



(86) Date de dépôt PCT/PCT Filing Date: 2005/07/26
(87) Date publication PCT/PCT Publication Date: 2006/02/02
(85) Entrée phase nationale/National Entry: 2007/01/25
(86) N° demande PCT/PCT Application No.: JP 2005/013647
(87) N° publication PCT/PCT Publication No.: 2006/011479
(30) Priorités/Priorities: 2004/07/27 (JP2004-218902);
2004/11/08 (JP2004-323579);
2005/04/25 (JP2005-125966)

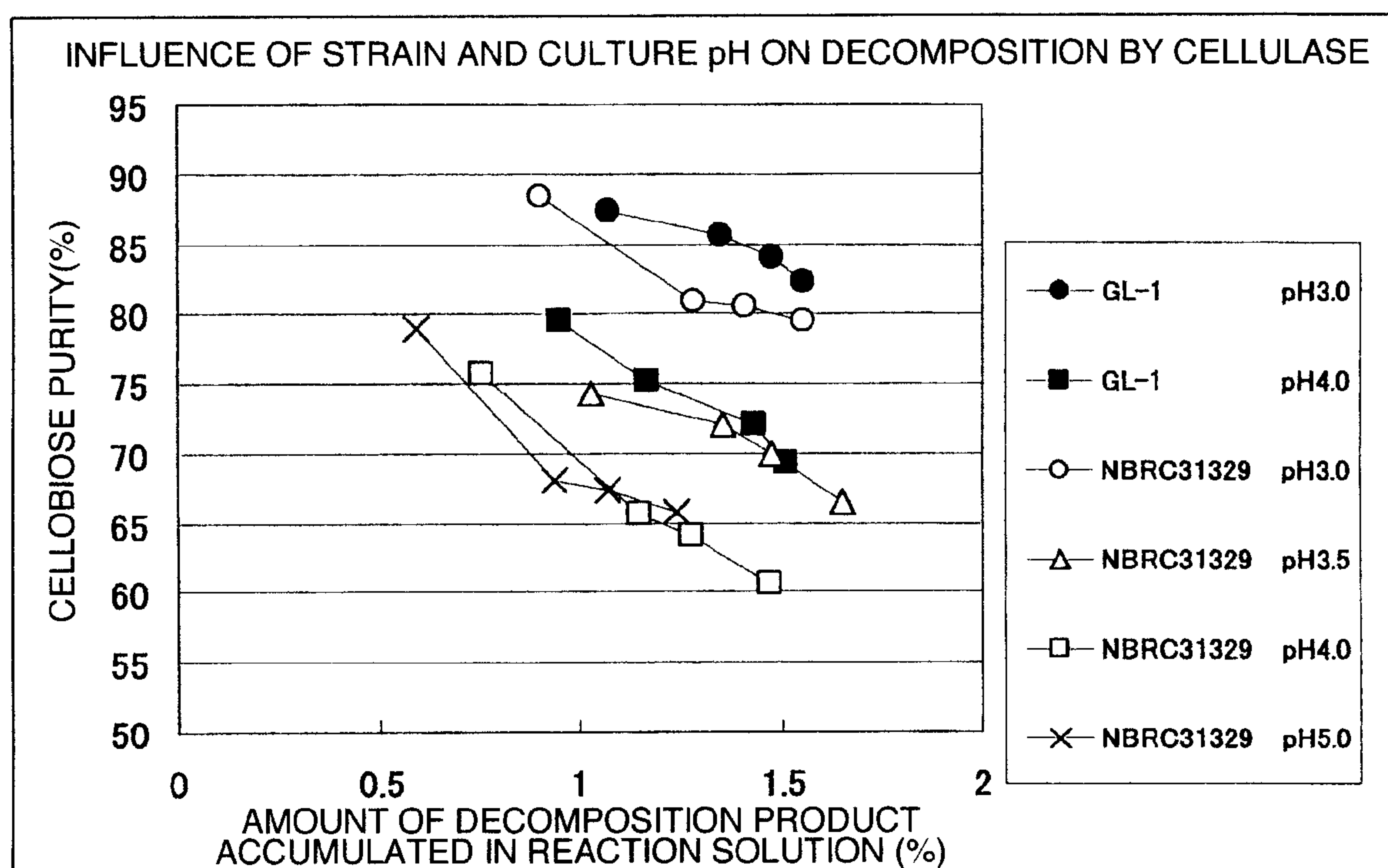
(51) Cl.Int./Int.Cl. *C12P 19/14* (2006.01),
C07H 3/06 (2006.01), *C12N 9/42* (2006.01),
A61K 31/702 (2006.01), *A23L 1/29* (2006.01)

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(54) Titre : PROCEDES DE PRODUCTION D'UN CELLO-OLIGOSACCHARIDE
(54) Title: PROCESSES FOR PRODUCING CELLOOLIGOSACCHARIDE



(57) Abrégé/Abstract:

A process for producing a celooligosaccharide which comprises enzymatically decomposing in the presence of a cellulase a water-insoluble natural cellulosic substance which has an average degree of polymerization of 700 or lower and an average particle diameter of 100 μm or smaller and in which the content of components soluble in diethyl ether is less than 1 mass%. Also provided is a process for celooligosaccharide production which comprises enzymatically decomposing in the presence of a cellulase a water-insoluble natural cellulosic substance which has an average degree of polymerization of 700 or lower and in which the content of colloidal cellulose components is 10 mass% or higher and the content of components soluble in diethyl ether is less than 1 mass%.

ABSTRACT

A process of producing cellooligosaccharide, comprising enzymatically decomposing, in the presence of cellulase, a water-insoluble natural cellulosic material having an average degree of polymerization not greater than 700, an average particle size not greater than 100 μm , and a diethyl ether-soluble substance content less than 1% by mass.

A process of producing cellooligosaccharide, comprising enzymatically decomposing, in the presence of cellulase, a water-insoluble natural cellulosic material having an average degree of polymerization not greater than 700, containing 10% or more by mass of a colloidal cellulose component and a diethyl ether-soluble matter content less than 1% by mass.

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DESCRIPTION

PROCESSES FOR PRODUCING CELLOOLIGOSACCHARIDE

TECHNICAL FIELD

The present invention relates to a process of obtaining cellooligosaccharide by enzymatically decomposing a cellulosic material. The present invention particularly relates to a process by which a water-insoluble natural cellulosic material whose average degree of polymerization, average particle size, colloidal cellulose component content, and diethyl ether-soluble matter content are controlled to fall within a certain range is used as a substrate and enzymatically decomposed with cellulase whose activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity) is controlled to fall within a certain range, thereby enhancing the decomposition rate of cellulose in a short time to selectively produce cellooligosaccharide in high yields.

BACKGROUND ART

Cellooligosaccharide is a general term for cellobiose, cellotriose, cellotetraose, cellopentaose, and cellohexaose and is one of oligosaccharides where 1 to 6 glucopyranose units are joined together through β -

1,4 linkages.

In recent years, the physiological function of the cellooligosaccharide is being elucidated as with other oligosaccharides. Therefore, the
5 cellooligosaccharide is expected as a novel raw material for functional foods (Non-Patent Document 1).

The cellooligosaccharide is obtained by hydrolyzing its polymer, cellulose, with an enzyme. However, naturally-occurring cellulose is hardly
10 soluble in water and highly crystalline and is therefore less likely to undergo enzymatic decomposition by cellulase. Thus, this has presented a problem.

In the enzymatic decomposition reaction of
15 cellulose, cellooligosaccharide obtained as a decomposition product is further decomposed into glucose units by β -glucosidase that is a component in cellulase, thereby causing reduction in the yield of cellooligosaccharide. Thus, this has presented another
20 problem (Non-Patent Document 2).

In light of the above-described problems, many attempts have heretofore been made for the purpose of improving the yield of cellooligosaccharide at the time when cellulose is enzymatically decomposed.

25 Processes of producing cellooligosaccharide using particular cellulose include the followings:

Patent Document 1 has described a process of producing cellooligosaccharide, in which a cellulose

raw material containing amorphous cellulose in large amounts is used and subjected to hydrolysis reaction with cellulase in the presence of lignin while at least cellobiose of cellooligosaccharides generated by the
5 hydrolysis reaction is collected from the reaction solution at any time.

Patent Document 2 has described a process of producing cellooligosaccharide, in which wet pulp, which is obtained without undergoing drying after the
10 cooking of a natural lignocellulose-containing raw material, is partially hydrolyzed with cellulase to collect at least cellobiose of generated cellooligosaccharides. In these production processes, cellooligosaccharide-decomposing enzyme β -glucosidase
15 contained in cellulase is adsorbed into lignin and inhibited from action of β -glucosidase, thereby reducing the decomposition of the cellooligosaccharide into glucose to enhance the reaction selectivity of cellooligosaccharide. However, in these production
20 processes, the resulting saccharification liquid contains lignin in large amounts, with the result that the yield of cellooligosaccharide is reduced. Moreover, because treatment for eliminating lignin from the saccharification liquid is required for obtaining
25 cellooligosaccharide of high purity, a complicated purification step has been a problem.

Patent Document 3 has described a process of producing cellobiose, a type of cellooligosaccharide,

by reacting lignocellulose containing 1 to 20% by mass of lignin with cellulase and a lignin-decomposing fungus such as a white-rot fungus. This process can enhance the action of cellulase on the substrate without treatment for eliminating lignin in cellulose. However, its decomposition product contains not only cellobiose but also lignin decomposition products, thereby causing reduction in the yield of cellooligosaccharide as in the above-described processes. Moreover, because a step of removing the lignin decomposition products is required for obtaining cellobiose of high purity, a complicated purification step has been a problem.

Patent Document 4 has described a process of producing cellooligosaccharide, in which, after cellulase is added to a cellulose solution obtained by dissolving cellulose in solvents such as amine oxide, lithium chloride/N,N-dimethylacetamide, cuprammonium, and viscose, cellulase-containing regenerated cellulose is obtained from the resulting solution and subsequently subjected to enzymatic reaction by the cellulase contained in the regenerated cellulose in the presence of a buffer to produce cellooligosaccharide. The process does not require special pretreatment such as purification given to cellulase and improves the yield of cellooligosaccharide. However, because the process requires a step of dissolving and regenerating cellulose, a complicated step has been a problem.

Chemical substances used in the dissolution of cellulose, such as amine oxide, lithium chloride/N,N-dimethylacetamide, cuprammonium, and viscose, have no small action on cellulase. As a result, there has been
5 a problem in that decomposition reaction of cellulose is affected by the chemical substances.

Patent Document 5 has described a process of producing cellobiose using, as a raw material, bleached slush pulp having water retentivity between 230 and
10 280% and drainability between 550 and 640 ml. The slush pulp used therein is undried pulp after cooking/bleaching treatment. Although the use of the pulp as a raw material certainly improves the production quantity of cellobiose, undried slush pulp
15 is restricted in substrate concentration at the time of enzymatic decomposition due to its high water retentivity. Thus, the poor productivity of cellooligosaccharide has been a problem.

Patent Document 6 has described a process in
20 which, after a cellulose component is solubilized from a cellulose-containing material using supercritical or subcritical water, the resulting treated liquid is supplemented with a cellulase preparation, and cellulose and cellooligosaccharide (partial
25 decomposition product of cellulose) having a high degree of polymerization are hydrolyzed with the cellulase preparation, thereby obtaining glucose and/or cellooligosaccharide. This process improves both of

the production quantity and the yield of celooligosaccharide such as cellobiose and cellotriose. However, there remains an issue surrounding the safety of cellulose pretreatment, for
5 example, the safety of facilities such as pressure-resistant/acid-resistant facilities required for supercritical or subcritical water treatment and the safety against pressurization and heating.

Patent Document 7 has described a process of
10 producing celooligosaccharide using, as a reaction substrate for cellulase, pulp having a degree of cellulose I crystallization from 10% to 80% determined by X ray diffractometry and water retentivity from 200% to 1000%, wherein the pulp is subjected to any one or
15 several treatment(s) selected from fibrillation treatment, mechanochemical treatment, and chemical treatment. The process improves the production quantity of cellobiose and the decomposition rate of cellulose. However, because of use of fibrous pulp
20 with high water retention as cellulose the process presents such a problem of poor productivity of celooligosaccharide that clogging occurs, substrate concentration is restricted, and so on at each producing step such as pretreatments (e.g. fibrillation
25 treatment, mechanochemical treatment, and chemical treatment) and, the subsequent enzymatic decomposition and purification of oligosaccharides. The process is essentially different from the process of the present

invention in which an average degree of polymerization, an average particle size, a colloidal component content, and so on, are controlled at high level and treating properties at each step including enzymatic
5 decomposition are enhanced.

Methods for improving the yield of cellooligosaccharide by enzymatically decomposing cellulose with particular cellulase include the following Patent Documents 8 to 11:

10 Patent Document 8 has described a process of producing cellooligosaccharide from a cellulosic material in an aqueous reaction solution by the action of cellulase produced by a microorganism belonging to the genus *Cellvibrio*, in which an ultrafiltration
15 reactor is used in combination, so that production inhibition is removed to produce and accumulate cellooligosaccharide. According to this process, cellooligosaccharides consisting only of cellobiose and cellotriose are obtained as decomposition products from
20 the enzymatic decomposition of the cellulosic material. However, because an enzyme produced by a microorganism of the genus *Cellvibrio* is less likely to act on crystalline cellulose, amorphous cellulose as a substrate is required for reducing reaction time and
25 improving yields. Thus, a complicated step has been a problem.

Patent Document 9 has described a process of producing cellooligosaccharide by decomposing cellulose

with cellulase, in which cellulase is brought in advance into contact with a weakly acidic cation-exchange resin equilibrated to pH 3.5 to 5.0 to thereby selectively remove β -glucosidase in the cellulase, and
5 the cellulase from which β -glucosidase has been removed is brought into contact with cellulose. According to the process, glucose is reduced by the enzymatic decomposition of the cellulose, so that a decomposition product having 60% or more cellooligosaccharide can be
10 obtained. However, the above-described method requires a step of removing β -glucosidase in cellulase. Thus, there has been a problem in that a step of producing cellooligosaccharide is complicated. Moreover, because this step of purifying cellulase requires the amount of
15 a cation-exchange resin 75 to 1000 times greater than that of untreated cellulase, the amount of cellulase treated is limited and the productivity of cellooligosaccharide is not sufficient. Thus, there has been a problem in that the cost of cellulase
20 purification and the cost of separation/purification agents of the cation-exchange resin are high.

Patent Document 10 has described a process for cellulase purification in which, after cellulase is dissolved along with either or both of cellulose ester
25 or(and) cellulose ether ester and incubated for a fixed period of time, pH is changed and an insolubilized solid fraction is separated from the solution to thereby selectively remove β -glucosidase in the

cellulase; and a process for cellobiose production in which cellulose together with the cellulase from which β -glucosidase has been removed is added to an aqueous medium to make a suspension which is in turn incubated
5 for a fixed period of time to produce cellobiose into the suspension, followed by the collection of the cellobiose.

Patent Document 11 has described a process for cellulase purification in which, after chitosan and
10 cellulase are dissolved in an aqueous medium whose pH has been adjusted to pH that renders the chitosan soluble and are incubated for a fixed period of time, pH is changed and an insolubilized solid fraction is separated from the solution to thereby selectively
15 remove β -glucosidase in the cellulase; and a process for cellobiose production in which cellulose together with the cellulase from which β -glucosidase has been removed is added to an aqueous medium to make a suspension which is in turn incubated for a fixed
20 period of time to produce cellobiose into the suspension, followed by the collection of the cellobiose. These processes improve the yield of cellobiose by subjecting cellulase to adsorption/separation treatment with a cellulose
25 derivative or chitosan and bringing cellulose into contact with the cellulase that remains adsorbed in the cellulose derivative or chitosan. However, these processes require treatment for purifying cellulase and

therefore complicate a producing step. There has been a problem in that high costs are needed because the cellulose derivative and the chitosan used in the purification of cellulase are expensive. Moreover, since the cellulase is used with the cellulose derivative and the chitosan in the enzymatic decomposition of cellulose, there has also been a problem in that a step of removing them from the decomposition reaction solution is required.

Heretofore, a process has not been known, by which a water-insoluble natural cellulosic material whose average degree of polymerization, average particle size, colloidal cellulose component content, and diethyl ether-soluble matter content are controlled by pretreatment to fall within a certain range is used as a substrate and enzymatically decomposed with cellulase whose activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity) is controlled to fall within a certain range, thereby enhancing the decomposition rate of cellulose in a short time to selectively produce cellooligosaccharide in high yields.

[Non-Patent Document 1] Cellulose Communications, 5, No 2, 91-97 (1998)

[Non-Patent Document 2] "Cellulase" published by Kodansha Scientific, 97-104 (1987)

[Patent Document 1] JP-A-05-317073

[Patent Document 2] JP-A-07-184678
[Patent Document 3] JP-A-08-89274
[Patent Document 4] JP-A-08-308589
[Patent Document 5] JP-A-09-107087
5 [Patent Document 6] JP-A-2001-95594
[Patent Document 7] JP-A-2005-68140
[Patent Document 8] JP-A-01-256394
[Patent Document 9] JP-A-05-115293
[Patent Document 10] JP-A-05-227957
10 [Patent Document 11] JP-A-05-227958

DISCLOSURE OF THE INVENTION

An object of the present invention is to selectively produce cellooligosaccharide in high yields by enzymatically decomposing a water-insoluble natural
15 cellulosic material used as a raw material in the presence of particular cellulase, thereby enhancing the decomposition rate of cellulose in a short time.

The present inventors have completed the present invention by finding out that, for solving the
20 above-described problems, a water-insoluble natural cellulosic material whose average degree of polymerization, average particle size, colloidal cellulose component content, and diethyl ether-soluble matter content are controlled to fall within a certain
25 range is used as a raw material and enzymatically decomposed with cellulase having particular activity, thereby enhancing the decomposition rate of cellulose

in a short time to selectively give
cellooligosaccharide in high yields.

Thus, the present invention is as follows:

(1) a process of producing
5 cellooligosaccharide, comprising enzymatically
decomposing, in the presence of cellulase, a water-
insoluble natural cellulosic material having an average
degree of polymerization not greater than 700, an
average particle size not greater than 100 μm , and a
10 diethyl ether-soluble matter content less than 1% by
mass;

(2) a process of producing
cellooligosaccharide, comprising enzymatically
decomposing, in the presence of cellulase, a water-
15 insoluble natural cellulosic material having an average
degree of polymerization not greater than 700,
containing 10% or more by mass of a colloidal cellulose
component and a diethyl ether-soluble matter content
less than 1% by mass;

20 (3) the process of producing
cellooligosaccharide according to (1) or (2), wherein
the above-described water-insoluble natural cellulosic
material has an average particle size not greater than
100 μm and contains 10% or more by mass of a colloidal
25 cellulose component;

(4) the process of producing
cellooligosaccharide according to any one of (1) to
(3), wherein the above-described water-insoluble

natural cellulosic material has an average degree of polymerization not greater than 500 and an average particle size not greater than 50 μm ;

(5) the process of producing
5 cellooligosaccharide according to any one of (1) to (4), wherein the above-described water-insoluble natural cellulosic material has an average degree of polymerization not greater than 400 and an average particle size not greater than 30 μm ;

10 (6) the process of producing cellooligosaccharide according to any one of (1) to (5), wherein the above-described water-insoluble natural cellulosic material contains 15% or more by weight of a colloidal cellulose component;

15 (7) the process of producing cellooligosaccharide according to any one of (1) to (6), wherein the above-described cellulase has an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C)
20 not greater than 0.7;

(8) the process of producing cellooligosaccharide according to (7), wherein the above-described cellulase has an activity ratio not greater than 0.5;

25 (9) the process of producing cellooligosaccharide according to (8), wherein the above-described cellulase has an activity ratio not greater than 0.35;

(10) the process of producing celooligosaccharide according to any one of (1) to (9), wherein the above-described diethyl ether-soluble matter is lignin;

5 (11) the process of producing celooligosaccharide according to any one of (1) to (10), wherein the above-described water-insoluble natural cellulosic material contains a cellulose I crystal;

10 (12) the process of producing cellulase according to any one of (1) to (11), wherein the above-described enzymatic decomposition is performed by culturing cellulase-producing microorganism, wherein an activity ratio of β -glucosidase activity to crystalline
15 cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) in a culture solution obtained by culturing the above-described cellulase-producing microorganism is not greater than 0.5;

20 (13) the process of producing cellulase according to (12), wherein the above-described activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity is not greater than 0.35;

25 (14) the process of producing cellulase according to any one of (12) or (13), wherein the above-described cellulase-producing microorganism is a strain selected and thereby obtained as a strain

reduced in β -glucosidase production;

(15) the process of producing cellulase according to any one of (12) to (14), wherein pH during culture is controlled at less than 3.5 when the above-
5 described cellulase-producing microorganism is cultured;

(16) the process of producing cellulase according to any one of (12) to (15), wherein the above-described cellulase-producing microorganism is a
10 strain belonging to the genus *Trichoderma*;

(17) cellooligosaccharide characterised in that diethyl ether-soluble matter content is 2000 ppm or less;

(18) cellooligosaccharide obtainable by the
15 process according to any one of claims 1 to 11, characterised in that diethyl ether-soluble matter content is 2000 ppm or less;

(19) cellooligosaccharide according to claim 18, wherein the diethyl ether-soluble matter content is
20 1000 ppm or less;

(20) a food, cosmetic, or pharmaceutical preparation, characterised by comprising cellooligosaccharide obtainable by the process according to any one of claims 1 to 11; and

25 (21) a food, cosmetic, or pharmaceutical preparation, characterised by comprising cellooligosaccharide according to claim 17 or 18.

According to the process of producing

cellooligosaccharide of the present invention by enzymatically decomposing a water-insoluble natural cellulosic material, the decomposition rate of cellulose can be enhanced in a short time and
5 cellooligosaccharide can selectively be produced in high yields.

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a graph showing changes over time in pH during culture in Examples 13 and 14 and
10 Comparative Example 6;

FIG. 2 is a graph showing changes over time in pH during culture in Example 15; and

FIG. 3 is a graph showing a change in the concentration of products from crystalline cellulose decomposition in Example 16 and Comparative Example 7.
15 In the drawing, the amount of the decomposition product accumulated (%) in a reaction solution is expressed as the total concentration of glucose and cellooligosaccharide in the reaction solution, while
20 cellobiose purity is expressed as the ratio (percentage) of cellooligosaccharide to the amount of the decomposition product accumulated in the reaction solution. The cellobiose purity was improved for the amount of the decomposition product accumulated by
25 using a mutant strain and reducing pH in a culture solution.

BEST MODE FOR CARRYING OUT THE INVENTION

Hereinafter, the present invention will be described in detail with particular emphasis on its preferred aspects.

5 A natural cellulosic material used in the present invention is a naturally-occurring water-insoluble fibrous substance containing cellulose. The natural cellulosic material may be derived from plants or animals. Examples of the animals and plants for
10 producing it include woods, bamboos, straws, rice straws, cotton, ramie, bagasse, kenaf, beet, sea squirts, and bacterial cellulose. One of these natural cellulosic materials may be used alone as a raw material, or alternatively two or more of them may be
15 mixed and used as a raw material.

 The cellulosic material used in the present invention needs to be a natural cellulosic material. Natural cellulose and regenerated cellulose can be discriminated by their crystal forms. The natural
20 cellulosic material of the present invention needs to contain a cellulose I crystal and have its content of 1% or more. A more preferable cellulose I crystal content is 50% or more. The cellulose I crystal form used herein can be distinguished by an X-ray
25 diffraction pattern obtained by wide-angle powder X-ray diffractometry (manufactured by Rigaku, trade name: Rotaflex RU300). Its content is expressed as a percentage of the peak area of the cellulose I crystal

to the total peak area of a diffraction image obtained by X-ray diffraction. A cellulosic material in a dry state subjected to wide-angle powder X-ray diffraction measurement may be pulverize by a method known in the art and then used in the measurement, whereas a cellulosic material in a wet state can be dried by a method known in the art, then pulverized, and used in the measurement. A higher cellulose I crystal content is preferred because a cellulosic material close to natural cellulose is used in enzymatic decomposition and an artificial chemical treatment step such as regeneration treatment for cellulose is simplified. The highest cellulose I crystal content is not particularly limited and however, is less than 99% in light of the composition of natural cellulose currently known.

The natural cellulosic material used in the present invention is water-insoluble. "Water-insoluble" used herein means that 90% or more by mass of a water-insoluble component is contained in the natural cellulosic material. This water-insoluble component is obtained by dispersing the cellulosic material in pure water at 25°C and removing a water-soluble component by ultrafiltration (molecular weight cut-off: 10000), followed by the quantification of a water-insoluble residue.

The water-insoluble natural cellulosic material in the present invention has an average degree

of polymerization not greater than 700. The average degree of polymerization used herein can be measured by a reduced specific viscosity method with a copper ethylenediamine solution specified by Confirmatory Test
5 for Crystalline Cellulose (3) in "the Japanese Pharmacopoeia, 14th Edition" (published by Hirokawa Publishing). Since the cellulosic material having an average degree of polymerization not greater than 700 is more likely to undergo physical treatment such as
10 stirring, crushing, and grinding, the amount of its colloidal component can readily be controlled. When the average degree of polymerization of the water-insoluble natural cellulosic material is controlled to fall within the above-described range, a fiber in the
15 cellulosic material is rendered porous. Therefore, the possibility of enzyme-substrate contact is increased and the decomposition rate of cellulose is improved when the cellulosic material is enzymatically decomposed. The average degree of polymerization is
20 preferably not greater than 500, more preferably not greater than 400. A smaller average degree of polymerization allows the easier control of the amount of a colloidal component and the decomposition rate. Thus, the smallest average degree of polymerization is
25 not particularly limited and however, is preferably more than 10 in light of the range of an average degree of polymerization obtained by convenient procedures.

The water-insoluble natural cellulosic

material used in the present invention has an average particle size not greater than 100 μm . The average particle size used herein refers to the 50% accumulated particle size in volume/frequency particle size distribution obtained as follows: The cellulosic material is made into an aqueous emulsion of a concentration of 0.2% by mass and dispersed therein by means of a high shear homogenizer (manufactured by NIPPON SEIKI CO., LTD., trade name, Excel Auto Homogenizer ED-7, treatment conditions: at a speed of 5000 rpm for 3 minutes) and, after the pH of the dispersion was adjusted to 7.5-8.5, subjected to a centrifuge (manufactured by KUBOTA Corporation, trade name, 6930 Centrifuge, treatment conditions: centrifugal force 2000G for 5 minutes), after which the dispersion is separated to the supernatant component and the sedimentation component and the ratios by weight of the respective components are measured. The volume/frequency particle size distributions of the respective components are obtained using water as a medium by laser diffractometry (manufactured by Horiba, trade name LA-910, ultrasonication for 1 min) and multiplied by the ratio by weight of the supernatant component and the sedimentation component to obtain the 50% accumulated particle size in volume/frequency particle size distribution. An average particle size not greater than 100 μm is preferred because the contact area (accessibility) of the cellulose to

cellulase is increased in the enzymatic decomposition of the cellulose, so that the production rate and yield of cellooligosaccharide are improved. The average particle size is more preferably not greater than 50 μm , particularly preferably not greater than 30 μm , still more preferably not greater than 10 μm . A smaller average particle size attains more improvement in the production rate, production selectivity, and yield of cellooligosaccharide. Therefore, the smallest average particle size is not particularly limited and however, is not smaller than 0.01 μm in light of the range of an average particle size obtained by convenient procedures.

The water-insoluble natural cellulosic material used in the present invention needs to contain 10% or more by mass of a colloidal cellulose component. The colloidal cellulose component used herein is expressed as a percentage of a cellulose solid content remaining in a supernatant after centrifugation, which is obtained by dispersing a water suspension having 0.2% by mass concentration of the natural cellulosic material with a high-shear homogenizer (manufactured by Nippon Seiki, trade name: Excel Auto Homogenizer ED-7, treatment conditions: at a speed of 5000 rpm for 3 minutes) and adjusting its pH to 7.5 to 8.5, followed by centrifugation (manufactured by Kubota Corp., trade name: Centrifuge Model 6930, treatment conditions at a centrifugal force of 2000 G for 5 minutes). A

colloidal cellulose component content of 10% or more by mass allows improvement in the production rate, production selectivity, and yield of cellooligosaccharide. The colloidal cellulose component content is more preferably 15% or more by mass, particularly preferably 40% or more by mass. The amount of this colloidal cellulose component is a factor that affects enzymatic decomposability independently of the average particle size of the cellulosic material. Although the mechanism of the amount of the colloidal cellulose component for improvement in the production rate, selectivity, and yield of cellooligosaccharide is not clear, it is probable that an increased amount of the colloidal cellulose component allows the stabilized suspension of the cellulose as a substrate and the uniform contact of the enzyme and the substrate, thereby improving the above-described enzymatic decomposability. A higher colloidal cellulose component content attains more improvement in the enzymatic decomposability. Therefore, the highest colloidal cellulose component content is not particularly limited and however, is not higher than 99.9% by mass in light of a range achieved by convenient pretreatment.

25 The water-insoluble natural cellulosic material used in the present invention has a diethyl ether-soluble matter content less than 1% by mass. The diethyl ether-soluble matter content used herein refers

to impurities in the cellulosic material that are soluble in diethyl ether, such as lignin and lignin decomposition products, and can be measured by a method of quantifying a diethyl ether-soluble matter specified
5 by Purity Test for Crystalline Cellulose (2) in "the Japanese Pharmacopoeia, 14th Edition" (published by Hirokawa Publishing). The use of cellulose of high purity having a lignin content less than 1% by mass more improves the purity of cellooligosaccharide
10 obtained by enzymatic decomposition. The improved purity of cellooligosaccharide results in improvement in production yield, thereby facilitating the purification of cellooligosaccharide and the collection of cellulase after enzymatic decomposition. The
15 diethyl ether-soluble matter content is more preferably 0.5% or less by mass, still more preferably 0.3% or less by mass. A lower diethyl ether-soluble matter content attains more improvement in the above-described purity of cellooligosaccharide. Therefore, the lowest
20 colloidal cellulose component content is not particularly limited and however, is not lower than 0.0005% by mass in light of the range of a lignin content achieved by convenient pretreatment.

Preferred treatment methods by which the
25 average degree of polymerization, average particle size, colloidal cellulose component content, and diethyl ether-soluble matter content of the natural cellulosic material satisfy the scope of the present

invention include the followings:

No particular limitation is imposed on a method of controlling the average degree of polymerization and the diethyl ether-soluble matter content as long as the method is known in the art. One example thereof includes hydrolysis treatment. This hydrolysis treatment is preferred because amorphous cellulose and hemicellulose and impurities (such as lignin) within the cellulose fiber are removed to render the interior of the fiber porous, into which cellulase is therefore more likely to infiltrate at the time of enzymatic decomposition, thereby improving both of the decomposition rate of cellulose and the yield of celooligosaccharide.

Moreover, the hydrolysis is preferred because, when the hydrolyzed cellulosic material is further treated by a method known in the art, the cellulosic material is more likely to undergo mechanical treatment because of its porous fibrous interior and the average particle size and colloidal component content of the cellulosic material are readily controlled.

A method for hydrolysis is not particularly limited and however, is exemplified by acid hydrolysis, alkaline oxidative decomposition, hydrothermal decomposition, steam explosion, and microwave decomposition. Any of these methods may be used alone, or otherwise two or more of them may be combined. When

acid hydrolysis of the above-described methods is performed, the average degree of polymerization can readily be controlled by adding an appropriate amount of protonic acid, carboxylic acid, Lewis acid, heteropolyacid, and the like to the cellulosic material that remains dispersed in an aqueous medium and heating the resulting mixture with stirring. In this case, reaction conditions such as temperature, pressure, and time differ depending on the type and concentration of cellulose as well as the type and concentration of acid and however, are appropriately adjusted to achieve an average degree of polymerization of interest. For example, for the above-described acid hydrolysis, preferred are such reaction conditions that the cellulose is treated with 1% or less by mass of a mineral acid solution under pressure at 100°C or higher for 10 minutes or more. This is because a catalytic component such as acid infiltrates into the interior of the cellulose fiber to promote hydrolysis, so that the amount of the catalytic component used is reduced.

A method of controlling the average particle size and the colloidal cellulose component content is not particularly limited as long as the method is known in the art. One example thereof includes grinding, crushing, sieve classification, cyclones, and centrifugation using a centrifuge. These methods may be used alone, or otherwise two or more of them may be combined. These methods may be conducted as both wet

and dry processes. Cellulosic materials individually obtained by the wet process may be mixed together prior to enzymatic decomposition, while cellulosic materials individually obtained by the dry processes may be mixed together prior to enzymatic decomposition. Or otherwise, cellulosic materials obtained by the wet process may be combined with those obtained by the dry process.

For example, when the cellulose is treated by the wet process, the average particle size or colloidal cellulose component content of the cellulosic material can readily be adjusted by subjecting a cellulose dispersion containing 1 to 99% cellulosic material and a medium to grinding, crushing, or the like, known in the art. In this case, the medium used is not particularly limited and includes water, alcohols such as methanol, ethanol, n-propyl alcohol, isopropyl alcohol, butyl alcohol, 2-methylbutyl alcohol, and benzyl alcohol, hydrocarbons such as pentane, hexane, heptane, and cyclohexane, and ketones such as acetone and ethyl methyl ketone. In particular, a preferred organic solvent is any of those used at a step of producing pharmaceuticals, foods, and additives thereof and includes those classified as solvents in "Dictionary of Pharmaceutical Additives" (published by Yakuji Nippo), and "Japanese Pharmacopoeia" and "Official Method for Food Additives" (published by Hirokawa Publishing). Water and the organic solvents

may be used alone, or two or more of them may be used in combination. Alternatively, after one medium is used in dispersion and then removed, the cellulosic material may be dispersed again in a different medium.

5 A grinding method includes: a grinding method using stirring blades such as unidirectional rotary-, multi-axis rotary-, reciprocal inverse-, vertical motion-, rotary and vertical motion-, and duct line-system stirring blades, such as portable mixers, solid
10 mixers, and lateral mixers; a jet-system stirring grinding method such as line mixers; a grinding method using high-shear homogenizers, high-pressure homogenizers, ultrasonic homogenizers, and the like; a rotary extrusion-system grinding method using kneaders;
15 and a grinding method combining consolidation with shearing, such as roll mills, ball mills, vibratory ball mills, and bead mills, any method of which may be used alone or in combination.

 A crushing method includes a screen-system
20 crushing method such as screen mills and hammer mills; a blade-rotating shear screen-system crushing method such as flash mills; an air jet-system crushing method such as jet mills; a crushing method combining consolidation with shearing, such as roll mills, ball
25 mills, vibratory ball mills, and bead mills; and a stirring blade-system crushing method, any method of which may be used alone or in combination.

Cellulase of the present invention is a

general term for cellulose-decomposing enzymes. Any of those having the activity of decomposing cellulose is encompassed in the cellulase according to the present invention. Examples of cellulase enzyme sources
5 include cellulase-producing live microorganisms themselves or culture supernatant liquids thereof, purified enzymes from enzymes produced by the cellulase-producing live microorganisms, or preparations made from the purified enzymes along with
10 additives such as excipients and stabilizers. When the cellulase preparation is used in enzymatic decomposition, the additive added to the preparation is not particularly limited. Its dosage form may be any of a powder, a granule, a liquid, and the like.

15 The origin of the cellulase is not particular limited and can include cellulase produced by cellulase-producing microorganisms known in the art such as microorganisms of the genus *Trichoderma*, the genus *Acremonium*, the genus *Aspergillus*, the genus
20 *Bacillus*, the genus *Pseudomonas*, the genus *Penicillium*, the genus *Aeromonas*, the genus *Irpex*, the genus *Sporotrichum*, and the genus *Humicola* described in "Cellulase" (published by Kodansha Scientific (1987)) and "Dictionary of Cellulose" (published by Asakura
25 Shoten (2000)). However, the cellulase of the present invention is not limited to the enzyme derived from the above-described microorganisms known in the art and also encompasses any of enzymes that decompose

cellulose, including enzymes derived from microorganisms newly discovered.

Preferably, the cellulase used in the present invention has an active ratio of β -glucosidase activity to crystalline cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C) not greater than 0.7. The activity ratio used herein is given by the ratio of the ability to decompose cellooligosaccharide (by β -glucosidase) to the ability of the cellulase to decompose cellulose (crystalline cellulose-decomposing activity). A smaller activity ratio is preferred because higher ability to decompose cellulose and lower ability to decompose oligosaccharide are attained and the productivity of oligosaccharide is improved. The activity ratio is more preferably not greater than 0.5, still preferably not greater than 0.4, particularly preferably not greater than 0.35, most preferably not greater than 0.30. Since a smaller activity ratio attains more improvement in the yield of cellooligosaccharide, the smallest activity ratio is not particularly limited and however, is not smaller than 0.01 in the light of the range of an activity ratio easily achieved.

The β -glucosidase activity used herein refers to the enzyme activity of producing glucose from cellobiose when cellobiose, a type of cellooligosaccharide, is used as a substrate, on which

cellulase is in turn allowed to act in an aqueous medium. The activity is measured by the number of moles of glucose generated in 1 mL of a reaction solution for 1 minute ($\mu\text{mol/mL}\cdot\text{min.}$) and expressed as a unit: U (unit)/mL. This β -glucosidase activity can be measured by dissolving 2% by mass of cellobiose (manufactured by Aldrich, special grade) and cellulase in 50 mM acetic acid/sodium acetate buffer at pH 4.5 and quantifying glucose concentration in the reaction solution after 1-hour reaction in a water bath at 55°C under sealed conditions.

The crystalline cellulose-decomposing activity used herein refers to the enzyme activity of producing celooligosaccharide such as cellobiose and cellotriose as well as glucose when crystalline cellulose is used as a substrate, on which cellulase is allowed to act in an aqueous medium. The activity is measured by the total number of moles of celooligosaccharide and glucose generated in 1 mL of a reaction solution for 1 minute ($\mu\text{mol/mL}\cdot\text{min.}$) and expressed as a unit: U (unit)/mL. This crystalline cellulose-decomposing activity can be measured by the above-described β -glucosidase activity measurement method, by which 5% by mass of crystalline cellulose (which is obtained by kneading and stirring Ceolus PH-101 (trade name, manufactured by Asahi Kasei Chemicals) whose moisture content has been brought to 60%, using a hook blade in an universal stirring mixer (trade name,

manufactured by Sanei Manufacturing) at 126 rpm for 90 minutes) is used instead of cellobiose and enzymatically decomposed in the same way as above to quantify the whole amount of sugars decomposed and generated such as cellooligosaccharide and glucose in the reaction solution.

In the above-described various activity measurement methods, cellooligosaccharide and glucose in the reaction solution can be quantified by high performance liquid chromatography (column: Asahipak NH₂P-50 (trade name, manufactured by Shimadzu), high performance liquid chromatography: SCL-10A model (trade name, manufactured by Shimadzu), moving bed: acetonitrile/water = 75/25 (by volume), circulation flow: 1 mL/min., sample solution: 10 μ L).

Methods of obtaining cellulase having an activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity) that satisfies the scope of the present invention include followings:

It is preferred that a strain that produces cellulase having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) not greater than 0.5 should be used as the cellulase-producing bacteria. Any strain can be used as long as the activity ratio satisfies the above-described range. Any of mutant strains obtained

by artificial mutagenesis methods of strains (e.g., ultraviolet irradiation, X-ray irradiation, treatment with mutation inducers), naturally-occurring mutant strains, or mutant strains obtained by gene
5 manipulation or cell fusion can be used in the present invention as long as the mutant strain produces cellulase having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) not greater than 0.5. This ratio
10 (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) is preferably not greater than 0.35, more preferably not greater than 0.2. Since a smaller activity ratio attains more improvement in the yield of
15 cellooligosaccharide, the smallest activity ratio is not particularly limited and however, is not smaller than 0.01 in the light of the range of an activity ratio easily achieved.

The β -glucosidase activity and the
20 crystalline cellulose-decomposing activity at a temperature of 40°C are measured by a method below.

(1) Crystalline cellulose-decomposing activity

After 0.4 ml of a substrate solution of 5% by
25 mass of crystalline cellulose (which is obtained by kneading and stirring Ceolus PH-101 (trade name, manufactured by Asahi Kasei Chemicals) whose moisture content has been brought to 60%, using a hook blade in

an universal stirring mixer (trade name, manufactured by Sanei Manufacturing) at 126 rpm for 90 minutes) suspended in 50 mM acetic acid-sodium acetate buffer (pH 5) is supplemented with 0.1 ml of an enzyme solution appropriately diluted, the mixture is reacted in a water bath at 40°C for 4 hours and then heated at 95°C for 10 minutes to terminate the reaction, followed by the quantification of glucose concentration in the reaction solution by a HPLC method. The amount of the enzyme that liberates a total of 1 μ mole of glucose and cellooligosaccharide for 1 minute is defined as 1 enzyme unit (1U).

(2) β -glucosidase activity

After 0.4 ml of a substrate solution of 2.5% by mass of cellobiose (manufactured by Aldrich, special grade) dissolved in 50 mM acetic acid-sodium acetate buffer (pH 5) is supplemented with 0.1 ml of an enzyme solution, the mixture is reacted in a water bath at 40°C for 4 hours and then heated at 100°C for 10 minutes to terminate the reaction, followed by the quantification of glucose concentration in the reaction solution by a HPLC method. The amount of the enzyme that liberates 1 μ mole of glucose for 1 minute is defined as 1 enzyme unit (1 U).

In the above-described various activity measurement methods, cellooligosaccharide and glucose in the reaction solution can be quantified by the above-described high performance liquid chromatography.

Here, an example of a typical strain used includes a *Trichoderma reesei* NBRC31329 strain.

In addition, the strain where an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) is small is obtained by, for example, a method below. A microorganism having the ability to produce cellulase is subjected, if necessary, to mutagenesis treatment known in the art such as ultraviolet irradiation or the use of a mutation inducer (e.g., nitrosoguanidine), and a strain where an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity) is small is selected from its strains. For example, *Trichoderma reesei* NBRC31329 is used as the microorganism (parent strain) used in mutagenesis treatment and is cultured on a potato dextrose agar slant medium at 28°C for 3 to 10 days. Generated spores are suspended at 10^5 to 10^8 spores/mL in saline and subjected to mutagenesis treatment with EMS (ethyl methanesulfonate) (100 to 500 μ g/ml, pH 7.0, 28°C, 5 to 24 hrs). The selection of a strain where an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) is small is achieved by collecting the spores from a suspension of the mutagenesis-treated spores by centrifugation and washing the spores, which are in turn cultured with glucose as a carbon source, followed by the measurement of enzyme activity of the resulting culture by a method

known in the art. A strain of interest may be selected quantitatively by using a culture from each mutagenesis-treated strain and enzymatically decompose cellobiose or crystalline cellulose used as a substrate to quantify a reducing sugar generated, or otherwise may be selected qualitatively by using a colorimetric substrate known in the art which is enzymatically reacted with the culture.

Cellulase can be acquired from a culture supernatant liquid obtained by culturing the cellulase-producing bacteria strain. The carbon source used in a medium is exemplified by cellulose powder, cellobiose, filter paper, general papers, sawdust, bran, chaff, bagasse, soybean cake, coffee grounds, starch, and lactose. Inorganic ammonium salts such as ammonium nitrate and ammonium sulfate as well as organic nitrogen-containing substances such as urea, amino acids, meat extracts, yeast extracts, polypeptone, and protein decomposition products are used as nitrogen sources. KH_2PO_4 , $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, $\text{Fe}_2\text{Cl}_3 \cdot 6\text{H}_2\text{O}$, $\text{MnCl}_3 \cdot 4\text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, and the like are used as inorganic salts. A medium containing an organic micronutrient is optionally used. For culture, a usual aerated spinner culture apparatus is used, and the above-described medium is used and controlled around a temperature and pH that allow the growth of the producing strains. Subsequently, the strain bodies are removed from the resulting culture solution by a method

known in the art such as centrifugation and filtration to obtain a supernatant liquid. This supernatant liquid can directly be used as a crude enzyme solution.

An example of a culture method for further
5 reducing the activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) includes a method of controlling the pH of the culture solution during culture at less than 3.5 and not smaller than pH that allows the growth
10 of the cellulase-producing bacteria. Specifically, the above-described *Trichoderma reesei* NBRC31329 strain or a mutant strain thereof is cultured on potato dextrose agar slant at 25 to 35°C for 3 to 10 days. The resulting cultures are inoculated and precultured at
15 28°C for 2 to 4 days in a medium where 100 mL of a medium containing cellulose as a carbon source suspended and dissolved has been dispensed into 500-mL Erlenmeyer flasks and autoclaved. The preculture solution is inoculated into a medium where 3 L of a
20 medium having the same composition as above has been placed in a 5-L jar fermentor and autoclaved, and is cultured at a temperature of 28°C, a stirring rate of 200 to 400 rpm, and an aeration rate of 0.3 to 1 vvm. The pH during culture is controlled at 2 to 3.5,
25 preferably 2.5 to 3.0, with NaOH or ammonia water. Following 4- to 7-day culture, the strain bodies are removed from the culture solution by a method known in the art such as centrifugation and filtration to obtain

a supernatant. This supernatant can directly be used as a crude enzyme solution.

The crude enzyme solution thus obtained may further be purified by a usual protein purification method, for example, ammonium sulfate fractionation, precipitation fractionation with a solvent, or column chromatography.

Alternatively, when the cellulase is obtained from a commercially-available enzyme, the enzyme is purified by a usual protein purification method such as ammonium sulfate fractionation, precipitation fractionation with a solvent, or column chromatography to obtain a fraction having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C) not greater than 0.7.

Hereinafter, a process of producing celooligosaccharide of the present invention will be described.

The process of producing celooligosaccharide of the present invention is a process of enzymatically decomposing the natural cellulosic material of the present invention in the presence of cellulase. It is preferred that the cellulase used in the process should have an activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C) not greater than 0.7. An aqueous solution mainly composed of the

cellooligosaccharide obtained in the present invention is purified and/or dried by a method known in the art.

Any method known in the art may be used without particular limitation as a method for enzymatic decomposition. One example thereof includes a method in which the cellulosic material of the present invention as a substrate is suspended in an aqueous medium, then supplemented with the cellulase of the present invention, and heated with stirring or shaking to perform saccharification reaction.

In the above-described method, reaction conditions such as suspending and stirring procedures, the procedure and order for adding the cellulase/substrate, and their concentrations are appropriately adjusted to give cellooligosaccharide in higher yields. In this case, the pH and temperature of the reaction solution may fall within the range that does not inactivate the enzyme and in general, may be in the temperature range of 5 to 95°C and the pH range of 1 to 11 when the reaction is performed under normal pressure. On this occasion, the pressure, temperature, and pH are also appropriately adjusted to give cellooligosaccharide in higher yields, as described above. However, in the case of using cellulase obtained with the above-described *Trichoderma reesei* NBRC31329 strain or a mutant strain thereof as cellulase-producing bacteria, it is preferred that the cellulose should enzymatically decomposed in an acetate

or phosphate buffer under normal pressure at a temperature of 50 to 60°C and a pH of 3.0 to 5.5.

This enzyme reaction may be performed as both batch and continuous systems. For avoiding product inhibition by cellobiose in the enzymatic decomposition reaction, cellobiose concentration in the reaction system, which is kept within a certain range, is important in improving the productivity of cellooligosaccharide. A method for keeping cellobiose concentration in the reaction system within a certain range may be a method where generated cellobiose is extracted from the reaction system by membrane filtration such as ultrafiltration or reverse osmosis filtration; a method where a porous organic base material such as a dried plant powder (e.g., activated carbon, a bamboo, and a wood), a porous inorganic base material such as silicon dioxide, and the like, are introduced into the reaction system and cellobiose is adsorbed in them; a method where the cellulose substrate is immobilized in a column or the like, in which a reaction solution containing the cellulase is circulated; or a method where the cellulase is immobilized in a polymer or the like, in which a reaction solution containing the cellulase is circulated.

An aqueous solution mainly composed of the cellooligosaccharide obtained by the above-described enzymatic decomposition can optionally be subjected to

purification treatment such as decolorization,
desalting, and enzyme removal. The purification method
is not particularly limited as long as the method is
known in the art. However, for example, activated
5 carbon treatment, ion-exchange resin treatment,
chromatography treatment, filtration treatment such as
microfiltration, ultrafiltration, and reverse osmosis
filtration, and crystallization treatment may be used.
These methods may be used alone, or two or more of them
10 may be combined.

The aqueous solution mainly composed of the
cellooligosaccharide, which has been purified by the
above-described method can be used without further
treatment and however, if necessary, may be solidified
15 by drying. The drying method is not particularly
limited as long as the method is known in the art.
However, for example, spray drying, freeze drying, drum
drying, thin-film drying, plate drying, flash drying,
and vacuum drying may be used. These methods may be
20 used alone, or two or more of them may be combined.

In the above-described purification and
drying treatments, for example, an organic solvent in
addition to water may optionally be used as a medium
for cellooligosaccharide. No particular limitation is
25 imposed on the organic solvent used in the treatment.
The organic solvent is preferably any of those used at
a step of producing, for example, pharmaceuticals,
foods, and additives thereof and includes those

classified as solvents in "Dictionary of Pharmaceutical Additives" (published by Yakuji Nippo), and "Japanese Pharmacopoeia" and "Official Method for Food Additives" (published by Hirokawa Publishing). Water and the
5 organic solvents may be used alone, or two or more of them may be used in combination. Alternatively, after one medium is used in dispersion and then removed, the cellooligosaccharide may be dispersed again in a different medium.

10 The cellooligosaccharide that has undergone the above-described steps can be used in a form including, but not particularly limited to, a solid, a suspension, an emulsion, a syrup, or a solution at normal temperature. One example of the solid
15 cellooligosaccharide includes a powder, a granule, a pellet, a molded matter, a laminate, and a solid dispersion.

Cellooligosaccharide obtainable by the process of the present invention is explained below.

20 The cellooligosaccharide of the present invention has a diethyl ether-soluble matter content preferably of 2000 ppm or less, more preferably of 1000 ppm or less. The diethyl ether-soluble matter content used herein refers to the content of impurities soluble
25 in diethyl ether, such as lignin, lignin-decomposed matter in the cellulosic material, and can be measured by the quantitative procedure for diethyl ether-soluble matter defined in Crystalline Cellulose Purity Test (2)

of Japanese Pharmacopoeia (the 14th revision, published by Hirokawa Publishing). Cellooligosaccharide having a diethyl ether-soluble matter content of 2000 ppm or less is preferable because it contains less impurities to show a high whiteness and can be easily purified upon using it in foods, cosmetics and pharmaceutical preparations. Particularly, when a cellooligosaccharide is used in combination with an active ingredient such as a medicament, it is preferable because it can reduce the decomposition of the active ingredient. When the cellooligosaccharide is used as a starting material for chemical conversion, it is preferable because it less likely causes side reactions and enhances chemical conversion and yield because of less impurities. The diethyl ether-soluble matter content is more preferably 1000 ppm or less, further preferably 500 ppm or less, still further preferably 300 ppm or less, most preferably 100 ppm or less. The less the diethyl ether-soluble matter content is, the more the above-mentioned effect becomes. Thus, although the lower limit thereof is not particularly restricted, the range of lignin content is 0.1 ppm or more, which can be achieved by concise procedure.

25 The cellooligosaccharide obtained by the present invention is not particular limited by applications and may be used as, for example, food, cosmetic, pigment, flavor, pharmaceutical active,

agrochemical, feed, fertilizer, medium, and analytical reagent ingredients, an additive, an intermediate raw material, and a fermentation raw material in fields such as foods, cosmetics, pharmaceuticals, and general
5 industrial products.

The application of the cellooligosaccharide obtained by the present invention in foods includes: gel such as jelly, pudding, and yogurt; seasonings such as mayonnaise, dressing, sauces, gravies, soup, and
10 processed vegetable; retort foods and chilled foods such as curry, hashed meat, meat sauce, stew, and soup; processed livestock products such as hamburger, bacon, sausage, salami sausage, and hams; fish paste products such as boiled fish paste, tube-shaped fish paste cake,
15 fish ham/sausage, and fried fish paste; processed wheat foods such as bread, wet noodle, dried noodle, macaroni, spaghetti, pasta wrapping for Chinese steamed bread, cake mix, premix, white sauce, and paste wrappings for jiao-zi and spring roll; canned and
20 bottled foods such as curry, sauce, soup, food boiled in soy sauce, and jam; confectioneries such as candy, troche, tablet, chocolate, biscuit, cookie, rice biscuit, Japanese/western confectionary, unbaked cake, snack food, confection, and pudding; cooked and
25 processed foods such as fried foods, croquette, jiao-zi, and Chinese steamed bread; and pastes such as vegetable paste, minced meat, fruit paste, and fish and seafood paste. Also included are milk products such as

ice cream, ice milk, lact ice, whipped cream, condensed milk, butter, yogurt, cheese, and white sauce as well as processed oil and fat products such as margarine, fat spread, and shortening. In addition, the
5 cellooligosaccharide may be used in carbonated beverages such as Coke; beverages such as carbonated fruit beverages, alcoholic fruit beverages, fruit beverages mixed with milk products, beverages with juice or pulp, and milk beverages; lactic acid/milk
10 beverages such as coffee, milk, soy milk, cocoa milk, fruit milk, and yogurt; and tea drinks such as boiled tea, oolong, green powdered tea, and black tea.

The cellooligosaccharide obtained in the present invention is expected to attain diverse
15 physiological activity such as the activation of useful intestinal bacterial flora (e.g., the activation of lactic acid bacteria and lactobacilli), reduction in blood sugar concentration and blood insulin concentration, reduction in blood cholesterol, decrease
20 in body fat percentage, the function of promoting lipid/carbohydrate metabolism, improvement in bowel movement/stercoral odor, and anti-carries properties. Thus, in addition to the above-described applications in usual foods, the cellooligosaccharide may be used as
25 a physiologically-active substance in applications such as functional foods, healthy foods, and diet foods.

Furthermore, because the cellooligosaccharide obtained in the present invention is highly pure, the

cellooligosaccharide may be used as a raw material for chemical conversion into a variety of cellooligosaccharide derivatives.

[Examples]

5 Although the present invention will be described in accordance with Examples, the present invention is not intended to be limited to them.

(Example 1)

 In a low-speed stirrer (30-L reactor), 2 kg
10 of commercially-available dissolving pulp derived from a coniferous tree (average degree of polymerization: 781, diethyl ether-soluble matter content: 1.1%, average particle size: 174 μm) and 30 L of 3 N hydrochloric acid solution were placed and hydrolyzed
15 with stirring at 105°C for 30 minutes. The resulting acid-insoluble residue was filtered with a Nutsche and washed four times in 70 L of pure water to obtain wet cake having a solid content of 40.1% (average degree of polymerization: 220, diethyl ether-soluble matter
20 content: 0.03% by mass, average particle size: 69.1 μm , colloidal cellulose content: 13.4% by mass, cellulose I crystals content: 85%).

 A commercially-available cellulase preparation derived from Trichoderma (trade name:
25 T"Amano"4) which had been dissolved in 0.2 N acetic acid-sodium acetate buffer (pH 4.5) was added to the wet cake so that the solid content and protein concentration of the wet cake were adjusted to 5% and

0.25%, respectively. The mixture (25 mL in total) thus obtained was placed in a 50-mL glass vial. This glass vial was placed in a constant-temperature shaking water bath at 48°C and reacted at a shaking speed of 90 rpm for a fixed period of time shown in Table 1. In a fixed period of time shown in Table 1 after the initiation of reaction, 300 μ L of the reaction solution remaining suspended was dispensed. After an ultrafiltration module (molecular weight cut-off: 5000) was used to remove the enzyme, the resulting solution was analyzed by high performance liquid chromatography (manufactured by Shimadzu, column: TSK-GEL AMIDO-80 (trade name, manufactured by Tosoh), moving bed: acetonitrile/water = 6/4). The obtained result is shown in Table 1. The selectivity of oligosaccharide in the table is a value calculated by (cellobiose concentration + cellotriose concentration)/total sugar concentration $\times$ 100 (%).

(Example 2)

Commercially-available dissolving pulp derived from a coniferous tree (average degree of polymerization: 781, diethyl ether-soluble matter content: 1.1%, average particle size: 174 μ m) was subjected to acid hydrolysis in the same way as Example 1. The resulting wet cake was made into a flock form, then placed in a flash drier at 60°C, and dried for 12 hours.

The resulting dried material was crushed with

a home-use mixer, and the obtained crushed cellulose material was pulverized with an air-jet crusher (manufactured by Seishin Enterprise, trade name: Jet Mill STJ-2000 model) to obtain a cellulose powder (average degree of polymerization: 220, diethyl ether-soluble matter content: 0.03% by mass, average particle size: 16.4 μm , colloidal cellulose content: 17.5% by mass, cellulose I crystals content: 86%). This cellulose powder was used as a substrate and enzymatically decomposed in the same way as Example 1. The obtained result is shown in Table 1.

Example 2 employed the average degree of polymerization and diethyl ether-soluble matter content identical to those in Example 1, the average particle size smaller than in Example 1, and the colloidal cellulose content larger than in Example 1. As seen from Table 1, in Example 2, the reaction time required for sugar concentration to reach 10% and 20% was reduced and the selectivity of oligosaccharide was improved for each sugar concentration, as compared with Example 1, by reducing the average particle size of the substrate.

(Example 3)

Commercially-available dissolving pulp derived from a broadleaf tree (average degree of polymerization: 1682, diethyl ether-soluble matter content: 0.9%, average particle size: 91 μm) was subjected to acid hydrolysis in the same way as Example

1. The resulting wet cake was supplemented with pure water to make a dispersion having a cellulose concentration of 10%. The dispersion was stirred for 30 minutes with a high-shear homogenizer (manufactured by Tokushu Kika Kogyo, trade name TK Homogenizer) to obtain a cellulose dispersion (average degree of polymerization: 151, diethyl ether-soluble matter content: 0.1% by mass, average particle size: 8.7 μm , colloidal cellulose content: 55.5% by mass, cellulose I crystals content: 85%). This cellulose dispersion was used as a substrate and enzymatically decomposed in the same way as Example 1. The obtained result is shown in Table 1.

Example 3 employed smaller average degree of polymerization, higher diethyl ether-soluble matter content, smaller average particle size, and higher colloidal cellulose content, than those in Examples 1 and 2. As seen from Table 1, in Example 3, the reaction time was further reduced and the selectivity of oligosaccharide was improved for each sugar concentration, as compared with Examples 1 and 2. Although the selectivity of oligosaccharide decreased with a rise in sugar concentration in Examples 1 and 2, the selectivity of oligosaccharide did not decrease in Example 3 even by a rise in sugar concentration.

(Example 4)

Commercially-available dissolving pulp derived from a coniferous tree (average degree of

polymerization: 781, diethyl ether-soluble matter
content: 1.1% by mass, average particle size: 174 μm)
was subjected to hydrolysis in the same way as Example
1 except for conditions of hydrolysis conducted with 5
5 N hydrochloric acid solution at hydrochloric acid
concentration at 18°C for 12 hours. As with Example 1,
the resulting acid-insoluble residue was washed and
filtrated to obtain wet cake (average degree of
polymerization: 690, diethyl ether-soluble matter
10 content: 0.7%, average particle size: 49.8 μm). This
wet cake was made into a water dispersion having a
cellulose concentration of 10%. The water dispersion
was subjected to consolidation/grinding treatment with
a super-performance dispersing/wet-pulverizing machine
15 (manufactured by Ashizawa, trade name: Pearl Mill RL,
with $\phi 2$ mm alumina beads, filling rate: 80%) to obtain
a cellulose particulate dispersion (average degree of
polymerization: 690, diethyl ether-soluble matter
content: 0.7% by mass, average particle size: 7.1 μm ,
20 colloidal cellulose content: 87.5% by mass, cellulose I
crystals content: 77%). This cellulose particulate
dispersion was used as a substrate and enzymatically
decomposed in the same way as Example 1. The obtained
result is shown in Table 1.

25 Example 4 employed higher average degree of
polymerization and diethyl ether-soluble matter
content, smaller average particle size, and higher
colloidal cellulose content, than those in Examples 1,

2, and 3. As seen from Table 1, in Example 4, the selectivity of oligosaccharide was equal to that in Example 3 and however, the reaction time was improved as compared with Examples 3. Moreover, the selectivity of oligosaccharide hardly decreased in Example 4 even by a rise in sugar concentration.

(Example 5)

Hydrolysis was conducted in the same way as in Example 1 except that commercially-available pulp derived from cotton linter (average degree of polymerization: 1853) was used and the hydrolysis was conducted in 5 N aqueous hydrochloric acid solution at 130°C for 12 hours, to obtain wet cake (average degree of polymerization: 49). This wet cake was made into a water dispersion having a cellulose concentration of 10%. The water dispersion was subjected to consolidation/grinding treatment with a super-performance dispersing/wet-pulverizing machine (manufactured by Ashizawa, trade name: Pearl Mill RL, with $\phi 2$ mm alumina beads, filling rate: 80%) to obtain a cellulose particulate dispersion (average degree of polymerization: 49, diethyl ether-soluble matter content: 0.9% by mass, average particle size: 10.3 μm , colloidal cellulose content: 94.1% by mass, cellulose I crystals content: 75%). This cellulose particulate dispersion was used as a substrate and enzymatically decomposed in the same way as in Example 1 except for changing the enzyme to CELLULASENAGASE (manufactured by

Nagase & Co., Ltd., trade name) derived from *Aspergillus niger*. The obtained result is shown in Table 1.

Example 5 employed lower average degree of polymerization, higher diethyl ether-soluble matter content and larger average particle size but higher colloidal cellulose content, than Example 4. As seen from Table 1, in Example 5, the reaction time was decreased by half and the selectivity of oligosaccharide increased than in Example 4. (Comparative Example 1)

The commercially-available coniferous tree-derived dissolving pulp used in Example 1 was added to 3 N hydrochloric acid solution to make a dispersion having a cellulose concentration of 10%. The dispersion was stirred at normal temperature for 60 minutes with a high-shear homogenizer (manufactured by Tokushu Kika Kogyo, trade name TK Homogenizer) to obtain a cellulose dispersion (average degree of polymerization: 723, diethyl ether-soluble matter content: 0.9% by mass, average particle size: 49.3 μm , colloidal cellulose content: 10.2% by mass, cellulose I crystals content: 85%). This cellulose dispersion without undergoing acid hydrolysis was used as a substrate and enzymatically decomposed in the same way as Example 1. The obtained result is shown in Table 1.

Comparative Example 1 employed the average particle size and diethyl ether-soluble matter content

falling within the scope of the present invention and the average degree of polymerization exceeding the scope. As seen from Table 1, in Comparative Example 1, the reaction time required for sugar concentration to reach 10% and 20% was extended and the enzymatic decomposition was slowed, as compared with each Example. In addition, the selectivity of oligosaccharide for any sugar concentration fell short of the level of each Example.

10 (Comparative Example 2)

The wet cake obtained by the procedures in Example 4 was made into a water dispersion having a cellulose concentration of 10%. The water dispersion was subjected to wet fractionation using a sieve having a mesh size of 45 μm . A solid content (average degree of polymerization: 690, diethyl ether-soluble matter content: 0.7% by mass, average particle size: 107.3 μm , colloidal cellulose content: 5.2% by mass, cellulose I crystals content: 85%) remaining on the sieve was used as a substrate and enzymatically decomposed in the same way as Example 1. The obtained result is shown in Table 1.

Comparative Example 2 employed the average degree of polymerization and diethyl ether-soluble matter content falling within the scope of the present invention and the average particle size exceeding the scope. As seen from Table 1, in Comparative Example 2, the reaction time was slowed as compared with each

Example, and the selectivity of oligosaccharide fell short of the level of each Example.

(Comparative Example 3)

Commercially-available unbleached kraft pulp
5 derived from a coniferous tree (average degree of
polymerization: 1670, diethyl ether-soluble matter
content: 12% by mass, average particle size: 154 μm)
was subjected to hydrolysis in the same was as Example
1 except for conditions of hydrolysis conducted with 4
10 N hydrochloric acid solution at hydrochloric acid
concentration at 35°C for 18 hours. As with Example 1,
the resulting acid-insoluble residue was washed and
filtrated to obtain wet cake (average degree of
polymerization: 490, diethyl ether-soluble matter
15 content: 4.4% by mass, average particle size: 48.7 μm ,
colloidal cellulose content: 12.8% by mass, cellulose I
crystals content: 86%).

This wet cake was used and enzymatically
decomposed in the same way as Example 1. The obtained
20 result is shown in Table 1.

Comparative Example 3 employed the average
degree of polymerization and average particle size
falling within the scope of the present invention and
the diethyl ether-soluble matter content exceeding the
25 scope. As seen from Table 1, in Comparative Example 3,
the yield of cellooligosaccharide was slightly improved
as compared with Comparative Examples 1 and 2 and
however, both of the reaction time and the selectivity

of oligosaccharide fell short of the levels of
Examples.

[Table 1]

	Fundamental physical property of cellulose substrate				Enzymatic decomposition data		
	Average degree of polymerization (-)	Average particle size (μm)	Colloidal component content (% by mass)	Diethyl ether-soluble matter content (% by mass)	Total sugar concentration (mg/mL)	Reaction time (hr)	Selectivity of oligo-saccharide (%)
Example 1	220	69.1	13.4	0.03	10 20	5 19	54.0 13.0
Example 2	220	16.4	17.5	0.03	10 20	4 17	61.0 15.0
Example 3	151	8.7	55.5	0.1	10 20	1.5 5	54.0 55.5
Example 4	690	7.1	87.5	0.7	10 20	1 4	57.0 52.0
Example 5	49	10.3	94.1	0.9	10 20	0.6 2	61.0 60.5
Comparative Example 1	723	49.3	10.2	0.9	10 20	10 36	33.0 7.5
Comparative Example 2	690	107.3	5.2	0.7	10 20	8 24	15.0 8.5
Comparative Example 3	490	48.7	12.8	4.4	10 20	12 44	37.2 10.5

(Production Example 1)

After *Trichoderma reesei* NBRC31329 was inoculated into a potato dextrose medium (manufactured by Difco) and cultured at 37°C for 7 days, one loopful
5 of spores taken from the surface of the medium was inoculated and precultured at 28°C for 3 days in a medium where 1 g of polypeptone, 0.5 g of a yeast extract, 2 g of monopotassium phosphate, 1.5 g of ammonium sulfate, 0.3 g of magnesium sulfate, 0.3 g of
10 calcium chloride, 1 mL of a trace element (which had been obtained by dissolving 6 mg of boric acid, 26 mg of ammonium molybdate tetrahydrate, 100 mg of iron (III) chloride hexahydrate, 40 mg of copper sulfate pentahydrate, 8 mg of manganese sulfate tetrahydrate,
15 and 200 mg of zinc sulfate heptahydrate in a total of 100 mL of purified water), 1 mL of Adecanol LG-109, and 10 g of crystalline cellulose (manufactured by Asahi Kasei Chemicals, trade name: PH-101) had been suspended and dissolved in a total of 1 L of purified water,
20 whose 100 mL had in turn been dispensed to 500-mL Erlenmeyer flasks and autoclaved. Further, 10 mL of the preculture solution was inoculated into a 5-L jar fermentor in which 1 L of a medium having the same composition as above had been placed, and was cultured
25 at a temperature of 28°C, a stirring rate of 400 rpm, and an aeration rate of 0.5 vvm. The pH during culture was controlled at 3 with NaOH. Following 7-day culture, the resulting solution was centrifuged. The

strain bodies were removed from the obtained supernatant with a microfiltration membrane having a mesh size of 0.46 μm . The filtrate was condensed tenfold by volume with an ultrafiltration membrane having a molecular weight cut-off of 13000 (manufactured by Asahi Kasei Chemicals, trade name: Microza Pencil Module ACP-0013) to obtain a crude enzyme.

Table 2 shows the result of this crude enzyme measured for an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C).

(Production Example 2)

After *Trichoderma reesei* NBRC31329 was inoculated into a potato dextrose medium (manufactured by Difco) and cultured at 37°C for 7 days, one loopful of spores taken from the surface of the medium was inoculated and cultured at 28°C for 3 days in a medium where 1 g of polypeptone, 0.5 g of a yeast extract, 2 g of monopotassium phosphate, 1.5 g of ammonium sulfate, 0.3 g of magnesium sulfate, 0.3 g of calcium chloride, 1 mL of a trace element (which had been obtained by dissolving 6 mg of boric acid, 26 mg of ammonium molybdate tetrahydrate, 100 mg of iron (III) chloride hexahydrate, 40 mg of copper sulfate pentahydrate, 8 mg of manganese sulfate tetrahydrate, and 200 mg of zinc sulfate heptahydrate in a total of 100 mL of purified water), 1 mL of Adecanol LG-109, and 10 g of

crystalline cellulose (manufactured by Asahi Kasei Chemicals, trade name: PH-101) had been suspended and dissolved in a total of 1 L of purified water, whose 100 mL had in turn been dispensed to 500-mL Erlenmeyer
5 flasks and autoclaved. Further, 10 mL of the preculture solution was inoculated into a 5-L jar fermentor in which 1 L of a medium having the same composition as above had been placed, and was cultured at a temperature of 28°C, a stirring rate of 400 rpm,
10 and an aeration rate of 0.5 vvm. The pH during culture was controlled at 4 with NaOH. Following 7-day culture, the resulting solution was centrifuged. The strain bodies were removed from the obtained supernatant with a microfiltration membrane having a
15 mesh size of 0.46 μm . The filtrate was condensed tenfold by volume with an ultrafiltration membrane having a molecular weight cut-off of 13000 (manufactured by Asahi Kasei Chemicals, trade name: Microza Pencil Module ACP-0013) to obtain a crude
20 enzyme.

Table 2 shows the result of this crude enzyme measured for an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C).

25 (Production Example 3)

Commercially-available cellulase (manufactured by Godo Shusei, trade name: GODO-TCD) was dissolved in 50 mM acetic acid-sodium acetate buffer

(pH 4.8) to bring the concentration of the cellulase to 500 mg/mL. The mixture was introduced into an anion-exchange column (manufactured by Amersham, trade name: DEAE-Sepharose FF). Fractionated samples were obtained from the commercially-available enzyme by a linear gradient method by which 50 mM acetic acid-sodium acetate buffer (pH 4.8) and 1 mole% sodium chloride dissolved in 50 mM acetic acid-sodium acetate buffer (pH 4.8) were circulated in the column. All of the obtained fractions were measured for β -glucosidase activity and crystalline cellulose-decomposing activity, and fractions having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C) not greater than 0.5 were combined. The obtained cellobiose fractions were condensed fivefold by volume with an ultrafiltration module having a molecular weight cut-off of 10000 (manufactured by Millipore, trade name: Amicon Ultra-15 Centrifugal Filter) to obtain a purified enzyme (protein concentration in the purified enzyme: 15.4 mg/mL).

Table 2 shows the result of this purified enzyme measured for an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C).

(Example 6)

In a low-speed stirrer (30-L reactor), 2 kg of Commercially-available dissolving pulp derived from

a coniferous tree (average degree of polymerization: 781, diethyl ether-soluble matter content: 1.1%, average particle size: 174 μm) was placed and subjected to hydrolysis under conditions of hydrolysis conducted with 3 N hydrochloric acid solution at 110°C for 30 minutes. The resulting acid-insoluble residue was washed and filtered to obtain wet cake. The obtained wet cake was made into a flock form and aerated/dried in an oven at 60°C for 12 hours. The resulting dried material was supplemented with purified water to bring its moisture content to 60%, and grinded with a mixer (manufactured by Sanei Manufacturing, trade name: universal stirring mixer, with a hook blade at 126 rpm for 90 minutes) to obtain ground cellulose (average degree of polymerization: 220, average particle size: 9.1 μm , colloidal cellulose component content: 66.1% by mass, diethyl ether-soluble matter content: 0.03% by mass, cellulose I crystals content: 78%).

Then, 5% by mass of this ground cellulose was suspended and dissolved in 50 mM acetic acid-sodium acetate buffer (pH 4.8) of the crude enzyme obtained in Production Example 1. The mixture (25 mL in total) thus obtained was placed in a glass vial. This glass vial was placed in a constant-temperature shaking water bath at 55°C and reacted at a shaking speed of 90 rpm. In a fixed period of time after the initiation of reaction, 300 μL of the reaction solution remaining suspended was dispensed. After an ultrafiltration

module (molecular weight cut-off: 10000) was used to remove the enzyme and undecomposed cellulose, the resulting solution was analyzed for sugar concentration by high performance liquid chromatography. The
5 obtained result is shown in Table 2.

Cellooligosaccharide and glucose in the reaction solution were quantified by high performance liquid chromatography (column: Asahipak NH₂P-50 (trade name, manufactured by Shimadzu), high performance
10 liquid chromatography: SCL-10A model (trade name, manufactured by Shimadzu), moving bed: acetonitrile/water = 75/25 (by volume), circulation flow: 1 mL/min., sample solution: 10 μ L).

Reaction time in the table is reaction time
15 required for the ratio of the total amount of sugars (cellooligosaccharide and glucose) generated to the amount of cellulose used to reach 20% by mass. The selectivity of oligosaccharide is represented by a value calculated by (cellobiose concentration +
20 cellotriose concentration)/total sugar concentration $\times$ 100 (%).

(Example 7)

Commercially-available dissolving pulp derived from a coniferous tree (average degree of
25 polymerization: 781, diethyl ether-soluble matter content: 1.1%, average particle size: 174 μ m) was subjected to hydrolysis in the same way as Example 1 except for conditions of hydrolysis conducted with 5 N

hydrochloric acid solution at hydrochloric acid concentration at 18°C for 12 hours. As with Example 1, the resulting acid-insoluble residue was washed and filtrated to obtain wet cake (average degree of polymerization: 690, diethyl ether-soluble matter content: 0.7% by mass, average particle size: 49.8 μm). This wet cake was made into a water dispersion having a cellulose concentration of 10%. The water dispersion was subjected to consolidation/grinding treatment with a super-performance dispersing/wet-pulverizing machine (manufactured by Ashizawa, trade name: Pearl Mill RL, with $\phi 2$ mm alumina beads, filling rate: 80%) to obtain a cellulose particulate dispersion (average degree of polymerization: 690, diethyl ether-soluble matter content: 0.7% by mass, average particle size: 7.1 μm , colloidal component content: 87.5% by mass, cellulose I crystals content: 77%). Moreover, the obtained wet cake was enzymatically decomposed in the same way as Example 6. The obtained result is shown in Table 2.

In Example 7, the cellulose having smaller average particle size and higher colloidal component content than those in Example 6 was enzymatically decomposed. The reaction time was reduced and the selectivity of oligosaccharide was improved, as compared with Example 6.

(Example 8)

The cellulose wet cake obtained in Example 6 was used and enzymatically decomposed with the purified

enzyme obtained in Production Example 3 in the same way as Example 1. The obtained result is shown in Table 2.

Example 8 employed the enzyme having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity) smaller than that in Example 6. Although the reaction time was extended by changing the enzyme, the selectivity was improved. (Example 9)

Commercially-available dissolving pulp derived from a coniferous tree (average degree of polymerization: 781, diethyl ether-soluble matter content: 1.1% by mass, average particle size: 174 μm) was hydrolyzed with stirring at 105 °C for 30 minutes. The resulting acid-insoluble residue was filtered with a Nutsche and washed four times in 70 L of pure water to obtain wet cake having a solid content of 40.1% (average degree of polymerization: 220, average particle size: 69.1 μm , colloidal component content: 13.4% by mass, diethyl ether-soluble matter content: 0.03% by mass, cellulose I crystals content: 85%). This cellulose wet cake was used and enzymatically decomposed with the purified enzyme obtained in Production Example 3 in the same way as Example 6. The obtained result is shown in Table 2.

Example 9 employed the enzyme having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity) smaller than that in Example 6 as well as the cellulose having larger

average particle size and lower colloidal component content than those in Example 6. Although the reaction time was extended by changing the enzyme and the substrate, the selectivity was improved.

5 (Example 10)

The cellulose wet cake obtained in Example 6 was used and enzymatically decomposed with the enzyme obtained in Production Example 2 in the same way as Example 6. The obtained result is shown in Table 2.

10 Example 10 employed the enzyme having an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity) larger than that in Example 6. Although the reaction time was equal to that in Example 6 by changing the enzyme, the
15 selectivity was reduced.

(Comparative Example 4)

The commercially-available pulp used in Examples 6 to 9 (average degree of polymerization: 781) was used without hydrolysis. The pulp was supplemented
20 with pure water (solid content: 40% by mass) and subjected to grinding treatment in the same way as Example 6 to obtain wet cake (average degree of polymerization: 781, average particle size: 49.3 μm , colloidal cellulose component content: 10.2% by mass,
25 diethyl ether-soluble matter content: 0.9% by mass, cellulose I crystals content: 85%). This wet cake was used and enzymatically decomposed in the same way as Example 6. The obtained result is shown in Table 2.

Comparative Example 4 employed the cellulose having the average degree of polymerization exceeding the scope of the present invention and the average particle size and colloidal cellulose component content falling within the scope of the present invention. The reaction time was extended and the selectivity of celooligosaccharide was reduced as compared with each Example.

(Comparative Example 5)

10 The wet cake obtained by the procedures in Example 6 was made into a water dispersion having a cellulose concentration of 10%. The water dispersion was subjected to wet fractionation using a sieve having a mesh size of 45 μm . A solid content (average degree
15 of polymerization: 220, average particle size: 103.4 μm , colloidal component content: 9.7% by mass, diethyl ether-soluble matter content: 0.03% by mass, cellulose I crystals content: 85%) remaining on the sieve was used as a substrate and enzymatically decomposed in the
20 same way as Example 6. The obtained result is shown in Table 2.

Comparative Example 5 employed the average degree of polymerization and diethyl ether-soluble matter content falling within the scope of the present
25 invention as well as the average particle size exceeding the scope and the colloidal component content smaller than the scope. In Comparative Example 5, the reaction time was slowed as compared with each Example,

and the selectivity of cellooligosaccharide fell short of the level of each Example.

[Table 2]

	Physical property value of cellulosic material				Physical property value of cellulase			Result of enzymatic decomposition	
	Average degree of polymerization (-)	Average particle size (μm)	Colloidal cellulose component content (% by mass)	Diethyl ether-soluble matter content (% by mass)	β-glucosidase activity : A (U/ml)	Crystalline cellulose-decomposing activity : B (U/ml)	Activity ratio : A/B at 55°C	Reaction time (hr)	Selectivity of oligo-saccharide (%)
Example 6	220	9.1	66.1	0.03	0.17	0.54	0.31	5	67.6
Example 7	690	7.1	87.5	0.7	0.17	0.54	0.31	4	75.7
Example 8	220	9.1	66.1	0.03	0.10	0.58	0.17	8	83.4
Example 9	220	69.1	13.4	0.03	0.10	0.58	0.17	24	72.6
Example 10	220	9.1	66.1	0.03	0.22	0.51	0.43	5	59.4
Comparative Example 4	781	49.3	10.2	0.9	0.17	0.54	0.31	39	50.4
Comparative Example 5	220	103.4	9.7	0.03	0.17	0.54	0.31	30	66.3

(Example 11)

Trichoderma reesei NBRC31329 was cultured on a potato dextrose agar slant medium at 28°C for 7 days. Generated spores were suspended at 10^6 spores/mL in 2 ml of 100 mM calcium phosphate buffer (pH 7) and supplemented with 24 μ l of EMS (ethyl methanesulfonate). The mixture was shaken at 28°C for 16 hours to apply mutagenesis treatment to the mixture. The spores were collected from the spore suspension by centrifugation, then well washed in 100 mM calcium phosphate buffer (pH 7), and diluted to attain 100 to 300 spores per plate. The diluent was cultured at 28°C for 5 days in a medium where 1 g of glucose, 1 g of a yeast extract, 2 g of $(\text{NH}_4)_2\text{SO}_4$, 4 g of KH_2PO_4 , 2 g of Na_2HPO_4 , 200 mg of $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 1 mg of $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, TritonX-100, 1 mL of a trace element (which had been obtained by dissolving 6 mg of boric acid, 26 mg of ammonium molybdate tetrahydrate, 100 mg of iron (III) chloride hexahydrate, 40 mg of copper sulfate pentahydrate, 8 mg of manganese sulfate tetrahydrate, and 200 mg of zinc sulfate heptahydrate in a total of 100 mL of purified water), and 20 g of agar had been dissolved or suspended in 1 L of purified water, then autoclaved, and sterilized by filtration with a membrane filter. The resulting culture solution was measured for β -glucosidase activity and crystalline cellulose-decomposing activity to select a mutant strain Trichoderma ressei GL-1. This mutant strain has

been deposited at International Patent Organism
Depository National Institute of Advanced Industrial
Science and Technology (AIST Tsukuba Central 6, 1-1,
Higashi 1-chome, Tsukuba-shi, Ibaraki-ken 305-8566
5 Japan) under the Budapest Treaty since April 15, 2005
and received Accession No. FERM BP-10323.

(Example 12)

Each of *Trichoderma reesei* NBRC31329 and the
mutant GL-1 strain obtained in Example 11 was cultured
10 on a potato dextrose agar slant medium at 25°C for 7
days to sufficiently form spores. One loopful of the
spores was inoculated and cultured with stirring at 28°C
for 5 days in a medium where 1.0 g of polypeptone, 0.5
g of a yeast extract, 2.0 g of KH_2PO_4 , 1.5 g of
15 $(\text{NH}_4)_2\text{SO}_4$, 0.3 g of $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 0.3 g of $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, 1.0
ml of Tween 80 (manufactured by Nacalai Tesque), 1.0 ml
of a trace element solution (a solution obtained by
dissolving and suspending 6 mg of H_3BO_3 , 26 mg of
 $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$, 100 mg of $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$, 40 mg of
20 $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$, 8 mg of $\text{MnSO}_4 \cdot 4\text{H}_2\text{O}$, and 200 mg of $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$
in 100 ml of water), and 7.5 g of tartaric acid had
been dissolved and suspended in 1 L of water followed
by the adjustment of pH to 4.0, whose 100 mL had been
dispensed to 500-mL Erlenmeyer flasks, then
25 supplemented with 1 g of crystalline cellulose
(manufactured by Asahi Kasei Chemicals, trade name: PH-
101), and autoclaved. On the five days, the culture
solution was centrifuged. The resulting supernatant

was measured for cellulase activity and β -glucosidase activity at a temperature of 40°C. The result is shown in Table 3.

(Example 13)

5 *Trichoderma reesei* NBRC31329 was inoculated into a potato dextrose medium (manufactured by Difco) and cultured at 37°C for 7 days. One loopful of spores taken from the surface of the medium were inoculated and precultured at 28°C for 3 days in a medium where 1 g
10 of polypeptone, 0.5 g of a yeast extract, 2 g of monopotassium phosphate, 1.5 g of ammonium sulfate, 0.3 g of magnesium sulfate, 0.3 g of calcium chloride, 1 mL of a trace element (which had been obtained by dissolving 6 mg of boric acid, 26 mg of ammonium
15 molybdate tetrahydrate, 100 mg of iron (III) chloride hexahydrate, 40 mg of copper sulfate pentahydrate, 8 mg of manganese sulfate tetrahydrate, and 200 mg of zinc sulfate heptahydrate in a total of 100 mL of purified water), and 1 mL of Adecanol LG-109 had been suspended
20 and dissolved in a total of 1 L of purified water, whose 100 mL had in turn been dispensed to 500-mL Erlenmeyer flasks, each of which had been supplemented with 1 g of crystalline cellulose (manufactured by Asahi Kasei Chemicals, trade name: PH-101) and
25 autoclaved. Further, 30 mL of the preculture solution was inoculated into a 5-L jar fermentor in which 3 L of a medium having the same composition as above had been placed, and was cultured at a temperature of 28°C, a

stirring rate of 400 rpm, and an aeration rate of 0.5 vvm. The lowest pH during culture was controlled at 3.0 with a NaOH solution. Following 5-day culture, the resulting solution was centrifuged to obtain a supernatant as a crude enzyme. The obtained enzyme solution was measured for crystalline cellulose-decomposing activity and β -glucosidase activity by the above-described method. Temporal changes in pH during culture are shown FIG. 1, and the result of activity measurement is shown in Table 4.

(Example 14)

When *Trichoderma reesei* NBRC31329 was cultured in the same way as Example 13, the lowest pH during culture was controlled at 2.5 with NaOH to obtain a crude enzyme solution. The obtained enzyme solution was measured for crystalline cellulose-decomposing activity and β -glucosidase activity by the above-described method. Temporal changes in pH during culture are shown FIG. 1, and the result of activity measurement is shown in Table 4.

(Comparative Example 6)

When *Trichoderma reesei* NBRC31329 was cultured in the same way as Example 13, the lowest pH during culture was controlled at 3.5 or 4 or 5 with NaOH to obtain a crude enzyme solution. The obtained enzyme solution was measured for crystalline cellulose-decomposing activity and β -glucosidase activity by the above-described method. Temporal changes in pH during

culture are shown FIG. 1, and the result of activity measurement is shown in Table 4.

(Example 15)

The GL-1 strain obtained in Example 11 was
5 cultured in the same way as Example 13. When the strain was cultured, the lowest pH during culture was controlled at 3 or 4 with NaOH to obtain a crude enzyme solution. Temporal changes in pH during culture are shown FIG. 2.

10 (Example 16)

To 8 ml of 5% by mass of crystalline cellulose (which had been obtained by kneading and stirring Ceolus PH-101 (trade name, manufactured by Asahi Kasei Chemicals) whose moisture content had been
15 brought to 60%, using a hook blade in an universal stirring mixer (trade name, manufactured by Sanei Manufacturing) at 126 rpm for 90 minutes), 2 mL of each of the cellulase crude enzyme solutions obtained in Examples 13 and 15 was added, and hydrolysis was
20 performed under stirring conditions at 55°C. After 2-hr, 4-hr, 6-hr, and 8-hr reactions, the mixtures were heated at 95°C for 15 minutes to terminate enzyme reaction. Supernatant liquids were obtained by centrifugation and measured for celooligosaccharide
25 and glucose concentrations by the above-described HPLC method. The result is shown in FIG. 3.

(Comparative Example 7)

When crystalline cellulose was enzymatically

decomposed in the same way as Example 16, the cellulase obtained in Comparative Example 6 was used as a crude enzyme solution. The result is shown in FIG. 3.

[Table 3]

Strain	Crystalline cellulose-decomposing activity (A) (U/ml)	β -glucosidase activity (B) (U/ml)	(B) / (A)
NBRC31329	0.50	0.23	0.46
GL-1	0.58	0.20	0.34

5 [Table 4]

Culture pH	Culture time (hr)	Crystalline cellulose-decomposing activity (A) (U/ml)	β -glucosidase activity (B) (U/ml)	(B) / (A)
2.5	90	0.402	0.052	0.13
3	65	0.501	0.069	0.14
3.5	65	0.571	0.214	0.37
4	65	0.358	0.145	0.40
5	65	0.272	0.102	0.38

(Example 17)

Commercially-available crystalline cellulose (manufactured by Asahi Kasei Chemicals, trade name: PH-101) was made into a water dispersion having 10% by mass of a solid content and subjected to wet grinding with a bead mill (manufactured by Ashizawa Finetech, trade name: Pearl Mill RL5, vessel size: 5 L, grinding medium: ϕ 1 mm zirconia beads, revolution speed: 1800 rpm, retention time in the vessel: 70 minutes). Then,

100 ml of the obtained ground cellulose water dispersion (average degree of polymerization: 220, average particle size: 0.7 μm , colloidal cellulose content: 54% by mass, diethyl ether-soluble matter content: 0.03% by mass, cellulose I crystals content: 75%) was supplemented with 200 mL of a crude enzyme solution obtained by condensing (fivefold by volume) the supernatant cultured at pH 3 in Example 15 by ultrafiltration (molecular weight cut-off: 13000). Its total volume was adjusted to 500 mL by the addition of 50 mM acetic acid/sodium acetate buffer (pH 4.5). The mixture was placed in a 1-L glass separable flask and reacted in a warm bath at 55°C with internal stirring with 3-1 Motor (trade name). In two hours after the initiation of reaction, 300 μL of the reaction solution remaining suspended was dispensed. After an ultrafiltration module (molecular weight cut-off: 10000) was used to remove the enzyme and undecomposed cellulose, the resulting solution was analyzed for sugar concentration by high performance liquid chromatography to quantify a cellulose residue present in the reaction solution. From the result, in the reaction time of 2 hours, the decomposition rate of cellulose was 82%, and the selectivity of oligosaccharide was 81%.

(Example 18)

The ground cellulose water dispersion obtained in Example 17 was placed in the same flask as

Example 17 and reacted under the same conditions as Example 17 using a reaction bath in which a polyacrylonitrile-made hollow ultrafiltration module having a molecular weight cut-off of 13000

5 (manufactured by Asahi Kasei Chemicals, trade name: Microza ACP-0013) was loaded. The reaction was conducted for 2 hours while the reaction solution was circulated in the ultrafiltration module at 0.1 MPa and a circulating flow rate of 4 L per hour. The
10 transmitted liquid obtained by ultrafiltration was measured for sugar concentration therein to quantify a cellulose residue present in the reaction solution.

From the result, the decomposition rate of cellulose was 95% by mass, and the selectivity of
15 oligosaccharide was 85%.

(Example 19)

Enzymatic decomposition was conducted using the same apparatus as Example 18 except that the cellulose concentration in the reaction solution was
20 set to 2.5% by mass. During enzymatic decomposition, the decomposition rate of cellulose was measured by the analysis of the transmitted liquid. The reaction was conducted for 24 hours while the ground cellulose water dispersion was added so that the cellulose
25 concentration in the reaction solution was constantly maintained at 2.5% by mass. The transmitted liquid was measured for sugar concentration therein in the same way as Example 18 to quantify a cellulose residue

present in the reaction solution.

From the result, the decomposition rate of cellulose was 98% by mass, and the selectivity of oligosaccharide was 92%.

5 (Example 20)

The aqueous cellooligosaccharide solution obtained in Example 19 was subjected to removal of acetic acid through an ion-exchange resin (manufactured by Mitsubishi Chemical Corporation, trade name, DIAION
10 WA30 and SK1B), then dried at 60°C for 8 hours and crushed in a mortar to obtain cellooligosaccharide powder. This powder was measured for diethyl ether-soluble matter content by the quantitative procedure for diethyl ether-soluble matter defined in Crystalline
15 Cellulose Purity Test (2) of Japanese Pharmacopoeia (the 14th revision, published by Hirokawa Publishing). The obtained diethyl ether-soluble matter content was 200 ppm.

(Comparative Example 8)

20 Commercially-available unbleached dissolving pulp (derived from Spuruce, average degree of polymerization: 1680, average particle size: 128 μm , colloidal cellulose content: 4% by mass, diethyl ether-soluble matter content: 1.5% by mass, cellulose I
25 crystals content: 85%) was crushed with a home-use mixer. To the obtained crushed cellulose as a substrate, an acetic acid buffer of pH 5.5 was added to make an aqueous dispersion with 2% by mass of

cellulose. In the above aqueous cellulose dispersion, commercially-available cellulase (manufactured by Godo Shusei, trade name: GODO-TCD) was dissolved in a concentration of 0.1% by mass based on the aqueous dispersion and allowed to conduct enzymatical decomposition at pH 5.0 for 24 hours in the same way as in Example 17. From the result, the decomposition rate of cellulose was 29% by mass, and the selectivity of oligosaccharide was 55%. This aqueous cellooligosaccharide solution was pulverized and measured for diethyl ether-soluble matter content in the same way as in Example 20. The diethyl ether-soluble matter content was 3200 ppm.

INDUSTRIAL APPLICABILITY

Cellooligosaccharide obtained by the method of the present invention can preferably be utilized not only as a raw material for usual foods but also as a raw material for functional foods, a raw material for chemical conversion such as materials for synthesizing intermediates for pharmaceuticals and the other chemicals, and a raw material for fermentation in the fields of foods, pharmaceuticals, and general industrial products.

CLAIMS

1. A process of producing cellooligosaccharide, comprising enzymatically decomposing, in the presence of cellulase, a water-insoluble natural cellulosic material having an average degree of polymerization not greater than 700, an average particle size not greater than 100 μm , and a diethyl ether-soluble substance content less than 1% by mass.
2. A process of producing cellooligosaccharide, comprising enzymatically decomposing, in the presence of cellulase, a water-insoluble natural cellulosic material having an average degree of polymerization not greater than 700, containing 10% or more by mass of a colloidal cellulose component and a diethyl ether-soluble matter content less than 1% by mass.
3. The process of producing cellooligosaccharide according to Claim 1 or 2, wherein the water-insoluble natural cellulosic material has an average particle size not greater than 100 μm and contains 10% or more by mass of a colloidal cellulose component.
4. The process of producing cellooligosaccharide according to any one of Claims 1 to 3, wherein the water-insoluble natural cellulosic material has an average degree of polymerization not greater than 500 and an average particle size not greater than 50 μm .
5. The process of producing cellooligosaccharide according to any one of Claims 1 to 4, wherein the water-insoluble natural cellulosic material has an

average degree of polymerization not greater than 400 and an average particle size not greater than 30 μm .

6. The process of producing cellooligosaccharide according to any one of Claims 1 to 5, wherein the water-insoluble natural cellulosic material contains 15% or more by weight of a colloidal cellulose component.

7. The process of producing cellooligosaccharide according to any one of Claims 1 to 6, wherein the cellulase has an activity ratio (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 55°C) not greater than 0.7.

8. The process of producing cellooligosaccharide according to Claim 7, wherein the cellulase has an activity ratio not greater than 0.5.

9. The process of producing cellooligosaccharide according to Claim 8, wherein the cellulase has an activity ratio not greater than 0.35.

10. The process of producing cellooligosaccharide according to any one of Claims 1 to 9, wherein the diethyl ether-soluble matter is lignin.

11. The process of producing cellooligosaccharide according to any one of Claims 1 to 10, wherein the water-insoluble natural cellulosic material contains a cellulose I crystal.

12. The process of producing cellulose according to any one of Claims 1 to 11, wherein the enzymatic decomposition is performed by culturing cellulase-

producing microorganism, wherein an activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity (β -glucosidase activity/crystalline cellulose-decomposing activity at a temperature of 40°C) in a culture solution obtained by culturing the cellulase-producing bacteria is not greater than 0.5.

13. The process of producing cellulase according to Claim 12, wherein the activity ratio of β -glucosidase activity to crystalline cellulose-decomposing activity is not greater than 0.35.

14. The process of producing cellulase according to Claim 12 or 13, wherein the cellulase-producing bacteria is a strain selected and thereby obtained as a strain reduced in β -glucosidase production.

15. The process of producing cellulase according to any one of Claims 12 to 14, wherein pH during culture is controlled at less than 3.5 when the cellulase-producing bacteria is cultured.

16. The process of producing cellulase according to any one of Claims 12 to 15, wherein the cellulase-producing bacteria is a strain belonging to the genus *Trichoderma*.

17. Celooligosaccharide characterised in that diethyl ether-soluble matter content is 2000 ppm or less.

18. Celooligosaccharide obtainable by the process according to any one of claims 1 to 11,

characterised in that diethyl ether-soluble matter content is 2000 ppm or less.

19. Cellooligosaccharide according to claim 18, wherein the diethyl ether-soluble matter content is 1000 ppm or less.

20. A food, cosmetic, or pharmaceutical preparation, characterised by comprising cellooligosaccharide obtainable by the process according to any one of claims 1 to 11.

21. A food, cosmetic, or pharmaceutical preparation, characterised by comprising cellooligosaccharide according to claim 17 or 18.

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FIG.1

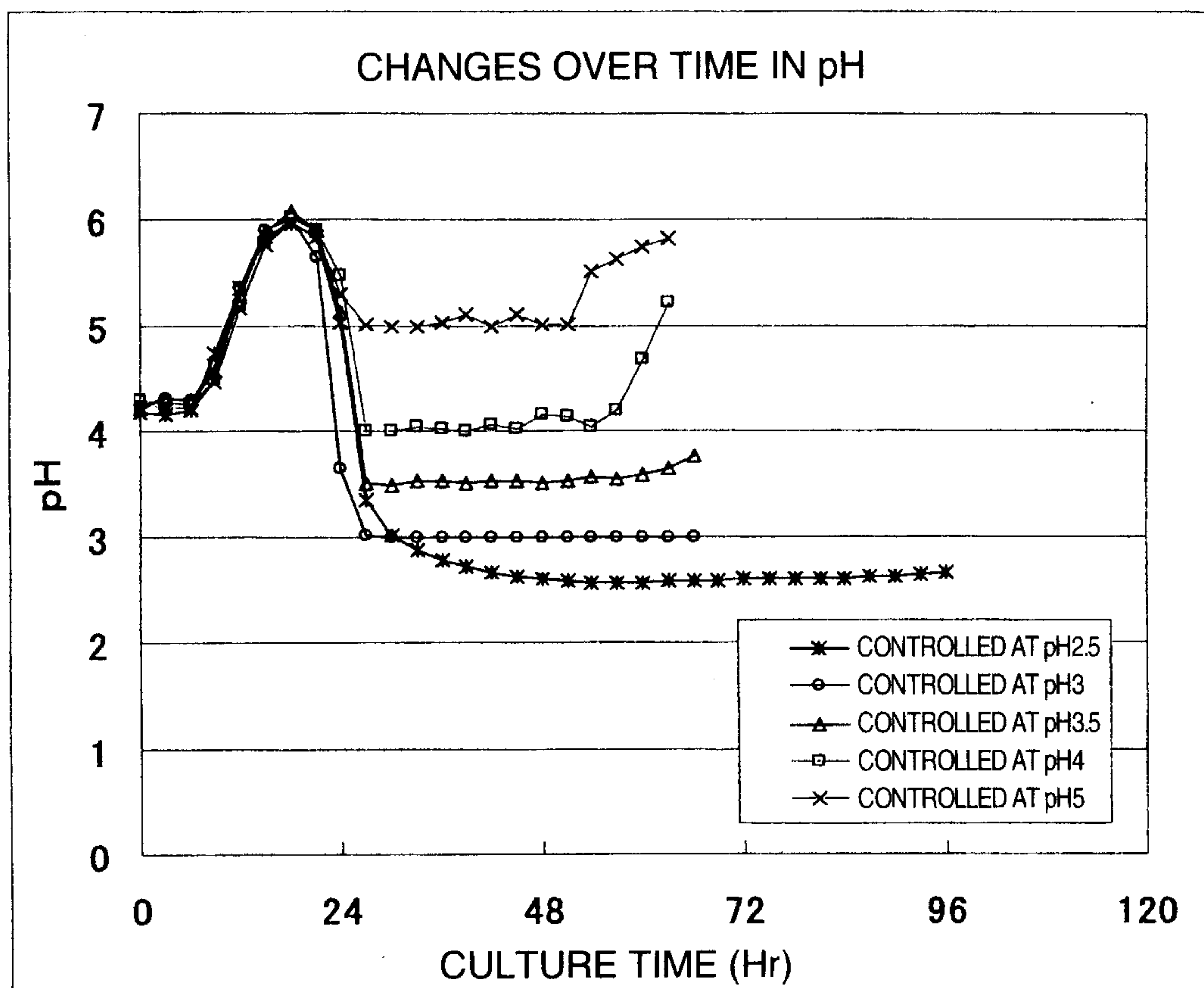
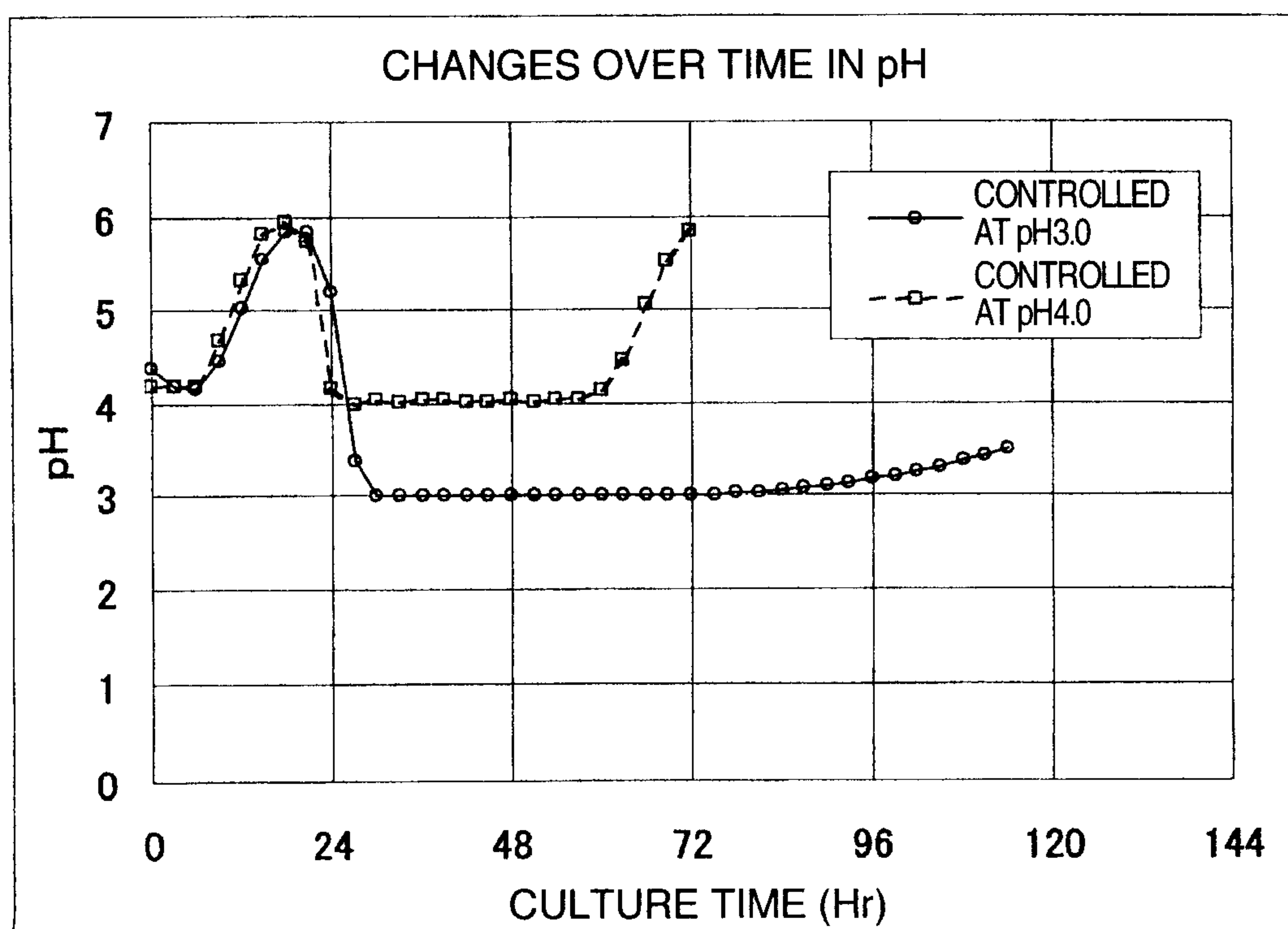
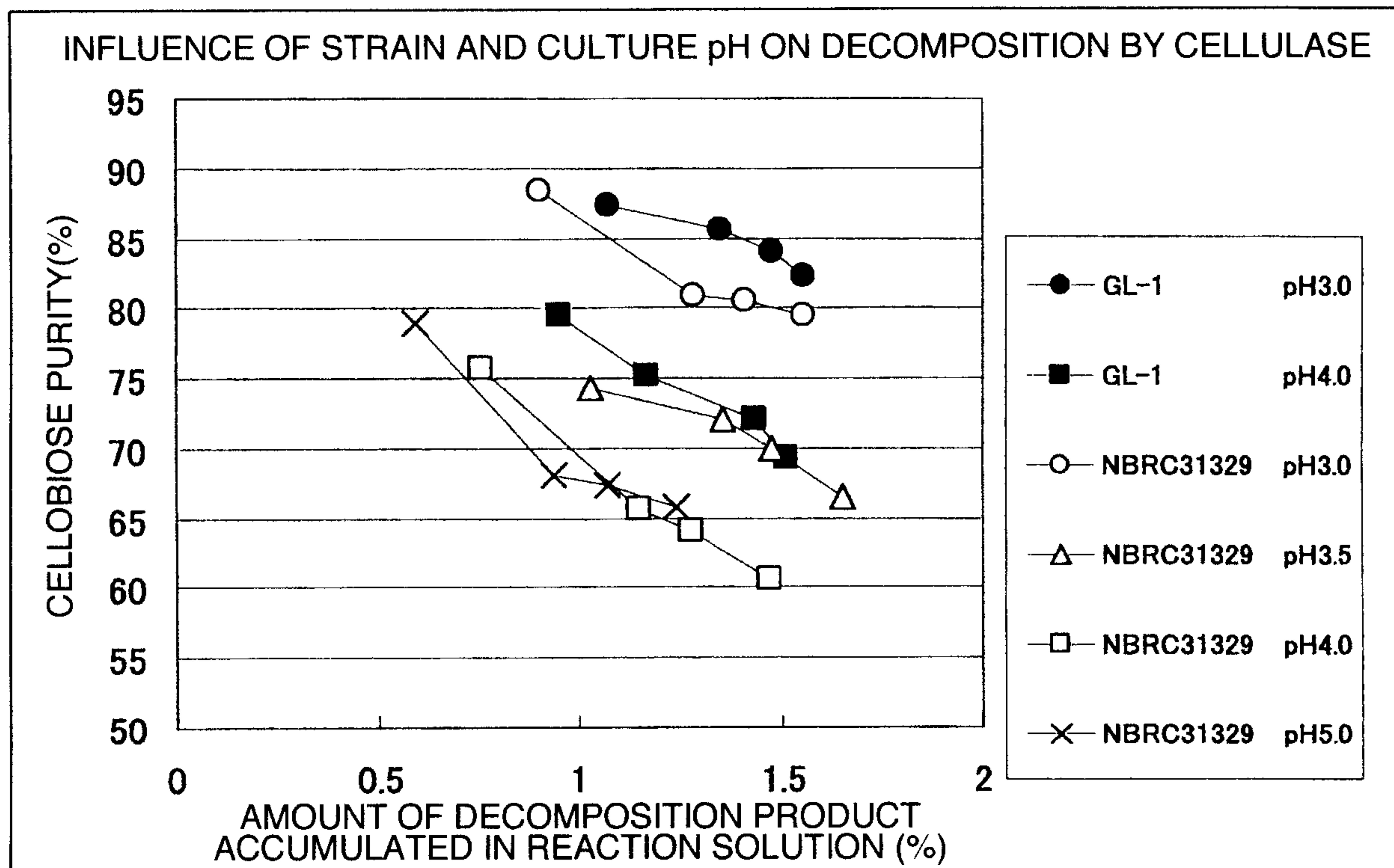


FIG.2



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FIG.3



INFLUENCE OF STRAIN AND CULTURE pH ON DECOMPOSITION BY CELLULASE

