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(54) **Title:**
**PROCESS AND APPARATUS FOR SPINNING FIBRES
AND IN PARTICULAR FOR PRODUCING A FIBROUS-
CONTAINING NONWOVEN**

(57) **Abstract:**
The apparatus (1) is used for producing meltblown fibres (MF). It comprises a die head (104) with several spinning orifices, means (100, 101, 102, 103) for extruding at least one melted polymeric material through the spinning orifices of the die head (104) in the form of meltblown filaments (f), and means (104a, 104b) for blowing a hot primary gas flow (F1) towards the outlet of the die head (104) in order to draw and attenuate the polymeric filaments (f) at the outlet of the die head, and a drawing unit (105) that is positioned below the die head (104), and that is adapted to create an additional gas flow (F3) that is oriented downstream to further draw and attenuate the meltblown filaments (f).



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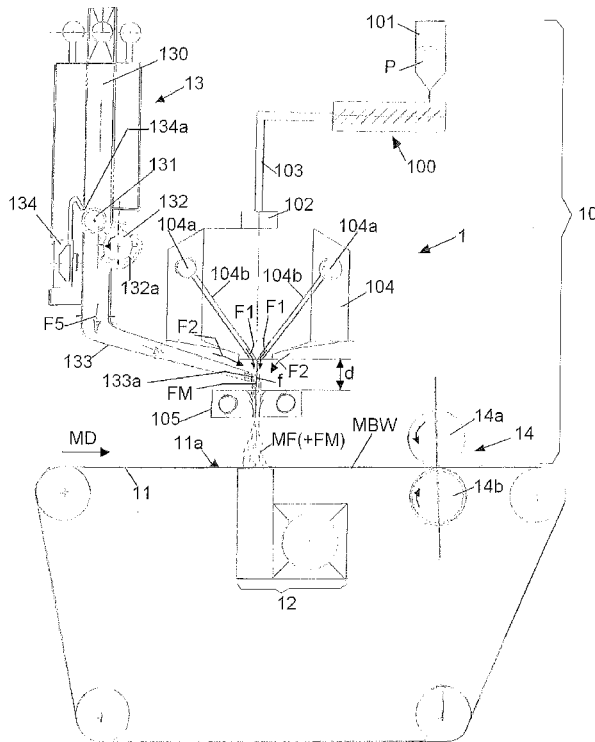
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FIG.1

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**PROCESS AND APPARATUS FOR SPINNING FIBRES AND IN
PARTICULAR FOR PRODUCING A FIBROUS-CONTAINING
NONWOVEN**

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Technical field

The present invention relates to the field of fibres spinning. In this field, the invention mainly relates to a novel improved process and apparatus for spinning fibres, and to a novel process and apparatus for producing a fibrous-containing nonwoven, and in particular pulp-containing meltblown nonwoven.

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Prior art

A well-known technology for spinning fibres and making a nonwoven is the so-called meltblown technology. A process and apparatus for manufacturing a meltblown nonwoven are well-known and described for example in US patent No 3,849,241 to Butin et al, and in US patent No 4,048,364 to Harding et al.

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Basically, the well-known process for manufacturing a meltblown nonwoven involves extruding a molten polymeric material through a die head into meltblown polymeric filaments, and attenuating these filaments by converging flows of a high velocity heated gas (usually air), hereafter called "primary air". This primary air is heated at a temperature which is typically equal or slightly greater than the melt temperature of the polymer. This hot primary air draws and attenuates the polymeric filaments immediately at the outlet of the die head. In a meltblown process, the drawing force for attenuating the meltblown filaments is thus applied immediately at the outlet of the die head while the polymer is still in the molten state. At the outlet of the die head, a large volume of cooling air, hereafter called "secondary air" is drawn into the primary air. This secondary air is cooling down the meltblown filaments downstream from the die head and provides the quenching of the meltblown filaments.

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Generally, in a meltblow process, the primary air is also adjusted in

such way that the meltblown filaments are broken at the outlet of the die head into discontinuous fibres (microfibrils or nanofibrils) of shorter length. The discontinuous fibres generally have a length exceeding the typical length of staple fibres. More particularly, to date with a standard known
5 meltblow process, discontinuous meltblown fibres having a length between 5mm and 20mm can be produced.

The meltblown fibres are delivered downstream from the die head onto a moving surface, like for example a cylinder or conveyor belt, in order to form a meltblown nonwoven web of unoriented meltblown fibres.
10 Preferably, the forming surface is air permeable, and even more preferably suction means are provided for sucking the fibres onto the forming surface. This meltblown nonwoven web can then be transported to consolidating means, like for example thermal bonding calendar, a water needling unit, an ultrasonic bonding unit, in order to form a consolidated meltblown nonwoven
15 web.

With a standard meltblow process, meltblown nonwovens made of very fine denier fibres can be advantageously produced. Typically, the average diameter of meltblown fibres can be less than 10µm. As a result, meltblown nonwovens of low air permeability and good coverage can be
20 advantageously obtained.

In return, the meltblown technology has several limitations and drawbacks.

During a standard meltblow process, the meltblown fibres have been submitted only to a small stretching, and the meltblown fibres thus exhibit a
25 low tenacity. The meltblown nonwovens have thus generally poor mechanical properties, and in particular exhibit a low tenacity, a low mechanical tensile strength in the machine direction and in the cross direction, and a low elasticity.

In addition, in a standard meltblow process, the velocity of the
30 primary air has to be adjusted, in order to achieve the required attenuation of the meltblown filaments as well as the appropriate breaking of the meltblown

filaments into discontinuous meltblown fibres of predetermined average length. In practise, in order to obtain a sufficient attenuation of the meltblown filaments and produce fine denier meltblown fibres, the velocity of the primary air has to be sufficiently high, which also leads to the production of shorter meltblown fibres. In a standard meltblow process the adjustment of the average diameter and length of the meltblown fibres is thus difficult and not very flexible. In particular, it is for example difficult to produce meltblown polypropylene fibres having a very small diameter, typically less than 10 μ m, and having a long length, for example higher than 20mm.

10 To date, in the standard meltblow technology, only polymer of high melt flow index, typically between 600 and 2000, can be processed. Even though a spinneret having non circular spinning orifices, and for example bilobal shaped orifices, is being used, this high melt flow index combined with the stretching of the filament leads to a deformation in cross section of the filament, and the filament shape conferred by the spinning orifices cannot be maintained. Actually, it is possible in practise to produce meltblown filaments having only a substantially circular shape in cross section,

In US patent 5, 075, 068, it is proposed to discharge an additional crossflow air toward the meltblown filaments to disrupt their shape by creating an undulation in the filaments. This undulation would enhance the drag forces imparted by the primary meltblown air. To the knowledge of the inventor, such a technology has never been commercialized and the undulation of the filaments by the crossflow air seems to be difficult to control, and could lead to detrimental undulation of the filaments.

A consolidated meltblown nonwoven can be used alone for making a textile product or can be used in a laminate comprising additional layers, such as for example other nonwoven web(s) [meltblown web(s), spunbonded web(s), carded web(s), air-laid web(s)] and/or additional fibrous layer(s), such as for example fibrous layer(s) made of wood-pulp fibres, and/or additional plastic film(s). The laminate can be consolidated by any

known consolidating means, including thermal bonding, mechanical bonding, hydroentangling, ultrasonic bonding, air-through bonding, and adhesive bonding.

More particularly, for making a laminate having high absorbency properties, it is known to laminate a meltblown nonwoven with at least one layer of fibrous material having high absorbency capacity, such as for example a layer of short wood-pulp fibres. This layer of wood-pulp fibres can also be mixed with particles, such as particles made of super absorbent material.

One important drawback of such a laminate is the low cohesion between the fibrous layer and the meltblown nonwoven prior to or even after the consolidation step of the laminate. This low cohesion leads to high and detrimental loss of fibrous material (e.g. wood-pulp fibres).

A process for producing a fibrous-containing meltblown nonwoven, and more particularly a pulp-containing meltblown nonwoven is also known in the prior art and is disclosed for example in US patent No 4,931, 355 and in US patent No 4,939,016 to Radwanski et al. The fibrous material, e.g. wood pulp, is fed directly into the polymer streams immediately downstream from the outlet of the meltblow die head.

In such a process, due to the high velocity of the polymer streams at the outlet of the die head, it is actually difficult to reliably incorporate the fibrous material inside the meltblown filaments that are extruded through the die head. As a result, during the manufacturing process, a large quantity of fibrous material is not incorporated inside the meltblown filaments, and is on the contrary pushed back by the air flow that surrounds the meltblown filaments downstream from the die head. Furthermore, in the fibrous-containing meltblown nonwoven that is obtained with such a process, the fibrous material is not strongly intermingled with the meltblown fibres, and the bonding of the fibrous material with the meltblown fibres is low. This low bonding leads to high loss of fibrous material when the fibrous-containing meltblown nonwoven is subsequently transported or handled. This loss of

fibrous material is even more important and detrimental in case the fibrous-containing meltblown nonwoven is submitted to a subsequent hydro-entanglement step, as described in aforesaid US patent No 4,931, 355 and US patent No 4,939,016.

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Summary of the invention

A first objective of the invention is to propose a novel improved technical solution for spinning meltblown fibres.

This first objective is achieved by the meltblow apparatus of claim 1 and by the meltblow process of claim 11.

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The apparatus for producing meltblown fibres comprises a die head with several spinning orifices, means for extruding at least one melted polymeric material through the spinning orifices of the die head in the form of meltblown filaments, and means for blowing a hot primary gas flow towards the outlet of the die head in order to draw and attenuate the polymeric filaments at the outlet of the die head, and a drawing unit positioned below the die head, and adapted to create an additional gas flow that is oriented downstream for further drawing and attenuating the meltblown filaments.

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The process comprises the following steps :

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(i) extruding through spinning orifices of a die head at least one melted polymeric material in order to form polymeric meltblown filaments,

(ii) drawing and attenuating the meltblown filaments at the outlet of the die head, by means of a hot primary gas flow,

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(iii) using a drawing unit positioned below the die head for generating an additional gas flow that is oriented downstream, in order to further draw and attenuate the meltblown filaments. A second objective of the invention is to propose a novel improved technical solution for making a fibrous-containing nonwoven, said novel improved technical solution notably overcoming the aforesaid drawbacks of the solution disclosed in US patent No 4,931, 355 and in US patent No 4,939,016 to Radwanski et

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al.

This second objective is achieved by the spinning apparatus of claim 23 and by the spinning process of claim 37.

The spinning apparatus for making a fibrous-containing nonwoven, 5 comprises a die head with several spinning orifices, means for extruding at least one melted polymeric material through the spinning orifices of the die head in the form of filaments, and a drawing unit positioned below the die head, and adapted to create a gas flow that is oriented downstream for drawing and attenuating the filaments, the apparatus further comprising 10 supplying means for continuously feeding a stream of fibrous material at a position between the die head and the drawing unit, and nearby the filaments.

The spinning process for making a fibrous-containing nonwoven comprises the following operations:

- 15 (i) at least one melted polymeric material is extruded through spinning orifices of a die head in order to form polymeric filaments, (ii) a drawing unit positioned below the die head is used for generating a gas flow that is oriented downstream, in order to draw and attenuate the filaments 20 (iii) fibrous material is continuously fed at a position between the die head, and the drawing unit, and nearby the filaments.

A third objective of the invention is to propose a novel improved technical solution for spinning discontinuous fibres.

This third objective is achieved by the apparatus of claim 51 and 25 by the process of claim 64.

The apparatus for spinning discontinuous fibres comprises a die head with several spinning orifices, means for extruding at least one melted polymeric material through the spinning orifices of the die head in the form of filaments, and a drawing unit positioned below the die head, 30 and adapted to create a gas flow (F3) that is oriented downstream for drawing and attenuating the filaments (f), and for breaking the filaments

into discontinuous fibres.

In the process for producing discontinuous fibres (MF) :

- (i) at least one melted polymeric material is extruded through spinning orifices of a die head in order to form polymeric filaments ,
- (ii) a drawing unit positioned below the die head is used for generating a gas flow that is oriented downstream, in order to draw and attenuate the filaments and in such a way to break the filaments into discontinuous fibres.

The word "fibres" as used therein and in the claims encompasses long continuous fibres (also commonly referred as "filaments") and shorter discontinuous fibres.

The word "downstream" used therein and in the claims means that the gas flow is oriented substantially in the direction of the polymer flow.

Another object of the invention is a nonwoven comprising at least one layer of non-staple fibres having a shaped cross-section and having an average length of not more than 250mm.

More particularly, the said layer also comprises fibrous material intermingled with the non-staple fibres.

The fibrous material can advantageously comprise absorbent pulp fibres.

The wording "non-staple fibres" used therein and in the claims defines discontinuous fibres that have been obtained by stretching polymeric filaments in such a way to break the filaments during their extrusion, in contrast with so-called "staple fibres" which are obtained by mechanically cutting filaments after their extrusion process notably by using cutting blades.

Staple fibres have generally the same length and are previously crimped before cutting. In contrast, the non-staple fibres have different lengths due to their random breaking during their extrusion and are generally not crimped.

The wording “shaped fibres” or “shaped cross section” used therein and in the claims means fibres having a cross section that is not circular.

Another object of the invention is the use of such a nonwoven for
5 making absorbent products, and more particularly dry or wet wipes, diapers, training pants, sanitary napkins, incontinence products, bed pads.

Brief description of the drawings

Other characteristics and advantages of the invention will appear more clearly on reading the following description of preferred
10 embodiments of the invention, which description is given by way of non-limiting example and is made with reference to the accompanying drawings, in which:

- Figure 1 is a schematic representation of an apparatus according to a first embodiment of the invention, and adapted to produce a novel
15 fibrous-containing meltblown nonwoven,
- Figure 2 is a detailed view in cross-section of an example of air-drawing unit that can be used in the apparatus of figure 1,
- Figure 3 is a view in cross-section of a bilobal meltblown fibre,
- Figure 4 is view in cross-section of a trilobal meltblown fibre,
- 20 - Figures 5A to 5C are a schematic representation of a production line adapted to produce a laminate comprising several meltblown nonwoven of the invention,
- Figure 6 is a schematic representation of an apparatus according to a second embodiment of the invention, and adapted to produce a
25 fibrous-containing nonwoven.

Detailed description

In reference to figure 1, the apparatus 1 comprises a meltblow equipment 10 for spinning polymeric meltblown fibres MF and a conveyor belt 11 for catching the meltblown fibres MF issued from the meltblow unit
30 10. This conveyor belt 11 is air permeable and is knowingly associated with a suction device 12 for sucking the meltblown fibres MF onto a

surface 11a of the conveyor belt 11. In operation, the surface 11a of the conveyor belt 11 is moved in machine direction MD, in such way that a meltblown nonwoven web MBW is formed on the surface 11a from at least the meltblown fibres MF that are randomly laid onto the surface 11a.

5 As already known in the art, the meltblow equipment 10 comprises:

- an extruder 100,
- a hopper 101 containing polymeric pellets P, said hopper 101 being connected to the extruder 100 and being adapted to supply by gravity the extruder 100 with polymeric pellets P,
- 10 - a spinning pump 102 connected to the outlet of the extruder via a duct 103,
- a meltblow die head 104 that knowingly comprises one or several parallel rows of spinning orifices that extend in the cross direction (direction perpendicular to figure 1) and air blowing means 104a, 104b for converging heated air flows F1 (hereafter called "hot primary air") towards the outlet of the die head 104 formed by the spinning orifices.

15 These components 100 to 104 of the meltblow equipment 10 are already known in the art and will not be described in details.

In operation of the meltblow equipment 10, the polymeric pellets P are melted by the extruder 100 into a molten polymeric material, which is fed by the extruder 100 to the spinning pump 102. Said spinning pump 102 feeds the die head 104 in order to extrude the molten polymeric material through the spinning orifices of the die head 104, and to form at the outlet of the die head 104 a vertical curtain of polymeric meltblown filaments f. This vertical curtain of polymeric meltblown filaments f extends in the cross direction perpendicular to the plane of figure 1.

25 The hot primary air (heated air flows F1) is drawing and attenuating the meltblown filaments f immediately at the outlet of the die head 104, while the polymer is still in the molten state. This hot primary air F1 is typically

heated at a temperature which is substantially equal or slightly higher than the melt temperature of the polymer. At the outlet of the die head, a large volume of cooling air (air flows F2), hereafter called "secondary air" is drawn into the primary air. This secondary air F2 is cooling down the polymeric filaments f downstream from the die head 104 and provides the quenching of the polymeric meltblown filaments f.

The meltblow equipment 10 newly comprises an additional air-drawing unit 105 that is positioned below the die head 104, and that is adapted to further draw and attenuate the polymeric meltblown filaments f.

10 Preferably, but not necessarily, the distance d between the outlet of the die head 104 and the inlet of the air-drawing unit 105 is adjustable.

Figure 2 shows a particular embodiment of a suitable air-drawing unit 105. The invention is however not limited to the particular structure of figure 2 and encompasses any drawing unit that can be used for continuously draw and attenuate the polymeric meltblown filaments f, in particular by means of gas flows.

In reference to the particular embodiment of figure 2, the drawing unit 105 comprises a vertical channel 1050 having an upper longitudinal slot-type inlet 1050a and a lower longitudinal slot-type outlet 1050b that both extend in the cross direction (direction perpendicular to figure 2). This channel 1050 is vertically aligned with the outlet (row of spinning orifices) of the die head 4, in such a way that the curtain of meltblown filaments f passes through the channel 1050. On each side of the channel 1050, the drawing unit 105 comprises successively four chambers 1051, 1052, 1053, 1054 that communicate through longitudinal slot-type openings 1051a, 1052a, 1053a. The last chamber 1054 is communicating with the channel 1050 through a longitudinal slot-type outlet 1054a. The first chamber 1051 is housing a longitudinal blowing duct 1055 that comprises a longitudinal slot-type outlet 1055a.

30 In operation, the blowing duct 1055a is supplied with gas under pressure at ambient temperature, and more particularly with air under

pressure at ambient temperature. This air is exhausted in chamber 1051 through the slot-type outlet 1055a, and then passes successively in the chambers 1052, 1053 and 1054. This air under pressure is exhausted in the channel 1050, through the slot-type outlet 1054a, in the form of
5 downward air flows F3 of high velocity. Each slot-type outlet 1054a is inclined in such a way that the air flows F3 are oriented downstream and substantially in the longitudinal direction of the filaments f, i.e. substantially in the same longitudinal downstream direction as the flow of polymer forming the filaments f.

10 In operation, the polymeric meltblown filaments f are passing through the channel 1050 of the drawing unit 105 and are drawn and attenuated by the air flows F3 (figure 2), that are blown at ambient temperature into the channel on each side of the curtain of meltblown filaments f, substantially in the longitudinal direction of the filaments f.
15 These air flows F3 are also cooling down the filaments F, and thus contribute also to the solidification (quenching) of the filaments f.

The high velocity air flows F3 also create by Venturi effect an air suction above the drawing unit 105. This air suction creates additional air flows F4 that are sucked into the channel 1050 through the inlet 1050a,
20 and that contribute to the cooling and solidification of the filaments f.

In the drawing unit 105, the airflows do not create turbulences that would impart a flapping movement or that would create undulations in the filaments. In the drawing unit 105, the filaments remain straight and do not have any flapping movement.

25 The velocities of the air flows F1 (died head 104) and F3 (drawing unit 105) can be advantageously selected in such a way to break the filaments f at the outlet 1050b of the drawing unit 105 and to form discontinuous meltblown fibres MF having a predetermined average length (figure 2).

30 The velocities of the air flows F1 and F3 can be advantageously adjusted separately, which improves the flexibility of the setting of the

meltblow equipment 10.

More particularly, in the invention the distance between the drawing unit 105 and the outlet of the die head 104 can be adjusted in order to break the filaments f and form discontinuous non-staple fibres of specific average length. Preferably, the distance between the drawing unit 105 and the outlet of the die head 104 can be adjusted in order to break the filaments f and form discontinuous non-staple fibres having an average length of not less than 20mm, preferably higher than 40mm, and of not more than 250mm, and preferably of not more than 150mm.

Thanks to the use of this additional drawing unit 105, the stretching of the polymer chains of the filaments f can be greater than the usual stretching practised in a standard meltblow equipment, which advantageously enables to increase the tenacity of the meltblown fibres MF, and thereby the tenacity and MD (Machine Direction) tensile strength of the meltblown nonwoven web MBW comprising such fibres.

In the invention, the air drawing unit 105 can be used and adjusted in order to produce very fine denier fibres MF having an average diameter less than $10\mu\text{m}$, and preferably less than $2\mu\text{m}$, but can also be advantageously used and adjusted in order to produce thicker discontinuous non-staple fibres MF having an average diameter of not less than $10\mu\text{m}$, and preferably between $10\mu\text{m}$ and $400\mu\text{m}$.

In another variant of the invention, the velocities of the air flows F1 (die head 104) and F3 (drawing unit 105) can also be advantageously selected in such a way that the filaments f of the drawing unit 105 are not broken at the outlet 1050b and thus form continuous meltblown fibres MF.

Thanks to the use of the air drawing unit 105, the polymer(s) used for making the filaments can advantageously have a low melt flow index, and in particular a melt flow index between 15 and 70 (ASTM D1238). It is thus possible to spin shaped fibres having a non-circular cross section, but having for example a multilobal cross section, in particular a bilobal cross section.

In the embodiment of figure 1, the apparatus 1 also comprises supplying means 13 for feeding a stream of fibrous material FM at a position between the die head 104 and the drawing unit 105, in order to continuously incorporate fibrous material FM in the curtain of polymeric meltblown filaments f that are extruded from the die head 104.

The terms "fibrous material" used therein and in the claims encompass any material comprising short length fibres and/or comprising particles.

The average length of the fibres of the fibrous material FM will generally not exceed the average length of the meltblown fibres MF. But fibres for the fibrous material, having an average length that is greater than the length of the meltblow fibres MF can be however also used.

More particularly, the fibrous material can advantageously comprise "pulp".

The term "pulp" as used therein and in the claims refers to absorbent material made of or containing fibres from natural sources such as woody and non-woody plants. Woody plants (i.e. wood-pulp) include, for example, deciduous and coniferous trees. Non-woody plants include, for example, cotton, flax, esparto grass, milkweed, straw, jute hemp, and bagasse. Typically, the average length of the pulp fibres is not more than 5mm. Longer fibres can be however also used for the fibrous material FM.

Within the scope of the invention, the fibrous material can be made solely of pulp, or can also be made of a dry mixture of pulp with other materials (fibres and/or particles). In particular the fibrous material can comprise dry mixture of pulp and particles of superabsorbent material (SAM).

The fibrous material can also comprise staple fibres (natural and/or synthetic), and for example cotton fibres.

In the particular embodiment of figure 1, the supplying means 13 comprise a vertical chimney 130 which is pneumatically fed in its upper part with the fibrous material FM. In the lower part of the chimney 130, the

supplying means 13 comprises two feeding counter-rotating rolls 131, 132, that longitudinally extend in the cross-machine direction on substantially the whole width of the chimney 130. The lower roll 132 is provided with tooth 132a on its whole periphery.

5 The supplying means 13 also comprise blowing means 134 that comprise a longitudinal slot-type outlet 134a extending in the cross-machine direction on substantial the whole width of the chimney. The blowing means 134 are adapted to blow compressed air through the said outlet 134a.

10 The supplying means 13 also comprise a feeding nozzle 133, that is positioned below the feeding roll 132. This nozzle 133 has an outlet 133a for the fibrous material MF. Said outlet 133a forms a longitudinal slot and is positioned between the die head 104 and the drawing unit 105, and nearby the curtain of meltblown filaments f. This longitudinal slot-type
15 outlet 133a extends in the cross-direction direction (direction perpendicular to the figure 1) substantially on the whole width of the curtain of meltblown filaments f, in order to feed fibrous material MF substantially on the whole width of the curtain of meltblown filaments f.

In operation, the fibrous material F is stacked in the chimney 130
20 Compressed air is continuously exhausted by the blowing means 134, through the longitudinal slot-type outlet 134a, inside the nozzle 133 (air stream F5). The rolls 131, 132 are rotated in order to continuously feed the nozzle 133 with fibrous material MF. Said fibrous material MF is entrained by the air stream F5 generated inside the nozzle 133 by the blowing
25 means 134. At the outlet 133a of the nozzle 133, the fibrous material MF is continuously delivered nearby to the curtain of meltblown filaments f.

Thanks to the use of the air-drawing unit 105, the fibrous material MF enters in contact with the meltblown filaments f and is entrained in the drawing unit 105. In addition, thanks to the air flows F4 (figure 2) created
30 by the drawing unit 105, the fibrous material FM is also sucked into the channel 1050 of the drawing unit 105, wherein the fibrous material FM is

intimately mixed with the polymer filaments f.

At the outlet 1050b of the drawing unit 105, the fibrous material FM is advantageously intimately mixed and also partially heat bonded with the meltblown fibres MF. As a result, a fibrous-containing meltblown web MBW is formed onto the surface 11a of the conveyor belt 11, wherein the intermingling and bonding of the fibrous material MF with the meltblown fibres MF are improved in comparison for example with the technical solution disclosed in US patent No 4,931, 355 and in US patent No 4,939,016 to Radwanski et al. As a result, the loss of fibrous material FM is dramatically reduced when the fibrous-containing meltblown web MBW is subsequently consolidated and/or handled.

In the invention, the use of the additional drawing unit 105 also enables to practise air flows F1 and F2 of lower velocities compared to a standard meltblow equipment having only a meltblown die head without additional drawing unit 105, like for example the meltblow equipment disclosed in US patent No 4,931, 355 and in US patent No 4,939,016 to Radwanski et al. By reducing the velocity of the air flows F1 and F2, there is advantageously less risk that the fibrous material FM is being pushed back. As a result, it is advantageously easier to incorporate higher amount of fibrous material inside the meltblown fibres MF.

In the particular embodiment of figure 1, the apparatus 1 further comprises consolidation means 14 that are positioned downstream from the meltblow equipment 10. In this particular example, these pre-consolidation means 14 are constituted by a thermal bonding unit that is known in the prior art. This thermal bonding unit 14 is a calender that comprises two pressure rolls 14a, 14b. The lower roll 14b has a smooth surface, for example a rubber surface. The upper roll 14a is a hard steel roll comprising for example an engraved surface with protruding ribs, that are regularly distributed over the whole surface of the roll, and that form a bonding pattern. The two rolls 14a, 14b are heated in order to obtain a softening of the surface of the meltblown fibres MF, and if appropriate of

the fibrous material FM when this fibrous material comprises thermoplastic fibres.

In operation, the conveyor belt 11 is used for transporting and passing the fibrous-containing meltblown nonwoven web MBW between
5 the two rolls 14a, 14b in order to pre-consolidate the fibrous-containing meltblown nonwoven web by heat and mechanical compression (thermo-bonding).

The invention is not limited however to the use of thermal bonding unit for consolidating the fibrous-containing meltblown nonwoven web
10 MBW, but any other consolidating technique already known in the art can be used, such as for example mechanical bonding, hydroentangling, ultrasonic bonding, air-through bonding, and adhesive bonding.

The hot primary air F1 can be generally obtained like in a standard meltblow process by heating the air with a heat source positioned outside
15 the die head 104. But in another variant of the invention, the heated air can be heated only by the heat generated by the die head 104, when this air passes through the die head 104.

In another variant of the invention, the apparatus of figure 1 can be modified in such a way that the polymeric material is only extruded in
20 the die head 104 in the form of filaments f without the generation of any hot primary air F1. In such a case, only the drawing unit 105 is used for drawing and attenuating the filaments f. In this case, the structure of the die head 104 can be simplified.

In another variant of the invention, the primary air F1 can be
25 generated at low speed in such a way that this primary air is not necessarily used for drawing and attenuating the filaments f at the outlet of the die head 104, but in such a way only to clean the die head 104 and avoid that broken filaments spoil the spinning orifices.

In another variant of the invention, the apparatus of figure 1 can be
30 modified in such a way that spunbonded filaments MF are being produced.

The polymer(s) P used for making the fibres MF can be any melt

spinnable polymer(s) than can be extruded through a die head. Good candidates are for example polyolefin (in particular homo or copolymer of polypropylene or polyethylene), homo or copolymer of polyester, or homo or copolymer of polyamide or any blend thereof. It can be also advantageously
5 any biodegradable thermoplastic polymer, like for example homo or copolymer of polylactic acid (PLA), or any biodegradable blend comprising a homo or copolymer of PLA. In such a case, when the fibrous material is made of biodegradable material, the nonwoven web MBW is advantageously totally biodegradable.

10 The fibres MF will be generally non elastic. But elastomeric or elastic fibres MF can be however also used.

The fibres MF can be monocomponent or multicomponent fibres, especially bicomponent fibres, and more especially sheath/core bicomponent fibres. When bicomponent fibres are produced, two extruders
15 are used for feeding simultaneously the die head 104 with each polymer.

Various shapes in cross section for the fibres MF can also be practised (round shape, oval shape, multilobal shape, in particular bilobal shape, trilobal shape, etc...). The shape in cross section of the meltblown fibres MF is determined by the geometry of the spinning orifices of the die
20 head 104.

The bonding of the fibrous material FM with the fibres is however surprisingly improved when multilobal-shaped fibres MF are used, especially when bilobal fibres like the one shown in figure 3 and also commonly referred as "papillon" fibres are used, or when trilobal fibres like the one
25 shown in figure 4 are used.

Figures 5A to 5C shows an example of a continuous production line for producing a four-layer laminate constituted by a bottom spunbonded nonwoven web S made of continuous spun filaments, a first intermediate meltblown web MBW1, a second intermediate fibrous-
30 containing meltblown web MBW2, a third intermediate fibrous-containing meltblown web MBW3, and top fibrous-containing meltblown web MBW4.

In particular, this production line 2 comprises (figure 5A) supplying means 20 for continuously providing the bottom spunbonded nonwoven web S onto a conveyor belt 21. In this particular example, these supplying means 20 comprise a storage roll 20a around which the spunbonded nonwoven S is being wound, and a motorized roll 20b associated with the storage roll 20a and adapted to continuously unwind the spunbonded nonwoven web S from the storage roll 20a and to lay down the spunbonded nonwoven web S onto the conveyor belt 21. These supplying means 20 can also be replaced by a spunbonded unit adapted to produce in line a spunbonded nonwoven web S made of continuous spun filaments that are laid down randomly directly onto the conveyor belt 21

Upstream from these supplying means 20, the production line 2 comprises successively four apparatus 22, 23 (figure 5B), 24 and 25 (Figure 5C). Apparatus 23, 24, 25 are identical to the apparatus 1 previously described in reference to figure 1. The apparatus 22 is similar to the apparatus 1 of figure 1, but does not comprise fibrous material supplying means.

The first apparatus 22 is used for continuously spinning the first meltblown web MBW1 directly onto the spunbonded nonwoven web S. The second apparatus 23 is used for continuously spinning the second intermediate fibrous-containing meltblown web MBW2 directly onto the first meltblown web MBW1. The third apparatus 24 is used for continuously spinning the third fibrous-containing meltblown web MBW3 directly onto the second intermediate fibrous-containing meltblown web MBW2. The fourth apparatus 25 is used for continuously spinning the fibrous-containing meltblown web MBW4 directly onto the third intermediate fibrous-containing meltblown web MBW3

The laminate MBW4/MBW3/MBW2/MBW1/S is then subsequently transported to a standard thermal bonding unit 26, in order to heat bond the different layers of the laminate and obtain a consolidated laminate. The consolidated laminate MBW4/MBW3/MBW2/MBW1/S is then

knowingly wounded in line around a storage roll 27a.

In a preferred embodiment, the meltblown fibres of the first and fourth meltblown nonwoven web MBW1 and MBW4 are bilobal or trilobal and the meltblown fibres of the second and third meltblown nonwoven web
5 MBW2 and MBW3 can have any shape, and in particular can be round. The invention is however not limited to such a particular laminate.

More generally, within the scope of the invention a laminate comprising at least one fibrous-containing meltblown web of the invention, laminated with one or more other layers, including notably spunbonded
10 layer, carded layer, meltblown layer, plastic film, can advantageously be produced.

The fibrous-containing meltblown web of the invention or a laminate comprising at least one fibrous-containing meltblown web of the invention can be used advantageously for making absorbent products, and
15 more particularly dry wipes, or wet wipes, or diapers, or training pants, or sanitary napkins, or incontinence products, or bed pads.

Figure 6 shows another variant of a spinning apparatus 1' of the invention that can be used for making a fibrous-containing nonwoven NW.

In this variant, the die head 104' of the spinning apparatus 1' is
20 modified in order to extrude several rows (three rows in this particular example) of polymeric filaments f, instead of one row for the apparatus of figure 1. Preferably, in this spinning apparatus 1', there is no generation in the die head 104' of any primary hot air F1, and the polymeric filaments f are only extruded through the spinning orifices of the die head 104'.

25 A cooling unit 106 is mounted below the outlet of the die head. Said cooling unit 106 comprises two blowing boxes 106a positioned on each side of the filaments f and adapted to blow several transverse forced air flows F6 towards the filaments f, in order to cool down and quench the filaments f, in a way similar to the quenching air used in a standard
30 spunbonding apparatus. This quenching air F6 is for example at a temperature between 5 °C and 20°C.

The same drawing unit 105 as the one previously described is being used at a position below the cooling unit 106 for generating the same air flows F3 oriented downstream as the ones previously described, said air flows F3 drawing and attenuating the filaments f.

5 All the previous explanations made before in connection with the drawing unit 105 of the first embodiment of figure 1, and in particular in connection with the use of this drawing unit 105 for breaking the filaments f into non-staple discontinuous fibres MF, also apply to second embodiment of figure 6, and will not be repeated.

10 In the particular embodiment of figure 6, fibrous material supplying means 13' are also provided. Said fibrous material supplying means 13' comprise also a vertical chimney 130 which is pneumatically fed in its upper part with the fibrous material FM. In the lower part of the chimney 130, the supplying means 13' comprises two feeding counter-rotating rolls
15 131, 132, that longitudinally extend in the cross-machine direction on substantially the whole width of the chimney 130. The lower roll 132 is provided with tooth 132a on its whole periphery.

The supplying means 13' also comprise a feeding channel 133' that is positioned below the feeding roll 132. This feeding channel 133' has
20 an outlet 133a for the fibrous material MF. Said outlet 133a forms a longitudinal slot and is positioned between the cooling unit 106 and the drawing unit 105, and nearby the curtains of filaments f. This longitudinal slot-type outlet 133a extends in the cross-direction direction (direction perpendicular to the figure 6) substantially on the whole width of the
25 curtain of filaments f, in order to feed fibrous material MF substantially on the whole width of the curtains of filaments f.

In contrast with the supplying means 13 of figure 1, the supplying means 13' of figure 6 do not comprise blowing means 134, but comprise a conveyor belt 135 forming the lower wall of the feeding channel 133' and
30 adapted to transport the fibrous material FM down to the outlet 133a.

In operation, the fibrous material F is stacked in the chimney 130.

The conveyor belt 135 is continuously rotated. The rolls 131,132 are rotated in order to continuously feed the conveyor belt 135 with fibrous material MF. Said fibrous material MF is entrained by the conveyor belt 135 and is continuously delivered nearby to the curtains of filaments f.

5 In the variant of figure 6, a guiding channel 106 delimited by flaps107 and air ducts 108 is extending between the outlet of the air drawing unit 105 and the conveyor belt 11. Such a guiding channel 106 has been previously disclosed in US patent application US 2008/0317895 which is incorporated therein by reference. In operation, air is sucked
10 (arrows F7) from the outside of the guiding channel 106 and enters into the guiding channel 106 through air ducts 108, in order to equilibrate the air pressure inside the guiding channel 106. The apparatus of figure 1 can also be equipped with such guiding channel 106, flaps 107 and air ducts 108.

15 In the variant of figure 6, two successive spinning apparatus 1' are provided with the same conveyor belt 11. In another variant, the spinning apparatus 1' can be used alone or in combination with any other type of apparatus adapted to laminate any kind of layer (textile layer or film) with the fibrous-containing nonwoven NW produced by the spinning apparatus
20 1'.

CLAIMS

1. An apparatus for producing meltblown fibres (MF) and comprising a die head (104) with several spinning orifices, means (100, 101, 102, 103) for extruding at least one melted polymeric material through the spinning orifices of the die head (104) in the form of meltblown filaments (f), and means (104a, 104b) for blowing a hot primary gas flow (F1) towards the outlet of the die head (104) in order to draw and attenuate the polymeric filaments (f) at the outlet of the die head, and a drawing unit (105) positioned below the die head (104), and adapted to create an additional gas flow (F3) that is oriented downstream for further drawing and attenuating the meltblown filaments (f).
2. The apparatus of claim 1, wherein the drawing unit (105) is adapted to break the meltblown filaments (f) into discontinuous meltblown fibres (MF).
3. The apparatus of claim 2, wherein the drawing unit (105) is adapted to break the meltblown filaments (f) into discontinuous meltblown fibres (MF) having an average length higher than 20mm, preferably higher than 40mm and preferably not more than 250mm.
4. The apparatus of any one of claims 1 to 3, wherein the drawing unit (105) comprises a channel (1050) that is positioned below the die head (104), in such a way that the meltblown filaments (f) delivered by the die head (104) can pass through the channel, and air blowing means (1051-1055) adapted to blow the said additional gas flow (F3) inside the channel (1050).
5. The apparatus of claim 4, wherein the drawing unit (105) is adapted to create above the drawing unit a sucked air flow (F4) that enters into the channel (1050).
6. The apparatus of any one of the previous claims, wherein the distance (d) between the outlet of the die head (104) and the inlet (1050a) of the drawing unit (105) is adjustable.

7. The apparatus of any one of the previous claims, wherein whole or part of the spinning orifices of the die head (104) are multilobal, and more particularly bilobal or trilobal.
8. The apparatus of any one of the previous claims, further comprising
5 a movable surface (11) positioned below the drawing unit (105) and adapted to form a meltblown nonwoven web (MBW) from the meltblown fibres (MF) delivered by the drawing unit (105).
9. The apparatus of any one of the previous claims, further comprising
10 supplying means (13) for continuously feeding a stream of fibrous material (FM) at a position between the die head (104) and the drawing unit (105), and nearby the meltblown filaments (f).
10. The apparatus of any one of the previous claims wherein the die head (104) is adapted to extrude vertical filaments, and the additional gas flow (F3) is oriented downwardly.
- 15 11. A process comprising the following steps :
(i) extruding through spinning orifices of a die head (104) at least one melted polymeric material in order to form polymeric meltblown filaments (f),
(ii) drawing and attenuating the meltblown filaments at the outlet of
20 the die head (104), by means of a hot primary gas flow (F1),
(iii) using a drawing unit (105) positioned below the die head (104) for generating an additional gas flow (F3) that is oriented downstream, in order to further draw and attenuate the meltblown filaments (f).
- 25 12. The process of claim 11, wherein step (iii) is performed in such a way to break the meltblown filaments (f) into discontinuous meltblown fibres (MF).
- 30 13. The process of claim 12, wherein step (iii) is performed in such a way to break the meltblown filaments (f) into discontinuous meltblown fibres having an average length higher than 20mm, and preferably higher than 40mm.

14. The process of claim 12 or 13, wherein step (iii) is performed in such a way to break the meltblown filaments (f) into discontinuous meltblown fibres having an average length of not more than 250mm, and preferably of not more than 150mm.
- 5 15. The process of any one of claims 11 to 14, wherein step (iii) is performed in such a way to break the meltblown filaments (f) into discontinuous meltblown fibres having an average diameter less than 10 μ m, and preferably less than 2 μ m.
- 10 16. The process of any one of claims 11 to 14, wherein step (iii) is performed in such a way to break the meltblown filaments (f) into discontinuous meltblown fibres having an average diameter between 10 μ m and 400 μ m.
- 15 17. The process of any one of claims 11 to 16, wherein the meltblown fibres (MF) are delivered onto a moving surface (11a) in order to form a meltblown nonwoven web (MWB).
18. The process of any one of claims 11 to 17, wherein fibrous material (MF) is continuously fed at a position between the die head (104) and the drawing unit (105), and nearby the meltblown filaments (f).
- 20 19. The process of any one of claims 11 to 18, wherein the shape in cross-section of the meltblown fibres (MF) is not circular.
20. The process of any one of claims 11 to 18, wherein the shape in cross-section of the meltblown fibres (MF) is multilobal, and preferably bilobal or trilobal.
- 25 21. The process of any one of claims 11 to 20, wherein the melt flow index of the polymer is between 15 and 70.
22. The process of any one of claims 10 to 21, wherein the filaments remain straight in the drawing unit and do not have any flapping movement.
- 30 23. An apparatus for making a fibrous-containing nonwoven, said apparatus comprising a die head (104, 104') with several spinning orifices, means for extruding at least one melted polymeric material

- through the spinning orifices of the die head in the form of filaments (f), and a drawing unit (105) positioned below the die head, and adapted to create a gas flow (F3) that is oriented downstream for drawing and attenuating the filaments (f), the apparatus further comprising supplying means (13, 13') for continuously feeding a stream of fibrous material (FM) at a position between the die head (104, 104') and the drawing unit (105), and nearby the filaments (f).
- 5
24. The apparatus of claim 23, wherein the die head does not comprise blowing mean for blowing a hot primary gas flow (F1) towards the outlet of the die head (104).
- 10
25. The apparatus of claim 23 or 24, further comprising cooling means (106) for blowing a quenching air (F6) towards the filaments (f) at a position between the die head (104') and the supplying means (13').
- 15
26. The apparatus of claim 23, further comprising means (104a,104b) for blowing a hot primary gas flow (F1) towards the outlet of the die head (104).
- 20
27. The apparatus of any one of claims 23 to 26, wherein the drawing unit (105) is adapted to break the filaments (f) into discontinuous fibres (MF).
28. The apparatus of claim 27, wherein the drawing unit (105) is adapted to break the filaments (f) into discontinuous fibres (MF) having an average length higher than 20mm, preferably higher than 40mm .
- 25
29. The apparatus of claim 27 or 28, wherein the drawing unit (105) is adapted to break the filaments (f) into discontinuous fibres (MF) having an average length of not more than 250mm, and preferably of not more than 150mm.
- 30
30. The apparatus of any one of claims 23 to 29, wherein the drawing unit (105) comprises a channel (1050) that is positioned below the die head (104, 104'), in such a way that the filaments (f) delivered

by the die head (104, 104') can pass through the channel, and air blowing means (1051-1055) adapted to blow the said additional gas flow (F3) inside the channel (1050).

- 5 31. The apparatus of claim 30, wherein the drawing unit (105) is adapted to create above the drawing unit a sucked air flow (F4) that enters into the channel (1050).
32. The apparatus of any one of claims 23 to 31, wherein the distance (d) between the outlet of the die head (104, 104') and the inlet (1050a) of the drawing unit (105) is adjustable.
- 10 33. The apparatus of any one of claims 23 to 32, wherein whole or part of the spinning orifices of the die head (104, 104') are non circular orifices.
34. The apparatus of of any one of claims 23 to 32, wherein whole or part of the spinning orifices of the die head (104, 104') are
15 multilobal, and more particularly bilobal or trilobal.
35. The apparatus of any one of claims 23 to 34, further comprising a movable surface (11) positioned below the drawing unit (105) and adapted to form a nonwoven web from the fibres delivered by the drawing unit (105).
- 20 36. The apparatus of any one of claims 23 to 35, wherein the die head (104) is adapted to extrude vertical filaments, and the additional gas flow (F3) is oriented downwardly.
37. A process for making a fibrous-containing nonwoven, wherein:
- 25 (i) at least one melted polymeric material is extruded through spinning orifices of a die head (104, 104') in order to form polymeric filaments (f),
- (ii) a drawing unit (105) positioned below the died head (104, 104') is used for generating a gas flow (F3) that is oriented downstream, in order to draw and attenuate the filaments (f).
- 30 (iii) fibrous material (MF) is continuously fed at a position between the die head (104, 104') and the drawing unit (105), and nearby

the filaments (f).

38. The process of claim 37, wherein the filaments at the outlet of the die head (104) are drawn and attenuated by means of a hot primary gas flow (F1).
- 5 39. The process of claim 37, wherein the filaments are not drawn at the outlet of the die head (104).
40. The process of claim 37 or 39, wherein the filaments are cooled down by a forced airflow (F6) below the die head (104') and prior to the feeding of the fibrous material (MF).
- 10 41. The process of any one of claims 37 to 40, wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres (MF).
42. The process of any one of claims 37 to 40, wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average length higher than 20mm, preferably higher than 40mm.
- 15 43. The process of any one of claims 37 to 42, wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average length of not more than 250mm, and preferably of not more than 150mm.
- 20 44. The process of any one of claims 37 to 43, wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average diameter less than 10 μ m, and preferably less than 2 μ m.
- 25 45. The process of any one of claims 37 to 43, wherein step (iii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average diameter between 10 μ m and 400 μ m.
- 30 46. The process of any one of claims 37 to 45, wherein the fibres (MF) are delivered onto a moving surface (11a) in order to form a nonwoven web (MWB).

47. The process of any one of claims 37 to 46, wherein the shape in cross-section of the fibres (MF) is not circular.
48. The process of any one of claims 37 to 46, wherein the shape in cross-section of the fibres (MF) is multilobal, and preferably bilobal or trilobal.
- 5 49. The process of any one of claims 37 to 48, wherein the melt flow index of the polymer is between 15 and 70.
50. The process of any one of claims 37 to 49, wherein the filaments remain straight in the drawing unit and do not have any flapping movement.
- 10 51. An apparatus for producing fibres (MF) and comprising a die head (104) with several spinning orifices, means (100, 101, 102, 103) for extruding at least one melted polymeric material through the spinning orifices of the die head (104) in the form of filaments (f), and a drawing unit (105) positioned below the die head (104), and adapted to create a gas flow (F3) that is oriented downstream for drawing and attenuating the filaments (f), and wherein the drawing unit (105) is adapted to break the filaments (f) into discontinuous fibres (MF).
- 15 52. The apparatus of claim 51, wherein the drawing unit (105) is adapted to break the filaments (f) into discontinuous fibres (MF) having an average length of not more than 250mm, and preferably of not more than 150mm.
- 20 53. The apparatus of claim 51 or 52, wherein the drawing unit (105) is adapted to break the filaments (f) into discontinuous fibres (MF) having an average length higher than 20mm, and preferably higher than 40mm.
- 25 54. The apparatus of any one of claims 51 to 53, further comprising supplying means (13) for continuously feeding a stream of fibrous material (FM) at a position between the die head (104) and the drawing unit (105), and nearby the filaments (f).
- 30

55. The apparatus of any one of claims 51 to 54, further comprising cooling means (106) for blowing a quenching air (F6) towards the filaments (f) at a position between the die head (104') and the drawing unit (105).
- 5 56. The apparatus of any one of claims 51 to 54, further comprising means (104a,104b) for blowing a hot primary gas flow (F1) towards the outlet of the die head (104).
57. The apparatus of any one of claims 51 to 56, wherein the drawing unit (105) comprises a channel (1050) that is positioned below the die head (104, 104'), in such a way that the filaments (f) delivered by the die head (104, 104') can pass through the channel, and air blowing means (1051-1055) adapted to blow the said additional gas flow (F3) inside the channel (1050).
- 10 58. The apparatus of claim 57, wherein the drawing unit (105) is adapted to create above the drawing unit a sucked air flow (F4) that enters into the channel (1050).
- 15 59. The apparatus of any one of claims 51 to 58, wherein the distance (d) between the outlet of the die head (104, 104') and the inlet (1050a) of the drawing unit (105) is adjustable.
- 20 60. The apparatus of any one of claims 51 to 59, wherein whole or part of the spinning orifices of the die head (104, 104') are non circular orifices
61. The apparatus of any one of claims 51 to 59, wherein whole or part of the spinning orifices of the die head (104, 104') are multilobal, and more particularly bilobal or trilobal.
- 25 62. The apparatus of any one of claims 51 to 61, further comprising a movable surface (11) positioned below the drawing unit (105) and adapted to form a nonwoven web from the fibres delivered by the drawing unit (105).
- 30 63. The apparatus of any one of claims 51 to 62, wherein the die head is adapted to extrude vertical filaments, and the additional gas flow

(F3) is oriented downwardly.

64. A process for producing fibres (MF) wherein :

(i) at least one melted polymeric material is extruded through spinning orifices of a die head (104, 104') in order to form polymeric filaments (f),

(ii) a drawing unit (105) positioned below the die head (104, 104') is used for generating a gas flow (F3) that is oriented downstream, in order to draw and attenuate the filaments (f), and in such a way to break the filaments (f) into discontinuous fibres (MF).

65. The process of claims 64, wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average length of not more than 250mm, and preferably of not more than 150mm.

66. The process of any claim 64 or 65 wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average length higher than 20mm, preferably higher than 40mm.

67. The process of any one of claims 64 to 66, wherein step (ii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average diameter less than 10 μ m, and preferably less than 2 μ m.

68. The process of any one of claims 64 to 66, wherein step (iii) is performed in such a way to break the filaments (f) into discontinuous fibres having an average diameter between 10 μ m and 400 μ m.

69. The process of any one of claims 64 to 68, wherein the filaments at the outlet of the die head (104) are drawn and attenuated by means of a hot primary gas flow (F1).

70. The process of any one of claims 64 to 68, wherein the filaments are cooled down by a forced airflow (F6) below the die head (104').

71. The process of any one of claims 64 to 70, wherein fibrous material (MF) is continuously fed at a position between the die head (104, 104') and the drawing unit (105), and nearby the filaments (f).
72. The process of any one of claims 64 to 71, wherein the fibres (MF) are delivered onto a moving surface (11a) in order to form a nonwoven web (MWB).
73. The process of any one of claims 64 to 72, wherein the shape in cross-section of the fibres (MF) is not circular.
74. The process of any one of claims 64 to 73, wherein the shape in cross-section of the fibres (MF) is multilobal, and preferably bilobal or trilobal.
75. The process of any one of claims 64 to 74, wherein the melt flow index of the polymer is between 15 and 70.
76. The process of any one of claims 64 to 75, wherein the filaments remain straight in the drawing unit and do not have any flapping movement.
77. A nonwoven comprising at least one layer (MBW) of non-staple fibres (MF) having a shaped cross-section and having an average length of not more than 250mm, and preferably of not more than 150mm.
78. The nonwoven of claim 77 wherein the shape in cross section of the non-staple fibres is multilobal.
79. The nonwoven of claim 77 wherein the shape in cross section of the non-staple fibres is bilobal
80. The nonwoven of any one of claims 77 to 78 wherein the average length of the non-staple fibres (MF) is higher than 20mm, and preferably higher than 40mm.
81. The nonwoven of any one of claims 77 to 80 wherein the average diameter of the non-staple fibres is less than 10 μ m, and preferably less than 2 μ m.
82. The nonwoven of any one of claims 77 to 81 wherein the average

diameter of the non-staple fibres is between 10µm and 400µm.

83. The nonwoven of any one of claims 77 to 82, wherein the non-staple fibres (MF) are not crimped.

5 84. The nonwoven of any one of claims 77 to 83, wherein said nonstaple fibres (MF) are meltblown fibres.

85. The nonwoven of any one of claims 77 to 83, wherein the said at least one layer (MBW) of non-staple fibres also comprises fibrous material (FM) intermingled with the non-staple fibres (MF).

10 86. Use of a nonwoven of any one of claims 77 to 85 or of a nonwoven issued from the process of any one of claims 11 to 22, or issued from the process of any one of claim 37 to 50 or issued from the process of any one of claims 64 to 76, for making absorbent products, and more particularly dry or wet wipes, diapers, training pants, sanitary napkins, incontinence products, bed pads.

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