## PATENT SPECIFICATION

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## (54) PREPARATION OF TETRAALKYLTHIURAM DISULFIDES

(71) We, OUCHI SHINKO KAGAKU KOGYO KABUSHIKI KAISHA, a company organized and existing under the laws of Japan, of 3—7, Nihonbashi-kobuna-cho 1-chome, Chuo-ku, Tokyo-to, Japan, do hereby declare the invention, for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following statement:—

This invention relates to a novel process for preparation of tetraalkylthiuram disulfides. More particularly, it relates to the process for preparing the disulfides in which an aqueous solution containing an alkali metal dialkyldithiocarbamate is subjected to electrolytic oxidation in the presence or absence of a supporting electrolyte, which aqueous layer is placed over a layer consisting essentially of carbon disulfide or a mixed solvent of carbon disulfide as a predominant component and a halogenated alkane having a higher density than water, to obtain directly the corresponding tetraalkylthiuram disulfide.

A typical industrial process for the production of tetraalkylthiuram disulfides to be used as vulcanizing accelerators or agents is as follows. An aqueous solution of a sodium dialkyldithiocarbamate is prepared by reacting the corresponding dialkylamine and carbon disulfide at a low temperature in the presence of an aqueous sodium hydroxide solution. The resulting aqueous solution is purified, and then sulfuric acid and hydrogen peroxide used as an oxidizing agent are added dropwise thereto to effect neutralization and oxidation of the dialkyldithiocarbamic acid. The resulting precipitate of the end product is subjected to filtration, washing with water, dehydration, drying and grinding if so desired.

In the oxidative dimerization of sodium dialkyldithiocarbamates, oxidizing agents such as nitrogen dioxide (NO<sub>2</sub>), chlorine (Cl<sub>2</sub>), iodine (I<sub>2</sub>), ozone (O<sub>3</sub>), oxygen (O<sub>2</sub>), sodium nitrite (NaNO<sub>2</sub>), sodium hypochlorite (NaOCl), sulfur monochloride (S<sub>2</sub>Cl<sub>2</sub>), sulfur dichloride (SCl<sub>2</sub>), potassium perbromate (KBrO<sub>3</sub>), selenic acid (H<sub>2</sub>SeO<sub>3</sub>) and ammonium persulfate [(NH<sub>4</sub>)<sub>2</sub>S<sub>2</sub>O<sub>8</sub>] can be employed instead of hydrogen peroxide. It should be noted that, in those oxidative processes in which oxidizing agents are used, the stoichiometric quantities of oxidizing agents, neutralizing agents and the like are required, and special handling care must be taken as to the reaction apparatus and accessory apparatus as well as the process controls of the reaction.

On the other hand, a process for preparing tetraalkylthiuram disulfides via direct electrolytic oxidation of the corresponding alkali metal dialkyldithiocarbamates, in which use of the oxidizing agents and the like is avoided, is disclosed in U.S. Patent No. 2,385,410. In this electrolytic oxidation process, the electrolytic reaction is carried out at a comparaively high temperature of 50 to 60°C. It is well known that tetraalkylthiuram disulfides are generally inferior in thermal stability. The resulting disulfide can be partially decomposed thermally at a reaction temperature of 50 to 60°C, and the yield and quality of the product are thus lowered.

An object of the present invention is to provide a novel process for preparing tetralkylthiuram disulfides via electrolytic oxidation in a high yield.

Another object of the present invention is to provide a process for preparing the disulfides without forming by-products and discharging pollutants outsides.

Still another object of the present invention is to provide an efficient process for continuously preparing the sulfides via electrolytic oxidation.

Other objects of the present invention will be made clear in the following description.

According to this invention, briefly summarized, there is provided a process for preparing a tetraalkylthiuram disulfide, which comprises subjecting an alkali metal dialkyldithiocarbamate represented by the formula:

wherein R represents an alkyl group having 1 to 4 carbon atoms, and M is an alkali metal selected from sodium, potassium and lithium, to electrolytic oxidation, whereby the carbamate is dimerized to form the corresponding tetraalkylthiuram disulfide, said electrolytic oxidation being conducted in the absence or presence of a supporting electrolyte in a two-layer electrolytic solution consisting essentially of an aqueous phase comprising water and a non-aqueous phase comprising carbon disulfide with electrodes in contact with the aqueous phase that contains the alkali metal dialkyldithiocarbamate dissolved therein, and allowing the resulting tetraalkylthiuram disulfide to be extracted by the non-aqueous phase.

The process according to the invention comprises subjecting an aqueous solution containing an alkali metal dialkyldithiocarbamate wherein the alkali metal is sodium, potassium or lithium to electrolytic oxidation to form the corresponding tetraalkylthiuram disulfide as shown in the reaction formula:

wherein R represents an alkyl group having 1 to 4 carbon atoms, and M represents an alkali metal, said electrolytic oxidation being conducted generally at approximately room temperature in the absence or presence of a supporting electrolyte by inserting electrodes in an aqueous layer of a two-layer electrolytic solution consisting essentially of either (1) water as an aqueous upper layer or phase and carbon disulfide as a non-aqueous lower layer or phase or (2) water as an aqueous upper layer or phase and a mixture containing carbon disulfide as a predominant component and a halogenated alkane as a non-aqueous lower layer or phase and passing electric current at a suitable terminal voltage for producing the sulfide for a time necessary to complete the reaction; allowing the resulting tetraalkylthiuram disulfide to be extracted into the lower layer comprising carbon disulfide; taking out the extractant layer; and removing the solvent(s) of the layer.

Solvent

The solvents suitable for use in the present invention can be conveniently classified into two groups.

The first group is water which is used as an actual electrolytic solvent.

The second group includes a hydrophobic solvent which is carbon disulfide, or a mixture containing carbon disulfide as a predominant component of the mixture and an appropriate quantity of a halogenated alkane having a higher density than water such as a  $C_{1-3}$  chloroalkane, preferably a  $C_{1-2}$  chloroalkane, e.g., dichloromethane, chloroform, dichloroethane or trichloroethane, or a lower alkyl  $(C_1-C_3)$  trichloroacetate, e.g. methyl or ethyl trichloroacetate. The mixture is hereinafter referred to as a "mixed solvent". These halogenated alkanes can be used in admixture with carbon disulfide in a desired proportion to improve the extracting effect of carbon disulfide on the reaction product, preferably in a quantity from 0.1 to 20 times by volume that of the carbon disulfide. The halogenated alkanes should preferably be those in which tetraalkylthiuram disulfides are soluble and which are miscible with carbon disulfide to form homogeneous mixtures.

to 30°C.

Supporting electrolyte A supporting electrolyte is not especially required in the present invention since an alkali metal salt of dialkyldithiocarbamic acid is employed as the starting material. An appropriate supporting electrolyte, however, can be used if so desired. 5 Representative examples of supporting electrolytes include perchlorates such as 5 lithium perchlorate, magnesium perchlorate, and quaternary alkylammonium perchlorates; perborates such as quaternary alkylammonium tetrafluoroborates, alkylammonium halides, alkali metal halides, quaternary alkylammonium nitrates; and quaternary alkylammonium para-toluenesulfonates, 10 wherein the alkyl group is methyl, ethyl, a propyl or a butyl, the alkali metal is 10 lithium, potassium or sodium, and the halogen is chlorine, bromine or iodine. As to the roles and embodiments of supporting electrolytes, reference is made to C. K. Mann: Electroanal. Chem. 16 157 (1969), cited herein by reference. Electrodes 15 The electrodes to be employed in the present invention include commercial 15 electrodes for electrolytic use produced from platinum or carbon, electrodes which have been fabricated into an electrode form from carbon, titanium oxide or other electroconductive metal oxide materials, and those electrodes whose surfaces have been subjected to special processes. 20 It should be noted that the mixed solvents, supporting electrolyte, and 20 electrodes to be employed in the present invention are not restricted to the examples illustrated above. Reaction and recovery The electrolytic oxidation reaction according to the present invention is 25 conducted by using a two-layer electrolytic solution which consists essentially of an 25 upper layer comprising an aqueous solution of an alkali metal dialkyldithiocarbamate and a lower layer comprising carbon disulfide, preferably with an aqueous layer to which an appropriate supporting electrolyte is added if desird in an amount of 0.01 to 0.5 mol/lifer. 30 Electrolysis may be carried out under stirring by means of electrodes such as 30 platinum or carbon electrodes inserted into the aqueous layer. Tetralkylthiuram disulfide can be continuously produced when carbon disulfide and a dialkylamine corresponding to the alkali metal dialkyldithiocarbamate consumed in the reaction are supplementally added and the electrolysis is continued. The reaction product is 35 extracted by the lower layer comprising carbon disulfide. When the resulting 35 product has reached a suitable concentration, the lower layer is taken out and the solvent is removed to obtain the end product, a tetraalkylthiuram disulfide. The reaction conditions of the electrolytic oxidation differ depending on the type of the electrolytic cell and the kind of amine to be used. The electrolytic 40 reaction in the two-layer solution according to the present invention can be 40 conducted under the conditions of electric current density and potential which are generally employed in the art. A feature of the present invention is that, by merely carrying out electrolysis by maintaining a constant terminal voltage of 1.0 to 10 V. preferably 1.5 to 3.0 V, only the desired product can be efficiently obtained. 45 Electrolytic oxidation at a constant terminal voltage can ensure the use of a simple 45 electrolytic apparatus and operation. The preferred current density is in the range of from 100 to 0.1 mA/cm<sup>2</sup>. In general, when electrolysis is conducted at a constant terminal voltage, some fluctuation occurs in the electrode potential. If a voltage which is somewhat higher 50 than the preferred voltage is employed in the electrolytic reaction, undesirable by-products may also be formed. The formation of such by-products is increased 50 under these electrolysis conditions especially when carbon electrodes which are highly adsorptive are employed. In the present invention, however, electrolysis is carried out in the two-liquid system consisting essentially of an upper aqueous layer 55 and a lower extractant, and the resulting product moves rapidly to the extractant 55 layer. The side reaction which is due to some fluctuation of electrode potential can be avoided by the cleaning effect of the electrode surfaces owing to occasional contact of the extractant solvent with the electrode surfaces. Therefore, a broad range of terminal voltages can be employed in accordance with the present 60 60 The reaction temperature may be in the range of from 5 to 40°C, preferably 10

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	The lower or hydrophobic solvent layer containing the resulting electrolytic product may be subjected to washing with water and dehydration, if desired, and then stripping of the extractant solvent and low-boiling volatile components to recover a tetraalkylthiuram disulfide in a yield of 98 to 100%.	
5	The production process according to the present invention can be carried out by either a continuous system of a batch system. The hydrophobic solvent and excess dialkylamine or excess carbon disulfide can be recovered as distillates when the solvents are stripped. The aqueous layer containing an alkali metal dialkyldithiocarbamate and a supporting electrolyte can be supplied to the	5
10	electrolytic reaction without modification. In the continuous reaction system, the advantage of a very long-run operation can be exhibited since dialkylamine and carbon disulfide in predetermined proportions are added to the reaction system when necessary, and the resulting product can be continuously separated from the	10
15	hydrophobic solvent layer.  Also, according to the process of the present invention, an alkali metal hydroxide produced in the course of the reaction reacts with the supplemented dialkylamine and carbon disulfide and is consumed to form the corresponding alkali metal dialkyldithiocarbamate. Therefore, the alkali metal hydroxide can be automatically recycled and used, and the pH in the reaction system is maintained	15
20	approximately at a constant level.  The present process can be carried out without a neutralizing agent and at a	20
25	temperature near room temperature. Furthermore, a supporting electrolyte can be used without replenishment since the electrolyte remains in the reaction system as it is, Moreover, little or no side-reaction takes place. Thus, tetraalkylthiuram	
25	disulfides can be obtained in a very good yield as high as 98 to 100% according to the present invention.  According to the process of the present invention, the aqueous layer in which the electrolytic reaction takes place is recycled and is not discharged outside.	25
30	Furthermore, the extractant solvent containing the end product is recovered by simply stripping it and can be recycled to the electrolytic reaction system. Thus, the present invention has been proved to be suitable for producing tetraalkylthiuram disulfides on an industrial scale, since the environmental pollution problems due to waste water containing the conventional by-products are eliminated by the present invention.	30
35	The invention will be understood more fully by reference to the following Examples, which are intended to illustrate the present invention and are not to be construed as limiting the scope of the invention.	35
	Example 1	
40	Preparation of tetramethylthiuram disulfide in a water-carbon disulfide- dichloromethane solvent system.  In a 50-ml branched test tube are placed 500 mg (3.5 millimols) of sodium	40
	dimethyldithiocarbamate, followed by the addition thereto of 20 ml of water to prepare a homogeneous aqueous solution. The solution is further supplied with 5	
45	ml of methylene chloride and 1 ml of carbon disulfide. The test tube is then equipped with a stirrer and a thermometer as well as platinum electrodes (1.5 cm×2 cm in dimension) which are inserted into the aqueous layer. Electrolysis is carried out with stirring under the conditions of a terminal voltage of 2 V and a current	45
50	density of 10 to 5 mA/cm <sup>2</sup> , while the reaction temperature is maintained at 15 to 20°C. The electrolysis is continued by adding 0.04 ml (0.3 millimol) of 50% aqueous dimethylamine solution and 23 mg (0.3 millimol) of carbon disulfide for every quantity of electricity of 0.3×10 <sup>-3</sup> F passed through the reaction system. Electrolysis	50
	is discontinued when a total quantity of electricity of $5 \times 10^{-3}$ F has been passed. The lower layer of the reaction system is taken out and subjected to washing with water, dehydration and concentration. In one actual instance of practice, 595 mg of the	
55	tetramethylthiuram disulfide (yield 99%) were obtained as white powdery crystals having a melting point of 146.0°C. The resulting product was confirmed to be tetramethylthiuram disulfide as a result of identification by thin-layer chromatography and infrared (IR) and nuclear magnetic resonance (NMR)	55
60	absorption spectra as well as a mixed melting point test with a standard sample thereof.	60

## Example 2 Preparation of tetraethylthiuram disuldide in a water-carbon disulfide solvent system

The experiment was carried out similarly to Example 1. The reaction system was prepared by dissolving 500 mg (2.92 millimols) of potassium diethyldithiocarbamate and 100 mg of sodium perchlorate used as a supporting electrolyte in 20 ml of water, followed by the addition thereto of 5 ml of carbon disulfide. Electrolytic reaction was carried out by using carbon electrodes (3 cm×2 cm in dimension) at a reaction temperature of 12 to 14°C with stirring under the conditions of a terminal voltage of 2 V and a current density of 10 to 5 mA/cm², during which diethylamine [67 mg (0.5 millimol)×10 times] was intermittently added and a quantity of electricity of 5×10<sup>-3</sup>F was passed. The lower layer of carbon disulfide solution was taken out and subjected to washing with water, dehydration and concentration.

Thus, 733 mg (yield 99%) of the tetraethylthiuram disulfide were obtained as slightly grayish-white powdery crystals having a melting point of 70.5°C. The resulting product was confirmed to be tetraethylthiuram disulfide as a result of identification by thin-layer chromatography and IR and NMR absorption spectra as well as a mixed melting point test with a standard sample thereof.

Example 3
Preparation of tetrabutylthiuram disulfide in a water-carbon disulfide system

The experiment was carried out by using platinum electrodes (2 cm×3 cm) similarly to Example 1. A homogeneous solution was prepared by adding 20 ml of water to 995 mg of lithium dibutyldithiocarbamate (5 millimols), followed by the addition of 5 ml of carbon disulfide. Electrolytic reaction was carried out with stirring at a reaction temperature of 18 to 20°C under the conditions of a terminal voltage of 2 V and a current density of 10×5 mA/cm². Every time a quantity of electricity of 0.5×10<sup>-3</sup>F was passed, the lower layer of the reaction system was taken out, and 65 mg (0.5 millimol) of dibutylamine and 3 ml of carbon disulfide were added to the aqueous solution of the upper layer, while the electrolysis was continued. The lower layer thus taken out was subjected to washing with water, dehydration and concentration to yield 102 to 99 mg (100 to 97% yield) each time of the tetrabutylthiuram disulfide as a dark-brown viscous liquid having a solidifying point of 20°C. The operations were repeated 15 times to yield a total of 1.51 g (98% yield) of tetrabutylthiuram disulfide. The resulting product was confirmed to be tetrabutylthiuram disulfide as a result of identification by thin-layer chromatography and IR and NMR absorption spectra as well as elemental analysis (as C<sub>18</sub>H<sub>28</sub>N<sub>2</sub>S<sub>4</sub>, Calculated: C 52.88%; H 8.89%; N 6.85, Found: C 52.83%: N 8.90%; N 6.77%).

As clearly shown also in these examples, the process according to the present invention is a process for preparing tetraalkylthiuram disulfides in a high yield with simple reaction steps and without side reaction and has the features that: an alkali metal salt of dialkyldithiocarbamic acid is subjected to electrolytic oxidation in an electrolytic solution which is a two-liquid system comprising water and carbon disulfide, so as directly to produce tetraalkylthiuram disulfides; the by-product alkali metal hydroxide formed in the electrolytic reaction reacts with the corresponding dialkylamine and the carbon disulfide which are added to the reaction system to produce the alkali metal salt of dialkyldithiocarbamic acid; and the alkali metal dialkyldithiocarbamate is thus supplied and the electrolytic reaction is continuously carried out.

## WHAT WE CLAIM IS:—

1. A process for preparing a tetraalkylthiuram disulfide, which comprises subjecting an alkali metal dialkyldithiocarbamate represented by the formula:

wherein R represents an alkyl group having 1 to 4 carbon atoms, and M is an alkali metal selected from sodium, potassium and lithium, to electrolytic oxidation,

	whereby the carbamate is dimerized to form the corresponding tetraalkylthiuram disulfide, said electrolytic oxidation being conducted in the absence or presence of a supporting electrolyte in a two-layer electrolytic solution consisting essentially of	
5	an aqueous phase comprising water and a non-aqueous phase comprising carbon disulfide with electrodes in contact with the aqueous phase that contains the alkali metal dialkyldithiocarbamate dissolved therein, and allowing the resulting tetraalkylthiuram disulfide to be extracted by the non-aqueous phase.  2. A process as set forth in claim 1, in which the non-aqueous phase consists	5
10	essentially of carbon disulfide.  3. A process as claimed in claim 1, in which the non-aqueous phase comprises a mixture of carbon disulfide as a predominant component of the mixture and a halogenated alkane having a higher density than water.	10
15	4. A process as set forth in any of claims 1 to 3, in which carbon disulfide and a dialkylamine corresponding to the alkali metal dialkyldithiocarbamate are gradually added to the aqueous layer, and an alkali metal hydroxide produced in the course of the electrolytic reaction reacts with the dialkylamine and carbon disulfide to form the corresponding alkali metal dialkyldithiocarbamate, whereby	15
20	the resulting carbamate is successively supplied to the reaction system and the tetraalkylthiuram disulfide is continuously produced.  5. A process as set forth in any of claims 1 to 4, in which the electrodes are produced from the materials selected from platinum, carbon, titanium oxide and other electroconductive metal oxide materials.	20
25	6. A process as set forth in any of claims 1 to 5, in which the electrolytic oxidation reaction is carried out at a terminal voltage of 1.0 to 10 V.  7. A process as set forth in any of claims 1 to 6, in which the electrolytic oxidation reaction is carried out at a temperature of from 5 to 40°C.  8. A process as set forth in any of claims 1 to 7, in which the reaction	25
30	temperature is approximately room temperature.  9. A process as set forth in any of claims 1 to 8, in which the halogenated alkane is employed in a quantity of from 0.1 to 20 times by volume that of the carbon disulfide.  10. A process as set forth in any of claims 1 to 9, in which the supporting	30
35	electrolyte is selected from lithium perchlorate, magnesium perchlorate, quaternary alkylammonium perchlorates, quaternary alkylammonium tetrafluoroborates, quaternary alkylammonium halides, alkali metal halides, quaternary alkylammonium nitrates and quaternary alkylammonium paratoluenesulfonates, wherein the alkyl group is methyl, ethyl, propyl or butyl, the alkali metal is lithium potassium or sodium, and the halogen is chlorine, bromine or	35
40	iodine.  11. A process according to claim 1, substantially as herein described with reference to any of the specific examples.  12. Tetraalkylthiuram disulfides when prepared by a process as claimed in any	40

12. Tetraalkylthiuram disulfides when prepared by a process as claimed in any of claims 1 to 11.

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