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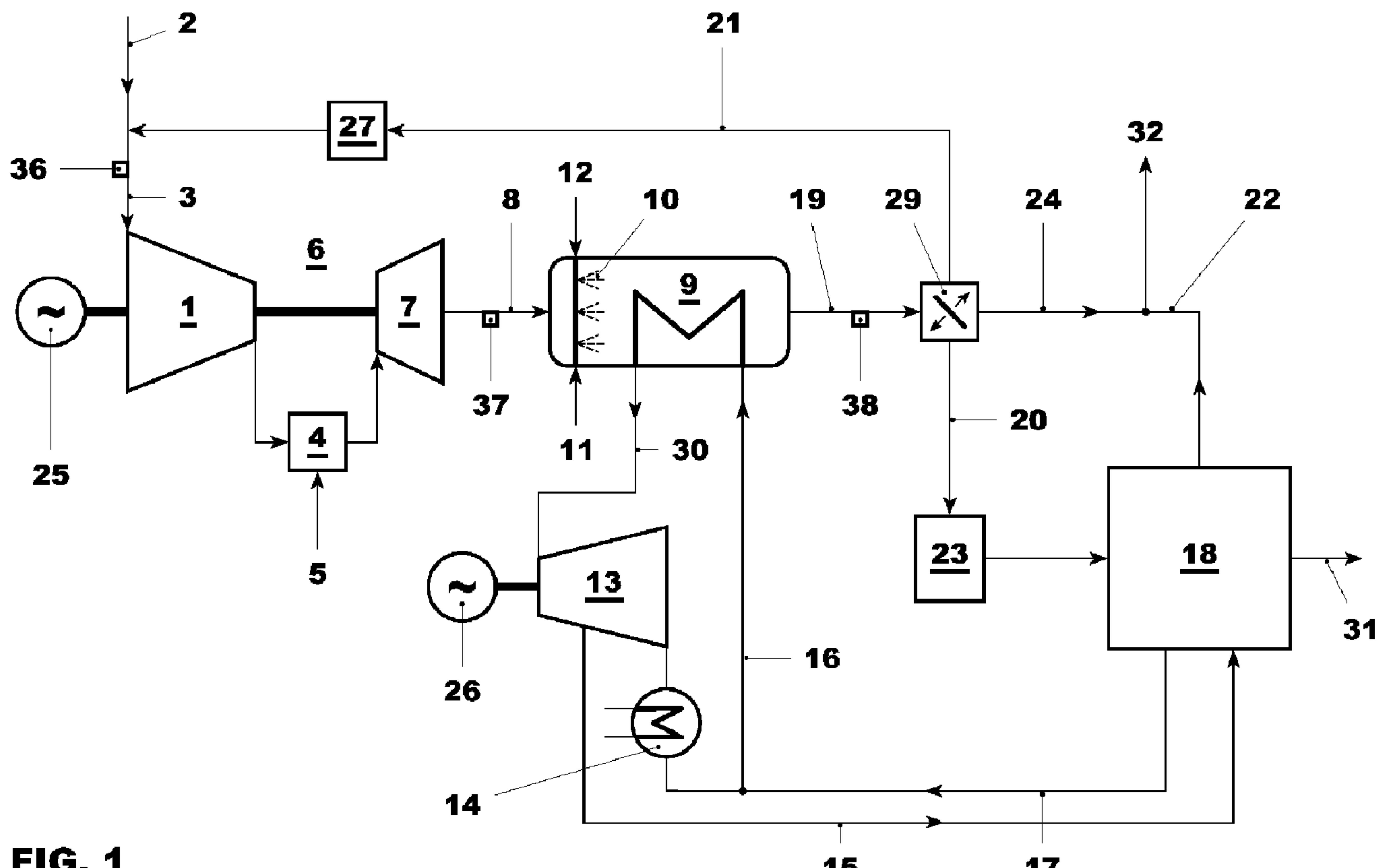
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(54) Titre : CENTRALE ELECTRIQUE AVEC CAPTURE DU CO2  
(54) Title: POWER PLANT WITH CO2 CAPTURE



**FIG. 1**

(57) Abrégé/Abstract:

Since CO<sub>2</sub> is identified as a main greenhouse gas, its capture and storage is essential to control global warming. Flexible operation of CCPPs (combined cycle power plants) with CO<sub>2</sub> capture system (18) will increase the competitiveness of CCPPs designed for

**(57) Abrégé(suite)/Abstract(continued):**

CO<sub>2</sub> capture and will allow earlier introduction of this kind of plants. The main objective of the present invention is to increase the CCPP net power and improve the operating characteristics by taking advantage of the additional power and flexibility, which can be obtained with supplementary firing (10) in CCPPs with flue gas recirculation and CO<sub>2</sub> capture systems (18). One particular aim is to minimize the impact of CO<sub>2</sub> capture on the capacity of a power plant, i.e. to maximize the electric power the plant can deliver to the power grid. To this end an operating method, in which the power consumption of CO<sub>2</sub> capture system is at least partly compensated by the operation of supplementary firing (10) in a HRSG (9) with low residual oxygen concentration in the flue gases (8), which is due to flue gas recirculation, is proposed. Further, additional ambient air and/or oxygen (11) injection into the supplementary firing (10) with corresponding operating methods are proposed. Besides the method a CCPP designed to operate according to this method is subject of the present invention.

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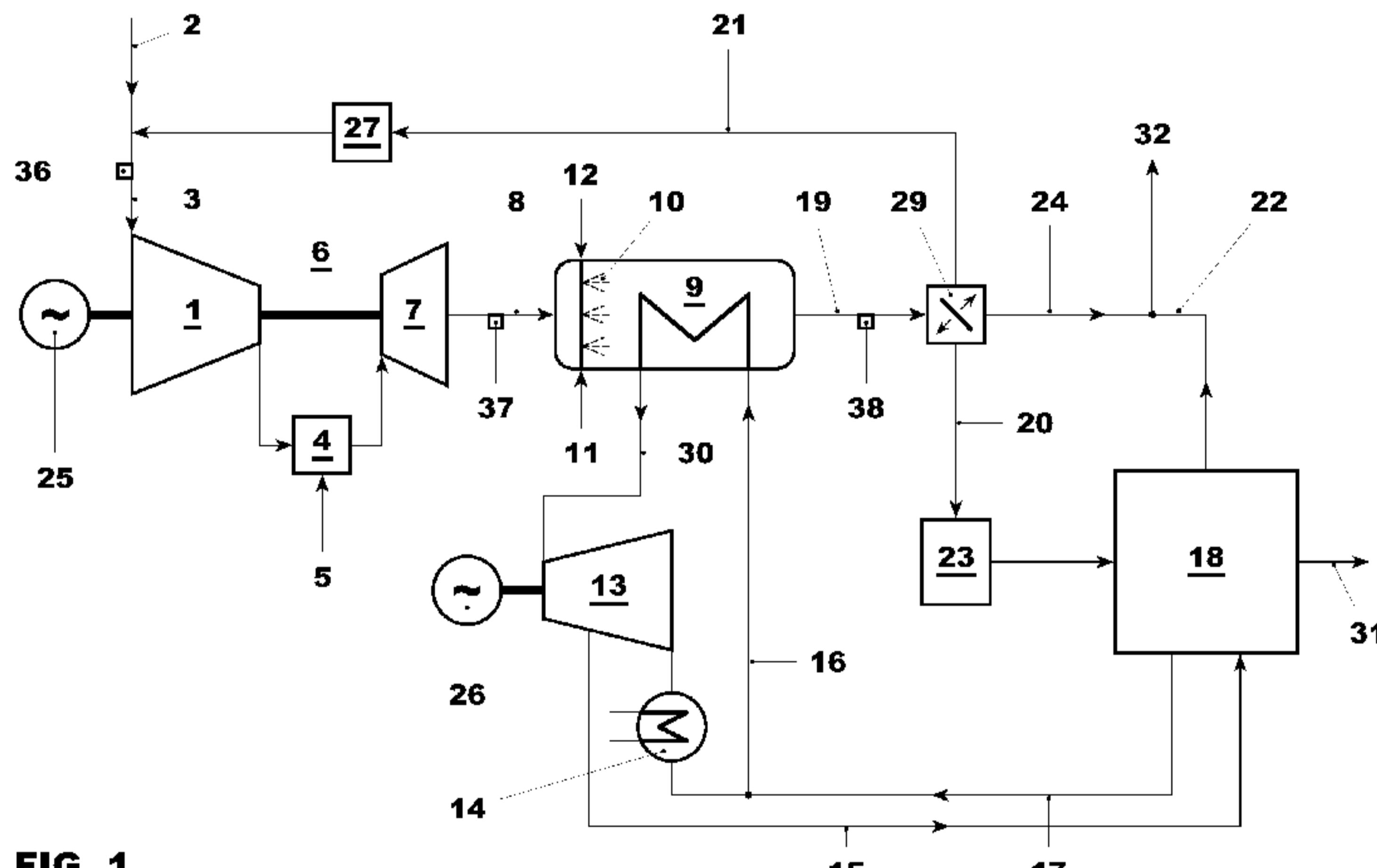


FIG. 1

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(57) **Abstract:** Since CO<sub>2</sub> is identified as a main greenhouse gas, its capture and storage is essential to control global warming. Flexible operation of CCPPs (combined cycle power plants) with CO<sub>2</sub> capture system (18) will increase the competitiveness of CCPPs designed for CO<sub>2</sub> capture and will allow earlier introduction of this kind of plants. The main objective of the present invention is to increase the CCPP net power and improve the operating characteristics by taking advantage of the additional power and flexibility, which can be obtained with supplementary firing (10) in CCPPs with flue gas recirculation and CO<sub>2</sub> capture systems (18). One particular aim is to minimize the impact of CO<sub>2</sub> capture on the capacity of a power plant, i.e. to maximize the electric power the plant can deliver to the power grid. To this end an operating method, in which the power consumption of CO<sub>2</sub> capture system is at least partly compensated by the operation of supplementary firing (10) in a HRSG (9) with low residual oxygen concentration in the flue gases (8), which is due to flue gas recirculation, is proposed. Further, additional ambient air and/or oxygen (11) injection into the supplementary firing (10) with corresponding operating methods are proposed. Besides the method a CCPP designed to operate according to this method is subject of the present invention.

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## Power plant with CO2 capture

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### FIELD OF THE INVENTION

10 The invention relates to combined cycle power plants with integrated CO2 capture and supplementary firing as well as to their operation.

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### BACKGROUND OF THE INVENTION

In recent years it has become obvious that the generation of greenhouse gases leads to global warming and that further increase in greenhouse gas production 20 will accelerate global warming. Since CO2 (carbon dioxide) is identified as a main greenhouse gas, CCS (carbon capture and storage) is considered as one of the potential major means to reduce the release of greenhouse gases into the atmosphere and to control global warming. In this context CCS is defined as the process of CO2 capture, compression, transport and storage. Capture is defined 25 as a process, in which CO2 is removed either from the flue gases after combustion of a carbon based fuel or the removal of and processing of carbon before combustion. Regeneration of any absorbents, adsorbents or other means to remove CO2 from a flue gas or fuel gas flow is considered to be part of the capture process.

30

Backend CO2 capture, also called post- combustion capture, is a commercially promising technology for fossil fueled power plants including CCPP (combined cycle power plants). In post-combustion capture the CO2 is removed from a flue gas. The remaining flue gas is released to the atmosphere and the CO2 is 35 compressed for transportation, and storage. There are several technologies known to remove CO2 from a flue gas such as absorption, adsorption, membrane

separation, and cryogenic separation. Power plants with post combustion capture are the subject of this invention.

All known technologies for CO<sub>2</sub> capture require relatively large amounts of energy. Due to the relatively low CO<sub>2</sub> concentration of only about 4 % in the flue gases of a conventional CCPP, the CO<sub>2</sub> capture system (also called CO<sub>2</sub> capture plant or CO<sub>2</sub> capture equipment) for a conventional CCPP will be more costly and energy consuming per kg of captured CO<sub>2</sub> than one for other types of power plants, which have flue gas flows at higher CO<sub>2</sub> concentrations.

10

The CO<sub>2</sub> concentration in the CCPP flue gas depends on the fuel composition, the gas turbine type and load and may vary substantially depending on the operating conditions of the gas turbine. This variation in CO<sub>2</sub> concentration can be detrimental to the performance, efficiency, and operability of the CO<sub>2</sub> capture system.

15

To increase the CO<sub>2</sub> concentration in the flue gases of a CCPP two main concepts are known. One is the recirculation of flue gases as for example described by O. Bolland and S. Sæther in „NEW CONCEPTS FOR NATURAL GAS FIRED POWER PLANTS WHICH SIMPLIFY THE RECOVERY OF CARBON DIOXIDE“ (Energy Convers. Mgmt Vol. 33, No. 5-8, pp. 467-475, 1992)). Another one is the so called tandem arrangement of plants, where the flue gas of a first CCPP is cooled down and used as inlet gas for a second CCPP to obtain a flue gas with increased CO<sub>2</sub> concentration in the flue gas of the second CCPP. Such an arrangement is for example described in the US20080060346. These methods reduce the total flue gas flow, increase the CO<sub>2</sub> concentration, and thereby reduce the required flow capacity of absorber and power consumption of the capture system.

25

These methods, as well as many further published methods for the optimization of the different process steps, and the reduction of the power and efficiency penalties by integrating these processes into a power plant, aim to reduce the capital expenditure and the power requirements of CO<sub>2</sub> capture system.

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## SUMMARY OF THE INVENTION

The main objective of the present invention is to provide a combined cycle power plant (CCPP) comprising at least one gas turbine, one heat recovery steam generator (HRSG), one steam turbine, and carbon dioxide (CO<sub>2</sub>) capture system with enhanced operational flexibility, and to reduce capacity penalties for CO<sub>2</sub> capture as well as an operating method for such a CCPP.

In particular the impact of CO<sub>2</sub> capture on the capacity of a CCPP is to be minimized, i.e. the electric power delivered to the power grid by the plant including the CO<sub>2</sub> capture system is to be maximized.

To this end an operating method for a CCPP with flue gas recirculation, CO<sub>2</sub> capture and supplementary firing is proposed as well as a plant to carry out such a method. The essence of the invention is an operating method for a CCPP with flue gas recirculation, which allows operation of a supplementary firing burner in flue gases of a CCPP with flue gas recirculation, which at least partially compensates for the power requirements of the CO<sub>2</sub> capture system. The supplementary firing burner can be installed in the HRSG of the CCPP or as a duct firing in the flue duct from the gas turbine to the HRSG.

For flue gas recirculation, the flue gas flow of a gas turbine is split into at least two partial flows downstream of the HRSG. A first partial flow is returned to the inlet of the gas turbine via a flue gas recirculation line, and a second partial flow is directed via the CO<sub>2</sub> capture system to the stack for release to the environment. Further, a bypass around the CO<sub>2</sub> capture system for direct release of flue gases to the environment can be provided to increase the operational flexibility. This allows any combination of recirculation rate, of flue gas flow to CO<sub>2</sub> capture unit, and direct flue gas flow to the stack without CO<sub>2</sub> capture.

Flue gas recirculation is applied to minimize the CO<sub>2</sub> capture system's size, its costs, and its power requirements. For optimized CO<sub>2</sub> capture the flue gas recirculation rate should be maximized. The recirculation rate is defined as the ratio of flue gas mass flow from the gas turbine, which is recirculated to the compressor inlet, to the total flue gas mass flow of the gas turbine.

For high CO<sub>2</sub> capture efficiency and to minimize the flue gas mass flow, the oxygen concentration in the flue gas would ideally be 0%. Due to cooling air, which bypasses the gas turbine's combustion chamber, and excess oxygen needed to assure complete combustion, recirculation is limited and some residual oxygen remains in the exhaust gas even with recirculation. Typical recirculation rates determined by the operational requirements of the gas turbine are in the order of 30% to 50% for base load operation.

Conventional supplementary firing burners are designed for residual oxygen concentration of 10% or more in the flue gas. The residual oxygen concentration after a gas turbine with flue gas recirculation is typically lower than 10% and is not sufficient for conventional supplementary firing burner. In order to enable operation under the boundary conditions of flue gases from a gas turbine with flue gas recirculation, the use of a low excess air supplementary firing burner is proposed. In this context a low excess air supplementary firing burner is a burner, which can be operated in a gas flow with less than 10% oxygen concentration with a low stoichiometric ratio. The stoichiometric ratio for this kind of a low excess air supplementary firing burner should be below 2, preferably below 1.5 or even below 1.2. Ideally this kind of burner can operate with a stoichiometric ratio as close as possible to 1.

A conventional duct burner or interstage burner could be used with additional air supply at a high excess air ratio. However, this would dilute the CO<sub>2</sub> concentration in the flue gas and increase the flue gas flow. It is therefore not an adequate solution for this application.

Instead of using CO<sub>2</sub> concentration or oxygen concentration the CO<sub>2</sub> content, respectively the oxygen content can also be used in the context of this invention.

30 In an embodiment, the recirculation rate can be controlled by at least one control organ. This can for example be a controllable damper or a fixed splitter with a control organ like a flap or valve in one or both of the flue gas lines downstream of the splitter.

35 This allows for example to control the recirculation rate to the highest possible rate under the conditions, that stable complete combustion in the gas turbine can

be maintained, and that the residual oxygen concentration after the gas turbine is sufficient to maintain stable complete combustion of the supplementary firing.

Stable complete combustion in this context means, that CO and unburned

5 hydrocarbon emissions stay below the required level, which is in the order of ppm or single digit ppms and that the combustion pulsations stay within the normal design values. Emission levels are typically prescribed by guarantee values. Design values for pulsation depend on the gas turbine, operating point, and combustor design, as well as on the pulsation frequency. They should remain well 10 below 10% of the combustor pressure. Typically they stay below 1 or 2 % of the combustor pressure.

The recirculation rate can for example also be used to control the oxygen

15 concentration of the compressor inlet gases after mixing ambient air with the recirculation flow. The target oxygen concentration of the inlet gasses can for example be a fixed value, which is sufficient to assure stable, complete combustion in the gas turbine under all operating conditions.

In a further embodiment the target oxygen concentration of the flue gases is a

20 function of relative load of the supplementary firing. It can be minimized according to the requirements of the gas turbine as long as the supplementary firing is switched off. Once supplementary firing is switched on, the requirements of the gas turbine and of the supplementary firing have to be considered. The larger one 25 of the two requirements determines the target residual oxygen concentration of the flue gas. The required residual oxygen concentration for the supplementary firing itself can be a fixed value or a function of the burner load of the supplementary firing.

Further, in order to assure complete stable combustion of the supplementary

30 firing, introduction of additional air, and/ or oxygen enriched air, and/or oxygen into the burner or upstream of the burner of the supplementary firing is proposed.

In a further embodiment the recirculation rate can be a fixed rate or determined

35 independently of the supplementary firing. In order to assure complete stable combustion of the supplementary firing under these conditions, the additional airflow, and/ or oxygen enriched airflow, and/or oxygen flow is controlled.

The additional airflow, and/ or oxygen enriched airflow, and/or oxygen flow can be a fixed flow. However, excess air or oxygen should be avoided in the flue gases in order to keep the efficiency of the CO<sub>2</sub> capture high. Therefore a control of the additional air, and/ or oxygen enriched air, and/or oxygen flow is proposed.

5

In one embodiment the additional airflow, and/ or oxygen enriched airflow, and/or oxygen flow is controlled as a function of the flue gas recirculation rate.

10 In another embodiment the additional airflow, and/ or oxygen enriched airflow, and/or oxygen flow is controlled as a function of residual oxygen concentration of the flue gases of the gas turbine.

15 In a further embodiment the additional airflow, and/ or oxygen enriched airflow, and/or oxygen flow is controlled as a function of the relative load of the supplementary firing.

Further parameters, such as the flue gas temperatures before and after the supplementary firing, the flue gas flow velocity etc. can be used.

20 A combination of the above control parameters and targets is possible. For example good operation conditions for the supplementary firing can be obtained with a combination of control as function of residual oxygen concentration of the flue gases and of load of supplementary firing.

25 To optimize the efficiency the additional ambient air flow, and/ or oxygen enriched airflow, and/ or oxygen flow is preheated by low-grade heat from a water steam cycle of the combined cycle power plant, and/ or the CO<sub>2</sub> capture system, and/ or the flue gases.

30 Besides the method a corresponding combined cycle power plant (CCPP) is part of the invention.

35 The CCPP comprises at least one gas turbine, one HRSG, one steam turbine, CO<sub>2</sub> capture system and a supplementary firing. Further, it comprises one recirculation line and one flue gas line to the CO<sub>2</sub> capture system.

According to one embodiment a low excess air supplementary firing is provided in the HRSG of the combined cycle power plant.

In a further embodiment ambient air, and/ or oxygen enriched air, and/ or oxygen

5 supply lines to the low excess supplementary firing is provided.

Additionally, an oxygen enrichment plant and/ or an air separation unit can be provided.

10 Further, at least one oxygen measurement or CO<sub>2</sub> measurement device can be installed to measure the oxygen concentration or CO<sub>2</sub> concentration of the inlet gases of the compressor inlet gas and/ or to measure the residual oxygen concentration of the hot flue gases of the gas turbine and/ or to measure the residual oxygen concentration of the flue gases from the HRSG.

15

Besides compensation of power losses due to the CO<sub>2</sub> capture, the supplementary firing can also be used to increase the plant flexibility and to provide power to compensate the influence of variations in the ambient conditions or to cover periods of peak power demand.

20

Typically, the recirculated flue gas has to be further cooled after the HRSG by a re-cooler before mixing it with ambient air for reintroduction into the compressor of the gas turbine. In one embodiment the control organ for controlling the recirculation rate is installed downstream of this re-cooler to reduce thermal load 25 on this control organ.

## BRIEF DESCRIPTION OF THE DRAWINGS

The invention, its nature as well as its advantages, shall be described in more detail below with the aid of the accompanying drawings. Referring to the drawings.

Fig. 1 schematically shows a CCPP with backend CO<sub>2</sub> absorption including flue gas recirculation and low excess air ratio supplementary firing.

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Fig. 2 schematically shows a low excess air ratio supplementary firing burner for application in a HRSG of a CCPP with flue gas recirculation.

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Fig. 3 schematically shows the normalized residual oxygen concentration of the gas turbine flue gas  $GT_{O_2}$  required for supplementary firing as a function of the relative load of the supplementary firing  $SF_{load}$  without additional ambient air or oxygen supply.

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Fig. 4 schematically shows the normalized residual oxygen concentration of the gas turbine flue gas  $GT_{O_2}$  required for supplementary firing as a function of relative load of the supplementary firing  $SF_{load}$  with additional ambient air or oxygen supply  $F_{air}$  and the residual oxygen concentration after supplementary firing  $SF_{O_2}$ .

## DETAILED DESCRIPTION OF THE DRAWINGS AND THE INVENTION

A power plant for execution of the proposed method consists a conventional CCPP, equipment for flue gas recirculation, a supplementary firing 10, plus a CO<sub>2</sub> capture system 18.

A typical arrangement with post combustion capture, flue gas recirculation, and supplementary firing 10 is shown in Fig. 1. A gas turbine 6, which drives a first generator 25, is supplied with compressor inlet gas 3, and fuel 5. The compressor inlet gas 3 is a mixture of ambient air 2, and a first partial flow 21 of the flue gases, which is recirculated via a flue gas recirculation line. The inlet gas is

compressed in the compressor 1. The compressed gas is used for combustion of fuel 5 in a combustor 4, and pressurized hot gasses expand in a turbine 7. Its main outputs are electric power, and hot flue gasses 8.

- 5 The gas turbine's hot flue gasses 8 pass through a HRSG 9, which generates steam 30 for a steam turbine 13. In the HRSG 9 or the flue gas duct from the gas turbine 6 to the HRSG 9 supplementary firing 10 is integrated. The supplementary firing is supplied with fuel gas 12 and ambient air/ oxygen 11.
- 10 The steam turbine 13 either is arranged in a single shaft configuration with the gas turbine 6 and the first generator 25, or is arranged in a multi shaft configuration to drive a second generator 26. Further, steam is extracted from the steam turbine 13 and supplied via a steam line 15 to a CO2 capture system 18. The steam is returned to the steam cycle as a condensate via a return line 17 and
- 15 is reintroduced into the steam cycle. The steam cycle is simplified and shown schematically without different steam pressure levels, feed water pumps, etc., as these are not subject of the invention.

A first partial flow 21 of the flue gases from the HRSG 19 is recirculated to the  
20 inlet of the compressor 1 of the gas turbine 6 where it is mixed with ambient air 2. The fist partial flow 21 is cooled in the recirculation flue gas cooler 27 before mixing with the ambient air 2.

A second partial flow 20 of the flue gases from the HRSG 19 is directed to the  
25 CO2 capture system 18 by a damper 29.

A CO2 capture system 18 typically consists of a CO2 absorption unit, in which CO2 is removed from the flue gas by an absorbent, and a regeneration unit, in which the CO2 is released from the absorbent. Depending on the temperature of  
30 the second partial flow 20 of the flue gases, and the operating temperature range of the CO2 absorption unit, a flue gas cooler 23 might also be required.

The CO2 depleted flue gas 22 is released from the CO2 capture system 18 to a stack 32. In case the CO2 capture system 18 is not operating, operating at part  
35 load, and to increase operational flexibility, the flue gases from the HRSG can be bypassed or partly bypassed via the flue gas bypass 24.

In normal operation the captured CO<sub>2</sub> 31 will be compressed in a CO<sub>2</sub> compressor and the compressed CO<sub>2</sub> will be forwarded for storage or further treatment.

5 Measurement devices to measure the oxygen concentration and/ or CO<sub>2</sub> concentration are proposed in order to better control the residual oxygen concentration. For example, an inlet air CO<sub>2</sub> and/or O<sub>2</sub> measurement device 36 can be applied for better control of inlet gas composition for the gas turbine 6. For the control of the gas turbine's flue gas composition a gas turbine flue gas CO<sub>2</sub> 10 and/or O<sub>2</sub> measurement device 37 can for example be applied. To control the gas composition of the HRSG flue gas 19 a HRSG flue gas CO<sub>2</sub> and/or O<sub>2</sub> measurement device 38 can for example be applied.

An example of a supplementary firing 10 for burning fuel gas 12 with ambient air 15 at low excess air ratio and with oxygen /oxygen enriched air 11 in an HRSG 9 is shown in Fig. 2. In the shown example burner boxes 28 for supplementary firing are arranged traversal, spaced apart in arrays in a cross section of the HRSG inlet 33 or inside the HRSG. Gas turbine flue gas 8 passes past the burner boxes 28 through the passages between the boxes while the flame of the supplementary firing is stabilized in them. Additional ambient air or oxygen 11 as well as fuel gas 20 12 are supplied to the burner boxes and injected via the fuel gas injection orifices 34 and the oxidizer injection orifices 35. Typically, oxygen is not injected directly into burner boxes 28 but diluted with some carrier gas like ambient air or recirculated flue gas before it comes into contact with the fuel gas 12.

25 In a conventional CCPP with HRSG and supplementary firing the oxygen concentration of the flue gases of the gas turbine 8 is not controlled and independent of the operation of supplementary firing. The supplementary firing typically is simply switched on, after the gas turbine reaches base load and 30 operated independently of the gas turbine 8. Base load is typically the operating condition with the lowest residual oxygen concentration in the flue gases. The oxygen concentration stays practically constant at this level and only slight changes due to changes in the ambient conditions occur. However, this approach 35 is not feasible with flue gas recirculation and minimized residual oxygen concentration in the hot flue gases from the gas turbine 8, as conventional supplementary firing does not work properly under these conditions.

In a first approach to maximize the CO<sub>2</sub> concentration of the flue gases from the HRSG 19 with supplementary firing, the residual oxygen concentration after gas turbine GT<sub>O<sub>2</sub></sub> is controlled as a function of the relative load of the supplementary firing as shown in Fig. 3. It is normalized with the minimum residual oxygen concentration of the flue gas from the gas turbine 8, which would be reached if the gas turbine 6 were operated at the recirculation limit of the gas turbines. For operation of the supplementary firing the residual oxygen concentration after gas turbine GT<sub>O<sub>2</sub></sub> is higher than the minimum residual oxygen concentration of the flue gas required for the gas turbine operation. Therefore the recirculation rate is restricted to allow supplementary firing.

In this case no additional ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow 11 is supplied to the supplementary firing 10. The amount of residual oxygen content and concentration required to assure stable, complete combustion with low CO and unburned hydrocarbon emissions depends on the temperature level and amount of fuel gas, which needs to react. At low relative load of the supplementary firing 10, the temperature is low and a relatively high oxygen concentration is required to assure complete combustion. This leads to a high residual oxygen concentration after the supplementary firing SF<sub>O<sub>2</sub></sub>. With increasing load, the flame temperature increases and the required oxygen concentration drops until it reaches a minimum. For high relative load of the supplementary firing 10 the required oxygen concentration increases again and is proportional to the injected fuel gas flow. Depending on the design of the supplementary firing, the required residual oxygen concentration varies as a function of load. For example, a required oxygen concentration, which is proportional to the load, is possible. Further, the load range might be restricted to higher loads, e.g. 40% to 100% load. In any case, in order to maximize the resulting CO<sub>2</sub> after supplementary firing, a variation of the residual oxygen concentration of the flue gases from the GT 8 is needed. This increases the complexity of the control integration, and can lead to combustion instabilities in the GT. Further, it leads to variation in the second partial flow 20 of the flue gases, which flows to the CO<sub>2</sub> capture system 18, as a function of the relative load of the supplementary firing. The required residual oxygen concentration for the supplementary firing can limit the recirculation ration and result in an increased maximum second partial flow 20.

In a proposed second approach, supplementary firing with additional ambient air, oxygen enriched air or oxygen flow  $F_{air}$  is applied. As schematically shown in Fig. 4, the normalized residual oxygen concentration of the gas turbine flue gas  $GT_{O2}$  required for supplementary firing over relative load of the supplementary firing

5  $SF_{load}$  can be kept constant independently of relative load of the supplementary firing. Therefore no complex control interface or logic between the gas turbine and supplementary firing is needed.

In this proposed second approach, the fuel gas is burned in the supplementary 10 firing burner with an additional ambient airflow, oxygen enriched airflow or oxygen flow  $F_{air}$ . The supplementary firing burner can thereby work independently from gas turbine flue gas oxygen concentration and produces flue gas at low O2 and high CO2 concentrations. With this method it can be assured that after mixing the 15 flue gases of the supplementary firing with flue gases of the gas turbine flue, the CO2 concentration in the resulting flue gas mixture will not be or only very slightly diluted. Thus the flue gas recirculation rate could and shall be designed at its maximum allowed value to keep the minimal oxygen concentration i.e. the highest 20 CO2 concentration in the gas turbine flue gases while sending the minimum amount of flue gas from CCPP to the CO2 capture plant.

20

Further, the normalized additional ambient air, oxygen enriched air or oxygen flow 25  $F_{air}$  required to assure stable and complete combustion is also shown in Fig. 4. It is normalized with the additional ambient air or oxygen flow required at 100% load. At low relative load of the supplementary firing 10, the temperature is low and a relatively high ambient airflow, oxygen enriched airflow or oxygen flow  $F_{air}$  is required to assure complete combustion. It is typically well above stoichiometric and results in high residual oxygen concentration  $SF_{O2}$  after the supplementary firing. With increasing load the flame temperature increases and the required 30 additional ambient airflow, oxygen enriched airflow or oxygen flow  $F_{air}$  only increases at a low rate. The fuel specific additional ambient airflow, oxygen enriched airflow or oxygen flow  $F_{air}$  can be reduced. Ideally almost stoichiometric combustion can be realized. For high relative load of the supplementary firing 10 the fuel specific additional ambient airflow, oxygen enriched airflow or oxygen flow 35  $F_{air}$  stays almost constant. The required additional ambient airflow, oxygen enriched airflow or oxygen flow  $F_{air}$  is mainly needed to assure a sufficient oxygen concentration for complete combustion and increases at a higher rate, which is proportional to the injected fuel gas flow. Depending on the design of the

supplementary firing this dependency of required residual oxygen concentration as a function of load varies. Further, the load range might be restricted to higher loads, e.g. 40% to 100% load.

5 The resulting normalized residual oxygen concentration after supplementary firing SF<sub>O<sub>2</sub></sub> is also shown in this Figure. It is normalized with the oxygen concentration after supplementary firing SF<sub>O<sub>2</sub></sub> at 100% load. For this example it reaches a minimum at 100% load. At 100% load the combustion temperature is highest, which facilitates a fast complete combustion down to very low residual oxygen 10 concentration and corresponding high CO<sub>2</sub> concentration.

In general the CO<sub>2</sub> concentration is inverse proportional to the residual oxygen concentration, and low oxygen concentration corresponds to a high CO<sub>2</sub> concentration.

15 The CO<sub>2</sub> and the residual oxygen concentration at different locations of the thermodynamic process of a CCPP can be determined using main process parameters. Based on the inlet mass flow, the recirculation rate, the fuel mass flows, mass flow of ambient airflow, oxygen enriched airflow or oxygen flow F<sub>air</sub> 20 injected, and the combustion efficiency, the oxygen concentration and CO<sub>2</sub> concentration in the inlet gas, after the gas turbine, and after the supplementary firing can be estimated. These estimated values are used in one embodiment of the invention.

25 Since the inlet mass flow of a gas turbine is difficult to measure one normally has to rely on compressor characteristics to determine the inlet mass flow. Due to compressor ageing the real inlet mass flow can differ from the value of the characteristics. Further, the fuel's heating value depends on the fuel gas composition, which can change over time. Therefore either additional 30 measurements like on line fuel gas analysis have to be applied or considerable uncertainties have to be taken into account for. For practical reasons it is therefore often easier to measure the gas compositions directly. These measurements are part of a further embodiment. Corresponding measurement devices were indicated in Fig. 1.

35 Besides conventional gas chromatography there are several different methods, systems, and measurement devices to measure the oxygen concentration and

CO<sub>2</sub> concentration of the different gas streams. CO<sub>2</sub> can for example easily be measured using Nondispersive Infrared (NDIR) CO<sub>2</sub> Sensors, or Chemical CO<sub>2</sub> Sensors. Oxygen concentration can, among others, be measured using zirconia, electrochemical or Galvanic, infrared, ultrasonic sensors, and laser technology.

5 Fast online sensors can be applied for optimized operation.

Exemplary embodiments described above and in the drawings disclose to a person skilled in the art embodiments, which differ from the exemplary embodiments and which are contained in the scope of the invention.

10

For example, blowers might be advantageous for first partial flow 21 of the flue gases, which is recirculation or for the second partial flow 20 of the flue gases, which flows to the CO<sub>2</sub> capture system 18. Without blowers the pipes and equipment size needed to allow sufficient flow with existing pressure differences 15 might become prohibitive.

Further, when an additional ambient airflow, oxygen enriched airflow or oxygen flow  $F_{air}$  is used for the supplementary firing this flow can be preheated by low grade heat from the water steam cycle, and/ or the CO<sub>2</sub> capture system 18, and/ 20 or the flue gases. Return condensate from intermediate pressure feed water can for example be utilized for this.

Further, one could replace dampers or other control organs, which inherently lead to a pressure drop, by controlled blowers. These could for example be variable 25 speed blowers or blowers with controllable blade or guide vane angles.

## List of reference symbols

5        1        Compressor  
2        Ambient air  
3        Compressor inlet gas  
4        Combustor  
5        Fuel gas for GT  
10      6        Gas turbine (GT)  
7        Turbine  
8        Hot flue gas from gas turbine  
9        HRSG (heat recovery steam generator)  
10      10      Low excess air supplementary firing (SF)  
15      11      Ambient air, and/or oxygen enriched air, and/or oxygen  
12      Fuel gas for supplementary firing  
13      Steam turbine  
14      Condenser  
15      Steam extraction for CO<sub>2</sub> capture  
20      16      Feed water  
17      Condensate return line  
18      CO<sub>2</sub> capture system  
19      Flue gas from HRSG  
20      Second partial flow (Flue gas CO<sub>2</sub> capture system)  
25      21      First partial flow (Flue gas recirculation)  
22      CO<sub>2</sub> depleted flue gas  
23      Flue gas cooler  
24      Flue gas bypass to stack  
25      First generator  
30      26      Second generator  
27      Recirculation flue gas cooler  
28      Burner box  
29      Damper  
30      Steam  
35      31      Captured CO<sub>2</sub>  
32      Stack  
33      Cross section of HRSG inlet

34 Fuel gas injection orifices  
35 Oxidizer injection orifices  
36 Inlet air CO<sub>2</sub> and/or O<sub>2</sub> measurement devices  
37 Gas turbine flue gas CO<sub>2</sub> and/or O<sub>2</sub> measurement devices  
5 38 HRSG flue gas CO<sub>2</sub> and/or O<sub>2</sub> measurement devices  
CCPP Combined cycle power plant  
SF<sub>load</sub> Relative load of supplementary firing (SF)  
GT<sub>O<sub>2</sub></sub> Normalized residual oxygen concentration after GT  
SF<sub>O<sub>2</sub></sub> Normalized residual oxygen concentration after SF  
10 F<sub>air</sub> Normalized supplementary air/ oxygen enriched air/ oxygen flow

## Patent claims

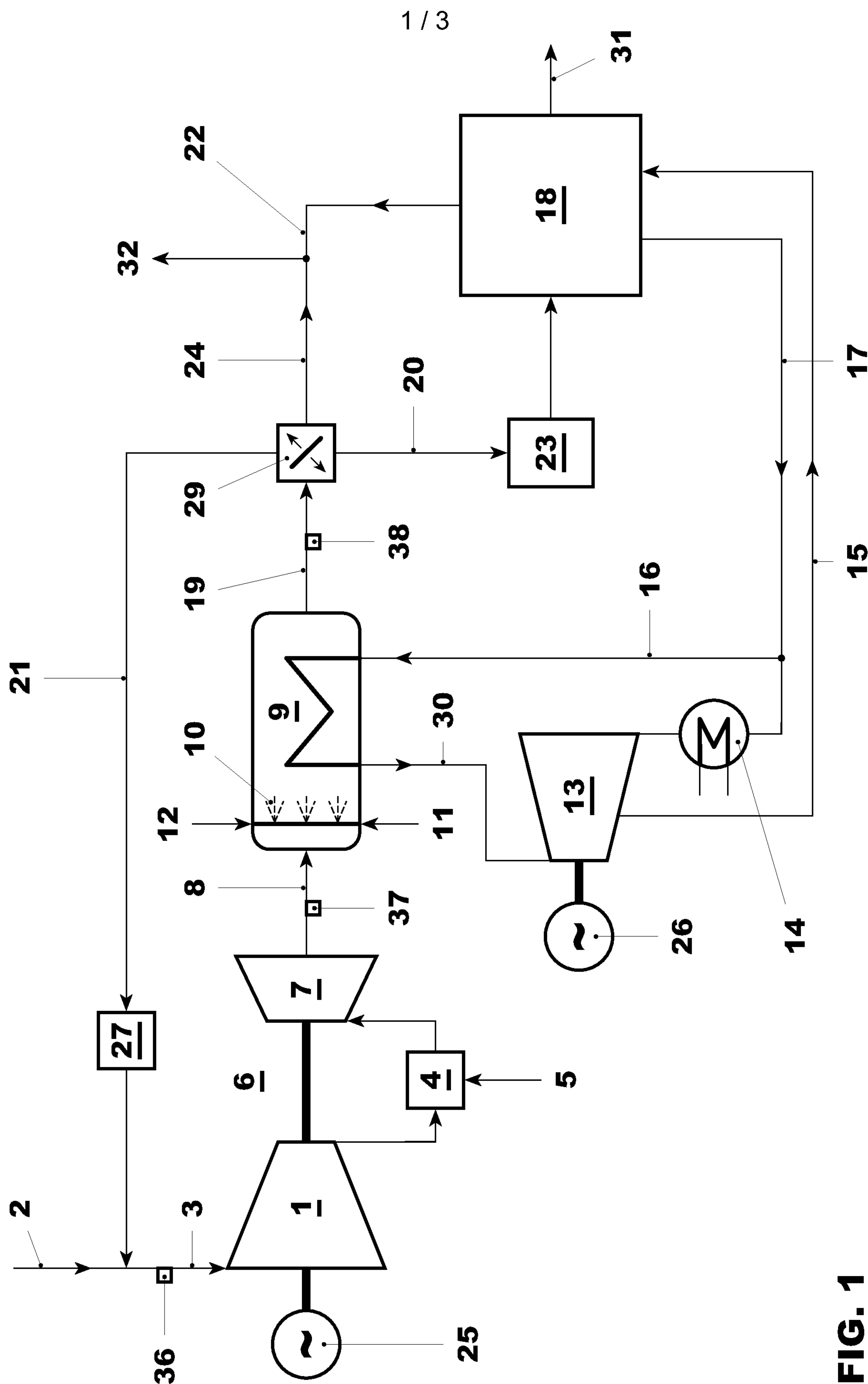
1. A method for operating a combined cycle power plant comprising at least one gas turbine (6), one heat recovery steam generator (9), one steam turbine (13) and CO<sub>2</sub> capture system (18), characterized in that a first partial flow (21) of the flue gases from the HRSG (19) is recirculated and that CO<sub>2</sub> is captured from a second partial flow (20) of flue gases from the HRSG (19), and that a supplementary firing (10) is operated to increase the net power output of the plant and to at least partly compensate the power consumption of the CO<sub>2</sub> capture system (18).  
5
2. A method according to claim 1, characterized in that the first partial flow (21) is recirculated at recirculation rate, which is controlled at a highest possible recirculation rate under the conditions, that stable complete combustion in the gas turbine (6) can be maintained, and that a residual oxygen concentration after the gas turbine (GT<sub>O<sub>2</sub></sub>) is sufficient to maintain stable complete combustion of the supplementary firing (10).  
10
3. A method according to claim 1 or 2, characterized in that an additional ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow (11) is injected into the supplementary firing (10) for stable complete combustion of the supplementary firing (10).  
15
4. A method according to claim 3, characterized in that a sufficient ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow (11) is injected into the supplementary firing (10), such that the recirculation rate can be controlled independently of the oxygen concentration required for stable complete combustion of the supplementary firing (10).  
20
5. A method according to claim 3 or 4, characterized in that the additional ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow (11) is a function of the recirculation rate.  
25
6. A method according to one of the claims 3 to 5, characterized in that the additional ambient air flow, and/ or oxygen enriched air flow, and/ or

oxygen flow (11) is a function of the residual oxygen concentration after the gas turbine (GT<sub>O<sub>2</sub></sub>).

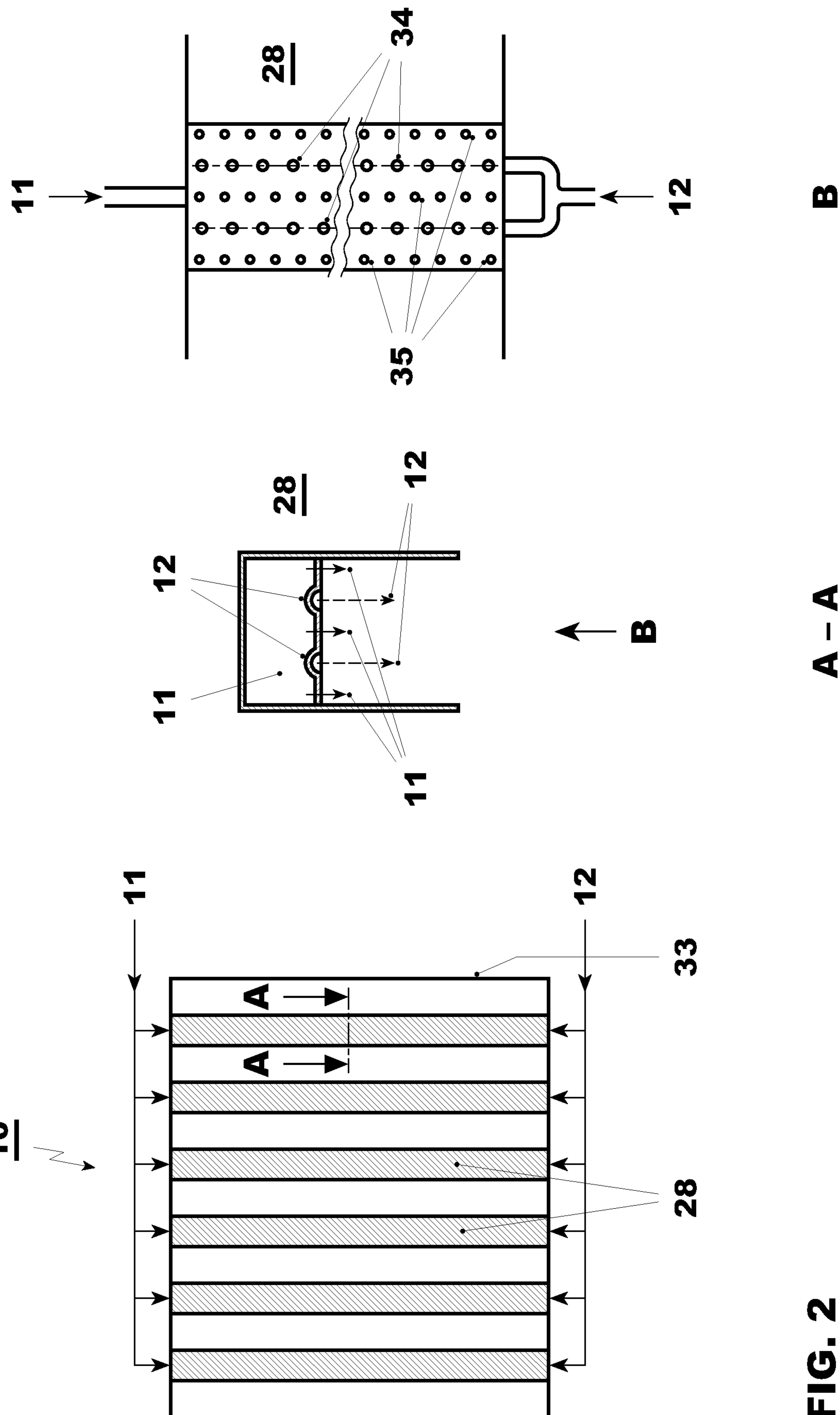
7. A method according to one of the claims 3 to 6, characterized in that the additional ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow (11) is a function of the supplementary firing load.
8. A method according to one of the claims 3 to 7, characterized in that the additional ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow (11) is a function of the recirculation rate and/ or a function of the residual oxygen concentration after the gas turbine and/ or a function of the supplementary firing load.
9. A method according to one of the claims 3 to 8, characterized in that the additional ambient air flow, and/ or oxygen enriched air flow, and/ or oxygen flow (11) is preheated by low grade heat from a water steam cycle of the combined cycle power plant, and/ or the CO<sub>2</sub> capture system (18), and/ or the flue gases.
10. A method according to one of the claims 1 to 9, characterized in that the supplementary firing (10) is operated to increase the net power output for power augmentation during peak demand and to increase its operational flexibility.
11. A combined cycle power plant comprising at least one gas turbine (6), at least one heat recovery steam generator (9), at least one steam turbine (13) and at least CO<sub>2</sub> capture system (18), and flue gas recirculation, characterized in that a low excess air supplementary firing (10) is provided.
12. A combined cycle power plant according to claim 11, characterized in that ambient air supply lines, and/ or oxygen enriched air supply lines, and/ or oxygen supply lines to the low excess air supplementary firing (10) are provided.
13. A combined cycle power plant according to claim 11 or 12, characterized in that an oxygen enrichment plant and/ or an air separation unit is provided.

14. A combined cycle power plant according to one of the claims 11 to 13, characterized in that at least one oxygen measurement device is installed to measure the oxygen concentration of the inlet gases of the compressor inlet gas (2) and/ or to measure the residual oxygen concentration of the hot flue gases of the gas turbine (8) and/ or to measure the residual oxygen concentration of the flue gases from the heat recovery steam generator (19).

15. A combined cycle power plant according to one of the claims 11 to 14, characterized in that at least one CO<sub>2</sub> measurement device is installed to measure the CO<sub>2</sub> concentration of the inlet gases of the compressor inlet gas (2) and/ or to measure the CO<sub>2</sub> concentration of the hot flue gases of the gas turbine (8) and/ or to measure the CO<sub>2</sub> concentration of the flue gases from the heat recovery steam generator (19).

**FIG. 1**

2 / 3

**FIG. 2**

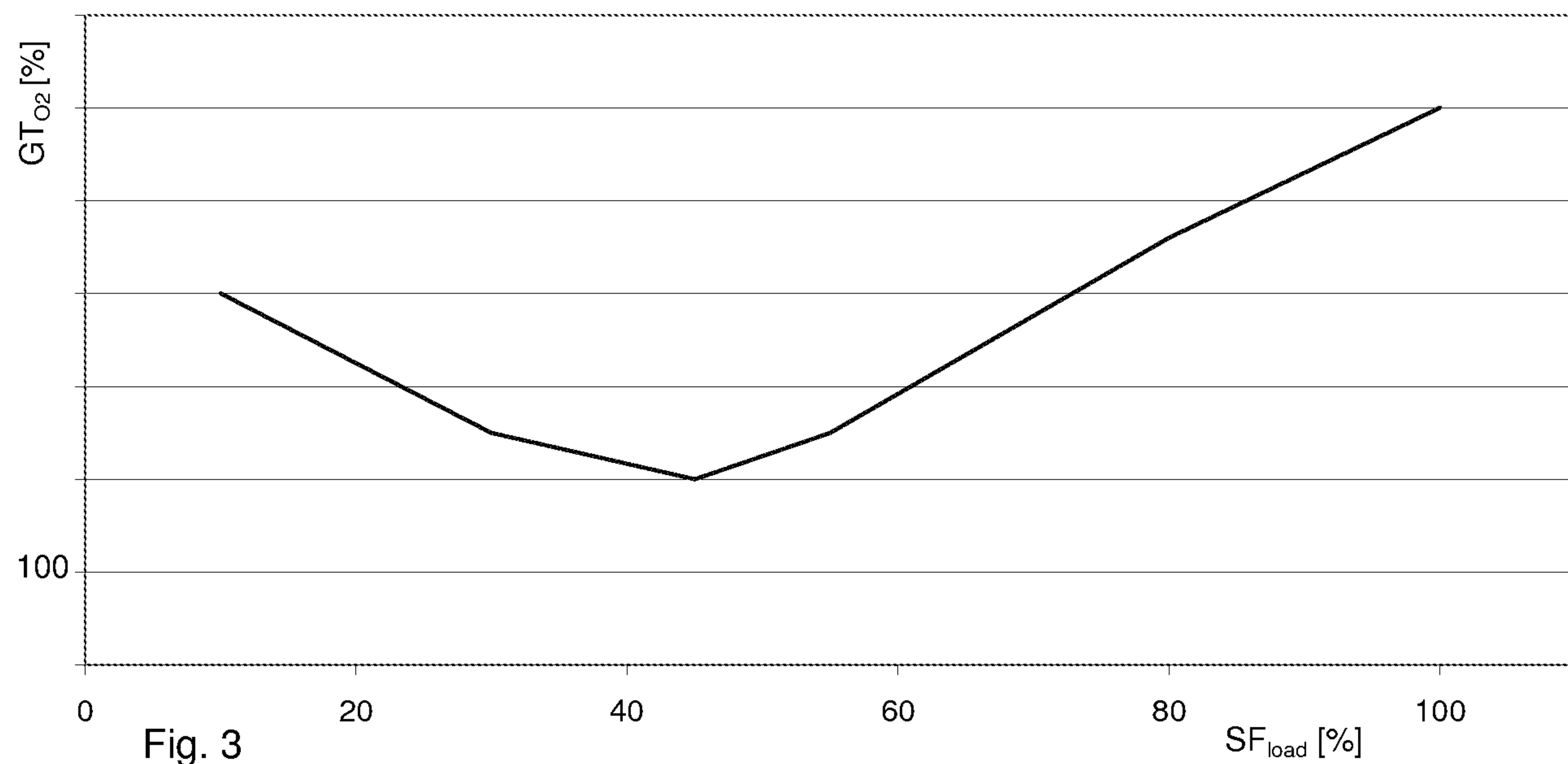


Fig. 3

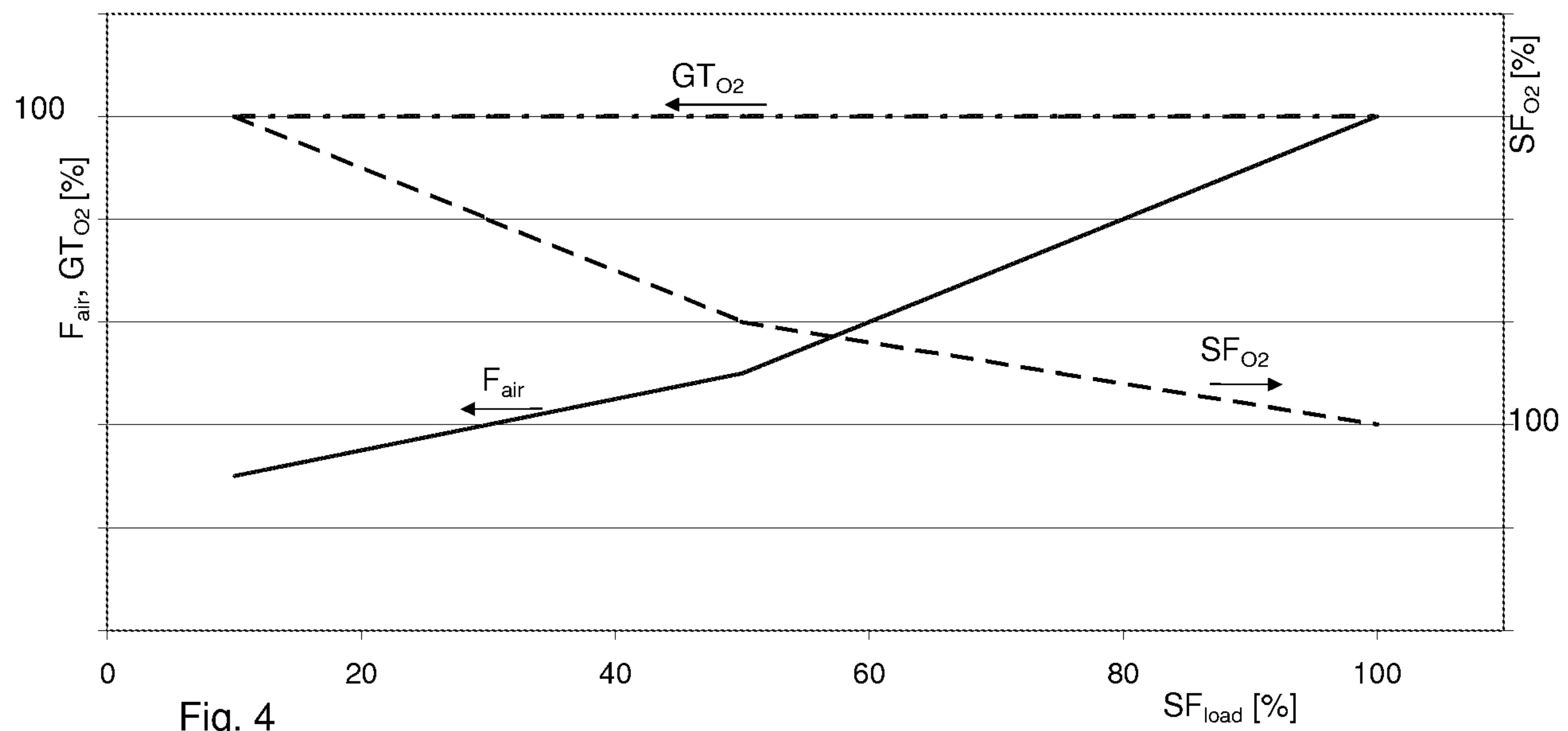


Fig. 4

