

(19) **DANMARK**

(10) **DK/EP 3156372 T3**



(12) **Oversættelse af
europæisk patentskrift**

Patent- og
Varemærkestyrelsen

-
- (51) Int.Cl.: **C 02 F 1/52 (2006.01)** **C 02 F 11/121 (2019.01)** **C 05 B 7/00 (2006.01)**
C 05 F 17/00 (2020.01) **C 05 F 17/10 (2020.01)** **C 05 F 17/20 (2020.01)**
C 05 F 17/40 (2020.01) **C 05 F 17/90 (2020.01)** **C 02 F 1/12 (2006.01)**
C 02 F 1/66 (2006.01) **C 02 F 9/00 (2006.01)** **C 02 F 11/04 (2006.01)**
C 02 F 11/12 (2019.01) **C 02 F 101/10 (2006.01)** **C 02 F 101/32 (2006.01)**
C 02 F 101/34 (2006.01)
- (45) Oversættelsen bekendtgjort den: **2021-04-06**
- (80) Dato for Den Europæiske Patentmyndigheds bekendtgørelse om meddelelse af patentet: **2021-01-06**
- (86) Europæisk ansøgning nr.: **16182448.7**
- (86) Europæisk indleveringsdag: **2009-02-02**
- (87) Den europæiske ansøgnings publiceringsdag: **2017-04-19**
- (30) Prioritet: **2008-02-01 US 12362**
- (62) Stamansøgningsnr: **09706488.5**
- (84) Designerede stater: **AT BE BG CH CY CZ DE DK EE ES FI FR GB GR HR HU IE IS IT LI LT LU LV MC MK MT NL NO PL PT RO SE SI SK TR**
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- (54) Benævnelse: **AFFALDSAKTIVERET FREMGANGSMÅDE TIL STRIPNING AF PHOSPHOR OG MAGNESIUM FRA SLAM**
- (56) Fremdragne publikationer:
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Fortsættes ...

DESCRIPTION

FIELD OF THE INVENTION

[0001] The invention relates generally to the field of "waste-activated sludge" (WAS) stripping. More particularly, the invention relates to inducing the release of phosphorous and magnesium from a mixture of microorganisms and waste solids to reduce downstream struvite build-up in a digester and to produce a usable struvite product therefrom.

BACKGROUND OF THE INVENTION

[0002] As part of secondary sewage treatment, primary treated sewage is treated with air or pure oxygen. In what is termed the "activated sludge" process, microorganisms utilize the oxygen to metabolize the incoming waste sewage, forming a mixture of microorganisms and sewage known as "mixed liquor." This mixture is moved to settling tanks for concentration, thereby forming concentrated activated sludge. A majority of this sludge is returned to the activated sludge process tankage. A separate portion of this sludge, termed waste-activated sludge (WAS), is removed from the activated sludge process and sent to a sludge handling system for further treatment and disposal. In a stable system, the daily WAS is equal to the daily conversion of sewage into microorganisms so no net increase in mixed liquor biomass occurs. By manipulating the activated sludge process, phosphorus and magnesium are removed from the liquid stream and concentrated in the mixed liquor. The process is known as Enhanced Biological Phosphorus Removal (EBPR).

[0003] Referring to Figure 1, in one typical scheme 10, the WAS is sent to a centrifuge (or other thickening apparatus) 14 for thickening, the liquids are tapped off and returned to the wastewater plant for treatment, whereas the resultant thickened sludge is sent to an anaerobic digester 16 with other sludges, where it remains for 15 days or more before being sent to a second centrifuge (or other dewatering apparatus) 18 for dewatering.

[0004] Unfortunately, struvite tends to form in digester 16, and other equipment downstream because of the ammonia, magnesium and phosphorus that are present can precipitate as struvite. This struvite is impractical to harvest and also has the deleterious effect of being deposited on surfaces in the reactor 16 and plugging pipes and equipment leading from the reactor.

[0005] A further centrifuge (or other dewatering apparatus) 18 produces further dewatered sludge 20, which is either beneficially reused or disposed of, and liquids 22, which are rich in ammonia and phosphorus. It has been learned that prilled struvite can be harvested from liquids 22, by a struvite reactor 24. This prilled struvite is a marketable product that can be used as a timed release fertilizer, thereby defraying some of the costs of sewage treatment.

Unfortunately, the struvite harvest requires the addition of magnesium into the process, which forms a large part of the costs of the process and reduces the profitability.

[0006] In A Feasible Approach of Integrating Phosphate Recovery as Struvite at Waste Water Treatment Plants, Proceedings, Institute Of Environmental Engineering, pp. 551-558 (2007), D. Montag, et al. describe a phosphate recovery system that effectively teaches away from the addition of one or more volatile fatty acids (VFAs) for phosphorous removal. They do so by teaching long retention times instead of the addition of external organic or inorganic acids. In The Modified Renphosystem: A High Biological Nutrient Removal System, Wat. Sci. Tech., Vol. 35, No. 10, pp. 137-146 (1997), J. H. Rensink, et al. describe a so-called modified Renpho system. They fail to teach the addition of VFAs as dosing agents to WAS, fail to teach magnesium as well as phosphate release/removal, fail to teach fermentation, fail to teach pH adjustment prior to mixing w/centrate, and fail to teach the use of a dewaterer in connection with a digester. In Struvite precipitation in the sludge stream at slough wastewater treatment plant and opportunities for phosphorus recovery, Environ. Techn., 1999, Vol. 20, No. 7, pp. 743-747, S. Williams, et al. analyse the composition of a number of process streams for potential phosphorous recovery at a UK WWTW employing EBNR and suggest to combine the centrate (which is high in ammonia) and the waste activated sludge liquor (which releases phosphorous on storage).

In An economic and environmental evaluation of the opportunities for substituting phosphorous recovered from wastewater treatment works in existing UKfertiliser markets, Environ, Tech., Vol. 21, No. 9., pp. 1067-1084 (2000), M. R. Gaterell, et al. describe a simplified potential process for maximising struvite precipitation (adapted from Williams et al. cited above).

[0007] Neither of these articles nor any other known prior art publication teaches separation of a VFA-enabled reagent into a phosphorus-rich and magnesium-rich liquid stream to a struvite reactor for pelletized struvite production nor into a phosphorus-poor and magnesium-poor sludge stream to a digester to reduce nuisance struvite build-up therein.

SUMMARY

[0008] The present invention may take the form of a method of treating a first mixture of waste solids and microorganisms containing phosphorus and magnesium, by first inducing the mixture microorganisms to release phosphorus and magnesium which is then tapped off as the mixture is thickened, to produce phosphorus and magnesium-rich liquid and phosphorus and magnesium-reduced treated mixture. This treated mixture is placed in an anaerobic digester where ammonia is formed but combines very little with phosphorus or magnesium as these elements have been greatly reduced in concentration. Next the high-ammonia mixture is dewatered, to produce an ammonia-rich liquid, which is combined with the phosphorus and magnesium-rich liquid and struvite is formed. In one preferred embodiment a useable struvite product is harvested from this combination. The invention is defined by the claims and any other aspects or examples set forth herein not falling within the scope of the claims are for information only.

[0009] Additionally, the production of nuisance struvite in the anaerobic digester is greatly reduced, in comparison with prior art waste treatment methods.

[0010] Systems and methods are shown in Figures 2, 3, and 2A and are described in the accompanying text, which should help to clarify the invention in its various examples.

BRIEF DESCRIPTION OF THE DRAWINGS

[0011]

Figure 1 is a block diagram of a prior art waste treatment system.

Figure 2 is a block diagram of a waste treatment system.

Figure 3 is a block diagram of an alternative waste treatment system.

Figure 2A is a block diagram of yet another waste treatment system.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

[0012] Referring to Figure 2, in a preferred embodiment of a waste activated sludge (WAS) treatment method 110, phosphorus and magnesium are released by microorganism action in an anaerobic reactor 112, where the WAS is held, for a minimum time of 0.5 hours. One method for effecting this release is by adding one or more readily biodegradable carbon compounds (RBCs), such as one or more volatile fatty acids (VFAs) to the sludge in the anaerobic reactor, with 3 to 8 grams (and preferably 4-6 grams) of the one or more VFAs added per gram of planned phosphorus release. In another technique, the activated sludge is held for 36 to 96 hours, without the addition of VFAs, for endogenous respiration and fermentation to release phosphorus and magnesium.

[0013] The resultant WAS is sent to a thickening device 114, such as a centrifuge, thickening belt or rotating screens and the resultant liquids 115, having enhanced phosphorus and magnesium levels, are sent to a struvite reactor 124, which will be discussed further below. There is only very minimal struvite production in the liquids 115, because they have a very low ammonia level. VFAs or other forms of RBCs can be generated by fermentation as in the unified fermentation and thickening (UFAT) process disclosed in U.S. Patent # 6,387,264 B1. Other methods of obtaining VFAs, include various fermentation methods, harvesting from various waste products and purchase as industrial chemicals, such as acetic acid.

[0014] The thickened WAS with reduced phosphorus and magnesium levels is sent to an

anaerobic digester 116 with other sludges and is typically held there for a minimum of fifteen days, where it further treated by anaerobic bacteria which generate high concentrations of ammonia. The production of struvite in digester 116, is however, greatly reduced in comparison with the amount of struvite produced in digester 16 of the prior art system (which could be identical to digester 116) because of the reduction in phosphorus and magnesium in the thickened WAS, both of which are necessary for the formation of struvite. This reduction in struvite formation greatly reduces the formation of struvite deposits in the digester and pipes and equipment downstream from anaerobic digester 116.

[0015] The treated sludge from digester 116 is dewatered 118, by use of a centrifuge, dewatering belt, screen, plate and frame presses, etc. with the resultant dewatered solids being beneficially reused or disposed. The ammonia-rich liquids 122, which are less able to make struvite in the associated pipes and equipment because of the reduced phosphorus and magnesium, are sent to struvite reactor 124, where the abundant ammonia combines with the phosphorus and magnesium of the liquids 115 to form struvite.

[0016] Referring to Figure 3, input to the system 210 is in the form of mixed liquor suspended solids (MLSS) 214 taken from the anaerobic zone 212 of the aeration basin, in an enhanced biological phosphorus removal (EBPR) system. The majority of the MLSS progresses to a further portion of the aeration basin 218. RBCs are added to the added to the MLSS in a standard EBPR system, thereby causing phosphorus and magnesium to be released from the microorganisms. Other than this difference the processing is largely the same, although some variation is necessary to accommodate the larger flow 214 into the thickener 216, as MLSS is typically three times as dilute as WAS. To handle the dilute flow, thickener 216 may utilize gravity thickening that is optionally followed by a belt or centrifuge or other thickening device. The anaerobic reactor 112 and supplemental addition of RBCs, shown in Figure 2, can be eliminated.

[0017] Figure 2A shows yet another system similar to that of Figure 2 (and having identical reference designators for identical elements). System 220 may be seen to include a mainstream flow 220a and a sidestream flow 220b, as illustrated, respectively above and below the dashed horizontal line. System 220 is referred to herein as providing for the *in situ*, i.e. closed or contained, production of usable struvite byproduct (e.g. marketable products such as regularly or irregularly shaped and sized pellets or particles, non-marketable products such as struvite sludge, etc.) from WAS, without external inputs being required to realize the production process.

[0018] As will be understood, primary sludge contained in a primary clarifier 222 is processed through an UFAT 224 in accordance with US Patent No. 6,387,264 or an equivalent process that includes a fermenter 226 and a thickener 228 or combined fermenter/thickener that collectively process primary sludge into VFAs and a thickened sludge. The VFAs from UFAT 224 are inputted to an EBPR aeration basin 112a and to a separator/thickener 114 including, for example, an anaerobic release tank 114a and a second thickener such as a thickening centrifuge 114b. (Anaerobic reactor 112 of Figure 2 in this alternative embodiment of the

invention thus takes the form of an EBPR aeration basin 112a and a secondary clarifier 112b, as illustrated in Figure 2A.)

[0019] The thickened sludge is fed to a digester 116, as shown in Figure 2A. Either downstream from digester 116 at the struvite reactor (as described above by reference to Fig. 2) or upstream from digester 116, the pH of the P-rich and Mg-rich liquids is adjusted by a pH adjuster 117 (shown in dashed outline since it is optionally located in this upstream location instead of in struvite reactor 124). Those of skill in the art will appreciate that, despite adjusting the pH of the P-rich and Mg-rich liquids before they reach the struvite reactor nevertheless struvite does not form in the upstream pipe because no ammonia is present). Moreover, peak concentrations of the fluids in the downstream struvite reactor are reduced. In this way, optionally upstream-located pH adjuster 117 produces a pH-adjusted phosphorus-rich and magnesium-rich liquids stream 115' as an input to struvite reactor 124. (Thus, upstream pH adjuster 117 provides a system 220 topology that is more cost-effective and straightforward than the system 110 topology described above by reference to Figure 2 wherein pH adjustment is performed in the struvite reactor.)

[0020] A separator/thickener 114 acts to separate the WAS input from a secondary clarifier 112b downstream from EBPR aeration basin 112a and the VFA input from UFAT 224 into two distinct output streams. A first relatively phosphorus-rich and magnesium-rich (P- & Mg-Rich) liquids stream 115 (or, preferably, pH-adjusted liquids stream 115') is fed into struvite reactor 124, as described above. A second relatively phosphorus-reduced and magnesium-reduced (P- & Mg-Poor) mixture 230 is fed into a digester 116 followed by a dewaterer or dewatering centrifuge 118 to produce an ammonia-rich liquids stream 122 that is also fed to struvite reactor 124. Phosphorus-reduced (P-reduced) biosolids are produced as another byproduct of the dewatering step. By separating the WAS into two separate, differentially concentrated streams containing phosphorus and magnesium, downstream so-called nuisance struvite production within digester 116 is minimized while concurrent struvite production within struvite reactor 124 is maximized.

[0021] Those of skill in the art will appreciate that further downstream treatment 232 within mainstream process 220a can be accomplished via precipitation, filtration, and disinfection (e.g. chlorination followed by de-chlorination) of the output of secondary clarifier 112b (some of which is returned to the input of EBPR aeration basin 112a, and some of which is detoured to the sidestream process 220b, as illustrated). Thus, the output of downstream treatment 232 is suitable for return to a river or other body of water is the mainstream output of the process and system while usable and potentially sellable struvite product, e.g. pelletized fertilizer, is the sidestream output of the invented process and system. Those of skill also will appreciate that other output of struvite reactor 124 can be recycled as shown to the plant influent stream in what may be thought of as a substantially "closed-loop" system 220.

[0022] For the examples the struvite reactor can take any form that permits the combination of the phosphorus and magnesium with the ammonium, to form struvite, including a simple settling tank, where spontaneously precipitated struvite would form and settle for reuse as a

raw material, a usable product such as fertilizer, or a waste product. In one preferred example prilled struvite is formed by a method disclosed in International Publication Number WO 2005/077834 A1.

[0023] In a first preferred variant of either the MLSS or the WAS example the diversion of magnesium from the anaerobic digester and the resulting reduced nuisance struvite formation protects process equipment and reduces operational costs. In a second preferred variant, magnesium is added to capture additional phosphorus, thereby causing the system to produce additional struvite and a waste stream with less phosphorus and ammonia to be recycled back to the wastewater plant for re-treatment. In addition, phosphorus and magnesium can be added to increase struvite production and reduce the amount of ammonia sent back for re-treatment.

[0024] The above description is intended to provide an example of one method that falls within the scope of the invention. Skilled persons will recognize that other methods will also fall within the scope of the invention.

[0025] It will be understood that the present invention is not limited to the method or detail of construction, fabrication, material, application or use described and illustrated herein. Indeed, any suitable variation of fabrication, use, or application is contemplated as an alternative embodiment, and thus is within the scope of the invention.

[0026] It is further intended that any other embodiments of the present invention that result from any changes in application or method of use or operation, configuration, method of manufacture, shape, size, or material, which are not specified within the detailed written description or illustrations contained herein yet would be understood by one skilled in the art, are within the scope of the present invention.

[0027] Accordingly, while the present invention has been shown and described with reference to the foregoing embodiments of the invented process it will be apparent to those skilled in the art that other changes in form and detail may be made therein without departing from the scope of the invention as defined in the appended method claims.

REFERENCES CITED IN THE DESCRIPTION

This list of references cited by the applicant is for the reader's convenience only. It does not form part of the European patent document. Even though great care has been taken in compiling the references, errors or omissions cannot be excluded and the EPO disclaims all liability in this regard.

Patent documents cited in the description

- [US6387264B](#) [0018]
- [WO2005077834A1](#) [0022]

Non-patent literature cited in the description

- **D. MONTAGA** Feasible Approach of Integrating Phosphate Recovery as Struvite at Waste Water Treatment Plants Proceedings, Institute Of Environmental Engineering, 2007, 551-558 [0006]
- **J. H. RENSINK** The Modified Renphosystem: A High Biological Nutrient Removal System Wat. Sci. Tech., 1997, vol. 35, 10137-146 [0006]
- **S. WILLIAMS** Struvite precipitation in the sludge stream at slough wastewater treatment plant and opportunities for phosphorus recovery Environ. Techn., 1999, vol. 20, 7743-747 [0006]
- **M. R. GATERELL** An economic and environmental evaluation of the opportunities for substituting phosphorous recovered from wastewater treatment works in existing UK fertiliser markets Environ, Tech., 2000, vol. 21, 91067-1084 [0006]

Patentkrav

1. Fremgangsmåde til behandling af en første blanding af faste affaldsstoffer og mikroorganismer, der indeholder phosphor og magnesium, hvilken fremgangsmåde omfatter trinnene:

- 5 i) at bringe blandingen til at frigive phosphor og magnesium fra mikroorganismene;
- ii) at fortykke blandingen og aftappe det frigivne phosphor og magnesium for at danne en phosphor- og magnesium-rig væske og en phosphor- og magnesium-reduceret behandlet blanding;
- 10 iii) at anbringe den phosphor- og magnesium-reducerede behandlede blanding i en anaerob digestor for at danne en højammoniakblanding;
- iv) at afvande højammoniakblandingen for at danne en højammoniak-rig væske;
- v) at kombinere den højammoniak-rige væske og den phosphor- og
15 magnesium-rige væske for at danne struvit.

2. Fremgangsmåden ifølge krav 1 der yderligere inkluderer trinnet: at høste et anvendeligt struvit-produkt efter trin (v).

3. Fremgangsmåde ifølge krav 1 eller 2, hvor den første blanding af faste stoffer og mikroorganismer der indeholder phosphor og magnesium, er affaldsaktiveret slam (WAS).
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4. Fremgangsmåde ifølge et hvilket som helst af de foregående krav, hvor den første blanding af faste stoffer og mikroorganismer der indeholder phosphor og magnesium, holdes i en anaerob reaktor, således at phosphor og magnesium frigives ved mikrobiel virkning i den anaerobe reaktor, og den første blanding holdes inde i den anaerobe reaktor i mindst 0,5 timer.
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- 5.** Fremgangsmåde ifølge et hvilket som helst af de foregående krav, hvor den første blanding af faste stoffer og mikroorganismer udsættes for endogen respiration og fermentering ved at blive holdt i en anaerob reaktor.
- 5 **6.** Fremgangsmåde ifølge et hvilket som helst af de foregående krav, hvor blandingen sendes til en fortykningsindretning efter trin (i), og den resulterende phosphor- og magnesium-rige væske sendes til en struvit-reaktor.
- 10 **7.** Fremgangsmåden ifølge krav 6, hvor fortykningsindretningen er en centrifuge, et fortykningsbælte eller en roterende skærm.
- 15 **8.** Fremgangsmåde ifølge et hvilket som helst af de foregående krav, hvor den fortykkede phosphor- og magnesium-reducerede behandlede blanding sendes til en anaerob digestor, hvor den behandles af anaerobe bakterier, således at der dannes ammoniak.
- 9.** Fremgangsmåden ifølge krav 7, hvor den fortykkede phosphor- og magnesium-reducerede behandlede blanding holdes inde i den anaerobe digestor i 15 dage.
- 20 **10.** Fremgangsmåde ifølge et hvilket som helst af de foregående krav, hvor højammoniakblandingen afvandes for at danne en højammoniak-rig væske ved anvendelse af: en centrifuge, et afvandingsbælte, en afvandings-skærm eller en afvandingsplade med ramme.

DRAWINGS

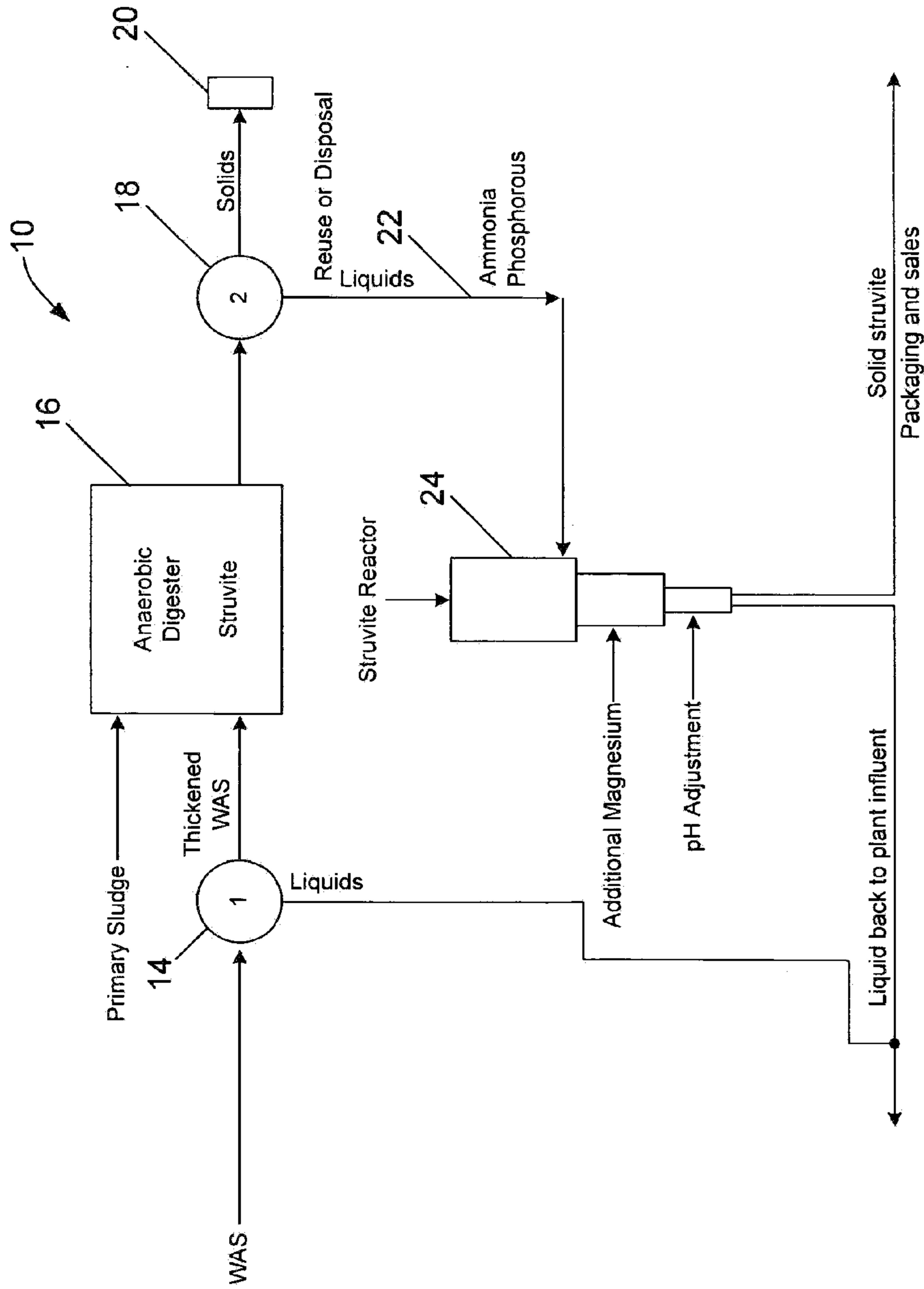


Figure 1 (Prior Art)

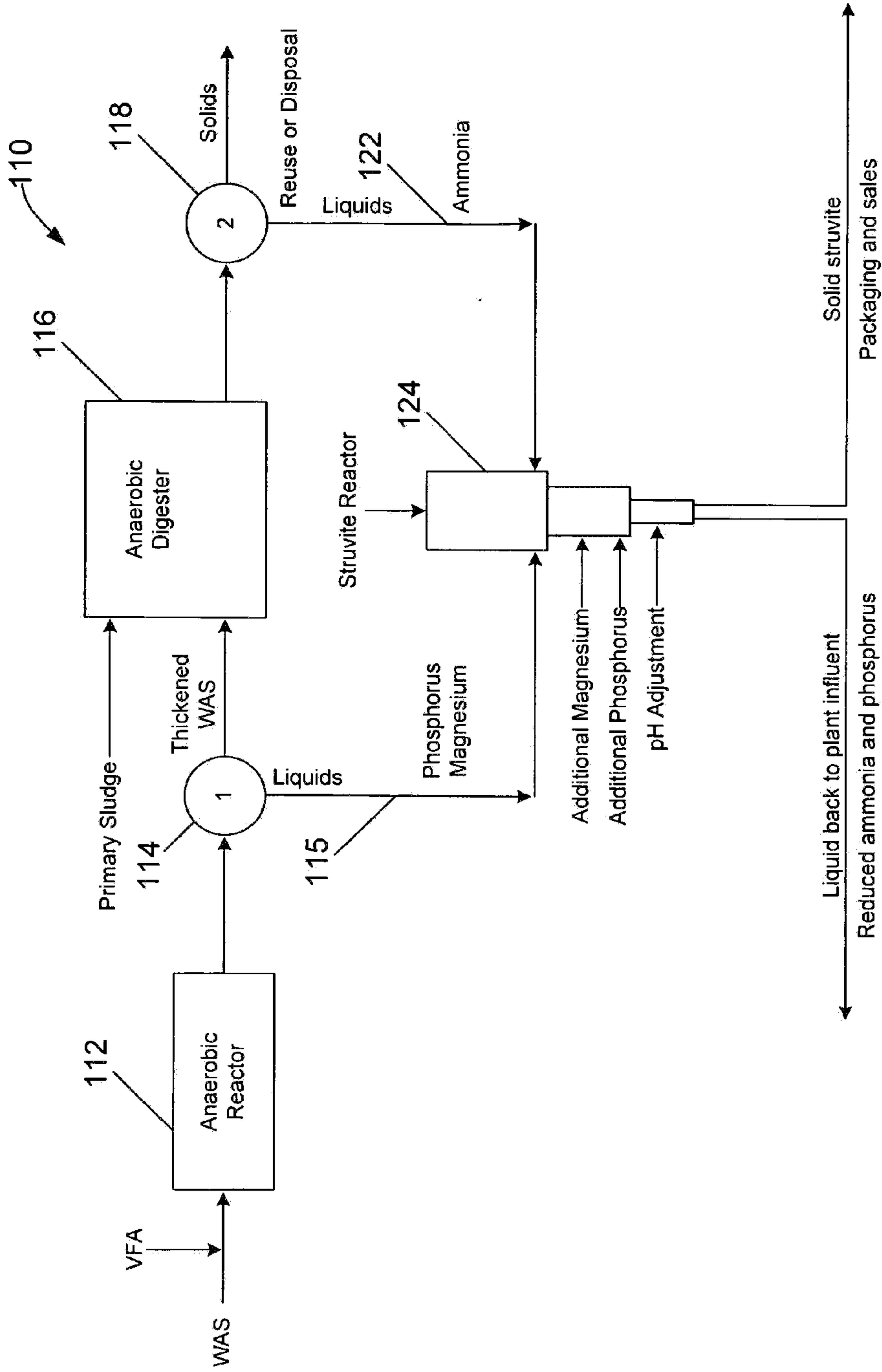


Figure 2

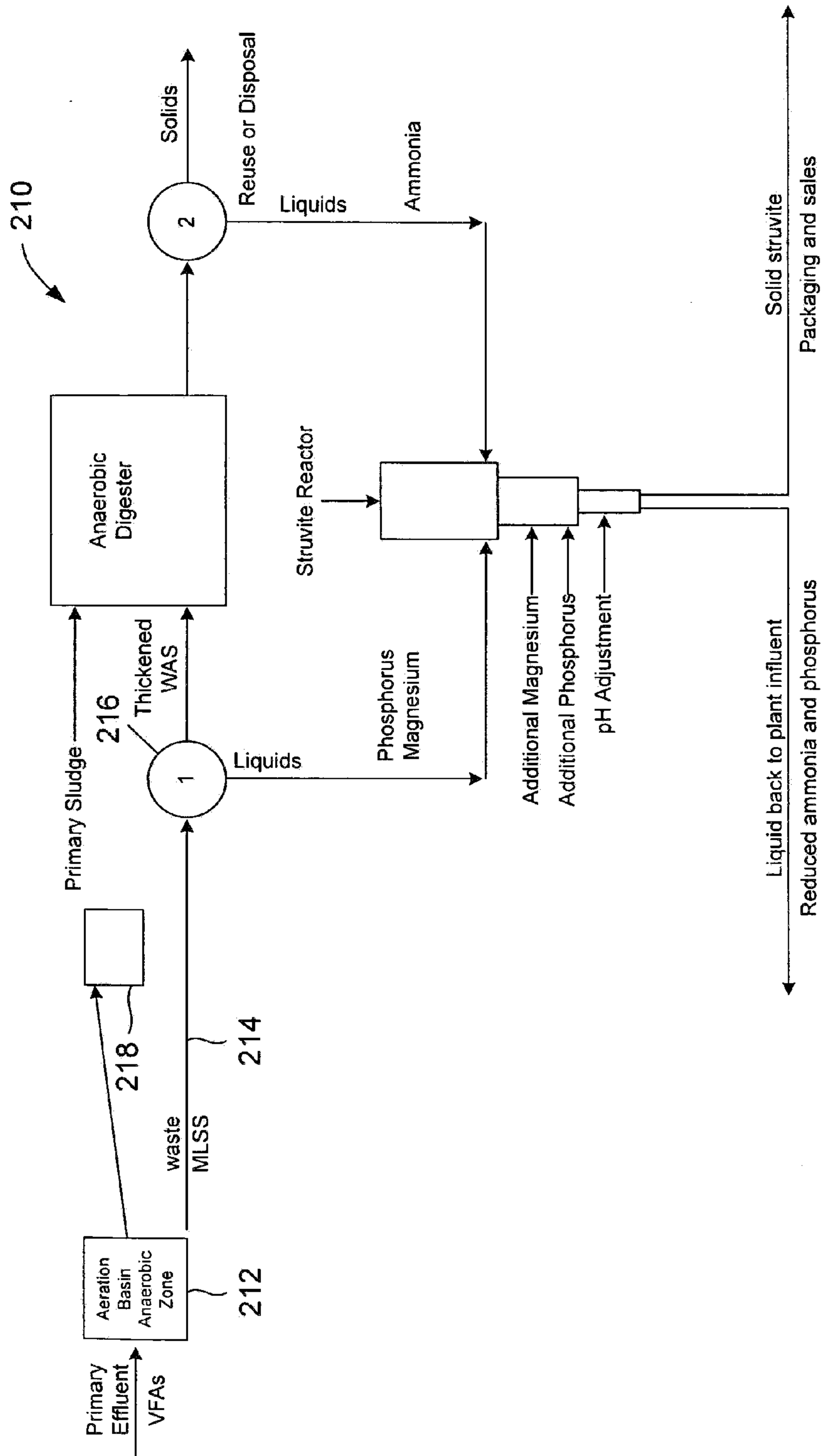


Figure 3

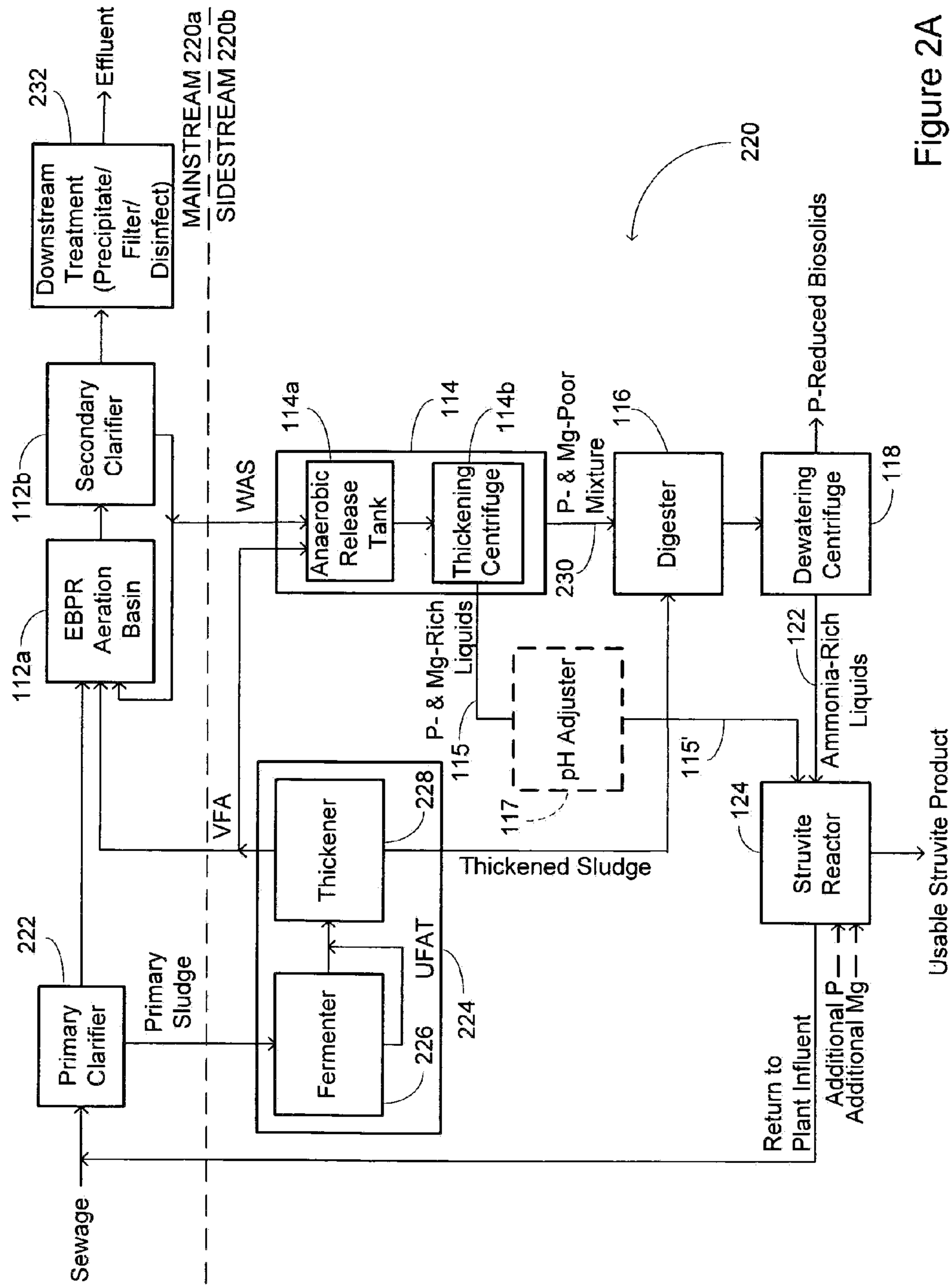


Figure 2A