

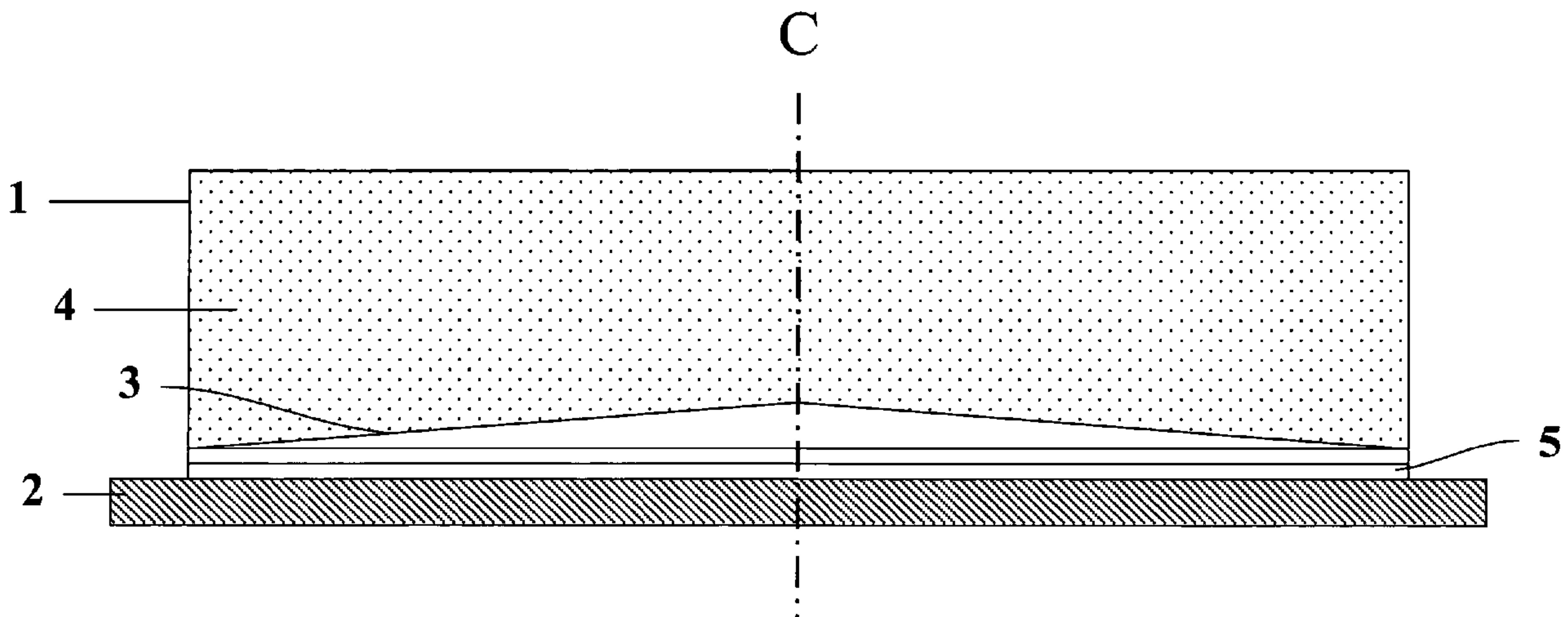


(86) Date de dépôt PCT/PCT Filing Date: 2006/12/20
(87) Date publication PCT/PCT Publication Date: 2007/10/25
(45) Date de délivrance/Issue Date: 2013/11/12
(85) Entrée phase nationale/National Entry: 2008/09/30
(86) N° demande PCT/PCT Application No.: EP 2006/012334
(87) N° publication PCT/PCT Publication No.: 2007/118510
(30) Priorité/Priority: 2006/04/13 (EP06007808.6)

(51) Cl.Int./Int.Cl. *C25C 3/16* (2006.01)
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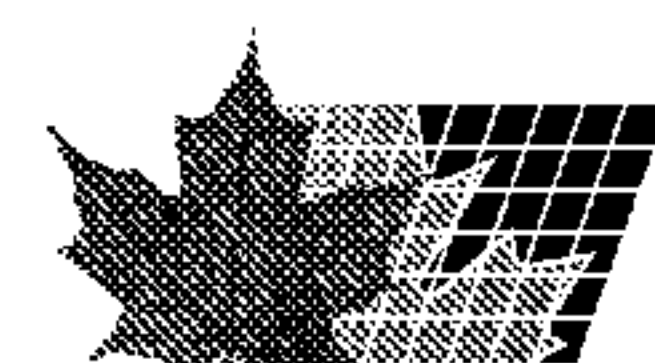
(54) Titre : CATHODES POUR CELLULE D'ELECTROLYSE DE PRODUCTION D'ALUMINIUM A MODELE DE FENTE
NON PLAN

(54) Title: CATHODES FOR ALUMINIUM ELECTROLYSIS CELL WITH NON-PLANAR SLOT DESIGN



(57) **Abrégé/Abstract:**

Cathodes (1) for aluminium electrolysis cells consisting of cathode blocks (4) and current collector bars (2) attached to those blocks whereas the cathode slots (3) receiving the collector bar have a higher depth at the center than at both lateral edges of the cathode block. Additionally, the collector bar thickness is higher at the center than at both lateral edges of the cathode block. This cathode design provides a more even current distribution and, thus, a longer useful lifetime of such cathodes and increased cell productivity.



(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
25 October 2007 (25.10.2007)

PCT

(10) International Publication Number
WO 2007/118510 A3

(51) International Patent Classification:
C25C 3/16 (2006.01)

(21) International Application Number:
PCT/EP2006/012334

(22) International Filing Date:
20 December 2006 (20.12.2006)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
06007808.6 13 April 2006 (13.04.2006) EP

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(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM,

AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT, HN, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KN, KP, KR, KZ, LA, LC, LK, LR, LS, LT, LU, LV, LY, MA, MD, MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RS, RU, SC, SD, SE, SG, SK, SL, SM, SV, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW.

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IS, IT, LT, LU, LV, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

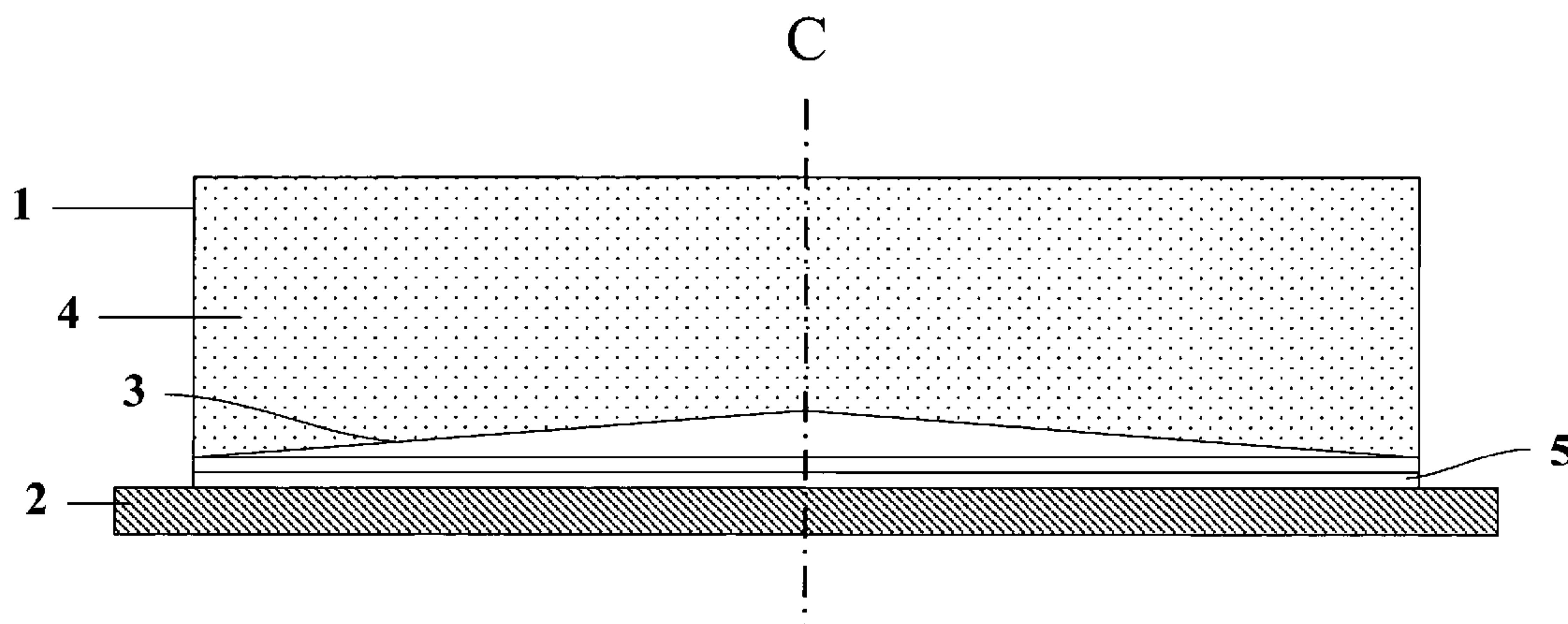
Published:

- with international search report
- before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

(88) Date of publication of the international search report:
13 December 2007

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: CATHODES FOR ALUMINIUM ELECTROLYSIS CELL WITH NON-PLANAR SLOT DESIGN



(57) Abstract: Cathodes (1) for aluminium electrolysis cells consisting of cathode blocks (4) and current collector bars (2) attached to those blocks whereas the cathode slots (3) receiving the collector bar have a higher depth at the center than at both lateral edges of the cathode block. Additionally, the collector bar thickness is higher at the center than at both lateral edges of the cathode block. This cathode design provides a more even current distribution and, thus, a longer useful lifetime of such cathodes and increased cell productivity.

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Cathodes for aluminium electrolysis cell with non-planar slot design

The invention relates to cathodes for aluminium electrolysis cells consisting of
5 cathode blocks and current collector bars attached to those blocks whereas the
cathode slots receiving the collector bar have a non-planar design. Further, the
collector bar design is adapted to such non-planar slot design.

As a result, a more uniform current distribution along the cathode length is achieved.
This provides longer useful lifetime of such cathodes by reduced cathode wear and
10 thus increased cell productivity.

Aluminium is conventionally produced by the Hall-Heroult process, by the electrolysis
of alumina dissolved in cryolite-based molten electrolytes at temperatures up to
around 970 °C. A Hall-Heroult reduction cell typically has a steel shell provided with
15 an insulating lining of refractory material, which in turn has a lining of carbon
contacting the molten constituents. Steel-made collector bars connected to the
negative pole of a direct current source are embedded in the carbon cathode
substrate forming the cell bottom floor. In the conventional cell design, steel cathode
collector bars extend from the external bus bars through each side of the electrolytic
20 cell into the carbon cathode blocks.

Each cathode block has at its lower surface one or two slots or grooves extending
between opposed lateral ends of the block to receive the steel collector bars. Those
slots are machined typically in a rectangular shape. In close proximity to the
electrolysis cell, these collector bars are positioned in said slots and are attached to
25 the cathode blocks most commonly with cast iron (called "rodding") to facilitate
electrical contact between the carbon cathode blocks and the steel. The thus
prepared carbon or graphite made cathode blocks are assembled in the bottom of
the cell by using heavy equipment such as cranes and finally joined with a ramming
mixture of anthracite, graphite, and coal tar to form the cell bottom floor. A cathode
30 block slot may house one single collector bar or two collector bars facing each other
at the cathode block center coinciding with the cell center. In the latter case, the gap
between the collector bars is filled by a crushable material or by a piece of carbon or
by tamped seam mix or preferably by a mixture of such materials.

35 Hall-Heroult aluminum reduction cells are operated at low voltages (e.g. 4-5 V) and

high electrical currents (e.g. 100,000-400,000 A). The high electrical current enters the reduction cell from the top through the anode structure and then passes through the cryolite bath, through a molten aluminum metal pad, enters the carbon cathode block, and then is carried out of the cell by the collector bars.

5 The flow of electrical current through the aluminum pad and the cathode follows the path of least resistance. The electrical resistance in a conventional cathode collector bar is proportional to the length of the current path from the point the electric current enters the cathode collector bar to the nearest external bus. The lower resistance of the current path starting at points on the cathode collector bar closer to the external
10 bus causes the flow of current within the molten aluminum pad and carbon cathode blocks to be skewed in that direction. The horizontal components of the flow of electric current interact with the vertical component of the magnetic field in the cell, adversely affecting efficient cell operation.

The high temperature and aggressive chemical nature of the electrolyte combine to
15 create a harsh operating environment. Hence, existing Hall-Heroult cell cathode collector bar technology is limited to rolled or cast mild steel sections. In comparison, potential metallic alternatives such as copper or silver have high electrical conductivity but low melting points and high cost.

Until some years ago, the high melting point and low cost of steel offset its relatively
20 poor electrical conductivity. The electrical conductivity of steel is so poor relative to the aluminum metal pad that the outer third of the collector bar, nearest the side of the pot, carries the majority of the load, thereby creating a very uneven cathode current distribution within each cathode block. Because of the chemical properties, physical properties, and, in particular, the electrical properties of conventional
25 cathode blocks based on anthracite, the poor electrical conductivity of steel had not presented a severe process limitation until recently. In view of the relatively poor conductivity of the steel bars, the same rationale is applicable with respect to the relatively high contact resistance between cathode and cast iron that has so far not played a predominant role in cell efficiency improvement efforts. However, with the
30 general trend towards higher energy costs, this effect becomes a non-negligible factor for smelting efficiency.

Ever since, aluminum electrolysis cells have increased in size as the operating amperage has increased in pursuit of economies of scale. As the operating amperage has been increased, graphite cathode blocks based on coke instead of

anthracite have become common and further the percentage of graphite in cathodes has increased to take advantage of improved electrical properties and maximise production rates. In many cases, this has resulted in a move to partially or fully graphitised cathode blocks. Graphitisation of carbon blocks occurs in a wide temperature range starting at around 2000 °C stretching up to 3000 °C or even beyond. The terms “partially graphitised” or “fully graphitised” cathode relate to the degree of order within the domains of the carbon crystal structure. However, no distinct border line can be drawn between those states. Principally, the degree of crystallisation or graphitisation, respectively, increases with maximum temperature as well as treatment time at the heating process of the carbon blocks. For the description of our invention, we summarise those terms using the terms “graphite” or “graphite cathode” for any cathode blocks at temperatures above around 2000 °C. In turn, the terms “carbon” or “carbon cathode” are used for cathode blocks that have been heated to temperatures below 2000 °C.

Triggered by the utilization of carbon and graphite cathodes providing higher electrical conductivities, increasing attention had to be paid to some technical effects that were so far not in focus:

- wear of cathode blocks
- uneven current distribution
- energy loss at the interface between cathode block and cast iron

All three effects are somewhat interlinked and any technical remedy should ideally address more than one single item of this triade.

The wear of the cathode blocks is mainly driven by mechanical erosion by metal pad turbulence, electrochemical carbon-consuming reactions facilitated by the high electrical currents, penetration of electrolyte and liquid aluminium, as well as intercalation of sodium, which causes swelling and deformation of the cathode blocks and ramming mixture. Due to resulting cracks in the cathode blocks, bath components migrate towards the steel cathode conductor bars and form deposits on the cast iron sealant surface leading to deterioration of the electrical contact and non-uniformity in current distribution. If liquid aluminium reaches the iron surface, corrosion via alloying immediately occurs and an excessive iron content in the aluminium metal is produced, forcing a premature shut-down of the entire cell.

Cathode block erosion does not occur evenly across the block length. Especially in the application of graphite cathode blocks, the dominant failure mode is due to highly localised erosion of the cathode block surface near its lateral ends, shaping the surface into a W-profile and eventually exposing the collector bar to the aluminum metal. In a number of cell designs, higher peak erosion rates have been observed for these higher graphite content blocks than for conventional carbon cathode blocks. Erosion in graphite cathodes may even progress at a rate of up to 60 mm per annum. Operating performance is therefore traded for operating life.

There is a link between the rapid wear rate, the location of the area of maximum wear, and the non-uniformity of the cathode current distribution. Graphite cathodes are more electrically conductive and as a result have a much more non-uniform cathode current distribution pattern and hence suffer from higher wear.

In US 2,786,024 (Wleügel) it is proposed to overcome non-uniform cathode current distribution by utilising collector bars which are bent downward from the cell center so that the thickness of the cathode block between the collector bar and the molten metal pad increases from the cell center towards the lateral edges. This proposal would have required not only curved components but also a significantly modified entire cell design being adapted. These requirements prevented this approach to become used in practise.

US 4,110,179 (Tschopp) describes an aluminium electrolysis cell with uniform electric current density across the entire cell width. This is achieved by gradually decreasing the thickness of the cast iron layer between the carbon cathode blocks and the embedded collector bars towards the edge of the cell. In a further embodiment of that invention, the cast iron layer is segmented by non-conductive gaps with increasing size towards the cell edge. In practise however, it appeared too cumbersome and costly to incorporate such modified cast iron layers.

In US 6,387,237 (Homley et al.) an aluminium electrolysis cell with uniform electric current density is claimed comprising collector bars with copper inserts located in the area next to the cell center thus providing higher electrical conductivity in the cell center region. Again, this method did not find application in aluminium electrolysis cells due to added technical and operational complexities and costs in implementing the described solution.

Neither prior art approach considered the use of cathode blocks with standard external dimensions having a modified slot design and collector bars adapted to such design.

Accordingly, in order to fully realise the operating benefits of carbon and graphite cathode blocks without any trade-offs with regards to existing operational procedures and standard cell designs there is a need for decreasing cathode wear rates and increasing cell life by providing a more uniform cathode current distribution and at the same time providing cathodes with standard external dimensions.

It is therefore an object of the present invention to provide carbon or graphite cathode blocks with standard external dimensions with collector bar slots, characterized in that the slot depth is increasing towards the cathode block center. In cathodes comprising such cathode blocks and standard steel collector bars, the electrical field lines, i.e. the electrical current, are drawn away from the lateral block edges towards the block center thus providing a more uniform current distribution along the cathode block length.

It is another object of the present invention to provide a cathode comprising a carbon or graphite cathode block with standard external dimensions with collector bar slots with increasing depth towards the cathode block center and attached current collector bars, characterized in that the current collector bar thickness is increasing towards the block center at the side facing the slot top face. In the respective cathodes, the electrical field lines, i.e. the electrical current, are drawn away from the lateral block edges towards the block center even more remarkably than in the case of alone changing the slot design. Hence, this embodiment provides a considerable improvement in uniform current distribution along the cathode block length.

It is another object of this invention to provide a method of manufacturing cathodes for aluminium electrolysis cells by manufacturing a carbon or graphite cathode block and attaching a steel collector bar to such lined block.

The invention will now be described in more detail with reference to the accompanying drawings in which:

Figure 1 is a schematic cross-sectional view of a prior art electrolytic cell for aluminum production showing the cathode current distribution.

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Figure 2 shows the schematic side view a prior art cathode.

Figure 3 is a schematic side view of a cathode according to this invention.

Figure 4 A, B is a schematic side view of two embodiments of a cathode block for a cathode according to this invention.

5 Figure 5 is a schematic side view of a cathode according to this invention.

Figure 6 is a schematic side view of a cathode according to this invention.

Figure 7 shows the schematic side view of an electrolytic cell for aluminum production with a cathode according to this invention showing the cathode current distribution.

10 Figure 8 is a schematic three-dimensional top view of a cathode according to this invention.

According to one aspect of the present invention, there is provided a cathode (1) for aluminium electrolysis cells comprising a carbon or graphite cathode block (4) with a collector bar slot (3) receiving one or two steel-made current collector bars (2),
15 wherein the depth of slot (3) is higher at the center (C) in longitudinal direction of the slot (3) than at both lateral edges of the cathode block (4).

According to another aspect of the present invention, there is provided a method of manufacturing a cathode (1) for an aluminium electrolysis cell, comprising the steps: manufacturing a carbon or graphite cathode block (4) with standard external
20 dimensions, machining at least one collector bar slot (3) with increasing depth towards the cathode block center (C) in longitudinal direction of the at least one slot (3), fitting at least one steel collector bar (2) into each of the at least one slot (3).

According to yet another aspect of the present invention, there is provided an aluminum electrolysis cell comprising a cathode (1) as described herein.

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Referring to FIG. 1, there is shown a cross-cut of an electrolytic cell for aluminum production, having a prior art cathode 1. The collector bar 2 has a rectangular transverse cross-section and is fabricated from mild steel. It is embedded in the collector bar slot 3 of the cathode block 4 and connected to it by cast iron 5. The cathode block 4 is made of carbon or graphite by methods well known to those skilled in the art.

Not shown are the cell steel shell and the steel-made hood defining the cell reaction chamber lined on its bottom and sides with refractory bricks. Cathode block 4 is in direct contact with a molten aluminium metal pad 6 that is covered by the molten electrolyte bath 7. Electrical current enters the cell through anodes 8, passes through the electrolytic bath 7 and the molten metal pad 6, and then enters the cathode block 4. The current is carried out of the cell via the cast iron 5 by the cathode collector bars 2 extending from bus bars outside the cell wall. The cell is built symmetrically, as indicated by the cell center line C.

As shown in FIG. 1, electrical current lines 10 in a prior art electrolytic cell are non-uniformly distributed and concentrated more toward ends of the collector bar at the

lateral cathode edge. The lowest current distribution is found in the middle of the cathode 1. Localized wear patterns observed on the cathode block 4 are deepest in the area of highest electrical current density. This non-uniform current distribution is the major cause for the erosion progressing from the surface of a cathode block 4 until it reaches the collector bar 2. That erosion pattern typically results in a “W—
5 shape” of the cathode block 4 surface.

FIG. 2 depicts a prior art cathode 1. The collector bar 2 has a rectangular transverse cross-section and is fabricated from mild steel. It is embedded in the collector bar slot
10 3 of the carbon or graphite cathode block 4 and connected to it by cast iron 5. The prior art slot 3 has a planar top face and a depth ranging between 100 mm to 200 mm. The side faces of slot 3 may be planar or slightly concave (dovetail shape). Although the steel collector bar 2 is secured to such block typically by cast iron 5, ramming paste or high-temperature glue are also appropriate for securing the
15 collector bar 2 to the cathode block 4.

FIG. 3 depicts a cathode 1 according to this invention. The prior art collector bar 2 has a rectangular transverse cross-section and is fabricated from mild steel. It is embedded in the collector bar slot 3 of the carbon or graphite cathode block 4 and
20 connected to it by cast iron 5. The slot 3 has not a planar top face but its depth is increasing towards its center C. The depth of slot 3 at the block center C can range between 10 to 60 mm in relation to the slot 3 depth at the lateral block edges. Taking the slot 3 depth at the lateral block edges of 100 mm to 200 mm into account, the overall depth of slot 3 at the block center C can range between 110 to 260 mm.

25 As shown in FIG. 4 A, B the slot 3 may also have e.g. a semi-circular or semi-ellipsoidal shape and the shape may comprise one or more steps.

Also shown in FIG. 4 A, B is that non-planarity of the top face of slot 3 may not necessarily start directly from lateral block edges but slot 3 may have an initial planar top face at both lateral block edges stretching over 10 to 1000 mm from each edge.

30 The slot 3 according to this invention is machined into the cathode block 4 using the standard manufacturing equipment and procedures as used for prior art slots 3.

In cathodes 1 comprising such inventive cathode blocks 4 and prior art steel collector bars 2, the electrical field lines 10, i.e. the electrical current, are drawn away from the lateral block edges towards the block center C thus providing a more uniform current

distribution along the cathode block 4 length.

FIG. 5 depicts a cathode 1 according to this invention. The cathode block 4 has a non-planar collector bar slot 3 according to this invention, as shown in FIG. 3. The steel collector bar 2 has a triangular shape fitting to the design of slot 3. The thickness of collector bar 2 is increasing at the face facing the slot 3 top face towards its center C.

Although depicted in triangular shape, the collector bar 2 may also have e.g. a semi-circular or semi-ellipsoidal shape. The shape may comprise one or more steps.

In cathodes 1 comprising inventive cathode blocks 4 as well as inventive steel collector bars 2, the electrical field lines 10, i.e. the electrical current, are drawn away from the lateral block edges towards the block center C thus providing a more uniform current distribution along the cathode block 4 length.

FIG. 6 depicts one embodiment of a cathode 1 according to this invention, as described in FIG. 5. In this embodiment, the steel collector bar 2 does not consist of one single piece but is comprises a prior art planar collector bar 2 having several steel plates 9 attached to it at the face facing the slot 3 top face. In this way, the overall non-planar shape of collector bar 2 can be accomplished without the need to provide a non-planar collector bar 2 as one single piece.

The width of the steel plates 9 is similar to that of the collector bar 2. The thickness of the steel plates may be chosen according to design as well as manufacturing considerations. The length of the steel plates 9 decreases stepwise according to design as well as manufacturing considerations. The edges of the steel plates 9 may be rounded or slanted.

At least one such steel plate 9 is attached to the collector bar 2.

The steel plates 9 are fixed to the collector bar 2 as well as to each other by welding, glueing, nuts and bolts or any other commonly known method.

In order to accomplish for the thermal expansion of the steel collector bar as well as steel plates and to ensure proper electrical contact, it is a preferred embodiment of this invention to place resilient graphite foil between the individual steel parts.

Instead of steel other metals may be used such as copper.

It is also within the scope of this invention to fix two short collector bars 2 symmetrically to a block of steel that is higher than the collector bars 2 and to use the such

assembled collector bar 2 to manufacture a cathode 1 according to this invention.

FIG. 7 shows a schematic three-dimensional top view of a cathode 1 according to this invention, depicting the inventive cathode described in FIG. 6. In this figure, the
5 cast iron 5 is not shown for simplicity. FIG. 7 rather shows the setup of the cathode 1 before the cast iron 5 is poured into the collector bar slot 3. In this embodiment, the collector bar 2 is fitted with four steel plates 9, thus providing an overall almost triangular shape of collector bar 2.

10 FIG. 8 shows a schematic cross-sectional view of an electrolytic cell for aluminum production with a cathode 1 according to this invention, as shown in FIG. 6. In comparison to the prior art (FIG. 1), the cell current distribution lines 10 distributed more evenly across the length of the cathode 1 due to the inventive shape of collector bar slot 3 and collector bar 2.

15

Although the drawings show cathode blocks 4, or parts thereof, having a single collector bar slot 3, this invention applies to cathode blocks 4 with more than one collector bar slot 3 in the same manner.

Although the drawings shows cathodes 1 with single collector bars 2 in each collector
20 bar slot 3, this invention applies to cathodes 1 with more than one collector bar 2 in each collector bar slot 3 in the same manner. Alternatively, two short collector bars 2 can be inserted into a collector bar slot 3 and joined at the cathode block 4 center C, both collector bars 2 having each at least one steel plate fixed to them at the end facing the other collector bar 2.

25

The invention is further described by following examples:

Example 1

30 100 parts petrol coke with a grain size from 12 μm to 7 mm were mixed with 25 parts pitch at 150 °C in a blade mixer for 40 minutes. The resulting mass was extruded to a blocks of the dimensions 700 x 500 x 3400 mm (width x height x length). These so-called green blocks were placed in a ring furnace, covered by metallurgical coke and heated to 900 °C. The resulting carbonised blocks were then heated to 2800 °C in a

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lengthwise graphitisation furnace. Afterwards, the raw cathode blocks were trimmed to their final dimensions of 650 x 450 x 3270 mm (width x height x length). Two collector bar slots of 135 mm width and a depth increasing from 165 mm depth at the lateral edges to 200 mm depth at the block center were cut out from each block.

- 5 Afterwards, conventional steel collector bars were fitted into the slots. Electrical connection was made in the conventional way by pouring liquid cast iron into the gap between collector bars and block. The cathodes were placed into an aluminium electrolysis cell. The resulting current density distribution was compared with that of prior art cathodes and proved to be more homogeneous.

10

Example 2

- Cathode blocks trimmed to their final dimensions were manufactured according to example 1. Two collector bar slots of 135 mm width and a depth increasing from 165 mm depth at the lateral edges to 200 mm depth at the block center were cut out from
15 each block.

Two steel collector bars according to this invention were manufactured by welding a single steel plate of 115 mm width, 40 mm thickness and 800 mm length centrically to a steel collector bar of the 115 mm width and 155 mm height at their center at the face eventually facing the slot top face.

- 20 The such manufactured two steel collector bars were fitted into the slots. Electrical connection was made in the conventional way by pouring liquid cast iron into the gap between collector bars and block. The cathodes were placed into an aluminium electrolysis cell. The resulting current density distribution was compared with that of prior art cathodes and proved to be more homogeneous.

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Key to figures:

(1) cathode

(2) steel-made collector bar

5

(3) collector bar slot

(4) carbon or graphite cathode block

10 (5) cast iron

(6) aluminium metal pad

(7) molten electrolyte bath

15

(8) anode

(9) steel plate

20 (10) cell current distribution lines

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CLAIMS:

1. A cathode (1) for aluminium electrolysis cells comprising a carbon or graphite cathode block (4) with a collector bar slot (3) receiving one or two steel-made current collector bars (2), wherein the depth of slot (3) is higher at the center (C) in longitudinal direction of the slot (3) than at both lateral edges of the cathode block (4).
5
2. A cathode (1) according to claim 1, wherein the collector bar slot (3) has a triangular, semi-circular or semi-ellipsoidal shape.
3. A cathode (1) according to claim 1 or 2, wherein the collector bar slot
10 (3) comprises one or more steps.
4. A cathode (1) according to any one of claims 1 to 3, wherein the collector bar slot (3) has an initial planar top face at both lateral block edges stretching over 10 to 1000 mm from each edge.
5. A cathode (1) according to any one of claims 1 to 4, wherein the
15 thickness of the one or two collector bars (2) is higher at the center (C) than at both lateral edges of the cathode block (4).
6. A cathode (1) according to claim 5, wherein the thickness of the one or two collector bars (2) is increased exclusively at the face facing the slot (3) top face.
7. A cathode (1) according to claim 5 or 6, wherein the one or two collector
20 bars (2) have a triangular, semi-circular or semi-ellipsoidal shape.
8. A cathode (1) according to any one of claims 5 to 7, wherein the thickness of the one or two collector bars (2) increases by one or more steps.
9. A cathode (1) according to any one of claims 5 to 8, wherein the one or two collector bars (2) have at least one steel plate (9) attached thereto.

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10. A cathode (1) according to claim 9, wherein resilient graphite foil is placed between the at least one steel plate (9) and the one or two steel collector bars (2) as well as between each subsequently attached steel plate (9).

11. A cathode (1) according to any one of claims 1 to 10 having more than
5 one collector bar slot (3).

12. A method of manufacturing a cathode (1) for an aluminium electrolysis cell, comprising the steps:

- manufacturing a carbon or graphite cathode block (4) with standard external dimensions,

10 - machining at least one collector bar slot (3) with increasing depth towards the cathode block center (C) in longitudinal direction of the at least one slot (3),

- fitting at least one steel collector bar (2) into each of the at least one slot (3).

15 13. A method according to claim 12, wherein the step of fitting the at least one steel collector bar (2) into each of the at least one slots comprises:

- fitting the at least one steel collector bar (2) with increasing thickness at the face facing the collector bar slot (3) top face towards its center (C) into each of the at least one slot (3).

20 14. An aluminium electrolysis cell comprising a cathode (1) as defined in any one of claims 1 to 11.

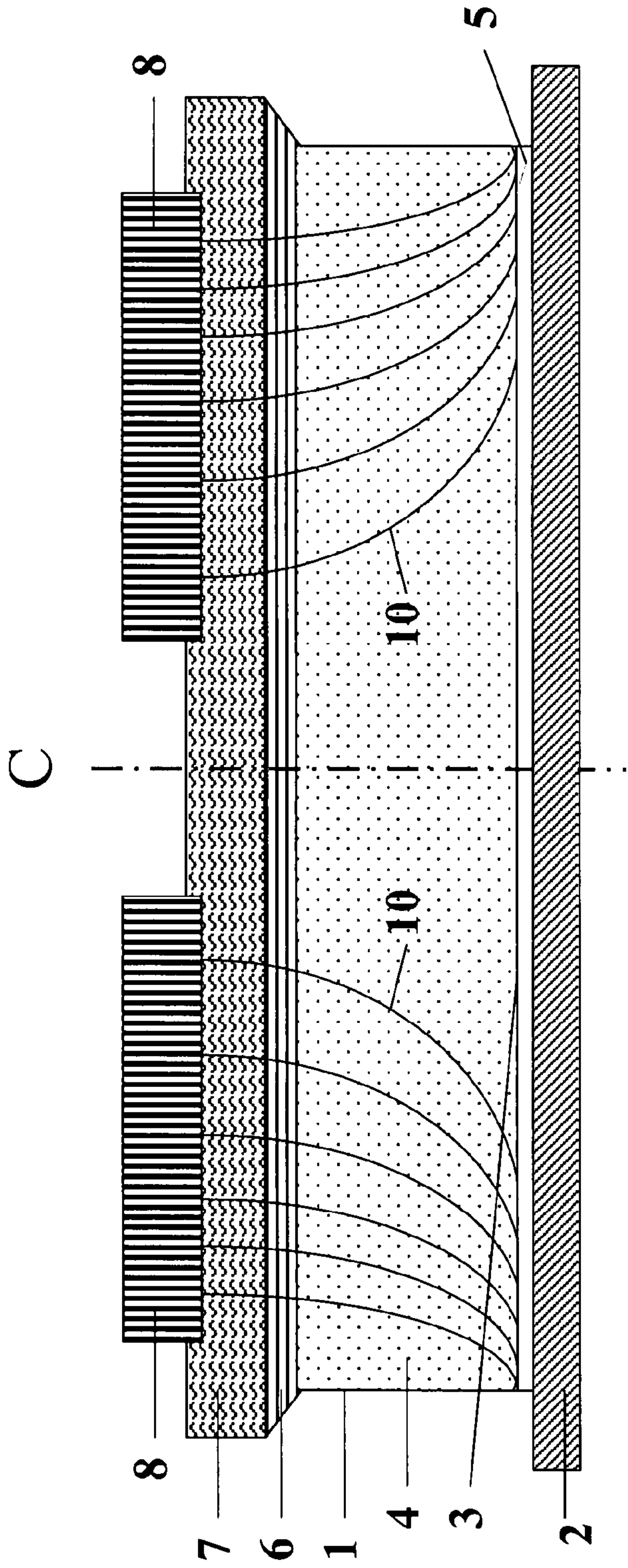


Figure 1

Prior art

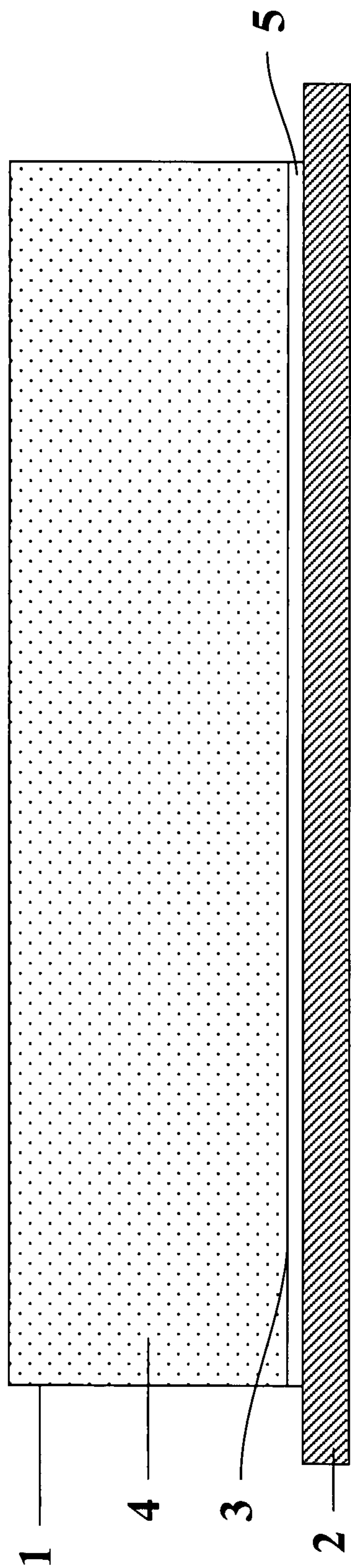


Figure 2

Prior art

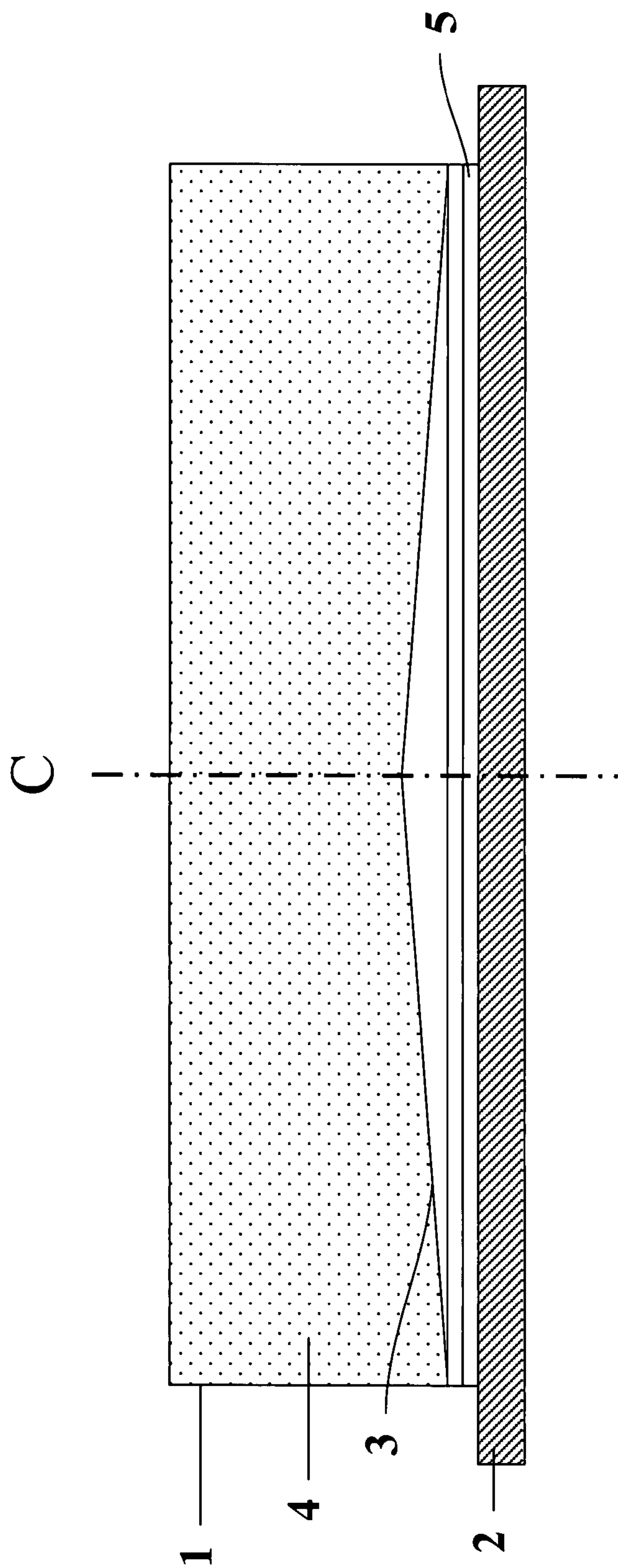


Figure 3

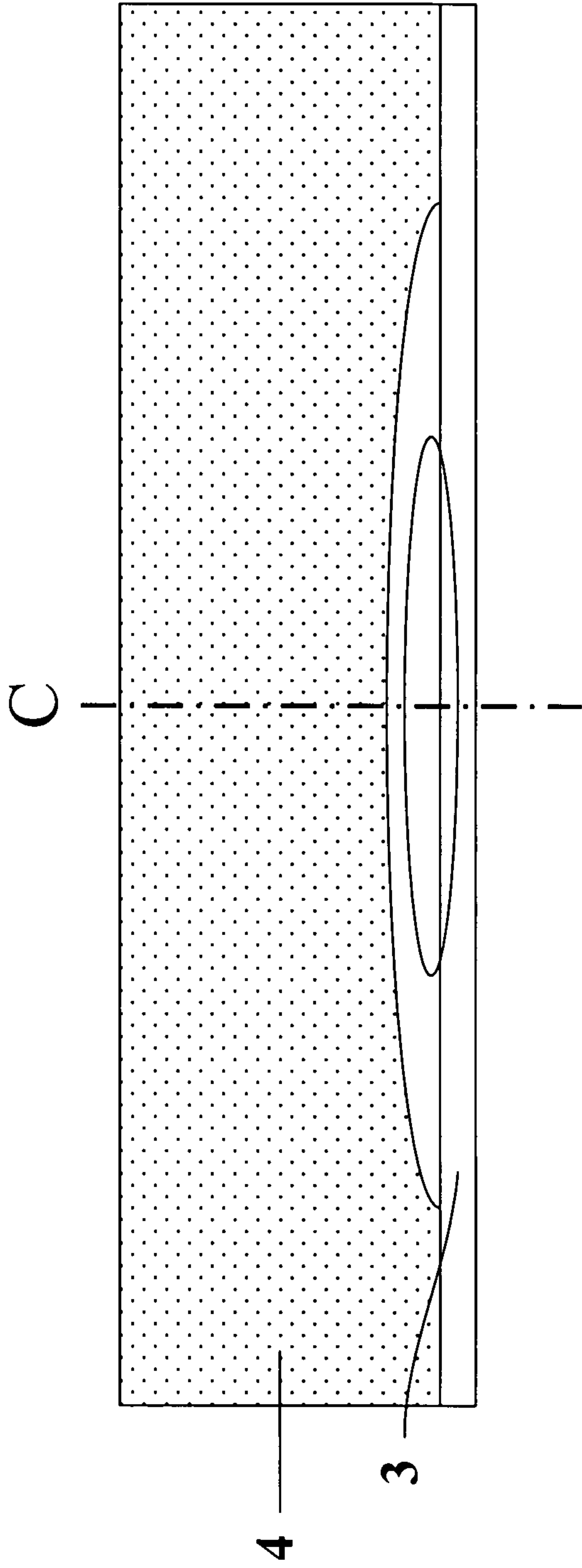


Figure 4A

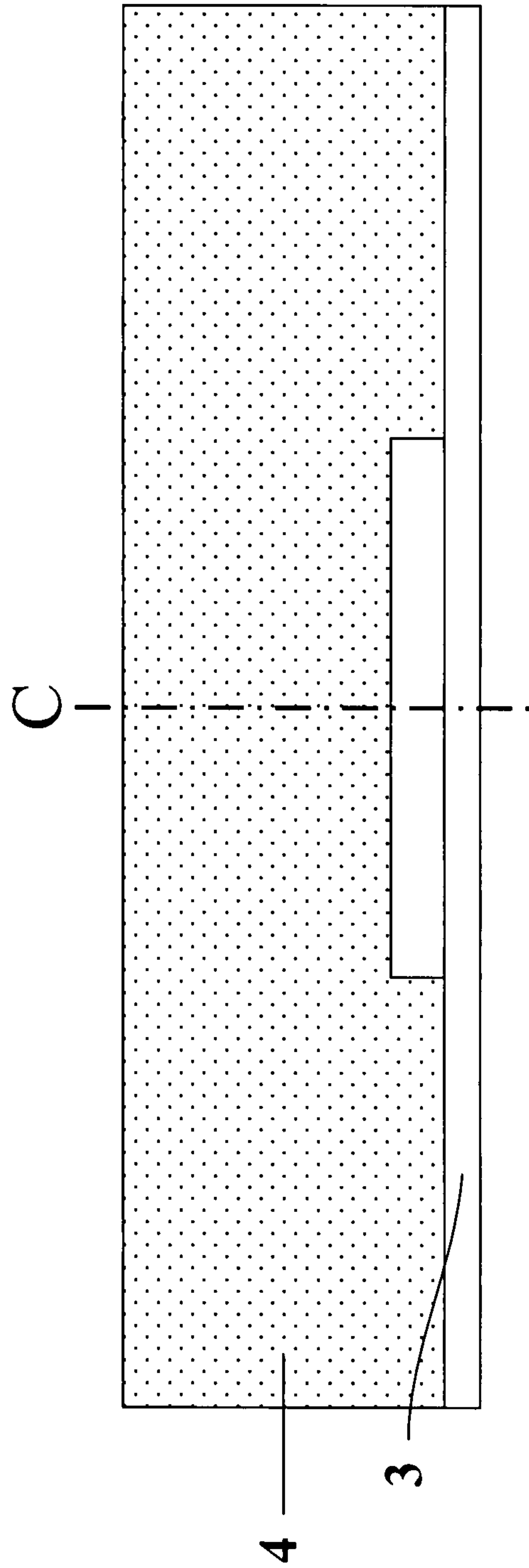


Figure 4B

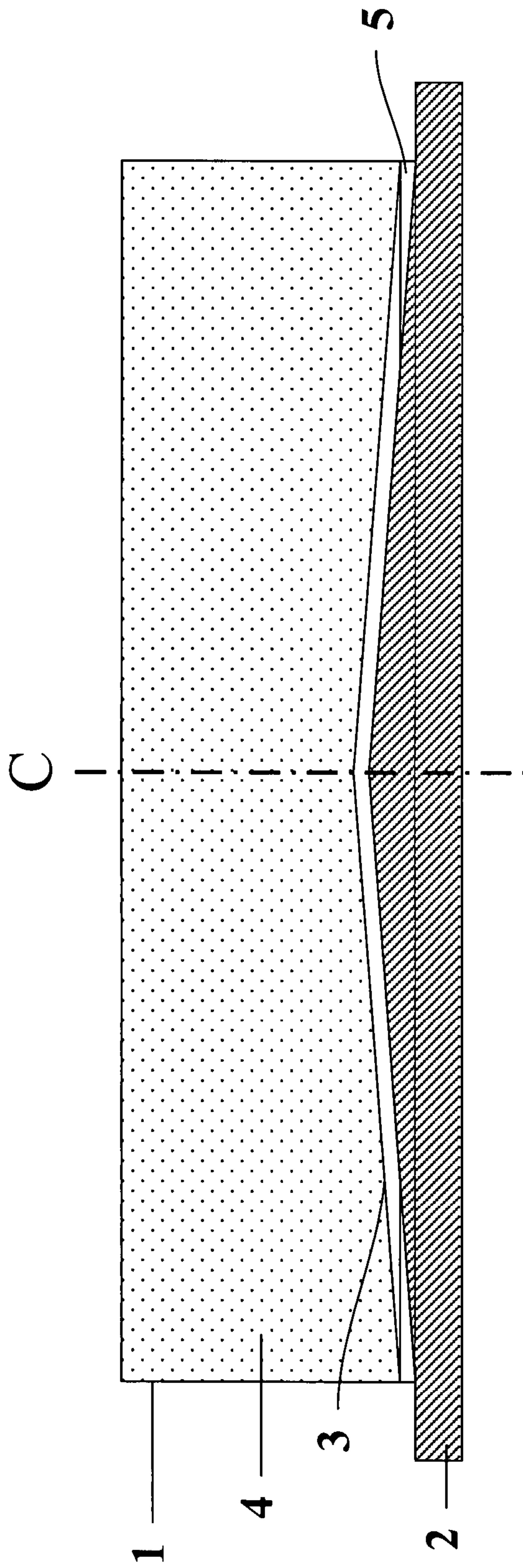


Figure 5

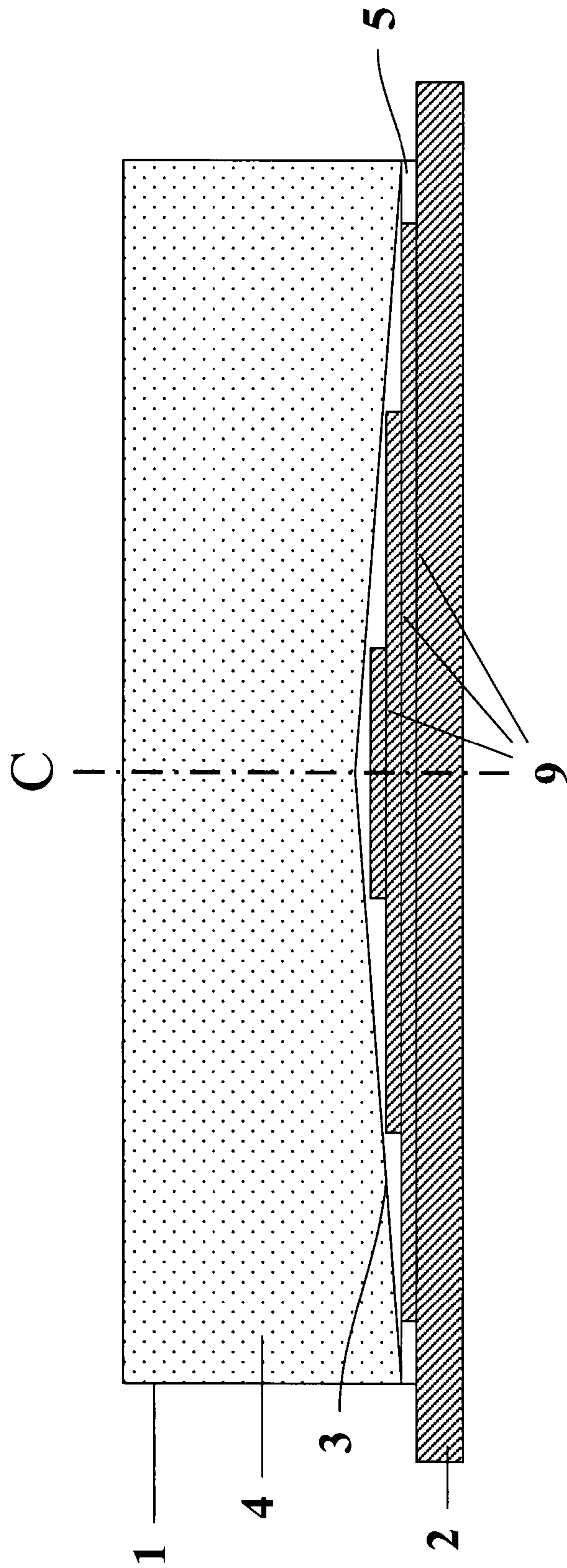
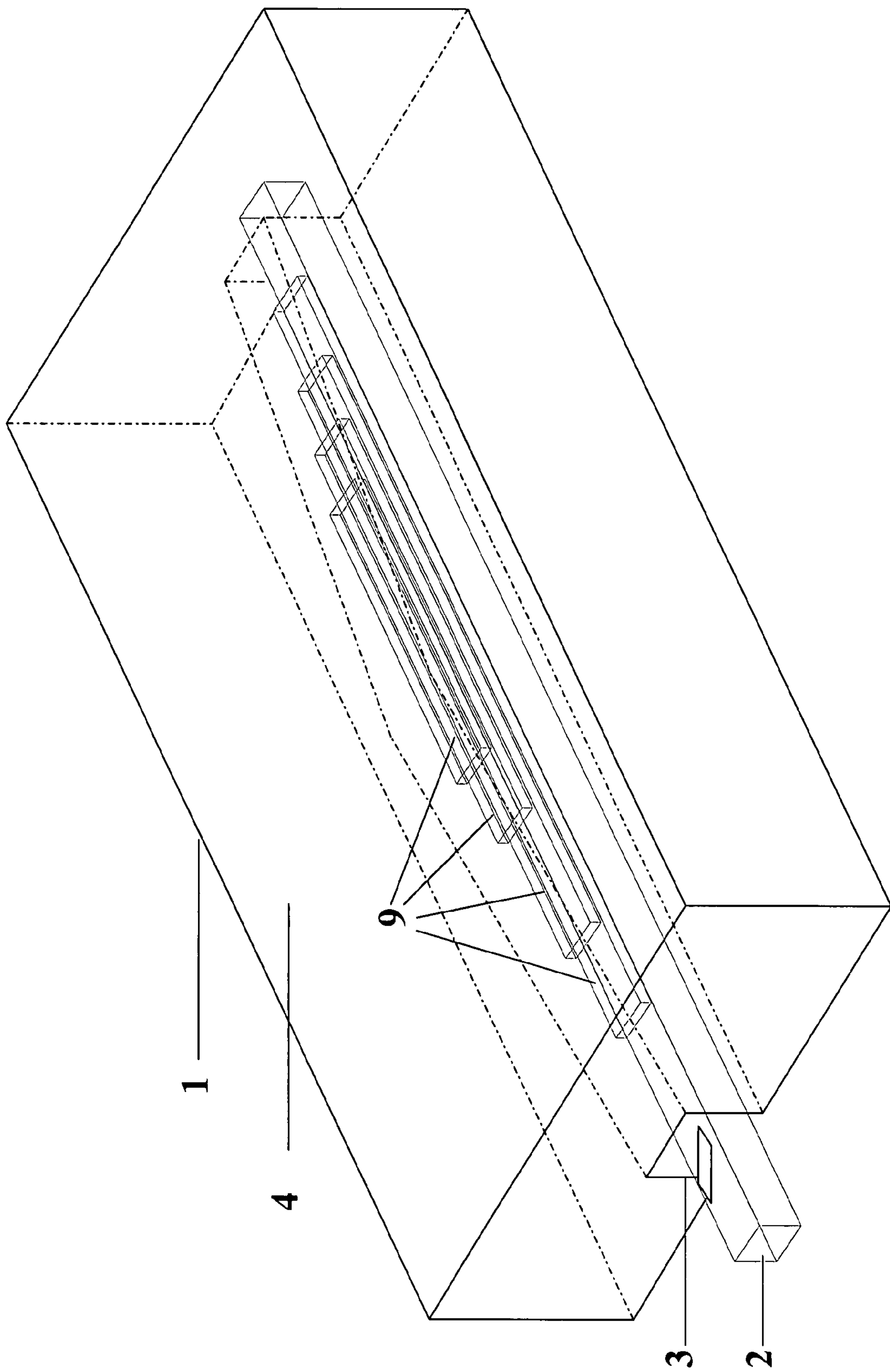


Figure 6

Figure 7



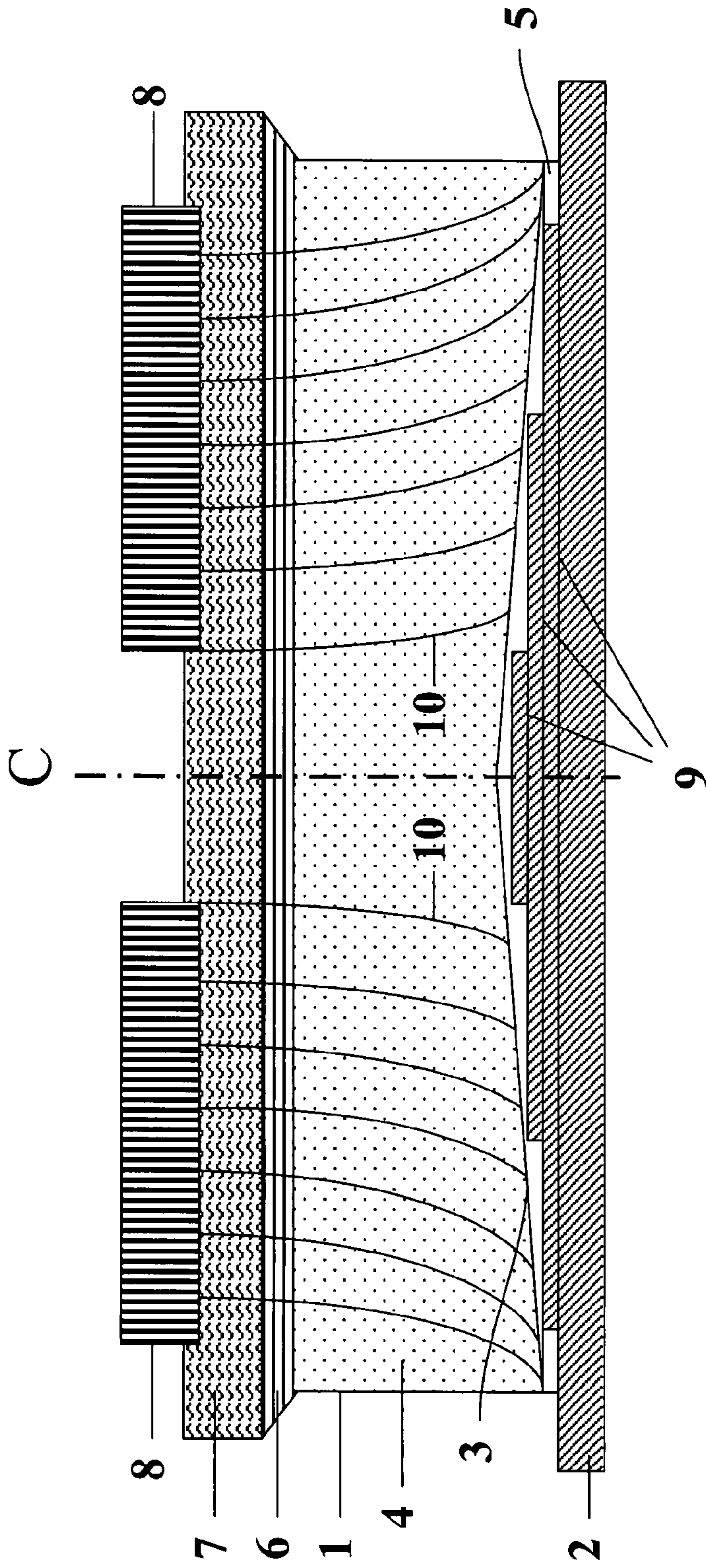


Figure 8

