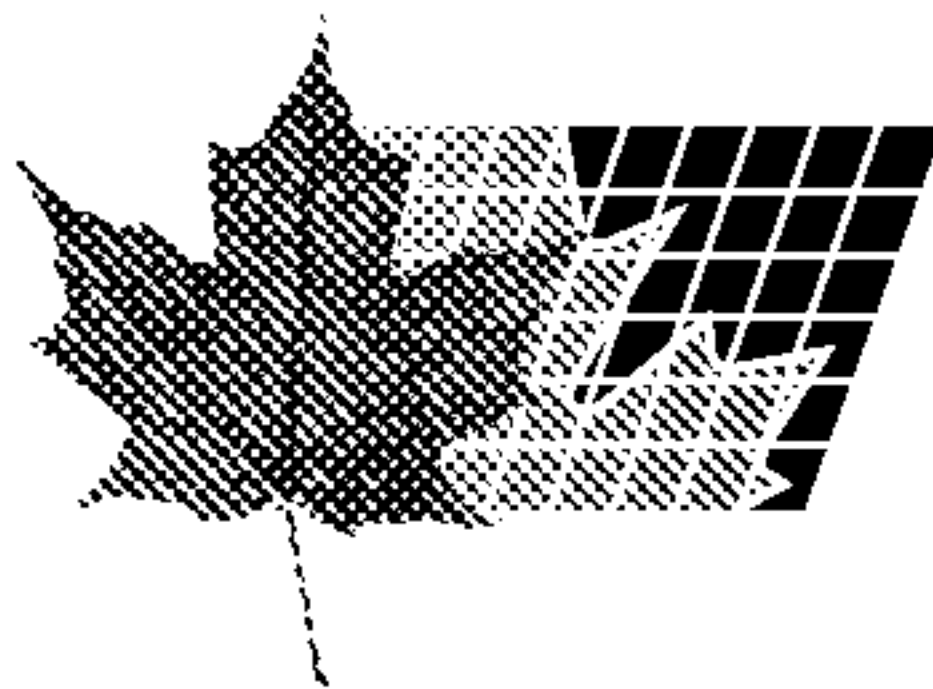




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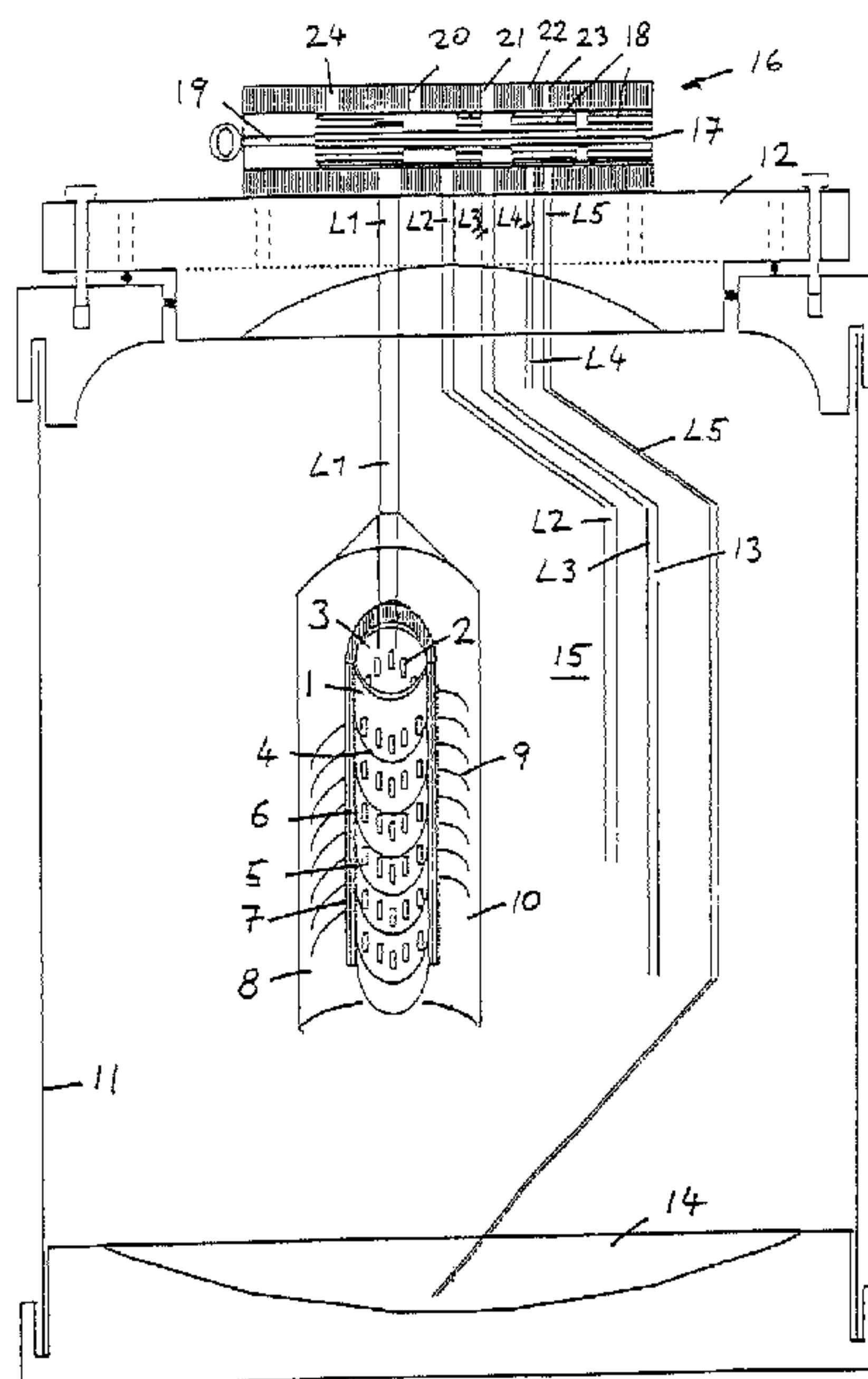
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(54) **APPAREIL ET PROCEDE DE TRAITEMENT DE L'EAU**

(54) **APPARATUS AND PROCESS FOR TREATING WATER**



(57) The invention relates to an apparatus for removing cations/anions from liquids, having a container (11) containing the liquid in which a layer of ion exchanger material (6) and also a cathode (9) and an anode (4), to which voltage is applied, are disposed, the layer of ion exchange material (6) being between the anode (4) and the cathode (9) and there being a free liquid-filled space as a treatment space (10) between the layer of ion exchange material (6) and the cathode (9) and there being a liquid-filled outer space (15) between the cathode (9) and the wall of the container (11), the treatment space (10) and the outer space (15) being connected to one another at least at both ends in order to permit liquid circulation.

Abstract of the disclosure

The invention relates to an apparatus for removing cations/anions from liquids, having a container (11) containing the liquid in which a layer of ion exchanger material (6) and also a cathode (9) and an anode (4), to which voltage is applied, are disposed, the layer of ion exchange material (6) being between the anode (4) and the cathode (9) and there being a free liquid-filled space as a treatment space (10) between the layer of ion exchange material (6) and the cathode (9) and there being a liquid-filled outer space (15) between the cathode (9) and the wall of the container (11), the treatment space (10) and the outer space (15) being connected to one another at least at both ends in order to permit liquid circulation.

Figure 1 is intended for the abstract of the disclosure.

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Apparatus and process for treating water

5 The invention relates to an apparatus for removing cations/anions from liquids, having a container containing the liquid in which a layer of ion exchanger material and also a cathode and an anode, to which voltage is applied, are disposed.

10 Processes and apparatuses are known in which liquids are subjected to a voltage field, as a result of which the ions, cations or anions contained in the liquid are separated from one another and/or are precipitated in extremely fine dispersion as a solid precipitate. Often, the liquid is passed through an ion exchanger in addition to the electrolytic process in order to increase the throughput rate of purified liquid. In that process, too,
15 solid materials are precipitated. The increase in the purified volume makes possible the continuous performance of the ion exchange process, without the liquid flow having to be interrupted.

20 An apparatus exploiting this combination of the electrolytic and chemical process principle is described in German Patent Application P 3,341,242, in which oxygen is removed from an aqueous solution electrochemically. In this application, the liquid flow is passed through a permeable, spatially extending ion exchanger. At the same
25 time, the liquid flow is subjected to a voltage field which propagates radially from concentrically disposed electrodes and extends coaxially with respect to the liquid flow. The oxygen produced in the ion exchange process is removed via pipes.

30 Other documents, for example German Patent Application P 3,805,813, disclose that the loaded ion exchange material can be retreated electrolytically, chemically or electrochemically, without having to be removed from the apparatus. In that case, the ion ex-
35 change material is subjected, for example, to a pulsating alternating voltage field or ionizing chemicals.

Common to all these processes and apparatuses is

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that the precipitating solid material remains in the liquid flow. As a result, the possibility cannot be excluded that this material reverts to the original state in a subsequent, even unintended, chemical or electro-chemical process and exhibits its harmful or undesirable effect.

Furthermore, it is not possible in the case of the known apparatuses to reduce cations and anions with the same ion exchanger material.

The object of the invention is to improve an apparatus/a process of the type mentioned in the introduction such that, with simple design and small construction, a high efficiency and a high functional reliability can be achieved with low energy requirement.

This object is achieved according to the invention by an apparatus wherein there is the layer of ion exchange material between the anode and the cathode and there is a free liquid-filled space as a treatment space between the layer of ion exchange material and the cathode and there is a liquid-filled outer space between the cathode and the wall of the container, the treatment space and the outer space being connected to one another at least at both ends in order to permit liquid circulation.

In accordance with one aspect of the present invention there is provided an apparatus for removing cations/anions from liquids, having a container containing the liquid in which a layer of ion exchanger material and also a cathode and an anode, are disposed, wherein there is the layer of ion exchange material between the anode and the cathode and there is a liquid-filled treatment space between the layer of ion exchange material and the cathode and there is a

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liquid-filled outer space between the cathode and the wall of the container, the treatment space and the outer space being connected to one another at least at both ends in order to permit liquid circulation.

5 Such an apparatus has a simple structure and possesses high efficiency. With a low energy requirement, both cations and anions can be removed using the same ion exchanger material. The ion
10 exchanger material does not become blocked and both inorganic and organic compounds, in particular salts, can be removed from the untreated water.

 A diffusion distribution of the pH and of the ions is achieved because of the circulation and, consequently, a homogenization of the concentration is
15 produced. Mixing the liquids taken from the inner space and outer space and/or mixing of the same individually or jointly with untreated water results in a stabilization of the pH of the
20 treated water. The regeneration of the ion exchanger material, in particular of a resin, depends

under these conditions on the concentration of the hydrogen ions produced. If the total pressure of the system is increased, the partial pressure of the ions required for the regeneration also increases. This takes place, in particular, as a result of isolating the equipment.

Whereas in the prior art to separate cations it is necessary to use a particular ion exchanger material which does not adsorb anions, in the apparatus according to the invention the ion exchanger material can reduce both anions and cations. In contrast to reverse osmosis, in the apparatus according to the invention inorganic and organic compounds contained in the untreated water can be separated with reduced energy input and at low pressure.

It is particularly advantageous if the outer space and/or the treatment space debouch into a settling space at the bottom.

This ensures that the treated water emerging from the apparatus does not contain flocculated material. A high efficiency is also achieved if the, in particular, elongated anode is centrally disposed axially and the layer of ion exchanger material, the treatment space, the cathode and the outer space are disposed in shell fashion around the anode.

It is particularly advantageous if the anode is disposed, in particular, in spiral form on the outside of a perforated or slotted inner tube. Furthermore, it is also proposed that the layer of ion exchange material is bounded on one or both sides by a grid, fabric or gauze. The operation of the apparatus is also improved if the treatment space and the outer space are separated by a partition, in particular a tube, on the inside of which the cathode is disposed. At the same time, the wall or the tube may be perforated or slotted.

It is preferably proposed that the inner tube, the layer of ion exchange material, the partition and/or the container wall, and also the annular intermediate spaces, are coaxial with respect to one another. An optimum flow inside the equipment is achieved if the

(longitudinal) axes of the walls, layers and/or tubes are vertical.

5 In order to achieve simultaneous water removal at the top and bottom of the equipment, so that a mixture of water with different pH values can be removed, it is proposed that a water removal pipe is provided which has at least one inlet opening in each case in the lower and upper outer space.

10 It is of greatest advantage if the inlet and outlet pipes of the container are connected to a multiway valve. As a result of this, all the functional capabilities of the equipment can be controlled by adjusting only a single valve control element.

15 Continuous treatment of the untreated water with a high throughput is achieved if the apparatus is a double or multiple system which operates in alternating fashion.

20 A process for removing cations/anions from liquids using the apparatus according to the invention is one which comprises switching the feed and drainage pipes in a manner such that the water treatment time is interrupted by time intervals during which the ion exchange material is regenerated and sludge is removed from the settling space. This achieves an optimum operating mode.
25 In addition, it is also proposed that, during the water treatment time, untreated water from time to time flows partly or completely into the outer space and/or into the treatment space. With this operating mode, the effectiveness is lower so that it is possible to ensure that the
30 treated water cannot be treated excessively and the desired pH is achieved.

An exemplary embodiment of the invention is shown in the drawings and is described in greater detail below. In the drawings:

35 Figure 1 shows a vertical section through the apparatus with a multiway valve mounted at the top and a treatment space disposed internally, the parts of the treatment space being shown isometrically,

Figure 2 shows a section through the multiway valve in the operating position,

Figure 3 shows the multiway valve in the mixing position,

5 Figure 4 shows the multiway valve in the low treatment position,

Figure 5 shows the multiway valve in the regeneration position,

10 Figure 6 shows the multiway valve in the flushing position, and

Figure 7 shows the multiway valve in the desludging position.

The apparatus has a vertical tube 1 which possesses openings 2, in particular in the form of slots, and
15 encloses an anode space 3. The tube 1 forms a support for a helical anode 4 situated on the outside. Above the anode there is a fabric 5, in particular a filter hose, which ensures that the ion exchanger material 6 situated on top and disposed circumferentially in a layer does not
20 pass through the openings 2 into the anode space 3. The ion exchanger material is a resin, in particular in the form of spheroids, and is surrounded on the outside by a steel grid 7.

Disposed coaxially at a distance from the grid 7
25 is a plastic tube 8 against the inside of which a cathode 9 rests in spiral fashion. Consequently, between the tube 8, and also the cathode 9, and the layer of ion exchanger material there is situated a treatment space 10 which is annular in cross section and which is open at the top and
30 bottom.

The parts 1 to 10 are situated roughly in the center of a cylindrical container 11, with the result that the tube 8 is at a roughly equal distance from the wall of the container 11 all around.

35 During the treatment time, untreated water flows via the pipe 11, which debouches in the interior of the anode space 3, into the anode space and leaves calcium behind in the resin of the ion exchanger material 6 in exchange for hydrogen ions.

In the regeneration mode, hydrogen ions migrate from the anode to the cathode and displace the calcium ions in the resin, which migrate to the cathode and are flocculated by the high pH.

5 From the top of the container 11, a second water inlet pipe L2 projects downwards into the container through the upper container lid 12 next to the water inlet pipe L1, which second water inlet pipe debouches roughly in the central region of the container outside
10 the tube 8. Furthermore, a water outlet pipe L3, which debouches in the lower region and possesses at least one further inlet opening 13 in the upper region, projects downwards. A venting pipe L4 debouches in the upper region and, finally, a desludging pipe L5 debouches in
15 the lowermost region, i.e. in the settling space 14. The pipes L2 to L5 consequently extend through the outer space (reservoir) 15 which is situated all around the tube 8.

20 All the pipes L1 to L5 extend through the lid 12 and are connected to a multiway valve 16 which is attached to the top of the lid 12. At the top, the multiway valve 16 is connected to an untreated water inlet 20, a water outlet 21, a venting pipe 22, a desludging pipe 23 and a vent 24 for the anode space. The multiway valve 16
25 possesses a valve control element 17 having a plurality of separate pistons 18 on a valve rod 19. By setting the valve rod 19 in a plurality of positions, the positions below and, consequently, operating modes of the apparatus can be achieved. The setting of the valve control element
30 17 and, consequently, of the piston rod 19 is preferably carried out by an electrical setting apparatus which can be regulated/controlled by an electronic apparatus:

I Operating position (Figure 2)

35 In the operating position shown in Figure 2, the pipes L2, L4 and L5 are closed and untreated water is fed through the pipe L1 into the anode space and the treated water is drained via the pipe L3.

II Mixing position (Figure 3)

5 In this position, the pipes L4 and L5 are closed and untreated water is admitted both through the pipe L1 and through the pipe L2, with the result that part of the untreated water passes into the anode space and part into the outer space. This produces a lower treatment effect, ensuring that the water emerging is not excessively treated.

III Lowest treatment position (Figure 4)

10 In this position, the pipes L1, L4 and L5 are closed and the untreated water enters only through the pipe L2 and consequently passes only into the outer space 15, with the result that the least possible treatment is achieved. The treated water once again emerges through
15 the pipe L3. In order to equalize the degree of treatment, the apparatus can alternate to and fro between positions I to III by means of a control or regulating device.

IV Regeneration (Figure 5)

20 The pipes L2, L3 and L5 are closed and a rectified voltage is applied between anode and cathode. As a result of ion migration, the hydrogen ions displace the other cations (e.g. calcium) adsorbed on the ion exchanger material 6 and the concentrations of the cations
25 and hydroxyl ions increase in the outer space 10 and treatment space 15, leading to simultaneous regeneration of the ion exchanger material, desiccation of hydroxides and carbonates in the outer space and treatment space and settling of the same in the settling space 14.

30 The anions, e.g. chloride, nitrate etc., accumulate in the anode space 3.

 During the regeneration time, continuous water extraction is ensured by an apparatus connected in parallel.

V Flushing (Figure 6)

5 The pipes L3, L4 and L5 are closed and untreated water enters via the pipe L2 and the water is displaced from the anode space 3 via the pipe L1, as a result of which the undesired anions are flushed out. This state lasts only seconds.

VI Desludging (Figure 7)

10 The pipes L2, L3 and L4 are closed, untreated water is forced in through the pipe L1 and sludge is forced out through the pipe L5. This state also lasts only seconds.

Claims

1. An apparatus for removing cations/anions from liquids, having a container containing the liquid in which a layer of ion exchanger material and also a cathode and an anode, are disposed, wherein there is the layer of ion exchange material between the anode and the cathode and there is a liquid-filled treatment space between the layer of ion exchange material and the cathode and there is a liquid-filled outer space between the cathode and the wall of the container, the treatment space and the outer space being connected to one another at least at both ends in order to permit liquid circulation.
2. The apparatus as claimed in claim 1, wherein the outer space and/or the treatment space debouch into a settling space at the bottom of the container.
3. The apparatus as claimed in claim 1 or 2, wherein the anode is elongated, and the layer of ion exchanger material, the treatment space, the cathode and the outer space are disposed coaxially in shell fashion around the anode.
4. The apparatus as claimed in claim 1, 2 or 3, wherein the anode is disposed in spiral form on the outside of a perforated tube.
5. The apparatus as claimed in any one of claims 1 to 4, wherein the layer of ion exchange material is bounded on one or both sides by a grid, fabric or gauze.
6. The apparatus as claimed in any one of claims 1 to 5, wherein the treatment space and the outer space are separated by a tube, on the inside of which tube the cathode is disposed.
7. The apparatus as claimed in claim 6, wherein the wall of the tube is perforated or slotted.

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8. The apparatus as claimed in any one of claims 1 to 7, wherein the (longitudinal) axes of the walls, layers the anode and the cathode are vertical.

5 9. The apparatus as claimed in any one of claims 1 to 8, wherein a water inlet pipe which debouches in the treatment space is provided.

10. The apparatus as claimed in any one of claims 1 to 9, wherein a water inlet pipe debouching in the outer space and/or in the treatment space is provided.

10 11. The apparatus as claimed in any one of claims 1 to 10, wherein a water outlet pipe which has at least one inlet opening in a lower part and an upper part of the outer space is provided.

15 12. The apparatus as claimed in any one of claims 1 to 11, wherein inlet and outlet pipes to the container are connected to a multiway valve.

20 13. The apparatus as claimed in any one of claims 1 to 12, wherein the electrodes are spiral electrodes and a magnetic direct or alternating field is arranged across the electrodes.

14. A device for removing ions from liquids, comprising a plurality of apparatuses according to any one of claims 1 to 13, which apparatuses operate in alternating fashion.

25 15. A process for removing cations/anions from liquids using an apparatus or device as claimed in any one of claims 1 to 14, the process comprising switching feed and drainage pipes in a manner such that the water treatment time is interrupted by time intervals during
30 which the ion exchange material is regenerated and sludge is removed from a settling space.

35 16. The process as claimed in claim 15, wherein, during the water treatment time, untreated water from time to time flows into the outer space and/or into the treatment space.

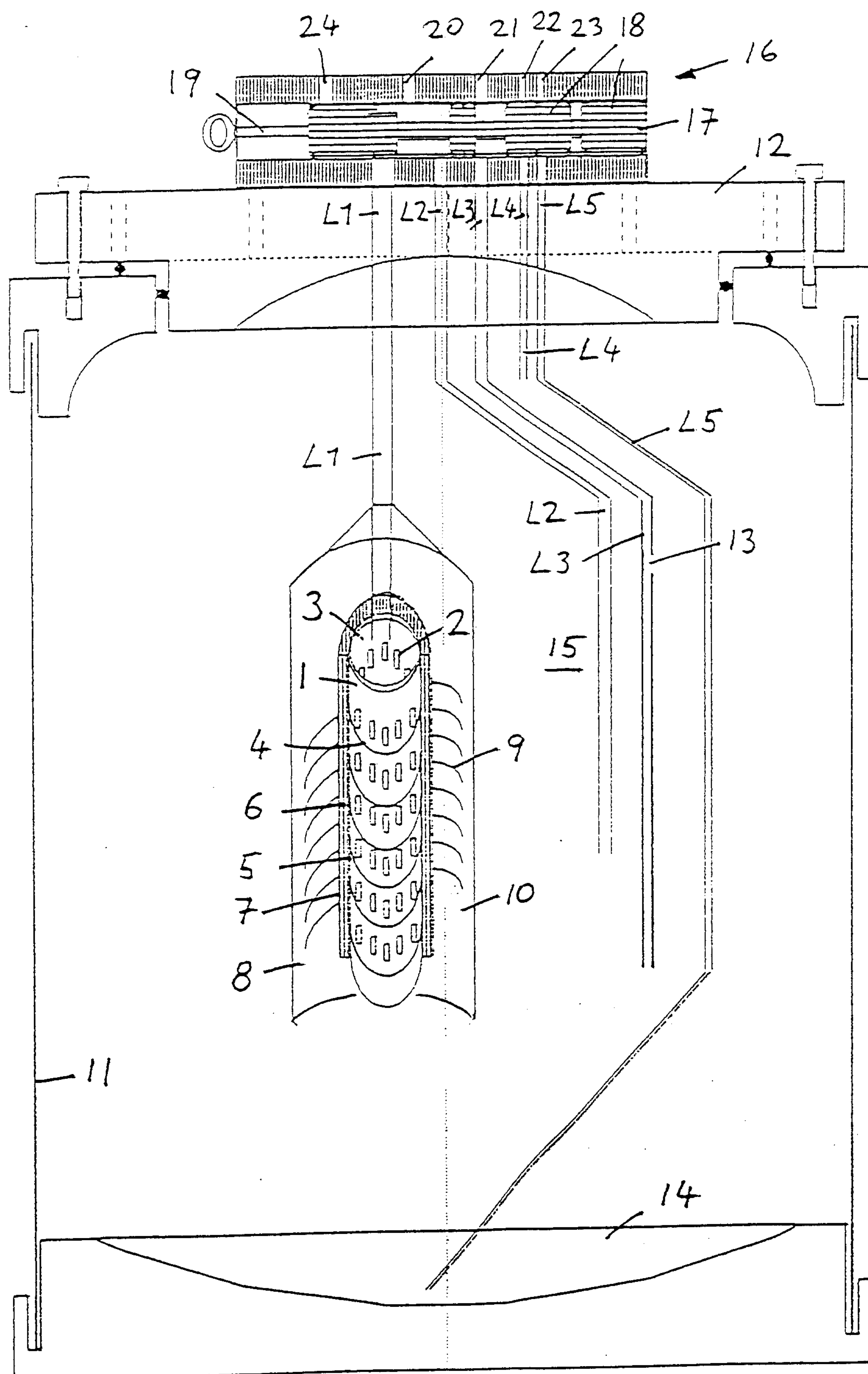
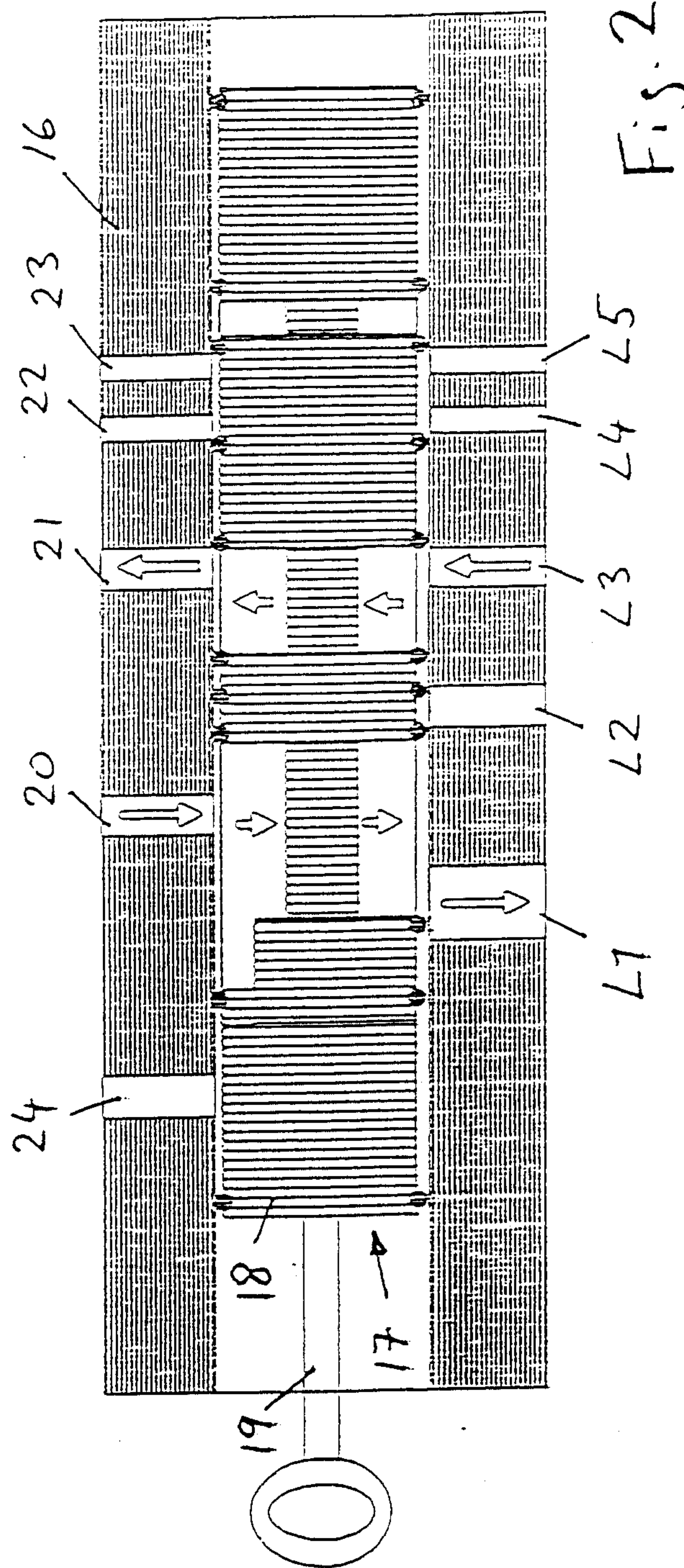


Fig. 1

Atty. Bldg. 6th
 Wash. D. C.

14



II

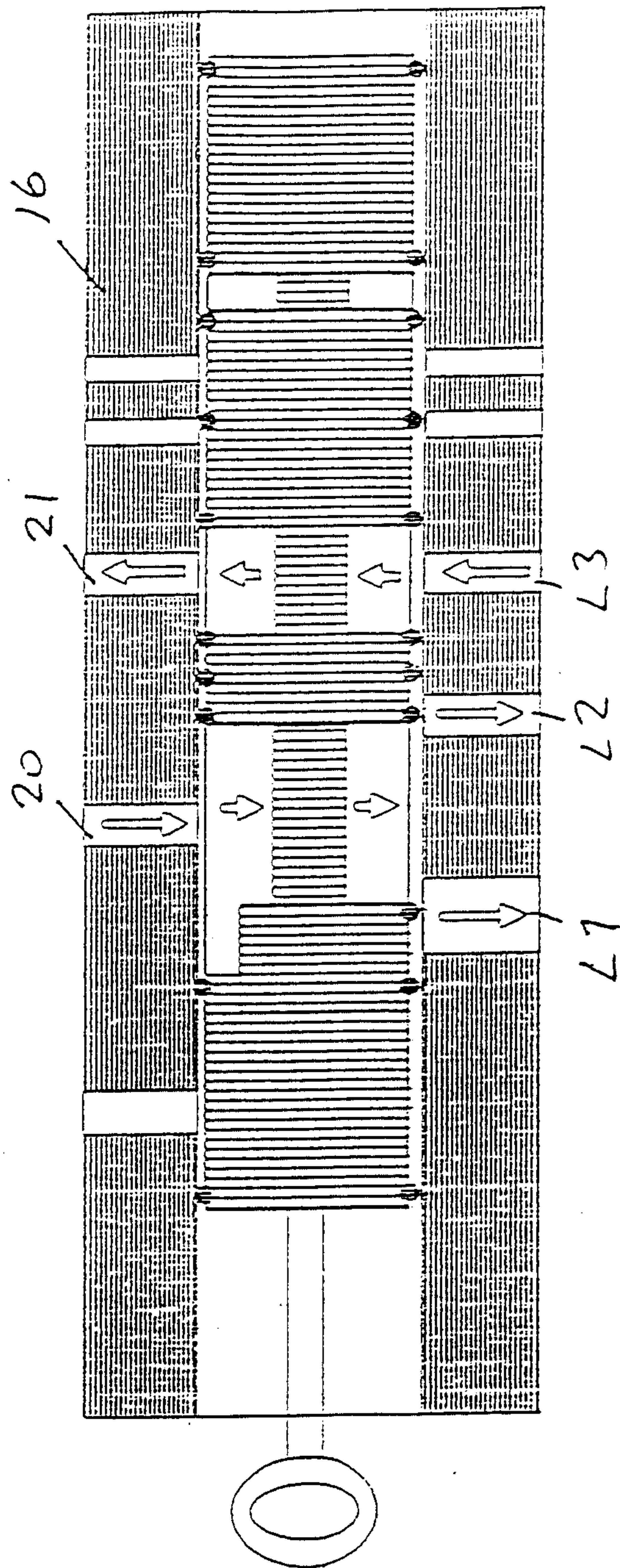


Fig. 3

III

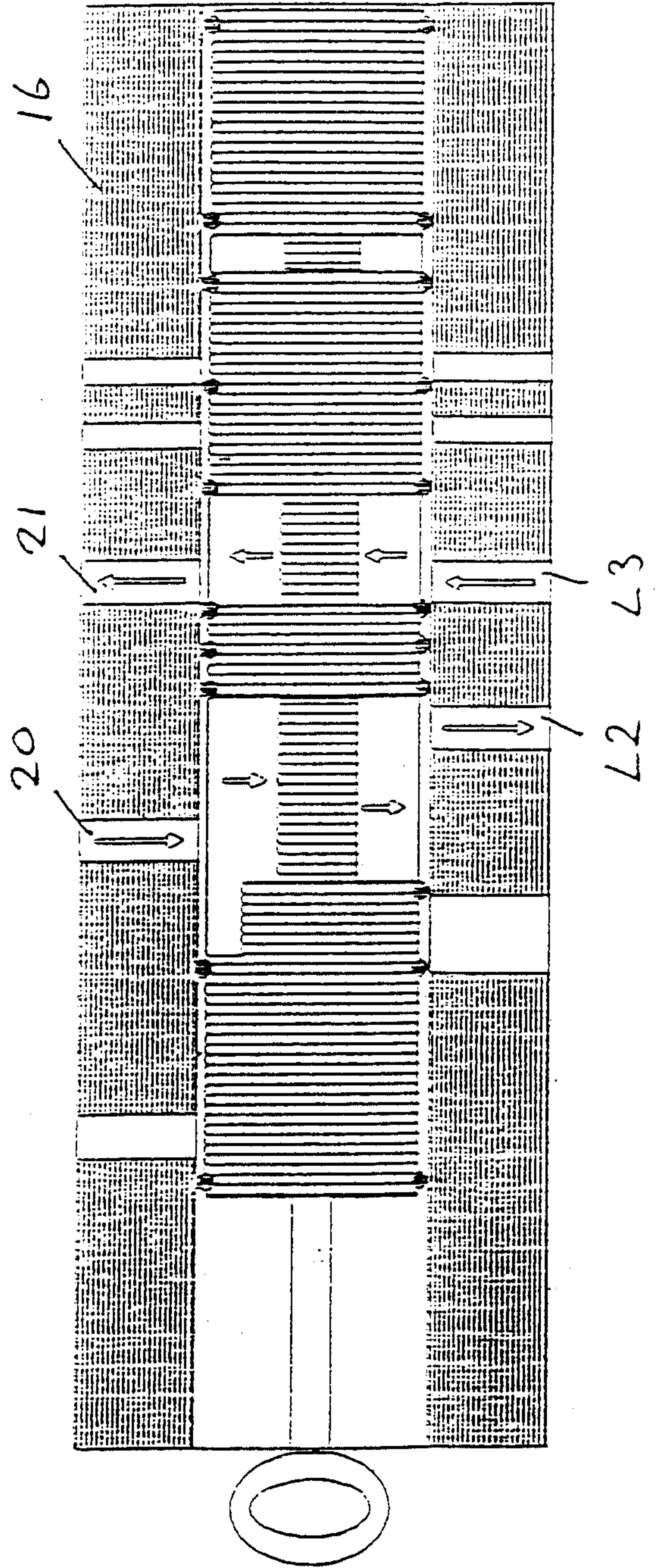


Fig. 4

IV

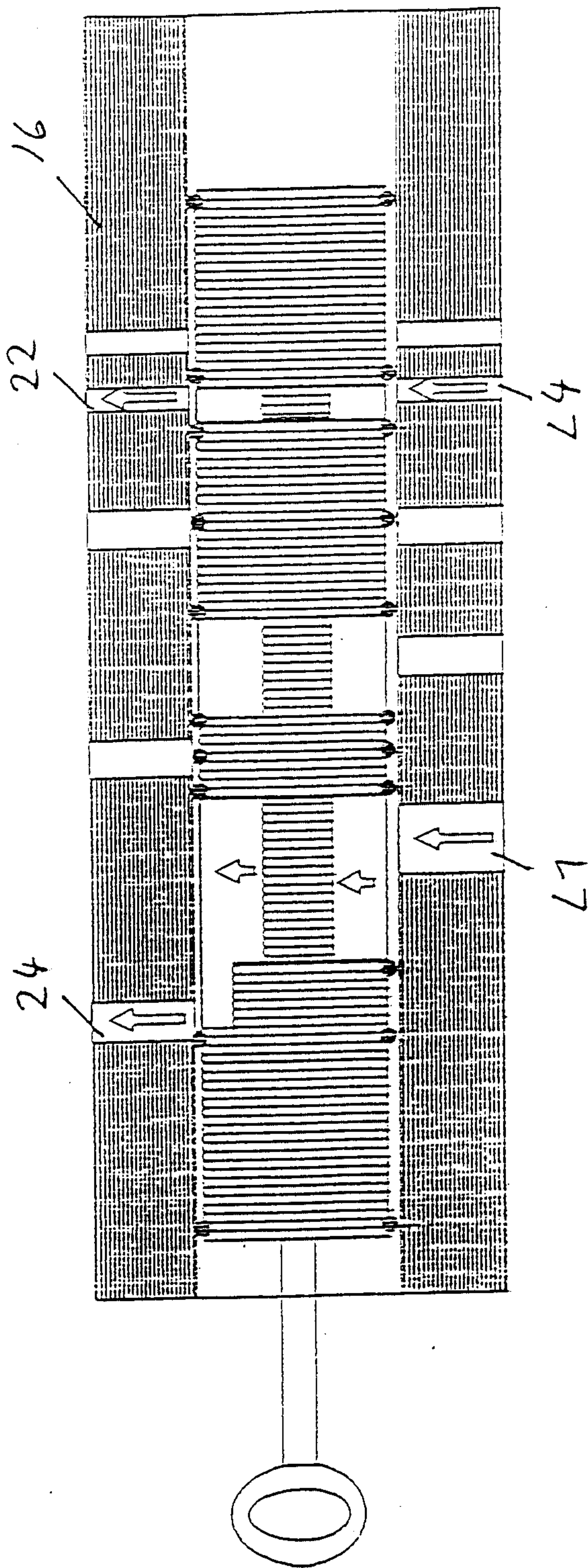


Fig. 5

V

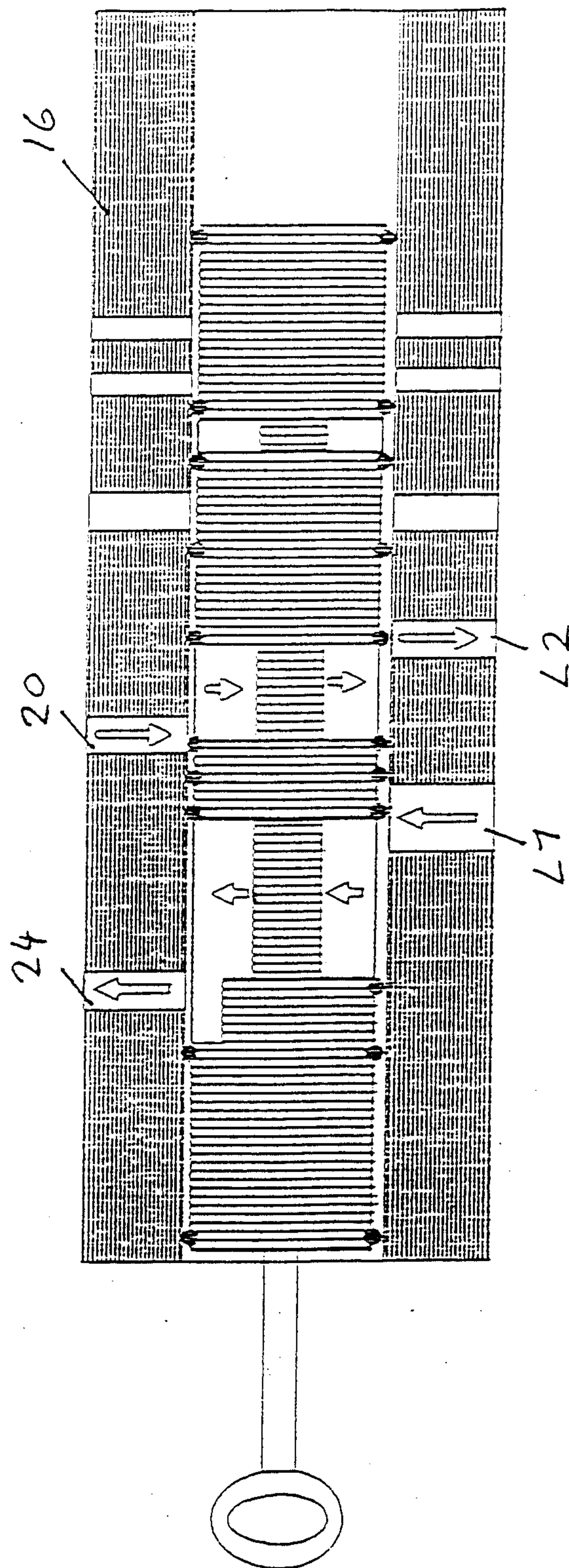


Fig. 6

