Extraction process

(51)<sup>6</sup> International Patent Classification(s)  
**C22B 11/06 (2006.01)7BHEP** C22B  
**C22B 11/02 (2006.01)11/02**  
C22B 11/06 20060101AL12007072  
20060101AFI2006042 1BMEP  
PCT/GB2005/004041

(21) Application No: 2005297064 (22) Application Date: 2005.10.20

(87) WIPO No: WO06/043065

(30) Priority Data

(31) Number (32) Date (33) Country  
0423213.8 2004.10.20 GB

(43) Publication Date: 2006.04.27

(71) Applicant(s)  
Minex Technologies Limited

(72) Inventor(s)  
Evans, Timothy

(74) Agent/Attorney  
Davies Collison Cave, 1 Nicholson Street, Melbourne, VIC, 3000

(56) Related Art  
US 3988415 A  
DE 2348977 A  
DE 30419 C  
CA 2193783 A

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization  
International Bureau



(43) International Publication Date  
27 April 2006 (27.04.2006)

PCT

(10) International Publication Number  
**WO 2006/043065 A1**

(51) International Patent Classification:  
*C22B 11/06* (2006.01)

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AB, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EB, EG, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LY, MA, MD, MG, MK, MN, MW, MX, MZ, NA, NG, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SI, SM, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM, ZW.

(21) International Application Number:  
PCT/GB2005/004041

(22) International Filing Date: 20 October 2005 (20.10.2005)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:  
0423213.8 20 October 2004 (20.10.2004) GB

(71) Applicant (for all designated States except US): **MINEX TECHNOLOGIES LIMITED** [GB/GB]; Oakleigh, Wild Oak Lane, Trull, Taunton TA22 7JT (GB).

(72) Inventors; and

(75) Inventors/Applicants (for US only): **BOWELL, Robert** [GB/GB]; SRK (UK) Ltd, Windsor Court, 1-3 Windsor Place, Cardiff CF10 3BX (GB). **WILLIAMS, Keith** [GB/GB]; Cardiff School of Engineering, Cardiff University, Queen's Buildings, The Parade, PO Box 925, Cardiff CF24 4YF (GB).

(74) Agents: **EVANS, Jacqueline, G., V. et al.**; Greaves Brewster LLP, Indigo House, Cheddar Business Park, Wedmore Road, Cheddar, Somerset BS27 3EB (GB).

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IS, IT, LT, LU, LV, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Published:

- with international search report
- before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: EXTRACTION PROCESS

(57) Abstract: A process for extracting a precious metal from a precious metal containing source is provided comprising the steps of :- (i) contacting the precious metal-containing source with a vapour phase chloride salt; (ii) condensing the precious metal containing volatile product of step (i); and (iii) recovering the precious metal from the condensed product of step (ii).

**WO 2006/043065 A1**

**Extraction Process****Field of the invention**

5

The present invention relates to a process for extracting a precious metal from a precious metal containing source. In particular, the invention relates to an improved process for extracting a precious metal, especially gold, from a precious metal containing source using a chlorination process.

10

**Background of the invention**

15 Various methods for extracting and recovering metals, particularly precious metals, present in complex source materials such as ores and the like are known in the art.

20 In the case of gold, for example, one well-established method for extracting the metal from its ore involves crushing the ore, treating the gold containing pulp with a solution of a cyanide and removing the gold in the form of a complex with cyanide ions. The gold is subsequently recovered from the complex by a precipitation reaction, for example with metallic zinc or by electrolysis.

25

Although cyanide leaching processes of this type have found widespread application in the past, they are potentially hazardous to operate and present serious environmental concerns. Indeed, such is the current level of concern that such processes 30 are no longer operated in many territories. Moreover, these methods are not generally applicable to other precious metals; for example, silver and copper cannot effectively be extracted using cyanidation technology.

35 Concerns about the environmental impact of the processes involving the use of cyanides have led to considerable interest in the development of alternative, commercially more attractive

and environmentally less damaging methods for extracting metals, particularly precious metals, from the materials in which they are contained.

5 This has led to a revival of interest in chlorination-based extraction processes whereby the metal is extracted from the material in which it is deposited by the formation of volatile chloride containing metal compounds from which the metal can be recovered. Chlorination-based processes are well known in the  
10 art and methods which have been described in the literature include the leaching of metal ores using aqueous solutions of chlorine, chlorides and hypochlorites as discussed, for example, in US Patent No. 4,353, 740 and US Patent No. 5,169,503.

15 Other methods commonly used for extracting precious metals from ores include autoclaving. Although this method is currently commercially used in the mining industries, the associated capital costs represent a considerable disadvantage of the method.

20 There therefore remains a continuing need for the development of further, improved, commercially viable methods for extracting metals, especially precious metals, from ores, concentrates or other materials in which they are found. In naturally occurring  
25 deposits of precious metals, the metal is commonly present at too low a concentration to be extracted profitably using existing methods. Methods for extraction of precious metals which avoid the environmental hazards associated with conventional cyanide leaching and which may be used in  
30 situations where cyanide leaching is ineffective are particularly sought.

Summary of the invention

The present invention provides a process for extracting a precious metal from a precious metal-containing source comprising the steps of:-

5

- (i) heating the precious metal-containing source in a reaction vessel;
- (ii) passing a vapour phase chloride salt through the reaction vessel containing the heated precious metal-containing source to form a volatile precious metal-containing chloride;
- 10 (iii) condensing the precious metal containing volatile product of step (ii); and
- (iv) recovering the precious metal from the condensed product of step (iii).

The present invention is based on the finding that precious metals may be extracted and recovered from materials in which they are contained in a cost-effective way and at a 15 commercially viable recovery level by forming a metal containing chloride compound in the vapour phase, condensing the precious metal containing vapour phase product, thereby extracting the metal from its source in the form of a metal chloride compound, and recovering the extracted metal from the condensed product.

20 By means of the invention, the environmental pollution risks associated with conventional cyanide extraction can be avoided. Moreover, the present inventors have found that by using the present chlorination extraction process it is possible to achieve levels of extraction of the contained metals which are significantly greater than those achievable using a cyanide based process. Levels of metal extraction obtained using the present 25 process have been found to be comparable, at least, to the levels achieved using autoclaving but can be achieved at a small fraction of the capital cost associated with this hitherto industry-standard process.

Detailed description

30

The method of the invention is applicable to the extraction of metals from a variety of

sources, including ores, concentrates and wastes produced by mining processes together with precious metal-containing minerals and soils.

Preferably, the process of the invention is performed using a metal-containing ore as the 5 source of the metal. The invention is not limited to one ore type, however, and the method may find application in the extraction of sulphide containing ores containing more than one metal species, for example.

The chlorination extraction process may be applied to the extraction of a variety of 10 precious metals, including but not limited to precious metals such as silver and especially gold. As used herein, the term "precious metal" has its conventional meaning and will be understood to encompass gold, silver, platinum and platinum group metals such as osmium, rhodium, ruthenium, iridium, and palladium.

15 Prior to being contacted with the vapour phase chloride, a metal-containing ore for use according to the invention may conveniently be ground and roasted at a suitably high temperature, typically in the presence of air or oxygen, in order to remove sulphides present in the ore by converting them to sulphur dioxide. Roasting may suitably be performed in a fluid-bed roaster. It will be appreciated that the temperature is not critical 20 provided that it is high enough to remove sulphides present in the ore.

The chloride for use according to the invention may suitably be any volatile chloride which is either already in vapour form or which may readily be vapourised. Preferably, the chloride is ammonium chloride. Conveniently, the chloride vapour is present in excess.

25 The temperature at which the reaction is performed

will be chosen to ensure that the chloride remains in the vapour phase and also that the reaction with the precious metal occurs at a suitable rate. Suitably, this will be achieved by maintaining the metal containing source at a temperature at or 5 above the temperature at which the chosen volatile chloride becomes vapourised, during the course of the reaction. It will be appreciated that the reaction temperature is not critical provided that it is high enough for the desired reaction to occur, and not so high that undesired reaction products also 10 enter the vapour phase along with the precious metal-containing chloride compound. Generally, temperatures of between 300°C to 650°C are contemplated.

Conveniently, the vapour phase chloride may be contacted with 15 the precious metal-containing source, such as a ground, roasted metal-containing ore, by passing the gaseous chloride through the source in a suitable reaction vessel such as a reactor or kiln. The process to form metal containing volatile chloride compounds may suitably be conducted continuously (for example by 20 continuously replenishing the metal containing ore in the reaction vessel) or in a batch mode (for example by intermittently contacting the chloride vapour with the metal containing source).

25 Following the formation of the metal containing volatile chloride compounds according to the first step of the process of the invention, the metal-containing volatile compound products are separated from the vapour phase by condensing them using methods conventional in the art.

30 The metal can be recovered from the condensed vapour phase solids by any recovery means conventional in the art. In the case of gold, for example, this may conveniently be achieved by dissolving the gold-containing condensed solid products in water 35 and treating the solution with metallic zinc to reduce the gold.

Example

Following the method set forth above, gold was extracted from a complex gold ore obtained from a Placer Dome mine in Nevada, using gaseous ammonium chloride as the 5 vapour phase chloride salt. The method was found to extract 26% of the gold present.

The results compare favourably with those obtained using a conventional cyanidation process which resulted in less than 5% recovery of the contained gold and are comparable to those obtained in bench scale autoclaving studies (30% recovery).

10

Throughout this specification and the claims which follow, unless the context requires otherwise, the word "comprise", and variations such as "comprises" and "comprising", will be understood to imply the inclusion of a stated integer or step or group of integers or steps but not the exclusion of any other integer or step or group of integers or steps.

15

The reference in this specification to any prior publication (or information derived from it), or to any matter which is known, is not, and should not be taken as an acknowledgment or admission or any form of suggestion that that prior publication (or information derived from it) or known matter forms part of the common general knowledge in the field of 20 endeavour to which this specification relates.

THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:

1. A process for extracting a precious metal from a precious metal-containing source comprising the steps of:-
  - 5 (i) heating the precious metal-containing source in a reaction vessel;
  - (ii) passing a vapour phase chloride salt through the reaction vessel containing the heated precious metal-containing source to form a volatile precious metal-containing chloride;
  - (iii) condensing the precious metal containing volatile product of step (ii); and
  - 10 (iv) recovering the precious metal from the condensed product of step (iii).
2. A process according to claim 1 wherein the metal-containing source is a metal ore.
3. A process according to claim 1 or claim 2 wherein the precious metal is gold.
- 15 4. A process according to any of claims 1 to 3 wherein the chloride salt is ammonium chloride.
5. A process according to any preceding claim wherein the precious metal-containing source is ground and roasted prior to being contacted with the vapour phase chloride salt.
- 20 6. A process according to any preceding claim wherein the temperature of the precious metal-containing source is maintained at a temperature at, or above, the vaporisation temperature of the chloride salt.
- 25 7. A process according to any preceding claim wherein the precious metal-containing source is contacted with the vapour phase chloride salt at a temperature at, or above, the vapourisation temperature of the chloride salt.
- 30 8. A process according to any preceding claim wherein the process is conducted in continuous mode.

2005297064 24 Nov 2010

3124635.1

- 8 -

9. A process according to claim 8 wherein the precious metal-containing source is replenished as the precious metal is extracted.

10. A process for extracting a precious metal substantially as hereinbefore described.

5