METHOD FOR PRODUCING A CONFECTIONERY SEMI-PROCESSED PRODUCT, SUCH AS A CHOCOLATE-TYPE PRODUCT

A method of producing a semifinished confectionery product, such as chocolate or similar, using at least one centrifugal unit for continuously grinding and mixing at least some of the ingredients of said semifinished product, the method comprising the steps of grinding at least a first ingredient to a larger grain size than that of said semifinished confectionery product; mixing the ground said first ingredient with at least one second ingredient inside a processing chamber of the centrifugal unit, by rotating a centrifugal member inside said chamber to move said ingredients inside said chamber along at least one straight, horizontal, simultaneous grinding and mixing path, and to grind and mix the ingredients to form a mixture of the same grain size as said semifinished confectionery product; and taking said mixture out of said chamber through an outlet of said processing chamber.
METHOD FOR PRODUCING A CONFECTIONERY SEMI-PROCESSED PRODUCT, SUCH AS A
CHOCOLATE-TYPE PRODUCT

TECHNICAL FIELD

The present invention relates to a method of producing a semifinished confectionary product, such as chocolate or similar.

More specifically, the present invention may be used to advantage for producing semifinished products containing no or only a small percentage (less than 5%) of cocoa paste, and in which the cocoa flavour is achieved using cocoa powder.

BACKGROUND ART

In practice, semifinished products containing substantially no cocoa paste do not need particularly thorough conging, unlike other mixtures in which conging is normally essential to reduce the viscosity of the mixture, and especially to eliminate some of the volatile components of the cocoa paste and initiate chemical reactions to enhance the flavour of the semifinished product.

The conventional method currently used is discontinuous, and comprises loading the basic ingredients inside mixers consisting of tanks fitted inside with agitators. After a first mixing stage, the entire mixture is transferred to known cylinder-type pre-refining machines, and then to known, conveniently also cylinder-type, refining machines, which gradually
reduce the mixture to the desired grain size, normally of less than 30 microns. The ground mixture is then transferred to conging machines known as conges, and, when the mixture in the conges reaches a given consistency, the other ingredients are added to make up the dosage, and the mixture is pumped into storage facilities, pending further processing. An example of such a system employing conging tanks is described, for example, in US Patent Application US 2007/0202241.

Though used for decades, the above method has various drawbacks. In particular, the refining process is discontinuous and slow, and involves bulky, high-cost machinery.

The conges normally used to process the semifinished product are also bulky and expensive, and the processing cycles are normally lengthy, to achieve a fluid enough product for further processing.

Conventional methods also pose problems when making production changeovers, which is a painstaking job, especially to clean the machinery.

**DISCLOSURE OF INVENTION**

It is an object of the present invention to provide a method of producing a semifinished confectionary product, such as chocolate or similar, designed to provide a simple, low-cost solution to the above drawbacks, and which in particular produces semifinished confectionary products with the same characteristics as known products, but much faster and with no need for
conging units or devices.

According to the present invention, there is provided a method of producing a semifinished confectionary product, such as chocolate or similar, using at least one centrifugal unit for continuously grinding and mixing at least some of the ingredients of said semifinished product, the method comprising the steps of grinding at least a first ingredient to a larger grain size than that of said semifinished confectionary product; mixing the ground said first ingredient with at least one second ingredient inside a processing chamber of the centrifugal unit, by rotating a centrifugal member inside said chamber to move said ingredients inside said chamber along at least one straight, horizontal, simultaneous grinding and mixing path, and to grind and mix the ingredients to form a mixture of the same grain size as said semifinished confectionary product; and taking said mixture out of said chamber through an outlet of said processing chamber.

_BRIEF DESCRIPTION OF THE DRAWINGS_

A non-limiting embodiment of the present invention will be described by way of example with reference to the accompanying drawings, in which:

Figure 1 shows a schematic, substantially block diagram of a preferred embodiment of a system for producing a semifinished confectionary product in accordance with the teachings of the present invention;
Figure 2 shows a larger-scale section along line II-II in Figure 1.

BEST MODE FOR CARRYING OUT THE INVENTION

Number 1 in Figure 1 indicates as a whole a system for producing a semifinished confectionary product such as chocolate or similar and comprising, for example, sugar, powdered milk, vegetable fat, and cocoa powder, to which the following description refers, both in terms of ingredients and production conditions, purely by way of example.

System 1 comprises a first and second centrifugal grinding and mixing unit 2, 3 separate from each other; and a centrifugal mixing unit 4 separate from units 2 and 3. Units 2, 3, 4 are cascaded or arranged in series to continuously supply a semifinished confectionary product of a given grain size, and which conveniently contains at most 10% of over 30-micron size grains, and has a viscosity of roughly 4000 pascals/second.

Each unit; 2, 3, 4 comprises a substantially horizontal outer casing 5, in turn comprising a tubular, preferably cylindrical, shell 6 extending coaxially with a respective axis 7 and closed at opposite ends by two end walls 9, 10. Tubular shell 6 and end walls 9, 10 together define an elongated processing chamber 12, which communicates with the outside through an in inlet A (shown schematically) for loading the ingredients for processing, and an outlet B (shown schematically) for unloading the processed ingredients.
A shaft 15, rotated by a motor reducer 16, extends, coaxially with axis 7, through end wall 10, and is fitted integrally with one or more coiled rows of radial appendixes 18. Each radial appendix 18 has a stem connected releasably to shaft 15, and is of such a length L (Figure 2) that its free-end surface 18a is separated by a distance D of 0.2 to 4 millimetres, and conveniently of 2 millimetres, from the inner surface 6a of shell 6 (Figure 2).

Casing 5 also comprises an annular portion 20, which encloses shell 6 and defines with it an annular chamber 21 communicating externally through an inlet and an outlet for a temperature-controlled fluid for conditioning shell 6.

As shown in Figure 1, system 1 also comprises a known metering device 27 mounted on load cells 27a to feed inlet A of unit 2 with precise measures or a continuous supply of granulated sugar with a conveniently 2000-3000 micron grain size.

As shown in Figure 1, outlet B of unit 2 communicates with a storage container 28, in turn connected to a known metering device 29 mounted on load cells 29a to feed inlet A of unit 3 with precise measures or a continuous supply of ground sugar containing at most 10% of 30-70-micron size grains. As shown in Figure 1, system 1 also comprises another four metering devices 31, 32, 33, 34 mounted on respective load cells 31a, 32a, 33a, 34a to respectively feed inlet
A of unit 3 with precise measures or continuous supplies of powdered milk of 50-100 micron grain size, vegetable oils, cocoa powder of 100-200 micron grain size, and technological additives such as soybean lecithin.

Unit 4, which, unlike units 2 and 3, is simply a mixing unit, is supplied by unit 3 with a mixture of the same grain size as the semifinished product, and is connected to a further metering device 36 mounted on load cells 36a to feed inlet A of unit 4 with fluidifying vegetable fat. As shown in Figure 1, processing chamber 12 of unit 4 is connected to a vacuum unit 37 for maintaining -0.1 to -0.5 bar negative pressure in chamber 12.

The semifinished confectionary product is produced as follows. Metering device 27 feeds granulated sugar into unit 2 through respective inlet A, and respective shaft 15 is then rotated at a speed ranging between 200 and 10,000 rpm, and conveniently of 5000 rpm, for a time ranging between 0.5 and 5 minutes, and conveniently for 4 minutes. As the shaft rotates, the centrifugal force produced by appendixes 18, and the small distance D between the ends of appendixes 18 and the inner surface 6a of shell 6, grind the sugar to a grain size containing at most 10% of 30- to 70-micron size grains. As the sugar is ground, the centrifugal force also spins it onto inner surface 6a of shell 6, where it forms a layer of a thickness S (Figure 2) ranging between 0.2 and 4 millimetres. During the grinding process, shell 6
is maintained at a temperature of -80 to +15°C by feeding a conditioning fluid, e.g. liquid nitrogen, through respective chamber 21.

The ground sugar is fed to storage container 28, and from there to metering device 29, which feeds it to inlet A of unit 3. Metering devices 31-34 also supply inlet A of unit 3, either simultaneously or successively, with given amounts of powdered sugar, vegetable oils, cocoa powder, and technological additives, following which, shaft 15 of unit 3 is rotated at a speed of 500 to 2000 rpm for 0.5 to 5 minutes, and at any rate long enough to obtain a homogeneous mixture of the same grain size as the semifinished product. As the mixture is ground, the corresponding processing chamber is maintained at a temperature of +10 to +50 °C by feeding conditioning fluid through respective chamber 21.

The mixture is then transferred to and mixed further in unit 4, to which metering device 36 adds a given amount of vegetable fat. Shaft 15 of unit 4 is rotated at a speed of 500 to 2000 rpm for 0.5 to 5, and preferably for 4 minutes, and at any rate long enough to obtain a perfectly homogenous mixture of substantially the same viscosity as the semifinished product. After the vegetable fat is added, the processing chamber of unit 4 is maintained at a temperature of 40 to 60 °C, by feeding conditioning fluid through respective chamber 21, and at a pressure
of -0.1 to -0.5 bar.

Once mixing is completed, the semifinished product in unit 4 is transferred to a storage container.

As will be clear from the above description, the semifinished product described is prepared using the 'continuous grinding' method, i.e. grinding some of the ingredients, in this case sugar, before mixing it with the other ingredients, and then grinding it again together with, the other ingredients to obtain a perfectly homogenous mixture, already with the same grain size as the semifinished product to be prepared.

The described preparation method provides above all for producing semifinished confectionary products with no need for conventional conging, grinding, and mixing devices, which complicate the system and increase system cost and production time. At the same time, the described method provides for producing perfectly homogeneous semifinished confectionary products of given constant grain size from course ingredients, in particular sugar, that are therefore readily available and easy to manage. In fact, the material being processed is spun onto, and forms a thin layer on, the lateral walls of the processing chamber; and the difference in speed between the layer of material on the rotating radial appendixes of the relative shaft and the layer of material on the inner wall of the processing chamber produces relative movement, and therefore thorough mixing and grinding, of the material.
Semifinished confectionary products can thus be produced fast using a system which, being 'modular', is extremely simple in design, easy to control, and, above all, compact. Units 2, 3 and 4, in fact, all form part of the same class, and range between 150 and 500 mm in diameter, and 200 and 2000 mm in length.

The significant reduction, as compared with conventional methods, of the number of parts coming into contact with the product drastically reduces washing operations between batches and simplifies the washing when making production changeovers. Thanks to this feature, the same system, as opposed to dedicated lines, can be used for producing different semifinished products.

Clearly, changes may be made to system 1 and the method described without, however, departing from the protective scope as defined in the accompanying Claims. As regards the method, the ingredients may obviously differ from those referred to by way of example.

As for the system, this may, obviously, even comprise only one centrifugal unit, similar or identical to one of units 2-4, which first grinds one of the ingredients, e.g. the granulated sugar, and is then loaded with the other ingredients, either all together or one at a time, grinding the mixture further each time. Once mixing is completed, the vegetable oil is added, again in the same centrifugal unit. This is a highly compact, low-cost solution which, compared with
the one described above, provides for further reducing production changeover cleaning time.
1) A method of producing a semifinished confectionary product, such as chocolate or similar, using at least one centrifugal unit for continuously grinding and mixing at least some of the ingredients of said semifinished product, the method comprising the steps of grinding at least a first ingredient to a larger grain size than that of said semifinished confectionary product; mixing the ground said first ingredient with at least one second ingredient inside a processing chamber of the centrifugal unit, by rotating a centrifugal member inside said chamber to move said ingredients inside said chamber along at least one straight, horizontal, simultaneous grinding and mixing path, and to grind and mix the ingredients to form a mixture of the same grain size as said semifinished confectionary product; and taking said mixture out of said chamber through an outlet of said processing chamber.

2) A method as claimed in Claim 1, characterized in that grinding said first ingredient comprises the steps of loading said first ingredient into said processing chamber; and of grinding the first ingredient inside said chamber before adding said second ingredient.

3) A method as claimed in Claim 1, characterized in that said first ingredient is ground outside said processing chamber.
4) A method as claimed in Claim 3, characterized in that said first ingredient is ground by moving said first ingredient along a straight, horizontal path inside a further processing chamber of a further centrifugal unit identical to said centrifugal unit for grinding and mixing.

5) A method as claimed in Claim 4, characterized by feeding the ground first ingredient exiting from said further centrifugal unit to a storage device before moving it towards said centrifugal unit for grinding and mixing.

6) A method as claimed in Claim 1, characterized by adding at least a third ingredient to said mixture; mixing said third ingredient to said mixture to form a further mixture; and bringing said further mixture to a given temperature and viscosity to obtain said semifinished product.

7) A method as claimed in Claim 6, characterized in that said third ingredient is added by moving said mixture into a processing chamber of a final centrifugal unit identical to said centrifugal unit for grinding and mixing.

8) A method as claimed in any one of the foregoing Claims, characterized in that said first ingredient is ground inside a processing chamber maintained at a temperature between -80 °C and +15 °C.

9) A method as claimed in any one of the foregoing Claims, characterized in that, when grinding said
mixture, said processing chamber is maintained at a
temperature between +10 °C and +50 °C.

10) A method as claimed in any one of the foregoing
Claims, characterized in that, after adding said third
ingredient, said processing chamber is maintained at a
temperature between 40 °C and 60 °C.

11) A method as claimed in any one of the foregoing
Claims, characterized in that, during said grinding
steps, said centrifugal member is rotated at a speed of
200 to 10,000 rpm for 0.5 to 5 minutes.

12) A method as claimed in Claim 7, characterized
in that, after adding said third ingredient, said
processing chamber is maintained at a negative pressure.

13) A method as claimed in Claim 6, characterized
in that, after adding said third ingredient, the
pressure of said processing chamber is reduced to -0.1
to -0.5 bar.
INTERNATIONAL SEARCH REPORT

International application No
PCT/IB2011/000681

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
A23G

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic database consulted during the international search (name of database and, where practical, search terms used)
EPO-Internal, WPI Data, FSTA

C. DOCUMENTS CONSIDERED TO BE RELEVANT

<table>
<thead>
<tr>
<th>Category</th>
<th>Citation of document, with indication, where appropriate, of the relevant passages</th>
<th>Relevant to claim No.</th>
</tr>
</thead>
<tbody>
<tr>
<td>X</td>
<td>US 4 861 615 A (W EDMANN WERNER [DE]) 29 August 1989 (1989-08-29) claims 1-15; figure 1; example 4 col umn 4, line 61 - line 63</td>
<td>1-13</td>
</tr>
</tbody>
</table>

Further documents are listed in the continuation of Box C. See patent family annex.

* Special categories of cited documents:
  "A" document defining the general state of the art which is not considered to be of particular relevance
  "E" earlier document but published on or after the international filing date
  "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another document or to provide a context other than that of an inventive step
  "O" document referring to an oral disclosure, use, exhibition or other means
  "P" document published prior to the international filing date but later than the priority date claimed

T later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
X document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
Y document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
A document member of the same patent family

Date of the actual completion of the international search
5 July 2011

Date of mailing of the international search report
15/07/2011

Name and mailing address of the ISA/
European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016

Authorized officer

Goh, Bjorn
<table>
<thead>
<tr>
<th>Category</th>
<th>Citation of document, with indication, where appropriate, of the relevant passages</th>
<th>Relevant to claim No.</th>
</tr>
</thead>
<tbody>
<tr>
<td>X</td>
<td>DE 33 331 445 A1 (MISSAI LIDIS M SPI ROS) 24 May 1984 (1984-05-24) page 7, line 20 - line 26; claims 1, 6, 7, 17</td>
<td>12, 13</td>
</tr>
<tr>
<td>X</td>
<td>SIMON E J: &quot;ZERKLEINERUNG BEI DER SCHOKOLADEN-HERSTELLUNG - GETRENNTE ODER GEMEINSAME VERMAHLUNG?&quot;, REVUE INTERNATIONALE DE LA CHOCOLATERIE, ZUERICH, CH vol. 24, no. 1, April 1, 1969 (1969-04-01), pages 140-155, XP001113163, ISSN: 0035-3345</td>
<td>1-3</td>
</tr>
<tr>
<td>A</td>
<td>page 140 - page 150; figure 1</td>
<td>4-10</td>
</tr>
<tr>
<td>X</td>
<td>EP 0 518 025 A2 (FRISSE RICHARD MASCHF [DE]) 16 December 1992 (1992-12-16) claims 1-3, 7-9; figure 1</td>
<td>1-13</td>
</tr>
<tr>
<td>Patent document cited in search report</td>
<td>Publication date</td>
<td>Patent family member(s)</td>
</tr>
<tr>
<td>----------------------------------------</td>
<td>-----------------</td>
<td>-------------------------</td>
</tr>
<tr>
<td>US 2007202241</td>
<td>30-08-2007</td>
<td>BR P10400056 A</td>
</tr>
<tr>
<td></td>
<td></td>
<td>Wo 2005077197 Al</td>
</tr>
<tr>
<td></td>
<td></td>
<td>CA 2556615 Al</td>
</tr>
<tr>
<td></td>
<td></td>
<td>CN 1929746 A</td>
</tr>
<tr>
<td></td>
<td></td>
<td>EP 1725119 Al</td>
</tr>
<tr>
<td></td>
<td></td>
<td>JP 2007521822 A</td>
</tr>
<tr>
<td></td>
<td></td>
<td>RU 2342845 C2</td>
</tr>
<tr>
<td>US 4861615</td>
<td>29-08-1989</td>
<td>DE 3629526 Al</td>
</tr>
<tr>
<td></td>
<td></td>
<td>DE 3772502 Di</td>
</tr>
<tr>
<td></td>
<td></td>
<td>EP 0262300 A2</td>
</tr>
<tr>
<td></td>
<td></td>
<td>JP 63063344 A</td>
</tr>
<tr>
<td></td>
<td></td>
<td>CH 682788 A5</td>
</tr>
<tr>
<td></td>
<td></td>
<td>DE 59309228 Di</td>
</tr>
<tr>
<td></td>
<td></td>
<td>ES 2125923 T3</td>
</tr>
<tr>
<td></td>
<td></td>
<td>JP 6014718 A</td>
</tr>
<tr>
<td></td>
<td></td>
<td>US 5419635 A</td>
</tr>
<tr>
<td>DE 3331445</td>
<td>24-05-1984</td>
<td>GR 70627 Al</td>
</tr>
<tr>
<td></td>
<td></td>
<td>DE 59209343 Di</td>
</tr>
</tbody>
</table>