(19) Europäisches Patentamt
European Patent Office
Office européen des brevets

(11) EP 0 646 189 B1

(12) EUROPEAN PATENT SPECIFICATION

(45) Date of publication and mention of the grant of the patent:
20.08.1997 Bulletin 1997/34

(21) Application number: **92904563.1**

(22) Date of filing: **29.01.1992**

(51) Int Cl.[6]: **D01F 6/62**

(86) International application number:
PCT/US92/00359

(87) International publication number:
WO 92/13119 (06.08.1992 Gazette 1992/21)

(54) PREPARING POLYESTER FINE FILAMENTS

HERSTELLUNG VON FEINEN POLYESTERFILAMENTEN

PROCEDE DE PREPARATION DE MINCES FILAMENTS DE POLYESTER

(84) Designated Contracting States:
CH DE ES FR GB IT LI NL

(30) Priority: **29.01.1991 US 647371**
29.01.1991 US 647381

(43) Date of publication of application:
05.04.1995 Bulletin 1995/14

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Remarks:

The file contains technical information submitted after the application was filed and not included in this specification

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Description

This invention concerns improvements in, and relating to, polyester fine filaments and their manufacture and use.

Historically, synthetic fibers for use in apparel, including polyester fibers, have generally been supplied to the textile industry for use in fabrics and garments with the object of more or less duplicating and/or improving on natural fibers. For many years, commercial synthetic textile filaments, such as were made and used for apparel, were mostly of deniers per filament (dpf) in a similar range to those of the commoner natural fibers; i.e., cotton and wool. More recently, however, polyester filaments have been available commercially in a range of dpf similar to that of natural silk, i.e. of the order of 1 dpf, and even in subdeniers, i.e., less than about 1 dpf, despite the increased cost. Various reasons have been given for the recent commercial interest in such lower dpfs, such as about 1 dpf, or even subdeniers.

Much has been written recently about this increasing interest in fine denier polyester filaments. Very little technical detail has, however, been published about any difficulties in spinning (i.e., extrusion and winding) techniques that have been used, or even would be desirable, for manufacturing such fine filaments, although it has been well understood by those skilled in the art that conventional preparation and handling techniques could not be used for such fine filaments. For instance, in Textile Month, June 1990, pages 40-46, three approaches are discussed for making microfibers; namely, 1) conventional spinning to fine deniers, 2) splitting bicomponent fibers (of higher deniers), and 3) dissolving away a component from bicomponent fibers of higher denier. It will be understood that the 2nd and 3rd approaches involve bicomponent spinning to form filaments first of higher denier, and processing such spun higher denier filaments to obtain the filaments of reduced denier; such processing techniques are not the subject of the present invention.

The present invention is concerned with the preparation of fine filaments by a novel direct spinning/winding process, in contrast with a process of first spinning and winding up bicomponent filaments of higher denier which then must be further processed to obtain the reduced fine denier filaments that are desired for use in textiles. Another 2-stage possibility of manufacturing filaments of reduced denier is to spin filaments of greater than one denier, and then, draw the filaments after the spinning operation, but this possibility has important disadvantages that have been discussed in the art; on the one hand, there are practical limitations to the amount of draw that can be effected; there are also product disadvantages in the properties of drawn yarns, as contrasted with direct spin-oriented yarns; and the cost of such processing (i.e., drawing) has to be considered, especially when the drawing is performed as a separate operation, after first packaging the spun filaments, such as single yarn or warp drawing. Such drawing proposals may have involved conventional drawing techniques, or may have involved other techniques, e.g., aerodynamic effects or reheating the filaments after they have been solidified, but still advancing under sufficient tension to draw (sometimes referred to as space-drawing, if performed without godets of differential speeds). Some direct spinning processes that have been proposed have relied on use of specific polymer compositions, for instance specific viscosities, that have disadvantages, so it would be desirable to use a process that does not require use of special viscosities or other special compositional aspects.

To summarize, previous polyester filament manufacturing techniques that have been disclosed in the art have not been specifically directed to and have not been suitable in practice for producing fine denier polyester filaments by a simple direct spinning/winding operation, or have involved limitations and disadvantages. So it has been desirable to provide such a direct spinning process for manufacturing fine polyester filaments of the desired dpf and properties without such disadvantages. The present invention solves this problem. The filaments of the invention are "spin-oriented", the significance of which is discussed in the art and hereinafter.

Commercial polyester filaments were made initially by "split" processes that involved a separate drawing stage after spinning and winding undrawn filaments. In the 1950's, Hebeler suggested in U. S. Patents Nos. 2,604,667 and 2,604,689, the possibilities of high speed spinning of polyester melts. In the 1970's, high speed spinning of polyester melts, as described by Petrille in U. S. Patent No. 3,771,307 and by Piazza and Reese in U. S. Patent No. 3,772,872, were made the basis of a process for preparing spin-oriented yarns that have been used as draw-texturing feed yarns. High speed spinning of polyester melts has also been the basis of other processes that were first disclosed in the 1970's, such as Knox in U. S. Patent No. 4,156,071, and Frankfort and Knox in U. S. Patent Nos. 4,134,882, and 4,195,051.

The art discloses fundamental differences in fine structure and properties between filaments that are spin-oriented, indicating orientation of the polyester molecules obtained from the (high speed) spinning, and drawn filaments, indicating orientation derived from drawing of the filaments as an entirely separate process, after winding the spun filaments, or even as a continuous process, before winding, but after cooling the melt to form solid filaments before drawing such filaments.

An object of the present invention is to provide fine filaments that have the characteristics of being spin-oriented, because of the advantageous properties that are provided by this characteristic.

Several aspects and embodiments are provided according to the present invention as follows:

1) a process for preparing spin-oriented polyester fine filaments;

2) spin-oriented polyester fine filaments with deniers about 1 or less, having enhanced mechanical quality and denier uniformity making these filaments especially suitable for high speed textile processing;

3) spin-oriented polyester fine filaments, especially suitable for use as draw feed yarns in high speed texturing, crimping, and warping processes;

4) spin-oriented polyester fine filaments, especially suitable for use as direct-use textile yarns, without need for additional draw or heat treatments, in critically dyed flat woven and knit fabrics; for use as feed yarns for air-jet texturing and stuffer-box crimping, wherein no draw is required; and may be uniformly cold drawn, if desired, to prepare warp yarns of higher shrinkage with dye uniformity suitable for critically dyed end-uses;

5) drawn spin-oriented polyester fine filaments, especially suitable for use as textile yarns in critically dyed flat woven and knit fabrics; and processes for preparing these fine drawn fine filament yarns;

6) bulked polyester fine filament yarns capable of being dyed uniformly under atmospheric conditions without the use of carriers; and a process for preparing these bulked fine filament yarns;

7) mixed filament yarns, wherein the fine filaments are of this invention; and especially mixed filament yarns, wherein, all filaments are of this invention, but differ in denier, cross-section, and/or shrinkage potential.

In particular according to the present invention, the following are provided:
A process for preparing spin-oriented polyester fine filaments of denier in the range of 1 to 0.2, wherein,

(i) the polyester polymer is selected to have a relative viscosity (LRV) in the range of 13 to 23, a zero-shear melting point ($T_M°$) in the range of 240°C to 265°C, and a glass transition temperature (T_g) in the range of 40°C to 80°C;

(ii) said polyester is melted and heated to a temperature (T_P) in the range of 25°C to 55°C, preferably in the range of 30°C to 50°C, above the apparent polymer melting point $(T_M)_a$;

(iii) the resulting melt is filtered sufficiently rapidly that the residence time (t_r) in the filter cavity is less than 4 minutes;

(iv) the filtered melt is extruded through a spinneret capillary at a mass flow rate (w) in the range 0.07 to 0.7 grams per minute (g/min), and the capillary is selected to have a cross-sectional area (A_c) in the range $125x10^{-6}$ cm^2 (19.4 $mils^2$) to $1250x10^{-6}$ cm^2 (194 $mils^2$) preferably in the range of $125x10^{-6}$ cm^2 (19.4 $mils^2$) to $750x10^{-6}$ cm^2 (116.3 $mils^2$) and a length (L) and diameter (D_{RND}) such that the (L/D_{RND})-ratio is at least 1.25 and preferably less than 6, and especially less than 4;

(v) protecting the extruded melt from direct cooling as it emerges from the spinneret capillary over a distance (L_{DQ}) of at least 2 cm and less than ($12dpf^{½}$)cm, where dpf is the denier per filament of the spin-oriented polyester fine filament, preferably in the range of 1 to 0.2 dpf, and especially in the range of 0.8 to 0.2 dpf; and desireably an average along-end denier spread (DS) less than 4%, and preferably less than 3%, and especially less than 2%;

(vi) cooling the attenuating spinline to below the polymer glass-transition temperature (T_g), preferably by radially directed air having a temperature (T_a) less than the polymer T_g and a velocity (V_a) in the range of 10 to 30 meters per minute (m/min);

(vii) attenuating to an apparent spinline strain (ε_a) in the range of 5.7 to 7.6, and to an apparent internal spinline stress (σ_a) in the range of 0.045 to 0.195 grams per denier (g/d), preferably in the range of 0.045 to 0.105 g/d for preparing filaments especially suitable for draw feed yarns, characterized by a tenacity-at-7%-elongation (T_7) in the range of 0.5 to 1 g/d; and to an apparent internal spinline stress (σ_a) preferably in the range of 0.105 to 0.195 g/d for preparing filaments especially suitable for direct-use yarns, characterized by a tenacity-at-7%-elongation (T_7) in the range of 1 to 1.75 g/d;

(viii) converging the cooled and attenuated filaments into a multifilament bundle by use of a low friction surface at a distance (L_c) in the range 50 cm to 140 cm, preferably in the range of 50 cm to ($50+90dpf^{½}$)cm;

(ix) withdrawing the multifilament bundle at a withdrawal speed (V) in the range of 2 to 6 kilometers per minute (km/min), preferably in the range of 2 to 5 km/min, and especially in the range of 2.5 to 5 km/min, followed by

winding up the withdrawn bundle at a speed which is 95% to 100% that of the withdrawal speed;

Preferably the filaments have a denier in the range of 0.6 to 0.2 and a denier spread (DS) less than 2%.

Also, according the present invention the following spin-oriented polyester fine filaments, and products there from, are provided:

Spin-oriented polyester fine filaments of denier per filament (dpf) 1 or less, preferably in the range of 0.8 to 0.2 dpf, wherein, said polyester is characterized by having a relative viscosity (LRV) in the range of 13 to 23, a zero-shear polymer melting point ($T_M°$) in the range of 240°C to 265°C, and a glass-transition temperature (T_g) in the range of 40°C to 80°C; and said fine filaments are further characterized by:

(i) boil-off shrinkage (S) less than the maximum shrinkage potential (S_m), wherein $S_m = [(550-E_B)/6.5]$,% and the percent elongation-to-break (E_B) is in the range 40% to 160%;

(ii) maximum shrinkage tension, (ST_{max}), in the range 0.05 to 0.2 g/d, with a peak temperature $T(ST_{max})$, in the range 5°C to 30°C above the polymer glass-transition temperature (T_g);

(iii) a tenacity-at-7%-elongation (T_7) in the range of 0.5 to 1.75 g/d, and such that the $[(T_B)_n/T_7]$-ratio is of at least $(5/T_7)$ and preferably at least $(6/T_7)$; wherein, $(T_B)_n$ is the tenacity-at-break normalized to a reference LRV of 20.8 and % delusterant (such as TiO_2) of 0%;

(iv) desireably an average along-end denier spread (DS) of less than 4%, preferably less than 3%, and especially less than 2%.

Spin-oriented fine filaments, especially suitable for use as draw feed yarns (DFY), characterized by a boil-off shrinkage (S) at least 12%, an elongation-at-break (E_B) in the range 80% to 160%, a tenacity-at-7%-elongation (T_7) in the range 0.5 to 1 g/d.

Spin-oriented fine filaments, especially suitable for use as direct-use yarns (DUY), characterized by a shrinkage differential (Δs = DHS - S) less than +2%, wherein, boil-off shrinkage (S) and dry heat shrinkage (DHS) are in the range of 2% to 12%, such that the filament denier after boil-off shrinkage, dpf(ABO), is 1 or less and preferably in the range of 1 to 0.2 dpf, and more preferably in the range of 0.8 to 0.2 dpf; a tenacity-at-7%-elongation (T_7) in the range of 1 to 1.75 g/d; an elongation-at-break (E_B) in the range of 40% to 90%, and a post-yield modulus (M_{py}) in the range of 2 to 12 g/d;

Spin-oriented fine filaments having the capability of being uniformly cold drawn, characterized by a shrinkage differential (ΔS = DHS - S) less than +2%, wherein, boil-off shrinkage (S) and dry heat shrinkage (DHS) are in the range of 2% to 12%, an onset of cold crystallization, T_{cc}(DSC), of less than 105°C and an instantaneous tensile modulus (M_i) at least 0.

Drawn spin-oriented polyester fine filaments with deniers after boil-off shrinkage, dpf(ABO), in the range of 1 or less, preferably in the range of 0.8 to 0.2 dpf, wherein, said drawn filaments are further characterized by:

(i) boil-off shrinkage (S) and dry heat shrinkage (DHS) in the range of 2% to 12%;

(ii) a tenacity-at-7%-elongation (T_7) of at least 1 g/d, such that the $[(T_B)_n/T_7]$-ratio is at least $(5/T_7)$; preferably at least $(6/T_7)$, wherein, $(T_B)_n$ is the tenacity-at-break normalized to a reference LRV of 20.8 and percent delusterant (such as TiO_2) of 0%; and an elongation-at-break (E_B) in the range of 15% to 55%;

(iii) a post-yield modulus (M_{py}), preferably in the range 5 to 25 g/d;

(iv) desirably an average denier spread (DS) less than 4%, preferably less than 3%, especially less than 2%.

Bulked spin-oriented polyester fine filaments of denier after boil-off shrinkage, dpf (ABO),in the range of 1 to 0.2 dpf, preferably 0.8 to 0.2 dpf, wherein, said bulked filaments are further characterized by a boil-off shrinkage (S) and dry heat shrinkage (DHS) in the range 2% to 12%, an elongation-at-break (E_B) in the of range 15% to 55%, a tenacity-at-7%-elongation (T_7) at least 1 g/d, and preferably with a post-yield modulus (M_{py}) in the range 5 to 25 g/d and a relative disperse dye rate (RDDR), normalized to 1 dpf, of at least 0.1.

Mixed filament yarns, wherein the fine filaments are of this invention; and especially mixed filament yarns, wherein, all filaments are of this invention, but differ in denier, cross-section, and/or shrinkage potential.

Preferred such spin-oriented, bulked and drawn flat filaments are capable of being dyed with cationic dyestuffs, on account of containing in the range of 1 to 3 mole % of ethylene-5-M-sulfo-isophthalate structural units, where M is

an alkali metal cation, such sodium or lithium.

Especially preferred such spin-oriented, bulked, and drawn flat filaments capable of being disperse dyed uniformly under atmospheric conditions without carriers, are characterized by a dynamic loss modulus peak temperature $T(E"_{max})$ of less than about 115°C, preferably less than about 110°C; and are of polyester polymer, essentially poly(ethylene terephthalate), composed of first alternating hydrocarbolenedioxy structural units A, [-O-C_2H_4-O-], and hydrocarbolenedicarbonyl structural units B, [-C(O)-C_6H_4-C(O)-], modified with minor amounts of other hydrocarbolenedioxy structural units A and/or hydrocarbolenedicarbonyl structural units B, that are different from the first structural units, such as to provide a polyester polymer with a zero-shear melting point (T_M°) in the range 240°C to 265°C and a glass-transition temperature (T_g) in the range of 40°C to 80°C.

The filaments of the present invention may be nonround for enhanced tactile and visual aesthetics, and comfort, where said nonround filaments have a shape factor (SF) at least 1.25, wherein the shape factor (SF) is defined by the ratio of the measured filament parameter (P_M) and the calculated parameter (P_{RND}) for a round filament of equivalent cross-sectional area. Hollow filaments may be spun via post-coalescence from segmented spinneret capillary orifices to provide lighter weight fabrics with greater bulk and filament bending modulus for improved fabric drape.

Further aspects and embodiments of the invention will appear herein.

FIG. 1 is a graphical representation of spinline velocity (V) plotted versus distance (x) where the spin speed increases from the velocity at extrusion (V_o) to the final (withdrawal) velocity after having completed attenuation (typically measured downstream at the point of convergence, V_c); wherein, the apparent internal spinline stress (σ_a) is taken as being proportional to the product of the spinline viscosity at the neck point $(\eta)_N$, (i.e., herein found to be approximately proportional to about the ratio LRV/T_p^6, where T_P is expressed in °C),and the velocity gradient at the neck point (dV/dx), (herein found to be approximately proportional to about V^2/dpf, especially over the spin speed range of about 2 to 4 km/min and proportional to about $V^{3/2}$/dpf at higher spin speeds, e.g., in the range of about 4 to 6 km/min). The spin line temperature is also plotted versus spinline distance (x) and is observed to decrease uniformly with distance as compared to the sharp rise in spinline velocity at the neck point.

FIG. 2 is a graphical representation of the birefringence (Δ_n) of the spin-oriented filaments versus the apparent internal spinline stress $(\sigma)_a$; wherein the slope is referred to as the "stress-optical coefficient, SOC" and Lines A, B, and C have SOC values of 0.75, 0.71, and 0.645 $(g/d)^{-1}$, respectively; with an average SOC of about 0.7; and wherein Lines A and C are typical relationships found in literature for 2GT polyester. The values of the apparent internal spinline stress (σ_a) agree well with values found in literature.

FIG. 3 is a graphical representation of the tenacity-at-7%-elongation (T_7) of the spin-oriented filaments versus the apparent internal spinline stress (σ_a). The near linear relationship of birefringence (Δ_n) and T_7 versus the apparent internal spinline stress (σ_a), as shown in FIGS. 2 and 3, permits the use of T_7 as a useful parameter being representative of the filament average orientation. Birefringence (Δ_n) is typically very difficult structural parameter to measure for fine filaments with deniers less than 1.

FIG. 4 is a graphical representation of the preferred values of the apparent internal spinline stress (σ_a) and the spin-oriented filament yarn tenacity-at-7%-elongation (T_7) plotted versus the spin line extension ratio E_R (= V/V_o) on a natural logarithm scale (where E_R-values of 200 and 2000, for example are expressed on the x-axis as 0.2 and 2; i.e., E_R/1000); wherein the natural logarithm $\ln(E_R)$ is called herein as the apparent spinline strain (ε_a), where V is the final (withdrawal) spinline velocity and V_o is the capillary extrusion velocity. The process of the invention is described by the enclosed region ADLI with region ADHE (II) preferred for preparing direct-use filaments and region EHLI (I) preferred for preparing draw feed yarns. Especially preferred processes are represented by regions BCGF and FGKI.

FIG. 5 is a representative Instron load-extension curve showing the graphical calculation of the "secant" post-yield modulus (M_{py}) calculated from the tenacity-at-7%-elongation (T_7), denoted by point C, and from the tenacity-at-20%-elongation (T_{20}), denoted by point A, and defined by the expression $(1.2T_{20} - 1.07\ T_7)/0.13$; and compares the "secant" M_{py} (herein denoted as tan β to that of the "tangential" M_{py} (herein denoted as tan α, i.e., slope of line segment AB). For yarns which have an instantaneous modulus M_i (= d(stress)/d(elongation) greater than about 0, the value of tan β is about the same as tan α.

FIG. 6 is a graphical representation of the secant M_{py} (tan β in FIG. 5) versus birefringence (Δ_n) of spin-oriented filaments. For yarns wherein tan α is essentially equal to tan β, the post-yield modulus (M_{py}) becomes a useful measure of molecular orientation.

FIG. 7 is a graphical representation of the Relative Disperse Dye Rate (RDDR), as normalized to 1 dpf, versus the average filament birefringence (Δ_n).

FIG. 8 is a graphical representation of the filament amorphous free-volume of the fiber ($V_{f,am}$, as defined herein after), versus the peak temperature of the fiber dynamic loss modulus, $T(E"_{max})$, taken herein as a measure of the glass transition temperature which is typically 20°C to about 50°C above the T_g of the polymer. A decreasing T(E"max) value corresponds to greater amorphous free-volume ($V_{f,am}$), and hence to improved dyeability, as measured herein by a Relative Disperse Dye Rate (RDDR) value (normalized to 1 dpf) of at least about 0.1.

FIG. 9 is a graphical representation of the filament density (ρ) versus birefringence (Δ_n); wherein the diagonal lines

represent combinations of density (ρ) and (Δ_n) of increasing fractional amorphous orientation (f_a), used in the calculation of the free-volume $V_{f,am}$ depicted in FIG. 8.

FIG. 10 is a representative Differential Scanning Calorimetry (DSC) spectrum showing the thermal transitions corresponding to the glass-transition temperature (T_g), onset of "cold" crystallization T_{cc}(DSC) and the zero-shear melting point T_M of the fiber, which is higher than the zero-shear melting point $T_M°$ of the polymer due to the effect of orientation and crystallinity of the fiber melting point. To measure the zero-shear melting point ($T_M°$) of the polymer, a second DSC heating of the previous melted DSC fiber sample is made to provide the DSC spectrum of the polymer rather than the fiber was extruded.

FIG. 11 is a representative shrinkage tension (ST)-temperature spectrum for the spin-oriented fine polymer filaments of the invention showing the maximum shrinkage tension $ST(_{max})$, peak temperature $T(ST_{max})$ and the preferred "heat set" temperature T_{set} below which heat setting does not appreciably adversely affect dye ability.

FIG. 12 are representative tenacity (T = load (gms)/original denier) versus percent elongation curves for a typical draw feed yarn of the invention (curve C); for a typical direct-use yarn of this invention (curve B); and for the preferred direct-use yarns of the invention after relaxed heat treatment (Curve A); i.e, akin to after dyeing.

FIG. 13 is a graphical representation of the preferred values for the tenacity-at-break $(T_B)_n$, normalized for the affects of LRV and percent delusterant (such as TiO_2), plotted as the $(T_B)_n/T_7$-ratio versus the reciprocal of the T_7 (i. e., versus $1/T_7$); wherein, Curve A: $[(T_B)_n/T_7] = (5/T_7)$; and curve B: $[(T_B)_n/T_7] = (6/T_7)$.

FIG. 14 is a plot of the ratio, $T_7/(V^2/dpf)$ versus the product of the number of filaments per yarn extrusion bundle ($\#_c$) and the ratio, $(D_{ref}/D_{sprt})^2$, where D_{ref} and D_{sprt} are the diameters of a reference spinneret (e.g., about 75 cm) and the test spinneret, respectively. The slope "n" from a ln-ln plot is found to be about negative 0.7 (-0.7); that is, the tenacity-at-7%-elongation (T_7) is found to vary proportionally to (V^2/dpf) and to $[(\#c)(D_{ref}/D_{sprt})^2]^{-0.7}$; that is, the tenacity-at-7%-elongation (T_7) decreases approximately linearly with an increase in the filament extrusion density to the power of plus 0.7 (+0.7); and thereby the filament extrusion density may be used to as a process parameter to spin finer denier filaments at higher spinning speeds (V). At higher spin speeds, e.g., in the range of 4 to 6 km/min, it is found that the apparent spinline stress increases less rapidly with spin speed (V); i.e., is found to be proportional to $(V^{3/2}/dpf)$.

The polyester polymer used for preparing spin-oriented filaments of the invention is selected to have a relative viscosity (LRV) in the range 13 to 23, a zero-shear melting point ($T_M°$) in the range 240°C to 265°C; and a glass-transition temperature (T_g) in the range 40°C to 80°C (wherein $T_M°$ and T_g are measured from the second DSC heating cycle under nitrogen gas at a heating rate of 20°C per minute). The said polyester polymer is a linear condensation polymer composed of alternating A and B structural units, where, A is a hydrocarbolenedioxy unit of the form [-O-R'-O-] and B is a hydrocarbolenedicarbonyl unit of the form [-C(O)-R"-C(O)-], wherein, R' is primarily [$-C_2H_4-$], as in the ethylenedioxy (glycol) unit [$-O-C_2H_2-O-$], and R" is primarily [$-C_6H_4-$], as in the 1,4-benzenedicarbonyl unit [$-C(O)-C_6H_4-C(O)-$], such to provide, for example, at least 85 percent of the recurring structural units as ethylene terephthalate, [$-O-C_2H_4-O-C(O)-C_6H_4-C(O)-$].

Suitable poly(ethylene terephthalate), herein denoted as PET or 2GT, based polymer may be formed by the DMT-process as described by H. Ludwig in his book "Polyester Fibers, Chemistry and Technology", John Wiley and Sons Limited (1971), and by the TPA-process as described in Edging U. S. Patent No. 4,110,316. Included are also copolyesters in which, for example, up to about 15 percent of the hydrocarbolenedioxy and/or hydrocarbolenedicarbonyl units are replaced with different hydrocarbolenedioxy and hydrocarbolenedicarbonyl units to provide enhanced low temperature disperse dyeability, comfort, and aesthetic properties. Suitable replacement units may be found in Most U. S. Patent No. 4,444,710 (Example VI), Pacofsky U. S. Patent No. 3,748,844 (Col. 4), and Hancock, et al. U. S. Patent No. 4,639,347 (Col. 3).

The polyester polymer may also be modified with ionic dye sites, such as ethylene-5-M-sulfo-isophthalate residues, where M is an alkali metal cation, such as sodium or lithium; for example, in the range of 1 to 3 mole percent ethylene-5-sodium-sulfo-isophthalate residues may be added to provide dyeability of the polyester filaments with cationic dyestuffs, as disclosed by Griffing and Remington U. S. Patent No. 3,018,272, Hagewood etal in U. S. Patent No. 4,929,698, Duncan and Scrivener U. S. Patent No. 4,041,689 (Ex. VI), and Piazza and Reese U. S. Patent. No. 3,772,872 (Ex. VII). To adjust the dyeability or other properties of the spin-oriented filaments and the drawn filaments therefrom, some diethylene glycol (DEG) may be added to the polyester polymer as disclosed by Bosley and Duncan U. S. Patent No. 4,025,592 and in combination with chain-branching agents as described in Goodley and Taylor U. S. Patent No. 4,945,151.

According to the present invention the preferred process for preparing spin-oriented polyester filaments having a fineness, for example, in the range of 1 to 0.2 denier per filament (dpf), preferably in the range 0.8 to 0.2 denier per filament (dpf); comprises

(a) melting and heating said polyester polymer, as described herein before, to a temperature (T_P) in the range of about 25°C to about 55°C, preferably in the range of about 30°C to about 50°C, above the apparent melting temperature $(T_M)_a$, wherein, $(T_M)_a$ is greater than the zero-shear melting temperature ($T_M°$) as a result of the

shearing action of the polymer during extrusion and is defined, herein, by:

$$(T_M)_a = [T_M^{\circ} + 2x10^{-4}(L/D_{RND})G_a],$$

where L is the length of the capillary and D_{RND} is the capillary diameter for a round capillary, or for a non-round capillary, wherein, for a non-round capillary, D_{RND} (cm) is the calculated equivalent diameter of a round capillary of equal cross-section area A_c (cm^2); and G_a (sec^{-1}) is the apparent capillary shear rate defined, herein after;

(b) filtering the resulting polymer melt through inert medium, such as described by Phillips in U. S. Patent No. 3,965,010, in a pack cavity (similar to that illustrated in FIG. 2-31 of Jamieson U. S. Patent No. 3,249,669), sufficiently rapidly that the residence time (t_r) is less than about 4 minutes, wherein, t_r is defined by ratio (V_F/Q) of the free-volume (V_F, cm^3) of the filter cavity (filled with the inert filtration medium) and the polymer melt volume flow rate (Q, cm^3/min) through the filter cavity. The polymer melt volume flow rate (Q) through the filter cavity is defined by the product of the capillary mass flow rate (w, g/min) and the number of capillaries ($\#_c$) per cavity divided by the melt density (herein taken to be about 1.2195 g/cm^3); that is, $Q = \#_c w/1.2195$. The free-volume (V_F,cm^3) of the filter cavity (filled with the inert filtration medium) is experimentally determined by standard liquid displacement techniques using a low surface tension liquid, such as ethanol. By replacing the capillary mass flow rate (w), by its equivalent $w = [(dpf \cdot V)/9]$, (where V is the withdrawal spin speed expressed as km/min), in above expression for the melt residence time t_r, it is found that the residence time t_r decreases with increasing filament denier, withdrawal speed (V) and number of filaments ($\#_c$) per filter cavity, and decreases with a reduction in the filter cavity free-volume (V_F). The cavity free-volume (V_F) may be decreased by altering the pack cavity dimensions and by utilizing inert material which provides sufficient filtration capabilities with less free-volume. The number of filaments (i.e, capillaries) per filter cavity ($\#_c$) may be increased for a given yarn count by extruding more than one multifilament bundle from a single filter cavity, that is, spinning a larger number of filaments and then splitting (herein, called multi-ending) the filament bundle into smaller filament bundles of desired yarn denier, preferably by using metered finish tip separator guides positioned between about 50 cm to about ($50+90dpf^{½}$)cm;

(c) the filtered polymer melt is extruded through a spinneret capillary at a mass flow rate (w) in the range of 0.07 to 0.7 grams per minute (g/min) and the capillary is selected to have a cross-sectional area, $A_c = (\pi/4)D_{RND}^2$, in the range of $125x10^{-6}$ cm^2 (19.4 $mils^2$) to $1250x10^{-6}$ cm^2 (194 $mils^2$), preferably in the range of $125x10^{-6}$ cm^2 (19.4 $mils^2$) to $750x10^{-6}$ cm^2 (116 $mils^2$), and a length (L) and diameter (D_{RND}) such that the L/D_{RND}-ratio is in the range of 1.25 to 6, preferably in the range of 1.25 to 4; wherein,

$$G_a\ (sec^{-1}) = [(32/60\pi)(w/\rho)/D_{RND}^3],$$

and w is the capillary mass flow rate (g/min), ρ is the polyester melt density (taken as 1.2195 g/cm^3), and D_{RND} is the capillary diameter (defined herein before) in centimeters (cm);

(d) protecting the freshly extruded polymer melt from direct cooling, as it emerges from the spinneret capillary over a distance L_{DQ} of at least 2 cm and less than ($12dpf^{½}$)cm, where dpf is the denier per filament of the spin-oriented polyester fine filament;

(e) carefully cooling the extruded melt to below the polymer glass-transition temperature (T_g), wherein, said cooling may be achieved by use of laminar cross-flow quench fitted with a delay tube (as described in Makansi U. S. Patent No. 4,529,368), and preferably by radially directed air (as described in Dauchert U. S. Patent No. 3,067,458), wherein the temperature (T_a) of the quench air is less than about T_g and the velocity (V_a) of the quench air is in the range of about 10 to about 30 m/min;

f) while attenuating the cooled melt to an apparent spinline strain (ε_a) in the range of 5.7 to 7.6, preferably in the range of 6 to 7.3, wherein, the apparent spinline strain ε_a is defined as the natural logarithm (ln) of the spinline extension ratio (E_R), and E_R is the ratio of the withdrawal speed (V) and the capillary extrusion speed (V_o); that is, for D_{RND} in centimeters, ε_a is given by:

$$\ln(E_R) = \ln(V/V_o) = \ln[(2.25x10^5\pi\rho)(D_{RND}^2/dpf)];$$

g) providing during attenuation the development of an apparent internal spinline stress (σ_a) in the range of 0.045 to 0.195 g/d, preferably in the range of 0.045 to 0.105 g/d for preparing spin-oriented filaments, especially suitable for draw feed yarns (DFY), characterized with tenacity-at-7%-elongation (T_7) values in the range of 0.5 to 1 g/d, and preferably an apparent internal spinline stress (σ_a) in the range of about 0.105 to about 0.195 g/d for preparing spin-oriented filaments especially suitable for direct-use yarns (DUY), characterized by tenacity-at-7%-elongation (T_7) in the range of 1 to 1.75 g/d; wherein, the apparent internal spinline stress (σ_a) is defined herein by the product of the apparent viscosity of the attenuating melt (η_m) and the spinline velocity gradient (dV/dx) at the point that attenuation is essentially complete (herein referred to as the 'neck-point'; and the apparent internal spinline stress (σ_a) is found to increase with increasing polymer LRV and withdrawal speed (V) and to decrease with increasing filament dpf, number of filaments ($\#_c$) for a given spinneret surface area (A_o cm^2) and polymer temperature (T_p); and herein is expressed by an empirical analytical relationship of the form:

$$(\sigma_a) = k(LRV/LRV_{20.8})(T_R/T_P)^6(V^2/dpf)(A_o/\#_c)^{0.7},$$

wherein k has an approximate value of $10^{-2}(\rho_m/SOC)$, where ρ_m is the density of the spin-oriented filaments (e.g., in the range of about 1.345 to about 1.385 g/cm^3, that is about 1.36 g/cm^3) and SOC is the "stress-optical coefficient" for the polyester polymer (e.g., about 0.7 in reciprocal g/d for 2GT homopolymer); T_R is the polymer reference temperature defined by ($T_M°$ + 40°C) where $T_M°$ is the zero-shear (DSC) polymer melting point; T_P is the polymer melt spin temperature,°C; V is the withdrawal speed expressed in km/min; $\#_c$ is the number of filaments (i.e., capillaries) for a given extrusion surface, A_o, expressed as $\#_c/cm^2$; LRV is the measured polymer (lab) viscosity and $LRV_{20.8}$ is the corresponding reference LRV-value (where LRV is defined herein after) of the polyester polymer having the same zero-shear "Newtonian" melt viscosity (η_o) at 295°C as that of 2GT homopolymer having an LRV-value of 20.8 (e.g., cationic-dyeable polyester of 15 LRV is found to have a melt viscosity as indicated by capillary pressure drop in the range of 2GT homopolymer of about 20 LRV and thereby a preferred reference LRV for such modified polymers is about 15.5 and is determined experimentally from standard capillary pressure drop measurements);

(h) converging the cooled and fully attenuated filaments into a multifilament bundle by use of a low friction surface, (that is, in a manner that does not abrade nor snub the filaments), such as by a finish roll, and preferably by a metered finish tip applicator (as described in Agers U. S. Patent No. 4,926,661), at a distance (L_c) from the face of the spinneret in the range of about 50 cm to about 140 cm, preferably in the range of about 50 cm to about (50+90dpf½)cm, wherein the finish is usually an aqueous emulsion of about 5% to about 20% by weight solids and finish-on-yarn is about 0.4% to about 2% by weight solids, depending on the end-use processing requirements;

(i) interlacing the filament bundle using an air jet, essentially as described by Bunting and Nelson in U. S. Patent No. 2,985,995 and by Gray in U. S. Patent No. 3,563,021, wherein, the degree of interfilament entanglement (herein referred to as rapid pin count RPC as measured according to Hitt in U. S. Patent No. 3,290,932), is selected based on yarn packaging and end-use requirements;

(j) withdrawing the multifilament bundle at a speed (V), herein defined as the surface speed of the first driven roll, in the range of 2 to 6 km/min, preferably in the range of 2 to 5 km/min, and especially in the range of 2.5 to 4.5 km/min, followed by winding up the withdrawn bundle at a speed which is 95% to 100% that of the withdrawal speed. In this case the retractive forces from aerodynamic drag are reduced by relaxing the spinline between the first driven roll and the windup roll by overfeeding in the range of about 0.5 to 5%, without the application of heat (except for use of heated interlace jet fluid (such as heated air or water-saturated air) for preventing finish deposits forming on the interlace jet surfaces as described by Harris in U. S. Patent No. 4,932,109.

The polyester fine filaments of this invention are manufactured by a simplified direct spin-orientation (SDSO) process which does not incorporate drawing or heat treatment, and therein provides a preferred balance of shrinkage and dyeability behavior making the polyester fine filaments of the invention especially suitable for replacement of natural continuous filaments, such as silk. By careful selection of SDSO process parameters fine filaments with excellent mechanical quality and uniformity are made; such that the fine filaments, having shrinkages less than 12%, may be used in multifilament direct-use yarns (DUY) and processed without forming broken filaments in high speed weaving and knitting; and filaments, having shrinkages preferably greater than about 12%, may be used in multifilament draw-feed yarns (DFY) in high speed textile draw processes, such as friction-twist texturing, air-jet texturing, stuffer-box crimping and warp-drawing, without forming broken filaments.

The fine filaments of this invention are characterized by having excellent mechanical quality permitting yarns made

from these filaments to be used in high speed textile processes, such as draw false-twist and air-jet texturing, warp drawing, draw gear and stuffer-box crimping, and air and water jet weaving and warp knitting, without broken filaments; and the filaments of this invention are further characterized by having excellent denier uniformity (as defined herein by along-end denier spread, DS) permitting use in critically dyed fabrics. The filaments of this invention may be used as filaments in draw feed yarns (and tows), preferably filaments having boil-off shrinkage (S) and dry heat shrinkage (DHS) greater than 12% are especially suitable for draw feed yarns; and filaments of this invention, having shrinkages less than 12%, are especially suitable flat untextured multifilament yarns, and as yarns for such texturing processes as air-jet texturing, gear crimping, and stuffer-box crimping, wherein, no draw need be taken, and the flat and textured filaments of this invention may be cut into staple fibers and flock; but the filaments with shrinkages less than about 12% may be uniformly cold drawn as described by Knox and Noe in U. S. Patent No. 5,066,447.

In contrast to the polyester fine filaments prepared according the invention, fine filaments made by such spinning technologies, which incorporate, for example, aerodynamic or mechanical draw and/or heat treatment steps for the reduction in filament denier and/or for the increase in molecular orientation and/or crystallinity, which are generally characterized by: 1) high shrinkage tension (ST_{max}) greater than 0.2 g/d; 2) peak shrinkage tension occurring at temperatures, $T(ST_{max})$, greater than about 100°C (i.e., greater than atmospheric dyeing temperatures); 3) dry heat shrinkage (DHS) which increases with treatment temperature over the normal textile dyeing and finishing temperature range of about 100°C to about 180°C (that is, having a $d(DHS)/dT > 0$ for T = 100°C to 180°C) and a differential shrinkage, (ΔS = DHS-S), greater than +2%, where S is the boil-off shrinkage and DHS is the dry heat shrinkage, and thereby requiring high temperature treatments of the polyester fine filaments, or textile products made therefrom, prior to, or after dyeing, to impart sufficient thermal dimensional stability to the textile fabrics made from these fine filaments; and 4) inferior dyeability, requiring dyeing under pressure at high temperatures with chemical dye assists, called carriers, to achieve deep shades and uniform dyed fabrics.

In particular, according to the present invention, there are provided:

1. Spin-oriented polyester fine filaments of 1 dpf or less, preferably less than 0.8 dpf, especially less than 0.6 dpf, and greater than 0.2 dpf; wherein said polyester is of relative viscosity (LRV) in the range of 13 to 23, with a zero-shear polymer melt temperature ($T_M°$) in the range of 240°C to 265°C, and polymer glass transition temperature (T_g) in the range of 40°C to 80°C; and said filaments are further characterized by:

   (a) a shrinkage differential, (ΔS = DHS-S), less than +2%, preferably less than +1%, and especially less than 0%; wherein, S is boil-off shrinkage and DHS is dry heat shrinkage measured at 180°C,

   (b) a maximum shrinkage tension, (ST_{max}), between 0.05 and 0.2 g/d, with the peak temperature of maximum shrinkage tension, $T(ST_{max})$, between about (T_g+5°C) and about (T_g+30°C); i.e., between about 75°C and about 100°C for poly(ethylene terephthalate) with a polymer T_g of about 70°C;

   (c) a tenacity-at-7%-elongation (T_7) in the range of 0.5 to 1.75 g/d and a $[(T_B)_n/T_7]$)-ratio at least ($5/T_7$); preferably at least about ($6/T_7$), wherein, $(T_B)_n$ is the tenacity-at-break normalized to a reference LRV of 20.8 and percent delusterant (such as TiO_2) of 0%, defined by: $(T_B)_n = (T_B)[20.8/LRV)^{0.75}](1-X)^{-4}$; where tenacity-at-break, $(T_B) = T(1+E_B/100)$; E_B, the percent elongation-at-break, is between 40% and 160%; X is the fractional weight percent of delusterant; and T is the tenacity defined as breaking load (grams) divided by original undrawn denier;

   (e) an average along-end denier spread (DS) of less than 4%, preferably less than about 3%, and especially less than 2%.

2. Spin-oriented fine filaments, especially suitable as use as draw feed yarns (DFY), such as for high speed draw false-twist and air jet texturing, draw warping, draw crimping and stuffer-box texturing, wherein, said filaments are further characterized by:

   (a) boil-off shrinkage (S) and dry heat shrinkage (DHS) greater than about 12% and less than about the maximum shrinkage potential, ($S_M = [(550-E_B)/6.5]$)%, and for elongation-at-break (E_B) in the range of 80% to 160%;

   (b) tenacity-at-7% elongation (T_7) in the range of 0.5 to 1 g/d.

3. Spin-oriented fine filaments, especially suitable for use as direct-use yarns (DUY), are further characterized by:

(a) boil-off shrinkage (S) and dry heat shrinkage (DHS) between in the range of 2% to 12%, preferably in the range of 6% to 12% for woven and preferably in the range of 2% to 6% for knits, such that the filament denier after boil-off, dpf(ABO) = dpf(BBO)x[(100/(100-S)], is in the range of 1 to 0.2 dpf, preferably in the range of 0.8 to 0.2 dpf, and especially in the range of 0.6 to 0.2 dpf;

(b) tenacity-at-7%-elongation (T_7) in the range of 1 to 1.75 g/d with an elongation-at-break (E_B) in the range of about 40% to about 90%;

(c) a post-yield modulus (M_{py}), as defined by the secant tan β in FIG. 5 (that is, $M_{py} = (1.2T_{20} - 1.07T_7)/0.13$), in the range of 2 to 12 g/d.

4. Spin-oriented fine filaments, capable of being cold drawn without heat setting to provide textile filaments, as further characterized by:

(i) a boil-off shrinkage (S) and dry heat shrinkage (DHS) less than 12%;

(ii) an onset of cold crystallization, T_{cc} (DCS), of less than 105°C, as measured by differential scanning calorimetry (DSC) at a heating rate of 20°C per minute;

(iii) an instantaneous tensile modulus, M_i (= d(stress)/d(elongation)]x100, greater than about 0; wherein [d(stress)/d(elongation)] is the tangent to a plot of stress (grams per drawn denier) versus percent elongation; and wherein draw stress is the draw force (grams) divided by the drawn denier, where the drawn denier is defined the ratio of the undrawn denier and the residual draw-ratio, ($RDR = 1+E_{B,\%}/100$);

The shrinkage (S) of said drawn filaments may be reduced, if desired, without significant loss in dyeability provided that the post heat set temperature (T_{set}) is less than about the temperature at which the shrinkage tension undergoes no significant further reduction with increasing temperature; that is, it is preferred to maintain T_{set} less than about the temperature at which the onset of rapid (re)crystallization begins. The maximum value for T_{set}, is herein, defined as the temperature, at which the slope, [d(ST)/dT], of a shrinkage tension versus temperature spectrum abruptly decreases in value (becoming less negative) - see FIG. 11.

5. Preferred drawn yarns made by drawing the said spin-oriented filaments of this invention and said drawn yarns are characterized by:

(a) denier per filament after boil-off shrinkage, dpf(ABO), in the range of 1 to 0.2 dpf, and preferably in the range of 0.8 to 0.2 dpf;

(b) boil-off shrinkages (S) and dry heat shrinkages (DHS) in the range of 2% to 12%, preferably in the range of 2% to 6% for knits, and in the range of 6% to 10% for wovens;

(c) tenacity-at-7%-elongation (T_7) at least 1 g/d, such that the $[(T_B)_n/T_7]$-ratio is at least $(5/T_7)$; preferably at least $(6/T_7)$, wherein, $(T_B)_n$ is the tenacity-at-break normalized to a reference LRV of 20.8 and percent delusterant (such as TiO_2) of 0%, and having an E_B in the range of 15% to 55%;

(e) post-yield modulus (M_{py}) in the range of 5 to 25 g/d;

(f) relative disperse dye rate (RDDR), normalized to 1 dpf, of at least 0.1, and preferably at least 0.15;

(g) a dynamic loss modulus peak temperature, T(E"max) less than about 115°C; and preferably less than about 110°C;

(h) an average along-end denier spread (DS) of less than 4%, preferably less than 3%, especially less than 2%.

6. Bulky fine filament yarns (or tows) are provided by passing the fine filament yarns of this invention through a bulking process, such as air-jet texturing, false-twist texturing, stuffer-box and gear crimping; wherein, said bulky filaments are characterized by having individual filament deniers (after shrinkage) less than 1, preferably less than 0.8, with boil-off shrinkage (S) and dry heat shrinkage (DHS) less than 12% and characterized by a $T(E"_{max})$ of less than 115°C, preferably less than 110°C, and a RDDR of at least 0.1, and preferably at least 0.15.

Especially preferred filaments for use in direct-use yarns (or tows) are also characterized by:

(a) an average crystal size (CS), as measured from the 010 plane by wide-angle x-ray scattering (WAXS), between about 50 and about 90 angstroms (Å) with a fractional volume crystallinity, $X_v = (\rho_m - 1.335)/0.12$, between about 0.2 and about 0.5 for density values (ρ_m) between about 1.355 and about 1.395 grams/cm^3, corrected for percent delusterant;

(b) an fractional average orientation function, $f = \Delta_n/\Delta_n°$ (where $\Delta_n°$ is the average intrinsic birefringence (defined herein with a value of 0.22), between about 0.25 and about 0.5, with a fractional amorphous orientation function, $f_a = (f-X_v f_c)/(1-X_v))$, less than about 0.4, preferably less than about 0.3, wherein (Δ_n) is the average birefringence and f_c is the fractional crystalline orientation function, $f_c = (180-COA)/180$, where COA is the crystalline orientation angle as measured by WAXS;

(c) an amorphous free-volume ($V_{f,am}$) of at least about 0.5x10^6 cubic angstroms (Å^3), preferably at least about 1x10^6 Å^3, where $V_{f,am}$ is defined herein by $(CS)^3[(1-X_v)/X_v)][(1-f_a)/f_a]$, providing a dynamic loss modulus peak temperature, $T(E"_{max})$, less than about 115°C, and preferably less than about 110°C;

(d) an atmospheric relative disperse dye rate (RDDR), normalized to 1 dpf, of at least 0.1, and preferably at least 0.15.

The yarn characteristics are measured as in U. S. Patent Nos. 4,134,882, 4,156,071, and 5,066,447; except the relative disperse dye rate (RDDR) is normalized to 1 dpf, dry heat shrinkage (DHS) is measured at 180C, and the lab relative viscosity (LRV) is defined according to Broaddus in U. S. Patent No. 4,712,998 and is equal to about (HRV - 1.2), where HRV is given in U. S. Patents Nos. 4,134,882 and 4,156,071. The value of $LRV_{20.8}$ is taken as the reference LRV of the polyester polymer of equal zero-shear "Newtonian" melt viscosity η_o to that of 20.8 LRV 2GT homopolymer (e.g., providing for the same capillary pressure drop at the same mass flow rate and temperature). In Tables I through VIII, alphanumerics which are "raised to the power" of a number is expressed using the symbol "^" (such as 10^2 = 10^2); very small or very large numbers (such as 0.00254 cm and 254000 cm/min, for example) are expressed, for convenience as 0.254 and 254 where the units are given as "cm x 10^2" and "cm/sec x 10^-3, respectively; dashes (---) in the place of a number denotes that the value was not measured; "NA" in the place of a number denotes that the measured value is not applicable; and dashed arrows (----->) are used to denote values of a given parameter for a given item is the same as that of the preceeding item. Spin speed (V) was measured in yards/minute and have been converted in the text to km/minute, rounded to the second decimal place (e.g., 4500 ypm = 4.115 km/min => 4.12).

The preferred embodiments of this invention are illustrated by the following examples:

Poly(ethylene terephthalate) having a polymer LRV in the range of 13 to 23 (which corresponds to an [η] in the range of 0.5 to 0.7), preferably in the range of 13 to 18 for ionically modified polyesters, and in the range of 18 to 23 for nonionically modified polyesters, a zero-shear melting point ($T_M°$) in the range of 240°C to 265°C, and a glass-transition temperature (T_g) in the range of 40°C to 80°C, and containing minor amounts of delusterants and surface friction modifiers (e.g., TiO_2 and SiO_2), is melted at a polymer temperature T_P (°C) and filtered through inert medium for a residence (hold-up) time (t_r, min) and then extruded through spinneret capillaries of diameter (D_{RND}) with length (L) at a capillary mass flow rate w [= (dpf·V)/9], g/min] providing an apparent capillary shear rate (G_a, sec^{-1} = $[(32/60\pi)(w/\rho)/D_{RND}^3)]$, where capillary dimensions are expressed in units of centimeters and the withdrawal spin speed (V) in units of km/min.

The filaments of most of the examples herein were spun from spinnerets having a filament density per extrusion surface area in the range of typically 2.5 to 13, while it was possible to spin and quench filament bundles with a extrusion filament density as high as 25 provided capillary hole pattern (filament array) was optimized for the type of quench (i. e., radial vs. cross-flow) and length/profile of the initial delay quench "shroud" and air velocity profile (see Example I); wherein the extrusion filament density is defined by the ratio of the number of filaments ($\#_c$) divided by the extrusion surface area (A_o), (i.e., $\#_c/A_o$, cm^{-2}), into a "shroud" which protects the freshly extruded filaments from direct quench air for a distance at least 2 cm and not greater than (12dpf^{½},cm); and then carefully cooled to a temperature less than about polymer T_g, preferably by radially directed air having a temperature T_a (herein about 22°C) less than about the polymer T_g (herein T_a was about 70°C for 2GT homopolymer) and of linear velocity V_a (m/min) in the range of 10 to 30 m/min. Suitable spinning apparatus used are essentially as that described in U. S. Patent Nos. 4,134,882, 4,156,071, and 4,529,368.

The along-end denier spread (DS) and draw tension variation (DTV) were minimized by balancing the values for the delay quench length (L_{DQ}), the quench air temperature (T_a), the quench air flow rate (V_a), and the convergence length (L_c), while selecting T_P for spinning continuity. Increasing the polymer spin temperature (T_P) (but less than about $[(T_M)_a + 55°C]$ usually increases spinning continuity and mechanical quality (i.e., T_B, g/d), but usually decreases along-

end uniformity and increases shrinkage. To minimize loss of along-end uniformity while spinning at elevated temperatures (T_P), as required for mechanical quality, heat can be imparted to the extruded filaments through use of high shear rate (G_a) capillaries (that is, small diameter capillaries). However, the spinning operability unexpectedly deteriorated when high shear capillaries are used with high L/D_{RND} ratios, such as use of a 9x50 mil capillary (see Example III). It is conjectured that at these low capillary mass flow rates and high shear conditions, incipient shear-induced molecular ordering (e.g., lower chain entropy and possible incipient "nucleation") of the polymer melt occurs, especially for polymer melt filtered prior to extrusion for residence times (t_r) greater than about 4 minutes, wherein this molecular ordering (possible incipient nucleation) is believed to increase the apparent polymer melting point from the zero-shear value ($T_M°$) to an apparent value $(T_M)_a$. This has the effect of reducing the spin temperature differential, $T_P-(T_M)_a$. To maintain a sufficiently large enough spin temperature differential, it is found that the bulk polymer temperature T_P needs to be further increased as given by the amount defined by the expression: $2x10^{-4}(L/D_{RND})G_a$,°C, for the selected values of L, D_{RND}, and G_a.

To obtain a balance of spinning continuity, mechanical quality and along-end uniformity, the apparent internal spinline stress (σ_a) at the "neck-point" is controlled in the range of 0.045 to 0.195 g/d while controlling the melt extension strain ε_a in the range of about 5.7 to about 7.6. The attenuated and cooled filaments are converged into a multifilament bundle and withdrawn at a spinning speed (V, km/min) as defined by the surface speed of the first driven roll. The external spinline tension arising from frictional surfaces (and air drag) is removed prior to packaging by slightly over feeding the spinline between the first driven roll and the windup, usually between about 0.5% and 5%. Finish is applied at the point of convergence and interlace is provided, preferably after the first driven roll. The values for finish-on-yarn (weight, %) and degree of filament entanglement (RPC) are selected to meet end-use processing needs.

Polyester fine filaments of the invention are of good mechanical quality and uniformity having a linear density less than about of that of natural worm silk, but greater than that of spider silk, that is between 1 and 0.2 denier per filament, and having the capability of being uniformly dyed without use of high temperatures and chemical dye assists; that is, more akin to that of natural silks.

Advantageously, if desired, the fine denier filament yarns may be treated with caustic in spin finish (according to the invention as taught by Grindstaff and Reese in the copending allowed Patent Application Serial No. 07/420,459 (US-A-5 069 844), filed October 12, 1989) to enhance their hydrophilicity and improved moisture-transport and comfort. Incorporating filaments of different deniers and/or cross-sections may be used to reduce filament-to-filament packing and thereby improve tactile aesthetics and comfort. Unique dyeability effects may be obtained by co-mingling filaments of differing polymer modifications, such as homopolymer dyeable with disperse dyes and ionic copolymers dyeable with cationic dyes.

Fine filaments of lower shrinkage may be obtained, if desired, by incorporating chain branching agents, on the order of about 0.1 mole percent, as described in part in Knox U. S. Patent No. 4,156,071, MacLean U. S. Patent No. 4,092,229, and Reese in U. S. Patents Nos. 4,883,032, 4,996,740, and 5,034,174; and/or increasing polymer viscosity by about +0.5 to about +1.0 LRV units.

The fine filament yarns of this invention are suitable for warp drawing, air jet texturing, false-twist texturing, gear crimping, and stuffer-box crimping, for example; and the low shrinkage filament yarns may be used as direct-use flat textile yarns and a feed yarns for air-jet texturing and stuffer-box crimping wherein no draw is need be taken. The filaments (and tows made therefrom) may also be crimped (if desired) and cut into staple and flock. The fabrics made from these improved yarns may be surface treated by conventional sanding and brushing to give suede-like tactility. The filament surface frictional characteristics may be changed by selection of cross-section, delusterant, and through such treatments as alkali-etching. The improved combination of filament strength and uniformity makes these filaments, especially suited for end-use processes that require fine filament yarns without broken filaments (and filament breakage) and uniform dyeing with critical dyes.

The fine denier filament polyester yarns of the invention are especially suitable for making of high-end density moisture-barrier fabrics, such as rainwear and medical garments. The surface of the knit and woven fabrics can be napped (brushed or sanded). To reduce the denier even further, the filaments may be treated (preferably in fabric form) with conventional alkali procedures. The fine filament yarns, especially those capable of being cationic dyeable, may also be used as covering yarns of elastomeric treatments yarns (and strips), preferably by air entanglement as described by Strachan in U. S. Patent No. 3,940,917. The fine filaments of the invention may be co-mingled on-line in spinning or off-line with higher denier polyester (or nylon) filaments to provide for cross-dyed effects and/or mixed shrinkage post-bulkable potential, where the bulk may be developed off-line, such as over feeding in presence of heat while beaming/slashing or in fabric form, such as in the dye bath. The degree of interlace and type/amount of finish applied during spinning is selected based on the textile processing needs and final desired yarn/fabric aesthetics.

The process of this invention and the product made therefrom is further illustrated by the following examples:

EXAMPLE I

Yarns of 100 and 300 filaments of nominal 0.5 dpf were spun from poly(ethylene terephthalate) of 19 LRV (corresponding to about 0.60 [η]) and containing 0.3 weight percent of TiO_2. The 300-filament yarns were spun using spinnerets of varying construction; e.g. so to provide: (i) 2 or more capillaries from a single counterbore without interfilament fusion by controlling the capillary-to capillary distance greater than about 40 mils (1 mm); (in) 300 "equally-spaced" single capillaries; and (iii) 300 capillaries arranged in concentric rings occupying about "initially" 50% of the "outer" half of the available extrusion surface area (A_o) so to increase the effective extrusion filament density (EFD) from about 12.5 to about 25; however, immediately after extrusion the polymer melt streams of spinneret (iii) converge to form a conical bundle similar to that of spinnerets (i) and (in); and therebyhaving an effective extrusion filament density (EFD) on the order of that for the spinneret constructions (i) and (in); i.e. less than 25 and larger than, 12.5, where the effective extrusion filament density (EFD) for such non-equally distributed filament configurations is experimentally determined following the graphical procedure in Figure 14. Experimentally, filaments equally spaced over the entire extrusion area and filaments spaced on the perimeter in concentric rings are found to have about the same effective filament extrusion density since the filaments bundles, immediately after extrusion, assume similar configurations. The data in Table I for the 300-filament yarns were spun with capillaries arranged in concentric rings occupying initially about 50% of the available extrusion surface area. The freshly extruded filaments were cooled to room temperature by using a radial quench apparatus, essentially as described in U. S. Patent No. 4,156,071, except for having a protective "shroud" of length (L_{DQ}) of about 1 inch (2.54 cm) for yarns spun at 3500 ypm (3.2 km/min) and about 2.25 inches (5.72 cm) for yarns spun at 4500 ypm (4.12 km/min). The filament yarns spun at 3500 ypm (3.2 km/min) had a high boil-off shrinkage (S), making these yarns especially suitable, for example, as draw feed yarns (DFY) in draw warping, draw air-jet texturing, draw false-twist texturing, and draw crimping. Increasing the spin speed to 4500 ypm (4.115 km/min), decreased boil-off shrinkage (S) to values less than 12% with a differential shrinkage (ΔS = DHS-S) less +2%, a maximum shrinkage tension (ST_{max}) less than 0.175 g/d at a peak temperatures $T(ST_{max})$ less than 100°C, and a yield tenacity (herein approximated by the tenacity-at-7% elongation, T_7) greater than 1 g/d, making these filaments fully suitable for direct-use applications without requiring additional drawing or heat treatment, such as use as filaments in flat, air-jet textured and stuffer-box crimped textile filament yarns.

It was observed that the filaments spun from spinneret capillaries with a cross-sectional area (A_c) of 176.8 $mils^2$ (0.1140 mm^2, $1.14x10^{-3}$ cm^2) had a lower tenacity-at-break (T_B) than the filaments spun from spinneret capillaries with an A_c of 28.3 $mils^2$ (.0182 mm^2, $1.82x10^{-4}$ cm^2). The lower tenacity of the yarns of this Example I, is also ,in part, due to the lower polymer LRV (19 vs. 20.8). The normalized values for T_B (denoted herein by $(T_B)_n$) are defined by the product the measured tenacity-at-break (T_B) and the factor $(20.8/LRV)^{0.75}(1-X)^{-4}$ which for these yarns is about 1.057; thereby, the normalized break tenacities $(T_B)_n$ are about 6% higher when compared to reference LRV and % TiO_2 of 20.8 and 0%, respectively.

The fine filament yarns of this example were capable of being dyed to deep shades at atmospheric conditions (100°C) without use of dye carriers as given by an Relative Disperse Dye rate (RDDR)-value (normalized to a 1 dpf) of about 0.16 versus an RDDR-value of 0.055 for a conventional fully drawn yarn.

To provide yarns of fewer filaments (and lower denier), it is possible to split, for example, the 300-filament yarn bundle into 2,3 or 4 individual bundles of 150, 100, and 75-filament yarn bundles, respectively, preferably by use of metered finish tip separating guides at the exit of the radial quench chamber. Multi-ending permits a higher mass flow rate (w) through the filter pack cavity and thereby reducing the residence time (t_r) in the pack cavity per threadline.

EXAMPLE II

Fine filaments were spun from poly(ethylene terephthalate) of nominal 20.8 LRV (about 0.65 [η]) and containing 0.1 weight percent TiO_2 at a withdrawal speed (V) of 4000 ypm (3.66 km/min) using a radial quench apparatus, essentially as described in Example I, except for having a delay "shroud" length (L_{DQ}) of about 2.25 inches (5.72 cm). Examples II-5 and II-6 had poor operability and no yarn was collected. The low apparent shear rates (G_a) for the 0.5 dpf filaments spun at 4000 ypm (3.66 km/min) using 15x60 mil (0.38x1.52 mm, 0.038x0.152 cm) capillaries is believed to contribute to the poor operability and broken filaments. Even increasing temperatures T_P to about 299°C did not provide an acceptable process. Temperatures higher than 299°C-300°C were not tried because of the concern for poor along-end denier uniformity. Process and product details are summarized in Table I.

EXAMPLE III

In Example III, 68-and 136-(unplied and plied) filament yarns were spun, essentially according to Example I, except convergence was by a metered finish tip as described in U. S. Patent No. 4,926,661 for Examples III-1 through III-9 and III-11 through III-25. Example III-10 used a metering finish roll surface to converge the filaments as described in

Examples I and II. Other process details are summarized in Tables I and II. The filaments of Example III-1 through III-5 and III-12 through III-15 have T_7-values greater than about 1 g/d making them especially suitable for use as filaments in direct-use textile filament yarns and as feed yarns in air-jet textured, wherein no draw is taken; and, if desired, can be drawn uniformly without heat (cold) in warp drawing (and air-jet texturing) as described in Knox and Noe U. S. Patent No. 5,066,447. The filaments of III-6,7, and III-16 through III-25 with T_7-values less than about 1 g/d are especially suitable as filaments in draw feed yarns (DFY) , such as draw false-twist texturing (FTT) and draw air-jet texturing (AJT) or as draw feed yarns in warp drawing.

In Examples III-1 through III-5, 50 denier 68-filament yarns were spun from a single pack cavity and plied at the convergence guide to give a 100 denier 136-filament yarns of excellent mechanical quality. Example III-4, for example, had a spinning continuity of 0.39 breaks per 1000 lbs. (0.86 per 1000 kg) which is equivalent to about 9.5 breaks per 10^9 meters. The yarns of Example III-4 were wound with about 10 cm interlace (as measured by the rapid pin count procedure described in U. S. Patent No. 3,290,932) for air-jet texturing on a Barmag FK6T-80 without drawing and wound with about 5-7 RPC interlace for direct-use as a flat textile yarn in wovens and warp knits. Example III-6 and 7 were drawn without broken filaments at 1.44X and 1.7X, respectively, to give drawn 35 denier 68-filament yarns. Example III-6 is preferred versus III-7 since the spinning productivity (spun denier x spin speed) of III-6 is about 25% greater than Example III-7. Yarns of Example III-6 were successfully cold warp drawn using a 1.44X draw-ratio.

It had been anticipated that increasing the L/D_{RND}-ratio of the 9 mil (0.229 mm, 0.0229 cm) capillary spinnerets from 2.22 to 5.56, as per the teaching of Frankfort and Knox in U. S. Patent No. 4,134,882, would significantly improve mechanical quality by providing for increased shear heating of the extruding polymer melt; wherein the degree of capillary shear heating was estimated by the expression in Frankfort and Knox: $660(wL/D^4)^{0.685,}°C$, wherein D is given mils, and w is given in lbs./hr.; however, broken filaments were observed for Examples III-8 and III-11.

Acceptable quality was obtained for Example III-12; wherein the residence time (t_r) during filtration in the pack cavity was reduced by spinning 136-filaments versus 68-filaments. The yarn bundle could be withdrawn as a single 136-filament bundle or split to wind-up two 68-filament yarn bundles. Residence times (t_r) less than about 4 minutes for high L/D_{RND} capillary spinnerets are found to be necessary to spin without having to use high "input" polymer temperatures (T_P). See Example IX for a more detailed discussion about the spinning with high shear capillary spinnerets. In Examples III-12 through III-15, 136-filament yarns were spun using 136-9x36 mil (0.229x0.916 mm, 0.0229x0.0916 cm) capillaries per spinneret, and thereby reducing the filtration residence time (t_r) by 50%, to provide yarns with good mechanical quality. The high filament count yarns are especially suitable for draw air-jet texturing (AJT) and for false-twist texturing (FTT), wherein, a straight draw-texturing machine configuration is preferred. Yarns from Examples III-19,22,24 and 25 were used for preparing warp drawn flat yarns of nominal 0.5 dpf as described in Example XII.

The structural properties of the filaments of Example III-10 are representative of spin-oriented filaments of this invention having shrinkages less than 6%. Example III-10 had a density ([ρ-measured = ρ-fiber - 0.0087(%TiO_2)] of 1.3667 g/cm^3 (corrected for 0.03% TiO_2), giving a calculated fractional volume crystallinity [$X_v = (\rho_m\text{-}1.335)/0.12$] of 0.264, and a weight percent crystallinity [$X_w = (1.455/\rho_c)X_v$] of 0.281; an average crystal size (CS) of 70 angstroms (Å); an average crystal orientation angle (COA) of 12 degrees which corresponds to a crystal orientation function [f_c = (180-COA)/180] of 0.93; an average birefringence (Δ_n) of 0.0744 giving an average orientation function [$f = \Delta_n/0.22$] of 0.34 and an amorphous orientation function [$fa = (f\text{-}X_vf_c)/(1\text{-}X_v)$] of 0.13 and an amorphous free-volume [$(V_{f,am}) = [(1\text{-}X_v)/X_v][(1\text{-}f_a)/f_a]CS^3$] of about $6x10^6$ cubic angstroms (Å^3). The filaments of this example also had a differential birefringence ($\Delta_{95\text{-}5}$) of 0.0113, an N_{iso} of 1.5882, a sonic velocity (SV) of 2.72 km/sec giving a sonic modulus (M_{son}) of 83.6 g/d, a maximum shrinkage tension (ST_{max}) of 0.143 g/d at a peak temperature, $T(ST_{max})$, of 80°C, a boil-off shrinkage (S) of 4.6%, giving a shrinkage modulus [$M_s = (ST_{max}/S)100$] of 3.1 g/d, a dry heat shrinkage (DHS) of 5.0% to give a differential shrinkage (ΔS = DHS-S) of less than +1%, an initial modulus of 71.6 g/d with a post-yield modulus (M_{py}) of 5.35 g/d, and an uncorrected disperse dye rate (DDR) of 0.144 and relative disperse dye rate RDDR, normalized to 1 dpf, of about 0.104.

EXAMPLE IV

Poly(ethylene terephthalate) of nominal 21.2 LRV (about 0.66 [η]) of 0.035, 0.3 and 1 weight percent TiO_2 were spun using a radial quench spinning apparatus, essentially as described in Example I, except the length (L_{DQ}) of the delay "shroud" was about 2-5/8 inches (6.7 cm), and the filament bundles were converged by a metered finish tip at 43 inches (109 cm) from the face of the spinneret. Other process details are summarized in Tables III and IV. Increasing weight percent TiO_2 is observed to decrease the tenacity-at-break (T_B) of these fine filaments. The amount of TiO_2 is usually varied between about 0.035% for minimum yarn-to-metal and yarn-to-yarn frictional needs and less than about 1.5%, more typically less than about 1% for desired mechanical quality and visual aesthetics.

EXAMPLE V

Poly(ethylene terephthalate) of nominal 21.1 LRV (about 0.655 [η]) and containing 0.3 weight percent TiO_2 was spun using apparatus similar to Example IV. Examples V-1 through V-4, IV-9 and IV-10 use 12x50 mil (0.305x1.270 mm, 0.0305x0.127 cm) spinneret capillaries. Examples V-5, 7, 8, and 11 through 13 use 9x36 mil (0.229x0.914 mm, 0.0229x0.0914 cm) spinneret capillaries, and Example V-6 uses 6x18 mil (0.152x0.457 mm, 0.0152x0.0457 cm) spinneret capillaries to spin 100-filament 85 denier feed yarns for warp draw and draw air-jet texturing (AJT). The length of delay quench (L_{DQ}) was increased from 2-5/8 inches (6.7 cm) to 4-5/8 inches (11.7 cm) in EX. V-8 and V-10. Increasing the length of delay (L_{DQ}), increased along-end non uniformity 4X and interfilament denier non uniformity, as measured optically from yarn bundle cross-sections, by 2X. When the delay length (L_{DQ}) is less than about ($12dpf^{½}$) cm, good uniformity may be obtained.

Example V-7 was repeated for Examples V-11 through V-13 at 2400, 3000, and 3500 ypm (2.2, 3.05, and 3.35 km/min); wherein, the capillary mass flow rate (w) was varied to spin a draw feed yarn such that the spun dpf would be drawn to a final denier of about 0.5 dpf [where, the drawn dpf = spun dpf/draw ratio = spun dpf x (drawn yarn RDR/spun yarn RDR), where the residual draw-ratio, RDR = (1+ E_B,%/100)]. Examples V-11 through V-13 have tenacity-at-7%-elongation (T_7) values less than about 1 g/d making them especially suitable as draw feed yarns even though the shrinkages of the undrawn yarns were less than 12%. The results of the warp drawing are summarized in Example VII.

EXAMPLE VI

In Example VI, Example V-13 was repeated at 3300 ypm (3.02 km/min) for varying spun deniers, delay quench lengths (L_{DQ}), spinning temperatures (T_P), and convergence guide lengths (L_C). Example VI-2, with a denier spread (DS) of 3.8% was successfully drawn 1.35X to give a drawn 0.3 dpf 100-filament yarn with a 2.3% denier spread, tenacity of 4.4 g/d, E_B of 32.5% and a boil-off shrinkage(S) of 6.3%. In this example it was observed that as total yarn bundle denier and individual filament denier is reduced, the along-end uniformity deteriorates unless the process is rebalanced. Increasing polymer temperature to insure good spinning continuity at these low mass flow rates is required. The along-end denier spread (DS) was improved from 12.1% (EX. VI-1) to less than 4% by reducing the delay length (L_{DQ}) to about 2.9 cm and decreasing the convergence length (L_C) from 109 cm to 81 cm. For yarns with dpf less than 0.5 it is difficult to achieve the same DS-values as for those of 0.5 to about 1 dpf. Process and product details are summarized in Tables III and IV.

EXAMPLE VII

Fine trilobal filaments were spun from poly(ethylene terephthalate) of nominal 21 LRV (about 0.65 [η] containing 0.035 weight percent TiO_2 using spinnerets with 9x36 mil (0.229x0.914 mm, 0.0229x0.0914 cm) and 12x50 mil (0.305x1.270 mm, 0.0305x0.127 cm) metering capillaries and a Y-shaped exit orifices of area (A_c) of about 197 $mils^2$ (1.27 mm^2, 0.0127 cm^2), which corresponds to a D_{RND} of about 15.9 mils (0.40 mm, 0.04 cm) with an L/D_{RND} of about 1.5 (as essentially as described in Examples 45-47 of U. S. Patent No. 4,195,051). The 9x36 mil metering capillaries provided better mechanical quality and along-end denier uniformity than the 12x50 mil metering capillaries. The 100-filament yarns could be drawn without forming broken filaments to nominal 50 denier, or about 0.5 dpf.

EXAMPLE VIII

Poly(ethylene terephthalate) polymer modified with about 2 mole % of ethylene 5-sodium-sulfo isophthate having a nominal LRV of about 15.3 was spun using a laminar cross-flow quench apparatus with a 2.2 inches (5.6 cm) delay, essentially as described in U. S. Patent No. 4,529,638, and converging the filament bundle at about 43-inches (109 cm) with metered finish tip guides. The lower LRV is usually preferred for ionically modified polyesters because the ionic sites act as cross linking agents and provide higher melt viscosity. The 15 LRV used, herein, had a melt viscosity about that of a 20 LRV homopolymer. If, however, one wanted to spin low LRV homopolymer, then typically it is advantageous to add viscosity builders, such as tetra-ethyl silicate (as described in Mead and Reese, U. S. Patent No. 3,335,211). It is generally preferred to spin ionically modified polyesters with LRV in the range of about 13 to about 18 and nonionically modified polyesters with LRV in the range of about 18 to about 23. Withdrawal speeds were increased from 2400 ypm (2.2 km/min) to 3000 ypm (2.74 km/min). As expected the cationic copolymer yarns had lower T_B-values based on their lower LRV. The lower LRV is preferred for filaments yarns used in napped and brushed fabrics and for tows to be cut into flock. The as-spun yarns could be drawn without breaking filaments to about 50 denier 100-filament yarns. The cationically modified polyester had a RDDR value of 0.225 versus 0.125 for the 2GT homopolymer spun under similar conditions.

EXAMPLE IX

Poly(ethylene terephthalate) of nominal 21.9 LRV (about 0.67 [η]) and containing 0.3 weight percent TiO_2 was spun using apparatus similar to Example IV with a air flow rate of about 30 m/min. Examples IX-1 through IX-3 use 12x50 mil (0.305x1.270 mm, 0.0305x0.127 cm) spinneret capillaries; Examples IX-4 through IX-8 use 9x36 mil (0.229x0.914 mm, 0.0229x0.0914 cm) spinneret capillaries; and Examples IX-9 through IX-11 use 6x18 mil (0.152x0.457 mm, 0.0152x0.0457 cm) spinneret capillaries to spin nominal 50 denier 100-filament low-shrinkage yarns suitable as direct-use textile yarns for warp knits and wovens and as feed yarns for air-jet and stuffer-box texturing wherein no draw is required.

It was expected that mechanical quality would improve by increasing the capillary shear rate (G_a) as taught by Frankfort and Knox in U. S. Patent No. 4,134,882. This improvement was observed for the 9x36 mil capillaries vs. the 12x50 mil capillaries; however, unexpectedly, higher polymer temperatures were required to spin with the 6x18 mil capillaries. From calculations of polymer temperature increase due to the higher shear rate (G_a), of the 6x18 mil capillaries, it was expected the 6x18 mil capillaries would actually require lower polymer temperatures (T_P) than that for the 9x36 and 12x50 mil capillaries, as per the teaching of Frankfort and Knox. However, it was necessary to increase polymer temperature by about 5-6°C to provide acceptable spinning continuity for the high shear 6x18 mil capillary spinnerets. It is speculated that at these low mass flow rates (w), the higher shear of the 6x18 mil capillaries induces molecular ordering of the polymer melt and may even induce nucleation with the effect of increasing the apparent polymer melting point $(T_M)_a$ as represented by the following empirical expression for $(T_M)_a$ as a function of capillary shear (Ga): that is, $(T_M)_a = T_M° + 2x10^{-4}[(L/D_{RND})(Ga),°C$. The differential polymer spin temperature, defined herein by:

$$[T_P-(T_M)_a] = [(T_P-T_M°)-[2x10^{-4}\ (L/D_{RND})Ga],$$

is effectively reduced as the product of the apparent shear rate (G_a) and L/D_{RND}-ratio is increased; and thereby requiring an increase in polymer temperature T_P to maintain a minimum differential spin temperature at least about 25°C and, preferably at least about 30°C for spinning continuity. This is contrary to what is expected from the teachings of Frankfort and Knox. Process and product results are summarized in Tables IV and V.

EXAMPLE X

Poly(ethylene terephthalate) of nominal 21.9 LRV (about 0.67 [η]) and containing 0.3 weight percent TiO_2 was spun using apparatus similar to Example IV with an air flow rate varied from about 11 to about 30 m/min. Examples X-1 through X-9 use 12x50 mil (0.305x1.270 mm, 0.0305x0.127 cm) spinneret capillaries and Examples X-10 through X-16 use 9x36 mil (0.229x0.914 mm, 0.0229x0.0914 cm) spinneret capillaries to spin nominal 70 denier 100-filament low-shrinkage yarns with T_7-values greater than about 1 g/d, making these especially suitable as direct-use textile yarns for warp knits and wovens and as feed yarns for air-jet and stuffer-box texturing wherein no draw is required. It was observed that mechanical quality improved with higher polymer temperatures, and lower air flow rates. Changing the convergence guide distance L_c had little effect on mechanical properties, as has been observed for higher dpf filaments (Bayer German Patent No. 2,814,104). Unfortunately the process changes which improve mechanical quality caused a deterioration in the along-end denier uniformity. Successful spinning of fine filaments with both good mechanical quality and denier uniformity requires a balance between "hot" polymer for mechanical quality and "rapid" cooling of polymer for uniformity. This in contrary to the teachings of Frankfort and Knox which wherein the combination of "hot" polymer with slow quenching by use of low quench rates, delay shrouds, and/or heated delay quench were used to provide for good quality filaments of deniers greater than 1. Balancing higher "input" polymer temperatures (T_P) with shear heating via smaller diameter capillary spinnerets and rapid quenching via short delay lengths (L_{DQ}) permits, in general, a better balance of yarn properties. Shortening the convergence length (L_c) improved the uniformity and a reduction in winding tensions as a result of lower air drag. At the higher spun deniers of Frankfort and Knox, no significant improvements are found for shortening the convergence length. Process and product results are summarized in Tables V and VI.

EXAMPLE XI

The fine filament feed yarns of Example V-11, 12, and 13 were uniformly drawn cold and at 155°C at 1.45X, 1.5X, and 1.55X draw-ratios, respectively, to give nominal 50 denier 100-filament drawn yarns that can be used as flat textile yarns. The drawn fine filament yarns have excellent mechanical quality and along-end denier uniformity with boil-off shrinkages (S) less than about 6%. The cold drawn yarns had slightly less shrinkage than the hot drawn yarns and also were slightly more uniform. With less interlace levels and a different finish, these yarns may be cold drawn air-jet

textured, consistent with the teachings of Knox and Noe in U. S. Patent No. 5,066,447. These fine filament spun yarns could also be used as feed yarns for draw air-jet/stuffer-box/friction-twist texturing. Warp draw process and product details are summarized in Table VII.

EXAMPLE XII

Examples III-20 through 25 were repeated by varying spin speed and spun denier to provide draw feed yarns capable of being drawn to provide 35 denier 68-filament yarns. Nominal 50 to 60 denier as-spun yarns with excellent mechanical quality and denier uniformity were drawn cold and heat set at 160°C to 180°C to obtain low shrinkage filaments of nominal 0.5 dpf yarns without loss in mechanical quality and along-end denier uniformity. Spin process and product details are summarized in Tables IV and V, and the corresponding draw process and product details are summarized in Table VII.

EXAMPLE XIII

In Example XIII the ability to obtain high T_7 fine filament yarns was explored. Spinning apparatus similar to that in Example X was used. Poly(ethylene terephthalate) of nominal 20.8 LRV (0.65 [η]) containing 0.3 weight percent TiO_2 was extruded through 9x36 mil (0.229x0.914 mm, 0.0229x0.0914 cm) spinneret capillaries and cooled using a radial quench apparatus as described in Example I, except for having a delay length L_{DQ} of about 2.25 inches (5.7 cm). The cooled filaments were converged into yarn bundles at a convergence length (L_c) of about 32 inches (81.3 cm) from the face of the spinneret by use of metered finish tip guides. The withdrawal speed (V) was varied from 4500 ypm (4.12 km/min) to 5300 ypm (4.85 km/min) to provide 68 and 100-filament direct-use textile yarns with T_7-values between about 1 and 1.5 g/d. The process and product details are summarized in Table VI. The tensiles of Example XIII were inferior due to use of lower polymer melt temperature (T_P) and higher quench air flow rates (V_a) than in Example X.

EXAMPLE XIV

A 91 denier 100-filament yarn made according to Example IV was air-jet textured using a Barmag FK6T80 at 300 km/min; wherein, the as-spun yarns were drawn cold (about 40°C) at 1.0X, 1.1X, 1.2X, and 1.32X draw-ratios and sequentially air-jet textured using a conventional air-jet at 125 lbs./in^2 (8.8 kg/cm^2) to provide bulky yarns with filament deniers between about 0.7 and 0.9 (before boil-off shrinkage) and between about 0.77 and 0.94 dpf (after boil-off shrinkage). The denier of the textured filament yarn, wherein no draw was taken, showed an increase in yarn denier of about 11% due to bulk (e.g., filament loops), where the ratio $(denier)_{AJT}/(denier)_{FLAT}$ is preferably greater than about 1.1); however, the filament denier showed no increase in denier. Textured yarn strengths, as expected, were lower than that of a drawn flat yarn due to the filament loops; but are adequate for bulky fabric end-uses. Even at a 1.32X draw-ratio, giving a textured yarn with a 27.2% residual elongation (corresponding to a 1.27 residual draw ratio RDR), the boil-off (S)and dry heat (DHS) shrinkages were only about 12.7% and 11%, respectively, with a shrinkage shrinkage (ΔS = DHS-S) less than about (1.7%). With heat setting these shrinkages can be reduced to about 2%, if desired. Example XIV-1 and 2 were uniformly cold partially drawn, as defined herein, by providing a RDR of at least about 1.4X in the drawn yarn. The capability of these fine filaments to be uniformly partially drawn is attributed to the crystalline structure of the as-spun filaments providing a thermal shrinkage less than about 12%, preferably less than about 10%, and especially less than about 8%, as per Knox and Noe in U. S. Patent No. 5,066,447. In Example XIV-5 through 8, 68-filament yarns were sequentially draw cold and air-jet textured. The shrinkage increased with draw ratio, providing a route to higher shrinkage AJT yarns. The process and product data for Example XIV is given in Table VIII.

Co-mingling (plying) 2 or more cold drawn AJT yarn textile yarns, wherein at least one AJT yarn has been heat set to shrinkages less than about 3%, and a second AJT yarn has not been heatset, so has significantly higher shrinkage, provides a simplified route to a mixed shrinkage yarn. Similar mixed shrinkage AJT yarns may be provided with the lower shrinkage component provided by alternate techniques, for instance by hot drawing, with or without heat setting. Alternatively, mixed shrinkage AJT yarns may be provided by co-mingling 2 or more drawn filament bundles wherein both bundles are drawn by cold drawing, without post heat treatment, but the bundles are cold drawn to different elongations, preferably by about 10% or more. The resulting mixed shrinkage drawn yarn may be AJT to provide a mixed shrinkage textured (bulked) yarn. Incorporating filaments of different deniers and/or cross-sections may also be used to reduce filament-to-filament packing and thereby improve tactile aesthetics and comfort. Unique dyeability effects may be obtained by co-mingling drawn filaments of differing polymer modifications, such as homopolymer dyeable with disperse dyes and ionic copolymers dyeable with cationic dyes. AJT process and product details are summarized in Table VIII.

EXAMPLE XV

In Example XV yarns were spun for use as draw feed yarns (DFY)in false twist texturing (FTT). Example XV-1, a nominal 58 denier 68-filament yarn was textured at 500 m/min on a L900 PU machine with a 1.707 D/Y-ratio at a 1.628X draw to provide 68-filament textured yarns of nominal 37 denier (0.54 dpf) with a tenacity (T) of 4.1 g/d, an elongation-at-break (E_B) of 26.8%, a tenacity-at-7%-elongation (T_7) of 2.19 g/d, and an initial modulus (M) of 44.6 g/d. In Example XV-2 a nominal 118 denier 200-filament draw feed yarn was prepared for false twist texturing, as in Example XV-1, except with a D/Y-ratio of 1.59 at a 1.461X draw-ratio to provide 200-filament textured yarns of 83.5 nominal denier (0.42 dpf) with a tenacity (T) of about 3.25 g/d and an elongation-at-break (E_B) of about 23.9%. The 200-filament yarns were also successfully "partially" warp drawn as per the teachings of Knox and Noe in U. S. Patent No. 5,066,447 with a 1.49X draw-ratio to provide a nominal 79.6 denier 200-filament flat yarn having a 4.81 g/d tenacity and a 45.1% elongation-at-break (E_B). In Example XV-3 a nominal 38 denier 100-filament yarn was prepared for use as a draw feed yarn in false-twist texturing and in warp drawing. The process operability for Example XV-3 was better with 6x18 mil (0.152x0.457 mm) capillaries than with 9x36 mil (0.229x0.914 mm) capillaries. The yarns of Example XV-3 were warp drawn over a range of conditions in Example XVIII to provide 0.22 to 0.27 dpf 100-filament yarns for wovens and knit fabrics.

EXAMPLE XVI

In Example XVI 21.2 LRV polyester polymer containing 0.035 weight percent TiO_2 was extruded at 285°C through 9x36 mil (0.229 x 0.914 mm) metering capillaries with a four-diamond-shaped corrugated ribbon cross-section exiting orifice of area 318 $mils^2$ (0.205 mm^2). The 80 denier 100-filament bundles were quenched using radial quench apparatus similar to that used in Example III having a delay length of 2.9 cm and converged by a metered finish tip applicator at 109 cm from the face of the spinneret and withdrawn at a spin speed of 2350 ypm (2.15 km/min). Yarns quenched with 47.5 mpm room temperature air had a along-end denier spread (DS) of about 1.6-1.8%, a BOS of about 2.8%, an average elongation-at-break (E_B) of 92.9% , an average tenacity-at-break (T_B) of 4.56 g/d to give a $(T_B)_n/T_7$-ratio of about 4.3. Decreasing quench air velocity to 21.7 m/min increased the T_B to about 4.64 g/d with a $(T_B)_n/T_7$-ratio of about 4.5. The lower T_B-values (i.e., less than about 5) are a consequence of the corrugated filament cross-sectional shape and such filaments may be used in processes, such as false-twist texturing (FTT) and air-jet texturing (AJT) where filament fracture is desired to give even finer filaments (i.e., even less than about 0.2 dpf) for a more spun-like aesthetics.

EXAMPLE XVII

In Example XVII nominal 43 denier 50-filaments with a concentric void of about 16-17% were spun at 3500 ypm (3.2 km/min) and at 4500 ypm (4.12 km/min). The hollow filaments were formed by post-coalescence of nominal 21.2 LRV polymer at 290°C using segmented capillary orifices with 15x72 mil (0.381x1.829 mm) metering capillaries as essentially described by Champaneria etal in U. S. Patent No. 3,745,061, Farley and Barker in Br. Patent No. 1,106,263, Hodge in U. S. Patent No. 3,924,988 (Figure 1), Most in U. S. Patent No. 4,444,710 (Figure 3), in Br. Pat. Nos. 838,141, and 1,106,263. The geometry of the entrance capillary (counterbore) to the segmented orifices was adjusted to optimize the extrudate bulge and minimize pre-mature collapse of the hollow melt spinline. The ratio of the inner and outer diameters of the circular cross-section formed by the segmented orifices was adjusted to provide percent void content greater than about 10% and preferably greater than about 15%. The void content is found to increase with extrusion void area ($\pi ID^2/4$), mass flow rate, polymer melt viscosity (i.e., proportional to LRV/T_P) and with increasing withdrawal speed (V) and the above process parameters are selected to obtain at least about 10% and preferably at least about 15% void content (VC). For example the fine hollow filaments were quenched using radial quench apparatus fitted with a short delay shroud as described in Example XVI, except air flow was reduced to about 16 m/min and converged via a metered finish tip applicator at a distance less than about 140 cm. The yarns spun at 3.2 km/min had tenacity/elongation/modulus of about 3 gpd/90%/45 gpd, respectively and a tenacity-at-7%-elongation (T_7) of about 0.88 g/d. Yarns spun at 4.115 km/min had tenacity/elongation/modulus of about 2.65 gpd/46%/64 gpd, respectively, and a tenacity-at-7%-elongation (T_7) of about 1.5 g/d. Yarns spun at 3.2 and 4.12 km/min had boil-off shrinkage (S) values between about 3-5%.

EXAMPLE XVIII

In Example XVIII, the spun yarns of Example XV-3 were drawn over a range of draw-ratios from 1.4X to 1.7X to provide drawn filament yarns of deniers 26.6 to 22.2, respectively; with tenacities increasing from 4.38 g/d to 5.61 g/d and elongations-at-break (E_B) decreasing from 36.6% to 15.8% with increasing draw-ratio. All the draw yarns had

boil-off shrinkages (S) of about 4%. See Table VIII for process and product summery.

EXAMPLE XIX

In Example XIX-1 and XIX-2, 200-filament and 168-filament yarns (feed yarns from Example XV-3 and 4, repsectively) of nominal 0.5 dpf were spun at 4400 ypm (4.02 km/min) for use as direct-use flat yarns in woven and knit fabrics. These yarns can also be air-jet textured (AJT) without draw to provide low-shrinkage AJT yarns of nominal 3% shrinkage.

EXAMPLE XX

In Example XX mixed filament yarns were prepared by co-spinning sub denier filaments of the invention with higher denier filaments, such as the low shrinkage filaments as described by Knox in U. S. Patent No. 4,156,071 and/or the high shrinkage filaments described by Piazza and Reese in U. S. Patent No. 3,772,872 to provide the potential for mixed-shrinkage (e.g., post-bulking in fabric) such as in the case when the low shrinkage filaments of this invention are combined with the high shrinkage filaments of Piazza and Reese. On-line thermal treatment by use of a heated tube or a steam jet, wherein essentially no reduction in filament denier takes place (i.e., no space drawing) of mixed dpf low shrinkage filament yarns, such as those prepared by co-spinning filaments of this invention with those as described by Knox in U. S. Patent No. 4,156,071, provides a route to unique mixed shrinkage post-bulkable filament yarns wherein the shrinkage of the sub denier filaments of this invention remain essentially unchanged while the shrinkage of the higher denier filaments (e.g., 2-4 dpf) is increased from initial boil-off shrinkage (S) of less than about 6-10% to greater than 10%, typically about 15-35%. The mixed shrinkage yarns prepared with the mentioned intermediate heat treatment differ from those obtained by combining the low shrinkage filaments of this invention with the higher shrinkage filaments of Piazza and Reese in that the heat treated high shrinkage filaments have significantly improved shrinkage tension (e.g., at least about 0.15 g/d) which permits development of the bulk from the mixed-shrinkage even in very tightly constructed woven fabrics.

The combination of high shrinkage and high shrinkage tension (herein called shrinkage power) was heretofore only obtained, for example, by fully drawing conventional LOY/MOY/POY followed by no or low temperature annealing. The sub denier filaments of the invention migrate to the surface on mixed shrinkage and provide a soft luxurious tactile aesthetics even in the most tightly constructed fabrics. The heat treatment is typically carried out after the filaments are fully attenuated and quenched to below their glass transition temperature and in a manner that the increase in tension during the heat treatment is of the magnitude equal to that of the observed increase in shrinkage tension by said heat treatment. Selecting heat treatment conditions greater than about the cold crystallization temperature T_{CC} (DSC), (typically about 95 to about 115°C) and less than about the temperature of maximum crystallization T_C (typically about 150 to about 180°C for most polyesters) gives high shrinkage tension filaments of excellent dyeability (e.g., high RDDR), while treatment under temperatures greater than T_C gives high shrinkage tension filaments of reduced dyeability. The filaments may be heated either by passing through high pressure superheated steam (e.g., 40-140 psi at about 245°C) or by passing through a heated tube. The high and low dpf filaments may be spun from separate pack cavities and then combined to form a single mixed-dpf filament bundle or may be spun from a single pack cavity, wherein the capillary dimensions (L and D) and the number of capillaries $\#_c$ are selected to provide for differential mass flow rates; e.g., by selecting capillaries such that the ratio of spun filament deniers, $[(dpf)_b/(dpf)_a]$, is approximately equal to $[(L_aD_b/L_bD_a)^n \times (V_a/V_b) \times (D_b/D_a)^3]$, where a and b denote filaments of differing deniers; n = 1 for Newtonian polymer melts (and herein determined experimentally from convetnional capillary pressure drop tests) and that the measured average dpf = $[(\#_a dpf_a + \#_b dpf_b)/(\#_a + \#_b)]$. The above heat treatment process can also be used to increase the lower shrinkage of the sub denier filaments of the invention as defined by the needs of the particular end-use, such as increasing from about 3% to about 6-8% with higher shrinkage tension (and shrinkage power) for tightly constructed wovens.

EXAMPLE XXI

In Example XXII 50 denier 68-filament undrawn flat textile yarns were uniformly cold drawn and heat treated at 160, 170, and 180°C to provide nominal 36 denier 50 filament drawn yarns of about 4-5% boil-off shrinkage (S) with a T_7 of about 3.5 g/d, a tenacity of about 4.5 g/d with an elongation-at-break (E_B) of about 27%. The drawn yarns have a percent Uster of about 2.1-2.4% and may be used for critically dyed fabrics.

EXAMPLE XXII

The fine denier filaments of this invention may be used to cover elastomeric yarns (and tapes) by high speed air-

jet entanglement as taught by Strachan in U. S. Patent No. 3,940,917. Polyester fine filaments prepared from polymer modified for cationic dyeability are especially suitable for elastomeric yarns, such as Lycra® to prevent "bleeding" of the dyestuff from the elastomeric yarns, such as observed for Lycra® covered with homopolymer polyester dyed with nonionic disperse dyes. The direct-use filaments of this invention are preferred (and those with increased shrinkage, shrinkage tension, and shrinkage power as described in Example XX are especially preferred) for air-entanglement covering and permit the covered elastomeric yarns to be dyed under atmospheric conditions without the use of carriers, e.g., similar to the dye bath conditions to dye nylon filament covered elastomeric yarns (except for being dyed with anionic acid dyes).

Some example fabrics made from the yarns of the invention are: 1) a medical barrier fabric constructed with a low shrinkage 70 denier 100-filament direct-use flat yarn filling and a 70 denier 34-filament conventional warp drawn POY in the warp and woven on a high speed water-jet loom at 420 picks per minute to give a plain weave fabric of 164 ends per inch in the warp and 92 picks per inch in the fill; 2) a lounge wear satin constructed using the above 70 denier 100-filament direct-use yarn in the warp and combining it with a 60 denier 100-filament false twist textured fill to provide a satin with 172 ends per inch in the warp and 100 picks per inch in the fill; and 3) a crepe de chines fabric constructed with the above 70 denier 100-filament direct-use yarn in the warp and a 2-ply 60 denier 100-filament false twist textured yarn in the fill.

For convenience the symbols, conversions, and analytical expressions used herein before are listed below:

PET	Poly(ethylene terephthalate)
2GT	PET
TiO_2	Titanium dioxide
SiO_2	Silicon dioxide
$(\ )_f$	"of the fiber"
$(\ )_p$	"of the polymer"
$(\ )_m$	"measured"
dpf	Denier per Filament (1 gram/9000 meters)
dpf(ABO)	DPF after boil-off shrinkage
dpf(BBO)	DPF before boil-off shrinkage
DS	Along-end % Denier Spread (±3 sigma)
DTV	Draw tension variation (%)
$[\eta]$	Intrinsic Viscosity (IV)
LRV	Relative Viscosity (Lab)
IV	Intrinsic Viscosity
$LRV_{20.8}$	LRV of the polyester polymer having the same melt zero-shear Newtonian melt viscosity as homopolymer (unmodified 2GT) of 20.8 LRV at 295 degrees centigrade (C)
C	Degrees centigrade
η_a	Apparent melt viscosity (poise)
η_o	Melt viscosity as shear rate -> 0
X	Weight fraction of delusterant
$T_M°$	Zero-shear polymer melting point (°C)
$(T_M)_a$	Apparent melting point of polymer (°C)
T_g	Polymer glass-transition temp.(°C
T_P	Polymer melt spin temperature (°C)
T_a	Quench air temperature (°C)
T_s	Spinline surface temperature
t_r	Filtration residence time (min)
w	Capillary mass flow rate (gpm)
q	Capillary volume flow rate (cm^3/min)
Q	Spin pack flow rate (gpm)
$\#_c$	Number of filaments per spin pack
V_F	Spin pack (filled) free-volume (cm^3)
L	Capillary Length (cm)
L/D_{RND}	Capillary Length-Diameter Ratio
D_{RND}	Capillary Diameter equal to round capillary of equal x-section area (A_c)
D_{ref}	Diameter of reference spinneret
D_{sprt}	Diameter of test spinneret
A_c	Capillary cross-sectional area (cm^2)
G_a	Apparent capillary shear rate (sec^{-1})

ε_a	Apparent spinline strain
E_R	Apparent spinline extension ratio
EFD	Extrusion filament density
dV/dx	Velocity gradient
σ_a	Apparent internal spinline stress (g/d)
V_a	Quench air laminar velocity (m/min)
L_{DQ}	Quench delay length (cm)
L_c	Convergence length (cm)
V_c	Spin speed at convergence (km/min)
V	Spin (withdrawal) speed (km/min)
V_o	Capillary Extrusion velocity (m/min)
A_o	Spin pack extrusion area (cm^2)
dV/dx	Spinline velocity gradient (min^{-1})
η	Melt viscosity (poise)
DQ	Delay quench
$(\ )_N$	Measured at the "neck" point
ypm, y/min	yards per min
mpm, m/min	meter per min
gpm, g/min	grams per min
ρ_m	Measured fiber density (g/cm^3)
ρ_c	Fiber density corrected for delusterant
ρ_a	Amorphous density (1.335 g/cm^3)
ρ_x	Crystal Density (1.455 g/cm^3)
X_v	Volume fraction crystallinity
X_w	Weight fraction crystallinity
S	Percent boil-off shrinkage
DHS	Percent dry heat shrinkage
ΔS	Shrinkage Differential (DHS-S)
S_m	Maximum shrinkage potential (%)
ST	Shrinkage Tension (g/d)
ST_{max}	Maximum shrinkage tension (g/d)
$T(ST_{max})$	Shrinkage tension peak temperature (°C)
P_S	Shrinkage power (g/d) (%)
T_{SET}	Maximum set temperature
Mi	Instantaneous tensile modulus (g/d)
M	Initial (Young's) tensile modulus (g/d)
M_{py}	Post yield modulus (g/d)
T_7	Tenacity-at-7%-elongation (g/d)
T_{20}	Tenacity-at-20%-elongation (g/d)
T	Tenacity (g/d)
T_B	Tenacity-at-break (g/dd)
$(T_B)_n$	Normalized T_B (g/d)
gpdd, g/dd	Grams per drawn denier
gpd, g/d	Grams per (original undrawn) denier
SF	Shape Factor (= P_M/P_{RND})
P_M	Measured perimeter (P)
P_{RND}	P of round filament of equal area
RDDR	Relative Disperse Dye Rate ($min^{1/2}$)
DDR	Disperse Dye Rate ($min^{1/2}$)
RDR	Residual Draw-Ratio
1.abX	Draw-ratio of value "1.ab", for example
E_B	Elongation-at-Break (%)
tan α	Secant post-yield modulus (g/d)
tan β	Tangent post-yield modulus (g/d)
Δ_n	Birefringence
Δ_a	Birefringence of amorphous regions
Δ_c	Birefringence of crystalline regions
Δ^o	Intrinsic Birefringence

SOC	Stress-Optical Coefficient $(gpd)^{-1}$
f_a	Amorphous orientation function
f_c	Crystalline orientation function
COA	Crystal orientation angle (WAXS)
LPS	Long Period Spacing (SAXS, Å)
CS	Average (WAXS, 010) crystal size (Å)
Tcc (DSC)	DSC- cold crystallization temp., (°C)
T(E"max)	E" peak temperature (T_α)
E"	Dynamic loss modulus (g/d)
M_{son}	Sonic Modulus (g/d)
M_S	Shrinkage Modulus (g/d)
SV	Sonic velocity (km/min)
$V_{f,am}$	Amorphous free-volume ($Å^3$) (1 $Å^3$ = $1x10^{-3}$ nm^3)
Å	Angstroms (= 0.1 mm)
mil	0.001 inches = .0254 mm = 25.4 microns
μ	Micron (10^{-6} m = 10^{-4} cm = 10^{-3} mm)
km/min	kilometers/min = 10^3 meters/minute
A	Hydrocarbylenedioxy units [-O-R'-O-]
B	Hydrocarbylenedicarbonyl units [-C(O)-R"-C(O)-]
R', R"	hydrocarbylene group
C,H,O	Carbon, hydrogen, and oxygen
-O-	"Oxy" (ether) linkage
-C(O)-	Carbonyl group
RPC	Rapid Pin Count
FOY	Percent weight finish-on-yarn
AJT	Air-jet texturing
LOY	Low-oriented yarns
MOY	Medium-oriented yarns
HOY	Highly oriented yarns
POY	Partially-oriented yarns
SOY	Spin-oriented yarns
DUY	Direct-use yarns
FDY	Fully drawn yarns
PBY	Post-bulkable yarns
WDFY	Warp draw feed yarn
DFY	Draw feed yarn
DTFY	Draw texturing feed yarn
FTT	False-twist texturing
SBC	Stuffer-box crimping
SBT	Stuffer-box texturing
SDSO	Simplified direct spin-orientation
WAXS	Wide-angle x-ray scattering
SAXS	Small-angle x-ray scattering
DSC	Differential Scanning Calorimetry
RAD	Radial quench
XF	Cross-flow quench
DT	Draw tension (gpd)
DTV	Draw tension variation (%)
IFDU	Interfilament denier uniformity
RND	Round
TRI	Trilobal
RIB	Ribbon
HOL	Hollow
ABO	After boil-off shrinkage
BBO	Before boil-off shrinkage
RV	Relative Viscosity
FVC	Fractional void content
EVA	Extrusion void area

ID	Inner diameter
OD	outer diameter
d	diameter of filament (cm)
N_{iso}	Isotropic index of refaction
HRV	LRV + 1.2
RV	1.28(HRV)
$(\eta_o)_{2GT}$	$[0.0653(LRV + 1.2)^{3.33}]$ at 295°C
$(\eta_o)Tp$	$(\eta_o)_{295°C}$ x (295/Tp)6
ft^3	0.0284 m^3
μ (micron)	10^{-4} cm
mil (0.001")	$2.54x10^{-3}$ cm = 25.4 microns
m/min	0.9144 yd/min
dpf	1 gram/9000 meters
g/min	0.132 pph
d(cm)	$11.89x10^{-4}$ $(dpf/\rho)^{½}$
$(T_M)_a$	$(T_M)° + 2X10^{-4}(L/D)G_a$, °C
G_a (sec^{-1})	$(32/60\pi)(w/1.2195)(1/D_{RND})^3$, ^{sec}-1
t_R (min)	$[1.2195\ V_F(cm^3)]/(w\ \#_c)$, min
σ_a	$10^{-3}(\rho/SOC)(LRV/LRV_{20.8})(T_R/T_P)^6\ [V^2/dpf][A_o(cm)/\#_c]^{0.7}$, g/d
E_R	$V/V_o = 2.25x10^5(1.2195\pi)(D_{RND}^2/dpf)$
ε_R	$Ln(E_R)$
T_s	$660(wL/D^4)^{0.685}$, °C; wherein W = pph and L and D are in mils
T_R	$(T_M)_a$ + 40°C
w	dpf V(mpm)/9000 = dpf V(km/min)/9, g/min
D_{RND}	$2(A_c/\pi)^{1/2}$, cm
X_v	$(\rho-\rho_a)/(\rho_c-\rho_a)$
X_w	$(\rho_c/\rho)X_v$
ρ_c	1.455 g/cm^3
ρ_a	1.335 g/cm^3
ρ_{cor}	$\rho_{measured}$ - 0.0087(%TiO_2), g/cm^3
ΔS	(DHS,% - S,%)
S_M	$(550-E_{B,\%})/6.5$, %
M_{py}	$(1.2T_{20} - 1.07T_7)/(1.2-1.07)$, g/d
T_B	(Tenacity,T)(RDR), g/d
RDR	$(1 + E_{B,\%}/100)$,
$(T_B)_n$	T_B x $LRV^{0.75}(1-X)^{-4}$
Δ_n	$\Delta_c + \Delta_a = \Delta°[X_v f_c + (1-X_v)f_a]$
f_c	(1 - COA/180)
f	$\Delta_n/\Delta° = ½(3<cos>^2-1)$
Δ°	0.220
SOC	$\Delta_n/\sigma_a = 0.7\ (g/d)^{-1}$
$V_{f,am}$	$CS^3[(1-X_v)/X_v][1-f_a)/f_a]$, $Å^3$
ΔP =	$4(L/D_{RND})^n\eta_a G_a$, n = 1 for Newtonian melts and as G_a -> 0
$(dpf)_b(dpf)_a$	$[(L/D)_a/(L/D)_b]^n[(V_a/V_b)(D_b/D_a)^3$
ΔP	$4(L/D)\eta_a G_a = 4(L/D)\tau_{wall}$
τ_{wall}	$\eta_a G_a$
G_a	$(32/\pi\rho)(w/D^3)$, sec^{-1}
V_o	(w/ρ)/(Area), cm/min
g/d	1.0893N/dtex
1 g	$0.9804x10^3$ dynes
1 N	10^3 dynes
PSI	0.0703 kg/cm^2
g/cm^2	$0.9(\rho)(g/d) = (\rho)(g/dtex)$
EVA	$\pi(ID^2/4)$
FVC	$(ID/OD)^2$
P_S	(ST, g/d)x(S,%)
ABO	BBO[100/(100-S)]

Referring to Table I which follows, Examples 1-2, 1-4, 2-6, 5-6, 5-8 and 5-10 are Comparative.

TABLE I

EX.-ITEM	1-1	1-2	1-3	1-4	2-1	2-2	2-3	2-4	2-5	2-6	3-1	3-2	3-3	3-4	3-5	3-6	3-7	3-8	3-9	3-10	3-11
POLYMER																					
LRV	19	---------->			20.8	---------->					21.2	---------->								20.8	21.2
TiO2,%	.30	---------->			.10	---------->					.035	---------->								.030	.035
FIL/YARN																					
dpf	.53	.52	.49	.51	.74	.99	.94	.75	.63	.50	.73	---------->					.88	.51	.76	.49	.51
# Fils	300	100	300	100	68	100	80	100	80	100	68	---------->									
Yarn Denier	150	51.7	148	50.6	50	99	75	75	50	---------->							60	35	51.5	33	35
EXTRUSION																					
TP, °C	290	290	295	295	299	301	300	--->	299	--->	288	---------->				289	289	300	288	294	290
#/Ao, cm^-2	12.6	4.2	12.6	4.2	2.8	4.2	3.3	4.2	3.3	4.2	2.8	---------->									
w, g/min	.188	.185	.225	.233	.300	.402	.382	.305	.256	.203	.282	.297	.312	.326	.341	.282	.224	.233	.332	.224	.241
q, cm^3/min	.155	.152	.185	.191	.246	.330	.313	.250	.210	.167	.231	.244	.256	.268	.280	.231	.184	.191	.272	.184	.198
tr, min	1.05	3.22	0.88	2.57	2.93	1.48	1.96	1.96	2.92	2.93	3.12	2.95	2.81	2.69	2.57	3.12	3.92	3.77	4.11	3.92	3.64
L, mils	9	60	9	60	---------->						20	---------->						50	---------->		
L, cm x10	.229	1.52	.229	1.52	---------->						.508	---------->						1.27	---------->		
DRND, mils	6	15	6	15	---------->						9	---------->									
DRND, cm x10	.152	.381	.152	.381	---------->						.229	---------->									
L/DRND	1.5	4	1.5	4	---------->						2.22	---------->						5.56	---------->		
AC, mil^2	28.3	176.8	28.3	176.8	---------->						63.6	---------->									
AC,cm^2 x10^3	.182	1.14	.182	1.14	---------->						.411	---------->									
Ga, sec^-1	7389	465	8844	586	755	1011	961	767	644	511	3284	3459	3634	3797	3971	3284	2609	2714	3867	2609	2807
(L/DRND)Gax10^-1	1108	186	1327	234	302	404	384	397	258	204	729	658	807	842	471	729	579	1509	2151	1451	1561
k(L/DRND)Ga,°C	2.2	0.4	2.7	0.5	0.6	0.8	0.7	0.8	0.5	0.4	1.4	1.3	1.6	1.7	0.9	1.4	1.2	3.0	4.3	2.9	3.1
QUENCHING																					
LDQ, cm	2.5	2.5	4.8	---->	5.7	---------->					6.7	---------->									
12/dpf, cm	8.7	8.7	7.6	8.6	10.1	11.9	11.6	10.4	9.5	8.5	10.3	---------->					11.3	8.6	10.5	8.4	8.6
Va, m/min	21.3	---------->			---------->						13.1	---------->				16.3	--->	21.3	--->	18.9	13.1
Lc, cm	137	---------->			---------->						109	---------->									
50+90/dpf,cm	116	115	117	114	126	140	137	128	121	114	127	---------->					135	115	129	113	114
SPINNING																					
V, y/min	3500	3500	4500	4500	4000	---------->					3800	4000	4200	4400	4600	3800	2500	4500	4300	4500	4650
V, m/min	3200	3200	4115	4115	3658	---------->					3475	3658	3841	4024	4206	3475	2286	4115	3932	4115	4252
ER(=V/Vo)	378	2407	409	2455	1692	1265	1332	1669	1987	2504	617	---------->					512	884	593	920	884
εo [=ln(ER)]	5.93	7.79	6.01	7.81	7.43	7.14	7.19	7.42	7.59	7.83	6.43	---------->					6.24	6.78	6.39	6.82	6.78
εo·T7, g/d	5.34	9.82	7.03	10.3	6.76	5.89	6.04	7.20	---	---	6.43	6.94	7.59	8.36	9.00	5.79	3.18	---	6.90	9.34	8.81
YARN																					
S, %	55	35	11.2	7.4	25	11	7	12	---	---	---	---	---	2.9	---	3.7	---	---	3.3	4.6	---
Mi, g/d	43	55	59	65	45	37	36	38	---	---	---	---	---	---	---	---	---	---	---	71.6	---
T7, g/d	0.90	1.26	1.17	1.32	0.91	0.84	0.84	0.97	---	---	1.00	1.08	1.18	1.30	1.40	0.90	0.51	---	1.08	1.37	1.30
EB, %	85	63	76	62	66	81	86	77	---	---	101	94.1	94.2	87.4	79.6	99.7	136.8	---	---	54.5	71.0
T, g/d	3.0	3.1	3.6	3.4	3.1	3.3	3.4	3.5	---	---	3.14	3.12	3.21	3.12	3.09	3.29	2.98	---	---	3.02	2.97
TB, g/d	5.55	5.05	6.34	5.51	5.15	5.97	5.58	6.20	---	---	6.32	6.06	6.23	5.85	5.55	6.57	7.06	---	---	4.67	5.08
(TB)n, g/d	5.77	5.57	6.87	5.97	5.17	6.00	5.60	6.23	---	---	6.23	5.98	6.11	5.77	5.47	6.48	6.96	---	---	4.69	5.01
(TB)n/T7	6.41	4.42	5.87	4.52	5.68	7.14	6.66	6.42	---	---	6.23	5.53	5.17	4.43	3.90	7.20	13.6	---	---	3.42	3.85
DS,%	---	---	---	---	3.5	2.7	2.0	3.5	---	---	1.24	1.22	1.26	1.26	1.35	1.69	1.56	---	1.3	---	1.42
DTV, %	---	---	---	---	---	---	---	---	---	---	0.29	0.21	0.26	0.26	0.21	0.34	0.50	---	1.0	---	0.37
BFS	NO	NO	NO	NO	NO	NO	NO	NO	YES	YES	NO	NO	NO	NO	NO	NO	NO	YES	YES	YES	YES

TABLE II

EX.-ITEM	3-12	3-13	3-14	3-15	3-16	3-17	3-18	3-19	3-20	3-21	3-22	3-23	3-24	3-25	4-1	4-2	4-3	4-4	4-5	4-6	4-7
POLYMER																					
LRV	21.2	--->														21.1	20.6	--->		20.6	--->
TiO2, %	.035	--->														.30	1.0	--->		1.0	--->
FIL/YARN																					
dpf	.51	--->			.89	.75	.70	.89	.88	.88	.83	.75	.75	.75	.70	--->				.70	--->
# Fils	136	--->			68	--->									100	--->				100	--->
Yarn Denier	70	--->			60.6	50.8	50.8	60.4	60.6	60.6	56.1	50.9	50.8	50.8	70	--->				70	--->
EXTRUSION																					
TP, °C	291	--->		287	287	291	291	288	--->							288	--->			288	--->
#/Ao, cm^-2	5.6	--->			2.8	--->									4.2	--->				4.2	--->
w, g/min	.209	.225	.246	.225	.244	.229	.235	.225	.244	.263	.260	.259	.274	.298	.331	.327	.327	.270	.285	.299	.313
q, cm^3/min	.172	.185	.202	.185	.200	.187	.192	.185	.200	.216	.213	.213	.225	.244	.271	.254	.254	.222	.233	.245	.257
tr, min	3.25	3.02	2.77	3.02	3.60	3.85	3.75	3.90	3.60	3.34	3.38	3.37	3.21	2.95	1.81	1.93	1.93	2.21	2.10	2.00	1.91
L, mils	36	--->						20	--->						36	--->				36	--->
L, cm x10	.914	--->						.508	--->						.914	--->				.914	--->
DRND, mils	9	--->																		9	--->
DRND, cm x10	.229	--->																		.229	--->
L/DRND	4	--->						2.22	--->						4	--->				4	--->
AC, mil^2	63.6	--->																		63.6	--->
AC,cm^2 x10^3	.411	--->																		.411	--->
Ba, sec^-1	2435	2621	2866	2621	2843	2668	2738	2620	2842	3063	3028	3028	3191	3471	3856	3810	3810	3146	3321	2484	3646
(L/DRND)Ba x10^-1	974	1049	1146	1049	1137	1067	1095	582	631	681	673	673	709	771	1543	1524	1524	1258	1328	1393	1459
k(L/DRND)Ba,°C	1.9	2.1	2.3	2.1	2.3	2.1	1.2	1.2	1.3	1.4	1.4	1.4	1.4	1.5	3.1	3.0	3.0	2.5	2.7	2.8	2.9
QUENCHING																					
LDQ, cm	6.7	--->																		6.7	--->
12Idpf, cm	8.6	--->			11.3	10.4	8.4	11.3	11.3	11.3	10.9	10.4	10.4	10.4	8.4	--->				8.4	--->
Vq, m/min	30.6	--->						16.3	--->						13.1	21.2	13.1	--->		13.1	--->
Lc, cm	109	--->																		109	--->
SD:90Idpf,cm	115	--->			135	128	125	135	135	135	132	128	128	128	125	--->				125	--->
SPINNING																					
V, y/min	4000	4300	4700	4300	2700	3000	3300	2500	2700	2900	3100	3400	3600	3800	4650	4600	4600	3800	4000	4200	4400
V, m/min	3658	3932	4298	3932	2469	2743	3018	2286	2469	2652	2835	3109	3292	3475	4252	4206	5206	3475	3658	3840	4023
ER(=V/Vo)	884	--->		506	610	644	644	506	506	506	546	603	603	603	644	--->				644	--->
Ea [=ln(ER)]	6.78	--->		6.23	6.41	6.47	6.47	6.22	6.22	6.22	6.30	6.40	6.40	6.40	6.47	--->				6.47	--->
Ea*T7, g/d	6.92	7.46	8.61	7.79	3.72	3.82	4.21	3.17	3.36	3.61	4.22	4.99	5.38	5.82	7.96	8.35	7.44	6.15	6.21	6.60	7.18
YARN																					
T7, g/d	1.02	1.10	1.27	1.25	0.58	0.59	0.65	0.51	0.54	0.58	0.67	0.78	0.84	0.90	1.23	1.29	1.15	0.95	0.96	1.02	1.11
EB, %	82.7	76.1	69.8	70.1	127.5	104.8	108.3	143.8	139.2	133.2	128.3	107.4	110.2	109.1	69.9	82.8	82.3	102.6	97.2	91.8	87.0
T, g/d	3.22	3.20	3.19	3.12	2.73	2.52	2.95	2.97	3.05	3.10	3.25	3.31	3.31	3.37	3.34	3.00	2.90	2.95	2.95	2.93	2.91
TB, g/d	5.88	5.63	5.42	5.31	6.20	5.16	6.14	7.24	7.30	7.23	7.42	6.78	6.96	7.05	5.67	5.48	5.29	5.98	5.82	5.62	5.44
(TB)n, g/d	5.82	5.57	5.37	5.26	6.14	5.11	6.08	7.17	7.23	7.16	7.35	6.71	6.89	6.98	5.61	5.37	5.18	6.10	5.70	5.51	5.33
(TB)n/T7	5.70	5.06	4.22	4.20	10.5	8.66	9.35	14.0	13.3	12.3	10.9	8.60	8.20	7.75	4.56	4.16	4.50	6.42	5.93	5.40	4.80
DS, %	1.17	1.36	1.72	1.61	0.99	1.06	1.03	1.56	1.54	1.48	1.60	1.71	1.73	1.69	1.7	1.46	2.01	2.10	2.07	2.08	1.98
DTV, %	0.22	0.36	0.28	0.33	0.53	0.40	0.46	0.67	0.65	0.47	0.34	0.52	0.52	0.34	----	----	0.44	0.52	0.44	0.47	0.42

TABLE III

EX.-ITEM	4-8	4-9	5-1	5-2	5-3	5-4	5-5	5-6	5-7	5-8	5-9	5-10	5-11	5-12	5-13	6-1	6-2	6-3	6-4	6-5	6-6
POLYMER																					
LRV	20.6	---->	21.1	----------														---->	21.1	---->	
TiO2, %	1.0	---->	.30	----------														---->	0.3	---->	
FIL/YARN																					
dpf	.70	---->	.85	----------					>.77	.78	.76	.76	.83	.76	.69	.42	.56	.75	.42	.56	.75
# fils	100	---->		----------																	
Yarn Denier	70	---->	85	----------					77	78	76	76	83	76	69	42	56	75	42	56	75
EXTRUSION																					
TP, °C	288	---->	286	----------			287	292	287				291								
$/Ro, cm^-2	4.2			----------																	
w, g/min	.316	.358	.207	.233	.259	.285	.259	.259	.258	.262	.255	.255	.202	.232	.245	.141	.188	.252	.141	.188	.252
q, cm3/m	.260	.293	.170	.191	.212	.234	.212	.212	.212	.214	.209	.209	.166	.190	.201	.115	.154	.206	.115	.154	.206
Lr, min	1.88	1.67	2.88	2.57	2.31	2.09	2.31	----------		2.29	2.34	---->	2.95	2.58	2.44	4.26	3.18	2.38	4.26	3.18	2.38
L, mils	36	---->	50	----------			36	18	36	---->	50	---->	36	----------							
L, cm x10	.914	---->	1.27	----------			.914	.457	.914	---->	1.27	---->	.914	----------							
DRND, mils	9	---->	12	----------			9	6	9	---->	12	---->	9	----------							
DRND, cm x10	.229	---->	.305	----------			.229	.152	.229	---->	.305	---->	.229	----------							
L/DRND	4	---->	4.17	----------			4	3	4	---->	4.17	---->	4	----------							
AC, mil^2	63.5	---->	113.1	----------			63.6	28.3	63.6	---->	113.1	---->	63.6	----------							
AC,cm^2 x10^3	.411	---->	.731	----------			.411	.182	.411	---->	.730	---->	.411	----------							
Ga, sec^-1	3681	4169	1016	1144	1272	1399	3017	10181	3006	3052	1252	---->	2352	2703	2854	1643	2190	2936	1643	2190	2936
(L/DRND)Ga*10^-1	1473	1668	424	477	530	584	1207	4072	1202	1221	522	---->	941	1081	1142	657	876	1174	657	876	1174
k(L/DRND)Ga,°C	2.9	3.3	0.8	0.9	1.1	1.2	2.4	8.1	2.4	2.4	1.0	---->	1.9	2.1	2.2	1.3	1.7	2.3	1.3	1.7	2.3
QUENCHING																					
LDQ, cm	6.			----------					---->	11.8	6.7	11.8	6.7	----------				---->	2.9	---->	
12Idpf, cm	8.4	---->	11.1	----------					---->	10.5	----------		---->	10.9	10.4	10.0	7.8	9.0	10.4	7.8	9.0	10.4
Va, m/min	13.1	---->	25	----------					---->	----------			---->	21	19	---->	16.3	----------			
Lc cm	109			----------																	
5019Qldpf,cm	125	---->	133	----------					---->	129	----------		---->	132	129	124	108	117	128	108	117	128
SPINNING																					
V, y/min	4450	4600	2400	2700	3000	3300	3000	---->	3300	----------			---->	2400	3000	3300	----------				
V, m/min	4069	4206	2195	2469	2743	3018	2743	---->	3018	----------			---->	2195	2743	3018	----------				
ER(=V/Vo)	644	---->	943	----------			530	236	585	---->	1054	---->	543	593	653	1023	805	601	1023	805	601
εo [=ln(ER)]	5.47	---->	6.85	----------			6.27	5.46	6.37	---->	6.96	---->	6.30	6.39	6.48	6.98	6.69	6.40	6.98	6.69	6.40
εaT7, g/d	7.38	7.44	4.38	5.14	5.62	6.58	5.27	4.48	6.12	5.92	6.68	6.61	5.86	6.22	6.29						
YARN																					
T7, g/d	1.14	1.15	0.64	0.75	0.82	0.96	0.84	0.82	0.96	0.93	0.96	0.95	0.93	0.96	0.97	---	---	---	---	---	---
EB, %	86.0	82.3	136.2	124.9	118.0	104.1	116.2	117.8	103.9	107.4	103.8	104.7	106.8	104.2	103.0	---	---	---	---	---	---
T, g/d	2.91	2.90	2.83	2.98	3.08	3.11	2.98	2.64	3.14	3.16	3.19	3.15	3.20	3.30	3.30	---	---	---	---	---	---
TB, g/d	5.38	5.29	6.68	6.70	6.71	6.35	6.27	5.75	6.40	6.55	6.50	6.45	6.62	6.74	6.70	---	---	---	---	---	---
(TB)N, g/d	5.59	5.50	6.65	6.61	6.62	6.26	6.18	5.67	6.31	6.46	6.41	6.36	6.53	6.65	6.61	---	---	---	---	---	---
(TB)n/T7	4.90	4.78	10.4	8.81	8.07	6.52	7.35	6.91	6.57	6.94	6.67	6.69	7.02	6.92	6.81	---	---	---	---	---	---
DS,%	1.61	2.01	1.85	1.46	1.09	1.01	0.97	0.89	1.09	3.98	0.99	4.16	1.26	1.44	1.26	12.1	3.8	2.4	3.6	2.6	1.1
DIV, %	0.42	0.44	0.57	0.53	0.38	0.34	1.50	0.57	0.37	1.01	0.37	0.74	0.84	0.96	0.69	---	1.3	0.9	1.5	0.7	1.7
IFDU,%	---	---	7.8	8.1	8.1	7.9	5.9	---	6.5	11.4	5.9	11.2	---	---	---	---	---	---	---	---	---

TABLE IV

EX.-ITEM	6-7	6-8	6-9	6-10	7-1	7-2	7-3	7-4	7-5	7-6	7-7	7-8	7-9	7-10	7-11	8-1	8-2	8-3	9-1	9-2	9-3
POLYMER																					
LRV	21.1	---------->														15.7	---------->		21.9	---------->	
TiO2, %	0.3	---------->			.035	---------->															
FIL/YARN																					
dpf	.42	---------->			.90	1.15	.81	.81	.81	.84	.84	.85	.81	.85	.81	.86	.76	.78	.5	---------->	
# Fils	100	---------->																			
Yarn Denier	42	---------->			90	115	80.9	81.2	80.8	80.5	81.2	84.7	81.2	84.5	81.2	85.6	76.0	78.1	50	---------->	
EXTRUSION																					
TP, °C	293	296	291	---->	288	290	---->	288	292	287	---------->		290	287	292	284	284	285	289	291	293
#/Ao, cm^-2	4.2	---------->																4.2	4.2	---------->	
w, g/min	.141	---------->			.215	.275	.247	.272	.272	.213	.233	.259	.247	.276	.272	.210	.208	.238	218	.239	.254
q, cm^3/gm	.115	---------->			.166	.225	.208	.223	.223	.175	.191	.212	.208	.227	.223	.172	.171	.195	169	.184	.208
tr, min	4.26	---------->			2.95	2.18	2.36	2.20	2.20	2.80	2.56	2.31	2.36	2.16	2.20	2.85	2.84	2.51	2.90	2.66	2.36
L, mils	36	---------->			50	---------->				36	---------->								50	---------->	
L, cm x10	.914	---------->			1.27	---------->				.914	---------->								1.27	---------->	
DRND, mils	9	---------->			12	---------->				9	---------->								12	---------->	
DRND, cm x10	.299	---------->			.305	---------->				.229	---------->								.305	---------->	
L/DRND	4	---------->			4.17	---------->				4	---------->								4.17	---------->	
AC, mil^2	63.6	---------->			113.1	---------->				63.6	---------->								113.1	---------->	
AC,mm^2 x10^3	.411	---------->			.730	---------->				.411	---------->								.730	---------->	
Ga, sec^-1	1643	---------->			1056	1350	1213	1336	1336	2481	2714	3017	2878	3215	3169	2447	2423	2773	1070	1166	1247
(L/DRND)Gax10^-1	6571	---------->			440	563	506	557	557	993	1086	1207	1151	1286	1268	979	969	1109	442	487	521
k(L/DRND)Ga,°C	13.1	---------->			0.9	1.1	1.0	1.1	1.1	2.0	2.2	2.4	2.3	2.6	2.6	1.9	1.9	2.2	0.9	0.9	1.0
QUENCHING																					
LDQ, cm	2.9	---------->			6.7	---------->										7.1	---------->		6.7	---------->	
12Jdpf, cm	7.8	---------->			11.4	12.9	10.8	---------->		11.0	11.0	11.1	10.8	11.1	10.8	11.1	10.5	10.6	10.0	---------->	
Va, m/min	16.3	---------->														25	--->	25	30.6	---------->	
Lc cm	109	---->	97	81	137	---------->										109	--->	109	100	---------->	
50+90Jdpf,cm	109	---------->			135	147	131	---------->		132	---->	133	131	133	131	133	128	129	114	---------->	
SPINNING																					
V, y/min	3300	---------->			2350	2350	3000	3300	3300	2500	2700	3000	3000	3200	3300	2400	2700	3000	4300	4700	5000
V, m/min	3018	---------->			2149	2149	2743	3018	3018	2286	2469	2743	2743	2926	3018	2195	2468	2743	3932	4298	4570
ER(=V/Vo)	1073	---------->			890	697	989	---------->		537	537	530	556	530	556	524	593	586	1602	---------->	
Ea [=ln(ER)]	6.98	---------->			6.79	6.55	6.90	---------->		6.29	6.29	6.27	6.56	6.27	6.56	6.26	6.39	6.37	7.38	---------->	
EaxT7, g/d	---	---	---	---	4.69	8.82	5.93	6.49	7.31	4.91	5.22	5.70	5.32	6.08	5.64	3.88	4.92	4.97	10.1	9.74	11.1
YARN																					
T7,	---	---	---	---	0.69	0.43	0.86	0.94	1.06	0.78	0.83	0.91	0.81	0.97	0.86	0.62	0.77	0.78	1.37	1.32	1.51
EB, %	---	---	---	---	120.6	132.8	94.3	93.7	73.8	121.6	116.8	108.5	98.5	102.8	93.3	127.8	113.	102.3	67.1	69.5	66.4
T, g/d	---	---	---	---	2.51	2.00	2.49	2.87	2.13	2.70	2.88	2.94	2.60	2.98	2.30	1.81	1.88	1.89	3.19	3.28	3.14
TB, g/d	---	---	---	---	5.55	4.66	4.83	5.57	3.71	5.99	6.25	6.14	5.17	6.05	4.44	4.13	4.00	3.82	5.33	5.56	5.22
(TB)N, g/d	---	---	---	---	5.47	4.59	4.76	5.49	3.65	5.90	6.16	6.05	5.09	5.96	4.33	5.54	5.36	5.12	4.58	4.78	4.49
(TB)n/T7	---	---	---	---	7.9	10.7	5.5	5.8	3.4	7.6	7.4	6.6	6.3	6.1	5.0	8.9	7.0	6.6	3.35	3.62	3.03
DS,%	3.8	3.8	3.3	3.1	---	---	9.9	4.3	5.0	14.2	8.4	2.4	9.1	1.7	4.95	2.33	3.47	2.33	1.42	1.34	1.29
DIV, %	1.7	1.9	1.3	1.0	---	---	---	---	---	1.70	1.19	0.44	---	0.33	----	0.81	0.75	0.63	.41	.36	.23

TABLE V

EX.-ITEM	9-4	9-5	9-6	9-7	9-8	9-9	9-10	9-11	10-1	10-2	10-3	10-4	10-5	10-6	10-7	10-8	10-9	10-10	10-11	10-12	10-13
POLYMER																					
LRV	21.9	---------->							21.9	---------->											
Ti02,%	0.3	---------->							---------->												
FIL/YARN																					
dpf	0.5	---------->							0.7	---------->											
# Fils	100	---------->							---------->												
Yarn Denier	50	---------->							70	---------->											
EXTRUSION																					
TP, °C	290	---------->	292	293	290	----------	---------->	297	286	---------->				294	---------->			286	294	---->	286
#/Ao, cm^2	4.2	---------->							---------->												
u, g/min	.171	.218	.239	.254	.171	.218	.239	.254	.334	---------->							.355	---------->		.334	---->
q, cm^3/min	.132	.169	.184	.208	.132	.169	.184	.208	.258	---------->							.291	---------->		.258	---->
tr, min	3.71	2.90	2.66	2.36	3.71	2.90	2.66	2.36	1.90	---------->							1.68	---------->		1.9	---->
L, mils	36	---------->			18	----------	---------->		36	---------->								50	----------	---------->	
L, cm x10	.914	---------->			.456	----------	---------->		.914	---------->								1.27	----------	---------->	
DRND, mils	9	---------->			6	----------	---------->		9	---------->								12	----------	---------->	
DRND, cm x10	.229	---------->			.152	----------	---------->		.229	---------->								.305	----------	---------->	
L/DRND	4	---------->			3	----------	---------->		4	---------->								4.17	----------	---------->	
AC, mil^2	63.6	---------->			28.3	----------	---------->		63.6	---------->								113.1	----------	---------->	
AC,cm^2x10^3	.411	---------->			.182	----------	---------->		.411	---------->								.730	----------	---------->	
Ga, sec^-1	1992	2540	2784	2959	6722	8570	9395	9985	3891	---------->							4136	1743	---->	1640	---->
(L/DRND)Ga*10^-1	397	1016	1114	1184	2017	2571	2819	2995	1556	---------->							1654	727	---->	684	---->
k(L/DRND)Ga,°C	0.8	2.0	2.2	2.3	4.0	5.5	5.6	6.0	3.1	---------->							3.3	1.4	---->	1.3	---->
QUENCHING																					
LDQ, cm	6.7	----------							8.5	----------								10.0	----------	---------->	
12Idpf, cm	10.0	----------							11.3	21.3	30.6	21.3	30.6	21.3	--->	30.6	21.3	----------		---------->	
Vo, m/min	30.6	----------							----------									----------		---------->	
LC, cm	100	----------							----------		---->	61	---------->	109	--->	61	109	----------		---------->	
50I90Idpf.cm	114	----------							125	----------								125	----------	---------->	
SPINNING																					
V, y/min	4100	4300	4700	5000	4100	4300	4700	5000	4700	----------							5000	5000	---------->	4700	---->
V, m/min	3749	3932	4298	4570	3749	3932	4298	4572	4298	----------							4572	4572	---------->	4298	---->
ER(=V/Vo)	1602	901	----------	---------->	401	----------	---------->	---------->	644	----------							644	1145	----------	---------->	
Ea [=ln(ER)]	7.38	6.80	----------	---------->	5.99	----------	---------->	---------->	6.47	----------							6.47	7.04	----------	---------->	
Ea*I7, g/d	9.08	8.27	11.0	11.0	5.63	8.03	7.85	8.81	7.70	7.81	8.22	8.09	8.35	7.18	7.44	7.44	7.89	8.10	8.88	8.66	7.74
YARN																					
S, %	3.7	3.3	3.7	3.2	4.9	3.8	3.9	4.3	3.3	3.1	3.0	2.9	3.0	3.4	3.1	3.1	3.1	3.2	3.4	3.1	3.5
Mi, g/d	42.1	39.4	42.7	46.1	35.1	47.1	45.8	50.9	44.2	50.7	47.1	45.3	44.6	45.2	47.1	39.5	48.6	41.4	48.5	48.7	42.6
I7, g/d	1.23	1.29	1.61	1.62	0.94	1.34	1.31	1.47	1.19	1.16	1.27	1.25	1.29	1.11	1.15	1.15	1.22	1.15	1.12	1.23	1.10
EB, %	72.9	72.8	53.1	62.8	76.4	64.3	67.9	62.7	77.5	76.8	71.7	71.9	68.1	77.3	75.8	74.6	74.3	78.0	78.0	75.2	83.0
T, g/d	3.18	3.31	2.96	3.21	3.05	3.12	3.28	3.31	3.41	3.40	3.28	3.37	3.24	3.51	3.50	3.43	3.55	3.53	3.58	3.47	3.47
TB, g/d	5.50	5.70	4.53	5.23	5.28	5.13	5.51	5.39	6.05	6.01	5.63	5.79	5.45	6.22	6.15	5.99	6.19	6.28	6.37	6.35	6.08
(TB)n, g/d	4.95	5.64	4.08	4.71	4.75	5.62	4.96	4.85	5.87	5.83	5.46	5.62	5.29	6.03	5.97	5.81	6.00	6.09	6.18	6.16	5.90
(TB)n/I7	4.02	4.37	2.53	2.90	5.05	4.19	3.78	3.29	4.93	5.02	4.29	4.49	4.10	5.43	5.19	5.05	4.91	5.29	5.51	5.00	5.36
DS,%	1.40	1.30	1.31	1.58	1.47	1.49	1.54	1.38	1.67	1.96	1.29	1.46	1.13	1.34	1.23	1.16	1.32	1.23	1.86	1.77	2.24
DIV, %	.52	.36	.23	.25	.47	.31	.40	.33	.43	.73	.37	.36	.22	.48	.26	.21	0.67	0.52	0.42	0.45	0.45

TABLE VI

EX.-ITEM	10-14	10-15	13-1	13-2	13-3	13-4	13-5	13-6	13-7	13-8	13-9	13-10	15-1	15-2	15-3	15-4	15-5	16-1	17-1	17-2
POLYMER																				
LRV	21.9	----->	20.8	---------->									21.2	---------->						
TiO2,Z	0.3	---------->											0.035	---------->						
FIL/YARN													290	294	---------->			285	290	----->
dpf	0.7	----->	0.5	---------->				0.7	---------->				.85	.59	.50	.45	.38	.82	.86	.86
# Fils	100	---------->											68	200	200	168	200	100	50	----->
Yarn Denier	70	----->	50	---------->				70	---------->				58	118	100	75.6	76	82	43	43
EXTRUSION																				
TP, °C	294	286	293	---------->									290	294	294	294	294	285	290	290
#/Ao, cm^-2	4.2	---------->																		
u, g/min	.306	----->	.229	.239	.249	.259	.269	.321	.335	.349	.363	.377	.207	.144	.224	.201	.093	.196	.306	.394
q, cm^3/min	.251	----->	.188	.196	.204	.213	.221	.263	.275	.286	.298	.309	.170	.119	.184	.165	.076	.161	.250	.324
tr, min	1.95	----->	2.61	2.50	2.4	2.3	2.22	1.86	1.79	1.71	1.64	1.58	4.22	3.19	2.06	2.74	4.99	3.03	3.90	3.01
L, mils	50	----->	36	---------->																
L, cm x10	1.27	----->	.914	---------->									1.27	.914	---------->			.457	.914	1.83 ---->
DRND, mils	12	----->	9	---------->									9	---------->				6	9	15 ---->
DRND, cm x10	.305	----->	.229	---------->									.229	---------->				.152	.229	.381 ---->
L/DRND	4.17	----->	4	---------->									5.6	4	---------->			3	4	4.8 ---->
AC, mil^2	113.1	----->	63.6	---------->									63.6	---------->				20.3	63.6	176.6 ---->
AC,cm^2x10^3	.730	----->	.411	---------->									.411	---------->				.182	.411	1.141 ---->
Ga, sec^-1	1502	----->	2668	2784	2901	3017	3134	3735	3836	4061	4224	4388	3349	1676	2602	2343	3543	2282	230	991
(L/DRND)Gax10^-1	627	----->	1067	1114	1160	1207	1254	1494	1534	1625	1690	1755	1875	670	1041	937	1093	912	110	476
k(L/DRND)Ga,°C	1.2	----->	2.1	2.2	2.3	2.4	2.5	3.0	3.1	3.2	3.4	3.5	3.8	1.4	2.1	1.9	2.2	1.8	0.2	1.0
QUENCHING																				
LDQ, cm	6.7	----->	5.7	---------->									6.7	2.9	---------->					
12Idpf, cm	10.0	----->	8.5	---------->				10.0	---------->				11.0	9.2	8.5	8.0	7.4	10.9	11.1	11.1
Vo, m/min	21.3	----->	18.5	---------->									16	30	---------->			16	22	13 13
Lc, cm	109	----->	81	---------->									109	---------->						
50+90Idpf,cm	125	----->	114	---------->				125	---------->				133	119	114	110	105	131	133	133
SPINNING																				
V, y/min	4300	----->	4500	4700	4900	5100	5300	4500	4700	4900	5100	5300	2400	2400	4400	4400	2400	2350	3500	4500
V, m/min	3932	----->	4115	4298	4481	4633	4846	4115	4298	4481	4633	4846	2195	2195	4023	4023	2195	2149	3200	4115
ER(=V/Vo)	1145	----->	901	---------->				644	---------->				530	764	901	1001	1527	550	2911	2911
E a [=ln(ER)]	7.04	----->	6.80	---------->				6.47	---------->				6.27	6.64	6.80	6.91	6.27	6.31	7.98	7.98
EaxT7, g/d	6.97	6.69	8.36	8.36	8.98	9.52	10.1	6.66	6.92	7.44	7.89	8.54	---	4.78	9.86	---	---	6.37	7.02	12.0
YARN																				
S, Z	3.5	3.6	---	3.2	4.0	4.0	3.2	3.5	4.5	3.5	3.4	4.0	---	2.8	3.4	---	---	2.5	4.3	5.10
Mi, g/d	46.7	36.4	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---
T7, g/d	0.99	0.95	1.23	1.23	1.32	1.40	1.49	1.03	1.07	1.15	1.22	1.32	---	.72	1.45	1.34	---	1.01	0.88	1.50
EB, Z	84.8	89.1	52.1	58.7	53.6	47.5	45.5	66.8	69.4	67.5	56.3	54.8	144.9	126.6	82.8	86.5	121.8	92.9	90.0	46.0
T, g/d	3.45	3.37	2.73	2.84	2.82	2.71	2.70	2.88	3.04	3.13	2.91	2.93	2.88	2.97	3.12	3.22	3.23	2.40	3.00	2.65
TB, g/d	6.35	6.38	4.37	4.15	4.51	4.33	4.00	3.93	5.15	5.24	4.55	4.54	7.05	6.72	5.70	6.01	7.16	4.64	5.70	3.87
(TB)n, g/d	6.16	6.19	4.41	4.19	4.56	4.37	4.04	3.97	5.20	5.29	4.60	4.59	6.98	6.66	3.89	5.64	7.09	4.54	5.64	3.83
(TB)n/T7	6.22	6.51	3.58	3.40	3.45	3.12	2.71	3.85	4.85	4.60	3.77	3.47	---	9.25	2.68	4.21	---	4.50	6.41	2.55
DS, Z	1.68	1.87	3.85	1.20	1.23	1.21	1.04	1.00	0.97	0.90	2.90	2.90	4.26	---	---	---	---	---	---	---
DIV, Z	0.38	0.71	---	---	---	---	----	---	---	---	---	---	---	---	---	---	---	---	---	---

TABLE VII

EX.-ITEM	XI-1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18
PROCESS																		
Type	WD	---------->																
Speed, mpm	600	---------->																
Draw Temp., °C	COLD	---------->	155	---------->			COLD	---------->		155	---------->		COLD	---------->		155	---------->	
Set Temp., °C																		
Draw Ratio	1.45	1.50	1.55	1.45	1.50	1.55	1.45	1.50	1.55	1.45	1.50	1.55	1.45	1.50	1.55	1.45	1.50	1.55
YARN																		
# fils	100	---------->																
Denier	58.4	56.2	54.7	58.6	56.7	55.0	53.2	51.4	50.3	53.5	51.8	49.8	48.3	46.7	45.5	48.6	47.1	46.1
S, Z	4.8	4.7	5.3	5.9	5.5	5.7	4.6	4.6	4.5	5.6	5.2	5.5	4.7	4.3	4.5	5.0	5.2	5.3
MOD., g/d	82.7	89.4	93.9	86.7	90.4	95.2	91.0	96.1	100.5	89.9	93.5	99.2	94.7	97.4	99.3	90.5	96.8	99.4
T7, g/d	3.2	3.7	4.1	3.2	3.7	4.1	3.4	3.9	4.3	3.4	3.9	4.4	3.6	4.0	4.4	3.6	4.0	4.4
EB, Z	33.7	28.8	25.7	35 3	31.2	25.8	34.0	26.5	22.6	32.6	28.2	24.0	30.8	27.0	22.8	30.8	25.5	22.5
I, g/d	4.9	5.1	5.3	4.9	5.1	5.2	5.0	5.1	5.3	4.8	5.1	5.3	5.0	5.2	5.3	4.9	5.0	5.2
DS, Z	1.8	1.7	1.9	2.0	1.9	1.9	1.8	1.9	1.8	2.0	2.7	2.1	2.1	2.2	2.2	2.2	2.2	2.3
Uster, Z	0.5	0.5	0.5	0.6	0.6	0.6	0.5	0.6	0.5	0.6	0.6	0.7	0.6	0.6	0.6	0.6	0.6	0.7

TABLE VIII

EX.-ITEM	XII-1	2	3	4	5	6	XIV-1	2	3	4	5	6	7	8	XVIII-1	2	3
PROCESS																	
Type	WD	---------->					AJT	---------->							WD	---------->	
Speed, mpm	600	---------->					300	---------->							600	---------->	
Draw Temp., °C	COLD	---------->															
Draw Ratio	1.69	1.57	1.44	1.42	1.42	1.42	1.0	1.1	1.2	1.32	1.0	1.1	1.2	1.32	1.42	---------->	
YARN																	
# fils	100	---------->					100	---------->			68	---------->			50	---------->	
Denier	35.9	35.6	35.4	35.9	36.1	36.1	91.4	95.0	85.8	77.3	81.8	75.1	70.4	64.7	35.9	36.1	36.1
Bulk, Z	NA	---------->					1.4	11.8	11.4	12.0	12.1	13.1	15.7	17.0	NA	---------->	
S, Z	3.9	4.2	4.4	4.0	4.0	4.9	3.5	4.3	8.2	12.7	3.4	4.9	8.2	11.8	4.0	4.0	4.9
DHS, Z	---	---	---	---	---	---	2.8	4.1	7.6	11.0	3.2	4.4	7.1	10.4	---	---	---
T7, g/d	3.97	3.84	3.56	3.54	3.54	3.49	---	---	---	---	---	---	---	---	3.54	3.54	3.49
EB, Z	23.2	24.4	26.7	26.7	27.2	28.6	61.1	57.1	41.3	27.2	64.4	60.9	43.3	29.6	26.7	27.2	28.6
I, g/d	5.23	4.96	4.54	4.56	4.50	4.50	1.96	2.22	2.42	2.64	2.12	2.46	2.58	2.78	4.56	4.50	4.50
DS, Z	1.9	1.8	2.0	2.1	2.1	2.4	NA	---------->			NA	---------->			2.1	2.1	2.4
Uster, Z	---	---	---	---	---	---	NA	---------->			NA	---------->			---	---	---

Claims

1. A process for preparing spin-oriented polyester fine filaments of denier in the range of 1 to 0.2, wherein

(i) the polyester polymer is selected to have a relative viscosity (LRV) in the range of 13 to 23, a zero-shear melting point ($T_M°$) in the range 240°C to 265°C, and a glass-transition temperature (T_g) in the range of 40°C to 80°C;

(ii) said polyester is melted and heated to a temperature (T_P) in the range 25°C to 55°C above the apparent polymer melting point $(T_M)_a$;

(iii) the resulting melt is filtered sufficiently rapidly that the residence time (t_r) in the filter cavity is less than 4 minutes;

(iv) the filtered melt is extruded through a spinneret capillary at a mass flow rate (w) in the range 0.07 to 0.7 grams per minute, and the capillary is selected to have a cross-sectional area (A_c) in the range $125x10^{-6}$ cm^2 to $1250x10^{-6}$ cm^2, and a length (L) and diameter (D_{RND}) such that the (L/D_{RND})-ratio is at least 1.25 and less than 6.

(v) the extruded melt is protected from direct cooling as it emerges from the spinneret capillary over a distance (L_{DQ}) of at least 2 cm and less than ($12dpf^{½}$)cm, where dpf is the denier per filament of the fine spin-oriented polyester filament,

(vi) the extruded melt is cooled to below the polymer glass-transition temperature (T_g) and attenuated to an apparent spinline strain (ε_a) in the range of 5.7 to 7.6, and to an apparent internal spinline stress (σ_a) in the range of 0.045 to 0.195 g/d,

(vii) the cooled filaments are then converged into a multifilament bundle by use of a low friction surface at a distance from the spinneret face (L_c) in the range 50 cm to 140 cm, and

(viii) the multifilament bundle is withdrawn at a speed (V) in the range of 2 to 6 km/min, and wound up at a speed which is 95% to 100% that of the withdrawal speed.

2. A process according to claim 1, wherein said polyester contains in the range of 1 to 3 mole percent of ethylene 5-M-sulfo-isophthalate structural units, wherein M is an alkali metal cation.

3. A process according to claim 1, wherein said polyester is essentially poly(ethylene terephthalate), composed of first alternating hydrocarbolenedioxy structural units A [-O-C_2H_4-O-], and hydrocarbolenedicarbonyl structural units B[-(O)C-C_6H_4-C(O)-], modified with minor amounts of other hydrocarbolenedioxy structural units A and/or hydrocarbolenedicarbonyl structural units B that differ from the first alternating hydrocarbolenedioxy structural units A and hydrocarbolenedicarbonyl structural units B, such as to provide a polyester polymer with a zero-shear melting point ($T_M°$) in the range 240°C to 265°C and a glass-transition temperature (T_g) in the range 40°C to 80°C.

4. A process according to claim 1, wherein the apparent spinline strain (ε_a) is in the range 6 to 7.3, and the apparent internal spinline stress (σ_a) is controlled to obtain an average orientation as represented by a tenacity-at-7%-elongation (T_7) in the range of 0.5 to 1.75 g/d.

5. A process according to any one of the claims 1 to 4, wherein the polymer temperature (T_P) is in the range of 30°C to 50°C above the apparent polymer melting point $(T_M)_a$, the spinneret capillary cross-section area (A_c) is in the range $125x10^{-6}$ cm^2 to $750x10^{-6}$ cm^2, the extrusion filament density ($\#_c/A_o$) is in the range 2.5 to 25 filaments per cm^2; and said cooling of the extruded melt is by use of radially directed air having a temperature (T_a) less than about the polymer glass-transition temperature (T_g) and a velocity (V_a) in the range 10 to 30 m/min, and said convergence is by a metered finish tip guide at a distance (L_c) in the range 50 cm to ($50+90dpf^{½}$)cm, and the withdrawal speed (V) is in the range 2 to 5 km/min.

6. A process according to any one of the claims 1 to 4, wherein the filaments have a denier in the range of 0.6 to 0.2 and a denier spread (DS) less than 2%.

7. Spin-oriented polyester filaments of fineness in the range of 1 to 0.2 denier per filament, wherein said polyester has a relative viscosity (LRV) in the range of 13 to 23, a zero-shear polymer melting point ($T_M°$) in the range 240°C to 265°C, and a polymer glass transition temperature (T_g) in the range of 40°C to 80°C; and said filaments have:

(i) boil-off shrinkage (S) less than the maximum shrinkage potential (S_m), wherein $S_m = [(550-E_B)/6.5]$ %, and the percent elongation-to-break (E_B) is in the range of 40% to 160%,

(ii) a maximum shrinkage tension, (ST_{max}), in the range 0.05 to 0.2 g/d, with a peak temperature, $T(ST_{max})$, in the range 5°C to 30°C above the polymer glass-transition temperature (T_g);

(iii) tenacity-at-7%-elongation (T_7) in the range of 0.5 to 1.75 g/d, such that the $[(T_B)_n/T_7]$-ratio is at least $(5/T_7)$, wherein $(T_B)_n$ is the normalized tenacity-at-break;

(iv) an average along-end denier spread (DS) of less than 4%.

8. Filaments according to claim 7, such as are especially suitable for use as draw feed yarns, and have a boil-off shrinkage (S) and dry heat shrinkage (DHS) at least 12%, an elongation-at-break (E_B) in the range of 80% to 160%, and a tenacity-at-7%-elongation (T_7) in the range of 0.5 to 1 g/d.

9. Filaments according to claim 7, such as are especially suitable for use as direct-use textile yarns, and have a shrinkage differential (ΔS) less than +2%, wherein boil-off shrinkage (S) and dry heat shrinkage (DHS) are in the range of 2% to 12%, such that the filament denier after shrinkage is less than 1; and a T_7 in the range 1 to 1.75 g/d, an (E_B) in the range 40% to 90%, and a post-yield modulus (M_{py}) in the range 2 to 12 g/d, wherein $M_{py} = (1.2T_{20} - 1.07T_7)/0.13$.

10. Filaments according to claim 7 having the capability of being uniformly cold drawn, and having a shrinkage differential (ΔS) less than +2%, boil-off shrinkage (S) and dry heat shrinkage (DHS) both being in the range of 2% to 12%, an onset of cold crystallization, T_{cc}(DSC), of less than 105°C, and an instantaneous tensile modulus at least 0.

11. Drawn spin-oriented polyester filaments with deniers after boil-off shrinkage, dpf(ABO), in the range of 1 to 0.2 dpf, wherein said polyester has a relative viscosity (LRV) in the range of 13 to 23, a zero-shear polymer melting point ($T_M°$) in the range of 240°C to 265°C, and a polymer glass-transition temperature (T_g) in the range of 40°C to 80°C; and said drawn filaments have:

(i) boil-off shrinkage (S) and dry heat shrinkage (DHS) in the range of 2% to 12%;

(ii) tenacity-at-7%-elongation (T_7) at least 1 g/d, such that the $[(T_B)_n/T_7]$-ratio is at least $(5/T_7)$, wherein $(T_B)_n$ is the normalized tenacity-at-break and the elongation-at-break (E_B) is in the range of 15% to 55%;

(iii) the post-yield modulus (M_{py}) in the range 5 to 25 g/d;

(iv) an average along-end denier spread (DS) less than 4%.

12. Bulked spin-oriented polyester filaments of fineness in the range of 1 to 0.2 dpf (after boil-off shrinkage), wherein said polyester has a relative viscosity (LRV) in the range of 13 to 23, a zero-shear polymer melting point ($T_M°$) in the range of 240°C to 265°C, and a polymer glass-transition temperature (T_g) in the range of 40°C to 80°C; and said filaments have:

(i) boil-off shrinkage (S) and dry heat shrinkage (DHS) in the range of 2% to 12%;

(ii) tenacity-at-7%-elongation (T_7) at least about 1 g/d and an elongation-at-break (E_B) in the range 15% to 55%, with a post-yield modulus (M_{py}) in the range 5 to 25 g/d.

13. Filaments according to Claim 11 or 12, wherein the filaments are further characterized by a dynamic loss modulus peak temperature $T(E"_{max})$ of less than 115° C.

14. Filaments according to Claim 11 or 12, wherein the filaments are further characterized by a relative disperse dye rate (RDDR) of at least 0.1.

15. Filaments according to any one of Claims 7 to 14, wherein the filaments have a shape factor (SF) at least 1.25.

16. Filaments according to any one of Claims 7 to 15, wherein the filaments have a denier in range of 0.8 to 0.2 dpf.

17. Filaments according to any of Claims 7 to 16, wherein the filaments have an along-end denier spread (DS) less than 2%.

18. Filaments according to any one of Claims 7 to 17, wherein said polyester fiber contains in the range of 1 to 3 mole % of 5-ethylene-M-sulfo-isophthalate structural units, wherein M is an alkali metal cation.

19. Filaments according to any one of claims 7 to 18, wherein said polyester is essentially poly(ethylene terephthalate), composed of first alternating hydrocarbolenedioxy structural units A, [-O-C_2H_4-O-], and hydrocarbolenedicarbonyl structural units B, [-C(O)-C_6H_4-C(O)-], modified with minor amounts of other hydrocarbolenedioxy structural units A and/or hydrocarbolenedicarbonyl structural units B, that differ from said first alternating hydrocarbolenedioxy structural units A and hydrocarbolenedicarbonyl structural units B, such as to provide a polyester polymer with a zero-shear melting point (T_M°) in the range 240°C to 265°C and a polymer glass-transition temperature (T_g) between 40°C and 80°C.

Patentansprüche

1. Verfahren zur Herstellung von spinnorientierten feinen Polyesterfilamenten mit einem Denier-Wert im Bereich von 1 bis 0,2, worin

(i) das Polyesterpolymer so gewählt ist, daß es eine relative Viskosität (LRV) im Bereich von 13 bis 23, einen Schmelzpunkt bei Null-Scherung (T_M°) im Bereich von 240 °C bis 265 °C und eine Glasumwandlungstemperatur (T_g) im Bereich vom 40 °C bis 80 °C besitzt;
(ii) der Polyester geschmolzen und auf eine Temperatur (T_p) im Bereich von 25 °C bis 55 °C über dem scheinbaren Schmelzpunkt $(T_M)_a$ des Polymers erhitzt wird;
(iii) die entstandene Schmelze schnell genug gefiltert wird, damit die Verweilzeit (t_r) im Hohlraum des Filters kürzer ist als 4 Minuten;
(iv) die gefilterte Schmelze mit einer Massendurchsatzmenge (w) im Bereich von 0,07 bis 0,7 g/min durch eine Spinndüsenkapillare extrudiert wird und die Kapillare so gewählt wird, daß sie eine Querschnittsfläche (A_c) im Bereich von 125 x 10^{-6} cm^2 bis 1250 x 10^{-6} cm^2 und eine solche Länge (L) und einen solchen Durchmesser (D_{RND}) aufweist, daß das Verhältnis (L : D_{RND}) mindestens 1,25 und weniger als 6 beträgt;
(v) die extrudierte Schmelze auf einem Stück (L_{DQ}) von mindestens 2 cm und weniger als (12 $dpf^{1/2}$) cm vor einer direkten Abkühlung geschützt ist, wenn sie aus der Spinndüsenkapillare austritt, wobei dpf der Denier-Wert pro Filament des feinen spinnorientierten Polyesterfilaments ist;
(vi) die extrudierte Schmelze bis unter die Glasumwandlungstemperatur (T_g) abgekühlt und auf eine scheinbare Spinnfadendehnung (ε_a) im Bereich von 5,7 bis 7,6 und eine scheinbare innere Spinnfadenspannung (σ_a) im Bereich von 0,045 bis 0,195 g/d abgeschwächt wird;
(vii) die abgekühlten Filamente dann mit Hilfe einer reibungsarmen Fläche in einem Abstand (L_c) von der Spinndüsenplatte im Bereich von 50 cm bis 140 cm zu einem Multifilamentbündel zusammengeführt werden; und
(viii) das Multifilamentbündel mit einer Geschwindigkeit (V) im Bereich von 2 bis 6 km/min abgezogen wird und mit einer Geschwindigkeit aufgewickelt wird, die 95 % bis 100 % der Abzugsgeschwindigkeit beträgt.

2. Verfahren nach Anspruch 1, worin der Polyester Struktureinheiten aus Ethylen-5-M-sulfoisophthalat im Bereich von 1 bis 3 Mol-% enthält, wobei M ein Alkalimetallkation ist.

3. Verfahren nach Anspruch 1, worin der Polyester im wesentlichen Poly(ethylenterephthalat) ist, bestehend aus ersten einander abwechselnden Hydrocarbolendioxy-Struktureinheiten A [-O-C_2H_4-O-] und Hydrocarbolendicarbonyl-struktureinheiten B [-(O)C-C_6H_4-C(O)-], modifiziert mit kleineren Anteilen an anderen Hydrocarbolendioxy-Struktureinheiten A und/oder Hydrocarbolendicarbonyl-Struktureinheiten B, die sich von den ersten einander abwechselnden Hydrocarbolendioxy-Struktureinheiten A und Hydrocarbolendicarbonyl-Struktureinheiten B unterscheiden, so daß ein Polyesterpolymer mit einem Schmelzpunkt bei Null-Scherung (T_M°) im Bereich von 240 °C bis 265 °C und einer Glasumwandlungstemperatur (T_g) im Bereich von 40 °C bis 80 °C entsteht.

4. Verfahren nach Anspruch 1, worin die scheinbare Spinnfadendehnung (ε_a) im Bereich von 6 bis 7,3 liegt und die scheinbare innere Spinnfadenspannung (σ_a) so reguliert wird, daß eine durchschnittliche Orientierung, dargestellt durch eine Festigkeit bei 7 % Dehnung (T_7), im Bereich von 0,5 bis 1,75 g/d erzielt wird.

5. Verfahren nach einem der Ansprüche 1 bis 4, worin die Temperatur des Polymers (T_p) im Bereich von 30 °C bis 50 °C über dem scheinbaren Schmelzpunkt $(T_M)_a$ des Polymers liegt, die Querschnittsfläche der Spinndüsenkapillare (A_c) im Bereich von 125 x 10^{-6} cm^2 bis 750 x 10^{-6} cm^2 1iegt, die Dichte des Extrusionsfilaments ($\#_c/A_o$) im Bereich von 2,5 bis 25 Filamenten/cm^2 liegt und die Abkühlung der extrudierten Schmelze mit Hilfe von radial gerichteter Luft mit einer Temperatur (T_a) erfolgt, die niedriger ist als etwa die Glasübergangstemperatur (T_g) des Polymers, und mit einer Geschwindigkeit (V_a) im Bereich von 10 bis 30 m/min, und das Zusammenführen mit einer Führungsspitze für dosiertes Appretieren in einem Abstand (L_c) im Bereich von 50 cm bis (50 + 90 $dpf^{1/2}$) cm erfolgt und die Abzugsgeschwindigkeit (V) im Bereich von 2 bis 5 km/min liegt.

6. Verfahren nach einem der Ansprüche 1 bis 4, worin die Filamente einen Denier-Wert im Bereich von 0,6 bis 0,2 und einen Denier-Schwankungsbereich (DS) von weniger als 2 % aufweisen.

7. Spinnorientierte Polyesterfilamente mit einer Feinheit im Bereich von 1 bis 0,2 den pro Filament, wobei der Polyester eine relative Viskosität (LRV) im Bereich von 13 bis 23, einen Schmelzpunkt bei Null-Scherung (T_M°) im Bereich von 240°C bis 265°C und eine Glasumwandlungstemperatur (T_g) des Polymers im Bereich von 40 °C bis 80 °C besitzt, und die Filamente folgendes aufweisen:

(i) einen Kochschrumpf (S) von weniger als dem maximalen Schrumpfpotential (S_m), wobei S_m = [(550-E_B)/6,5] % ist und die prozentuale Reißdehnung (E_B) im Bereich von 40 % bis 160 % liegt,
(ii) eine maximale Schrumpfspannung (ST_{max}) im Bereich von 0,05 bis 0,2 g/d mit einer Spitzentemperatur T (ST_{max}) im Bereich von 5°C bis 30°C über der Glasumwandlungstemperatur (T_g) des Polymers;
(iii) eine Festigkeit bei 7 % Dehnung (T_7) im Bereich von 0,5 bis 1,75 g/d derart, daß das Verhältnis [$(T_B)_n/T_7$] mindestens ($5/T_7$) beträgt, wobei $(T_B)_n$ die normierte Reißfestigkeit ist;
(iv) einen durchschnittlichen Denier-Schwankungsbereich (DS) von weniger als 4 % längs des Fadens.

8. Filamente nach Anspruch 7, wie sie besonders geeignet sind zur Verwendung als Streckvorlagegarne, und die einen Kochschrumpf (S) und einen Trockenwärmeschrumpf (DHS) von mindestens 12 %, eine Reißdehnung (E_B) im Bereich von 80 % bis 160 % und eino Festigkeit bei 7 % Dehnung (T_7) im Bereich von 0,5 bis 1 g/d aufweisen.

9. Filamente nach Anspruch 7, wie sie besonders geeignet sind zur Verwendung als direkt eingesetzte Textilgarne, und die eine Schrumpfdifferenz (ΔS) von weniger als +2 % aufweisen, wobei der Kochschrumpf (S) und der Trokkenwärmeschrumpf (DHS) im Bereich von 2 % bis 12 % liegen, so daß der Denier-Wert der Filamente nach der Schrumpfung kleiner ist als 1, und einen T_7-Wert im Bereich von 1 bis 1,75 g/d, einen (E_B)-Wert im Bereich von 40 % bis 90 % und einen Modul nach dem Strecken (M_{py}) im Bereich von 2 bis 12 g/d aufweisen, wobei M_{py}= (1,2 T_{20}-1,07 T_7)/0,13 ist.

10. Filamente nach Anspruch 7 mit einem Vermögen, gleichmäßig kaltverstreckbar zu sein, und mit einer Schrumpfdifferenz (ΔS) von weniger als + 2 %, wobei der Kochschrumpf (S) und der Trockenwärmeschrumpf (DHS) beide im Bereich von 2 % bis 12 % liegen, einem Beginn der Kaltkristallisation T_{cc} (DSC) von weniger als 105°C sowie einem augenblicklichen Zugmodul von mindestens 0.

11. Gestreckte, spinnorientierte Polyesterfilamente mit Denier-Werten nach dem Kochschrumpf dpf(ABO) im Bereich von 1 bis 0,2 dpf, worin der Polyester eine relative Viskosität (LRV) im Bereich von 13 bis 23, einen Schmelzpunkt des Polymers bei Null-Scherung (T_M°) im Bereich von 240 °C bis 265 °C und eine Glasumwandlungstemperatur (T_g) des Polymers im Bereich von 40°C bis 80°C besitzt, und die gestreckten Filamente folgendes aufweisen:

(i) einen Kochschrumpf (S) und einen Trockenwärmeschrumpf (DHS) im Bereich von 2 % bis 12 %;
(ii) eine Festigkeit bei 7 % Dehnung (T_7) von mindestens 1 g/d, so daß das Verhältnis [$(T_B)_n/T_7$] mindestens ($5/T_7$) beträgt, wobei $(T_B)_n$ die normierte Reißfestigkeit ist, und die Reißdehnung (E_B) im Bereich von 15 % bis 55 % liegt;
(iii) einen Modul nach dem Strecken (M_{py}) im Bereich von 5 bis 25 g/d;
(iv) einen durchschnittlichen Denier-Schwankungsbereich (DS) von weniger als 4 % längs des Fadens.

12. Gebauschte spinnorientierte Polyesterfilamente mit einer Feinheit im Bereich von 1 bis 0,2 dpf (nach dem Kochschrumpf), worin der Polyester eine relative Viskosität (LRV) im Bereich von 13 bis 23, einen Schmelzpunkt des Polymers bei Null-Scherung (T_M°) im Bereich von 240 °C bis 265 °C und eine Glasumwandlungstemperatur (T_g) des Polymers im Bereich von 40 °C bis 80 °C besitzt, und die Filamente folgendes aufweisen:

(i) einen Kochschrumpf (S) und einen Trockenwärmeschrumpf im Bereich von 2 % bis 12 %;
(ii) eine Festigkeit bei 7 % Dehnung (T_7) von mindestens etwa 1 g/d und eine Reißdehnung (E_B) im Bereich von 15 % bis 55 %, wobei der Modul nach dem Strecken (M_{py}) im Bereich von 5 bis 25 g/d liegt.

13. Filamente nach Anspruch 11 oder 12, worin die Filamente weiter gekennzeichnet sind durch eine Spitzentemperatur bei einem dynamischen Verlustmodul T($E"_{max}$) von weniger als 115°C.

14. Filamente nach Anspruch 11 oder 12, worin die Filamente weiter gekennzeichnet sind durch eine relativen Dispersionsfarbstoffwert (RDDR) von mindestens 0,1.

15. Filamente nach einem der Ansprüche 7 bis 14, worin die Filamente einen Formfaktor (SF) von mindestens 1,25 besitzen.

16. Filamente nach einem der Ansprüche 7 bis 15, worin die Filamente einen Denier-Wert im Bereich von 0,8 bis 0,2 dpf besitzen.

17. Filamente nach einem der Ansprüche 7 bis 16, worin die Filamente einen durchschnittlichen Denier-Schwankungsbereich (DS) von weniger als 2 % längs des Fadens aufweisen.

18. Filamente nach einem der Ansprüch 7 bis 17, worin die Polyesterfaser Struktureinheiten aus Ethylen-5-M-sulfoisophthalat im Bereich von 1 bis 3 Mol-% enthält, wobei M ein Alkalimetallkation ist.

19. Filamente nach einem der Ansprüche 7 bis 18, worin der Polyester im wesentlichen Poly(ethylenterephthalat) ist, bestehend aus ersten einander abwechselnden Hydrocarbolendioxy-Struktureinheiten A [-O-C_2H_4-O-] und Hydrocarbolendicarbonyl-Struktureinheiten B [-C-(O)-C_6H_4-C(O)-], modifiziert mit kleineren Anteilen an anderen Hydrocarbolendioxy-Struktureinheiten A und/oder Hydrocarbolendicarbonyl-Struktureinheiten B, die sich von den ersten einander abwechselnden Hydrocarbolendioxy-struktureinheiten A und Hydrocarbolendicarbonyl-Struktureinheiten B unterscheiden, so daß ein Polyesterpolymer mit einem Schmelzpunkt bei Null-Scherung ($T_M°$) im Bereich von 240 °C bis 265 °C und einer Glasumwandlungstemperatur (T_g) im Bereich von 40 °C bis 80 °C vorliegt.

Revendications

1. Un procédé de préparation de filaments fins de polyester orienté au filage d'un denier compris entre 1 et 0,2, où

(i) le polymère de polyester est choisi de façon à présenter une viscosité relative (LRV) comprise entre 13 et 23, un point de fusion à cisaillement zéro ($T_M°$) compris entre 240°C et 265°C, et une température de transition vitreuse (Tg) comprise entre 40°C et 80°C;
(ii) ledit polyester est fondu et chauffé à une température (T_p) comprise entre 25°C et 55°C, de préférence compris entre 30°C et 50°C, au-dessus du point de fusion apparent du polymère $(T_M)_a$;
(iii) la masse fondue obtenue est filtrée suffisamment vite pour que le temps de séjour (t_r) dans la cavité du filtre soit inférieure à 4 minutes;
(iv) la masse fondue filtrée est extrudée par des capillaires de filières à un débit massique (w) compris entre 0,07 et 0,7 g par minute (g/min), et le capillaire est choisi de façon à ce que sa surface en section transversale (A_c) soit de 125x10^{-6} cm^2 (19,4 $mils^2$) à 1250x10^{-6} cm^2 (194 $mils^2$), de préférence entre 125x10^{-6} cm^2 (19,4 $mils^2$) à 750x10^{-6} cm^2 (116,3 $mils^2$) et une longueur (L) et un diamètre (D_{RND}) tel que le rapport (L/D_{RND}) soit d'au moins 1,25 et de préférence inférieur à 6.
(v) protection de la masse fondue extrudée du refroidissement direct au moment où il sort des capillaires de filières sur une distance (L_{DQ}) d'au moins 2 cm et inférieure à (12 dpf $^{1/2}$) cm, où dpf est le denier par filament de filaments fins de polyester orientés au filage;
(vi) la masse fondue extrudée est refroidie en dessous de la température de transition vitreuse du polymère (Tg) et atténuée à une déformation de la ligne de filage apparente (ε_a) comprise entre 5,7 et 7,6, et à une contrainte de ligne de filage interne apparente (σ_a) comprise entre 0,045 et 0,195 g par denier (g/d).
(vii) les filaments refroidis sont ensuite refroidis en une mèche multifilamentaire en utilisant une surface à faible friction à une distance de la phase de la filière (L_c) comprise entre 50 cm et 140 cm, et
(viii) la mèche multifilamentaire est tirée à une vitesse (V) comprise entre 2 et 6 kilomètres par minute et bobinée à une vitesse qui est de 95 à 100% de la vitesse de reprise.

2. Un procédé selon la revendication 1, dans lequel ledit polymère contient de 1 à 3 moles% de motifs structuraux éthylène-5-M-sulfo-isophtalate où M est un cation de métal alcalin.

3. Un procédé selon la revendication 1, dans lequel ledit polyester est essentiellement du poly(éthylène téréphtalate) composé de premiers motifs structuraux alternés hydrocarbolènedioxy A [-O-C_2H_4-O-] et motifs structuraux hydrocarbolènedicarbonyle B [-(O)C-C_6H_4-C(O)] modifiés par des quantités mineures d'autres motifs structuraux hydrocarbolènedioxy A et/ou motifs structuraux hydrocarbolènedicarbonyle B différents des motifs structuraux hydrocarbolènedioxy alternants A et des motifs hydrocarbolènedicarbonyle B de façon à obtenir un polymère de polyester avec un point de fusion à cisaillement (T_M°) compris entre 240°C et 265°C et une température de transition vitreuse (Tg) comprise entre 40°C et 80°C.

4. Un procédé selon la revendication 1, dans lequel la déformation en ligne (ε_a) est comprise entre 6 et 7.3, et la contrainte en ligne interne apparente (σ_a) est réglée de façon à obtenir une orientation moyenne, telle que représentée par la ténacité à 7% d'allongement (T_7) comprise entre 0,5 et 1,75 g/d.

5. Un procédé selon l'une quelconque des revendications 1 à 4, dans lequel la température de polymère (Tp) est comprise entre 30°C et 50°C au-dessus du point de fusion apparent du polymère $(T_M)_a$, la surface de la section du capillaire de filière (A_c) est comprise entre $125x10^{-6}$ cm_2 et $750x10^{-6}$ cm^2, la densité de filament extrudée ($\neq_c$/A_o) est comprise entre 2,5 et 25 filaments par cm^2, et ledit refroidissement de la masse fondue extrudée est effectuée en dirigeant radialement de l'air ayant à peu près une température (T_a) inférieure à environ la température de transition vitreuse du polymère (T_g) et une vitesse (V_a) comprise entre 10 et 30 m/min, et ladite convergence étant effectuée par un guide de pointe doseuse d'application d'apprêt à une distance (L_c) comprise entre 50 cm et (50+90 $dpf^{1/2}$) cm, et que la vitesse de reprise (V) est comprise entre 2 et 5 km/min.

6. Un procédé selon une quelconque des revendications 1 à 4, dans lequel les filaments ont un denier compris entre 0,6 et 0,2 et une dispersion de denier (DS) inférieure à 2%.

7. Filaments de polyester orienté de filage de finesse comprise entre 1 et 0,2 denier par filament, dans lesquels ledit polyester présente une viscosité relative (LRV) comprise entre 13 et 23, un point de fusion du polymère à cisaillement zéro (T_M°) compris entre 240°C et 265°C, et une température de transition vitreuse du polymère (Tg) comprise entre 40°C et 80°C; et lesdits filaments ont:

   (i) un retrait à l'ébouillantage (S) inférieur au potentiel de retrait maximum (S_m) dans lequel S_m = [(550-E_B)/6,5]% et l'allongement à la rupture % (E_B) compris entre 40% et 160%.
   (ii) l'obtention de retrait maximum (ST_{max}) compris entre 0,05 et 0,2 g/d, avec une température maximum, T (ST_{max}), comprise entre 5°C et 30°C au-dessus de la température de transition vitreuse du polymère (Tg);
   (iii) une ténacité à 7% d'allongement (T_7) comprise entre 0,5 et 1,75 g/d, telle que le rapport [$(T_B)_n/T_7$] est au moins inférieur à ($5/T_7$), où $(T_B)_n$ est la ténacité à la rupture normalisée.
   (iv) une dispersion moyenne de denier sur la longueur (DS) inférieure à 4%.

8. Filaments selon la revendication 7, tels qu'ils conviennent particulièrement comme fils d'alimentation d'étirage et qui présentent un retrait à l'ébouillantage (S) et un retrait à la chaleur sèche d'au moins 12%, un allongement à la rupture (E_B) compris entre 80% et 160%, et une ténacité à 7% (T_7) compris entre 0,5 et 1 g/d.

9. Filaments selon la revendication 7, tels qu'ils soient particulièrement convenables pour servir pour fils textiles directement utilisables et ayant un différentiel de retrait (ΔS) inférieur à +2%, et dans lequel le retrait à l'ébouillantage (S) et le retrait à la chaleur sèche (DHS) sont comprises entre 2% et 12%, tel que le denier de filament après retrait soit inférieur à 1; et un T_7 compris entre 1 et 1,75 g/d, un (E_B) compris entre 40% et 90%, un module post-élastique (M_{py}) compris entre 2 et 12 g/d, où M_{py} = (1,2 T_{20} - 1,07 T_7)/0,13.

10. Filaments selon la revendication 7 ayant l'aptitude à être retirés à froid uniformément et ayant un différentiel (ΔS) inférieur à +2%, un retrait à l'ébouillantage (S) et un retrait à la chaleur sèche (DHS) tous deux compris entre 2% et 12%, un début de cristallisation froide T_{cc}(DSC) inférieur à 105°C et un module de tension instantané d'au moins 0.

11. Filaments de polyester orienté de filage étiré de deniers après ébouillantage, dpf(ABO) compris entre 1 et 0,2 dpf, ledit polyester ayant une viscosité relative (LRV) comprise entre 13 et 23, un point de fusion du polymère à cisaillement zéro (T_M°) compris entre 240°C et 265°C et une température de transition vitreuse de polymère (T_g)

comprise entre 40°C et 80°C, et lesdits filaments étirés ayant:

(i) un retrait à l'ébouillantage (S) et un retrait à la chaleur sèche (DHS) compris entre 2% et 12%;
(ii) une ténacité à 7% d'allongement (T_7) d'au moins 1 g/d, tel que $[(T_B)_n/T_7]$ soit d'au moins $(5/T_7)$ où $(T_B)_n$ est la ténacité à la rupture normalisée et l'allongement à la rupture (E_B) est compris entre 15% et 55%.
(iii) le module post-élastique (M_{py}) est compris entre 5 et 25 g/d;
(iv) une dispersion moyenne de denier sur la longueur (DS) inférieure à 4%.

12. Filaments de polyester orienté au filage gonflé d'une finesse comprise entre 1 et 0,2 dpf (après retrait à l'ébulltion) dans lesquels ledit polyester présente une viscosité relative (LRV) comprise entre 13 et 23, un point de fusion du polymère à cisaillement zéro ($T_M°$) compris entre 240°C et 265°C, et une température de transition vitreuse du polymère (T_g) comprise entre 40°C et 80°C; et lesdits filaments ont:

(i) un retrait à l'ébouillantage (S) et un retrait à la chaleur sèche (DHS) compris entre 2% et 12%;
(ni) une ténacité à l'allongement à 7% (T_7) d'au moins environ 1 g/d et un allongement à la rupture (E_B) compris entre 15% et 55%. avec un module post-élastique (M_{py}) compris entre 5 et 25 g/d.

13. Filaments selon la revendication 11 ou 12, dans lesquels les filaments sont en outre caractérisés par une température maximum de module de perte dynamique $T(E"_{max})$ de moins de 115°C.

14. Filaments selon la revendication 12, dans lesquels les filaments sont en outre caractérisés par une vitesse relative de teinture disperse (RDDR) d'au moins 0,1.

15. Filaments selon l'une quelconque des revendications 7 à 14, dans lesquels des filaments présentent un facteur de forme (SF) d'au moins 1,25.

16. Filaments selon l'une des revendications 7 à 15, où les filaments ont un denier compris entre 0,8 et 0,2 dpf.

17. Filaments selon l'une quelconque des revendications 7 à 16, dans lesquels les filaments ont une dispersion de deniers sur la longueur (DS) inférieure à 2%.

18. Filaments selon l'une quelconque des revendications 7 à 17, dans lesquels lesdites fibres de polyester contiennent de 1 à 3 moles% de motifs structuraux 5-éthylène-M-sulso-isophtalate où M est un cation de métal alcalin.

19. Filaments selon l'une quelconque des revendications 7 à 18, dans lesquels ledit polyester est essentiellement un poly(éthylène téréphtalate), constitué de premiers motifs structuraux alternés hydrocarbolènedioxy A [-O-C_2H_4-O-] et motifs structuraux hydrocarbolènedicarbonyle B [-(O)C-C_6H_4-C(O)] modifiés par des quantités mineures d'autres motifs structuraux hydrocarbolènedioxy A et/ou motifs structuraux hydrocarbolènedicarbonyle B différents des motifs structuraux hydrocarbolènedioxy alternants A et des motifs hydrocarbolènedicarbonyle B de façon à obtenir un polymère de polyester avec un point de fusion à cisaillement ($T_M°$) compris entre 240°C et 265°C et une température de transition vitreuse (Tg) comprise entre 40°C et 80°C.

FIG.1

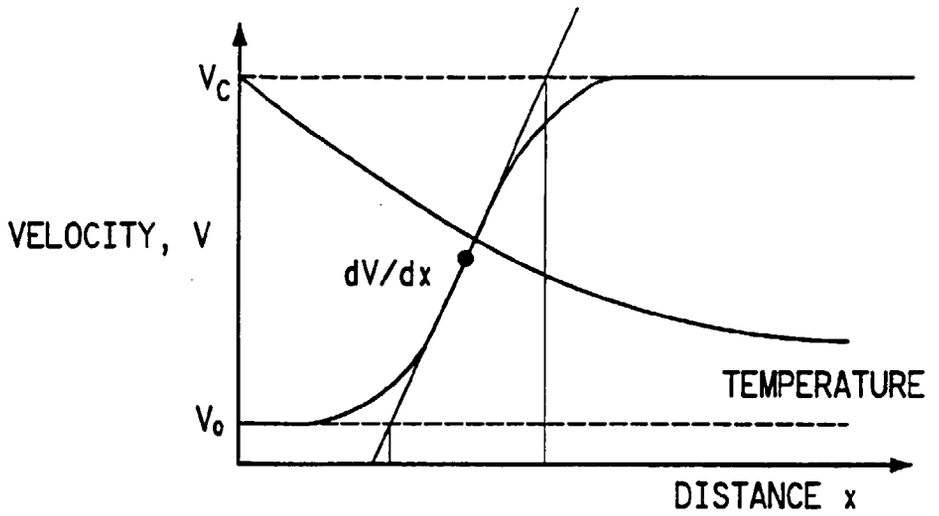

V_C
VELOCITY, V
dV/dx
TEMPERATURE
V_o
DISTANCE x

FIG.2

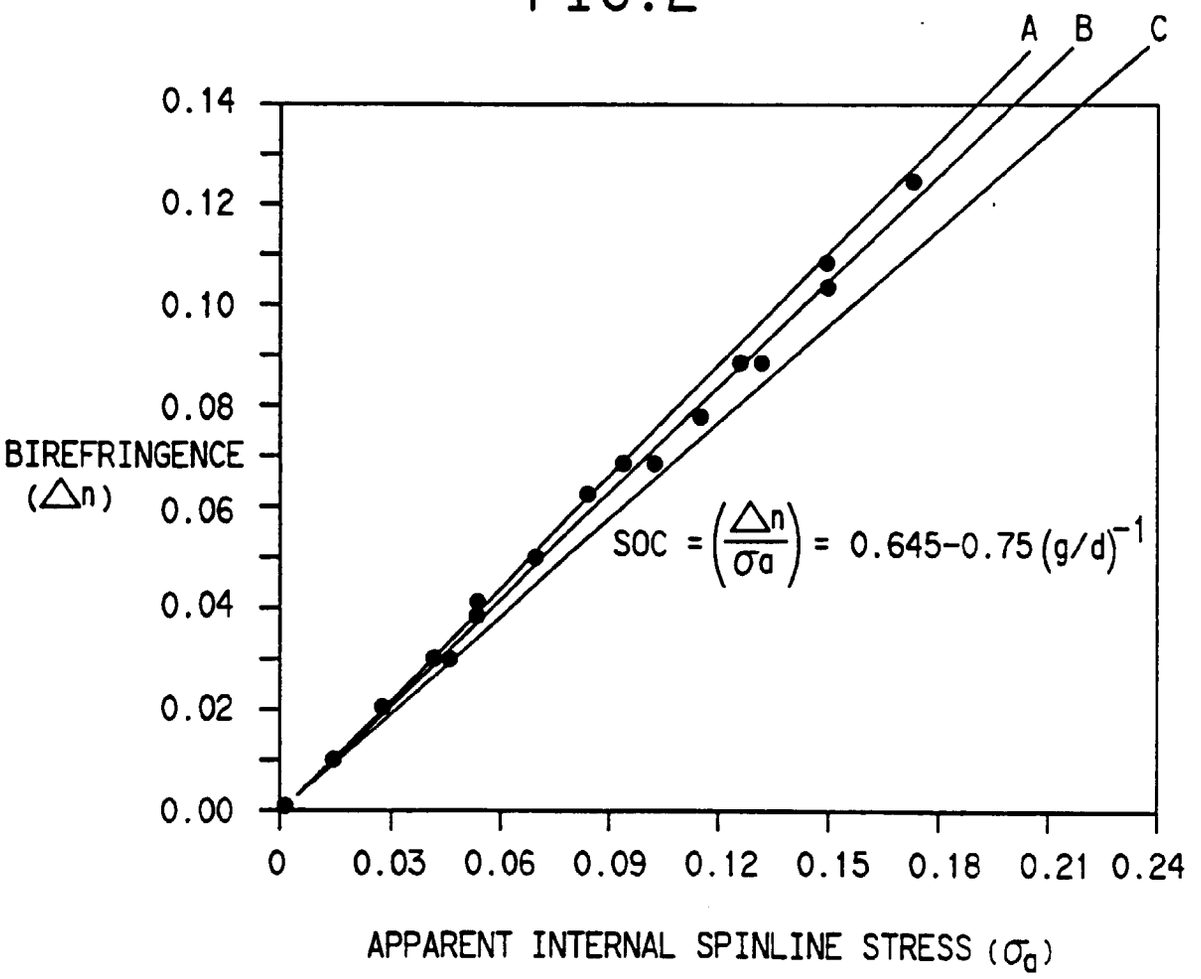

A
B
C
0.14
0.12
0.10
0.08
BIREFRINGENCE
(△n)
0.06
0.04
0.02
0.00
$SOC = \left(\frac{\triangle n}{\sigma a}\right) = 0.645 - 0.75\,(g/d)^{-1}$
0
0.03
0.06
0.09
0.12
0.15
0.18
0.21
0.24
APPARENT INTERNAL SPINLINE STRESS (σ_a)

FIG.3

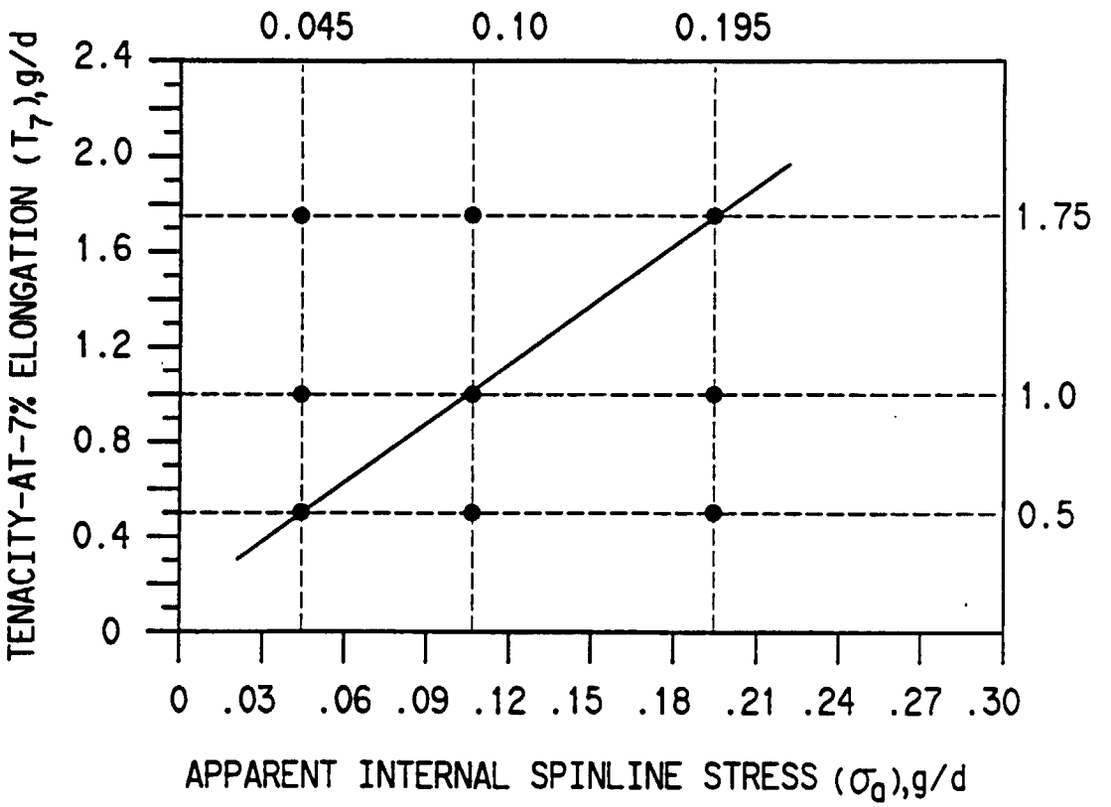

0.045
0.10
0.195
2.4
2.0
1.6
1.2
0.8
0.4
0
1.75
1.0
0.5
0 .03 .06 .09 .12 .15 .18 .21 .24 .27 .30
TENACITY-AT-7% ELONGATION (T_7),g/d
APPARENT INTERNAL SPINLINE STRESS (σ_0),g/d

FIG.4

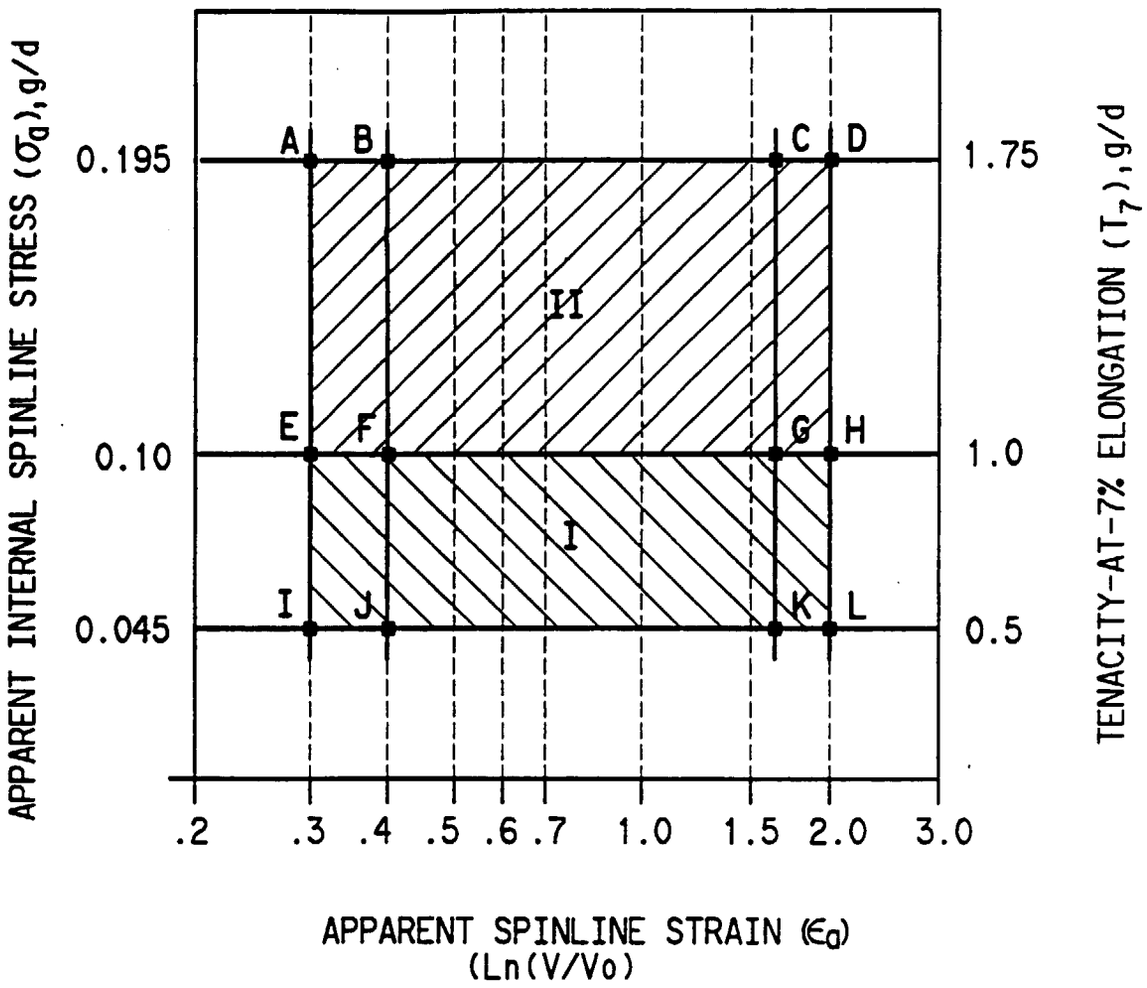

APPARENT INTERNAL SPINLINE STRESS (σ_a), g/d
0.195
0.10
0.045
A
B
C
D
E
F
G
H
I
J
K
L
II
I
1.75
1.0
0.5
TENACITY-AT-7% ELONGATION (T_7), g/d
.2
.3
.4
.5
.6
.7
1.0
1.5
2.0
3.0
APPARENT SPINLINE STRAIN (ϵ_a)
(Ln(V/Vo)

FIG.5

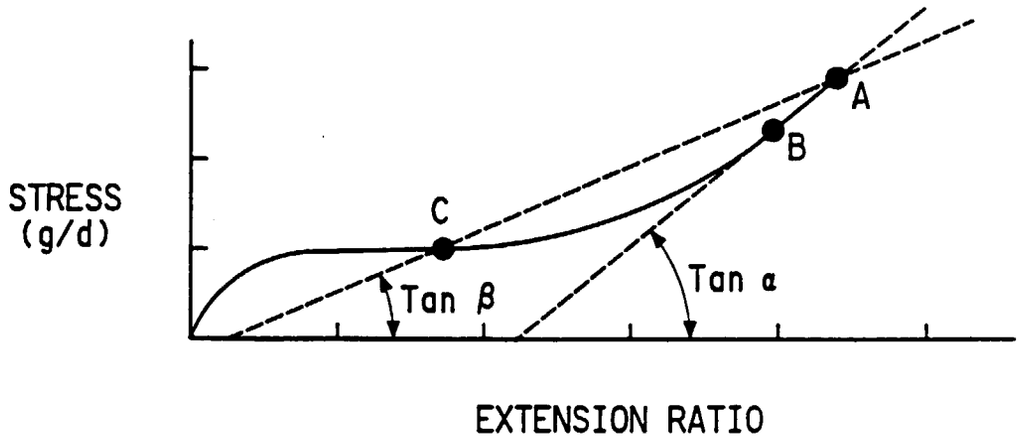
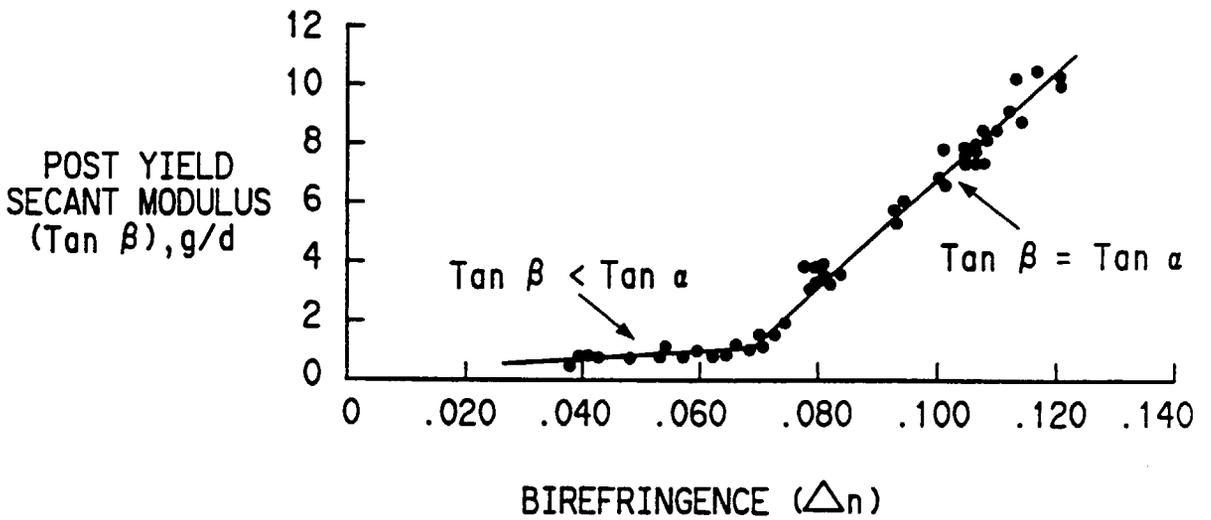

STRESS
(g/d)
A
B
C
Tan β
Tan α
EXTENSION RATIO

FIG.6


POST YIELD
SECANT MODULUS
(Tan β), g/d
12
10
8
6
4
2
0
0
.020
.040
.060
.080
.100
.120
.140
Tan β < Tan α
Tan β = Tan α
BIREFRINGENCE (△n)

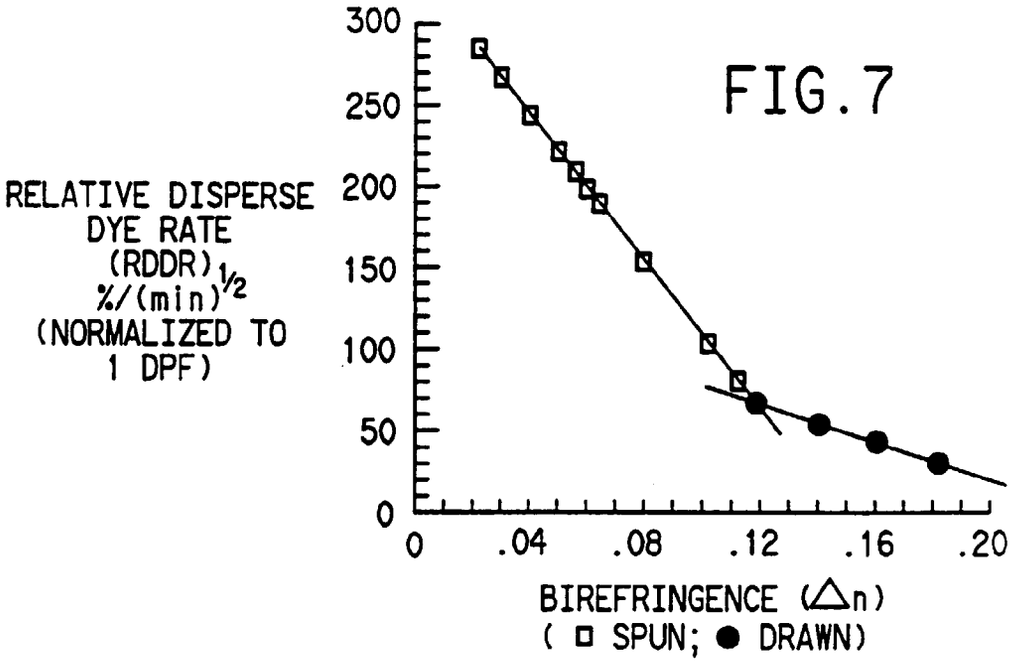

RELATIVE DISPERSE DYE RATE (RDDR)$_{1/2}$ %/(min)$^{1/2}$ (NORMALIZED TO 1 DPF)
300
250
200
150
100
50
0
0
.04
.08
.12
.16
.20
BIREFRINGENCE (△n)
(□ SPUN; ● DRAWN)

FIG.7

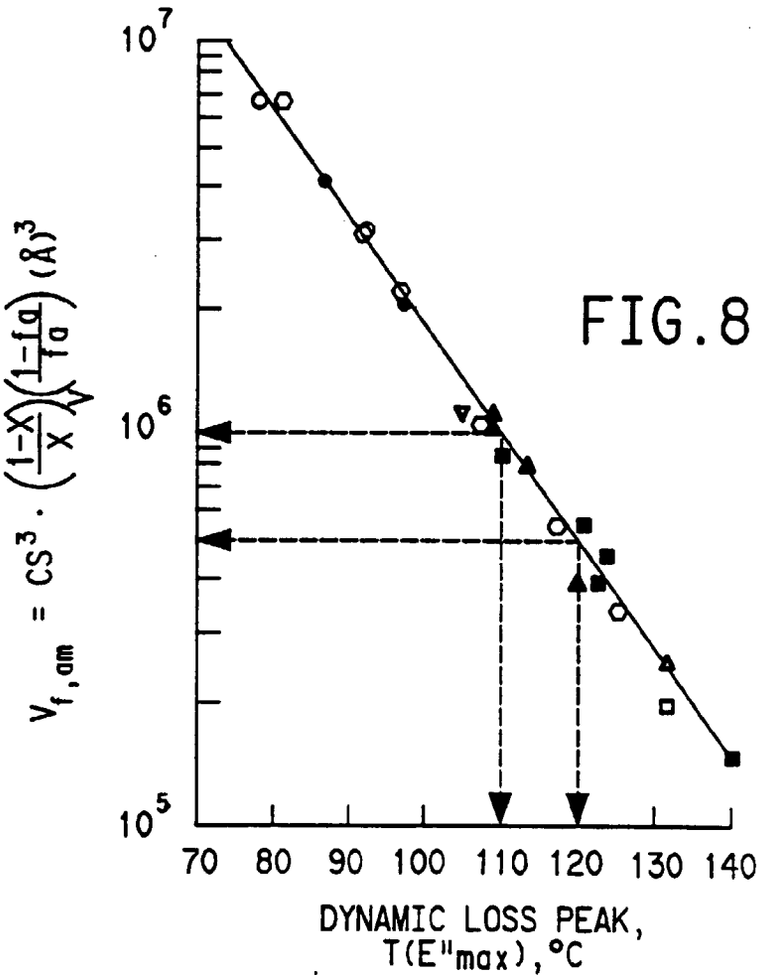

$V_{f,am} = CS^3 \cdot \left(\frac{1-X}{X}\right)\left(\frac{1-f_a}{f_a}\right)(\text{Å})^3$
10^7
10^6
10^5
70
80
90
100
110
120
130
140
DYNAMIC LOSS PEAK, T(E"max), °C

FIG.8

FIG.9

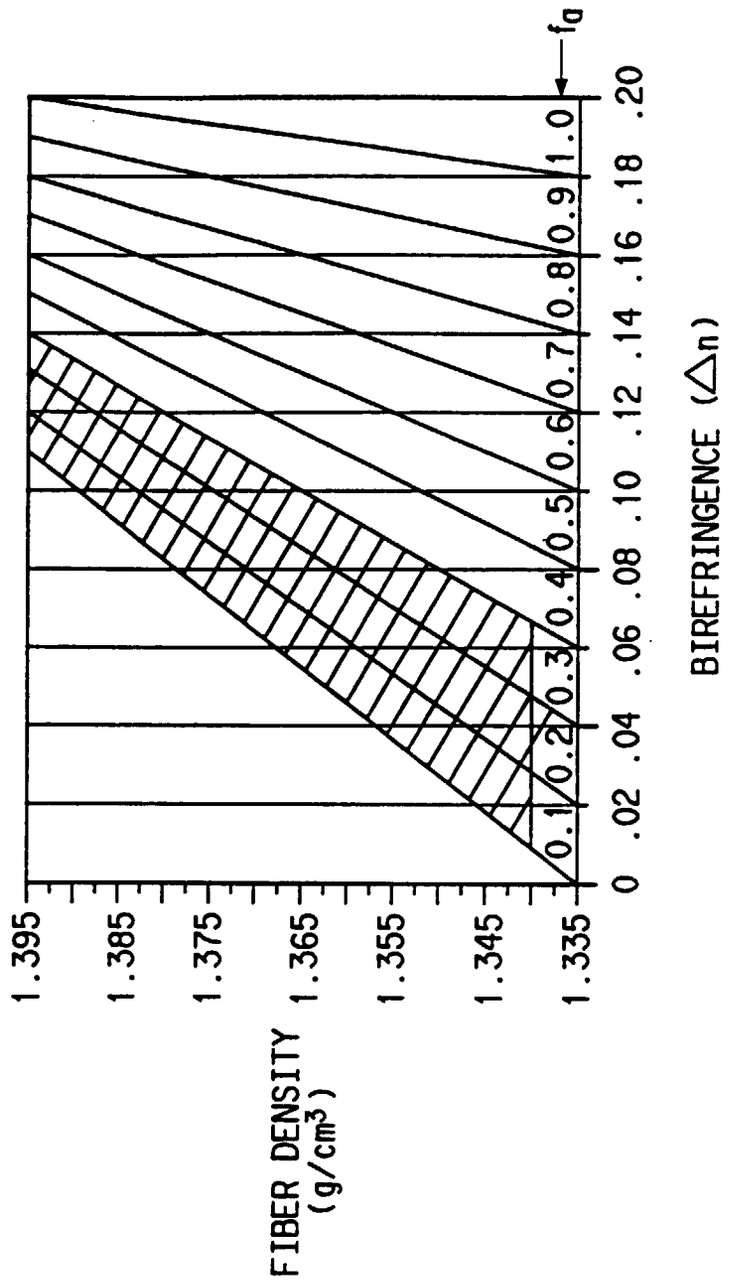

f_a
1.0
0.9
0.8
0.7
0.6
0.5
0.4
0.3
0.2
0.1
0 .02 .04 .06 .08 .10 .12 .14 .16 .18 .20
BIREFRINGENCE (△n)
1.395
1.385
1.375
1.365
1.355
1.345
1.335
FIBER DENSITY (g/cm³)

FIG.10

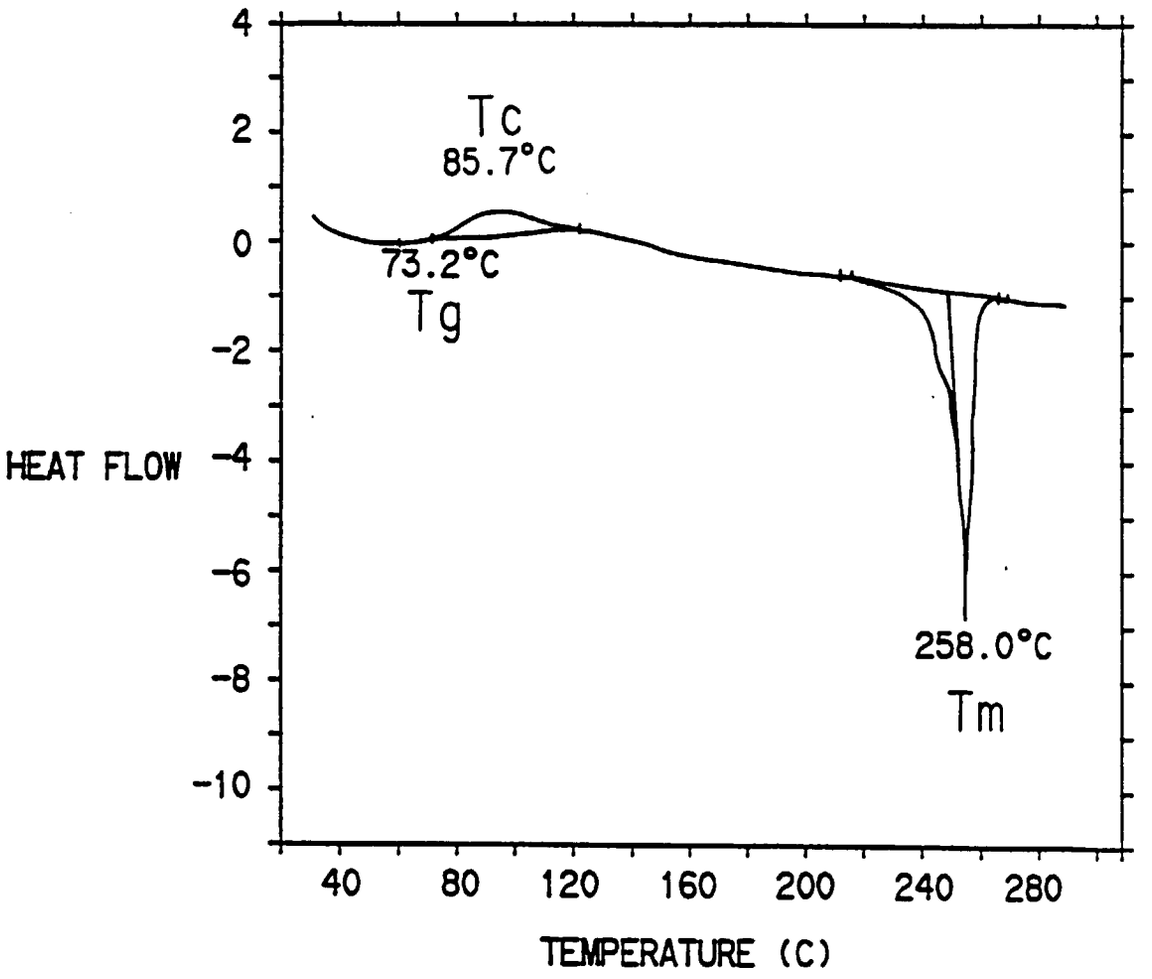

4
2
0
-2
-4
-6
-8
-10
HEAT FLOW
Tc
85.7°C
73.2°C
Tg
258.0°C
Tm
40
80
120
160
200
240
280
TEMPERATURE (C)

FIG. 11

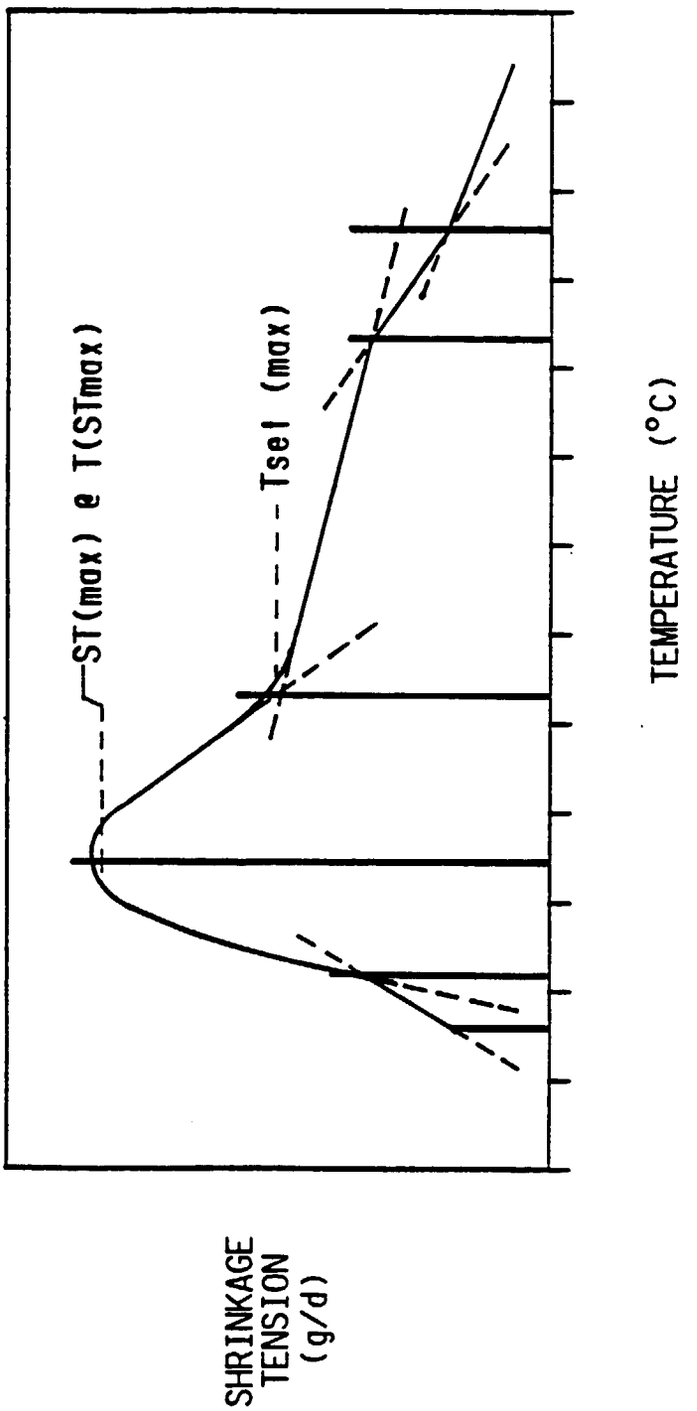


FIG. 12

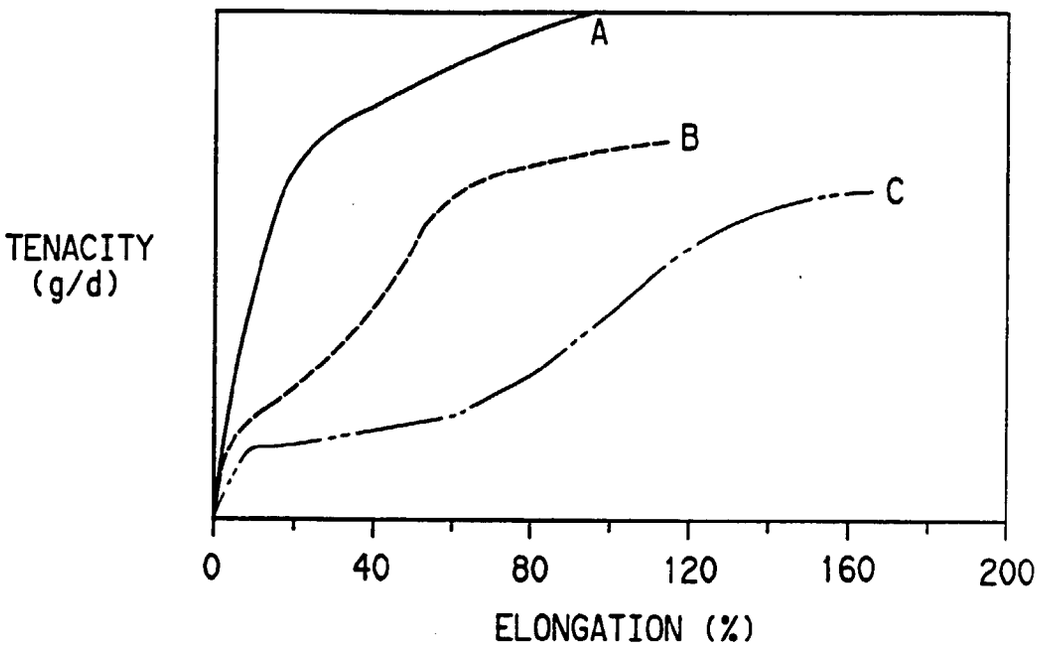

A
B
C
TENACITY
(g/d)
0
40
80
120
160
200
ELONGATION (%)

FIG. 13

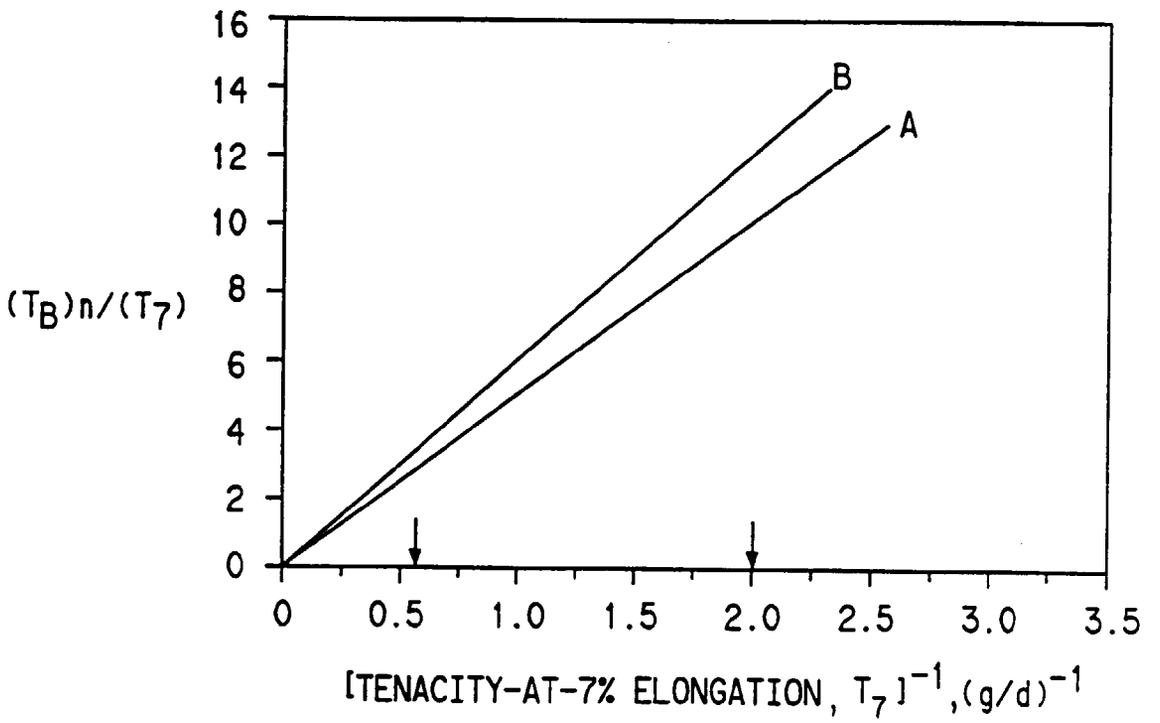

16
14
12
10
8
6
4
2
0
B
A
$(T_B)n/(T_7)$
0
0.5
1.0
1.5
2.0
2.5
3.0
3.5
[TENACITY-AT-7% ELONGATION, T_7]$^{-1}$,(g/d)$^{-1}$

FIG.14

