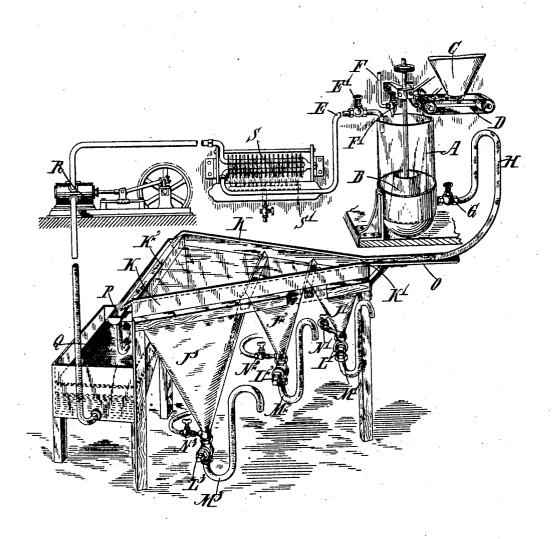
No. 835,143.

H. L. SULMAN.
ORE CONCENTRATION.
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## UNITED STATES PATENT OFFICE.

HENRY LIVINGSTONE SULMAN, OF LONDON, ENGLAND.

## ORE CONCENTRATION.

No. 835,143.

Specification of Letters Patent.

Patented Nov. 6, 1906.

Application filed October 20, 1905. Serial No. 283,704.

To all whom it may concern:

Be it known that I, HENRY LIVINGSTONE SULMAN, a subject of the King of England, residing at London, England, have invent-5 ed certain new and useful Improvements in Ore Concentration, of which the following is a specification.

This invention relates to improvements in the concentration of ores, the object being to 10 separate metalliferous matter, graphite, and the like from gangue by means of oils, fatty acids, or other substances which have a preferential affinity for metalliferous matter over

gangue.

In the process described in the specification of the previous patent application, Serial No. 262,889, filed May 29, 1905, a mineral pulp is agitated with a small proportion of an oily substance, such as oleic acid or pe-20 trol or other oil, amounting to a fraction of one per cent, on the ore until the oil-coated metalliferous matter forms into a froth which can be separated from the gangue by flotation, the pulp being acidified. It is also 25 stated that the pulp may be warmed, say, to 30° to 40° centigrade to increase the tendency for the oily substance to disseminate through the pulp and the rapidity with which the metalliferous matter becomes coated.

It is now found that if the finely-powdered ore suspended in water is mixed with a small proportion of an oily substance—say five per cent. or less of the ore—agitated and heated to a high temperature—say, to boiling-pointthat is to say, to a temperature at which bubbles of steam or vapor are generated in the pulp—the formation of a froth containing the oil-coated metalliferous matter is considerably promoted, and a very efficient separa-40 tion of the metalliferous matter from the

gangue may thus be obtained.

The water in which the oiling is effected may be slightly acidified by adding, say, a fraction of one per cent. of sulfuric acid or 45 other mineral acid or acid salt, or the water may be neutral or alkaline. It is to be understood that the object of using acid in the pulp according to this invention is not to bring about the generation of gas for the pur-5c pose of flotation thereby, and the proportion of acid used is insufficient to cause chemical action on the metalliferous minerals present.

The quantity of oil employed is not sufficient to cause the flotation of the metallifer-55 ous matter by the buoyancy of the oil; but the quantity may be sufficient—say five per

cent. or less on the quantity of ore—to coat the metalliferous particles with a thin film of oil.

The following is an example of the applica- 60 tion of this invention to the concentration of ore: Broken Hill or certain copper ores are finely powdered and mixed with water, acidified or not. To this is added a proportion, as above described, of an oily substance, such as 65 oleic acid, and the mixture is agitated in a cone mixer or the like in order to effect due oiling of the mineral particles. may now be removed from the agitation (oiling) vessel and subjected to heat in suitable 70 As the liquor becomes heated, apparatus. and especially as the boiling-point of the liquor is approached, a froth or scum rises to the surface containing practically the whole of the metalliferous matter, while the gangue 75 remains in the pulp. The froth may be removed from the liquid by skimming or in any usual way, or the frothy portion may be separated from the remainder of the pulp by causing this to flow through a spitzkasten or 80 the like. The froth after separation and collection may be allowed to subside, and the oily substance may be removed from the metalliferous matter by treatment with an alkali or a solvent or otherwise.

The heating of the pulp may be effected by means of closed steam-coils, or of free steamjets, or surrounding the agitating vessels with steam-jackets, or by any other suitable means, or the treatment of the pulp by heat 90 may be made continuous by causing it to flow over heated surfaces in a continuous stream and collecting the suitably-heated product in an apparatus wherein the separation of the froth so produced from the mineral-depleted 95 ore-pulp can be effected; or the contents of the agitation (oiling) vessel may be heated to the necessary extent, which approaches the boiling temperature, and on cessation of agitation the mineralized froth rises to the sur- 100

Should any coarser particles of oiled mineral (unremoved as "froth") remain in the coarse sands of the separated pulp, these particles may be recovered by passage over a concentration or aeration apparatus or the

It is to be understood that the details of the process may be varied without departing from this invention.

The accompanying drawing is a perpective view of one form of apparatus suitable for

carrying this invention into practice, the arrangement being such that the contents of the agitation vessel may be heated to the

necessary extent.

A mixing vessel A (of which there may be any number in series) is provided with a rotatable stirrer B. Crushed ore is fed from a hopper C into the vessel by a band D. A pipe E, controlled by a tap E', delivers cir-10 cuit-water to the vessel, and oleic acid or other oil is introduced through the pipe F and tap F'. The outer cock G from the vessel A communicates, through a swan-neck pipe H, with the froth-separating apparatus.

In passing from the frothing apparatus A to the spitzkasten (say between O and K) the pulp may, if desired, be run in a thin layer over a smooth slightly-inclined plane.

The froth-separating apparatus comprises 20 several (say three) pointed boxes J' J2 J3, which open at the top into a horizontal channel consisting of side walls K. The channel has a narrow inlet K' and spreads out to a wide outlet K<sup>2</sup>. The pointed boxes J' J<sup>2</sup> J<sup>3</sup> 25 have full-way cocks L' L<sup>2</sup> L<sup>3</sup> at the bottom leading to swan-neck discharge-pipes M' M<sup>2</sup> An upcurrent of water may be led in at the bottom of each box through a tap

The boxes are all filled with circuit-water. The pulp from the vessel A is distributed horizontally from the flat trough O through the inlet K'. The heavy sands and coarser particles of mineral sink into the first box J', 35 from which they are led to a shaking-table, convex buddle, or the like, to be treated as above described. The middlings or medium sands fall into the box J<sup>2</sup>, and if they contain any mineral may be removed for further treatment by agitation. The upcurrent of water from the taps N' N2 prevents the deposition of any slime in these boxes. fine sands or gangue slimes settle in the last box J<sup>3</sup>, from which they are discharged to 45 waste or further treatment.

The slime mineral in the form of froth or scum floats from the liquid and is carried by the stream over the outlet K2 into a launder P and thence to a filter Q, where the metal-50 liferous matter is removed from the circuitwater, which is returned to the vessel A by a pump R. The circuit-water may be brought to the proper temperature approximately to boiling-point by passing it through a heater 55 S, having a burner S', before admitting the

water to the vessel A.

What I claim as my invention, and desire

to secure by Letters Patent, is-

1. The herein-described process of concen-60 trating ores which consists in mixing the powdered ore with water, adding a small proportion of an oily liquid having a preferential

affinity for metalliferous matter, agitating the mixture, heating the mixture approximately to boiling-point until the oil-coated 65 mineral matter forms into a froth and separating the froth from the remainder by flota-

2. The herein-described process for concentrating ores which consists in mixing the 70 powdered ore with water, adding a small proportion of oily liquid having a preferential affinity for metalliferous matter, agitating the mixture, heating the mixture until gaseous bubbles are generated therein so that the 75 oil-coated mineral matter forms into a froth and separating the froth from the remainder

by flotation.

3. The herein-described process of concentrating ores which consists in mixing the 30 powdered ore with slightly-acidified water, adding a small proportion of oily matter having a preferential affinity for metalliferous matter, agitating the mixture, heating the mixture approximately to boiling-point until &5 the oil-coated mineral matter forms into a froth and separating the froth from the re-

mainder by flotation.

4. The herein-described process of concentrating ores which consists in finely powder- 90 ing the ore, mixing it with slightly-acidified water, adding a small proportion of an oily substance having a preferential affinity for metalliferous matter in quantity insufficient to cause the flotation of the metalliferous 95 matter by the buoyancy of the oil, agitating the mixture, heating the mixture to boilingpoint until the oil-coated mineral matter forms into a froth, separating the froth from the remainder by flotation and removing the 100 oil coating from the mineral by a solvent.

5. The herein-described process of concentrating ores which consists in finely powdering the ore, mixing it with water containing less than one per cent. of sulfuric acid, adding 105 a proportion of less than ten per cent. of oleic acid, agitating the mixture until the oleic acid has come into sufficient contact with the mineral, heating the mixture up to boiling-point until the metalliferous matter has been 110 raised in a froth to the surface, running the mixture over a current of water so that the froth is floated away by the current while the remaining mineral sinks, separating the froth and removing the oleic acid therefrom 115 by a solvent.

In testimony whereof I have signed my name to this specification in the presence of

two subscribing witnesses.

## HENRY LIVINGSTONE SULMAN.

Witnesses:

R. WILLIAMS, T. B. Buss.